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Report

on

Scale Model Tests of High-Temperature High Pressure Steam Piping -CV9 Class Vessel

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ABSTRACT

Scale model tests of piping of ships of the CV9 Class have been made to determine the reaction forces and moments at various points on the piping system. Effects of horizontal tie rods at certain points have been determined.

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SCALE MODEL TESTS OF HIGH TEMPERATURE HIGH PRESSURE

STEAM PIPING - CV9 CLASS VESSEL

Introduction

A. Authorization

1. This problem was authorized by Bureau of Ships letter CV9Class/ S48-10(350) of 17 January 1943.

B. Statement of Problem

- 2. End reactions of steam piping of a CV9Class Vessel were required for several conditions of constraint. The points at which end reactions were to be determined are shown on plates 5 through 9, and are listed below.
 - a, No. 2 engine room and Nos. 3 and 4 fire rooms.

End reactions of the starboard and port side steam piping were to be measured both without and with constraint on the superheated branches from boilers 7 and 5, respectively. These constraints are described in paragraph 17, and their locations are shown in plates 6 and 8. In the following, Condition No. I will refer to the condition with no constraint, and Condition No. II will refer to the condition with this constraint, on the proper superheated branch.

Point A. - Connection of superheated steam branch to boiler No. 8 for conditions I and II, see plates 5a and 6a.

Point B. - Connection at superheated branch from starboard side main steam piping to No. 4 turbo-generator for conditions I and II, see plates 5a and 6a.

Point C. - Connection of superheated steam branch to boiler No. 7 for conditions I and II, see plates 5a and 6a.

Point L. - Connection of superheated steam branch from port side main steam piping to No. 4 turbo-generator for condition I, see plates 7a and 8a.

Point 0. - Connection of superheated branch to boiler No. 6 for conditions I and II, see plates 7a and 8a.

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Point P. - Connection of superheated branch to boiler No. 5 for conditions I and II, see plates 7a and 8a.

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b. No. 1 engine room and Nos. 1 and 2 fire rooms

Point I. - Connection of superheated branch from main steam piping to No. 2 turbo-generator, see plate 9.

- C. Statement of Method
 - 3. These end reactions were obtained by the use of scale models. The method of scale models for the determination of end reactions in the case of three-dimensional piping systems having several branches has been described in previous reports 1,2,3.

Description of Piping Under Consideration

- A. Main Steam Piping
 - 4. The main steam piping in No. 2 engine room and Nos. 3 and 4 fire rooms consists of two piping systems connected by a 7 inch cross-over pipe. These systems are: (1) port side main steam piping from boilers Nos. 5 and 6 to Turbine Set No. 3 (plates 7 and 8), and (2) starboard side main steam piping from boilers Nos. 7 and 8 to Turbine Set No. 2 (plates 5 and 6).
 - 5. In the determination of end reactions at various points of a piping system, one must first know the location of all points of constraint and the type of each constraint. In the main steam piping systems under investigation all piping is permitted to "float" in the vertical direction, with the exception of boiler, turbine, and turbogenerator connections. At two points the main steam piping is constrained by means of the rods which prevent motion in the horizontal plane but allow vertical motion and all rotations. These points are on the pipe axis at bulkhead 131 (see plates 5a and 7a). At several other points the main piping is constrained by means of horizontal the rods which prevent motion parallel to the rod, but allow displacements in the two perpendicular directions and all rotations. These points of constraint are labelled G, M, N, S in plates 5, 6, 7, 8.
 - 6. The large number of points of constraint involved made it impractical to set up these two systems together and measure all of the desired reactions. Therefore, each system was set up separately and the reactions determined. To approximate the effect of the cross-over pipe it was included in both systems, as shown in plates 1 and 2.

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- B. Auxiliary Steam Piping
 - 7. The auxiliary piping investigated consists of superheated branches from the port and starboard main steam lines to turbo-generators Nos. 3 and 4, in Nos. 3 and 4 fire rooms; and of the superheated branch to turbo-generator No. 2, in No. 1 engine room.

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- 8. The rigidity of the auxiliary piping is much less than that of the main steam piping and was neglected, therefore, when the reactions at points on the main steam piping were measured. To determine the reactions of the auxiliary piping, these were built as separate models of convenient size. The proper relative motions of the ends of these pipes were obtained by measuring the translations of the main steam piping at the point of connection of each auxiliary pipe. These translations were added to the thermal expansions of the auxiliary piping, and the reactions caused by the relative translations were measured. The effect of the rotations at the connection to the main steam line was assimilated by displacing the arms of the measuring head amounts proportional to the measured rotations. The additional reactions due to the rotations were thus obtained. the total reactions were then determined by adding the two sets of reactions.
- 9. This procedure was also followed in the case of the superheated branch to No. 2 turbo-generator in engine-room No. 1. It was assumed, to avoid building a model of the whole main piping system in engine-room No. 1 and fire rooms Nos. 1 and 2, that the deflections and rotations of the corresponding point of the cross-over pipe in engine-room No. 2 (point I') would be approximately the same as those of the point of the cross-over pipe in engine-room No. 1, to which the pipe is actually connected.

Construction of Scale Models

A. Selection of Model Tubing

10. The scale factor s, or ratio of axial dimensions of the model to those of the full scale pipe, is given by

$$r = \left(\frac{r_{\rm m}}{r_{\rm a}}\right)^2 \frac{t_{\rm a}}{t_{\rm m}}$$

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where r_a = mean radius of full-scale pipe r_m = mean radius of model pipe t_a = wall thickness of full-scale pipe t_m = wall thickness of model pipe

This condition should be satisfied for each pipe size which contains a bend.

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11. A second condition which must be satisfied when the piping system is composed of several pipe sizes is that the ratio of the moment of inertia of a pipe in the full-scale system to that of the corresponding pipe in the model system should be maintained constant for all the pipe sizes. In the present model system, due to the use of standard sizes of tubing, these requirements were satisfied to within about 4 percent.

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12. When the above conditions are satisfied, the full-scale pipe forces are obtained by multiplying those measured on the model by the factor K, where

$$K = \frac{E_a I_a}{E_m I_m} s^3 \frac{\Delta L_a}{\Delta I_m}$$

The full-scale moments are obtained by multiplying the moments measured on the model by the factor K/s.

here $E_a = 24.8 \times 10^6 \#/in^2 =$ Young's modulus for full-scale piping at operating temperature.

 $E_m = 29.0 \times 10^6$ #/in² = Young's modulus for model tubing.

- Ia = moment of inertia of full-scale pipe.
- Im = moment of inertia of corresponding model pipe.
- s = scale factor, ratio of axial lengths of model to fullscale piping.
- La = end displacement of full-scale pipe.
- Im = displacement of corresponding end of model system.
- 13. Dimensions of full-scale and model piping are given in the following tables:
 - Table I Main and Auxiliary Steam Piping. Cross-sectional Dimensions and Moments of Inertia of Full-size Piping (see plates 5-9).

Pipe size in.	0. D. in.	Wall Thickness in.	I. D. in.	Moment of Inertia in.4
3-1/2	4.00	.225	3.55	4.76
7	7.625	.429	6.767	63.3
8	8.625	.486	7.653	103.5
10	10.750	.605	9.54	249.0

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Table II - Main Steam Piping. Cross-sectional Dimensions and Moments of Inertia of Model Tubing (see plates 1,3).

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Full Scale Pipe Size in.	0. D. in.	Wall Thickness in.	I. D. in.	Moment of inertia in.4	Scale Factor s
7	•562	.022	•518	1.365 x 10-3	1/9.4
8	•626	.0245	•577	2.15 x 10-3	1/9.4
10	•755	.0365	•682	5.36 x 10-3	1/9.4

Table III - Auxiliary Steam Piping. Cross-sectional Dimensions and Moments of Inertia for Model of Superheated Branch from Starboard Main Steam Piping to Turbo-Generator No.4

Full Scale Pipe Size in.	0. D. in.	Wall Thickness in.	I. D. in.	Moment of inertia in.4	Scale Factor
3-1/2	0.756	.0362	.6836	5.36 x 10-3	1/4.43

Table IV - Auxiliary Steam Piping. Cross-sectional Dimensions and Moment of Inertia for Models of (1) Superheated Branch from Port Side Main Steam Piping to No. 4 Turbo-Generator, (2) Superheated Branch from Port Side Main Steam Piping to No. 3 Turbo-Generator, and (3) Superheated Branch from Main Steam Piping to No. 2 Turbo-Generator.

Full Scale Pipe Size in.	0. D. in.	Wall Thickness in.	I. D. in.	Moment of inertia in.4	Scale Factor
3-1/2	0.751	.0288	.694	4.27 x 10-3	1/3.5

- B. Construction of Constraints and Anchors Starboard Side Main Steam Piping
 - 14. Diagrams of this system are given in plates 5 and 6, and a photograph of the model set-up is given in plate 1.
 - 15. The piping is considered to be rigidly anchored at points A and C, i.e., at connections to boilers 7 and 8 (motions of anchor points are considered). At bulkhead 131, the rods prevent translation in the horizontal plane but allow vertical translation and all rotations. These constraints are assimilated at point D in the model by the device shown in plate 2. A metal plate is mounted on roller bearings inside a fixed housing which permits motion in one direction.

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The model tubing passes through the plate and is fixed to it by means of a self-aligning ball bearing in the manner shown in plate 2.

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- 16. The system is terminated at the main steam strainer (turbine set No. 2), point E on plates 1,5,6. At this point all horizontal translation is prevented while vertical translation and all rotations are permitted. The rotations of this point due to the thermal expansions of the turbine and turbine connections are not known, but since this point is a considerable distance from the points where reactions are to be measured, the effects of these rotations were assumed to be negligible. The vertical displacement given this end of the model set-up was taken as the thermal expansion of the piping from the turbine-set connection to the strainer, plus the given vertical motion of the turbine-set connection.
- 17. The reactions at points A, B, and C were desired without and with a horizontal tie rod placed at point G on the superheated branch from boiler No. 7 (conditions I and II respectively). This constraint was constructed as shown in plate 4, consisting of a horizontal rod connected to the model tubing and to the anchor by means of self-aligning ball bearings. This device prevents horizontal translation parallel to the rod, but permits translations in the two perpendicular directions, and all rotations.
- 18. The relative translations and rotations of point H (point of connection to the port side piping system) are not known. As the best approximation, it was assumed that the rotations at this point are negligible and that the only translations are those due to the thermal expansion across the ship between points F and H.
- 19. For the purpose of calculating end motions, the piping system was considered fixed at a point on the pipe axis 22" aft of bulkhead 131. This was merely an arbitrary reference point and its location in no way affects the results.
- C. Construction of Constraints and Anchors Port Side Main Steam Piping
 - 20. Diagrams of this system are given in plates 7 and 8, and a photograph of the model set-up is given in plate 3.
 - 21. As in the case of the starboard side main steam piping, the boiler connections (points 0 and P) were assumed to be rigid. The constraints at bulkhead 131 and at the main steam strainer (turbine set No. 3) were assumed to be identical with the corresponding constraints on the starboard side. The horizontal tie rods at points M, N, and S are identical to that shown in plate 4 and described above.

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22. The rotations at point F were assumed to be negligible. The across-ship translation was taken to be equal to the thermal expansion between F and H. The vertical translation of F was assumed to be equal to that measured on the model of the starboard side main piping.

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23. In calculating the end displacements, the pipe was considered fixed at a point on the pipe axis 22" aft of bulkhead 131 (see paragraph 19).

Results

- 24. Data obtained and calculations leading up to the results are given in Appendix I. A summary of results is included in Tables V through XI.
- 25. In the tables, forces and moments are those exerted by constraints on the pipes. Forces are given in pounds, moments in inch-pounds.
- Table V Starboard Side Main Steam Piping. Condition No. I: no constraint on superheated branch from boiler 7 Condition No. II: with constraint on superheated branch from boiler 7

	Condit	ion No. I	Condition No. II	
Reaction	Point A	Point C	Point A	Point C
Fx	+282	+403	+462	+364
Fv	-484	-1325	-785	-1618
F_z	-227	+215	-78	+272
Resultant	604	1405	944	1681
Mx	+80,000	+160,500	+72,700	+146,000
My	+47,700	# 11,800	+42,500	- 14,900
Mz	-29,300	-160,000	-16,800	-161,000
Resultant	97,600	226,500	85,900	217,200



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Table VI - Superheated Steam Branch from Starboard Side Main Steam Piping to No. 4 Turbo-Generator, Without Constraint on Superheated Branch from Boiler No. 7 (Condition No. I).

	Point B			Point B'		
	Translations	Rotations		Translations	Rotation	ns
Reaction	only	only	Sum	only	only	Sum
Fx	+219.0	-9	+210	-208.0	+ 9	-199
Fv	-128	+28	-100	+100	-28	+ 72
F'_{Z}	6	+24	+30	+21	-24	- 3
Resultant	253	38	234	232	38	212
M _x	700	-5,340	-4,640	+2570	+540	1+3110
My	910	-6,870	-5,960	+3430	+1140	+4570
Mz	+19,270	+100	+19,370	-12,700	+460	-12240
Resultant	19,300	8,700	20,800	13,380	1340	13400

Table VII - Superheated Steam Branch from Starboard Main Steam Piping to No. 4 Turbo-Generator. With Constraint on Superheated Steam Branch from Boiler No. 7 (Condition No.II).

	Point	¢ В	Point B'			
Reaction	Translations only	Rotations only	Sum	Translations only	Rotations only	Sum
F _X Fy Fz	+185 - 96 - 4	0 + 3 -37	+185 - 93 - 41	-205 + 91 + 25	0 - 3 +37	-205 + 88 + 62
Resultant	208	38	211	226	38	232
Mx My Mz	+ 910 +1550 +20,350	+4,960 +5,360 -3,614	+5,770 +6,920 16,736	+2,970 +4,040 -12,070	+1350 +3110 +4330	+3320 +7150 -7740
Resultant	20,400	8,150	18,700	13,100	5,500	11000

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Table VIII - Port Side Main Steam Piping. Contition I: No constraint on Superheated Branch from Boiler No. 5. Condition II: With Constraint on Superheated Branch from Boiler No. 5.

Reaction	Cond	ition I	Condition II		
	Point O	Point P.	Point O	Point P	
Fx	- 1178	- 1171	- 865	+ 1420	
Fy	- 872	- 1467	- 1105 .	- 2780	
Fz	- 62	+ 521	+ 1	- 56.5	
Resultant	1466	1947	1400	3140	
Mx	+ 99,600	+168,500	+153,200	+338,000	
· My	-140,500	-133,100	-102,700	+239,700	
Mz	+ 65,700	- 93,400	+ 76,800	-116,600	
Resultant	184,200	233,800	200,000	471,000	

Table IX - Superheated Branch from Port Side Main Steam Piping to No. 4 Turbo-Generator. Without Constraint on Superheated Branch from Boiler No. 5 (Condition I).

	Poir	nt L		Poi	nt L!	
Reaction	Translations	Rotations	Sum	Translations only	Rotations	Sum
Fx Fy Fz	- 231 - 38 - 100	- 28 + 14 + 1	-259 - 24 - 99	+ 195 + 57 + 82	+ 28 - 14 - 1	+223 + 43 + 81
Result ant	254	31	278	221	31	241
M _X My Mz	+6,360 -5,400 -11,000	-1,203 -1,300 - 280	+5,160 -6,700 -11,280	-5,440 +2,450 +14,270	+880 +520 +1620	-4560 +2970 +15890
Resultant	13,760	1,800	14,100	15.470	1,910	16,760

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Table X - Superheated Branch from Port Side Main Steam Piping to No. 3 Turbo-Generator. Without Constraint on Superheated Branch from Boiler No. 5 (Condition I).

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	Point	Q		Point Q'				
Reaction	Translation only	Rotation	Sum	Translation only	n Rotation only	Sum		
F _x Fy F _z	-152 - 90 - 48	- 14 + 2 + 18	166 88 30	+141 +108 + 40	+ 14 - 2 - 18	+155 +106 + 22		
Resultant	183	23	190	182	23	1.89		
M _x My Mz	+4870 -4200 -7970	-1220 + 580 - 960	+3650 -3600 -8930	+1730 -6050 +7780	-570 +1980 790	+1160 -4070 +6990		
Resultant	10,250	1,660	10,200	10,050	2,210	8,170		

Table XI - Superheated Branch from Main Steam Piping to No. 2 Turbo-Generator.

	Poi	nt I				
	Translation	Rotation		Translation	Rotation	
Reaction	only	only	Sum	only	only	Sum
Fr	-41	+ 30	- 11	+ 38	- 30	8
F	+120	- 18	+402	-472	+ 18	-454
Fz	+ 82	+ 33	+115	- 84	- 33	-117
Resultant	430	48.1	418	481	48.1	468
My	-2520	+1506	-1010	-2650	+1832	-820
Mar	+ 25	+3569	+3590	+4800	+ 219	+4580
Mz	-3840	-810	-4650	-35500	-157	-35340
Resultant	4600	3960	5,940	35,950	1855	35700

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Discussion of Results

- 26. Tables V through X give end reactions for the points considered on the main steam piping and auxiliary steam piping in engine room No. 2 and fire rooms Nos. 3 and 4. The tables giving reactions for the auxiliary piping include results due to relative translations of the ends, rotation produced by the action of the main steam piping and a summation of these two results.
- 27. Table XI gives the results for the superheated steam branch from the main steam piping to No. 2 turbo-generator. Due to the method of obtaining the end-rotations for this pipe, the reactions caused by the rotations are known to be inaccurate, but the orders of magnitude are believed to be correct. However, as the resultant forces and moments caused by the rotations are less than 10 percent of the re-sultant forces and moments caused by translations, for this case, it is evident that these errors are of little importance.
- 28. For the auxiliary steam piping a check of the results may be obtained by transferring the reactions from one end to the other. Table XII gives a comparison of the results measured at the connection to the main steam lines with those obtained by transferring from the other end. The values agree to within a reasonable percentage.

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Table XII - Measured Reactions of the Auxiliary Steam Piping at the Connections to the Main Steam Piping, Compared to Values Obtained by Transferring Reactions from Turbo-Generator Connections.

	Point B'		Point B'		Point L'		Point Q'		Point I'	
	Condition I		Condition II		Condition I		Condition I		Condition I	
	Measured	Trans.	Measured	Trans.	Measured	Trans.	Measured	Trans.	Measured	Trans.
Reaction	at B'	from B	at B'	from B	at L'	from L	at Q'	from Q	at I'	from I
Fx	-199	- 210	-205	-185	+223	+259	+155	+166	+ 8	+ 11
Fv	+ 72	+100	+ 88	+ 93	+ 43	+ 24	+106	+ 88	-454	-402
Fz	- 3	- 30	+ 62	+ 41	+ 81	+ 99	+ 22	+ 30	-117	-115
Resultant	212	234	232	211	241	278	1.89	190	468	418
%										
Difference		+ 11		- 10		+ 15		0	in many series	- 12
My	+3110	+1320	+3320	+3590	-4560	-7070	+1160	+1290	- 802	+2970
Myr	+4570	+4010	+7150	+6980	+2970	+4550	-4.070	-5180	+4580	+7280
M	-12240	-5970	-7740	-6030	+15890	+16800	+6990	+7230	-35340	-33100
-										
Resultant	13400	7040	11050	9900	16790	18750	8170	8980	35680	34000
%										
Difference		- 47		- 10		+ 12		+ 10		- 5

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Table XIII - Summary of Results Including Data Given in Previous NRL Report(3).

Pipe End	Condi-	Piping System	F _X	Fy #	Fz #	Mx	My in_4	Mz in-#
A	I	Stbd.	+282	-484	-227	+80000	+47700	-29300
A	II	Stbd.	+462	-785	- 78	+72700	+42500	-16800
A	III	Stbd.	+332	-237	+1164	+72400	+67800	-26500
B	I	Stbd.	+210	-100	+ 30	-4640	-5960	+19370
B	II	Stbd.	+185	- 93	- 41	+5770	+6920	+16736
B	III	Stbd.	+238	-182	+ 8	+2450	- 168	+19500
C	I	Stbd.	+403	-1325	+215	+160500	-11800	-160000
C	II	Stbd.	+364	-1618	+272	+146000	-14900	-161000
C	III	Stbd.	+127	-1709	+532	+171000	-67000	-202000
L	I	Port	-259	- 24	- 99	+5160	-6700	-11280
0	I	Port	-1178	-872	- 62	+99600	-140500	+65700
	II	Port	- 865	-1105	+ 1	+153200	-102700	+76800
P	I .	Port	-1171	-1467	+521	+168500	-133100	-93400
	II	Port	+1420	-2780	-565	+338000	+239700	-116100
Q	I	Port	166	- 88	- 30	+3650	-3600	-8930
I		No. 1 Engine Room	- 11	+402	+115	1010	+3590	-4650

Table XIII gives a summary of all the work that has been done at the Naval Research Laboratory on the piping of the CV9Class Vessel. In Table XIII the type of constraint is designated as follows:

- Condition I: At bulkhead 131, piping is permitted to have only vertical translation. All rotations are permitted. For the starboard side piping, there is no constraint on the superheated branch from boiler No. 7. For the port side piping, there is no constraint on superheated branch from boiler No. 5 (see paragraph 2a).
- Condition II: (1) At bulkhead 131, piping is permitted to have only vertical translation. All rotations are permitted.

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(2) For the starboard side piping, there is a constraint on the superheated branch from boiler No. 7. For the port side piping, there is a constraint on superheated branch from boiler No. 5.

Condition III: Piping is anchored at bulkhead 131. There are no constraints on superheated branch from boiler No. 7. (The data for this condition was taken from the previous work?)

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(1). Scale Model Tests for High-Pressure High-Temperature Steam Piping, First Partial Report. NRL Report No. 0-1684.

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APPENDIX I

Model Test Data

A. Starboard Side Main Steam Piping Note: "Condition I" refers to tests made with no constraint on superheated branch from boiler No. 7. "Condition II" refers to tests made with constraint against horizontal motion caused by a tie rod on the superheated branch from boiler No. 7, in position shown in Plates 5 and 6 (see paragraph 2a).

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Coordinate systems used are as follows3:

(x,y,z) = pipe coordinates; x = starboard, y = forward, z = up. $(x_r, y_r, z_r) = reference coordinates; arbitrary fixed axes.$ <math>(x', y', z') = measuring head coordinates.

1. Point A: Pipe connection to Boiler No. 8

End motions:

 $\Delta x = +.3682$ in. $\Delta y = -.5847$ $\Delta z = +1.1016$

Coordinates of pipe-end:

x' = 0, y' = 0, z' = 2.625 in.

Scale constants:

K = 288, K/s = 2144

Condition I

 $R_{x}' = +1.293 \text{ lb.}$ $R_{y}' = -9.14$ $R_{z}' = -2.342$ $R_{x}'y' = +2.665$ $R_{y}'z' = +8.68$ $R_{z}'x' = +2.8$



Condition II

 $R_{x}' = +0.824 \text{ lb.}$ $R_{y}' = -10.23$ $R_{z}' = -3.2$ $R_{x}'y' = +2.77$ $R_{y}'z' = +8.4$ $R_{z}'x' = +2.02$





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End motions:

Δx = + .3602 in. Δy = - 2.600 Δz = + 1.1016

Coordinates of pipe-end:

 $x^{1} = 0, y^{1} = 0, z^{1} = 2.625$ in.

Scale constants:

K = 228, K/s = 2144

Reactions: Condition I

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Condition II

 $R_x' = + 18.65 lb.$ $R_x' = + 18.25 lb.$ $R_y' = - 24.5$ $R_y' = - 25.02$ $R_z' = - 1.4$ $R_z' = - 1.67$ $R_x'y' = -14.2$ $R_x'y' = -14.37$ $R_y'z' = + 18.6$ $R_y'z' = + 17.87$ $R_z'x' = + 3.42$ $R_z'x' = + 3.18$

3. Point B': Superheated branch from starboard side main steam line to No. 4 turbo-generator, connection to valve at main steam line.

Condition I

End Motions:

 $\Delta x = -1.932$ ine $\Delta y = +1.935$ $\Delta z = +.420$

Rotations:

$$p_{x} = + .019$$

 $p_{y} = + .00125$
 $p_{z} = + .019$

Ocordinates of pipe-end:

 $x^{1} = 0, y^{1} = 0, z^{1} = 2.625$ in.



y

X



Appendix I

2

Scale constants:

K = 26.9, K/s = 119.0

Reactions at B! (due to translations)

 $R_{x}' = + 10.07 \text{ lb}.$ $R_{y}' = - 33.6$ $R_{z}' = + 2.86$ $R_{x}'y' = - 7.14$ $R_{y}'z' = + 25.5$ $R_{z}'x' = + 2.47$

Condition II

End motions:

 $\triangle x = -2.169$ in. $\triangle y = +1.921$ $\triangle z = +.453$

Rotations:

Coordinates of pipe-end:

$$x^{1} = 0, y^{1} = 0, z^{1} = 2.625$$
 in.

Scale constants:

$$K = 26.9, K/s = 119$$

Reactions at B¹ (due to translations)

 $\begin{array}{l} R_{x}{}^{i} = + 11.2 \quad 1b_{\bullet} \\ R_{y}{}^{i} = - 32.35 \\ R_{z}{}^{i} = + 2.52 \\ R_{x}{}^{i}y{}^{i} = - 8.4 \\ R_{y}{}^{i}z{}^{i} = + 24.35 \\ R_{z}{}^{i}x{}^{i} = + 2.52 \end{array}$

Reactions at B' (due to rotations)

 $R_{x}' = -.42 \text{ lb.}$ $R_{y}' = + 27.3$ $R_{z}' = -1.05$ $R_{x}'y' = -2.8$ $R_{y}'z' = -24.15$ $R_{z}'x' = -5.94$



Reactions at B' (due to rotations)

 $R_{x}' = -13.30 \text{ lb.}$ $R_{y}' = +22.74$ $R_{z}' = 0$ $R_{x}'y' = -7.0$ $R_{y}'z' = -22.4$ $R_{z}'x' = -16.10$

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Appendix I

3

4. Point B: Connection to No. 4 turbo-generator of superheated steam branch from starboard side main steam line.

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End motions:

A = 0 in. A = 0A = 0

Coordinates of pipe-end:

$$v^{1} = 0, v^{1} = 0, z^{1} = 3.375 \text{ in.}$$

Scale constants:

K = 26.9, K/s = 119

Condition I Reactions (due to translations of B')

 $R_{x}' = + 41.4 \text{ lb.}$ $R_{y}' = + 1.89$ $R_{z}' = -7.7$ $R_{x}'y' = -1.18$ $R_{y}'z' = -1.68$ $R_{y}'z' = + 35.55$



Condition II Reactions (due to translations of B')

R_1	=	+	41	.7	10	•
RI	-	÷	2.	38		
RY'	-	-	6.	86		
R ^Z I	1			1.	54	
RI	y ,	20	-	2.	52	
RY I	z,	-	+	36	.6	
Z	X			1000	(78) - L	

B. Port Side Main Steam Piping Note: "Condition I" refers to tests made with no constraint on superheated branch from boiler No. 5; "Condition II" refers to tests made heated branch from boiler No. 5; "Condition caused by tie rod on superwith constraint against horizontal motion caused by tie rod on superheated branch from boiler No. 5, in position shown in Plates 7 and 8 (see paragraph 2a).

4

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1. Point 0: Superheated branch connection to Boiler No. 6.

End motions:

x = -3445 in. x = -3.466x = +1.100

Coordinates of pipe-end:

 $x^{1} = 0, y^{1} = 0, z^{1} = 2.625$ in.

Scale constants:

K = 299, K/s = 2810



Appendix I

Reactions:

Condition I

Condition II

 $R_{x}' = -3.99$ lb. $R_{x}^{1} = +2.17 lb.$ $R_{v}' = -6.37$ $R_{v}' = -9.1$ Rz = + 3.64 $R_{z}^{1} = +2.52$ $R_{x'y'} = -8.05$ $R_{x'y'} = -11.55$ Ry'z' = + 3.29 $R_{y'z'} = +5.32$ $R_{z'x'} = -10.85$ $R_{z'x'} = -8.19$

2. Point P: Reactions at superheated branch, connection to boiler No. 5

End motions:

 $\Delta x = -.3254$ in. △ y = - 5.490 A z = + 1.100

Coordinates of pipe-end:

 $x^{i} = 0, y^{i} = 0, z^{i} = 2.625$ in.

Scale constants:

K = 299, K/s = 2810

Reactions: Condition I

 $R_{x}' = + 6.37 1b$ Ry' = 0 $R_{Z}' = + 3.64$ $R_{x'v'} = -12.6$ Ry'z' = -5.39 $R_{z'x'} = -6.93$

3. Point L': Superheated branch from port side main steam line to No. 4 turbo-generator, connection to main steam line.

Condition I

End motions:

Ax = + 0.7875 in. $\Delta y = + 0.300$ Az = + .5595



5

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Condition II

 $R_x' = + 39.9 \, 1b.$ Ry! = - 8.96 $R_{z}' = -5.32$ $R_{x'y'} = -23.1$

Rotations:

Øx = + .0195 Coordinates of pipe-end: $x^{i} = 0, y^{i} = 0, z^{i} = +2.625$ in. Scale Constants: K = 44.9, K/s = 157.0 Reactions at L' (due to rotations at L') Reactions at L' (due to translations at L') $\begin{array}{l} R_{x}' = + 1.82 \quad lb.\\ R_{y}' = + 2.69\\ R_{z}' = + 0.31\\ R_{x}' y' = - 0.67\\ R_{y}' z' = - 2.07\\ R_{y}' z' = + 1.16 \end{array}$ $R_{x}' = + 12.45$ lb. Ry' = + 25.35 $R_{z}^{*} = + 0.35$ $R_{x'y'} = -5.39$ $R_{y'z'} = -20.60$ $R_{z'x'} = +6.09$ 4. Point L: Superheated branch from port side main steam line to No. 4 turbo-generator, connection to turbo-generator. Condition I End motions: AX = 0 in. .∴y = 0 42=0 AX. Coordinates of pipe-end: x' = 0, y' = 0, z' = 2.625 in. ZI ZT Reactions: (due to translations at L') y' yr $R_{x}' = -0.7 \text{ lb.}$ $R_{y}' = -9.38$ $R_{z}' = -2.24$ $R_{x}'y' = -14.06$ $R_{y}'z' = +8.54$ $R_{z}'z' = -9.6$ x' Xr Appendix I 6

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y

5. Point Q': Superheated branch from port side main steam line to No. 3 turbo-generator, connection to superheated branch from boiler No. 5.

Condition I

End motions:

 $\triangle x = + 1.920$ in. $\wedge y = + 0.157$ $\triangle z = + 1.176$

Rotations:

Coordinates of pipe-end:

x' = 0, y' = 0, z' = 2.625 in.

Scale constants:

K = 62.5, K/s = 219

Reactions (due to translations at Q')

 $R_{x}' = -11.34 \text{ lb.}$ $R_{y}' = -9.08$ $R_{z}' = -1.54$ $R_{x}'y' = +5.60$ $R_{y'z}' = +6.72$ $R_{z'x}' = -5.04$

Reactions (due to rotations at Q')

yr

Z

У

$R_{y}' = + 1.89 1b_{e}$
$R_{v}^{*} = + .37$
$R_{m}^{o'} = + .035$
$R_{y}^{\prime} = -1.81$
$R_{u}^{*}a^{*} =61$
$R_{2}^{\prime} = + .37$

zr

Ar

IXI

6. Point Q: Superheated steam branch from port side main steam line to No. 3 turbo-generator, pipe connection to No. 3 turbo-generator.

Condition I

End motions:

 $\Delta_X = \Delta y = \Delta z = 0$ in.

Coordinates of pipe-end:

$$x' = 0, y' = 0, z' = 2.625$$
 in.



7

Scale constants:

K = 62.5, K/s = 219

Reactions: (due to translations at Q')

 $R_{x}' = + 13.85 \text{ lb}_{\bullet}$ $R_{y}' = -7.54$ $R_{z}' = -0.77$ $R_{x}'y' = -7.28$ $R_{y'z}' = +5.11$ $R_{z}'x' = +5.18$

- 7. Point I': Superheated steam branch from No. 2 turbo-generator to main steam line, connection to main steam line.
 - Condition I

End motions:

 $\Delta x = + 0.157$ in. $\Delta y = - 3.039$ $\Delta z = - 0.538$

Rotations:

Coordinates of pipe-end:

x' = 0, y' = 0, z' = 2.625 in

Scale constants:

K = 98, K/s = 343

Reactions (due to translations at I')

 $\begin{array}{l} R_{x}! = + \ 0.56 \ 1b. \\ R_{y}! = - \ 28.75 \\ R_{z}! = + \ 0.14 \\ R_{x}! y! = - \ 1.4 \\ R_{y}! z! = + \ 23.85 \\ R_{z}! x! = - \ 0.84 \end{array}$

(due to rotations at I')

Zr

 $R_{x}' = + 1.40 \text{ lb.}$ $R_{y}' = -.108$ $R_{z}' = -.162$ $R_{x}'y' = -.108$ $R_{y}'z' = +.081$ $R_{z}'x' = +.943$

1 z1

Xr

Appendix I

net 1 a 1910

yr

X'

y

8

8. Point I: Superheated steam branch from No. 2 turbo-generator to main steam line, pipe connection to No. 2 turbo-generator.

Condition I

End motions:

 $\Delta x = \Delta y = \Delta z = 0$ in.

Coordinates of pipe-end:

 $x^{!} = 0, y^{!} = 0, z^{!} = 2.625$ in.

Scale constants:

K = 98, K/s = 343

Reactions: (due to translations at I')

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 $\begin{array}{l} R_{x}' = -5.74 \text{ lb.} \\ R_{y}' = -0.63 \\ R_{z}' = +0.84 \\ R_{x}'y' = -2.24 \\ R_{y}'z' = +0.21 \\ R_{z}'x' = -3.71 \end{array}$





Appendix I





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1







































