A Large Deformation Multiphase Continuum Mechanics Model for Shock Loading of Lung Parenchyma: Investigating the Effects of Fluid Viscous Stress

by Zachariah T Irwin, Richard A Regueiro, and John D Clayton

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A Large Deformation Multiphase Continuum Mechanics Model for Shock Loading of Lung Parenchyma: Investigating the Effects of Fluid Viscous Stress

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A finite-strain theory of a biphasic mixture, with coupled pore fluid flow and solid skeleton deformation, of a soft porous material has been developed for high-strain-rate dynamic loading. The constitutive model is nonlinear elastic and accounts for the compressibility of the pore air. The formulation does not require equivalency of acceleration of pore fluid to that of solid skeleton, but rather allows them to be different. Through implementation of the concept of solid extra stress, the theory is able to distinguish among solid skeleton, pore fluid (air), and total pressures, and similarly among stress tensors for each constituent. Herein, we depart from prior work, which assumed a nearly inviscid pore fluid, and account for the pore fluid's viscous effects on its stress.
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1. Introduction

1.1 Background

The lung parenchyma is a highly heterogeneous material composed of alveolar air sacs ranging from 100–330 µm in diameter\(^1\) and connective tissues consisting of a complex network of collagen and elastin fibers.\(^2\) At high rates of strain, such as those induced by a shock wave, the fibers in lung parenchyma are prone to rupture\(^3\) and the remaining stress response percolates through the collagen fibril networks as the collagen fibers start to extend to their uncoiled lengths. This increases the stress response of the entire lung parenchyma.\(^4\) The complex roles that collagen and elastin fibers play in the dynamics of the lung parenchyma are discussed by Freed et al.\(^3\) Dynamic influences of the bronchiole tubes, which are stiffer than the parenchyma, on the response of impacted lung are observed in experiments by Brannen et al.\(^5\) The present focus is on the role that 1-D poro-elasto-dynamics plays at the mesoscopic level. Outcomes of the current research are intended to inform macroscopic, single-phase models of the lung for 3-D modeling of much larger domains.\(^6\)–\(^11\)

Mixture theory was first established at finite strain by Truesdell and Toupin.\(^12\) Subsequent works by Bowen\(^13\)–\(^15\) and others\(^16\)–\(^18\) applied this rich continuum theory to porous media. Shock waves in mixtures were studied using analytical methods by Bowen, Chen, and Wright,\(^19\)–\(^22\) and more recently by Clayton.\(^23\) The Theory of Porous Media (TPM) is an approximation to a more computationally expensive Fluid-Structure Interaction (FSI) model at the pore length scale. In TPM, interactions are smeared across a continuum material point, simplifying not just the governing mathematical equations but the discretization of the geometry itself.

Lung parenchyma is a complex heterogeneous material.\(^24\) Resolution would require representation by a detailed 3-D finite-element (FE) mesh to model the \textit{explicit} FSI. Resolution could be possible via Computational Fluid Dynamics-Computational Solid Mechanics with arbitrary Lagrangian-Eulerian modeling. However, such frameworks would involve costly simulations and mesh generation and bias regarding the structure of the FE mesh.

Shock waves induce large pressure gradients that are thought to directly cause microstructural tearing of the lung parenchyma leading to hemorrhaging.\(^24\)–\(^26\) Injury
propagations through the lung parenchyma at the ultrastructural (tissue fibers) and microstructural (air sac) levels are not well understood and constitute active research.\textsuperscript{3,8} The fine-scale approach initiated by Freed et al.\textsuperscript{3} to model the microstructure necessitates a multiscale model of the whole lung tissue, which includes the highly heterogeneous structure of the lung parenchyma. Work is needed to first accurately simulate the deformation of lung parenchyma using a multiphysics approach, before addressing damage and injury pathology at the microscale (i.e., alveolar regime) and linking that to the macroscale (i.e., parenchymal regime). In the current program,\textsuperscript{27,28} we incorporate TPM to take into account the different response times of the two constituents in the lung parenchyma subjected to shock loading: solid skeleton (s) (lung parenchyma) and the pore fluid (f) (air) that occupies the pore space.

In prior work,\textsuperscript{27,29} we assumed a nearly inviscid stress response of the pore fluid; viscous effects were accounted for via the “hydraulic conductivity” parameter that governs the magnitude of the seepage flow (the difference in velocity between the pore fluid and the solid skeleton). However, total pore fluid Cauchy stress, assuming a locally homogeneous temperature model between the two constituents (i.e., the temperature of the pore fluid is assumed to be equal to that of the solid skeleton at a finite point, even if the temperature of the fluid-solid mixture is allowed to fluctuate), is written as

\[
\sigma_f := \sigma_E^f - n_f p_f \mathbf{1},
\]

where \(n_f p_f = p_f\) is the partial pressure contribution, and \(\sigma_E^f\) is the viscous contribution (hereafter referred to as the pore fluid “extra” stress), which is ignored in the nearly inviscid assumption. Such an assumption may be invalid at high-strain-rates where momentum diffusivity of the pore fluid (air) in lung parenchyma may alter the dynamic response of lung tissue subjected to shock loading. The objective of the present work is to verify whether or not the nearly inviscid pore fluid assumption is valid for our 1-D FE model in various strain-rate regimes. This objective is achieved by comparing numerical simulations between our numerical FE model where the pore fluid extra stress is assumed to be equal to zero to simulations with a modified FE model where it is not.
1.2 Organization

The remainder of this report is organized in the following manner. Section 2 summarizes a brief history of the validity of including the pore fluid extra stress in the framework of TPM. Discussion continues with the associated difficulties with modeling this term in a FE framework, and concludes with the modeling approach employed in the current work. Section 3 presents the modified variational forms of the balance equations from those reported in Irwin et al., wherein we apply the standard Bubnov-Galerkin spatial-discretization procedure for the FE model to solve for the variables of interest: lung parenchyma displacement (and velocity and acceleration), pore fluid pressure and pore fluid displacement (and velocity and acceleration). A review of the numerical time integration schemes from Irwin et al. then follows, with modifications for the pore fluid extra stress presented as needed. Section 4 presents a comparison of the Darcy (i.e., nearly inviscid pore fluid flow) and Darcy-Brinkman (i.e., viscous pore fluid flow) numerical simulation results.

2. Theory

2.1 The Fluid Extra Stress Tensor: Background and Challenges

An extensive background of TPM is provided by Bowen, Coussy, Ehlers and de Boer, and originally in Truesdell and Toupin. For truncated derivations disclosed in the aforementioned works, refer to Irwin et al. We continue to follow the notation of Holzapfel (for solid mechanics) and de Boer.

We assume that the porous solid continuum body constitutes a control space \( B \) (current configuration of the solid skeleton) and that only liquids or gases in the pores can leave this control space. Rather than modeling the exact microstructure of the porous solid, we assume that the pores are modeled in a statistical sense such that their specific locations are arbitrary. This concept of volume fraction is illustrated in Fig. 1a. The volume fractions \( n^\alpha \) are defined such that they relate the “real” differential volumes \( dv_\alpha \) of each constituent, or phase, \( \alpha \) to the smeared (i.e., homogenized) total differential volume \( dv \):

\[
n^\alpha(\mathbf{x}, t) = \frac{dv_\alpha(\mathbf{x}, t)}{dv(\mathbf{x}, t)},
\]

where \( \mathbf{x} \) is the position vector in the current configuration \( B \) (see Fig. 1(b)), and \( t \) is current time. Thus, for any mixture, the constituents \( \alpha \) occupying some control
volume $dv$ in the control space $B$ must satisfy

$$
\sum_{\alpha} n^\alpha(x, t) = 1, \quad \sum_{\alpha} dv^\alpha(x, t) = dv(x, t).
$$

(3)

---

Fig. 1 Concept of volume fraction for biphasic (solid(s)-fluid(f)) mixture theory (a), showing solid skeleton composed of alveolar tissue. Note that in the theory of porous media, it is assumed that the control space is that of the solid phase $B = B^s$, also known as “solid skeleton.” Kinematics (b) of a biphasic (solid-fluid) mixture theory.

We furthermore assume that the constituents are immiscible (following the principle of phase separation\cite{16}) such that we can relate the partial mass density $\rho^\alpha$, that is, the mass density of constituent $\alpha$ occupying the total differential volume $dv$ containing multiple constituents, to the real mass density $\rho^{\alpha R}$, the mass density of constituent $\alpha$ occupying the differential volume $dv_\alpha$ containing only constituent $\alpha$, as follows:

$$
m^\alpha(x, t) = \int_{B^\alpha} \rho^{\alpha R}(x, t) dv^\alpha(x, t)
= \int_B \rho^{\alpha R}(x, t) n^\alpha(x, t) dv(x, t) = \int_B \rho^\alpha(x, t) dv(x, t),
$$

(4)

where $m^\alpha$ is the mass of constituent $\alpha$ in the control space $B$. Hereafter we assume that variables written in the current configuration $B$ are dependent on position $x$ at time $t$ so as to simplify the notation. Similarly, variables written in the reference
configuration $B_0$ are dependent on position $X$ at time $t$.

For a materially incompressible solid (s) phase and compressible fluid (f) phase, the balance of mass of the mixture expressed in the reference configuration $B_0$ is written as:

$$
\frac{J_sn^f}{K_f^0}D_t p_f + D_t s + J_s \frac{1}{K_s^0} \nabla_s (p_f) \cdot F_s^{-1} \cdot (n^f \tilde{v}_f) + J_s \nabla_s (n^f \tilde{v}_f) : F_s^{-T} = \frac{J_s \hat{\rho}^f}{\rho^R},
$$

where $J_s$ denotes the Jacobian of deformation $F_s$ of the solid (s) phase, $K_f^0$ is the isentropic bulk modulus of the fluid (f) phase, $p_f$ is the pore fluid pressure, $\tilde{v}_f$ is the difference in velocities of the fluid (f) and solid (s) phase, that is, $\tilde{v}_f := \nabla - v_s$, and $\hat{\rho}^f$ is the mass supply to the fluid phase from the other phase(s), which we typically assume to be negligible. In present work, the $(n^f \tilde{v}_f)$ term is modeled using an appropriate constitutive law, for example, Darcy’s law:

$$
n^f \tilde{v}_f = -\hat{k} \left( \nabla p_f + \rho^R (\nabla - g) \right).
$$

However, when the pore fluid extra stress $\sigma^f_E$ is to be accounted for, we use the extension of Eq. 6, the Darcy-Brinkman equation:

$$
n^f \tilde{v}_f = -\hat{k} \left( \nabla p_f + \rho^R (\nabla - g) - \frac{1}{n^f} \\text{div} \sigma^f_E \right).
$$

Furthermore, it can be shown that the balance of momenta of the mixture and the fluid phase under the assumptions laid out in Irwin et al.\cite{27} (namely: locally homogeneous temperatures, negligible mass supplies of solid and fluid phases, materially incompressible solid phase and compressible fluid phase and gravity as the only active body force), may be written as follows:

$$
\text{DIV}_s P_s + \rho_{0(s)} g = \rho_{0(s)}^s a_s + \rho_{0(s)}^f \alpha_f, \quad P_s = P_{E(s)}^s + P_{E(s)}^f - J_s p_f F_s^{-T},
$$

$$
\rho_{0(s)}^f \alpha_f + J_s n^f \nabla s p_f \cdot F_s^{-1} - \text{DIV}_s P_{E(s)}^f + J_s \frac{(n^f)^2}{k} (\nabla - \nabla s) - \rho_{0(s)}^f g = 0.
$$

$P_s$ denotes the mixture first Piola-Kirchhoff stress, $P_{E}^s$ denotes the extra stress
of phase $\alpha$ (i.e., material stress described by an appropriate constitutive model), $a_\alpha$ is the acceleration of phase $\alpha$ and $\hat{k}$ is the deformation dependent hydraulic conductivity:

$$
\hat{k} := \frac{\zeta}{\eta_f} \frac{\mathcal{F}(n_f)}{\mathcal{F}(n_0)} ,
$$

(9)

where $\eta_f$ is the pore fluid shear viscosity (assumed constant), $\zeta$ is the intrinsic permeability of the solid skeleton (assumed constant), and $\mathcal{F}$ is a nonlinear function of porosity $n_f$ accounting for change in hydraulic permeability due to change in porosity (e.g., the Kozeny-Carman relation):

$$
\mathcal{F}(n_f) := \frac{(n_f)^3}{1 - (n_f)^2} .
$$

(10)

In prior work,$^{27-30}$ it was assumed that the pore fluid first Piola-Kirchhoff extra stress

$$
P_f^{E(s)} := J_s \sigma_f^E F_{sw}^{-T} \approx 0 .
$$

(11)

In the present work, this assumption is not made, and a Newtonian fluid law is assumed,$^31$ such that

$$
\sigma_f^E := n_f \kappa_f \text{tr}(d_f) 1 + 2 \eta_f d_f ,
$$

(12)

where $\kappa_f$ denotes the constant bulk viscosity of the compressible pore fluid and

$$
d_f := \frac{1}{2} (\text{grad} v_f + \text{grad}^T v_f) .
$$

(13)

Thus, taking the divergence of Eq. 12 as required by Eq. 8 and insertion of Eq. 7 into Eq. 5, introduces a porosity gradient as well as a Laplacian of the pore fluid
where the porosity gradient, under the assumption of a mechanically incompressible solid (s) constituent, can be expressed as

\[
\frac{\partial n_f}{\partial x_j} = \frac{\partial n_f}{\partial X_j} F^{-1}_{Jj(s)} = \frac{\partial n^s}{\partial X_j} F^{-1}_{Jj(s)} = \frac{\partial}{\partial X_j} \left( \frac{n^s_0}{J_s} \right) F^{-1}_{Jj(s)} = \frac{n^s_0}{J_s^2} \frac{\partial \det(1 + \partial u_i(s)/\partial X_I)}{\partial X_j} F^{-1}_{Jj(s)} = \frac{n^s_0}{J_s^2} \frac{\partial^2 u_i(s)}{\partial X_I \partial X_j} F^{-1}_{Jj(s)}.
\]

The terms highlighted in red in Eqs. 14 and 15 possess second derivatives and thus convergence is not guaranteed for standard FE implementations if not weakened appropriately. In other words, they would require finite elements (for the respective fields) that possess \(C^1\) continuity rather than the standard \(C^0\) continuity (e.g., a typical Lagrange element). We will proceed to show that such a weakening of these terms will be very difficult.

Dropping now the \((\cdot)^s\) and \((\cdot)_s\) superscripts and subscripts for notational convenience, the strong form of the balance of mass for the biphasic mixture under the assumption of locally homogeneous temperatures and barotropic constituents is written as

\[
\frac{J n^f}{K^f_t} \partial_t p_t + D_t J + \frac{J}{K^p_t} \text{GRAD}(p_t) \cdot F^{-1} \cdot (n^f \tilde{v}_t) + J \text{GRAD} (n^f \tilde{v}_t) : F^{-T} = 0,
\]

\[
p_t(X,t) = g^p(X,t) \quad \forall X \in \Gamma_0^p,
\]

\[
- [J F^{-1} \cdot (n^f \tilde{v}_t)] \cdot N = Q_t(X,t) \quad \forall X \in \Gamma_0^{Q_t},
\]

where \(g^p\) is the prescribed pore fluid pressure on \(\Gamma_0^p\) (typically set for the “drained” boundary condition), and \(Q_t\) is the prescribed fluid flux (positive inward) on \(\Gamma_0^{Q_t}\), where we have assumed that the mass supply of the pore fluid (f) constituent is
Let $\mathcal{H}(u, u_t, p_t, w_{p_t})$ be the variational form of Eq. 16, and let $w_{p_t}$ be a set of scalar valued weighting (test) functions associated with pore fluid pressure $p_t$. We may then rewrite Eq. 16 in indicial notation as

$$
\mathcal{H}(u, u_t, p_t, w_{p_t}) = \int_{\Omega} w_{p_t} \left( \frac{J n_f^f}{K_f^\eta} \dot{p}_t + \dot{J} \right) \, dV \\
+ \int_{\Omega} w_{p_t} \frac{J}{K_f^\eta} \frac{\partial p_t}{\partial X_I} F^{-1}_{fi} \left( n_f^i \tilde{v}_{i(t)} \right) \, dV \\
+ \int_{\Omega} w_{p_t} J \frac{\partial}{\partial X_I} \left( n_f^i \tilde{v}_{i(t)} \right) F^{-1}_{fi} \, dV = 0 . \quad (17)
$$

Using chain rule, the last term in Eq. 17 can be rewritten as follows:

$$
\int_{\Omega} w_{p_t} J \frac{\partial}{\partial X_I} \left( n_f^i \tilde{v}_{i(t)} \right) F^{-1}_{fi} \, dV = \int_{\Omega} \frac{\partial}{\partial X_I} \left( w_{p_t} J \left( n_f^i \tilde{v}_{i(t)} \right) F^{-1}_{fi} \right) \, dV \\
- \int_{\Omega} \frac{\partial w_{p_t}}{\partial X_I} J \left( n_f^i \tilde{v}_{i(t)} \right) F^{-1}_{fi} \, dV \\
- \int_{\Omega} w_{p_t} \frac{\partial}{\partial X_I} \left( \frac{J F^{-1}_{fi}}{F_{fi}} \right) \, dV , \quad (18)
$$

wherein the last term goes to zero because of the Piola identity (as shown in Holzapfel\textsuperscript{31} p. 146). Substitution of Eq. 18 into Eq. 17 gives

$$
\mathcal{H}(u, u_t, p_t, w_{p_t}) = \int_{\Omega} w_{p_t} \left( \frac{J n_f^f}{K_f^\eta} \dot{p}_t + \dot{J} \right) \, dV \\
+ \int_{\Omega} w_{p_t} \frac{J}{K_f^\eta} \frac{\partial p_t}{\partial X_I} F^{-1}_{fi} \left( n_f^i \tilde{v}_{i(t)} \right) \, dV \\
+ \int_{\Omega} \frac{\partial}{\partial X_I} \left( w_{p_t} J \left( n_f^i \tilde{v}_{i(t)} \right) F^{-1}_{fi} \right) \, dV \\
- \int_{\Omega} \frac{\partial w_{p_t}}{\partial X_I} J \left( n_f^i \tilde{v}_{i(t)} \right) F^{-1}_{fi} \, dV = 0 . \quad (19)
$$

Applying the divergence theorem to the third term in Eq. 19, using the boundary
conditions in Eq. 16 (where $w^{pt} \to 0$ on $\Gamma^p_0$) and Eq. 16, the variational form for the balance of mass of the biphasic mixture becomes

$$
\mathcal{H}(u, u_i, p, w^{pt}) = \int_{B_0} w^{pt} \left( \frac{J n^f}{K_i} \tilde{p}_t + \dot{J} \right) dV
$$
$$
+ \int_{B_0} w^{pt} \frac{J}{K_i} \frac{\partial p_t}{\partial X_i} F_i^{-1} \left( n^f \tilde{v}_i(t) \right) dV
$$
$$
- \int_{\Gamma^0} \frac{\partial w^{pt}}{\partial X_i} J \left( n^f \tilde{v}_i(t) \right) F_i^{-1} dV - \int_{\Gamma^0} w^{pt} Q_t dA = 0 . \quad (20)
$$

Given the Darcy-Brinkman equation (Eq. 7), for notational simplicity, we will denote the separate terms as

$$
\mathcal{H} = \mathcal{H}^{\text{INT}}_1 + \mathcal{H}^{\text{INT}}_2 + \mathcal{H}^{\text{INT}}_3 + \mathcal{H}^{\text{INT}}_4 + \mathcal{H}^{\text{INT}}_5 - \mathcal{H}^{\text{EXT}} = 0 , \quad (21)
$$

where

$$
\mathcal{H}^{\text{INT}}_1 = \int_{B_0} w^{pt} \left( \frac{J n^f}{K_i} \tilde{p}_t + \dot{J} \right) dV ,
$$

$$
\mathcal{H}^{\text{INT}}_2 = \int_{B_0} w^{pt} \frac{J}{K_i} \frac{\partial p_t}{\partial X_i} F_i^{-1} \left( n^f \tilde{v}_i(t) \right) dV ,
$$

$$
\mathcal{H}^{\text{INT}}_3 = \int_{B_0} \frac{\partial w^{pt}}{\partial X_i} J F_i^{-1} \tilde{k} \frac{\partial p_t}{\partial X_i} F_i^{-1} dV ,
$$

$$
\mathcal{H}^{\text{INT}}_4 = \int_{B_0} \frac{\partial w^{pt}}{\partial X_i} J F_i^{-1} \tilde{k} p^R \left( a_{i(t)} - g_i \right) dV ,
$$

$$
\mathcal{H}^{\text{INT}}_5 = - \int_{\Gamma^0} \frac{\partial w^{pt}}{\partial X_i} \tilde{k} n^f J F_i^{-1} \frac{\partial \sigma_{ij}^{(E)}}{\partial X_j} F_i^{-1} dV ,
$$

$$
\mathcal{H}^{\text{EXT}} = \int_{\Gamma^0} w^{pt} Q_t dA .
$$

9
Considering $H^{\text{INT}}_2$, we have, upon expanding the Darcy-Brinkman term:

\[
H^{\text{INT}}_2 = - \int_{\Omega} w^{(p)} \frac{J_k}{K_i} \frac{\partial p_t}{\partial X} F_{Kk}^{-1} dV - \int_{\Omega} w^{(p)} \frac{J_k}{K_i} \frac{\partial p_t}{\partial X} F_{Kk}^{-1} dV - \int_{\Omega} w^{(p)} \frac{J_k}{K_i} \frac{\partial p_t}{\partial X} F_{Kk}^{-1} p^R (a_{i(t)} - g_i) dV
\]

\[
+ \int_{\Omega} w^{(p)} \frac{J_k}{K_i} \frac{\partial p_t}{\partial X} F_{Kk}^{-1} \left( \frac{1}{n^f} \left( \kappa_i \frac{\partial v_k(t)}{\partial X} F_{Kk}^{-1} F_{ji}^{-1} + \eta_f \left( \frac{\partial^2 v_i(t)}{\partial X_j \partial X_K} F_{Kj}^{-1} F_{ji}^{-1} + \frac{\partial^2 v_j(t)}{\partial X_j \partial X_K} F_{Kj}^{-1} F_{ji}^{-1} \right) \right) \right) dV.
\]

The first two terms can be integrated normally; however, the last cannot be integrated by parts to reduce continuity requirements of the solid skeleton (s) displacement and pore fluid (f) displacement given that a gradient is also applied to pore fluid pressure $p_t$ (i.e., weakening continuity requirements on the displacements in turn strengthens the continuity requirement on pore fluid pressure). This problem also arises in $H^{\text{INT}}_5$, although there the gradient is applied to the weighting function $w^{(p)}$:

\[
H^{\text{INT}}_5 = - \int_{\Omega} \frac{\partial w^{(p)}}{\partial X} J F_{Kk}^{-1} dV - \int_{\Omega} \frac{\partial w^{(p)}}{\partial X} J F_{Kk}^{-1} dV - \int_{\Omega} w^{(p)} \frac{J_k}{K_i} \frac{\partial p_t}{\partial X} F_{Kk}^{-1} p^R (a_{i(t)} - g_i) dV
\]

\[
+ \int_{\Omega} w^{(p)} \frac{J_k}{K_i} \frac{\partial p_t}{\partial X} F_{Kk}^{-1} \left( \frac{1}{n^f} \left( \kappa_i \frac{\partial v_k(t)}{\partial X} F_{Kk}^{-1} F_{ji}^{-1} + \eta_f \left( \frac{\partial^2 v_i(t)}{\partial X_j \partial X_K} F_{Kj}^{-1} F_{ji}^{-1} + \frac{\partial^2 v_j(t)}{\partial X_j \partial X_K} F_{Kj}^{-1} F_{ji}^{-1} \right) \right) \right) dV.
\]

Furthermore, the “mixed approach” taken by Vuong et al.\textsuperscript{32,33} to treat porosity $n^f$ as an independent field variable in the FE implementation (with the assumption of incompressible pore fluid (f) constituent, i.e., $\nabla \cdot \mathbf{v}_f = 0$), thereby eliminating strict dependence on solid skeleton (s) displacement, does not in and of itself relieve the issue of higher-order continuity requirements since second derivatives appear for pore fluid velocity when the pore fluid is assumed to be compressible ($\nabla \cdot \mathbf{v}_f \neq 0$), in both the balance of mass of the mixture and the balance of linear momentum of the pore fluid (assuming the divergence on the pore fluid extra stress is not weakened in the latter; details to follow in Section 3).

One potential remedy is to ignore the pore fluid extra stress tensor $\mathbf{\sigma}_f$ altogether.
It was shown by Markert\textsuperscript{34} and Ehlers\textsuperscript{35} (originally in Ehlers et al.\textsuperscript{36}) that the fluid friction (viscous) forces are negligible when compared to the drag forces on the macroscale. The derivation from Ehlers\textsuperscript{35} proceeds as follows.

Begin by assuming an incompressible pore fluid constituent and a rigid, non-deforming solid constituent:

\begin{equation}
D_t^f \rho^f \rightarrow 0, \quad \mathbf{u} \rightarrow \mathbf{0}.
\end{equation}

Then, the balance of mass of phase $\alpha$ reduces to (still under the assumption of negligible mass supply to phase $\alpha$)

\begin{equation}
D_t^\alpha n^\alpha + n^\alpha \text{div} \mathbf{v}_\alpha = 0.
\end{equation}

Given that

\begin{equation}
\sum_{\alpha} D_t^\alpha n^\alpha = \text{grad}(n^f) \cdot \tilde{\mathbf{v}}_t = \text{div}(n^f \tilde{\mathbf{v}}_t) - n^f \text{div} \mathbf{v}_t + (1 - n^s) \text{div} \mathbf{v}_s,
\end{equation}

the balance of mass of the mixture for incompressible constituents reduces to

\begin{equation}
\text{div}(n^f \tilde{\mathbf{v}}_t) = 0.
\end{equation}

For non-deforming solid, $n^s$ is constant ($\text{grad}(n^f) \rightarrow \mathbf{0}$), and thus

\begin{equation}
\text{div} \mathbf{v}_t = 0.
\end{equation}

Pore fluid momentum balance is written as

\begin{equation}
\rho^f \mathbf{a}_t + \text{div}(n^f p_t) - \text{div} \sigma_E^f - \mathbf{h}_f - \rho^f \mathbf{g} = \mathbf{0}.
\end{equation}

In a prior report,\textsuperscript{27} it was shown that the drag force

\begin{equation}
\mathbf{h}_f = \mathbf{h}_E^f + p_t \text{grad} n^f,
\end{equation}

with

\begin{equation}
\mathbf{h}_E^f = -S_w \tilde{\mathbf{v}}_t = -\frac{(n^f)^2}{k} \tilde{\mathbf{v}}_t, \quad S_w := \frac{(n^f)^2}{k} 1.
\end{equation}
With this, and by inserting the Newtonian fluid law given by Eq. 12 (using the identity $\text{tr}(d_t) = \text{div} \upsilon_t$, which is zero by Eq. 29) into Eq. 30 gives the pore fluid momentum balance for incompressible constituents and non-deforming solid skeleton:

$$\rho' \alpha_t + n^f \text{grad} p_t - n^f \eta_t \text{div} \text{grad} \upsilon_t + \frac{(n^f)^2}{k} \upsilon_t - \rho' g = 0. \quad (33)$$

Introducing the dimensionless quantities

$$\star x := \frac{x}{L} \quad \star \upsilon_t := \frac{\upsilon_t}{V}, \quad (34)$$

with $L$ as a characteristic length scale and $V$ as a characteristic velocity allows us to write the dimensionless gradient and divergence operators as

$$\star \text{grad}(\cdot) = L \text{grad}(\cdot), \quad \star \text{div}(\cdot) = L \text{div}(\cdot). \quad (35)$$

Then we may recast the viscous and drag forces in Eq. 33 as, respectively,

$$\begin{align*}
\text{div} \sigma^f_E &= n^f \eta_t \frac{V}{L^2} \text{div}(\star \text{grad} \star \upsilon_t), \\
\mathbf{h}^f_E &= -\frac{(n^f)^2}{k} V \star \upsilon_t.
\end{align*} \quad (36)$$

Taking the ratio of the viscous force to the drag force yields

$$\frac{\text{Viscous force}}{\text{Drag force}} \propto \eta_t \frac{\dot{k}}{n^f L^2} = \frac{\kappa}{n^f L^2}. \quad (37)$$

For porous media applications, $\kappa$ is typically several orders of magnitude smaller than the length scale of interest $L$ (e.g., in the current work $\kappa \sim \mathcal{O}(10^{-10} \text{ m}^2)$ for lung parenchyma\textsuperscript{37} and $L \sim \mathcal{O}(10^{-2} \text{ m})$). Thus, it may be appropriate to ignore the pore fluid extra stress (the viscous force) when solving the balance equations for the macroscale regime, but not necessarily for the microscale regime where the pore size $\sqrt{\kappa}$ is on the order of $L$.

However, as Vuong points out (see Section 3.3.6 of Vuong\textsuperscript{33} and the figures therein), a nearly inviscid fluid creates infinitesimally large velocity gradients at the porous channel walls to counteract an infinitesimally small boundary layer, which could lead to numerical instability for 3-D simulations, particularly for highly permeable
materials, that is, those with larger pore sizes (larger fluid domains). Whether or not it is necessary to account for the boundary layer in a numerical simulation where flow is modeled on the macroscale regime is an area of debate.\textsuperscript{38} This boundary layer has thickness of order $\tilde{\eta}_f \sim (\tilde{\eta}_f/\eta_f)^{1/2}$, where $\tilde{\eta}_f$ is an effective viscosity of the pore fluid. For lung parenchyma,\textsuperscript{37} $\sim \times 10^{-10}$ m$^2$, thus these viscous effects are probably negligible at the mesoscale level of interest for lung parenchyma, which is $O(10^{-2})$ m.

Generally speaking, it is believed that both the Darcy and Darcy-Brinkman equations only hold in the range of Reynolds numbers\textsuperscript{33,38–40} $1 < Re < 10$—for reference, in prior work,\textsuperscript{28,29} the maximum Reynolds number resulting from numerical simulations was roughly $Re = 10.7$. Nevertheless, the Reynolds number-based limits are based upon experimental data wherein it is difficult to measure the inertia forces,\textsuperscript{41} and, with the exception of Vuong et al.,\textsuperscript{32,33} many authors do not include the inertia term in Darcy’s law, and use instead the classical form that relates seepage velocity to pore fluid pressure gradient and (if applicable) body forces.

2.2 Satisfying $C^1$ Continuity

If the pore fluid extra stress is to be included, elements with continuous first derivatives along their boundaries must be used to guarantee convergence. The approach taken by Vuong et al.\textsuperscript{32,33} to guarantee $C^1$ continuity was to use Non-Uniform Rational Basis Splines (NURBS) (refer to work by Hughes et al.\textsuperscript{42} for a FE application). However, for the simple 1-D geometry considered herein, NURBS would introduce an additional layer of complexity given that the basis functions are not interpolatory.

A simpler solution would be to invoke the Hermite cubic polynomial element (which is $C^1$ continuous), typically employed in FE analysis of beams. Herein, the analogy to a rotational degree of freedom (DOF) in beam analysis is the gradient DOF. However, unlike beam analysis, the gradient DOFs of the field variables of interest ($u$ and $u_f$) are allowed to “float,” that is, no Dirichlet nor Neumann boundary conditions are prescribed on these DOFs; in essence, they go unused outside of their interpolatory functionality.

The element (refer to Fig. 2) will not be isoparametric, that is,

$$x^h(\xi) = N^e(\xi) \cdot \mathbf{x}^e, \quad u^e(\xi) = N^e_{H^e}(\xi) \cdot \mathbf{d}^e,$$  \hspace{1cm} (38)
Fig. 2 The Q3H-Q3H-P1 line element used for $C^1$ continuity of the field variables $u$ and $u_f$. Shown in red are the gradient DOFs that are allowed to “float,” that is, no boundary conditions are prescribed for these DOFs.

with

$$N^e_1 := \frac{1}{2}(1 - \xi),$$

$$N^e_2 := \frac{1}{2}(1 + \xi),$$

(39)
and
\[
\mathbf{d}^e = \begin{cases}
  \begin{pmatrix}
    d_1^e \\
    d_2^e \\
    d_3^e \\
    d_4^e
  \end{pmatrix} = \\
  \begin{pmatrix}
    u^h_e(\xi = -1) \\
    u^h_{x}(-1) \\
    u^h_e(1) \\
    u^h_{x}(1)
  \end{pmatrix},
\end{cases}
\]
\[(40)\]
such that
\[
u^h_e(\xi) = \begin{bmatrix}
  N_{1(H)}^{e,u} & j^e N_{2(H)}^{e,u} & j^e N_{3(H)}^{e,u} & j^e N_{4(H)}^{e,u}
\end{bmatrix}
\begin{pmatrix}
  d_1^e \\
  d_2^e \\
  d_3^e \\
  d_4^e
\end{pmatrix} = N_{H}^{e,u}(\xi) \cdot \mathbf{d}^e,
\]
\[(41)\]
where \(N_{H}^{e,u}(\xi)\) are the element Hermite cubic polynomials:
\[
N_{1(H)}^{e,u} := \frac{1}{4}(1 - \xi)^2(2 + \xi),
\]
\[
N_{2(H)}^{e,u} := \frac{1}{4}(1 - \xi)^2(1 + \xi),
\]
\[
N_{3(H)}^{e,u} := \frac{1}{4}(1 + \xi)^2(2 - \xi),
\]
\[
N_{4(H)}^{e,u} := \frac{1}{4}(1 + \xi)^2(-1 + \xi),
\]
\[(42)\]
and
\[
\frac{\partial u^h_e}{\partial \xi} = j^e \frac{\partial u^h_e}{\partial x},
\]
\[
w^{u,e}_e(\xi) = N_{H}^{e,u} \cdot e^{u,e} = (e^{u,e})^T \cdot (N_{H}^{e,u})^T.
\]
\[(43)\]
Herein, the “strain-displacement” matrix \(H^{e,u}\) is defined as
\[
\frac{\partial^2 u^h_e}{\partial x^2} = \frac{d^2 N_{H}^{e,u}(\xi)}{\partial x^2} \cdot \mathbf{d}^e = \frac{1}{(j^e)^2} \frac{d^2 N_{H}^{e,u}(\xi)}{\partial \xi^2} \cdot \mathbf{d}^e = H^{e,u}(\xi) \cdot \mathbf{d}^e,
\]
\[(44)\]
and
\[
\frac{\partial u^h_e}{\partial x} = \frac{d B_{H}^{e,u}(\xi)}{\partial x} \cdot \mathbf{d}^e = \frac{1}{j^e} \frac{d B_{H}^{e,u}(\xi)}{\partial \xi} \cdot \mathbf{d}^e = B_{H}^{e,u}(\xi) \cdot \mathbf{d}^e.
\]
\[(45)\]
For notational purposes, the \((\cdot)_H\) subscript will be dropped from \(N_{H}^{e,u}\) and \(B_{H}^{e,u}\).

In the finite element equations where \(H^{e,u}\) is used, the reader should assume that the shape functions for the respective field, and its first derivative, are the Hermite shape functions shown here (i.e., only one element type will be used to represent a field variable, not a mix of element types). Of course the same interpolation applies to the shape functions \(N_{H}^{e,u_f}\), \(B_{H}^{e,u_f}\), and \(H^{e,u_f}\) when the pore fluid displacement \(u_f\) requires a \(C^1\) continuous element.

### 3. Numerical Implementation

#### 3.1 1-D Kinematics

One-dimensional uniaxial solid skeleton strain and unidirectional pore fluid flow simplifications are implemented for (s) and (f) phases, respectively. If we assume that the soft porous material only undergoes compression or expansion in one dimension, specifically the vertical direction \(X\), then both the solid skeleton displacements in the transverse directions as well as all shear terms in the deformation gradient go to zero. The solid skeleton deformation gradient becomes

\[
F_s = \begin{bmatrix}
1 + \frac{\partial u}{\partial X} & 0 & 0 \\
0 & 1 & 0 \\
0 & 0 & 1
\end{bmatrix}, \quad J_s = \det F_s = F_{11(s)} = 1 + \frac{\partial u}{\partial X}
\]  

(46)

where \(u(X, t)\) is the axial displacement in the \(X\) direction. Similarly, if we assume that pore fluid flow is confined in direction \(X\) (i.e., surrounded by an impermeable sleeve, drained or undrained at its ends), then

\[
v_f = \begin{bmatrix} v_f \\ 0 \\ 0 \end{bmatrix}, \quad a_f = \begin{bmatrix} a_f \\ 0 \\ 0 \end{bmatrix}, \quad u_f = \begin{bmatrix} u_f \\ 0 \\ 0 \end{bmatrix}
\]  

(47)

where in the \(X\) direction, \(v_f\) is the pore fluid velocity, \(a_f\) is the pore fluid acceleration, and \(u_f\) is the pore fluid displacement. Variational forms that follow are first presented in a general 3-D regime before simplifications to the 1-D regime; the \((\cdot)^s\) and \((\cdot)_s\) superscripts and subscripts are dropped for notational convenience.
3.2 Variational Formulation

The strong and variational form of the balance of mass of the mixture was given in Section 2, but is briefly restated here as

\[
\frac{Jn^f}{K_t^p} D_t p_t + D_t J + \frac{J}{K_t^p} \text{GRAD}(p_t) \cdot F^{-1} \cdot (n^f \tilde{v}_t) + J \text{GRAD} (n^f \tilde{v}_t) : F^{-T} = 0 ,
\]

\[
p_t(X, t) = g^p(X, t) \quad \forall X \in \Gamma_0^p ,
\]

\[- \left[ J F^{-1} \cdot (n^f \tilde{v}_t) \right] \cdot N = Q_t(X, t) \quad \forall X \in \Gamma_0^{Q_t} ,
\]

(48)

where \( g^p \) is the prescribed pore fluid pressure on \( \Gamma_0^p \) (typically set for the “drained” boundary condition), and \( Q_t \) is the prescribed fluid flux (positive inward) on \( \Gamma_0^{Q_t} \), where we have assumed that the mass supply of the pore fluid (f) constituent is negligible.

Let \( \mathcal{H}(u, u_t, p_t, w_{p_t}) \) be the variational form of Eq. 48, and let \( w_{p_t} \) be a set of scalar valued weighting (test) functions associated with pore fluid pressure \( p_t \). We may then rewrite Eq. 48 in indicial notation as

\[
\mathcal{H}(u_i, u_{t_i}, p_t, w_{p_t}) = \int_{B_0} w_{p_t} \left( \frac{Jn^f}{K_t^p} p_t + J \right) dV
\]

\[
+ \int_{B_0} w_{p_t} J \frac{\partial p_t}{\partial X_i} F_{-i}^{-1} (n^f \tilde{v}_{t_i}) dV
\]

\[- \int_{B_0} \frac{\partial w_{p_t}}{\partial X_i} J (n^f \tilde{v}_{t_i}) F_{-i}^{-1} dV - \int_{\Gamma_0^{Q_t}} w_{p_t} Q_t dA = 0 .
\]

(49)

For notational simplicity, we will denote the separate terms as

\[
\mathcal{H} = \mathcal{H}_1^{\text{INT}} + \mathcal{H}_2^{\text{INT}} + \mathcal{H}_3^{\text{INT}} + \mathcal{H}_4^{\text{INT}} + \mathcal{H}_5^{\text{INT}} - \mathcal{H}^{\text{EXT}} = 0 ,
\]

(50)
where

\[ H_{\text{INT}}^1 = \int_{B_0} w^{p_0} \left( \frac{J n^f}{K_i^f} \hat{p} + J \right) dV , \]

\[ H_{\text{INT}}^2 = \int_{B_0} w^{p_0} \frac{J}{K_i^f} \frac{\partial p_f}{\partial X_i} F^{-1}_{ii} \left( n^f \tilde{v}_{i(f)} \right) dV , \]

\[ H_{\text{INT}}^3 = \int_{B_0} \frac{\partial w^{p_0}}{\partial X_i} J F^{-1}_{ii} \hat{k} \frac{\partial p_f}{\partial X_K} F^{-1}_{Ki} dV , \]

\[ H_{\text{INT}}^4 = \int_{B_0} \frac{\partial w^{p_0}}{\partial X_i} J F^{-1}_{ii} \hat{k} \rho^{R} \left( a_i(t) - g_i \right) dV , \]

\[ H_{\text{INT}}^5 = - \int_{B_0} \frac{\partial w^{p_0}}{\partial X_i} \hat{k} n^f J F^{-1}_{ii} \frac{\partial \sigma_{11}^f(E)}{\partial X_j} F^{-1}_{ji} dV , \]

\[ H_{\text{INT}} = \int_{\Gamma_0^Q} w^{p_0} Q_f dA . \]

The 1-D reduction of Eq. 51 is

\[ H_{\text{INT}}^1 = \int_{0}^{X=H} w^{p_0} \left( \frac{J n^f}{K_i^f} \hat{p} + J \right) A dX , \]

\[ H_{\text{INT}}^2 = \int_{0}^{X=H} w^{p_0} \frac{1}{K_i^f} \frac{\partial p_f}{\partial X} n^f \tilde{v}_l A dX , \]

\[ H_{\text{INT}}^3 = \int_{0}^{X=H} \frac{\partial w^{p_0}}{\partial X} \hat{k} \frac{\partial p_f}{\partial X} F^{-1}_{11} A dX , \]

\[ H_{\text{INT}}^4 = \int_{0}^{X=H} \frac{\partial w^{p_0}}{\partial X} \hat{k} \rho^{R} \left( a_l + g \right) A dX , \]

\[ H_{\text{INT}}^5 = - \int_{0}^{X=H} \frac{\partial w^{p_0}}{\partial X} \hat{k} \frac{\partial \sigma_{11}^f(E)}{\partial X} F^{-1}_{11} A dX , \]

\[ H_{\text{EXT}} = \int_{\Gamma_0^Q} w^{p_0} Q_f dA = Q_f|_{X=H} A . \]

The strong form of the balance of linear momentum of the biphasic mixture is given
as

\[ \text{DIV } \mathbf{P} + \rho_0 \mathbf{g} - (\rho_0^a a_i + \rho_0^f a_i) = 0, \]

\[ \mathbf{u}(\mathbf{X}, t) = \mathbf{g}^u(\mathbf{X}, t) \quad \forall \mathbf{X} \in \Gamma_0^u, \quad (53) \]

\[ \mathbf{P}(\mathbf{X}, t) \cdot \mathbf{N}(\mathbf{X}) = \mathbf{t}^\sigma(\mathbf{X}, t) \quad \forall \mathbf{X} \in \Gamma_0^t. \]

Let \( \mathcal{G}(u_i, u_{i(f)}, p_I, w^{u_i}) \) be the variational form of Eq. 53 and let \( w^{u_i} \) be a set of vector-valued weighting (test) functions associated with solid skeleton displacement \( u_i \).

We may then rewrite Eq. 53 as

\[
\mathcal{G}(u_i, u_{i(f)}, p_I, w^{u_i}) = \int_{B_0} w^{u_i} (\rho_0^a a_i + \rho_0^f a_{i(f)}) \, dV + \int_{B_0} \frac{\partial w^{u_i}}{\partial X_I} P^w_{i(I(E))} \, dV
\]

\[- \int_{B_0} \frac{\partial w^{u_i}}{\partial X_I} JF_{Ii}^{-1} p_I \, dV + \int_{B_0} \frac{\partial w^{u_i}}{\partial X_I} P^f_{i(I(E))} \, dV - \int_{B_0} w^{u_i} \rho_0 g_i \, dV
\]

\[- \left( \int_{\Gamma_0^t} w^{u_i} t^{\sigma_E}_{i} \, dA - \int_{\Gamma_0^t} w^{u_i} p_I JF_{Ii}^{-1} N_I \, dA + \int_{\Gamma_0^t} w^{u_i} t^{\sigma_f}_{i} \, dA \right) = 0, \quad (54) \]

where the divergence on total first Piola-Kirchhoff stress of the mixture was weakened using divergence theorem, producing the second, third, fourth, and last terms in Eq. 54. The last term represents the total traction applied to solid and fluid phases (the mixture). Thus, there is no need to compute any of its components, for example, the integrand of the “viscous traction” \( t^{\sigma_f}_{i} \) term. For notational simplicity, we denote the separate terms as

\[ \mathcal{G} = \mathcal{G}_1^{\text{INT}} + \mathcal{G}_2^{\text{INT}} + \mathcal{G}_3^{\text{INT}} + \mathcal{G}_4^{\text{INT}} - (\mathcal{G}_1^{\text{EXT}} + \mathcal{G}_2^{\text{EXT}} + \mathcal{G}_3^{\text{EXT}}) = 0, \quad (55) \]
where

\[ G_{1}^{\text{INT}} = \int_{B_0} w_i^u \left( \rho_0^s a_i + \rho_0^f a_i(f) \right) \, dV , \]

\[ G_{2}^{\text{INT}} = \int_{B_0} \frac{\partial w_i^u}{\partial X_I} P_{iI(E)} \, dV , \]

\[ G_{3}^{\text{INT}} = - \int_{B_0} \frac{\partial w_i^u}{\partial X_I} J F_{iI}^{-1} p_I \, dV , \]

\[ G_{4}^{\text{INT}} = - \int_{B_0} w_i^u \rho_0 g_i \, dV , \]

\[ G_{5}^{\text{INT}} = \int_{B_0} \frac{\partial w_i^u}{\partial X_I} P_{iI(E)} \, dV , \]

\[ G_{1}^{\text{EXT}} = \int_{\Gamma_0'} w_i^u t_i^g \, dA , \]

\[ G_{2}^{\text{EXT}} = - \int_{\Gamma_0'} w_i^u p_I J F_{iI}^{-1} N_I \, dA , \]

\[ G_{3}^{\text{EXT}} = \int_{\Gamma_0'} w_i^u t_i^g \, dA . \]
The 1-D reduction of Eq. 56 is

\begin{align*}
    G_1^{\text{INT}} &= \int_0^{X=H} w^u \left( \rho_0^a_s + \rho_0^a_t \right) A dX , \\
    G_2^{\text{INT}} &= \int_0^{X=H} \frac{\partial w^u}{\partial X} P_{11(E)}^s A dX , \\
    G_3^{\text{INT}} &= -\int_0^{X=H} \frac{\partial w^u}{\partial X} pt A dX , \\
    G_4^{\text{INT}} &= \int_0^{X=H} w^u \rho_0 g A dX , \\
    G_5^{\text{INT}} &= \int_0^{X=H} \frac{\partial w^u}{\partial X} P_{11(E)}^f A dX , \\
    G_1^{\text{EXT}} &= \int_{\Gamma_0^i} w^u t^{\sigma_k} dA = t^{\sigma_k} A , \\
    G_2^{\text{EXT}} &= -\int_{\Gamma_0^i} w^u pt dA = -pt A , \\
    G_3^{\text{EXT}} &= \int_{\Gamma_0^i} w^u t^{\sigma_k} dA = t^{\sigma_k} A .
\end{align*}

If we combine Eq. 57\textsubscript{6,7,8} we see that

\[ G_1^{\text{EXT}} + G_2^{\text{EXT}} + G_3^{\text{EXT}} = A \left( t^{\sigma_k} - pt + t^{\sigma_k} \right) = At^\sigma . \]  

The strong formulation of the balance of linear momentum for a viscous pore fluid is given as

\[ \rho_0^f a_t + Jn^f \text{GRAD}(pt) \cdot F^{-1} - \text{DIV} P_E^f + \frac{J(n^f)^2}{k} (u_t - v) - \rho_0^f g = 0 , \]

\[ u_t(X, t) = g_{u_t}(X, t) \forall X \in \Gamma_0^i . \]

Let \( I(u_i, u_{i(t)}, pr, w_i^{nu}) \) be the variational form of Eq. 59 and let \( w_i^{nu} \) be a set of vector-valued weighting functions associated with pore fluid displacement \( u_{i(t)} \). We
may then rewrite Eq. 59 as follows:

\[
\mathcal{I}(u_i, u_i(f), p_f, w_i^{ut}) = \int_{B_0} w_i^{ut} \rho_0 a_i(f) \, dV + \int_{B_0} w_i^{ut} J n_t \frac{\partial p_f}{\partial X_t} F_{fi}^{-1} \, dV
\]

\[
+ \int_{B_0} w_i^{ut} J \frac{(n_t)^2}{k} (v_i(f) - v_i) \, dV
\]

\[
- \int_{B_0} w_i^{ut} \frac{\partial P_{ii(E)}}{\partial X_t} \, dV - \int_{B_0} w_i^{ut} \rho_0 g_i \, dV = 0 , \quad (60)
\]

wherein the second to last term in Eq. 60 can be split into two terms, similar to the procedure in the balance of momentum of the mixture, as follows:

\[
\mathcal{I}(u_i, u_i(f), p_f, w_i^{ut}) = \int_{B_0} w_i^{ut} \rho_0 a_i(f) \, dV + \int_{B_0} w_i^{ut} J n_t \frac{\partial p_f}{\partial X_t} F_{fi}^{-1} \, dV
\]

\[
+ \int_{B_0} w_i^{ut} J \frac{(n_t)^2}{k} (v_i(f) - v_i) \, dV
\]

\[
+ \int_{B_0} \frac{\partial w_i^{ut}}{\partial X_t} P_{ii(E)} \, dV - \int_{B_0} w_i^{ut} t_{\sigma f}^{\gamma} \, dA
\]

\[
- \int_{B_0} w_i^{ut} \rho_0 g_i \, dV = 0 . \quad (61)
\]

However, doing so creates an additional complexity, namely that now \(t_{\sigma f}^{\gamma}\) must be determined. In Vuong et al.,\(^32,33\) such a traction is merely a stress balance between solid and fluid phases, and does not take into account an external load as implied here. There are at least two ways in which one might approximate the viscous traction.

The first follows from analysis by Heider\(^43\) for a nearly inviscid pore fluid. It involves applying traction to the solid and fluid phases separately, which thus necessitates an equation that solves balance of linear momentum of the solid phase, rather than an equation that solves the balance of linear momentum of the mixture. Supposing then that the total traction

\[
t^\sigma = \overbrace{t^{\sigma s}}^{\text{applied to solid mom. bal.}} + \overbrace{t^{\sigma f}}^{\text{applied to fluid mom. bal.}} \quad (62)
\]
is specified (e.g., from known data), one may deduce the viscous traction component $\mathbf{t}^\sigma_{\text{fE}}$ via an implicit solve using the solutions $\mathbf{u}$ and $p_f$, that is,

$$
\mathbf{t}^\sigma_{\text{fE}} = \mathbf{t}^\sigma - \mathbf{t}^{\sigma^s} = \mathbf{t}^\sigma - (\mathbf{\sigma}^s_{\text{E}} - n^s p_f \mathbf{1}) \cdot \mathbf{n} + n^f p_f \mathbf{n},
$$

(63)

where $\mathbf{\sigma}^s_{\text{E}}, n^s, n^f$ are functions of solid displacement $\mathbf{u}$. Heider$^{43}$ observed inaccurate pore fluid pressure solutions with such a scheme for low permeabilities, small strain theory and low-strain-rate loadings, unless additional stabilization parameters were provided. Given difficulties obtaining stable solutions at finite strain for high-strain-rate loadings,$^{28,29}$ it is outside the current scope to pursue such a method.

The other approach would be to use the mixture linear momentum balance equation, and approximate the value of $\mathbf{t}^\sigma_{\text{fE}}$ using the interpolated values of porosity and pore fluid velocity gradient at the Gauss point closest to the boundary where $\mathbf{t}^\sigma_{\text{fE}}$ is applied. However, this would be inconsistent with how the total traction is applied to the mixture in the balance of linear momentum of the mixture; there, no such approximations are used for $\mathbf{t}^\sigma_{\text{fE}}$, nor $\mathbf{t}^{\sigma^s_{\text{E}}}$ nor the pore fluid pressure component.

The most consistent assumption, in contrast to the previous two cumbersome alternatives, is to not weaken the divergence of the pore fluid extra stress term, in other words, to use Eq. 60. We have already established in Section 2 that the pore fluid velocity cannot be weakened in the balance of mass of the mixture equations; therefore, requiring $C^1$ continuity in the balance of linear momentum of the pore fluid raises no issues, and alleviates the problem of specifying the “viscous traction” term.

For notational simplicity, we will denote the separate terms in Eq. 60 as

$$
\mathcal{I} = \mathcal{I}_1^{\text{INT}} + \mathcal{I}_2^{\text{INT}} + \mathcal{I}_3^{\text{INT}} + \mathcal{I}_4^{\text{INT}} + \mathcal{I}_5^{\text{INT}} = 0,
$$

(64)
where

\[ I_{\text{INT}}^1 = \int_{B_0} w_i^{u_e} \rho_0 a_i(t) \, dV , \]

\[ I_{\text{INT}}^2 = \int_{B_0} w_i^{u_e} J n^f \frac{\partial p_{11}^f}{\partial X_1} F_{3i}^{-1} \, dV , \]

\[ I_{\text{INT}}^3 = \int_{B_0} w_i^{u_e} J \frac{(n^f)^2}{k} (v_{i(t)} - v_i) \, dV , \]

\[ I_{\text{INT}}^4 = - \int_{B_0} w_i^{u_e} \rho_0 g_i \, dV , \]

\[ I_{\text{INT}}^5 = - \int_{B_0} w_i^{u_e} \frac{\partial P_{1i}^{f(E)}}{\partial X_1} \, dV . \]

The 1-D reduction of Eq. 65 is

\[ I_{\text{INT}}^1 = \int_0^{X=H} w_i^{u_e} \rho_0 a_i A \, dX , \]

\[ I_{\text{INT}}^2 = \int_0^{X=H} w_i^{u_e} n^f \frac{\partial p_{11}^f}{\partial X} A \, dX , \]

\[ I_{\text{INT}}^3 = \int_0^{X=H} w_i^{u_e} J \frac{(n^f)^2}{k} (v_{i(t)} - v) A \, dX , \]

\[ I_{\text{INT}}^4 = \int_0^{X=H} w_i^{u_e} \rho_0 g A \, dX , \]

\[ I_{\text{INT}}^5 = - \int_0^{X=H} w_i^{u_e} \frac{\partial P_{1i}^{f(E)}}{\partial X} A \, dX . \]
3.3 FE Implementation

The FE implementation follows from Irwin et al.,\textsuperscript{29,30} though in the present work we invoke the Q3H-Q3H-P1 element as discussed in Section 2 to be able to handle second-order spatial derivatives of solid and fluid displacements. In other words, the Hermite cubic polynomials are used to interpolate solid skeleton and pore fluid displacement and their associated gradients, and linear shape functions are used to interpolate pore fluid pressure and associated gradients.

For our solution variables of interest (i.e., \( u \), \( u_f \), and \( p_f \)) we introduce the corresponding discretizations \( d \), \( d_t \), and \( \pi \), respectively. For solid skeleton displacement \( d \), we have

\[
\begin{align*}
  u^h_e(\xi, t) &= \sum_{a=1}^{n_{dof}^{s,e}} N^u_a(\xi) d^e_a(t) = \left\{ N^{e,u} \right\} \cdot \left\{ d^e \right\},
  \end{align*}
\]

(67)

where for the Q3H-Q3H-P1 element \( n_{dof}^{s,e} = 4 \). The solid skeleton velocity and acceleration are defined similarly:

\[
\begin{align*}
  v^h_e(\xi, t) &= \sum_{a=1}^{n_{dof}^{s,e}} N^u_a(\xi) \dot{d}^e_a(t) = \left\{ N^{e,u} \right\} \cdot \left\{ \dot{d}^e \right\},
  \end{align*}
\]

(68)

\[
\begin{align*}
  a^h_e(\xi, t) &= \sum_{a=1}^{n_{dof}^{s,e}} N^u_a(\xi) \ddot{d}^e_a(t) = \left\{ N^{e,u} \right\} \cdot \left\{ \ddot{d}^e \right\}.
  \end{align*}
\]

Solid skeleton displacement gradient, velocity gradient, and acceleration gradient
are defined as follows, respectively:

\[
\frac{\partial u^h_e(\xi, t)}{\partial X} = \sum_{a=1}^{n_{\text{def}}^{s,e}} B_{a}^{u}(\xi) d_{a}^{e}(t) = \begin{bmatrix} B^{e,u} \end{bmatrix}_{1 \times n_{\text{def}}^{s,e}} \cdot \begin{bmatrix} d^{e} \end{bmatrix}_{n_{\text{def}}^{s,e} \times 1},
\]

(69)

\[
\frac{\partial v^h_e(\xi, t)}{\partial X} = \sum_{a=1}^{n_{\text{def}}^{s,e}} B_{a}^{u}(\xi) \dot{d}_{a}^{e}(t) = \begin{bmatrix} B^{e,u} \end{bmatrix}_{1 \times n_{\text{def}}^{s,e}} \cdot \begin{bmatrix} \dot{d}^{e} \end{bmatrix}_{n_{\text{def}}^{s,e} \times 1},
\]

\[
\frac{\partial a^h_e(\xi, t)}{\partial X} = \sum_{a=1}^{n_{\text{def}}^{s,e}} B_{a}^{u}(\xi) \ddot{d}_{a}^{e}(t) = \begin{bmatrix} B^{e,u} \end{bmatrix}_{1 \times n_{\text{def}}^{s,e}} \cdot \begin{bmatrix} \ddot{d}^{e} \end{bmatrix}_{n_{\text{def}}^{s,e} \times 1}.
\]

Second-order gradients are defined as follows:

\[
\frac{\partial^2 u^h_e(\xi, t)}{\partial X^2} = \sum_{a=1}^{n_{\text{def}}^{s,e}} H_{a}^{u}(\xi) d_{a}^{e}(t) = \begin{bmatrix} H^{e,u} \end{bmatrix}_{1 \times n_{\text{def}}^{s,e}} \cdot \begin{bmatrix} d^{e} \end{bmatrix}_{n_{\text{def}}^{s,e} \times 1},
\]

(70)

\[
\frac{\partial^2 v^h_e(\xi, t)}{\partial X^2} = \sum_{a=1}^{n_{\text{def}}^{s,e}} H_{a}^{u}(\xi) \dot{d}_{a}^{e}(t) = \begin{bmatrix} H^{e,u} \end{bmatrix}_{1 \times n_{\text{def}}^{s,e}} \cdot \begin{bmatrix} \dot{d}^{e} \end{bmatrix}_{n_{\text{def}}^{s,e} \times 1},
\]

\[
\frac{\partial^2 a^h_e(\xi, t)}{\partial X^2} = \sum_{a=1}^{n_{\text{def}}^{s,e}} H_{a}^{u}(\xi) \ddot{d}_{a}^{e}(t) = \begin{bmatrix} H^{e,u} \end{bmatrix}_{1 \times n_{\text{def}}^{s,e}} \cdot \begin{bmatrix} \ddot{d}^{e} \end{bmatrix}_{n_{\text{def}}^{s,e} \times 1}.
\]

Discretizations of the pore fluid displacement \( d_{f} \) are given as follows, where for the
Q3H-Q3H-P1 element $n_{\text{dof}}^{f,e} := 4$:

$$
\begin{align*}
    u_h^e(\xi, t) &= \sum_{a=1}^{n_{\text{dof}}^{f,e}} N_a^{u_f}(\xi) d_{a,f}^e(t) = \left\{ N^{e,u_f} \right\}_{1 \times n_{\text{dof}}^{f,e}} \cdot \left\{ d_f^e \right\}_{n_{\text{dof}}^{f,e} \times 1}, \\
    v_h^e(\xi, t) &= \sum_{a=1}^{n_{\text{dof}}^{f,e}} N_a^{u_f}(\xi) \ddot{d}_{a,f}^e(t) = \left\{ N^{e,u_f} \right\}_{1 \times n_{\text{dof}}^{f,e}} \cdot \left\{ \ddot{d}_f^e \right\}_{n_{\text{dof}}^{f,e} \times 1}, \\
    a_h^e(\xi, t) &= \sum_{a=1}^{n_{\text{dof}}^{f,e}} N_a^{u_f}(\xi) \dddot{d}_{a,f}^e(t) = \left\{ N^{e,u_f} \right\}_{1 \times n_{\text{dof}}^{f,e}} \cdot \left\{ \dddot{d}_f^e \right\}_{n_{\text{dof}}^{f,e} \times 1}, \\
    \frac{\partial u_h^e(\xi, t)}{\partial X} &= \sum_{a=1}^{n_{\text{dof}}^{f,e}} B_a^{u_f}(\xi) \dot{d}_{a,f}^e(t) = \left\{ B^{e,u_f} \right\}_{1 \times n_{\text{dof}}^{f,e}} \cdot \left\{ \dot{d}_f^e \right\}_{n_{\text{dof}}^{f,e} \times 1}, \\
    \frac{\partial v_h^e(\xi, t)}{\partial X} &= \sum_{a=1}^{n_{\text{dof}}^{f,e}} B_a^{u_f}(\xi) \ddot{d}_{a,f}^e(t) = \left\{ B^{e,u_f} \right\}_{1 \times n_{\text{dof}}^{f,e}} \cdot \left\{ \ddot{d}_f^e \right\}_{n_{\text{dof}}^{f,e} \times 1}, \\
    \frac{\partial a_h^e(\xi, t)}{\partial X} &= \sum_{a=1}^{n_{\text{dof}}^{f,e}} B_a^{u_f}(\xi) \dddot{d}_{a,f}^e(t) = \left\{ B^{e,u_f} \right\}_{1 \times n_{\text{dof}}^{f,e}} \cdot \left\{ \dddot{d}_f^e \right\}_{n_{\text{dof}}^{f,e} \times 1}, \\
    \frac{\partial^2 u_h^e(\xi, t)}{\partial X^2} &= \sum_{a=1}^{n_{\text{dof}}^{f,e}} H_a^{u_f}(\xi) \ddot{d}_{a,f}^e(t) = \left\{ H^{e,u_f} \right\}_{1 \times n_{\text{dof}}^{f,e}} \cdot \left\{ \ddot{d}_f^e \right\}_{n_{\text{dof}}^{f,e} \times 1}, \\
    \frac{\partial^2 v_h^e(\xi, t)}{\partial X^2} &= \sum_{a=1}^{n_{\text{dof}}^{f,e}} H_a^{u_f}(\xi) \dddot{d}_{a,f}^e(t) = \left\{ H^{e,u_f} \right\}_{1 \times n_{\text{dof}}^{f,e}} \cdot \left\{ \dddot{d}_f^e \right\}_{n_{\text{dof}}^{f,e} \times 1}, \\
    \frac{\partial^2 a_h^e(\xi, t)}{\partial X^2} &= \sum_{a=1}^{n_{\text{dof}}^{f,e}} H_a^{u_f}(\xi) \ddddot{d}_{a,f}^e(t) = \left\{ H^{e,u_f} \right\}_{1 \times n_{\text{dof}}^{f,e}} \cdot \left\{ \ddddot{d}_f^e \right\}_{n_{\text{dof}}^{f,e} \times 1}.
\end{align*}
$$

(71)
Pore fluid pressure discretizations $\pi$ are given as follows:

\[
\begin{align*}
\tilde{p}^h_t(\xi, t) &= \sum_{a=1}^{n_{dof}^{p,t}} N^e_a(\xi) \tilde{\pi}^e_a(t) = \left\{ N^{e,p_t} \right\}_{1 \times n_{dof}^{p,t}}^{n_{dof}^{p,t}} \cdot \left\{ \tilde{\pi}^e \right\}_{n_{dof}^{p,t} \times 1}, \\
\tilde{\dot{p}}^h_t(\xi, t) &= \sum_{a=1}^{n_{dof}^{p,t}} N^e_a(\xi) \dot{\tilde{\pi}}^e_a(t) = \left\{ N^{e,p_t} \right\}_{1 \times n_{dof}^{p,t}}^{n_{dof}^{p,t}} \cdot \left\{ \dot{\tilde{\pi}}^e \right\}_{n_{dof}^{p,t} \times 1}, \\
\tilde{\ddot{p}}^h_t(\xi, t) &= \sum_{a=1}^{n_{dof}^{p,t}} N^e_a(\xi) \ddot{\tilde{\pi}}^e_a(t) = \left\{ N^{e,p_t} \right\}_{1 \times n_{dof}^{p,t}}^{n_{dof}^{p,t}} \cdot \left\{ \ddot{\tilde{\pi}}^e \right\}_{n_{dof}^{p,t} \times 1},
\end{align*}
\]

(72)

\[
\begin{align*}
\frac{\partial p^h_t(\xi, t)}{\partial X} &= \sum_{a=1}^{n_{dof}^{p,t}} B^e_a(\xi) \pi^e_a(t) = \left\{ B^{e,p_t} \right\}_{1 \times n_{dof}^{p,t}}^{n_{dof}^{p,t}} \cdot \left\{ \pi^e \right\}_{n_{dof}^{p,t} \times 1}, \\
\frac{\partial \dot{p}^h_t(\xi, t)}{\partial X} &= \sum_{a=1}^{n_{dof}^{p,t}} B^e_a(\xi) \dot{\pi}^e_a(t) = \left\{ B^{e,p_t} \right\}_{1 \times n_{dof}^{p,t}}^{n_{dof}^{p,t}} \cdot \left\{ \dot{\pi}^e \right\}_{n_{dof}^{p,t} \times 1}, \\
\frac{\partial \ddot{p}^h_t(\xi, t)}{\partial X} &= \sum_{a=1}^{n_{dof}^{p,t}} B^e_a(\xi) \ddot{\pi}^e_a(t) = \left\{ B^{e,p_t} \right\}_{1 \times n_{dof}^{p,t}}^{n_{dof}^{p,t}} \cdot \left\{ \ddot{\pi}^e \right\}_{n_{dof}^{p,t} \times 1}.
\end{align*}
\]

The weighting functions for solid skeleton displacement $d$ and their interpolations (including gradients) are given as follows:

\[
\begin{align*}
w^{u,s}^c(\xi) &= \left\{ N^{e,u} \right\}_{1 \times n_{dof}^{s,c}}^{n_{dof}^{s,c}} \cdot \left\{ \mathbf{c}^{u,s} \right\}_{n_{dof}^{s,c} \times 1}^{T}, \\
\frac{\partial w^{u,s}^c(\xi, t)}{\partial X} &= \left\{ B^{e,u} \right\}_{1 \times n_{dof}^{s,c}}^{n_{dof}^{s,c}} \cdot \left\{ \mathbf{c}^{u,s} \right\}_{n_{dof}^{s,c} \times 1}^{T} \cdot \left\{ B^{e,u} \right\}_{n_{dof}^{s,c} \times 1}^{T}, \\
\frac{\partial^2 w^{u,s}^c(\xi, t)}{\partial X^2} &= \left\{ H^{e,u} \right\}_{1 \times n_{dof}^{s,c}}^{n_{dof}^{s,c}} \cdot \left\{ \mathbf{c}^{u,s} \right\}_{n_{dof}^{s,c} \times 1}^{T} \cdot \left\{ H^{e,u} \right\}_{n_{dof}^{s,c} \times 1}^{T}.
\end{align*}
\]

(73)

The weighting functions for pore fluid displacement $d_t$ and their interpolations (in-
cluding gradients) are given as follows:

\[
\begin{align*}
  w^{ue} \left( \xi \right) &= \{N^{u,e}\} \cdot \{c^{u,e}\} = \{N^{u,e}\}^T, \\
  \frac{\partial w^{ue} \left( \xi, t \right)}{\partial X} &= \{B^{u,e}\} \cdot \{c^{u,e}\} = \{B^{u,e}\}^T, \\
  \frac{\partial^2 w^{ue} \left( \xi, t \right)}{\partial X^2} &= \{H^{u,e}\} \cdot \{c^{u,e}\} = \{H^{u,e}\}^T, \\
\end{align*}
\]

(74)

The weighting functions for pore fluid pressure \(\pi\) and their interpolations (including gradients) are given as follows:

\[
\begin{align*}
  u^{pe} \left( \xi \right) &= \{N^{p,e}\} \cdot \{c^{p,e}\} = \{N^{p,e}\}^T, \\
  \frac{\partial u^{pe} \left( \xi, t \right)}{\partial X} &= \{B^{p,e}\} \cdot \{c^{p,e}\} = \{B^{p,e}\}^T, \\
  \frac{\partial^2 u^{pe} \left( \xi, t \right)}{\partial X^2} &= \{H^{p,e}\} \cdot \{c^{p,e}\} = \{H^{p,e}\}^T. \\
\end{align*}
\]

(75)

### 3.4 Numerical Integration

After applying the Galerkin approximation\(^{44}\) to the coupled variational equations in Section 3 substituting interpolations and their derivatives in Section 3 applying boundary conditions at the nodes, and assembling the FE equations, the general coupled system of matrix-vector equations resembles the following nonlinear form:

\[
M \ddot{x} + C \dot{x} + F^{INT}(\ddot{x}, x) = F^{EXT},
\]

(76)

where \(M\) is the mass matrix, \(C\) is the viscous matrix, \(F^{INT}\) is the nonlinear internal “force” vector, and \(F^{EXT}\) is the vector of applied external forces and fluxes for the full coupled variational form. Similarly, the accelerations, velocities, and
displacements are given by the global DOF vectors $\ddot{x}$, $\dot{x}$, and $x$, respectively, as

$$
\begin{align*}
\ddot{x} &= \begin{bmatrix} \ddot{d} \\ \ddot{d}_f \\ \ddot{\pi} \end{bmatrix}, \\
\dot{x} &= \begin{bmatrix} \dot{d} \\ \dot{d}_f \\ \dot{\pi} \end{bmatrix}, \\
x &= \begin{bmatrix} d \\ d_f \\ \pi \end{bmatrix}
\end{align*}
$$

where $d$, $d_f$, and $\pi$ are the global nodal DOFs of solid skeleton displacement, pore fluid displacement (part of the time integration procedure, not used in any of the balance equations), and pore fluid pressure, respectively.

### 3.4.1 Newmark-beta Integrators

For the dynamic equations that retain inertia terms, we apply the Newmark-beta (NB) method\textsuperscript{44,45} and a nonlinear solver (Newton-Raphson method; for details, refer to Irwin et al.\textsuperscript{30}) for solving Eq. 76 wherein

$$
\begin{align*}
M \ddot{x}_{n+1} + C \dot{x}_{n+1} + F_{\text{INT}}(\ddot{x}_{n+1}, x_{n+1}) &= F_{\text{EXT}}^{n+1}, \\
x_{n+1} &= x_n + \Delta t \dot{x}_n + \frac{(\Delta t)^2}{2} [(1 - 2\beta) \ddot{x}_n + 2\beta \ddot{x}_{n+1}], \\
\dot{x}_{n+1} &= \dot{x}_n + \Delta t [(1 - \gamma) \ddot{x}_n + \gamma \ddot{x}_{n+1}].
\end{align*}
$$

Here $(\bullet)_{n+1}$ implies a quantity to be solved or updated at current time $t_{n+1}$, $(\bullet)_n$ implies a quantity known at previous time $t_n$, $\beta$ and $\gamma$ are integration parameters, and the time increment $\Delta t = t_{n+1} - t_n$ may be variable or held constant during the time marching solution.

The predictors are written as

$$
\begin{align*}
\ddot{x}_{n+1} &= x_n + \Delta t \dot{x}_n + \frac{(\Delta t)^2}{2} (1 - 2\beta) \ddot{x}_n, \\
\dot{\ddot{x}}_{n+1} &= \dot{x}_n + \Delta t (1 - \gamma) \ddot{x}_n,
\end{align*}
$$

such that the correctors are

$$
\begin{align*}
x_{n+1} &= \ddot{x}_{n+1} + \beta (\Delta t)^2 \ddot{x}_{n+1}, \\
\dot{x}_{n+1} &= \dot{\ddot{x}}_{n+1} + \gamma \Delta t \ddot{x}_{n+1}.
\end{align*}
$$

Writing in residual form for solution via the Newton-Raphson method, this allows
us to solve for the accelerations \( \ddot{x}_{n+1} \) at the next time step \( t_{n+1} \) as follows:

\[
R(\ddot{x}_{n+1}) = M\ddot{x}_{n+1} + C\dot{x}_{n+1} + F^{\text{INT}}(\ddot{x}_{n+1}, x_{n+1}) - F^{\text{EXT}} = 0 \quad (81)
\]

In Eq. 81, the internal forces are nonlinear, therefore requiring us to employ a non-linear solver (e.g., the Newton-Raphson method).

With the linearized equations, we can construct the coupled linear equations to solve at each current iteration \( k + 1 \) as

\[
\begin{bmatrix}
K_{u,u} & K_{u,uf} & K_{u,pf} \\
K_{uf,u} & K_{uf,uf} & K_{uf,pf} \\
K_{pf,u} & K_{pf,uf} & K_{pf,pf}
\end{bmatrix}^k \begin{bmatrix}
\delta \ddot{d} \\
\delta \dot{d}_f \\
\delta \dot{\pi}
\end{bmatrix} = \begin{bmatrix}
-R_u \\
-R_{uf} \\
-R_{pf}
\end{bmatrix}^k
\]

(82)

The “stiffness” matrices in Eq. 82 remain mostly unchanged from those given in Irwin et al.\textsuperscript{29,30} Minor differences arise with the inclusion of the pore fluid extra stress. Specifically, variations of the pore fluid extra stress tensor and the divergence of the pore fluid extra stress tensor contribute to block matrices \( K_{u,u}, K_{u,uf}, K_{uf,u}, K_{pf,u}, K_{pf,uf} \). The derivation of the Gateaux derivative of the pore fluid extra stress tensor, which contributes to block matrices \( K_{u,u}, K_{u,uf} \), proceeds as follows:

\[
\delta G^{\text{INT}} = \delta \left( \frac{n^f}{J} \left( \frac{\beta \Delta t^2}{\partial X} \frac{\partial (\delta a)}{\partial X} + n^f (\gamma \Delta t) \frac{\partial (\delta a_f)}{\partial X} \right) + \left( \frac{n^s}{J} \left( \frac{\beta \Delta t^2}{\partial X} \frac{\partial (\delta a)}{\partial X} + n^f (\gamma \Delta t) \frac{\partial (\delta a_f)}{\partial X} \right) \right) \right),
\]

(83)

where we assume pore fluid bulk viscosity \( \kappa_f \) and pore fluid shear viscosity \( \eta_f \) are not functions of the independent variables \( u, u_f, p_f \). Thus, \( \delta G^{\text{INT}}_5 \) is

\[
\delta G^{\text{INT}}_5 = \int_0^{X=H} n^f \left( \frac{\beta \Delta t^2}{\partial X} \frac{\partial (\delta a)}{\partial X} + n^f (\gamma \Delta t) \frac{\partial (\delta a_f)}{\partial X} \right) (\kappa_f + 2\eta_f) A dX. \quad (84)
\]

Divergence of the pore fluid extra stress tensor simplifies to the following with the 1-D uniaxial strain assumption:

\[
\left[ \frac{\partial n^f}{\partial X} \frac{\partial v_f}{\partial X} + n^f \frac{\partial^2 v_f}{\partial X^2} \right] (\kappa_f + 2\eta_f) F_{11}^{-2}.
\]

(85)
The Gateaux derivatives of new variables are given as follows:

\[
\delta \left( \frac{\partial n^f}{\partial X} \right) = \delta \left( n^s \frac{\partial^2 u}{\partial X^2} F_{11}^{-2} \right) = (\beta \Delta t^2) \left( -\frac{n^s}{J} \frac{\partial^2 u}{\partial X^2} F_{11}^{-2} \frac{\partial (\delta a)}{\partial X} + n^s \frac{\partial F_{11}^{-2} (\delta a)}{\partial X} - 2 \frac{n^s}{J} \frac{\partial^2 u}{\partial X^2} \frac{\partial (\delta a)}{\partial X} \right) = (\beta \Delta t^2) \left( n^s F_{11}^{-2} \frac{\partial^2 (\delta a)}{\partial X} - 3 \frac{n^f}{J} \frac{\partial (\delta a)}{\partial X} \right),
\]

\[
\delta \left( \frac{\partial v_t}{\partial X} \right) = (\gamma \Delta t) \frac{\partial (\delta a_t)}{\partial X},
\]

\[
\delta \left( \frac{\partial^2 v_t}{\partial X^2} \right) = (\gamma \Delta t) \frac{\partial^2 (\delta a_t)}{\partial X^2}.
\]

(86)

Thus, the variation of the divergence of the pore fluid extra stress term, which contributes to block matrices \( K_{u_t,u}, K_{u_t,u_f} \), is

\[
\delta \left( \frac{\partial \sigma_{11(E)}^f}{\partial X} \right) = (\kappa_f + 2\eta_f) \left( \left[ (n^s - n^f) \frac{\partial^2 v_t}{\partial X^2} - 4 \frac{\partial n^f}{\partial X} \frac{\partial v_t}{\partial X} \right] F_{11}^{-2} (\beta \Delta t^2) \frac{\partial (\delta a)}{\partial X} + (\gamma \Delta t) F_{11}^{-1} \left[ \frac{\partial n^f}{\partial X} \frac{\partial (\delta a_t)}{\partial X} + n^f \frac{\partial^2 (\delta a_t)}{\partial X^2} \right] \right). \]

(87)

With that, \( \delta L_5^{IN} \) is

\[
\delta L_5^{IN} = \int_0^X w_u (\kappa_f + 2\eta_f) \left( \left[ (n^s - n^f) \frac{\partial^2 v_t}{\partial X^2} - 4 \frac{\partial n^f}{\partial X} \frac{\partial v_t}{\partial X} \right] F_{11}^{-2} (\beta \Delta t^2) \frac{\partial (\delta a)}{\partial X} + (\gamma \Delta t) F_{11}^{-1} \left[ \frac{\partial n^f}{\partial X} \frac{\partial (\delta a_t)}{\partial X} + n^f \frac{\partial^2 (\delta a_t)}{\partial X^2} \right] \right) A dX.
\]

(88)

The Gateaux derivative of the divergence of the pore fluid extra stress term that is scaled by porosity, hydraulic conductivity, and inverse deformation gradient, is used
in variation of $\mathcal{H}^\text{INT}_2$, $\mathcal{H}^\text{INT}_5$, and is given by

$$
\delta \left( \frac{\dot{k}}{n^l} \frac{\partial \sigma^f_{11(E)}}{\partial X} F^{-1}_{11} \right) = \left( \frac{\dot{k}}{n^l} F^{-2}_{11} \frac{\partial \sigma^f_{11(E)}}{\partial X} \left[ \frac{3}{n^l} \left( \frac{2n^f}{1 - (n^l)^2} \right) - \frac{1}{n^l} \right] - 2 \right)
+ (\kappa_t + 2\eta_t) \left[ \frac{n^s \partial^2 v_t}{J \partial X^2} - \frac{3 \partial n^f \partial v_t}{J \partial X} \right] (\beta \Delta t^2) \frac{\partial (\delta a)}{\partial X}

+ \frac{\dot{k}}{n^l} J \frac{n^s v_t}{F^{-3}_{11}(\kappa_t + 2\eta_t) (\beta \Delta t^2) \frac{\partial^2 (\delta a)}{\partial X^2}}

+ \frac{\dot{k}}{n^l} F^{-2}_{11}(\gamma \Delta t) \left( \frac{\partial n^f}{\partial X} \frac{\partial (\delta a_t)}{\partial X} + n^f \frac{\partial^2 (\delta a_t)}{\partial X^2} \right)

(89)
$$

Thus, $\delta H^\text{INT}_2$ becomes

$$
\delta H^\text{INT}_2 \bigg|_{X=H} = \int_0^x w^{pt} \left[ (n^l \bar{V}) - \frac{\dot{k}}{n^l} \frac{\partial p_{rf}}{\partial X} \right] (\beta \Delta t^2) \frac{\partial (\dot{\delta p}_{rf})}{\partial X} - \frac{\dot{k}}{n^l} \frac{\partial p_{rf}}{\partial X} (a_t + g) \frac{\rho R}{K_t^{\eta}}

\times (\beta \Delta t^2) \frac{\partial^2 \delta p_{rf}}{\partial X^2} + \frac{\dot{k}}{n^l} \frac{\partial \sigma^f_{11(E)}}{\partial X} \left[ \frac{3}{n^l} \left( \frac{2n^f}{1 - (n^l)^2} \right) - \frac{1}{n^l} \right] - 2 \right]

+ (\kappa_t + 2\eta_t) \left[ \frac{n^s \partial^2 v_t}{J \partial X^2} - \frac{3 \partial n^f \partial v_t}{J \partial X} \right] (\beta \Delta t^2) \frac{\partial (\delta a)}{\partial X}

- \frac{\dot{k}}{n^l} \frac{n^s \partial v_t}{J \partial X} F^{-3}_{11}(\kappa_t + 2\eta_t) (\beta \Delta t^2) \frac{\partial^2 (\delta a)}{\partial X^2} - \frac{\dot{k}}{n^l} \frac{\partial p_{rf}}{\partial X} \frac{\partial R}{K_t^{\eta}}

- \frac{\dot{k}}{n^l} \frac{\partial v_t}{J \partial X} F^{-2}_{11}(\gamma \Delta t) \left( \frac{\partial n^f}{\partial X} \frac{\partial (\delta a_t)}{\partial X} + n^f \frac{\partial^2 (\delta a_t)}{\partial X^2} \right)

\frac{A}{K_t^{\eta}} \, dX \bigg) . \quad (90)
$$
Next, \( \delta H_5^{\text{INT}} \) is given as
\[
\delta H_5^{\text{INT}} = - \int_0^H \frac{\partial w}{\partial X} \left( \frac{\dot{k}}{n^t} F^{-2}_{11} \left[ \frac{\partial \sigma_{11}^{\text{f}}(E)}{\partial X} \left( n^s \left[ \left( \frac{3}{n^t} - \frac{2n^f}{1 - (n^f)^2} \right) - \frac{1}{n^t} \right] - 2 \right) \right.ight.
\]
\[
+ (\kappa_f + 2\eta_f) \left( n^s \frac{\partial^2 v_f}{\partial X^2} - 3 \frac{\partial n^f}{\partial X} \frac{\partial v_f}{\partial X} \right) \frac{(\beta \Delta t^2)}{\partial X} \frac{\partial (\delta a)}{\partial X}
\]
\[
+ \frac{\dot{k}}{n^t} \left( \frac{n^s \partial^2 v_f}{J} F^{-3}_{11}(\kappa_f + 2\eta_f) (\beta \Delta t^2) \frac{\partial^2 (\delta a)}{\partial X^2} \right)
\]
\[
+ \frac{\dot{k}}{n^t} \left( n^s \frac{\partial (\delta a_e)}{\partial X} + n^t \frac{\partial^2 (\delta a_e)}{\partial X^2} \right) \right) \right) A dX .
\]
\[(91)\]

Following the procedure described in Irwin et al.,\(^{30}\) the global residual for the solid skeleton displacement is given by
\[
c^{u,T} \cdot R_u = \mathcal{G} = \mathcal{G}_1^{\text{INT},h} + \mathcal{G}_2^{\text{INT},h} + \mathcal{G}_3^{\text{INT},h} + \mathcal{G}_4^{\text{INT},h} + \mathcal{G}_5^{\text{INT},h} - \mathcal{G}^{\text{EXT},h} = 0 ,
\]
\[(92)\]
which remains unchanged from Irwin et al.,\(^{29,30}\) with the exception of
\[
\mathcal{G}_5^{\text{INT},h} = \mathcal{A} \left\{ c^{u,e} \right\}^T \left( \int_{-1}^{1} \left\{ B^{e,u} \right\}^T P^{f,h_e}_{11(E)} A_J^e d\xi \right).
\]
\[(93)\]

The global residual for the pore fluid displacement is given by
\[
c^{u_f,T} \cdot R_{u_f} = \mathcal{T} = \mathcal{T}_1^{\text{INT},h} + \mathcal{T}_2^{\text{INT},h} + \mathcal{T}_3^{\text{INT},h} + \mathcal{T}_4^{\text{INT},h} + \mathcal{T}_5^{\text{INT},h} = 0 ,
\]
\[(94)\]
which remains unchanged from Irwin et al.,\(^{29,30}\) with the exception of
\[
\mathcal{T}_5^{\text{INT},h} = \mathcal{A} \left\{ c^{u_f,e} \right\}^T \left( \int_{-1}^{1} \left\{ N^{e,u} \right\}^T \frac{\partial P^{f,h_e}_{11(E)}}{\partial X} A_J^e d\xi \right).
\]
\[(95)\]
The global residual for the pore fluid pressure is given by

\[ c_{pf}^T R_{pf} = H^h = H_1^{INT,h} + H_2^{INT,h} + H_3^{INT,h} + H_4^{INT,h} + H_5^{INT,h} - H_1^{EXT,h} = 0, \]  

(96)

which remains unchanged from Irwin et al.,\textsuperscript{29,30} with the exception of

\[ H_2^{INT,h} = \mathbf{A} \left\{ \mathbf{c}_{pf,e} \right\}_{1 \times n_{pf,e}}^T \left( \int_{-1}^{1} \left\{ \mathbf{N}^{e,pt} \right\}_{n_{pf,e} \times 1}^T \frac{1}{K_1} \left( \frac{\partial p_{pf}^h}{\partial X} \right) \mathbf{A}_{j,e} d\xi \right), \]

(97)

\[ H_5^{INT,h} = \mathbf{A} \left\{ \mathbf{c}_{pf,e} \right\}_{1 \times n_{pf,e}}^T \left( -\int_{-1}^{1} \left\{ \mathbf{B}^{e,pt} \right\}_{n_{pf,e} \times 1}^T \frac{\mathbf{k}^h}{n_{t,he}} \frac{\partial \mathbf{\sigma}_{11}^{h,e}}{\partial X} \left( F_{11}^h \right)^{-1} \mathbf{A}_{j,e} d\xi \right), \]

where the pore fluid extra stress is embedded within the discretized Darcy velocity in \( H_2^{INT,h} \). When pressure stabilization is enabled, an additional term \( H_{stab} \) is added to the left-hand side of Eq. 96 and is defined as

\[ H_{stab} = \mathbf{A} \left\{ \mathbf{c}_{pf,e} \right\}_{1 \times n_{pf,e}}^T \left( \int_{-1}^{1} \left\{ \mathbf{B}^{e,pt} \right\}_{n_{pf,e} \times 1}^T \alpha_{stab} \frac{\partial p_{pf}^h}{\partial X} \mathbf{A}_{j,e} d\xi \right), \]

(98)

Recall that the tangent matrix for each iteration must be of the form

\[ 0 = R^k = \begin{bmatrix} K_{u,u} & K_{u,u1} & K_{u,pt} \\ K_{u1,u} & K_{pt,u} & K_{pt,pt} \end{bmatrix} \begin{bmatrix} \delta \mathbf{d} \\ \delta \mathbf{d}_f \\ \delta \mathbf{\pi} \end{bmatrix} \]

(99)

Block stiffness matrices remain unchanged from Irwin et al.,\textsuperscript{29,30} with the following
Specifically, the following new additions (denoted by \( i = 5 \) in all of Eq. 100, as well as \( i = 2 \) in Eq. 100\(_{b,h}\)) are made to account for the pore fluid extra stress:

\[
\begin{align*}
\left[ k_{u,u}^{\text{INT},e} \right] &= \int_{-1}^{1} \frac{\partial v_{f,e}^{h} (n^{s,h,e} - n^{f,h,e}) (\kappa_{f} + 2\eta_{f}) (F_{11}^{h,e})^{-2} (\beta \Delta t)^{2}}{\partial X} \left( B_{e,u}^{e} \right)_{\text{INT}}^{T} \left( B_{e,u}^{e} \right)_{\text{INT}} A f^{e} d\xi, \\
\left[ k_{u,u,l}^{\text{INT},e} \right] &= \int_{-1}^{1} \frac{\partial v_{f,e}^{h} (n^{s,h,e} - n^{f,h,e}) (\kappa_{f} + 2\eta_{f}) (F_{11}^{h,e})^{-2} (\beta \Delta t)^{2}}{\partial X} \left( B_{e,u}^{e} \right)_{\text{INT}}^{T} \left( B_{e,u}^{e} \right)_{\text{INT}} A f^{e} d\xi, \\
\left[ k_{u,u,l}^{\text{INT},e} \right] &= \int_{-1}^{1} \frac{\partial v_{f,e}^{h} (n^{s,h,e} - n^{f,h,e}) (\kappa_{f} + 2\eta_{f}) (F_{11}^{h,e})^{-2} (\beta \Delta t)^{2}}{\partial X} \left( B_{e,u}^{e} \right)_{\text{INT}}^{T} \left( B_{e,u}^{e} \right)_{\text{INT}} A f^{e} d\xi, \\
\left[ k_{u,u,l}^{\text{INT},e} \right] &= \int_{-1}^{1} \frac{\partial v_{f,e}^{h} (n^{s,h,e} - n^{f,h,e}) (\kappa_{f} + 2\eta_{f}) (F_{11}^{h,e})^{-2} (\beta \Delta t)^{2}}{\partial X} \left( B_{e,u}^{e} \right)_{\text{INT}}^{T} \left( B_{e,u}^{e} \right)_{\text{INT}} A f^{e} d\xi.
\end{align*}
\]
\[
\begin{align*}
[k_{u_t,u_t}^{\text{INT},e}] &= - \int_{1}^{\frac{1}{n_{t,1}^{e}}} \left\{ N_{e,u_t}^{e} \right\}^{T} \left( \frac{\partial n_{t,1}^{e}}{\partial X} \left\{ B_{e,u_t}^{e} \right\} + n_{t,1}^{e} \left\{ H_{e,u_t}^{e} \right\} \right) \left( \kappa_{t} + 2\eta_{t} \right) (F_{11}^{h_{t}})^{2} (\gamma \Delta t) A_{j}^{e} d\xi,
\end{align*}
\]

\[
\begin{align*}
[k_{p_t,u_t}^{\text{INT},e}] &= \int_{1}^{\frac{1}{n_{t,1}^{e}} \times n_{x,1}^{e}} \left\{ N_{e,p_t}^{e} \right\}^{T} \left( \left[ \frac{3}{n_{p,1}^{e} - \left( n_{t,1}^{e} \right)^{2}} \right] \left( n_{p,1}^{e} \right)^{2} n_{s,1}^{e} \right) \left( \frac{3}{n_{p,1}^{e} - \left( n_{t,1}^{e} \right)^{2}} - \frac{1}{n_{t,1}^{e}} \right) - 2 \right) \left\{ B_{e,u_t}^{e} \right\} \frac{1}{n_{t,1}^{e}} d\xi
\end{align*}
\]

\[
\begin{align*}
[k_{p_t,u_t}^{\text{INT},e}] &= \int_{1}^{\frac{1}{n_{t,1}^{e}} \times n_{x,1}^{e}} \left\{ N_{e,p_t}^{e} \right\}^{T} \left( \left[ \frac{3}{n_{p,1}^{e} - \left( n_{t,1}^{e} \right)^{2}} \right] \left( n_{p,1}^{e} \right)^{2} n_{s,1}^{e} \right) \left( \frac{3}{n_{p,1}^{e} - \left( n_{t,1}^{e} \right)^{2}} - \frac{1}{n_{t,1}^{e}} \right) - 2 \right) \left\{ B_{e,u_t}^{e} \right\} \frac{1}{n_{t,1}^{e}} d\xi
\end{align*}
\]

\[
\begin{align*}
[k_{H_{t},e}] &= \int_{1}^{\frac{1}{n_{t,1}^{e}} \times n_{x,1}^{e}} \left\{ N_{e,H_{t}}^{e} \right\}^{T} \left( \rho_{H_{t}}^{R} \left\{ N_{e,H_{t}}^{e} \right\} \right) \rho_{H_{t}}^{R} \left\{ N_{e,H_{t}}^{e} \right\} \left( \frac{3}{n_{p,1}^{e} - \left( n_{t,1}^{e} \right)^{2}} - \frac{1}{n_{t,1}^{e}} \right) - 2 \right) \left\{ B_{e,u_t}^{e} \right\} \frac{1}{n_{t,1}^{e}} d\xi
\end{align*}
\]
\[
\begin{bmatrix}
H_{p_t, u_t}^{\text{INT}, e}
\end{bmatrix}_e^{n_{\text{def}, e} \times n_{\text{def}, e}} = - \int_{-1}^{1} \left\{ B_{e, p_t}^{e, e} \right\}^T \left\{ \frac{1}{n_{t, h}^e} \frac{\partial n_{t, h}^e}{\partial X} \begin{bmatrix} B_{e, u_t}^{e, e} \\ H_{e, u_t}^{e, e} \end{bmatrix} + \begin{bmatrix} H_{e, u_t}^{e, e} \end{bmatrix} \right\} \left( \kappa_f + 2\eta_e \right) \frac{k_{h}^{e}}{(F_{11}^h)^2} \gamma \Delta t A_j^e. \tag{101}
\]

### 3.4.2 Runge-Kutta Integrators

For explicit time integration of the matrix-vector equations, we apply a generalized adaptive time-stepping Runge-Kutta method (specifically, the Runge-Kutta Cash-Karp scheme,\(^{46}\) henceforth referred to as “RKFNC”) for solving Eq. 76, which involves transforming the second-order ordinary differential equations (ODEs) into first-order ODEs by variable substitution:

\[
z := \begin{bmatrix} z_x \\ z_{\dot{x}} \end{bmatrix} = \begin{bmatrix} x \\ \dot{x} \end{bmatrix}, \tag{102}
\]

such that

\[
\dot{z} := \begin{bmatrix} \dot{z}_x \\ \dot{z}_{\dot{x}} \end{bmatrix} = \begin{bmatrix} \dot{x} \\ \ddot{x} \end{bmatrix}. \tag{103}
\]

For a general nonlinear multi-degree-of-freedom ODE

\[
\dot{z} = f(t, z), \tag{104}
\]

where \(f(t, z)\) is in general a nonlinear equation in terms of time \(t\) and unknown variable \(z\). For a general Runge-Kutta method of \(m\)th order, the intermediate stages \(k_i\) are defined as follows using standard notation for a Butcher table:

\[
k_i = f \left( t_n + c_i \Delta t, z(t_n) + \Delta t \sum_{j=1}^{i-1} a_{ij} k_j \right). \tag{105}
\]

The higher-order solution is given by

\[
z^m(t_{n+1}) = z(t_n) + \Delta t \sum_{i=1}^{m+1} b_i^m k_i, \tag{106}
\]
and the lower-order solution is given by

\[ z^{m-1}(t_{n+1}) = z(t_n) + \Delta t \sum_{i=1}^{m} b^m_{i} k_i, \]  

(107)

where the \( b^m_i \) coefficients are different from the \( b^{m-1}_i \) coefficients; refer to the literature\(^{46,47}\) for specific values. The difference between the higher and lower order solutions allows us to define a truncation error

\[ \epsilon_{TE} := \left| z^m(t_{n+1}) - z^{m-1}(t_{n+1}) \right|_2. \]  

(108)

Note that in comparison to prior work,\(^{28–30}\) here we define the truncation error with the \( L_2 \) norm rather than the \( L_\infty \) norm because the former has better performance with the new Q3H-Q3H-P1 element than the latter. The adapted time step \( \Delta t^* \) is typically adjusted as follows:

\[ \Delta t^* = SF \times \left( \frac{\epsilon_a}{\epsilon_{TE}} \right)^{1/(m-1)} \Delta t, \]  

where \( SF \) is a safety factor, typically set to 0.9, and \( \epsilon_a \) is a user-defined absolute tolerance, typically set to \( \epsilon_a \in [10^{-8}, 10^{-2}] \). If the absolute error

\[ \left( \frac{\epsilon_{TE}}{\epsilon_a} \right)^{1/(m-1)} < 1, \]  

(110)

then the solution \( z^m \) is accepted with \( \Delta t_{n+1} \leftarrow \Delta t^* \). Otherwise, the stages \( k_i \) are recomputed at time \( t_n \) with \( \Delta t_n \leftarrow \Delta t^* \), new solutions are computed, and a new absolute error is computed until the condition defined by Eq. 110 is met.

The Runge-Kutta integrators transform the general solution variables given by Eq. 104 to

\[
\begin{bmatrix}
\dot{z}_u \\
\dot{z}_v \\
\dot{z}_{u_i} \\
\dot{z}_{v_i} \\
\dot{z}_{p_i}
\end{bmatrix} = \begin{bmatrix}
\dot{f}_u(t, z) \\
\dot{f}_v(t, z) \\
\dot{f}_{u_i}(t, z) \\
\dot{f}_{v_i}(t, z) \\
\dot{f}_{p_i}(t, z)
\end{bmatrix},
\]  

(111)
such that

\[
\begin{align*}
\{ z \} &= \begin{bmatrix} d \\ \dot{d} \\ d_t \\ \dot{d}_t \\ \pi \end{bmatrix}, \quad \dot{z} = \begin{bmatrix} \dot{d} \\ \ddot{d} \\ \dot{d}_t \\ \ddot{d}_t \end{bmatrix}.
\end{align*}
\] (112)

The FE formulation for the balance of momentum of the mixture, variational Eq. 54, is written in block-matrix form as

\[
\begin{bmatrix} R_u \end{bmatrix}_{n_s \times 1} = 0,
\] (113)

where the global residual for the solid skeleton displacement is given as

\[
c^{u,T} \cdot R_u = G^h = G_1^{INT,h} + G_2^{INT,h} + G_3^{INT,h} + G_4^{INT,h} + G_5^{INT,h} - G^{EXT,h} = 0.
\] (114)

The weighted residual remains unchanged from Irwin et al., with the exception of

\[
G_5^{INT,h} = A_e \begin{bmatrix} e^{u,e} \end{bmatrix}_{1 \times n^{s,e}_{dof}}^T \begin{bmatrix} f^{G^{INT,e}} \end{bmatrix}_{n^{s,e}_{dof} \times 1}.
\] (115)

The FE formulation for the balance of mass, variational Eq. 49, is written in block-matrix form as

\[
\begin{bmatrix} R_{pf} \end{bmatrix}_{n_p \times 1} = 0,
\] (116)

where the global residual for the pore fluid pressure is given as

\[
c^{p,f,T} \cdot R_{pf} = H^h = H_1^{INT,h} + H_2^{INT,h} + H_3^{INT,h} + H_4^{INT,h} + H_5^{INT,h} - H_1^{EXT,h} = 0.
\] (117)
The weighted residual remains unchanged from Irwin et al.,\textsuperscript{29,30} with the exception of

\begin{align}
\mathcal{H}_2^{\text{INT},h} &= \mathbf{A} \begin{bmatrix} e \end{bmatrix}_{1 \times n_{\text{dof}}^e}^T \begin{bmatrix} \mathbf{c}^{\gamma} \end{bmatrix}_{n_{\text{dof}}^e \times 1} \begin{bmatrix} \mathbf{f}_2^{\text{INT},e} \end{bmatrix} , \\
\mathcal{H}_5^{\text{INT},h} &= \mathbf{A} \begin{bmatrix} e \end{bmatrix}_{1 \times n_{\text{dof}}^e}^T \begin{bmatrix} \mathbf{c}^{\gamma} \end{bmatrix}_{n_{\text{dof}}^e \times 1} \begin{bmatrix} \mathbf{f}_5^{\text{INT},e} \end{bmatrix} ,
\end{align}

where the pore fluid extra stress is embedded within the discretized Darcy velocity in \( \mathbf{f}_5^{\text{INT},e} \).

The FE formulation for the balance of momentum of the fluid, variational Eq. 60, is written in block-matrix form

\begin{equation}
\begin{bmatrix} R_{uf} \end{bmatrix}_{n_f \times 1} = 0 ,
\end{equation}

where the global residual for the pore fluid displacement is given as

\begin{equation}
\mathbf{c}^{\gamma} \cdot R_{uf} = \mathbf{T}^{h} = \mathbf{T}_1^{\text{INT},h} + \mathbf{T}_2^{\text{INT},h} + \mathbf{T}_3^{\text{INT},h} + \mathbf{T}_4^{\text{INT},h} + \mathbf{T}_5^{\text{INT},h} = 0 .
\end{equation}

The weighted residual remains unchanged from Irwin et al.,\textsuperscript{29,30} with the exception of

\begin{align}
\mathcal{I}_5^{\text{INT},h} &= \mathbf{A} \begin{bmatrix} e \end{bmatrix}_{1 \times n_{\text{dof}}^e}^T \begin{bmatrix} \mathbf{c}^{\gamma} \end{bmatrix}_{n_{\text{dof}}^e \times 1} \begin{bmatrix} \mathbf{f}_5^{\text{INT},e} \end{bmatrix} , \\
\mathbf{f}_5^{\text{INT},e} &= - \int_{-1}^{1} \begin{bmatrix} \mathbf{N}^{\gamma,u} \end{bmatrix}_{n_{\text{dof}}^e \times 1}^T \frac{\partial \mathbf{P}_{11}^{\gamma,h}}{\partial X} A f^e d\xi .
\end{align}
The block system of equations to solve is

\[
\begin{align*}
\begin{pmatrix}
\dot{z} \\
\dot{d}
\end{pmatrix}
&=
\begin{pmatrix}
\begin{pmatrix}
F^{Z1}_{\text{INT}} \\
F^{Z2}_{\text{INT}} \\
F^{Z3}_{\text{INT}} \\
F^{Z4}_{\text{INT}} \\
F^{Z5}_{\text{INT}}
\end{pmatrix} \\
\begin{pmatrix}
F^{H1}_{\text{INT}} \\
F^{H2}_{\text{INT}} \\
F^{H3}_{\text{INT}} \\
F^{H4}_{\text{INT}} \\
F^{H5}_{\text{INT}}
\end{pmatrix} \\
\begin{pmatrix}
F^{C1}_{\text{INT}} \\
F^{C2}_{\text{INT}} \\
F^{C3}_{\text{INT}} \\
F^{C4}_{\text{INT}} \\
F^{C5}_{\text{INT}}
\end{pmatrix}
\end{pmatrix}
-
\begin{pmatrix}
\begin{pmatrix}
\frac{n_{zf}^s}{n_{zf}^s \times 1} \\
\frac{n_{zf}^s}{n_{zf}^s \times 1} \\
\frac{n_{zf}^s}{n_{zf}^s \times 1} \\
\frac{n_{zf}^s}{n_{zf}^s \times 1} \\
\frac{n_{zf}^s}{n_{zf}^s \times 1}
\end{pmatrix} \\
\begin{pmatrix}
\frac{n_{zf}^f}{n_{zf}^f \times 1} \\
\frac{n_{zf}^f}{n_{zf}^f \times 1} \\
\frac{n_{zf}^f}{n_{zf}^f \times 1} \\
\frac{n_{zf}^f}{n_{zf}^f \times 1} \\
\frac{n_{zf}^f}{n_{zf}^f \times 1}
\end{pmatrix}
\end{pmatrix}
-
\begin{pmatrix}
\begin{pmatrix}
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1}
\end{pmatrix} \\
\begin{pmatrix}
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1}
\end{pmatrix}
\end{pmatrix}
\end{pmatrix}
-
\begin{pmatrix}
\begin{pmatrix}
\frac{n_{zf}^s}{n_{zf}^s \times 1} \\
\frac{n_{zf}^s}{n_{zf}^s \times 1} \\
\frac{n_{zf}^s}{n_{zf}^s \times 1} \\
\frac{n_{zf}^s}{n_{zf}^s \times 1} \\
\frac{n_{zf}^s}{n_{zf}^s \times 1}
\end{pmatrix} \\
\begin{pmatrix}
\frac{n_{zf}^f}{n_{zf}^f \times 1} \\
\frac{n_{zf}^f}{n_{zf}^f \times 1} \\
\frac{n_{zf}^f}{n_{zf}^f \times 1} \\
\frac{n_{zf}^f}{n_{zf}^f \times 1} \\
\frac{n_{zf}^f}{n_{zf}^f \times 1}
\end{pmatrix}
\end{pmatrix}
-
\begin{pmatrix}
\begin{pmatrix}
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1}
\end{pmatrix} \\
\begin{pmatrix}
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1} \\
\frac{n_{zf}^p}{n_{zf}^p \times 1}
\end{pmatrix}
\end{pmatrix}
\end{pmatrix}
\end{align*}
\]

where assembled mass matrices and vectors remain unchanged from those given in
Irwin et al.,\textsuperscript{29,30} with the exception of

\[
\begin{align*}
\mathbf{F}^{G\text{INT}}_G &= \mathbf{A}^{n_e} \mathbf{f}^{G\text{INT}}_e, \\
\mathbf{F}^{\tau\text{INT}}_G &= \mathbf{A}^{n_e} \mathbf{f}^{\tau\text{INT}}_e, \\
\mathbf{F}^{H\text{INT}}_G &= \mathbf{A}^{n_e} \mathbf{f}^{H\text{INT}}_e.
\end{align*}
\]  
(123)

4. Results

4.1 Verification

Here, we present results comparing the numerical solutions to an analytical solution developed by de Boer et al.\textsuperscript{48}

A porous column is subjected to an external traction load while its base and sides remain fixed. Values of material and geometric parameters used in this example are given in Tables 1 and 2, respectively, where different load amplitudes and frequencies are included in the latter. The top of the porous column is perfectly drained with reference pressure $p_f(X = H, t) = 0$ atm and subjected to a harmonic loading, as shown in Fig. 3. The analytical solution for this problem was given in Irwin et al.\textsuperscript{28} (originally by de Boer et al.\textsuperscript{48}), and is not repeated here for brevity.

Table 1 Material parameters for the poroelastodynamics verification example. Viscosity values are obtained from Holmes et al.,\textsuperscript{49} assuming a temperature $= 20^\circ$ C.

<table>
<thead>
<tr>
<th>$\lambda$ (MPa)</th>
<th>$\mu$ (MPa)</th>
<th>$\rho_0^{RT}$ (kg/m$^3$)</th>
<th>$\rho_0^{HT}$ (kg/m$^3$)</th>
<th>$n_0^{T}$</th>
<th>$k_0$ (m/s)</th>
<th>$\eta_f$ (mPa-s)</th>
<th>$\kappa_f$ (mPa-s)</th>
</tr>
</thead>
<tbody>
<tr>
<td>5.6</td>
<td>8.4</td>
<td>2700</td>
<td>1000</td>
<td>0.42</td>
<td>$10^{-4}$</td>
<td>1</td>
<td>2.86</td>
</tr>
</tbody>
</table>

Table 2 Geometrical and loading parameters for the poroelastodynamics verification example

<table>
<thead>
<tr>
<th>$H$ (m)</th>
<th>$A$ (m$^2$)</th>
<th>$h_0^0$ (m)</th>
<th>$t_0^{G}$ (kPa)</th>
<th>$\omega$ (rad/s)</th>
</tr>
</thead>
<tbody>
<tr>
<td>10</td>
<td>1</td>
<td>0.1</td>
<td>40</td>
<td>50</td>
</tr>
</tbody>
</table>
Here we compare the results between the analytical solution, the new Q3H-Q3H-P1 element type—with and without the pore fluid extra stress—and the old Q2-Q2-P1 element type, which is restricted to the nearly inviscid assumption. Solid skeleton displacement results (refer to Fig. 4(a)) are improved for the Hermite cubic element, but pore fluid displacement results (refer to Fig. 4(b)) suffer slightly, though remain reasonably accurate. Excellent agreement is observed between pore fluid pressure and solid skeleton extra (effective) stress for all element types. Appearance of improvement of the Hermite cubic element over the standard Lagrange quadratic element arises only since the Hermite cubic element is integrated with 4-point quadrature rather than 3-point quadrature; thus, the quadrature points that are sampled for the Hermite cubic element are closer to the nodes where the analytical solution is defined.
Fig. 4 Verification results for the numerical approximation to the de Boer analytical solution showing (a) solid skeleton displacement, (b) pore fluid displacement, (c) pore fluid pressure, and (d) solid extra stress

Pore fluid extra stress is shown in Fig. 5(a); it is six orders of magnitude smaller than the pore fluid pressure contribution (refer to Fig. 5(b)). This is in agreement with the argument laid out in Section 2 (originally in Ehlers et al.\textsuperscript{36}), where the soil column in this example is essentially a low permeability, rigid, non-deforming solid skeleton (approximate for small strain) and the pore fluid is nearly incompressible (via large pore fluid bulk modulus given in Table1). Furthermore, porosity gradients for this example are inherently small for small strains, rendering that contribution to the divergence of the pore fluid extra stress negligible as well.
4.2 Shockwave Loading of Lung

Of key importance for dynamic injury predictions is how lung tissue deforms under shock loading. In Section 4 we present our findings for a column of lung parenchyma subjected to external traction loadings on the order of milliseconds or less. In all of the simulations, the lung parenchyma column is fixed on its sides and base. In contrast to prior work, the pore fluid pressure boundary condition at the top of the column is allowed to vary, such that the top of the membrane can be represented as both impermeable (i.e., “undrained”) or permeable (i.e., “drained”). The latter might be more experimentally feasible and is an advantage of our model to the one implemented by Clayton et al. For example, one might excise a small section of lung parenchyma, place it in a sleeve such that the sleeve need not enclose the end of excised tissue, and then load it uniaxially wherein the impacting device would need only to maintain contact with a part of the tissue during loading. Material, geometrical, and loading parameters are given in Tables 3 and 4.

We begin our discussion of the effects of the pore fluid extra stress with a simulation that mimics a shock tube test in a laboratory setting. The traction is a linear triangular impulse, hereafter referred to as the Yen impulse, shown in Fig. 6(a), which rises to a maximum overpressure \( t_0^\sigma = 50 \text{ kPa} \) (relative to atmospheric pressure at sea level) at a time \( t_0 = 170 \mu s \). It then decays to \( t^\sigma = 0 \text{ kPa} \) at time \( 2t_0 = t_1 = 340 \mu s \). The time scales and pressure profile were chosen based on an experimental study of rabbit lung exposed to shock tubes by Yen et al. Overpressure amplitude
was chosen arbitrarily, though we note that Yen et al. observed that overpressures greater than 2 psi ($\approx 14$ kPa) resulted in edema of the exposed rabbit lung.

Table 3 Material parameters for multiphase lung parenchyma simulations. Values taken from Clayton et al., Lande and Mitzner, Holmes et al., Rand et al. and Shang et al. Viscosity values for air are interpolated for resting body temperature $37^\circ$ C; bulk modulus, density and bulk viscosity for blood are estimated using values for water at resting body temperature $37^\circ$ C, while shear viscosity is estimated from Rand et al.

<table>
<thead>
<tr>
<th>$K^{acc}$ (kPa)</th>
<th>$G$ (kPa)</th>
<th>$K_s$ (kPa)</th>
<th>$K_f^0$ (kPa)</th>
<th>$\rho_0^R$ (kg/m$^3$)</th>
</tr>
</thead>
<tbody>
<tr>
<td>7.5</td>
<td>3</td>
<td>$2.2 \times 10^6$</td>
<td>140; $2.2 \times 10^6$</td>
<td>1000</td>
</tr>
</tbody>
</table>

<table>
<thead>
<tr>
<th>$\rho_0^R$ (kg/m$^3$)</th>
<th>$n_0^f$</th>
<th>$k_0$ (m$^2$/Pa-s)</th>
<th>$\eta_f$ (mPa-s)</th>
<th>$\kappa_f$ (mPa-s)</th>
</tr>
</thead>
<tbody>
<tr>
<td>1.2; 1000</td>
<td>0.664; 0.99</td>
<td>$10^{-5}$; $6.3 \times 10^{-8}$</td>
<td>$1.89 \times 10^{-2}$; 3</td>
<td>2.03 $\times 10^{-2}$; 1.93</td>
</tr>
</tbody>
</table>

Table 4 Geometrical and loading parameters for multiphase lung parenchyma simulations

<table>
<thead>
<tr>
<th>Overpressure load type</th>
<th>H (cm)</th>
<th>A (cm$^2$)</th>
<th>$h_0$ (cm)</th>
<th>$t_0^G$ (kPa)</th>
<th>$t_0$ (ms)</th>
<th>$t_1$ (ms)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Yen impulse</td>
<td>10</td>
<td>1</td>
<td>0.1</td>
<td>25; 50</td>
<td>0.17</td>
<td>0.34</td>
</tr>
<tr>
<td>Friedlander impulse</td>
<td>10</td>
<td>1</td>
<td>0.1</td>
<td>25; 50</td>
<td>10</td>
<td>N/A</td>
</tr>
</tbody>
</table>

To start, we assume an impermeable membrane of lung parenchyma, in other words, the pore air is allowed to move freely within the column of lung parenchyma, but cannot escape at either end. Displacement profiles between the nearly inviscid (Darcy) and viscous (Darcy-Brinkman, inclusion of pore fluid extra stress) simulations are shown in Fig. 7. It is evident that inclusion of the pore fluid extra stress for this example has a negligible effect on the motion of the lung parenchyma and pore fluid within. This is likely due to how small of a contribution the pore fluid extra stress, shown in Fig. 8(a), has on the total fluid stress, shown in Fig. 8(b). Pore fluid extra stress is three orders of magnitude smaller than the pore fluid pressure for this application.
Fig. 6 (a) Yen impulse traction application (b) Friedlander traction application (c) schematic of multiphase column mesh for examples of lung parenchyma deformations. Note that in (c), for the impermeable membrane, the boundary condition $p_i(H, t) = p_{i0}$ is not set.
Fig. 7 Displacement results from applying the Yen impulse (50 kPa) to the impermeable lung parenchyma for (a) solid skeleton displacement $u(X = H, t)$ (and by extension due to the no-slip/no-penetration condition, $u_f(X = H, t)$), and (b) solid skeleton displacement $u(X = H/2, t)$ and pore fluid displacement $u_f(X = H/2, t)$.
Fig. 8 Pore fluid stress results from applying the Yen impulse (50 kPa) to the impermeable lung parenchyma for (a) pore fluid extra stress at the Gauss point closest to $X = H$, and (b) total pore fluid stress $\sigma_{11}^* = \sigma_{11(E)}^* - n^* p_f$ at the Gauss point closest to $X = H$. 
Next, we assume a permeable membrane (which might be more experimentally feasible), in other words, the pore air is allowed to escape from the top of the column. We note that the prescription of this pore fluid pressure boundary condition restricts the maximum overpressure we are able to apply to the mixture (i.e., the simulations fail for $t_0^a = 50$ kPa; $\Delta t \to 0$ for RKFNC, NB does not converge). Again we see that the pore fluid extra stress has negligible effects on displacements (refer to Fig. 9) and total fluid stress (refer to Fig. 10). However, pore fluid extra stress is only one order of magnitude smaller than total pore fluid stress for the permeable membrane. In Fig. 11, we see how pore fluid extra stress “scales” with pore fluid velocity gradient—denoted by the slope of the velocity contour curve—and porosity, and how each evolve over time. Sampled times are (a) at maximum overpressure loading, (b) when overpressure loading stops, and (c) well after loading has ended. Peak overpressure loading occurs at 170 $\mu$s, but the effects of the shock loading are not observed until later, see, for example, Fig. 11(b) when the impulse ends. In Fig. 11(c) we see that the magnitude of the pore fluid extra stress has greatly dissipated well after load is removed.
Fig. 9 Displacement results from applying the Yen impulse (25 kPa) to the permeable lung parenchyma for (a) solid skeleton displacement $u(X = H, t)$ and pore fluid displacement $u_f(X = H, t)$, and (b) solid skeleton displacement $u(X = H/2, t)$ and pore fluid displacement $u_f(X = H/2, t)$
Fig. 10 Pore fluid stress results from applying the Yen impulse (25 kPa) to the permeable lung parenchyma for (a) pore fluid extra stress at the Gauss point closest to $X = H$, and (b) total pore fluid stress $\sigma_{11} = \sigma_{11(E)} - n^l p_l$ at the Gauss point closest to $X = H$.
Fig. 11 Contours along the length of the mesh for pore fluid extra stress $\sigma_{11}^f(E)$, pore fluid velocity $v_t$ and porosity $n_f$ for permeable lung parenchyma after applying the Yen impulse with 25 kPa maximum overpressure.
Since a permeable membrane induces higher pore fluid extra stress, we now swap
the pore air for pore blood, in others words, we assume the lung is saturated with
blood as the pore fluid, assuming blood can be modeled as a Newtonian fluid. We
adjust the pore fluid density, bulk modulus, and viscosities appropriately (refer to
Table 3). Initial porosity is also increased to $n_f^0 = 0.99$ (from 0.664), and maxi-
mum applied overpressure is increased to $t_0^o = 50$ kPa (from 25 kPa). While the
high initial porosity is not a physically realistic scenario, the magnitude of the pore
fluid extra stress should increase as pore fluid extra stress scales with porosity and
viscosity. This is what is observed in Fig. 12: the pore fluid extra stress accounts
for some oscillations in the total pore fluid stress at the onset of the shock load.
However, the solid extra stress (i.e., the material stress of the lung parenchyma tis-
sue itself) is not affected by the inclusion of the pore fluid extra stress (as shown in
Fig. 13). This may have to do with the fact that the motion of the lung parenchyma
and the pore blood are not affected either (refer to Fig. 14).

In contrast to the example with pore air (refer to Fig. 9), pore fluid (blood) and
solid skeleton (lung parenchyma) displacements are similar. When shear viscos-
ity of the pore fluid is increased, the initial hydraulic conductivity $\hat{k}_0$ is reduced.
Since seepage velocity $(n^f \tilde{v}_f)$ scales with hydraulic conductivity per Darcy’s (and
Darcy-Brinkman’s) law, relative velocity between solid and fluid phases is reduced.
Comparing now the contours of pore fluid extra stress, pore fluid velocity, and
porosity (Fig. 15) for blood-saturated lung parenchyma to that of air-saturated lung
parenchyma (Fig. 11), we see that in the latter the shock wave percolates more
quickly through the mixture than in the former. Velocity of pore air is also greater
in magnitude than for pore blood, even though the blood-saturated lung parenchyma
was subjected to greater maximum overpressure (50 kPa versus 25 kPa). Further-
more, porosity gradients are small for high initial porosity in blood-saturated lung
parenchyma compared to moderate initial porosity in air-saturated lung parenchyma.
In fact, we see that porosity remains high for the duration of the simulation as com-
pared to air-saturated lung parenchyma, where more fluctuations in porosity are
observed.

In addition, because the density of the mixture is higher when pore air is swapped
for pore blood, wave speed is thus also higher; correspondingly, the estimated sta-
bile time-step for explicit integrators (via CFL condition) is reduced by a factor of
approximately $10^3$. We found that the RKFNC integrator does not perform well
with this restriction on time-step, and often $\Delta t \to 0$, which is why the afore-
mentioned results use the implicit Newmark-beta scheme with constant acceleration
($\beta = 0.25, \gamma = 0.5$).

Fig. 12 Pore fluid stress results from applying the Yen impulse (50 kPa) to the permeable,
blood-saturated lung parenchyma for the Gauss point closest to $X = H$

Fig. 13 Solid extra stress results from applying the Yen impulse (50 kPa) to the permeable,
blood-saturated lung parenchyma for the Gauss point closest to $X = H$
Fig. 14 Displacement results from applying the Yen impulse (50 kPa) to the permeable, blood-saturated lung parenchyma for (a) solid skeleton displacement $u(X = H, t)$ and pore fluid displacement $u_f(X = H, t)$, and (b) solid skeleton displacement $u(X = H/2, t)$ and pore fluid displacement $u_f(X = H/2, t)$.
Fig. 15 Contours along the length of the mesh for pore fluid extra stress $\sigma_{11}^f(E)$, pore fluid velocity $v_f$ and porosity $n_f$ for permeable, blood-saturated lung parenchyma after applying the Yen impulse with 25 kPa maximum overpressure
We now present the results of the simulations using the Friedlander impulse loading\textsuperscript{53} at maximum overpressure $t_0 = 25$ kPa (refer to Fig. 6(b)), which is more applicable for free-field shock loading (i.e., a shock wave resulting from a detonation of an explosive device).\textsuperscript{54} Proceeding as before, we first assume an impermeable membrane of air-saturated lung parenchyma. Looking at Figs. 16 and 17, we see a similar trend: the pore fluid extra stress is small and does not account for any discrepancy between motions of solid and fluid, and total fluid stress, between nearly inviscid (Darcy) and viscous (Darcy-Brinkman) pore fluid flow.
Fig. 16 Displacement results from applying the Friedlander impulse (25 kPa) to the impermeable lung parenchyma for (a) solid skeleton displacement $u(X = H, t)$ (and by extension due to the no-slip/no-penetration condition, $u_f(X = H, t)$), and (b) solid skeleton displacement $u(X = H/2, t)$ and pore fluid displacement $u_f(X = H/2, t)$.
Fig. 17 Pore fluid stress results from applying the Friedlander impulse (25 kPa) to the impermeable lung parenchyma for (a) pore fluid extra stress at the Gauss point closest to $X = H$, and (b) total pore fluid stress $\sigma_{11} = \sigma_{11}^{(E)} - n^i p_i$ at the Gauss point closest to $X = H$. Slightly higher amplitude of pore fluid extra stress when zoomed in is due to finer resolution of the data points in a second, shorter simulation.
When the top of the column allows fluid to escape (i.e., when we use the permeable boundary condition), we again see no difference between the nearly inviscid (Darcy) and viscous (Darcy-Brinkman) displacements (refer to Fig. 18), though we note that strains are much larger here than for the impermeable boundary. Total pore fluid stress is unaffected by the pore fluid extra stress (refer to Fig. 19). Furthermore, pore fluid extra stress begins to diminish as the shock wave moves along the mesh (where the time sampling locations in used for the contour stills are shown in by Fig. 20), as shown in Fig. 21. We again see how pore fluid extra stress is influenced by large gradients in pore fluid velocity (Figs. 21(a) and 21(b)). In contrast to the Yen impulse (shock-tube loading), we also see larger porosity gradients (Fig. 21(b)).
Fig. 18 Displacement results from applying the Friedlander impulse (25 kPa) to the permeable lung parenchyma for (a) solid skeleton displacement $u(X = H, t)$ and pore fluid displacement $u_f(X = H, t)$, and (b) solid skeleton displacement $u(X = H/2, t)$ and pore fluid displacement $u_f(X = H/2, t)$.
Fig. 19 Pore fluid stress results from applying the Friedlander impulse (25 kPa) to the permeable lung parenchyma for (a) pore fluid extra stress at the Gauss point closest to $X = H$, and (b) total pore fluid stress $\sigma_{11}^f := \sigma_{11}^f(E) - n^f p_i$ at the Gauss point closest to $X = H$
Fig. 20 Sampling locations along the Friedlander impulse for 25 kPa maximum overpressure used in the contour plots
Fig. 21 Contours along the length of the mesh for pore fluid extra stress $\sigma_{11(E)}^f$, pore fluid velocity $v_t$ and porosity $n^f$ for permeable lung parenchyma after applying the Friedlander impulse with 25 kPa maximum overpressure.
Continuing, the pore air is now swapped for pore blood; pore fluid density, bulk modulus and viscosities are adjusted accordingly. Initial porosity and load are increased to 0.99 and 50 kPa, respectively. We observe that the pore fluid extra stress has no impact on displacement (refer to Fig. 22), although its magnitude is on par with the total pore fluid stress, at least at the onset of the shock load before the pore fluid pressure response dominates (refer to Fig. 23). However, the pore fluid extra stress does not affect the solid extra stress, that is, no additional tensile forces indicative of potential damage in the lung parenchyma are observed as compared to the nearly inviscid pore fluid (refer to Fig. 24). Similarly to the Yen impulse for blood-saturated lung parenchyma, we see (refer to Fig. 25) the shock wave percolating more slowly through the mixture than for air-saturated lung parenchyma, for either type of impulse loading.
Fig. 22 Displacement results from applying the Friedlander impulse (50 kPa) to the permeable, blood-saturated lung parenchyma for (a) solid skeleton displacement $u(X = H, t)$ and pore fluid displacement $u_l(X = H, t)$, and (b) solid skeleton displacement $u(X = H/2, t)$ and pore fluid displacement $u_l(X = H/2, t)$.
Fig. 23 Pore fluid stress results from applying the Friedlander impulse (50 kPa) to the permeable, blood-saturated lung parenchyma for the Gauss point closest to $X = H$

Fig. 24 Solid extra stress results from applying the Friedlander impulse (50 kPa) to the permeable, blood-saturated lung parenchyma for the Gauss point closest to $X = H$
Fig. 25 Contours along the length of the mesh for pore fluid extra stress $\sigma_{11}^{f}(E)$, pore fluid velocity $v_{f}$ and porosity $n^{f}$ for permeable, blood-saturated lung parenchyma after applying the Friedlander impulse with 50 kPa maximum overpressure.
5. Conclusion

We have expanded upon prior work\textsuperscript{27–30} by assuming non-negligible contributions of pore fluid viscous stress to total pore fluid stress. It has been shown that inclusion of the pore fluid viscous stress (the pore fluid extra stress) led to higher-order continuity requirements in the variational forms of the governing equations for balance of mass of the mixture and balance of linear momentum of the pore fluid, via the porosity gradient and Laplacian of pore fluid velocity. A $C^1$ continuous finite-element, the Hermite cubic polynomial, has been employed to ensure global convergence of the weakened forms of the aforementioned equations. The implementation was verified for a small-strain analytical solution assuming finite strain numerical implementation.

Numerical simulations for shock loading of lung parenchyma then followed. It was shown that for impermeable (undrained) and permeable (drained) boundary conditions, with air as the pore fluid, inclusion of the pore fluid extra stress had negligible effects on deformations. For permeable boundary conditions, effect of pore fluid extra stress on total fluid stress is more noticeable, particularly when the saturating fluid is changed from air to blood, where the latter has viscosities two orders of magnitude larger than the former. However, inclusion of pore fluid extra stress does not affect the solid extra stress, that is, the material response of the lung tissue itself.

A limiting factor in the present simulations is the assumption of 1-D uniaxial strain. Indeed, pore fluid viscous stresses along the direction of flow are not expected to be as significant compared to shear stresses at the fluid-structure interface. The latter are responsible for development of boundary layers in the pore channels, which, though not necessary to model given the length scale of interest, could affect numerical results for 3-D simulations. Notwithstanding, we have demonstrated for 1-D uniaxial strain shock problems that pore fluid pressure is the dominant force compared to viscous effects, and that the pore fluid extra stress may be ignored in such scenarios.

Furthermore, overcoming the $C^1$ continuity requirement for solid skeleton displacement will allow for appropriate implementation of distinct phase temperatures via balances of energy of each phase. Recall from Irwin et al.\textsuperscript{27} the dissipation inequal-
ity for distinct phase temperatures $\theta^s \neq \theta^f$:
\[
\sum \alpha \frac{1}{\theta^\alpha} \left( \rho^\alpha [D^\alpha \psi^\alpha + \eta^\alpha D^\alpha \theta^\alpha] - \sigma^\alpha : l_{\alpha} - \hat{\epsilon}^\alpha + \hat{\rho}^\alpha \left[ \psi^\alpha - \frac{1}{2} v_{\alpha} \cdot v_{\alpha} \right] + h^\alpha \cdot v_{\alpha} \right.
\]
\[
\left. + \frac{1}{\theta^\alpha} \grad(\theta^\alpha) : q^\alpha \right) \geq 0.
\]
(124)

With the assumption of negligible mass supplies (i.e., $\hat{\rho}^s = \hat{\rho}^f = 0$), the Clausius-Duhem inequality (dissipation inequality) for the mixture, now assuming thermally compressible solid (s) constituent, is written as
\[
\left( \rho^s D^s \psi^s + \frac{\theta^s}{\theta^f} \rho^f D^f \psi^f \right) + \left( \left[ \rho^s \eta^s - \Lambda \frac{n^s}{\rho^R} \frac{\partial \rho^R}{\partial \theta^s} \right] D^s \theta^s + \frac{\theta^s}{\theta^f} \rho^f D^f \theta^f \right)
\]
\[
- \left( \left[ \sigma^s + \Lambda n^s 1 \right] : d_s + \left[ \frac{\theta^s}{\theta^f} \sigma^f + \Lambda n^f 1 \right] : d_f \right)
\]
\[
+ (h^f - \Lambda \grad n^f) \cdot \tilde{v}_f - \Lambda \frac{n^f}{\rho^R} D^f \rho^R
\]
\[
- \hat{\epsilon}^f \left( \frac{\theta^f}{\theta^s} - 1 \right) + \left( \frac{1}{\theta^s} \grad(\theta^s) : q^s + \frac{\theta^s}{\theta^f} \frac{1}{(\theta^f)^2} \grad(\theta^f) : q^f \right) \geq 0,
\]
(125)

where $\eta^\alpha$ is the phase entropy, $\hat{\epsilon}^f$ is the local interaction energy supply to the pore fluid (e.g., heat transfer), and $\Lambda$ is a Lagrange multiplier satisfying the saturation constraint
\[
\Lambda \left( \frac{n^s}{\rho^R} \frac{\partial \rho^R}{\partial \theta^s} D^s \psi^s + n^s d_s : 1 + \frac{\rho^f}{\rho_R} D^f \rho^R + n^f d_f : 1 + \grad(n^f) \cdot \tilde{v}_f \right) = 0.
\]
(126)

Introducing the so-called “extra” terms,
\[
\sigma^s_E = \sigma^s + \Lambda n^s 1,
\]
\[
\sigma^f_E = \sigma^f + \Lambda \frac{\theta^f}{\theta^s} n^f 1,
\]
\[
\eta^s_E = \eta^s - \Lambda \frac{1}{(\rho^R)^2} \frac{\partial \rho^R}{\partial \theta^s},
\]
\[
h^f_E = h^f - \Lambda \grad n^f,
\]
(127)

it can be shown that in order to satisfy the thermodynamic identity\(^{56,57}\)
\[
\frac{\partial \psi^f}{\partial \theta^f} = -p_t \Rightarrow \frac{\partial \psi^f}{\partial \rho^R} \frac{\partial \rho^R}{\partial \theta^f} = -p_t \Rightarrow (\rho^R)^2 \frac{\partial \psi^f}{\partial \rho^R} = p_t,
\]
(128)
the following must hold:

$$\Lambda = \frac{\theta_s}{\theta_t} \frac{p_t}{p_l}.$$  \hfill (129)

This means that

$$h_E^f = h^f - \frac{\theta_s}{\theta_t} p_t \text{grad} n^f,$$  \hfill (130)

such that the distinct phase temperature Darcy-Brinkman equation is written as

$$n^f \mathbf{v}_l = -k \left( \rho^B (a_l - b) + \text{grad} p_t - \frac{1}{n^l} \text{div} \sigma_E^f + \frac{1}{n^l} p_t \text{grad} (n^f) \left[ 1 - \frac{\theta_s}{\theta_l} \right] \right).$$  \hfill (131)

Thus, the porosity gradient must be calculated when assuming distinct phase temperatures. Future work will include implementation of distinct phase temperatures in the numerical model, with the aim of formulating rate equations for phase entropies to enable a thermodynamically-consistent damage model for the solid (s) phase of lung parenchyma (similar to the one developed by Clayton et al.\textsuperscript{9,10}) thus allowing us to quantify damage in lung tissue subjected to high-strain-rate loading.
6. References


33. Vuong AT. A computational approach to coupled poroelastic media problems [thesis]. Technische Universität München (DEU); 2016.

34. Markert B. Porous Media Viscoelasticity with Application to Polymeric Foams [thesis]. Institut für Mechanik (Bauwesen) der Universität Stuttgart (DEU); 2005.


# List of Symbols, Abbreviations, and Acronyms

## TERMS:

<table>
<thead>
<tr>
<th>Abbreviation</th>
<th>Description</th>
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</thead>
<tbody>
<tr>
<td>1-D</td>
<td>one-dimensional</td>
</tr>
<tr>
<td>2-D</td>
<td>two-dimensional</td>
</tr>
<tr>
<td>3-D</td>
<td>three-dimensional</td>
</tr>
<tr>
<td>ARL</td>
<td>Army Research Laboratory</td>
</tr>
<tr>
<td>CFD</td>
<td>computational fluid dynamics</td>
</tr>
<tr>
<td>CFL</td>
<td>Courant-Friedrichs-Lewy</td>
</tr>
<tr>
<td>DEVCOM</td>
<td>US Army Combat Capabilities Development Command</td>
</tr>
<tr>
<td>DOF</td>
<td>degree(s) of freedom</td>
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<tr>
<td>FE</td>
<td>finite element</td>
</tr>
<tr>
<td>FSI</td>
<td>fluid-structure interaction</td>
</tr>
<tr>
<td>NB</td>
<td>Newmark-beta integrator</td>
</tr>
<tr>
<td>NURBS</td>
<td>Non-uniform rational B-spline</td>
</tr>
<tr>
<td>ODE</td>
<td>ordinary differential equation</td>
</tr>
<tr>
<td>RKFNC</td>
<td>Runge-Kutta Cash-Karp integrator</td>
</tr>
<tr>
<td>SF</td>
<td>safety factor</td>
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<tr>
<td>TPM</td>
<td>theory of porous media</td>
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</table>
MATHEMATICAL SYMBOLS:

\( t \) \hspace{1cm} \text{time}

\( x, x_k \) \hspace{1cm} \text{Cartesian spatial coordinates}

\( X, X_K \) \hspace{1cm} \text{Cartesian reference coordinates}

\( u_\alpha, u_i(\alpha) \) \hspace{1cm} \text{displacement of phase } \alpha

\( n^\alpha \) \hspace{1cm} \text{volume fraction of phase } \alpha

\( m_\alpha \) \hspace{1cm} \text{mass of phase } \alpha

\( \rho^{\alpha R} \) \hspace{1cm} \text{real mass density of phase } \alpha \ [\text{Mass}/\text{Length}^3]

\( \rho^\alpha \) \hspace{1cm} \text{partial mass density of phase } \alpha \ [\text{Mass}/\text{Length}^3]

\( \dot{\rho}^\alpha \) \hspace{1cm} \text{mass supply to phase } \alpha

\( J_\alpha \) \hspace{1cm} \text{Jacobian of deformation of phase } \alpha

\( F_\alpha, F_{iI}(\alpha) \) \hspace{1cm} \text{deformation gradient of phase } \alpha

\( p_\alpha \) \hspace{1cm} \text{Cauchy pressure of phase } \alpha \ [\text{Force}/\text{Length}^2]

\( v_\alpha, v_i(\alpha) \) \hspace{1cm} \text{velocity of phase } \alpha \ [\text{Length}/\text{Time}]

\( d_\alpha, d_{ij}(\alpha) \) \hspace{1cm} \text{velocity gradient of phase } \alpha \ [\text{Time}^{-1}]

\( a_\alpha, a_i(\alpha) \) \hspace{1cm} \text{acceleration of phase } \alpha \ [\text{Length}/\text{Time}^2]

\( h^\alpha, h_i^\alpha \) \hspace{1cm} \text{interaction force of phase } \alpha \text{ with other phases}

\( \sigma^\alpha, \sigma^\alpha_{ij} \) \hspace{1cm} \text{partial Cauchy stress of phase } \alpha \ [\text{Force}/\text{Length}^2]

\( P^\alpha, P_{iI}^\alpha \) \hspace{1cm} \text{first Piola-Kirchhoff stress of phase } \alpha \ [\text{Force}/\text{Length}^2]

\( \eta^\alpha \) \hspace{1cm} \text{entropy per unit mass of phase } \alpha \ [\text{Length}^2/\text{Time}^2 \cdot \text{Temperature}]

\( \psi^\alpha \) \hspace{1cm} \text{free energy per unit mass of phase } \alpha \ [\text{Length}^2/\text{Time}^2]

\( \theta^\alpha \) \hspace{1cm} \text{temperature of phase } \alpha

\( \varepsilon^\alpha \) \hspace{1cm} \text{energy supply per unit mass to phase } \alpha \ [\text{Length}^2/\text{Time}^2]

\( q_\alpha, q_i^\alpha \) \hspace{1cm} \text{heat flux vector of phase } \alpha \ [\text{Length} \cdot \text{Mass}/\text{Time}^2]

\( \dot{k} \) \hspace{1cm} \text{hydraulic conductivity} \ [\text{Length}^3 \cdot \text{Time}/\text{Mass}]

\( \eta_\alpha \) \hspace{1cm} \text{shear viscosity of phase } \alpha \ [\text{Force}/\text{Time}]

\( \kappa_\alpha \) \hspace{1cm} \text{bulk viscosity of phase } \alpha \ [\text{Force}/\text{Time}]
κ solid skeleton intrinsic permeability [Length$^2$]
$K_\alpha^\eta$ isentropic bulk modulus of phase $\alpha$ [Force/Length$^2$]