

US Army Corps of Engineers_® Engineer Research and Development Center

Detailed Fuel Cell Demonstration Site Summary Report

Edwards Air Force Base, CA

J. Michael Torrey, John F. Westerman, William R. Taylor, Franklin H. Holcomb, and Joseph Bush

August 2006



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Final Report

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Prepared for U.S. Army Corps of Engineers Washington, DC 20314-1000 **Abstract:** Fuel cells are an environmentally clean, quiet, and a highly efficient method for generating electricity and heat from natural gas and other fuels. In fiscal year 1993 (FY93), the Engineer Research and Development Center, Construction Engineering Research Laboratory (ERDC-CERL) was assigned the mission of managing the DOD Fuel Cell Demonstration Program. Specific tasks included developing turnkey PAFC packages, devising site criteria, screening candidate DOD installation sites based on selection criteria, evaluating viable applications at each candidate site, coordinating fuel cell site designs, installation and acceptance of the PAFC power plants, and performance monitoring and reporting.

CERL selected and evaluated 30 application sites, supervised the design and installation of fuel cells, actively monitored the operation and maintenance of fuel cells, and compiled "lessons learned" for feedback to fuel cell manufacturers. At the conclusion of the demonstration period, each of the demonstration fuel cell sites was given the choice to either have the fuel cell removed or to keep the fuel cell power plant. This report presents a detailed review of a 200 kW fuel cell installed at Edwards Air Force Base (AFB) and operated between July 1997 and July 2002.

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Preface

In fiscal years 93 and 94, Congress provided funds for natural gas utilization equipment, part of which was specifically designated for procurement of natural gas fuel cells for power generation at military installations. The purchase, installation, and ongoing monitoring of 30 fuel cells provided by these appropriations has come to be known as the "DOD Fuel Cell Demonstration Program." Additional funding was provided by: the Office of the Deputy Under Secretary of Defense for Industrial Affairs & Installations, ODUSD (IA&I)/HE&E; the Strategic Environmental Research & Development Program (SERDP); the Assistant Chief of Staff for Installation Management (ACSIM); the U.S. Army Center for Public Works (CPW); the Naval Facilities Engineering Service Center (NFESC); and Headquarters (HQ), Air Force Civil Engineer Support Agency (AFCESA).

The work was performed by the Energy Branch (CF-E), of the Facilities Division (CF), Construction Engineering Research Laboratory (CERL). The CERL Principal Investigator was Franklin H. Holcomb. Part of this work was done by Science Applications International Corporation (SAIC) under General Services Administration (GSA) contract No. 5TS5703C166. J. Michael Torrey and John F. Westerman are associated with SAIC. Dr. Thomas Hartranft is Chief, CEERD-CF-E, and L. Michael Golish is Chief, CEERD-CF. The associated Technical Director was Gary W. Schanche, CEERD-CVT. The Director of CERL is Dr. Ilker R. Adiguzel.

CERL is an element of the U.S. Army Engineer Research and Development Center (ERDC), U.S. Army Corps of Engineers. The Commander and Executive Director of ERDC is COL Richard B. Jenkins, and the Director of ERDC is Dr. James R. Houston.

Unit Conversion Factors

Multiply	Ву	To Obtain
acres	4,046.873	square meters
cubic feet	0.02831685	cubic meters
cubic inches	0.00001638706	cubic meters
degrees (angle)	0.01745329	radians
degrees Fahrenheit	(5/9) x (°F – 32)	degrees Celsius
degrees Fahrenheit	(5/9) x (°F – 32) + 273.15.	kelvins
feet	0.3048	meters
gallons (U.S. liquid)	0.003785412	cubic meters
horsepower (550 ft-lb force per sec- ond)	745.6999	watts
inches	0.0254	meters
kips per square foot	47.88026	kilopascals
kips per square inch	6.894757	megapascals
miles (U.S. statute)	1.609347	kilometers
pounds (force)	4.448222	newtons
pounds (force) per square inch	0.006894757	megapascals
pounds (mass)	0.4535924	kilograms
square feet	0.09290304	square meters
square miles	2,589,998	square meters
tons (force)	8,896.443	newtons
tons (2,000 pounds, mass)	907.1847	kilograms
yards	0.9144	meters

1 Introduction

1.1 Background

In fiscal year 1993 (FY93), the U.S. Congress appropriated \$18 million to advance the use of phosphoric acid fuel cells (PAFCs) at Department of Defense (DOD) installations. An additional \$18.75 million was appropriated in FY94 to expand the program. The Engineer Research and Development Center, Construction Engineering Research Laboratory (ERDC-CERL) was assigned the mission of managing the DOD Fuel Cell Demonstration Program. Specific tasks included developing turnkey PAFC packages, devising site criteria, screening candidate DOD installation sites based on selection criteria, evaluating viable applications at each candidate site, coordinating fuel cell site designs, installation and acceptance of the PAFC power plants, and performance monitoring and reporting.

Thirty DOD fuel cell sites were selected based on the following criteria:

- 1. Geographic diversity
- 2. Application diversity
- 3. Fuel cell utilization at site
- 4. Energy cost savings.

The first two criteria are related more to overall program goals; the last are typical criteria for most fuel cell evaluations. It was important for the DOD Fuel Cell Program sites to represent a cross section of both "base" (including climate) and "building" applications. It was also important to identify applications where a high percentage of the fuel cell thermal and electrical output could be used at the site to demonstrate the greatest benefits.

Energy savings were less important in this Program than is typical with commercial applications since fuel cells purchased by the DOD were given to the Program sites. The economic criteria for each application was to generate at least \$25,000 per year in energy savings, which would essentially cover annual maintenance costs. This would enable the fuel cell to pay for itself once the responsibility for maintenance was turned over to the base (after approximately 5 years).

The program followed a consistent approach for selecting sites, designing and reviewing installation plans, installing and maintaining the fuel cells, collecting fuel cell performance data and project decommissioning. This involved:

- 1. *Preliminary Screening*. Base energy data from the Defense Energy Information System (DEIS) were used to rank DOD sites by utility rates and potential fuel cell energy savings. DOD base personnel were contacted to identify their interest in hosting a fuel cell demonstration unit and identify a preliminary list of potential building applications. The Navy and Air Force provided an initial list of candidate sites for consideration.
- Site Visits. ERDC/CERL and Science Applications International Corporation (SAIC) representatives visited each base, evaluated potential fuel cell application sites and discussed possibilities with site personnel. Data on energy consumption and rates, hours of operation, availability of space, etc. were collected during the site visit.
- 3. *Site Evaluation Reports.* SAIC prepared a site evaluation report^{*} documenting site information, presenting conceptual fuel cell installation plans, estimation of electrical and thermal energy savings, and projected fuel cell energy savings. Based on the viability of the proposed fuel cell application, the base was accepted as a program site.
- 4. Kick-off Meetings. ERDC/CERL, SAIC, United Technologies Corp. (UTC) Fuel Cells (formerly ONSI Corp. and International Fuel Cells) and site personnel met to review the site evaluation report, discuss relevant issues, schedules, and any other concerns. UTC Fuel Cells collected site data for use in preparing the detailed site installation drawings.
- 5. Design Review Meetings. Detailed design drawings were submitted by UTC Fuel Cells for review by ERDC/CERL, SAIC, and site personnel. Specific issues related to the design were discussed and UTC Fuel Cells would incorporate changes to the drawings based on the input received.
- 6. *Acceptance Tests.* Installation of the fuel cells was the responsibility of UTC Fuel Cells. After the fuel cell installation was completed, a series of tests were performed to validate fuel cell performance. On successful completion, the fuel cell was turned over to the base, but operation and maintenance remained the responsibility of UTC Fuel Cells for approximately 5 years. Appendix A includes a copy of the acceptance test report.

^{*} Michael J. Binder, Franklin H. Holcomb, and William R. Taylor. (March 2001). Site Evaluation for Application of Fuel Cell Technology: Edwards AFB, ERDC/CERL Technical Report (TR) 01-60/ ADA395031, paa. Champaign, IL: Engineer Research and Development Center, Construction Engineering Research Laboratory (ERDC-CERL).

- 7. *Dedication Ceremonies*. Many of the fuel cell sites held a fuel cell dedication ceremony as part of their program participation. Often, dignitaries such as Generals and State Governors were in attendance.
- 8. *Fuel Cell Operations*. The fuel cells operated for 3 to 5 years. UTC Fuel Cells was responsible for maintenance of the power plant as well as collection of fuel cell performance data.
- 9. Fuel Cell Decommissioning. At the conclusion of the demonstration period, UTC Fuel Cells was responsible for removing the fuel cell and returning the site to the its condition before to the fuel cell installation. Each of the FY93 fuel cell sites, including Edwards AFB was given the opportunity to keep the fuel cell power plant at the end of the demonstration and take responsibility for all costs and issues related to operation, performance, and decommissioning.

This report presents a detailed review of a 200 kW fuel cell installed at Edwards Air Force Base (AFB). The base is located in near Palmdale, CA, approximately 60 mi north of Los Angeles. The fuel cell was installed at the hospital as part of the DOD Fuel Cell Demonstration Program. The fuel cell operated between July 1997 and July 2002.

1.2 Objectives

The overall objectives of the Fuel Cell Demonstration Program were to:

- demonstrate fuel cell capabilities in real-world situations
- stimulate growth and economies of scale in the fuel cell industry
- determine the role of fuel cells in DOD's long-term energy strategy.

The specific objective of this part of the program was to give a detailed review of the PAFC fuel cell demonstration at Edwards AFB.

1.3 Approach

The review process involved:

- 1. Collecting data from stage of the Fuel Cell Demonstration Program at Edwards AFB
- Analyzing the data in terms of the technology's capabilities, performance, and potential for a continuing role in the DOD's long-term energy strategy
- 3. Compiling lessons learned from the demonstration experience
- 4. Making recommendations for continued/improved use of the technology at DOD installation.

1.4 Mode of Technology Transfer

Results of this work will be forwarded directly to the funding sponsor and to the participating installation. This report will be made publicly accessible through the World Wide Web (WWW) at URLs:

http://www.cecer.army.mil http://www.dodfuelcell.com

2 Project Overview and Participants

2.1 Project Timeline

The first formal activity related to the fuel cell demonstration unit at Edwards AFB was a site evaluation meeting held in August 1996. (Appendix B contains notes from this meeting and from the meeting of 25 March 1997.) The fuel cell was started up in June 1997 and, over the next 5 years, it operated for over 28,000 hours and generated more than 5 million kWh of electricity. The demonstration unit remains at the Edwards AFB, although it is not currently operational. Table 1 lists the major events and milestones for this fuel cell demonstration unit.

	Date		Event
15-16	August	1996	Site Evaluation Meeting held at Edwards AFB
29	January	1997	Site Evaluation Report submitted by SAIC
5	February	1997	Project Kick-off Meeting held at Edwards AFB
18	February	1997	Draft design drawings submitted by UTC Fuel Cells
25	March	1997	Fuel Cell Design Review meeting held at Edwards AFB
25	April	1997	ERDC/CERL authorizes UTC Fuel Cells to commence construc- tion.
23-25	June	1997	Acceptance testing performed
16	July	1997	Acceptance Test Meeting; Form DD250 signed by Edwards AFB
25	October	1997	1,000 hours of operation milestone
26	October	1997	Fuel cell shut down due to failed cooling coil and cell sub-stacks. Cell stack removed and sent back to UTC Fuel Cells for repair.
4	February	1998	Repaired cell stack installed
11	March	1998	Power plant restarted after 3,203 outage hours.
12	October	1998	5,000 hours of operation milestone
4	July	1999	10,000 hours of operation milestone
17	February	2000	15,000 hours of operation milestone
3	November	2000	20,000 hours of operation milestone
1	July	2002	Fuel cell shut down for final time

Table 1. Time line of major events and milestones.

Chapter 4 of this report gives a more detailed analysis of the fuel cell operation and performance history.

There was an approximately 10-month period between the initial site evaluation meeting and the fuel cell acceptance test. It took approximately 3 months to install the fuel cell following acceptance of the installation design. UTC Fuel Cell was responsible for the installation of all 30 fuel cells installed as part of this program. GBC Electrical Services installed the fuel cell at Edwards AFB as a subcontractor to UTC Fuel Cells.

2.2 Project Participants

The successful demonstration of this fuel cell unit required the efforts of several organizations and individuals:

- *ERDC/CERL* had overall responsibility for the DOD Fuel Cell Demonstration Program unit installed at the Naval Hospital. ERDC/CERL was responsible for contracting with the fuel cell manufacturer, identifying all sites, managing all site evaluations, and overseeing all design, installation, operation, and maintenance activities.
- *UTC Fuel Cells* manufactured the PC25B and PC25C fuel cells used at the bases. They were responsible for manufacturing the fuel cell as well as the detailed design drawings, fuel cell installation, operation/maintenance and, if necessary, fuel cell removal.
- *SAIC* was responsible for evaluating potential building applications at each site, developing fuel cell conceptual designs, performing a preliminary economic analysis and submitting the site evaluation report for review by all parties. In addition, SAIC was involved in the detailed design reviews and participating in the design review meetings. For this demonstration unit, SAIC also conducted independent performance monitoring of the fuel cell.
- *GBC Electrical Services* was the installation contractor for this fuel cell. In addition, they performed the maintenance on the fuel cell and were involved in its removal.
- *Edwards AFB Hospital* was directly involved in the review and approval of the fuel cell project.
- *Edwards AFB Personnel* provided review and approval for various aspects of the project including fire and utilities interfaces.

Table 2 lists the individuals involved in this demonstration project at the Hospital. Figure 1 shows the fuel cell installation.

Name	Project Role
Dr. Michael Binder	Manager, Fuel Cell Demonstration Pro- gram
Franklin Holcomb	Fuel Cell Project Manager
William Taylor	Fuel Cell Project Manager
Joseph Staniunis	Installation Designer
Douglas Young	Technical Representative
Thomas Pompa	Installation/Maintenance Coordinator
Gerry Merten	Principal Technical Manager
Mike Torrey	Project Manager
Ken Munson	Base Point of Contact
Lt. Matt Sufnar	95CEG/CEO
Jose DeLavega	95CEG/CECV
F.P. Woodland	95MG/SGAF
George Collard	Installation/Maintenance Contractor
	Dr. Michael Binder Franklin Holcomb William Taylor Joseph Staniunis Douglas Young Thomas Pompa Gerry Merten Mike Torrey Ken Munson Lt. Matt Sufnar Jose DeLavega F.P. Woodland

Table 2.	Principal	project	participants.
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Figure 1. Fuel cell installation.

3 Fuel Cell Design and Installation

3.1 Fuel Cell Building Application

The Hospital, built in 1955, is a 65,000 sq ft building with an emergency room, several clinic facilities, and 30 hospital beds. Additions were made to the hospital in 1966. The average occupancy for inpatients was approximately 10 beds per night. Two back-up generators, rated at 300 kW and 500 kW, provide backup power to the facility. Space heating and domestic hot water is provided by the two steam boilers located inside the mechanical room. The steam distribution system operates throughout the year and provides for instrument sterilization and also to control building humidity levels. For space cooling requirements, there are two 200 ton chillers that operate throughout the year to provide space cooling and to control humidity. More details about the site can be obtained from ERDC/CERL TR-01-60, available through URL:

http://www.cecer.army.mil/techreports/Hol SE Edwards/Hol SE Edwards TR.pdf

3.2 Conceptual Installation Design

A preliminary conceptual design for the fuel cell installation was prepared. based on the initial site evaluation meeting in August of 1996. Figure 2 shows the layout of the mechanical room, fire system pump room, existing chillers, and the proposed fuel cell location, including proposed fuel cell interface connections.

The proposed fuel cell location was adjacent to the fire system pump room and the mechanical room at the end of an asphalt driveway. This location was close to the facility steam lines located inside the pump room, and approximately halfway between the electric transformer and main natural gas line for the hospital.

Initial plans were to connect the fuel cell electrical interface into the low voltage side of the 12,000/480V transformer (1,000 kVA) that supplied electricity to the hospital facility. This connection would allow the electrical wiring distance to be approximately 60 ft. No grid-independent mode operation was proposed for this application.

The proposed thermal interface was to take the fuel cell's high grade heat exchanger (a fuel cell option) and tie into the space heating loop to add heat on the return side. Figure 3 shows the proposed fuel cell thermal interface where 180 °F return water is heated up by the fuel cell prior to entering the steam heat exchanger. The thermal piping distance was estimated to be approximately 15 ft.

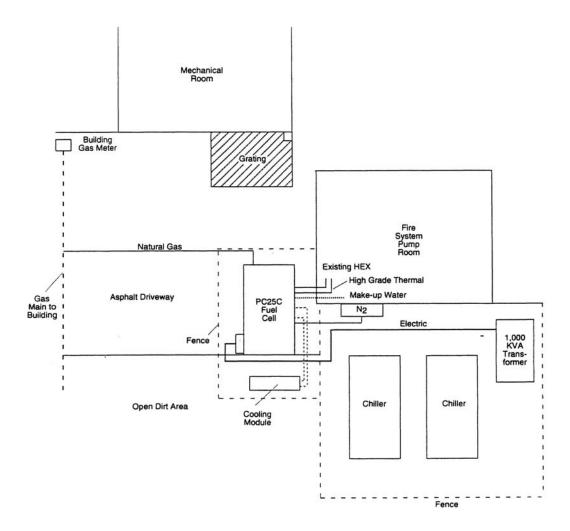


Figure 2. Conceptual design fuel cell location and interfaces.

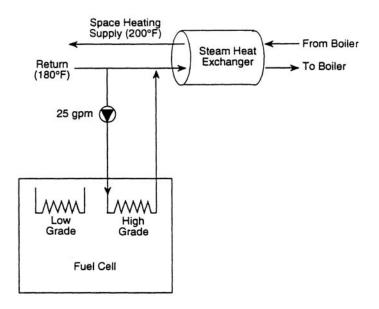


Figure 3. Conceptual design fuel cell thermal interface.

3.3 Detailed Design Drawings

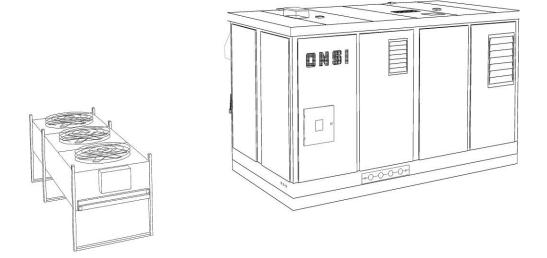
UTC Fuel Cells submitted an original set of design drawings on 18 February 1997. The drawings were reviewed by base personnel, ERDC/CERL, and SAIC. A design review meeting was held 25 March 1997 at Edwards AFB, at which the following drawings were submitted:

S-1:	Site Foundation Plan
ME-1:	Mechanical/Electrical Layout Plan
M-1 :	Mechanical Piping and Instrumentation Diagram
M-2:	Mechanical Piping Details
E-1:	Electrical Wiring Diagrams
E-2:	Electrical Details.

The orientation of the fuel cell was rotated 90 degrees from the initial conceptual design layout to accommodate maintenance activities. Thermal piping was run above ground on the new fuel cell cement pad located inside the fenced area. Reviewers submitted comments based on the initial drawings. (Appendix C includes copies of these comments.) Table 3 lists the changes made to the detailed site drawings, both before and after the design review meeting. Figures 4 through 10 show the final installation drawings.

Drawing		Changes
	1.	Provide standard wall penetration detail.
S-1	2.	Note that equipment pad will have #4 rebar on 2-ft centers instead of 1-ft centers.
	3.	Provide dimension of power module frame wide, fence width (short side) and clearance between fuel cell fence and open grate area.
	1.	Extend arrow for #7 polygon (electrical connection) note to indicate the make-up water line.
	2.	Add "boxed M" to symbol list.
ME-1	3.	Note the #3 and #5 mechanical connections are not used.
	4.	Move the nitrogen bottles 2 ft closer to hospital (Bldg. 5500) so that it is fully supported by the wall of Building 5700.
	5.	Disconnect labels changed (reversed grid-connected and grid-independent.
	1.	Correct the note for the source of natural gas to indicate the interface is at the existing gas piping under the parking lot (as noted in Drawing ME-1)
M-1	2.	Indicate the gas meter should be installed with a bypass (as noted on M-2, gas piping detail.
	3.	In the Equipment Schedule List, change the P1 pump specification to 1-1/2AA, $1/2$ HP. (This was incorrectly listed as 1-1/2A, $1/2$ HP).
M-2		No changes.
E-1	1.	Change the conduit size for the telephone conductors to 1-in. to match power module interface opening size.
E-2		No changes.

Table 3. Changes to design drawings based on comments.



PC25[™]C ON SITE FUEL CELL POWER PLAN BASE HOSPITAL, BUILDING 5500, I F'±BRUARY 17, 1997



195 GOVFRNORS HIGHWAY SOUTH WINDSOR, CONNECTICUT (860) 727-2237

Figure 4. Final installation drawings - cover page with code information.

DRAWING LIST

NO.	TITLE
S-1	SITE FOUNDATION PLAN
ME-1	MECHANICAL/ELECTRICAL LAYOUT PLAN
M 1	MECHANICAL PIPING AND INSTRUMENTATION DIAGRAM
X-S	MECHANICAL PIPING DETAILS
E 1	ELECTRICAL WIRING DIAGRAMS
E 2	ELECTRICAL DETAILS

CODE INFORMATION

INSTALLATION SHALL COMPLY WITH THE FOLLOWING CODES:

THE BOCA NATIONAL BUILDING CODE 1990 THE BOCA NATIONAL MECHANICAL CODE 1990 THE BOCA NATIONAL PLUMBING CODE 1990 THE NATIONAL ELECTRICAL CODE 1993 THE NATIONAL FIRE PROTECTION CODE 1993

T INSTALLATION L'DWARDS AFB, CALIFORNIA

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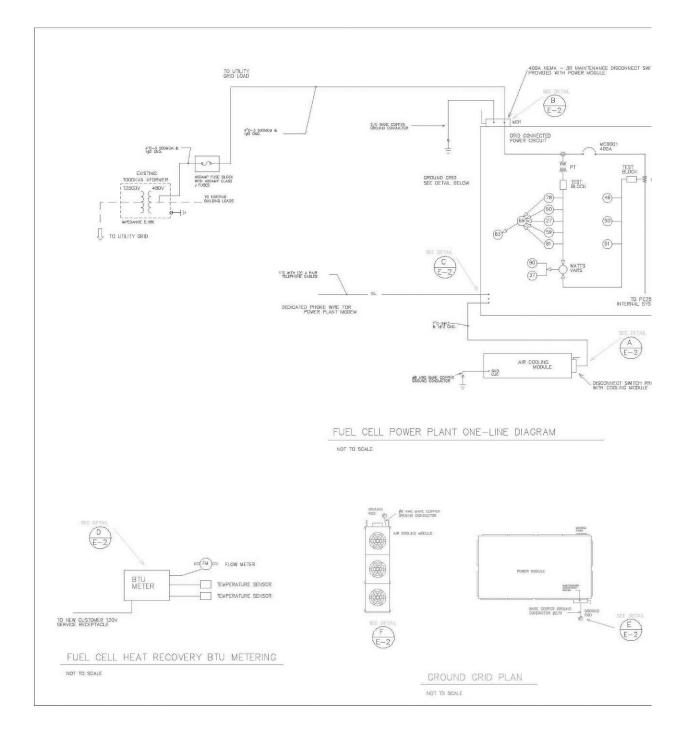
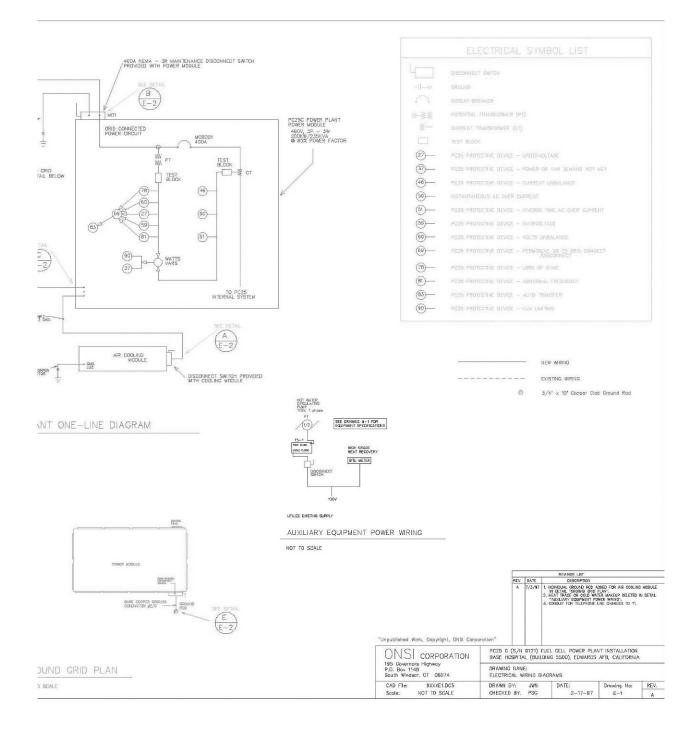


Figure 5. Final installation drawings – auxiliary equipment power wiring.



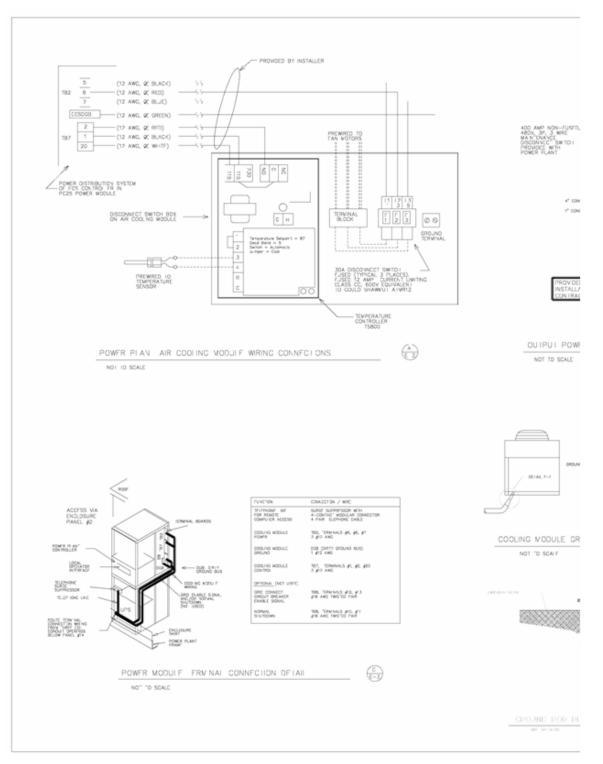
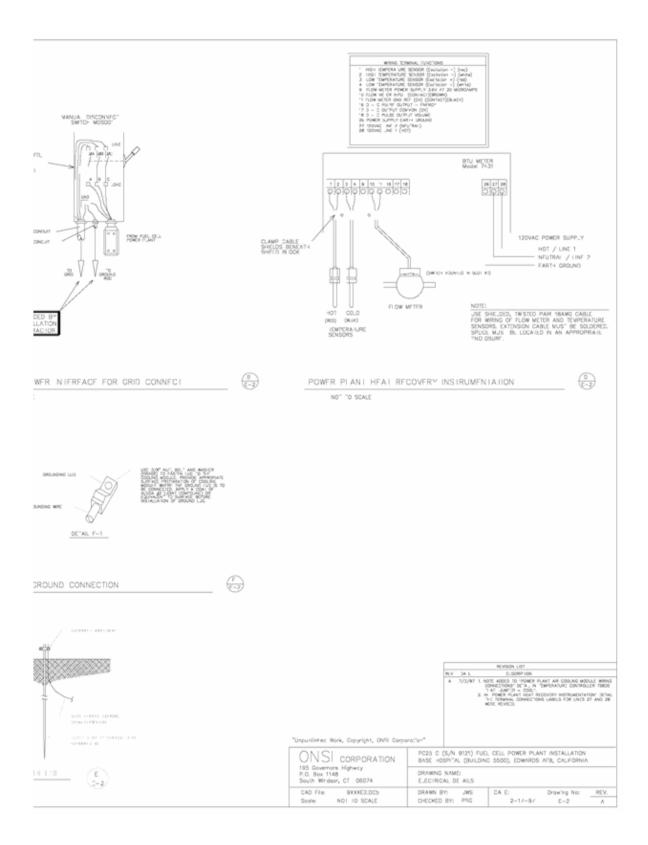


Figure 6. Final installation drawings – electrical details.



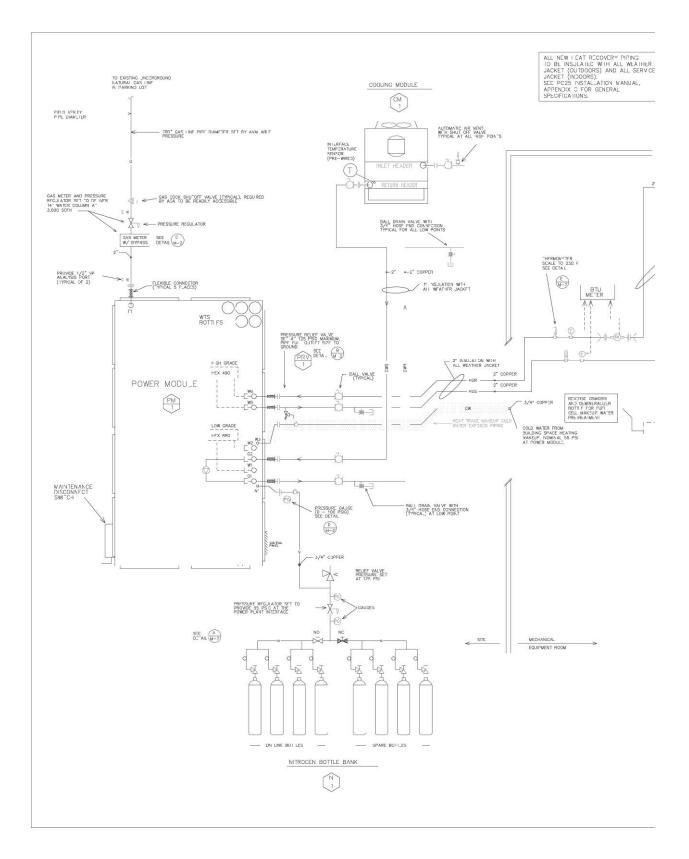
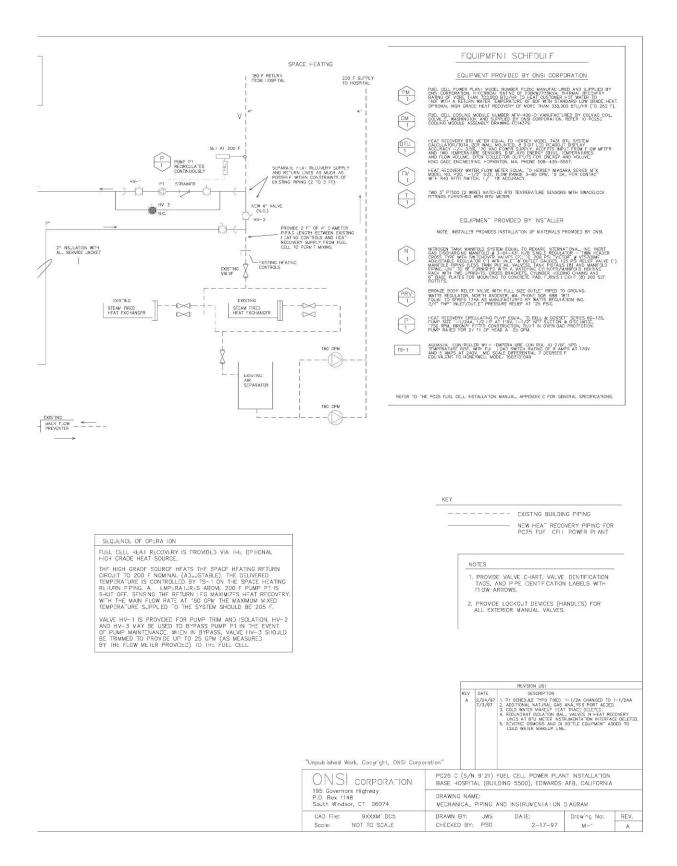


Figure 7. Final installation drawings – mechanical piping and instrumentation diagram.



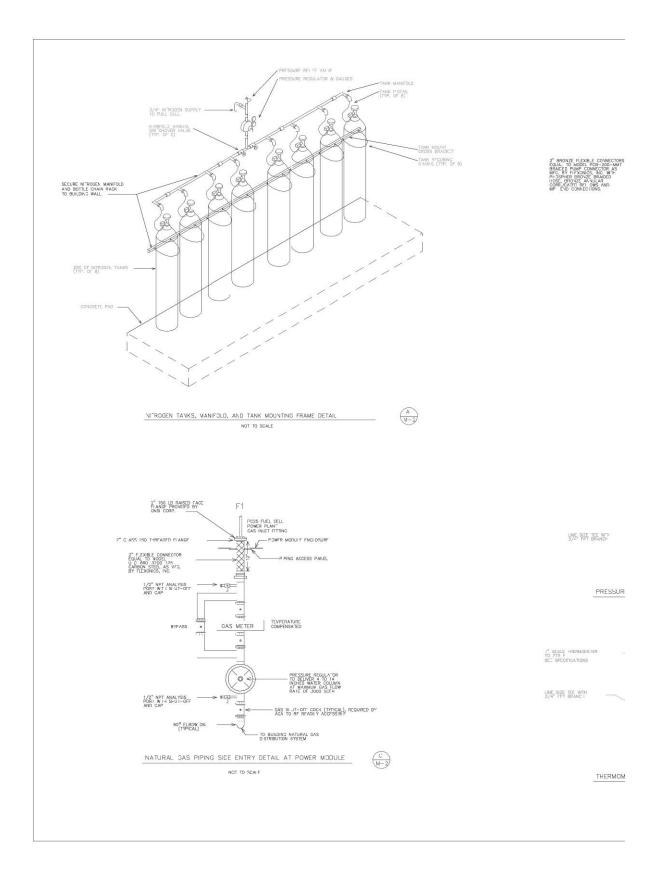
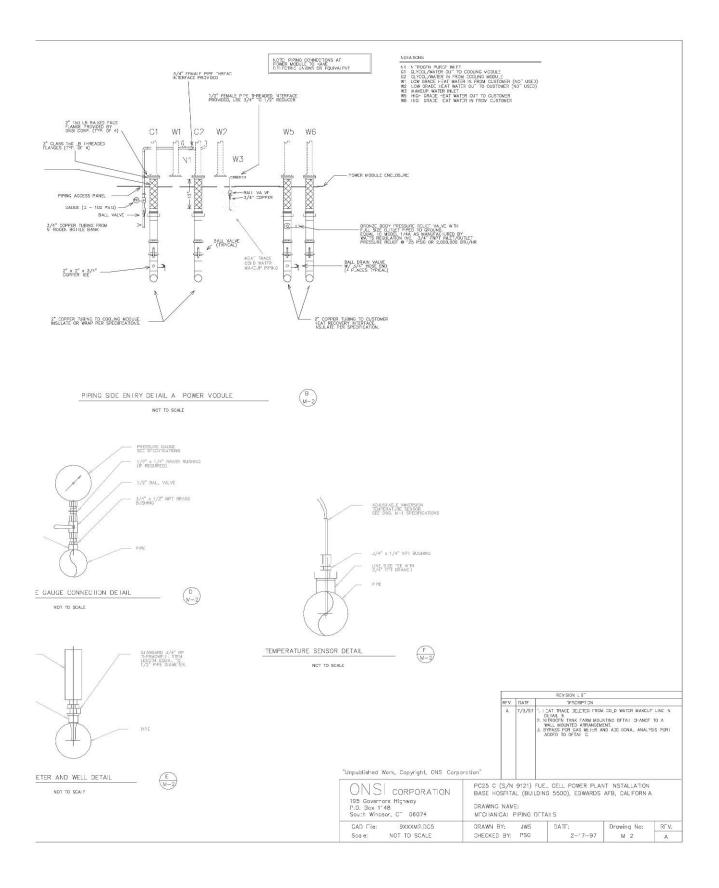


Figure 8. Final installation drawings – mechanical piping details.



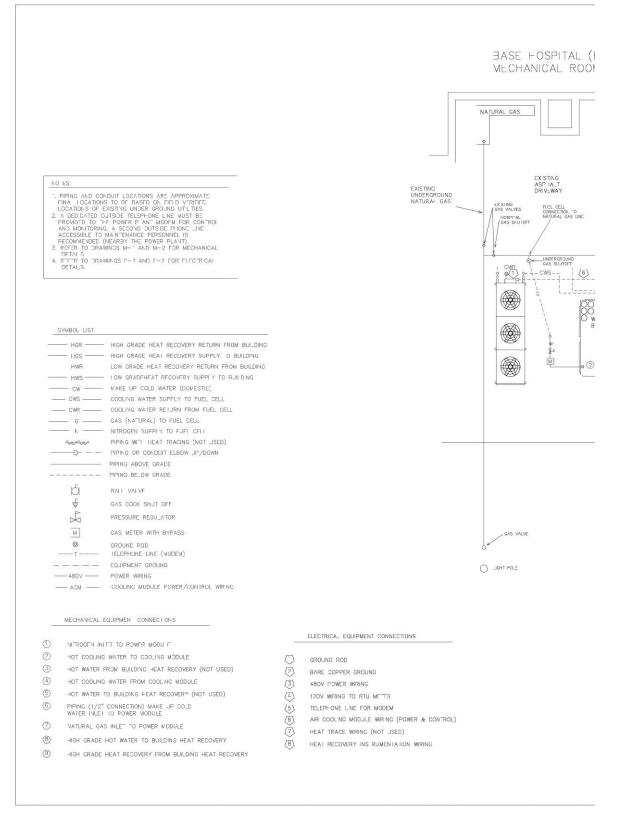
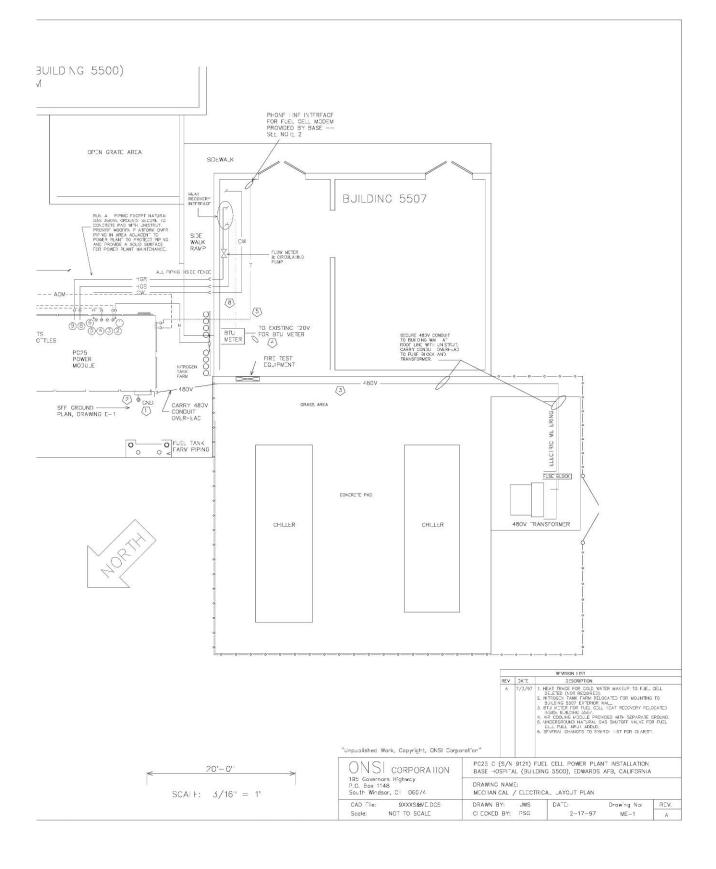


Figure 9. Final installation drawings – mechanical / electrical layout plan.



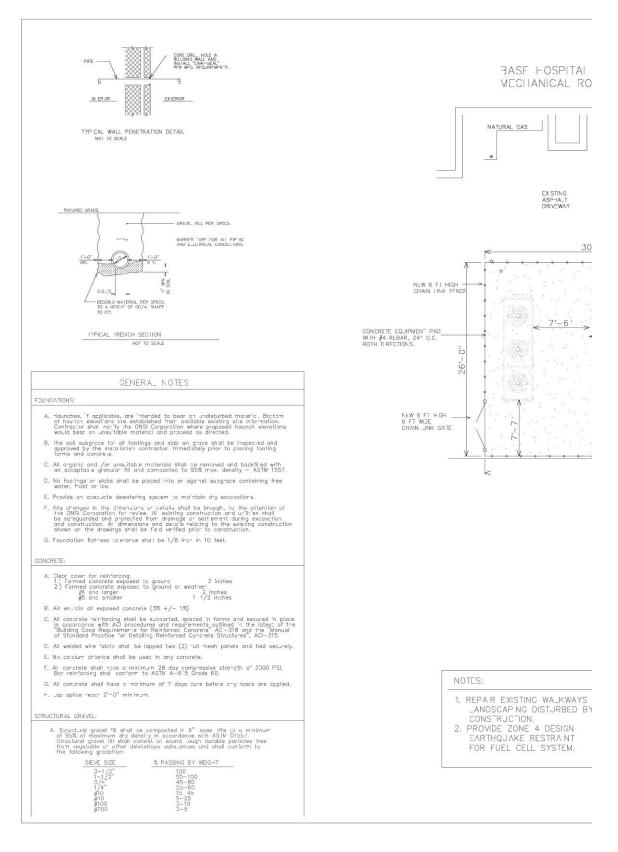
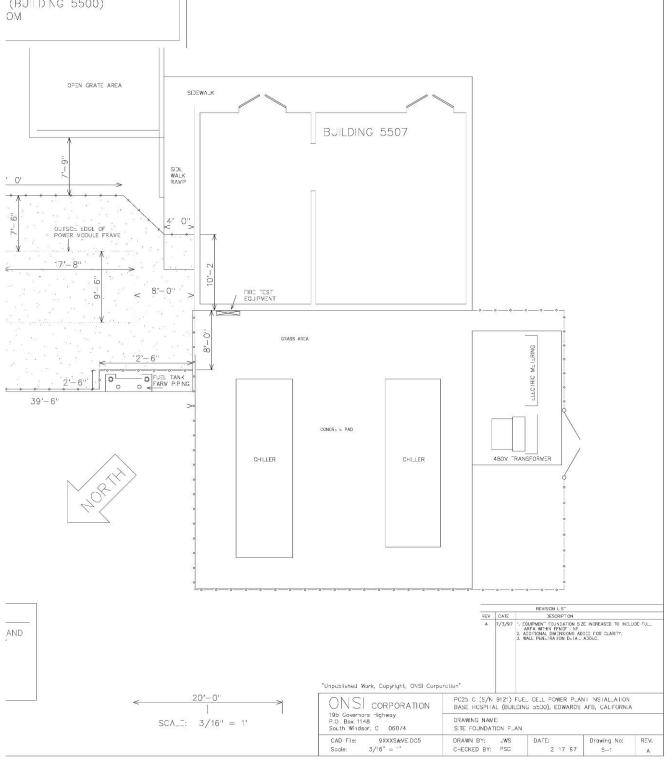


Figure 10. Final installation drawings – site foundation plan.





4 Fuel Cell Performance, Outage History and Maintenance Activities

4.1 Operating History

The fuel cell was started up in mid-June 1997. Acceptance tests were done between 23–25 June. (Appendix A includes the Acceptance Test Report.) Official data recording for the demonstration began on 17 July. The formal acceptance test meeting was held on 16 June, with title to the fuel cell transferred to the Edwards AFB using Form DD250. The power plant continued to operate until an event on 18 July 1997. A total of 27 power plant shutdowns were recorded between 17 July 1997 and the final shutdown on 1 July. 2002. There were 16 forced outages and 11 non-forced outages.

Performance data were collected via UTC Fuel Cells' RADAR data acquisition system. Using a modem and telephone line, the power plant was called daily to retrieve a "snapshot" of the current status. Included in the metrics collected were cumulative totals for hot time, load time, MWHrs, input fuel, etc. Thermal heat recovery was not monitored. These data records were then used to generate the various performance parameters discussed in this report.

A total of 28,358 operating load hours were recorded for the Hospital fuel cell. Of the 27 separate operating periods, eight had continuous fuel cell operating hours of more than 1,000 hours. The longest continuous operating period was 4,507 hours (~ 6 months) and occurred between 21 July 1999 and 25 January 2000. Table 4 lists the distribution of continuous periods of operation for this fuel cell.

12	su ibution of continuous nours o			
	Hours of Operation	Occurrences		
	Over 3,000 hours	3		
	2,001 - 3,000 hours	3		
	1,001 - 2,000 hours	2		
	751 - 1,000 hours	1		
	501 - 750 hours	5		
	250 - 500 hours	6		
	Less than 250 hours	7		

 Table 4. Distribution of continuous hours of operation.

Figure 11 shows the hours of operation and outages on a monthly basis for the entire demonstration period.

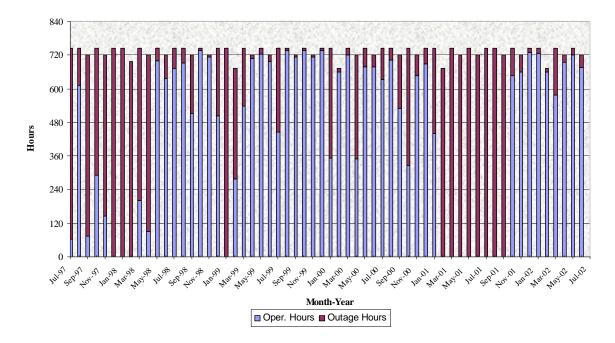


Figure 11. Fuel cell operating hours by month.

The fuel cell generated over 5.1 million kWh of electricity for the Hospital during the demonstration period. Average output of the fuel cell during operation was 179 kW over the 5+ year period. Table 5 lists data related to annual fuel cell electrical operation during the demonstration. The average output represents the fuel cell's average rate of electrical generation while the fuel cell was operating. The average rate of generation through 1999 was 194 kW, 97.2 percent of the fuel cell's nominally rated electrical output of 200 kW. For the period of 2000 to the end of the demonstration, the average generation rate was 164 kW, 82 percent of the fuel cell's nominally rated electrical output.

Year	Operating Hours	Generation (MWh)	Average Generation. (kW)
1997	1,024	192.8	188
1998	5,630	1,100.3	195
1999	7,340	1,426.5	194
2000	7,326	1,243.7	170
2001	2,823	447.2	158
2002	4,215	670.9	159
Total/Avg.	28,358	5,081.4	179

Table 5. Fuel cell electrical performance characteristics.

The RADAR system did not measure thermal utilization. Table 6 lists the input fuel data. The fuel cell consumed natural gas at an average rate of 1,744.3 cu ft/hour of operation or 9.7 cu ft/kW during the course of the demonstration.

Year	Input Fuel (cu ft)	Input Fuel (cubic ft/hr)
1997	1,200,000	1,788.4
1998	9,811,327	1,742.7
1999	13,824,858	1,883.5
2000	12,845,496	1,753.4
2001	4,713,880	1,669.8
2002	7,068,103	1,677.1
Total/Avg.	49,463,664	1,744.3

Table 6. Fuel cell input fuel characteristics.

Table 7 lists the fuel cell electrical efficiency based on higher heating value (HHV) for each year of operation. The average electrical efficiency over the course of the demonstration was 34.0 percent (HHV).

Year	Generation (MWh)	Input Fuel (cu ft)	Electrical Efficiency (% -HHV)*
1997	192.8	1,200,000	34.9
1998	1,100.3	9,811,327	37.2
1999	1,426.5	13,824,858	34.2
2000	1,243.7	12,845,496	32.1
2001	447.2	4,713,880	31.4
2002	670.9	7,068,103	31.5
Total/Avg.	5,081.4	49,463,664	34.0
*Higher Heating	Value (HHV) is based on a	natural gas heating valu	e of 1,030 Btu/cubic foot.

 Table 7. Fuel cell electric efficiency.

*Higher Heating Value (HHV) is based on a natural gas heating value of 1,030 Btu/cubic foot. Efficiency =([MWhrs x 1,000,000 Watt-hrs/MWhrs x 3.413 Btu/Watt] / [cu ft x 1,030 Btu/cu ft]) x 100

4.2 Fuel Cell Outage Summary

Between 17 July 1997 and 1 July 2002 (43,419 hours), the fuel cell had 27 outages resulting in 15,061.5 hours of down time. The fuel cell's availability was 65.3 percent:

 $65.3\% = ([43,419 - 15,061.5] / [43,419]) \ge 100$

Figure 12 shows the fuel cell's monthly availability.

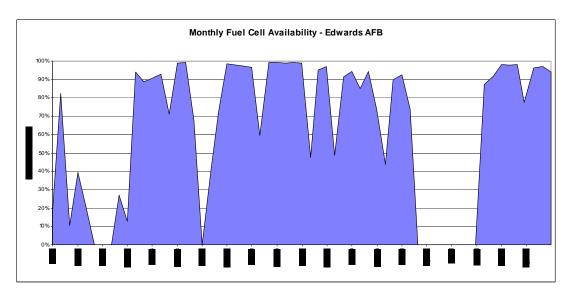


Figure 12. Monthly fuel cell availability.

The outages were identified from the RADAR performance monitoring system data. Because data records are collected on average once per day, outage times had to occasionally be interpolated. Sometimes the modem did not respond or the phone line was down, which prevented collection of a full complement of data records.

The longest outage was for 6,193 hours and occurred between 19 January and 14 October 2001. The next longest outage period occurred between 19 October 1997 and 12 February 1998 (2,556 hours). Table 8 lists the distribution of outage periods by hours of duration.

Outage Hours	Occurrences
Over 3,000 hours	1
2,001 - 3,000 hours	1
1,001 - 2,000 hours	1
751 - 1,000 hours	1
501 - 750 hours	1
250 - 500 hours	7
Less than 250 hours	15

 Table 8. Distribution of non-operational hours by duration.

Table 9 lists, in chronological order, the start and end dates/times, the outage duration hours, and the outage type for the 27 individual events. Appendix D has the complete list of outage codes for the PC25C fuel cell.

Outage No.	Off Date Stamp	On Date Stamp	Total Outage Hours	Hours to Next Outage	Туре	System	Part
Outage No.	on Date Stamp	7/17/97 09:34	Tiouis	25.93	туре	System	rait
1	7/18/97 11:30		307.50		N		
	, ,	7/31/97 07:00		630.40			
2	8/26/97 13:24	9/13/97 16:00	434.60	5.00	N		
3	9/13/97 21:00	9/22/97 12:58	207.97	70.53	F	TMS	
4	9/25/97 11:30	10/15/97 18:45	487.25	323.97	F	TMS	TCV830
5	10/29/97 06:43	2/12/98 18:35	2,555.87	269.00	F	TMS	
6	2/23/98 23:35	3/11/98 18:35	379.00	56.03	F	TMS	
7	3/14/98 02:37	4/21/98 17:13	926.60	91.70	Ν		
8	4/25/98 12:55	5/2/98 14:23	169.47	1,344.87	Ν		
9	6/27/98 15:15	7/1/98 15:00	95.75	243.57	F	WTS	LT450
10	7/11/98 18:34	7/13/98 21:00	50.43	881.28	Ν		
11	8/19/98 14:17	8/21/98 11:50	45.55	473.75	F	OTR	
12	9/10/98 05:35	9/18/98 15:15	201.67	2,264.75	F	OTR	
13	12/22/98 00:00	2/16/99 17:03	1,361.05	3,326.38	F	FPS	REF300
14	7/5/99 07:26	7/6/99 17:50	34.40	96.67	Ν		
15	7/10/99 18:30	7/21/99 12:00	257.50	4,507.42	F	OTR	CRL
16	1/25/00 07:25	2/1/00 23:00	183.58	656.33	F	APS	FCV140
17	2/29/00 07:20	2/29/00 16:47	9.45	708.72	N		
18	3/30/00 05:30	3/30/00 14:30	9.00	328.67	N		
19	4/13/00 07:10	4/27/00 21:21	350.18	636.00	F	TMS	TE431
20	5/24/00 09:21	5/26/00 13:00	51.65	2,953.67	N		
21	9/26/00 14:40	10/17/00 21:25	510.75	327.05	F	WTS	LT450
22	10/31/00 12:28	11/1/00 16:30	28.03	259.08	N		
23	11/12/00 11:35	11/14/00 19:30	55.92	520.50	F	OTR	CRL
24	12/6/00 12:00	12/8/00 15:30	51.50	1,007.25	F	NPS	CV720
25	1/19/01 14:45	10/4/01 16:07	6,193.37	4,189.30	N		
26	3/28/02 05:25	4/3/02 11:48	150.38	2,137.20	F	OTR	CRL
27	7/1/02 13:00	Final Shutdown			F	WTS	LT450

 Table 9. Fuel cell outage periods.

Category	Description
APS	Air Processing System
CVS	Cabinet Ventilation System
ES	Electrical System
FPS	Fuel Processing System
NPS	Nitrogen Purge System
OTR	Other
PSS	Power Section System
TMS	Thermal Management System
WTS	Water Treatment System

Table 10.	Forced	outage	categories.
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Table 11. For	ced outage	statistics.
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Category	Number of Occurrences	Total Outage Time	Min. Outage Time per Occurrences	Max. Outage Time per Occurrences	Avg. Outage Time per Occurrence
APS	1	183.6	183.6	183.6	183.6
CVS	0	0	0	0	0
ES	0	0	0	0	0
FPS	1	1,361.1	1,361.1	1,361.1	1,361.1
NPS	1	51.5	51.5	51.5	51.5
OTR	5	711.0	45.6	257.5	142.2
PSS	0	0	0	0	0
TMS	5	3,980.3	208.0	2,55.99	796.1
WTS*	3	606.5	N/A	510.8	303.3
	16	6,893.9			430.9
*Includes the final outage which has no time associated it.					

The fuel cell experienced a total of 15,061.5 hours of outage time consisting of 16 forced outages (F) and 11 non-forced (N) outages. Table 10 lists the forced outages, broadly classified by the major fuel cell sub-systems. Table 11 lists the forced outages by major system category, along with statistics related to frequency of occurrence and time duration.

Most of the forced outages were classified as Other (OTR) or Thermal Management System (TMS). (Each had five occurrences.) The most frequent number of Other outages were three, which were attributed to the controller (CRL) for a total of 463.8 hours of outage. The longest outage in the TMS category was 2,555.87 hours between October 1997 and February 1998 due to a problem with the sub stack. This occurred early on in the demonstration. Similar characteristics were also observed in other fuel cells installed in the southwestern region of the country, which included Camp Pendleton, Twentynine Palms, Davis-Monthan AFB, and Fort Huachuca. It was concluded that the hard water characteristics of the water supply was contributing to the water conductivity in the fuel cell. Hard water is water that contains a high level of dissolved minerals, most notably calcium and magnesium. The degree of hardness increases with increased levels of calcium and magnesium. When hard water is heated, the dissolved minerals come out of solution (precipitate) and attach to plumbing and heat exchangers. Water treatment systems were installed to control the water chemistry of these systems.

Figure 13 shows a graph of force outage occurrences. The cabinet ventilation system, electrical system, and power section system did not contribute to any forced outages during the demonstration. An outage associated with the water treatment system was the final outage in July 2002, which was not resolved.

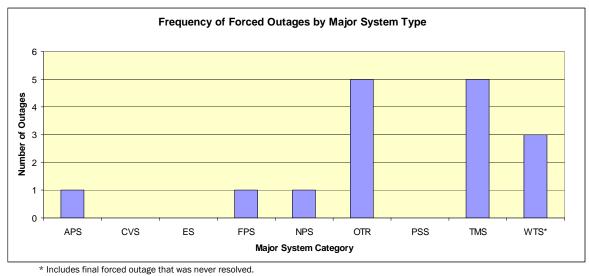


Figure 13. Forced outage occurrences by major system types.

Figure 14 shows the average duration of forced outage hours by major system category. The fuel processing system was associated with the highest average duration per outage (1,361.1 hours). (Note that this represents just one outage.) The next highest average duration per outage was associated with the thermal management system, with an average of 796.1 hours per occurrence over a total of five outages. The longest TMS outage was attributed to problems with the cooling-side of the fuel cell stack and occurred for 2,555.87 hours. The shortest duration TMS outage lasted for 208 hours and was attributed to a failure of a steam ejector.

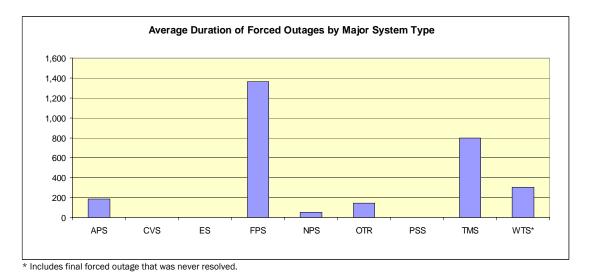


Figure 14. Average forced outage durations by major system types.

The outages that occurred most frequently for a specific fuel cell component were due to an alarm triggered by the water level transmitter (LT450). The three outages associated with this were for 95.75 hours in June 1998, 510.75 hours in September 2000 and for final outage in July 2002.

These data show that forced outages have a significant impact on the availability of the fuel cell. The shortest duration outage lasted for 45.6 hours. Five of the outages had a duration between 1 and 7 days. There were two outages that had a duration longer than 30 days, of which one was greater than 90 days. Figure 15 shows the outages by duration, which demonstrates that there is a high risk of not achieving the monthly demand savings in the economics for the fuel cell due to forced outages.

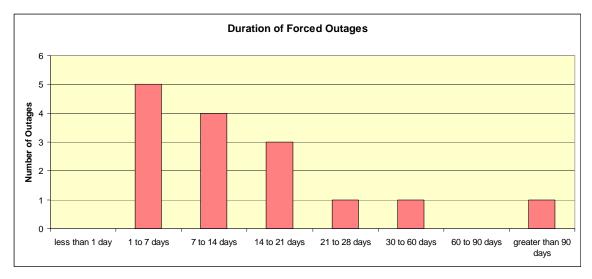


Figure 15. Number of forced outages by outage duration.

Figure 16 shows the distribution of forced outages by major system categories. The major system category contributing to most of the outage hours was the thermal management system (57.7 percent). The next highest category was the fuel processing system with 19.7 percent of the forced outage time.

Typical non-forced outages were due to the natural gas supply being turned off, site operator error, or scheduled maintenance activities. The longest non-forced outage occurred between January and October 2001 for a total of 6,193.37 hours. This outage was due to site personnel shutting off the natural gas supply to the fuel cell and opening the maintenance disconnect switch. This resulted in a hot shutdown of the fuel cell. UTC Fuel Cells informed Edwards AFB that this event could have a permanent negative impact on the fuel cell performance, specifically affecting the fuel cell stack. This outage occurred with approximately 22,000 stack load hours of the total 28,358 load hours for the fuel cell. Fuel cell electric efficiency as shown in Figure 17 shows a variation in efficiency occurring around 22,000 hours, but not a significant step change in the performance of the fuel cell after the time of the event.

4.3 Fuel Cell Stack Degradation

The trend of the fuel cell electrical efficiency based on the lower heating value of natural gas was analyzed based on the hours of fuel cell operation. The data were acquired through the UTC Fuel Cells' RADAR system. Data records are for fuel cell operation when the electrical output was greater than 50 kW to eliminate data from fuel cell testing and startup operation.

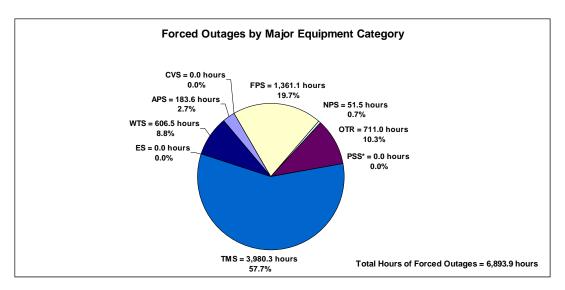


Figure 16. Total forced outage hours by major system types.

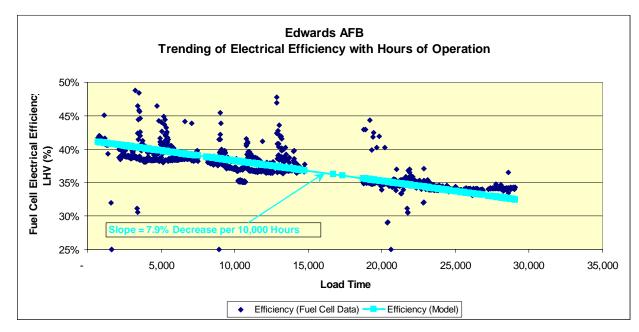


Figure 17. Fuel cell stack electrical efficiency degradation over time.

Note that the data records were not recorded on regular intervals and 1,435 data points were used for this analysis. The individual data points are plotted with hours of operation in an X-Y plot (Figure 17). The average electrical efficiency for the data is 37.2 percent.

A linear regression was conducted on the data to characterize average efficiency trends for the fuel cell. The regression equation is:

Electric Efficiency % (LHV) = ([Load Hours] x [-3.03424 x 10⁻⁴]) + 41.28840 Eq 1

The linear curve fit shows that the trend is a reduction in electrical efficiency with increasing hours of operation. Table 12 lists the resulting efficiencies at 5,000 load hour intervals.

Load Hours	Electrical Efficiency (%)
0	41.3%
5,000	39.8%
10,000	38.3%
15,000	36.7%
20,000	35.2%
25,000	33.7%

Table 12. Trend of electrical efficiency with fuel cell load hours.

The data in Table 12 show that the fuel cell electrical efficiency decreased 1.5 basis points for every 10,000 hours of operation. The regression shows that the average initial electrical efficiency of the fuel cell was approximately 41.3 percent and that it decreased at a rate of approximately 7.9 percent per 10,000 hours of operation. For example, the average decrease between 10,000 hours (38.3 percent) and 20,000 hours (35.2 percent) is:

7.9% = ([38.3% - 35.2%] / 38.3%).

The R Square statistic for the above regression is 0.22. This means that 22 percent of the variation seen in the trend of electrical efficiency can be attributed to load hours. Thus other factors in the system are significantly affecting the changes observed in electrical efficiency. The efficiency data (as shown in Figure 9) indicate sub-trends in electrical efficiency within the life of the fuel cell's operation. Figure 10 shows the outages and identification of major system changes. Each of the 27 outages is represented as a circle on the 45 percent efficiency line. The figure identifies regions of operational trends that are attributed to a major change to the system or lack of data. The number identifier presented for the change corresponds to the outage number listed in Table 8. The most significant changes were the installation of a new cell stack and the installation of an external reverse osmosis (RO) water treatment system (#5), and the installation of a new reformer (#13). For a period of approximately 4,000 load hours, the natural gas meter failed which resulted in the inability to determine the efficiency during this period.

The five operational regions shown in Figure 18 were analyzed to determine the electrical efficiency trend by major system change. The trend in efficiency for each region was determined by a linear regression and the slope is reported in terms of percent change per 10,000 hours of operation. Note that the unit of percent change per 10,000 is presented for consistency and only one of the regions evaluated (E) consists of 10,000 hours of data. Table 13 lists the dates, fuel cell load hours, system changes and electric efficiency trends for each of the time frames. For the regions analyzed, the R Square statistic is less than the 0.22 for the entire data set (B=0.05, C=0.02 and E=0.02). This indicates that the major system changes identified did not have a significant impact on the fuel cell performance and that this approach does not improve on the original efficiency trend model.

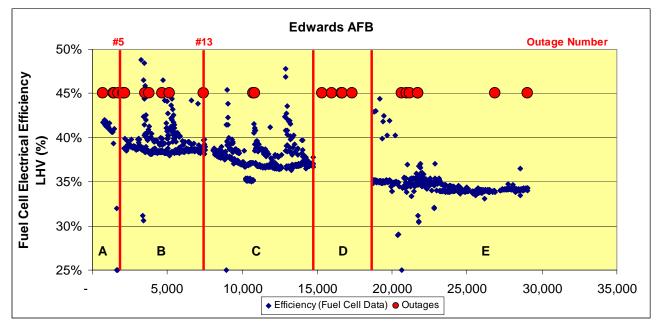


Figure 18. Electric efficiency trends with major system changes.

Table 13.	Major system	changes and	l electrical	efficiency trends.
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Range	Date	Fuel Cell Load Hours at End of Period	Change to System at Start of Period	Slope (% / 10000 hrs)
А	7/17/97 - 2/12/98	1,769	Initial system	-41.8%
В	1/12/98 - 2/16/99	7,407	Install new reformer	-15.0%
с	2/16/99 - 12/31/99	14,747	Install new cell stack and Install RO water treat- ment	-4.9%
D	12/31/99 - 6/29/00	18,168	Gas meter failure	No data
E	6/29/00 - 7/1/02	29,055	Gas meter repaired	-3.1%

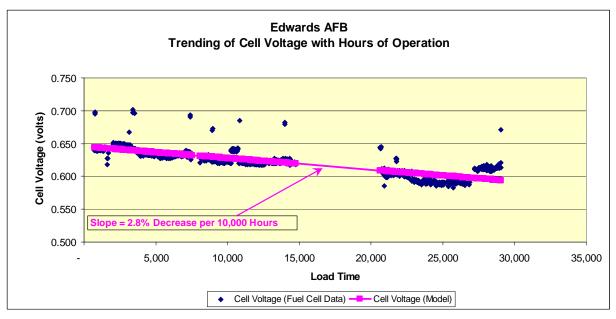


Figure 19. Fuel cell stack cell voltage degradation over time.

The trend of the fuel cell stack cell voltage based on the lower heating value of natural gas was analyzed based on the hours of fuel cell operation. The data are based on the same readings acquired through the UTC Fuel Cells RADAR system as the electrical efficiency data in the previous section. The individual data points are plotted with hours of operation in an X-Y plot. Figure 19 shows that the data fall into the typical operating range of 0.55 to 0.70 volts. The average cell voltage for the data is 0.623 volts. A linear regression was conducted on the data to characterize average cell voltage trends for the fuel cell. The resulting equation is: Cell volts = ([Load Hours] x [-1.7694 x 10-6]) + 0.645519 Eq 2

The regression shows a reduction in cell voltage with increased hours of operation. Table 14 lists the resulting cell voltages at 5,000 load hour intervals.

Load Hours	Cell Voltage (%)
0	0.646
5,000	0.637
10,000	0.628
15,000	0.619
20,000	0.610
25,000	0.601

 Table 14. Trend of cell voltage with fuel cell load hours.

The linear curve fit shows that the average initial cell voltage was approximately 0.646 volts and that it generally decreased at a rate of 2.8 per-

cent per 10,000 hours of operation. For example, the average decrease between 10,000 hours (0.628) and 20,000 hours (0.610) is:

2.8% = ([0.628 - 0.610] / 0.628)

This is equal to a cell voltage reduction rate of 0.018 volts per 10,000 hours of operation. The R Square statistic for the above regression is 0.61. This means that 61 percent of the variation seen in the trend of cell voltage can be attributed to load hours. Thus, other factors in the system are affecting the changes observed in cell voltage. The cell voltage data shown in Figure 11 indicate sub-trends in cell voltage during the life of the fuel cell's operation. Since the cell voltage is affected by the electrical output of the fuel cell, an additional analysis was conducted. The data were sorted by the fuel cell electrical output for the most frequent operating levels of 200 kW, 175 kW, and 150 kW. Then a linear regression was conducted for load hours greater than 5,000 hours (i.e., for the fuel cell after the stack was replaced). Table 15 lists the results of the analysis.

Fuel Cell Output	200 kW	175 kW	150 kW
Data points	950	256	110
R Square statistic	0.54	0.95	0.42
Slope (%/10,000 hrs)	-3.41%	-5.44%	-2.67%

Table 15. Cell voltage analysis by electrical output.

The analysis shows that the curve fit was very good for the 175 kW regression with an R Squared value of 0.95. This indicates that 95 percent of the decrease in cell voltage can be attributed to load hours for this data set. The 200 kW and 150 kW regressions have R Squared values that are lower than the original regression model, indicating that this approach does not improve the model for these two data sets. The slopes of the lines for the three power levels range from -2.67 percent to -5.44 percent per 10,000 load hours. Figure 20 shows the regression lines of the analysis for each data set projected over the entire fuel cell operating range.

While the efficiency remains relatively constant along the various fuel cell power levels, power plant cell voltages tend to increase at lower electrical output levels. This is most evident for fuel cell operation between 10,000 and 20,000 load hours. There is no data to indicate why the slope of the data varies at the different power levels.

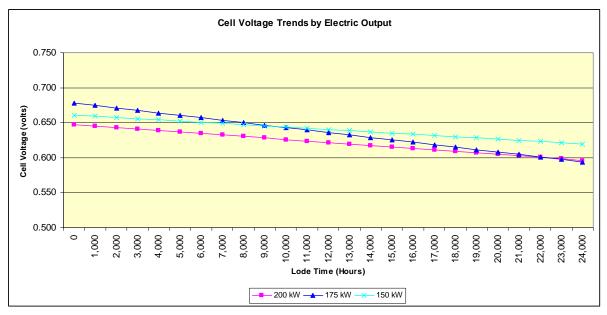


Figure 20. Cell voltage trends by electrical output.

4.4 Fuel Cell Maintenance Activities

UTC Fuel Cells had overall responsibility for maintenance on the fuel cell during the 5-year demonstration period. GBC Electrical Services, as the maintenance contractor, performed most maintenance activities under the guidance of UTC Fuel Cells. Invoices from GBC Electrical Services were obtained to assess maintenance activity levels. Table 16 lists the number of maintenance days at the site and total labor hours by year. No maintenance records were available for 2002.

Year	Days at Site	Labor Hours
1997	39	323
1998	42	344
1999	21	193
2000	29	222
2001	9	30
Total	140	1,112

Table 16. Maintenance days and labor hours by year.

Tables 17 through 21 present the date, labor hours, and a brief description of the maintenance activities that were billed between the years 1997 and 2001. Appendix E includes detailed cost and maintenance summary information.

1997	Labor Hrs	Description of Activity
10-Jun	10.0	Worked with UTC Fuel Cells at site.
11-Jun	9.0	Worked with UTC Fuel Cells at site.
12-Jun	11.5	Worked with UTC Fuel Cells at site.
13-Jun	2.5	Worked with UTC Fuel Cells at site.
16-Jun	8.0	Worked with UTC Fuel Cells at site.
17-Jun	10.0	Worked with UTC Fuel Cells at site.
	10.0	
18-Jun 19-Jun	8.0	Worked with UTC Fuel Cells at site. Worked with UTC Fuel Cells at site.
20-Jun	3.0	Worked with UTC Fuel Cells at site.
23-Jul	8.0	Worked with UTC Fuel Cells at site.
24-Jul	5.0	Worked with UTC Fuel Cells at site.
25-Jul	6.0	Worked with UTC Fuel Cells at site.
27-Aug	9.0	Changed nitrogen bottles.
5-Sep	6.0	Changed out resin bottles.
8-Sep	2.0	Changed nitrogen bottles.
9-Sep	0.0	Travel
20-Sep	13.0	Changed ejector assembly.
22-Sep	7.5	Restarted power plant.
26-Sep	3.5	Troubleshot ancillary cooling loop.
29-Sep	9.5	Replaced TVC830.
30-Sep	9.5	Started power plant.
6-Oct	16.0	Installed new controller. Restarted power plant and installed retrofits.
13-0ct	1.0	Worked with UTC Fuel Cells at site.
14-0ct	7.5	Worked with UTC Fuel Cells at site.
15-0ct	12.5	Worked with UTC Fuel Cells at site.
16-0ct	12.5	Worked with UTC Fuel Cells at site.
27-0ct	3.0	Worked with UTC Fuel Cells at site.
28-0ct	9.0	Worked with UTC Fuel Cells at site.
29-0ct	8.5	Worked with UTC Fuel Cells at site.
7-Nov	9.0	Worked with UTC Fuel Cells at site.
8-Nov	2.5	Worked with UTC Fuel Cells at site.
11-Nov	6.0	Worked with UTC Fuel Cells at site to go over wet-up procedure.
13-Nov	2.0	Worked with UTC Fuel Cells at site.
14-Nov	9.5	Started wet-up process.
17-Nov	9.5	Started wet-up process.
18-Nov	12.0	Started wet-up process.
19-Nov	7.0	Started wet-up process.
7-Dec	12.5	Prepared cell stack assembly for removal.

Table 17. Maintenance activities in 1997.	Table 17.	Maintenance a	activities	in 1997.
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1998	Labor Hrs	Description of Activity
10-Jan	22.0	Worked with UTC Fuel Cells on retrofits
12-Jan	7.5	Worked with UTC Fuel Cells on retrofits
13-Jan	5.0	Worked with UTC Fuel Cells on retrofits
2-Feb	4.0	Installed new strainer.
4-Feb	24.0	Installed new cell stack assembly.
5-Feb	9.0	Worked with UTC Fuel Cells at site.
10-Feb	3.5	Worked with UTC Fuel Cells to trouble shoot short in inverter.
11-Feb	9.0	Troubleshot, disassembled and re-assembled inverter.
12-Feb	2.0	Started power plant.
22-Feb	6.5	Worked with UTC Fuel Cells personnel on phone. Restarted power plant.
24-Feb	6.0	Checked ejector and FCV012 for proper movement. Started power plant.
5-Mar	3.0	Took measurements on old inverter drawer.
6-Mar	8.0	Removed and replaced inverter drawer No. 3 and attempted to start power plant.
11-Mar	6.0	Removed and replaced FCV110 and restarted power plant.
7-Apr	15.0	Worked on high grade heat exchanger skid retrofit.
8-Apr	17.0	Worked on high grade heat exchanger skid retrofit.
9-Apr	5.5	Worked on high grade heat exchanger skid retrofit.
13-Apr	18.0	Worked on high grade heat exchanger skid retrofit.
14-Apr	23.0	Worked on high grade heat exchanger skid retrofit.
15-Apr	20.0	Worked on high grade heat exchanger skid retrofit.
16-Apr	27.0	Worked on high grade heat exchanger skid retrofit.
17-Apr	5.5	Troubleshot and repaired short in power conditioning system.
20-Apr	2.0	Replaced pop out fuse for UPS.
21-Apr	8.0	Started power plant.
28-Apr	3.0	Worked with UTC Fuel Cells at site.
29-Apr	6.5	Worked with UTC Fuel Cells at site.
30-Apr	6.5	Worked with UTC Fuel Cells at site.
30-Apr	1.0	Travel
18-Jun	3.0	Tested water, burner air and cathode air. Completed new checklist.
30-Jun	6.0	Plugged reverse osmosis unit back in. Replaced fuse in cooling towers.
1-Jul	5.0	Restarted power plant.
8-Jul	3.5	Took amp readings on cooling tower.
13-Jul	4.5	Took override off LCV452. Changed nitrogen bottles. Started power plant.
10-Sep	4.0	Tested fuses in the cooling tower.
11-Sep	5.0	Troubleshot tripped breaker No. 33.
12-Sep	5.0	Put in new Ground Fault Interrupter (GFI) and new breaker. Breaker still tripped.
17-Sep	6.5	Tested circuit breaker No. 33.
18-Sep	8.5	Installed six temperature testers. Started fuel cell and left running at 200 kW.

Table 18. Maintenance activities in 1998.

1998	Labor Hrs	Description of Activity
12-0ct	5.0	Changed resin and charcoal bottles.
11-Dec	6.0	Recorded water treatment system and pump 400 data. Cleaned filters 100 $\&$ 150.
22-Dec	5.5	Took stack voltage readings. Fixed leak on water bottles. Removed humidity sensor. Checked pump 451 on/off times. Checked R/O unit power on.
28-Dec	3.0	Tested TE's on reformer.

1999	Labor Hrs	Description of Activity
8-Jan	2.0	Reset lockout relay. Filled accumulator. Filled tank 450 to 30 in Left power plant in P30-S30.
12-Jan	24.0	Prepared reformer for removal.
13-Jan	10.0	Completed reformer preparations.
24-Jan	2.0	Started taking doors and frame apart.
26-Jan	12.0	Removed old reformer and put in new reformer.
28-Jan	5.0	Began quarterly maintenance on power plant.
1-Feb	16.0	Started annual maintenance. Set up for welders.
2-Feb	16.0	Continued with annual service. Assisted/supervised welders. Installed retrofit.
3-Feb	16.0	Insulated reformer piping. Continued annual service.
4-Feb	13.0	Completed piping insulation and annual maintenance activities. Did hydro test.
9-Feb	10.0	Conducted hydro test on ancillary loop.
10-Feb	6.0	Completed site cleanup, seals on door and changed fans.
15-Feb	4.0	Worked with UTC Fuel Cells in troubleshooting ejector.
16-Feb	10.5	Installed ejector. Started power plant while doing reduction on reformer.
17-Feb	8.0	Conducted gas analysis and brought power plant up to 200 kW.
15-Apr	3.0	Built rack for nitrogen bottles.
6-Jul	6.0	Changed nitrogen bottles and tested all three legs of electricity coming into P/T. Started power plant.
12-Jul	4.0	Updated controller software to 4.1 and attempted to start power plant.
20-Jul	8.0	Started power plant. Updated software on Base's laptop computer and explained to site coordinator.
21-Jul	8.0	Traveled to site to retrieve data.
1-Sep	10.0	Changed out water treatment system bottles.

Table 19. Maintenance activities in 1999.

Table 20. Maintenance activities in 2000.

2000	Labor Hrs	Description of Activity	
1-Jan	11.0	Changed brake on FT140 and I/O modules for FT140.	
3-Feb	2.5	lushed charcoal bottle out and troubleshot pump 450.	
29-Feb	8.0	Replaced pump 451 & fan 800 motor. Started power plant, left running at 150 kW.	
30-Mar	8.0	Replaced Multi Source Discovery Protocol (MSDP) card & microchips for another MSDP card.	
18-Apr	6.0	Changed out electronic card underneath inverter and boost cards on white panel. Re- moved #3 motor from cooling tower.	

2000	Labor Hrs	Description of Activity
20-Apr	11.0	Removed #2 and #1 fan blades and motors from cooling tower. Replaced relay card.
26-Apr	6.0	Installed new motors and fan blades back into cooling tower.
27-Apr	6.0	Replaced relay card again with correct relay card. Started power plant and left running at 125 kW.
10-May	3.0	Changed master Digital Signal Processing (DSP) card and restarted power plant.
12-May	4.0	Changed slave DSP and CB rating module. Restarted power plant.
3-Jul	3.0	Back flushed charcoal bottle.
21-Sep	4.0	Troubleshot long feed water cycle and tried to repair leak.
28-Sep	6.0	Tri-annual maintenance.
29-Sep	5.0	Tri-annual maintenance.
2-Oct	18.0	Tri-annual cleaning.
3-Oct	20.0	Tri-annual cleaning.
4-Oct	16.0	Tri-annual cleaning.
5-Oct	14.0	Tri-annual cleaning.
6-Oct	8.0	Cleaned condenser and attempted to start power plant.
11-0ct	7.0	Replaced air conditioner.
12-0ct	10.0	Rewired air conditioner. Attempted to start power plant.
16-0ct	6.0	Attempted to start power plant.
17-0ct	10.0	Troubleshot failed attempted to start power plant. Purchased UPS battery.
18-0ct	4.0	Installed UPS battery. Started power plant.
23-0ct	4.0	Tuned up power plant.
24-0ct	2.0	Changed brake.
1-Nov	6.5	Troubleshot process flame off and restarted power plant.
14-Nov	6.0	Installed new controller and started power plant. Left running at 175 kW.
8-Dec	7.0	Restarted power plant and took sub stack readings.

Table 21. Maintenance activities in 2001.

2001	Labor Hrs	Description of Activity
23-Jan	1.0	Turned power on and put power plant in water conditioning.
5-Mar	5.0	Checked thermal management system and water treatment system for leaks. Preformed pressure test on TMS loop.
6-Jun	1.0	Checked on modem - no communication.
8-Jun	2.0	Applied power to power plant. Extended TE350 to CSA. Cleaned heaters 310A & 310B.
16-Jul	2.0	Reset motor controllers for pumps 400, 450 and 830. Put power plant back in water conditioning. Rewired TE350.
4-Oct	7.0	Checked and started power plant.
5-Oct	7.0	Changed WTS bottles. Tuned power plant at all power levels, checked heat recovery sys- tem.
9-Oct	4.0	Rebuilt circulating pump for heat recovery system. Reset parameters for heat recovery system.
15-Nov	1.0	Removed and replaced TCV400.

4.5 Fuel Cell Retrofits

As part of the fuel cell demonstration and overall fuel cell development, UTC Fuel Cells refined the fuel cell design based on operational experience gained through the operation of the fleet of fuel cells. These improvements and modifications were classified as retrofits. Once a retrofit was developed, it would be incorporated into the production of new fuel cells or retrofit in the field for installed fuel cells. The details of the retrofits are considered proprietary information by UTC Fuel Cells and are not available for this report. The data in Tables 17 through 21 indicate that five retrofits (Table 22) were added to the fuel cell in the field.

Date of Retrofit Retrofit Description	
Oct. 1997	Install new controller and software
Jan. 1998	Upgrade base drive in inverter
Jan. 1998	Install strainer and filter in TMS
Apr. 1998	Replace high grade heat exchangers (redesign)
Feb. 1999	Replace breakers with higher grade version

Table 22. Summary of fuel cell retrofits.

Fuel Cell Operation and Outage Summary

Figure 12 shows the operational and outage periods for each hour within the 62 months that the fuel cell was active (June 1997 to July 2002). The outage times are highlighted in gray along with a listing of the outage number, duration in hours and minutes, and a brief description of the shutdown. Days where on-site maintenance was performed is shown graphically by an 8 hour box. GBC Electrical Services, the maintenance contractor, provided maintenance activity records.

5 Fuel Cell Economics

5.1 Hospital Energy Costs

The Base purchases electricity from Southern California Edison (SCE) under a time of use rate schedule, TOU-8. This rate has summer and winter seasons consisting of on-peak, mid-peak and off-peak time periods with associated demand and energy charges. The Base also purchases electricity from the Western Area Power Administration (WAPA) for a percentage of its total electricity requirements. Because the WAPA portion of the electricity was assumed to be significantly smaller than the SCE portion as discussed in ERDC/CERL TR-01-60, the focus of the economics will be based on the SCE TOU-8 rates. This rate has a summer and winter season consisting of on-peak, mid-peak, and off-peak time periods. Table 23 summarizes the structure of the TOU-8 tariff.

	Summer	Winter
Months	June – September	October – May
On Peak Period	Noon – 6:00 pm	None
Mid-Peak Period	8:00 am – Noon 6:00 pm – 11:00 pm	8:00 am - 9:00 pm
Off-Peak Period	All other hours and holidays	All other hours and holidays
Charges	Facility Charge (\$/meter) Energy Charge (\$/kWh) Facility Related Demand Charge (\$/kW) Time Related Demand Charge (\$/kW) Excess Transformer Capacity (\$/kVA) Power Factor Adjustment (\$/kVA)	Facility Charge (\$/meter) Energy Charge (\$/kWh) Demand Charge (\$/kW) Excess Transformer Capacity (\$/kVA) Power Factor Adjustment (\$/kVA)

Table 23. SCE TOU-8 rate structure.

The Base purchases the natural gas commodity from the Defense Fuel Supply Center (DFSC) and the natural gas transportation is provided by the Pacific Gas and Electric Company (PG&E).

The Base did not provide Base-wide or Hospital energy usage or cost information for the fuel cell demonstration time period. To estimate the fuel cell economics, the average electric and natural gas rates used from another customer involved in the DoD Fuel Cell Demonstration Program (Twentynine Palms, CA) were used to approximate cost savings. Both facilities purchase electricity from SCE under the same rate schedule, but purchase natural gas through different suppliers. Table 24 lists the annual average electric and natural costs used for the fuel cell economics analysis.

Average Energy Costs	1997	1998	1999	2000	2001	2002
Electricity (\$/kWh)	\$0.1040	\$0.1017	\$0.1017	\$0.1017	\$0.1500	\$0.1500
Natural Gas (\$/therm)	\$0.5800	\$0.4080	\$0.4080	\$0.4810	\$0.9500	\$0.7000

 Table 24. Annual electric and natural gas costs.

Note that electric and natural gas costs were extremely volatile and high during the years of 2001 and 2002 when California was experiencing the energy crisis brought on by deregulation.

5.2 Fuel Cell Maintenance Costs

Table 25 lists maintenance costs from GBC Electrical Services between 1997 through the end of the 2001. Although the fuel cell was restarted once in 2002, invoices for that service call and others were not available for this report.

Category	1997	1998	1999	2000	2001	Totals
Labor Hours	323	342	193.5	218	30	1,107
Labor Costs	\$16,788	\$18,025	\$9,970	\$12,208	\$2,020	\$59,010
Nitrogen Costs	\$2,072	\$2,128	\$836	\$885	\$135	\$6,057
Charcoal (cu ft)	0	2	2	2	2	8
Charcoal Costs	\$0	\$186	\$206	\$186	\$186	\$764
Resin (cu ft)	24	8	9	8	8	57
Resin Costs	\$6,490	\$1,808	\$2,420	\$2,160	\$2,240	\$15,118
Other Costs	\$9,512	\$6,217	\$4,752	\$2,079	\$1,721	\$24,282
Travel Costs	\$6,413	\$8,238	\$4,868	\$9,141	\$3,934	\$32,594
Shipping Costs	\$309	\$205	\$25	\$23	\$0	\$562
Totals	\$41,583	\$36,808	\$23,077	\$26,682	\$10,237	\$138,386
Note:. Maintenand	e data was	not available	e for 2002.			

Table 25. Summary of fuel cell maintenance costs.

The cost of maintenance over the entire operating period is estimated at \$138,386. Again, the maintenance costs for 2002 are not included as the information was not available. These costs correspond to an average maintenance cost of \$27,677/year or 2.72 cents/kWh (\$138,386/ 5,081,500 kWh) for all the electricity supplied to the Hospital. *Note that the maintenance costs presented do not include the cost of any parts or labor provided by UTC Fuel Cells to repair or modify the fuel cell.*

Figure 21 shows that labor was the highest cost category at \$59,010, representing 42.6 percent of total maintenance costs. Labor hours averaged 221 man-hours per calendar year. The highest number of man-hours in a calendar year was 342 in 1998. Nitrogen costs totaled \$6,057 and represents only 4.4 percent of the total maintenance costs. Spread across the 27 outages that occurred, the average cost of nitrogen was \$224 per outage. While charcoal used in the water treatment system was a relatively minor cost (~\$150/year), resin was a moderate program cost totaling approximately \$15,000 or 10.9 percent of the maintenance costs. Resin costs were \$533 per 1000 operating hours. The second highest cost category behind labor was travel costs, at 23.6 percent. Appendix E presents maintenance costs by invoice date.

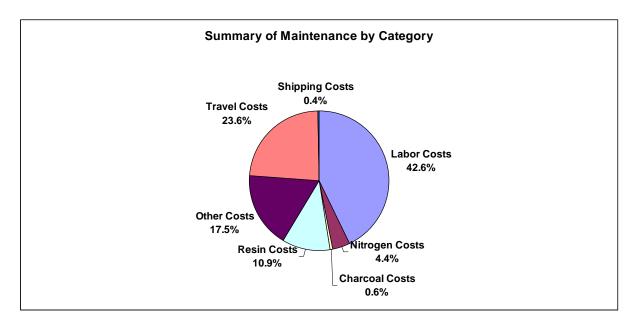


Figure 21. Summary of maintenance costs by category

Figure 22 presents the trend in annual maintenance costs for the fuel cell. Note that the costs for 1997 are for less than 6 months of the demonstration as the fuel cell data collection started on 17 July 1997. The fuel cell concluded operation on 1 July 2002. The high costs on 1997 and 1998 are attributed to the hard water problems which resulted in the replacement of the cell stack and the installation of an external water treatment system.

Fuel cell maintenance costs for the 5-year demonstration period were included in the original purchase contract with the fuel cell manufacturer. First year maintenance costs were included in the original fuel cell purchase price. The final 4 years of contract maintenance paid by ERDC/CERL was \$98,223, at an average of \$24,556 per year.

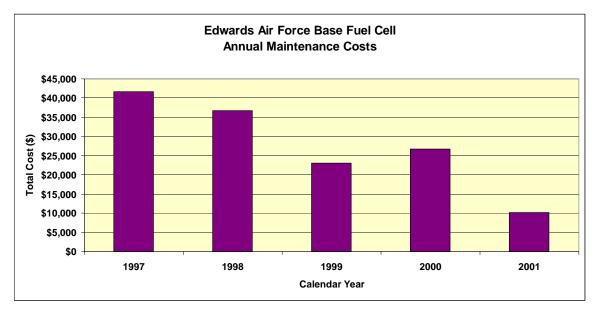


Figure 22. Annual trend in fuel cell maintenance costs.

5.3 Fuel Cell Energy Savings

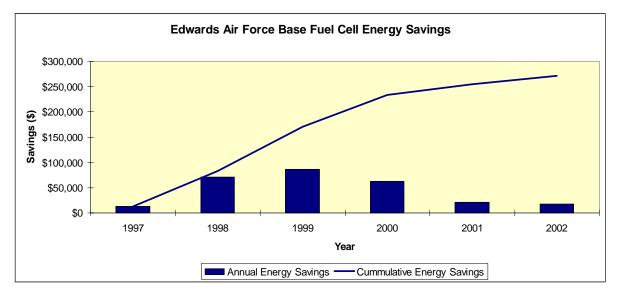
Energy savings from the fuel cell were calculated based the annual performance data collected through the UTC Fuel Cells RADAR system and the assumed electric and natural gas costs presented in Table 25. Note that the RADAR system did not monitor the thermal heat recovery loop on the fuel cell. Therefore, no data are available to estimate the value of the heat recovered by the Hospital from the fuel cell. Notes from the fuel cell acceptance test indicate that an artificial thermal load had to be established to demonstrate the heat recovery functionality because there was insufficient load at the Hospital. It is inferred that the level of heat recovery was not significant. Table 26 lists the fuel cell energy savings. Net energy savings without heat recovery over the entire program were \$304,145.

			0	0	-		
	1997	1998	1999	2000	2001	2002	Total
Electric Savings Thermal Savings*	\$20,053	\$111,896	\$145,079	\$126,488	\$67,076	\$100,640	\$571,232
Total Savings	\$20,053	\$111,896	\$145,079	\$126,488	\$67,076	\$100,640	\$571,232
Natural Gas Costs	\$7,169	\$41,191	\$58,041	\$63,601	\$46,125	\$50,961	\$267,087
Net Savings	\$12,884	\$70,706	\$87,038	\$62,888	\$20,950	\$49,678	\$304,145
*Thermal heat recovery data was not monitored by UTC Fuel Cells' RADAR system.							

Table 26. Annual energy savings at hospital.

Overall electric savings were \$571,232 with a maximum annual savings of \$145,079 occurring in 1999. The cost of natural gas to operate the fuel cell

totaled \$267,087 over the course of the demonstration and corresponds to a fuel cost for electrical generation of \$0.0526/kWh (\$267,087/ 5,081,400 kWh). Figure 23 shows the trend in annual energy savings.





5.4 Fuel Cell Lifecycle Costs

The fuel cell lifecycle cost analysis is presented for the operational life of the fuel cell at Edwards AFB. The installed cost of the fuel cell was \$1,260,727. The lifecycle cost analysis uses the utility rates presented in Section 5.1, the maintenance costs presented in Section 5.2 and the savings presented in Section 5.3. Note that the analysis is based on the average cost of electricity that the Hospital is charged. That is to say that demand savings are not calculated separately in the analysis. A review of the data shows that demand savings would have been realized in only 20 of the 59 full months of operation and that the average demand reduction for the 20 months would have been 184.8 kW. In 1999, demand savings could have been realized in 9 of the 12 months. In 1998 and 2001, demand savings could have been realized in 2 of the 12 months. The criterion for determining demand savings is that the fuel cell was operational during all hours of the peak period hours for the calendar month. Table 27 lists the months in which demand savings could have been attributed to the fuel cell and the average output of the fuel cell during the month.

Month of Demand Savings	Fuel Cell Demand Savings
Oct 1998	200
Nov 1998	200
Mar 1999	200
Apr 1999	196
May 1999	200
Jun 1999	186
Aug 1999	200
Sep 1999	197
Oct 1999	200
Nov 1999	199
Dec 1999	200
Jun 2000	125
Jul 2000	200
Aug 2000	200
Nov 2001	175
Dec 2001	175
Jan 2002	173
Feb 2002	170
May 2002	150
Jun 2002	150
Average Demand:	184.8
Number of Months:	20

Table 27.	Fuel cell	demand	savings.
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The data listed in Table 28 summarize the lifecycle cost analysis. The analysis allocates the capital cost of the fuel cell in the 1997 calendar year. In addition, values are actual costs and are not adjusted to a base year. The analysis shows that the operational costs exceeded the savings in 2001 and that the cumulative operational savings were \$158,545.

	1	1	ycie cost an	-		
	1997	1998	1999	2000	2001	2002
HOURS OF OPERATION						
Operation Hrs/Yr	1,024	5,630	7,340	7,326	2,823	4,215
Total Operation Hours	1,024	6,654	13,995	21,320	24,123	28,358
Hours Since Overhaul	1,024	6,654	13,995	21,320	24,123	28,358
OPERATION VALUES	•	·			•	
Electrical Eff (%)	34.9%	37.2%	34.2%	32.1%	31.4%	31.5%
Thermal Eff (%)	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%
Demand Disp. (kW)	0	400	1,778	525	350	643
Electrical Output (MWh)	192.8	1100.3	1426.5	1243.7	447.2	670.9
Thermal Displ. (MMBTU)	0.00	0.00	0.00	0.00	0.00	0.00
Fuel Input (MMBTU)	1,236.0	10.105.7	14,239.6	13,320.9	4,855.3	7,280.1
AVERAGE ENERGY RATES	•	•		•	•	•
Demand Rate (\$/kW)	-	_	_	-	-	-
Electrical Rate (\$/kW)	0.1040	0.1017	0.1017	0.1017	0.1500	0.1500
Facility Gas Rate (\$/MMBTU)	5.80	4.08	4.08	4.81	9.50	7.00
Generator Gas Rate (\$/MMBTU)	5.80	4.08	4.08	4.81	9.50	7.00
GENERATOR SAVINGS / ENERGY	SAVINGS	•	L		•	
Demand	-	_	_	-	-	-
Energy	\$20.051	\$111,901	\$145,075	\$126,484	\$67,080	\$100,635
Displaced Fuel	\$0	\$0	\$0	\$0	\$0	\$0
Subtotal (\$)	\$20.051	\$111,901	\$145,075	\$126,484	\$67,080	\$100,635
COSTS	•	•	I		•	
Fuel Cost	\$7,169	\$41,231	\$58,098	\$63,641	\$46,125	\$50,961
Maintenance	\$2,222	\$53,823	\$27,428	\$28,485	\$26,470	\$7.029
Generator Overhaul	\$0	\$0	\$0	\$0	\$0	\$0
Subtotal (\$)	\$9,391	\$95,054	\$85,526	\$92,126	\$72,595	\$57,990
Annual Savings	\$10660	\$16,846	\$59,549	\$34,359	(\$5,515)	\$42,645
Cumulative Savings	\$10660	\$27,507	\$87,056	\$121,415	\$115,899	\$158,545
Installed Cost	\$1,260,727					
Net Cash Flow	(\$1,250,067)	\$16,846	\$59,549	\$34,359	(\$5,515)	\$42,645
Cumulative Cash Flow	(\$1,250,067)	(\$1,233,220)	(\$1,173,671)	(\$1,139,312	(\$1,144,828)	(\$1,102,182)

Table 28. Lifecycle cost analysis.

6 Summary and Conclusions

6.1 Review of Fuel Cell Demonstration at Edwards AFB

The 200 kW phosphoric acid fuel cell operated for 28,357.9 hours which corresponds to an availability of 65.3 percent. A total of 27 outages were recorded, 16 of which were classified as a "Forced Outage(s)." The fuel cell delivered more than 5,081 MWh of electricity to the Hospital facility at an average rate of 179 kW. The fuel cell electrical efficiency averaged 34.0 percent (HHV) over the course of the demonstration. Thermal heat recovery was not monitored for this fuel cell. The data listed in Table 29 summarizes the performance of the fuel cell operation.

	1997	1998	1999	2000	2001	2002	Totals
Fuel Cell Operation							
Hours in the Period	3.998.4	8,760.0	8,760.0	8,784.0	8,760.0	4,357.0	43,419.4
Fuel Cell Operation Hours	1,024.3	5,630.0	7,340.2	7,325.9	2,823.0	4,214.6	28,357.9
Fuel Cell Outage Hours	2,974.2	3,130.0	1,419.9	1,458.1	5,937.0	142.4	15,061.5
Availability	25.6%	64.3%	83.8%	83.4%	32.2%	96.7%	65.3%
Electrical Generation							
Total Generation (MWh)	192.8	1,100.3	1,426.5	1,243.7	447.2	670.9	5,081.5
Average Rate of Generation (KW)	188.2	195.4	194.3	169.8	158.4	159.2	179.2
Natural Gas Consumption	1,236.0	10,105.7	14,239.6	13,230.9	4,855.3	7,280.1	
Total Consumption (cu ft/hr)	1,200,000.0	9,811,327.0	13,824,858.0	12,845,496.0	4.713,880.0	7,068,103.0	49,463,664.0
Average Rate of Generation (cu ft/hr)	1,788.4	1,742.7	1,883.5	1,753.4	1,669.8	1,677.1	1,744.3
Heat Recovery							
Total Heat Recovered (MMBTU)	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Average Rate of Recovery (MMBTU)	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Efficiencies							
Electrical (%)	34.9%	37.2%	34.2%	32.1%	31.4%	31.5%	34.0%
PURPA* (%)	34.9%	37.2%	34.2%	32.1%	31.4%	31.5%	34.0%

Table 29. Summary of fuel cell performance.

The longest continuous period of operation was 4,507.4 hours, or about 6 months. The fuel cell stack had to be replaced once during the demonstration period and an external water treatment system had to be retrofit to the fuel cell due to high conductivity of the water. In addition, five fuel cell design retrofits were installed on the fuel cell which included a new controller and software as well as a new high grade heat exchanger system.

At the completion of the demonstration, the fuel cell was down due to a forced outage associated with the water treatment system. Edwards AFB has elected to keep the fuel cell and plans to restore operation at the current facility or to move it to another facility.

6.2 Lessons Learned

Based on the experience of installing, and operating the fuel cell, the following lessons learned can be considered:

- High conductivity of water, particularly due to the hardness of the water in the Southwest region of the U.S., must be addressed to prevent negatively impacting the performance of the fuel cell stack.
- Installation of the fuel cell is a relatively straightforward process with no major concerns at this site. The installation took 2 months from the authorization to commence construction to the completion of the acceptance testing (25 April 1997 to 25 June 1997).
- During the course of the demonstration, the fuel cell operation resulting an a cumulative savings of \$158,545 or \$31,700/yr. The level of energy savings was less than the anticipated \$72,500/yr to \$108,400/yr due to the following:
 - $\circ~$ The average fuel cell electrical output was 179 kW and not the anticipated 200 kW
 - The fuel cell availability was only 65.3 percent instead of 95 percent.
 - The level of heat recovery was not measured and therefore not included in the savings values.
 - The fuel cell was able to potentially reduce the demand of the Hospital in only 20 of the 59 months of the demonstration.
- The fuel cell experienced a total of 8,167.6 hours of non-forced outages attributed to due to the natural gas supply being turned off, site operator error or scheduled maintenance activities. The longest non-forced outage occurred in January to October 2001 for a duration of 6,193.37 hours due to site personnel shutting off the natural gas supply to the fuel cell and opening the maintenance disconnect switch.
- Most of the forced outages were categorized as Other and Thermal Management System issues. The total duration of forced outages was 6,893.9 hours or 46 percent of all outages.
- The average duration of a forced outage was 430.9 hours, or approximately 18 days.
- The maintenance costs averaged \$27,677/year, which represents an average cost of 2.72 cents/kWh. This does not include the equipment cost of the replacement cell stack, the reverse osmosis system, the re-

design high grade heat exchanger system, or the other hardware provided by UTC Fuel Cells.

- The average fuel cost to generate electricity was 5.26 cents/kWh. (\$267,087 / 5,081,500 kWh).
- The average operating and maintenance costs to generate electricity was 7.98 cents/kWh (5.26 cents/kWh [fuel cost] + 2.72 cents/kWh [O&M costs]). Note that this does not include the value of the heat recovered from the fuel cell. Over the same period of time, the average cost of electricity purchased from SCE is estimated to be 11.8 cents/kWh.

6.3 Issues for Further Analysis

The review and analysis of the 200 kW phosphoric acid fuel cell that was installed at Edwards AFB. resulted in the identification of several issues appropriate for further analysis:

- Water Quality Requirements. UTC Fuel Cells has identified through the demonstration that the hardness of the water impacts the fuel cell operation. The Edwards AFB fuel cell required the installation of a reverse osmosis water treatment system. The hardness level at which the fuel cell will require an RO system should be identified.
- **Fuel Cell Electrical Efficiency Trends.** The analysis of the electrical efficiency trends showed that in addition to the number of load hours, other factors affect the efficiency degradation. The secondary analysis that was conducted based on evaluating the trends between major system changes did not substantially improve on the ability to better quantify the electrical efficiency degradation. Further evaluation of trends of other demonstration fuel cells might provide more insight.
- Cell Voltage Trends. The analysis of the cell voltage trend showed that the trend for operation at the 175 kW output had the best regression with an R Squared value of 0.95. The 200 kW and 150 kW regressions have R Squared values that are lower than the original regression model indicating that this approach does not improve the model for these two data sets. The slopes of the lines for the three power levels range from -2.67 percent to -5.44 percent per 10,000 load hours. These trends should be further analyzed with additional C models to see if better characterizations can be developed.
- **System Design Improvements.** As part of the fuel cell demonstration and overall fuel cell development, UTC Fuel Cells refined the fuel cell design based on operational experience gained through the operation of the fleet of fuel cells. These improvements and modifications were classified as retrofits. The details of the retrofits are considered

proprietary information by UTC Fuel Cells and are not available for inclusion in this report. Investigation of maintenance activities for a larger number of C type fuel cells may provide greater insight into the modifications to the fuel cell design that can be attributed to the demonstration program.

Acronyms and Abbreviations

<u>Term</u>	Spellout
ACSIM	Assistant Chief of Staff for Installation Management
AFB	Air Force Base
AFCESA	Air Force Civil Engineer Support Agency
ANSI	American National Standards Institute
CEO	corporate executive officer
CERL	Construction Engineering Research Laboratory
CPW	U.S. Army Center for Public Works
CVS	Cabinet Ventilation System
DEIS	Defense Energy Information System
DFSC	Defense Fuel Supply Center
DOD	Department of Defense
DSP	Digital Signal Processing
ERDC	Engineer Research and Development Center
FPS	Fuel Processing System
GFI	Ground Fault Interrupter
HHV	Higher Heating Value
HPLC	high performance low chromatography
HQ	headquarters
I/0	input/output
ILIR	In-house Laboratory Independent Research
kW	Kilowatt
LHV	lower heating value
MSDP	Multi Source Discovery Protocol
N/A	not applicable
NFESC	Naval Facilities Engineering Service Center
NPS	National Park Service
ODUSD	Office of the Deputy Under Secretary of Defense
OMB	Office of Management and Budget
PAFC	Phosphoric Acid Fuel Cell
PG&E	Pacific Gas and Electric Company
PO	purchase order
PSS	Power Section System

<u>Term</u>	Spellout
PURPA	Public Utility Regulatory Policy Act
RO	reverse osmosis
RADAR	Radio Detection And Ranging
SAIC	Science Applications International Corporation
SCE	Southern California Edison
SERDP	Strategic Environmental Research and Development Program
SI	Systeme Internationale
TMS	Thermal Management System
TOC	Table of Contents
TOU	time-of-use
UPS	Uninterruptible Power Supply
URL	Universal Resource Locator
UTC	United Technologies Corp.
WAPA	Western Area Power Administration
WTS	Water Treatment System
WWW	World Wide Web

Appendix A: Fuel Cell Acceptance Test Report

ONSI CORPORATION

ON SITE ACCEPTANCE TEST REPORT

POWER PLANT: LOCATION: SIN 9061 NAVAL HOSPITAL MCAGCC TWENTY NINE PALMS, CALIFORNIA JUNE 16 THROUGH JUNE 21, 1995

TEST DATES:

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UNSI CORPORATION

01/23/95

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	DOD ACCEPTANCE TEST OF PC25 TM POWER PLANT INSTALLATION
	Following a normal power plant start-up, operate at IDLE for one hour.
	At the completion of the one hour, obtain prints of the following five
	(5) display screens.
	- KEY PARAMETERS (screen 09)
	- REACTANT SUPPLY SYSTEM (screen 10)
	- STACK LOOP, ANC LOOP, & WTS (Screen 11)
	- ELECTRICAL OVERVIEW (screen 14)
	- POWER CONDITIONER SYSTEM (screen 25)
	In the grid connect mode with unity power factor and no heat recovery,
	operate at each of the following powers for one hour. After one hour
	obtain prints of the five (5) screen displays outlined above. Also
	perform the additional demonstrations at 100 KW and 200 KW listed
	below which are accomplished after the one hour hold. The required
	display screen prints for verification are shown in brackets {}.
	* 50 KW
	* 100 KW
	- demonstrate leading and lagging power factor for 5 minutes
	* max leading power factor up to 0.85 within limitiations
	imposed by the grid {screen 14}
	¥ 0.85 lagging power factor {screen 14}
	* 150 KW * 200 KW (Rated Power)
	- demonstrate < 3% harmonic distortion [using THD meter
	across the output power breaker)
	- demonstrate 60 Hz \pm 3 Hz frequency [using a Fluke Model 87
	True RMS Multimeter or equivalent]
	 demonstrate leading and lagging power factors for 5 minutes x max leading power factor up to 0.85 within limitiations
	max leading power factor up to 0.85 within limitiations imposed by the grid {screen 14}
	× 0.85 lagging power factor {screen 14}
	- demonstrate minimum of 2 hours of heat recovery at time
	of normal site heat usage and consistent with site design
	x {screen 09 at beginning and end of demonstration
	plus screen 11 at beginning and every hour until
	heat recovery demonstration completed}
	<pre>x confirmation of 1900 SCFH ± 100 SCFH natural gas concurration during this two hour hold</pre>
	consumption during this two hour hold Grid Independent operation will be demonstrated at those sites where
	such capability is installed, at power conditions consistent with
	normal site demand. After one hour of grid independent operation,
	each of the five (5) screens displays noted above shall be printed as
	verification.
	- demonstrate 60 Hz ± 3 Hz frequency [using a Fluke Model 87
	True RMS Multimeter or equivalent] - demonstrate 480 volts ± 3%
	- <i>ACMANIACTACE</i> 400 10102 7 34

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3656:41	FT012ACT= 21.2 TE400FT	KWACNET=	2 VT310DEL= -0.91 EVEN TE012FT= 1495 CVERRI	
73400	SEFARATOR TEMP (PRIMARY)	370.2 D	EGF SETPOINT:	370.0
TE400R	SEPARATOR TEMP (BACKUP)	369.8 D	EGF SEP TEMP FACTOR (DEGF)	1.0
TS40CDBL	SEP TEMP DELTA	0.4 D	BGF	
LS450	WATER TANK LEVEL SWITCH	On	STK FLOW SW (FS400)	Qд
23431	POLISHER TEMP	75.7 D	BGF F/W TEMP SW (TS451)	On
TE810	CONDENSOR EXIT TEMP	138.8 D	EGF	
13820	CUST HEX HOT IN TEMP	153.3 D	EGF CUMHEATREC(MMBTU)	0.689
TES80	CUST REX COLD IN TEMP	90.G D	EGF FT880 FLOW (PPH)	21940
2E681	CUST HEX COLD EX TEMP	102.3 D	EGF REAT REC (MBTU/HR)	270
TE401	STACK COOLANT INLET TEMP	361.2 D	BGF	
LT400	SEPARATOR LEVEL	11.2 I	N	
PMP451 STARTTEMP IDCNET	WTS FEEDWATER PUMP TEMP FOR REF HEATUP MET DC CURRENT		ON TIME, MIN.(FWPUMP): BGF MPS	0
HTR4CO	SLEMENT "A"	OR	ELEMENT "C"	OB
	ELEMENT "B"	On	ELEMENT "D"	Off

KEY PARAMETERS (ENGLISH UNITS)								
P/P 9061 06/16/95	0653:	35	EVENTS	OVERR	IDE: C			
P 150 R 160 S 60 W 20	A 30 N	40 C	30 L 13 C 26	-	who a			
POWER OUTPUT (NET) POWER OUTPUT (GROSS) STACK CURRENT	2.5	KWAC	CPERATING TIME	0b./	HRS			
PCWER OUTPUT (GROSS)	56.3	KWAC	POWER FACTOR	0.90				
STACK CURRENT	239.1	AMES	CUMULATIVE POWER	0.839	MWHR			
STACK VOLTAGE	227.4	VOLTS	EALF STACK VOLTAGE	-0.09	VOLTS			
STACK VOLTAGR Volumetric fuel ficw	461.2	SCFE	FURE FROM RECPONNE	457.5	SCFH			
ACTUAL FUEL FLOW								
ZTOIO EJECTOR POSITION	18.9	÷	ZTO10 SETPOINT	13.1	9 .			
PHI MONITOR	1.03		TOTAL FUEL CONS	32622	SCF			
FT140 BURNER AIR FLOW	206.7	РРН	FT140 SETFOINT	210.0	РРК			
TE012 REFORMER TEMP			ZTILC POSITION	41.9	3			
TSOLER BACKUP REF TEMP		DEGY	TE012 SETFOINT		DEGE			
TEOCE HDS TEMP	499.7	DEGR	TE356 ANODE INLET TRM	P 395.6	DEGF			
TRACOST STEAM SEP TEMP	271.8	DECF	TE400 SETFOINT	379.0	DEGF			
TZ881 TEMP TO CUST	102.3	DEGF	RECOVERED HEAT	289	MBTU/HR			
			TE401 FOLISHER TEMP	75.7	DEGF			
LT400 SEPARATOR LEVEL	13.5	13	TESIO GLYCOL TEMP	1.46.8	DEGF			
PMP451 STATUS	Ōtt		TE160 MOTOR COMP AIR	68.7	DZGF			
			TE150 MOT COMP AIR IN	62.7	DEGE			
ELECTRICAL REFICTENCY	Z.0	8	press (NEXT PAGE> key		RM data			
			-					

0655:38	1DC- 243.5 VDC= 237 FTG12ACT= 21.4 1U400F P 150 R 160 S 60 W 20	WACNET T= 370	= 2 CE012	2T= 1494 🛹 - OVERB	NTS 0 LDE D				
TAG12 TEC12R TEC12REL	REF TURE TEMP (PRIMARY) REF TURE IEMP (BACKUP) REF TURE TEMP DELTA	1487.4	DEGF	SETPOINT: REF/FURL CONT OUTPUD:					
PTC12	RET TUBE TEMP DELTA ACTUAL MASS FUEL FLOW UNCORR. MASS FUEL FLOW ACTUAL VOLUME FUEL FLOW TOTAL FUEL CONSUMED	22.6	PPH	SECPOINT: TECLI FUES TEMP(DEGF) SECPOINT: PTOLE VENTURI(PSIA)	21.0 56.9 468.0 7.88				
Z2010	EJECTOR POSITION PHI MONITOR ANCOE INLET TEMP	19.0	έ	ERTPOINT: STEAM FLOW S.P.(PPH):	18.3				
TE002	NDS BED TEMP	499.3	DEGN	HTR002 STATUS:	Cr.				
ZTFRZY	REFORMER REFIGIENCY	77.6	£						
SLECTRICAL CV3RVISW 06/16/95 IDC= 239 VDC= 237 KWACNET= 2.5 VT310DBL0.91 EVENTS C 0657:53 FT012ACT+ 21.1 T3490FT= 369 T3012FT= 1498 P/P 9061 P 150 R 160 S 60 W 20 A 30 N 40 C 30 L 10 (126)									
0657:53	IDC= 239 VDC= 237 K FT012ACT+ 21.1 T3490F	WACNET= T= 369	2.5 T3012:	T= 1498 OVERRIE	NTS C ES O				
0657:53 P/P 9061 LOADTIME HOTTIM2 CELV	IDC= 239 VDC= 237 K FT012ACT+ 21.1 T3490F P 150 R 160 S 60 W 20 TOTAL LOAD TIME TOTAL HOT TIME AVG VOLTS PER CELL	WACNET= T= 369 A 30 N 66 120 .741	2.5 T3012: 40 C HR HR V/C	T= 1498 OVERRIE	INTS C ES O				
0657:53 P/P 9061 LOADTIME HOTTIM2 CELV	IDC= 239 VDC= 237 K FT012ACT+ 21.1 T3490F P 150 R 160 S 60 W 20 TOTAL LOAD TIME TOTAL HOT TIME AVG VOLTS PER CELL	WACNET= T= 369 A 30 N 66 120 .741	2.5 T3012: 40 C HR HR V/C	T= 1498 OVERRIE	:ES 0				
0657:53 P/P 9061 LOADTIME HOTTIM2 CELV ASF KWDC VT310DEL	IDC= 239 VDC= 237 K FT012ACT+ 21.1 T3400F P 150 R 160 S 60 W 20	WACNET= T= 369 A 30 N 66 120 .741 42 56.7 -0.91 239 99.3 4.4 1.9	2.5 T3012: 40 C HP HR V/C ASF KW V A 8 8 8 8 8 8	TT= 1498 30 L 10 I 26 VT310 HALF STK VOLT CELL EFFICIENCY (%) REF EFFICIENCY (%) HEAT RATE (BTU/KWHR)	-0.C8 59.3 75.5				

REACTAND BUPPLY SYSTEM

POWER CONDITIONER SYSTEM 06/15/95 IDC= 239 VDC= 237 KWACNET= 2.5 VT310DEL= -0.92 EVENTS 0 0658:49 FT012ACT= 21.1 TE400FD= 370.0 TE012FT= 1500.6 OVERRIDE 0 P/P 9061 P 150 R 160 S 60 W 20 A 30 N 40 C 30 L 10 (226) 483.7 V INV AC VOLTAGE, PHASE A PT001A PT001B INV AC VOLTAGE, PHASE B 480.6 ប INV AC VOLTAGE, PHASE C v 475.5 9T001C INV AC CURRENT, PHASE A 0.5 A CT001A CT001B INV AC CURRENT, PHASE B 0.0 А INV AC CURRENT. PHASE C Q.J. A CURRENT UNBAL (%) 0.0 CTC01C PTC03A NET AC VOLTAGE, PHASE A 494.5 V NET AC VOLTAGE, PHASE B 492.0 V PT003B NET AC VOLTAGE, PHASE C v VOLTAGE UNBAL (%) 1.0 489.2 9T003C v LINKADC LINK VOLTAGE 600.3 PERCENNE PERCENT FUNDAMENTAL 83.8 8 2.0 DEG PSREQ PHASE SHIFT REQUEST Off MCB901 G/1 BREAKER STATUS G/C BREAKER STATUS Off MCB002 INTER-TIE BREAKER STAT MCB003 On INTCOUNT INTERRUPT COUNT 0

KEY PARAMETERS (ENGLISH UNITS)										
P/P 9061 06/16/95	0837:0		EVENTS <u>:</u> 0	CVERR	IDE: 0					
<u>2 190 R 160 S 52 W 20</u>	<u>x 25 x</u>	49 5	30 L 10 🕧 50)							
CROWER_CUTRUT_(NET)	- South	KWAC	OPERATING TIME	68.4	HRS					
POWER CUTPUT (GROSS)	102.5	KWAC		-1.00						
STACK CURRENT	459.8		CUMULATIVE POWER							
STACK VOLTAGE	223.0	V0172	HALF STACK VOLTAGE							
VOLUMETRIC FUEL FLOW		SCFH	FUEL FLOW SETPOINT	850:7	SCFH					
	40.5	рън								
		8	20010 SETFOINT	23.7	3					
PHI MONITOR	0.98		TOTAL FUEL CONS		SCF					
FT140 BURNER AIR FLOW			FT140 SETFOINT		PPH					
	1523.4	DRGF	ZTIIO POSITION	45.7	8					
TE012R BACKUP REF TEMP	1522.1	DEGY	TE012 SETFOINT	1514.4	DEGF					
TEOC2 HDS TEMP	500.1	DEGF	TE350 ANODE INLET TEM	F 195.4	DEGF					
TE4007T STEAM SEP TEMP	357.7	DEGZ	TE400 SETPOIND	360.6	DEGF					
TESSI TEMP TO CUST	129.8	DEGF	RECOVERED HEAT	0	MBTU/HR					
			TR431 POLISHER TEMP	74.6	DEGF					
17400 SEPARATOR SEVEL	<u>11</u> 4	IN	TZ813 GLYCCL TEMP	139.3	DEGF					
FMP451 STATUS	Off		TEISS MOTOR COMP AIR	64.9	DEGF					
			T2150 NOT COMP AIR IN	67.6	DEGF					
ELECTRICAL SEFTCIENCY	20.5	à.	press «NEXT PAGE> key	to view	RM data					

0839:24	REACTANT S IDC= 457.6 VDC= 226 FT012ACT= 38.3 TE400FT P 360 R 160 S 60 W 20	<u>киасият</u> - 358	= <u>45</u> TE012	○ VT310DEL= -0.58 RVE FT= 1524 OVERE	NTS 0 1115 0
TE012 TE012R TE012DEL YT012ACT YTD12 SCFH YV2LTCT	REF TUBE TEMP DELTA ACTUAL MASS FUEL PLOW UNCORK, MASS FUEL FLOW ACTUAL VOLUME FUEL FLOW	1522.5 1.7 38.3 42.0 851.7	DSGF DEGF PPH PPH CFN	REF/FUEL CONT OUTPUT: SETPOINT: TEO11 FUEL TEMP(DEGF) SETPOINT:	37.0 71.1 900.4
ZTC10 FRIMON TE350	EJECTOR POSITION PHI MONITOR ANODE INLET TEMP	24.5 1,13 396.6	₽DEGF	SETFOINT: STEAM FLCW S.F.(PPH):	23.3 143.8
T3C02	EDS BED TEMP	500.1	CEGF	HTROOZ STATUS:	On
3PPRB7	REFORMER EFFICIENCY	80.7	8		
0549:06	STACK LOCI IDC= 459.9 VDC= 223 (PT012ACT+ 41.2 TE400PT= P 160 R 160 S 60 W 20 /	WACNET 359.9	- <u>4</u> TE013	9) VT310DEL= -0.78 EVE 27T- 1511 OVERR	NTS O IDY O
0549:06	IDC= 459.9 VDC= 223 (PT012ACT+ 41.2 TE400PT= P 160 R 160 S 60 W 20 / SEPARATOR TEMP (PRIMARY) SEPARATOR TEMP (BACKJP) SEF TEMP DELTA WATER TANK SEVEL SWITCH DOLISER TEMP	WACNET 359.9 359.9 359.9 259.3 0.4 On 74 6	TE012 40 C DSGF DSGF DEGP DEGF	9) VT310DEL= -0.78 EVE 27T- 1511 OVERR	IDF C 358.3
0549:06 P/P 9061 TE40CR TE40CR TE40D3L US450 TE401 TE820 TE820 TE820 TE820 TE820 TE821 TE821 TE8401 UT400	IDC= 459.9 VDC= 223 (PT012ACT= 41.2 TE400PT= P 160 R 160 S 60 W 20 P SEPARATOR TEMP (PRIMARY) SEP TEMP DELTA WATER TANK SEVEL SWITCH POLISHER TEMP CONDENSOR EXIT TEMP CUST HEX HOT IN TEMP CUST HEX COLD IN TEMP STACK COOLANT INLET TEMP SEPARATOR LEVEL	WACNET: 359.9 359.9 259.3 0.4 0n 74.6 139.9 173.8 172.9 123.6 339.0 11.2	4 TE012 40 C DSGF DEGF DEGF DEGF DEGF DEGF DIGF DIGF DIGF IN	9) VT310DEL= -0.78 EVE 27T- 1511 OVERR 30 L 10 I 50 SETPOINT: SEP TEMP FACTOR(DEG2) STK FLOW SW (FS400)	1DF 0 358.3 1.0 On On
0549:06 P/P 9061 TE40CR TE40CR TE40D3L US450 TE401 TE820 TE820 TE820 TE820 TE820 TE821 TE821 TE8401 UT400	IDC= 459.9 VDC= 223 (PT012ACT= 41.2 TE400PT= P 160 R 160 S 60 W 20 P SEPARATOH TEMP (PRIMARY) SEP TEMP DELTA WATER TANK SEVEL SWITCH POLISHER TEMP CONDENSOR EXIT TEMP CUST HEX HOT IN TEMP CUST HEX COLD IN TEMP CUST HEX COLD IN TEMP STACK COOLANT INLET TEMP SEPARATOR LEVEL WTS FEEDWATER PUMP TEMP FOR REF HEATUP	WACNET: 359.9 359.9 259.3 0.4 0n 74.6 139.9 173.8 172.9 123.6 339.0 11.2	4 TEO12 40 C DSGP DEGP DEGF DEGF DEGF DEGF IN DEGF	<pre>9) VT310DEL= -0.78 EVE 2FT- 1511 OVERR 30 L 10 I 50 SETPOINT: ESP TEMP FACTOR(DEGP) STK FLOW SW (FS400) P/W TEMP SW (TS451)</pre>	1DF 0 358.3 1.0 On 1.056 0 0 0

06/05/85 0845:35 P/P 9051	10c= 413 VDc= 724 🕅 P0012ACT= 37.7 TE400F	<u>CAL OVERU</u> W&CNET= T= 361 A 35 K	50.2 18012		ents O Des o
LOADTIME HOTTIME CELV ASI KWOC	TOTAL LOAD TIME TOTAL HOT TIME AVG VOLTS PER CEAL CURRENT DENSITY DC KILOWATTS	68 122 .700 84 106.2	ER Ha V/C ASF KW		
VT210DBL SFFINV F2FMECH SFFBL3C	DELTA HALF STK VOLT INSTANTANEOUS STK AMPS INVERTER SFFLCIENCY MECHANICAL EFFICIENCY SLECTRICAL EFFICIENCY	-0.85 465 99.0 48.0 23.0	V A 8 8	VIGIO HALY STR VOLT CELL EFFICIENCY (%) REF SFFICIENCY (%) HEAT RATS (BTU/KWHR)	-0,01 56.0 86.6 16306
KWACNET PFACT KVARNET RVANET PARPOWER KWACGROS MWHRSGR MWHRSGR	NET AC POWER ACTUAL POWER FACTOR NET KVAR NET KVA PARASITE POWER GROSS AC POWER GROSS AC MW HRS NET AC MW HOURS	50.2 -1.00 -1.1 49.7 55.0 105.2 2.549 0.922	KWAC - KVAR KVA KW KW MWHR MWHR	DISPATCHED POWER: DISPATCHED P.F.: DISPATCHED KVAR:	50.0 1,00 0,0

POWER CONDITIONER SYSTEM 06/16/95 IDC= 462 VDC= 224 (WACHET= 49.9) VT310DEL= -0.80 EVENTS 0 0846:35 FT012ACT= 40.4 TE400FT= 361.5 TE012FT= 1511.1 P/P 9061 P 160 R 160 2 60 W 20 A 30 N 40 C 20 L 10 (I 50) 497.5 V PT001A INV AC VOLTAGE, PRASE A PT001B INV AC VOLTAGE, PHASE B 494.2 Y INV AC VOLTAGE, PHASE C INV AC CURRENT, PHASE A 493.2 53.7 v PT001C CT001A A CT031B INV AC CURRENT, PHASE B 56.9 A 7.5 CTC01C INV AC CURRENT, PHASE C 58.2 A CURRENT UNBAL (%) 497.6 V PT003A NET AC VOGTAGE, PHASE A NET AC VOLTAGE.PHASE P NET AC VOLTAGE,PHASE C PT0033 495.3 v 492.3 V VOLTAGE UNBAL (%) 1.0 PT003C 599.7 LINKVDC LINK VOLTAGE v PERCEUND PERCENT FUNDAMENTAL 86.8 % PHASE SHIFT REQUEST 4.8 DEG PSREQ G/I BREAKER STATUS G/C BREAKER STATUS MCB001 Off MCB002 O'n MCB003 INTER-TIE BREAKER STAT INTERRUPT COUNT MCB003 On - 0

P/P 9051 05/16/95		37	SVENTS: 0	OVERE:	152: 0
<u>P 160 R 160 S 50 W 20</u>	<u>A 30 M</u>	<u>_40_</u> _C			
POWER OUTPUT (N3T)	101.0	KWAC)	OPERATING TIME	70.3	HRS
POWRE CUTPUT (GROSS)	117.7	KWAC	POWER FACTOR	0.99	
STACK CURRENT	539.5	AMPS	CUMULATIVE POWER	1.084	MWHR
STACK VOLTAGE	220.9	VOLTS	HALF STACK VOLTAGE	0,03	VOLTS
VOLUMETRIC FUEL FLOW	993.2	SCTH	FUEL FLOW SETPOINT	1002.5	SCFH
ACTUAL FUEL FLOW					
2T010 EJECTOR POSITION	26.9	રુ	ZTO10 SETPOINT	25.9	9
PHI MONITCE	1.05		TOTAL FUEL CONS	35819	SCF
FT140 BURNER AIR FLOW	315.1	PPH	FT140 SETFOINT	319.3	PPH
TEC12 REFORMER TEMP	1521.2	DEGF	ZT110 POSITION	48.7	8
TE012R BACKUP REF TEMP	1519.0	DEGF	TED12 SETPOINT	1520.5	DEGF
TEO02 HDS TEMP	510.7	DEGF	TE350 ANODE INLET TE	KP 397.3	DEGF
TEADOFT STEAM SEP TEMP	355.3	DEGF	TE400 SETPOINT	356.8	BEGF
TE881 TEMP TO CUST	10Z.5	DECF	RECOVERED HEAT	0 0	MBTU/HR
			TE431 POLISHER TEMP	82.3	DEGF
LT400 SEPARATOR LEVEL	11.1	I N	TE810 GLYCOL TEMP	140.6	DEGF
PMP451 STATUS	011		TE160 MOTOR COMP AIR	74.4	DEGF
			TE150 MOT COMP AIR IN	N 69.8	DEGF
BLECTRICAL BEFICIENCY	37.3	£	press <next page=""> ke</next>	y to view	RM data

1028:43	REACTANT ; IDC≂ 521.3 VDC= 222 (FT012ACT= 44.4 TE400P P 150 R 150 S 60 ₩ 20	<u>RWACNET</u> I= 357	= <u>101</u> TEC12:) VT310DEL= -0.80 EVE FT= 1522 30 L 10 I 50	NTS Q IDE C
TE012 TE012R TE012DE5	REF TUBE TEMP (PRIMARY) REF TUBE TEMP (BACKUP) REF TUBE TEMP DELTA	1520.4	DEGF DEGF DEGF	SETPOINT: REF/FUEL CONT CUTPUT:	1519.6 1.09
FT012ACT FT012	ACTUAL MASS FUEL FLOW UNCOER, MASS FUEL FLOW	44.4	PPH PPF	SETPOINT: TE011 FUEL TEMP(DEGF)	
SCFH FUELTOT	ACTUAL VOLUME FUEL FLOW TOTAL FUEL CONSUMED	986.9 35836	CFH SCF	SETPOINT: PT012 VENTURI(PSIA)	957.6 6,85
STGIÓ PHIMCN	PHI MONITOR	26.3 1.02	-	SETPCINT: STEAM FLOW S.F.(PPH):	25.3 161.9
TE350	ANOCE INLET TEMP	398.2	DRG7		
TEC02	HDS BED TEMP	510.2	DEGF	HTR002 STATUS:	0a
EFFREF	REFORMER EFFICIENCY	78.9	3		

1029:40	STACK LOOP IDC= 542.1 VDC- 221 C FT012ACT= 44.6 TE400FT P 160 R 160 S 60 W 20 A	(WACNET: 355.9	CE012FT- 1524 OVERRIDE O
TE400 TE4002 TE4002EL	SEFARATOR TEMP (PRIMARY) SEPARATOR TEMP (BACKUP) SEP TEMP DELTA	357.3	
LS450 TS431 TF310		on	STX FLOW SW (78400) On
T382D TE880 T3581	CUST HEX HOT IN TEMP CUST HEX COLD IN TEMP	160.6 150.0 103.4	
TE401 LT400	STACK COOLANT INLET TEMP SEPARATOR LEVEL		
PMP451 STARTTEMP IDCNET	WTS FEEDWATER FUMP TEMP FOR REF HEATUP NET DC CURRENT	Cn 350.0 544.5	ON TIME, MIN.(PWPUMP): 0 DEGP AMPS
HTR400	ELEMENT "A" ELEMENT "B"	Off Off	

1031:21	IDC= 535 VDC= 222 🕻 K	T= 356	<u>99.1</u> TE012		
LOADTIME HOTTIME CELV ASF	TOTAL LOAD TIME TOTAL NOT TIME AVG VOLTS PER CELL CURRENT DENSITY	7D 123 .695 96	HR HR V/C ASF		
KWEC VT310DRI. EFFINV ERFMECH BFFELZC	DC KILOWATTS DELTA HALF STK VOLT INSTANTANEOUS STK AMPS INVERTER EFFICIENCY MECHANICAL EFFICIENCY ELECTRICAL EFFICIENCY	119.3 -0.84 539 98.0 86.9 37.5	KW V & & &	VT310 HALF STE VOLT CELL EFFICIENCY (%) REF EFFICIENCY (%) HEAT RATE (BTU/KWHR)	-0.01 55.5 79.6 10093
KWACNET FFACT KVARNET KVANET PARPOWER KWACGROS MWHRSGR MWHRSNET	NET AC POWER ACTUAL POWER FACTOR NET KVAR PARASITE POWER GROSS AC POWER GROSS AC MW HRS NET AC MW HOURS	100.3 -1.00 -0.5 100.4 16.3 116.5 2.754 1.091	KWAC - KVAR KVA KW KW MWHR MWHR	DISPATCHED POWER: DISPATCHED P.F.: DISPATCHED KVAR:	100.0 1.00 0.0

1032:46	[DC= 539 VDC+ 221 €	KWACNET= = 356.8	
PT001A PT001E PT001C CT001A CT001E CT001C	INV AC VOLTAGE, FHASE B INV AC VOLTAGE, PHASE C INV AC CURRENT, PHASE A INV AC CURRENT, PHASE B	490.5 V 108.0 A	
PTOOBA PTOOBB PTOOBC LINKVDC	NET AC VOLTAGE, PHASE A NET AC VOLTAGE, PHASE B NET AC VOLTAGE, PHASE C LINK VOLTAGE	493.1 V 490.8 V 488.4 V 599.8 V	VOLTAGE UNBAL (%) 1.0
MCB002 MCB003	PEECSNT FUNDAMENTAL PHASE SHIFT REQUEST G/I BREAKER STATUS G/C BREAKER STATUS INTER-TIE BREAKSE STAT INTERRUPT COUNT	86.3 % 6.5 D Off On On 0	5G
06/16/95 1041:36 D/0 2061	IDC= 546 VDC≃ 221 🛞		0.1) VT310D3L= -0.80 EVENTS 0 1012FT= 1529OVERRICES 0

P/2 9061	P 160 R 363 S 60 W 20	A 30 N	40 C	30 6 10 (1 50)	
LOADTIME	TOTAL LOAD TIME	70	HR		
HOTTIME	TOTAL HOT TIME	124	HR		
CELV	AVG VOLTS PER CELL	.591	V/C		
ASF	CURRENT DENSITY	98	ASF		
XWEC	DC KILOWATTS	121.1	KW		
VT310DSL	DELTA HALF STK VOLT	-0.8C	v	VT31C HALF STK VOLT	D.D2
	INSTANTANEOUS STE AMPS	542	А		
BEFINV	INVERTER REFICIENCY	97.9	8	CELL EFFICIENCY (%)	55.4
BFFMSCH	MECHANICAL EFFICIENCY	84.5	8	REF EFFICIENCY (%)	77.5
EFFSLEC	ZLECTRICAL EFFICIENCY	35.5	8	HEAT RATE (BTU/KWHR)	10669
KWACNET	NST AC POWER	100.1	XWAC	DISPATCHED POWER:	100.0
PFACT	ACTUAL POWER FACTOR	<u></u>	- 1	DISPATCHED P. R.	0.85
XVARNET	NET KVAR	45.9	XVAR	DISPATCHED KVAR:	61.9
KVANET	NET KVA	110.6	KVA		
PARFOWER	PARASITÉ POWER	18.3	KW		
KWACGROS	GROSS AC POWER	118.4	KW		
MWHRSGR	GROSS AC MW HRS	2.773	MWITR		
MWERSNET	NET AC MW HOURS	1.107	MWHR		

05/16/95 1051:11 P/P 9061		<u>CAL CVBR)</u> WACNET= T= 356 A 30 N	(159) 100.9) VT310DEL= -0.80 EVENTS 0 TS01277= 1531 CVERNIDES 0 40 C 30 L 10 (I 50)
LOADTIME	TOTAL LOAD TIME	70	HR
HOTTIME	TOTAL HOT TIME	124	HR
CELV	AVG VOLTS PER CELL	.690	V/C
ASE	CURRENT DENSITY	97	ASP
	DC KILOWATTS	120.1	KW
KWDC	DELTA HALF STK VOLT	-0.80	V VT310 HALF STK VOLT 5.02
VT31CDEJ	INSTANTANEOUS STK AMPS	544	
ZFFINV	INVERTER EFFICIENCY	97.7	% CELL EFFICIENCY (%) 55.3 % REF EFFICIENCY (%) 78.5
ZFFMÉCH	MECHANICAL SEFICIENCY	85.9	
BF7ELEC	ELECTRICAL EFFICIENCY	36.3	HEAT RATE (BTU/KWRK) 10415
KWACNET	NET AC POWER	<u>100.9</u>	<pre>XWAC DISPATCHED POWER: 100.0 - DISPATCHED P.F.: -0.85)</pre>
XVARNET	NET RVAR	-59.0	KVAR DISPATCHED KVAR: -61.3
KVANET	NET XVA	116.8	KVA
PARPOWER	FARASITE FOWER	18.1	KW
KWACGROS	GROSS AC POWER	119.0	RW
MWHRSGR	GROSS AC MW HES	2.793	MWHR
MWHRSNET	NET AC MW HOURS	1.124	MWHR

KE	Y PARAMET	RRS (E	ENGLISH UNITS)		
P/P 9061 06/16/95	1201:5		EVENTS	OVERS:	IDE: C
<u>2 160 B 160 S 60 W 20</u>					
POWER OUTPUT (MET;	150 I	KWAC)	OPERATING TIME	71.9	HRS
FOWER OUTPUT (GROAS)	165.0	ZWAC	POWER FACTOR	-1.00	
STACK CURRENT		AMPS	CUMULATIVE FOWER		MWHR
STACK VOLTAGE		VOLTS	HALF STACK VOLTAGE		VOLTS
VOLUMETRIC FUEL FLOW		SCFE	FUEL FLOW SETPOINT	1458.7	SCFH
ACTUAL FUEL FLOW	65 6	PPH			
ZTOID EJECTOR POSITION		3	ZT010 SETPOINT	42.1	8
PHI MONITOR	1,05		TOTAL FUEL CONS		SCF
FT14D BURNER AIR FLOW		PPH	FT140 SETPOINT	435.2	PPH
TEO12 REFORMER TEMP		DEGE	3T110 POSITION	63.1	8
TE012R BACKUP REF TEMP	1592.0	DZGZ	TEC12 SETPOINT	1596.6	DEGF
	505 A	DRCE	TE350 ANODE INLET TE	W7 300 E	DEGF
TEGOZ HDS TEMP	537.1	DEGF	16320 ARODE INCS: 12	MF 19913	DEGE
TE4COFT STEAM SEP TEMP	343.1	DEGE	TE400 SETPOINT	348.4	DEG?
TESSI TEMP TO CUST	94.6	DEGF	RECOVERED HEAT	0 0	MBTV/HR
			TE431 POLISHER TEMP	86.5	DEGF
ST400 SEPARATOR SEVEL	11.3	TN	TES10 GLYCOL TEMP	155.5	DEGF
PMP451 STATUS	051		TE160 MOTOR COMP AIR	74.2	DEGP
			TE150 MOT COMP AIR I.	N 73.5	DEGF
REACTRICAL BEFECIENCY	28.6	3	press (NEXT PAGE) ke	y to view	EM data

1203:45	R2ACTANT (IDC= 800.6 VDC= 212 (FT012ACT= 96.5 TE40CM P 160 R 160 S 60 W 20	<u>KWACNET</u> I- 349	150	FT- 1599 OVERF	ENTS O RIDE O
TE012R		1505.6	DEGY	SETPOINT: REF/FUEL CONT OUTPUT:	1597.1 1.07
FUSLICT	ACTUAL VOLUME FUEL FLOW TOTAL FUEL CONSUMED	66.5 71.1 1477.0 37950	PPH CFH SCF	SETPOINT: TED11 FUBL TEMP(DEGF) SETPOINT: PTD12 VENTURI(PSIA)	76.8 1460.1
ZTC10 201000 22250	•	42.1 1.01 399.3	3 Degf	SETPOINT: STEAM FLOW 2.P.(PPH):	
T2002	HDS BED TEMP	537.9	DEGF	HTR002 STATUS:	Qff
EFFREF	REFORMER SPRICISNCY	8C.6	ę.		

1205:01		WACNET 343.0	15:	D) VT310DEL= ~C.&7 EVE.	NTS 0 IDE 0
TE400	SEPARATOR TEMP (PRIMARY)	343 6	DEG7	SETPOINT:	348.5
TE40CR	SEPARATOR TEMP (BACKUP)	348.7	DEGF	SEP TEMP FACTOR (DEGP)	
TE400R	·····	3.6	DEGE	SEP TERM TROIDE(DESC)	
15450 LS450	WATER TANK LEVEL SWITCH	0n	U.G.	STK FLOW SW (FS400)	On
			BROD	F/W TEMP SW (TS451)	On
TE431		84.5		F/W TEMP SW (15451/	on
73810		157.5	DEGY		
TE820	CUST HEX HOT IN TEMP	189.8	DEGF	CUMHEATREC (MMBTV)	1.055
0SS3T	CUST HEX COLD IN TEMP	156.8	DEGF	FTSSO FLOW (PPR)	0
TE381	CUST HEX COLD EX TEMP	95.0	DEGF	HEAT REC (MBTV/RR)	D C
TE401	STACK COCLANT INLET TEMP	308.0	DEGF		
LT400	SEPARATOR LEVEL	10.8	13		
F1400	5900 mail 1000 1000 100	2010			
PMP451	WTS FEEDWATER PUMP	On		ON TIME, MIN. (FWFUMP):	0
STARTTEMP	TEMP FOR REF HEATUP	350.0	DEGT		
			AMPS		
IDCNET	NET DC CURRENT	809.4	សារិទ័		
900 D 40 D	ELEMENT "A"	Off		RLEMENT "C"	Off
HTR400					Öff
	ELEMENT "B"	Off		BL3MENT "D"	011

1206:00	ELECTRIC IDC= 797 VDC= 212 (K) PTC12ACT= 64.1 TE4COF P 160 R 160 S 60 W 20	1=-350-	TE012	$\begin{array}{c} 0 & \text{vT31cDEL} = -0.65 & \text{EV3} \\ \text{ZT} = & 1607 & \text{OVERRID} \\ 30 & \text{L} & 10 & \text{I} & 50 \end{array}$	(TS 0 25 0
LOADTIME HOTTIME CELV ASP KWDC VT310DEL EFFINV EFFMECH SFVESEC	TOTAL HOT TIME AVG VOLTS PER CELL CURRENT DENSITY DC KILOWATTS DELTA HALF STK VOLT INSTANTANEOUS STK AMPS INVERTER EFFICIENCY MECHANICAL EFFICIENCY	97.6 90.1	HR V/C ASF KW V A %	VT310 HALF STK VOLT CELL EFFICIENCY (%) REF EFFICIENCY (%) HEAT RATE (BTU/KWHR)	D.18 53.1 82.0 9919
KWACGROS MWHRSGR	NET XVA PARASITE POWER GROSS AC POWER GROSS AC MW HES	148.8 -1.30 -1.3 149.3 154.7 2.995 1.307	- KVAR KVA KW KW MWHR		150.0 1.00 0.0
2TOOIA PTOOIB	IDC= 801 VDC= 212 FT012ACT= 64.0 TE4COF 9 160 R 160 S 60 W 20 INV AC VOLTAGE.PHASE A INV AC VOLTAGE.PHASE 9	<u>KWACNET</u> I= 348.5 A 30 N 498.2 496.3	= 150. TE01 40 C V V	SYSTEM 1) VT31DDEL= -0.65 EVE 27T= 1599.5 30 L 10 150	NTS 0 ICE 0
PT051C CT001A CT001B CT001C	INV AC VOLTAGE, PHASE C INV AC CURRENT, PHASE A INV AC CURRENT, PHASE B	496.5 164.0 176.0 179.5	V А А А С	CURRENT UNBAL (%)	\$.1
PTC03A PTO03B PT003C LINKVDC	NET AC VOLTAGE, PHASE B			VOLTAGE UNBAL (%)	1.0
FERCFUND PSREQ MCB001 MCB002 MCB003 INTCOUNT	PERCENT FUNDAMENTAL PHASE SHIFT REQUEST G/I BREAXER STATVS G/C BREAKER STATVS INTER-TIE BREAKER STAT INTERRUPT COUNT	88.8 6.9 Cff On On U	¥ DEG		

KR	Y PARAME	TERS (E	NGLISH UNITS)		
/P 9061 06/20/95	1746:		EVENTSO	OVERR.	1D E: 0
150 8 160 5 60 W 20	<u>A 30 N</u>		30 г.10 (1 <u>59</u>)		
JWER OUTPUT (NET)	193.8	KWAC	OPERATING TIME	150.1	HRS
OWER OUTPUT (GROSS)	-216.1	KWAC	POWER FACTOR	-1,0C	
TACK CUERENT	1084.4	AMPS	CUMULATIVE POWER		MWHR
TACK VOLTAG3	207.0	VOLTS	HALF STACK VOLTAGE		VOLTS
OLUMETRIC FUEL FLOW		SCFH	FUEL FLOW SETPOINT	1992.6	SCFH
CTUAL FUEL FLOW	88.9	PPH			
TO10 EJECTOR POSITION	66,7	8	ZT010 SETPOINT	66.2	8
HI MONITOR	1.00		TOTAL FUEL CONS	139495	SCF
T140 BURNER AIR FLOW	555.9	ЬЪЯ	FT140 SETPOINT	533.3	PPH
BO12 REFORMER TEMP	1663.2	DEGF	ZT110 POSITION	84.0	÷.
2012R BACKUP REF TEMP	1676.0	DEGF	TS012 SETPOINT	1635.6	DEGF
	503 0				
FEOG2 HDS TEMP	581,9	DEGE	TE350 ANODE INLET TEM	IP 407.8	DEGF
E400FT STEAM SEP TEMP	350.8	DEGF	TE400 SETPOINT	350.1	DEGF
22881 TEMP TO CUST	177.1	DEGF	RECOVERED HEAT	254	MBTU/HR
			TE431 POLISHER TEMP	119.0	DEGF
T400 SEPARATOR SEVEL	:1.2	1 N	TES10 GLYCOL TEMP		DEGF
FMP451 STATUS	Off		TE163 MOTOR COMP AIR		DEGF
			TE150 MOT COMP AIR IN		DEGF
LECTRICAL EFFICISNCY	36.2	*	press (NEXT PAGE) key		

1746:55	REACTANT IBC= 1085.5 VDC= 207 % PT012ACT≃ 88.3 TE400F" P 160 R 160 S 60 W 20 REF TUBE TEMF (PRIMARY) REF TUBE TEMP (BACKUF)	KWACNET T= 351 A 30 N 2657.1	200	FT= 1656 OVER!	RIDE 0
TE012DEL FT012ACT FT012 SCFH	REF TUBE TEMP DELTA ACTUAL MASS FUEL FLOW UNCORR. MASS FUEL FLOW ACTUAL VOLUME FUEL FLOW TOTAL FUEL CONSUMED	14.5 88.3 91.7	DEGF FPH 2PH CFH	SETPOINT: TSO11 FUEL TEMP(DEGF) SETPOINT: PTO12 VENTURI(PSIA)	89.8 99.0 1996.0
2TC10 PHIMON TE350	BJECTOR POSITION PHI MGNITOR ANODE INLET TEMP	65.8 1.02 407.4		SETPOINT: STEAM FLOW S.P.(PPH):	65.7 322.3
TEOGZ	HDS BED TEMP	582.B	DECF	HTROO2 STATUS:	Off

EFFREF REFORMER EFFICIENCY 81.2 %

1747:41	STACK LOO IDC= 1089.6 VDC= 207 (FTG12ACT= 90.8 TS400PT) P 150 R 160 S 50 W 20 .	KWACNET	200 TE01	NT31CDEL= -0.37 EVEN	
TE400	SEPARATOR TEMP (PRIMARY)	351.1	DEGF	SETPOINT:	350.4
TE400R	SEPARATOR TEMP (BACKUF)	350.7	DEG7	SEP TEMP FACTOR (DEGF)	-
TE4CODEL	SEP TEMP DELTA	G.4	DEGF		
LS450	WATER TANK LEVEL SWITCH	OR		STK FLOW SW (F5400)	Ôn
TE431	POLISHER TEMP	119.0	DEGF	F/W TEMP SW (TS451)	Оq
TE310	CONDENSOR EXIT TEMP	153.3	DEGP		
TE820	CUST MEX HOT IN TEMP	177.5	DEGF	CUMEEATREC(MMBTU)	1.210
TE880	CUST HEX COLD IN TEMP	105.4	DEGF	FT880 FLOW (PPH)	2763
72881	CUST NEX COLD EX TEMP	178,5	DEGF	HEAT REC (MBTU/HR)	202
TE401	STACK COOLANT INLET TEMP		CEGF		
GT405	SEPARATOR LEVEL	10.8	IN		
PMP451 STARTTEMP IDCNET		On 350.0 1092.8	DBG7 AMPS	ON TIME, MIN. (FWPUMP):	D
HTR400	ELEMENT "A" BLEMENT "B"	Off Off		ELEMENT "C" ELEMENT "D"	Off Off

1748:44	IDC= 1092 VDC= 207 (K)	CAL OVERN NACNET= F= 351 A 30 N	199.7 12012	,	NTS Ó ES O
LOADTIME ECTTIME CELV ASF	TOTAL LOAD TIME TOTAL HOT TIME AVG VOLTS PER CELL CURRENT DENSITY DC KILOWATTS	150 210 .646 194 224.5	HR HR V/C ASF KW		
KWDC VT310DEL EFFINV EFFMECH EFFELSC	DELTA HALF STK VOLT INSTANTANEOUS STR AMPS INVERTER EFFICIENCY MECHANICAL EFFICIENCY ELECTRICAL EFFICIENCY	-0.36 1078 96.0 92.4 36.3	V A	VT310 HALY STK VOLT CELL EFFICIENCY (%) REF EFFICIENCY (%) HEAT RATE (BTU/KWHR)	0.46 51.7 79.2 10435
KWACNET PFACT KVARNET KVANET PARFOWER KWACGROS MWERSGR MWHRSNET	NET AC POWER ACTUAL POWER FACTOR NET KVAR NET KVA FARASITE POWER GROSS AC POWER GROSS AC MW HRS NET AC MW HOURS	199.9 -1.00 -0.7 200.2 16.8 216.2 24.718 11.591	KWAC - KVAR KVA KW KW MWHR MWHR	DISPATCHED POWER: DISPATCHED P.F.: DISPATCHED KVAR:	200.0 1.00 0.0

 POWER CONDITIONER SYSTEM

 C6/20/95 IDC= 1086 VDC= 207
 KWACNET= 199.3) VT310DEL= -0.35 EVENTS 0

 1749:30
 FT012ACT= 89.7 TE400PT= 351.2 TE012PT= 1659.3
 OVERRIDE 0

 P/P
 9061 P 160 R 160 S 60 W 20 A 30 N 40 C 30 L 10 (250)
 50
 INV AC VOLTAGE, PHASE A 491.2 PT001A v PT0016 INV AC VOLTAGE, PHASE B 489.9 ٧ INV AC VOLTAGE, PHASE C v PTGÓIC 489.8 INV AC CURRENT, PHASE A INV AC CURRENT, PHASE B 225.1 A CT001A CT001B 242.1 A INV AC CURRENT, PHASE C 239.5 A CURRENT UNBAL (%) 7.1 C2001C P2003A NET AC VOLTAGE, PHASE A 489.5 V PT0533 NET AC VOLTAGE, PHASE B 486.3 V 484.2 PT003C NET AC VOLTAGE, PHASE C v VOLTAGE UNBAL (%) 1.1 LINE VOLTAGE ٧ LINKVOC 599.9 PERCEUND PERCENT FUNDAMENTAL 8.36 ÷ PHASE SHIFT REQUEST 8.8 DEG PSR30 G/I BREAKER STATUS G/C BREAKER STATUS Off MCBD01 MCE002 On. MCBDC3 INTER-TIE BREAKER STAT 0n INTCOUNT INTERRUPT COUNT Ó

ONSI CORPORATION

TOTAL HARMONIC DISTORTION

PASS

DEMONSTRATED:	1.27 %
REQUIRED :	< 3.00 %

RESULT

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06/20/95 13:04:46 UQLTS = 483.7 FMPS = 0.04 LATTS = 17 F.F. ⇒ +1.00 HAFF PWR = а Approx TDF = 0.95VOLTS. AMPS 77 TIF (1, 27%)17.39% THC 0.04A F 474.3U ż 0.46% 13.04% 4,35% 0.40% 4.35% 4.35% 4 0.06% 5 0.84% 0.00% 0.04% 6 7 4.35% 0.32% 0.00% æ 0.04% 0.08% 0.06% 9 4.35% 4.35% 10 9.08% 0.48× 0.02× 11 0.00% 12 13 4.35% 0.38% 14 9.02% 0.00% 15 0.00% 0.02% 0.02% 16 0.00% 0.00× 17 0.04% 0.02% 0.90% 18 0.02× 0.00% 19 0.90% 20 0.02% 0.00% 21 0.00% 22 0.02% 0.00% 4.35% 0.00% 23 0.04% 0.00% 24

0.00%

25

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0.00%

1822:17	FT012ACT= 90.1 TE400F		TROIZ	PT= 1661 OVERHIDES O	
9/9 9061	. F 160 R 160 S 60 W 20	A 30 N	40 C	; 30 L 10 (1 <u>50</u>)	
LCADTIME	TOTAL LOAD TIME	150	НŘ		
HOTTIME	TOTAL HOT TIME	211	ня		
CELV	AVG VOLTS PER CELL	.646	v/c		
ASF	CURRENT DENSITY	196	ASF		
XWDC	DC KILOWATTS	226.7	KW		
VT310DEL	DELTA HALF STR VOLT	-0.40	v	VT310 HALF STK VOLT 0.43	
A13100E0	INSTANTANEOUS STR AMPS	1091	À		
3F7INV	INVERTER REFICIENCY	95.6	1	CELL EFFICIENCY (%) 51.7	
EFFMECH	MECRANICAL EFFICIENCY	92.2	8	REF EFFICIENCY (%) 81.1	
	ELECTRICAL EFFICIENCY	36.5	8	HEAT RATE (BTU/KWHR) 10268	
RFFELEC	REPORTED AND REALIZED	30.0	Ð	MARI MILL (Die) Million (Die)	
KWACNET	NET AC POWER	200.2	KWAC	DISPATCHED POWER:	
PFACT	ACTUAL POWER FACTOR	0.99)) —	(DISPATCHED P.F. Q.85)	
KVAENET	NET XVAR	25.1	KVAR	DISPATCHED XVAR: 123.9	
KVANET	NET KVA	202.0	KVA		
PARPOWER	PARASITE POWER	16.1	KW		
KWACGROS	GROSS AC POWER	216.4	KW		
MWHRSGR	GROSS AC MW HRS	14.541	MWHR		
NWHRSNET	NET AC MW HOURS	11.704	MWHR		
NWEARSNEI	MAL NO NU MOORD	11.701			

06/20/95	IDC≂	1093	ELECTRICAL VDC- 207 (KWACI	VT310DEL= -0.40) EVENTS	0

RESULT:

DEMONSTRATED:	60.00 HZ	
REQUIRED:	54 623 HE	

PASS

OUTPUT FREQUENCY (GRID CONNECT)

ONSI CORPORATION

1829	20/95	FT012A		VD 88.	С= 2 8 Т	ECTRI 06 (<u>k</u> E40CF	WAC.	NET= 351	_	200. TSOI	ZFT=	1	1005 656		~ C	9 B 9 BRR	VENT		0	
P/P	9061	P 160	R 160) S	60	W 20	А	30	Ņ	40	C 30	5	10	U.	$\underline{50}$					
LOAI	DITME	LATOT	LOAD	TIM	3			150		HR										
SOLS	IME	TOTAL	HOT T	EMI				211]	HR										
CELV	7	AVG VO	LTS F	BR (CELL			.645		v/c										
ASF		CURREN			Y			198		ASF										
KWOC	-	DC XIL					_	29.1		KW										
VTBS	LÓDEL	DELTA				-		0.39		v	VT	310	HAL	P 81	rx v	TLO		0.4	13	
		INSTAN						1113		A										
EFFI		INVERT				-		95.2		8			EFFI					51.		
		MECHAN						92.4		£.			FFIC			•		82.		
EFFE	LEC	ELECTR	ICAL	RFF	ICIE	NCY		37.1		8	HE.	AΤ	RATE	(81	CO/K	(RHW	1	019	8	
KWAC	INET	NET AC	POWE				_ 1	99.7		KWAC	DI	SFA	TCHE	0 20	WER		2	00.	Q.	
(2FAC	Ť. Č.	ACTUAL	POWE	ÊR Ê	ACTO	R	_	0.85).	_	$\overline{\Omega}$	SPA	тснеі	Ρ.	P.			0.8	5)	
XVAF	NET	NET KV	AR	~	<u> </u>		-1	22.6	<u> </u>	KVAR	DI	SPA	TCHE	D KV	AR :			23.	9	
KVAN	(ET	NET KV	A				2	34.8	i	KVA										
FARF	OWER	PARASI	TE PO	WER				17.4		KW										
KWAC	GROS	GROSS .	AC PO	WER			2.	17.2	E	KW										
MWHS	RSGR	GROSS	AC MW	(HR:	S		14	.866	H	MWHR										
SWIFE	RENET	NET AC	MW H	IOURS	5		11	.724	3	MWHR										

ĸ	EY PARAMET	FERS (S	ENGLISH UNITS)		
⊋/⊋ 9061 0 6/20/95	1834:(SVENTS: 0	OVERRI	DB: 0
P 150 R 160 S 60 W 20		40 C	30 L 10 (L <u>5</u> 0)		
CROWER OUTSUT (NST)	200 2	KWAC	OPERATING TIME		ERS
POWER OUTPUT (GROSS)	214.3	KWAC	POWER FACTOR	-1.00	
STACK CURRENT	1077.0	AMPS	CUMULATIVE POWER		MWHR
STACK VOLTAGE	207.2	VOLTS	HALP STACK VOLTAGE		VOLTS
VOLUMETRIC FUEL FLOW	1943.4	SCFH	FUEL FLOW SETPOINT	1963.9	SCFH
ACTUAL FUEL FLOW	87.5	PPH			
ZTOID EJECTOR POSITION	54.8	8	ZTOIC SETEDINT	<u>64</u>].	\$
PHI MONITOR	1.02		TOTAL FUEL CONS	141110	<u>scf</u>)
FT140 SURNER AIR FLOW	536.8	PPH	FT140 SZTPOINT	519.6	PPH
TE012 REFORMER TEMP	1660.1	DEGF	ZT110 POSITION	84.4	₽ - _
TEG12R BACKUP REF TEMP	1672.9	DEGF	TE012 SETPOINT	1656.3	DEGF
TECO2 HDS TEMF	595.5	DEGF	TE350 ANODÉ INLET TEN	4P 409.8	DEGF
				•	
TE400FT STEAM SEP TEMP		DEGF	T2400 SETPOINT	350.2	DËGF
TE881 TEMP TO CUST	134.0	DEGY	RECOVERED HEAT	912	MBTU/HR
			TE431 POLISHER TEMP	119.0	DEGF
LT40D SEPARATOR LEVEL	11.0	IN	TES10 GLYCCL TEMP	150.2	DEGF
PMP451 STATUS	Cn		TE160 MCTOR COMP AIR		DEGF
			TE150 MOT COMP AIR IN		DEGT
ELECTRICAL REFICIENCY	37.4	*	press (NEXT PAGE) key	y to view	RM data

7	o
1	o

LS450 TE431 TE810 TE820 TE880 TE881 TE881 TE801	WATER TANK LEVEL SWITCH POLISHER TEMP CONDENSOR EXIT TEMP CUST HEX HOT IN TEMP CUST HEX COLD IN TEMP CUST HEX COLD EX TEMF STACK COOLANT TNLET TEMP	On 119.0 149.4 176.6 92.6 130.2 239.7	DEGF DEGF DEGF DEGF DEGF DEGF DEGF	SEP TEMP FACTOR(DEGF) STK FLOW SW (FS400)	0.9 On 1.350 22075
ST4CO PMP451 STARTTEMP IDCNST	SEPARATOR LEVEL WTS FREDWATER PUMP TEMP FOR REF HEATUP NET DC CURRENT		IN DEGF AMPS	ON TIME, MIN. (FWPUMP):	٥
	ELEMENT "A" Element "B"				
1934:51 P/P 3061 TE400	STACK LOG IDC= 1088.1 VDC= 207 \$T012ACT= 91.6 TE400F0 F 160 R 160 S 60 W 20 SEPARATOR TEMP (PRIMASY) SEPARATOR TEMP (BACKUP) ESF TEMP DELTA	KWACNET r→ 351.0 A 30 N) 351.1	2≕ 20 7501 40 C 386F	0 VT310DRL= -0.45 EVE 2FT= 1651 OVER 30 L 10 I 50 SETPOINT:	350.4
LS450 T2431 TE810 TE820 TE880 TE881 TE401 LT400	SEPARATOR TEMP (BACKUP) SEP TEMP DELTA WATER TANK LEVEL SWITCH POLISHER TEMP CONDENSOR EXIT TEMP CUST HEX HOT IN TEMP CUST KEX COLD IN TEMP CUST HEX COLD EX TEMP STACK COOLANT INLET TEMP SEPARATOR LEVEL	On 119.5 152.2 180.6 145.1 179.9 P 303.4 10.8	DEGF DEGF DEGF DEGF DEGF IN	STX FLOW SW (FS400) F/W TEMP SW (TS451) CUMHEATREC(MMBTU) FT850 FLOW (PPH) HEAT REC (MBTU/HR)	0n 0n 1.942 0 0
PMP451 STARTTEMP 1DCNBT	WTS FEEDWATER PUMP TEMP FOR REF HEATUP NET DC CURRENT	Or. 350.D 1087.2	deg? Amps	ON TIME, MIN. (FWPUMP):	. 0
HTR400	ÉLEMENT "A" Element "B"	Off Off		PLEMENT "C" Blement "d"	Off Of≓

STACK LOOP, ANC LOOP, & WTS 06/20/95 IDC= 1065.4 VDC= 208 (KWACNET= 199) VT310DEL= -0.37 EVENTS 0 1834:50 FT012ACT= 27.5 TE400FT= 350.7 TE012FT= 1656 OVERRIDE 0 P/P 9061 P 160 R 160 S 60 W 20 A 30 N 40 C 39 L 10 I 50

KEY PARAMETERS (ENGLISH UNITS)					
P/P 9061 06/20/95	2034:	51	EVENTS <u>:</u> 0	OVERR	IDE: 0
<u>P 160 R 160 S 60 W 20</u>			30 L 10 🛈 50)		
POWER OUTPUT (NET)	<u>د ۲، ۵۵ م</u>	KWAC	OPFRATING TIME	152.9	ARS
POWER OUTPUT (GROSS)	215.7	KWAC	POWER FACTOR	1.00	
STACK CURRENT	1086.0	AMPS	CUMULATIVE FOWER	12.144	MWHR
STACK VOLTAGE	206.7	VOLŢŞ	HALF STACK VOLTAGE	0.39	VOLTS
VOLUMETRIC FUEL FLOW		SCFH	FUEL FLOW SEIPDINT	1997.0	SCFR
ACTUAL FUEL FLOW	69.8	PPH			
ZT010 EJECTOR POSITION	66.9	8	ZT010 SETPOINT	<u>66.</u>	_ <u></u>
PHI MONITOR	1.01		TOTAL FUBL CONS	145056	SCF)
. =	517.7	PPN	FT14C SETFOINT	517.8	PPE
	1652.2	DEGT	ZT110 POSITION	85.2	8
TEC12R BACKUP REF TEMP	1661.9	DEGF	TE012 SETPOINT	1657.1	DECF
TEOO2 HDS TEMP	6D3.9	DEGF	TE350 ANODE INLET TEM	P 409.8	DEGF
		+			
TE400FT STEAM SEP TEMP	350.9	DEGF	TE4DO SETPOINT	350.Z	DECE
TE881 TEMP TO CUST	180.4	DEGF	RECOVERED HEAT	101	MBTU/HR
			TE431 POLISHER TEMP	121.9	DEGF
17400 SEPARATOR LEVEL	11.0	IN	TE810 GLYCOL TEMP	153.3	DEGF
PMP451 STATUS	Off		TE160 MOTOR COMP AIR		DEGF
			TE150 MOT COMP AIR IN		DEGE
ELECTRICAL EFFICIENCY	27.4	¥.	press <next page=""> key</next>	to view	RM data

ONS] CORPORATION

FUEL CONSUMPTION

<u>TIME</u> 1834:08 2034:51 CUMULATIVE FUEL CONSUMED IAI,110 SCF IA5,086 SCF

ELAPSED TIME: INCREMENTAL FUELCONSUMED: ANG. VOLUMETRIC PUEL FLOW RATE; REQUIRED FUEL FLOW RATE; 2.012 HRS 39716 SCF 1976 SCFH 19002 100 SCFH

REJULT:

PASS

	STACK LOO	P, ANC :	LOCP % WTS
06/20/95	IDC= 1086.1 VDC= 207 🕻	XWACNET:	199) VT310DEL= -0.44 EVENTS 0
2035:32		= 350.8	
P/P 9061	F 160 R 160 5 60 W 20	A 30 N	40 C 30 L 10 (T 50)
- ,			
72400	SEPARATOR TEMP (PRIMARY)	350.9	DEGF SETPOINT: 350.1
TE40OR	SEPARATOR TEMP (BACKUP)		DEGF SEP TEMP FACTOR(DEGF) 0.9
7340CDSL	SEP TEMP DELTA	0.0	DBGF
18459	WATER TANK LEVEL SWITCH	Ċъ	STK FLOW SW (FS40G) On
TE431	POLISHER TEMP	121.9	DEGF F/W TEMP SW (TS451) On
TE810	CONDENSOR EXIT TEMP		DEGF
TE825	CUST HEX HOT IN TEMP		DEGE (CUMHEATREC(MMBTU) 1.997)
TE280	CUST HEX COLD IN TEMP		DEGF FT880 FLOW (PPH) 2591
TE581	CUST HEX COLD EX TEMP		DEGF HEAT REC (METU/HR) 83
73401	STACK COOLANT INLET TEMP		DEGF
LT400	SEPARATOR LEVEL	10.8	IN
L1400		,	
PMP451	WTS FEZDWATER PUMP	Off	ON TIME, MIN. (FWPCMP): 0
STARTTEMP	TEMP FOR REF HEATUP	350.0	DEGF
IBCNET		1081.8	AMPS
LDCHEI	MEI DO GUNDMI	1001-0	Ant P
HT2400	ELEMENT "A"	Off	BLEMENT "C" Off
N17400	ELEMENT "B"	Off	BLEMSNI C
	2020201 0	OLT	REPEAL D

ONSI CORPORATION

HENT RECOVERY

<u>TIME</u>	CUMULATIVE HEAT RECOVERY
1834:50	1,350,000 BTU
2035:32	1,997,000 BTU
ELAPSED TIME:	2,012 HRS UTS 000, TA

5LA INCREMENTAL HEAT RECOVERY: 321, 5TO BTU/HR. AVERAGE RATE OF HEAT RECOVERY :

KE	Y PARAME	TERS (3	NGLISH UNITS)		
P/P 9061 06/21/95	0935:		EVENTSC	OVERR.	IDZ: 0
2 161 R 160 S 60 W 20	<u>A 30 N</u>	<u>40 </u>	30 L 10 (1 80)		
POWER CUTPUI (NET)	38.1	KWAC)	OPERATING TIME	166.0	ARS
FOWER OUTPUT (GROSE)	90.3	KWAC	POWER FACTOR	0.95	
STACK CURRENT	410.4	AMPS	CUMULATIVE POWER	14.561	MWHE
STACK VOLTAGE	227.9	VOLT5	HALF STACK VOLTAGE	-0.00	VOLTS
VOLUMETRIC FUEL FLOW	711.9	SCFH	FUEL FLOW SETPOINT	717.6	SCFH
ACTUAL FUEL FLOW	32.0	PPE			
ZTO10 EJECTOR POSITION	23.2	8	ZT010 SETPOINT	21.8	8
PHI MONITOR	1.07		TOTAL FUEL CONS	1€9280	SCF
FT140 BURNER AIR FLOW	250.4	PPH	FT140 SETPOINT	253.7	PPH
TED12 REFORMER TEMP	1515.5	DEGF	ZT110 POSITION	45.5	8
TE012R BACKUP REF TEMP	1510.2	DEGY	TE012 SETPOINT	1527.3	DEGF
TE002 HDS TEMP	633.0	DEGF	TRADO ANCOS INLET TS	MP 406.7	DEGF
TE4COFT STEAM SEP TEMP	364.0	DSGF	TE400 SETPOINT	363.4	DEGF
TE281 TEMP TO CUST	162.1	DEGF	RECOVERED HEAT	237	MBTU/HR
			TE431 FOLISHER TEMP		DEGF
LT400 SEPARATOR LEVEL	10.9	IN	TESIC GLYCOL TEMP	151.3	DEGF
PMP451 STATUS	ΩD		TE160 MOTOR COMP AIR		DEGF
			TE150 MOT COMP AIR I		DEGF
ELECTRICAL EFFICIENCY	18.4	Έ.	press «NEXT PAGE» ke	y to view	xM data
	•				

	REACTANT IDC= 398.5 VDC= 229 (FT012ACT= 32.3 TE400P P 161 R 160 S 60 W 20	XWACNET T= 363	= 31 78012		NTS O NDE O
TE012 TE012R TE012DEL	REF TUBE TEMP (PRIMARY) REF TUBE TEMP (BACKUP) REF TUBE TEMP DECTA	1511.6	DEGF DEGF DEGF	SETPOINT: REF/FVEL CONT OUTPUT:	1526.8 1.04
FT012ACT FT012 SCPH ZUBLTOT	ACTUAL MASS FUEL FLOW UNCORE. MASS FUEL FLOW ACTUAL VOLUME FUEL FLOW TOTAL FUEL CONSUMED	32.0 36.1	PPH PPH CFH SCF	SETFOINT: TEO11 FUSL TEMP(DEGF) SETFOINT: FTO12 VENTURI(PSIA)	31.7 85.4 700.5 7.15
27010 PHIMON TE350		22.9 1.04 406.7	۶ Degp	SETPOINT: STEAM FLOW S.F. (PPH):	21.6 1 34 .4
TECO2	NDS BED TEMP	602.1	DEGF	HTRDO2 STATUS:	Off

BFFREF	REFORMER	EFFICIENCY	83.7	¥

0937:07		WACNET	5 TEOI	4) VT31008L= -0.80 EV81	
TE400	SEPARATOR TEMP (PRIMARY)	362.5	DECF	SETPOINT:	358.6
734008	SEPARATOR TEMP (BACKUP)	362.1	DEGF	SEP TEMP FACTOR(DEGF)	1.0
TE40CDEL	SEP TEMP DELTA		DEGF	551 10th 11to 10th (5401)	1.0
12450	WATER TANK LEVEL SWITCH	0n	DIGI	STK FLOW SW (FS400)	ao
TE431	POLISHER TEMP		DEGF	F/W TEMP SW (TS451)	On
TE810	CONDENSOR BXIT TEMP	153.3	DEGF	-,,	
TE820	CUST HEX HOT IN TEMP		DEGF	CUMHEATREC(MMSTU)	3.231
TE280	CUST HEX COLD IN TEMP	150.5	DEGF	FT88C FLOW (PPH)	22247
TE881		160.6	DEGT	HEAT REC (METU/HR)	224
75401	STACK COOLANT INLET TEMP		DEGF	,,	
LT400	SEPARATOR LEVEL	11.3	TN		
РМР451	WTS FEEDWATER PUMP	Off		ON TIME, MIN. (FWFUMP);	0
STARTTEMP		350.0	DEGF		
IDCNET	NET DC CURRENT	209.3	AMPS		
HTR400	PLEMENT "A"	On		BLEMENT "C"	Ôn
	ELEMENT "B"	Cn		RLEMENT "D"	Off

06/21/95	5	CAL OVER: WACNETTE	<u>v:sw.</u> 44.5	VT310DEL= -0.85 EV	INTS O
0938:12 2/P 9061	FT012ACT# 35.0 TS400F		TE012		
LOADTIME	TOTAL LOAD TIME	166	HR		
HOTTIME	TOTAL HOT TIME	226	HR		
CELV	AVG VOLTS PER CELL	.704	9/C		
ASY	CURRENT DENSITY	81	ASF		
SWDC	DC KILOWATTS	102.1	KW		A 0.7
VT310DEL	DELTA HALF STX VOLT	-0.85	v	VT310 HALF STK VOLT	-0.02
	INSTANTANEOUS STR AMPS	452	A		56.1
EFFINV	INVERTER EFFICIENCY	97.4	*	CELL EFFICIENCY (%)	56.1
3FFMBCH	MECHANICAL EFFICIENCY	50.1	₽ -	REF EFFICIENCY (%)	88.4
EFFSLEC	BLECTRICAL EFFICIENCY	23-8	5	HEAT RATE (BTU/XWHR)	16152
KWACNET	NKT AC POWER	44.5	EWAC	DISPATCHED FOWER:	0.0
FFACT	ACTUAL POWER FACTOR	0.95	-	DISPATCHED P.F .:	1.00
KVARNET	NET KVAR	14.5	RVAR	DISPATCHED KVAR:	0.0
XVANST	NET KVA	46.8	KVA		
PARPOWER	PARASITE POWER	54.5	RW		
XWACGROS	GROSS AC POWER	99.1	KW		
MWHRSGR	GROSS AC MW HRS	17.986	MWHR		
MWHRSNET	NET AC MW HOURS	14.563	NWHR		

0939:11	IDC= 427 VDC= 227 (_KWACNET T= 261.9	<u>TION3R SYSTEM</u> = 42.6) VT310DEL= -0.81 EVENTS 0 TE012PT= 1525.2 OVERRIDE 0 40 C 30 L 10 I 80
PT001A PT001B PT001C CT001A	INV AC VOLTAGE, PHASE A INV AC VOLTAGE, PHASE B INV AC VOLTAGE, PHASE C INV AC CURRENT, PHASE A	482.9 480.0 478.9 52.3	V V V
CT001B CT001C PT203A	INV AC CURRENT, PHASE E INV AC CURRENT, PHASE C	54.9 47.5	A CURRENT UNBAL (%) 14.3
PT003B PT003C LINKVDC	NET AC VOLTAGE, PHASE A NET AC VOLTAGE, PHASE B NET AC VOLTAGE, PHASE C LINK VOLTAGE		V V VOLTAGY UNBAL (%) 1.0
PERCPUND PSREQ MCEOC1 MCEOC2 MCEOC3 INTCOUNT	PERCENT FUNDAMENTAL PHASE SHIFT REQUEST G/I BREAKER STATUS C/C BREAKER STATUS INTER-TIE BREAKER STAT INTERRUPT COUNT	85.4 2.0 On Off Off 0	% DEG

DEMONSTRATED OUTPUT VOLTAGE:	4789 TO 482.9 VAC
REQUIRED OUTPUT VOLTAGE :	480 ± 3% NAC

RESULT!

PASS

ONSI CORPORATION

OUT PUT FREQUENCY (GRID INDEPENDENT)

DEMONSTRATED:	59.99 42
REQUIRED:	6023 HZ

RESULT:

PASS

Appendix B: Project Meeting Notes

EDWARDS AFB SITE EVALUATION MEETING 14-15 AUG96 I. OVERALL INBRIEFING TO BLONEL KULKUK & STAFF II. POTENTIAL SITES - Swimmind four - DINING HALL (WITH NEIGHBORING DORMITORIES) - HUSPITAL - FLIGHT LINE (SPACE HEATING, 3-4 MINTEDNCY) -AGING ELECTRICAL INFRASTRUCTURE - COULD REPLACE DIZSEL GENERATOR AT HUSPITAL WITH GRID-INDEPENDENT OPTION (DOUBLE BACKUP System - THEY HAVE UPS ON ALL CRITICAL LOAD ON BASE WITH DIESEL GENERATORS AS 2- BACKUP) III. VISIT TO BOTENTIAL SITES - HOSPITAL HAS BEST THERMAL APPLICATION II. OUTBRIEFING - 15-20 % THERMAL UTHLIGATION - NEED TO SEE IF FUEL CELL CAN HANDLE lof the two 200- for chilles in gild-independent mode (4 Compressions for chiller), Can switch over occur without compressors Shatting down? Confuel cell start compregns from shat down state? SAIL to chech.

I CAPT FAABORG TO WORK WITTI SAIL ON GETTING MORE EXACT RATE STRUCTURE MATH TO BETTER REFINE ECONOMIC SAVINGS,

CHAIN LINK FENCE IS REQUIRED.

Whyne Holfildt is Elison Electric Poc. Cept Raborg is Somewhat concerned about whether "selling" power to the hospital, I don't think that, a concern - we set precedent at 29 Rilms, Locar AGMD is KERN COUNTY.

QUESTION OF WHETHER SPACE HEATING OF OHW (or both) is best application - WILL GO BACK TO HOUPITAL TO DOUBLE CHECKE,

· get ful all seriel #'s, etc into database

Hospital has 500 KW + (2) 250 kW generators

* USE KEN MUNSON as PRIMARY PUC. KICKOFF MEETING 05 Feb 97 EDWARDS AFB FOR SARE OF. I. INTRODUCTIONS / OVERALL PROGRAM (NEW POC) - POSSIBLE PAPERWORK NEEDED BY EDWARDS - 1391 - ENUIRONMENTAL SITE EVALUATION REPORT SUMMARY (TORNEY) TI. - Pump Room - They're going to put a drain in these because There's a lot of 140 Water - Will need to Coordinate drain installation with fiel cell design. - Possibility of removing one of Free tauks (fuel) - Needs to be checked out. - Joe's question. 15 8' Clearence to the grates sufficient - yes. GENERAL DESCRIPTION OF ONSI / FUEL CECC III. UPCOMING EVENTS TK. - 5 Sets of drawings - 3 weeks -BAJE RESPONSIBILIES - los Boch - Philos - Publoz Relations

DESIGN REVIEW 25 MAR97 EDWARDS AFB I PURPOSE OF MEETING - BINDER INITAL BASE QUESTINS - BASE - FORM 332 NEEDS TO BE SUBMITTED TI, By KEN For BASE ASPROJAL (COMPREMENSIVE PLANNING FUGHT & ENURCONMENTAL MANABERTER;) Nect Makin, 11 May 5 For Approvel - Will WORK IT INTERNALLY THIS WEER & MAY BE ASLE TO GET PAPELWORK SIGNED OFF THINKER TT. DESIGN REVIEW - THE SAIC Comments (Unless of horaide Roted) ME-1 (1) TO BE Corrected on AT-BUILT (2) Which BE APDED ON AT-BUILT (3) Will be Labeled as not used on An- PULLIC, BAUE QUESTIC - ON PHONE LINE - Explained Connection is all that's required, (2 Class A lines). ME-1 (TAYLOR) (1) Should be adequate as is ME-1 (Itoleands) (1) Will Move on row so it doesn't

extend post and of Bldg. (2) BASE WOULD' PREFER THAT DISGING BE AVOLDED IF POSSIBLE - MIGHT SLOW PRUJEST DOWNER COMMENT IS WITHDRAWNY M-1 (SAIC) (1) Equil. LENGTH <19'- OR (2) MUST BE LESS THAN 170 prig => OK. (3) FIELD EXPERIENCE HAT STOWN THAT ONE BLEED LINE IS SUFFICIENT - INSTRUMPION (4) SEGUENCE OF OPERATION STATEMENT WILL BE REWRITTEN. HU-2 & HU-3 CAN BE USED TO OBTAIN HEAT RECOVER , STRULD FUMP P-1 FAIL. (5) WILL BE ADDED TO AJ-BUILT, M-1 (TAYLOR) (2) M-1 TO BE CHANCED TO INDICATE NEW GALINE TO CHNEET TO EXISTINC. BURIED GAS LINE. M-2 (SAIC) (1) By-Pais Values will be shown on Assailti-

E-1 (SAIC) (1) BASE & GEORGE CONTRO WILL DISCUSS AT PRECONSTRUCTION BRIEFING, (2) Will be changed to I" on AJ-BRICT. S-1 (SAIC) (1) TO BE ADDED TO AS BUILT. 5-1 (Holcomb) (1) Change on RS-BUILT (2) J/2 AJ 15

IV. Schedule (1) Base Meno to Me (2) My Memo to ONII (3) Base to key log (4) Base to take photos Or Apr - Bajt World try by ct me letter by 31 Mer

- 3 -

NOTE: BASE SUBMITED NE COMMENT FOR THE DESIGN REVIEW

25 MAR 97 EDWARDS AFB DESIGN REVIEW

Base needs to fill form 332 to got approval / review for the puziet. Normelly needs to so this planning + zoning committee. May is is when the next P+2 meets. George wants to start a week from monday (7 NR 97).

· JUE - DESIGN COMMENTS

- comment by base, they cannot run any phone line. Response for for, all they need to do is provide a phone interface, George will run the cable.

- The will move to is bottlis back so that they are flush with building. - Comment about drigging waterground, base does not want to do ing drigging, overhead lines are fine.

- Granding of fince and No bottles, george will descuss with base at the preconstruction meeting.

KER MUNISON- DOESN'T USE EMAIL I USE SAME SKNMAX AS SUFNARS -

-4-

EDWARDS AFB ACCEPTANCE TEST 16 JUL 97 KEN MUNSON - EDWARDS AFB DOUG YOUNG - ONSI MIKE BINDER - USACERL KEN MUNSON DIDN'T WANT TO REVIEW ARCETTANC TEST REPORT OR AS-BUILTS, HE WANTED TO TREAT -THE FUEL CELL AS REAL PROPERTY WHICH WOULD REQUIRE THE COMMANDER TO SIGN THE DO250. THIS COULD TAKE A COMPLE WEEKS, KEN CAUCO LT MATT SUFWAR IN. THE LT SHIP THE FUEL CELL COULD BE TREATED AS THE EQUIPMENT (SAME AS A GENERATOR ON CHILLER) AND THAT KEN COULD SIGN THE DDZSD, KEN SAID THE HOSPITAL DID NOT WANT A DEDICATION CEREMUNY -SINCE THEY WERE LOSING MONEY. EDWARDS BILLS THE HOSPITAL AT AN AVERAGE PRICE FOR ELECTRICITY (INCLUDING WAPA) WITCH DOES NOT OFFSET THE NATION GAS PRICE. I REMINDED KEN THAT EDWARDS AFB WAS SAUNCS THE MGH PRUE ELECTRICITY RURCHASED FROM THE UTILITY. HE AGREED BUT SAID THE HOSPION DOESN'T SEE THAT SAVINGS, DOUG & I TOURED THE FUEL CELL SITE,

Appendix C: Review Letters for Original Design Drawings



February 14, 1995

Or, Mike Binder USACERL Energy and Utilities Systems Division 2002 Newmark Drive Champaign, (L. 61821/1076

Subjeen Twenty-Niae Patros Final Design Review

Dear Mike:

SAIC and our licensed machanical and electrical subconstructors, have reviewed the fuel collinstallation design drawings for the 'Fwenty Ning Palms Marine Corps, Base, Our comments are presented below.

1. HEAT REJECTION LOOP (COOLING MODULE)

- a. Assumed 30 gpin Row rate.
- b. Total equivalent piping length of 335 feet.
- Pressure drop 30 gpm in 2" pipe ± 27100".
- d. Fluid coster pressure drop 12 at 30 gpm.
- c. Total pressure drop external to fuel cell is $(3.35^\circ \times 2^\circ) + 12^\circ = 18.7^\circ$

Pipe sizing and velocity are alequate at 2°. Discharge head for circulating pump located in piel cell power module should include the 18.7° pipting loop pressure drop.

- 2. HEAT RECOVERY PIPING CUSTOMER SIDE
 - a. Flow rate 50 gptt.
 - 5. Total equivalent piping length 318 fort.
 - e. Pipe size 0"
 - d. Pressure drop +25 gpm in 3" pipe = 0.8/100".
 - c_s Piping pressure loss = 3.18 x 0.8 = 2.8°
 - $\xi_{\rm e}$. Pressure drop through (LEX880 (in power condule) = 15^{110}
 - g. For al pump head required = 2.8 % if $\beta=17.7^{\circ}$

Piping sizing and vehenty are adequate at 3"; however, as not velocity is low at 2.3 feet per second, some savings could be realized by utilizing 2" pipe versus 3". A check valve is <u>recommended</u> at the discharge of Recipculating Pump P 2.

10260 Campus Fourt Dave, Sun Dicigo, Celifurnia 92191-1578 (619, 546-6006



MEAD RECOVERY PPING - FOFF, CELL SIDE (HEX8501 O STORAGE TANK LOOP W/P-D)

- all province (25 gpm)
- Is Pipe size ossurae 2 -
- Total equivalent piparg length 2211
- d = Procesure crop 25 gpm in 21 pipe = 1.591(0)1
- e. Piping pressure loss = $2.21 \times 1.5 \pm 3.5$
- f. Pressure arap through HFX880 = $(2^{\circ}\pm$
- $g = Total bump (non-required = 3.3) = (5.4 \pm 0.3)$

Piping strong and valueity are adoptate of 7". The B&G Series 90, vize 1-1/0A, 1/2 H.P. pump is adecuate.

4. CITY WATER TO FUSE, CHU, SOWER MODULE

- a. Flow rate assume 10 gpm ±
- Woter pressure assume 50 psig 11.
- n. Total equivalent piping length 1561
- c. Pressure drop 10 gpm in 3/4" pipe = 10 psig/100"
- Pressure drop through HSX880 assume 15¹¹
- Jotal pressure deep then is (1.56 x 10) + ((5) x .45) = 22 psig. The 3/4" pipe size is compute assuming that about 23 psig at the first cell inforths satisfactory.

Should the City water supply not be isolated from the pathle system elsewhere in the plant, an approved backflow prevention device second be provided.

- 5. NATURAL GAS
 - a. Connocteu Joad 1,900 CEH
 - b. Pipe size 3
 - c. Pressure at point-of-consocition assume under 14" W.C.
 - b. Cotal equivalent proine length 180%
 - Moximum delivery capacity of 0.00 specific gravity natural gas per nour with pressure drop of 0.5 inon water column in 5° ppe is 8,257 CFR. Pipe sizing at 3° is adequate.
- a. NITROGEN
 - a Required flow rate could not be reformined from data providen.
 - b. Proe size 3/4"
 - 5. Totol equivalent proing length = 50.

Assuming a required delivery pressure or 50 psig at the triel cell power module connection, capacity of a 361 pipe is in excess of 0.600 there, per minute. This tope size should be adoptize depending on ONSP's maximum enticipated flow rate.



ELECTRICAL

- a. The many should be stranged by a registerior electrical engineer.
- More details should be given for the new 400A subpanel: i.e., mounting ACC, breaker sizes, etc.
- "Do sizes of conduits and conductors from new sub-panel to "NTH" and "HNH" should be given.
- d. The 120V power source to the fuel ed.) power medule should be shown
- e. Show ground grad around fuel cell enclosure and all termination points.
- f. Show routing to more P005 along with feeder length and voltage drop.

Based on the 10.5% and 14.5% supply temperatures for the domestic hot water coops, the 5,000 gallon storage took appears adequate. The datailed electrical and thermal designs are sufficient, With consideration of the above comments, we believe that the site design is adequate to proceed with construction.

Sincerely,

.

Genry Mesters

Division Manages, Advanced Energy Systems

	PALMS RECORD DRAWING CHANGES 6/19/95
DRAWING	<u>C.KANGE</u>
	Equipment positioning adjustments including notrogen rock to have side of pad
	Fance lengtheneel 1 ft to 52 ft
<u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u></u>	Equipant position adjustments
ME-1	Equipment responsituried do on 5-1
	Spape conduct: added <u>Centergency</u> power cond) Building wall percentations noted
	Disornet lubel: changed (reversed GCFGI)
	Storage tamle dimension typo corrected Wirking values labeled! ("mlets StC, outlet A) Closed values illustrated
	No changer
	Grounding Misstration changed to correspond to ground gril on 9061 E-3 dreaving
E-2	No changes
<u> </u>	Ground grill updated,

Appendix D: PC25C Fuel Cell Forced Outage Description Codes

Fleet Log

			Model C				μαί	
FORCED OUTAGE ORIGIN BY POWER PLANT		ANT		CHANGE IN STATE		FORCED OUTAGE/ UNFORCED OUTAGE		
DESCRIPTION				DESCRIPTION		DESCRIPTION		
	CODE1	CODE2	CODE3		CODE		CODE	
	PSS	CODEZ	CODES	POWER UP	PU	FORCED	F	
POWER SECTION SYSTEM	P55		HTR310A	POWER DOWN	PD	UNFORCED	Ů	
FREEZE PREVENTION HEATER A			HTR310B	IDLE UP	IU	ON ONOLD		
FREEZE PREVENTION HEATER B			GFD-001	IDLE DOWN	ID			
GROUND FAULT DETECTOR			VT310	SHUTDOWN	S			
HALF-STACK VOLTAGE MONITOR			1010	NONE	N			
FUEL PROCESSING SYSTEM	FPS			Home				
SHUTOFF VALVE	110		CV000					
SHUTOFF VALVE			CHV100					
CHECK VALVE			CV100					
FLOW CONTROL VALVE			FCV012					
EJECTOR			EJT010					
REFORMER			REF300					
LOW TEMP SHIFT CONVERTER			SC300					
AIR PRE-HEATER			HEX910					
BURNER CONTROL			BSC001					
INTEGRATED LOW TEMP SYSTEM		ILS						
	101000							
AIR PROCSSING SYSTEM	APS							
FILTER			FIL100					
PROCESS AIR BLOWER			BLO100					
CATHODE			FCV100					
CATHODE AIR VALVE			FCV110					
REFORMER BURNER			FCV140 ZT110					
VALVE POSITION INDICATIOR			FT140					
AIR FLOW TRANSMITTER			HO135					
HAND ORIFICE			FO130					
FIXED ORIFICE REFORMER BURNER SENSOR			BE030					
Ref officer borner benoon								
THERMAL MANAGEMENT SYSTEM	TMS							
FLOW SWITCH			FS400					
THERMAL TEMP MANAGEMENT CONTROL			TE400					
THERMAL TEMP MANAGEMENT CONTROL		0000	TE431					
CELL STACK COOLING H20 SUB-SYSTEM		CSCW	100400					
COOLANT ACCUMULATOR			ACC400 PMP400					
COOLANT PUMP			HEX400					
THERMAL CONTROL HEAT EXCHANGER			FO400					
FLOW ORIFICE			FO400					
FLOW ORIFICE			HEX310					
BLOWDOWN COOLER BLOWDOWN VALVE			FCV430					
BLOWDOWN VALVE MIXED RESIN DEMINERALIZER BED			DMN440					
ELECTRIC HEATER			HTR400					
MOTORIZED VALVE			TCV400					
ANCILLARY COOLANT SUB-SYSTEM		ACS						
PUMP			PMP830					
BLOWDOWN COOLER			HEX431					
CONDENSER			HEX920					
CUSTOMER HEAT EXCHANGER			HEX880					
FORCED CONVECTION COOLING MODULE			HEX800					
SELF-ACTUATED FLOW CONTROL VALVE			TCV800					
MOTORIZED VALVE			TCV830					
HAND ORIFICE			HO840					

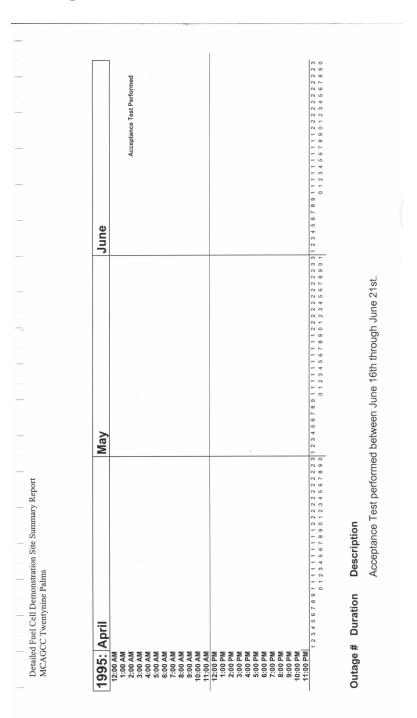
page1

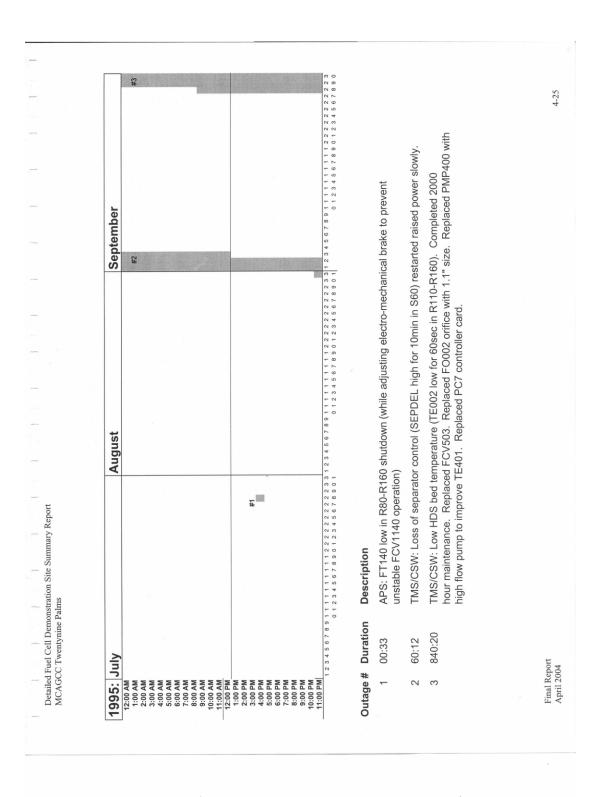
		Model C		
WTS				
		CHV451		
NPS				
		CV720		
		CV710		
		F0720		
		EJT710		
CVS				
		FAN165		
		FAN150		
		FS165		
		FIL150		
		FCD150		
		TE150B		
		CV500		
ES				
	PCS			
		MCB001		
		MCB002		
		MCB003		
	PDS			
		UPS001		
	PPC			
		LDT		
	ECS			
OTR				
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		SBSTK		
	OTRG	GRID		
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page2

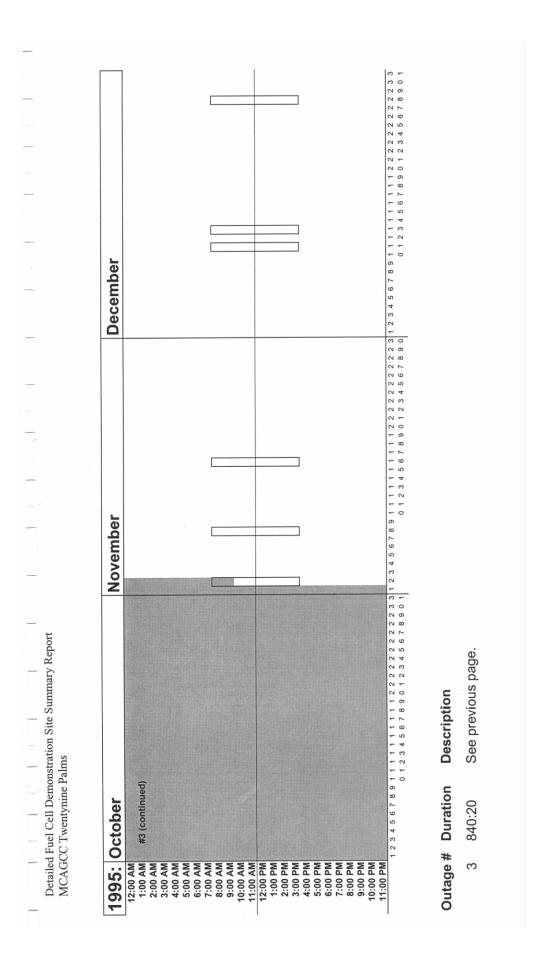
99

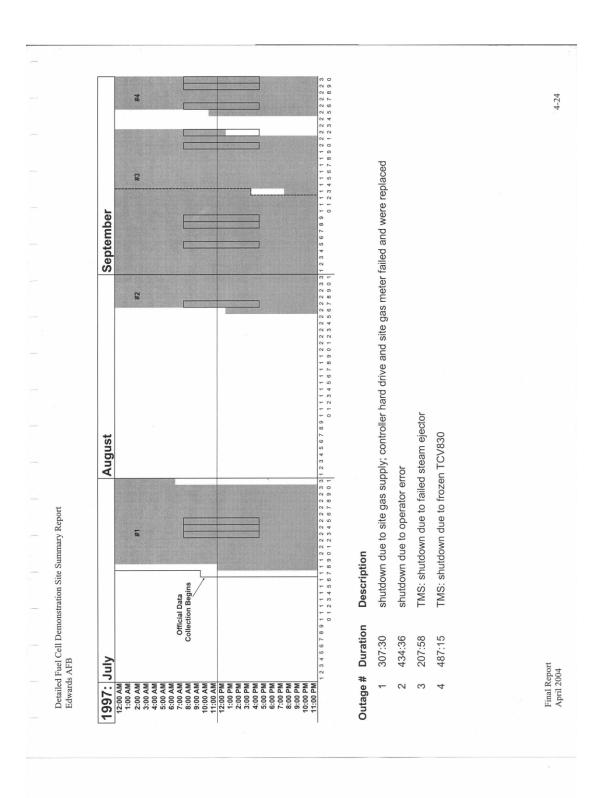
Appendix E: Summary of Maintenance Invoices by Year

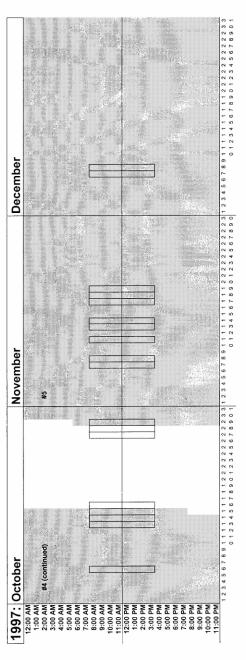




101







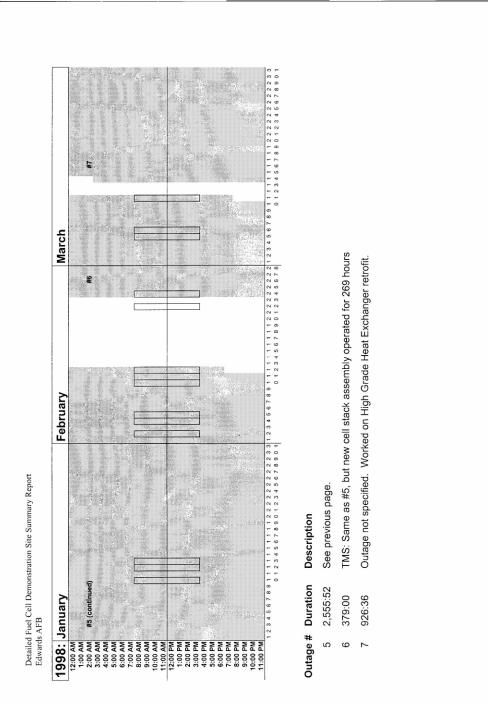
Outage # Duration Description

4 487:15 See previous page.

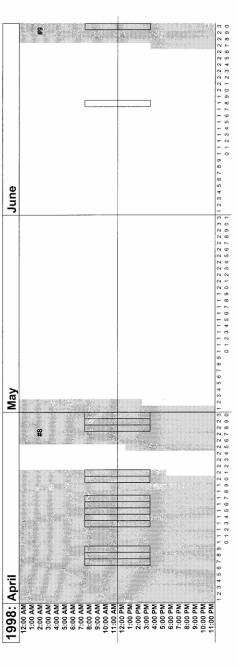
S

TMS: P/P shutdown due to failed cell stack assembly cooler. Foreign restricted cooler coil #17, causing failure of sub stack nos. 16 & 17. The fuel cell stack was removed and sent to UTC Fuel Cells for repair. 2,555:52

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Outage # Duration Description

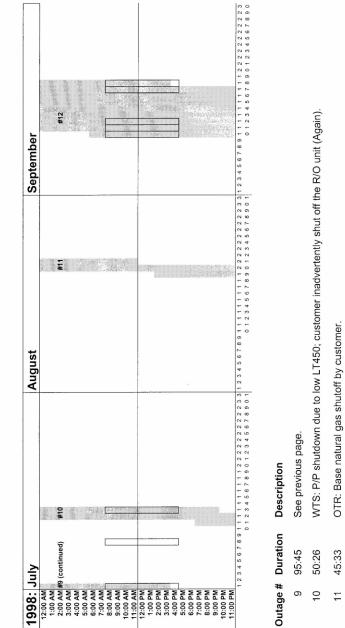
926:36 See previous page.

~ 8

- 169:30 Outage not specified. UTC Fuel Cells worked at site.
- 95:45 WTS: P/P shutdown due to low LT450; customer inadvertently shut off the R/O unit.

σ

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OTR: Shutdown due to blown cooling module motor fuse; found and repaired cut wire.

201:40

12

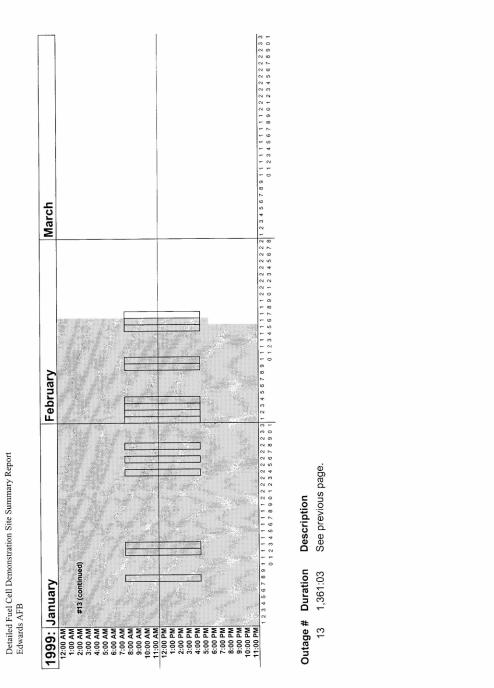


1998:	1998: October	November	December
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4:00 AM			
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Outage # Duration Description

13 1,361:03 FPS: New reformer installed.

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4-30

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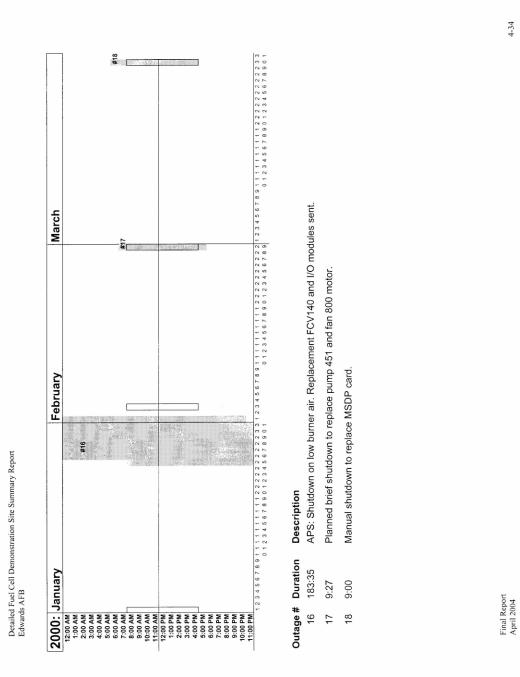
Final Report April 2004

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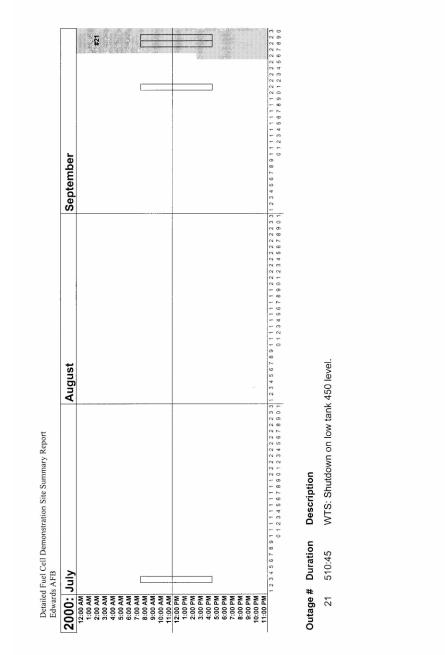
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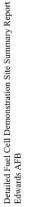




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20	51:40	Outage not specified.				



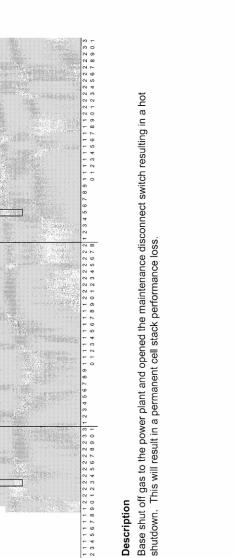
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	D	1 2 3 4 5 6 7 8 9 0 1 2 3 4 5 6 7 8 9 0	0123456789012345678901	0 1 2 3 4 5 6 7 8 9 0 1 2 3 4 5 6 7 8 9 0
# 020		Decembrica		
outage #		rescription		
21	510:45	See previous page.		
22	28:00	Power plant shutdown whe	Power plant shutdown when base contractor cut natural gas line.	
23	55:55	OTR: Shutdown on controller failure.	ller failure.	
24	51:30	NPS: Shutdown due to sus	NPS: Shutdown due to suspected failure of CV720, solenoid valve.	



Outage # D

- 21 22 23 24

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23456789111111112222222233 01234567890123456789012345678901

Description

Outage # Duration

6,193:22

25

Detailed Fuel Cell Demonstration Site Summary Report Edwards AFB

2001: January

March

February

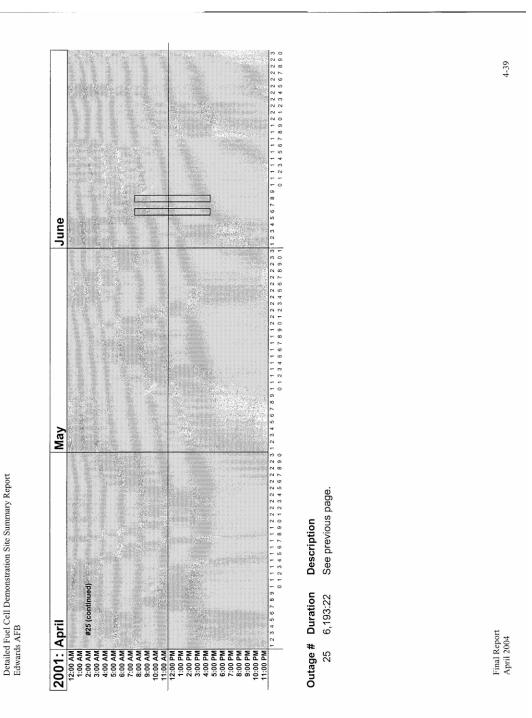
1. S. A.

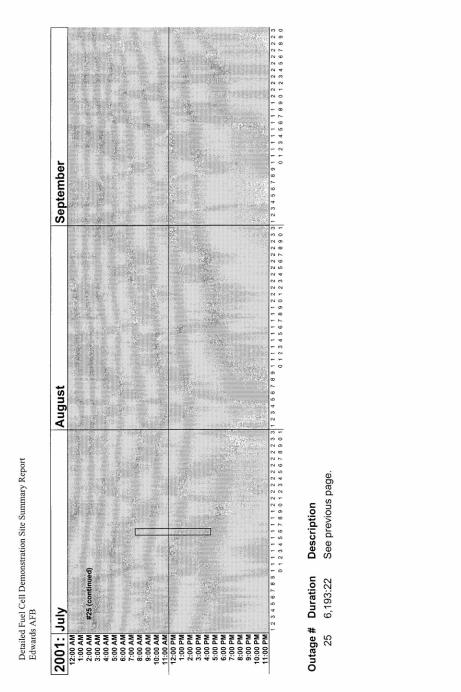
#25

E

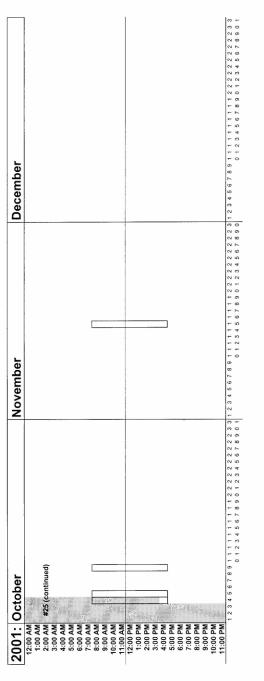
12:00 AM 2:00 AM 2:00 AM 3:00 AM 5:00 AM 5:00 AM 8:00 AM 11:1:00 AM 11:1:00 PM 4:00 PM 6:00 PM 6:00 PM 6:00 PM 7:00 PM 11:00 PM 7:00 PM 11:00 PM

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Outage # Duration Description

25 6,193:22 See previous page.

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Site Summary Report	
el Cell Demonstration	B
Detailed Fue	Edwards AF

2002:	January	February	March
12:00 AM			
2:00 AM			#26
3:00 AM			
4:00 AM			
6:00 AM			
7:00 AM			
8:UU AM			
10:00 AM			
11:00 AM			
12:00 PM			
1:00 PM			
2:00 PM			
3:00 PM			
5:00 PM			
6:00 PM			
8:00 PM			
9:00 PM			
10:00 PM 11:00 PM			
	12345678911111111122222222223312345678911111111122222222222	123456789111111111222222222	1234567891111111111222222233
	0 1 2 3 4 5 6 7 8 9 0 1 2 3 4 5 6 7 8 9 0 1	0 1 2 3 4 5 6 7 8 9 0 1 2 3 4 5 6 7 8	0 1 2 3 4 5 6 7 8 9 0 1 2 3 4 5 6 7 8 9 0 1

Outage # Duration 26 150:23

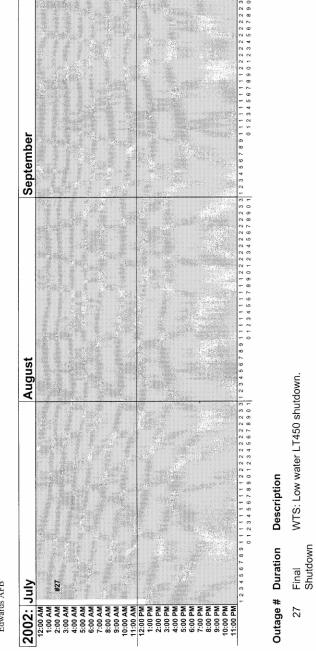
Description OTR: Shutdown (unknown cause) with controller reboot.

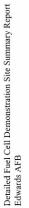
Final Report April 2004

2002: April		May	June
12:00 AM 1:00 AM 2:00 AM #26 (continued) 3:00 AM	(pe		
4:00 AM 5:00 AM 6:00 AM 7:00 AM			
8:00 AM 9:00 AM 10:00 AM 11:00 AM			
12:00 PM 1:00 PM 2:00 PM			
3:00 PM 4:00 PM 5:00 PM			
6:00 PM 7:00 PM 8:00 PM		×	
9:00 PM 10:00 PM 11:00 PM			
12345678	191111111122222223 012345678901234567890	123456789111111111111222222222221234567891111111122222222233123456789111111222222223 012345678901234567890 012345678901234567890	1 2 3 4 5 6 7 8 9 1 1 1 1 1 1 1 1 1 1 2 2 2 2 2 2 2 2 2
Outage # Duration Description	n Description		
26 150:23	See previous page.		

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Final Report April 2004





REPORT DOCUMENTATION PAGE

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OMB No. 0704-0188

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14. ABSTRACT								
Fuel cells are an environmentally clean, quiet, and a highly efficient method for generating electricity and heat from natural gas and other fuels. In fiscal year 1993 (FY93), the Engineer Research and Development Center, Construction Engineering Research Laboratory (ERDC-CERL) was assigned the mission of managing the DOD Fuel Cell Demonstration Program. Specific tasks included developing turnkey PAFC packages, devising site criteria, screening candidate DOD installation sites based on selection criteria, evaluating viable applications at each candidate site, coordinating fuel cell site designs, installation and acceptance of the PAFC power plants, and performance monitoring and reporting.								
CERL selected and evaluated 30 application sites, supervised the design and installation of fuel cells, actively monitored the operation and maintenance of fuel cells, and compiled "lessons learned" for feedback to fuel cell manufacturers. At the conclusion of the demon- stration period, each of the demonstration fuel cell sites was given the choice to either have the fuel cell removed or to keep the fuel cell power plant. This report presents a detailed review of a 200 kW fuel cell installed at Edwards Air Force Base (AFB) and operated between July 1997 and July 2002.								
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