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EXECUTIVE SUMMARY

A. OBJECTIVES

The objective of this reseach is to document the performance of the electrolysis process for hydrogen generation when pulsed DC and anode depolarization are used. The resulting data were to be used in designing an efficient electrolytic cell that meets the Air Force needs.

B. BACKGROUND

Hydrogen can play an important role in future energy systems because of the diversity of its applications, the variety of ways in which it can be stored, its environmental advantages, and the possibility of producing hydrogen using solar, nuclear, wind, hydropower, and other renewable energy sources. The environmental impact of hydrogen as a source of energy is very favorable. Signs of the world moving to the hydrogen economy are evident. The Euro-Quebec Hydro-Hydrogen agreement will produce 20 million cubic feet of pure electrolytic hydrogen per day for use as transportation fuel at Hamburg, Germany, and to fuel a hydrogen-powered version of the European-made Airbus_aircraft.

The U.S. Department of Defense interest in hydrogen applications is growing fast. The Army Research Office (ARO) obtained a 500-watt fuel cell design that weighs less than 10 pounds for individual soldier power. Currently, ARO is exploring the feasibility of using fuel cells for power generation on the battlefield. The requirement is a small, light, and inexpensive hydrogen supply device which could convert a readily available material to hydrogen of sufficient purity to operate the fuel cells. If such a device can be engineered with efficiencies much higher than those of existing methods, hydrogen would play a viable economic role in future Air Force applications. These applications could include heat pumps; power generation; and fuel for cooking, vehicles, and aircraft.

Water electrolysis is a simple process where electrical energy is converted to chemical energy in the form of hydrogen. However, the very use of electrical energy is the major disadvantage of the water electrolysis. Electrical energy is relatively expensive, and efforts are underway to maximize the efficiency of the water electrolysis process so that hydrogen can be produced at levels competitive with the production of petroleum fuel.

C. SCOPE

This research effort investigated the performance of water electrolysis using anode depolarization and pulsed DC power. The research consisted of four major tasks: 1) develop a laboratory experiment; 2) examine the anode depolarization effects; 3) examine the pulsed DC power operation; and 4) examine the combined effects of pulsed DC and anode depolarization. Due to the lack of 6.1 funds, only the first task was completed while the second and third tasks were partially accomplished.

D. RESULTS

The experimental results show that significant improvement in the performance of the water electrolysis is feasible. Using sulfur dioxide as anode depolarizer dissolved in a 10 percent by weight sulfuric acid anolyte has the potential of improving the process performance up to three times that of the conventional water electrolysis. In the case of pulsed DC, the results are in conflict with those reported in the literature, and further work is needed to settle the issue of using pulsed DC in water electrolysis.

E. RECOMMENDATIONS

This research offers many potential payoffs that would benefit the Air Force and other branches of the United States Government. Given a clearer understanding of the electrolytic process behavior at ionic level, advances are possible in the areas of electrode material and design, depolarizers, and electrolytes. Therefore, a basic research program is recommended and a new design based on the state-of-the-art ultramicroelectrode technology, is proposed. The use of these three-dimensional electrodes will increase the contact time with the depolarizer material which translate to larger hydrogen production. The hydrogen yield density is expected to be 1 to 2 order of magnitude greater than the conventional two-dimensional electrodes. The overall goal of the proposed research is to explicitly account for the characteristics of the double-layer and the nature of the oxidation process at the anode in describing the electrolytic process behavior under varied loading conditions.

PREFACE

This report was prepared by the Air Force Civil Engineering Support Agency (AFCESA), Research, Development, and Acquisition Division, Air Base Operability and Repair (RACO) and Applied Research Associates (ARA). ARA efforts were performed under SETA Contract Number F08635-C-88-0067.

The author wishes to express his gratitude to Mr Edgar Alexander for his interest in this project and continuous encouragement and support during the course of this effort. The author wishes to thank Dr Larry C. Muszynski for his help during the course of this effort and Mr Daniel J. Weston for his contributions in setting up the experiment and the design of the electrical setup.

This report summarizes work done between June 1991 and November 1992. Mr Edgar Alexander was the AFCESA Project Officer.

This report has been reviewed by the Public Affairs Office and is releasable to the National Technical Information Service (NTIS). At NTIS, it will be available to general public, including foreign nations.

This technical report has been reviewed and is approved for publication.

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SECTION I

INTRODUCTION

A. OBJECTIVES

The principal objective of this research is to examine the effects of pulsed DC power and anode depolarization on the performance of the water electrolysis process. The resulting data then to be used in the design of an efficient electrolytic machine that meets Air Force needs.

B. BACKGROUND

Hydrogen can play an important role in future energy systems because of the diversity of its applications, the variety of ways in which it can be stored, its environmental advantages, and the possibility of producing hydrogen using solar, nuclear, wind, hydropower, and other renewable energy sources. The environmental impact of hydrogen as a source of energy is very favorable. It burns cleanly and can be obtained from water with water vapor as its combustion product.

The present market for hydrogen is limited to food hydrogenation, ammonia, and metallurgical processes. In the future, when the so-called hydrogen economy starts to take place, energy will be a major hydrogen user market which will dwarf the present market. Hydrogen applications in energy areas range from consumption of hydrogen as a fuel (e.g. transportation fuel, home heating and cooking, etc.) to closed cycle applications as in the metal hydrides heat pump. Signs of the world moving to the hydrogen economy are evident. The Euro-Quebec Hydro-Hydrogen agreement [1] will produce 20 million cubic feet of pure electrolytic hydrogen per day for use as transportation fuel at Hamburg, Germany, and to fuel a hydrogen-powered version of the European-made Airbus aircraft.

Combined with other elements hydrogen can be found in abundance. For example, one mole of water consists of one mole of hydrogen combined with half a mole of oxygen. Several methods were devised to liberate hydrogen from hydrides. Water electrolysis is the commercially applied process to obtain hydrogen from water at 99.99 percent purity. Water electrolysis is a simple process where electrical energy is converted to chemical energy in the form of hydrogen. However, the very use of electrical energy is the major disadvantage of the water electrolysis. Electrical energy is relatively expensive and efforts are underway to maximize the efficiency of the water electrolysis process so that hydrogen can be produced at levels competitive with the production of petroleum fuel.

The U.S. Department of Defense interest in hydrogen applications is growing fast. The Army Research Office (ARO) obtained a 500-watt fuel cell design that weighs less than 10 pounds for individual soldier power. Currently, ARO is exploring the feasibility of using fuel cells for power generation on the battlefield. The requirement is a small, light, and inexpensive hydrogen supply device which could convert a readily available material to hydrogen of sufficient purity to operate the fuel cells. If such a device can be engineered with efficiencies much higher

than those of existing methods, hydrogen would play a viable economic role in future Air Force applications. These applications could include heat pumps; power generation; and fuel for cooking, vehicles, and aircraft.

C. SCOPE

This effort experimentally studied the performance of water electrolysis for hydrogen generation under two concepts: (1) the depolarization of the anode using sulfur dioxide to reduce/eliminate the anodic losses; and (2) the use of pulsed DC electric power instead of the nonpulsed DC currently used.

The effort involved the development of a laboratory experiment which consisted of a series of tests using the Fm01-LC electrolytic cell, manufactured by ICI Chemicals & Polymers. The tests were divided into four series: (1) A nonpulsed DC power test set to determine the cell's baseline performance; (2) Anode depolarization under nonpulsed DC power test set to determine the cell baseline performance efficiency using sulfur dioxide as anode depolarizer; (3) A pulsed DC power test set to determine the cell performance as a function of the pulsed energy parameters; and (4) Anode depolarization under pulsed DC power test set. Due to cuts in 6.1 findings, only the first three were partially accomplished.

SECTION II

WATER ELECTROLYSIS PROCESS

A. WATER ELECTROLYSIS THERMODYNAMICS

In the conventional electrolysis of water, hydrogen is generated by electrolyzing an acidic or alkaline aqueous solution. The overall reaction takes place as follows :

$$H_2O + Electrical Energy \rightarrow H_2 + \frac{1}{2}O_2$$
 (1)

where the electrical energy is converted to chemical energy as hydrogen. The reaction at the electrodes can be as follows:

a. Cathode (Hydrogen Electrode)

$$2H_{2}O + 2\theta^{-} \rightarrow H_{2} + 2OH^{-}$$
⁽²⁾

b. Anode (Oxygen Electrode)

$$2 OH^{-} \rightarrow \frac{1}{2} O_2 + H_2 O + 2 \theta^{-}$$
 (3)

In this process water is consumed and only two electrons are involved in the dissociation of one molecule of water. There are no side reactions in water electrolysis that could yield undesirable products, so the process is clean and requires no extra separation or purification of products.

The first law of thermodynamics for an open system states that :

$$Q - W_{g} = \Delta H \tag{4}$$

where Q is the heat added to the system, W_s is the useful work done by the system and ΔH is the change in system enthalpy. Since the work done is the electrical energy applied to the electrolyzer, W_s is given as :

$$W_{s} = -nFE \tag{5}$$

where:

- *n* is the number of electrons transferred;
- F is the Faraday constant; = 23,074 cal/volt.gm equiv; and
- *E* is the electric potential applied to the cell in volts.

manipulating Equations (4 and 5) gives

$$E = \frac{\Delta H - Q}{n F} \tag{6}$$

For isothermal reversible process (no losses), Q is given as

$$Q_{rov} = T \Delta S \tag{7}$$

where T is temperature and ΔS is the change in system entropy. Substituting Equation (7) into Equation (6) results in the definition of the cell reversible potential below which neither hydrogen nor oxygen can be generated.

$$E_{nev} = \frac{\Delta H - T\Delta S}{n F}$$
(8)

 $(\Delta H-T_{\Delta}S)$ is the change in the system Gibbs free energy ΔG . At standard conditions (25 °C and 1 atm) ΔH equals 68,320 cal/gmole and ΔG equals 56,690 cal/gmole. Therefore, the cell reversible potential equals to

$$E_{nov} = \frac{\Delta G}{n F} = \frac{56,690}{2 (23,074)} = 1.23 \text{ volts}$$
(9)

Because of the inefficiencies in the electrolysis process, the potential required to drive an electrolysis cell at a practical hydrogen generation rate (i.e. current, *I*, which is proportionate to hydrogen generation) is higher than the cell reversible potential. In Equation (6), *n* and *F* are constants, and for the same conditions of pressure, temperature, and electrolyte concentration, $_{\Delta}H$ is constant and *Q* will change as *E* changes. As the process becomes irreversible and inefficient, *Q* decreases and eventually becomes negative where electric energy is wasted as heat. At the point where no heat need to be added to the cell (*Q=0*) and all energy needed is supplied by electrical energy, the corresponding cell potential is called the thermoneutral voltage. This potential is given by :

$$E_{thermo} = \frac{\Delta H}{n F} = 1.48 \quad volts \tag{10}$$

However, current cell design requires operating voltages higher than the thermoneutral voltage. At these operating voltages, part of the electrical energy is lost as heat which raises the cell temperature and requires cell cooling.

The operating potential of an electrolyzer is given by:

$$E = E_{mev} + Losses \tag{11}$$

where the electrolysis process losses are :

$$Losses = E_{anode} + E_{cathode} + E_{mt} + IR$$
(12)

where

Eanode	is anode activation overpotential
Ecalhode	is cathode activation overpotential
E _{mt}	is mass transfer overpotential
IR	is ohmic overpotential (I is current and R is cell resistance which include
	electrolyte, electrode, and terminals)

The efficiency of a conventional electrolysis cell is given by:

$$\eta = \frac{\Delta H}{\Delta G + losses} = \frac{E_{thermo}}{E}$$
(13)

Therefore, under ideal conditions (no losses or reversible process), the production of hydrogen will take place with an efficiency of 120 percent, and at thermoneutral conditions the cell efficiency is 100 percent.

Current electrolyzers are running at 75 percent efficiency. The exergy analysis of the water electrolysis process shows the majority of the losses are caused by the cell internal design and not external emission. To reach higher electrolysis efficiency, current research efforts are devoted to optimizing cell design to reduce internal losses.

B. DOUBLE-LAYER THEORY - ELECTRIFIED INTERFACE

In the interior laminas of an electrolyte, the net charge is zero. This is because the solvent dipoles are in random orientation and equal distribution of positive and negative charges exists. For the ion discharge to take place, the electrical charge on the electrode has to be matched by an opposite charge in the electrolyte across the electrode-electrolyte interface where a potential difference arises. Therefore, upon applying an electrical field, the electrical forces operating at the electrode-electrolyte interface give rise to another arrangement of solvent dipoles and charged species. A net orientation of solvent dipoles and a net or access charge on a lamina parallel to the electrode are established. The existence of two oppositely charged layers gave rise to the term *double-layer*. The term *double-layer* is used to describe the arrangement of charges and orientated dipoles constituting the interphase region at the boundary of the electrolyte. Figure 1 shows the electrified interface in the double-layer concept. The charge and discharge of the double-layer could play a role in improving the performance of water electrolysis.

C. IMPROVEMENT IN WATER ELECTROLYSIS

The thermodynamic analysis of water electrolysis indicates that the electrical energy required for a practical dissociation rate can be reduced if the number of electrons involved in the reaction (Equation 6) is maximized and the losses that increase the cell potential (Equation 11) are minimized. The activation overpotential is one of these losses and represents the energy required to overcome the surface potential barrier which retards the ionic discharge processes to the electrodes. The activation overpotential is largely at the anode [2] and represents most of the losses in the electrolyzer cell. In order to enhance the ionic discharge, and thus the hydrogen evolution rate, we must diminish the energy barrier at the anode. However, diminishing the anode overpotential by using catalysts [3] while keeping oxygen evolution is expensive and will not reduce the cell potential below the reversible potential of 1.23 volts.



Figure 1: Arrangement Of Charges And Orientated Dipoles In The Double-Layer Concept

If the oxygen evolution is replaced by another anodic reaction that takes place at lower potential than that of oxygen, then the cell potential (Equation 6) would be reduced. This process is called anode depolarization. Further, if the new anodic reaction involves more electrons, then the reversible potential, E_{rev} , and hence the cell potential, E, would be reduced dramatically.

Another likely approach to enhance ion discharge [4] would be a modification to the conventional electrolysis process and would involve assisting the electrochemical reaction by supplying either part or all of the energy required to overcome the surface potential barrier by using some energy form other than DC electric energy. In this area Brookhaven National Laboratory (BNL) [5] identified the utilization of heat and electricity in water vapor electrolysis, while Gutmann and Murphy [4] suggested the use of pulsed DC.

One major disadvantage in water electrolysis is the use of electricity as raw energy. If the electricity is produced by a thermal conversion of coal or oil, the Carnot limitation is applied, thereby limiting the process's overall efficiency. Renewable energy such as solar/photovoltaic, wind power, and hydroelectric power are attractive raw energy sources for water electrolysis. The use of solar energy in water electrolysis for hydrogen production has been studied in laboratory settings using a polycrystalline Si photovoltaic 100 W generator [6]. During the same period it has been demonstrated on a practical scale at an existing 350 kW photovoltaic site in Saudi Arabia [7]. This link between photovoltaic power and electrolysis eliminated the complex power conditioning interface required when AC electric energy is used and, in turn, eliminated the losses encountered in converting AC to DC.

1. Anode Depolarization

In the electrochemical decomposition of water, the overpotential in the splitting of water is largely at the anode. A lower anodic overpotential can be expected if some alternative anodic product other than oxygen can be produced. This can be achieved by introducing a depolarizer into the anolyte. The depolarizer must be sufficiently cheap while the anodic product

must be nontoxic, easy to remove from anolyte, and marketable.

Work on anode depolarization for hydrogen production was reported as early as 1967 by Juda and Moulton [8]. In their search for cheap hydrogen to be used in the nitrogen fertilizer industry, they used sulfur dioxide (SO2) as an anode depolarizer which had been used earlier as an anode depolarizer in the electrolysis of copper sulfate for electroplating. In their experiment, a 30 percent sulfuric acid was used as electrolyte and a 6 percent sulfurous acid was pumped through the porous carbon anode. They found that hydrogen could be produced cathodically while sulfur dioxide is oxidized anodically to sulfuric acid (H₂SO₄). The effect of SO₂ oxidation is reported to reduce the cell potential approximately 0.8 volts below that of nondepolarized cell. Conversely, the reaction would yield sulfur on the electrodes, so a cheap method would be needed to utilize the sulfur and recover it successfully [4]. Since the publication of Juda and Moulton's work [8], much work has been published on developments in the technology of sulfur dioxide depolarized electrolysis. For example, Lu et al [9] studied the effect of H₂SO₄ concentration on the operation of SO₂-depolarized electrolyzers. They reported that optimum acid concentration is about 30 percent by weight where the observed cell potential is 0.71 at 200 mA/cm². They observed that cell potential increased significantly with acid concentration.

Recent attempts to explore suitable depolarizer reactions have concentrated on the oxidation of fuel-like substances such as coal [11-16], methanol [17], and glucose [18]. All such reactions can be represented by the following general reaction:

$$F + x H_2 O \rightarrow FO_x + 2x H^+ + 2x \theta^-$$
(14)

where F is the fuel-like molecule which becomes oxidized to FO_x with generation of hydrogen ions and electrons. The oxidation of the fuel-like molecule insures favorable thermodynamics in the form of a reversible potential more negative than oxygen evolution.

Renewable organic materials such as biomass (animal manures, sewage sludge, or food processing wastes) which contain too little caloric value to make them practical alternate sources of energy can be used as depolarizers. Dhooge and Henson [19] investigated the reaction rates and activation energies for the catalyzed electrolytic oxidation of wood chips, cattle manure, and municipal sewage sludge. They showed that the process is practical and can be used to produce hydrogen at potential of 1 volt with carbon dioxide and methane as anodic products.

Bockris, Dandapani, Cocke, and Ghoroghchian [10] reported that the use of lignite and anthracite as depolarizers has created a new field for coal slurry electrolysis. Using coal as anode depolarizer, Coughlin and Farooque [11-13] found the potential for CO_2 evolution about 1.0 volt. Current densities were very low around 0.01 to 0.02 mA/cm², not enough for commercial operations. Their work was carried out in coal slurries in sulfuric acid solution and the electrodes were platinum screens. They attributed the current obtained to the direct oxidation of coal particles at the anode surface. Okada et al [19] disputed some of Coughlin and Farooque's findings on the basis that acid washing of coal removed the reactive compounds. Dhooge and Park [20-22] indicated that much of the electrode depolarization reaction observed by Coughlin and Farooque was a result of the oxidation of ferrous ions that were leached out of the coal by the sulfuric acid. Further, production of hydrogen on large scale should avoid carbon compounds as depolarizers because their use injects an increasing amount of CO₂ into the atmosphere.

Other anode depolarizers suggested by Gutmann and Murphy [4] are NO, which can be obtained from stack gases, and sea water. In the case of sea water, the expected anodic product is chlorine. The industrial production of chlorine by brine electrolysis is a large industry and involves sophisticated technologies. Adaptation of these technologies could yield efficient electrolyzers for hydrogen production. One advantage of the anode depolarization process is that instead of oxygen evolution at the anode there will be some valuable by-products that can be sold and further reduce hydrogen production costs.

2. Pulsed DC Power

Using a mechanically interrupted DC power supply, Bockris et. al. [14,15] reported two phenomena in 1952. Immediately upon application of voltage to an electrochemical system, a high but short-lived current spike is observed. When the applied voltage is disconnected, significant current continues to flow for a short time. They explained the first phenomenon as a double-layer capacitance-charging transient, followed by the electrochemical discharge of the first ionic layer, giving rise to the current, then replenished by the ionic mass transport from the bulk of the electrolyte. The second phenomenon is due to ions in the double-layer facing the electrode being discharged in the absence of the externally applied field.

In 1984, Ghoroghchian and Bockris [23] designed a homopolar generator to drive an electrolyzer on pulsed DC voltage. They concluded that the rate of hydrogen production would be nearly twice as much as the rate for DC. Their conclusion was in agreement with the earlier works of Tseung and Vassie [24] and Jasem and Tseung [25]. In these earlier works [24,25] they attributed the increase in hydrogen and oxygen evolutions to an improvement in electrolyzer mass transfer. Ibl [26] also has shown that the application of short high-voltage pulses yields the highest possible electrolysis current. He concluded that pulsing affects the surface state of the electrodes. During conventional electrolysis, film of the gas bubbles forms on the electrode, raising its resistance overpotential. Pulsed voltage will eliminate the resistance overpotential of the gas bubbles. Viswanathan et. al. [29] showed that the thickness of the pulsating double-layer (they termed it as diffusion layer) is a function of the characteristics of pulsed DC. Further, pulsing action on electrochemical systems could give rise to the ionic vibration potentials. A more drastic effect is to be expected if pulsed power is applied at frequencies resonating with the dominant ionic discharge components. Thus, one of the methods for enhancing the ionic exchange is the pulsed electrolysis.

The use of pulsed DC for electrochemical reactions, especially in electroplating, is not new. In 1955 Robotron Corporation obtained a patent for "High Voltage Electroplating" using pulsed power [28]. In 1966 Popkov [29] further substantiated the advantage of using pulsed current. Avila and Brown [30] reviewed and confirmed the advantages of pulse plating on the quality of gold plating for integrated circuitry use, while Bockris and Kita [31] obtained a reduction in energy requirement by a factor of two. Pulsed electrolysis was also used in battery charging by Wagner and Williams [32] and Bedrossian and Cheh [33]. In pulsed DC related work, Savage and Thorntron [34] established that pulsed DC has advantages over continuous DC as reaction promoter in gas phase synthesis. They attributed the enhancement to the higher mean electron energies.

SECTION III

EXPERIMENTAL WORK

A. EXPERIMENT SETUP

To quantify the effects of pulsed energy and anode depolarization on the performance of the water electrolysis process, an experimental effort was initiated. The effort involved developing a laboratory experiment. The laboratory effort consisted of a series of tests using the Fm01-LC electrolytic cell, manufactured by ICI Chemicals & Polymers, and rated at 38 gram of H₂/KAmp.Hour.

The laboratory setup is shown in Figures 2, 3 and 4. It consists of an electrolyzer setup, electrolyte make-up water system, pH control, nonpulsed DC and pulsed DC power supply sources. The electrolyzer setup includes an electrolytic cell (Figure 3) model Fm01-LC, rated at 38 gram of H2/KAmp.Hour, and manufactured by ICI Chemicals & Polymers Company. The anolyte and catholyte compartments are separated by a Du Pont 324-Naflon[®] membrane. The anolyte and the catholyte are pumped through the corresponding compartment so that the anolyte and catholyte are separate except for ionic exchange through the membrane. The electrolyzer has a stainless steel cathode and a platinum-coated titanium anode which were placed 3 millimeters apart. Each electrode has a projected area of 64 square centimeters. Throughout the experiment a 10 percent by weight sulfuric acid solution was used as the electrolyte.



Figure 2 : Water Electrolysis Experiment Setup



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Figure 3 : Electrolyzer Exploded View



Figure 4 : Experiment Electrical and Instrument Diagram

The key electronic equipment (Figure 4) used in this experiment included the following: Industrial Equipment Co. power amplifier POWERTRAN model 2000 SHF-1-XA, (The POWERTRAN was modified to remove the output transformer to allow it to operate from DC to 70 kHz). The POWERTRAN 2000 SHF-1-XA is capable of 0 to \pm 40 volts, 0 to \pm 120 Amps with a maximum continuous power output of 2000 watts AND AN AMPLIFICATION FACTOR OF 25; a B&K Precision model 3011B function generator capable of generating square, triangle, and sine waves at frequencies up to 2 MHz with duty cycles ranges from 1 to 99 percent, with output amplitude up to 5 volts; a Rapid Power Technologies Inc., DC power supply, model TRSAA100012, with output 0 to +12 vDC, 0 to 100 Amps and continuous power available of 1000 watts. The electrolyzer was connected to the power supply by two one-foot long #4 AWG bare copper wires.

The pressure, temperature, and flow (in ccm) of the generated hydrogen and oxygen were measured using Ashcroft pressure sensors, a J-type thermocouple, and a Teledyne Hastings-Raydist flowmeters, model HFM-200, of 0 to 500 sccm range. The electric current was measured using a F.W.Bell hall-effect current sensor, model IHA-100, capable of measuring DC and pulsed current up to 50 kHz. Both current and voltage were displayed using a TEKTRONIX 2232 100 MHz oscilloscope then plotted using a TEKTRONIX HC-100 plotter. The plots were digitized using Summa Sketch II. Professional digitizer. The current was measured in volts, 50 millivolts being equal to 1 amp. Voltage measurements were taken at the cell and at power supply output. This allowed the measurement of line losses.

B. LABORATORY TEST SERIES

Four sets of tests were planned. The four test series consisted of: (1) A nonpulsed DC power test set to determine the cell's baseline performance; (2) A pulsed DC power test set to determine the cell performance as a function of the pulsed energy parameters; (3) Anode depolarization under nonpulsed DC power test set to determine the cell baseline performance efficiency using sulfur dioxide as anode depolarizer; and (4) Anode depolarization under pulsed DC power test set. Due to cuts in 6.1 findings, only the first three were partially accomplished. The work accomplished is given in the following paragraphs.

1. Baseline Test, Nonpulsed DC Power.

This test series established the performance baseline for the laboratory setup. First, the deactivation of the cell was studied by recording the change in current at fixed voltage as a function of time. As shown in Figure 5, the cell reached steady-state conditions 5 minutes after potential was applied on the cell. Using this cell property throughout the experiment, data was collected at least 10 minutes after each test started. The cell's hydrogen yield as a function of cell potential and current was measured (Figures 6 and 7) to determine the cell's baseline performance. The cell's baseline performance was used for comparison with cell performance under pulsed DC and anode depolarization.

2. Pulsed DC Power.

For comparison purposes, the hydrogen yield was kept at 100 cubic centimeter per minute (ccm) for all pulsed DC runs. This selection was based on the baseline nonpulsed DC current density results. At 100 ccm of hydrogen (Figure 7), the measured current density was

around 320 mA/cm² which is in the current densities range of 100-500 mA/cm² for economical hydrogen production. The test runs were carried out using square pulse for seven frequencies and four duty cycles. The duty cycle is the ratio of the pulse on-time to the pulse period. The seven frequencies are 10 Hz, 500 Hz, 1 kHz, 5 kHz, 10 kHz, 25 kHz, and 40 kHz. The duty cycles are 10 percent, 25 percent, 50 percent, and 80 percent. The test was divided into four test runs, one for each duty cycle. Each test run started by measuring the nonpulsed DC current and voltage for a 100 ccm of hydrogen yield. Then, a duty cycle was selected and the test run pulse frequency was changed. The cell potential was then changed to maintain the 100 ccm hydrogen yield. Data collection started after a period of fifteen minutes to allow for steady state condition.

The applied potential was measured at the power amplifier output terminals and at the cell electrodes. The voltage drop across the one-foot long #4 AWG bare copper wire was also recorded for some cases. The rate of electrical energy consumption (power) can be calculated using the relationship:

$$P = \frac{1}{T} \int_{0}^{T} i(t) \, \theta(t) \, dt \tag{15}$$

where T is the pulse period, i(t) is the current wave form, and e(t) is the voltage wave form.



Figure 5: Current Decay Characteristics of The ICI Electrolyzer with 10 Percent by Weight Sulfuric Acid Operating at 2.8 volts.



Figure 6: Performance Characteristics of the ICI Electrolyzer Using 10 Percent by Weight Sulfuric Acid





3. Baseline Anode Depolarization

In this test series, sulfur dioxide was used to depolarize the cell anode. Used in its gaseous state, it was bubbled through the anolyte prior to and during the cell's nonpulsed DC operation. The test started by setting the DC power supply output to zero. Then, the potential was incremented by 0.05 of a volt until a 5 ccm of hydrogen yield was recorded. The applied potential was then incremented by 0.2 of a volt thereafter. For each voltage increment, the cell potential, current, and hydrogen flow were measured after steady state was reached.

SECTION IV

RESULTS AND DISCUSSION

A. PULSED DC POWER

During the preliminary test runs, conducted to examine the experiment setup, the current reversed polarity during the off-period of the pulse (Figure 8). The polarity reversal is attributed to a reversible reaction in the electrolyzer cell during the off-period. The effect of the current polarity reversal was seen in the catholyte when its color changed to a light blue. To examine and quantify the various metals in the catholyte, the atomic absorption spectrometry was used. The observations were made with a Perkin-Elmer 6500 flame atomic absorption spectrometer, using a laminar flame burner and equipped with hollow-cathode emission lamps for the different metals sought. Metals sought were based on the stainless steel alloy content of the cathode. The catholyte was found to give no absorbance signal for Molybdenum and Titanium, and only a weak absorbance for copper. Low absorbencies were obtained for Chromium and Zinc, but a large signal was given for Nickel and Iron. These analyses showed that the cathode had lost some of its content to the catholyte. This was confirmed by weighing the cathode which showed 2 grams loss. To separate the power amplifier from the cell during the off-time, a Motorola schottky diode, model MBR8045, was installed. The diode's maximum ratings are 45 volts and 80 Amps. Use of the diode stopped the current polarity reversal, but allowed the cell to maintain about a 2.3 volts instead of zero volt during the off-period.



Figure 8 : Applied Current Polarity Reversal.

The digitized waveforms of the current, power amplifier output voltage (source V), and the cell voltage (cell V) are given in Figures 9-31. The digitized data is given in Appendix A. These figures represent the experiment setup responses in generating the 100 ccm of hydrogen and cover the test matrix. A careful examination of these figures reveals the current is lagging behind the voltage, an indication of an inductive circuit. However, the delay in the current is also due to the cell voltage. With the diode installed, the cell has maintained a DC level of about 2.3 volts. Until the power supply voltage overcame the cell potential and the losses in the circuit, no current flowed. As shown in Figure 24 (50 percent duty cycle and 25 kHz), the applied potential is higher than the electrolyzer's potential by about 25 to 40 percent, and the voltage rise and fall times are less than 4 micro-seconds with a high current rate of change which is attributed to the low impedance of the circuit. The high voltage drop is due to the large reactive losses mainly produced by the inductive reactance caused by the high current rate of change. This can be seen by examining the voltage drop of the negative lead connecting the cell to the power amplifier and the current waveforms (Figure 24). The relation between the lead voltage drop and the current is given as:

$$v_i = -L \frac{di}{dt} \tag{16}$$

where L is the wire inductance. For a one-foot long #4 AWG copper wire, the inductance is in the range of micro farads; however, the time rate of change of the current is about 2 million amps per second causing, the high voltage drop.

Figures 9-31 also reveal the interesting shape of the source voltage waveform. Although the function generator produced a clean voltage square wave, the resulting source voltage waveform was far from being a clean one. For example, in Figure 24 the source voltage waveform has a step and a ringing at its trailing side instead of turning off at the 20th microsecond from pulse initiation. The shape of the source voltage waveform during the off-time period of the pulse is the result of the induced voltage in the #4 AWG wires and the cell maintained voltage of 2.3 volts. The induced voltage in the #4 AWG wires connecting the cell to the power amplifier is induced by the discharge of current generated by the collapse of magnetic flux around these wires.

Using Equation (15), the electrical power delivered to the setup circuit and electrolyzer were calculated. For the setup circuit, the source voltage and current waveforms were used, while for the electrolyzer the cell potential and current were used to calculate the power consumption. The results are summarized in Figure 32 for the setup circuit and in Figure 33 for the electrolyzer. From Figures 32, 33 and 34 the nonpulsed DC (100 percent duty cycle) requires the least electrical power. The effects of pulse frequency and duty cycle on the electrical power needed are noticeable. The demand for electrical power increases with the decrease of duty cycle and pulse frequency. At 10 percent duty cycle the electrolyzer power demand for 10 Hz is slightly more than twice that of nonpulsed DC, while for 25 kHz it is only 27 percent higher. It is clear that during this effort one of the two phenomena reported by Bockris et al [14,15] was not seen, namely, the high but short-lived current spike. Furthermore, the conclusion that nonpulsed DC requires the least electrical power conflicts with those of Ghoroghchian and Bockris [23] and Tseung and Vassie [24]. The difference between these results should be investigated in details so that the use of pulsed DC issue can be settled.



Figure 9: Experiment Setup Response For 10 Percent Duty Cycle and 10 Hz Pulse at 100 ccm Hydrogen Yield.



Figure 10: Experiment Setup Response For 10 Percent Duty Cycle and 500 Hz Pulse at 100 ccm Hydrogen Yield.



Figure 11: Experiment Setup Response For 10 Percent Duty Cycle and 1 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 12: Experiment Setup Response For 10 Percent Duty Cycle and 5 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 13: Experiment Setup Response For 10 Percent Duty Cycle and 10 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 14: Experiment Setup Response For 10 Percent Duty Cycle and 25 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 15: Experiment Setup Response For 25 Percent Duty Cycle and 500 Hz Pulse at 100 ccm Hydrogen Yield.



Figure 16: Experiment Setup Response For 25 Percent Duty Cycle and 1 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 17: Experiment Setup Response For 25 Percent Duty Cycle and 5 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 18 : Experiment Setup Response For 25 Percent Duty Cycle and 10 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 19: Experiment Setup Response For 25 Percent Duty Cycle and 25 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 20 : Experiment Setup Response For 50 Percent Duty Cycle and 500 Hz Pulse at 100 ccm Hydrogen Yield.



Figure 21: Experiment Setup Response For 50 Percent Duty Cycle and 1 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 22: Experiment Setup Response For 50 Percent Duty Cycle and 5 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 23 : Experiment Setup Response For 50 Percent Duty Cycle and 10 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 24 : Experiment Setup Response For 50 Percent Duty Cycle and 25 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 25: Experiment Setup Response For 50 Percent Duty Cycle and 40 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 26: Experiment Setup Response For 80 Percent Duty Cycle and 10 Hz Pulse at 100 ccm Hydrogen Yield.



Figure 27: Experiment Setup Response For 80 Percent Duty Cycle and 500 Hz Pulse at 100 ccm Hydrogen Yield.



Figure 28: Experiment Setup Response For 80 Percent Duty Cycle and 1 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 29: Experiment Setup Response For 80 Percent Duty Cycle and 5 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 30 : Experiment Setup Response For 80 Percent Duty Cycle and 10 kHz Pulse at 100 ccm Hydrogen Yield.


Figure 31 : Experiment Setup Response For 80 Percent Duty Cycle and 25 kHz Pulse at 100 ccm Hydrogen Yield.



Figure 32 : Experiment Setup Circuit Power Demands.



Figure 33 : Electrolyzer Power Demands (power vs. duty cycle)



Figure 34 : Electrolyzer Power Demands (power vs. frequency)

B. BASELINE ANODE DEPOLARIZATION

The results of anode depolarization and the baseline nonpulsed DC test series are given in Figures 35 and 36 for comparison. Using anode depolarization with 10 percent by weight sulfuric acid at 30 °C with the anolyte fully saturated with SO₂, a current of 100 mAmps was recorded at cell potential of 0.635 volts instead of the 1.8 volts required for nondepolarized operation. The cell potential fell 1.3 volts below that of the nondepolarized cell potential at a current density of 30 mA/cm². At this current density, as seen in Figure 36, the depolarized-cell's hydrogen yield was three times that of the nondepolarized cell for the same 1.71 watts of electrical power delivered.

During test runs the catholyte gradually changed to an opaque bluish color. The test run was terminated when the current dropped suddenly. Examining the catholyte, revealed a rotten egg odor confirming the generation of hydrogen sulfide which dissolved in the catholyte, changing its color. The electrolyzer was dismantled, and sulfur powder was found on the cathode side of the membrane. This explained the sudden drop in current. The sulfur powder had covered all the membrane area preventing the ion exchange from taking place. The generation of hydrogen sulfide and the sulfur covering of the membrane had affected the slope of the anode depolarization curve given in Figure 36. At the beginning of the first change of slope, hydrogen yield had tripled when sulfur dioxide was used as a depolarizer. Overcoming these obstacles is technically feasible which makes anode depolarization a viable avenue to decrease hydrogen production costs.



Figure 35 : Performance Characteristics of the ICI Electrolyzer With SO₂ Saturated Anolyte.



Figure 36 : Anode Depolarized Hydrogen Generation Rate vs. Power Demand.

SECTION VI

CONCLUSIONS AND RECOMMENDATIONS

A. CONCLUSIONS

This effort experimentally studied the effects of pulsed DC and anode depolarization on the performance of the water electrolysis process for hydrogen generation. The selection of the these two concepts was based on works published in the fifties, sixties, and seventies. Juda and Moulton [8] found that using 6 percent by weight sulfurous acid (sulfur dioxide dissolved in water) to depolarize the cell anode reduces the cell potential by 0.8 volts below that of nondepolarized cell potential. Bockris et al [14, 15, and 22] and Tseung and Vassie [23] concluded that pulsed DC may be used to improve the electrolysis process for hydrogen generation for up to twice the performance of the nonpulsed DC electrolysis.

The work accomplished during this effort showed the potential of the anode depolarization method in reducing the cost of electrolysis for hydrogen production. A three-to-one improvement in electrolysis performance is feasible.

In the case of pulsed DC, one of the phenomena recorded by Bockris in 1953 was not duplicated by this effort, namely the high but short-lived current spike. The second phenomenon, significant current continue to flow for a short time, was observed. Bockris explained the cause of this phenomenon as the discharge of the ions in the double-layer facing the electrode in the absence of the externally applied electric field. However, the current flow during the off-period of the pulse is largely due to the discharge of the current generated by the collapse of the magnetic flux around the leads connecting the cell to the power amplifier. Since the results of this effort contradict those of Backris et al [14, 15 and 22] and Tseung and Vassie [23] more effort is needed to settle the pulsed DC issue.

B. **RECOMMENDATIONS**

Due to the lack in 6.1 funds this effort was terminated before its conclusion. To achieve the objectives, a basic research program, which consists of an aggressive experimental and theoretical investigation of the water electrolysis behavior under pulsed DC and anode depolarization loadings, is proposed. A new cell design is also proposed. The new design is based on a dispersion of ultramicroelectrodes to maximize surface area per unit volume under high mass transport conditions. The overall philosophy is to explicitly account for the characteristics of the double-layer and the nature of the oxidation process in describing the electrolytic process behavior under varied loading conditions. Observations of charging, discharging, and the thickness of the double-layer and electrode oxidation process are proposed, backed up by theoretical modeling. The following describes the proposed research.

C. PROPOSED RESEARCH OBJECTIVES

The long-term objective of this research is the development of an efficient electrolytic cell using pulsed DC power and anode depolarization concepts. Because few, if any, researchers have ever studied the electrolyzer behavior using the dispersive ultramicroelectrodes under pulsed

DC combined with anode depolarization, considerable experimental effort is required before definitive answers can be found. Therefore, specific objectives of the proposed effort :

- 1. Develop quantitative descriptions of the double-layer behavior under pulsed DC.
- 2. Study the anodic oxidation process under both nonpulsed and pulsed DC.

D. WORK BREAKDOWN STRUCTURE

A combined experimental-theoretical investigation is planned. Emphasis is on developing the experimental capabilities and techniques required for studying double-layer behavior and anodic oxidation kinetics. Parallel development of theoretical descriptions of this behavior will be used to guide the experiments toward meaningful results. Three major task areas, consisting of (1) laboratory experiments, (2) theoretical modeling, and (3) data analysis, are described in the following paragraphs.

Task 1. Laboratory Experiment

The success of this effort depends on the understanding of the double-layer behavior and the oxidation process at the anode as well as the direct measurement of changes in these processes under various test conditions. All experimental work for this project falls under Task 1. A combination of linear sweep cyclic voltammetry, atomic absorption spectrometry, gas/liquid chromatography, and computerized histogrammetry is proposed. The cathodic and anodic products will be analyzed for selected cases using a gas chromatograph. These analyses will determine the hydrogen weight percentages in the cathodic product and the anodic product makeup. Consideration will be given to the measurement of overpotentials, hydrogen generation rate, cell potential and current, and double-layer charge and discharge processes. The oxidation process of the sulfur dioxide at the anode has been examined [35]; therefore, only the oxidation process of chlorides will be studied in the proposed effort. In addition to the subtasks detailed below, possible additions, improvements, and enhancements to the proposed experimental methods will be considered throughout the effort when appropriate.

Subtask 1a. Baseline Characterization.

Under this subtask the baseline performance of an electrolytic cell will be characterized for depolarized and nondepolarized operations. The baseline performances will be used to compare with the cell performance under pulsed DC operations. Existing laboratory facilities at AFCESA/RACO will be used for testing under this subtask, which include the following:

► Electrolyzer Cell Development. A successful hydrogen production process requires low power consumption, kWh/kg product. This can be achieved with a cell design that has a large surface area per unit volume and operates under a high mass transport condition. Both of these objectives will be achieved by using Dispersion of Ultramicroelectrodes. These three-dimensional electrodes and some of their applications have been reported by Ghoroghchian et al [37-40]. We will utilize dispersion of ultramicroelectrodes in the form of a monopolar fluidized bed, packed bed, and/or slurry systems. The development of spherical diffusion fields in the bulk of the solution surrounding these electrodes lead to high rates of mass transfer to the electrode surface. Equally the spherical potential fields leads to a decrease of charging times, so that transient measurements are simplified (the time constants are proportional to the radius of the electrodes). This system will be used for all the depolarization processes discussed above. The use of ultramicroelectrodes is a powerful new methodology for hydrogen production. The number of particles that can be put into the suspension may be as large as 10^9 Ultramicroelectrodes per cubic centimeter of solution. This will increase the contact time with the depolarizer materials such as SO_2 or biomass, which in turn translate to large hydrogen generation. The space time yield (amount of product produced per time of electrolysis and per cell volume) is expected to be 1-2 order of magnitude greater than 2-D systems.

Different electrode material, metallic powders, such as pt, Ru, Pb, PbO, metal supported materials as well as carbon, graphite and semiconductors will be used and their performance from a catalytic point of view will be studied. The preparation of ultramicroelectrode dispersion will be undertaken by various methods, depending on the conducting substrates and their physical form. Metal powders, carbon, and some supported metal powders are available from a variety of commercial sources. Other materials will be prepared in-house by grinding and crushing techniques followed by appropriate sieving and cleaning methods. Reactions will be studied as function of microelectrode size and concentration (due to difference in mass transfer rates as size is changed and thus possibility of changing reaction pathway, also microelectrode concentration will affect reaction pathways by changing the intermediate concentration of chemical product(s)).

► Anode Depolarization. A few important anode depolarizer materials will be considered and characterized under the nonpulsed DC and pulsed DC conditions as outlined below.

(a) The anodic process of solid metal oxides formed at potentials lower than those required for oxygen evolution are of particular interest. Once formed, the oxide is then removed from the electrolytic cell, and the anode substrate is subsequently regenerated by chemical reduction or by thermal dissociation. The anodic reaction involves either a metal/metal oxide couple of a lower/higher oxide couple. The thermal reduction phase is thus described as:

$$MO_s \rightarrow MO_{s-x} + \frac{x}{2}O_2$$
 (17)

Among the oxides that will be studied are oxides of lead, tin, and cobalt. Chemical reduction of the oxides at medium temperature (e.g. by carbon monoxide) will also be considered. Following established favorable equilibrium behavior, the kinetics of the anodic process are of great importance. After a favorable kinetic behavior is demonstrated, the investigation will turn to other features relevant to the chosen process. These include oxide coherence (minimize degradation of substrate weight ratio), oxide layer conductivity, and thermal reduction parameters.

(b) Sulfur dioxide as an anode depolarizer will also be considered. Although this has been well documented, the process will be examined from the point of view of a new cell design (dispersion of ultramicroelectrodes) and the use of pulsed DC power as discussed below.

(c) Study of the anodic products in biomass slurry electrolysis. The

principle variable would be current density, electrocatalysis via dispersion of ultramicroelectrodes, pulsed DC parameters. Ascertaining the nature of the products would be the primary aim, while the secondary aim would be determining the current efficiency of their production. During this study, hydrogen product data would be collected because of the interaction the anodic products have upon hydrogen economics. The study of the anodic products in slurry electrolysis by using non aqueous solutions will be conducted. DMSO, dimethylformamide, acetonitrile, and their systems with water will be used. Other organic systems will also be sought.

Nonpulsed DC Power. Initial testing will be made using nonpulsed DC power to determine the electrolyzer baseline performance. The baseline performance is to be used for comparison with the anode depolarization and pulsed DC performances. The effects of electrolyte concentration and temperature will be examined. In this testing, linear sweep cyclic voltammetry will be performed to measure current-voltage curves. These curves will allow us to study the qualitative and quantitative changes in the electrolyzer behavior. Hydrogen yield will also be measured to facilitate comparison of the actual hydrogen generation rate. Measurements of double-layer charge time will be recorded using an oscilloscope in a storage mode.

Subtask 1b. Pulsed DC Power

Using the same conditions tested in subtask 1a, pulsed DC power will be examined for both anodically depolarized and nondepolarized cells. To help reduce the size of the test matrix, the cell performance under pulsed DC power will be examined at two hydrogen yields which will be determined from the baseline data for low and medium ranges. Under this subtask, combinations of duty cycles, frequencies, and waveforms will be examined. Consideration will be given to the effects of the waveform's rise-time and the combination of pulsed and nonpulsed DC formations.

Task 2. Theoretical Modeling

Theoretically-based relationships for hydrogen evolution rate, limiting current density, overpotentials, pulsed DC power, and double-layer charging will be pursued. Applicable theories which will be considered include: mass transfer, activation energy, and Butler-Volmer theory. These are grouped into two main thrust areas for theoretical development.

Reacting Ion Mass Transfer. One of the important advantages of pulsed electrolysis frequently cited by investigators is the enhancement of mass transfer. Since mass transfer limitation can be reduced very effectively by pulsed DC electrolysis, a mass transport model for the reacting ions can be used to obtain quantitative ion discharge information. The concentration of the reacting ions in the double-layer depends on the transport characteristics of the system as well as the applied current density and is independent of reaction kinetics. It can be calculated by solving the convective diffusion Equation subject to Fick's law of diffusion as a boundary layer. Several mass transport theoretical models under pulse conditions which can be adapted to this research needs are available in the literature. For example, Popov et al [36] studied mass transfer under pulsed conditions in both stirred and unstirred solutions for electrodeposition. The mass transport modeling results will help us better understand the behavior and the characteristics of the double-layer under pulsed DC conditions, determining the maximum rate of electrolysis, and will lead to the kinetic study of the electrode reactions.

Oxidation Kinetics. The modeling of the electrode reaction kinetics will provide a wealth of information. This information will help us to understand the anodic oxidation process. Parameters that can be calculated include the number of electrons involved in the reaction, double-layer thickness, and diffusion coefficient. For this modeling to be useful, mass transfer limitations must either be negligible or be quantitatively accounted for. The mass transfer limitations can be obtained from the mass transfer model while the rate of reaction can be represented by the Butler-Volmer Equation.

Task 3. Develop Quantitative Description

The information gathered in the Task 1 experiments and in the Task 2 modeling must be analyzed to provide quantitative descriptions of electrolyzer performance along with basic insights for the physical processes which are occurring. Task 3 of this effort will be data analysis.

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APPENDIX A

WAVEFORMS' DIGITIZED DATA

Time	Source V	Time	Current	Time	Cell V
0.0000	0.00000	0.0000	0.00000	0.0000	1.92754
0.0862	0.30387	0.2152	0.12837	0.0434	4.13913
0.1725	1.98101	0.5595	4.33552	0.3476	6.22029
0.2587	2.71147	0.9899	7.22392	0.6082	6.28116
0.3018	3.73411	1.3772	7.22392	1.5206	6.22609
0.4743	4.94960	2.3671	7.46900	2.6067	6.73333
0.7330	7.33966	4.8204	7.16557	4.5183	6.20870
1.4661	7.75457	5.5951	7.44566	5.4741	6.64058
3.2340	7.31045	6.1976	7.38731	7.4292	6.26667
4.2688	7.92988	7.6179	7.06054	8.4284	6.59710
5.9505	7.29291	8.4356	7.41065	9.1235	6.44348
6.9854	7.88897	10.3293	7.10722	9.7318	6.29275
8.9689	7.30460	10.7167	3.11597	9.8621	5.96812
9.9606	7.85975	11.2332	0.00000	10.2531	4.04058
10.2193	7.17604	114.0000	0.00000	10.4269	2.42899
10.4781	4.04383			11.0351	2.37391
10.8661	1.03433			11.5999	2.31014
10.9955	0.00000			12.9033	2.26377
14.0000	0.00000	-		14.3804	2.22899
				16.2051	2.19420
				18.4209	2.17391
				20.2890	2.15362
				22.8957	2.12464
				25.3287	2.09855
				27.8920	2.08406
				31.4110	2.06087
				34.8432	2.04928
				37.5368	2.04638
				42.5765	2.04638
				47.4858	2.03188
				51.0049	2.01449
				56.2618	1.99130
				59.9981	1.98261
				65.2116	1.97391
				70.2078	1.96522
				74.8130	1.95942
				79.9830	1.95944
				85.5440	1.94203
				114 0000	1 92754

Approximate 10 Hz, 10% Duty Cycle December 13, 1991, (time in milli-seconds)

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500 Hz, 10% Duty Cycle November 13, 1991, (time in micro-seconds)

Time	Source V	Time	Current	Time	Cell V
0.0000	0.00000	0.0000	0.00000	.0000	2.10000
1.1343	3.38528	1.0333	0.00000	. 5175	2.25519
3.2998	5.93567	2.1700	0.21761	1.1385	2.42188
7.5277	5.83846	13.1232	2.92054	2.6909	2.60293
11.5494	5.82702	26.1431	4.56979	4.5538	2.75813
22.3769	6.25590	43.7096	5.90408	6.1063	2.96505
28.9765	6.32452	54.5595	6.33357	8.3832	3.16335
59.1905	6.83345	69.0261	6.61417	10.1426	3.36739
80.3300	7.06219	85.3526	6.75161	12.8335	3.56857
107.9660	7.18227	105.5025	6.90623	15.4209	3.77836
128.8992	7.26233	141.0488	6.92341	18.3188	3.95367
155.2978	7.34239	174.5285	6.98067	21.6306	4.14909
196.5455	7.40529	196.4350	7.03794	25.4600	4.37038
199.4328	2.65332	197.8817	6.99785	30.4278	4.58880
200.7734	2.31594	198.9150	6.90623	36.2236	4.80147
203.6607	2.46462	209.0416	4.02577	40.9844	4.94804
205.5169	2.25304	221.3382	1.47173	45.9522	5.10898
206.8574	2.29878	231.1547	0.06299	52.9899	5.28716
210.9822	2.29307	296.6675	0.05727	59.9241	5.45672
231.3998	1.64689	320.0000	0.00000	67.9968	5.58030
232.9466	0.71480	2000.0000	0.00000	74.6205	5.67513
266.2542	0.24589			81.3477	5.77860
301.0054	0.12009			88.7994	5.83320

339.1596	0.00000
2000.0000	0.00000

93.7673	5.89355
100.7015	5.96252
107.5322	5.99989
113.7420	6.04299
118.9167	6.07461
123.7811	6.09185
130.3013	6.12059
137.1320	6.15220
152.8634	6.18381
161.4535	6.22692
173.0451	6.22692
180.8073	6.25854
188.6730	6.26428
194.2617	6.26716
197.0561	5.86481
199.0225	5.51994
200.4715	5.26704
201.9204	4.97103
204.19/3	4.63490
200.0812	1.31134
211.8580	3 41012
219 5147	3 10587
222.8266	2.85584
226.2419	2.63742
226.2419	2.63167
228.9328	2.43912
234.9356	2.43625
251.2879	2.41901
260.9131	2.39314
276.4374	2.37877
295.6877	2.37302
325.0805	2.35291
449.6895	2.29543
2000.0000	2.10000

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1 kHz, 10% Duty Cycle November 13, 1991, (time in micro-seconds)

Time	Source V	Time	Current	Time	Cell V
0.0000	0.00000	0.0000	0.00000	0.0000	2.19274
1.3385	0.04644	2.9897	0.0000	0.4132	2.19274
2.0592	0.22061	4.5361	0.12192	2.7893	2.19274
2.6770	2.41509	5.3608	0.48766	4.8554	2.20718
3.5006	4.83019	6.7010	0.96952	5.8884	2.27363
5.4569	6.56604	9.0722	1.50363	6.7149	2.47586
10.5019	6.60668	10.4124	1.95646	7.9545	2.68097
12.7671	6.50798	12.5773	2.42671	9.6074	2.89476
19.4595	6.75181	15.1546	3.01306	11.1570	3.10565
24.2986	7.03628	18.2474	3.54136	13.7397	3.31077
29.6525	7.05370	22.6804	4.27866	15.7025	3.52167
47.3616	7.40203	28.2474	4.95210	18.1818	3.79323
66.9241	7.70972	32.1649	5.49202	20.1446	3.98102
85.0450	7.87808	36.59/9	5.86938	22.3140	4.22369
97.9151	7.88970	40.7216	6.20610	25.5165	4.40858
99.0476	5.35268	40.4948	6.54282	28.5124	4.33881
100.3861	2.94920	54.123/	0./0343	31.0110	4./2920
102.1364	2.18868	61.23/1	0.89115	35.0207	4.925/1
103.8430	1.85196	0/.9381 22 1050	0.90002	38./39/	3.0/883
107.7992	1.99129	73.1959	7.04/90	42.8/19	5.2/81/
110.10/3	1 77069	/9.38/6	7.11176	4/.3333 50 0707	5.40040
117 5904	1 69360	00.1030	7 19723	57 3347	5.02405
122 0610	1 60913	JI.23/1	7 10723	61 7760	5 96752
129.0000	1 49621	100 0000	7 16401	65 5992	5 97730
132 7156	1 30332	102 7835	6 96081	69 9050	6 05241
137 3488	0 59797	104 3299	6 49057	71 6942	6 10442
143.1145	0.51669	106.5979	5.96807	75.1033	6.16508
152.7928	0.41800	108.3505	5.32946	77.6860	6.21131
162.4710	0.31350	110.4124	4.71408	81.9215	6.27198
188.5199	0.24383	112.3711	4.05225	85.9504	6.32109
213.0245	0.19158	114.6392	3.46009	90.2893	6.37309
245.3539	0.14514	117.0103	2.92017	94.4215	6.42798
273.6680	0.10450	119.3814	2.31060	97.5207	6.44820
317.0142	0.00000	124.1237	1.46880	98.5537	6.48287
1000.0000	0.00000	127.9381	0.91147	100.9297	6.46843
		131.6495	0.34253	101.9628	6.35865
		133.6082	0.01161	103.6157	6.10731
		137.4227	0.00000	104.9587	5.76641
		141.9588	0.00000	105.5785	5.67107
		1000.0000	0.00000	106.3017	5.48906
				107.6446	5.29261
				108.7810	5.09327
				110.2273	4.87082

110.8471	4.65415
112.1901	4.45770
113.6364	4.23236
115.7025	4.00702
117.9752	3.77590
120.6612	3.51589
122.5207	3.31366
123.9669	3.14321
127.1694	2.90054
130.0620	2.68386
132.5413	2.53941
134.2975	2.45852
139.9793	2.43830
150.6198	2.42674
163.5331	2.41808
183.9876	2.38919
201.1364	2.36030
224.2769	2.35741
239.9793	2.34585
250.3099	2.34585
254.0289	2.34007
283.2645	2.31118
305.8884	2.31407
330.5785	2.29963
358.2645	2.29385
386.9835	2.27363
1000.0000	2.19274

5 kHz, 10% Duty Cycle November 13, 1991 (time in micro-seconds)

vember 13	, 1991 (ti	ne in micro	-seconds /		
Time	Source V	Time	Current	Time	Cell V
0 0000	0 00000	00000	0.00000	0.0000	2.30000
0.0000	0.00000	2.7207	0.00000	1.3652	2.57930
0.3330	0 14569	3.0505	0.06997	2.7718	2.92770
1 2160	2 05128	5.4002	1.10204	4.2611	3.23292
1.3109	4 71445	8.9866	2.76968	5.5436	3.44599
2.1333	7 26690	14.2219	4.53644	7.1570	3.78576
2.9210	7 99534	19.0450	5.87172	8.8531	4.07082
J. JOUZ	8 64802	21.0237	6.37318	10.7975	4.35300
6 3374	8 65385	23.0024	6.37901	12.3282	4.55743
6.3374	9 59557	25.1872	5,72012	13.7761	4.75899
9 9477	8 61888	28.9797	4.27405	15.5550	5.00374
10 7919	8 57226	33,1020	2.94461	17.2098	5.19953
12 0165	8 57226	37.8839	1.76093	18.9474	5.35790
14 0393	8 76457	43.0780	0.74052	19.8161	5.46732
16 6667	8 84033	46.4170	0.27405	21.5537	5.18226
10 0000	8 99767	49.8385	0.00000	23.4153	4.81370
20 8230	9.03846	200.0000	0.00000	24.4909	4.61790
20.8230	7 93124			26.4767	4.32420
21.1111	5 57692			27.9660	4.07370
22.7030	2 96620			30.2827	3.77136
22.8333	1.58508			32.5580	3.50934
24.0741	1 46270			34.9989	3.24156
24.5210	1.40443			37.9361	3.00545
25 2675	1 38695			40.8734	2.75206
25.2075	1.52098			43.8934	2.52747
26 9724	1 46270			46.3342	2.41230
28 0658	1 34033			53.7807	2.37774
20 6296	1 30536			64.1646	2.37774
30 7919	1 42774			81.4158	2.36911
32 1399	1 44522			111.2020	2.34895
33 1276	1 32284			142.9740	2.32016
37 4496	1.32867			167.5063	2.33167
39 9066	1.16550			180.0000	2.30576
40 7819	1.16550			200.0000	2.30000
43 7449	1.13054				
47 2016	1.10140				
47 9835	0.94406				
48 8066	0.29720				
49.2181	0.25641				
50.1235	0.36713				
51,9342	0.27389				
52.9218	0.30303				
54.1152	0.25641				
62.5926	0.19814				
79.2181	0.13403				
90.0134	0.00000				
200.0000	0.0000				

10 kHz, 10% Duty Cycle November 13, 1991 (time in micro-seconds)

Time	Source V	Time	Current	Time	Cell V
0 0000	0.0000	0.0000	0.0000	0.0000	2.30218
0.2684	0.02900	1.4859	0.00000	0.8073	2.30218
0.3304	0.13340	1.8367	0.08687	1.6352	2.30791
0.5575	1.33398	2.4140	1,15251	2.5597	2.35092
1.7550	6.37989	5.4896	2.05019	3.1877	2.47706
2.4157	8.57806	8.1312	3.50965	3.6224	2.59461
2.9319	9.45964	10.2775	4.95753	4.2019	2.74656
4.0262	10.43403	11.5983	5.01544	4.3882	2.83830
5.3889	10.43403	11.9491	4.96911	4.7401	2.92144
5.6573	10.38183	12.2380	4.95174	5.5267	3.19094
9.9931	10.35283	13.0016	4.94595	5.6923	3.18234
10.1376	10.32383	14.6732	4.30888	5.9200	3.32569
10.2822	10.23103	15.0860	4.29730	6.6237	3.47477
11.4178	5.60851	20.3485	2.49614	6.9756	3.56651
11.9546	3.68874	22.9489	1.88224	7.1826	3.65826
12.2849	3.04495	25.1983	1.14672	7.9071	3.75860
13.2347	1.32818	26.4572	1.14093	8.5281	3.90195
13.3999	1.25278	26.8700	0.99614	8.8178	3.98509
14.2051	1.05558	28.9956	0.63127	9.7079	4.20298
15.7330	1.37458	29.7386	0.58494	10.2461	4.30906
17.2815	1.36878	30.2958	0.34749	10.5566	4.35780
19.7385	1.24090	32.0500	0.18533	11.4259	4.54989
20.3166	1.33398	33.0612	0.04633	11.9227	4.66743
22.2161	1.32238	86.3265	0.00000	12.0676	4.71904
23.3310	1.18318	100.0000	0.00000	13.5373	4.65023
24.1982	1.17738			13.7443	4.65023
24.9209	1.53697			14.4066	4.51835
27.9972	1.37458			14.6757	4.44667
29.0502	1.23538			15.0690	4.35206
29.6490	1.09038			16.1247	4.17431
32.7254	1.14258			16.6421	4.10837
32.9319	0.40599			17.4908	4.01376
33.1590	0.82939			18.5051	3.86181
33.5719	0.67859			19.4365	3.75573
33.9642	0.07540			19.8919 20 8441	3.69553
34.3152	0.31319			21.4029	3.51491
34.7075	0.37699			21.9204	3.43463
34.9346	0.22620			22.8312	3.28268
35.2650	0.21460			23.3487	3.21674
35.5127	0.26680			23.7213	3.18234
36.8135	0.22620			25.2323	3.04186
38.0936	0.26680			25.7705	2.98452
40.5506	0.25520			27.3229	2.81823
45.7123	0.16240			27.9025	2.77523
46.0427	0.02320			28.7305	2.67775
46.6621	0.13340			30.5313	2.55161
47.5912	0.06960			31.1109	2.49713
48.2312	0.00000			32.0009	2.44839
48.9332	0.02320			33.5534	2.36239
88.5960	0.00000			33.9673	2.35092
100.0000	0.00000			34.1950	2.38245
				35.4163	2.39679
				36.1201	2.36812
				38.2107 42.0814	2.38243
				46.9250	2.36525
				51.1270	2.36239
				59.3031	2.32225
				63.5879	2.32511
				67.8726 73.0681	2.32511
				76.2351	2.32225

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79.4641	2.33085
82.8174	2.33085
86.3983	2.29644
90.0621	2.32511
91.8629	2.30505
93.7466	2.30505
100.0000	2.30218

25 kHz, 10% Duty Cycle November 13, 1991 (time in micro-seconds)

Time	Source V	Time	Current	Time	Cell V
0 0000	0.0000	0.0000	0.00000	0.0000	2.33218
0.0718	0.04636	1.0103	0.00000	0.0829	2.33218
0.1744	0.12169	1.2577	0.00572	1.0158	2.32928
0.2462	0.28974	1.3505	0.04292	1.4097	2.33218
0.5848	2.23993	1.8247	0.10300	1.6792	2.32928
1.3234	6.58278	1.9794	0.10300	1.8658	2.35822
1.7543	8.85430	2.1856	0.18312	2.1353	2.58681
2.3904	11.46772	2.6082	0.40916	2.6432	2.72280
2.8520	13.21192	2.8247	0.55222	2.9852	2.90509
3.6112	13.72185	2.9897	0.69814	3.3895	3.22627
4.0010	13.87831	3.2474	0.8/208	4.1047	3.41435
4.1139	13.87252	3.6495	1.21602	4.4467	3.54167
4.4832	13.04387	3.8969	1.38197	4.8199	3.68345
4.8320	11.13742	4.0309	1.54793	5.0790	3.91204
5.1500	8.65149	4.2080	1.81688	5.4833	3.96701
5.7040	2.70613	4.5361	2.01717	5.7735	3.97280
7.0172	1.51821	4.6907	2.13734	6.1363	3.9/309
7.3865	0.90397	4.8144	2.30043	6.8412	3.84259
7.6019	0.86341	5.1134	2.58655	7.2143	3.80208
7.7860	0.67219	5.4639	2.70672	7.5460	3.73553
8.5560	0.62583	5.5773	2.79542	7.9295	3.65162
8.6689	0.70695	5.7732	2.91845	8.8209	3.51852
9.0793	0.70695	5.8969	3.07868	9.1941	3.43461
9.4281	0.94454	6.4639	3.15021	9.6916	3.35069
10.5360	0.97930	6.6598	3.14449	10.3032	3.30440
12.1467	0.94454	6.8454	3.18455	11.0288	3.19155
12.6494	0.93295	7 1856	3.15594	11.5470	3.14815
12.8443	1.17053	7.4021	3.14163	11.8269	3.11343
13.4906	1.39652	7.5670	3.07582	12.2415	3.04688
13.6753	1.30960	7.9381	2 96137	12.9360	3.00347
13.8087	1.29222	8,4536	2.88984	13.2988	2.96007
14.1370	1.41970	8.6289	2.80973	13.5994	2.93981
14.3421	1.30381	9.0412	2.69242	14.0431	2.84144
14.5576	1.49503	9.4/42	2.42060	15.0091	2.78646
14.7833	1.42550	10.2784	2.33190	15.3511	2.75174
15.4604	1.41391	10.6392	2.22604	15.7554	2.71123
17.0095	1.44868	10.8557	2.15737	16.7194	2.63310
17.1121	1.37914	11.2680	1,91989	17.1340	2.60417
18.9382	1.27483	11.8454	1.89700	17.5486	2.56076
20.5694	1.12417	12.2062	1.82260	17.7041	2.56070
20.6412	0.0000	12.4227	1.73104	18.2638	2.49421
20.7438	0.69536	12.7210	1.61373	18.8235	2.45660
20.8//1	0.00000	13.0928	1.56795	19.1760	2.42188
21.0310	1.08361	13.2577	1.52790	19.7771	2.39003
21.1234	0.99089	13.4639	1.51359	20.2747	2.31481
21.2157	0.13907	13.9175	1.39342	21.3527	2.27141
21.4100	0.01159	14.3711	1.29041	21.4460	2.35822
21.7081	0.67798	14.8351	1.18455	21.6325	2.35532
21.8825	0.00000	15.1546	1.09299	22.4514	2.34954
22.0467	0.43460	16.1856	0.89843	23.3221	2.34375
22.2008	0.30132	16.4639	0.82403	24.2446	2.33507
22.4878	0.11010	16.8454	0.73247	25.2397	2.33507
22.5904	0.21440	17.0309	0,63233	27.3024	2.34664
22.7853	0.00000	17.5670	0.58369	28.3908	2.33218
40.0000		18.0206	0.54650	29.0956	2.33507
		18.2680	0.47210	30.8992	2.32639
		18.5567	0.37196	32.0912	2.32060

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⁵⁰⁰ Hz, 258 Duty Cycle November 13, 1991, (time in micro-seconds)

Time	Source V	Time	Current	Time	Cell V
0.0000	0.00000	0.0000	0.00000	0.0000	2.17366
2.2738	0.99652	5.5849	0.0000	9.2903	2.76883
5.1677	2.98667	9.9288	0.49913	19.8194	3.09373
5.5811	3.96002	14.0657	0.96924	25.6000	3.19436
15.0896	3.93975	19.0301	1.31747	35.3032	3.36688
23.7712	4.09907	27.5109	1.76146	41.0839	3.45026
35.5535	4.19467	37.2328	2.09228	48.7226	3.53939
54.9839	4.33951	49.4369	2.43180	55.5355	3.60265
67.5930	4.38297	65.7780	2.69878	61.7290	3.64577
89.710 6	4.44380	90.5999	2.86419	72.6710	3.71765
110.7947	4.48146	124.9368	2.98317	80.1032	3.72340
128.5714	4.50174	152.4477	3.05572	92.6968	3.76366
140.1470	4.54809	218.0188	3.04701	109.0065	3.79528
163.9182	4.54809	297.4489	3.04701	124.4903	3.82979
194.0974	4.58575	406.4583	3.04701	138.9419	3.85854
222.8296	4.58575	506.1595	3.04411	152.3613	3.89017
264.1709	4.57706	525.1896	0.00000	186.4258	3.89304
308.6128	4.59154	2000.0000	0.00000	220.9032	3.90454
341.2724	4.60023			279.5355	3.91892
388.6082	4.63789			335.4839	3.94192
444.4189	4.61761			400.1032	3.95630
503.5370	4.60023			451.3032	3.97355
507.6711	3.24739			486.4000	3.97930
511.3918	1.5/300			499.2000	3.94192
520.4869	1.99099			515.509/	2.48994
524.20/6	0.04036			564.0/1U	2.40943
636 7347	0.00290			745 0920	2.30343
2000 0000	0.00000			709 0677	2.32092
2000.0000	0.00000			2000.0000	2.17360
					=: = = = = = =

¹ kHz, 25% Duty Cycle November 13, 1991 , (time in micro-seconds)

Time	Source V	Time	Current	Time	Cell V
0.0000	0.00000	0.0000	0.00000	0.0000	2.19364
0.5106	0.06560	3.9604	0.00000	4.3488	2.47110
0.7660	0.34985	4.8521	0.13439	8.6977	2.68208
1.0213	0.98154	5.7885	0.33476	12.8394	2.84104
1.1915	1.76142	8.2571	0.59866	17.9130	2.97399
1.7872	2.42468	11.2364	0.91142	22.0548	3.13006
2.3830	3.18756	14.5563	1.19487	28.0603	3.22832
3.7447	3.97473	17.3654	1.42944	36.6544	3.39306
4.3404	4.06706	19.5786	1.62004	47.1123	3.54335
11.3191	4.07677	23.0687	1.76665	55.3958	3.63295
14.2979	4.14723	27.8357	2.02566	66.6820	3.72254
17.3617	4.20554	34.7308	2.29688	81.0746	3.79769
20.2553	4.23955	38.5614	2.43128	98.2628	3.87572
23.9149	4.29057	42.1366	2.51436	120.3175	3.91329
27.6596	4.31973	48.0953	2.68051	139.6802	3.95665
31.0638	4.35374	57.0334	2.82468	160.0782	3.97977
35.6596	4.39018	64.4392	2.94930	181.0976	4.00867
40.4255	4.42420	68.2698	2.96885	217.7520	4.00578
45.7872	4.45092	70.0575	3.02260	239.4961	4.00578
47.5745	4.48251	72.6963	3.03971	250.1611	4.01734
54.5532	4.48980	74.3137	3.07147	265.5891	2.45665
55.4043	4.52381	79.5914	3.08369	303.7966	2.39595
61.7872	4.52381	80.6129	3.11790	342.3148	2.37861
64.4255	4.55782	86.9972	3.12523	370.1680	2.35549
72.5106	4.56268	90.6576	3.19853	398.1247	2.32659
73.6170	4.60398	103.7668	3.19365	427.5311	2.30636
88.7660	4.61127	104.6180	3.23519	450.2071	2.30636
90.6383	4.64529	113.4710	3.23274	1000.0000	2.19364

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	4 64006	114 7470	3 26940
38.4081 102 6383	4.64772	125.8140	3.28161
103.6596	4.67930	133.4752	3.31827
109.7872	4.67930	146.1588	3.32315
119.4043	4.68659	160.2043	3.34026
127.3191	4.68902	173.2283	3.35736
128.8511	4.70845	188.6359	3.35247
137.8723	4.72303	206.2567	3.33/30
145.5319	4.72340	219.4309	3.33/39
158.2128	4.74976	251.2875	3.34270
162 8936	4.75705	252.9900	3.11790
164.9362	4.72546	254.0115	2.76848
167.6596	4.73032	256.0545	2.27245
168.9362	4.76433	258.0975	1.75932
170.8936	4.74247	260.8214	1.15333
172.8511	4.76676	264.6520	0.46671
174.6383	4.73761	266.6950	0.06842
176.3404	4.75948	207.4012	0.02688
181.8723	4.75100	2/3.5050	0.00000
203.1004	4.76190	1000.0000	0.00000
241 2766	4.76676		
249.1915	4.76676		
249.7021	4.55539		
249.7872	4.25413		
250.2979	3.75364		
250.4681	3.42323		
251.0638	3.01506		
251.3192	2.38095		
253 3617	1.43586		
254.8936	1.40185		
257.3617	1.33139		
259.4893	1.35326	-	
261.2766	1.30224		
+262.2128 264 0000	1.30/09		
265 6170	1 27794		
266.5532	1.27065		
267.1489	1.23907		
267.3192	1.06657		
268.2553	0.82362		
269.3617	0.47376		
270.9787	0.31098		
272.5957	0.39843		
278.0000	0 34014		
280.0000	0.26725		
282.8085	0.26968		
284.2553	0.30126		
285.9575	0.23324		
286.8936	0.25267		
291.4043	0.20408		
302 2128	0.17493		
303.1489	0.14334		
304.3404	0.20651		
305.8723	0.1530 6		
311.1489	0.13362		
312.1702	0.15063		
321 9793	0.11905		
323.3192	0.10933		
324.9362	0.05831		
327.1489	0.10933		
328.7660	0.08260		
330.2128	0.11176		
334.6383	0.08746		
337.9373	0.08989		
330 8208	0.07775		
341.7021	0.07046		
344.0000	0.08260		
347.4043	0.05345		
349.1064	0.08260		
350.9787	0.05588		
354.0425	0.08017		
350.7447	0.000/4		
360.1702	0.05831		
361.3617	0.07289		
364.0000	0.03887		
368.7660	0.03644		
371.1489	0.07775		
372.8511	0.04859		

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378.7234	0.04130
385.8723	0.02915
393.9575	0.00972
400.0000	0.00000
1000.0000	0.00000

5	kHz, 3	258	Du	ity Cy	rc.)					
N	vembe	r 13	3,	1991	,	(time	in	micro-seconds)

Time	Source V	Time	Current	Time	Cell V	
0.0000	0.00000	0.0000	0.00000	0.0000	2.31139	
0.5093	0.06960	3.5000	0.00000	1.0204	2.41470	
1.2733	1.36800	3.8396	0.18204	2.8061	2.56127	
1.9525	2.58240	4.9488	0.43114	5.1871	2.76309	
2.2920	3.54720	7.1672	0.78802	9.2687	3.01778	
2.9711	4.14720	10.0683	1.20958	12.4150	3.20279	
3.6503	4.57920	13.9079	1.64790	16.2415	3.36857	
4.5840	4.85760	18.2594	2.06228	18.1973	3.44065	
6.4516	4.86960	23.6348	2.50539	19.55/8	3.44065	
9 5076	4.90300	20.3030	2.01130	20.3231	3.50555	
12 7334	4 94160	33 1058	3 11856	25 4252	3 68333	
14.2615	4.98960	36.8601	3.25988	26.3605	3.73138	
16.9779	5.03040	37.1160	3.31018	28.7415	3.77463	
18.6757	5.06160	38.6519	3.32216	32.3129	3.85872	
21.8166	5.07120	40.1877	3.42515	34.8639	3.91158	
22.2411	5.10000	41.6382	3.44671	37.4150	3.98126	
25.8065	5.10720	45.6485	3.60479	40.9014	4.03652	
26.8251	5.04720	46.8430	3.61677	43.1122	4.07496	
29.6265	5.0/360	48.2935	3./19/6	45.5/82	4.11821	
37 1917	5.14320	50.4200	3 63932	40.003/	4.15906	
40 7470	5 22720	51 5358	3 58563	48 8095	4 13023	
44.5671	5.22480	52.8157	3.30060	49.1497	4.06055	
46.3497	5.25840	53.9249	3.00838	50.4252	3.84671	
49.0662	5.25840	54.9488	2.72335	52.7211	3.60884	
49.4907	5.14080	56.3140	2.35928	54.4218	3.38299	
49.4907	4.83600	58.2765	1.90659	57.3129	3.09467	
49.9151	4.27920	60.1536	1.42994	59.5238	2.82556	
50.3396	3.93840	63.2253	0.91257	62.6701	2.61893	
50.9338	3.52320	66.3823	0.39521	65.7313	2.41711	
51.2/33	2.84100	76 1945	0.03988	13.1/UL 93.0272	2.40029	
52 4618	1.60080	100.0000	0.00000	109.7789	2.35704	
53.5654	1.30320	200.0000	0.00000	131.3775	2.34983	
54.6689	1.29360			151.7007	2.32580	
57.4703	1.18560			167.0918	2.32340	
60.6112	1.17360			200.0000	2.31139	
62.6486	1.11120					
63.7521	1.13280					
65.2801	1.06320					
67.31/3	1 00800					
68.0815	0.70560					
68.6757	0.00720					
69.4397	0.31200					
70.6282	0.17520					
73.1749	0.16800					
75.1273	0.25440					
76.4856	0.16560					
79.4567	0.15840					
80.0390 81 5789	0.14640					
82 5976	0 10560					
84.2105	0.12480					
88.2003	0.12000					
91.1715	0.05760					
93.0390	0.04800					
93.8879	0.08880					
96.6893	0.07680					
98.1324	0.04560					
106 2919	0.04360					
116.4686	0.04080					
127.1647	0.04080					
133.7012	0.04320					
135.9083	0.00000					
200.00 00	0.00000					

Time	Source V	Time	Current	Time	Cell V
0.0000	0.0000	0.0000	0.00000	0.0000	2.22730
0.2048	0.04069	2.7380	0.00000	0.9129	2.21873
0.3754	0.09813	3.6780	0.06593	1.6183	2.22159
0.5802	0.64380	4.2092	0.16054	2.1577	2.23015
0.7167	1.09613	4.8631	0.32680	2.7801	2.2/299
0.8191	1.61308	5.9256	0.59627	3.8389	2.3/293
1.0580	2.14200	7.2742	1 00509	4.5300	2.45003
1.2628	2.67092	8.4103	1 29575	4.8548	2.54997
1.6382	3.32190	10 7479	1.51362	5.5187	2.57853
2 4915	4.49701	12.0147	1.71715	6.4315	2.70702
2.9352	4.99960	13.6085	1.95509	6.7635	2.70417
3.2765	5.17192	14.9980	2.10989	7.4274	2.78127
3.7884	5.28680	16.0196	2.28476	7.8008	2.83207
3.8908	5.30834	17.4908	2.43903	8.9627	2.87550
5.6997	5.30834	19 2072	2.70330	9.9170	2.96688
6 5188	5.27962	20.1880	2.74343	10.4564	3.02113
6.8259	5.30594	20.8010	2.84377	11.3278	3.08395
8.0887	5.30834	22.2313	2.98997	11.7427	3.11251
11.8089	5.31073	23.5799	3.12470	12.2407	3.22102
12.1843	5.34663	24.3564	3 21070	13.7344	3.24385
12.8328	5.38492	25.5006	3.27090	14.5643	3.26385
14 5051	5.41125	25.8275	3.31104	14.8133	3.31239
14.9829	5.39210	26.8901	3.31390	15.7261	3.38664
15.5973	5.42800	28.0752	3.16197	15.9751	3.42020
16.3481	5.47108	29.3012	2.86383	17 3444	3.50942
16.7577	5.49262	31.3854	1 94075	17.9668	3.51228
17.0307	5.50439	34.0008	1.63688	18.5477	3.57796
19 6246	5.55006	35.3494	1.34735	19.8340	3.60937
20.1706	5.57399	37.2701	0.96894	21.3278	3.68361
20.5802	5.56203	38.4552	0.80268	22.2822	3.70360
21.2969	5.63383	38.4961	0.68227	22.8210	3 80069
21.9795	5.63383	39.5995	0.31001	24.4813	3.83495
22.4573	5.59/93	41.0298	0.30674	25.3112	3.90205
22.9010	5.62665	42.4193	0.06880	26.5000	3.91205
24.6075	5.55724	43.1140	0.03440	26.8050	3.84066
24.9147	5.41364	44.7078	0.00573	27.3859	3.77499
24.9829	5.21260	47.1189	0.01433	28.0/22	3.60080
25.1536	4.93498	20.4303 65 8766	0.01433	29.5851	3.49229
25.3584	4.50103	98.8966	0.01147	30.2490	3.40091
25.8703	3.65696	100.0000	0.00000	30.6224	3.32953
26.1775	3.24531			31.4108	3.20388
26.3140	2.88392			32.3237	2 99258
26.8601	2.26406			34.9793	2.85551
27.3720	1.84523			36.1826	2.77841
27.7474	1.43598			37.3859	2.68418
28.2594	1.38572			38.4232	2.59852
28.5324	1.33307			39.9170	2.47858
28.7372	1.29956			40.0039	2.36150
29.4198	1.32110			41.7427	2.33581
29.7611	1 40247			42.4481	2.27299
31.1263	1.33785			43.3610	2.25585
31.8430	1.33067			43.6100	2.31868
32.4915	1.29717			43.9419	2.25871
33.0375	1.33067			44.2/3 9 44 7719	2.29298
33.8567	1.33067			47.0954	2.30725
34.4027	1.41683			50.2075	2.30440
36.1775	1.39051			53.5685	2.29869
37.1672	1.38093			58.9627	2.27299
37.6792	1.30195			69.128£	2.28441
38.2594	1.28999			74,9793	2.28641
38.7031	1 26366			80.4149	2.27299
39.8635	1.28520			82.2822	2.26728
40.3072	1.25648			82.6556	2.27870
40.9215	1.25648			83.5685	2.25300
41.2969	1.25648			83.2097	2.26728
41.8430	1.17750			90.9544	2.25014
42.4915	0.00000			93.3195	2.25871
43.1/41	0,10531			95.3112	2.25300
44.4710	0.22736			97.8008	2.25014
44.6758	0.16514			99.9585	2.25871

10 kHz, 25% Duty Cycle November 13, 1991, (time in micro-seconds)

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45.2218	0.15796
46.2799	0.08377
47.2014	0.07898
47.7133	0.15317
48.8055	0.15317
49.0785	0.18907
49.5222	0.15796
50.3072	0.12684
51.2628	0.08616
51 0705	0 08616
52 2526	0 10770
53 5496	0 10770
55.0069	0.10521
57 2014	0.10331
57.2014	0.08855
39.4198 69 E030	0.08616
62.5939	0.08855
64.0614	0.08137
64.8464	0.07419
65.4949	0.04069
68.1229	0.03829
72.1160	0.03351
75.5290	0.02393
77.1672	0.01436
80.0000	0.00000
100.0000	0.00000

25	kHz,	258	Duty	Cyc	1.			
Nov	rember	: 13,	1991	ι, ⁻ (time	in	micro-seconds)

Time	Source V	Time	Current	Time	Cell V
0.0000	0.00000	0.0000	0.00000	0.0000	2.35193
0.3042	0.06318	2.2593	0.00000	0.2269	2.35193
0.7099	0.06804	2.6161	0.13880	0.8045	2.34907
0.8282	0.34994	2.8029	0.13880	1.2584	2.35479
1.0986	1.34629	3.4485	0.28003	1.9185	2.35479
1.3521	2.19684	4.0430	0.46510	2.3724	2.37768
1.6225	3.05225	4.5866	0.71591	2.7849	2.42918
1.8761	3.77643	5.0453	0.82062	3.2800	2.52647
2.2310	4.62697	5.5379	1.02516	3.8783	2.63519
2.6535	5.45808	6.2005	1.22727	4.5384	2.73820
2.8732	5.87606	7.0498	1.46591	5.4048	2.85837
3.1606	6.18226	7.7973	1.69724	6.0031	2.95565
3.4310	6.47874	8.6806	1.93831	6.6013	3.04149
3.7521	6.70717	9.4621	2.16477	7.2202	3.13591
4.0732	6.87728	10.1586	2.32305	7.6122	3.15021
4.3268	7.01823	10.7871	2.48377	7.9010	3.19599
4.6817	7.01823	11.2967	2.58604	8.3961	3.27039
6.2873	7.00851	11.5006	2.59091	9.0562	3.33619
6.6085	6.95018	11.6874	2.62257	9.6545	3.40200
6.9296	6.93074	12.1631	2.63474	10.2114	3.47926
7.1831	6.78007	12.6897	2.52760	10.7684	3.54220
9.4986	6.77035	12.9615	2.51299	11.3254	3.60229
9.6507	6.70717	13.3692	2.39123	12.1300	3.57082
10.0901	6.62454	13.5051	2.39123	12.5219	3.53076
10.2592	6.6383/	13.7429	2.29870	12.8314	3.48498
10.5127	6 47300	14 2016	2.298/0	13.2027	3.43062
10 8676	6 25030	14 4054	2.10102	14 2960	3.33308
10.9859	5.83232	14.7622	2 02841	14 5642	3 20172
11.1042	5.50182	15.5096	1.86282	15.2862	3.13591
11.2901	4.95747	16.1891	1.68263	16.0908	3.05579
11.5437	4.27217	16.9026	1.50487	16.6684	2.98999
11.7296	3.89307	17.3443	1.36851	17.7411	2.87840
12.0000	3.24666	17.5821	1.36364	18.6900	2.80401
12.3380	2.71689	17.8199	1.28328	19.4740	2.73248
12.6423	2.17254	18.5674	1.12500	20.5467	2.64950
13.098 6	1.60875	19.7225	0.89610	21.2068	2.58083
13.4873	1.22965	20.4700	0.73539	22.2589	2.48355
13.7408	1.12758	21.1495	0.56250	23.3729	2.40629
13.8592	1.05954	21.8460	0.46266	24.3631	2.32904
13.9775	0.99149	22.4236	0.35552	25.2708	2.32904
14.2479	0.98177	23.2729	0.22159	26.3435	2.35479
15.5662	0.98663	23.9864	0.06575	28.1382	2.35193
15.8197	1.14702	24.5470	0.02679	29.2934	2.35193
17.7127	1.06440	26.1224	0.00000	31.0469	2.36910
18.0000	1.01580	40.0000	0.00000	33.2336	2.36624
10.3408	1.01094			35.6679	2.34907
18 9461	1 00100			30.3 902 37 0759	2.33/03
10 3183	1 00122			30 E147	2.30338
19 7408	1 07412			30.319/	2.30338
20.6704	1.06440			40 0000	2.33/03
21.5155	1.13244				
21.5324	1.08870				

100.0000 2.22730

22.9014	1.07412
23.4254	0.93317
23.6958	0.92345
23.8648	0.97205
24.3211	0.93803
24.5577	0.89429
25.0310	0.82139
25.2169	0.11179
25.4197	0.51033
26.0282	0.35480
26.2310	0.05346
26.4169	0.32564
26.6535	0.03402
26.8056	0.01458
26.9239	0.13609
27.3972	0.06318
27.9549	0.02430
28.5972	0.00000
40.0000	0.0000

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500 Hz, 50% Duty Cycle November 13, 1991, (time in micro-seconds)

Time	Source V	Time	Current	Time	cell V
0.0000 2.0471 5.1177 15.3531 31.7298 47.0829 65.5067 92.1187 122.8250 156.6018 245.6499 344.9335 498.4647 770.7267 939.6111 991.8116 1021.4944 1038.8945 2000.0000	0.00000 1.00724 2.01158 3.21852 3.37482 3.47902 3.56874 3.62084 3.63821 3.65557 3.66425 3.66425 3.66136 3.68162 3.69030 0.22576 0.00000 0.00000	0.0000 9.1978 19.4175 33.7251 51.0986 59.2744 71.5381 80.7358 92.9995 175.7793 230.9658 380.1737 561.0629 753.1937 910.5774 997.4451 1017.8845 2000.0000	0.00000 0.0000 0.50794 1.00866 1.30880 1.38240 1.45166 1.49495 1.53824 1.54690 1.52525 1.48485 1.47042 1.46032 1.46898 1.47475 0.00000 0.00000	0.0000 24.4648 39.7554 57.0846 70.3364 84.6075 102.9562 146.7890 188.5831 209.9898 293.5780 503.5678 704.3833 864.4241 1005.0969 1015.2905 1024.4649 1046.8909 103.7819 1152.9052 1222.2222 1367.9918 1516.8196	2.15518 2.54097 2.77883 2.99057 3.10370 3.17041 3.21392 3.21392 3.19072 3.16171 3.15861 3.15301 3.15301 2.72951 2.40174 2.34953 2.30602 2.27701 2.23640 2.21030 2.19579 2.16389
				1516.8196 1692.1509 2000.0000	2.19 2.16 2.15

1 kHz, 50% Duty Cycle							
November 13	, 1991, (t	ime in micr	o-seconds)	1			
Time	Source V	Time	Current	Time	Cell V		
0.0000	0.00000	0.0000	0.00000	0.0000	2.13888		
2.0000	1.01010	8.1716	0.03324	7.3052	2.22793		
2.0429	2.00866	11.8488	0.23988	8.9286	2.35557		
3.6772	3.01299	14.7089	0.48121	16.6396	2.50695		
8.5802	3.32756	17.9775	0.62572	23.5390	2.64349		
16.3432	3.33911	23.6977	0.79191	35.3084	2.76519		
22.8805	3.43723	28.6006	0.97688	49.5130	2.85127		
35.5465	3.50072	35.9551	1.11561	66.5584	2.95219		
56.7926	3.54690	45.3524	1.24566	80.3571	2.99078		
80.0817	3.59885	52.2983	1.34971	97.8084	3.05015		
119.7140	3.64502	59.2441	1.40607	113.6364	3.07686		
173.2380	3.67388	69.8672	1.44942	136.7695	3.09170		
271.2972	3.69697	82.5332	1.50000	162.3377	3.11248		
358.3248	3.70851	95.6078	1.53324	189.5292	3.11248		
422.4719	3.72006	110.7252	1.55347	226.8669	3.10951		
470.6844	3.72294	163.8407	1.56069	257.7110	3.12435		
496.4249	3.70851	210.4188	1.55925	306.0065	3.11248		
500.5107	3.37374	290.5005	1.54913	333.1981	3.10358		
502.1451	2.55700	351.3790	1.54046	372.1591	3.10951		
508.6823	1.38240	411.8488	1.52168	408.6851	3.11248		
513.9939	0.25397	483.3504	1.49855	437.9059	3.10654		
522.982 6	0.19625	503.7794	1.49855	465.5032	3.10654		
530.3371	0.21068	510.3167	1.10694	487.0130	3.10951		
535.6486	0.13276	512.7681	0.71243	497.1591	3.10358		
552.4004	0.11544	518.3673	0.00000	502.4351	3.00562		
576.5067	0.10678	1000.0000	0.00000	504.0584	2.75925		
595.9183	0.00000			507.3052	2.49804		
1000.0000	0.00000			511.3636	2.31104		

545.8604 2.2635	5
584.4156 2.23090)
636.3636 2.19528	
676.1364 2.18044	
740.2598 2.14482	2
810.0649 2.16559)
871.7532 2.16263	3
917.2078 2.15966	i
954.9513 2.14185	5
976.4611 2.14185	5
1000.0000 2.13888	1

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5 kHz, 50% Duty Cycle November 13, 1991, (time in micro-seconds)

ovember 13,	1991, (6				
Time	Source V	Time	Current	Time	Cell V
0.0000	0.00000	0.0000	0.00000	0.0000	2.20000
0.5111	0.11264	5.1783	0.00000	2.9561	2.22943
1.1073	0.67825	6.4450	0.15196	4.8986	2.27748
1.1925	1.10485	8.5934	0.33898	8.2770	2.40240
1.5332	1.50749	11.1509	0.45149	9.9662	2.47688
1.7888	1.98922	12.6854	0.57569	11.4865	2.50571
2.4702	2.60755	15.1407	0.66774	14.1892	2.58739
2.9813	3.07969	18.5166	0.84015	16.8074	2.67387
3.7479	3.42960	21.9949	0.96727	20.1014	2.72192
4.0034	3.50150	25.8824	1.08416	23.7331	2.77477
4.5145	3.52786	28.6445	1.18352	26.4358	2.83243
7.7513	3.53026	33.2481	1.28434	31.0811	2.89249
8.6031	3.56141	37.2379	1.37347	35.8953	2.94775
10.0511	3.53505	42.2506	1.46259	40.7095	3.01261
11.4140	3.52786	47.1611	1.54734	42.8209	3.06306
13.6286	3.60695	51.9693	1.59848	46.1149	3.09910
17.3765	3.60695	57.5959	1.64962	48.6486	3.10631
18.4838	3.64769	63-5294	1.68177	53.9696	3.09670
22.6576	3.64530	68.7468	1.72414	56.5878	3.11832
23.7649	3.68364	75.9079	1.76651	62.8378	3.12793
32.5383	3.69083	82.8644	1.79866	66.7230	3.17117
33.7308	3.72678	88.2864	1.81327	72.5507	3.18318
39.1823	3.73877	91.6624	1.833/2	/3.8440	3.10/99
41.2266	3.77711	94.5269	1.84249	81.0/23	3.19/00
47.7002	3.77711	98.3100	1 04933	03 0199	3 21201
52.2146	3.80827	102.3018	1 20076	93.9109	3 22643
67.1210	3.8106/	105 0639	1 55026	101 1924	3 22643
09.3330	3.04102	106 0970	1 32379	102 2804	3.21922
100 6914	3 46794	106 9054	1.14553	103.2939	3.07027
101 3629	2 59119	107 7238	0.92344	104.7297	2.91652
102.5554	1 72798	109 2583	0.72618	105.9966	2,77718
103 3220	1.32774	110.4859	0.52162	107.1791	2.62823
104.6848	1.21270	111.7136	0.27469	108.8682	2.49369
106.1329	1.24626	112.2251	0.05114	110.3041	2.39039
107.3254	1.20791	114.2857	0.00000	111.4865	2.27748
109.2845	1.26303	200.0000	0.00000	112.6689	2.28949
110.2215	1.26303			115.4561	2.28949
110.8177	1.20312			120.9459	2.29429
112.6917	0.18214			124.8311	2.29670
114.5656	0.17735			126.3513	2.25586
115.4174	0.11504			129.6453	2.27267
116.6951	0.13901			138.1757	2.27267
118.6542	0.11744			142.9899	2.27267
120.5281	0.08388			152.2804	2.26787
121.2947	0.03116			155.9966	2.26787
123.5094	0.10785			161.9932	2.26306
126.0647	0.07909			165.2027	2.26306
127.6831	0.12463			174.1554	2.25826
128.9608	0.14859			179.1385	2.25826
131.3458	0.07909			101 0473	2.24144
132.1976	0.11025			191.04/3	2.22222
133.8160	0.07430			200.0000	2.20000
136.6269	0.07430				
139.6082	0.00000				
200.0000	0.00000				

10 kHz, 50% Duty Cycle November 13, 1991 , (time in micro-seconds)

Source V	Time	Current	Time	Cell V
0.0000	0.0000	0.00000	0.0000	2.27378
0.09632	2.7435	0.00000	0.0208	2.27378
0.32107	6.0440	0.32351	0.7897	2.27666
0.74431	8.9319	0.53871	2.0781	2.28242
1.11208	11.9849	0.73368	3.0341	2.31412
1.54991	13.3257	0.80878	4.3849	2.37464
	Source V 0.00000 0.09632 0.32107 0.74431 1.11208 1.54991	Source V Time 0.00000 0.0000 0.09632 2.7435 0.32107 6.0440 0.74431 8.9319 1.1208 11.9849 1.54991 13.3257	Source V Time Current 0.00000 0.00000 0.00000 0.09632 2.7435 0.00000 0.32107 6.0440 0.32351 0.74431 8.9319 0.53871 1.11208 11.9849 0.7368 1.54991 13.3257 0.80878	Source V Time Current Time 0.00000 0.0000 0.00000 0.0000 0.9632 2.7435 0.00000 0.0208 0.32107 6.0440 0.32351 0.7897 0.74431 8.9319 0.53871 2.0781 1.1208 11.9849 0.73368 3.0341 1.54991 13.3257 0.80878 4.3849

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		14 4983	A 88533	5.9850	2.42939
1.1358	1.88336	16 1105	0 96620	7.0657	2.47262
1.3217	2.13070	17 0504	1 03408	8.0840	2.49280
1.5489	2.4109/	10 4035	1 11496	9.6841	2.56196
1.7760	2.70280	21 2012	1 21028	10.9934	2.64265
2.0858	2.90090	22.3914	1 28827	12.5520	2.68300
2.3543	3.22825	23.2030	1 25471	14 7340	2.72334
2.4989	3.42966	23.3100	1 40114	16 4599	2 76369
2.8706	3.52306	27.4359	1 40760	10.1000	2 79251
3.0978	3.63106	29.7043	1.49/09	10.2000	2 92709
3.5108	3.69235	32.2828	1.30990	19.3890	2.02/05
3.6966	3.73322	34.7582	1.63200	21.0/23	2.00933
3.9032	3.77408	37.1717	1.66956	22.9011	2.90202
4.8118	3.77408	39.9977	1.72010	24.2934	2.93084
5.9683	3.76824	42.0605	1.76921	26.3924	2.98271
8.1161	3.76532	44.1439	1.80965	28.1380	3.02305
10.6356	3.77700	47.2794	1.85442	28.6783	3.04035
11.8128	3.79451	49.0534	1.86453	30.6733	3.05475
12.9899	3.79743	50.4767	1.87753	31.9202	3.07205
14.5801	3.79743	51.1987	1.87753	33.5827	3.08069
15.5507	3.83246	51.6319	1.87753	35.6401	3.12680
16.5420	3.84121	52.1476	1.83420	37.2402	3.14986
17.9463	3.85289	52.8283	1.70422	38.8820	3.16715
18.6898	3.88792	53.5916	1.56268	41.6459	3.18156
21.1886	3.88208	54.2104	1.41392	44.0150	3.19885
22.7994	3.89083	54.7261	1.30560	44.4306	3.22190
24.5961	3.89959	55.5719	1.13807	45.2411	3.18444
26.4341	3.90835	56.3763	0.96187	46.1139	3.21902
28.4167	3.92878	57.2840	0.80589	47.3192	3.21902
30.3373	3.92878	58.1504	0.63403	48.5245	3.24496
31.3699	3.96381	59.0374	0.48382	50.0000	3.27378
33.2492	3.97548	59.9656	0.29896	51.1845	3.27378
35.2524	3.99883	60.8526	0.14876	52.4522	3.20749
35.8100	3.99299	61.8221	0.01978	53.5952	3.08646
37.9784	4.00759	62.2347	0.00000	55.0083	2.94813
39.7132	4.01343	100_0000	0.00000	56.50 46	2.78386
41 6957	4.00175			57.751 5	2.65706
43 1827	4.00175			59.1022	2.55620
45 3304	4.01635			60.7440	2.41787
47 5195	4.03386			61.7207	2.33718
19 0032	4 04262			62.6351	2.30259
40 4105	4 05429			64.6509	2.29683
40 0771	4 05721			67.0615	2.28530
43.3111	4.05429			69.8670	2.28530
50.2249	4 01635			73.6700	2.28242
50.5034	3 90835			76.8080	2.28242
50.5140	3 80911			80.9435	2.27378
50.03/9	3 66900			84.8088	2.28530
51 0303	3 35377			88.6741	2.29683
51 0509	3 23409			92.0615	2.25072
51 1542	3 14069			95.3034	2.27089
51 1955	3.00934			98.2128	2.27089
51 2781	2,91302			99.9377	2.27378
51 3401	2.77875			100.0000	2.27378
51 4433	2.65616				
51 5879	2.55692				
51 6292	2.39930				
51.7118	2,30882				
51.7738	2.22125				
52.0216	2.08990				
52.1661	1.92936				
52.2487	1.84764				
52.2900	1.78926				
52.4966	1.76299				
52.6824	1.54991				
52.9715	1.49737				
53.1987	1.41856				
53.3846	1.37186				
53.5498	1.28722				
53,7150	1.22008				
54.0454	1.19089				
54.2313	1.21133				
54.7269	1.22008				
54.9541	1.25511				
55.2226	1.17630				
55.7389	1.16754				
55.9041	1.22300				
56.1106	1.19381				
56.9573	1.19089				
57 4530	1 10214				
	T'TOTTE				
57,9073	1.16170				
57.9073 58.2997	1.16170				
57.9073 58.2997 58.6921	1.16170 1.15879 1.17338				
57.9073 58.2997 58.6921 58.9605	1.16170 1.15879 1.17338 1.19381				
57.9073 58.2997 58.6921 58.9605 59.3736	1.16170 1.15879 1.17338 1.19381 1.22008				
57.9073 58.2997 58.6921 58.9605 59.3736 59.8073	1.16170 1.15879 1.17338 1.19381 1.22008				

60.7779	1.21424
61 1703	1 21424
01.1/03	1.41444
61.3974	1.20841
61.62 46	1.12960
61 7485	1 04203
GL . 7400	0.07200
61.7898	0.9//82
62.1615	0.00000
62.3681	1.15295
60 7300	0 04096
62.7398	0.04088
62.9670	0.66258
63.2354	0.01751
62 4419	0 33567
03.4443	0.0000
63.7517	0.26562
63.937 6	0.22767
64.1235	0.17513
64 3300	0 11384
	0.11004
04.0191	0.12843
65.0734	0.10216
65.3213	0.07005
65 7136	0.06130
66 0000	0.00468
00.0028	0.00400
66.6843	0.07881
67.4897	0.08465
69 1092	0 10216
00.1092	0.10210
68.5223	0.1196/
69.2864	0.08465
69 8027	0.03503
70 0000	0.01450
10.3809	0.01439
71.1037	0.01168
71.8472	0.02627
70 4461	0.02010
/2.4401	0.02919
72.9624	0.04378
73.4374	0.02335
74 1602	0 04378
74.1002	0.04370
74.7591	0.05254
75.1927	0.05254
76.2460	0.04670
77 3100	0.05546
77 6503	0 06713
77.0303	0.08/13
78.3525	0.09924
78.8481	0.09340
79.1992	0.06421
70 9907	0.05546
/9.000/	0.00010
80.2111	0.05838
80.5828	0.07005
81.0785	0.06130
81 5048	0.04086
01.0340	0.02705
82.3861	0.03/93
83.4121	0.04962
84.3001	0.03503
84 7338	0.02043
OE E106	0.02043
03.3190	0.02043
86.4273	0.02919
87.3153	0.03211
88.1620	0.04670
00 7106	0 02627
99.1730	0.0202/
90.0000	0.00000
100.0000	0.00000

25 kHz, 50% Duty Cycle November 13, 1991 , (time in micro-seconds)

Time	Source V	Time	Current	Time	Cell V	time	Lead DV
0.0000	0.00000	0.0000	0.00000	0.0000	2.32425	0.0000	0.00000
0.1342	0.01739	0.1651	0.01583	0.3214	2.31277	0.5752	0.00000
0.2168	0.05507	0.5986	0.01439	0.6221	2.31277	1.1505	0.00000
0.3511	0.31014	1.1558	0.01871	0.8709	2.30129	1.4792	0.00000
0.7124	1.04348	1.7337	0.01871	1.2442	2.29842	1.6025	0.00000
1.1461	2.06087	2.2601	0.01439	1.7937	2.30703	1.8285	-0.06975
1.5694	2.75942	2.4458	0.03166	2.1047	2.32425	2.2599	-0.18998
1.8379	3.12754	2.8277	0.05613	2.4780	2.36155	2.6502	-0.31304
2.1786	3.50725	3.1682	0.09067	2.9549	2.37877	2.9173	-0.37032
2.3025	3.53913	3.8803	0.18854	3.3074	2.41894	3.1228	-0.39301
2.5297	3.77101	4.6336	0.29793	3.7636	2.44763	3.3282	-0.40265
2.7568	3.95652	5.6140	0.44617	4.3961	2.48207	3.5336	-0.42079
2.9427	4.07246	6.4499	0.55699	4.7589	2.51363	3.8007	-0.43951
3.1492	4.11594	7.1207	0.65343	5.3810	2.54519	5.0334	-0.43951
3.4590	4.19420	7.8122	0.73546	5.7024	2.58250	5.0950	-0.42703
3.6758	4.24928	8.9164	0.85636	6.0135	2.60832	5.5265	-0.41456
3.9133	4.28116	9.8142	0.95423	6.6874	2.63702	5.7524	-0.40038
4.1404	4.30145	10.7224	1.05354	7.0710	2.66858	6.1428	-0.39641
4.6980	4.31304	11.7853	1.16005	7.4857	2.69727	6.6769	-0.37996
6.4739	4.31304	12.4458	1.22913	8.2219	2.71162	7.0262	-0.37089
7.2380	4.37391	13.7874	1.34715	8.6366	2.73458	7.6836	-0.37032
11.1926	4.37681	15.3148	1.46661	9.1239	2.75753	8.1972	-0.35728

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13.4435 16.2519 17.9866 20.0310 20.1342 20.2272 20.3614 20.4853 20.8983 21.3629 21.6107 22.0547 22.2509 22.4677 23.5312 23.5312 23.5312 23.5312 24.3263 25.4104 26.4223 30.0465 30.3975 30.6970 30.7383 30.8725 31.0274 31.3271 31.5333 31.6262 31.0274 31.3271 32.0496 32.1322 32.3283 32.4522 32.3283 32.4522 32.6000 40.0000	4.37971 4.42319 4.44928 4.46927 4.41739 4.32754 4.18841 3.98841 3.59130 2.31594 2.08116 1.67536 1.52174 1.67536 1.52174 1.3043 1.126667 1.16812 1.13043 1.12754 1.13043 1.12754 1.13043 1.12754 1.16522 1.16522 1.16522 1.16522 1.16522 1.17971 1.17681 1.12464 -0.77681 1.41159 -0.17681 1.41159 -0.17771 0.71304 -0.28696 0.54783 -0.11014 0.48406 0.02899 0.00000	16.8524 18.3488 19.5666 20.3612 20.6708 21.7131 21.9505 22.7141 23.3333 23.9525 24.7059 25.2528 25.8411 26.6254 27.4200 28.3385 28.9061 29.3911 29.8555 30.3302 30.5263 31.2281 31.4345 31.8266 32.5387 32.8277 33.6429 34.4066 36.2126 37.3065 38.3488 39.6078 40.0000	1.57311 1.66091 1.7302 1.80628 1.82642 1.83506 1.60915 1.68826 1.56736 1.4638 1.26223 1.13126 0.94485 0.69229 0.49223 0.40155 0.09211 0.02303 0.01295 0.02447 0.01205 0.02447 0.01205 0.02447 0.01205 0.02447 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	9.6423 10.3370 10.9279 11.5604 12.2447 12.8357 13.5200 14.3494 14.8678 15.8424 16.5785 17.1488 17.7605 18.3307 18.6336 19.0876 19.9689 20.4873 21.0368 21.3167 21.8351 22.1980 22.4469 23.4215 23.8362 24.2820 24.6345 24.8730 25.2981	2.78910 2.80918 2.8776 2.88092 2.89478 2.97561 3.01291 3.03874 3.06456 3.09900 3.11047 3.12482 3.16786 3.18221 3.21090 3.21951 3.22812 3.21951 3.12482 3.07317 2.95839 2.91822 2.86083 2.82353 2.79770 2.95839 2.91822 2.86083 2.82353 2.79770 2.95839 2.91822 2.86083 2.82353 2.79770 2.95839 2.31564 2.32712 2.32594 2.32712 2.32425 2.32425 2.32425 2.32425	8.5876 8.9985 9.3066 10.0462 10.7653 11.4432 11.9158 12.4088 13.0252 13.7237 14.3811 14.6276 15.4905 16.2917 16.6615 17.2573 17.8942 18.9625 19.3734 19.7637 20.0514 20.1746 20.3390 20.4828 20.9348 21.1813 21.5100 21.9414 22.8454 23.0508 23.3385 23.3672 23.9548 24.3041 22.8454 23.0508 23.3672 23.9548 24.3041 25.1258 25.5573 25.6625 26.6256 27.1186 27.4474 28.1253 29.6184 29.0498 29.3785 29.8100 30.1387 30.9605 31.1864 30.9399 31.9573 31.5973 31.5973 31.5973 31.750 34.4530 35.0760 37.0055 37.7401 38.5208 39.0509 40.0000	$\begin{array}{c} -0.35217\\ -0.34310\\ -0.3006\\ -0.32779\\ -0.31304\\ -0.30567\\ -0.29943\\ -0.28942\\ -0.28242\\ -0.28242\\ -0.28681\\ -0.25860\\ -0.25180\\ -0.25180\\ -0.25180\\ -0.25180\\ -0.25123\\ -0.22120\\ -0.23648\\ -0.23025\\ -0.22344\\ -0.21720\\ -0.21607\\ -0.21607\\ -0.21607\\ -0.21607\\ -0.21607\\ -0.22803\\ 0.38847\\ 0.50468\\ 0.62268\\ 0.65785\\ 0.62268\\ 0.65785\\ 0.62268\\ 0.65785\\ 0.62268\\ 0.65785\\ 0.62268\\ 0.65785\\ 0.68053\\ 0.5924\\ 0.70888\\ 0.67259\\ 0.5785\\ 0.63924\\ 0.68393\\ 0.57259\\ 0.55350\\ 0.55350\\ 0.58526\\ 0.55350\\ 0.58526\\ 0.5785\\ 0.6397\\ 0.59603\\ 0.59603\\ 0.57259\\ 0.55350\\ 0.57449\\ 0.58526\\ 0.57353\\ 0.6397\\ 0.59603\\ 0.57221\\ 0.63516\\ 0.61985\\ 0.6397\\ 0.59603\\ 0.57259\\ 0.55350\\ 0.57449\\ 0.47354\\ 0.44234\\ 0.34367\\ 0.22741\\ 0.20813\\ -0.50246\\ 0.0005\\ 0.00000\\ 0.0000\\ $
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40 kHz, 50% Duty Cycle November 13, 1991 , (time in micro-seconds)

Time	Source V	Time	Current	Time	Cell V
0.0000	0.00000	0.0000	0.00000	0.0000	2.33333
0.12 53	0.22284	2.0408	0.00000	0.3857	2.35774
0.2036	0.42652	2.1739	0.05187	0.6428	2.43217

0 0103	0 60144	2 3945	0.07841	0.8999	2.41297
0.2193	0.00111	2 6544	0 10736	1.0884	2.44418
0.3133	0.01054	2 9670	0 14475	1.2513	2.47059
0.3994	1 16033	3 0492	0 17973	1.4741	2.47539
0.4033	1 20749	3 2451	0 22919	1.6112	2.52101
0.5404	1 52034	3 5050	0 27503	1 7912	2.50420
0.6109	1.33034	3.3030	0 20207	2 1255	2 52341
0.6971	1.74920	3.7371	0.32207	2.1233	2 56422
0.7989	2.01518	3.9225	0.35826	2.0034	2.30423
0.8772	2.22604	4.0879	0.40531	2.9654	2.59344
1.0338	2.50399	4.2927	0.44632	3.3339	2.62905
1.1278	2.75799	4.4660	0.47889	3.7796	2.66747
1.1905	2.86821	4.6786	0.52111	4.2081	2.70108
1.2845	3.04313	4.8598	0.55971	4.6538	2.73469
1.3471	3.19649	5.0646	0.60193	5.1080	2.77311
1.4176	3.33546	5.2930	0.65259	5.5451	2.80672
1.5194	3.44808	5.5372	0.68758	5.8708	2.80432
1.6369	3.56070	5.7498	0.72376	6.1536	2.85234
1.7466	3.68770	5.9861	0.77684	6.7964	2.87635
1.7544	3.78115	6.1437	0.80217	7.0963	2.90996
1.8640	3.90815	6.4587	0.85163	7.7477	2.93878
1.9737	4.04473	6.6871	0.88902	8.1162	2.96038
2.0677	4.16933	6.9313	0.93245	8.4676	2.98920
2.1695	4.28195	7.1755	0.97346	8.8190	3.01080
2.2713	4.39217	7.3882	1.00241	9.3075	3.04202
2.4514	4.48802	7.6402	1.05308	9.7446	3.07803
2 5376	4.56230	7.8765	1.09168	10.3017	3.10684
2 6707	4.66294	8.1364	1.12786	10.6531	3.11405
2 7882	A 72045	8.4200	1.18456	11.0644	3.15006
2.7002	4 91150	8 6484	1.22316	11.3901	3.17167
3.0232	4 01214	8 9792	1 25694	11.6730	3.17167
3.2/30	4.04000	0.3732	1 29674	11 9643	3.14286
3.4401	4.94000	0 4012	1 33896	12 4272	3.09724
3.049/	4.93327	0 7511	1 37515	12 9242	3 06363
3.7751	4.95/6/	9.7311	1 41406	13 1095	3 03241
3.9004	5.00080	10.0098	1 45476	13 6442	2 07050
3.9944	4.97204	10.4049	1.434/0	14 0555	2.3/333
4.2841	4.96486	10.6884	1.489/3	14 2010	2.33337
4.6288	4.95767	10.9011	1.518/0	14.3012	2.00030
4.8324	4.95767	11.1218	1.55006	16 1611	2.33072
4.9499	4.93131	11.3343	1.56333	15.1011	2./3334
5.5060	4.91693	11.5469	1.39469	15.0134	2.73070
6.0542	4.92412	11.9408	1.62485	16.0207	2./2203
6.3910	4.92173	12.1377	1.64777	10.4290	2.0010/
6.6181	4.92412	12.3976	1.66827	10.9200	2.03800
6.8139	4.92412	12.7914	1.67310	17.4000	2.38383
6.923 6	4.96486	13.0356	1.66586	17.8180	2.53061
7.1977	4.96965	13.2561	1.63932	18.3151	2.48233
7.4013	4.96486	13.4452	1.62244	18.7350	2.433/6
7.5345	4.98163	13.6342	1.59952	19.0778	2.42257
7.7773	4.99361	13.8390	1.56815	19.5235	2.40810
8.3647	4.99361	14.0517	1.52232	19.7635	2.35//4
9.0852	4.99121	14.2643	1.47889	20.0463	2.34814
9.6335	4.98882	14.3904	1.43546	25.0000	2.33333
10.0642	4.99121	14.6030	1.39445		
10.1974	4.98882	14.8314	1.34741		
10.2209	5.01757	15.0284	1.29916		
10.6125	5.02955	15.2568	1.21834		
10.9101	5.03195	15.3592	1.18094		
11.1059	5.03195	15.4852	1.15682		
11.2625	5.05351	15.7294	1.09288		
11.3800	5.03435	15.8396	1.06755		
11.4583	5.00559	15.9578	1.03016		
11.5445	4.94329	16.1704	U. 97829		
11.5993	4.90016	16.4461	0.92521		
11.6306	4.83786	16.5879	0.89264		
11.677 6	4.76118	16.7454	0.85645		
11.8108	4.50240	16.8951	0.82027		
11.9753	4.27955	17.0920	0.77081		
12.1084	3.94888	17.3677	0.71291		
12.2024	3.70447	17.5567	0.67310		
12.3120	3.51757	17.7930	0.62485		
12.4608	3.20847	17.9820	0.56936		
12.5783	2.92812	18.1159	0.54403		
12.7898	2.56629	18.3365	0.49940		
12.9934	2.29553	18.5964	0.45356		
13.2754	1.93610	18.8563	0.41013		
13.5103	1.62460	18.9981	0.37636		
13.6591	1.44968	19.2265	0.33052		
13.8706	1.31070	19.3919	0.28468		
14.0038	1.20288	19.5810	0.24970		
14.1291	1.15016	19.8330	0.20265		
14.3014	1.04712	20.0063	0.16405		
14.4424	1.00160	20.2583	0.12425		
14.6382	0.94169	20.4789	0.0/961		
14.7713	0.92013	20.6364	0.03498		
15.1472	0.90815	20.9357	0.01086		
15.5858	0.89856	21.0539	0.01930		

15 0226	0 89856	21.3059	0.00965
16 1684	0 00335	21 6997	0.00965
10.1034	0.30333	22 0049	0 00483
10.4030	0.93211	22.0005	0.00400
16.9251	0.92492	22.6530	0.00000
17.2541	0.91773	25.0000	0.00000
17.9746	0.91294		
18.2566	0.90815		
18.6404	0.90335		
19.1338	0.89617		
19.5254	0.89617		
20.0580	0.88898		
20 2929	0 88419		
20.2929	0 00000		
20.4009	0.00000		
20.7707	0.00000		
21.1153	0.90096		
21.4051	0.00000		
21.6635	0.43610		
21.9455	0.00000		
22.0395	0.17252		
22.3058	0.23722		
22 6530	0.00000		
25 0000	0 00000		
23.0000	0.00000		

10	Hz,	808	Duty	Cycle				
Dec	:embe	ir 10), 199)1 , (time	in	milli-seconds)

Time	Source V	Time	Current	Time	Cell V
0 0000	0.00000	0.0000	0.00000	0.0000	2.09483
0.2079	0.67393	0.0414	0.07826	0.2484	2.76149
0.2910	1.87654	0.4549	0.85507	1.1592	2.80460
0.4157	3.29412	0.7857	1.21014	1.9044	2.83621
1.2887	3.40450	2.6466	1.01449	, 2.7738	2.89080
2.4528	3.33479	2,7707	1.13768	3.8916	2.82184
3.7415	3.41031	4.2594	0.92174	4.4298	2.8/009
5.0302	3.30283	5.9135	1.1521/	3.9010	2.0/931
6.4437	3.44808	0.99/9	1 07536	9 4392	2.82184
7.6077	3.31133	0 6353	0 91884	10.5984	2.88793
9.0447	3 37545	10 7105	1.01159	12.0474	2.79598
12 4301	3 49165	11.2068	1.14203	12.7512	2.80172
13 6357	3 32317	12.6128	0.86812	14.1174	2.93391
15.2154	3.50617	13.2744	0.93913	15.0282	2.79023
16.5873	3.30864	14.0188	1.05797	16.3116	2.92529
17.8760	3.43355	15.2594	0.77101	17.5950	2.78161
19.2479	3.27088	15.8383	0.90435	19.3752	2.95115
20.6198	3.43355	16.9135	1.04348	20.3688	2.81034
22.0748	3.27959	18.2368	0.78406	21.6522	2.94540
23.5299	3.52360	19.6842	1.11594	23.0184	2.81034
24.7354	3.27959	20.9002	1 10970	25 9164	2.81034
26.2736	3.52360	22.3/09	0 82029	26.8686	2.89368
21.3024	3.51/30	24 1090	0.98261	27.9451	2.88218
29.2232	3 32317	24.9774	0.97826	28.5247	2.79598
31 8443	3.52070	25.2669	1.08841	29.4355	2.79310
33.2577	3.31155	26.4662	0.85942	30.3463	2.89080
34.5049	3.45389	27.2519	0.97101	31.4227	2.82184
36.0015	3.23312	27.9962	1.10870	32.1265	2.80172
37.2902	3.46550	29.3609	0.79420	33.0787	2.93966
38.5374	3.28540	29.6090	0.92029	34.2793	2.79310
39.7846	3.45970	30.1053	0.92029	35.2729	2.86494
41.1980	3.23602	30.7669	1.05652	36.1009	2.95402
42.9856	3.51489	32.2143	0.73333	37.0943	2.029/1
44.3575	3.35512	32.7519	0.90433	30.0/4/	2 91667
45.9788	3.49746	33.2401	1 06097	30 9511	2 84770
40.8934	3.3/030	33.4345	0 75362	41.2759	2.93678
48.3464 50 2609	3 31445	35 3985	0.90870	43.0147	2.82184
51 5079	3.45098	35.5639	0.93043	43.8013	2.89943
52.5057	3.29702	36.3083	1.09565	45.4159	2.78161
54.3764	3.46841	37.6316	0.74203	46.6579	2.83908
55.2494	3.30574	37.9211	0.92464	47.1961	2.96264
56.9123	3.51198	38.2932	0.95072	48.2725	2.79023
58.3673	3.32898	39.0789	1.12899	48.9349	2.79310
59.0741	3.35222	40.4850	0.80145	49./029 E1 0040	2.3100/
59.7808	3.52360	40.0504	0.97681	51 5431	2.87069
60.8201	3.33222	42 0150	1.09130	52.0813	2.87356
62 7740	3 44517	43.3383	0.85362	52.7437	2.94828
63.7302	3.35222	44.5789	1.08841	53.8201	2.81897
65.1436	3.52651	46.0263	0.79855	54.5653	2.88218
66.5986	3.34060	46.3985	0.92174	55.7245	2.92816
68.0121	3.43646	46.8947	0.92609	56.5939	2.86494
69.3840	3.27669	47.4323	1.03623	57.9187	2.93678
69.79 97	3.38417	48.8797	0.77971	59.3677	2.80747

70.6727	3.38126	50.5338	1.05797	59.9473	2.87069
71 1716	3.44808	51.6504	0.81594	60.8167	2.90230
72 0446	3.28540	52.9323	1.09130	62.3071	2.80460
73 3749	3.46841	54.3383	0.81594	63.6733	2.93678
74 7469	3 29993	55.8271	1.12029	64.8325	2.74138
76 5760	3 50617	56.9850	0.88696	65.5777	2.79885
77 6569	3 33479	57.5226	0.98696	66.4471	2.92529
70 1110	3 52941	58.1429	0.98986	67.4407	2.80172
00 1027	3 36383	58.6391	1.08841	69.1381	2.94540
01 0EEE	3 53522	59.5902	0.90145	70.0489	2.89080
03 0612	3 31736	61.0789	1.11449	71.4151	2.88218
04 5004	3 44227	62.7744	0.87681	72.2017	2.95115
96 1276	3 25054	64.0150	1.03333	73.4437	2.83621
97 5094	3 44517	65.0902	0.80725	74.6443	2.92241
99 9645	3.27378	66.6617	1.03478	76.3831	2.82759
00.1285	3 46841	67.8609	0.79130	77.4181	2.89368
91 4172	3.32607	69.5150	1.10580	78.4117	2.79023
91 6251	2.05374	70.8797	0.80000	79.9435	2.80460
91 8367	0.00000	72.2857	1.11884	80.2747	2.90517
110.0000	0.00000	73.5677	0.85942	81.5582	2.76149
	•••••	75.0977	1.08986	83.0486	2.93103
		76.1729	0.87536	83.7523	2.81322
		77.9098	1.13043	84.8288	2.81034
		79.1090	0.82754	85.8638	2.96552
		80.5977	1.05217	87.2714	2.01897
		81,8383	0.74348	87.7268	2.87931
		83.4925	1.05942	89.0102	2.93391
		84.6917	0.73623	89.7554	2.85920
		86.3045	1.09420	90.7076	2.90230
		87.4211	0.74493	91.1630	2.91954
		87.9586	0.92899	91.4528	2.36782
		88.4962	0.95652	92.6948	2.30172
		89.3233	1.13478	94.4336	2.23851
		90.3571	0.79420	96.2138	2.19828
		91.1842	0.98551	98.1596	2.19540
		91.8367	0.00000	100.5608	2.15230
		110.0000	0.00000	102.7964	2.13218
				105.2390	2.11494
				106.5224	2.12069
				110 0000	2 09483

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500 Hz,	808	Duty	Cyc	1				
November	12,	, 1991	,	(time	in	micro-seconds)

Time	Source V	Time	Current	Time	Cell V
0 0000	0.00000	0.0000	0.00000	0.0000	2.16667
A 1173	1.97353	16.4779	0.00148	2.0534	2.24638
3.0880	2.45000	17.5077	0.28994	3.0801	2.39130
2 0587	2.85882	21.6272	0.37574	10.2669	2.46667
A 1173	3.02059	24.7168	0.47633	15.4004	2.54493
5 1467	3 10000	27.8064	0.52515	21.5606	2.63478
14 4107	3.17647	28.8363	0.57249	35.9343	2.72754
25 7334	3 22941	35.0154	0.63757	56.4682	2.81159
40 1799	3 27353	38,1050	0.69970	75.9754	2.83768
65 9775	3 29412	43.2544	0.76036	105.7495	2.85797
03.6696	3 31471	49.4336	0.80473	143.7372	2.87536
124 9430	3 32941	59.7322	0.85799	166.3244	2.88406
173 0579	3 33529	70.0309	0.90976	200.2053	2.88986
200 0552	3 30882	80 3296	0.94379	233.0596	2.88986
208.9332	3 32941	115.3450	0.95414	284.3943	2.89855
234.0000	3 33529	155.5098	0.96154	339.8357	2.90145
320 1235	3 33529	193.6148	0.95414	388.0904	2.91594
370 5610	3 34706	225.5407	0.95562	416.8378	2.91594
427 1745	3.33824	268.7950	0.95266	462.0123	2.91884
490.9933	3.34118	325.4377	0.95118	495.8932	2.92174
528.0494	3.34118	382.0803	0.95414	524.6407	2.91015
578.4869	3.33235	438.7230	0.95414	588.2957	2.91884
625.8364	3.33529	490.2163	0.94527	625.2567	2.92754
685.5378	3.32059	541.7096	0.94231	652.9774	2.91304
733.9166	3.32059	578.7847	0.94527	716.6324	2.92464
826.5569	3.31471	634.3975	0.94083	758.7269	2.91594
878.0237	3.31471	688.9804	0.93787	790.5544	2.91594
928.4611	3.32941	750.7724	0.93935	802.8748	2.90725
995.3680	3.32941	829.0422	0.93935	866.5298	2.91015
1044.7761	3.32647	898.0433	0.93639	914.7844	2.91015
1088.0082	3.33824	974.2534	0.94379	976.3860	2.90435
1143.5924	3.34412	1022.6570	0.94379	1044.1478	2.91015
1182.7072	3.34118	1098.8672	0.94083	1121.1499	2.91594
1230.0566	3.34118	1165.8085	0.94231	1191.9918	2.90725
1300.0515	3.34706	1228.6302	0.94379	1253.5934	2.90435
1352.5476	3.34412	1289.3923	0.94379	1317.2484	2.90725
1400.9264	3.34412	1377.9608	0.94231	1362.4230	2.91015
1449.3052	3.34412	1425.3347	0.94231	1411.7043	2.91594
1488.4199	3.35000	1487.1267	0.95118	1477.4127	2.91594
1529.5934	3.34412	1541.7096	0.95118	1516.4271	2.91304
1564 8000	3 33924	1578 7848	0.95710	1549.2814	2.91015
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1504.3304	3 34412	1607 6210	0 95266	1574 9486	2.90435
1369.2999	3.34412	1619 0406	0.90690	1589 2957	2.90435
TODO' 1330	3.34412	1617 0107	0.96539	1503 4202	2.89855
1608.8523	3.12333	1017.9197	0.00000	1607 6360	2 91159
1609.8816	2.84706	1617.9197	0./810/	1000 6160	2.01100
1612.9696	2.50588	1617.9197	0.67751	1000.0100	2.73043
1612.9696	2.00294	1618.9496	0.57840	1601.642/	2.0000/
1616.0576	1.74412	1615.8600	0.43491	1602.6694	2.59130
1613.9990	1.37647	1621.0093	0.32692	1603.6960	2.47826
1618.1163	0.71176	1626.1586	0.24408	1607.8029	2.42609
1620.1749	0.16765	1623.0690	0.17604	1618.0698	2.39420
1621.2043	0.07059	1621.0093	0.11095	1629.3634	2.36522
1632.5270	0.03529	1621.0093	0.06953	1647.8440	2.34203
1639.7324	0.02647	1621.0093	0.02219	1664.2710	2.33333
1657.2311	0.00882	1625.1288	0.00444	1685.8317	2.33043
1673.4694	0.00000	1643.6664	0.00000	1701.2321	2.31594
2000.0000	0.00000	2000.0000	0.00000	1715.6057	2.29565
				1744.3531	2.29565
				1776.1807	2.28406
				1798.7679	2.27826
				1833.6755	2.26667
				1861.3964	2.25797
				1872.6899	2.25217
				1905.5442	2.24058
				1929.1581	2.22899
				1939.4250	2.22899
				1956.8789	2.23768
				1967.1458	2.23188
				2000.0000	2.16667

¹ kHz, 80% Duty Cycle November 12, 1991 , (time in micro-seconds)

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Time	Source V	Time	Current	Time	Cell V
0 0000	0.00000	0.0000	0.00000	0.0000	2.30747
0 4117	0.79066	2.8866	0.00000	0.4122	2.38021
0 8234	1.19912	5.7732	0.01744	2.0610	2.41513
1 6468	1.62801	7.0103	0.03343	4.9464	2.46460
2 0585	2.39825	9.0722	0.17151	7.4196	2.49370
2 8818	2.72794	11.5464	0.27180	8.6562	2.54898
4 1169	3.00219	12.3711	0.34157	11.5416	2.58390
5 3520	3.18308	13.6082	0.39244	16.0758	2.63919
11,9391	3.20642	16.0825	0.44622	18.9613	2.68865
18.9378	3.24143	17.3196	0.49855	22.6711	2.71775
28.4068	3.24726	19.7938	0.54942	27.6175	2.73521
38.6991	3.31437	22.6804	0.60320	37.5103	2.76140
53.5200	3.31729	28.8660	0.67733	45.3421	2.78758
72.0461	3.32312	31.3402	0.72238	52.7617	2.80795
86.4553	3.32604	34.6392	0.76453	59.7692	2.82250
92.6307	3.34938	39.1753	0.80378	70.0742	2.85160
96.3359	3.34063	43.2990	0.82994	72.5474	2.86033
102.5113	3.35813	48.6598	0.86337	84.9134	2.87779
107.8633	3.33479	56.4948	0.91279	96.4551	2.88943
115.6855	3.36105	65.1546	0.94477	107.9967	2.89816
120.6258	3.33771	75.8763	0.97093	121.5993	2.89816
125.9778	3.35230	84.1237	0.98256	131.0800	2.90689
131.7415	3.34938	106.3918	0.98983	140.9728	2.92144
139.5636	3.32604	120.8247	1.00145	151.2778	2.92144
145.7390	3.36397	143.5052	1.00872	171.0635	2.92435
159.7365	3.36105	168.2474	1.00872	178.0709	2.91853
164.6768	3.32604	190.9278	1.00581	191.6735	2.91562
177.4393	3.32604	221.4433	1.00436	206.5128	2.92144
184.8497	3.36105	238.7629	1.00145	232.8936	2.92144
191.0251	3.35522	273.8144	1.00000	244.8475	2.91853
196.3771	3.33187	294.4330	0.99855	255.9769	2.91853
206.2577	3.36689	327.8351	0.99855	268.7552	2.91853
210.7863	3.33771	352.9897	0.99855	284.8310	2.92435
214.0799	3.34938	383.5052	0.99855	301.7312	2.92726
229.3125	3.35230	416.0825	0.99855	312.8607	2.92726
249.4854	3.35813	435.0515	0.99855	327.6999	2.92726
271.7168	3.35230	464.7423	0.99855	341.7148	2.92726
286.9494	3.35522	489.4845	1.00291	353.2564	2.93307
298.8884	3.34938	504.3299	1.02035	373.0421	2.93307
317.4146	3.35230	531.1340	1.01017	383.3471	2.93016
331.4121	3.35522	558.7629	1.01308	390.3545	2.93016
348.2915	3.35813	596.7010	1.01453	407.6669	2.93016
375.8748	3.35522	620.2062	1.02035	418.7964	2.93016
397.6945	3.35230	658.1443	1.01890	429.1014	2.93016
415.3973	3.34646	691.1340	1.02035	449.2993	2.93307
442.1573	3.34646	710.9279	1.01744	463.3141	2.93307
465.2120	3.34646	731.5464	1.02180	482.6876	2.93016
487.4434	3.35230	764.9484	1.02471	500.8244	2.93016
512.9683	3.34063	781.0309	1.02180	512.7783	2.92726
536.0231	3.34063	792.1650	1.01744	526.3809	2.92144

549.1972	3.34354	804.1237	1.00000	550.2885	2.93016
576 3689	3.33187	809.0721	0.99128	560.5936	2.92726
502 9365	3 33479	810 3093	0.94477	577.9060	2.92726
620 R316	3 32604	811 1340	0 87645	602 6381	2.92726
620.0310	2 21720	010 3710	0 55669	614 5919	2.92144
030.3400	3.31/49	014 4320	0.35669	620 0100	2 92144
058.2950	3.32890	014.4330	0.43640	640 0729	2.96114
677.2335	3.32604	813.8/01	0.319/7	640.3726	2.32433
691.6426	3.32604	817.7319	0.1104/	653.7510	2.74199
708.9337	3.33479	819.3813	0.03924	667.3337	2.91033
722.5195	3.32896	820.2082	0.00000	676.8343	2.91302
731.1651	3.35813	1000.0000	0.00000	686.3149	2.93307
735.6937	3.34646			695.7955	2.90980
744.3392	3.35813			708.9860	2.90980
751.3380	3.33187			735.3669	2.90980
758.7485	3.32896			746.9085	2.91271
764.5121	3.34354			771.2283	2.91271
768.2173	3.35230			784.4188	2.91853
779.3331	3.35813			795.9604	2.90689
790.4487	3.35813			798.8458	2.90689
799.9177	3.35230			801.7313	2.90398
804.4463	3.34938			802.5557	2.83705
806.5048	3.33187			803.7922	2.77886
806.9164	3.19767			804.6166	2.70029
807.7398	3.08972			805.8533	2.61591
808.9749	2.25821			80 6.6777	2.55771
810.6216	1.79723			807.08 98	2.48788
811.0333	1.61050			809.5630	2.44132
811.8568	1.40919			819.0437	2.41513
812.2684	1.30124			823.1657	2.41222
813.9152	0.85485			828.9365	2.38894
815.1503	0.65062			833.4708	2.37730
817.6204	0.47265			841.7148	2.36857
816.7971	0.33260			849.9588	2.35694
816.3853	0.17797			859.4394	2.35694
817.6204	0.06127			867.6834	2.35112
819.2672	0.00292	-		877.9885	2.35112
826.6777	0.00000			893.2399	2.35112
1000.0000	0.00000			905.1937	2.33948
				920.4452	2.32784
				932.3990	2.32493
				946.4139	2.32493
				957.1311	2.31620
				962.4897	2.31620
				968.6727	2.30747
				1000.0000	2.30747

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⁵ kHz, 80% Duty Cycle November 12, 1991, (time in micro-seconds)

Time	Source V	Time	Current	Time	Cell V
0.0000	0.00000	0.0000	0.00000	0.0000	2.22222
0.4124	0.05535	3.4038	0.00000	1.0315	2.30858
0.7216	0.29716	4.3321	0.01017	1.9598	2.33173
0.9278	0.57684	5.2604	0.02471	3.3007	2.35776
1.4433	0.89731	5.6730	0.04360	5.1573	2.38669
1.3402	1.07793	5.7762	0.06250	6.6013	2.40984
1.6495	1.27021	6.1888	0.11919	8.1485	2.44455
1.7526	1.52367	6.6013	0.15843	9.9020	2.47927
1.9588	2.15586	7.2202	0.18750	11.2429	2.50241
2.3711	2.33066	8.2517	0.22674	12.7901	2.52845
2 4742	2.53460	9.2831	0.26017	14.7499	2.56027
2 5773	2.73270	10.6240	0.29651	15.7813	2.57473
2 8866	2 79971	12.0681	0.35320	17.5348	2.60077
3 2990	2 92498	12.9964	0.38953	20.7323	2.63838
3 5052	3 05900	14.0278	0.42733	23.1047	2.65574
4 4330	3 16096	15.5750	0.46948	26.1991	2.68177
4 6392	3 20757	16.6065	0.50291	27.3337	2.68756
6 7010	3 22505	18 4631	0.54506	30.1186	2.70781
8 4536	3.25127	19.8040	0.58285	32.1815	2.71938
10 6186	3 25127	20.6292	0.59593	34.8633	2.73385
12 2680	3.27749	21.9701	0.59302	38.0609	2.73385
13.5052	3.25710	23.0015	0.63808	41.9804	2.74542
14 5361	3.28915	24.0330	0.67006	43.2182	2.75410
15 7732	3.26001	25.5802	0.69477	45.5905	2.78303
17.0103	3.28332	27.4368	0.71512	46.6220	2.78592
18.0412	3.25710	29.8092	0.74564	48.2723	2.78592
19.4845	3.28332	31.4595	0.76308	50.1289	2.78303
21.5464	3.28332	33.8319	0.78343	52.9139	2.78592
22.4742	3.26001	36.3074	0.81686	55.6988	2.78303
23.0928	3.30371	38.3703	0.83721	57.9680	2.79460
24.8454	3.27167	40.9489	0.86192	61.6813	2.80617
27.1134	3.30954	42.9087	0.88372	64.6725	2.81196
30.1031	3.32411	45.7968	0.90552	67.1480	2.81485
34.8454	3.32993	48.9943	0.93023	70.0361	2.81196

30 0722	3 32411	53 0170	0 94767	73.4399	2.81774
A0 4742	3 33709		0 05404	76 6374	2 81774
42.4/44	3.32702	33.0300	0.93494	70.03/4	2 92064
45.4039	3.32/02	30.6900	0.90037		2.02004
47.1134	3.36489	62.0939	0.97965	80.7633	2.82064
49.0722	3.36198	65.0851	0.98983	82.5168	2.83799
51.7526	3.36198	68.4889	1.00291	84.7860	2.83799
54.7423	3.36489	70.5518	1.01599	87.2615	2.83510
58 0412	3.36489	73.1305	1.01890	90.1496	2.83799
62 2000	3 37655	77 4626	1 02762	92 3156	2 83510
03.2990	2 27655	90 4529	1 03062	03 5534	2 94099
00.1830	3.3/033	00.4330	1.03032	93.3334 06 8446	2.04005
73.4021	3.3/0/2	83.2388	1.03343	Y0.3440	2.8493/
78.6598	3.36781	86.6426	1.03488	98.1949	2.85824
84.0206	3.36781	89.8401	1.04360	100.4642	2.86114
89.6907	3.37072	93.3471	1.04360	102.7334	2.85824
97.1134	3.37655	95.8226	1.04797	104.4868	2.85824
101 9588	3.37946	98.0918	1.05523	107.5812	2.85824
105 0515	3 37363	101 4956	1.06105	111,7071	2.86403
100.7600	3 36109	106 4466	1 06250	113 0480	2 86692
108.7629	3.30130	100.4400	1.00230	115.0460	2.00032
113.9175	3.3/655	110.8819	1.03939	115.4203	2.6/2/1
117.5258	3.38237	114.0794	1.06250	117.9990	2.88139
121.7526	3.38237	118.9273	1.06105	119.4430	2.88139
123.5052	3.38237	122.8468	1.06105	122.7437	2.89007
126.7010	3.39111	126.4569	1.06250	125.1160	2.87850
131.0309	3.39403	135.1212	1.07122	129.1387	2.87560
134.3299	3.39694	139.1439	1.06831	132.1300	2.88428
138 0412	3, 39111	142.5477	1.07267	136.9778	2.88139
140 7216	3 30111	146 2610	1.07413	142.8571	2.88139
144 0454	3 30530	140 2207	1 07413	146 5704	2 88139
144.0434	3.30323	153 6560	1.07004	160 1905	2 99139
149.2/84	3.38329	152.6360		150.1603	2.00139
150.0000	3.40859	157.0913	1.07703	153.0686	2.88139
153.8144	3.39403	160.1857	1.07267	155.2346	2.88428
157.2165	3.39403	162.1454	1.06977	156.7818	2.88717
159.7938	3.37363	162.8675	1.04215	158.3290	2.88428
161.0309	3.36489	163.3832	1.01599	159.2574	2.86982
161.2371	3.21049	164.3115	0.89680	160.0825	2.85535
161.7526	2.65987	164-4146	0.83866	160.4951	2.84089
162.2680	2.29862	165.0335	0.77326	161.0108	2.80617
163.0928	2.11508	165.3430	0.69622	161.5266	2.78013
163.4021	1.53532	165.8587	0.60610	162.2486	2.71360
163.8144	1.45666	166.4776	0.52616	162.8675	2.65863
164 4330	1 26730	167 3027	0 42297	163 3832	2.56895
164 6303	1 16242	169 0247	0 32559	163 8989	2 52266
104.0392	1.10444	160.0247	0.15407	164 E170	2 47059
103.4039	T.01301	100.2310	0.1340/	168.31/8	2.3/039
166.7010	0.95557	108./408	0.09393	103.2398	2.92/19
167.6289	0.88857	108.8499	0.04797	103.8387	2.38380
168.1443	0.80699	169.3877	0.00000	166.1681	2.34619
168.2474	0.70211	200.0000	0.00000	167.0964	2.35198
168.5567	0.57684			168.0247	2.36066
168.8660	0.00000			169.9845	2.35487
169.3814	0.28551			174.5229	2.34040
169.6907	0.00000			177.2047	2.34040
170.2062	0.27677			180.9180	2.33462
171 6495	0.00000			188.8602	2.32305
200 0000	0 00000			191.3357	2.32594
200.0000	0.00000			193 9144	2 33173
				106 8060	2.JJ4/J
				100 2245	2.32013
				128.2260	2.31726
				200.0000	2.22222

Time	Source V	Time	Current	Time	Call V
0.0000	0.00000	0.0000	0.00000	0.0000	2.29878
0.4479	0.17567	2.6884	0.00431	0.0822	2.29878
0.5700	0.56443	3.2994	0.02157	0.7401	2.27019
0.8143	0.83225	4.3177	0.09490	1.3980	2.25590
0.9772	1.26710	6.0285	0.18692	1.8914	2.24732
1.5879	1.74802	8.0244	0.28181	2.7549	2.27591
1.7508	1.98704	9.2057	0.33214	3.7007	2.31022
1.8730	2.20590	10.1833	0.37815	5.1398	2.35597
2.1580	2.50540	11.4460	0.41984	5.9622	2.37312
2.4837	2.73002	12.3829	0.45291	7.7303	2.39600
2.7687	2.90281	13.6864	0.49461	9.0872	2.42173
3.0007	3.02952	15.1120	0.53630	10.8964	2.44460
3.0537	3.08423	16.0489	0.56794	12.6234	2.47891
3.2573	3.13031	17.9226	0.62401	14.1036	2.49321
3.5016	3.16775	19.1853	0.65852	15.1727	2.51894
3.8274	3.23686	20.9369	0.70597	16.6941	2.53896
4.0309	3.27718	21.9145	0.72897	17.3931	2.58184
6.7997	3.30886	23.2994	0.75485	18.9145	2.59328
11.0749	3.29734	25.1324	0.79655	20.8470	2.59042
12.0114	3.32613	25.9878	0.81668	21.1349	2.61901
12.9886	3.31461	27.0876	0.83537	23.5197	2.63903

13 8436	3 33180	29.2872	0 86269	24.7122	2.65046
16 9789	3. 36069	30.9572	0.90007	25.9869	2.65332
21 4984	3 38949	33 6049	0 92308	28 4951	2.67048
26.9951	3.39813	35.5601	0.95471	30.5510	2.68763
32 4511	3 38661	37 3523	0 97915	32 6891	2.70765
34 8127	3 38949	39 3493	0 99353	34 9095	2.72480
35 3013	3 43269	A1 0145	1 00503	35 6497	2 73624
36 4414	3 40389	45 2139	1 02948	36 5132	2 74768
30 1207	3 41929	47 1797	1 04917	37 3355	2 77627
43 9925	3 42117	50 1833	1 05536	39 7336	2 72766
45.6925	3 42603	52 0163	1 07836	30 6392	2.72700
50 8143	3 43557	54 2974	1 08986	40 0493	2 77341
52 1580	3 47012	56.7006	1,10568	42.2697	2 74196
56.1075	3.47012	58.6965	1.11431	43.0921	2.75911
56.9218	3.43844	61.2627	1.12437	44.6546	2.75911
59.4870	3.44708	63.1365	1.13156	45.2714	2.78485
64.9023	3.46436	66.7617	1.14450	45.8470	2.75340
71.5798	3.45860	69.4094	1.15744	47.1217	2.75911
75.5293	3.45860	72.6680	1.16319	47.9852	2.80772
77.2801	3.45284	75.3564	1.16319	48.9720	2.74196
78.9088	3.46148	77.5967	1.17613	49.8355	2.81344
79.7638	3.25990	78.5743	1.18045	50.6579	2.75625
80.1303	2.89129	79.9185	1.18045	51.4803	2.83059
80.2524	2.42765	81.4257	1.05679	52.3849	2.75340
80.6189	2.03600	82.4033	0.89144	52.9194	2.79914
80.9853	1.58675	83.6253	0.60963	54.2763	2.79914
81.5961	1.17207	84.5214	0.41409	55.3454	2.80200
82.1661	1.02232	85.9878	0.17254	55.7566	2.80486
82.8990	0.93017	86.8024	0.00575	56.0855	2.76483
83.7541	0.91289	97.2709	0.00431	56.6612	2.81630
85.1792	0.88409	99.0224	0.00000	57.6480	2.81630
85.5049	0.83801	100.0000	0.00000	59.3750	2.83345
86.4414	0.84665			61.5543	2.85633
87.2150	0.00000			63.2813	2.85347
87.9072	0.52412			65.9128	2.84775
88.8844	0.00000			69.3668	2.83631
89.4137	0.04320			71.4227	2.84775
93.3225	0.01728			74.5988	2.84489
94.0147	0.03168			76.9737	2.83917
100.0000	0.00000			78.2072	2.85061
				79.8931	2.85919
				81.3734	2.78485
				82.8330	2.0/334
				84 9507	2.33010
				84.9307	2.99/90
				00.2004 07 5411	2.3/398
				88 0757	2 35311
				88 6102	2 27019
				89.1036	2.33024
				90.5016	2.24446
				92.5164	2.24446
				94.3257	2.25876
				96.1760	2.25876
				97.1217	2.26162
				99.1776	2.25874
				100.0000	2.29879
25 kHz, 80%	Duty Cycle				

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11100	Source V	TLINE	Current	TLINE	Cell V
0.0000	0.00000	0.0000	0.00000	0.0000	2.36812
0.0824	0.19144	2.6531	0.00000	0.0830	2.36812
0.1030	0.53372	2.9102	0.05630	0.5189	2.31884
0.1442	1.22988	3.2405	0.08518	1.1002	2.26957
0.2884	1.51704	3.9216	0.14148	1.2247	2.34203
0.4531	1.68528	4.5408	0.18912	1.8267	2.33623
0.5561	1.90573	5.2219	0.24398	2.6155	2.35942
0.6591	2.11168	5.9236	0.29740	3.5911	2.37391
0.7415	2.20160	6.4396	0.33782	4.5874	2.42319
0.8651	2.26541	7.1207	0.39269	5.6046	2.43768
0.9887	2.45975	8.0908	0.45476	6.7878	2.46957
1.0917	2.59608	8.6068	0.49086	8.0125	2.51884
1.3182	2.68600	9.2466	0.53850	9.2164	2.58261
1.4418	2.82814	9.8658	0.57170	9.9637	2.60870
1.5860	3.00798	10.4644	0.59769	11.0016	2.63188
1.6684	3.14141	11.1249	0.65111	11.9564	2.67246
1.7920	3.18492	11.7028	0.68431	13.6793	2.7072
2.0185	3.28644	12.7967	0.73773	15.7343	2.72174
2.3893	3.46918	13.4778	0.77093	17.7478	2.73913
2.6159	3.47788	14.1796	0.80703	19.4084	2.79130
2.8424	3.54170	14.8194	0.83446	21.7955	2.83188
3.1308	3.59971	15.4180	0.84745	24.1412	2.86957

3.3574	3.62292	15.6450	0.87777	26.4868	2.90435
4 0271	3 62972	16 2023	0 89076	29 0400	2.91884
4.0371	3.04074	16 6367	0.02307	31 1790	2 94493
4.4902	3.03//2	10.0337	0.92397	31.1/60	2.94493
5.0051	3.00002	17.4407	0.942/3	32.9210	2.93942
5.5407	3.66062	18.0392	0.96728	33.7312	2.96522
6.0144	3.69833	18.8029	0.99615	34.6445	2.87536
7.2297	3.69253	19.8142	1.02791	35,5786	2.77971
7 9064	3 65192	20.3096	1.03946	36.8033	2.64928
0.0560	2 66642	21 1071	1 06933	38 0903	2 53043
8.8308	3.00042	21.13/1	1.00033	30.0903	2.33043
9.9485	3.67223	21.9008	1.0/844	39.0244	2.99390
10.7930	3.72444	22.4355	1.08277	40.0000	2.36812
11.5757	3.72154	22.8070	1.12031		
12.5438	3.72734	23.3024	1.12031		
13.7384	3.73314	23.5088	1.13908		
14 4799	3 74184	23.9422	1.14196		
18 4490	3 77666	24 3550	1 16506		
13.4400	3.77003	24.3330	1 16506		
10.0039	3.7/003	24.0040	1.10300		
17.0546	3.77955	24.9123	1.18239		
18.4552	3.78535	25.2219	1.18961		
19.5675	3.78535	26.1919	1.20404		
20.8033	3.78535	27.6161	1.23003		
21 5654	3 90956	28 5862	1 23725		
21.3034	3.00030	20.1022	1 27011		
22.2245	3.802/6	29.1022	1.2/911		
22.6365	3.77955	29.9071	1.29933		
23.5839	3.78245	30.4850	1.30221		
24.5520	3.80276	31.0836	1.32243		
25.1699	3.80276	31.8266	1.32387		
26.0556	3.80566	32.7348	1.32387		
27 1679	3.80566	33.1476	1.31232		
20 6718	3 91726	33 3540	1 28633		
20.0713	3.01726	33 5604	1 24447		
29.5//8	3.81/20	33.3004	1.10690		
30.6076	3.81146	33.8900	1.19082		
31.1226	3.81146	34.1176	1.14774		
31.4727	3.78535	34.8194	1.03802		
31.5963	3.71574	35.2735	0.93840		
31.7405	3.61131	3 5.6 244	0.86333		
31.9258	3.39086	36.2229	0.75072		
32 0906	3 16171	36.7802	0.63956		
22.0000	2 03036	37 1703	0 57170		
32.33/0	2.93030	37.1/23	0.37270		
32.5232	2.10/22	37.3439	0.493/4		
32.6056	2.61639	37.8947	0.42012		
32.9145	2.25671	38.2250	0.36670		
33.0793	2.10877	38.6997	0.28730		
33.3059	1.91153	39.1331	0.21655		
33.5118	1.75780	39.4840	0.15014		
33 6766	1 63307	39,8968	0.09528		
33.0700	1 44743	40 0000	0 00000		
33.3444	1 26170	40.0000	0.00000		
34.1/10	1.35170				
34.4593	1.22988				
34.6035	1.18347				
35.0154	1.07324				
35.262 6	1.03263				
35.8805	0.99492				
36.7250	0.99492				
37.3841	0.98622				
37 8373	0.97172				
20 2110	0 96303				
39.3110	0.90304				
38.9083	0.93431				
39.2997	0.94851				
39.6704	0.94851				
39.9588	0.50761				
40.0000	0.00000				
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