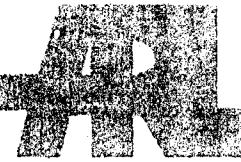


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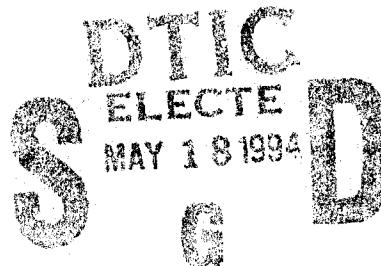


**Electrothermal-Chemical Modeling
Workshop, 12-13 May 1993—
Volume I**

Gloria P. Wren
William F. Oberle
CONTRIBUTING EDITORS

ARL-SR-10

May 1994



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INTRODUCTION

An Electrothermal-Chemical (ETC) Gun Modeling Workshop was held at the Weapons Technology Directorate (WTD), U.S. Army Research Laboratory (ARL)(formerly the Ballistic Research Laboratory (BRL)) on 12-13 May 1993. The workshop was specifically focused on technical aspects of ETC gun modeling and was sponsored by the WTD/ARL. Thus, the meeting was not as broad in scope as an earlier meeting held at BRL under the sponsorship of the JANNAF Combustion Subcommittee on 9-11 July 1991.

The objectives of the workshop were to: (a) assess the current state of ETC modeling; (b) determine the class of problems currently being addressed by various organizations; (c) encourage exchange of ideas and modeling techniques among participants; and (d) provide recommendations for future work, particularly in view of declining research funds.

The following compilation contains: (1) the meeting agenda; (2) a list of current known U.S. ETC modeling activities; (3) diagnostics measurements desired by ETC modelers as summarized by the group; (4) presentations by organizations attending the workshop; and (5) a list of participants. The workshop benefitted greatly from the participation of university, industry, and government (Army, DNA, Navy) personnel and contractors who all worked toward the common goal of understanding ETC processes through modeling.

We would like to thank Ms. Sharon Richardson for her excellent administering of the workshop; each participant for their active roles during the workshop; each author and funding agency for allowing work to be reprinted in this compilation (note that there are unclassified/unlimited and unclassified/government & contractors only sections)—and Army, DNA and Navy personnel in many different agencies for their cooperation and support in this endeavor. The modeling community has made significant advances in understanding ETC gun interior ballistics over the past several years and continues to impact gun cartridge design. It is hoped that this compilation will convey the development of state-of-the-art models for ETC guns.

Gloria Wren
Bill Oberle
Weapons Technology Directorate
Army Research Laboratory

Electrothermal-Chemical (ETC) Gun Modeling Workshop AGENDA
Weapons Technology Directorate, U.S. Army Research Laboratory

Wednesday, May 12, 1993

- 8:15 Administrative Remarks
Sharon Richardson
- 8:30 Science Applications International Corporation, San Diego, CA
C.-C. Hsiao, Fred Su
- 9:30 General Dynamics Land System/GT-Devices
Niels Winsor
- 10:30 Break
- 10:45 Science Applications International Corporation, Ft. Washington, PA
Sandy Dash
- 11:45 Lunch
- 1:00 Sandia National Laboratories, Albuquerque, NM
Steve Kempka
- 2:00 FMC Corporation, Minneapolis, MN
Patrick Janke
- 3:00 Break
- 3:15 U.S. Army Armament Research, Development, and Engineering Center
Lee Harris
- 4:15 Pennsylvania State University
F. Cheung
- 5:00 Adjourn
- 7:00 No-host dinner at Tidewater Grille, Havre de Grace

Thursday, May 13

- 8:30 U.S. Army Research Laboratory
Gloria Wren
- 9:00 Olin Corporation
Hugh McElroy
- 10:00 California Research and Technology
Phil Hookham
- 11:00 Group discussion and wrap-up
- 12:00 Adjourn

Current ETC Modeling Activities in the U.S. (May 1993)

Organization	Program Funding	Current Activities
1. ARDEC	Army	1. 0D*
2. ARL	Army	2. 1D Plasma, 0D, End - to - end (Power Plasma, IB)
3. Eli Freedman & Associate	Army	3. Thermochemistry (BLAKE - ETC)
4. FMC	IR & D, Services	4. 0D*,1D,2D (Finite Difference),End-to-end,Inverse Ballistic Model
5. GDLS	IR & D , Services	5. 0D*, 1D*, 2D (Finite Element)
6. LLNL	DNA	6. 2D/3D, AMR code
7. NC State University	Army, IR & D	7. 1D Plasma
8. Olin Corporation	IR & D	8. 0D*,1D*,1 1/2 D*
9. Paul Gough Associates	Army	9. 0D, 1D
10. Penn State University	IR & D, Army	10. 2D (2 phase, multiple sites, detailed droplet shedding)
11. SAIC, Atlanta	Army, DNA	11. 1D Plasma, 0D*, End - to - end
12. SAIC, Ft. Washington	Army	12. 2D/3D (Upwind/Implicit)
13. SAIC, San Diego	DNA	13. 0D*, 2D (FCT), 3D potential
14. S-Cubed, Maxwell Labs	DNA	14. 0D/1D
15. Sandia National Labs	Army, DoD/DOE MOU	15. 2D Plasma
16. CRT	DNA	16. 2D (TVD-Adaptive Grid), 3D potential

Note: • ARL model extension

Diagnostic Measurements Desired by ETC Modelers

Measurement	Status	Organization Addressing
<ul style="list-style-type: none"> *1. Degree of burning rate augmentation of SP by plasma or intense radiation source in local contact with plasma *2. SP burning rate law with plasma compared to conventional for bulk propellant *3. Effects of plasmas on burning rate of liquids, gels & solids *4. Burning rate and/or mass generation effects in two - component systems for slurries (mixtures of liquid and solid propellant) 5. Location of reaction front in bulk homogeneous energetic liquid vs. two phase 6. Effects of changes in plasma mass on mixing (Thermal energy vs. momentum) 7. Analysis of closed bomb experimental data via fluid dynamic models 	<ul style="list-style-type: none"> 1. Now doing; With solid propellant and with proposed alternate ETC propellants 2. Some data is available 3. Need data, will soon be doing 4. Need data; efforts starting at ARL & ongoing at Penn State 5. Important; no ongoing efforts directly addressing issue, but feasibility is an issue 6. SNLA experiments have not yet shown a significant influence 7. Can be done (GTD) 	<ul style="list-style-type: none"> 1. ARL, Penn State, NC State 2. ARL, FMC 3. ARL, ARDEC 4. ARL, Penn State, FMC 5. N/A 6. SNLA 7. ARL will share closed bomb data with GTD

Diagnostic Measurements Desired by ETC Modelers

Measurement	Status	Organization Addressing
8. Rates of droplet formation in liquid propellant ETC designs	8. Penn State can perform diagnostics	8. None
9. Plasma pressure, exit velocity, ablation rates, species composition, temperature	9. Pressure, temperature and ablation rates have been measured in some low power diagnostic fixtures. Other measurements extremely difficult.	9. SNLA, ARL, NC State
10. "Benchmark experiments" for community model validation	10. Needed, but time consuming. Experimentalists could all supply carefully obtained data sets for model validations.	10. Groundrules need to be worked out for study

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ARL WORKSHOP ON ETC MODELING

**RESULTS, METHODS AND PLANS
FOR 0, 1 AND 2-DIMENSIONAL
ETC MODELING AT GT-DEVICES**

Niels Winsor, Bob Greig

Jon Earnhart and Dave Hurlburt

12-13 MAY 1993

**Work performed under: DAAA15-90-C-1061,
DAAA15-92-C-0017 and GDLS IR&D.**

MANY THANKS!

The assistance of many Government, Olin and other personnel is gratefully acknowledged. In particular, Ron Anderson, Joe Buzzett, Paul Gough, Arpad Juhasz, George Keller, Ed Lilliot, Hugh McElroy, Dennis Worthington and Gloria Wren contributed either directly or by helping with codes or documentation.

ETC MODELING WORK

- IBHVG2 ENHANCEMENTS & DOC
- XNOVAKTC COMPUTATIONS
- FETC EXPERIMENTS
- FUTURE SIMULATION PLANS

IBHVG2 UPDATES

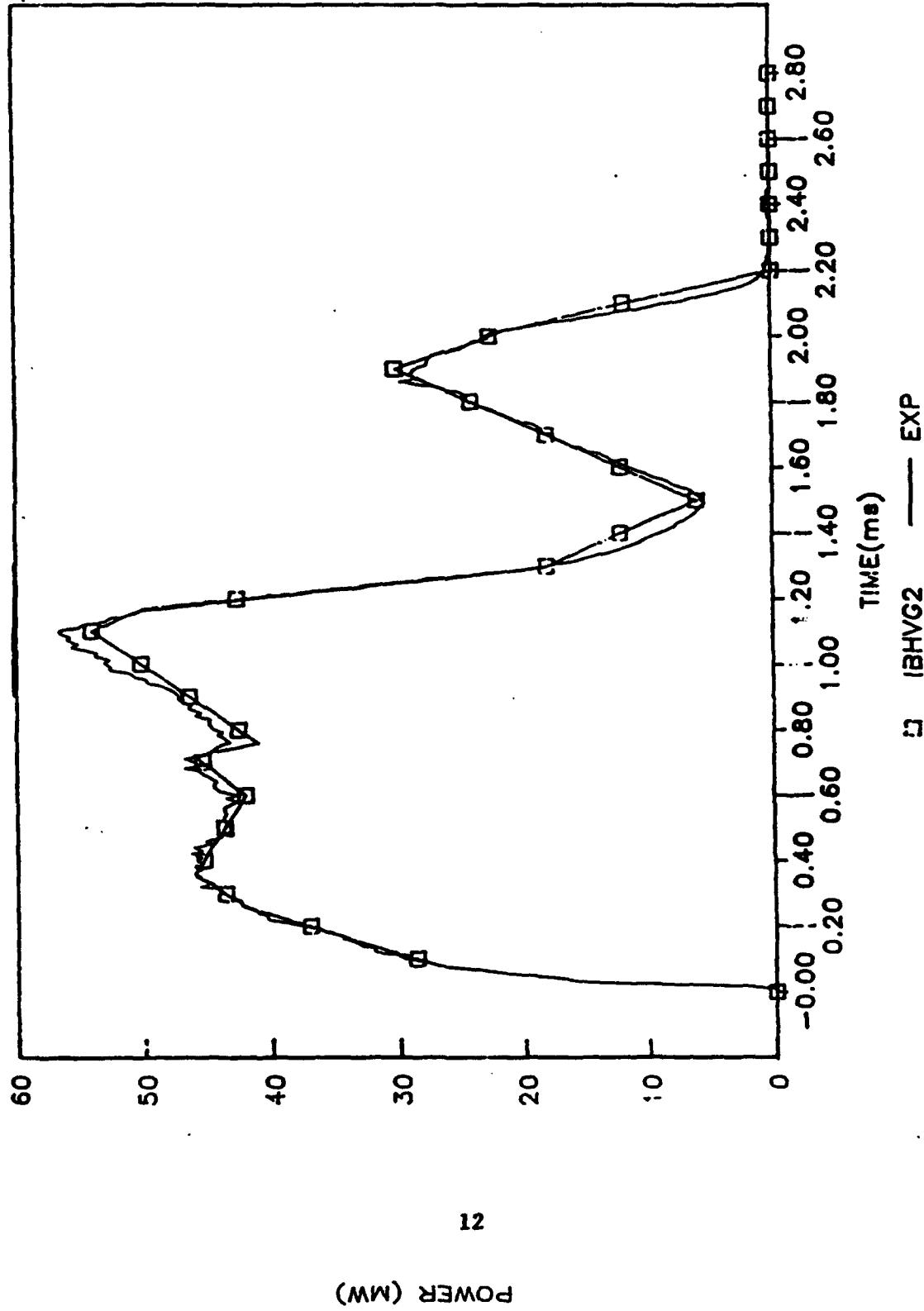
- ETC ENHANCEMENTS
- ETC TUTORIAL
- GENERAL DOCUMENTATION
- COORDINATION WITH OLIN

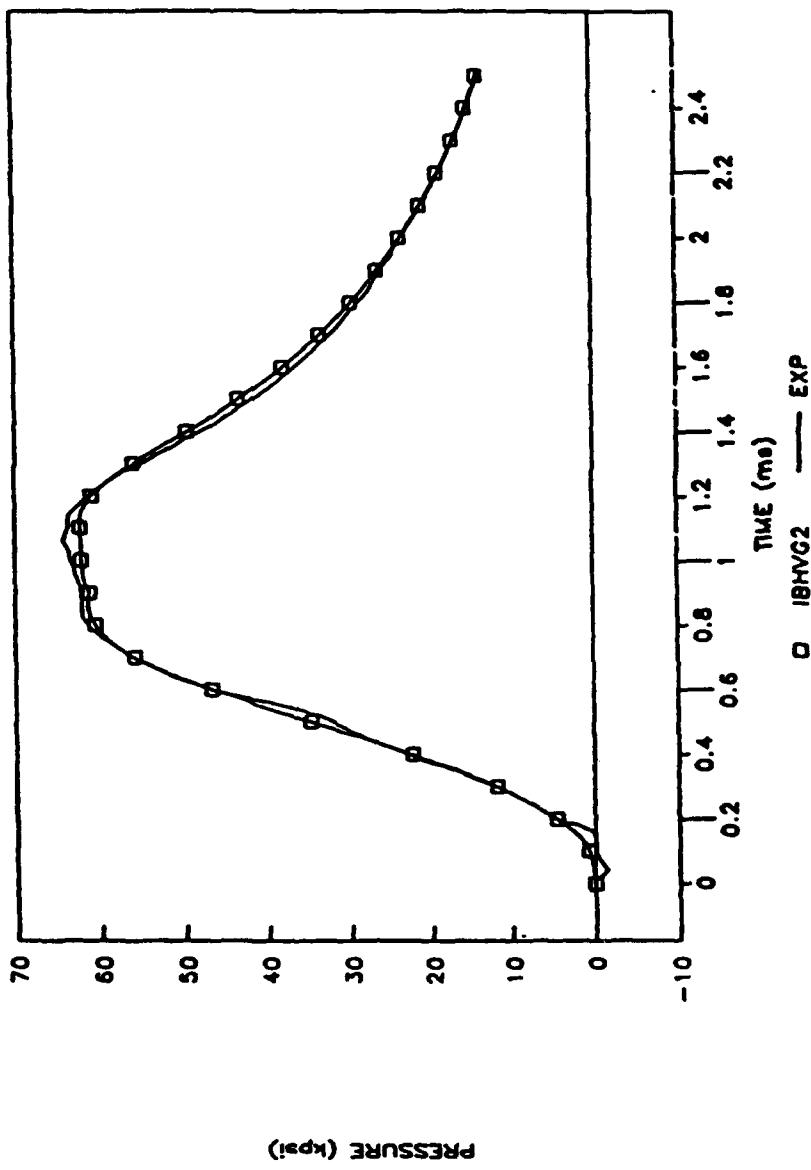
ETC ENHANCEMENTS

- ELECTRIC POWER INPUT
- ENERGY EQUATION MODES
- BURN RATE CONTROL
- ETC OUTPUT DATA

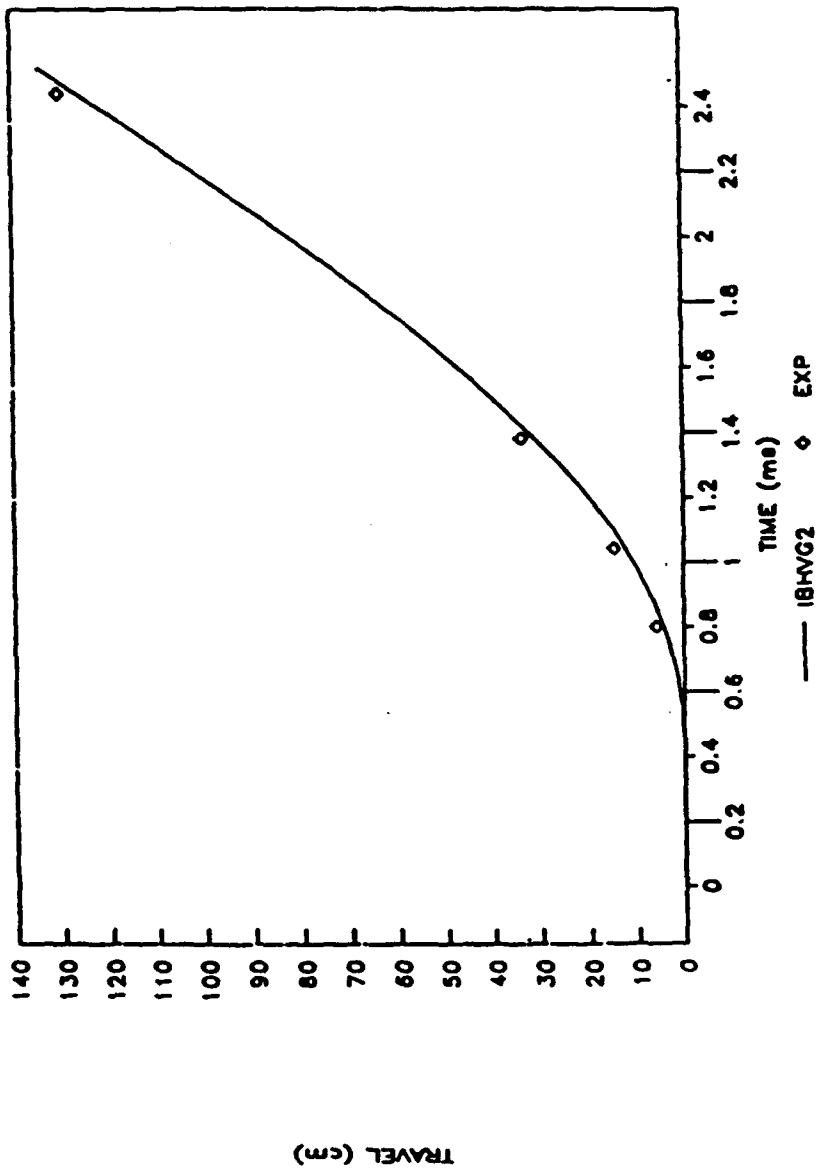
GT - Devices

GENERAL DYNAMICS
Land Systems Division



30mm OLIN EXP. DATA vs. CODE RESULTS
OC26 PCI

CODE AND EXP. PROJECTILE TRAVEL
OC26



ETC TUTORIAL

- FEB 92 DRAFT TR-2829 + TUTOR
- MAR 93 REISSUE -> PICATINNY
- TUTORIAL IN PROCESS AT ARL

XNOVAKTC TRIALS

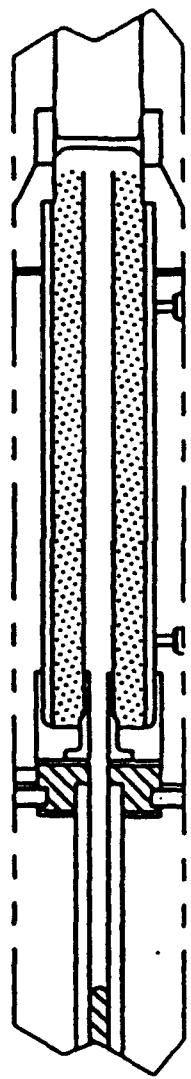
- AXIAL WAVE EXPERIMENTS
- POSTPROCESSOR CHANGES
- PROPELLANT ISSUES
- DOCUMENTATION STATUS

AXIAL WAVES

- EXPERIMENTAL GEOMETRY
- BREECH IGNITION
- XNOVAKTC APPROXIMATIONS
- COMPARISON WITH EXPERIMENT

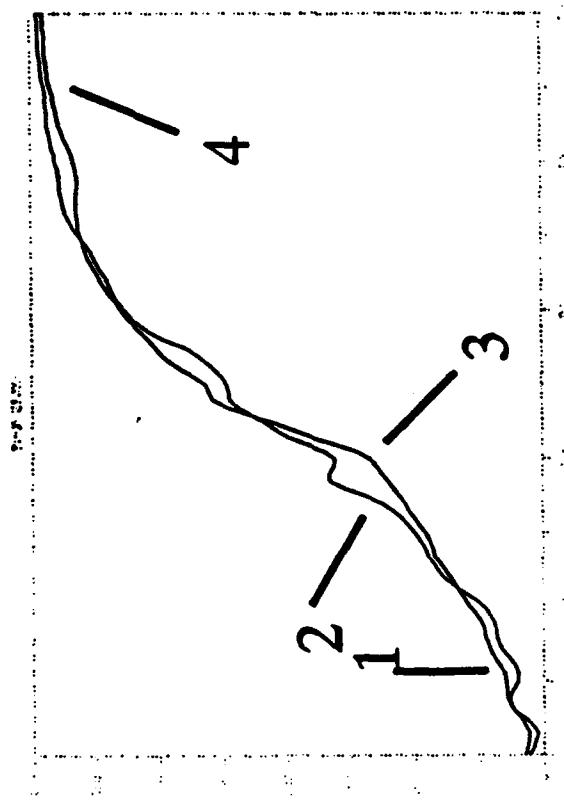
LOADING GEOMETRY

OC26



EARLY BREECH IGNITION CAUSES AXIAL WAVE

EXPERIMENT WITH AXIAL WAVE.



EXPERIMENT

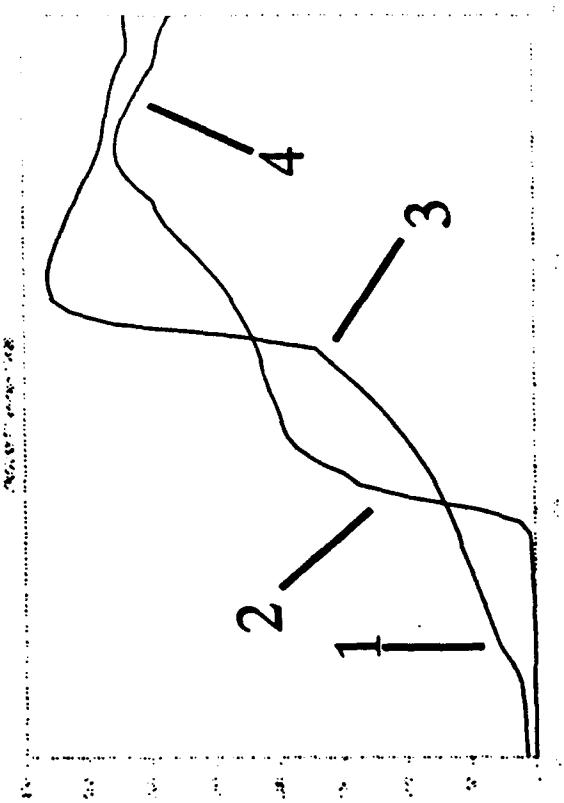
1. Breech overpressure

2. Shock reaches front

3. Reflection reaches breech

4. Waves decay

SIMULATION OF AXIAL WAVE.



COMPUTATION

- A. Breech ignition drives waves.

- B. Wave steepens to shock during bed transit.

- C. Wave decays after 2 transits.

FETC EXPERIMENTS

- MODEL EXTENSIONS
- PLASMA CHANNEL STABILITY
- CHANNEL WALL STRENGTH
- BASIC BALLISTIC LAUNCH

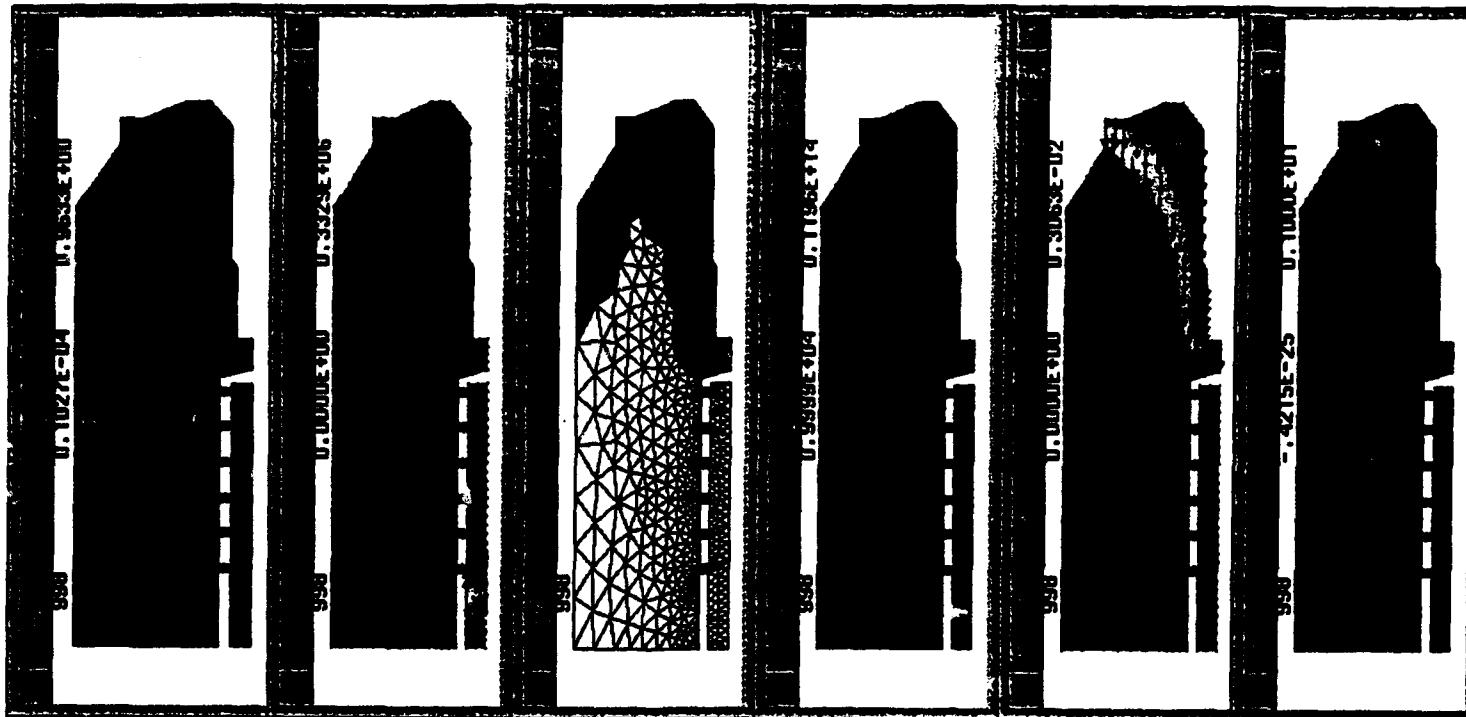


Figure 10. Evolution of a simulated fire spread model. The fire front moves from left to right. The time interval between each image is 500 s. The fire front is represented by a white boundary, and the area behind it is filled with a pattern of black and white dots. The background is solid black.

FETC EXTENSIONS

- LONG, THIN FINITE ELEMENTS
- RIGID, FRANGIBLE MEMBRANES
- MORE COMPLETE CHEMISTRY
- IGNITION MODELS

PLASMA CHANNEL

- MULTIFLUID TRANSPORT
- FCT BOUNDARY MAINTENANCE
- DISSIMILAR SOUND SPEEDS
- PHYSICAL IMPLICATIONS

xx, yy, zz -2, 0.01 -1, 0.01 -5, 1.01 +0.1

DENSITY



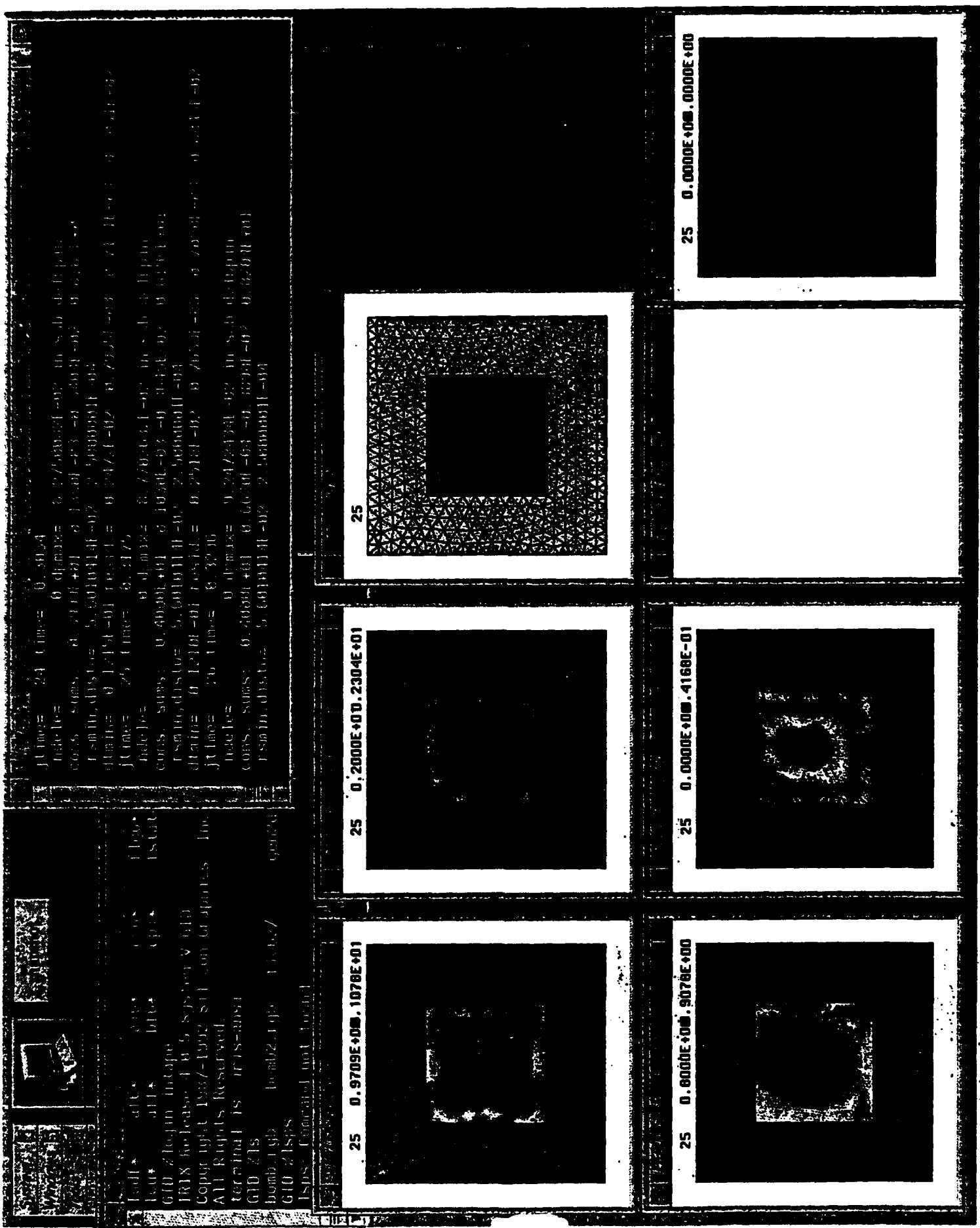
xx, yy, zz -2, 0.01 -1, 0.01 -5, 1.01 +0.1

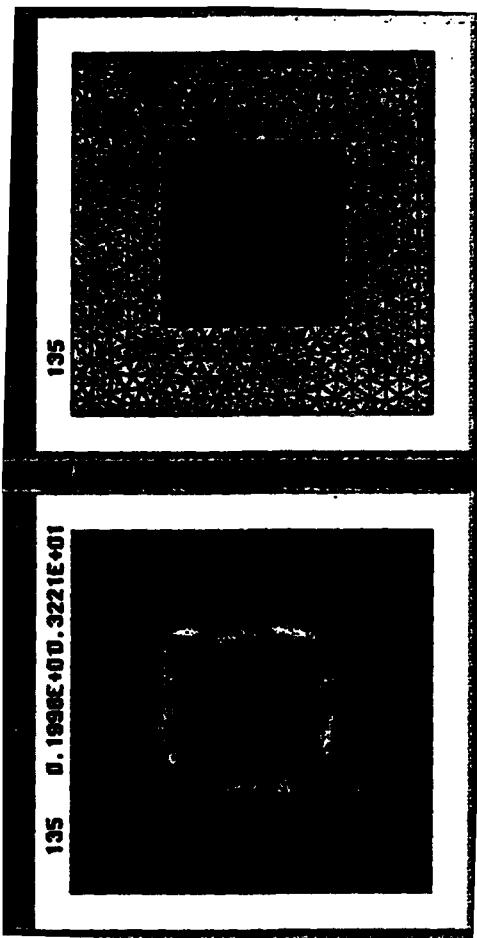
PRESSURE

Current values are set to:
maximum value : 0.1100 +0.1
minimum value : 0.1100 -0.1
contour interval : 0.4374 -0.1
please input min & max val
please input an idenitfying name for the object
you have so far built (the building objects)
or :
1) name: qd
2) name: qd_d
and you have displayed in the last figure the following
1 object.
please input how many objects you would
like to see in the next figure, default is 1
please input the idenitfied object(s)
in the order you desire than to be drawn

CHANNEL WALL

- FLUID-SOLID BOUNDARY
- DELTA-PRESSURE BREAKS
- CLOSED-BOMB TEST





BALLISTIC LAUNCH

- FULL 120 MM GUN TUBE
- ROD, SABOT, IGNITER
- IGNITION FLAMESPREAD
- PROJECTILE LAUNCH

FUTURE WORK

- 120 MM ETC ANALYSIS
- IBHVG2 POST-PROCESSING
- XKTC ETC INCORPORATION
- FETC CHEMISTRY MATCHING

PRODUCTS MENTIONED

**IBHVG2, VERSION 5.04, WITH ETC EXTENSIONS
SEE GLORIA WREN FOR DETAILS OR COPIES**

**XNOVAKTC, VERSION 10426
SEE GEORGE KELLER FOR INFORMATION**

**CASEVision/Toolworks VERSION 1.1.1
SEE SILICON GRAPHICS UN-EXPRESS
1-800-800-7441 Cost \$1500 for 1-user Indigo**

**FORTRAN LINT, Version 2.90
SEE IPT CORP, 1-800-944-5468, \$3900 / 1-user**

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**MULTI-DIMENSIONAL SIMULATION
OF LIQUID AND SOLID PROPELLANT
ETC GUN INTERIOR BALLISTIC FLOWFIELDS**

S. M. Dash, A. Hosangadi and N. Sinha
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MAY 12 & 13, 1993

Presentation at:

ETC MODELING WORKSHOP
U.S. Army Research Laboratory
Aberdeen Proving Ground, MD 21005-5066

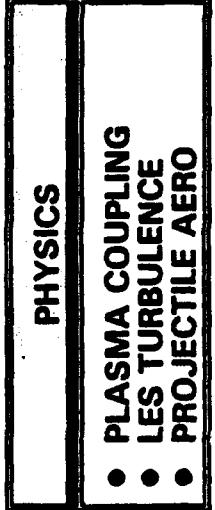
TOPICS

- CRAFT FINITE-VOLUME UPWIND/IMPLICIT CODE
 - Brief Overview of Numerics
 - Requirements for ETC Gun Simulation
- BASIC CRAFT UPGRADES FOR ETC GUN SIMULATION
 - Gridding: Dynamic/Blanking/Embedding
 - Thermochemistry: Liquid EOS/Virial EOS
 - Plasma Code Coupling/Quasi-Steady
- PROGRESS TOWARDS DEVELOPMENT OF CRAFT/LP-ETC MODEL
 - Gas/Liquid Equilibrated Formulation
 - Comparisons with Coffee LPG Code Predictions
 - Comparisons with FMC Shots
 - LES Turbulence Modelling/Subscale Terms
- PROGRESS TOWARDS DEVELOPMENT OF CRAFT/SP-ETC MODEL
 - Solid Propellant Burn Formulation and Integration into CRAFT
 - Comparisons with GDLS Shots
- FUTURE DIRECTION/MULTI-PHASE FLOW UPGRADES
 - Eulerian Solver/Volumetric Effects/Droplet Formation at G/L Interface – LP-ETC
 - Lagrangian Solver/Discrete Particle Combustion/Erosion of Particles from Surface – SP-ETC
 - Plasma Upgrades/Unsteady + Use of CRAFT Numerics

ETC MODELING PHILOSOPHY

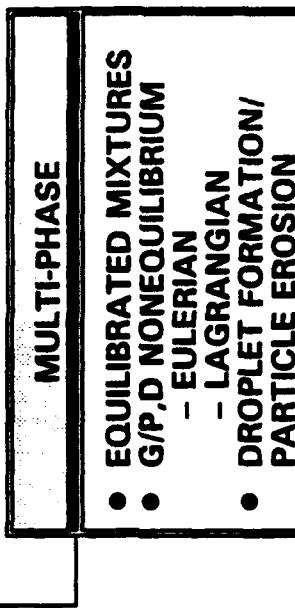
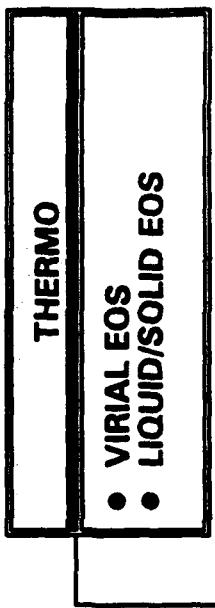
- USE OF ADVANCED STATE-OF-THE-ART NUMERICS AND RESOLVED GRIDS
 - Minimize errors associated with numerical dissipation, etc. for adequate simulation of instabilities and turbulent/vortical structure
- INCORPORATE WELL-ESTABLISHED MODELS AND DATA SETS FOR PROCESSES WELL UNDERSTOOD, e.g., BALL PROPELLANT COMBUSTION
- INCORPORATE SIMPLEST PLAUSIBLE MODELS FOR PROCESSES NOT WELL UNDERSTOOD, e.g., LIQUID/PLASMA INTERFACE
- PERFORM SENSITIVITY STUDIES TO UNDERSTAND INFLUENCE OF MODEL MODIFICATIONS/UPGRADES, e.g., SUBSCALE LES MODELS FOR LP/ETC
- SYSTEMATIC MODELING UPGRADES AS REQUIRED BASED ON SHOT DATA COMPARISONS
 - Understanding processes emphasized

ETC GUN MODELING REQUIREMENTS



NUMERICAL FRAMEWORK

- CONSERVATIVE, HIGHER-ORDER,
- NON-DISSIPATIVE
- STRONGLY-COUPLED/IMPLICIT
TREATMENT OF NONEQUILIBRIUM
SOURCE TERMS
- DYNAMIC GRIDDING,
GENERALIZED BC



CRAFT CODE FEATURES FOR PROPULSIVE FLOWFIELD SIMULATION

NUMERICS	<ul style="list-style-type: none"> • 1D/2D/AXI/3D Finite-Volume Discretization • Implicit, Higher-Order Upwind (Roe/TVD) Formulation • Fully Implicit Source Terms/Boundary Conditions
GRID FEATURES	<ul style="list-style-type: none"> • Grid Dynamics to Account for Moving Boundaries • Grid Patching/Blanking for Complex Geometries • Solution-Adaptive Gridding
THERMOCHEMISTRY	<ul style="list-style-type: none"> • Hybrid Structured/Unstructured Formulation for Multi-Body Problems • Real Gas Mixtures (Calorically and Thermally Imperfect/JANNAF Thermo Tables/Virial EOS) • Finite-Rate Chemistry/Arbitrary Number of Species and Reactions • Fully Implicit Source Term Linearization
MULTI-PHASE FLOW	<ul style="list-style-type: none"> • Nonequilibrium Particle/Droplet Solvers (Eulerian and Lagrangian Formulations) • Gas/Liquid Equilibrium Formulation • Grain/Ablative Coupling Including Surface Recession and Interior Burning
TURBULENCE	<ul style="list-style-type: none"> • k-ϵ Formulation with Compressibility/Vortical Upgrades and Several Low Re Near-Wall Formulations • LES Subgrid Scale Models of Menon and Madabushi • Particle Dispersion Formulations
APPLICATIONS	<ul style="list-style-type: none"> • Electrothermal Chemical (ETC) Gun • Regenerative Liquid Propellant Gun (RLPG) • Ram Accelerator • Solid /Liquid Propellant Rocket Motors/Exhausts • Ducted Rocket • Vertical Launcher Interactions • Turbulence/Multi-Phase Jet Research

CURRENT PROGRAMS UTILIZING CRAFT CODE

SPONSOR	PROGRAM	CODE	APPLICATIONS/FEATURES
NASA/LaRC	Jet Research	CRAFT/JR	<ul style="list-style-type: none"> • Jet structure, steady & unsteady • RS & LES turbulence models
MICOM	Tactical Missile Interactions	CRAFT/TM	<ul style="list-style-type: none"> • Missile propulsive/aero interactions • Nonequilibrium metallic oxide particles ($\text{Al}_2\text{O}_3, \dots$)
ARL	ETC	CRAFT/LP-ETC	<ul style="list-style-type: none"> • Liquid propellant ETC - gas/liquid equilibrated mixture \rightarrow droplet combustion • Solid propellant ETC - fixed bed combustion \rightarrow fluidized bed/particle combustion
NSWC	VLS Interactions	CRAFT/TM	<ul style="list-style-type: none"> • Vertical launcher interactions including particle erosion/ablation • Nonequilibrium particles
MICOM	Advanced Technology	CRAFT/*	<ul style="list-style-type: none"> • Multiple body problems • Hybrid structured/unstructured solver
AFOSR	Ram Accelerator	CRAFT/RAM	<ul style="list-style-type: none"> • Ram accelerator simulation • Turbulence/combustion research
MICOM	Ducted Rocket	CRAFT/DR	<ul style="list-style-type: none"> • Ducted rocket • Carbon particulate combustion/dense loadings
ARL	LPG	CRAFT/LP	<ul style="list-style-type: none"> • Liquid propellant gun simulation • Vortex shedding/LES research

OVERVIEW OF BASIC NUMERICS

- FINITE-VOLUME DESCRETIZATION

$$\begin{aligned} & \frac{\partial}{\partial t} \iint Q dV + \iint (E_{i-1/2} - E_{i+1/2}) d\eta d\xi + \iint (F_{i-1/2} - F_{i+1/2}) d\xi d\zeta + \iint (G_{i-1/2} - G_{i+1/2}) d\xi d\eta \\ &= \frac{1}{Re} \iint (R_{i-1/2} - R_{i+1/2}) d\eta d\xi + \iint (S_{i-1/2} - S_{i+1/2}) d\xi d\zeta + \frac{1}{Re} \iint (T_{i-1/2} - T_{i+1/2}) d\xi d\eta + \iint f dV \end{aligned}$$

- CONSERVATIVE/IMPLICIT METHODOLOGY REQUIRES TIME LINEARIZATION OF FLUX VECTORS E, F, etc. WITH REPEAT TO Q

$$Q^{n+1} = Q^n + \Delta Q, \quad E^{n+1} = E^n + [A] \Delta Q, \quad F^{n+1} = F^n + [B] \Delta Q$$

$$Q = (\rho, \rho u, \rho v, \rho w, e, \epsilon_1, \epsilon_2, \dots); \quad n \text{ variables}$$

A, B, C, etc. — n x n block non-sparse matrices

- VISCOUS AND SOURCE TERMS ALSO LINEARIZED AND INTEGRATED IN A STRONGLY COUPLED FASHION

DISCRETIZED FORM IS:

$$[I + \delta_\xi A - W] [I - W]^{-1} [I - \delta_\eta B - W] [I - W]^{-1} [I + \delta_\zeta C - W] = R.H.S.$$

- FLUX EVALUATION (E_{i-n}, E_{i-n}, \dots , etc.) USING UPWIND Roe/TVD DIFFERENCING

JACOBIAN OF THE FLUX VECTORS

$$\hat{A} = \begin{bmatrix} 0 & l_1 & l_2 & l_3 & \dots & l_n & 0 \\ -Uu + l_1 \frac{\partial U}{\partial \rho_s} & U + l_2 u + l_3 \frac{\partial U}{\partial \rho_s} & l_4 u + l_5 \frac{\partial U}{\partial \rho_s} & l_6 u + l_7 \frac{\partial U}{\partial \rho_s} & \dots & l_{n-1} u + l_n \frac{\partial U}{\partial \rho_s} & l_n \frac{\partial U}{\partial \rho_s} \\ -Uv + l_1 \frac{\partial v}{\partial \rho_s} & l_2 v + l_3 \frac{\partial v}{\partial \rho_s} & U + l_4 v + l_5 \frac{\partial v}{\partial \rho_s} & l_6 v + l_7 \frac{\partial v}{\partial \rho_s} & \dots & l_{n-1} v + l_n \frac{\partial v}{\partial \rho_s} & l_n \frac{\partial v}{\partial \rho_s} \\ -Uw + l_1 \frac{\partial w}{\partial \rho_s} & l_2 w + l_3 \frac{\partial w}{\partial \rho_s} & l_4 w + l_5 \frac{\partial w}{\partial \rho_s} & U + l_6 w + l_7 \frac{\partial w}{\partial \rho_s} & \dots & l_{n-1} w + l_n \frac{\partial w}{\partial \rho_s} & l_n \frac{\partial w}{\partial \rho_s} \\ -UH + U \frac{\partial H}{\partial \rho_s} & l_2 H + U \frac{\partial H}{\partial \rho_s} & l_3 H + U \frac{\partial H}{\partial \rho_s} & l_4 H + U \frac{\partial H}{\partial \rho_s} & (1 + \frac{\partial H}{\partial \rho_s})U & l_{n-1} H + U \frac{\partial H}{\partial \rho_s} & l_n H + U \frac{\partial H}{\partial \rho_s} \\ -c_1 U & c_1 l_1 & c_1 l_2 & c_1 l_3 & \dots & c_1 l_{n-1} & c_1 l_n \\ c_2 U & c_2 l_1 & c_2 l_2 & c_2 l_3 & \dots & c_2 l_{n-1} & c_2 l_n \\ \vdots & \vdots & \vdots & \vdots & \vdots & \vdots & \vdots \\ -c_{n-1} U & -c_{n-1} l_1 & -c_{n-1} l_2 & -c_{n-1} l_3 & \dots & -c_{n-1} l_{n-1} & -c_{n-1} l_n \end{bmatrix}$$

NEED TO EVALUATE THE
PRESSURE DERIVATIVES

$$\frac{\partial P}{\partial \rho}, \frac{\partial P}{\partial \rho U}, \dots, \frac{\partial P}{\partial \rho}, \dots, \text{etc.}$$



UPWIND NUMERICAL FLUX CALCULATION

- NUMERICAL FLUX AT CELL INTERFACE IS EVALUATED IN AN UPWIND FASHION
- FLUX DIFFERENCES ARE BASED UPON THE SIGN OF THE EIGENVALUE
- FLUX AT THE CELL INTERFACE $E_{i+\frac{1}{2}}$ IS GIVEN BY

$$E_{i+\frac{1}{2}} = \frac{1}{2} [E_i^+ + E_{i+1}^- + E_{i+\frac{1}{2}}^+ - E_{i+\frac{1}{2}}^-] + \text{higher order fluxes}$$

E_i^+ = contribution of waves travelling in negative direction

$E_{i+\frac{1}{2}}^+$ = contribution of waves travelling in positive direction
with

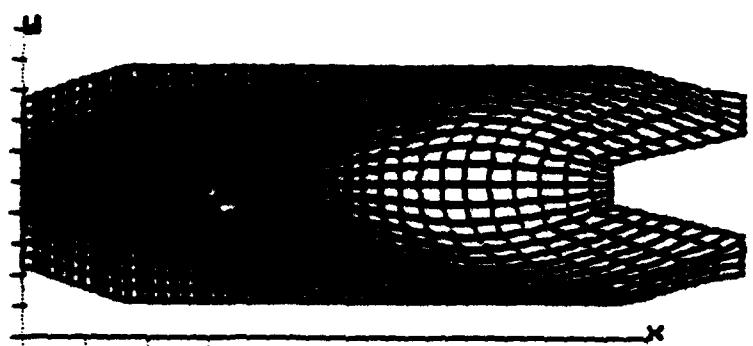
$$E_{j+\frac{1}{2}}^+ = \frac{1}{2} [R_{j+\frac{1}{2}} (\Lambda + |\Lambda|)_{j+\frac{1}{2}} L_{j+\frac{1}{2}}] (Q_{j+1} - Q_j)$$

R and L are $n \times n$ block matrices containing the right and left eigenvectors, respectively.

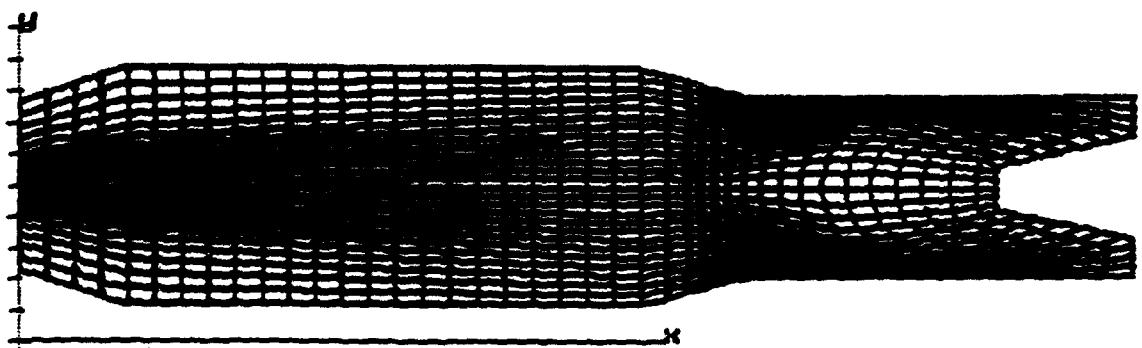
DYNAMIC GRID COMPUTATIONS

EQUATIONS	Term I Term II Term III	Term I Term II Term III	METHODOLOGY	NUMERICS
$\int_{t_i} Q \partial v - \int_{t_i} Q \partial v + \int_{t_i}^t \int_{\Omega} \vec{v} \cdot \vec{f} dt = \int_{t_i}^t \int_{\Omega} \Phi \partial v dt$	<p>Term I: PRIMARY CONSERVED VARIABLES</p> <p>Term II: FLUX TERMS</p> <p>Term III: SOURCE TERMS</p> <p>$\vec{v}(t)$: TIME VARYING VOLUME</p>	<ul style="list-style-type: none"> TREAT GRID AS PURELY GEOMETRIC QUANTITY, i.e., DEFINITION OF CONTRAVARIANT VELOCITY UN-CHANGED EVALUATE FLUX TERM BY ASSUMING GRID IS HELD CONSTANT AT TIME-AVERAGED VALUE INCLUDE ADDITIONAL FLUX ARISING FROM CELL FACE MOTION EVALUATE SOURCE TERM FOR THE GRID AT THE NEW TIME LEVEL, THUS GIVING: $\left(\frac{Q^{n+1} - Q^n}{\Delta t} \right) \vec{v}^{n+1} + Q \cdot \left(\frac{\vec{v}^{n+1} - \vec{v}^n}{\Delta t} \right) + F_n^{n+1} \bar{S} \Delta t = \Phi^{n+1} v^{n+1}$ <p>$F_n = f \cdot \bar{F}$, and \bar{S} is the time averaged metric</p>	<ul style="list-style-type: none"> SPECIFY GRID MOVEMENT AS A FUNCTION OF TIME EVALUATE F_n AS A THIRD-ORDER UPWIND BIASED FLUX SOLVE LINEARIZED IMPLICIT OPERATOR USING ADI PROCEDURE USE NEWTON ITERATION FOR HIGHER ORDER ACCURACY IN TIME 	<p style="text-align: right;">(111)</p>

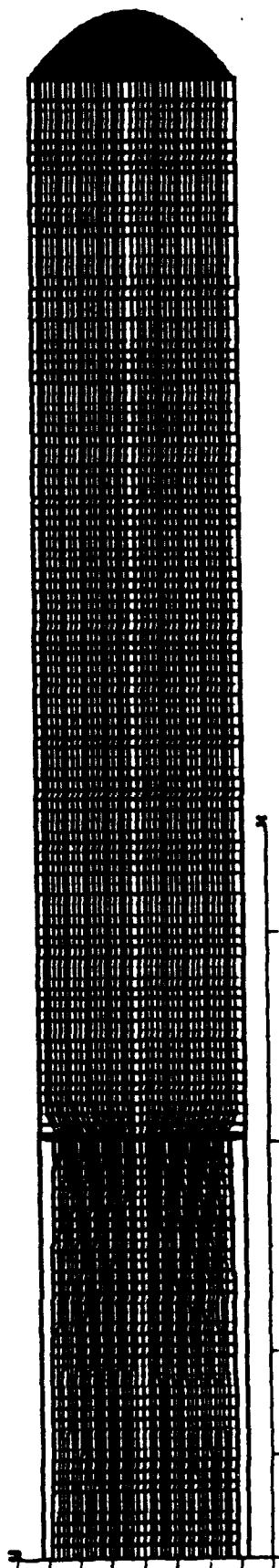
"INITIAL GRID IN GUN CHAMBER"



"GRID IN GUN CHAMBER AT 0.8 TS"

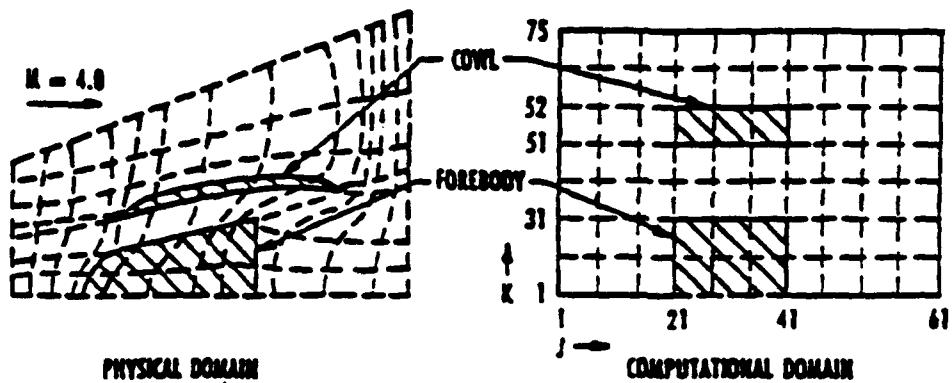


"LOS REFRIGERADORES SON 1.055 m.
S.º ETC 3001-5.



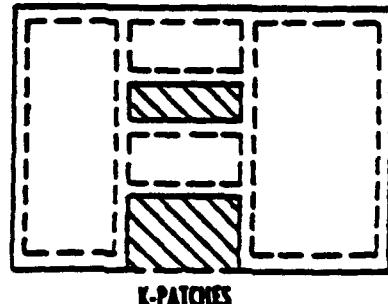
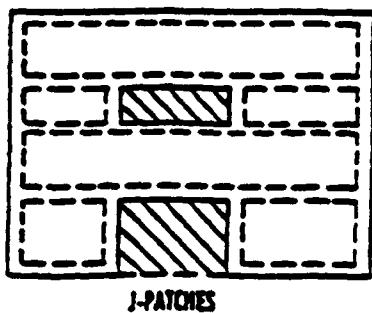
PATCHED GRIDDING IN PARCH (FROM PARC)

- SIMPLE GRIDS/COMPLEX GEOMETRY
- SINGLE DOMAIN/NO BLOCKING INEFFICIENCY



J-Constant Index Class				
Segment Number	J Index	K-Indices		Sign of Normal
		Min	Max.	
1	1	1	75	1
2	21	1	31	-1
3	41	1	30	1
4	51	22	74	-1

K-Constant Index Class				
Segment Number	K Index	J-Indices		Sign of Normal
		Min	Max.	
1	1	1	20	1
2	1	42	61	1
3	75	2	61	-1
4	31	22	41	1
5	51	21	41	-1
6	52	21	41	1

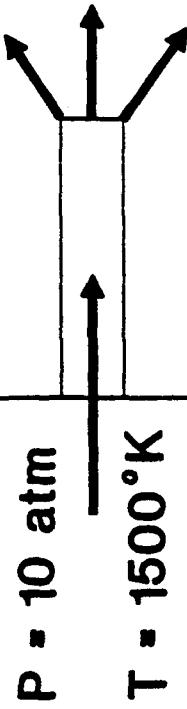


GEOMETRY

Subsonic Outflow

Subsonic
Outflow

$$\begin{aligned}P &= 1 \text{ atm} \\T &= 300 \text{ }^{\circ}\text{K}\end{aligned}$$



Subsonic
Outflow

Subsonic Outflow

Figure 1. Schematic of Coupled Two-Dimensional Model Problem.

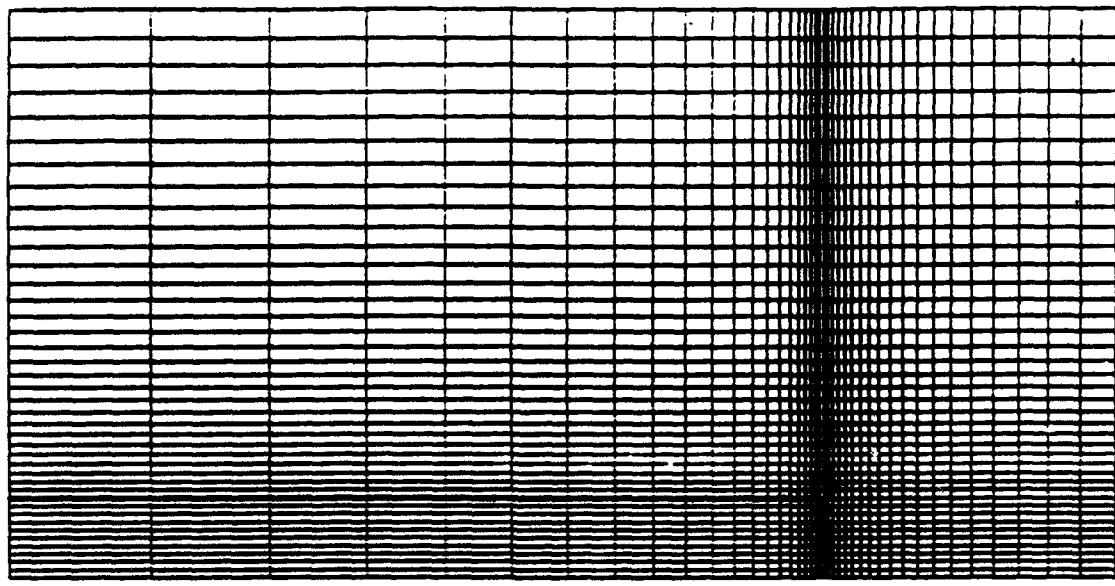
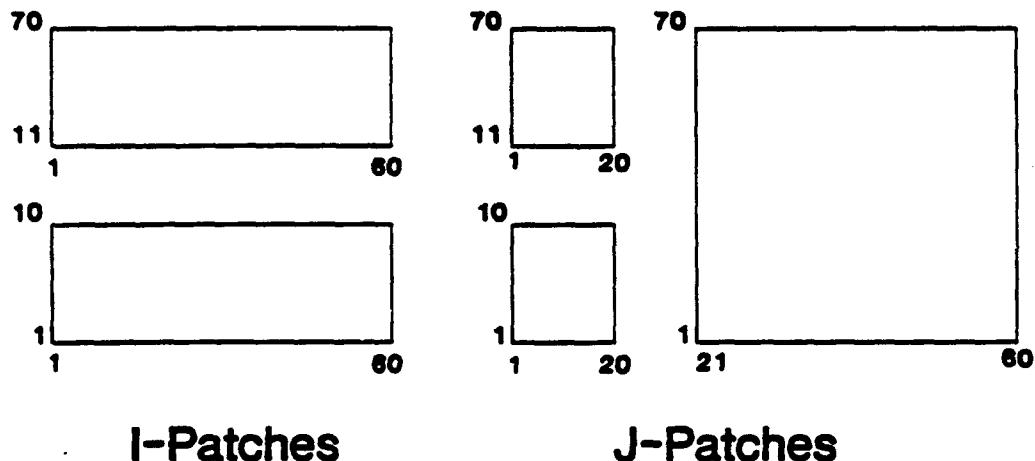


Figure 2a. Numerical Grid for Two-Dimensional Model Problem.

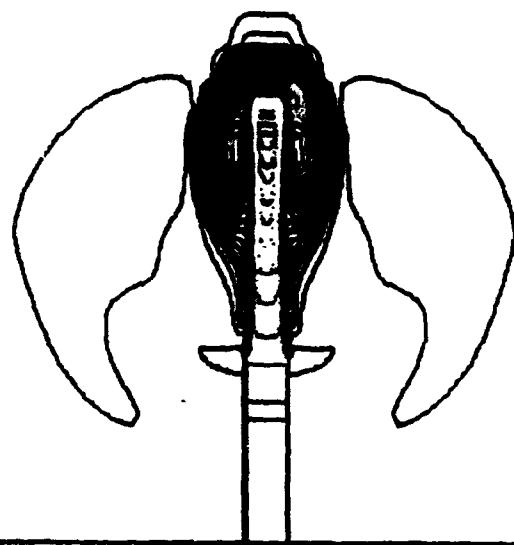


I-Patches

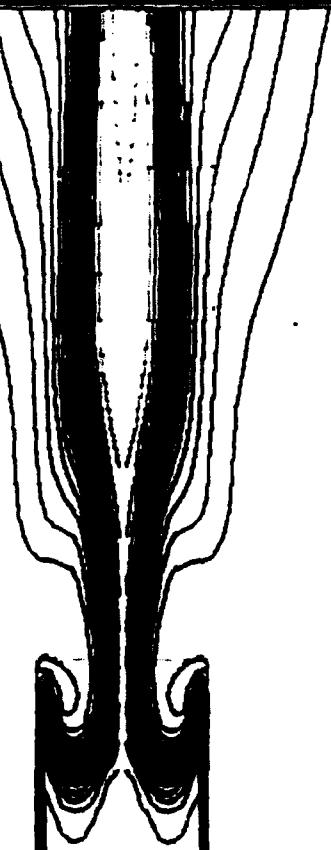
J-Patches

Figure 2b. Grid Patches Employed for Flux Calculation.

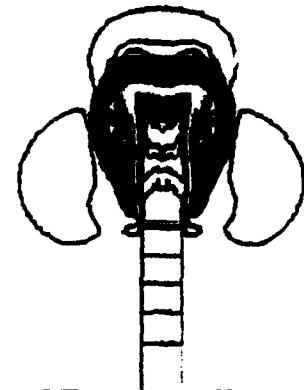
SIGMARILION ENTRAPMENT
20 NOZZLE DISCHARGE



SIGMARILION ENTRAPMENT
11.3 = 3 m
20 NOZZLE DISCHARGE



SIGMARILION ENTRAPMENT
20 NOZZLE DISCHARGE



SIGMARILION ENTRAPMENT
11.3 = 3 m
20 NOZZLE DISCHARGE

DENSE-GAS MODELING CAPABILITIES

- REAL GAS EFFECTS AT HIGH PRESSURES AND TEMPERATURES ARE MODELED BY INCORPORATING THE VIRIAL EOS
- THE VIRIAL EQUATION OF STATE FOR A MULTI-COMPONENT GAS MIXTURE IS GIVEN BY:

$$P = \bar{R}T \sum_n \frac{\rho_i}{w_i} \left[1 + B_m(T) \sum_n \rho_i + C_m(T) \sum_n (\rho_i)^2 \right]$$

THE SECOND AND THIRD VIRIAL COEFFICIENTS FOR THE MIXTURE ARE RELATED TO THE INDIVIDUAL SPECIES VIRIAL COEFFICIENTS.
IN GENERAL

$$B_m(T) = \sum_{ij} B_{ij} X_i X_j$$

HOWEVER, IF DATA IS UNAVAILABLE FOR CROSS COEFFICIENTS SUCH AS B_{ij} , WE APPROXIMATE THE RELATIONSHIP BY

$$B_m(T) = \sum_i B_i Y_i \quad \{ \text{suggested by Ell Freedman}\}$$

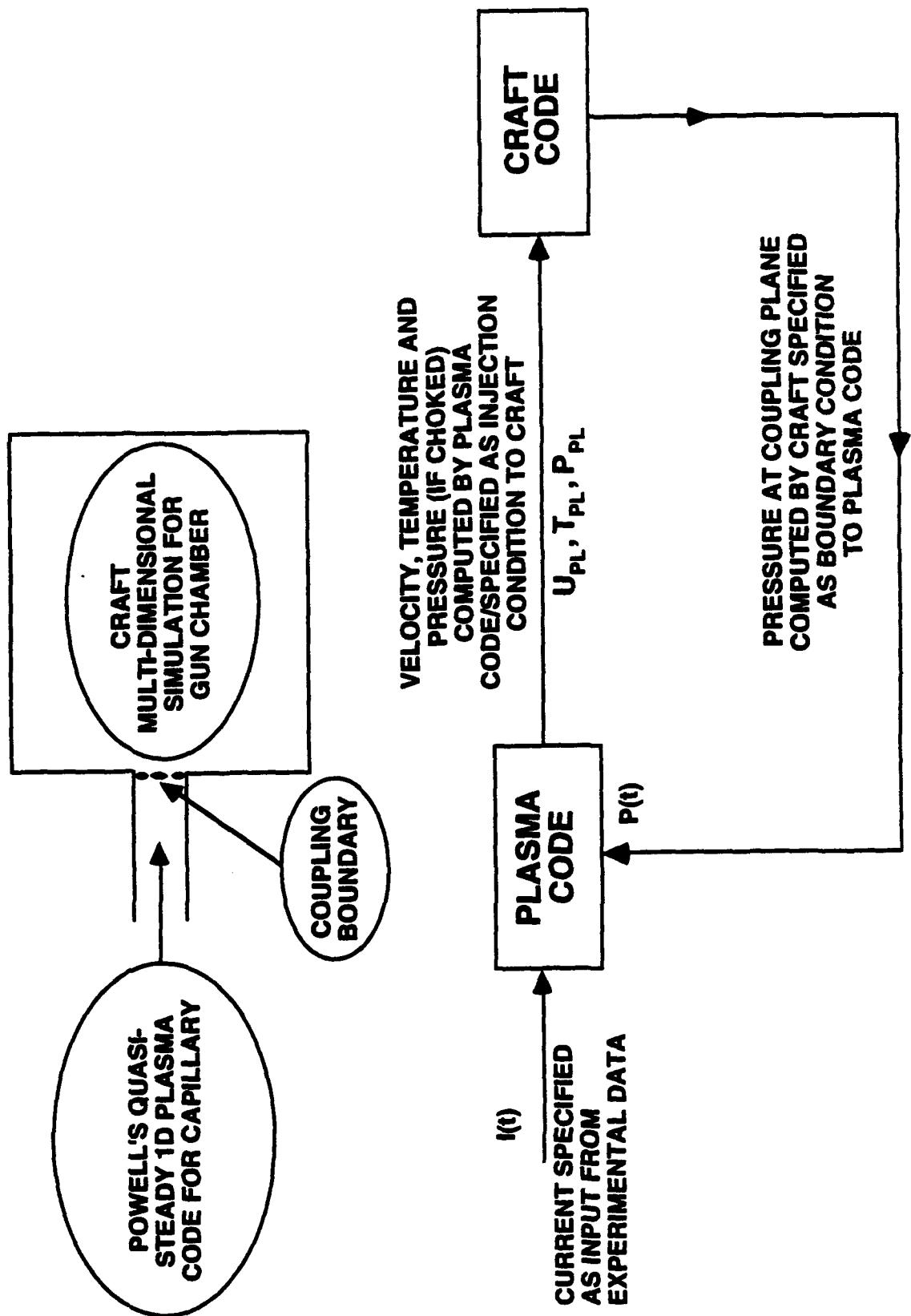
WHERE y_i IS THE MASS FRACTION.

THE VIRIAL COEFFICIENTS FOR EACH INDIVIDUAL COMPONENT CAN BE SPECIFIED IN TABULAR FORM AS A FUNCTION OF TEMPERATURE

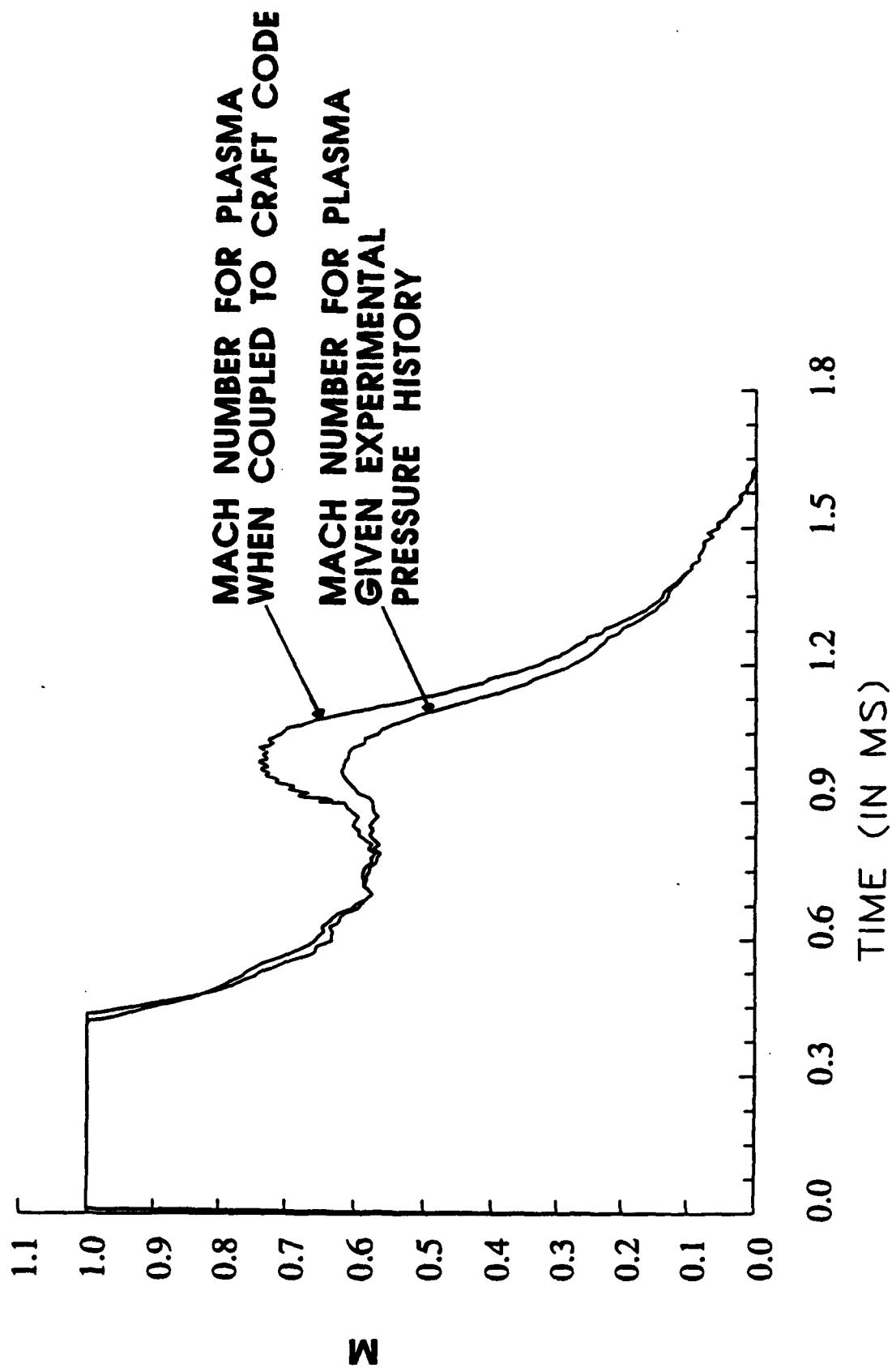
- TEST CASES: HIGH PRESSURE SHOCK TUBE STUDIES

Best Available Copy

PLASMA COUPLING PROCEDURE

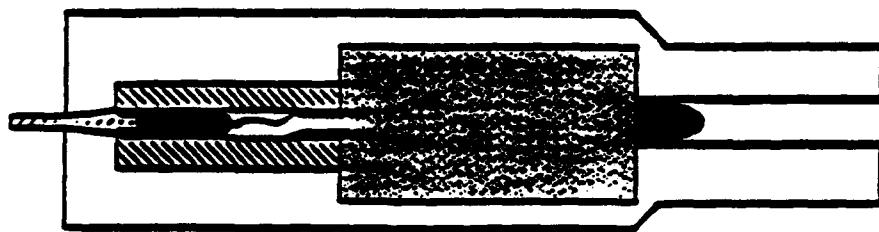


INFLOW MACH NUMBER HISTORY FOR PLASMA

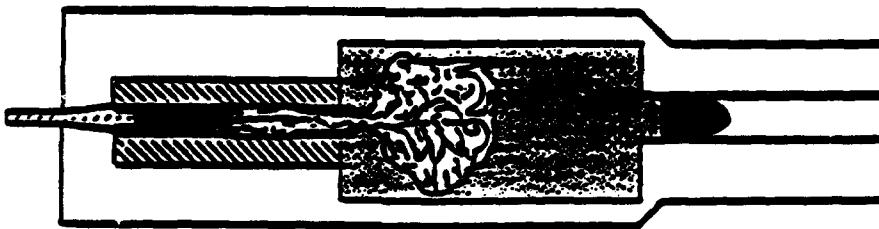


ETC PROCESS

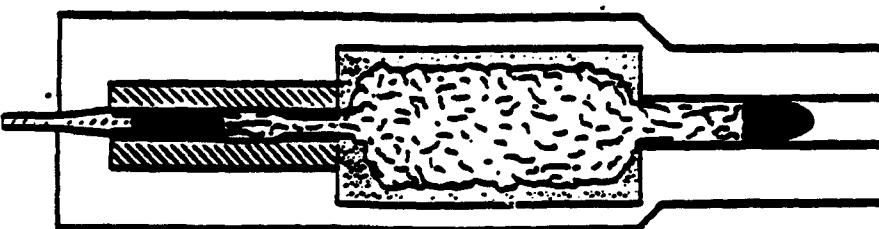
- Initial Configuration



- Initiation of Plasma into Working Fluid



- Interaction/ Combustion/ Vaporization of Plasma and Working Fluid



GAS-LIQUID EQUILIBRIUM FORMULATION

P_L, \bar{V}_L, T_L, V_L LIQUID	P_G, \bar{V}_G, T_G, V_G GAS
--------------------------------------	-----------------------------------

- TWO-PHASE MIXTURE IS GOVERNED BY *AMAGAT'S LAW*

TOTAL VOLUME = SUM OF PARTIAL VOLUMES

$$\phi_G + \phi_L = 1$$

PRESSURE IS IDENTICAL IN BOTH PHASES

$$P_G = P_L$$

- GAS AND LIQUID PHASES TAKEN TO BE IN EQUILIBRIUM

$$\bar{U}_G = \bar{U}_L$$

$$T_G = T_L$$

THIS ALLOWS US TO FORMULATE GLOBAL CONSERVATION EQUATIONS FOR THE MIXTURE RATHER THAN SEPARATE EQUATIONS FOR EACH PHASE

TWO-PHASE EQUATIONS IN CRAFT

$$\frac{\partial Q}{\partial t} + \frac{\partial E}{\partial \xi} + \frac{\partial F}{\partial \eta} + \frac{\partial G}{\partial \zeta} = \text{viscous} + \text{source terms}$$

$$Q = [\rho_m, \rho_m u, \rho_m v, \rho_m w, e, \rho_g \phi_g, \dots, \dots]^T$$

global conservation equations

species mass conservation

$$E = [\rho_m \partial_t, \rho_m \partial_u, \rho_m \partial_v, \rho_m \partial_w, (e + P) \partial_t, \rho_g \phi_g \partial_t, \dots, \dots]^T$$

$$+ \ell_x P + \ell_y P + \ell_z P$$

Liquid mass is obtained from

$$\rho_m = \rho_g \phi_g + \rho_L (1 - \phi_g)$$

$$\therefore \rho_L (1 - \phi_g) = \rho_m - \rho_g \phi_g$$

$$\phi_g = \frac{V_g}{V_g + V_L}$$

HOW DO WE OBTAIN THE DERIVATIVES OF THE PRESSURE TERM?

THE GAS AND LIQUID PRESSURES ARE FUNCTIONS OF THREE VALUES:

$$P_g = f(\hat{\rho}_g, T, \Phi_g), P_L = f(\hat{\rho}_L, T, (1 - \Phi_g))$$

$$dP_g = f(d\hat{\rho}_g, dT, d\Phi_g)$$

$$dP_L = f(d\hat{\rho}_L, dt, d(1 - \Phi_g))$$

56

SINCE WE DO NOT SOLVE DIRECTLY FOR Φ_g , WE ELIMINATE THE $d\Phi_g$ TERM BY EVALUATING $dP_g = dP_L$ AND GETTING AN EXPRESSION FOR $d\Phi_g$.

USING THIS RELATIONSHIP FOR $d\Phi_g$, IT IS STRAIGHTFORWARD TO DERIVE THE DERIVATIVES OF THE PRESSURE

SPEED OF SOUND IN TWO-PHASE SYSTEM

- CALCULATE EIGENVALUES OF THE FLUX JACOBIAN A:

$$A - \lambda I = 0$$

- EIGENVALUES OF A ARE EVALUATED TO BE:

$$\Lambda = [\hat{U} + k_t C, \hat{U} - k_t C, \hat{U}, \hat{U}, \dots \hat{U}]^T \quad \left\{ k_t = [\tilde{\zeta}_x^2 + \tilde{\zeta}_y^2 + \tilde{\zeta}_z^2]^{1/2} \right\}$$

WHERE, C, THE SPEED OF SOUND IN THE MIXTURE IS:

$$C_m = \left\{ \frac{\tilde{\gamma}}{\rho_m} \left[\frac{\Phi_g}{\rho_g C_g^2} + \frac{1 - \Phi_g}{\rho_L C_L^2} \right]^{-1} \right\}^{1/2}$$

$$C_g = \text{Isothermal Speed of Sound in Gas} \quad = \quad \left(\frac{\partial P_g}{\partial \rho_g} \right)_T^{1/2}$$

$$C_L = \text{Isothermal Speed of Sound in Liquid} \quad = \quad \left(\frac{\partial P_L}{\partial \rho_L} \right)_T^{1/2}$$

VALIDATION STUDIES FOR GAS-LIQUID FORMULATION

- SOLUTIONS FOR TWO-PHASE 1-D SHOCK TUBES WERE COMPARED WITH TERRY COFFEE'S COMPUTATIONS

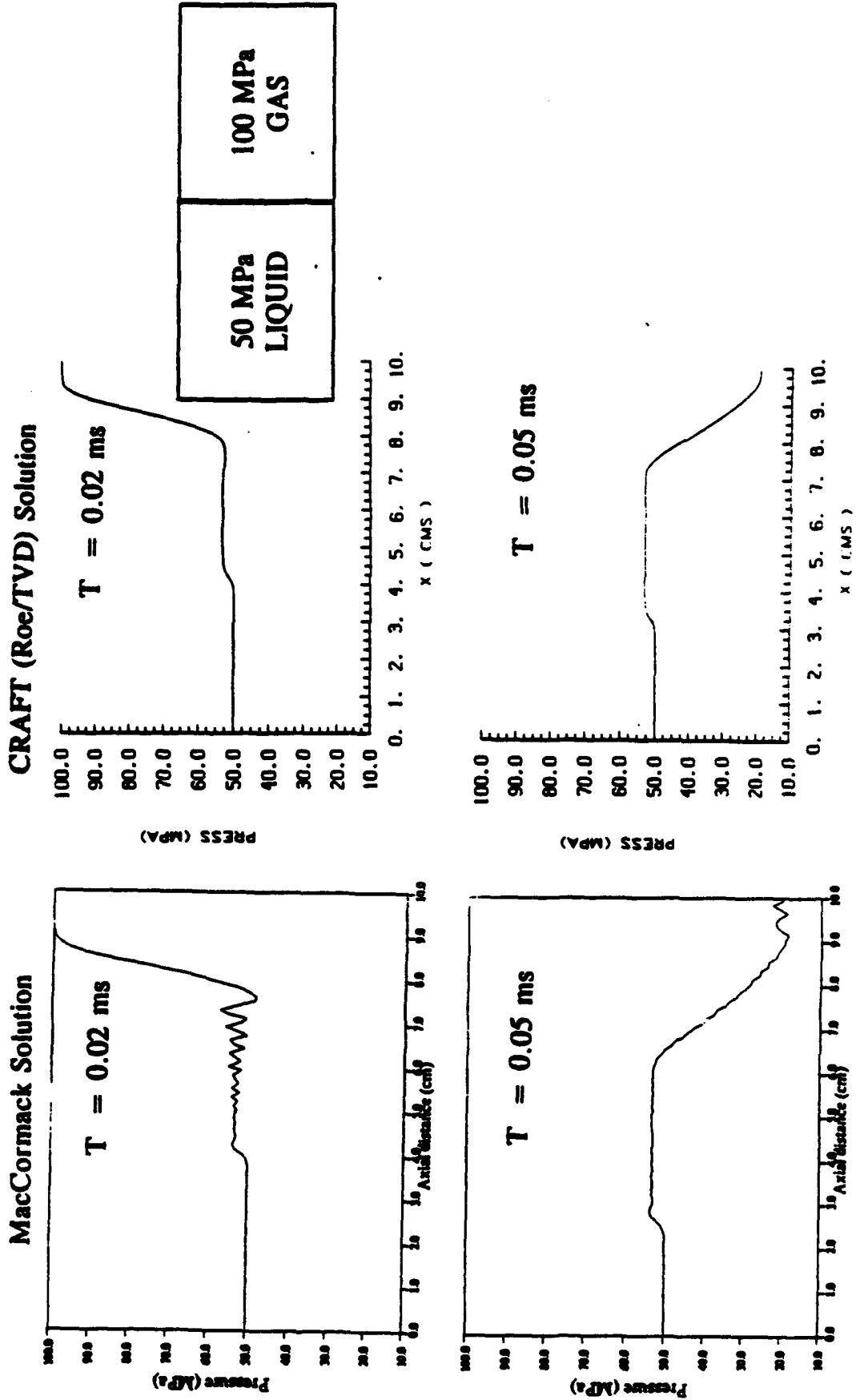
CASE I	LIQUID - HIGH PRESSURE SIDE GAS - LOW PRESSURE SIDE	50 MPa	100 MPa
CASE II	LIQUID - LOW PRESSURE SIDE GAS - HIGH PRESSURE SIDE		
CASE III	UNIFORM MIXTURE OF GAS AND LIQUID ON BOTH SIDES		



- CASE IV RADIAL SHOCK TUBE - UNIFORM MIXTURE WITH HIGH PRESSURE AT CORE

PRESSURE PROFILES FOR A TWO-PHASE SHOCK TUBE

Gas = High Pressure Side and Liquid = Low Pressure Side

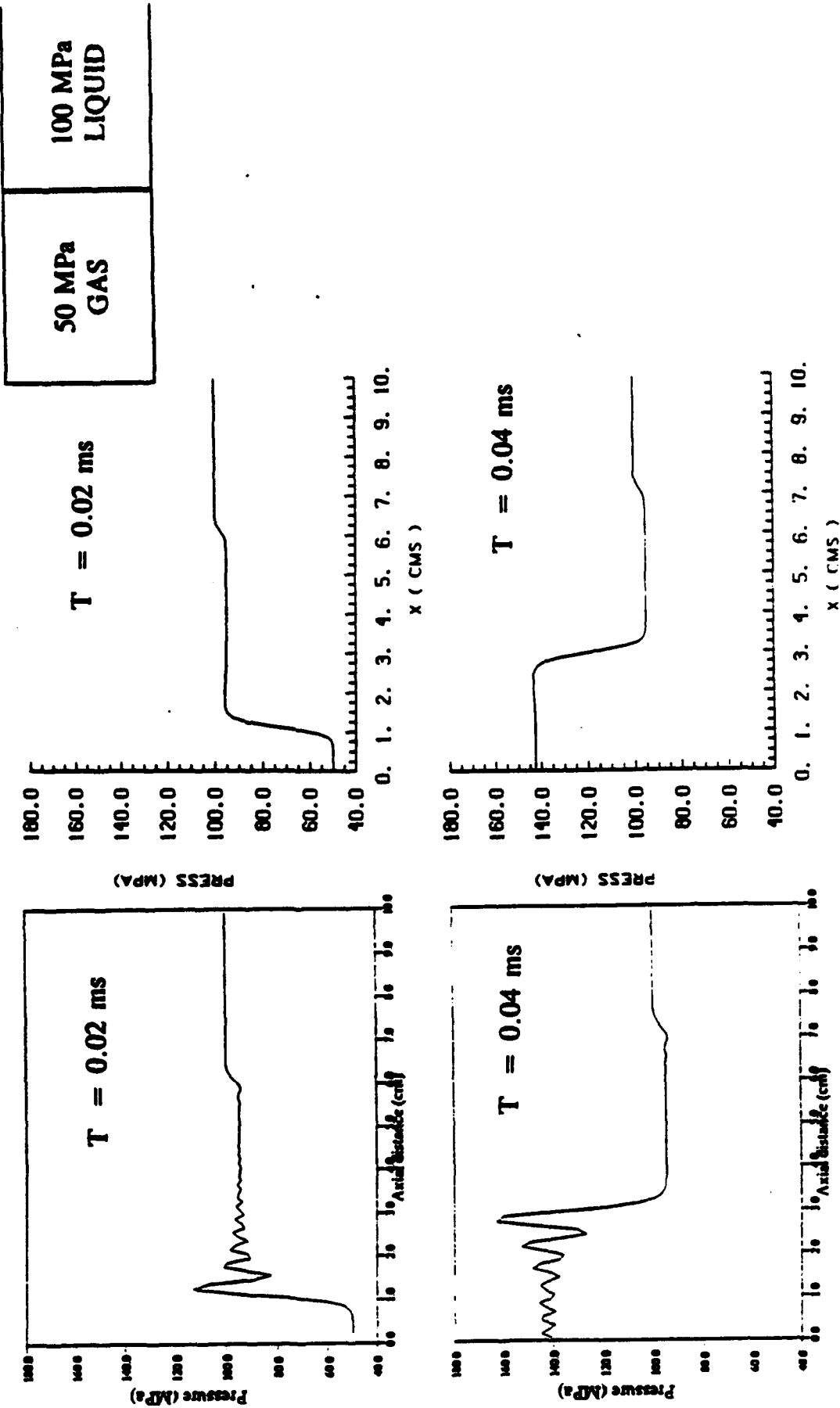


PRESSURE PROFILES FOR A TWO-PHASE SHOCK TUBE

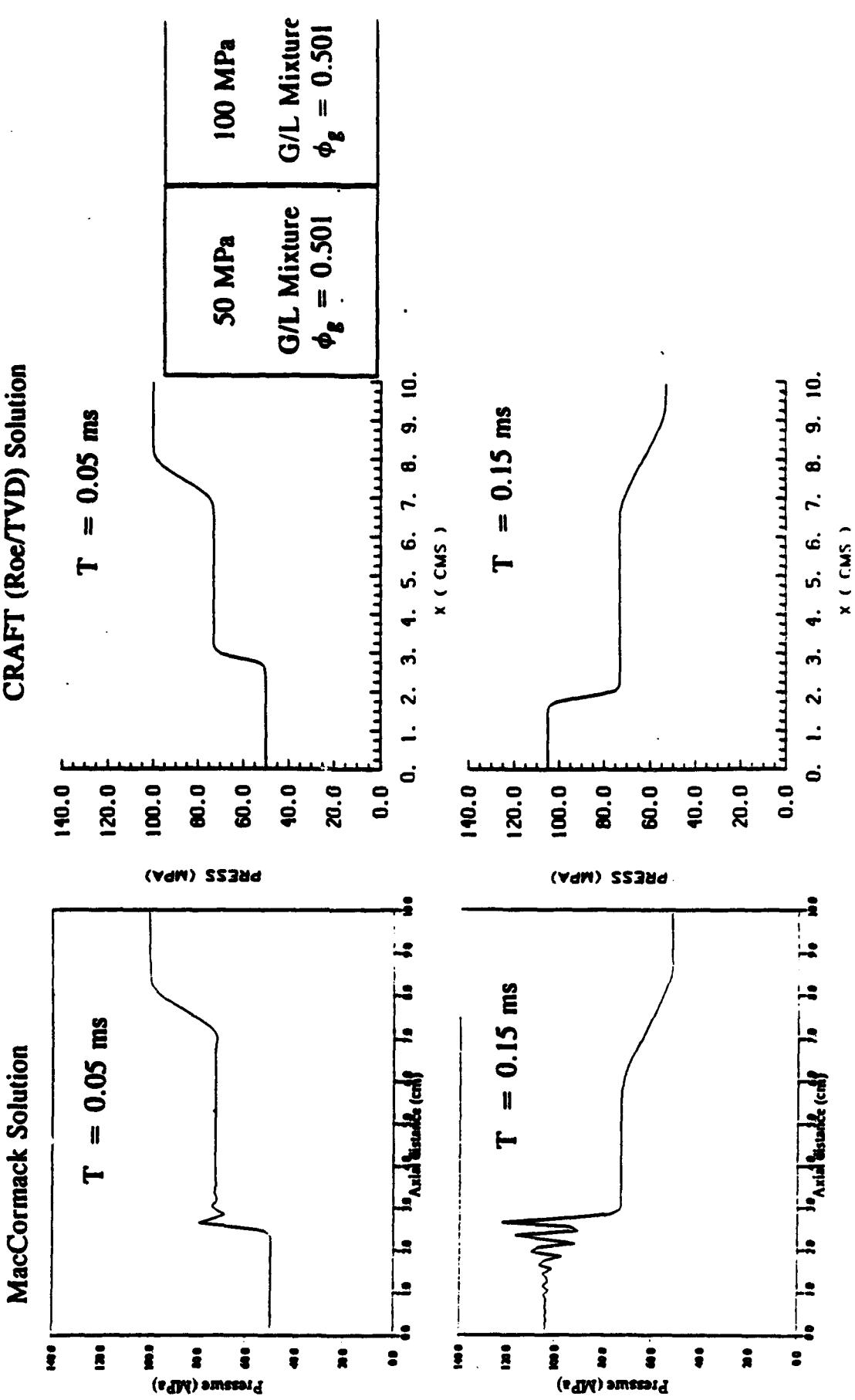
Gas = Low Pressure Side and Liquid = High Pressure Side

MacCormack Solution

CRAFT (Roe/TVD) Solution

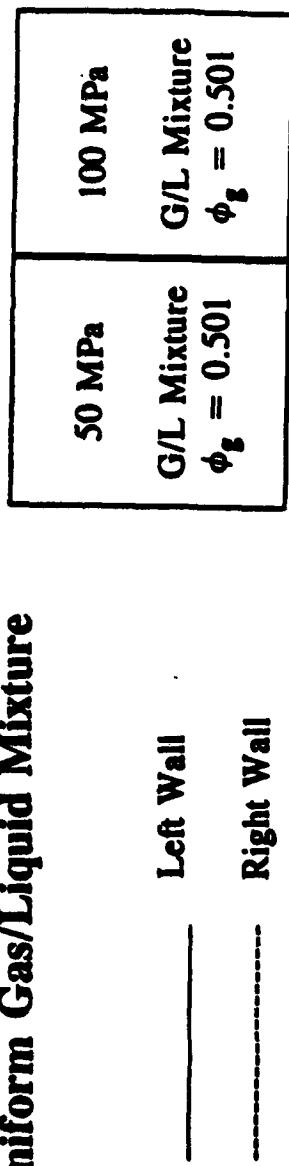


PRESSURE PROFILES FOR A TWO-PHASE SHOCK TUBE
 Uniform Gas/Liquid Mixture

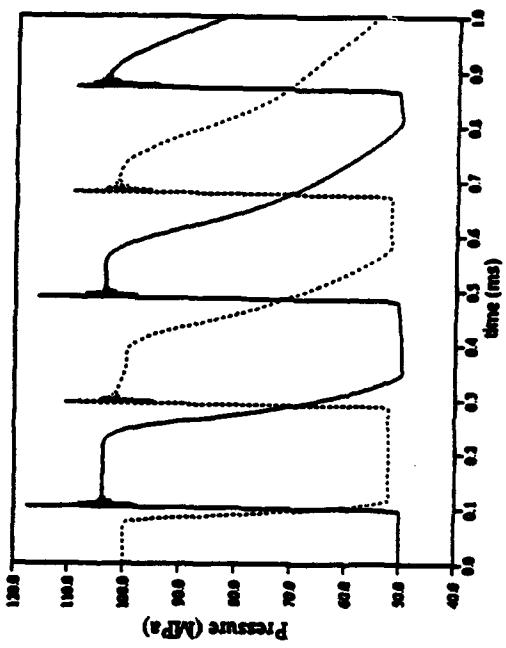


PRESSURE HISTORY ON WALL OF TWO-PHASE SHOCK TUBE

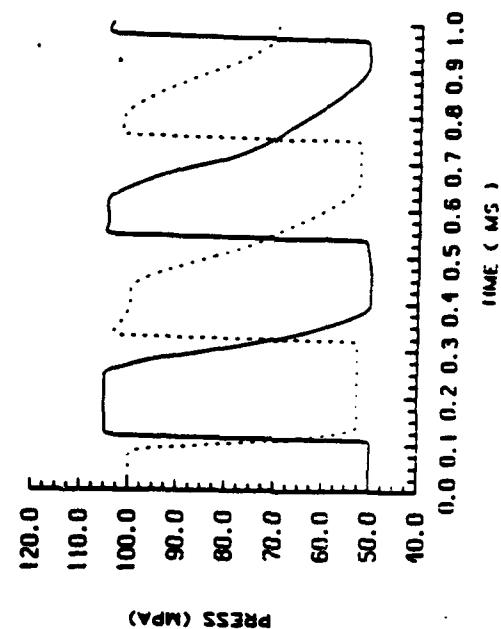
Uniform Gas/Liquid Mixture



MacCormack Solution

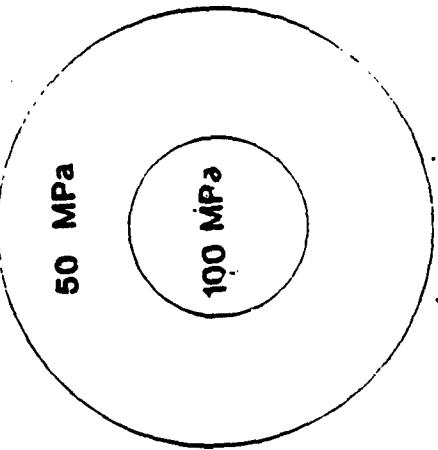


CRAFT (Roe/TVD) Solution

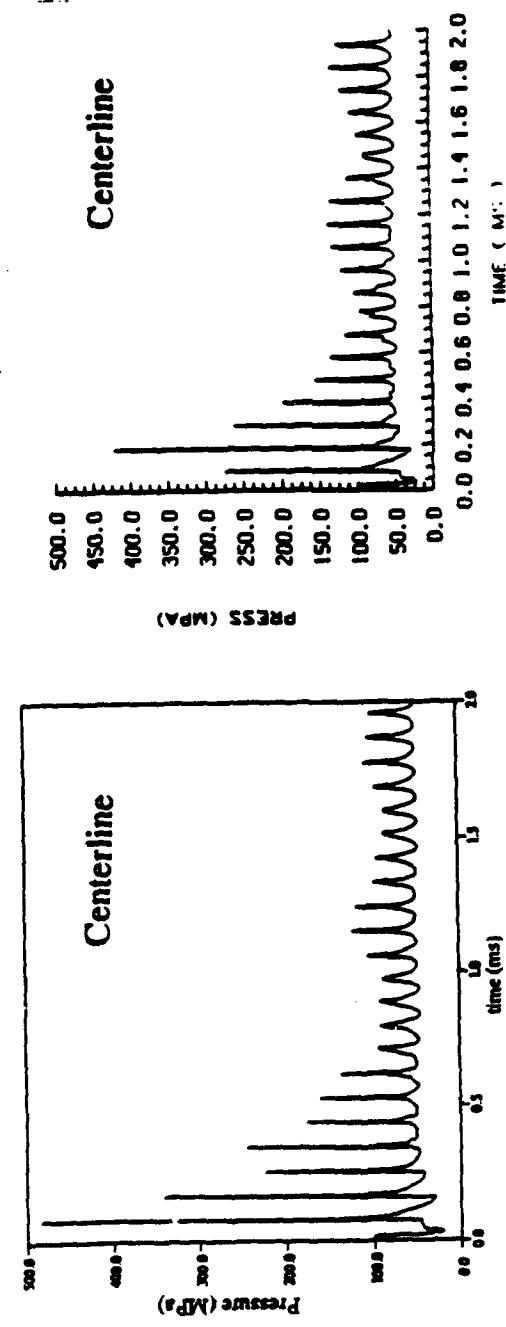


PRESSURE HISTORY FOR A RADIAL TWO-PHASE SHOCK TUBE

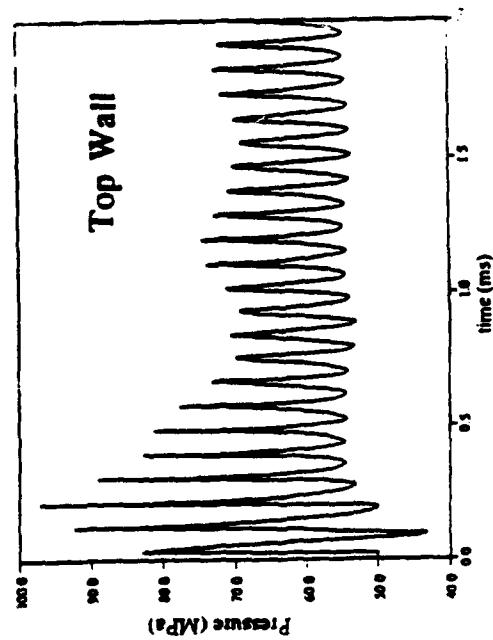
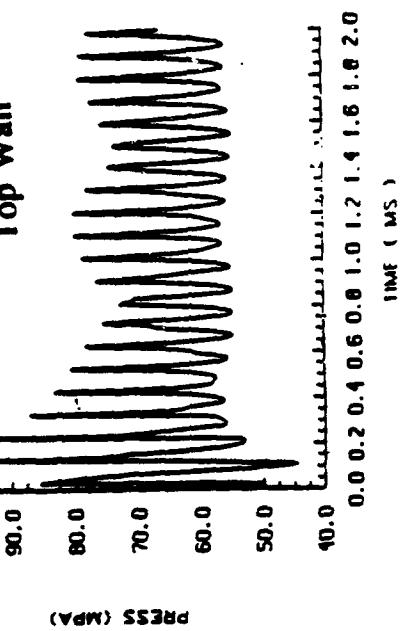
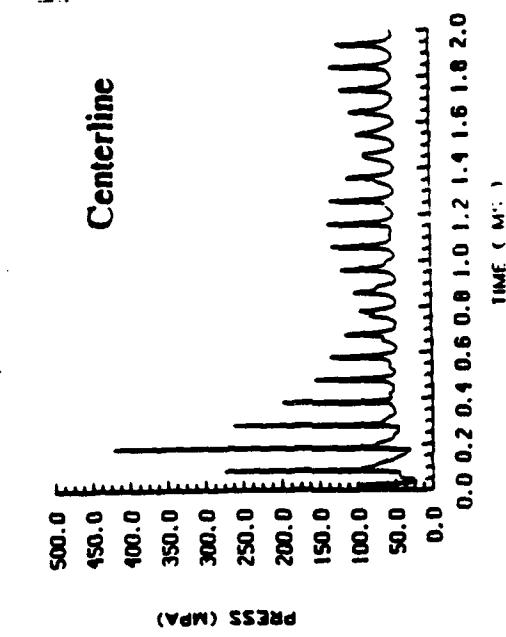
Uniform Gas/Liquid Mixture



MacCormack Solution

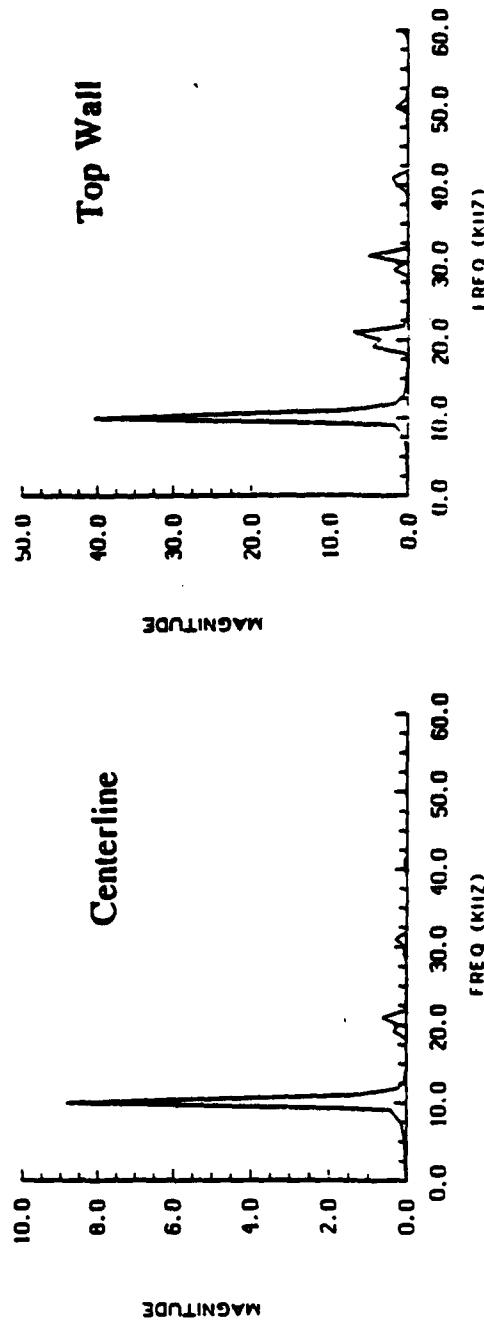
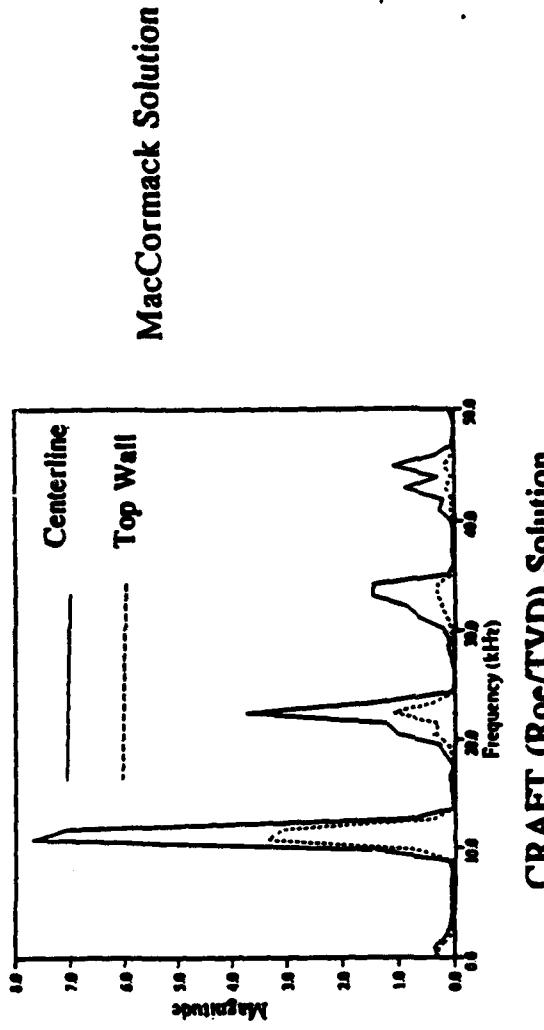
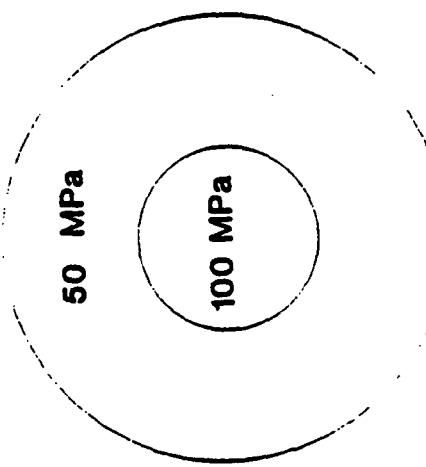


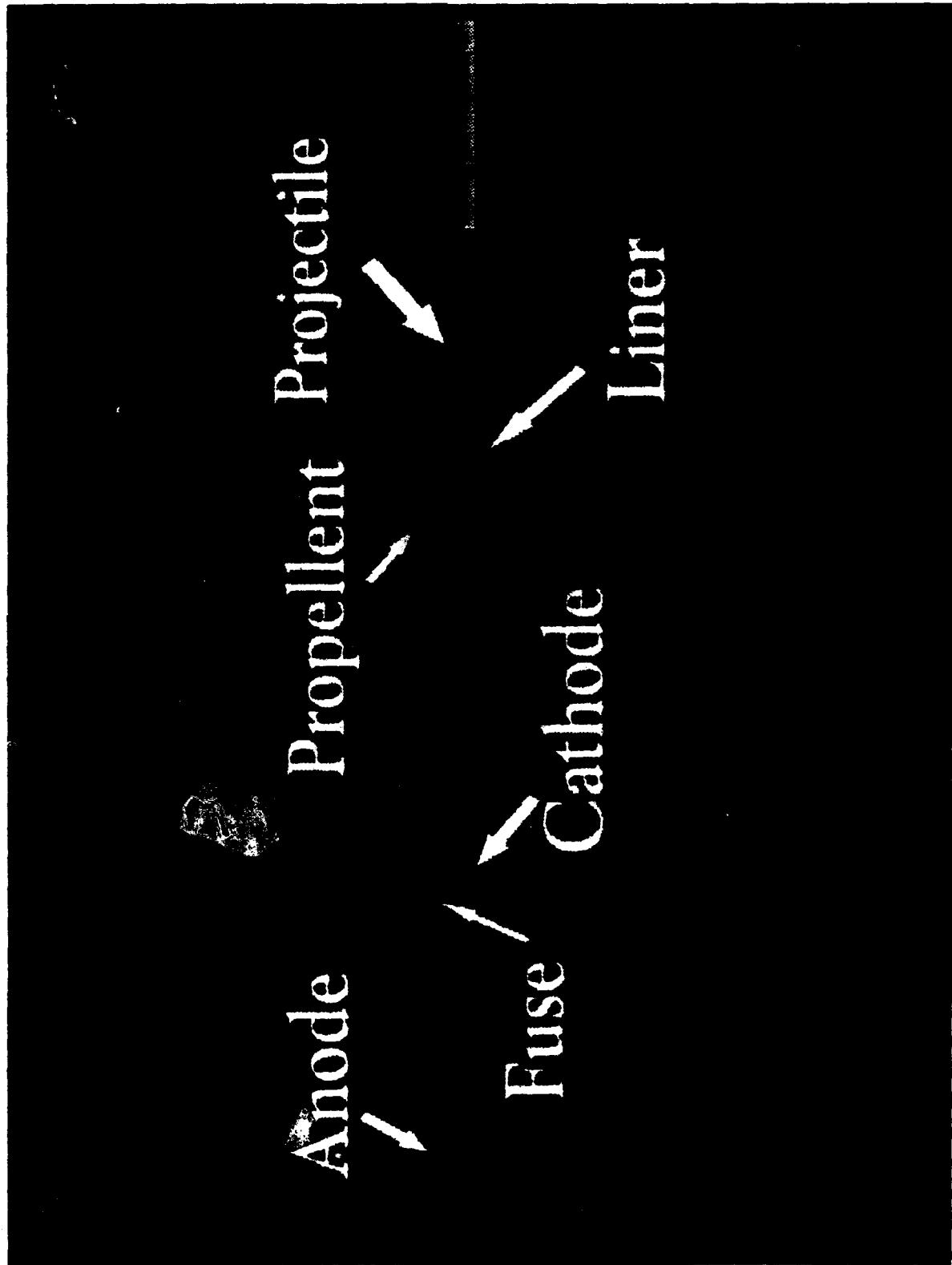
CRAFT (Roe/TVD) Solution



FREQUENCY SPECTRA FOR A RADIAL TWO-PHASE SHOCK TUBE

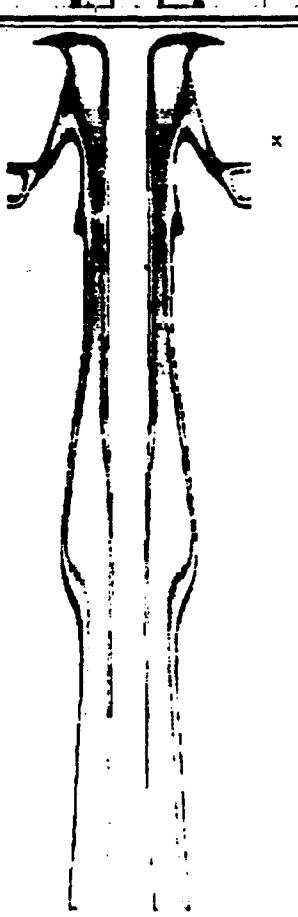
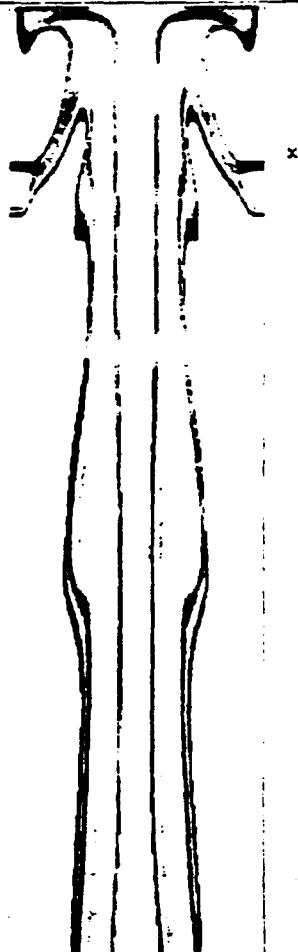
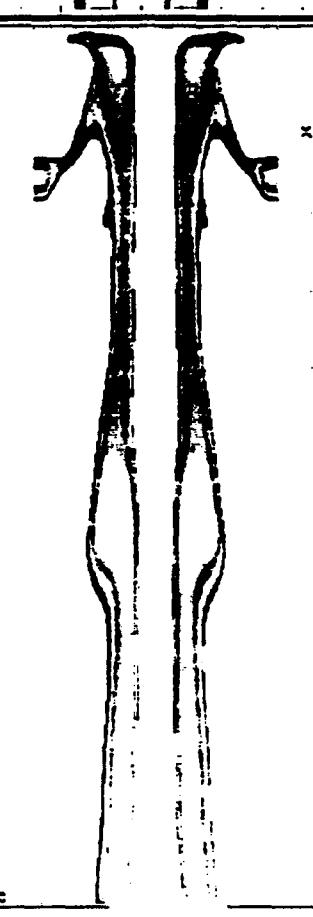
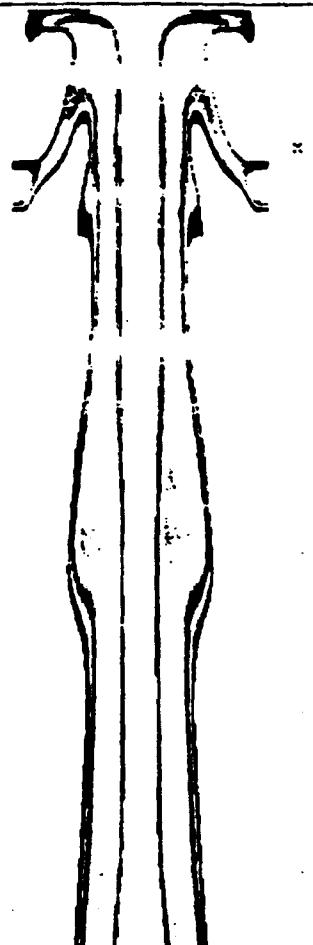
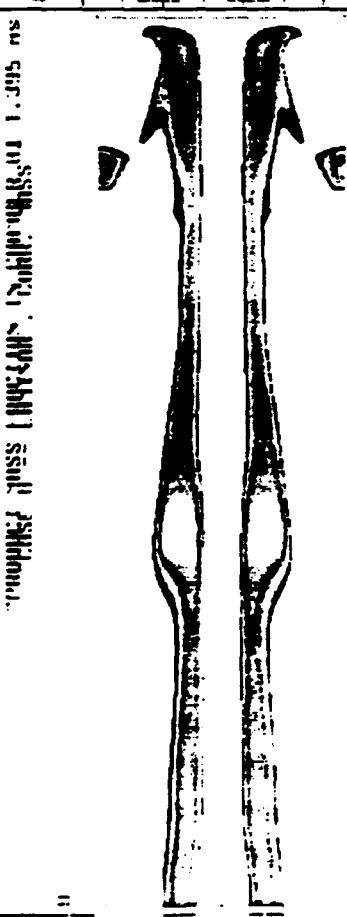
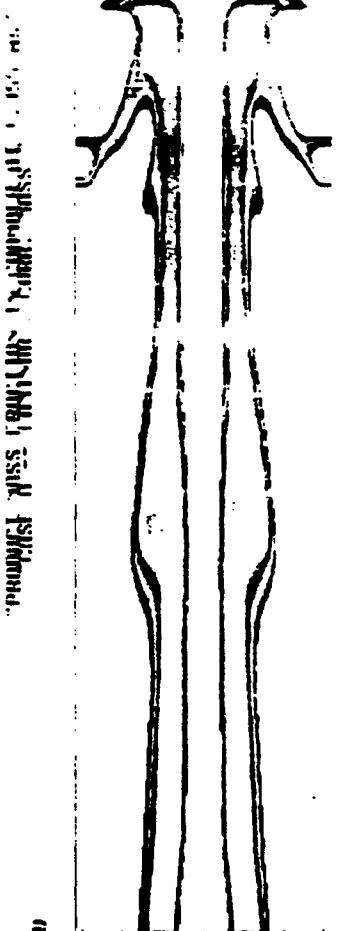
Uniform Gas/Liquid Mixture





“କୁଳାବ୍ଦ ପରିମାଣ କରିବାର ନିଷେଧିତ

ଏହାରେ କିମ୍ବା କିମ୍ବା କିମ୍ବା କିମ୍ବା



અને એવા કાળીઓની પણ જરૂર હોય કે આ કાળીની લાંબીતા કાઢી રહેની ચાહેરી હોય.

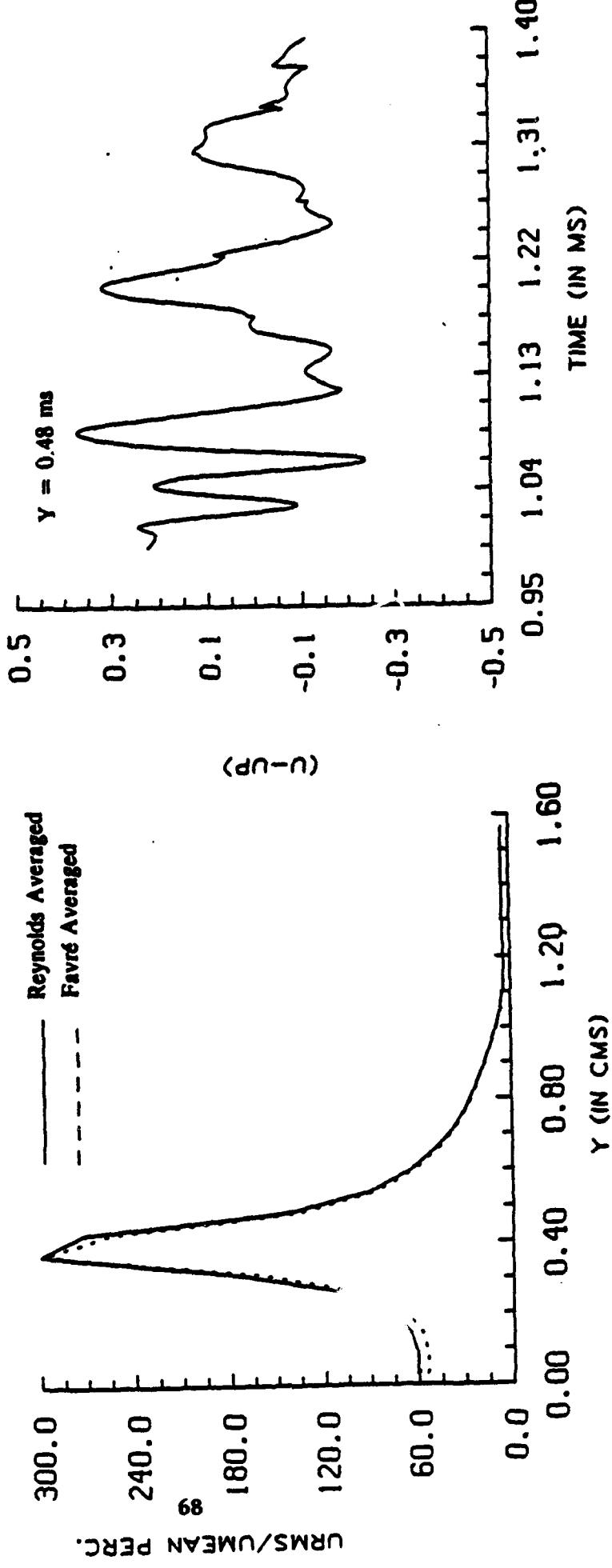
અને એવા કાળીઓની પણ જરૂર હોય કે આ કાળીની લાંબીતા કાઢી રહેની ચાહેરી હોય.

અને એવા કાળીઓની પણ જરૂર હોય કે આ કાળીની લાંબીતા કાઢી રહેની ચાહેરી હોય.

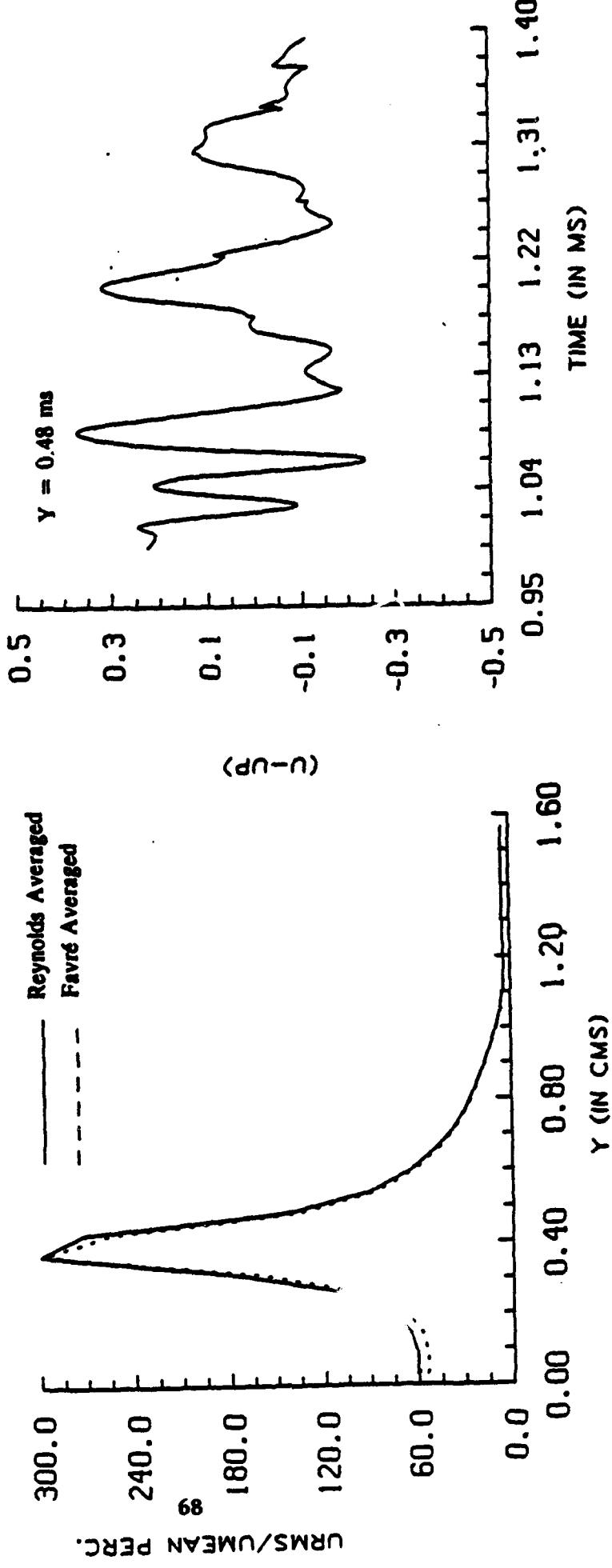
અને એવા કાળીઓની પણ જરૂર હોય કે આ કાળીની લાંબીતા કાઢી રહેની ચાહેરી હોય.

**TURBULENCE CHARACTERISTICS IN ULLAGE TUBE
17.5 cms FROM PROJECTILE BASE**

(A) Radial Variation of U_{rms}



(E) Instantaneous Axial Velocity at $y=0.48$ cms



LES vs RNS OVERVIEW / INCOMPRESSIBLE

1. DECOMPOSITION

- LES $u = \bar{u} + u'$ \bar{u} - *resolvable*
 u' - *nonresolvable*

- RNS $u = \bar{u} + u'$ \bar{u} - *mean*
 u' - *fluctuating*

2. AVERAGING

- LES → SPATIAL FILTER TO ELIMINATE HIGH FREQUENCY COMPONENTS

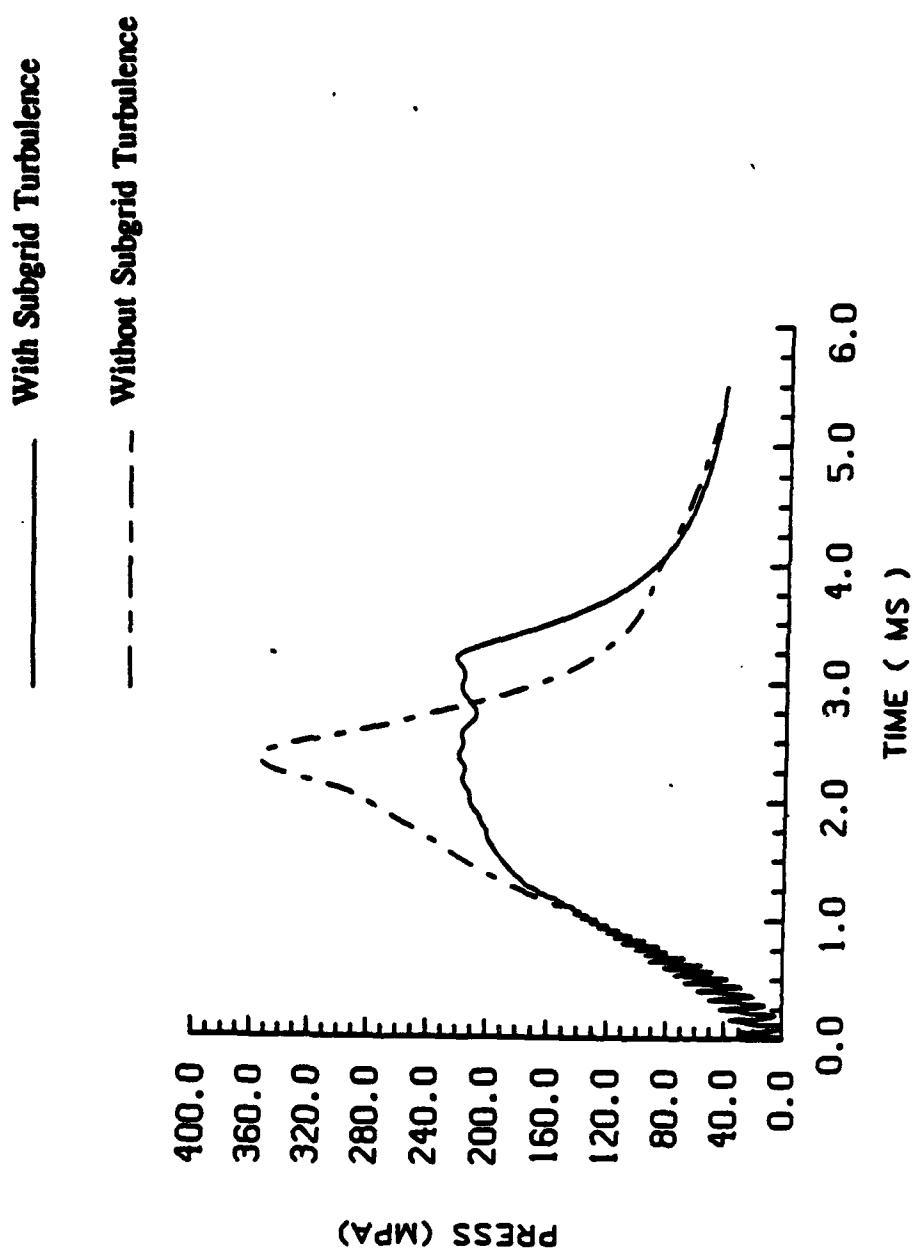
- RNS → TIME-AVERAGING, INTERVAL MUST BE LARGER THAN CONVECTIVE MOTION OF LARGE SCALE STRUCTURE; NOT APPLICABLE FOR SHORT-DURATION FLOWS

3. TERMS FROM AVERAGING

- LES $\overline{\overline{u'_i u'_j}} + (\overline{\overline{u_i u_j}} - \overline{u_i} \overline{u_j}) + (\overline{u_i} u'_j - u'_i \overline{u_j}) \rightarrow$ INVARIANT ?

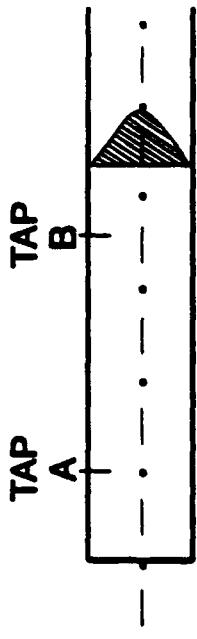
- RNS $\overline{\overline{u'_i u'_j}} \rightarrow$ NOT INVARIANT, COEFFICIENTS ARE PROBLEM-DEPENDENT

**COMPARISON OF PRESSURE HISTORY WITH
AND WITHOUT SUBGRID TURBULENCE**



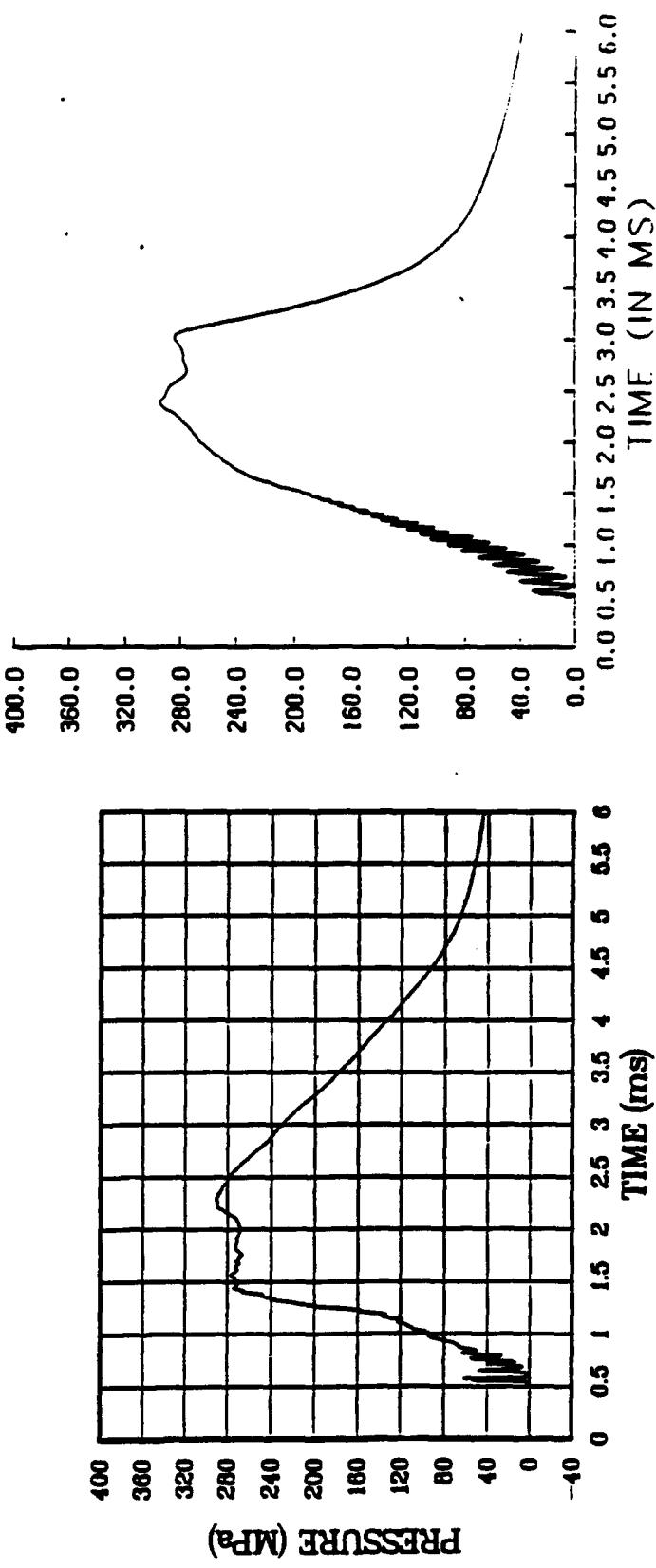
PRESSURE HISTORY AT TAP A

EXPERIMENTAL DATA vs NUMERICAL COMPUTATION FOR FMC SHOT 17

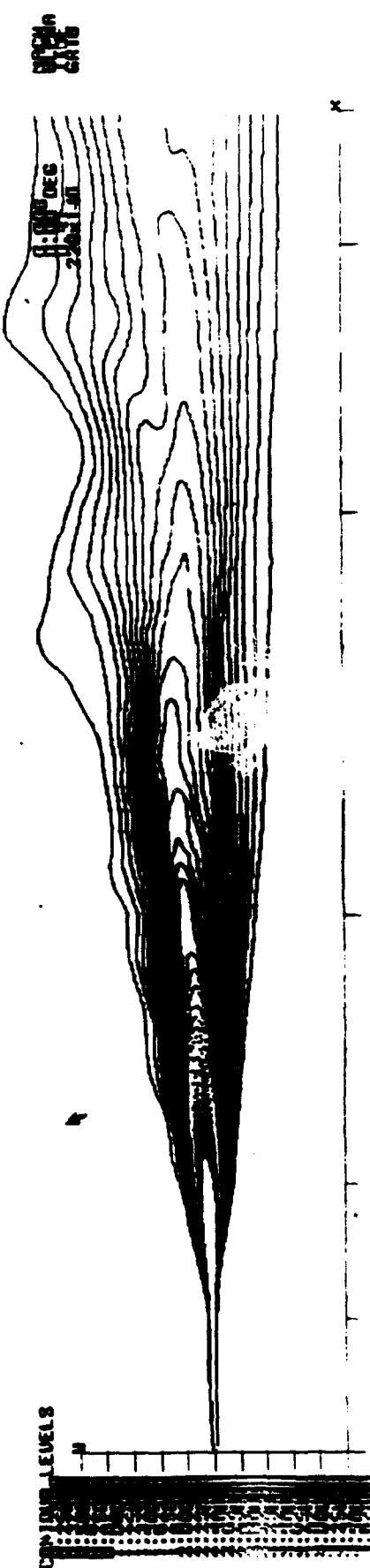
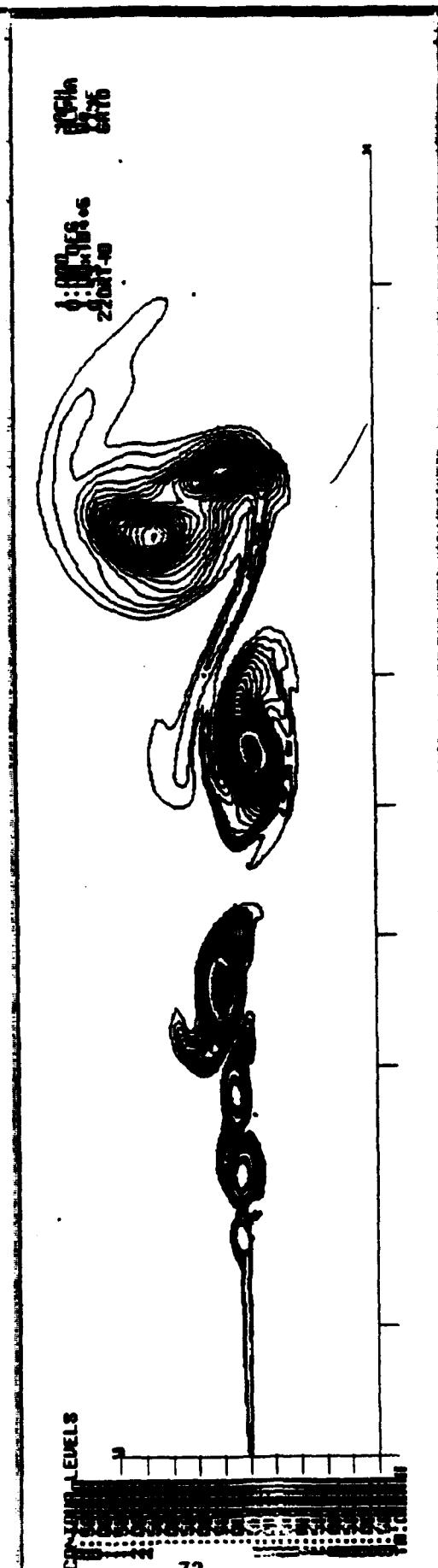
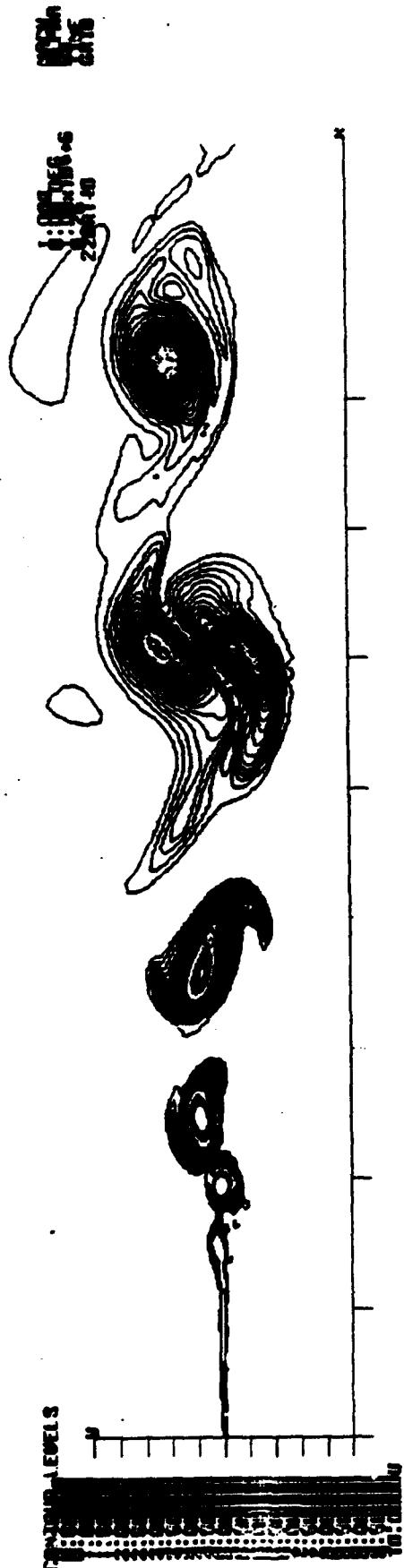


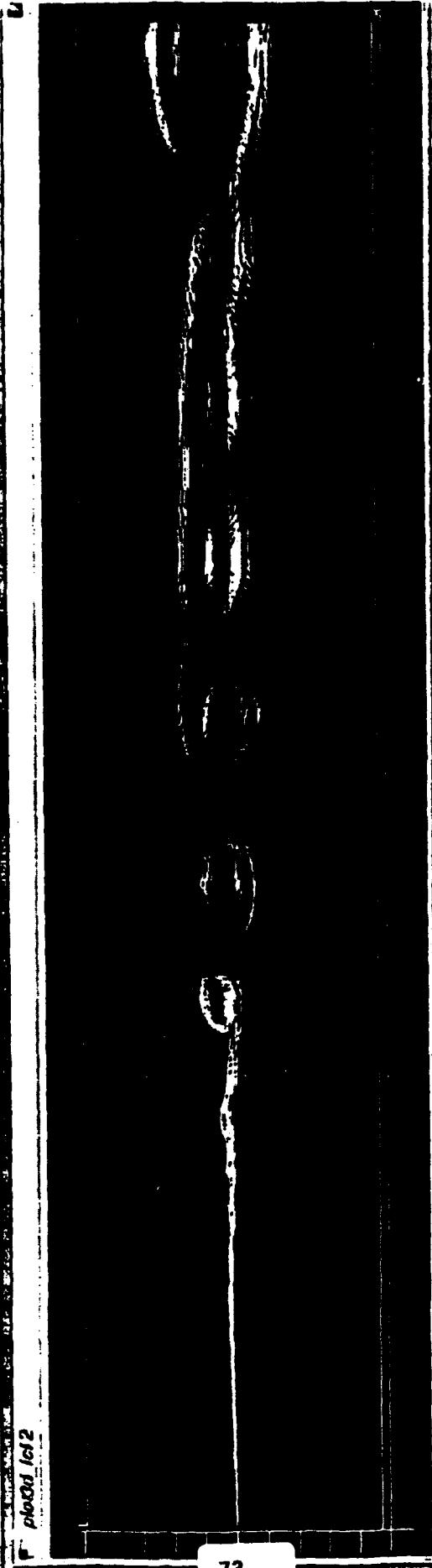
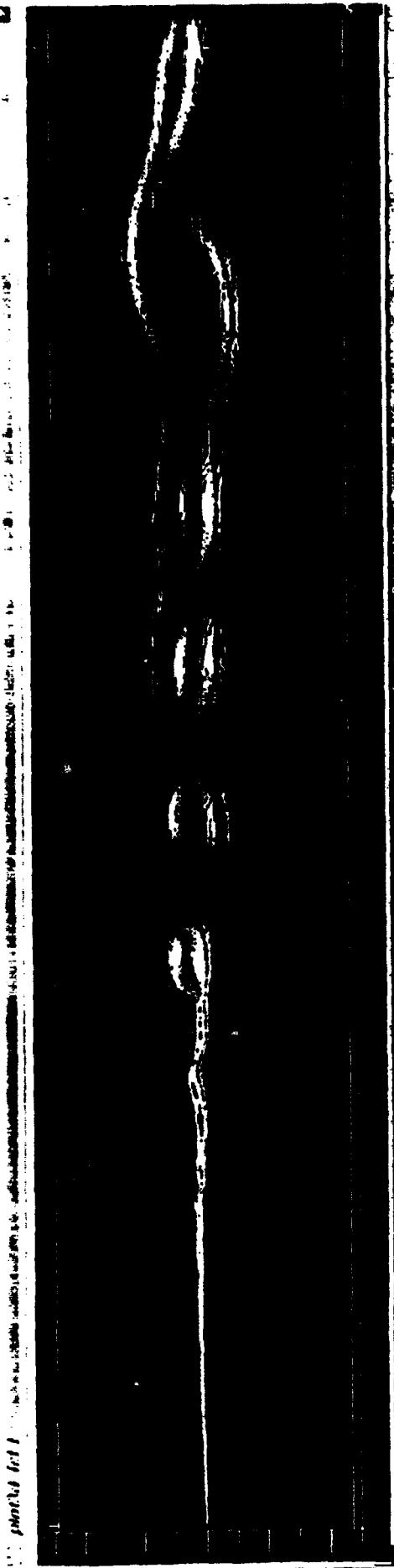
EXPERIMENTAL DATA

NUMERICAL COMPUTATION



Z-COMPONENT OF WINDICITY





F photo 1 of 2

73

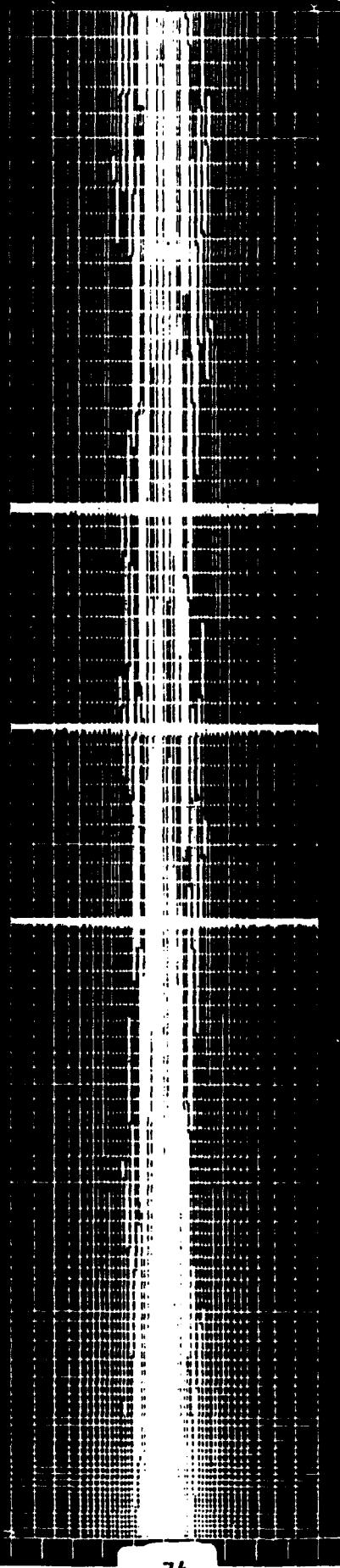


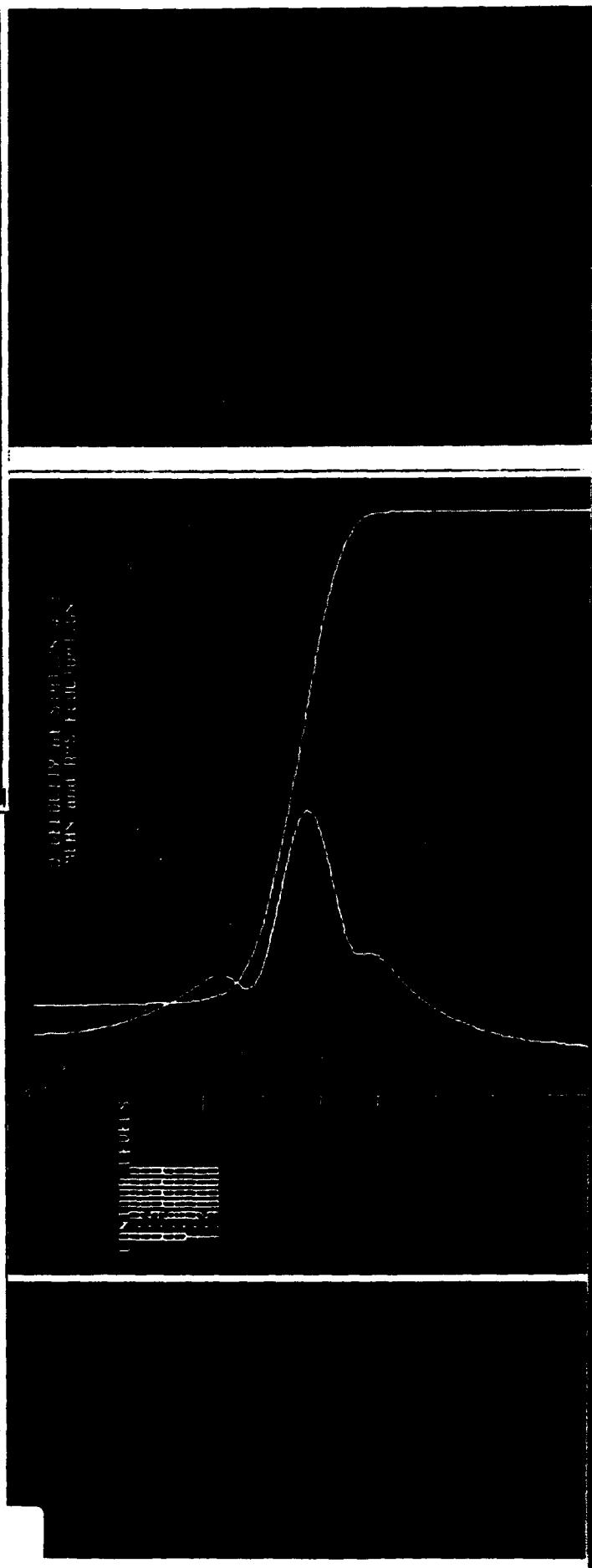
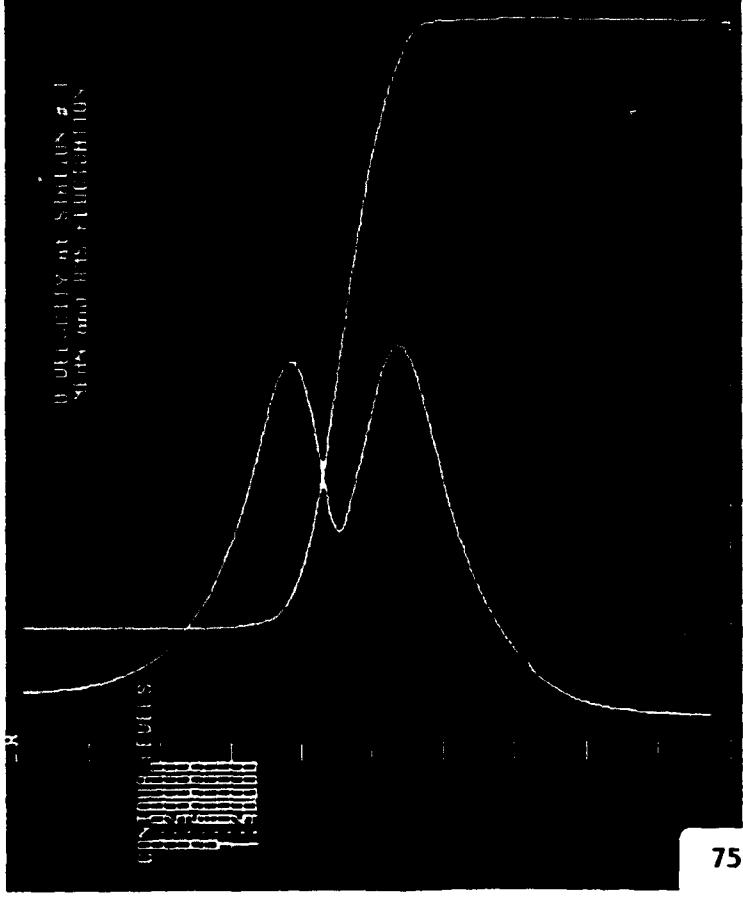
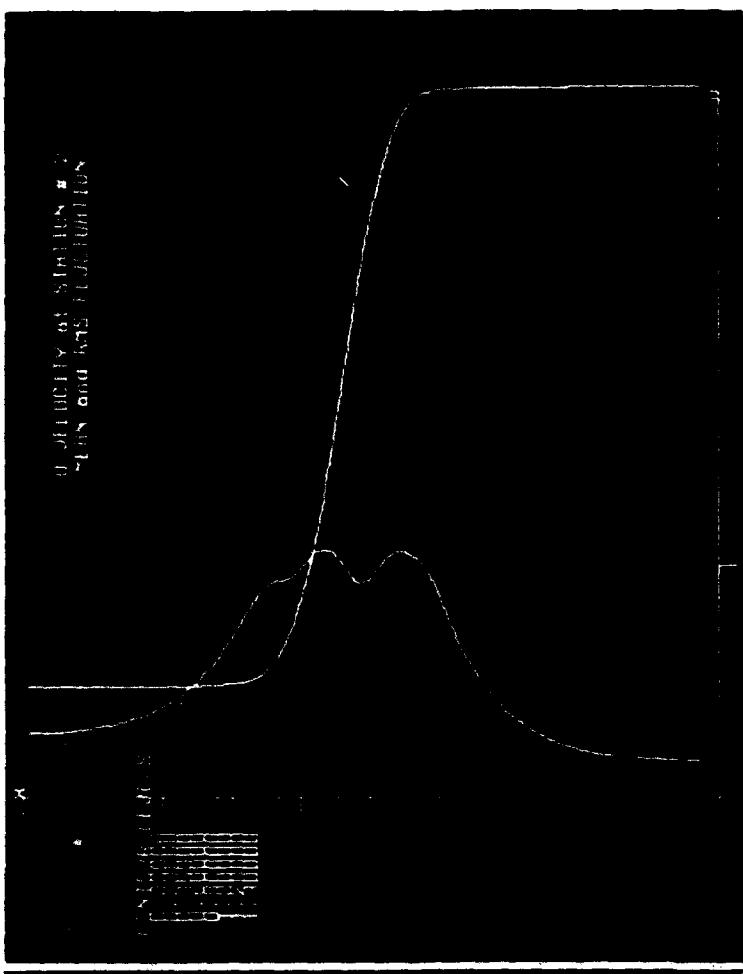
F photo 1 of 3

170

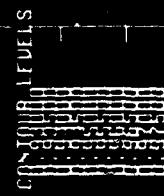
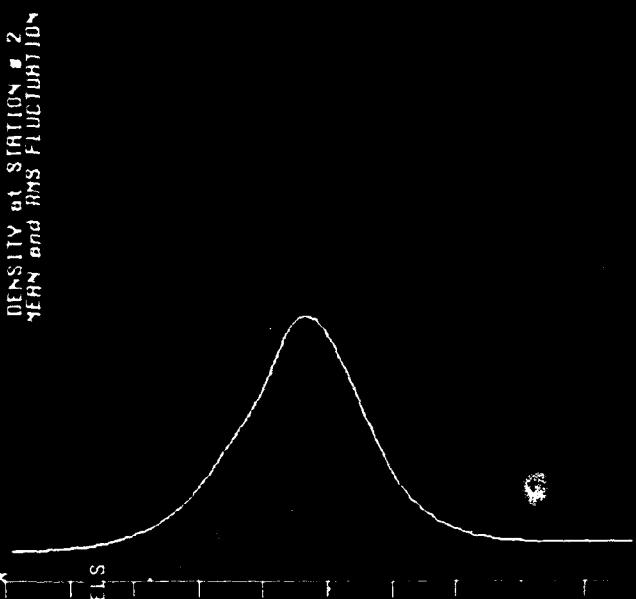
EFFICACY OF VACCINES IN CHILDREN
FOR SEVERE ACUTE RESPIRATORY SYNDROME

111 Selected Test I

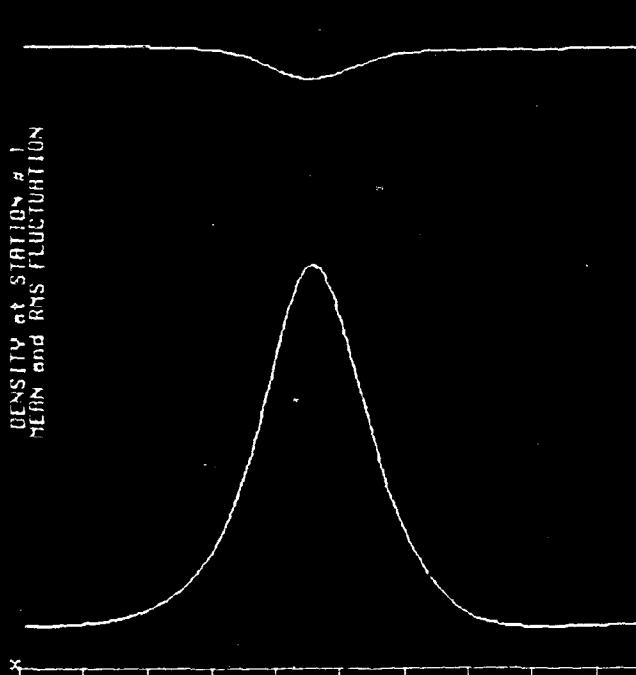




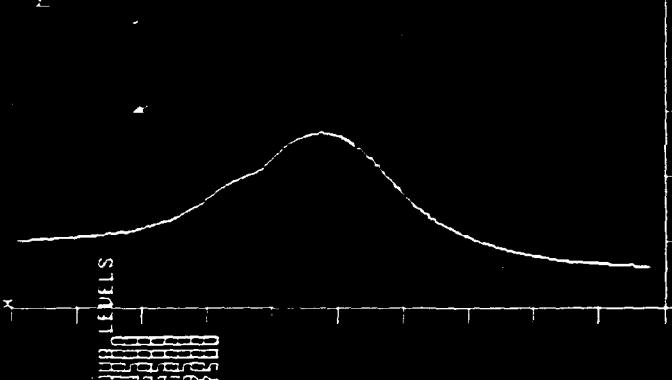
DENSITY at STATION # 2



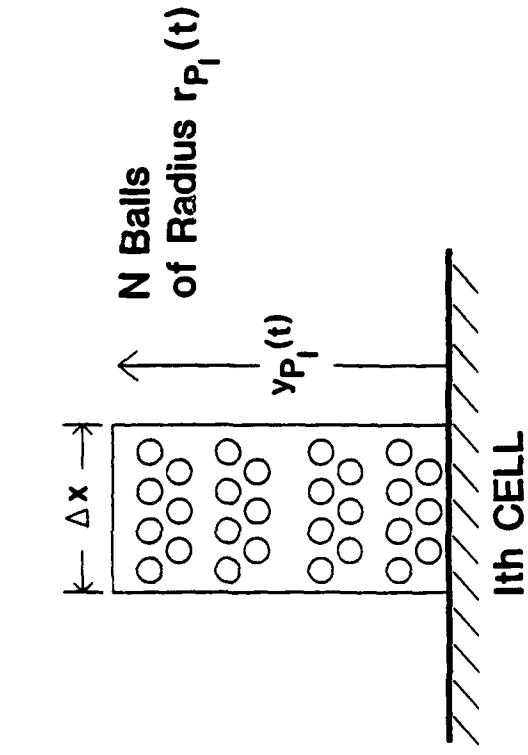
DENSITY at STATION # 1



DENSITY at STATION # 2



PRELIMINARY SOLID PROPELLANT BURNING MODEL



- FIXED-BED ASSUMPTION
- ALL BALLS IN EACH CELL BURN AT SAME RATE
- $r_p(t)$ TRACKED IN EACH CELL
- PRESSURE DEPENDENT BURN RATE
 - EXTERNAL SURFACE PRESSURE
 - UTILIZED WHICH VARIES AXIALLY

$$\text{MASS OF PROPELLANT IN CELL} = M_p = \frac{4}{3}\pi r_p^3 \times \rho_p \times N$$

RADIUS CHANGE:

$$r_p \rightarrow r_p - (\dot{r}) \Delta t \quad \{ \dot{r} \text{ function of pressure} \}$$

MASS CHANGE:

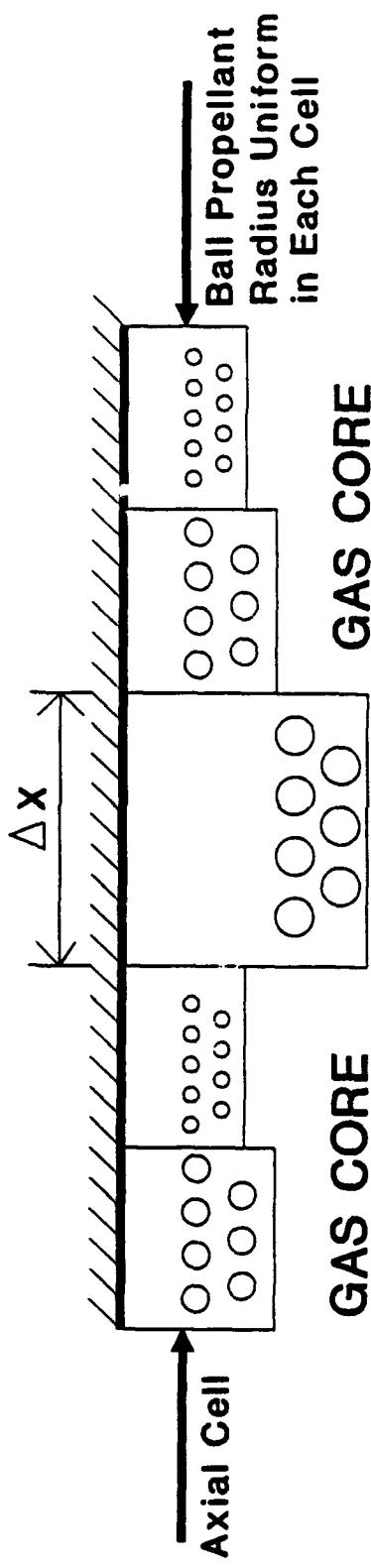
$$\dot{m} = (4\pi r_p^2) \dot{r} \rho_p \times N$$

REGRESSION VELOCITY:

$$V_s = \frac{\dot{m}}{\rho L} \quad \{ \rho L \text{ is loading density} \}$$

COMBUSTION PRODUCT FLUX: $\rho_s V_s = \rho_L V_s$

COUPLING OF SOLID PROPELLANT BURN MODEL INTO CRAFT

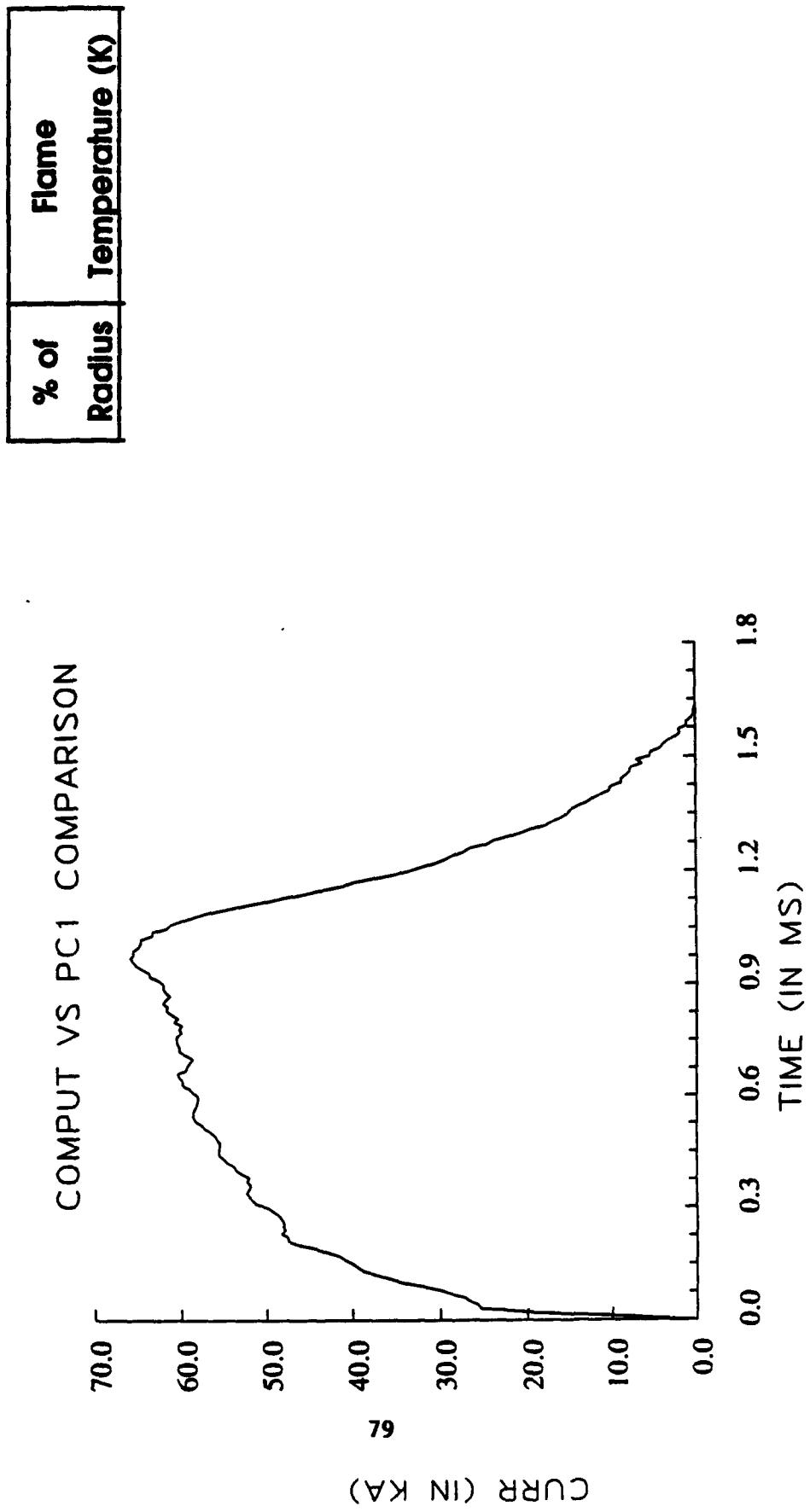


- BURNING RATE FUNCTION OF LOCAL SURFACE PRESSURE
- GASEOUS PRODUCTS MASS AND ENERGY FLUXES FROM SOLID PROPELLANT SERVE AS BOUNDARY CONDITIONS
- DYNAMIC MOTION OF RECESSING SOLID PROPELLANT ACCOUNTED FOR

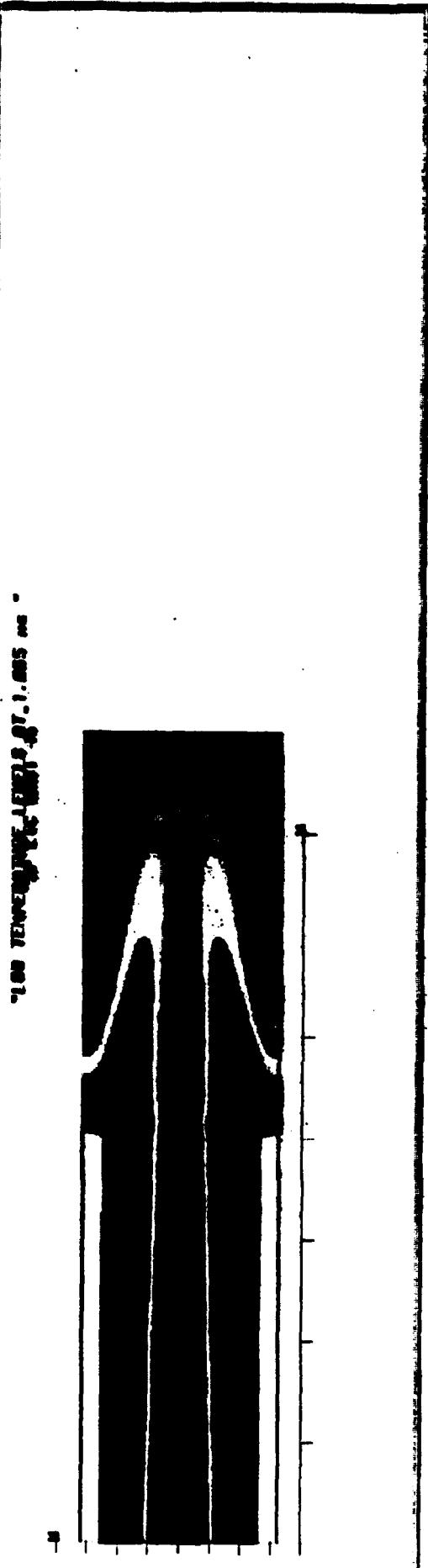
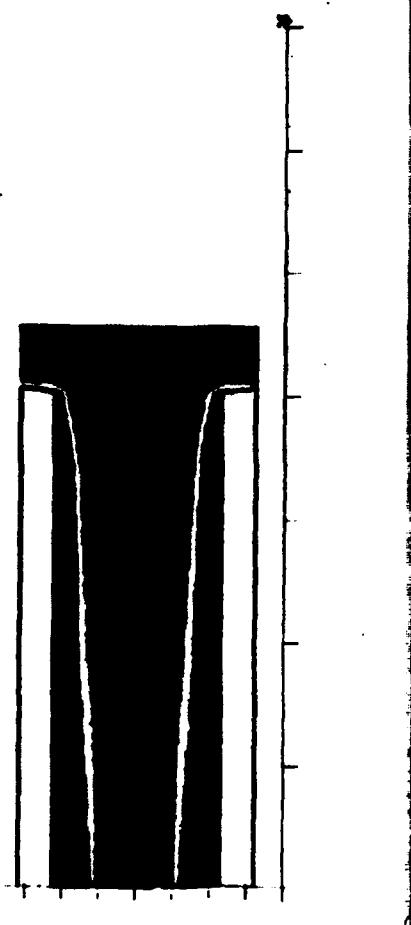
GDLS SHOT 45 INPUT DATA

CURRENT HISTORY

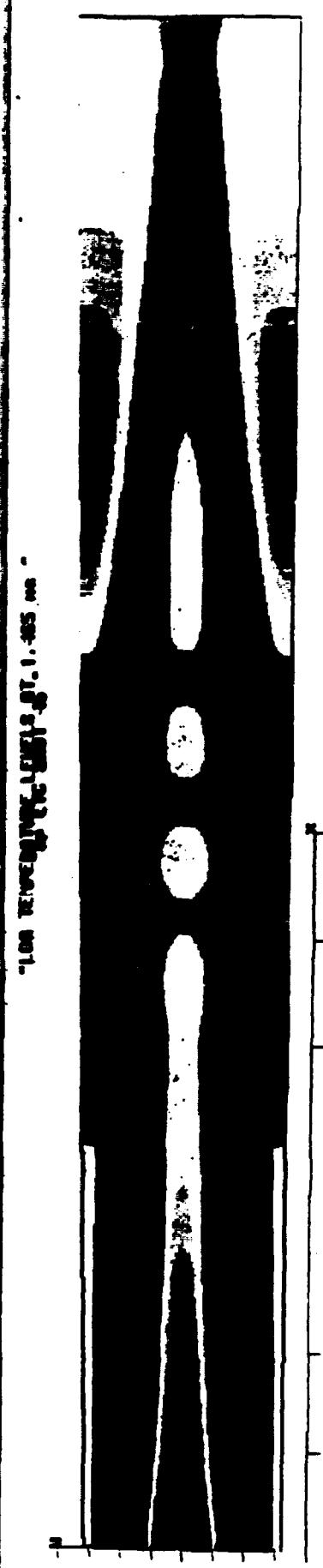
15 LAYER THERMOCHEMISTRY



• 80. 100% THERMOPOLYESTER 20.00% POLY(1,4-DIISOPROPYL-BENZYLIC ACID)



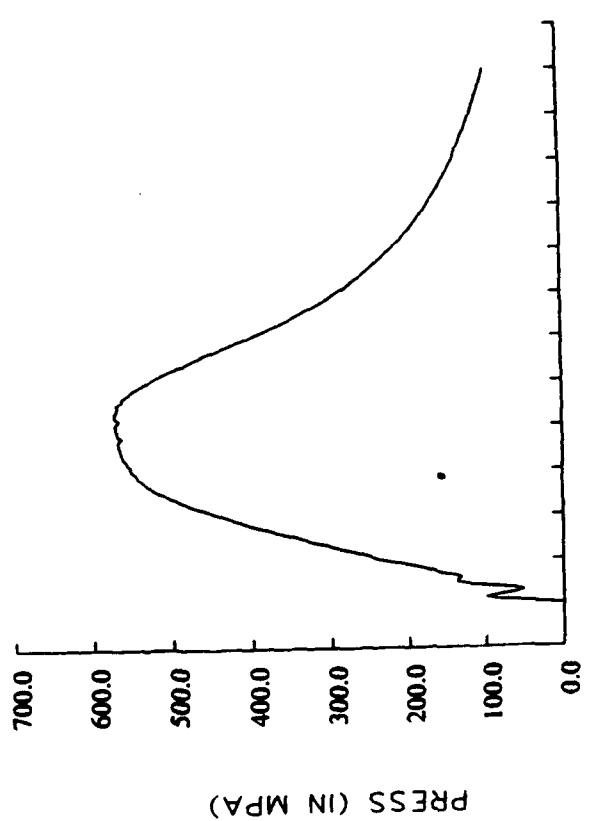
• 81. 100% THERMOPOLYESTER 20.00% POLY(1,4-DIISOPROPYL-BENZYLIC ACID)



GDLS SHOT 45

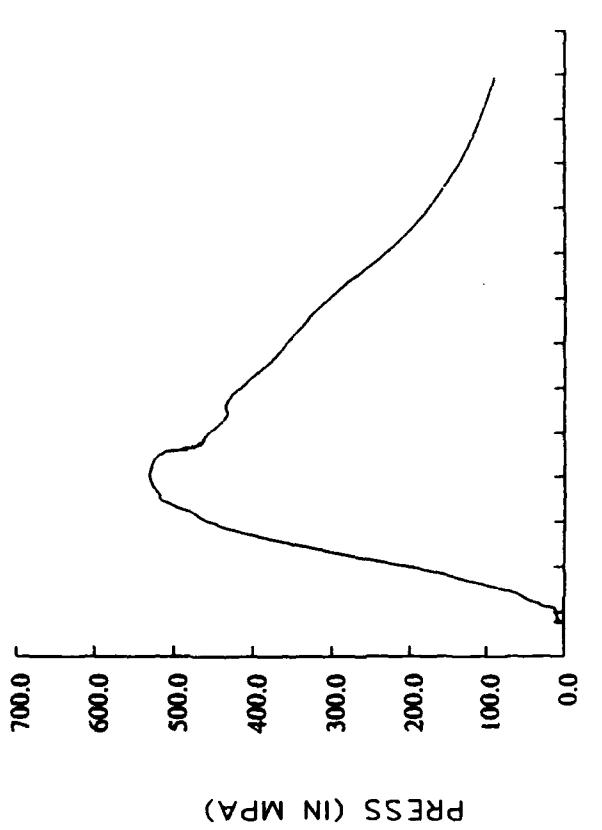
PRESSURE HISTORY COMPARISON AT PORT 1

EXPERIMENTAL PRESSURE



0.0 0.2 0.4 0.6 0.8 1.0 1.2 1.4 1.6 1.8 2.0 2.2 2.4 2.6 2.8
TIME (IN MS)

COMPUTED PRESSURE



0.0 0.2 0.4 0.6 0.8 1.0 1.2 1.4 1.6 1.8 2.0 2.2 2.4 2.6 2.8
TIME (IN MS)

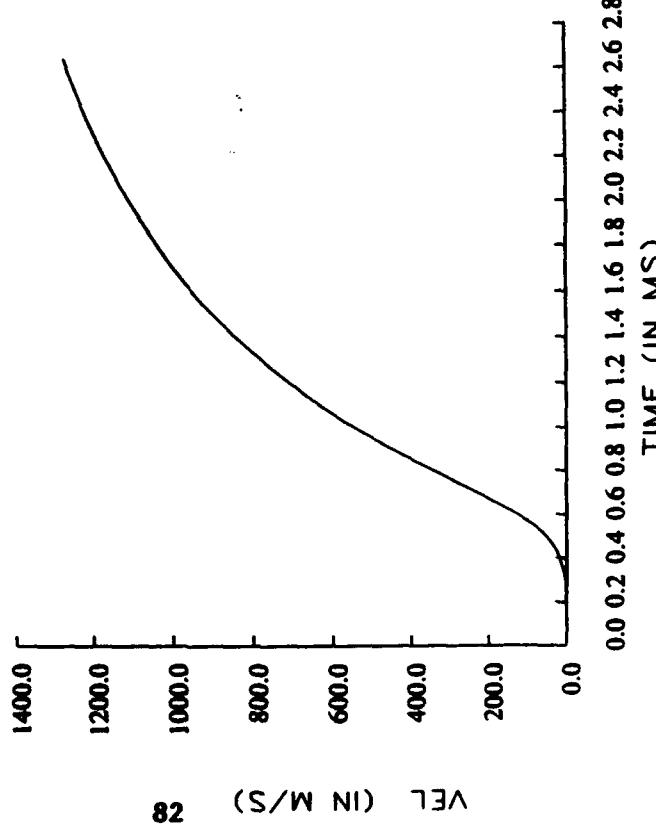
GDLS SHOT 45

PROJECTILE DYNAMICS vs TIME

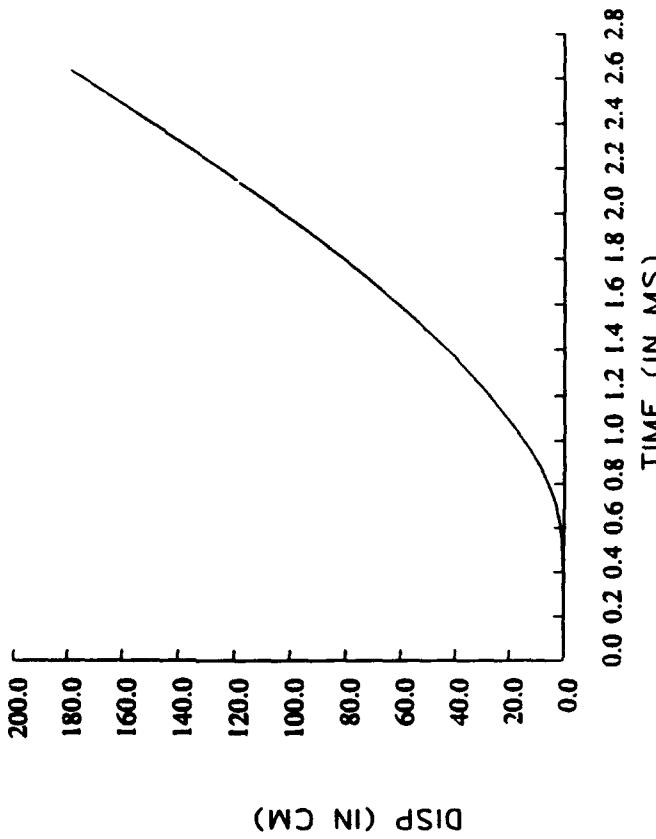
EXPERIMENTAL EXIT VELOCITY AT 130.5 cm = 1170.0 m/s

NUMERICAL EXIT VELOCITY AT 130.5 cm = 1183.75 m/s

VELOCITY



DISPLACEMENT



GDLS SHOT 122 INPUT DATA

CURRENT HISTORY

7 LAYER THERMOCHEMISTRY



CURR VS TIME

20.0

16.0

12.0

8.0

4.0

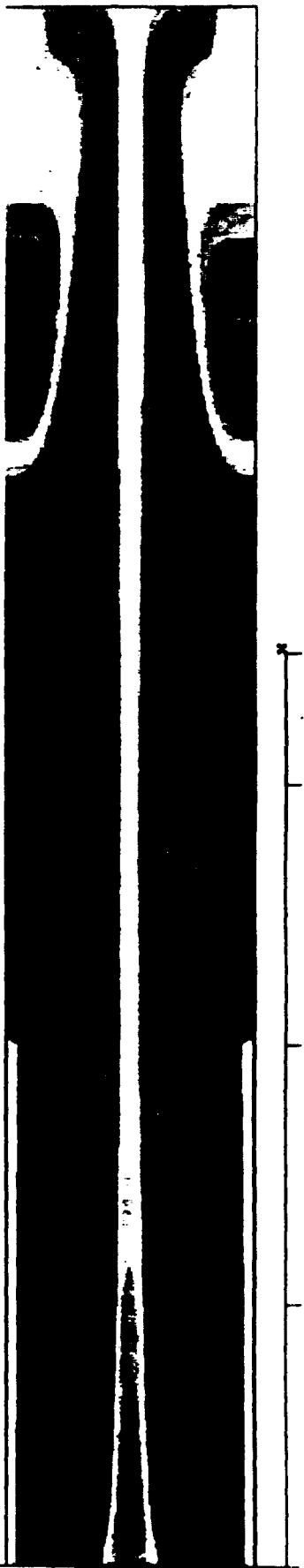
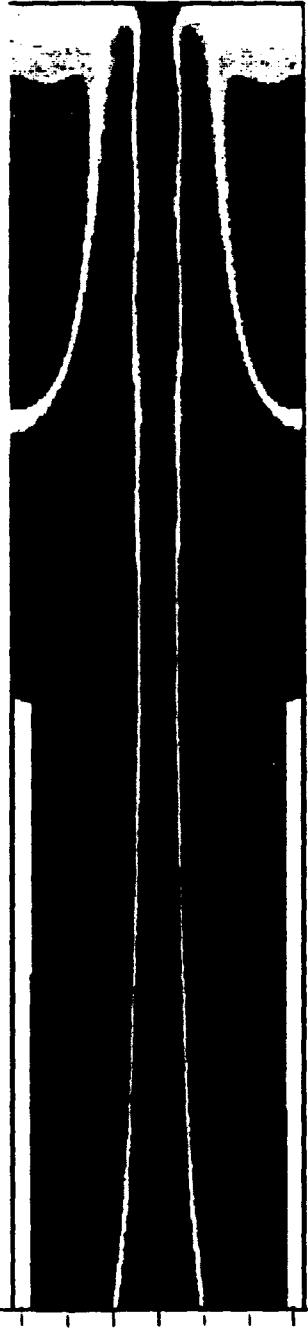
0.0

CURR (IN KA)

0.0 0.4 0.8 1.2 1.6 2.0
TIME (IN MS)

• 1.00 वार्षिक अवधि के लिए 1.77 रु.

- 1.00 वार्षिक अवधि के लिए 1.77 रु.

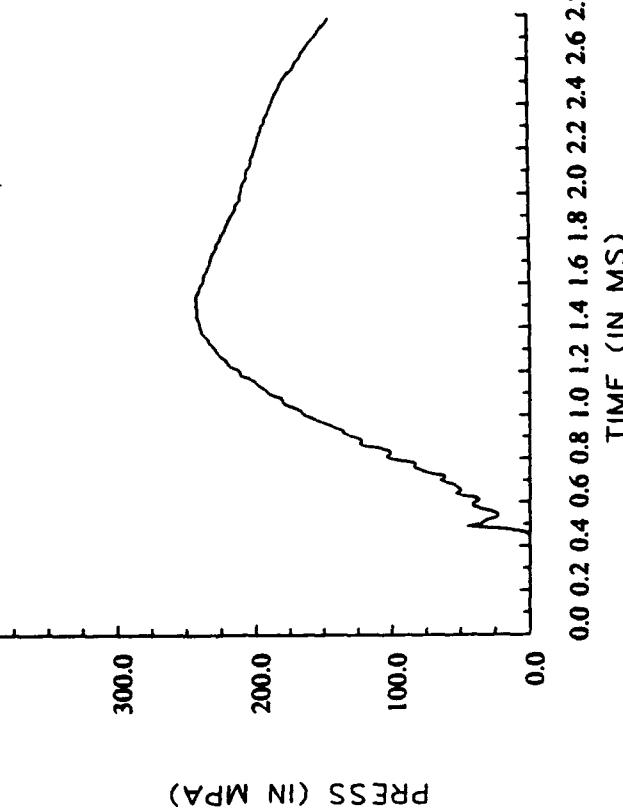


GDLS SHOT 122

PRESSURE HISTORY COMPARISON AT PORT 1

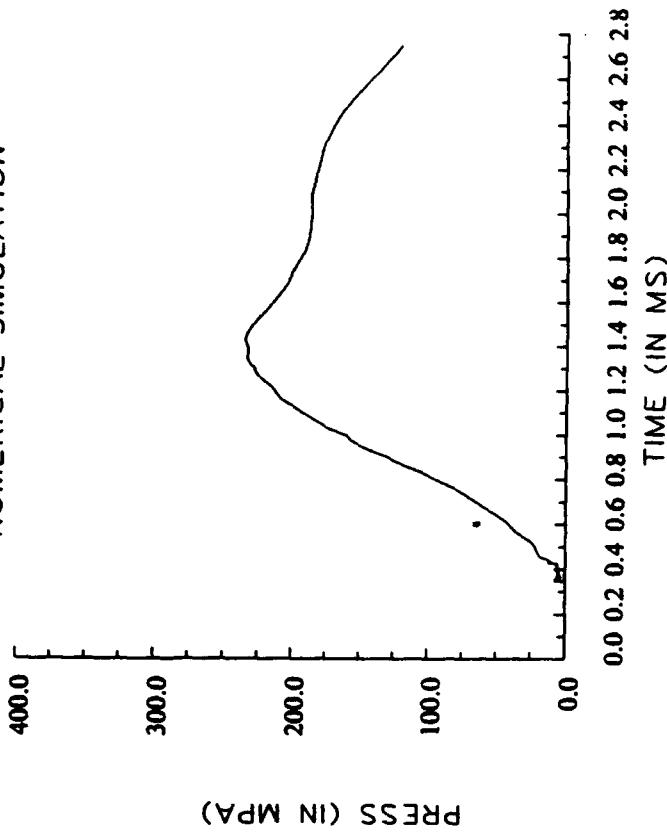
EXPERIMENTAL PRESSURE

EXPERIMENTAL MEASUREMENT



COMPUTED PRESSURE

NUMERICAL SIMULATION



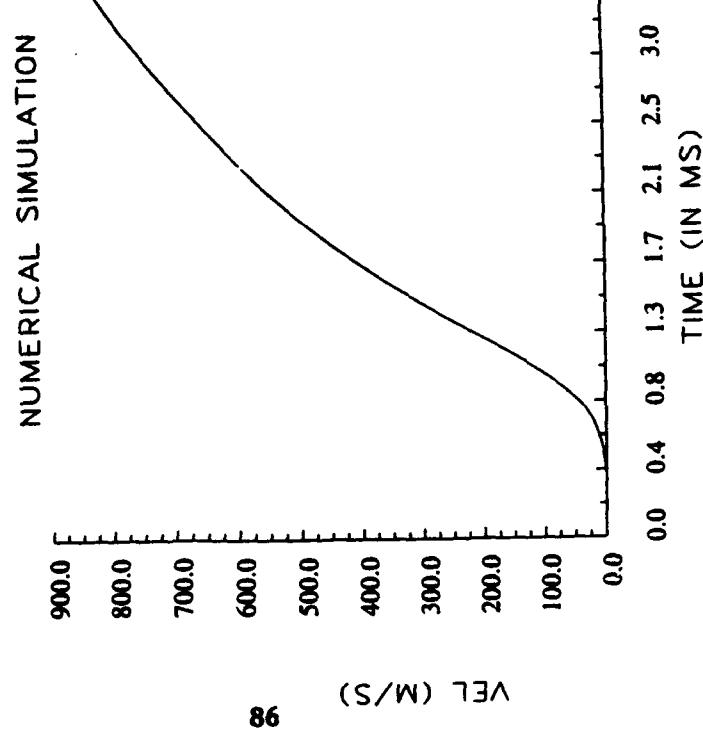
GDLS SHOT 122

PROJECTILE DYNAMICS vs TIME

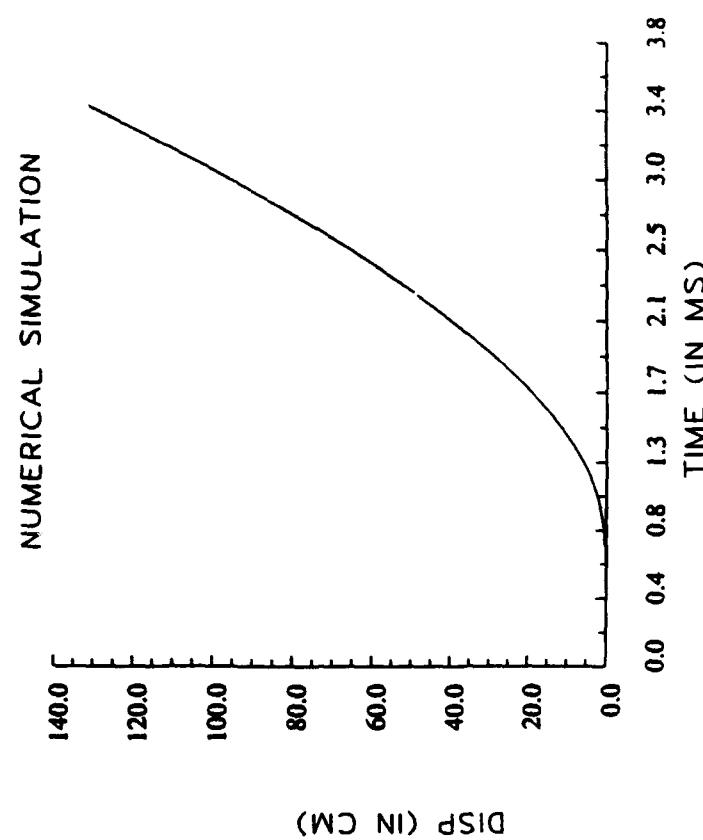
EXPERIMENTAL EXIT VELOCITY AT 130.7 cm = 857 m/s

NUMERICAL EXIT VELOCITY AT 130.7 cm = 837 m/s

VELOCITY



DISPLACEMENT



FUTURE DIRECTION

LP/ETC – PLASMA/WORKING FLUID INTERFACE

- DROPLET FORMATION/CONVECTION/COMBUSTION
- EULERIAN PARTICLE SOLVER OPERATIONAL IN CRAFT
- STRONG NONEQUILIBRIUM COUPLING
- VOLUMETRIC CONTRIBUTIONS

SP/ETC – FLUIDIZED BED/PARTICLE EROSION

- PARTICLE CONVECTION/COMBUSTION
- LAGRANGIAN PARTICLE SOLVER OPERATIONAL IN CRAFT

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Transient, Two-Dimensional Numerical Model of Plasma Behavior in an ETC Capillary

S. N. Kempka, M. W. Glass, D. A. Benson, D. W. Kuntz, G. F Homicz
Sandia National Laboratories
Fluid and Thermal Sciences Department
Albuquerque, NM

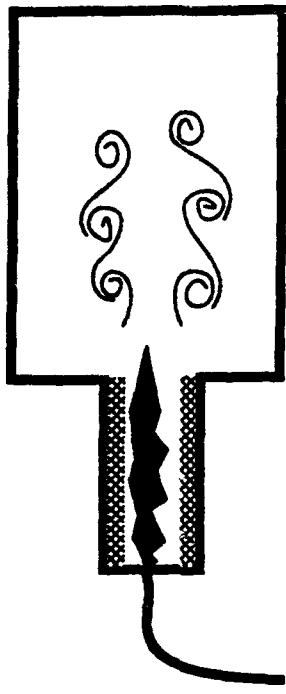
Work sponsored by Army Research Laboratory
ARL contact: Gloria Wren



ETC Objectives/Issues



- ETC Propulsion Objective: Initiate and control combustion with a plasma
 - use a strong, sustained plasma jet to avoid LP combustion instabilities
 - plasma flow provides significant mixing during combustion process
 - control combustion by electrically controlling plasma discharge
- Issue: Lack of repeatability
 - is plasma behaving as expected?



Overview



- General Approach: Combined experimental and modelling effort
 - non-combustion capillary discharge (SNL experiments)
- Review of Plasma Phenomena
- Motivation for multi-dimensional, transient model
- Phenomenological models
 - turbulence
 - ablation
 - thermal radiation
 - electrical power dissipation: electric field, electrical conductivity
 - plasma initiation
- Demonstration calculation: simulation of SNL experiment ET038

Modelling Focus: Plasma Nonuniformities

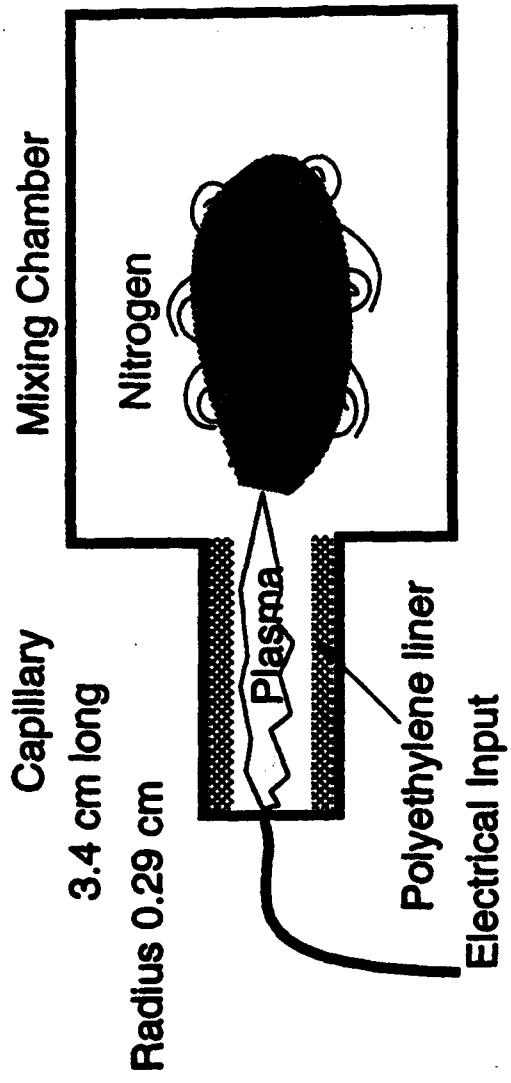


- **Modeling Objective:** Do plasmas behave as expected? (~ isothermal?)
 - Non-uniformity not unlikely in a positive feedback system:
ohmic deposition increases with increasing temperature
 - Evidence of plasma non-uniformities:
throughput limit, repeatability problems, 1D model
- **Importance of plasma behavior on ETC Performance:**
 - Power dissipation: controls plasma flow rate
 - Scaling: relationship of small-scale data to large-scale performance

SNL Capillary Discharge Experiments

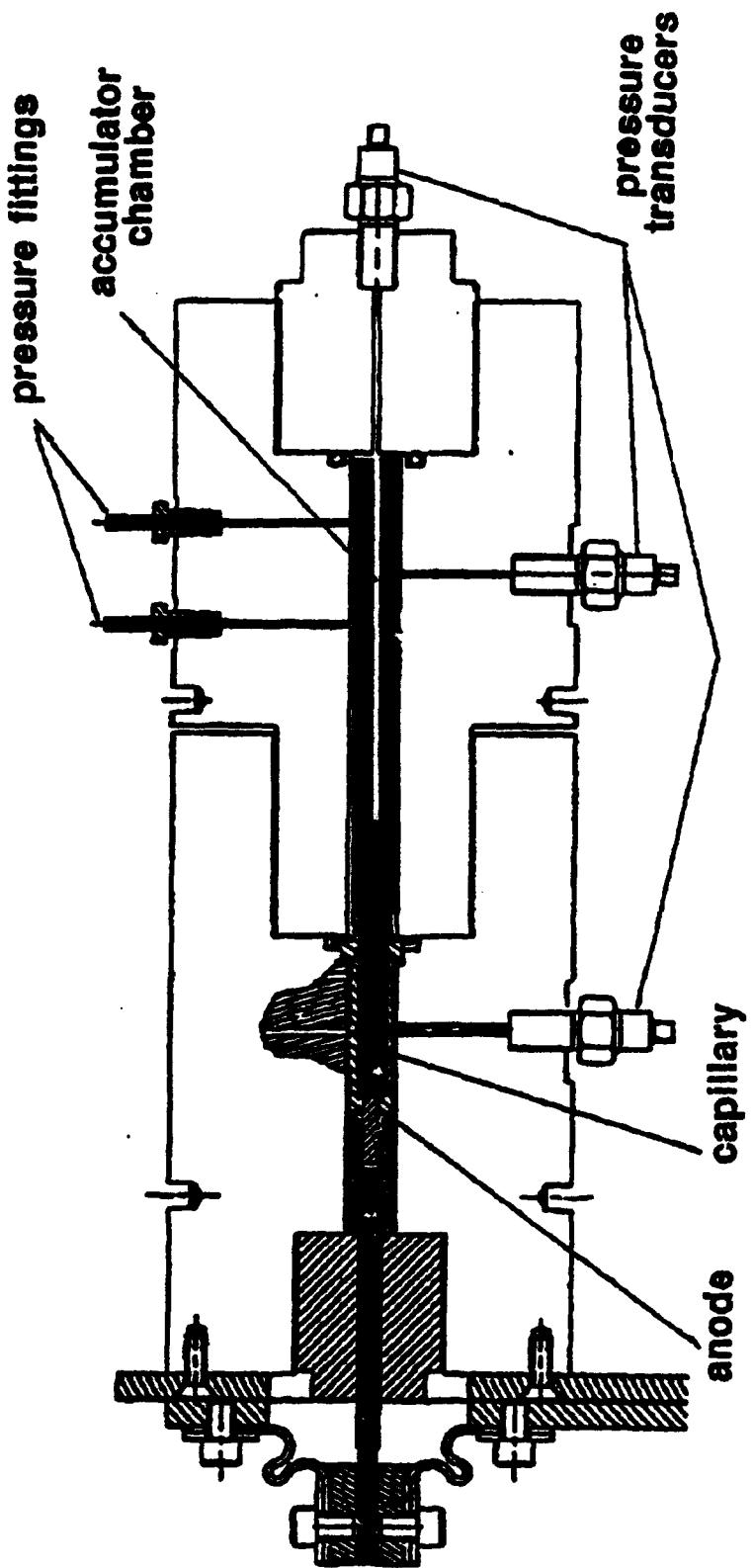


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- pulsed power system charged to 4.0 kV, 3.2 kJ stored energy
- system pre-pressurized to 1000 psi, nitrogen - no propellant
- ablating polyethylene capillary liner

Experimental Setup

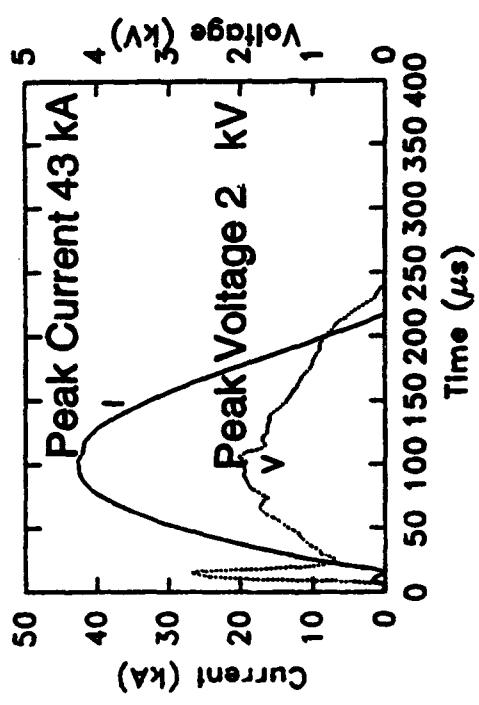


Capillary Discharge Data

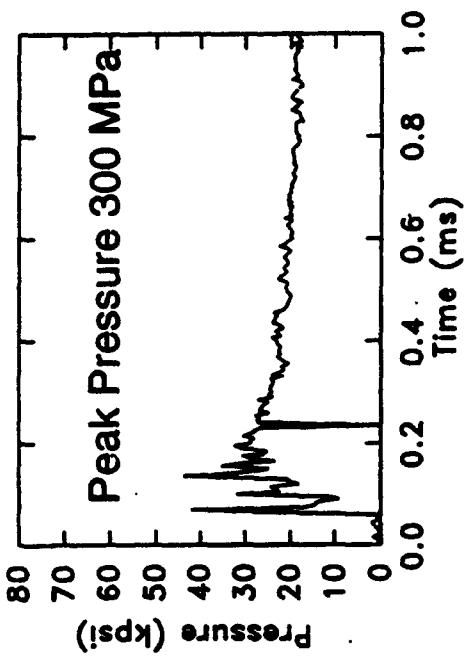
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Capillary Current and Voltage vs Time



Capillary Pressure vs Time



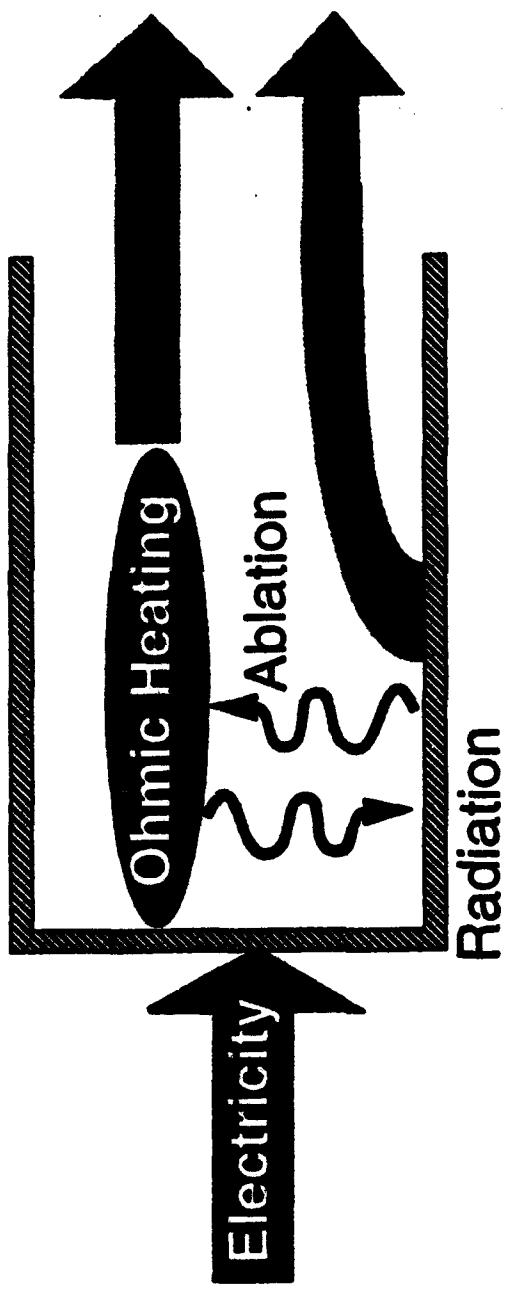
- Duration: ~ 200 μs, peak current occurs at 100 μs

- Mass of ablated polyethylene: 122 mg

Energy Transformation in an ETC Capillary



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- Electrical energy in = convective flow out

Motivation for 2D Transient Model

- Why 2D?



- plasma flow from capillary into mixing chamber is 2D
 - 2D Hydrodynamic coupling between capillary and mixing chamber
 - electric field and electric current could be 2D

- Why transient?

- assess assumption of steady-state: does it exist?
 - ablation rates are transient: only time-averaged rate data available
- Reduce reliance on experimental data in simulations
 - 1D models require Pressure, Electric Field, Current specifications
 - developing 2D model to require only voltage data

Model Description



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- Gas species, including dissociation and ionization
 - C, C⁺, C⁺⁺, H, H⁺, N₂, N, N⁺
 - Saha equations for ionization
 - Lighthill dissociation model for nitrogen
- Conservation equations: compressible mass, momentum, energy
- Ohmic heating due to transient applied voltage difference
 - 2D Electric field based on transient voltage data
 - plasma electrical conductivity: ion-electron, neutral-electron terms
- Radiative transport: Method of Discrete Ordinates
 - Zel'dovich and Raizer model for gas absorptance
- Ablation of polyethylene
- Ideal Gas Equation of State

Governing Equations



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- Mass Conservation for species $i=C, H, N$ $\frac{\partial \rho_i}{\partial t} + \nabla \cdot (\rho_i \vec{u}) = 0$

- Conservation of Momentum $\frac{\partial}{\partial t}(\rho u_j) + \nabla \cdot (\rho u_j \vec{u}) = -\nabla P$

- Conservation of Energy

$$\frac{\partial}{\partial t}(\rho E) + \nabla \cdot (\rho \vec{u} (E + \frac{P}{\rho})) = \xi^2 \sigma + \nabla \cdot q_r$$

Thermal Radiation
Ohmic Heating
(Electric Field) 2 *Electrical Conductivity

Temperature Evaluation



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- Find temperature from energy values
 - Energy = thermal energy (lions, neutrals) + kinetic
 - All species, ions in a cell have the same temperature

$$\rho E = \rho |\bar{u}|^2 / 2 +$$

$$\sum_j \frac{3}{2} n_j k T (1 - (1 - \chi_{diss,j}) \Theta_{diss,j}) + n_j \chi_j^+ (\frac{3}{2} k T + I_j^t)$$

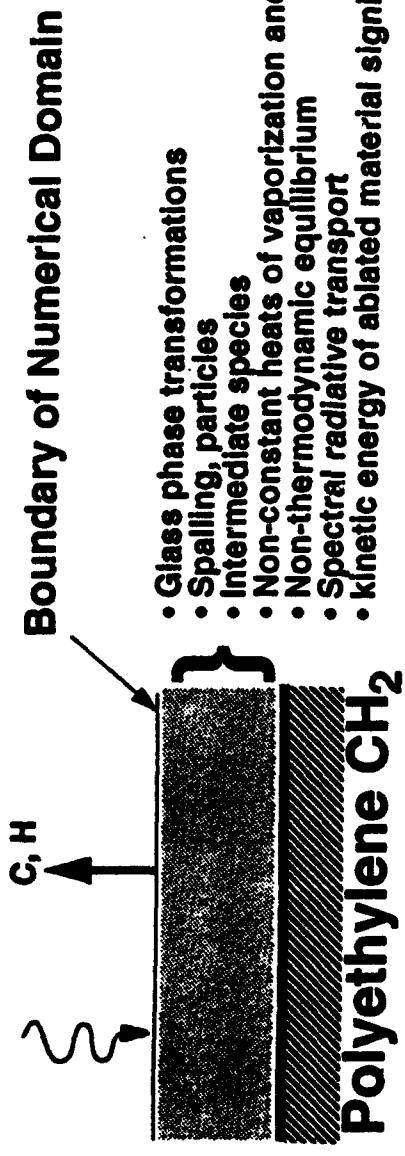
$$n_j \chi_j^{++} (3 k T + I_j^t + I_j^{++}) , n_j -$$

n_j number density, χ_j^+ - ionization fraction, I_j^t - ionization energy

Ablation



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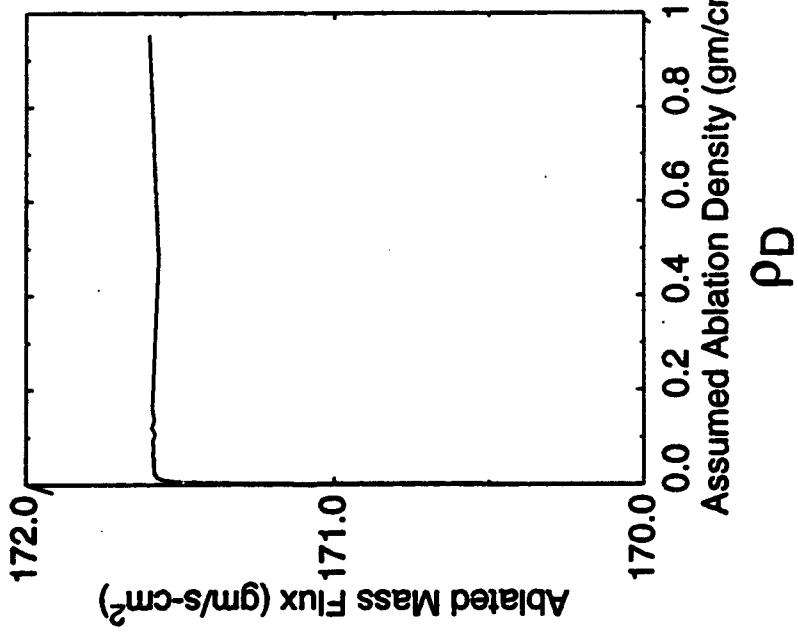


- Idealization of ablation equilibrium energy balance: incident radiation = ablative enthalphy flux

$$q''_{radiation} = \rho_D u \left\{ \frac{5}{2} R T_D + \frac{u^2}{2} + \gamma \right\}$$

- Assume dissociation temperature T_D, density ρ_D, latent heat γ
- Solve cubic equation for u, given radiative flux

Ablation Model Features

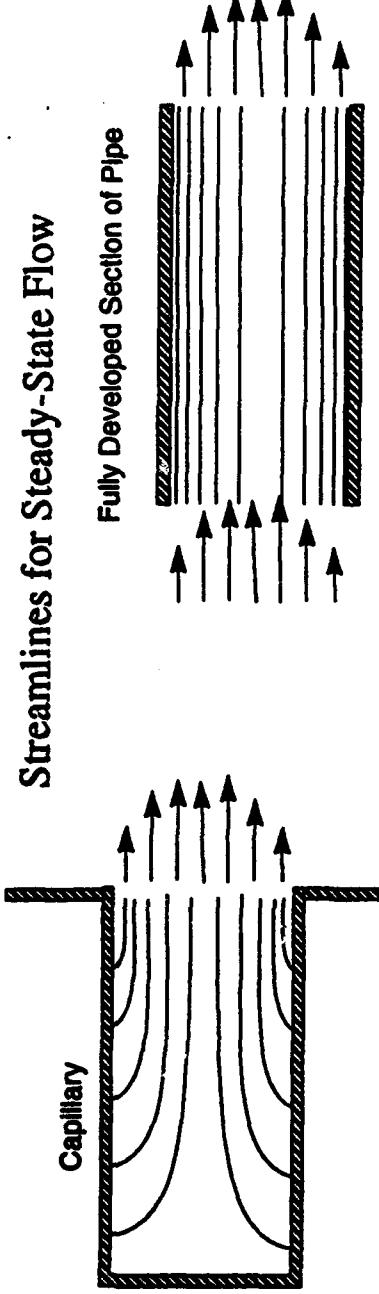


- Assume 4 eV blackbody heat flux
- Find that ablation mass flux is relatively insensitive to assumed polyethylene density
- Calculated ablation rate for ET038: 340 gm/s
- ET038 Ablation rate data (time-averaged) rate: 610 gm/s

Turbulence in ETC Capillaries



- Need to assess importance of turbulence



- Compare capillaries to pipe flows
 - no flow at back wall, no development length - turbulence questionable
 - different boundary conditions (capillary wall blowing drives flow)
 - volumetric heat source
 - radiation

Turbulence In ETC Capillaries, Cont'd



- Compare conductivities: fluid, turbulent, radiative

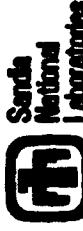
$$\rho C_p \frac{DT}{Dt} = \nabla \cdot [(k_{fluid} + k_{turbulence} + k_{radiation}) \nabla T]$$

typically, $k_{fluid} \ll k_{turbulence}$

- Compare $k_{radiation}$ and $k_{turbulence}$

- at $5 \text{ eV}, 10^{22} \text{ cm}^{-3}$ (1D model: significant radial variations)

Turbulence in ETC Capillaries, Cont'd



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- Turbulent conductivity (wall-generated turbulence)

- $k_{turbulence} \approx \mu_{turbulence} C_p$, $\mu_{turbulence} \approx O(10^2) \mu_{fluid}$

- Spitzer formula for plasma viscosity

$$k_{turbulence} \approx 9 \cdot 10^3 \text{ W/cm-eV}$$

- Radiative conductivity: Zel'dovich and Raizer

$$k_{radiation} \approx 3 \cdot 10^6 \text{ W/cm-eV}$$

- Radiation dominates wall-generated turbulence for this example

- radiation and turbulence are equivalent at 2 eV, where radial variations (due to radiation) are negligible

Turbulence In ETC Capillaries, Cont'd

Turbulent conductivity (wall-generated turbulence)



- Turbulent conductivity (free-shear layer turbulence)

$$k_{turbulence} \approx 9 \cdot 10^5 \text{ W/cm-eV}$$

- Radiative conductivity: Zel'dovich and Raizer

$$k_{radiation} \approx 3 \cdot 10^6 \text{ W/cm-eV}$$

- Radiation & free shear layer turbulent transport rates are similar
 - origin of free-shear layer turbulence: baroclinic vorticity generation
 - turbulence models inappropriate for transitional flow
- Approach: use no turbulence model, examine solution fields for waves

Electric Field Model



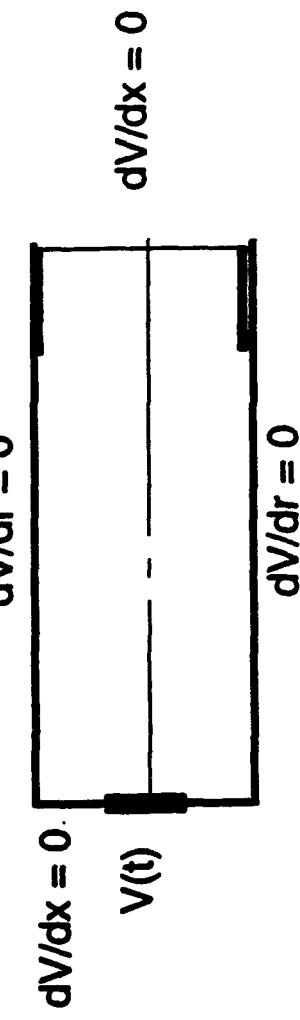
- Assume quasi-steady state

- Zero divergence of current

$$\nabla \bullet (\sigma(T) \nabla V(t)) = 0$$

- time t
- temperature T
- electrical conductivity σ
- ohmic heating: $\sigma(\nabla V \cdot \nabla V)$

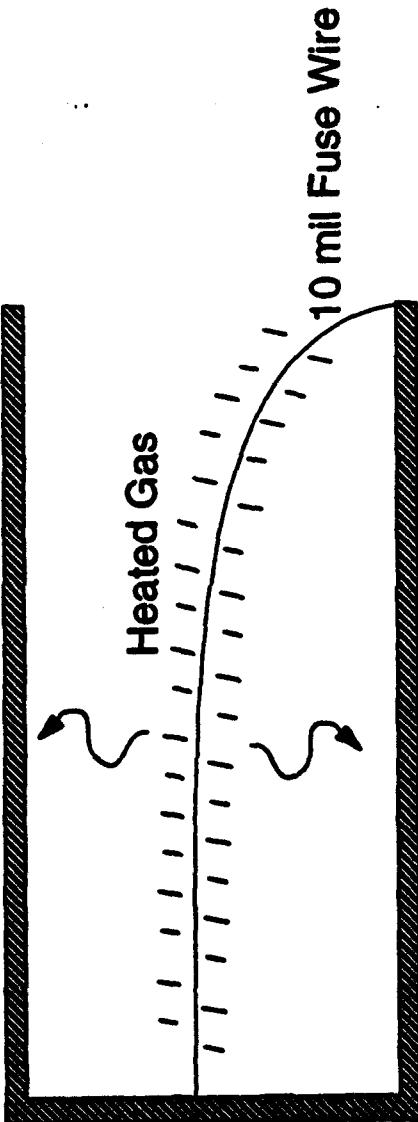
- Solver: Stabilized Error Vector Propagation (SEVP)



Plasma Initiation



Engineering Science Center



- Initially, all current carried by fuse wire
- At late times, ionized gas carries all the current
- How does this transition occur?

Uniform Power Deposition Calculation



Engineering Services Group

$$\frac{\partial}{\partial t} \left(\rho E \right) + \nabla \cdot \left(\rho \vec{u} \left(E + \frac{P}{\rho} \right) \right) = \xi^2 \sigma + \nabla \cdot q_r$$

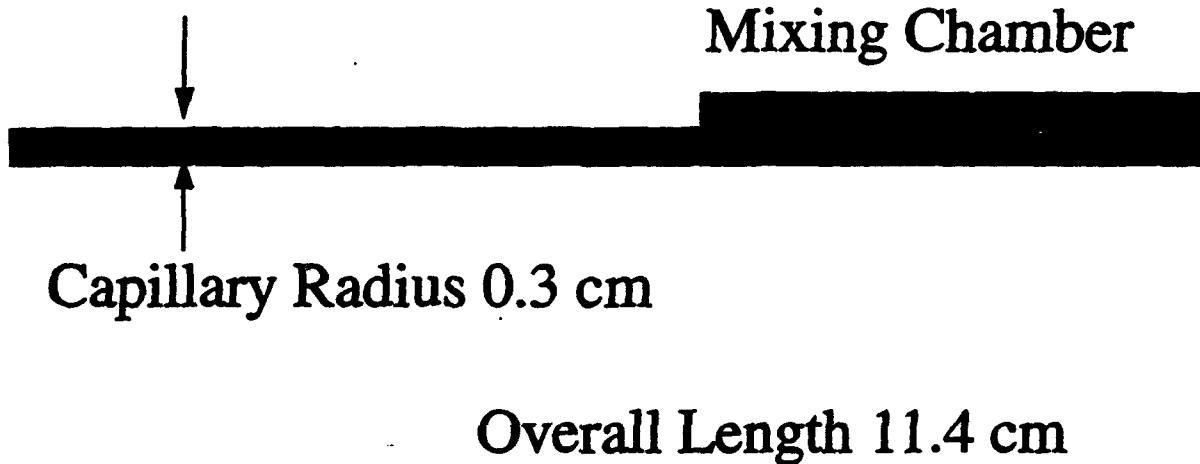
Thermal
Radiation

Ohmic Heating
 $(\text{Electric Field})^2 * \text{Electrical Conductivity}$
Replace with (Power data)/(Capillary Volume)

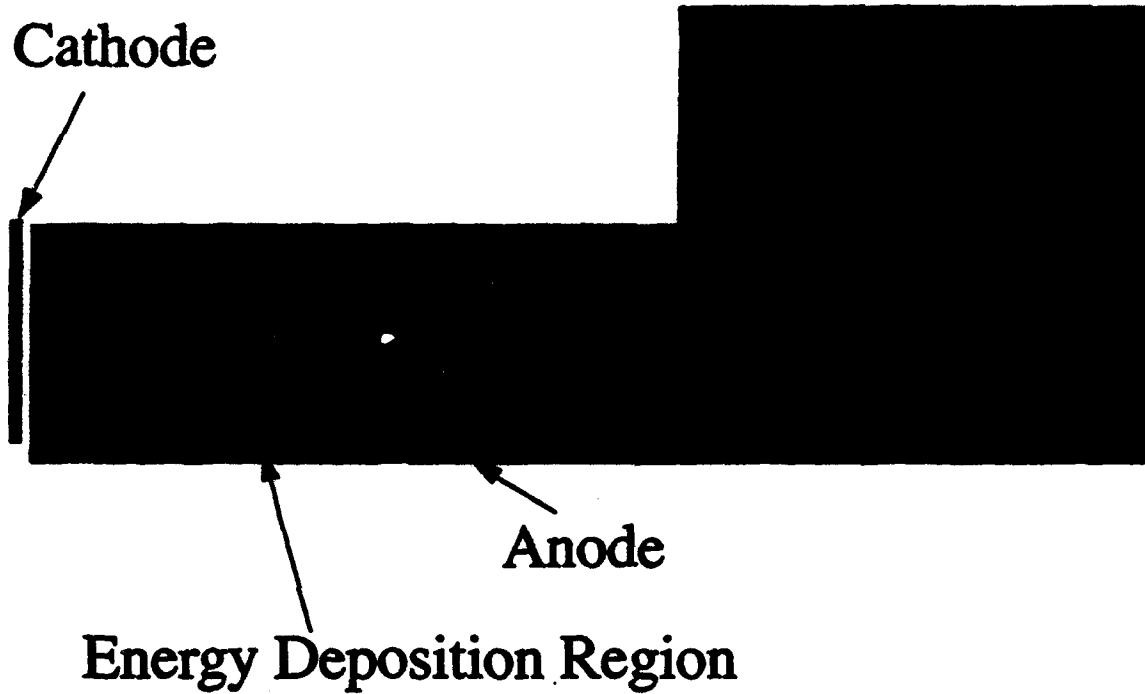
- Calculate ohmic heating given voltage data

- but don't use it, just compare with power data
- if ohmic heating agrees with power data:
 - Current will agree with data: power = voltage * current
 - Resistance will agree with data: power = voltage² / R

Axisymmetric Model of Capillary and Mixing Chamber



Distorted Geometry



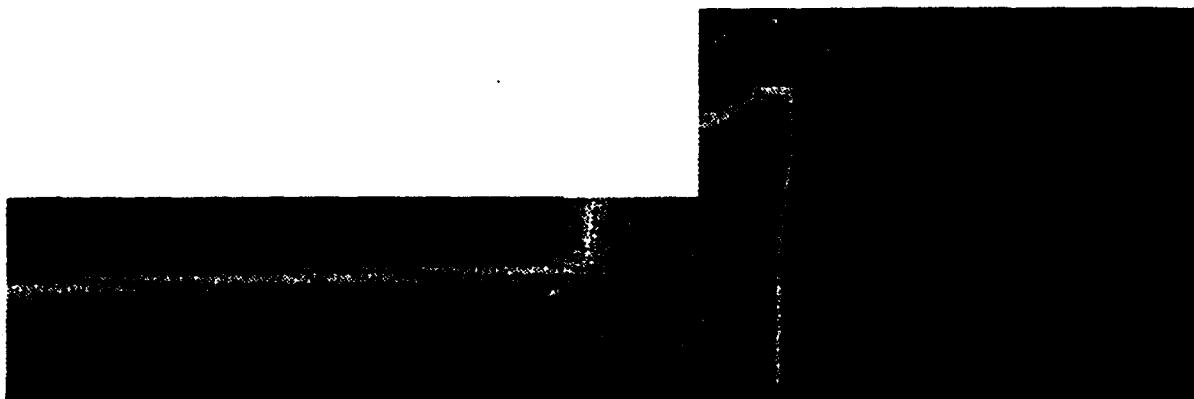
$100 \mu\text{s}$

Temperature (4.2 eV)



$200 \mu\text{s}$

Temperature (3.3 eV)



$100 \mu\text{s}$

Pressure



$200 \mu\text{s}$

Pressure



$100 \mu\text{s}$

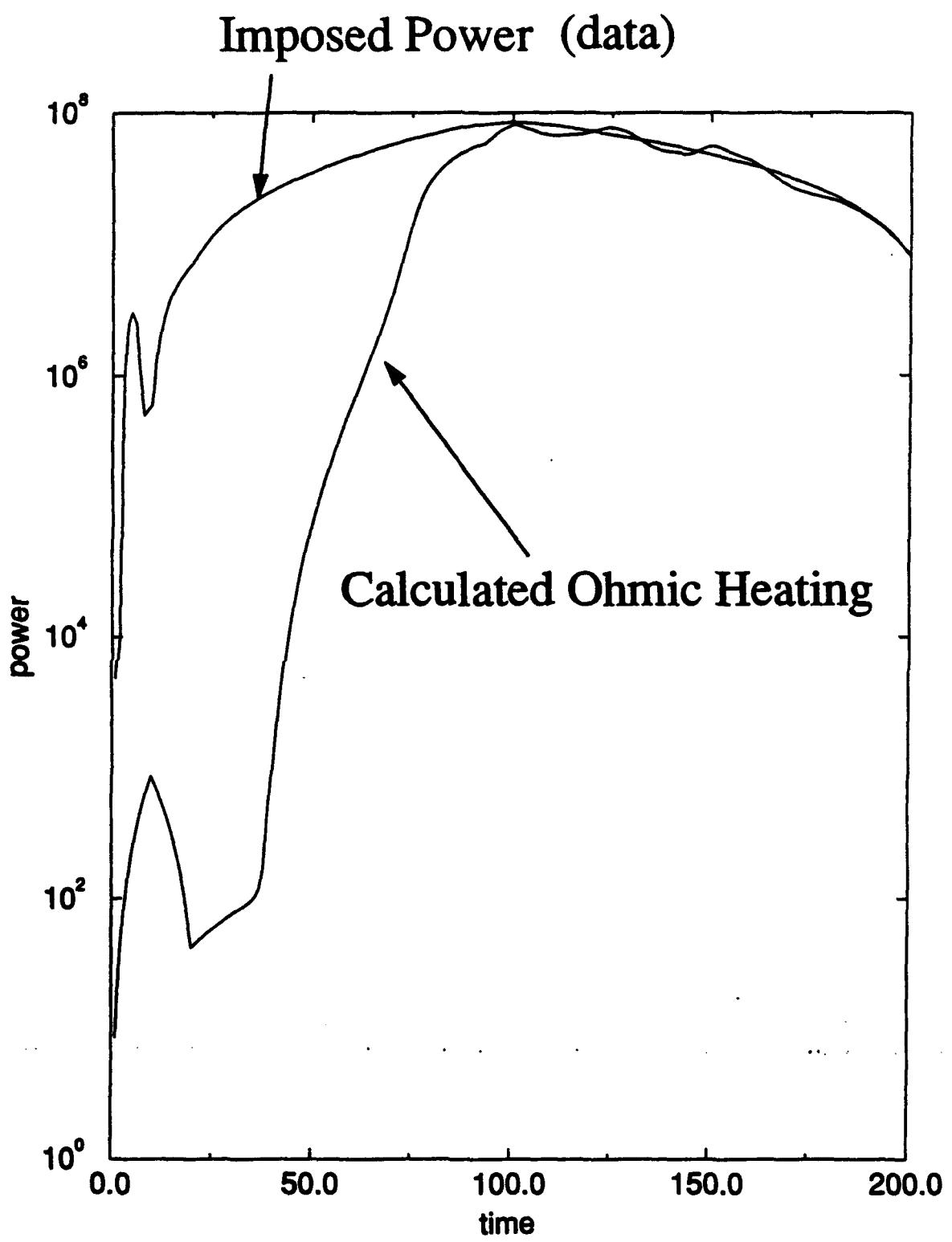
Polyethylene Density (10^{-3})



$200 \mu\text{s}$

Polyethylene Density (10^{-2})





Plasma Initiation, cont'd



Engineering Sciences Center



Centerline of Cartridge

- Radiative flux on polyethylene very small even if wire is initially hot
 - Ablated polyethylene is not an early participant
- Aluminum vaporizes, provides new electrical path
- Lee-More Model for aluminum electrical conductivity - progress

Summary



Engineering Sciences Center

- Two-dimensional, transient model formulation
 - ohmic heating (voltage data, electrical conductivity -> voltage field)
 - discrete ordinate thermal radiation
 - ablation model
 - ionization, dissociation
- Uniform Power Deposition calculation (no fuse wire)
 - Transient pressure larger than data
 - Ohmic heating small at early times, good at later times
 - electrical conductivity too low at early-time
- Work in progress: include fuse wire vaporization
 - provides high electrical conductivity at early times
 - convected out of cartridge by late times



FMC

In-Bore Doppler Radar Measurements Of Projectile Kinematics

Workshop on ETC Modeling
Army Research Laboratory
Aberdeen, Maryland
May 12 - 13, 1993

Patrick Janke, Senior Engineer
Jahn Dyvik, Staff Engineer
Advanced Armaments
FMC Naval Systems Division
Minneapolis, Minnesota
U.S.A.



OUTLINE

- Automated Data Acquisition, Transfer and Reduction
- In-Bore Radar Measurements of Projectile Kinematics
- Development of an Inverse Ballistic Model
- Conclusions

Electric Arrements

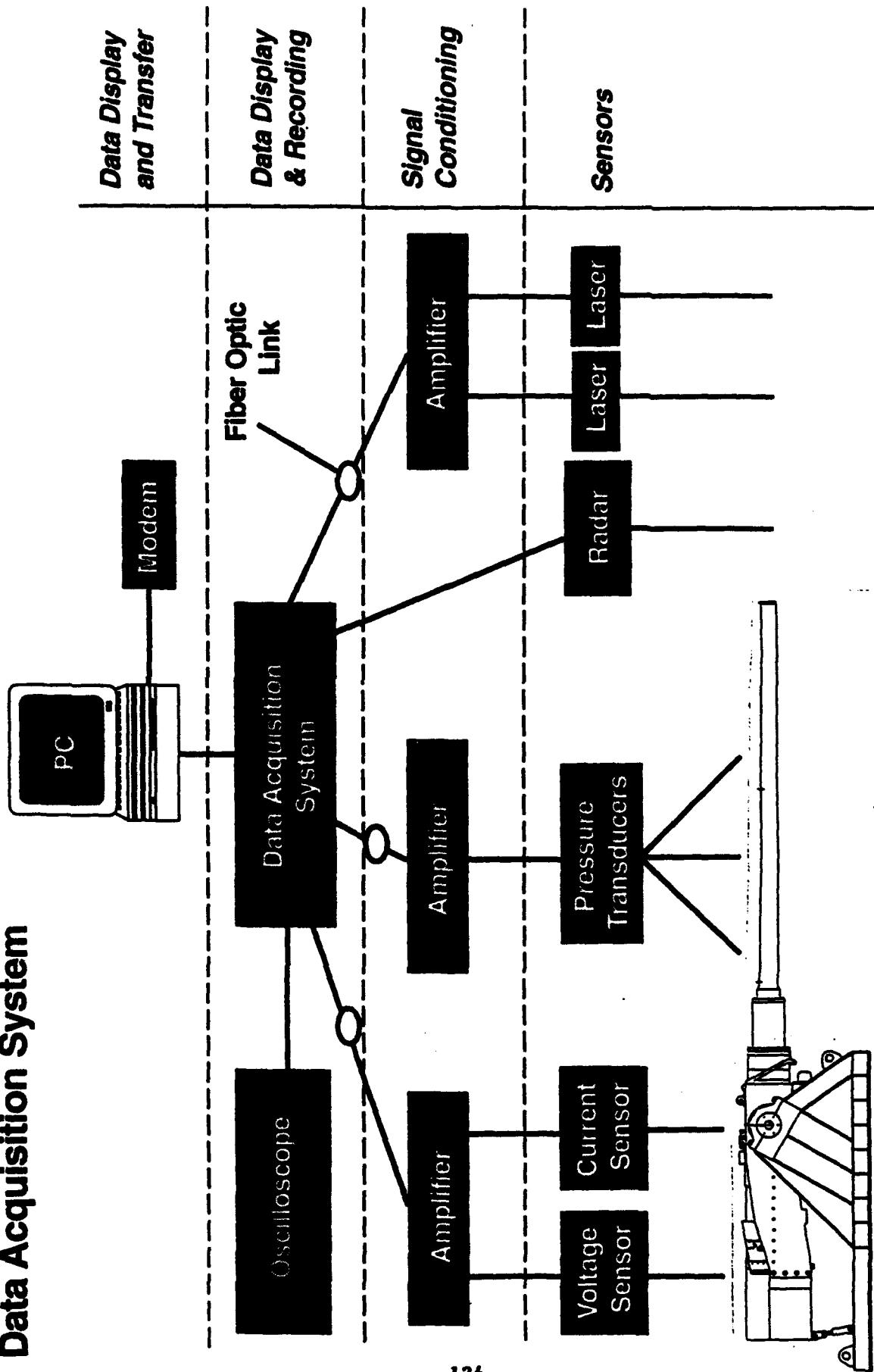


fmc

Automated Data Acquisition, Transfer, and Reduction



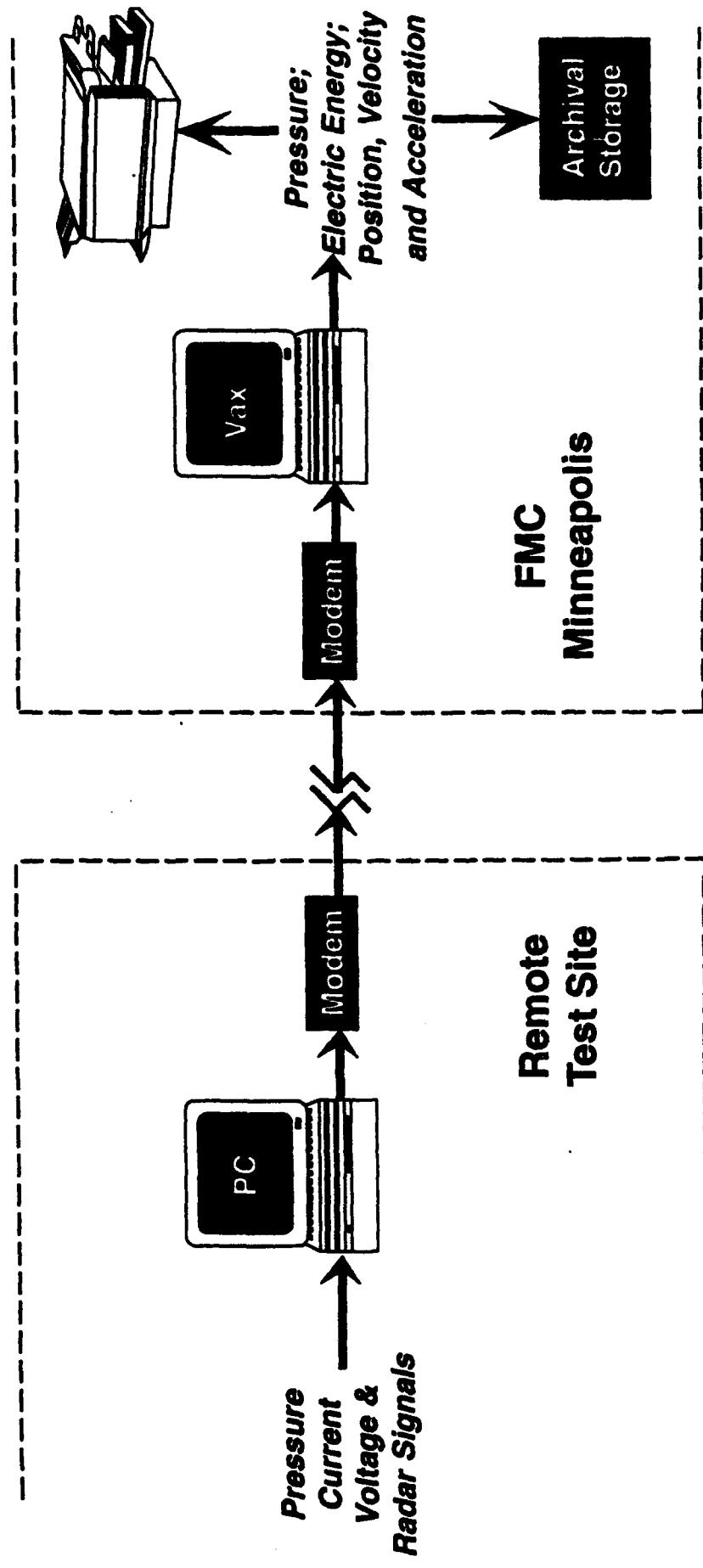
Data Acquisition System



Electric Armaments

FMC

Automated Data Transfer & Reduction



Electric Ammunitions

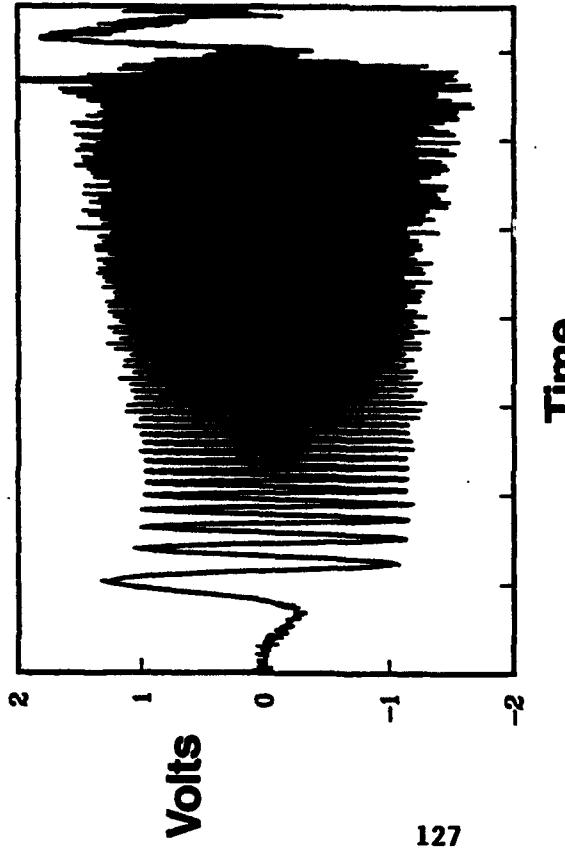
+FMC

In-Bore Radar Measurements of Projectile Kinematics

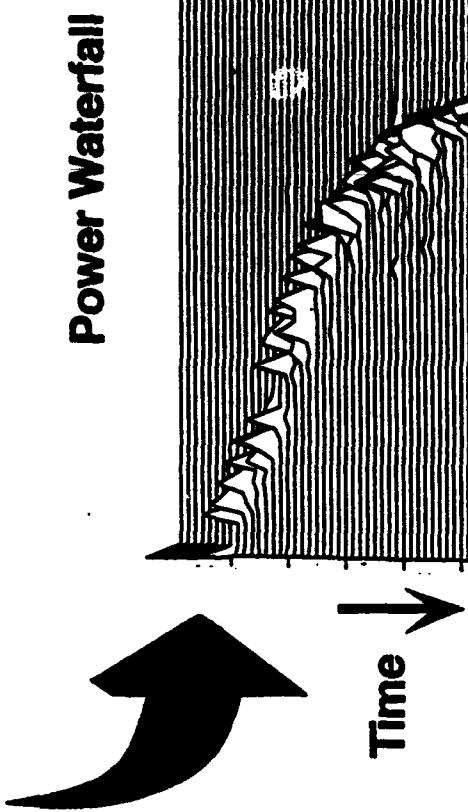
Electric Armaments

FMC

Doppler Signal

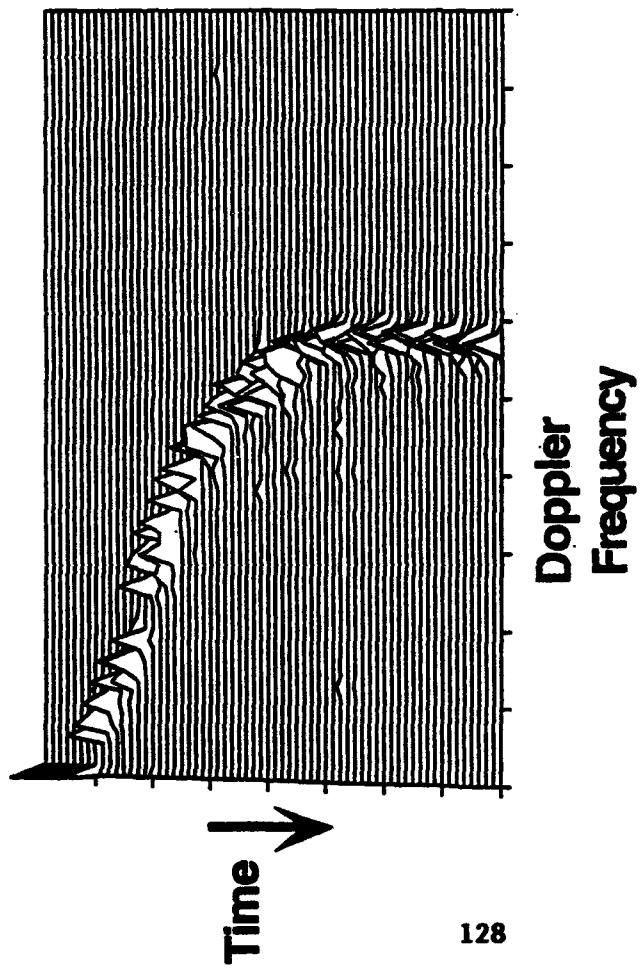


Analysis of In-Bore Doppler Radar Data



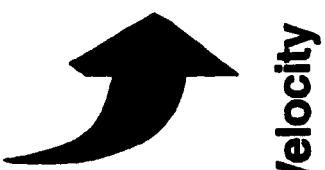
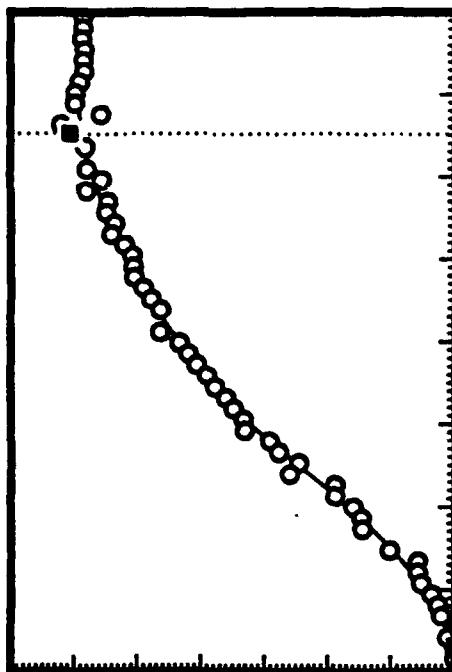
- Separate into overlapping intervals
- FFT each interval
- High pass filter at muzzle exit

Power Waterfall



Analysis of In-Bore Doppler Radar Data

Projectile Velocity



- Locate peak of power spectrum
- Remove data points with low SNR
- Convert Doppler frequency to projectile velocity



Electric Armaments

— fMC —

Projectile Velocity

Free Flight:

$$V(t) = \frac{c}{1 + 2\left(\frac{f_o}{f_D(t)}\right)} \approx \frac{cf_D(t)}{2f_o}; \quad \text{since } \left(\frac{V(t)}{c} \ll 1\right)$$

In-Bore:

$$V(t) = \left(\frac{cf_D(t)}{2f_o}\right) \frac{1}{\sqrt{1 - \left(\frac{f_c}{f_D(t)}\right)^2}}; \quad f_c = \frac{0.293c}{D/2}$$

$V(t)$ = Projectile Velocity

f_c = Cutoff Frequency

$f_D(t)$ = Doppler Frequency

c = Speed of Light

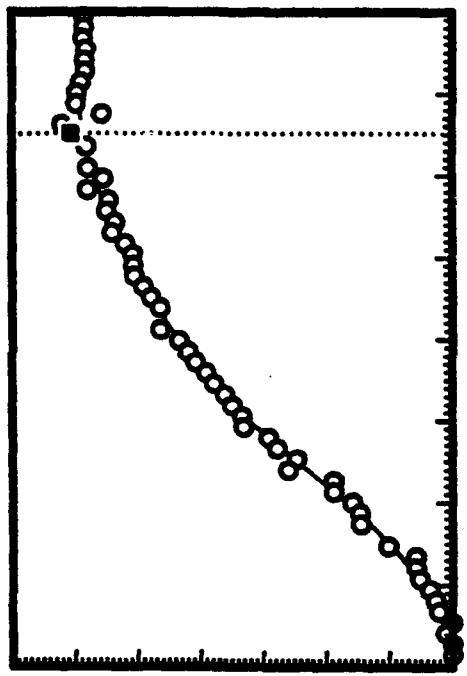
f_o = Transmit Frequency

D = Bore Diameter

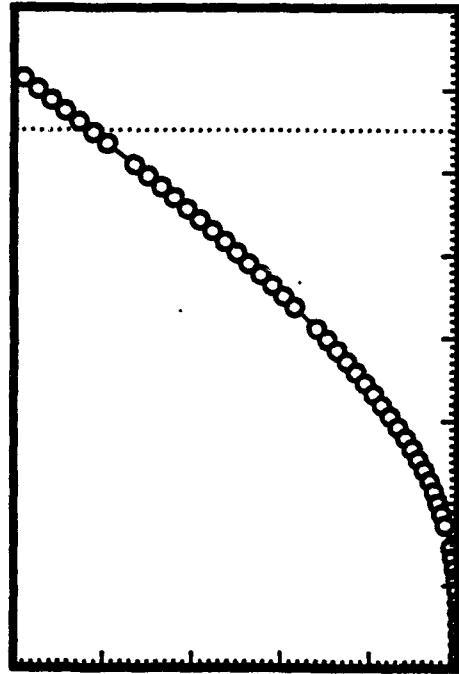


Projectile Travel and Acceleration

Velocity



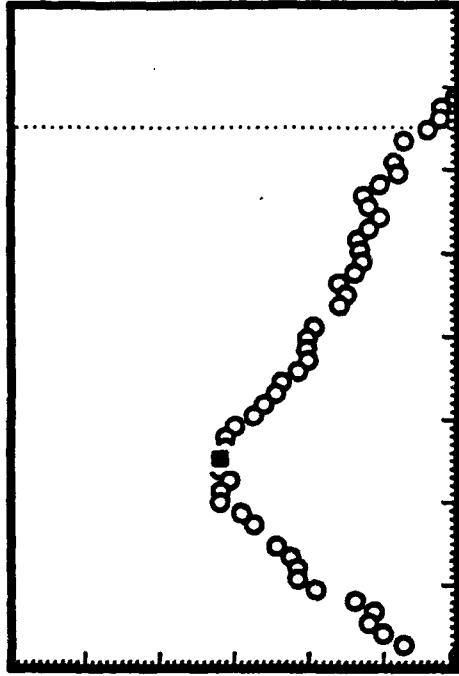
Integrate



Travel

Time

Smooth and
Differentiate



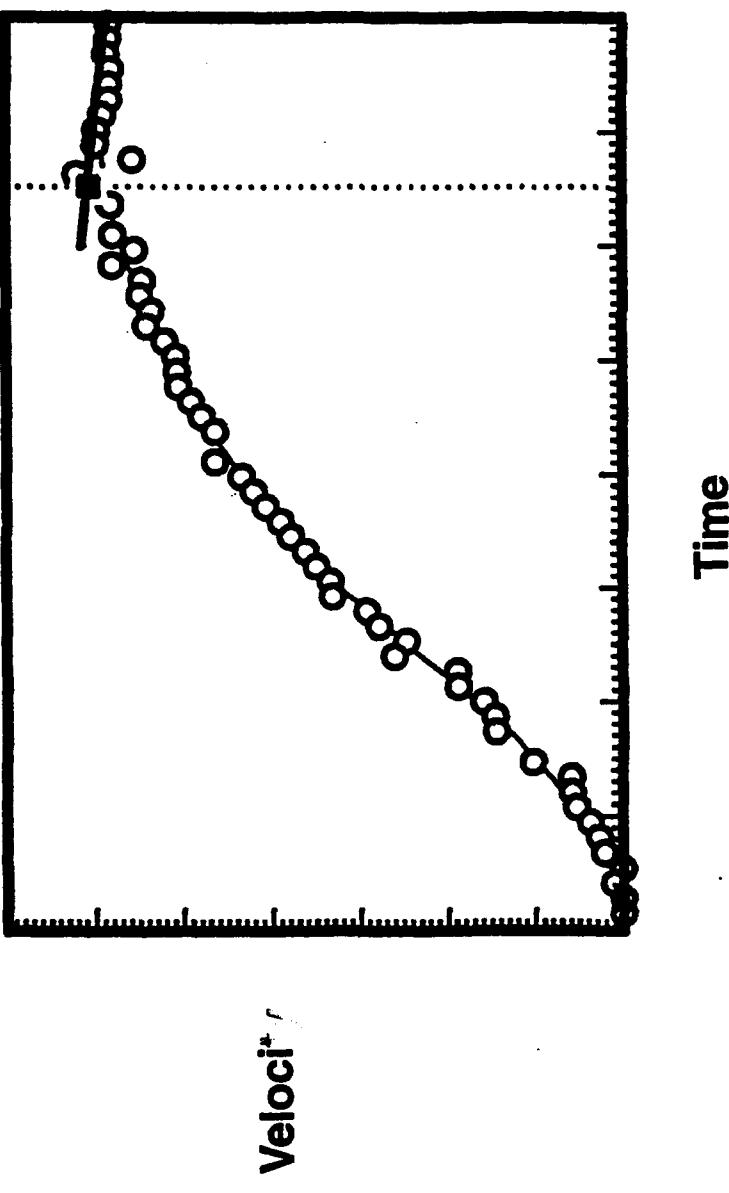
Acceleration

Time



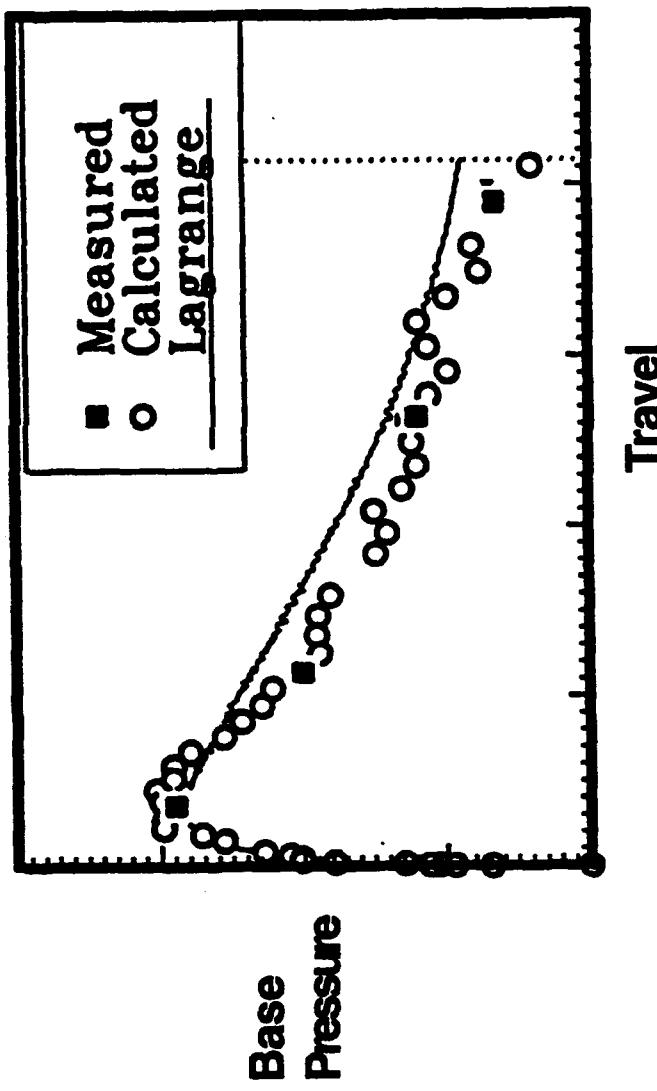
fMC —

Muzzle Velocity



Projectile Base Pressure

$$P_{base}(t) = \frac{ma(t) + F_{res}(t)}{A_b}$$



Electric Armaments



finc —

Development of an Inverse Ballistic Model



Electric Armaments

— FMC —

Inverse Model - Formulation

1st Law Energy Balance:

Electrical + Chemical = Work + Heat Loss

$$E_{elec}(t) + cz(t) \left(\frac{I}{T_f(\gamma - 1)} \right) (T_f - T(t)) = \left(\frac{1}{2} m V^2(t) + \frac{1}{2} c V^2(t) \right) + E_{heat}(t)$$

Noble - Abel Equation of State:

$$\overline{P(t)} \left(V_c + X(t) A_b - \frac{c(1-z(t))}{\rho_s} - bcz(t) \right) = RT(t) \frac{cz(t)}{M}$$

Inverse Model - Formulation

Combine and Solve for Fraction Burned:

$$z(t) = \frac{\frac{V^2(t)(m + c/3) + \frac{P(t)}{\gamma-1}(V_c + X(t)A_b - c/\rho_s) + E_{heat}(t) - E_{elec}(t)}{\gamma-1(I + \overline{P(t)}(b - 1/\rho_s))}}{\rightarrow}$$

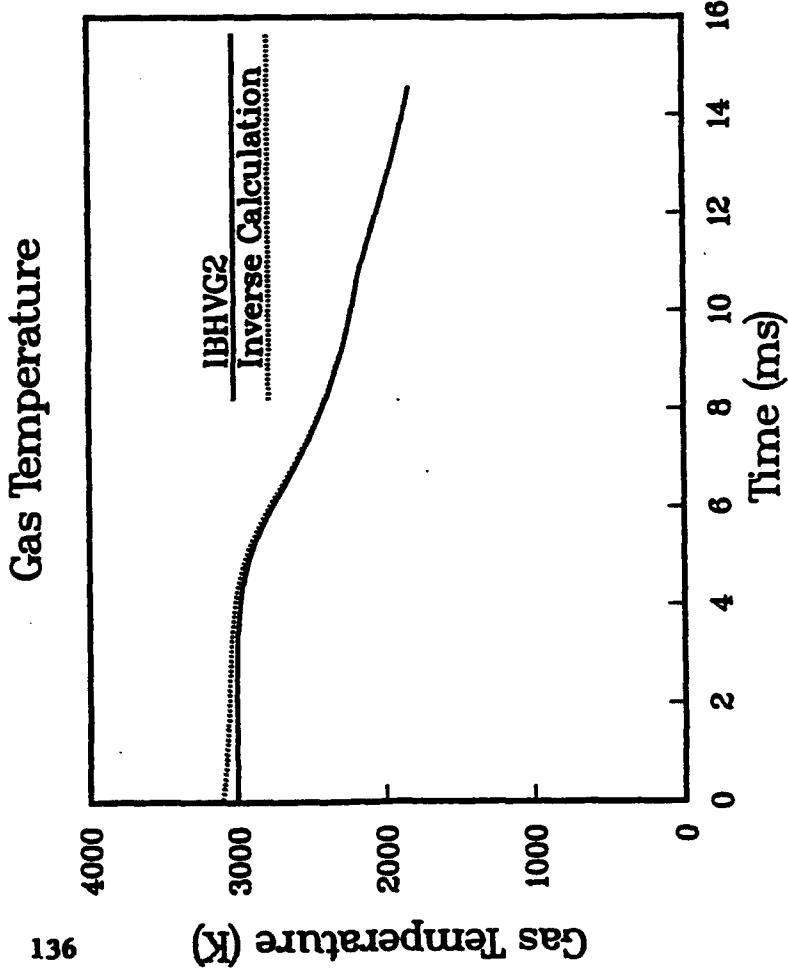
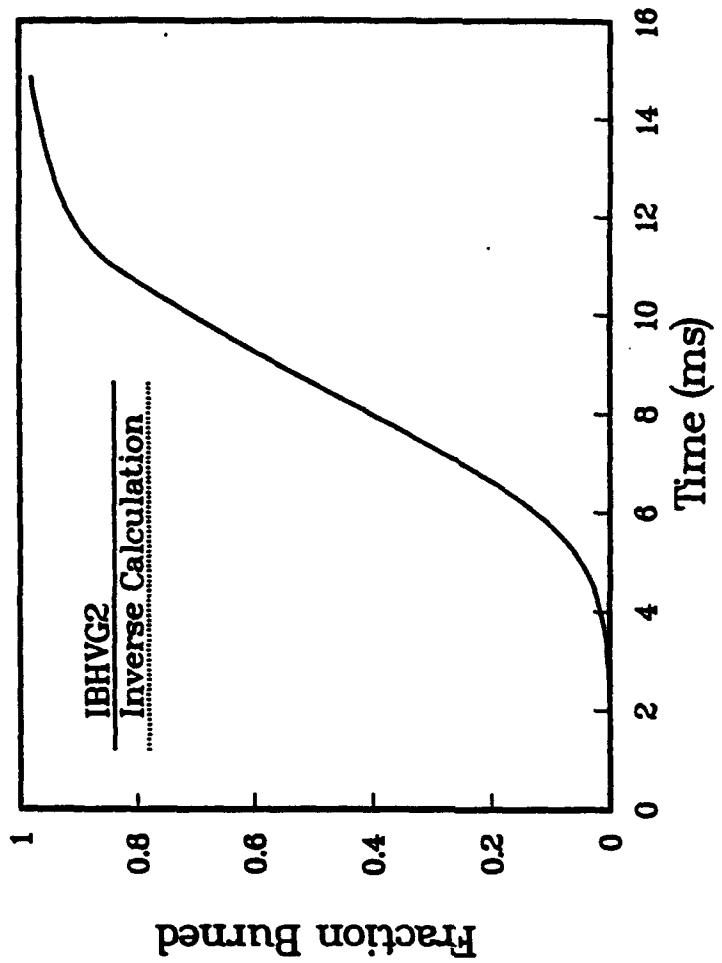
$E_{heat}(t)$ is calculated by modified Nordheim model.



FMC

Verification of Inverse Model

Fraction of Propellant Burned





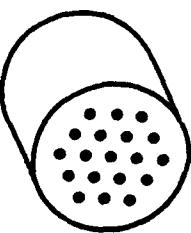
Inverse Model - Solid Propellant Extensions

Mass Burn Rate:

$$\dot{m}(t) = c \frac{dz(t)}{dt}$$

Linear Regression Rate:

$$\dot{r}(t) = \frac{\dot{m}(t)}{\rho_s S(z)}; \quad S(z) = \text{Geometric Form Function}$$

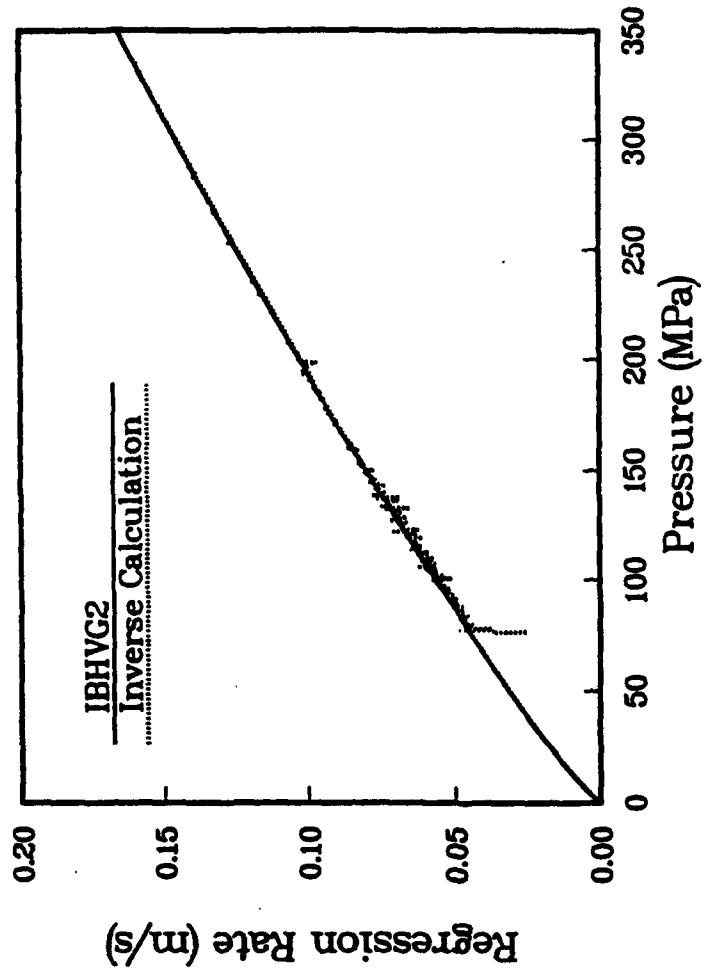




FMC

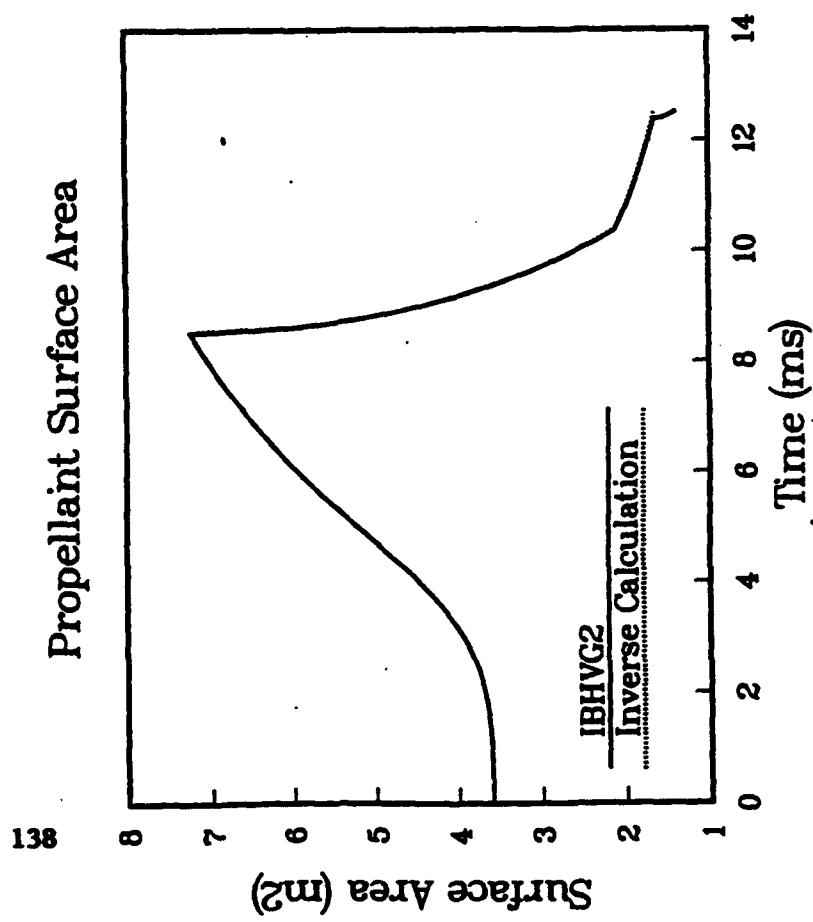
Verification of Inverse Model

Linear Regression Rate



Jankowski ARL Pres5/12/2018

Propellant Surface Area





Conclusions:

- Automated data transfer and reduction system provides fast, convenient access to shot results.
- Projectile travel is accurately measured using in-bore radar.
- In-bore radar provides a reasonable estimate of projectile acceleration and base pressure.
- Inverse analysis matches IBHVG2 results very well; model is ready for application to experimental data.

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Enhanced Propellant Burn Rate
through Plasma Erosion

L.E. Harris, D. Chui, J. Prezelski, P. O'Reilly, D.S. Downs
US Army Research, Development, and Engineering Center
Picatinny Arsenal, NJ
and
W.F. Oberle
US Army Research Laboratory
Aberdeen Proving Ground, MD
and
J.R. Greig
GT-Devices
Alexandria, Va
and
H.A. McElroy and J.G. Buzzett
Olin Ordnance
St. Petersburg, FL

ABSTRACT

In both ETC gun firings and ETC closed bomb experiments to date, it has been observed that the burn rates of solid propellants are not altered by the presence of the ET plasma except through the pressure created by the addition of the electric energy. However, in a recent series of ET gun firings, we have observed that the burn rate of the propellant can be dramatically increased by the erosive effect of the plasma. The propellant was JA-2, and for these ETC gun firings the whole propellant charge was cast as a "single perf" monolithic grain. The central perforation was 0.25 inch diameter and the outside diameter of the grain was 1.10 inch. The propellant was fired in a 30mm (bore diameter) gun in the Army's ET Gun Facility at GT-Devices. The plasma generator was a high pressure capillary discharge and the emerging plasma was carefully injected into the central perforation in the propellant grain. All other surfaces of the propellant grain were inhibited using silicone grease. The charge design is described in detail, and results obtained by simulating these firings using IBHVG2 are discussed. From these simulations, it is concluded that the burn rate achieved in these gun firings was enhanced significantly through the erosive effect of the plasma.

Enhanced Propellant Burn Rate Through Plasma Erosion

L. E. Harris, D. Chiu, J. Prezelski, P. O'Reilly, R. Marchak and
D. S. Downs

US Army Research, Development and Engineering Center
Picatinny Arsenal, NJ

W. F. Oberle

US Army Research Laboratory
Aberdeen, MD

J. R. Greig
GT Devices
Alexandria, Va

OUTLINE

- CBP Model
- System Requirements
 - Tank
 - TMD
- JA2 Monolith Gun Firings
 - Experimental configuration
 - IBHVG2 Predictions
 - Pt traces and Residue
 - Inverse analysis

CBP EQUATIONS

$$Z_p = \frac{1}{\gamma} \left(\frac{Im}{P_{max} A_b} - \frac{V_e - m \eta - V_a}{A_b} \right) \quad (1)$$

$$Z_p = \frac{1}{2} \ddot{Z}_p t^2 \quad (2)$$

$$\dot{Z}_p = \frac{1}{2} \ddot{Z}_p t \quad (3)$$

$$m = \frac{Z_p \gamma A_b + V_e - C / \rho}{\frac{1}{P_{max}} + \eta - \frac{1}{\rho}} \quad (4)$$

$$m = \frac{\frac{1}{2} \ddot{Z}_p t^2 \gamma A_b + V_e - C / \rho}{\frac{1}{P_{max}} + \eta - \frac{1}{\rho}} \quad (5)$$

$$\dot{m} = \frac{\ddot{Z}_p t \gamma A_b}{\frac{1}{P_{max}} + \eta - \frac{1}{\rho}} \quad (6)$$

CBP EQUATIONS

$$\bar{m} = \frac{\bar{Z}_p r A_b}{\frac{1}{P_{mean}} + \eta - \frac{1}{\rho}} \quad (7)$$

$$m = \frac{1}{2} \bar{m} t^2 + m_0 \quad (8)$$

$$m_0 = \frac{V_c - C / \rho}{\frac{1}{P_{mean}} + \eta - \frac{1}{\rho}} \quad (9)$$

$$Z_p^{bo} = \frac{1}{\gamma} \left(\frac{IC}{P_{mean}^{bo} A_b} - \Lambda \right) \quad (10)$$

$$E_p^{bo} = E_p^{bo} \left\{ 1 + \frac{1}{\gamma - 1} \left[\frac{\bar{Z}_p^{bo}}{Z_p^{bo}} \right] \left[1 - \left(\frac{\bar{Z}_p^{bo}}{Z_p^{bo}} \right)^{\gamma - 1} \right] \right\} \quad (11)$$

CBP EQUATIONS

$$\dot{m} = \rho S i \quad (12)$$

$$i_p = \frac{\bar{m}}{2\pi l_c r_p \rho} \quad (13)$$

$$r_p = \left(\frac{\bar{m} l^2}{2\pi l_c \rho} + r_h^2 \right)^{\frac{1}{2}} \quad (14)$$

Table III CBP Calculation of Interior Ballistics Time Profiles
in a 120mm M256 Tank Gun

$t(\text{MS})$	$Z_p(\text{M})$	$V_p(\text{M/S})$	$T_m(\text{K})$	$f(1)$	$\dot{M}(\text{KG/S})$
0.00	0.000	0	3,424	0.004	0
0.10	0.002	42	3,244	0.002	268
0.20	0.008	85	3,037	0.007	536
0.30	0.019	127	2,933	0.016	804
0.40	0.034	169	2,881	0.028	1,072
0.50	0.053	211	2,854	0.043	1,341
1.00	0.211	423	2,812	0.173	2,681
1.50	0.476	634	2,804	0.388	4,022
2.00	0.846	846	2,801	0.690	5,362
2.40	1.218	1,015	2,800	0.994	6,435
2.41	1.225	1,018	2,800	1.000	6,453

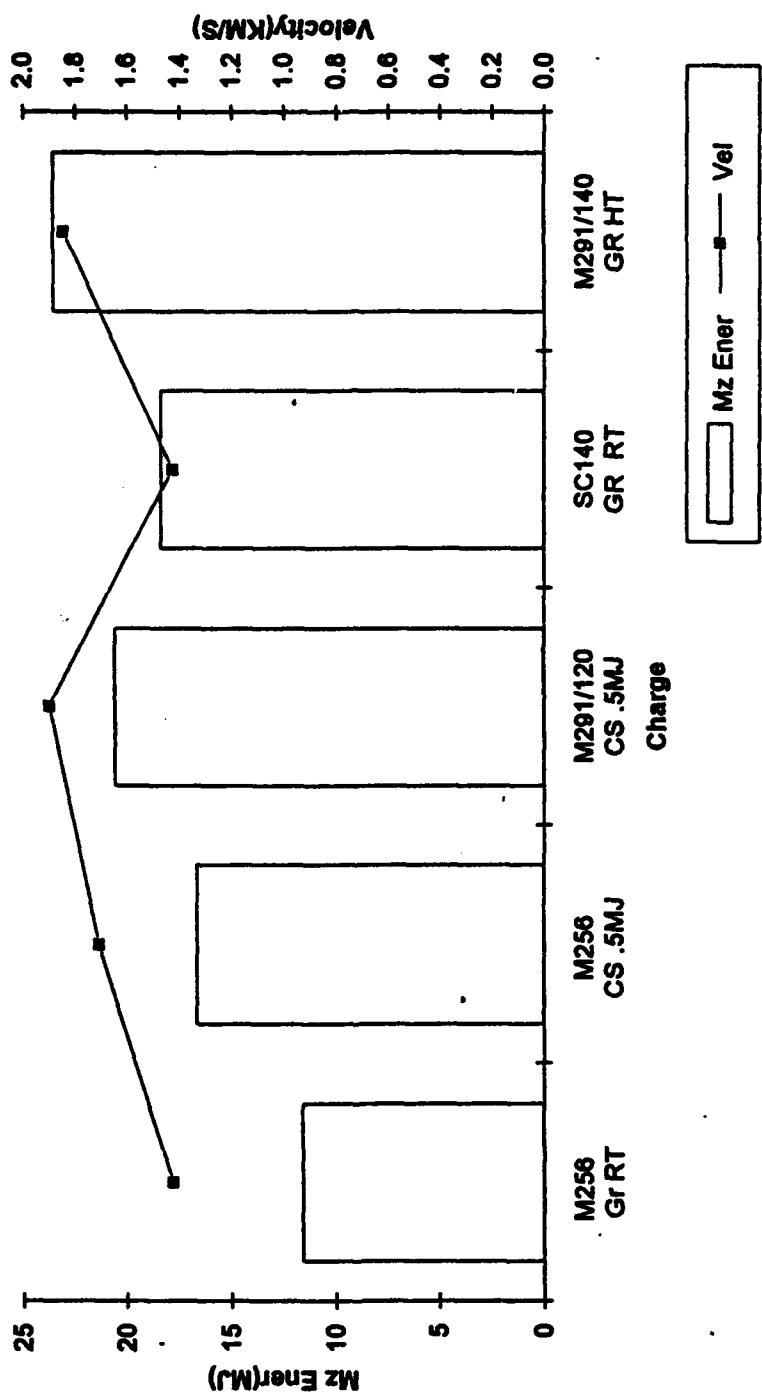


Figure 4. Projectile muzzle velocity versus velocity for 120- and 140-mm tank guns



Figure 6. 120-mm M291 ETC tank gun cartridge

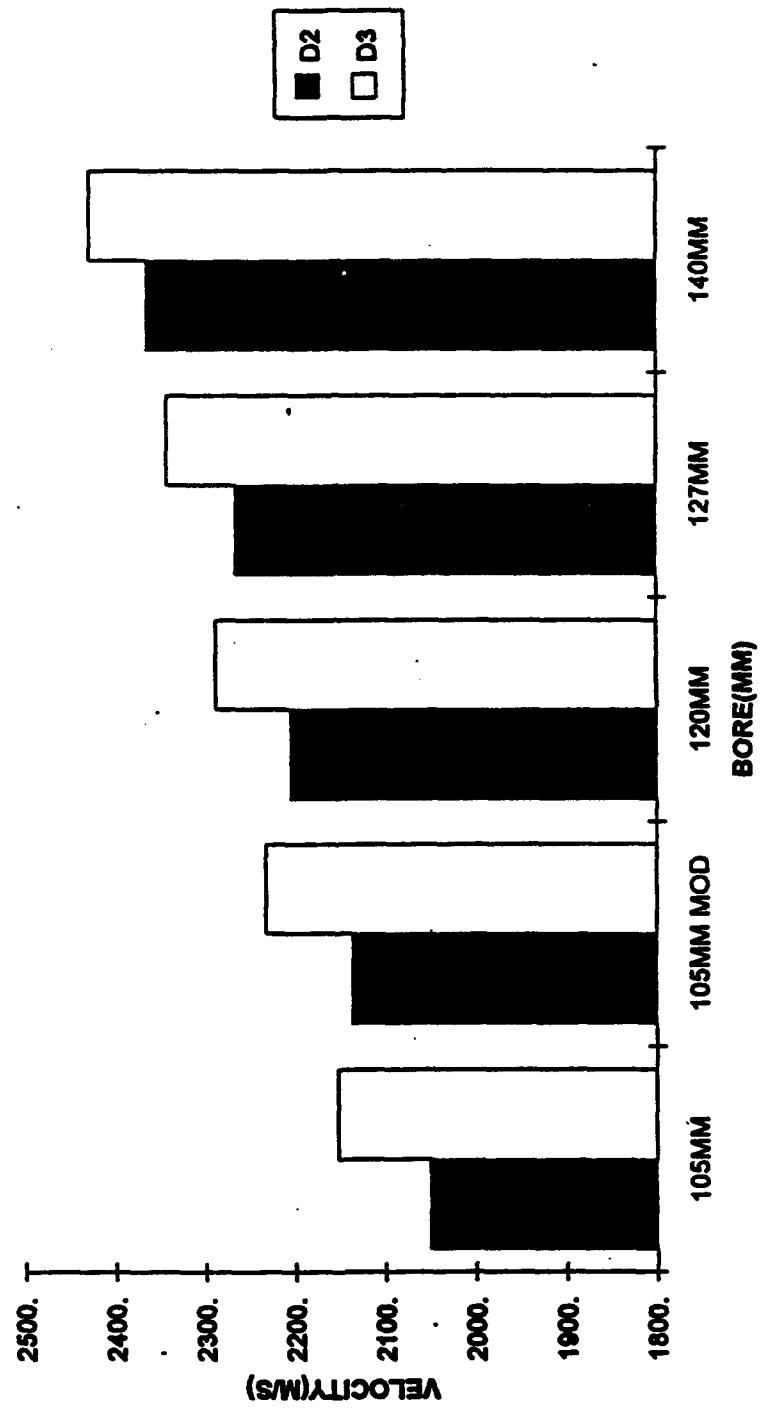


Figure 8. Muzzle velocity in various air defense guns

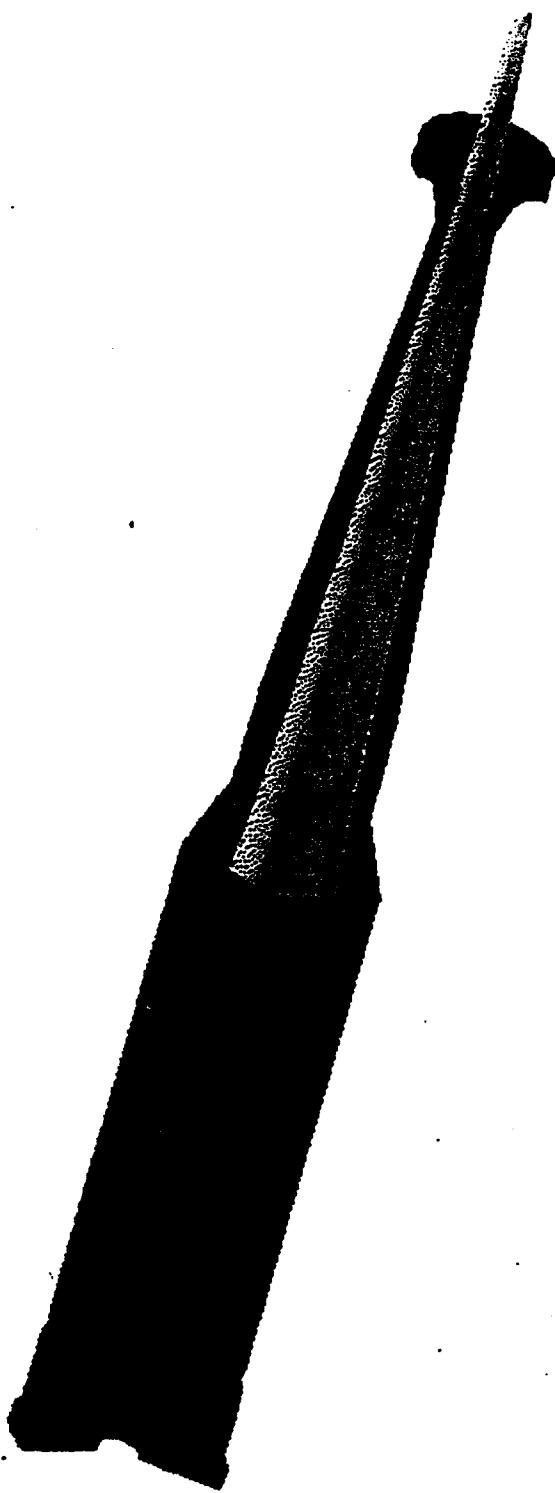


Figure 9. 105-mm ETC air defense cartridge

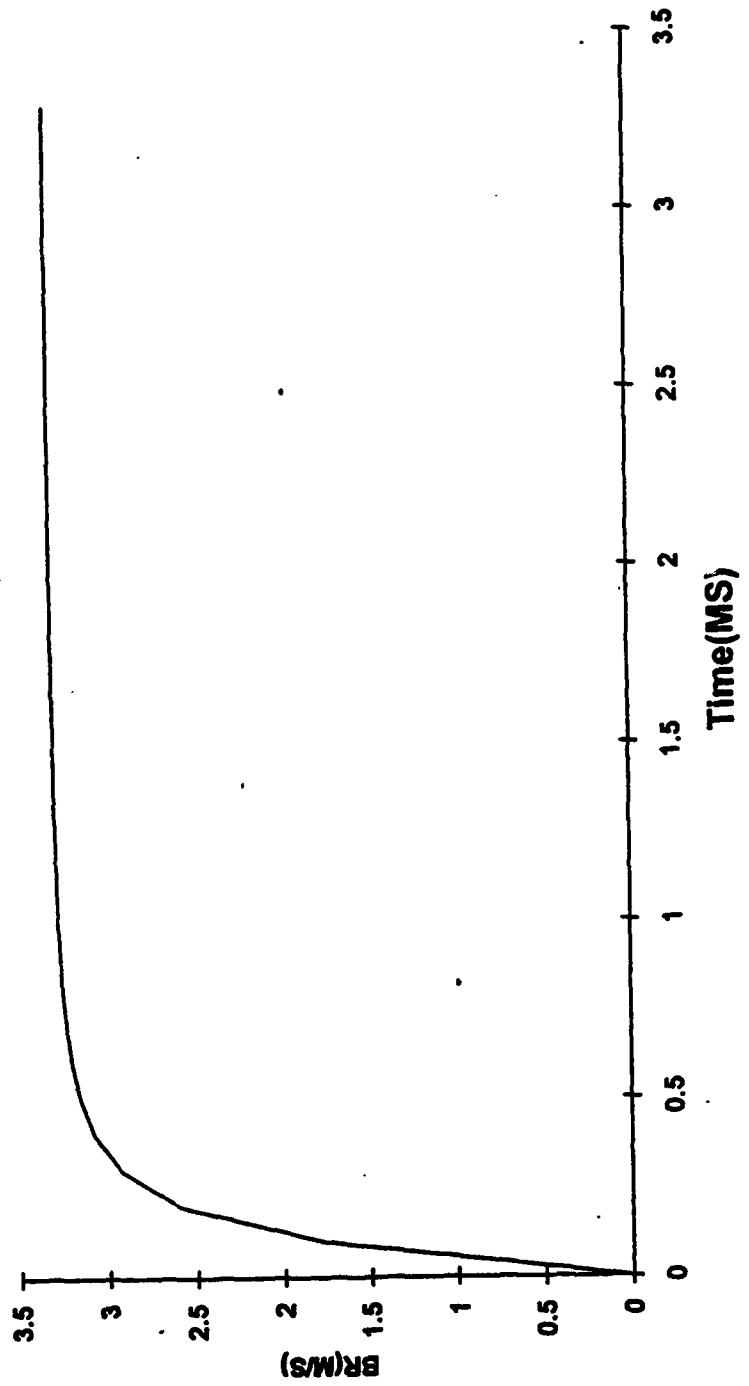
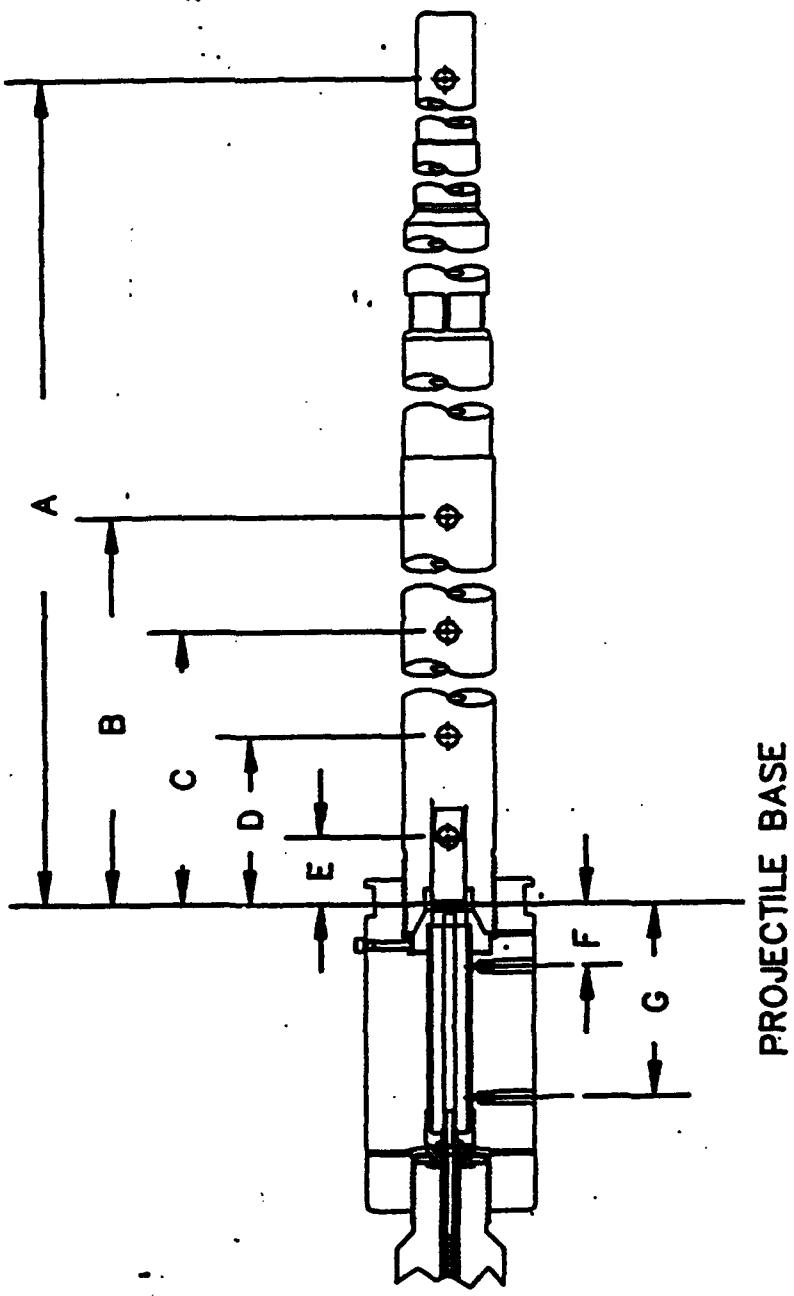


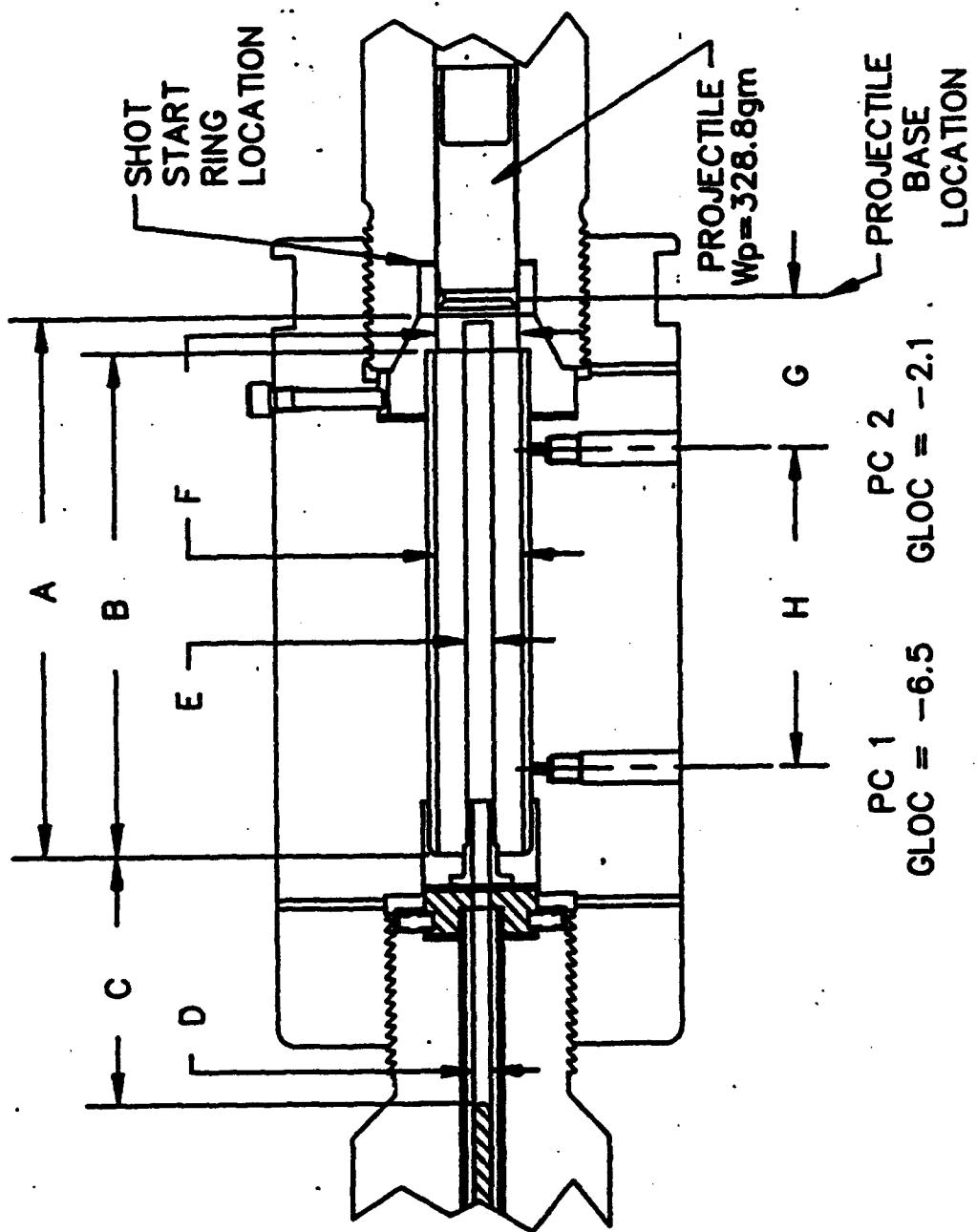
Figure 10. Propellant burning rate versus time for 120-mm M291 ETC cartridge

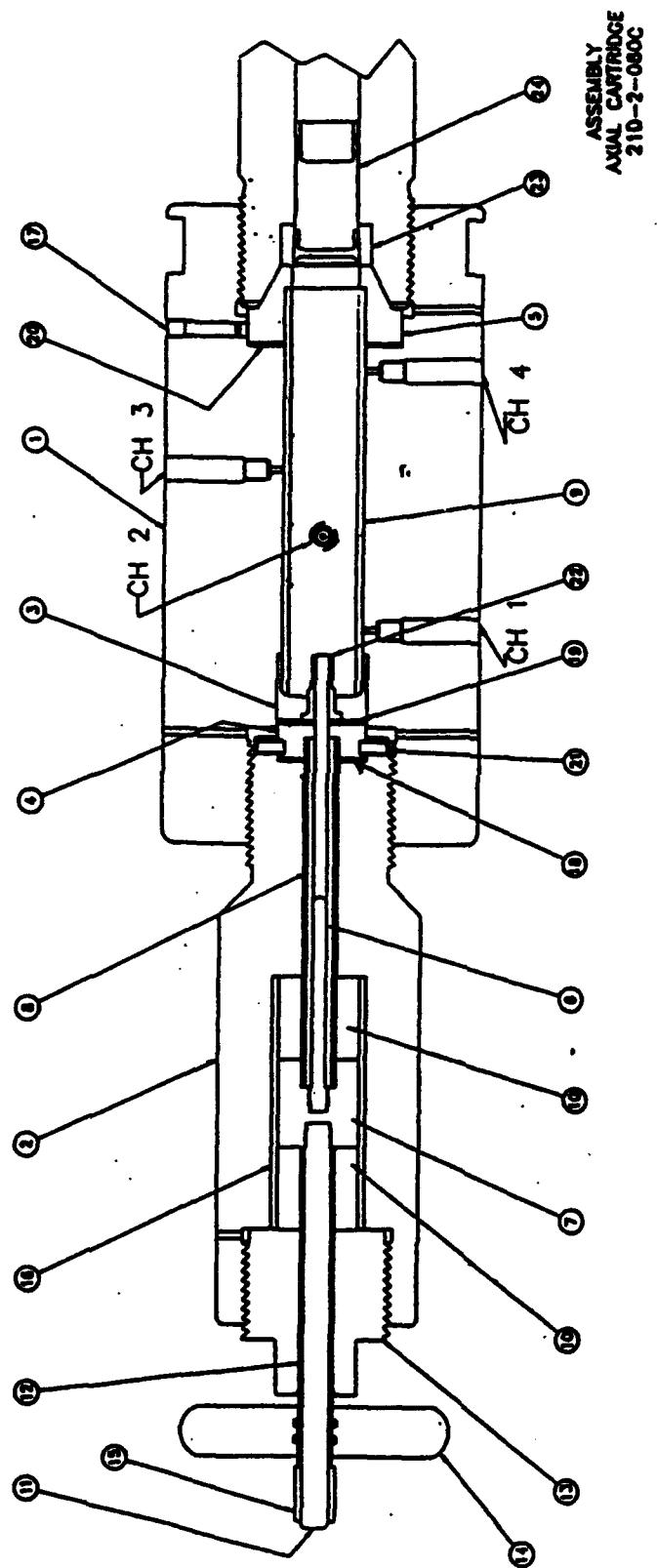
Summary

- In the CBP model a 120mm M291 ETC gun using a cartridge with JA2 at a LD equal to its density with 0.5 MJ/KG EE attains a muzzle velocity of 1900 M/S that is slightly higher than a conventional 140mm M291 Tank Gun using granular JA2 at a LD of 1.
- CBP calculations indicate that a similar design for a 105mm ETC Air Defense gun will achieve velocities greater than 2 KM/s for both the D2 and D3 smart projectiles.
- If the mass generation rate required to meet the above performance is not achievement, plasma influenced grain de-consolidation at the correct rate would be required to meet performance.

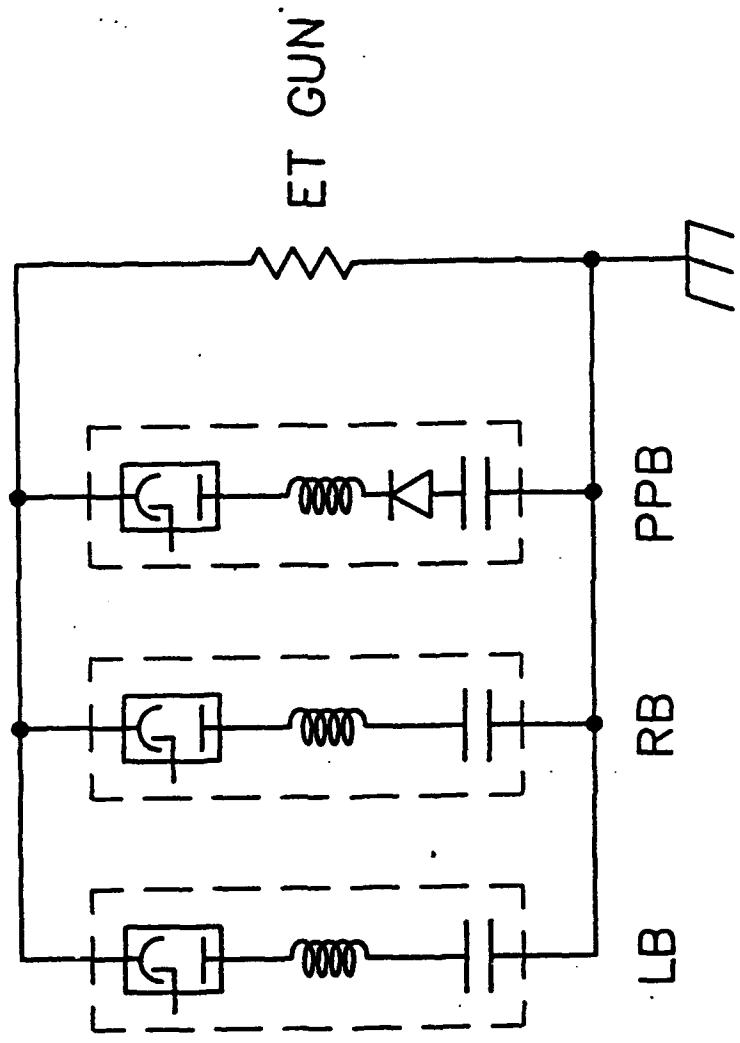


PROJECTILE BASE



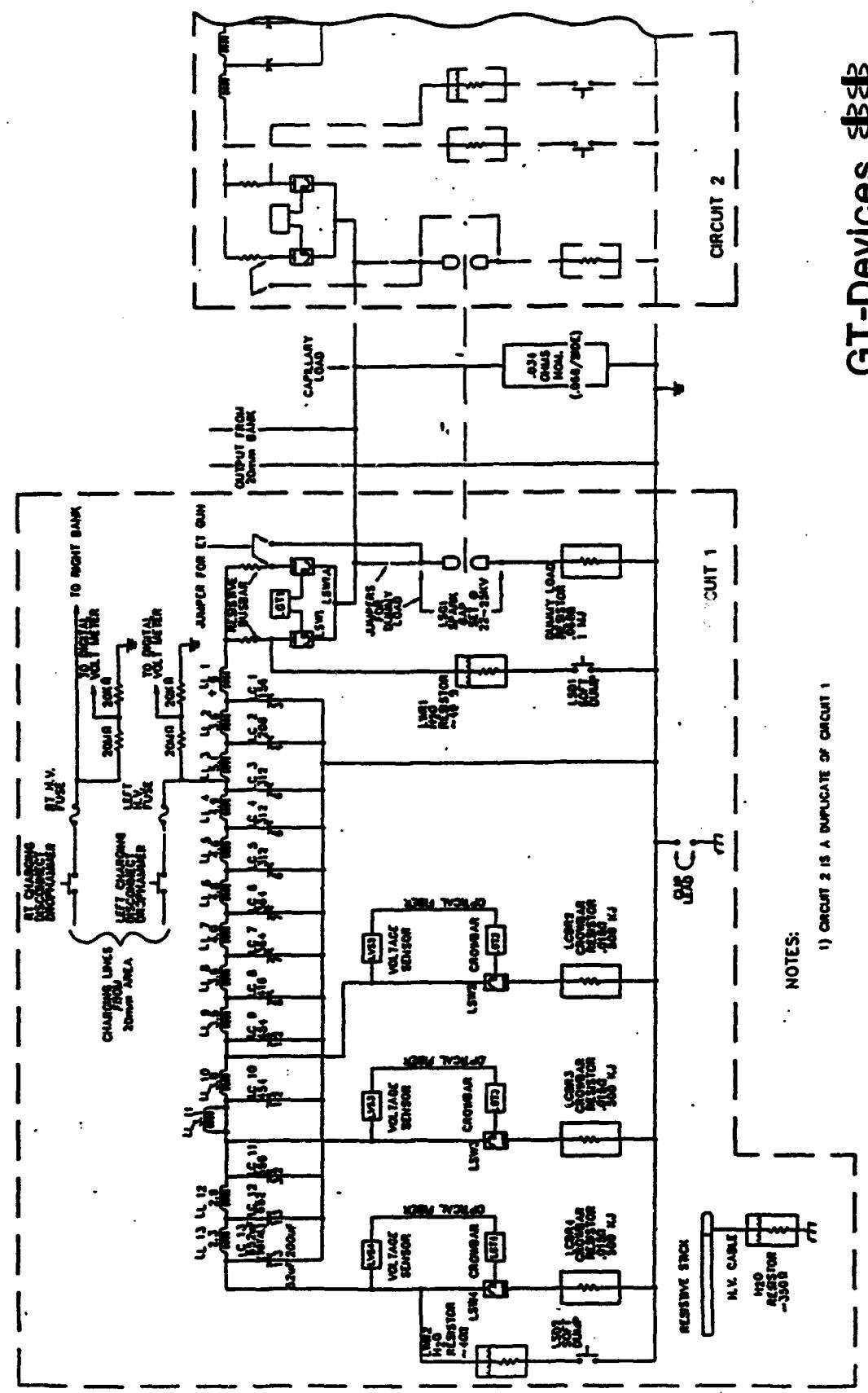


ASSEMBLY
AXIAL CARTRIDGE
210-2-080C

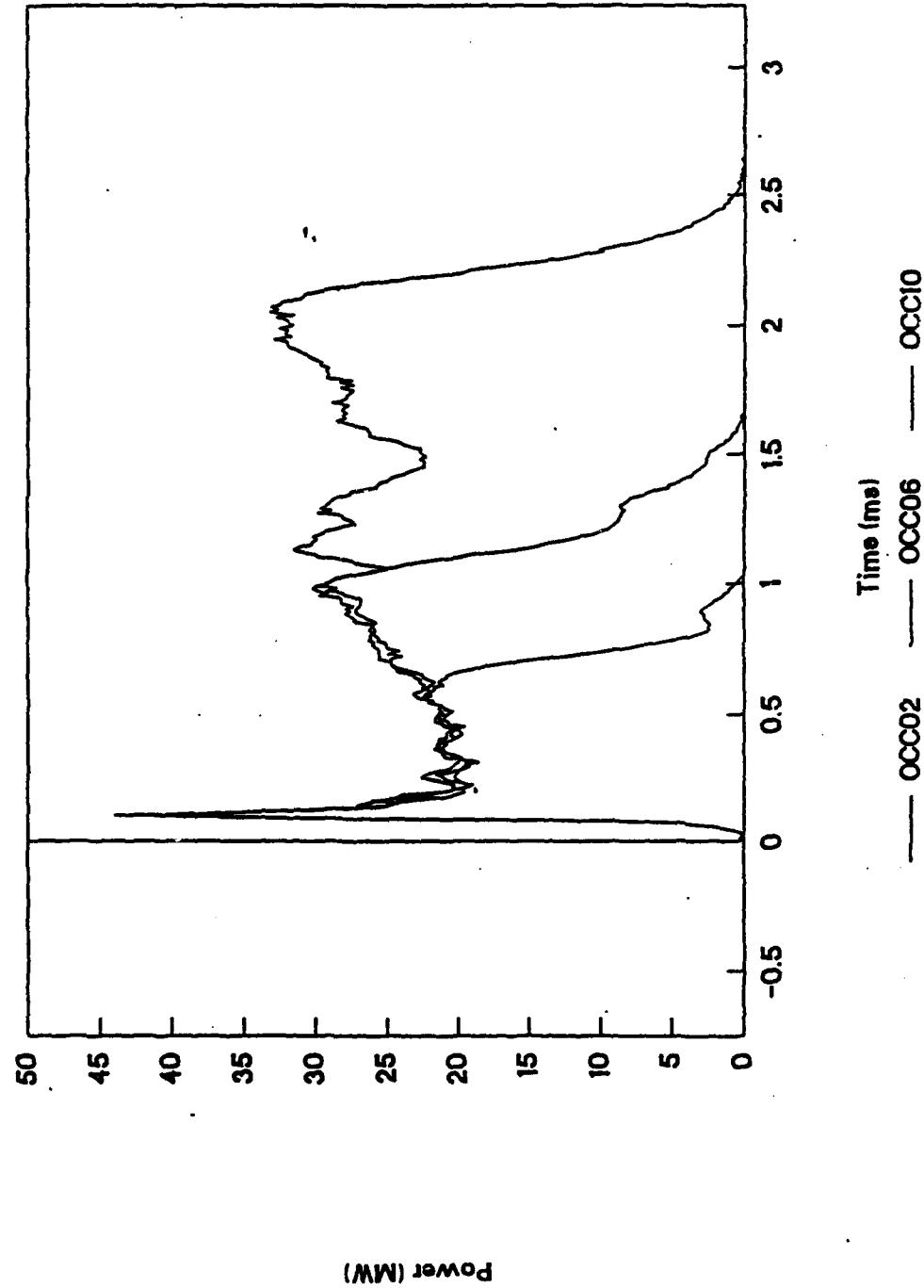


21A-6-193

GT-Devices 
SCHEMATIC DIAGRAM
30mm PFN

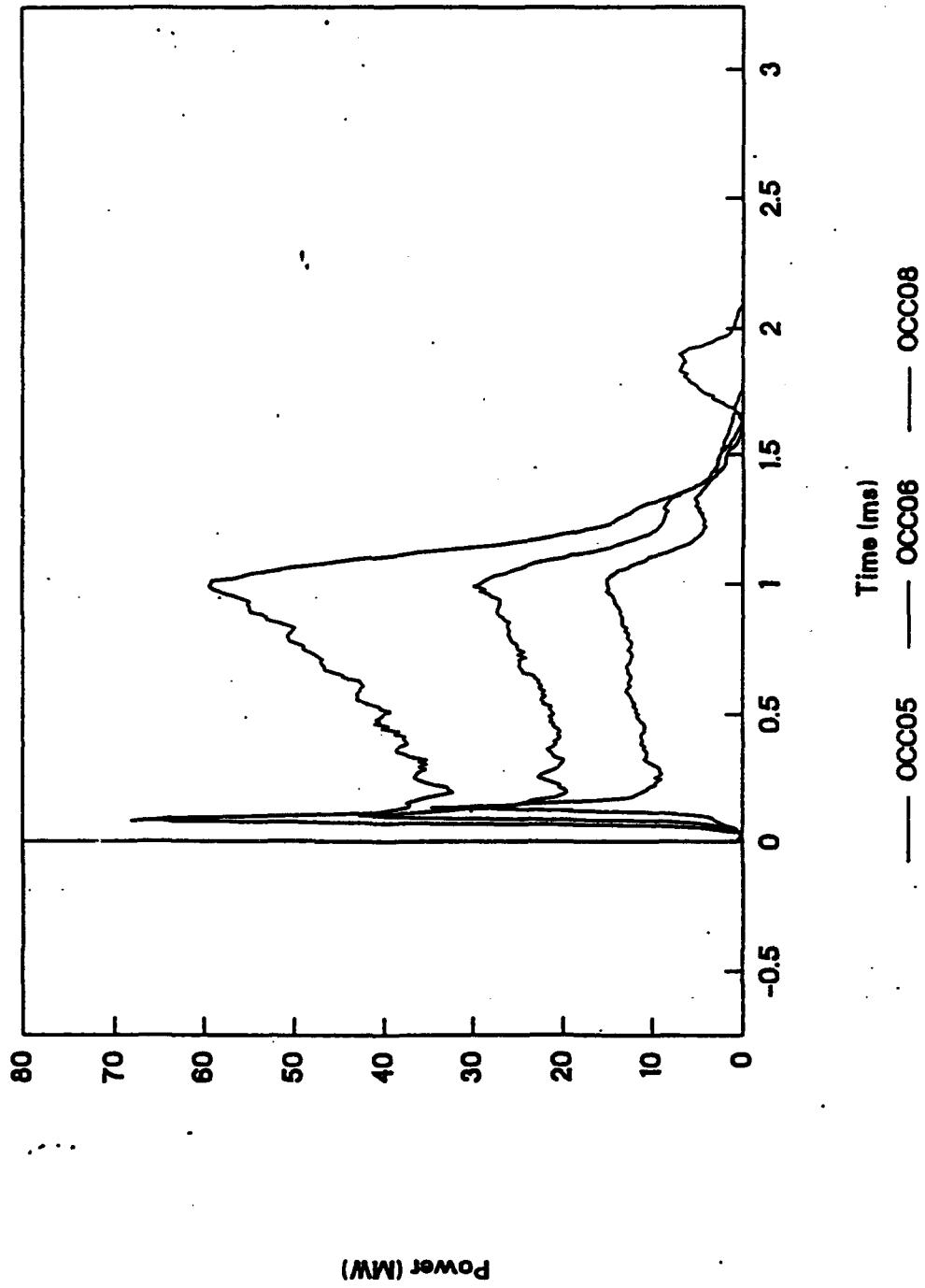


Alternate Propellants
occ series



Power (MW)

Alternate Propellants OCC Series

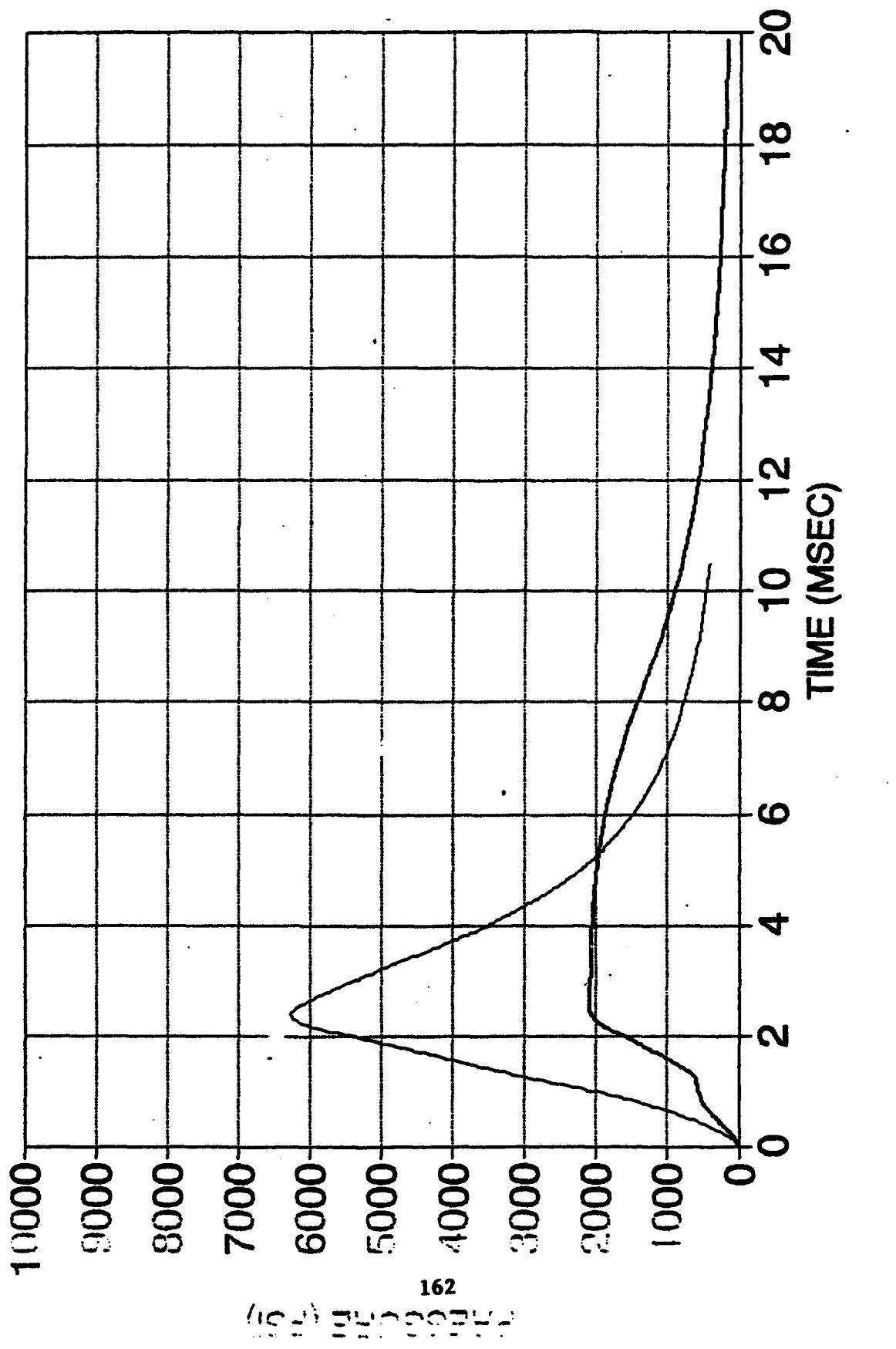


Power (MW)

IBHVG2 PREDICTIONS FOR CENTER CORE BURNING JA2 MONOLITHS

CHARGE	P(KSI)	V(M/S)	%BURNT
1/4	2	146	0.4
1/2	6	221	0.6
1	13	334	0.7

JA-2 PRESHOT IBHVG2 RESULTS
2.4 MSEC AT 0.5 MJ/KG EE



— QUARTER CHG — HALF CHARGE

Firing Schedule
As Fired

May 3, 1993

Shot Number / Date	Charge Weight	Power Pulse Length (ms)	Energy Density (kJ/gm)	(kV)
1 4/08/93	1/4	2.2	.75	2.6 -LB+RB
2 4/08/93	1/2	2.2	.75	3.7 -LB+RB
3 4/14/93	3/4	2.2	.75	4.6 -LB+RB
4 4/14/93	F	2.2	.75	5.3 -LB+RB
5 4/15/93	1/4	1.1	.37	2.6 -LB
6 4/15/93	1/2	1.1	.37	3.7 -LB
7 4/16/93	1/4	1.1	0.75	3.7 -LB
8 4/16/93	1/2	1.1	0.75	5.2 -LB
9 4/20/93	1/4	0.6	.2	2.6 -½LB
10 4/20/93	1/2	0.6	.2	3.7 -½LB
11 4/21/93	1/4	1.1	0.75	3.7 -½LB
12 4/21/93	1/2	1.1	0.75	5.2 -½LB
13 4/22/93	1/2	2.2	0.75	3.7 -½LB
14 4/22/93	1/4	0.6	0.75	5.2 -½LB
15 4/27/93	3/4	2.2	0.75	4.6 -LB+RB
16 4/27/93	F	2.2	0.75	5.3 -LB+RB
17 4/28/93	3/4	2.2	0.37	3.25-LB+RB
18 4/28/93	F	2.2	0.37	3.7 -LB+RB

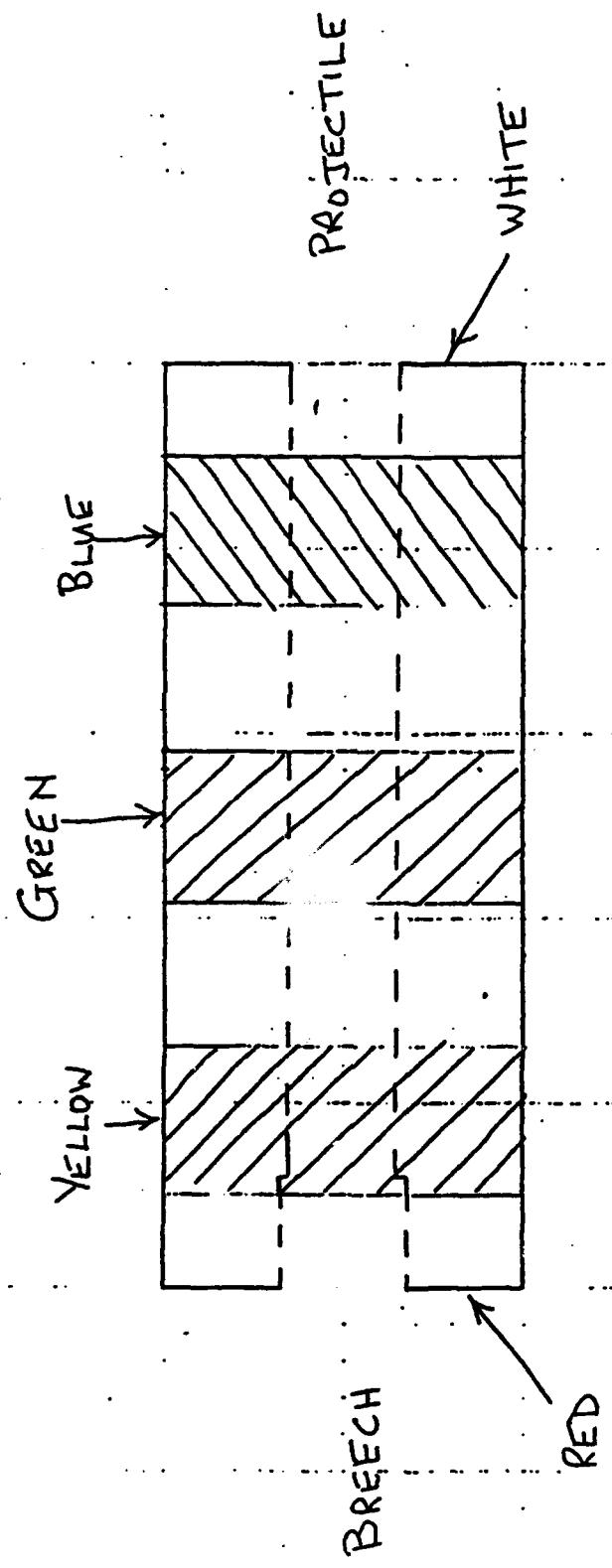
LB - 30mm Left Bank
RB - 30mm Right Bank

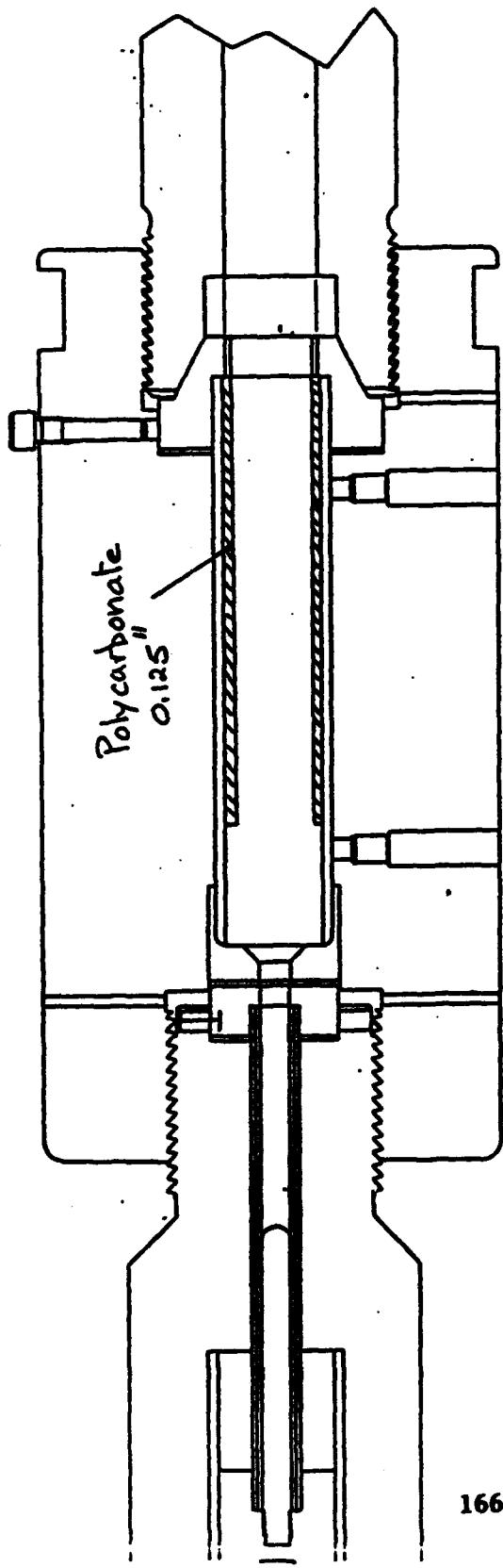
LB+RB - LB fired first, RB fired after delay of 1050 μ s.
LB - LB alone.
½LB - LB with LL9 disconnected from LC8.

DATE 04/30/93
08:52 AM

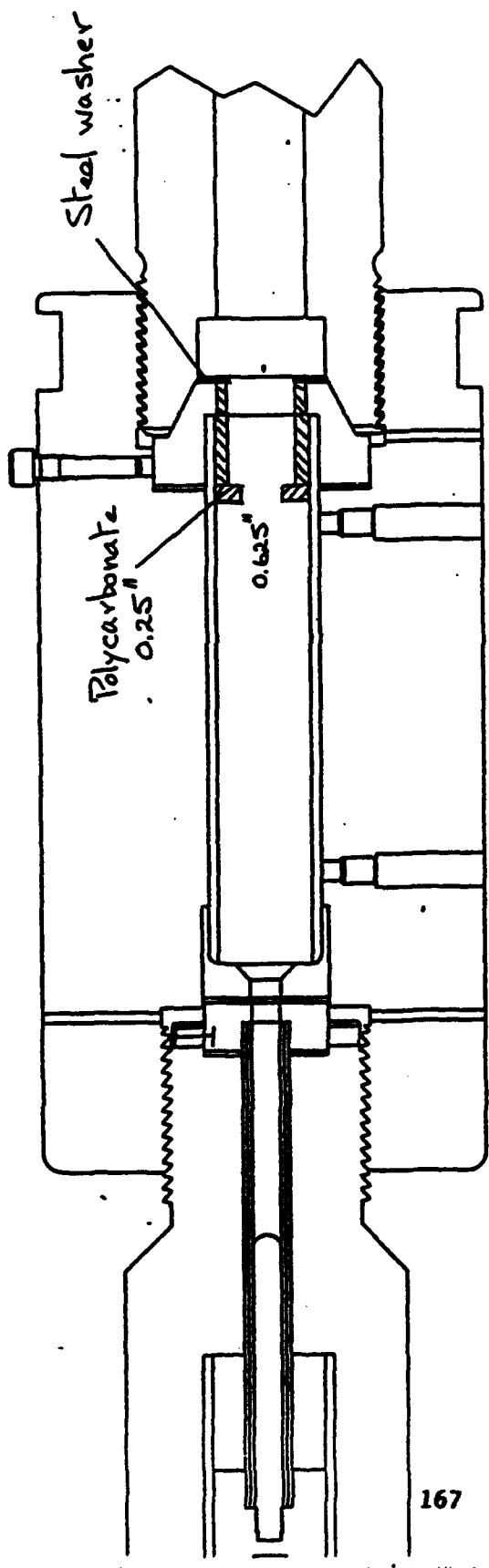
30MM AXIAL CARTRIDGE DATA BASE
REVISED 4/93 FOR QLN 'C' SERIES DATA

SHOT NUMB	DATE	GUN	PROJ MASS	PROP FILL	CART ENER	PROJ COMPRESS	VEL	VOLTS	POWER	PRESS	NOTES AND COMMENTS		CHAMBER ENERGY (kJ)	VOLUME DENSITY SHOT (cm ³)	KJ/GN MASS
											PEAK	CIRR			
1	04/08/93	322.3	41.3		30	0.319		2.60	16	10	JA-2 F VGLE PERF SINGLE GRAIN 1/4 CHARGE; 0.75kJ/GN 2.2ms PULSE		161.0	0.74	1
2	04/08/93	322.3	83.8		58	0.678		3.68	33	18	JA-2 (SPSG) 1/2 CHARGE; 0.75kJ/GN 2.2ms PULSE		161.0	0.70	2
3	04/14/93	322.6	139.8		77	0.480		4.60	47	27	JA-2 (SPSG) 3/4 CHARGE; 0.75kJ/GN 2.2ms PULSE; MODS. TO HOLD GRAIN		161.0	0.59	3
4	04/14/93	321.9	176.1		111	0.547		5.30	68	30	JA-2 (SPSG) FULL CHARGE; 0.75kJ/GN 2.2ms PULSE		161.0	0.63	4
5	04/15/93	323.1	41.3		15	0.271		2.60	15	10	JA-2 (SPSG) 1/4 CHARGE; 0.37kJ/GN 1.1ms PULSE (LEFT BANK)		161.0	0.37	5
6	04/15/93	322.1	85.1		28	0.396		3.70	30	17	JA-2 (SPSG) 1/2 CHARGE; 0.37kJ/GN 1.1ms PULSE; SH PROP LEFT IN CHAM		161.0	0.33	6
7	04/16/93	329.1	41.2		29	0.362		3.70	30	11	JA-2 (SPSG) 1/4 CHARGE; 0.75kJ/GN 1.1ms PULSE (OCG1 V/SHORT PULSE)		161.0	0.70	7
8	04/16/93	328.6	84.9		54	0.433		5.20	69	19	JA-2 (SPSG) 1/2 CHARGE; 0.75kJ/GN 1.1ms PULSE (OCG2 V/SHORT PULSE)		161.0	0.63	8
9	04/20/93	329.2	41.0		8	0.192		2.60	12	7	JA-2 (SPSG) 1/4 CHARGE; 0.2kJ/GN 0.6ms PULSE; PAINTED PROPELLANT		161.0	0.20	9
10	04/20/93	329.5	84.7		15	-260		3.70	22	17	JA-2 (SPSG) 1/2 CHARGE; 0.2kJ/GN 0.6ms PULSE; BAD VELOCITY DATA		161.0	0.18	10
11	04/21/93	329.1	38.5		30	0.162		3.70	32	5	JA-2 (SPSG) 1/4 CHARGE; 0.75kJ/GN 1.1ms PULSE W/MOD TUBE; NO VEL 3		161.0	0.74	11
12	04/21/93	329.8	78.9		94	0.359		5.20	55	20	JA-2 (SPSG) 1/2 CHARGE; 0.75kJ/GN 1.1ms PULSE W/MOD TUBE		161.0	0.69	12
13	04/22/93	329.0	78.0		57	0.365		3.70	31	18	JA-2 (SPSG) 1/2 CHARGE; 0.75kJ/GN 2.2ms PULSE; MOD TUBE; PROP INTACT		161.0	0.73	13
14	04/22/93	329.5	38.5		30	0.218		5.20	47	6	JA-2 (SPSG) 1/4 CHARGE; 0.75kJ/GN 0.6ms PULSE MOD TUBE; PROJ TUMBLED		161.0	0.77	14
15	04/27/93	328.3	120.5		86	0.426		4.60	68	14	JA-2 (SPSG) 3/4 CHARGE; 0.75kJ/GN 2.2ms PULSE MOD TUBE; GRAIN RECOV.		161.0	0.71	15
16	04/27/93	328.9	162.5		102	0.554		5.30	63	31	JA-2 (SPSG) FULL CHARGE; 0.75kJ/GN 2.2ms PULSE; V/ MODERATOR TUBE		161.0	0.63	16
17	04/28/93	329.0	121.4		46	0.322		3.25	26	11	JA-2 (SPSG) 3/4 CHARGE; 0.37kJ/GN 2.2ms PULSE V/ MODERATOR TUBE		161.0	0.38	17
18	04/28/93	328.9	156.2		59	-350		3.70	32	16	JA-2 (SPSG) FULL CHARGE; 0.37kJ/GN 2.2ms PULSE MOD TUBE; BAD VELOC.		161.0	0.37	18

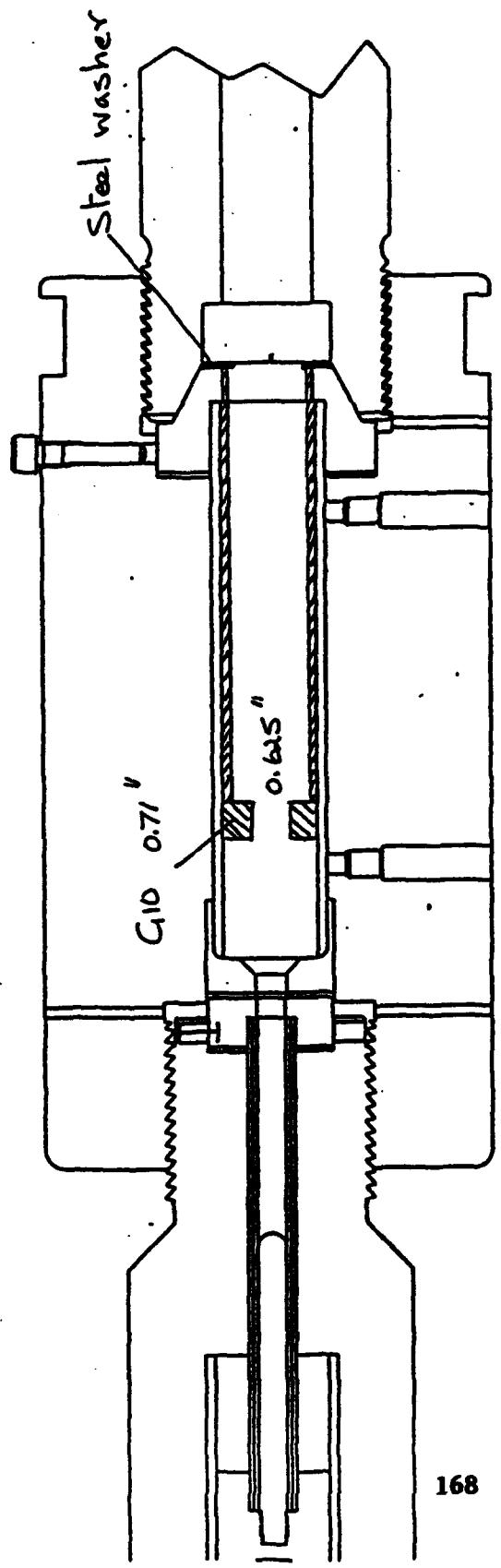




Shot occ ϕ 1 and ϕ 2.

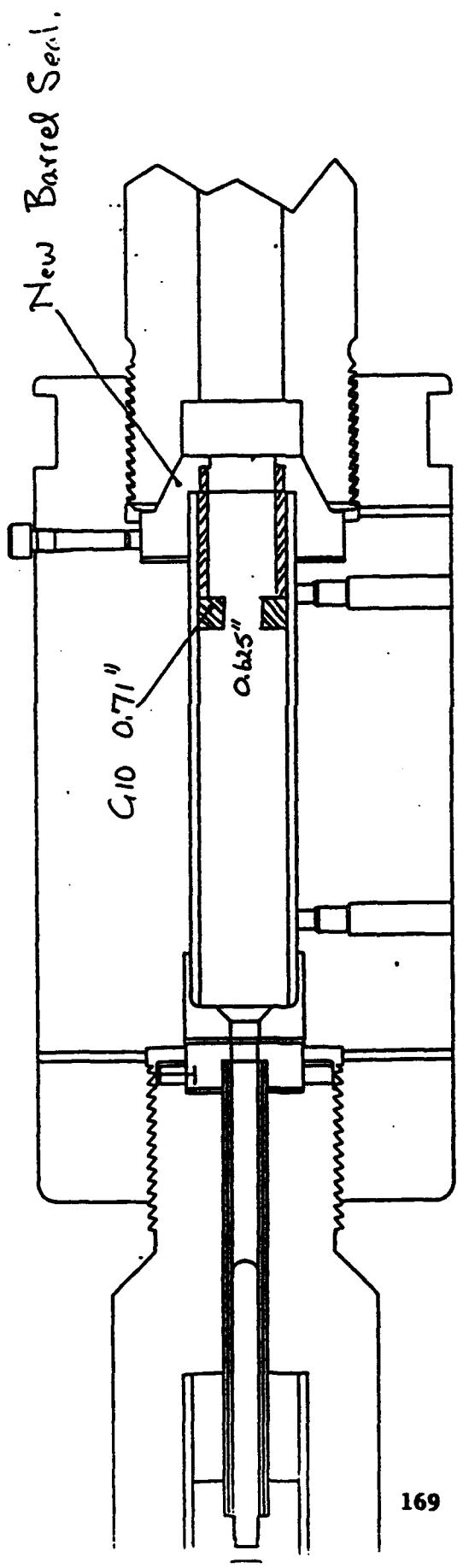


shots occ $\phi 3$ - $\phi 8$



Shot occY - 14

Shots OCC 15 - 18

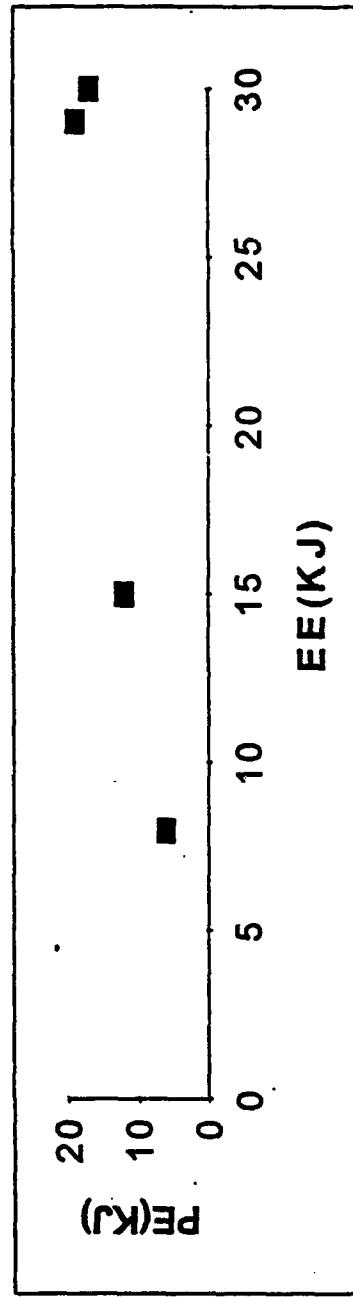


SHOT Notes on retainer system

NUMB	Retainer System
1	Insert tube pushed slightly into barrel.
2	Insert tube stuck in barrel, > 1 inch.
3	All retainers launched.
4	All retainers launched.
5	Nozzle melted, tube in place, melted.
6	Ring launched, tube in chamber.
7	Ring launched, tube moved forward.
8	Ring launched, tube pushed into barrel.
9	Nozzle melted, tube in place, ring launched.
10	G10 retainer pushed into barrel seal.
11	Inserts in place.
12	Melt down. Liquid in barrel.
13	G10 ring in chamber, tube pushed into barrel seal.
14	All retainers in place.
15	All retainers in place.
16	Retainers launched.
17	G10 ring pushed into barrel seal, tube launched.
18	Steel ring in place.

J A 2 MONOLITHS QUARTER CHARGE

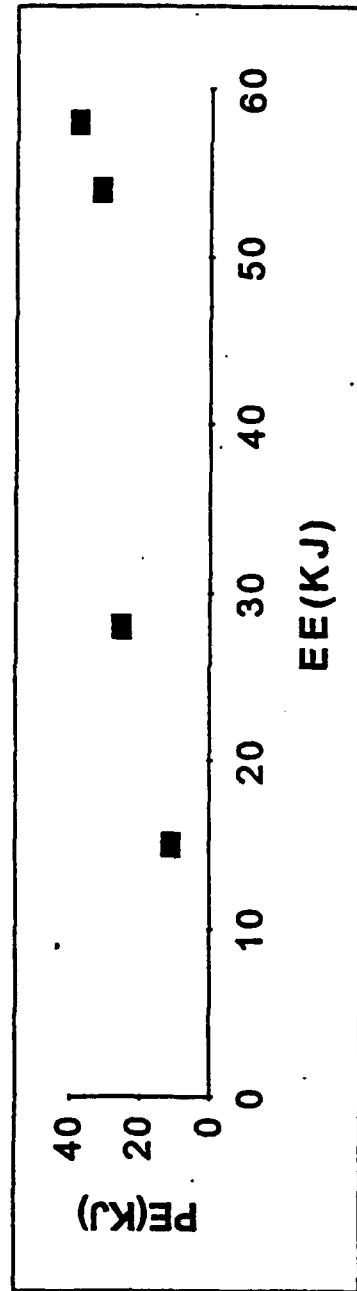
SHOT	P(MW)	EE(KJ)	V(M/S)	PE(KJ)
1	16	30	316	17
5	15	15	271	12
7	30	29	342	19
9	12	8	192	6.1
11 MT	32	30	162	4.4
14 MT	47	30	218	7.9



JA2 MONOLITHS

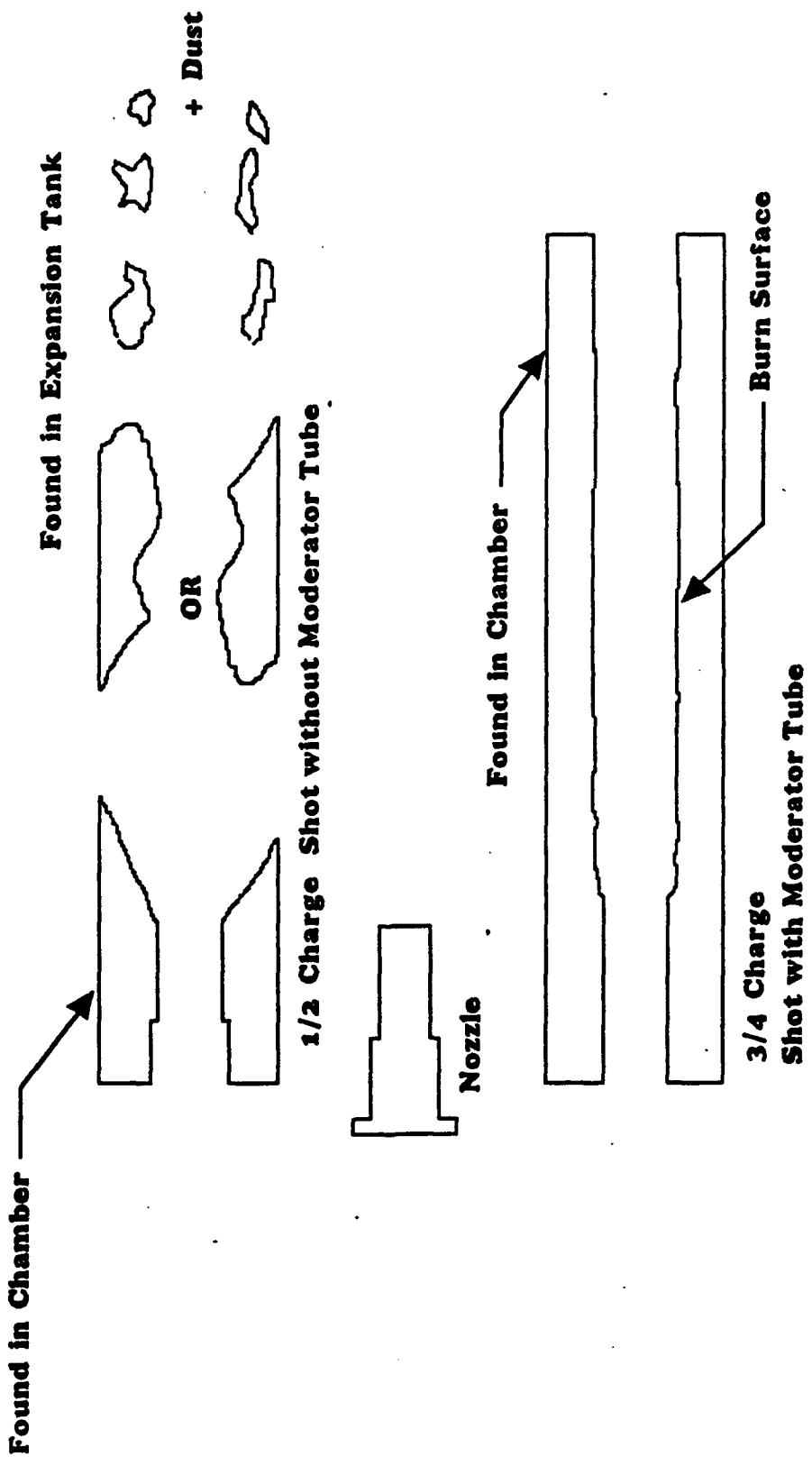
HALF CHARGE

SHOT	P(MW)	EE(KJ)	V(M/S)	PE(KJ)
2	33	58	478	38
6	30	28	386	2.5
8	60	54	433	31
10	22	15	260	11
12	55	54	358	21
15	31	57	365	22



SHOT NUMB	PROP TANK FILL RESIDUE GM	Chamber Residue gm	Barrel Residue gm	
			TRACE	0.9
1	41.3	18.4	Broken not burned	TRACE
2	83.8	32.5	Some burned	TRACE
3	130.8	57.8	18 chunks, 40 dust	TRACE
4	176.1	27.1	powder	3.9 pieces, burned
5	41.3	10.0	powder	TRACE melt down
6	85.1	48.4	28 chunks, 20 powder	17.3 cracked, burned
7	41.2	20.8	11 chunks, 10 dust	18.0 cracked, burned
8	84.9	55.0	22 chunks, 33 dust	16.6 large pieces, burned
9	41.0	21.0	few chunks, rest dust	TRACE
10	84.7	44.7	5 chunks, 40 dust	10.0 pieces, burned
11	38.5	7.7	dust	37.8 whole
12	78.9	6.3	dust	LIQUID
13	78.0	10.9	dust	0.1
14	38.5	8.9	dust	66.8 cracked, burned
15	120.5	18.0	few chunks, rest dust	32.9 cracked, burned
16	162.5	69.0	26 chunks, 43 dust	109.9 whole
17	121.4	65.1	dust	0.2
18	156.2	87.4	27 chunks, 61 dust	0.7
			NONE	NONE
				1.3

Residue



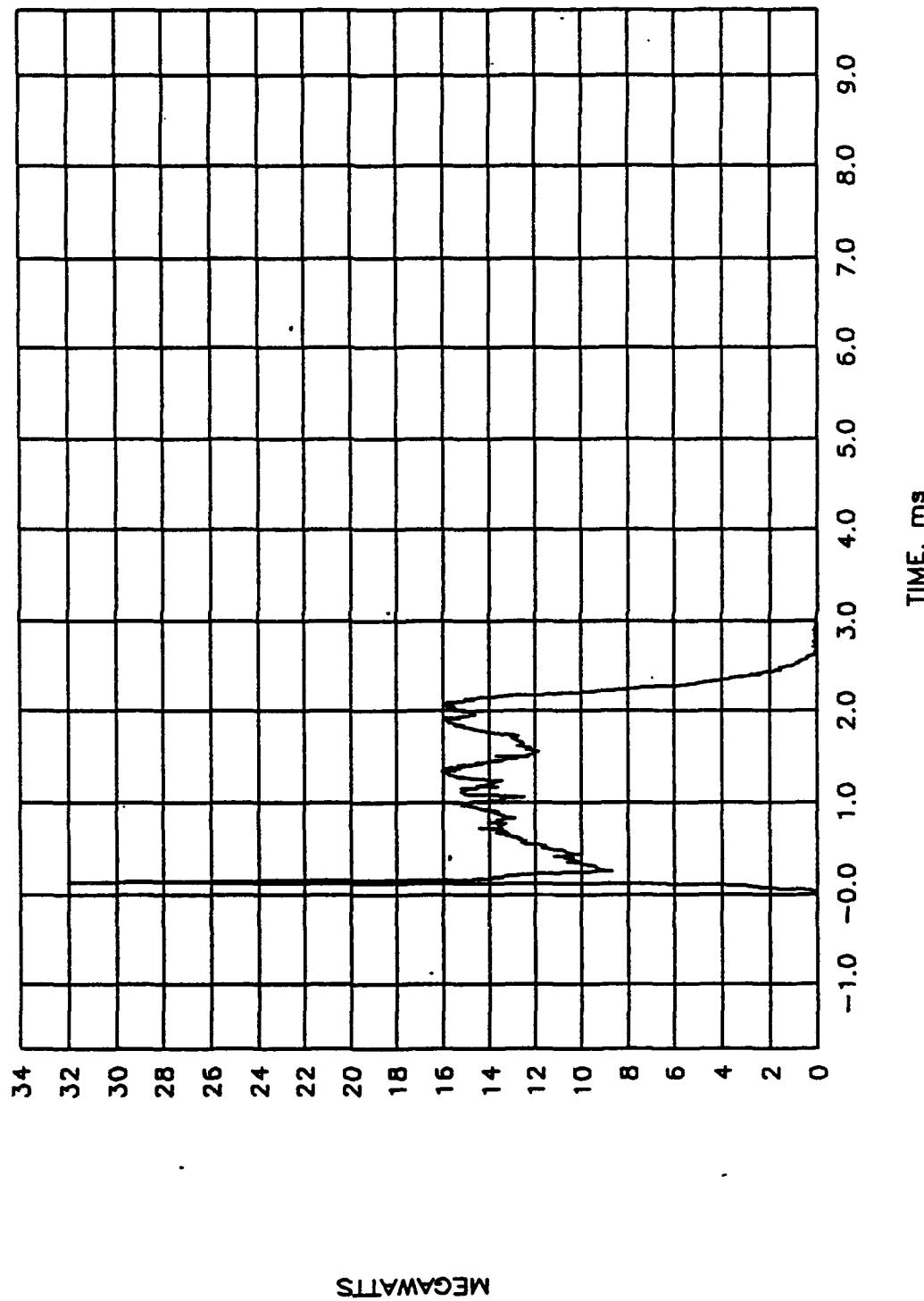
JA2 MONOLITHS BURNING RATES

$$r = b [P_{mean}]^{\alpha} + c v$$

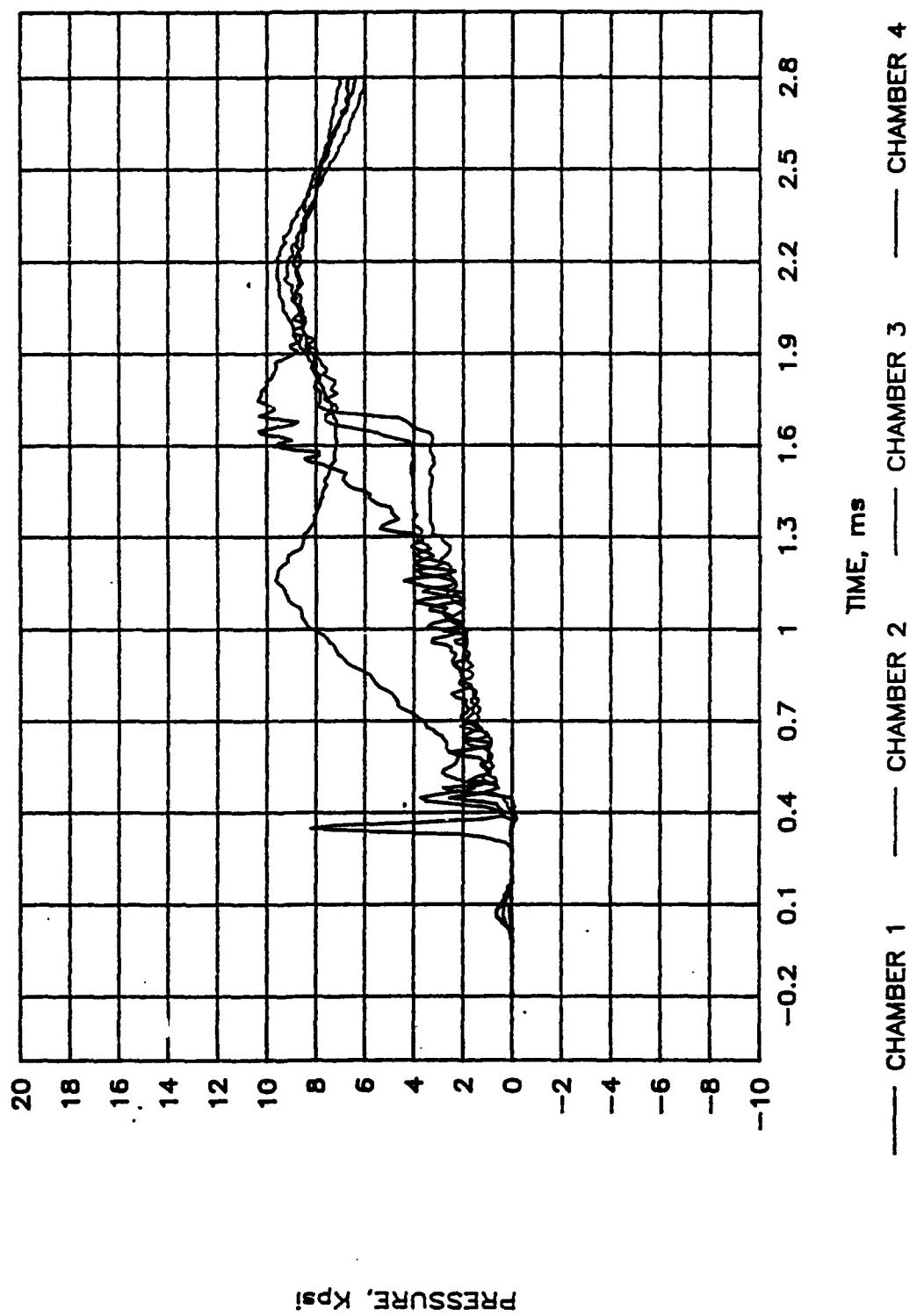
$v = v_p$ proj velocity for prop/gas surface

$v = v_j$ plasma velocity for prop/plasma surface

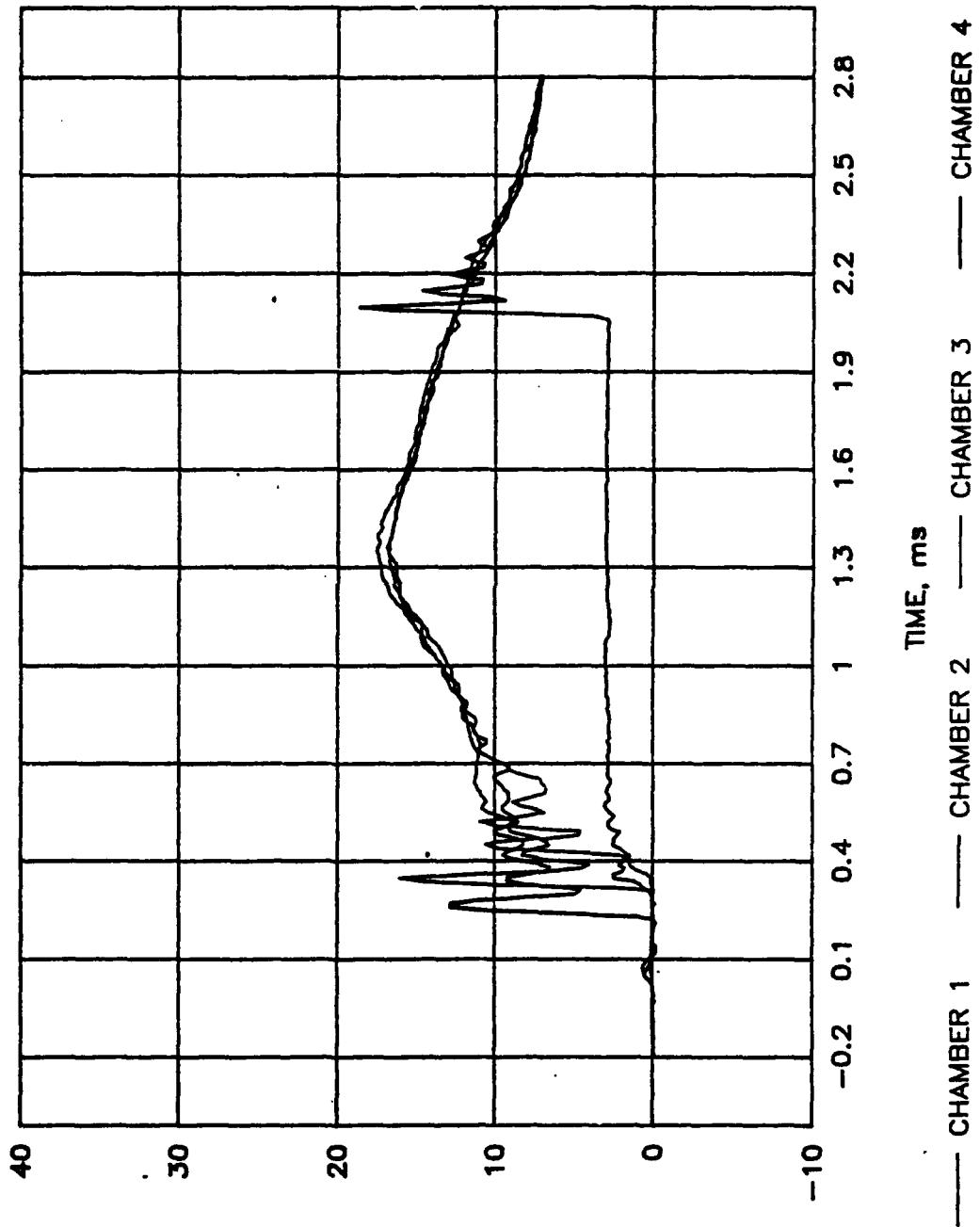
POWER
OCC01 4-8-93



ALL CHAMBERS
OCC01 4-8-93

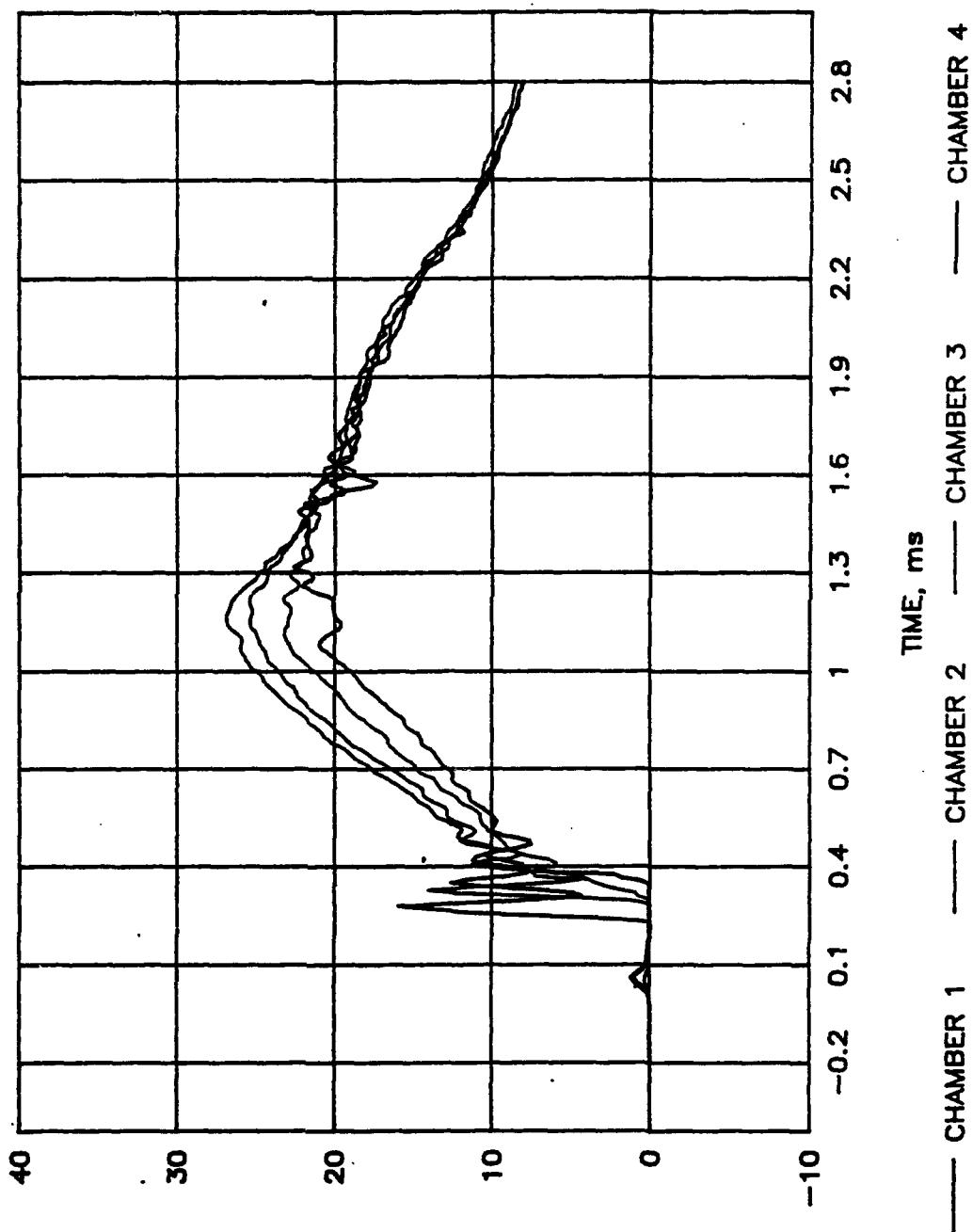


ALL CHAMBERS
OCC02 4-8-93

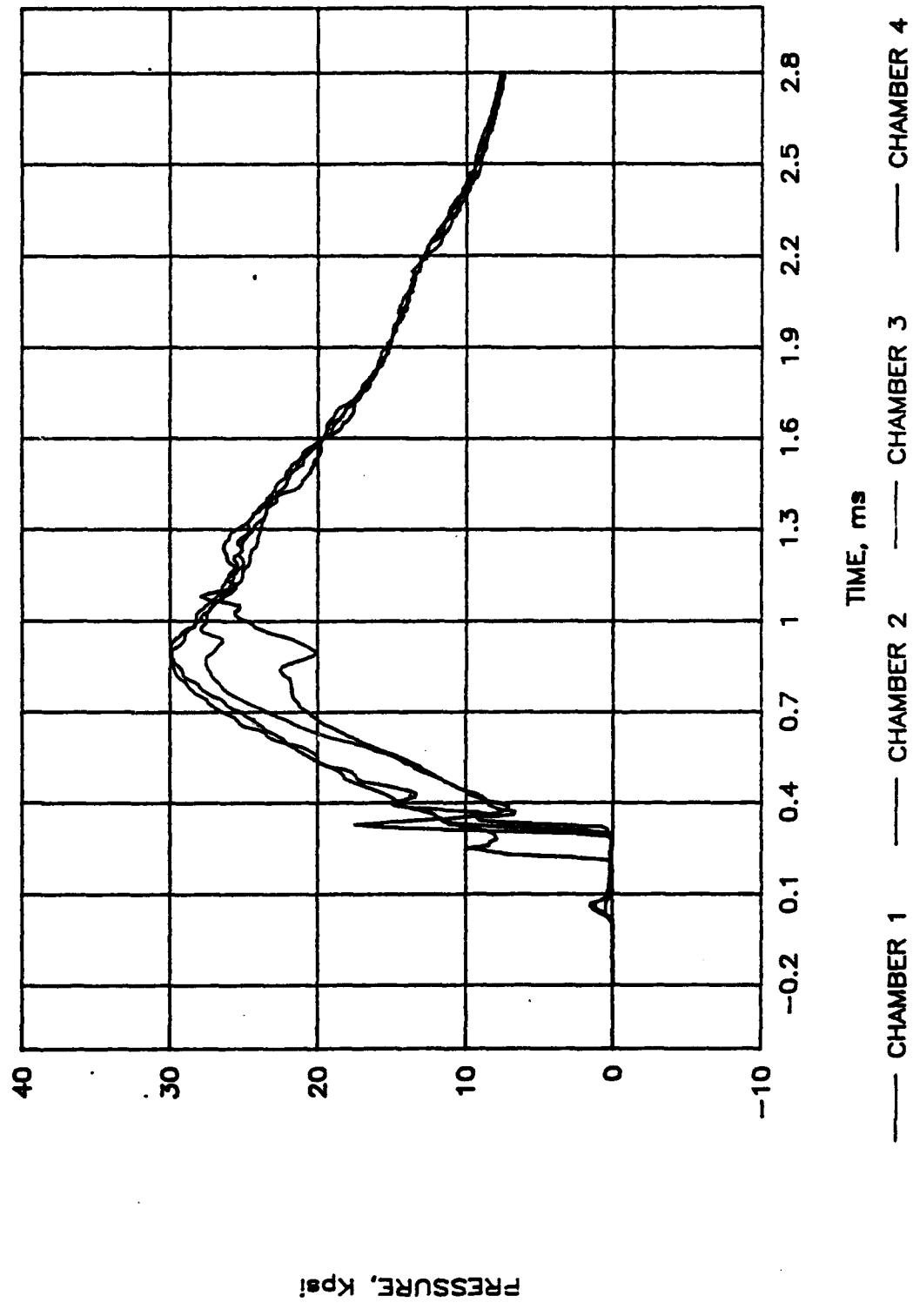


ALL CHAMBERS

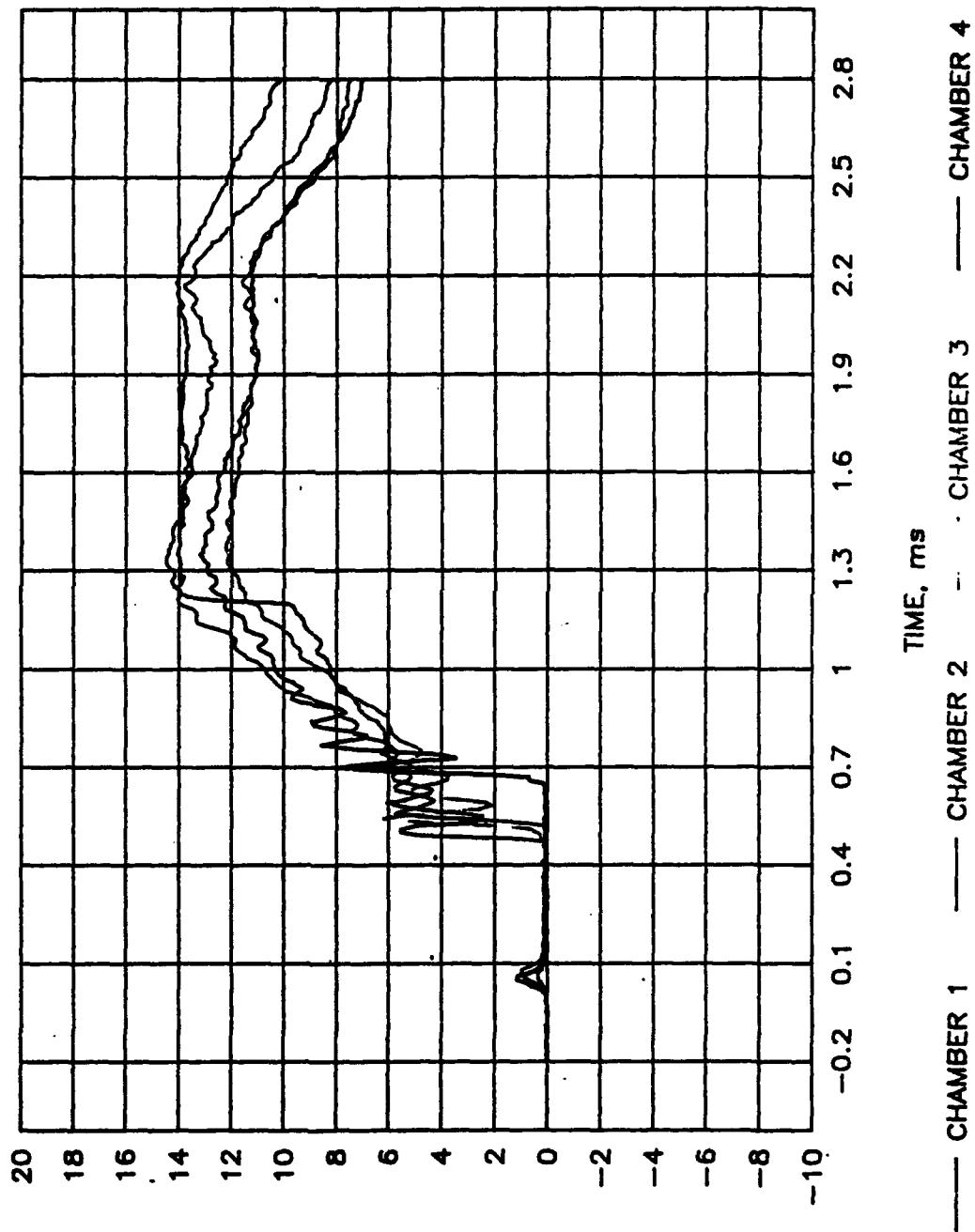
OCC03 4-14-93



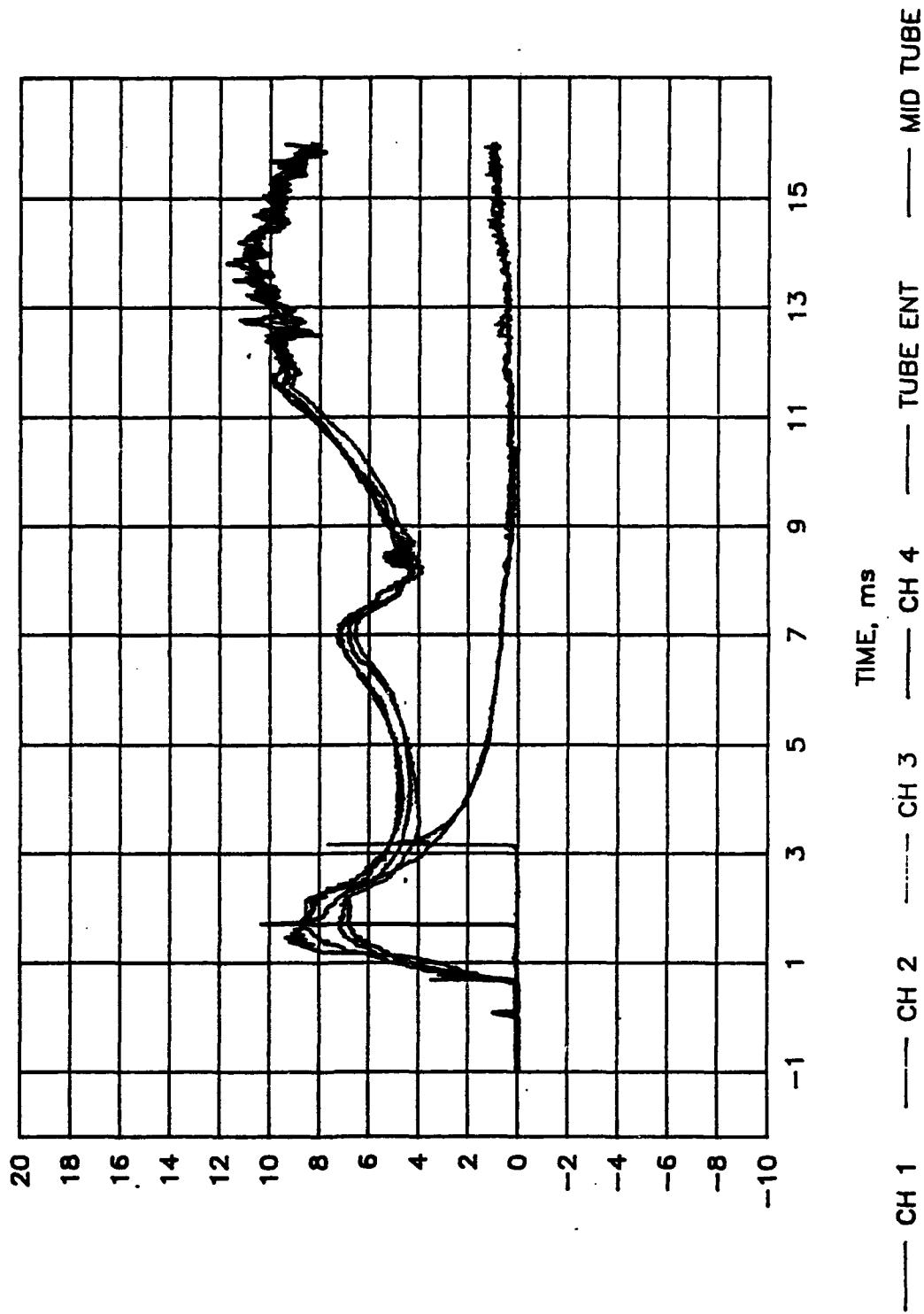
ALL CHAMBERS
OCC04 4-14-93



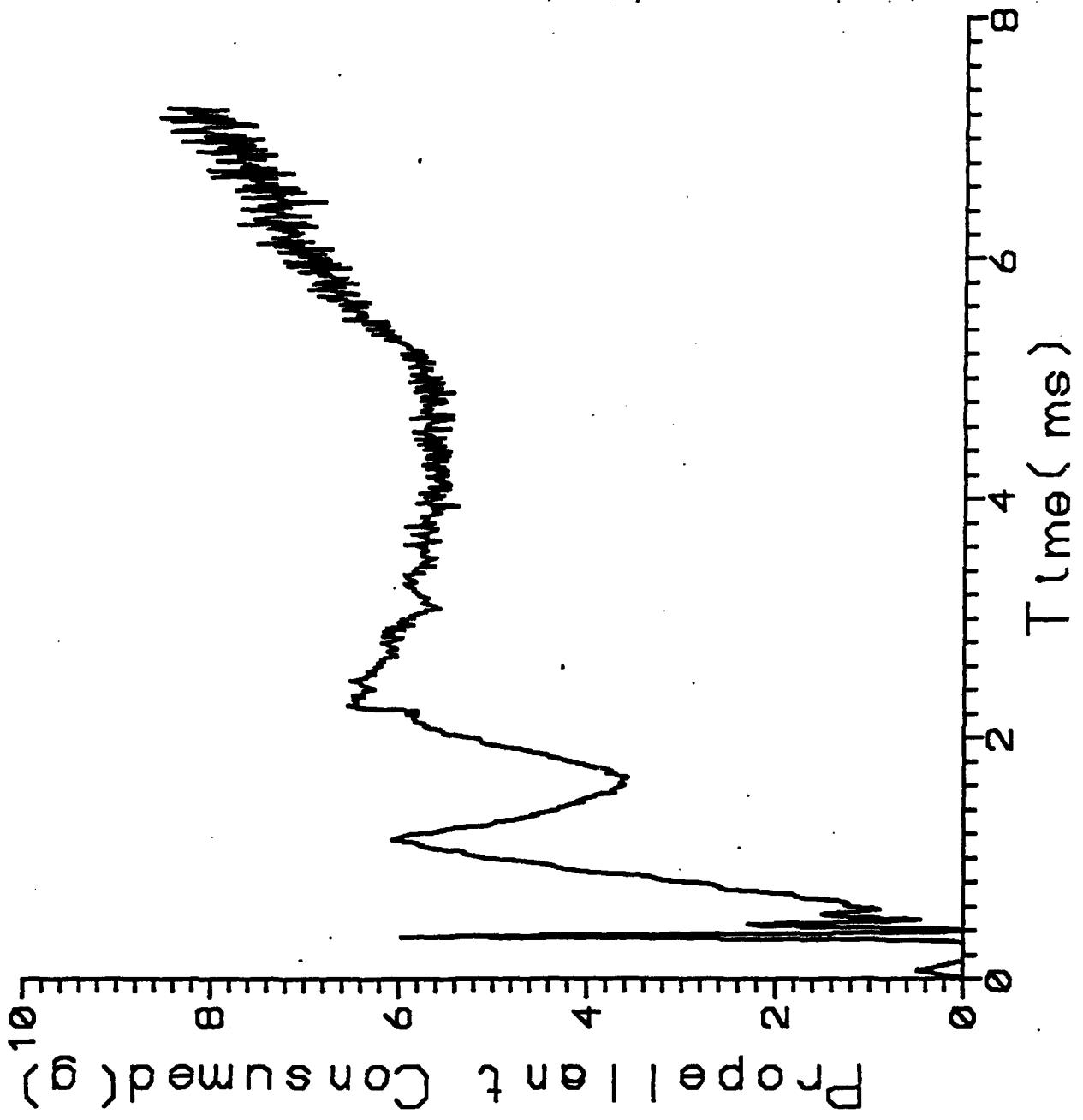
ALL CHAMBERS
OCC15 4-27-93



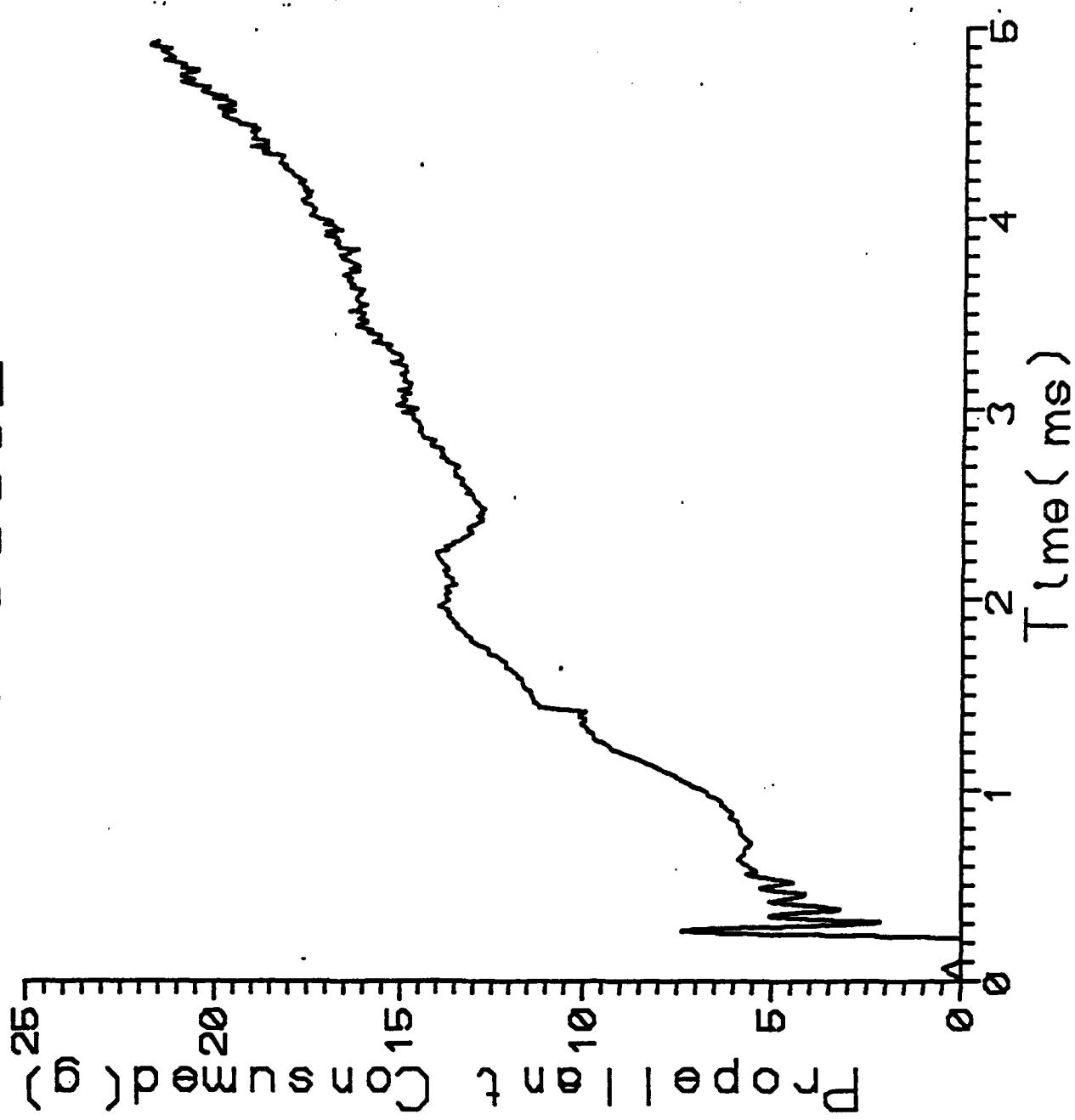
ALL PRESSURES
OCC17 4-28-93



Shot 00001



Shot 00002



Evidence Concerning Plasma Enhanced Erosive Burning

- For
 - Shape of large residual grains
 - Smooth pt and inverse cp traces
 - Higher than predicted pressure and velocity
- Against
 - residue
 - Some cracking in larger grains
- **More data will be obtained in the at least six remaining shots**

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DROPLET ENTRAINMENT AND BREAKUP BY SHEAR FLOWS*

Kenneth K. Kuo and F. Bill Cheung

**(Presented in the ETC Modeling Workshop at the Army
Research Laboratory, Aberdeen Proving Ground, MD)**

May 12, 1993

- * Work sponsored by the U. S. Army Research Laboratory under Contract No. DAAA15-92-D-0011. The support and encouragement of Gloria P. Wren are highly appreciated.

OBJECTIVES

- To evaluate the applicability of existing correlations for describing the entrainment and subsequent breakup of the liquid propellant droplets caused by the discharge of a plasma jet from a plasma generating cartridge.
- To identify the key elements of plasma/liquid propellants interaction that are not fully understood.
- To summarize the findings of this critical review and to define basic research needs for future modeling and diagnostic activities in this subject area.
- To perform a theoretical analysis to provide guidance in the development of a suitable correlation applicable to ETC gun conditions.

CHARACTERISTIC LENGTH AND VELOCITY SCALES

- Two Macro-Length Scales

d_h — Hydraulic Diameter of the Core Region
(Associated with phenomena of the Interfacial Shear Action and Inertia of the Core Flow)

δ — Liquid Film Thickness
(Associated with Phenomena of Liquid-Film Motion and Induced Surface Wave Form)

- One Micro-Length Scale

l_{TW} — Taylor Wavelength
(On the same Order as Ligament or Initial Droplet Size Before Secondary Breakup)

$$l_{TW} = \left[\frac{\sigma}{g (\rho_f - \rho_g)} \right]^{1/2}$$

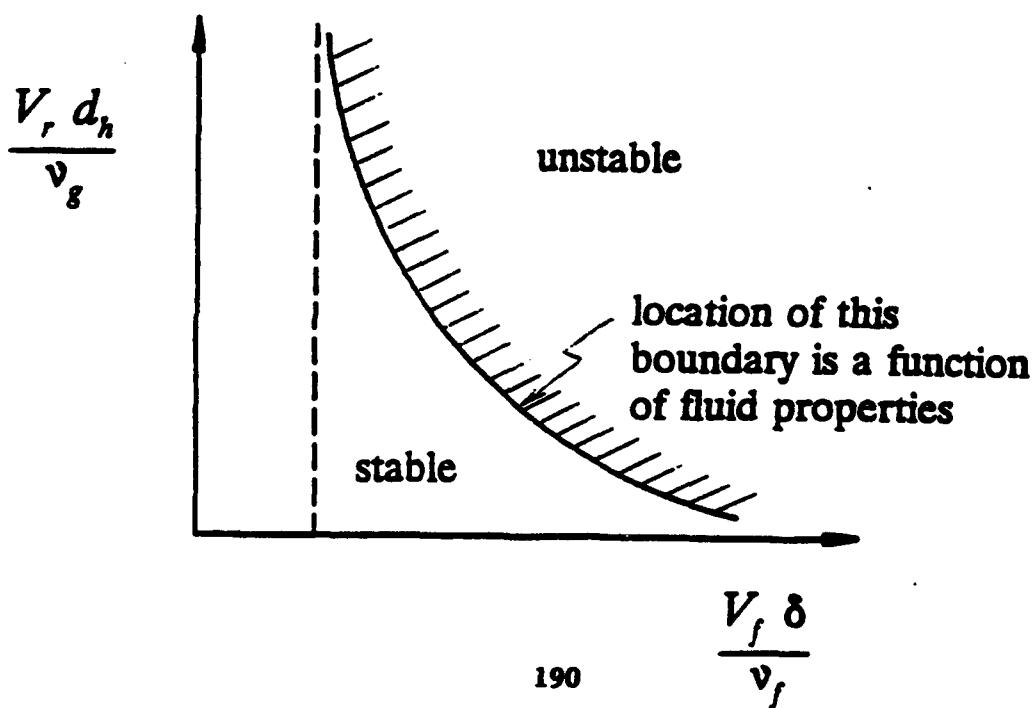
- Two Independent Velocity Scales

{ V_f — Bulk Liquid Film Velocity
 V_r — Relative Velocity Between Gas and Liquid Phases ($V_r = V_g - V_f$)

or

OBSERVATIONS OF ENTRAINMENT PHENOMENA

- Similarities exist between the entrainment of liquid propellant by a plasma jet in an ETC gun and entrainment of droplets in two-phase annular mist flow.
- The interface of the two fluids is inherently unstable.
- When $V_r > (V_r)_{\text{critical}}$ or $V_f > (V_f)_{\text{critical}}$, instabilities set in and grow in the interfacial region.
 - formation of wavy interface and large amplitude roll wave (so-called Kelvin-Helmholtz instability)
 - ligaments and droplets torn off from the interface dynamic interaction
- Critical Conditions for the Onset of Entrainment:



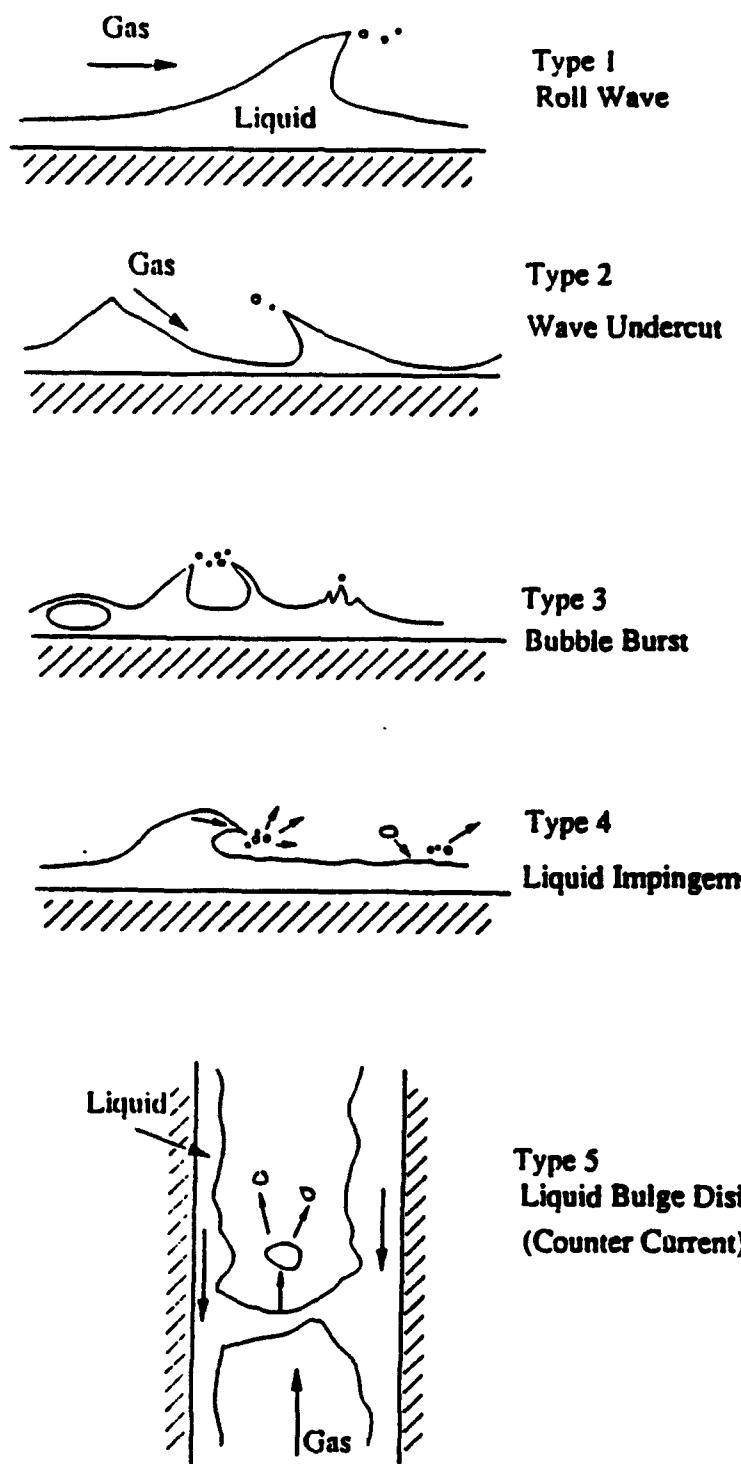
OBSERVATIONS OF ENTRAINMENT PHENOMENA

(continued)

- Detailed studies of entrainment mechanism have been performed by Newitt et al. (1954), Hanratty and Hershman (1961), Chung and Murgatroyd (1965), and Ishii and Grolmes (1975).
- In general, entrainment may take place in a number of different ways, depending on the flow situation.
- Hydrodynamic and surface tension forces govern the motion and deformation of the wave crests. Under certain conditions, these forces lead to an extreme deformation of the interface that results in the breakup of a portion of a wave into liquid droplets. The forces acting on the wave crests depend on the flow pattern around them as well as on the shape of the interface.

RELEVANT ARTICLES ON ENTRAINMENT MECHANISM STUDIES

- "Liquid Entrainment: The Mechanism of Drop Formation from Gas or Vapor Bubbles," Newitt, D. M., Dombrowski, N. and Knelman, F. H., *Tran. Inst. Chem. Engng.*, Vol. 32, p. 244, 1954.
- "Fundamentals of the Hydrodynamic Mechanism of Splitting in Dispersion Process," Hinze, J. O., *AICHE J.*, Vol. 1, p. 289, 1955.
- "Initiation of Roll Wave," Hanratty, T. J. and Hershman, A., *AICHE J.*, Vol. 7, p. 488, 1961.
- "Studies of the Mechanism of Roll Wave Formation on Thin Liquid Films," Chung, H. S. and Murgatroyd, W., *Symp. on Two-Phase Flow*, Vol. 2, Paper A2, Exeter, UK, 1965
- "Prediction of Onset of Entrainment for Liquid Metals," Ishii, M. and Grolmes, M., *Trans. Am. Nucl. Soc.*, Vol. 21, p. 325, 1975



A Schematic Diagram Showing the Five Types of Entrainment Mechanisms

FIVE BASIC TYPES OF ENTRAINMENT MECHANISMS FOR TWO-PHASE ANNULAR MIST FLOW [ISHII AND GROLMES (1975)]

ROLL WAVE:

The drag force acting on the wave tops deforms the interface against the retaining force of the liquid surface tension. The tops of the large amplitude roll waves are sheared off from the wave crest by the gas flow and then broken into small droplets. (most relevant to ETC gun conditions)

WAVE UNDERCUT:

Entrainment is caused by the undercutting of the liquid film by the gas flow. This mechanism is similar to droplet disintegration by the gas stream. (could also happen in ETC gun condition)

BUBBLE BURST:

Associated with the bursting of gas bubbles. The droplets may be generated by the bubble rising to the surface of a liquid.

LIQUID IMPINGEMENT:

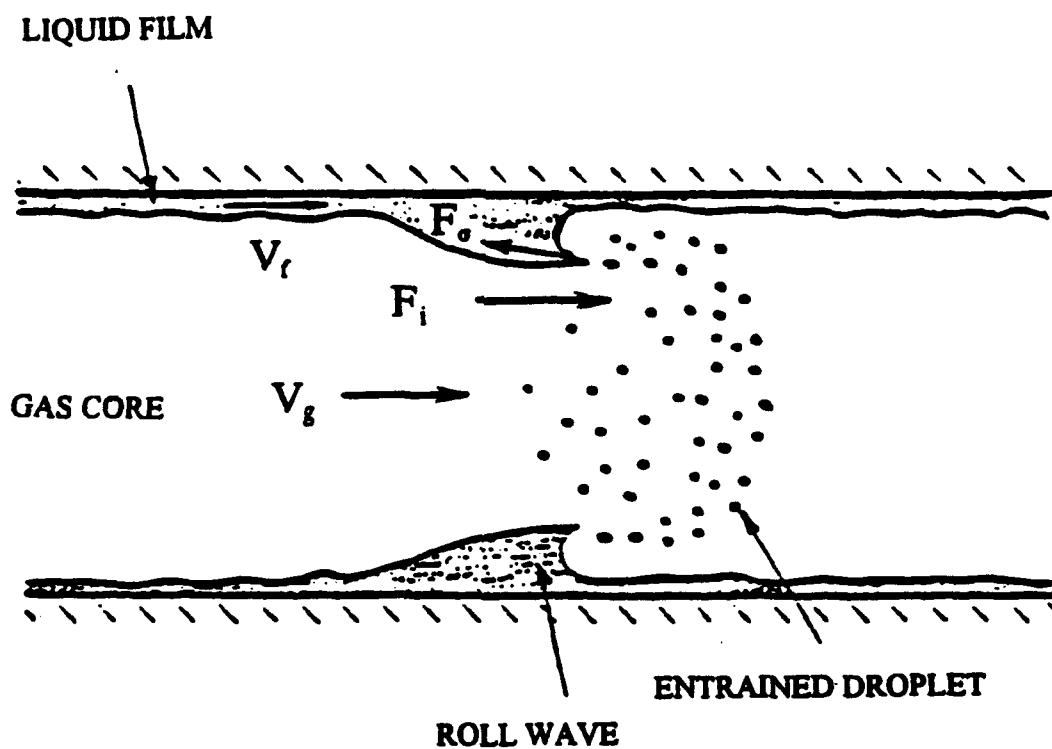
This is caused by the impingement of relatively large liquid droplets to the film interface for production of small droplets.

LIQUID BULGE DISINTEGRATION:

When a counter-current flow reaches the flooding condition, large amplitude waves can emerge from the liquid film and coalesce to form a bridge. Bulged regions of the bridge can then disintegrate into small droplets due to the gas dynamics. (not relevant to ETC gun conditions)

ONSET OF KELVIN-HELMHOLTZ INSTABILITY

- When both the gas flow and the induced liquid film motion are sufficiently high, the interfacial waves transform into large amplitude roll waves.
- Beyond this critical point, the interfacial shear forces become greater than the surface tension forces, and the onset of entrainment occurs.



ONSET OF ENTRAINMENT

- The criterion developed by Ishii and Grolmes (1975) was based upon a force balance at the crest of roll waves. Droplet entrainment starts when

$$F_i > F_o$$

[interfacial shear force] [surface tension retaining force]

- The dimensionless critical superficial gas velocity at the onset of entrainment was found to depend on the film Reynolds number and the viscosity number of the fluids, i. e.

$$(J_g)_{\text{critical}} = f(Re_f, N_\mu)$$

$$Re_f \equiv \frac{\rho_f j_f d_h}{\mu_f}$$

$$N_\mu \equiv \frac{\mu_f}{[\rho_f \sigma l_{TW}]^2} = \frac{\mu_f}{\left[\rho_f \sigma \left(\frac{\sigma}{g(\rho_f - \rho_g)} \right)^{\frac{1}{2}} \right]^2}$$

where ρ_f and μ_f are the density and viscosity of the liquid, d_h the hydraulic diameter of the cone, and j_f the superficial velocity of the liquid (including liquid film and droplets).

- J_g is defined as

$$\begin{aligned}
 J_g &\equiv \frac{j_g}{(\sigma / \mu_f)} \left(\frac{\rho_g}{\rho_f} \right)^{\frac{1}{2}} = \left(\frac{\rho_g j_g^2 d_h}{\sigma} \right) \left(\frac{\mu_g}{\rho_g j_g d_h} \right) \left(\frac{\mu_f}{\mu_g} \right) \left(\frac{\rho_g}{\rho_f} \right)^{\frac{1}{2}} \\
 &= We_g \quad (Re_g)^{-1} \left(\frac{\mu_f}{\mu_g} \right) \left(\frac{\rho_g}{\rho_f} \right)^{\frac{1}{2}}
 \end{aligned}$$

ONSET OF ENTRAINMENT (continued)

- For a horizontal two-phase annular flow with $160 < Re_f < 1635$, the criterion of Ishii and Grolmes (1975) gives

$$J_g \geq 11.78 N_\mu^{0.8} Re_f^{-1/3} \quad \text{for } N_\mu \leq \frac{1}{15}$$

and

$$J_g \geq 1.35 Re_f^{-1/3} \quad \text{for } N_\mu > \frac{1}{15}$$

- For values of Re_f that are above 1635, a so-called completely rough turbulent regime occurs in which the critical superficial gas velocity becomes independent of the film Reynolds number. According to Ishii and Grolmes (1975), the inception criterion for this flow regime is given by

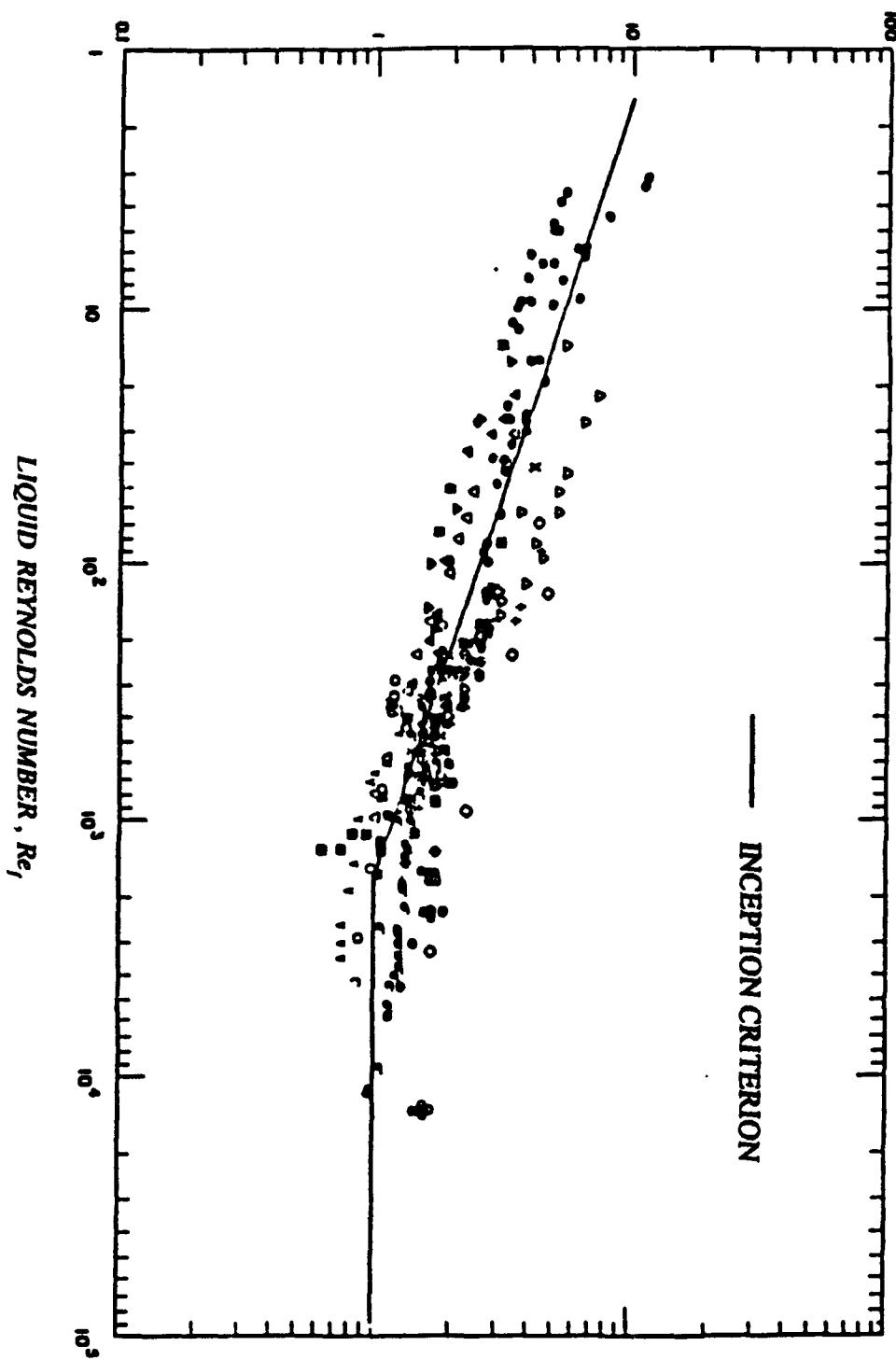
$$J_g \geq N_\mu^{0.8} \quad \text{for } N_\mu \leq \frac{1}{15}$$

and

$$J_g \geq 0.1146 \quad \text{for } N_\mu > \frac{1}{15}$$

- The inception criterion compares favorably with a large number of experimental data for various types of fluids covering a wide range of the film Reynolds numbers and the viscosity number.
- The inception criterion of Ishii and Grolmes should be applicable to the case of plasma/liquid propellants interaction provided that fluid properties are known.

$$\text{DIMENSIONLESS GAS VELOCITY} \times \left(\frac{1}{N_s}\right)^{0.8} = \frac{u_g j_t}{\sigma} \sqrt{\frac{\rho_g}{\rho_l}} \left(\frac{1}{N_s}\right)^{0.8}$$



Comparison of the Inception Criterion of Ishii and Groffnes with Data

METHODS FOR MEASURING THE FRACTION OF LIQUID MASS FLUX ENTRAINED IN THE GAS CORE

- Local Probe Measurements
 - To determine the axial liquid mass flux at the location of the sampling probe.
 - Used with limited success by Wicks and Dukler (1960), Magiros and Dukler (1961), Wallis (1962), Steen and Wallis (1964), Cousins et al. (1965), Gill and Hewitt (1968), and Yablonik and Khaimov (1972).
 - Measurement along the centerline with the assumption that the mass flux is radially uniform.
- Liquid Film Flow Measurements
 - Flow rate determined by removing liquid film completely from the test section.
 - This method, which eliminates those uncertainties associated with the local probe measurement, is probably a more accurate measurement technique.
 - Successfully employed by a number of investigators including Paleev and co-workers (1962, 1966), Cousins and Hewitt (1968), Petrovichev et al. (1971), and Ishii and Mishima (1981).

ENTRAINMENT CORRELATIONS

- **Purely Empirical Approach**
 - Wicks and Dukler (1960)
 - Minh and Huyghe (1965)
 - Paleev and Filipovich (1966)
 - Wallis (1968)
- **Semi-Empirical Approach Based Upon Mechanistic Models**
 - Hutchinson and Whalley (1973)
 - Dallman, Laurinat, and Hanratty (1984)
 - Ishii and Mishima (1989)

ENTRAINMENT CORRELATION OF WICKS AND DUKLER (1960)

- Developed a correlation that relates the entrainment parameter, R, to the Martinelli parameter X, i. e.

$$R = R(X)$$

- Entrainment Parameter:

$$R \equiv \frac{We_c (j_f / j_g)}{(dP/dz)_g} W_d$$

where W_d is the liquid drop mass flow rate, and We_c the critical Weber number defined in terms of the film thickness δ by

$$We_c \equiv \frac{\rho_g v_g^2 \delta}{\sigma}$$

where v_g is the velocity of the gas phase.

- Martinelli Parameter

$$X = \left[\frac{(dP/dz)_f}{(dP/dz)_g} \right]^{1/2}$$

where quantities in the numerator and denominator represent the single-phase pressure drops which would exist if each phase flowed alone.

- Two Major Drawbacks

- The dependence of the entrainment on various controlling factors is hidden by the use of the Martinelli parameter.
- The correlation is dimensional which severely limits the range of applicability.

ENTRAINMENT CORRELATION OF MINH AND HUYGHE (1965)

- Empirical correlation relates the entrained fraction, E, to the gas core momentum, i. e.

$$E = E(\bar{\rho}_g j_g^2)$$

where $\bar{\rho}_g$ is the homogeneous density of the gas core given by

$$\bar{\rho}_g = \rho_g \left(1 + \frac{\rho_f j_d}{\rho_g j_g} \right)$$

where j_d is the superficial velocity of the entrained liquid droplets.

- Entrained Fraction:

$$E = \frac{W_d}{W_f} = \frac{j_d}{j_f}$$

where W_d is the mass flow rate of the droplets and W_f the total liquid mass flow rate including both the liquid film and the droplets.

- Two Major Drawbacks

- The use of the dimensional parameters results in uncertainties regarding the dependence of the correlation on the fluid properties.
- The range of applicability is virtually unknown as the effects of many important factors such as the liquid Reynolds number are not included.

ENTRAINMENT CORRELATION OF PALEEV AND FILIPOVICH (1966)

- The shortcoming in the Minh and Huyghe correlation (1965) was eliminated by introducing a dimensionless gas flux in correlating the entrained fraction in the following form.

$$\frac{W_{ff}}{W_f} = 0.985 - 0.44 \log \left[\frac{\bar{\rho}}{\rho_f} \left(\frac{\mu_f j_g}{\sigma} \right)^2 \times 10^4 \right]$$

where W_{ff} is the mass flow rate of the film and W_f the total liquid flow rate including the film and droplets.

- Entrained Fraction:

$$E = 1 - \frac{W_{ff}}{W_f}$$

- This correlation showed fairly good agreement with a limited number of data.
- Major Drawback
 - The range of applicability is not well defined as the important effects of the hydraulic diameter and the Reynolds number were not included.
 - The dimensionless gas flux is very similar to J_g used in the onset of entrainment.

ENTRAINMENT CORRELATION OF WALLIS (1968)

- In an effort to improve the correlation of Paleev and Filipovich (1966), Wallis introduced a modified dimensionless gas flux (π) by replacing the liquid viscosity by the gas viscosity in the Paleev and Filipovich correlation, i. e.

$$E = E(\pi)$$

where

$$\pi = \left(\frac{\nu_g \mu_g}{\sigma} \right) \left(\frac{\rho_g}{\rho_f} \right)^{\frac{1}{2}}$$

- Major Drawbacks
 - The range of applicability is not well defined.
 - The dimensionless gas flux is not general enough to account for the effect of fluid properties.

ENTRAINMENT CORRELATION OF HUTCHINSON AND WHALLEY (1973)

- Proposed a mechanistic model to correlate the rates of entrainment and deposition of droplets to the liquid film.
- The deposition rate is taken to be a linear function of the droplet concentration in the gas core, i. e.,

$$\dot{D} = k C$$

where k is the mass transfer coefficient.

- The entrainment rate is considered proportional to the equilibrium concentration, i. e.

$$\dot{E} = k C_e$$

The equilibrium concentration is correlated in a functional form given by

$$C_e = C_e \left(\frac{\tau_i \delta}{\sigma} \right)$$

where τ_i is the interfacial shear of the two-phase flow and δ the liquid film thickness.

- Major Drawbacks
 - It is difficult to accurately determine the equilibrium concentration. The data for this quantity showed considerable scattering, sometimes up to more than an order of magnitude.
 - In order to estimate the entrainment, two different correlations, i. e., one for the entrainment rate and the other for the deposition rate, need to be employed. Any error in determining the deposition would add to the error associated with the entrainment rate.
 - Conceptually, the entrainment rate is not dictated by the equilibrium concentration.

ENTRAINMENT CORRELATION OF DALLMAN, LAURINAT AND HANRATTY (1984)

- Conducted an experimental study of horizontal annular two-phase flow using air and water.
- The amount of liquid entrained in the gas flow is assumed to be governed by a dynamic balance between the rate of atomization of the liquid film and the rate of deposition of droplets from the gas core.
- The rate of deposition of liquid droplets was considered to vary linearly with the concentration of the droplets whereas the rate of atomization of the liquid film was assumed to vary linearly with the liquid film flow rate.
- Entrainment Correlation Developed:

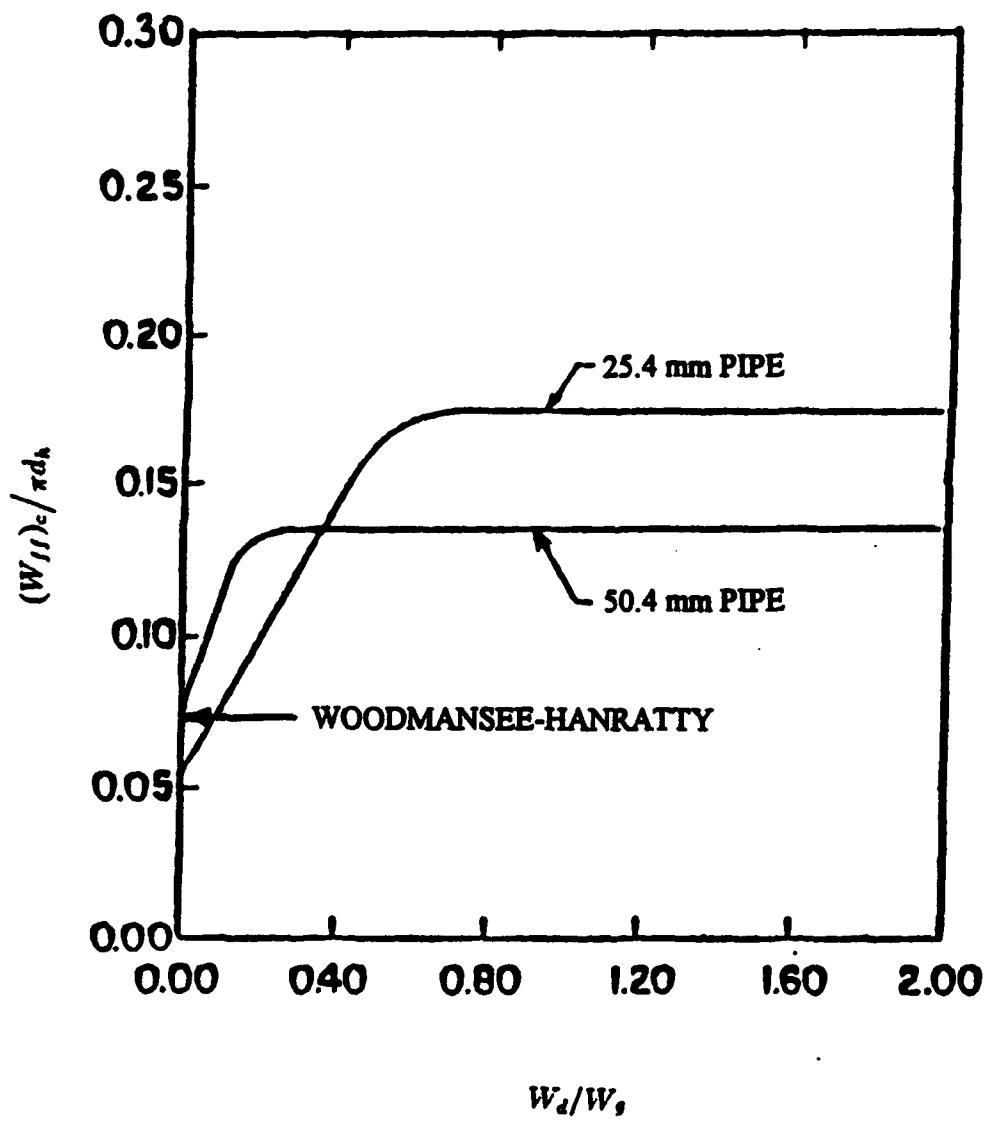
$$\frac{E}{E_m} = \frac{A [(d_h - 2\delta) \rho_g^{1/2} \rho_f^{1/2} v_g^3]^{1.5}}{1 + A [(d_h - 2\delta) \rho_g^{1/2} \rho_f^{1/2} v_g^3]^{1.5}}$$

where A is a dimensional constant having the value of 3.6×10^{-8} in SI unit and E_m the maximum entrainment fraction. The latter quantity is given by

$$E_m = 1 - \frac{(W_{ff})_c}{W_f}$$

where $(W_{ff})_c$ is the so-called critical film flow rate.

- Critical Film Flowrate
 - The critical film flow rate has been determined by Dallman et al. (1984) as a function of the ratio between the droplet mass flow rate and the mass flow rate of the gas.



Variation of the Critical Film Flow Rate with the Mass-Flow-Rate Ratio

**ENTRAINMENT CORRELATION OF DALLMAN,
LAURINAT AND HANRATTY (1984)**
(continued)

● Major Drawbacks:

- The correlation is given in dimensional form; thus, the applicability is limited.
- The effect of fluid properties are not included.
- While the concept of critical film flow rate is correct, the functional dependence of $(W_{ff})_c$ is generally unknown.
- The correlation is cumbersome as E_m and δ are unknown quantities.

ENTRAINMENT CORRELATION OF ISHII AND MISHIMA (1989)

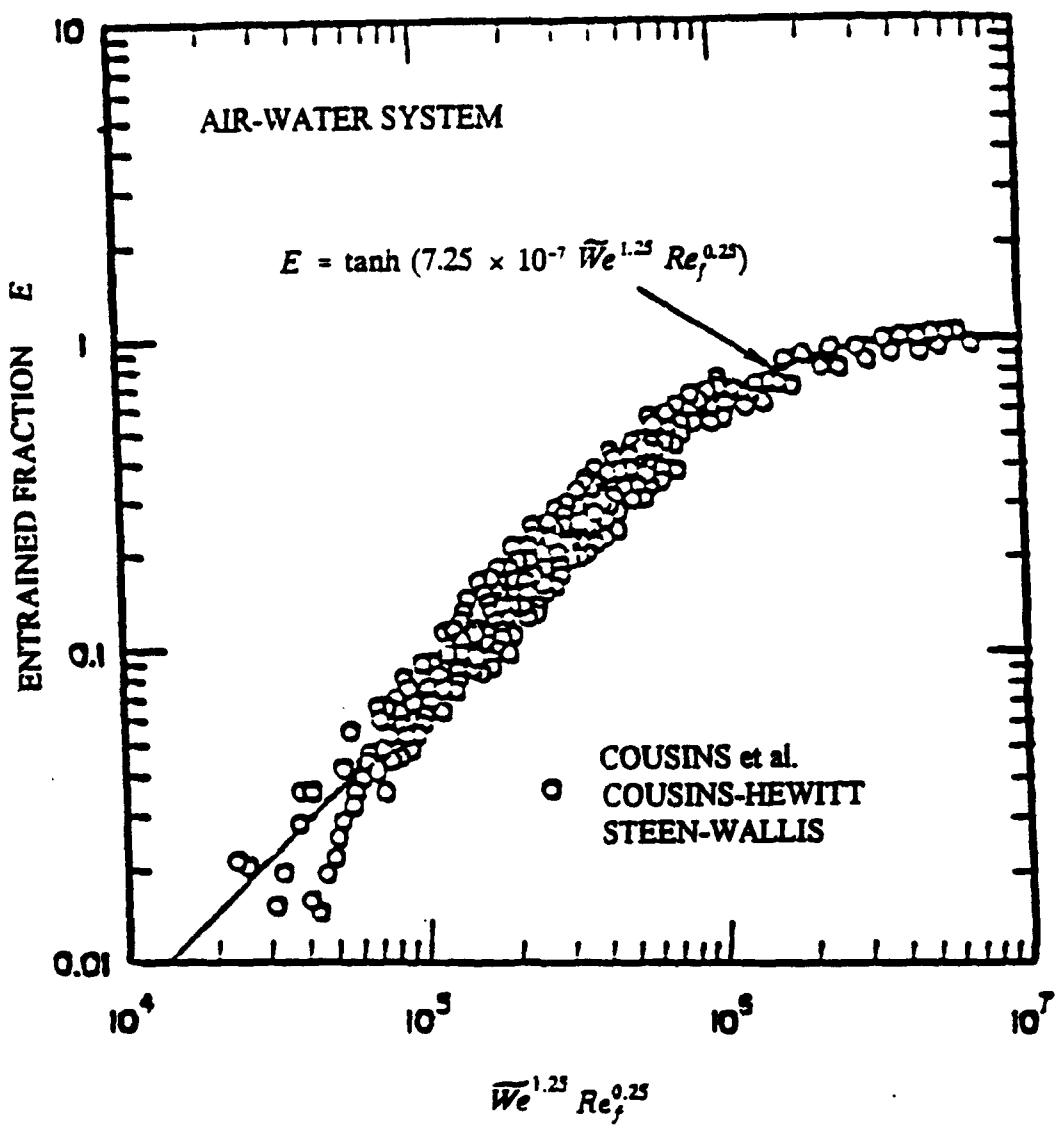
- Based upon the mechanism of roll wave entrainment: The shearing off of roll wave crests was considered to be the dominant mechanism of liquid entrainment.
- Droplet entrainment would result whenever the retaining force of surface tension is exceeded by the interfacial shear force.
- The same forces controlling the onset of entrainment were assumed to control the entrainment itself. However, a modification of the inertia of the gas core flow was made to account for the effect of droplet inertia, since there are many droplets flowing in the gas core.
- Under an equilibrium condition in which the deposition rate exactly balances the entrainment rate, the entrained fraction was correlated in the following form:

$$E = \tanh (7.25 \times 10^{-7} \tilde{We}^{1.25} Re_f^{0.25})$$

where \tilde{We} is an effective gas-phase Weber number defined by

$$\tilde{We} = \frac{\rho_g j_g^2 d_h}{\sigma} \left(\frac{\rho_f - \rho_g}{\rho_g} \right)^{\frac{1}{3}}$$

- The Ishii and Mishima correlation, which compares favorably with a large number of data , is probably the best correlation available today.
- Unfortunately, the entrained fraction represents the equilibrium value that includes the contribution due to droplet deposition. Thus, this correlation tends to underestimate the actual entrainment rate in the ETC gun environment.



Comparison of the Entrainment Correlation of Ishii and Mishima with Data

SPECIAL FEATURES OF DROPLET ENTRAINMENT IN AN ETC GUN ENVIRONMENT

- Droplet life times are relatively short due to
 - High rates of heat transfer
 - Evaporation, thermal decomposition, and combustion
 - Secondary breakup to smaller droplets by highly turbulent flow conditions
- The deposition rate is negligible since the droplets have very little chance to return to liquid film before they are totally consumed. The absence of the deposition process in an ETC gun represents a unique feature which is different from all annular two-phase flows studied by previous researchers.
- For ETC guns utilizing piccolo igniters, the phenomena of mixing of plasma and liquid propellants involve two sequential stages.
 - 1) Development of numerous mini-Taylor cavities and subsequent expansion of cavity sizes.
 - 2) Merging of mini-Taylor cavities onto a single large cavity.

RESEARCH NEEDS ON DROPLET ENTRAINMENT

- The single most important element in accurate prediction of the performance of ETC guns is the droplet entrainment rate, since it controls the rate of conversion of chemical energy into propulsive energy.
- A suitable entrainment correlation, excluding the effect of droplet deposition, should be developed for ETC gun application. This can be accomplished by performing an experimental study to measure the rate of entrainment for the case without the effect of deposition.
- In order to develop a realistic model for simulating the mixing phenomena of plasma jets and liquid propellants in ETC guns using piccolo igniters, it is useful to conduct detailed observations of the evolution of mini-Taylor cavities.

THEORETICAL ANALYSIS OF DROPLET ENTRAINMENT IN AN ETC GUN ENVIRONMENT

- The starting point of the analysis is the selection of an appropriate inception criterion. Since the roll wave mechanism is the prevailing mechanism of entrainment during plasma/liquid propellant interaction in an ETC gun, it is deemed appropriate to adopt the inception criterion of Ishii and Grolmes (1975) in the present analysis.
- Owing to the relatively high velocity of the plasma jet, the plasma/liquid propellant system in an ETC gun is likely to be significantly above the inception criterion. However, there is a potential for the liquid film Reynolds number to be reduced to a critical value as the liquid film thickness decreases. Below this critical Re_f , no further entrainment is possible.

THEORETICAL ANALYSIS OF DROPLET ENTRAINMENT IN AN ETC GUN ENVIRONMENT

(continued)

- An upper theoretical limit for the entrained fraction may thus be determined by assuming that the liquid film flow rate is given by the critical condition for the onset of entrainment:

$$(Re_f)_c^{1/3} = 11.78 N_{\mu}^{0.8} \left(\frac{\sigma}{\mu_f j_g} \right) \left(\frac{\rho_f}{\rho_g} \right)^{1/2}$$

where $(Re_f)_c$ is now the critical Reynolds number on the critical film flow rate introduced initially by Dallman, Laurinat and Hanratty (1984).

- The critical Reynolds number is defined by

$$(Re_f)_c = \frac{\rho_f (j_{ff})_c d_h}{\mu_f}$$

where $(j_{ff})_c$ is the critical superficial velocity of the liquid film. The use of this definition in the above equation is equivalent to ignoring the effect of droplets in determining the critical condition.

- In terms of the liquid film Reynolds number (Re_f) , the critical superficial velocity of the liquid film is given by

$$(j_{ff})_c = \frac{j_f}{Re_f} \left[11.78 N_{\mu}^{0.8} \left(\frac{\sigma}{\mu_f j_g} \right) \left(\frac{\rho_f}{\rho_g} \right)^{1/2} \right]^3$$

THEORETICAL ANALYSIS OF DROPLET ENTRAINMENT IN AN ETC GUN ENVIRONMENT (continued)

- Following the conventional definition, the entrained fraction, E , can be expressed in terms of the superficial velocities of the total liquid (including the liquid film and the entrained droplets) and the liquid film alone, i. e.,

$$E = \frac{j_d}{j_f} = \frac{j_f - j_{ff}}{j_f} = 1 - \frac{j_{ff}}{j_f}$$

- The upper limit of the entrained fraction is given by

$$E_{up} = 1 - \frac{(j_{ff})_c}{j_f}$$

After substituting the expression of $(j_{ff})_c$ into the above equation, E_{up} can be expressed as

$$E_{up} = 1 - \frac{1}{Re_f} \left[11.78 N_\mu^{0.8} \left(\frac{\sigma}{\mu_f j_g} \right) \left(\frac{\rho_f}{\rho_g} \right)^{1/2} \right]^3$$

- Theoretically, the actual entrainment during the mixing of plasma and liquid propellants in an ETC gun should be bounded by the above upper limit and the lower limit given by Ishii and Mishima (1989), i. e.

$$(E)_{IM} < E < E_{up}$$

THEORETICAL ANALYSIS OF DROPLET ENTRAINMENT IN AN ETC GUN ENVIRONMENT (continued)

- From the above equations, a functional form can be postulated for the actual entrained fraction as

$$E = 1 - B Re_f^{-1} N_{\mu}^{2.4} \left(\frac{\sigma}{\mu_f J_g} \right)^3 \left(\frac{\rho_f}{\rho_g} \right)^{3/2}$$

where B is a coefficient that needs to be determined experimentally.

- In view of the fact that the critical superficial velocity of the liquid film represents the lower limit of the liquid film flow, the value of B should be bounded by

$$B \geq 1.635 \times 10^3$$

- In terms of the dimensionless characteristic gas velocity as

$$J_g = j_g \left(\frac{\mu_f}{\sigma \sqrt{\rho_f / \rho_g}} \right)$$

a more general expression for the entrained fraction can be postulated. This is

$$E = 1 - B N_{\mu}^a Re_f^b J_g^c$$

- Based upon the preceding physical arguments, the values of the exponents should be approximately equal to: $a = 2.4$, $b = -1$, and $c = -3$. Experimental data to be obtained in the proposed experiments will be used to obtain a final expression for the entrainment correlation.

ENTRAINED DROPLET SIZE DISTRIBUTION

- In an ETC gun environment, the chemical reactions that are directly responsible for the transfer of chemical energy to propulsive energy are controlled not only by the entrainment rate but also by the entrained droplet size distribution.
- In an ETC gun chamber, the majority of droplets are generated by entrainment and not by secondary breakup mechanisms. Examples of secondary breakup are turbulence eddy-induced breakup and particle/particle collision generated breakup.
- The size distribution should be governed by the process of the droplet entrainment based on shearing off of the roll waves.
- Studies of droplet sizes have been performed by Hinze (1955), Hass (1964), Wicks and Dukler (1966), Cousins and Hewitt (1968), Tatterson et al. (1977), and Kataoka, Ishii, and Mishima (1983).
- A correlation of droplet size distribution, which could be applied to the interior ballistic processes of an ETC gun, was obtained by Kataoka, Ishii, and Mishima (1983).

DROPLET SIZE CORRELATION BY TATTERSON DALLMAN AND HANRATTY (1977)

- An experimental study was performed to measure the entrained droplet size in an annular two-phase flow using a log-normal distribution function to simulate the droplet size distribution:

$$We(d_{vm}) = 0.106 \ Re_g^{1.1} \left(\frac{\mu_g^2}{d_h \sigma \rho_g} \right)^{1/2}$$

where μ_g is the gas viscosity, Re_g the gas Reynolds number, and $We(d_{vm})$ the characteristic Weber number based on the volume median diameter.

- The gas Reynolds number and the characteristic Weber number are defined respectively by

$$Re_g = \frac{\rho_g j_g d_h}{\mu_g} \quad \text{and} \quad We(d_{vm}) = \frac{\rho_g j_g^2 d_{vm}}{\sigma}$$

where d_{vm} is the volume median diameter. Physically, d_{vm} is defined such that droplets having diameters greater than the volume median diameter would occupy exactly half of the total droplet volume in the gas core.

- Major Drawback:

Their assumption of a potential flow is not strictly valid for two-phase annular-mist flow with a highly turbulent gas core. As a result, the correlation of Tatterson et al. does not compare favorably with experimental data over a wide range of gas Reynolds number.

DROPLET SIZE CORRELATION BY KATAOKA ISHII AND MISHIMA (1983)

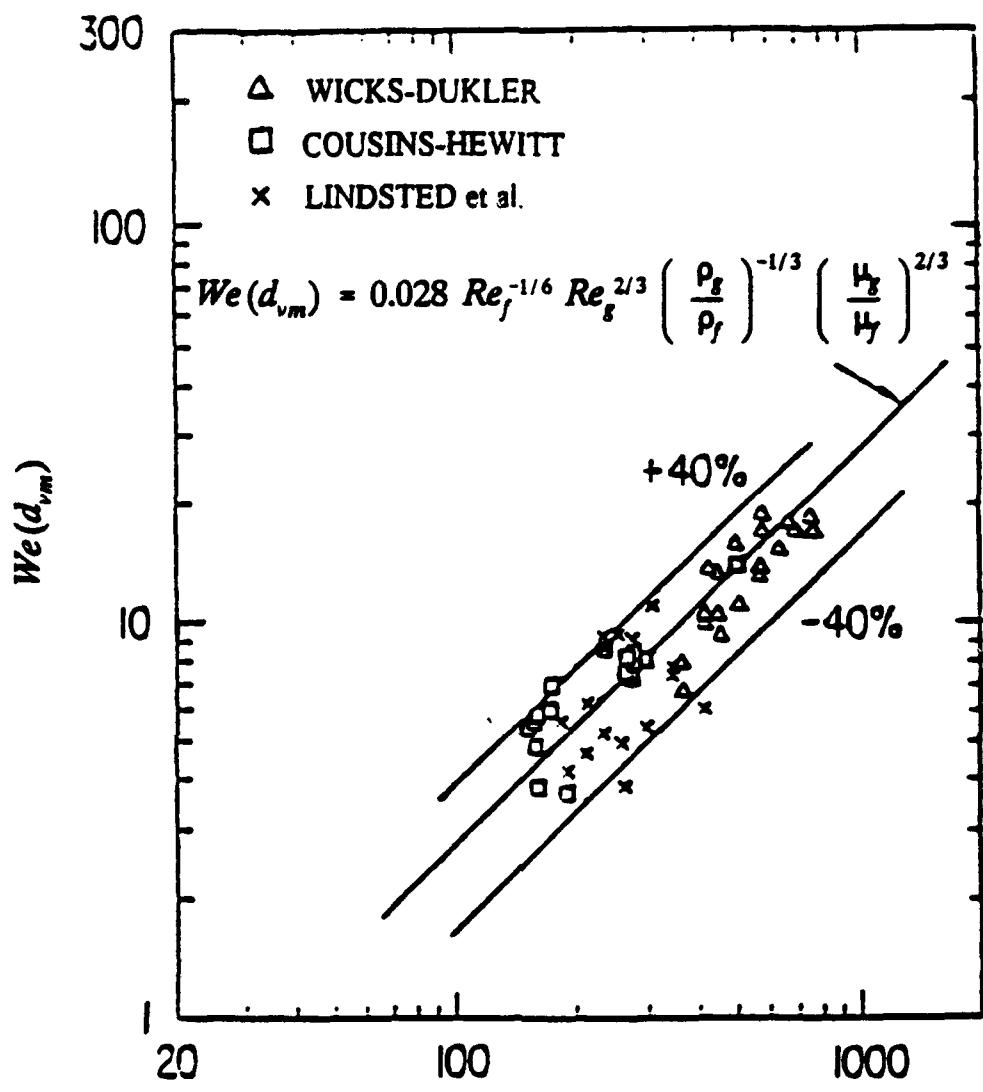
- A mechanistic model was developed that was based on the mechanism of shearing off of the roll-wave crest for generation of liquid droplets by a viscous shear flow. The potential flow assumption employed in the standard Weber number criterion was eliminated in developing the model development.
- By incorporating the mechanistic model with test data, Kataoka, Ishii, and Mishima (1983) successfully derived a correlation for deducing the volume median diameter from the Weber number

$$We(d_{vm}) = 0.028 \ Re_f^{-1/6} Re_g^{2/3} \left(\frac{\rho_g}{\rho_f} \right)^{-1/3} \left(\frac{\mu_g}{\mu_f} \right)^{2/3}$$

- In terms of the characteristic Weber number, the volume median diameter is given by

$$d_{vm} = \frac{\sigma We(d_{vm})}{\rho_g j_g^2}$$

The above expression correlates the experimental data of volume median diameter within $\pm 40\%$ errors.



$$Y = Re_f^{-1/6} Re_g^{2/3} \left(\frac{\rho_g}{\rho_f} \right)^{-1/3} \left(\frac{\mu_g}{\mu_f} \right)^{2/3}$$

Correlation of the Volume Median Diameter by Kataoka, Ishii and Mishima

DROPLET SIZE CORRELATION BY KATAOKA ISHII AND MISHIMA (1983) (continued)

- The mean values of the data on drop size distribution were fitted by Kataoka, Ishii, Mishima (1983) to the upper limit log-normal distribution:

$$\frac{d \Delta}{dy} = - \frac{\xi}{\sqrt{\pi}} \exp[-(\xi y)^2]$$

where Δ is the volume fraction oversize defined as the volume fraction of droplets having a diameter larger than a given diameter, d .

- In the above equation, ξ is a distribution parameter and y is defined in terms of the maximum diameter d_m and volume mean diameter d_{vm} as

$$y = \ln \left[\frac{k d}{(d_m - d)} \right] \quad \text{and} \quad k = \frac{(d_m - d_{vm})}{d_{vm}}$$

- Based upon the experimental results, the values of ξ and k were found to be $\xi = 0.884$ and $k = 2.13$ whereas using the upper limit log-normal distribution, the maximum diameter was related to the volume mean diameter by

$$d_m = 3.13 d_{vm}$$

**DROPLET SIZE CORRELATION BY KATAOKA
ISHII AND MISHIMA (1983)**
(continued)

- The correlation of drop size distribution developed by Kataoka, Ishii, and Mishima (1983) is probably the most suitable one among the existing correlations for use in simulating the phenomena of mixing of plasma and liquid propellants in the ETC gun environment.
- It is recommended that the correlation be used in future modeling. The reasons are:
 - The correlation is based upon a sound physical model, taking full account of key elements involved in the droplet formation process
 - The use of the upper limit log-normal distribution function is evidently appropriate for annular-mist flow
 - The correlation compares very well with available experimental data on drop size distribution covering a wide range of conditions
 - The correlation is easy to use since the primary quantity that needs to be determined is the volume median diameter.

ARL

Electrothermal-Chemical Gun Interior Ballistic Modelling

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APL

Interior Ballistic Component Processes

LPETC	SPETC
Plasma generation: Variety of plasma generation concepts. Not dependent on propellant type. Generates little mass; temperatures 10 - 30,000 K. Coupled to combustion chamber.	Ignition: Little or no ignition delay. No detailed information.
Gas flow and flame spread: Similar to bulk-loaded LPG. Moving to higher ullage charge designs.	Combustion & Mixing: Complex process. Propellant surface area not well defined. Similar to processes in BiLPG. Droplet entrainment & breakup at high shear flows.
Expansion: Anticipate diminishing plasma influence with increasing projectile travel for breech/chamber injected plasmas.	Data suggests plasma does not directly affect SP combustion process in a major way. Impact on gas internal energy & pressure.

Appropriate Dimensionality

- Practical motivation to utilize codes with lowest dimension to obtain desired information

- reduce complexity, decrease run time, decrease post processing
- reduce need for specialized personnel
- 'user friendly' models needed for the larger ballistics community

- Lumped parameter IB codes

- macroscopic parameters such as max pressure & muzzle velocity
- mean IB history
- ETC applications currently require empiricism, especially for liquids

- quasi 1D, multi-phase, IB codes

- axial structure of flame spreading
- energy, mass & momentum of plasma at various axial locations
- details of multi-phase flow
- investigate sources of longitudinal pressure waves

- 2D / 3D, multi-phase IB codes

- radial structure of flame spreading
- influence of turbulence
- radial structure of plasma in combustion chamber
- investigate sources of radial, tangential & longitudinal pressure waves
- detailed interaction of multiple plasma sources
- influence of complex geometries

Dimensionality for IB Simulations

	Plasma	LPETC	SPETC
0D (Lumped parameter)	Not generally utilized. Models available. Require specification of mass generation rate. e.g. as function of injected plasma energy. Closely coupled to experiment. Both 0D & 1D models can be used to simulate experiment, but predictive capability is limited.	 Adaptations of existing IB models. Reasonable agreement with experiment using traditional assumptions at modest electrical energy densities & breach plasma capillaries.	 Adaptations of existing IB models available. Reasonable agreement with experiment. Design of plasma generator (e.g. internal, burst tube,) may have large effect; currently not explicitly modeled.
1D	 Ideal & nonideal, quasi-steady & transient models provide good agreement with macroscopic measurables. Has been coupled to 2D/3D IB model.		 Initial efforts to develop multi-phase, CFD, solid propellant IB models.
2D/3D			 IB process appears to be at least 2D. Macroscopic agreement good. Microscopically complex. Research in turbulence submodels. Uniqueness?



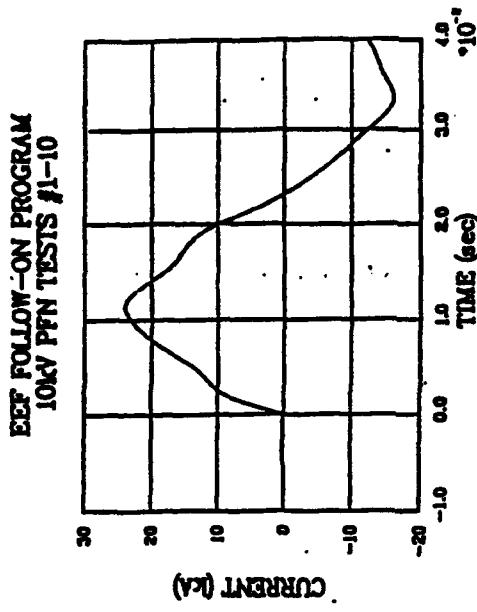
ETC iB Models

Model	Description	Status
P2SIM	0D, power systems for electric guns, includes mission scenarios	Complete
Plasma	1D steady state capillary 1D transient capillary - treats metals (In Progress) 1D piccolo tube 2D capillary	Complete Complete In Progress In Progress (SNL)
BLAKE-ETC	Thermochemical code, treats electrical energy as a constituent	Complete
IBHVG2 -ETC	0D, EE source term Input power - coupled to plasma (In Progress)	Complete
SPETC	0D, SP, Determines power pulse for given performance - optimization (In Progress)	Complete
LUMPET	0D, LP, Arrhenius EOS EE source term	Complete
Compress	0D, Constant pressure solution, EE source term	Complete
XKTC-ETC	1D, Solid propellant code, EE source term	Complete
CRAFT	1D/2D/3D research code, fundamental physics, state-of-the-art numerics - gas/gas (Complete) - gas/liquid (Complete) - gas/liquid/solid (In Progress).	In Progress

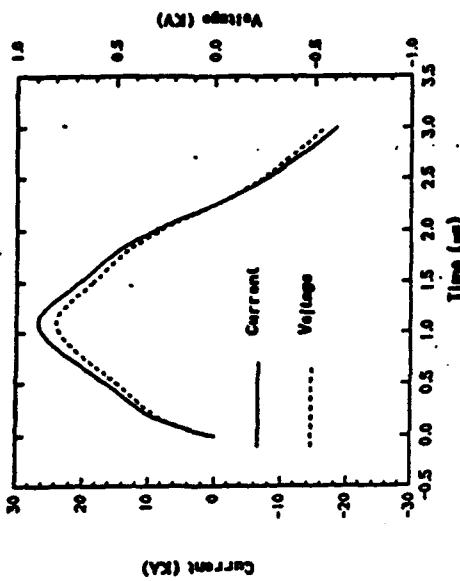
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Power Model

- Virtually all electric gun power systems
- Includes mission scenarios
- Developed by PCRL
- Application by P. Tran



P2SIM PREDICTION



FMC Pulse-Power Module
for 9MJ ET Skid Gun:
Verification Test 1

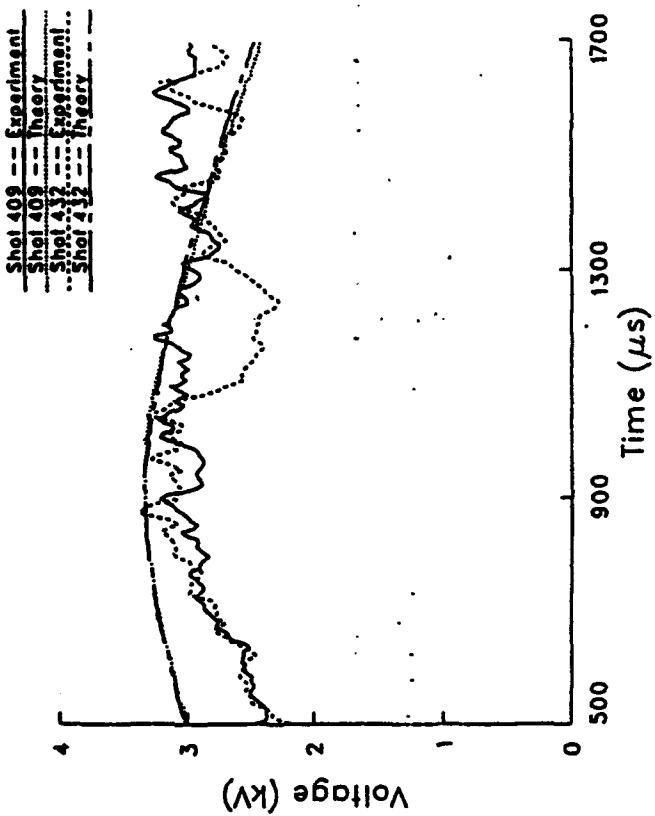
Plasma Models

- Past Accomplishments:

- Develop 1D, steady-state, capillary model for breech-fed mixing chamber
- Included nonideal effects for relatively high-density, low-temperature plasmas
- Extended solution to 1D, fully transient case
- Effectuated comparison with various sets of experimental data

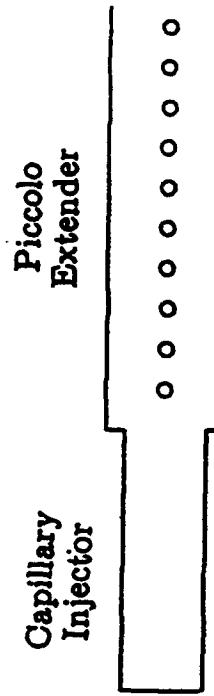
- Present Activities:

- Develop capability for treating mixture of several different species
- Account for electrode ablation
- Account for fuse vaporization
- Extend model to treat "piccolo" Injector
- Couple plasma model to 2D, Interior Ballistic, CFD models



Status of Plasma Activities

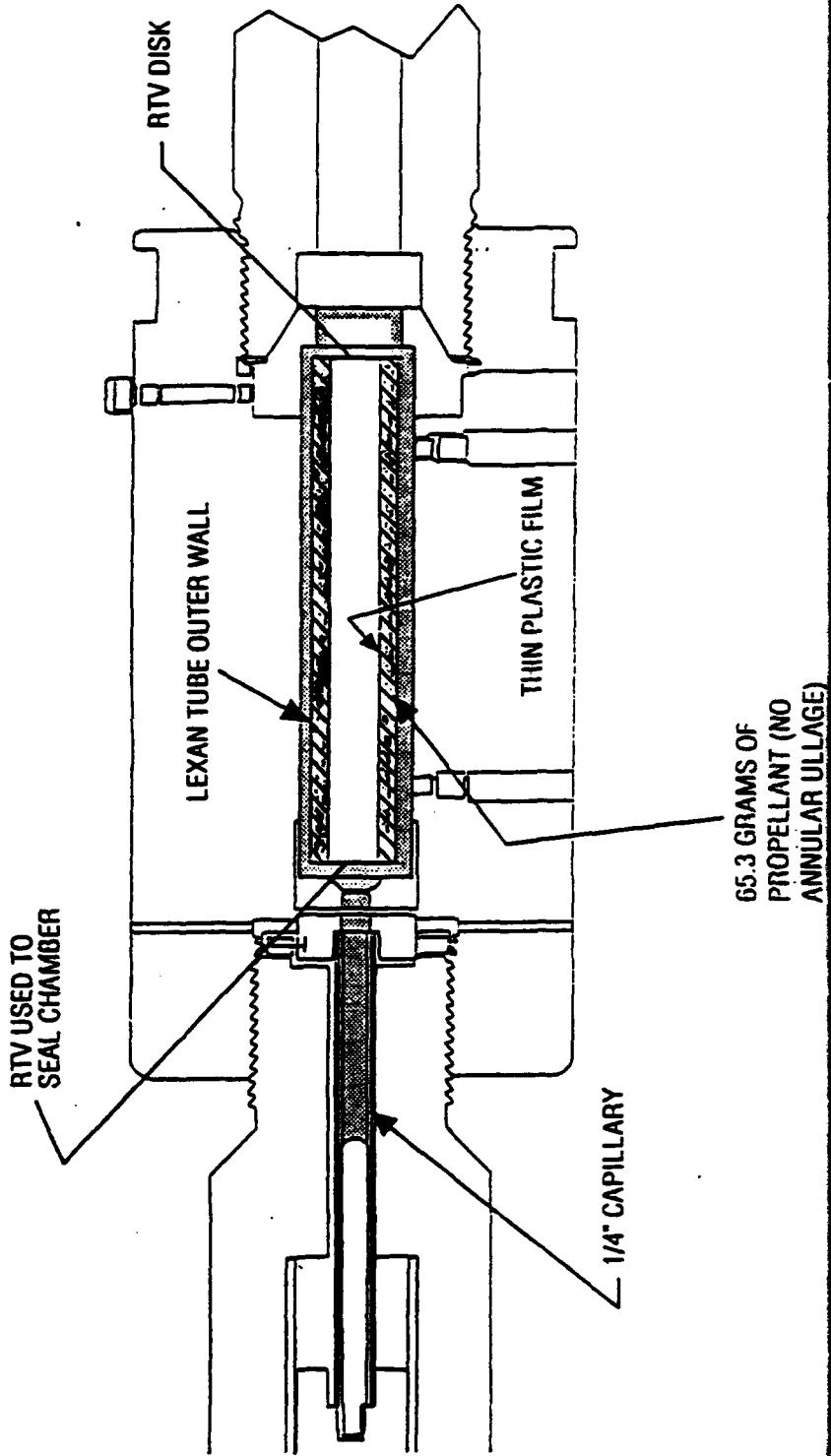
- Piccolo
 - Developed 1D, transient model for piccolo extension to breech-fed injector
 - Performing calculations to compare with FMC experimental data
- Coupling to CFD models
 - Isothermal, steady-state, breech-fed plasma code included in CRAFFT
 - Coupled calculations performed for FMC and GDLS data
- Mixtures
 - Formulated equations for calculating EOS's and conductivity for arbitrary mixture of C, H, Cu, Al, Fe, O, and N
 - Developed stand-alone code and subroutine for performing calculations
 - Initiated calculations for breech-fed injector accounting for vaporization of Al fuse



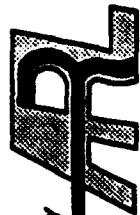
Experimental Fixture

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Bore diameter: 30mm
Chamber volume: 160 cc
Chamber diameter: 3.175 cm
Chamber L/D: 6.15
Travel: 16.1 cm
Projectile mass: 328.8 g

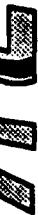


Ignition Characteristics



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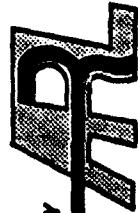
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- Ignition time delays close for same material (Average 0.35 ms)
- Plasma driven propellants appear to exhibit reduced variability in ignition

Shot	Propellant	Ignition delay	Shot	Propellant	Ignition delay
1	LGP1846	0.36	17	RDX/NC/NG	0.30
2	<u>LGP1846</u>	<u>0.24</u>	19	RDX/NC/NG	0.33
3	LGP1846	0.28	22	AN/Cyanoguanidine	1.68
4	LGP1846	0.24	23	AN/MEAN/H2O	0.27
5	LGP1846	0.20	24	AN/MEAN/H2O	0.30
6	LGP1846	0.17	25	AN/5AT/H2O	0.94
8	N2H4/IHN	0.28	26	AN/5AT/H2O	0.82
9	HAN/DEG/H2O	0.26	27	JA2	0.24
10	HAN/DEG/H2O	0.30	28	JA2	0.30
11	HAN/DEG/H2O	0.29	29	JA2 - X	0.23
12	HAN/NMP/H2O	0.26	30	JA2 - X	0.30
13	HAN/NMP/H2O	0.32	31	JA2	0.27
14	M43	0.24	32	JA2	0.27
15	M43	0.24	33	Compacted CAB	0.87
16	DINA/NC	0.23	34	Compacted CAB	0.12
20	DINA/NC	0.25	35	Loose CAB	0.23
			36	Loose CAB	0.20
			37	Loose CAB	0.16
			38	Loose CAB	0.16

Pressurization Rate



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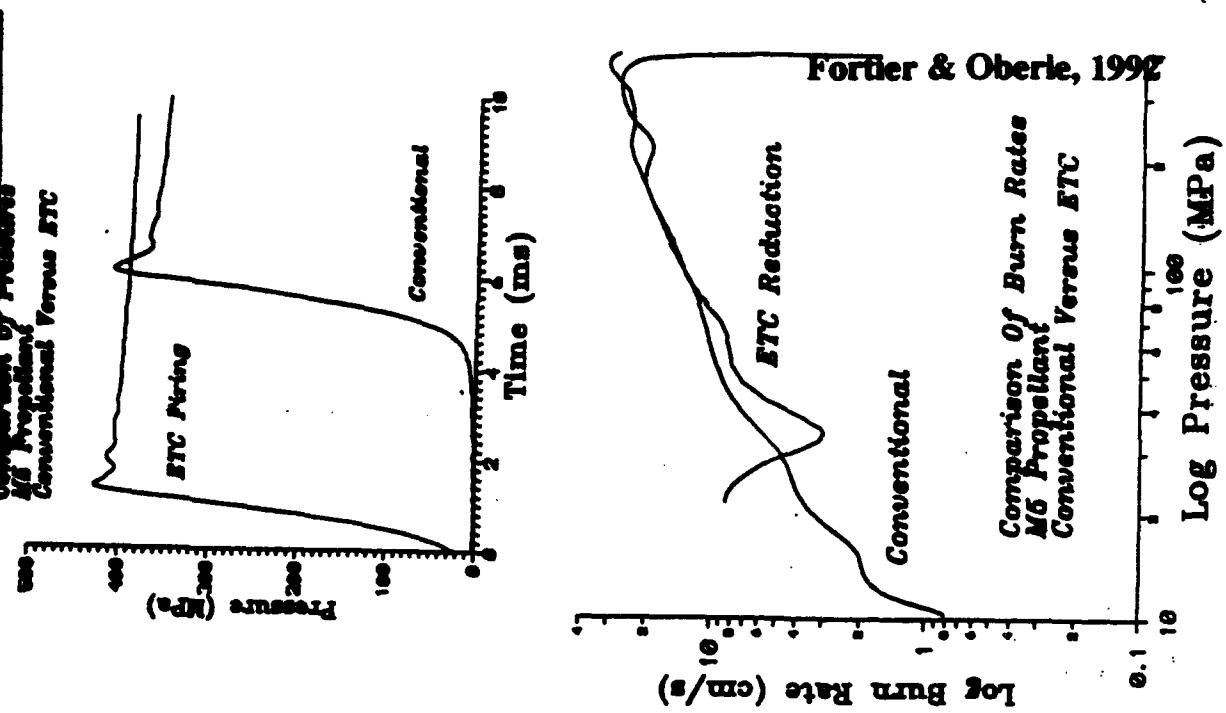
- 'Runaway' combustion does not occur
- 120mm tank round: $dP/dt = 0.4 \text{ MPa/s}$
- 155mm artillery round: $dP/dt = 0.09 \text{ MPa/s}$

Shot	Propellant	Derivative (MPa/s)	Shot	Propellant	Derivative (MPa/s)
1	LGP1846	3.820	17	RDX/NC/NG	0.129
2	LGP1846	3.670	19	RDX/NC/NG	0.123
3	LGP1846	0.134	22	AN/Cyanoguanidine	0.113
4	LGP1846	0.084	23	AN/MEAN/H ₂ O	0.150
5	LGP1846	0.327	24	AN/MEAN/H ₂ O	0.180
6	LGP1846	0.121	25	AN/5AT/H ₂ O	0.338
8	N2H4/HN	0.151	26	AN/5AT/H ₂ O	0.272
9	HAN/DEG/H ₂ O	0.124	27	JA2	0.198
10	HAN/DEG/H ₂ O	0.133	28	JA2	0.186
11	HAN/DEG/H ₂ O	0.119	29	JA2 - X	0.161
12	HAN/NMP/H ₂ O	0.122	30	JA2 - X	0.183
13	HAN/NMP/H ₂ O	0.137	31	JA2	0.179
14	M43	0.117	32	JA2	0.172
15	M43	0.136	33	Compacted CAB	0.075
16	DINA/NC	0.108	34	Compacted CAB	0.218
20	DINA/NC	0.153	35	Loose CAB	0.119
36	Loose CAB		37	Loose CAB	0.112
38	Loose CAB		38	Loose CAB	0.228

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Closed Chamber Burn Rate

- Research at ARL in SP combustion with plasma
 - ETC diagnostic closed chamber/gun fixture
 - Specialized ETC closed chamber data analysis code
- M5 solid propellant with conventional ignition vs plasma augmented
 - 50 cc closed chamber data
 - Plasma pulse 1.2 ms, 125 kJ
 - Analyzed using BRILCB
- Prompt ignition with plasma
 - In closed chamber plasma does not appear to influence burn rate of SP

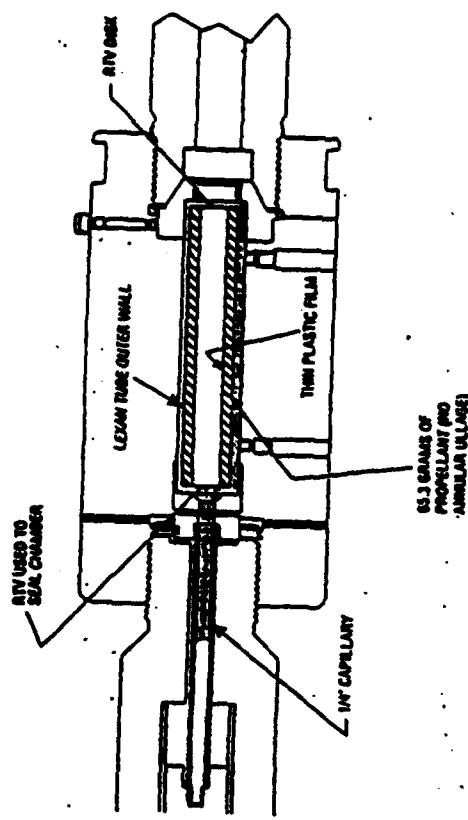


A4

Experiment OCB14

- 30mm fixture

- Chamber volume: 160 cc
- Propellant mass: 65.3 g
- Chamber diameter: 3.175 cm
- Chamber L/D: 6.15
- Travel: 161 cm
- Projectile mass: 324.36 g



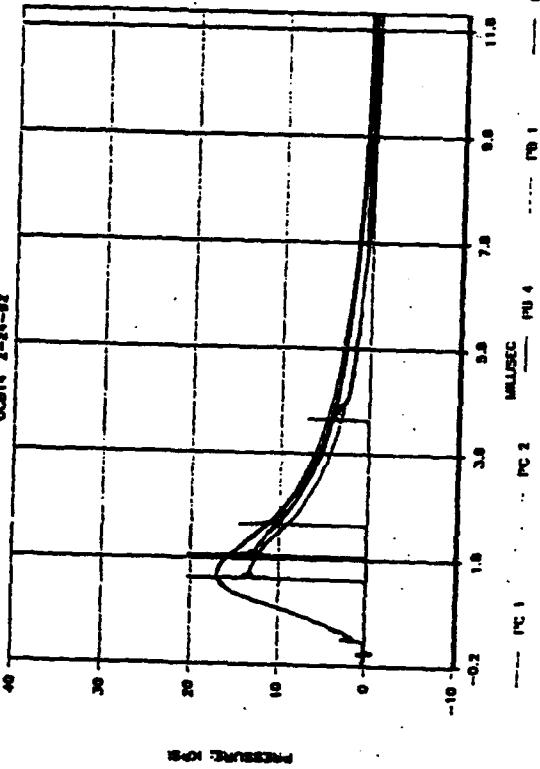
- M43 solid propellant

- Number of perfs: 7
- Outer diameter 0.2895 cm
- Diameter perf: 0.0119
- Grain length: 0.6197 cm

- Central ullage tube

- Electrical energy

- Ramped pulse over 1.9 ms
- $41.167 \mu J$



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M43 Burn Rate with Plasma

- Closed chamber data at ARL

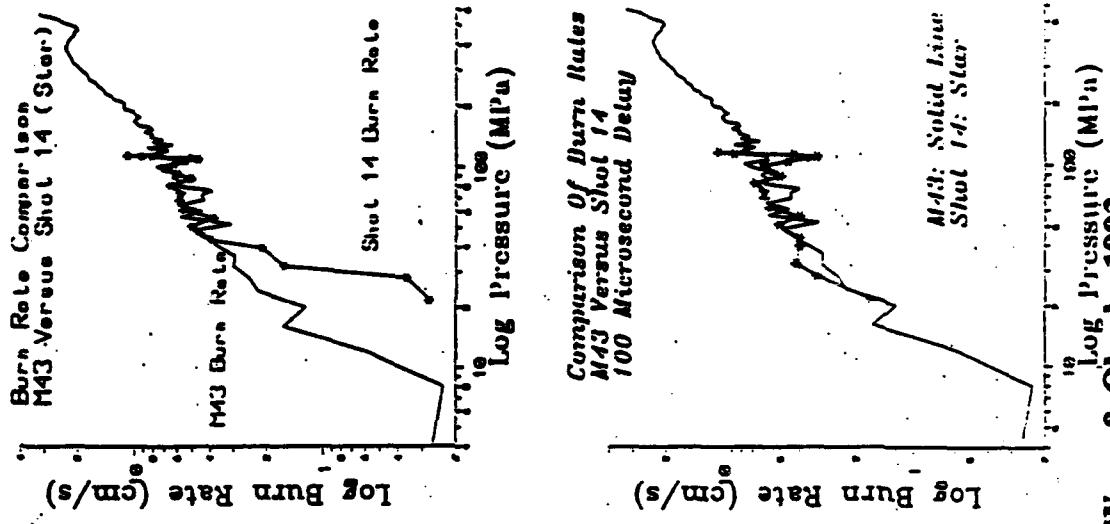
- M43, lot IH91H-E00040
- analyzed using BRLCB

- Inverse code results

- use experimental data to obtain mass burned history
- use m dot & grain geometry to deduce burn rate using modified BRLCB

- Delay in plasma

- current & voltage measured at rear of capillary
- assume 0.0 and 100 microsecond delay in energy release in combustion chamber



Wren & Oberle, 1993



■ Shots 160 and 161 from Soreq

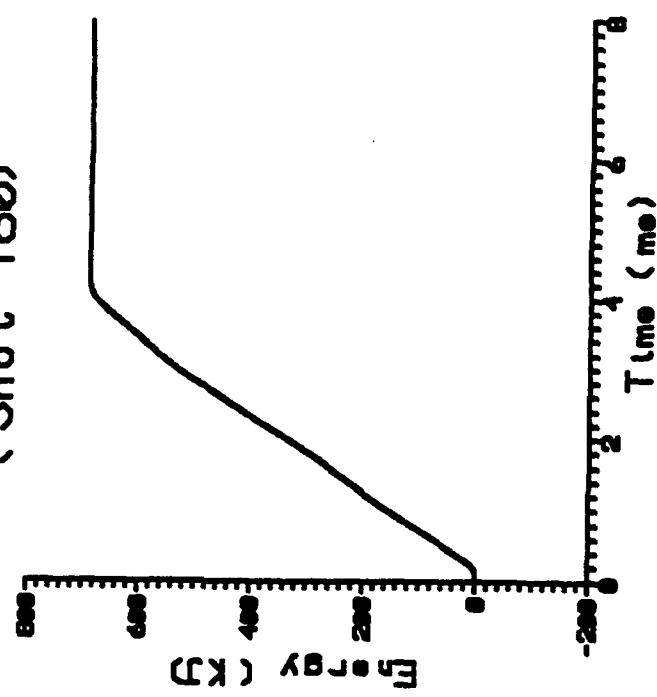
Input parameters:

- Bore diameter: 60-mm
- Travel: 3.881 m
- Chamber volume: 2183 cc
- Charge weight: 1.73 Kg
- Propellant: M30, 7perf
- Projectile mass: 1.35 Kg

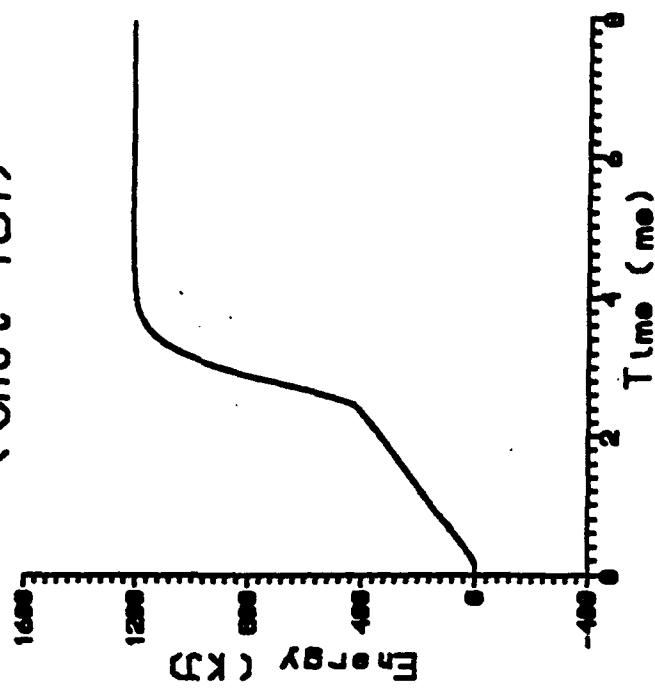
Energy vs Time

ANL

Energy vs Time
(Shot 160)



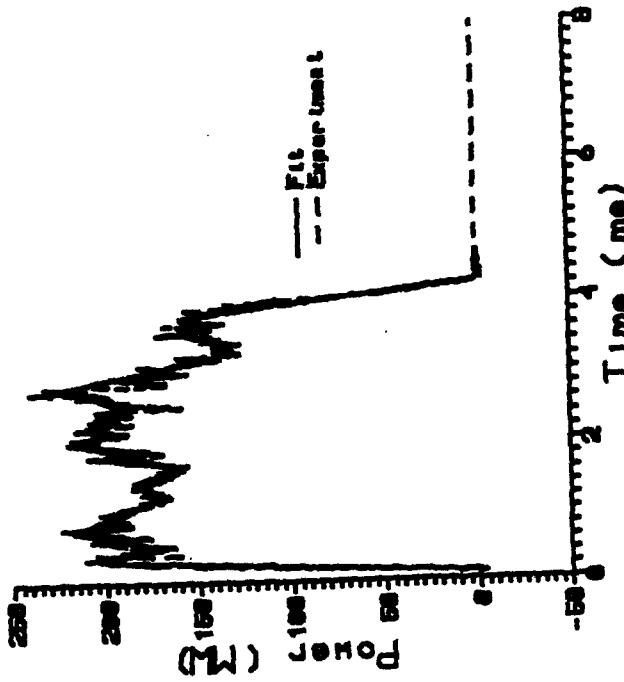
Energy vs Time
(Shot 161)



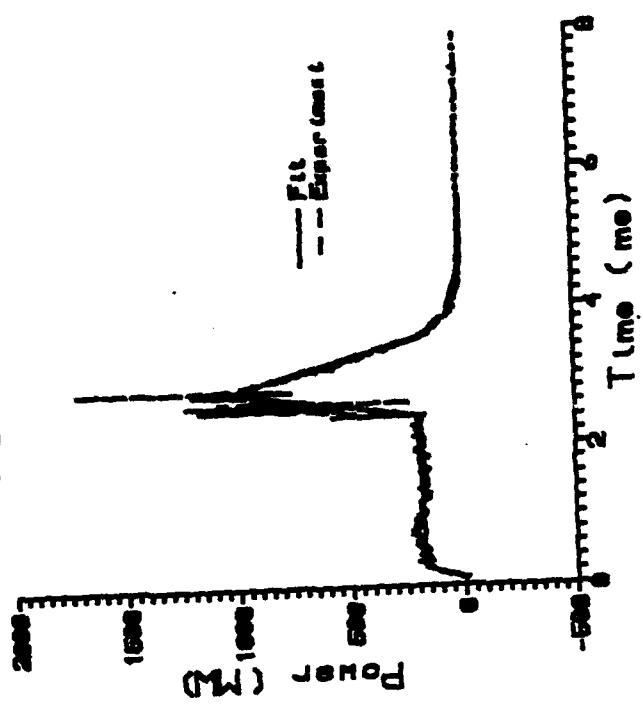
Power vs Time

AB

Power vs Time
(Shot 160)

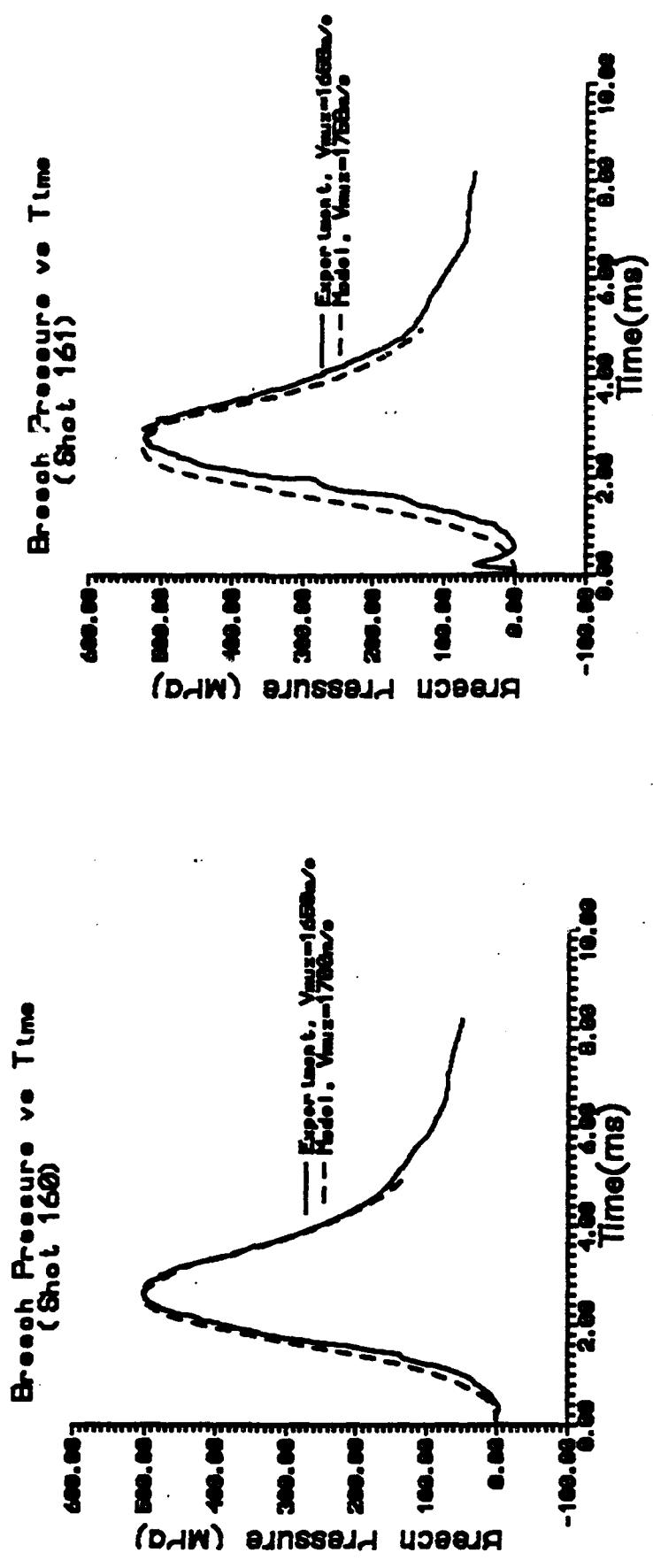


Power vs Time
(Shot 161)

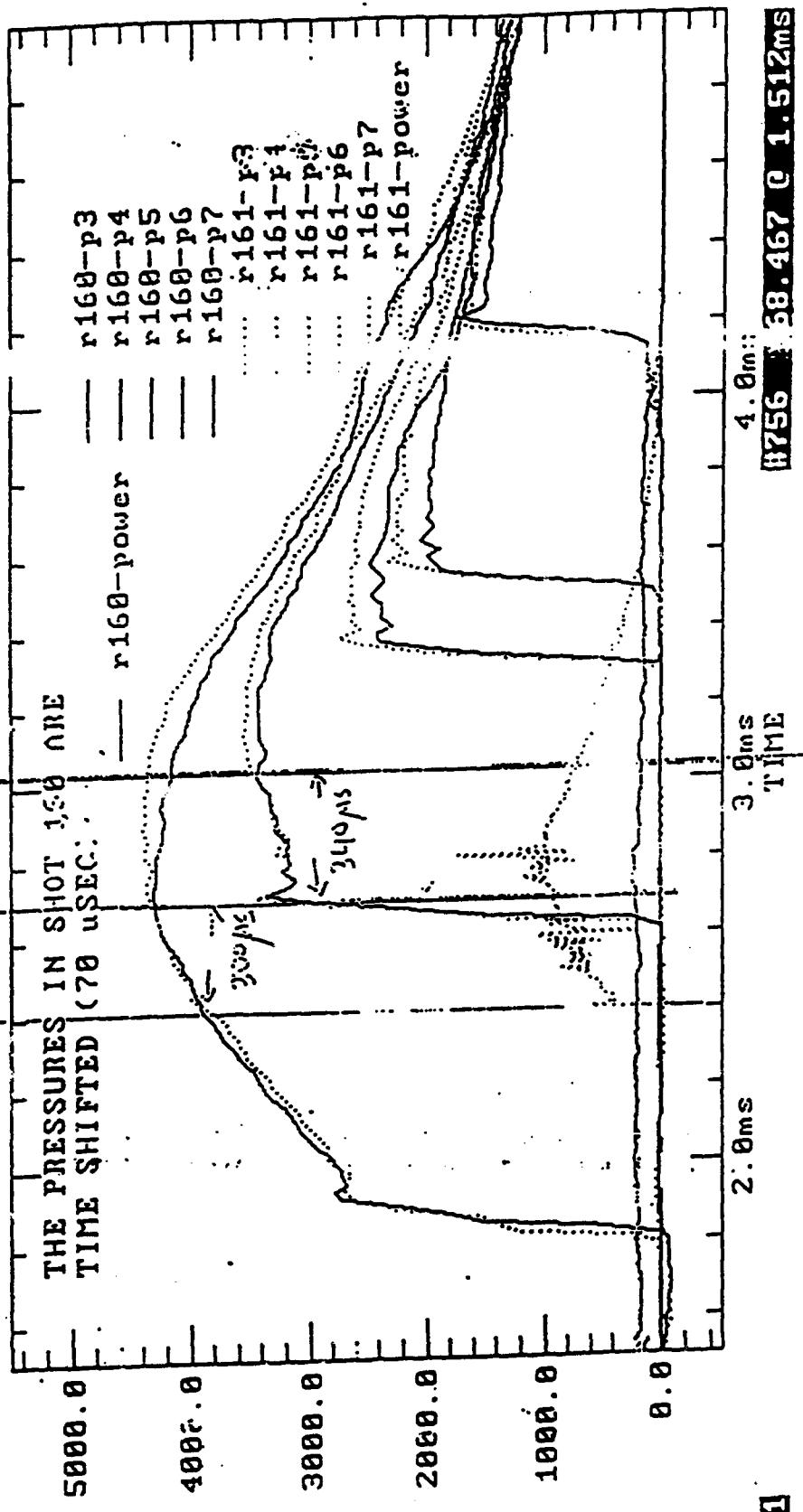


R

Pressure vs Time



injection influence time
 influence time on P_3
 influence time on P_4



241

Set 1

$$\begin{aligned}
 P_3 &\rightarrow x = 50.7 \text{ cm} \\
 P_4 &\rightarrow x = 90.7 \text{ cm}
 \end{aligned}$$

$$\begin{aligned}
 V_1 &= 164 \text{ m/s} \\
 V_2 &= 1176 \text{ m/s}
 \end{aligned}$$

#756 38.467 0 1.512ms

APL

Simulation of OCB14

- XNOVAKTC-ETC, 1D SP IB model (Gough)
 - uniform rupture of moderator tube at 0.3 ms based on pressure rise at combustion chamber gage
 - uniform ignition of propellant
 - plasma source term based on experiment
 - 100 microsecond delay in plasma energy

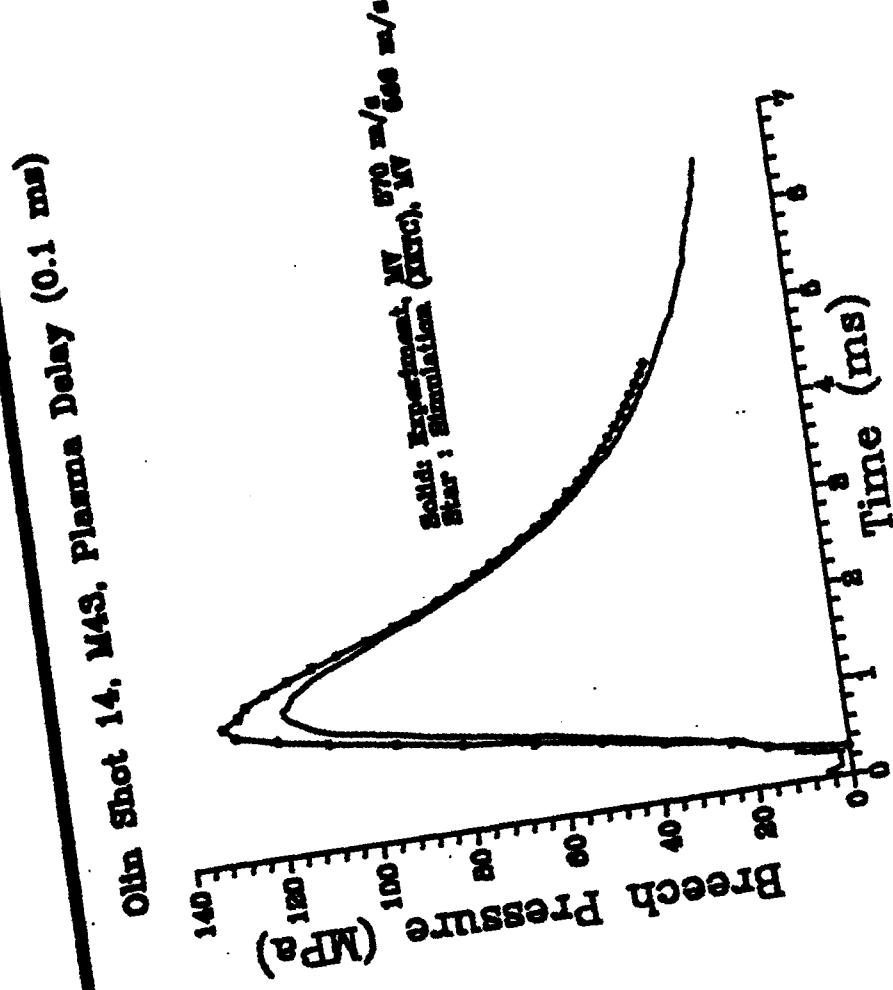
- Comparison

	Pmax	MV	Consumed mass
Experiment	117 MPa	570 m/s	35.36 g (inverse)
Simulation	131 MPa	569 m/s	33.93 g (XKTC)

(initial charge: 65.3 g M43 propellant)

RL

Simulation of CCB14



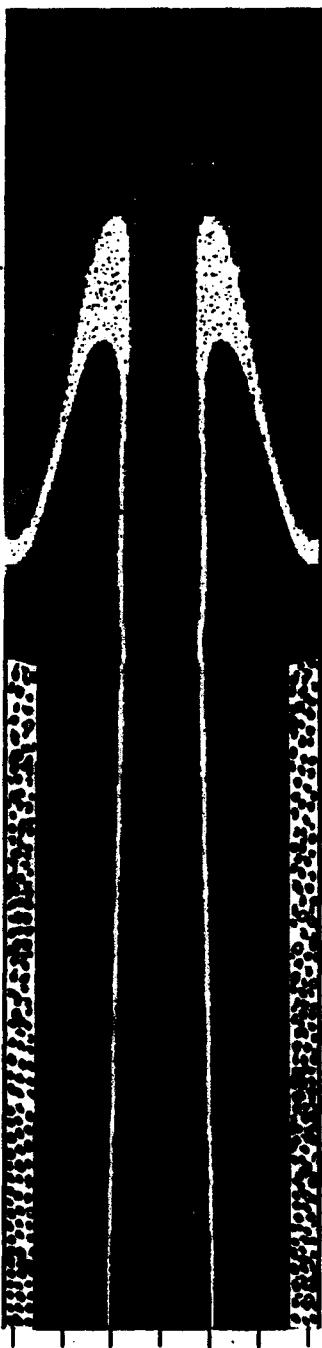
243

- Unknowns
 - 20 MPa)
 - M43 burn rate data at low pressure
 - effect on bed rheology
 - rupture of ullage tube & effect on flame spreading
 - effect of plasma on flame
 - response of projectile to ullage tube pressurization

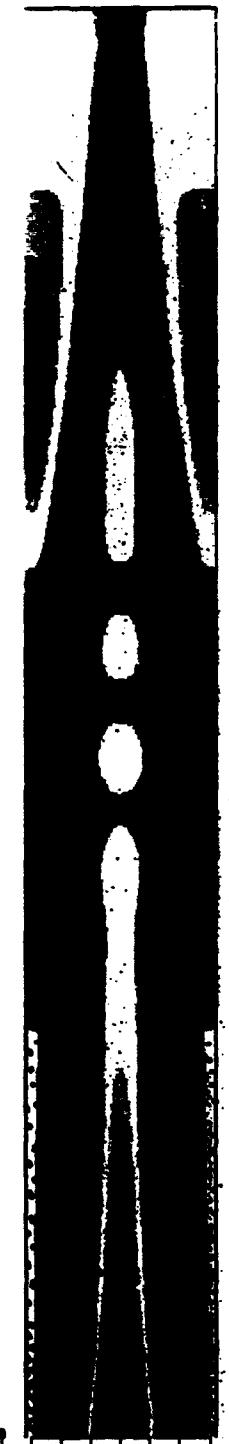
APL

Radial Structure of Temperature

**"LOG TEMPERATURE LEVELS AT 1.085 ms"
"SP ETC SHOT 45"**



**"LOG TEMPERATURE LEVELS AT 1.465 ms"
"SP ETC SHOT 45"**

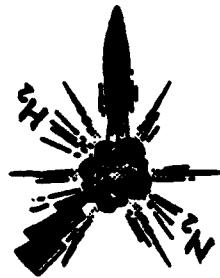


APL

Summary

- ETC gun models integral to research efforts
- Goal: predictive end-to-end models (appropriate dimensionality)
 - dependent on physical process of interest
 - 0D, 1D, 2D, 3D models pertinent
- Burn rate of solid propellant does not appear changed under influence of plasma at electrical energy densities investigated (<1.0 kJ/g)
- Status of 1B models
 - 0D models adequately capture macroscopic measurements & can be used for scoping studies
 - 1D models appear to be adequate if plasma components can be sufficiently modeled; useful for study of longitudinal phenomena such as pressure waves
 - 2D/3D models under active development; required to capture radial structure which is necessary for detailed cartridge design

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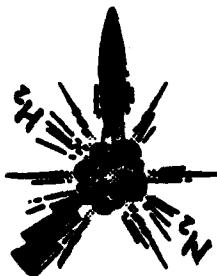


ARL ETC MODELING WORKSHOP

OLIN IRAD EFFORTS
RELATED TO ETC MODELING

H. McElroy, K. Linde

12 - 13 MAY, 1993

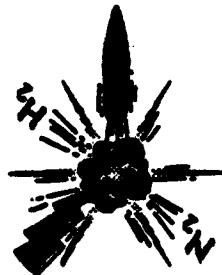


ACKNOWLEDGMENTS

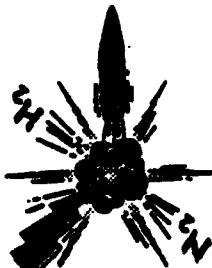
Many Government, GT-Devices and other personnel have been of significant assistance in conducting the efforts described to date. We hope that the cooperative efforts outlined and planned for the future will also be supported as in the past.

In particular, G. Keller, P. Conroy, B. Oberle, G. Wren and N. Winsor contributed significantly to all phases and efforts.

TOPICS



- Why Model - At Olin
- What we model now (routinely)
 - Equilibrium Thermochemistry
 - Simple Optimum Systems Upper Limit Bounds
 - Lumped Parameter or 0-D IB Models
- What we perceive as necessary for the future
- Challenges and Conclusions



WHY MODEL - AT OLIN

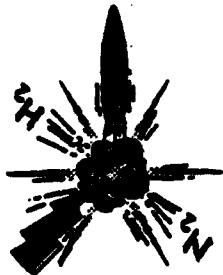
- Scoping new products/processes
- Quality Control
- Developing understanding of product capabilities & Limits
- Unraveling experimental data
- Preliminary safety & charge design
- Charge design verification studies
- Incident Analysis



WHAT WE MODEL ROUTINELY AT

OLIN

- Equilibrium thermochemistry (Blake & MCVECP aka Hunter) with ET-C extensions
- CONPRESS - or constant chamber pressure model
- *HUNT-CON - a combined equilibrium thermochem code with CONPRESS (hunter + compress) and ET-C Extensions

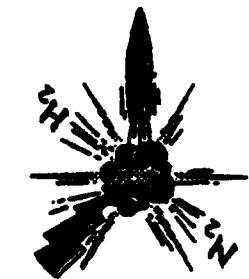
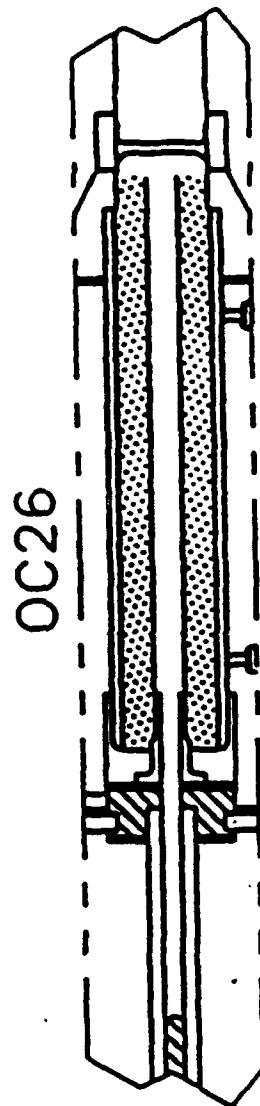


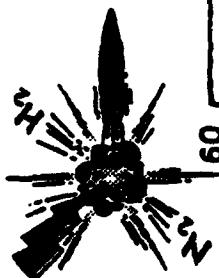
LUMPED PARAMETER Ø-D IIB Code - IBHVG2.504G6

• Propellant Form Function Extensions

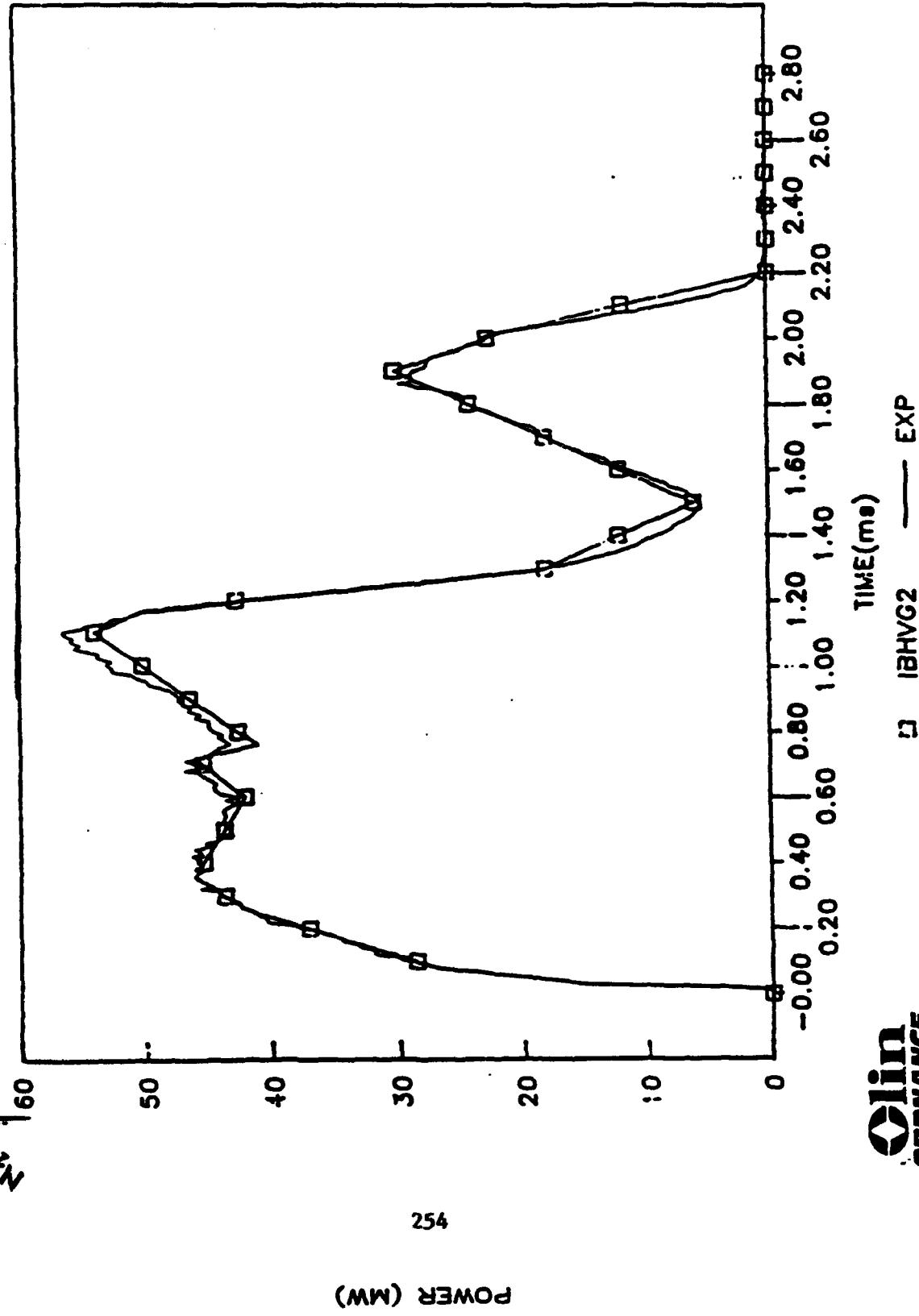
- Inside Burner Single Perf Outside Inhib Grain
- 15 point deterrent function/layer model
- 10 propellant bins
- Cased telescoped system
- Cigarette burn - attached to chamber
- ET-C Functionality - added by GT-Devices
- English to metric and vice versa input/output capability - added by D. Chiu ARDEC - Preserves extensive .400 series data bases.

LOADING GEOMETRY





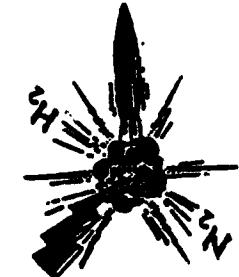
30mm Olin EXP DATA VS CODE RESULTS
OC 26-PCI



254

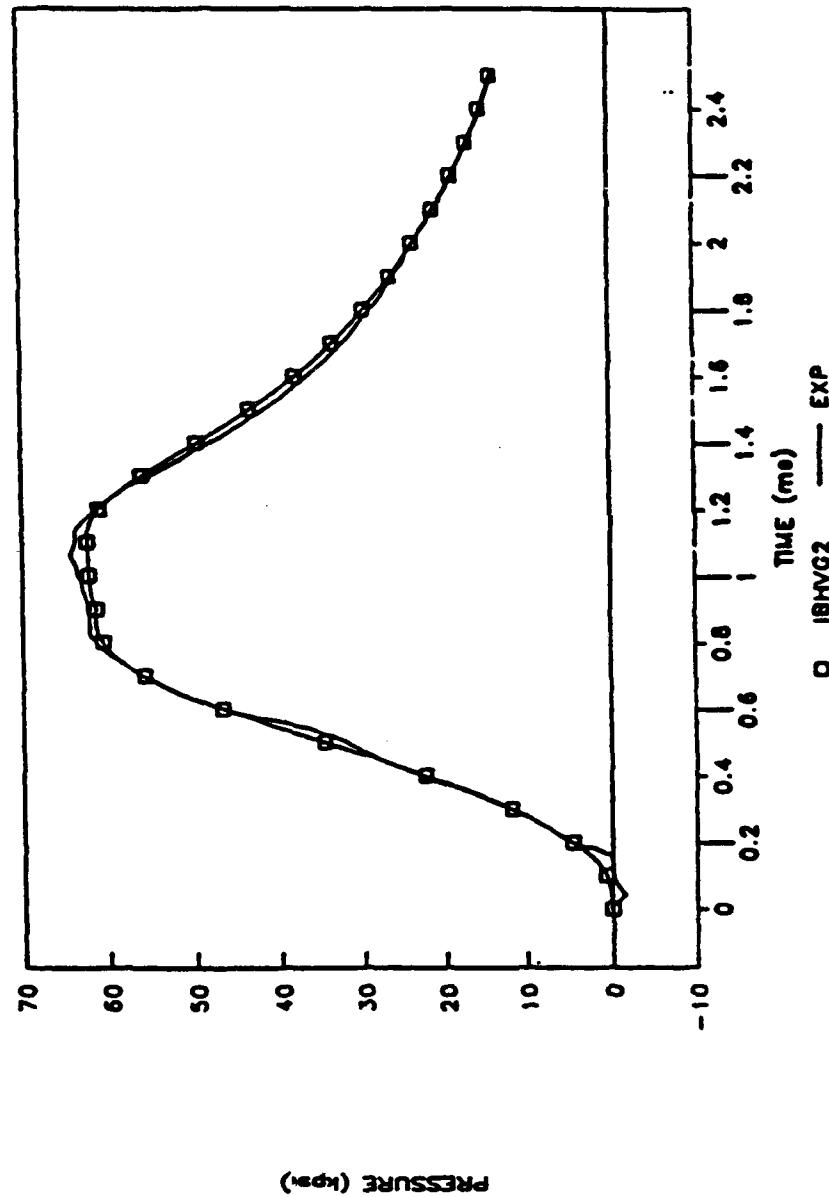
Olin
ORDNANCE

THIS DOCUMENT CONTAINS OLIN CORPORATION COMPETITION-SENSITIVE MATERIAL

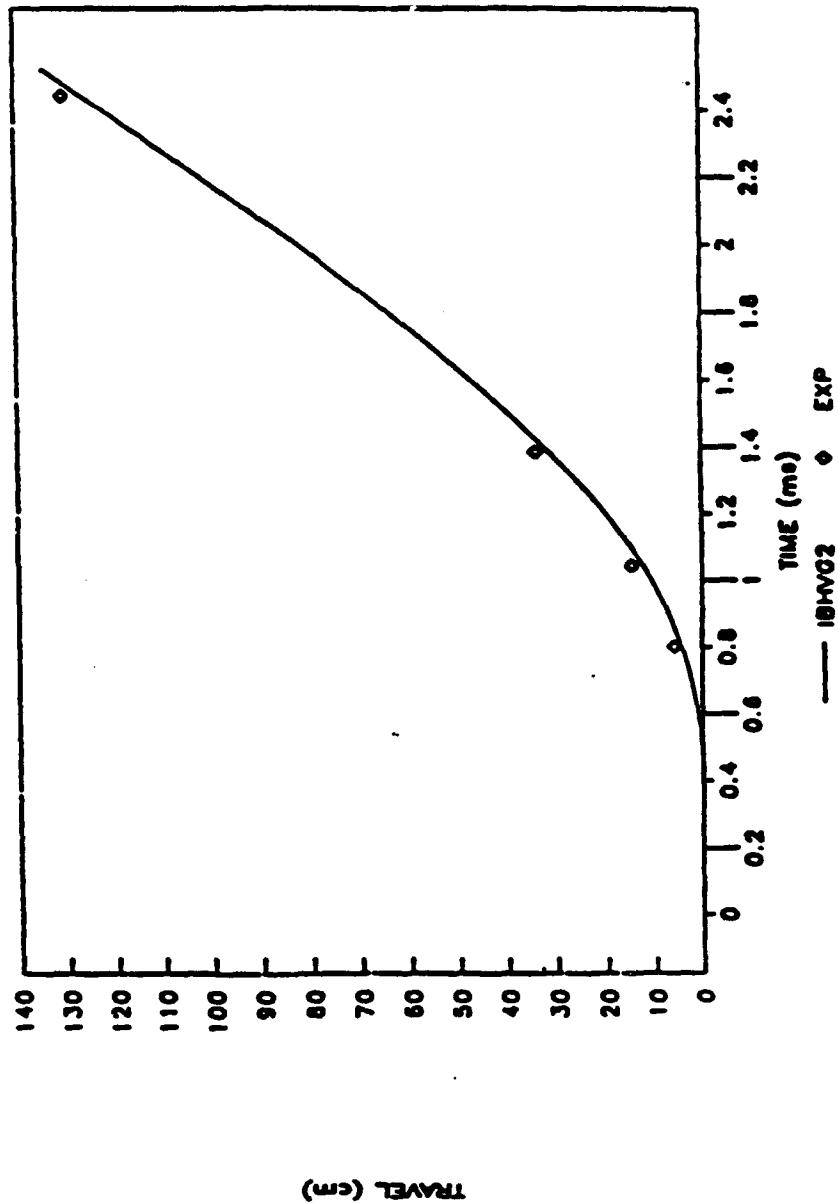


30mm OLIN EXP. DATA vs. CODE RESULTS

OC26 PCI

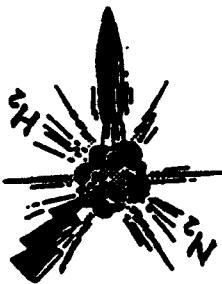


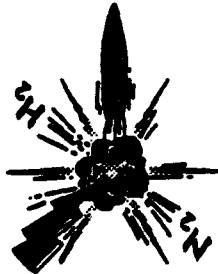
CODE AND EXP. PROJECTILE TRAVEL



THIS DOCUMENT CONTAINS OLIN CORPORATION COMPETITION-SENSITIVE MATERIAL.

Olin
ORDNANCE

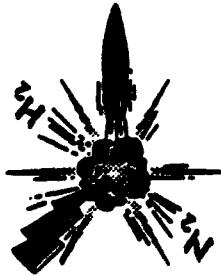




1-D XNOVAKTC (modified)

Beta Version
10426.+

- Modified input routines to accept extended IBHVG2.504 input decks - or old style card image input if you don't want to change.
- Added those extensions which we added to IBHVG2.504G6 which were not already in XNOVAKTC. (e.g. Pan Cake Function).
- Corrected minor chemistry bug in layer properties - they defaulted to all being the same and increased points to 15.
- Release to GT-Devices for input of ET-C functionality - End of May.



SAMPLE DUAL INPUT DECK

30mm Subscale Artillery for Shot EF044

Combined IBHVG2.504G6 & XNOVAKTC extensions

(E)

\$COMM This run converted to XNOVAKTC 3/19/93 FRL
NO885.IN !! Commented out at stuff.
30mm SUBSCALE ARTILLERY REVERSE ENGINEERING FOR EF044
USING ADJUSTED 4TH LAYER TRANSITION
ADJUSTING RATIO OF LARGE TO SMALL GRAIN SIZES TO DEMONSTRATE
PROCESS CONTROL

\$INFO

RUN = 30mm ARTILLERY RESULTS

\$XCONTROL \$M2 CONTROL DATA

NPRINT = 1 NGRAPH = 0
NDISK = 0 DEKRD = 0
IBTABL = 1 NFLAM = 1
NPTABL = 1 NEROS = 0
NDYN = 0 NHTW = 1
NBC = 0,0
\$ NRES(1)= 0 NRES(2) = 0 \$not used
LDBED = 1 \$ 0 = PROP BED INITIALLY UNCOMPACTED, 1=COMPACTED
JHTW = 0 \$1
LYER = 0 \$IBRES = 1 moved to resi
NTC = 0
\$ INHIB = 0,0,0 NO LONGER NEEDED
NXCW = 0
NBLOWN = 0
NSWSOL = 0
KMODE = 0
MODET = 0 \$ 1 = TANK GUN allows modeling of center hole in prop
NECHO = 0
INBCX = 0

\$XINTEGRA \$M3 INTEGRATION PARAMETERS

NDIM = 15 \$40 \$20 \$ 10 \$20
DTPRT = 0
NSTEP = 100 TSTOP = 0.02 \$0.0002 \$.0200
NDTST = 0 ZSTOP = \$0.184
NSTOP = 3500 TINT = 0.0002
NUNIN = 0 SAFE = 1.1 \$3 \$1.1
NUNOUT = 0 CRIT = 0.2
RZOLV = 0.05 \$0.1 \$0.05
TABLIB = 0.0002
TABLP = 0.0001

\$XFILECNT \$M4 FILE COUNTERS

NSTA = 4 moved to GUN \$NUMBER OF TUBE DIAMETER STATIONS
NTEM = 0 NEL = 0
NEPS = 0,0,0
NZPT = 3 \$ MOVED TO RESI DECK
MORE = 0,0,0
NBL = 0

\$GUN

NAME	= '30MM SMOOTHBORE'	\$	CHAM	= 10.0384
\$ GRVE	= 1.1811		LAND	= 1.1811
\$ G/L	= 1.0000		TWST	= 99999.9
\$ TRAV	= 53.7008		CLEN	= 7.8740
NGAG	= 5	GLOC	= -0.0929, -2.0079, 2.4016, 25.2362, 51.+173	
NSTA	= 4	\$NUM of Stations in tube profile		
ZA	= 0.0, 7.95, 8.05, 30.184			
GUNDIA = 1.26, 1.26, 1.1811, 1.1811 \$ or use RA (radius)				
TWST = 99999 & RIF = 6.0 or use TWST (TWST=360/RIF) Is this right????				

\$RESI T012 BORE RESISTANCE - ERI = DIST. BR = PRESSURE

IBRES = 1 \$LINEAR RESISTANCE . 2=BASED ON VELOCITY
 * if TRAV or BRZ start with 0.0, the rest of the values are relative
 * to initial proj. location. if > 0.0 all is relative to breach

\$ AIR = 1
 NPTS = ~
 TRAV = 0.0, 0.5169, 0.6169, 53.7008
 PRES = 0.0, 1200.0, 100.00, 50.0018

3PROJ \$M13 PROJECTILE AND RIFLING CHARACTERISTICS
 ZBPR = 8.05 \$7.85 \$8.05 \$9.856
 PRWT = 0.725 \$ WTPR or PRWT or WT
 PRIN = 0.14 \$=POLAR MOM OF INERTIA --LBM-IN**2
 \$RIF = 6.0 moved to \$GUN

3XAMBGS \$M5 AMB GAS PROPS
 TEMST = 530 PST = 14.7
 GMST = 29 GAMST = 1.4

3XPROPBED \$M6 PROPELLANT BED GENERAL PROPS
 \$ can use either: TEMPB , or TEMPF, or, TEMPc
 TEMPc = 21.0

3PRIM \$C8 IGNITER THERMOCHEMISTRY
 NAME = 'LX CAPILLARY' \$ CHWT = .22046E-03
 GAMA = 1.1100 COV = 22.9743
 TEMP = 300.00 FORC = 33455.3
 * EIG = 630300. or if FORC is used it will be used internally.
 * to calculate EIG = (FORC*12.00) * (GAMA-1.00)
 GMIG = 36.13
 * NOTE: Following is a guess and may not match IBHVG
 JJ = 3 \$NUMBER OF TIMES
 II = 3 \$NUMBER OF POSITIONS (SEE M4)
 POISIG = 0.0, 2.0, 4.00
 TIMEIG = 0.006, 0.008, 0.010
 RATEIG = 0.070, 0.070, 0.070,
 0.040, 0.040, 0.040,
 0.010, 0.010, 0.010 \$ no comments above this allow

3PROP
 NAME = 'LX CAPILLARY' GRAN = 'IPF \$2 \$'IPF'
 CHWT = 0.0231 LEN = 3.0000
 DIAM = 0.5116 DP = 0.1875
 \$ WEB = 0.1621
 GAMA = 1.1100 RHO = 0.0434
 COV = 22.9743 FORC = 33455.3
 TEMP = 300.00 BETA = 55.1181
 ALPH = 0.0
 \$ NTBL = 1
 * Note: nova input needs follow for prop det
 ZGRLFT = 0.0 \$LEFT HAND LOC OF BAG OF PROP I
 ZGRRHT = 3.0 \$ is this right ??
 RGRI = 0.09375 \$INNER RAD OF PROP note this is one dimensional
 RGRO = 0.2558 \$OUTER RADIUS note: NOT used in code

SLW = 0.0 \$SLOT WIDTH
 NFIX = 0 \$ 0=GRAIN FREE TO MOVE, 1 = ATTACH TO E, 2= ATT PROJ
 BONDX = 0.0 \$ STRENGTH OF BOND

GAP = 17400. \$RHEOLOGY RATE OF PROPAGA OF STRESS OF SETTLED BED
 GEPO = 0.8 \$0.35 \$ 0.820.28 \$0.25 \$0.301 \$0.58387
 GCAP = 50000. \$RATE OF PROPAGA
 ANU = 0 \$POISSONS RATIO OF PROP

TEMPIG = 810. \$ IGNITION TEMPERATURE
 KP = .0277 \$ THERMAL CONDUCTIVITY
 ALPHAP = .0001345 \$ THERMAL DIFFUSIVITY
 EMMIS = .6 \$ EMMISIVITY FACTOR

*PROP

NAME	= 'LX MOD TUBE'			
CHWT	= 0.003307			
LEN	= 7.2441			
GRAN	= '1PF' \$ 2 \$ '1PF'			
DIAM	= 0.19625	DPERF	= 0.1875	
* WEB	= 0.008736	RHO	= 0.0434	
GAMA	= 1.1100	FORC	= 33455.3	
COV	= 22.9743	BETA	= 0.1969	
TEMP	= 300.00			
ALPHA	= 0.0			
NTBL	= 1			

* Note: nova input needs follow for prop dek

ZGRLFT = 0.0 \$LEFT HAND LOC OF BAG OF PROP I

ZGRRHT = 7.24412 \$RIGHT HAN BOUND

RGRI = 0.1875 \$INNER RAD OF PROP note this is one dimensional
RGRO = 0.19625 \$OUTER RADIUS note: NOT used in code

SLW = 0.0 \$SLOT WIDTH

NFIX = 0 \$ 0=GRAIN FREE TO MOVE. 1 = ATTACH TO TUBE, 2= ATT PROJ
BONDX = 0.0 \$ STRENGTH OF BOND

GAP = 17400. \$RHEOLOGY RATE OF PROPAGA OF STRESS OF SETTLED BED

GEPO = 0.8 \$0.35 . \$ 0.820.28 \$0.25 \$0.301 \$0.58387

GCAP = 50000. \$RATE OF PROPAGA

ANU = 0 \$POISSONS RATIO OF PROP

B1 = 0.0 \$ BURN RATE CONSTANT

TEMPIG = 810. \$ IGNITION TEMPERATURE

KP = .0277 \$ THERMAL CONDUCTIVITY

ALPHAP = .0001345 \$ THERMAL DIFFUSIVITY

EMMIS = .6 \$ EMMISIVITY FACTOR

*PROP

NAME	= 'WC885'	GRAN	= BALL \$18
* IGNC	= 1	THRC	= .50000E-03
NTBL	= 1 \$-1		
DIAM	= 0.0630		
* DL/S	= 0.008570, 0.0315, 0.0851	I NOVA does not like /'s	
DLS	= 0.008570, 0.0315, 0.0851		
* DEPL	= 0.0005399, 0.0019845, .0053613		
RHOL	= 0.0539, 0.0539, 0.0548, 0.0589		
GAML	= 1.2850, 1.2850, 1.2790, 1.2340		
FRCL	= 254259.7, 254259.9, 278213.9, 373962.8		
COVL	= 30.8077, 30.8077, 30.9184, 26.4897		
TMPL	= 1896.7, 1896.9, 2109.4, 3471.2		
COEL	= .62236E-03, .62236E-03, .75113E-3, 0.001788		
EXPL	= 0.8053, .8053, .8053, .8053		
CHWT	= 0.3336		

* Note: nova input needs follow for prop dek

ZGRLFT = 0.0 \$LEFT HAND LOC CF BAG OF PROP I

ZGRRHT = 7.5 \$guess \$RIGHT HAN BOUND

RGRI = 0.25 \$guess \$INNER RAD OF PROP note this is one dimensional
RGRO = 0.63 \$CLTER RADIUS note: NOT used in code

SLW = 0.0 \$SLCT WIDTH

NFIX = 0 \$ 0=GRAIN FREE TO MOVE. 1 = ATTACH TO TUBE, 2= ATT PROJ
BONDX = 0.0 \$ STRENGTH OF BCND

GAP = 17400. \$RHEOLOGY RATE OF PROPAGA OF STRESS OF SETTLED BED

GCAP = 30000 RATE OF PROPAGA
ANU = 0 SPOTSSONE RATIO OF PROF

(4)

B1 = 0.0 BURN RATE CONSTANT
TEMPIG = 810. IGNITION TEMPERATURE
TP = .0277 THERMAL CONDUCTIVITY
ALPHAP = .0001345 THERMAL DIFFUSIVIT
EMMIS = .5 EMMISIVITY FACTOR

*COMM

* FOUR LAYER PROPELLANT MODEL (NOMINAL 1MM DIAM)
* warning this deck is metric because was commented out during conversion

NAME	= 'WC885'	GRAN	= BALL
IGNC	= 1	THRC	= 0.0002
DIAM	= 0.00100838		
NTBL	= -1		
DL/S	= 0.0136, 0.0500, 0.1350		
RHOL	= 1492.6, 1492.6, 1515.6, 1631.3		
GAML	= 1.285, 1.285, 1.279, 1.234		
FRCL	= 760000, 760000, 831600, 1117800		
COVL	= 0.001113, 0.001113, 0.001117, 0.000957		
TMPL	= 1896.9, 1896.9, 2109.4, 3471.2		
CF1L	= 0.00087	EX1L	= 0.8053
CF2L	= 0.00087	EX2L	= 0.8053
CF3L	= 0.00105	EX3L	= 0.8053
CF4L	= 0.00250	EX4L	= 0.8053
CHWT	= 0.1513		

*ETC

* WARNING This is metric et deck*****
PFAC=1
NPWR = 9
TPWR = 0, 3E-5, 6E-5, 1.2E-4, 1E-3, 1.25E-3, 1.52E-3, 1.7E-3, 2E-3
PWR = 0, 0, 4.4E6, 2.4E6, 4.6E6, 1.85E6, 0.45E6, 0.09E6,

*END



WHAT WE PERCEIVE AS NECESSARY FOR THE FUTURE • IRAD PLAN

CY 93 → BEYOND

**OLIN IRAD
FUNDS**

**COOPERATIVE
PARTNER SHARE**

**COOPERATIVE
EXPERIMENTS WITH:**

<u>U.S. GOVT.</u>	<u>GT DEVICES</u>
ARL / NAVY	GDLs
ARDEC	
SSDC / EGLIN AFB	
NAT LABS	

PHYSICS

- HIGH LD>1.3 g/cc
- BED RHEOLOGY
- BED POROSITY
- BED COMPACTION

CODE

0-D IB

**1-D IB
XKTC(M)**

**1-1/2-D IB
XKTC(M)**

2D NG

3D NG

FLAME SPREAD ISSUES

PLASMA / MODERATOR INTERACTIONS

PLASMA / PROPELLANT INTERACTIONS

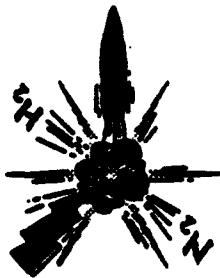
CHEMICAL KINETICS / PATH MODIFICATION STUDIES

VISUALIZATION STUDIES / X-RAY DIAGNOSTICS

GUN FIRINGS / DIAGNOSTICS / SHORT TUBE / LONG TUBE

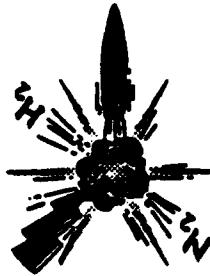
(* U.S. GOVT. DEVELOPED)

**Olin
ORDNANCE**



CHALLENGES FOR ETC MODELING

- Modeling technology must advance rapidly over next two years.
- Funds for 6.1/6.2 work appear scarce.
- For solids (ET-C) near to medium term technology (modeling) issues not as severe as liquids but significant technology challenges are present.
- Severe lack of high charge density/loading density experimental data with ET-C systems critical potential show stopper for modeling.
- US Government must articulate IM requirements more strongly as associated with ET-C.

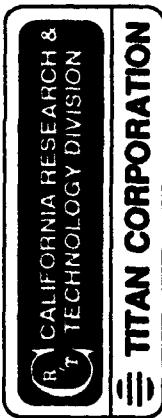


CONCLUSIONS

- Modeling community must pull together - under A.R.L. Guidance/Sponsorship/Leadership.
- Physics experiments must be jointly/cooperatively conducted to leverage scarce 6.1/6.2 resources all sources
 - Navy, Army, SDC, DNA, Air Force.
- We must be creative in our approaches.
- Olin will sell no propellant or cartridge systems before their time.

Our goal is to field ammunition/ctg systems. NOT Conduct long term R & D - Modeling is only one of the tools (but a necessary one)

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Application of PDF Turbulent Combustion Model to Electrothermal-Chemical (ETC) Guns

Philip A. Hookham
Leonard Walitt

Presented at:

U.S. Army Research Laboratory
Aberdeen Proving Ground, Maryland 21005

12 May 1993



ETC Gun Modeling at CRT: Background

- Defense Nuclear Agency (DNA) sponsored ETC gun modeling under Turbulent Chemistry Modeling contract
- Work was performed over ~1 year period ending 12-92
- Contract emphasized turbulent mixing and combustion aspects of problem

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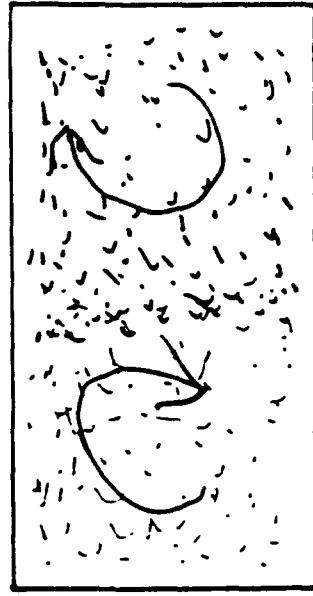
Unmixedness Modeling Using PDF Approach

Problem Definition

- Suppose we have a computational cell containing reactants α and β and product γ which is generated in an irreversible reaction (the assumption of irreversibility is not required):
$$\alpha + \beta \rightarrow \gamma$$

- The mean mass fractions of α and β , $\overline{C_\alpha}$ and $\overline{C_\beta}$, are known
- The turbulent correlation $\overline{C'_\alpha C'_\beta}$ can be calculated from the second-order closure turbulence model (we have to model a source term in the evolution equation for this correlation, however)
- What is the rate of production of γ , i.e., \dot{W}_γ ?

$$\dot{W}_\gamma = K C_\alpha C_\beta$$



Computational cell

Unmixedness Modeling Using PDF Approach (continued)

Donaldson Unmixedness Approach

- Postulate the existence of N states within the cell, where each state is characterized by $C_{\alpha,i}$ and $C_{\beta,i}$ (and, in general, temperature T_i), i.e., approximate a continuous pdf with a finite number of Dirac delta functions δ_i with strengths ϵ_i .
-

- Calculate the probability ϵ_i of each state.
- Calculate the expectation of the rate of production of γ from the known states and ϵ_i s:

$$\bar{\dot{W}}_\gamma = \sum_{i=1}^N \epsilon_i \dot{W}_{\gamma,i}$$

Turbulent Unmixedness Modeling: Choice of States for a Two Species System

Suitable events should include states at the mean (i.e., when turbulence levels are low) as well as states where one or both concentrations disappear (intermittency).

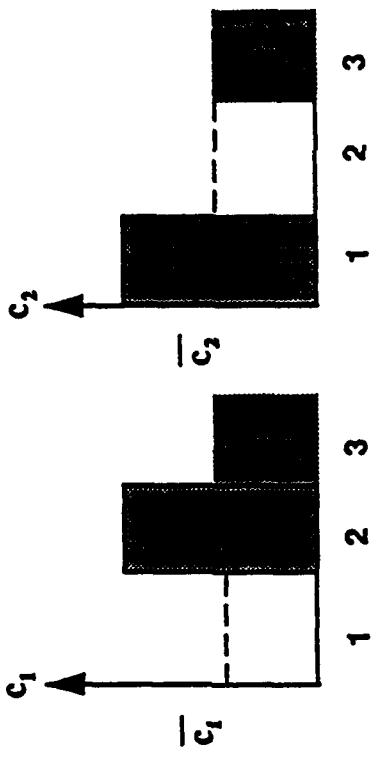
If $\overline{c'_1 c'_2} < 0$, we may choose

State 1: $c_{1,1} = 0, c_{2,1} = 2\overline{C_2}$

State 2: $c_{1,2} = 2\overline{C_1}, c_{2,2} = 0$

State 3: $c_{1,3} = \overline{c_1}, c_{2,3} = \overline{c_2}$

Or if

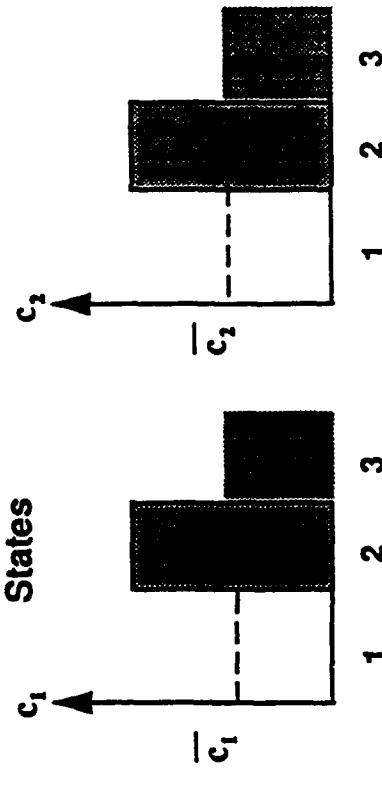


$\overline{c'_1 c'_2} > 0$,

State 1: $c_{1,1} = 0, c_{2,1} = 0$

State 2: $c_{1,2} = 2\overline{C_1}, c_{2,2} = 2\overline{C_2}$

State 3: $c_{1,3} = \overline{c_1}, c_{2,3} = \overline{c_2}$



Determination of POF

Constraints

$$\sum_{i=1}^N \epsilon_i c_{ij} = \bar{c}_j$$

$$\sum_{i=1}^N \epsilon_i c_{ij} c_{kj} = \bar{c}_k$$

$$\sum_{i=1}^N \epsilon_i c_{ij} c_{kj} c_{lj} = \bar{c}_l = \bar{c}_x \bar{c}_y + \bar{c}'_x \bar{c}'_y$$

$$\sum_{i=1}^N \epsilon_i = 1$$

If number of states exceeds number of constraints, we need an additional criterion.

Maximize Entropy by minimizing

$$\sum_{i=1}^N \epsilon_i \ln(\epsilon_i)$$

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Solution Procedure for Probabilities

Lagrange multiplier method

Define $F =$

$$\sum_{i=1}^N \epsilon_i \ln \epsilon_i + \lambda_{01} \left(\sum_{i=1}^N \epsilon_i C_{\alpha,i} - \bar{C}_\alpha \right) + \lambda_{02} \left(\sum_{i=1}^N \epsilon_i C_{\beta,i} - \bar{C}_\beta \right) + \lambda_{12} \left(\sum_{i=1}^N \epsilon_i C_{\alpha,i} C_{\beta,i} - \bar{C}_\alpha \bar{C}_\beta \right) + \lambda_{00} \left(\sum_{i=1}^N \epsilon_i - 1 \right).$$

Then:

$$\epsilon_i = \exp(-1 - \lambda_{01} C_{\alpha,i} - \lambda_{02} C_{\beta,i} - \lambda_{12} C_{\alpha,i} C_{\beta,i} - \lambda_{00}).$$

Solve for Lagrange multipliers using Newton's method, e.g.

Temperature Spottiness Modeling

Approach

- Determine the temperatures T_i associated with each state i (whose probabilities have already been calculated) by minimizing the function:

$$\sum_{i=1}^N \epsilon_i T_i^2$$

subject to the constraints:

$$\sum_{i=1}^N \epsilon_i C_{\alpha,i} T_i = \overline{C_{\alpha} T} \quad \text{and} \quad \sum_{i=1}^N \epsilon_i C_{\beta,i} T_i = \overline{C_{\beta} T}.$$

i.e., maximize the entropy of mixing. Again, using Lagrange multipliers, solve for T_i

$$T_i = \lambda_1 C_{\alpha,i} + \lambda_2 C_{\beta,i}$$



Temperature Spottiness Modeling (continued)

- We must also satisfy a constraint on $\overline{T^2}$, however, and therefore an additional degree of freedom is needed (consider the case of only 1 species when there could be no unmixedness, but still there are temperature fluctuations). Introduce an additional parameter δ such that:

$$\begin{aligned}\varepsilon_{i1} &= \varepsilon_i(1+\delta)/2, & \varepsilon_{i2} &= \varepsilon_i(1-\delta)/2, \\ T_{i1} &= T_i/(1+\delta), & T_{i2} &= T_i/(1-\delta).\end{aligned}$$

The constraint then becomes:

$$\overline{T^2} = \sum_{i=1}^N (\varepsilon_{i1} T_{i1}^2 + \varepsilon_{i2} T_{i2}^2) ,$$

and delta is:

$$\delta = \sqrt{1 - \frac{1}{\overline{T^2}} \sum_{i=1}^N \varepsilon_i T_i^2} .$$

$C_{R/T}$

ETC Gun Modeling Approach

- Model from “first-principles”:

- Fluid dynamics of plasma, liquid and vaporized working fluid components, reaction products

- Use detailed parameterizations for:

- Mass, momentum, and heat transfer between gas and liquid (droplet) phases
- Turbulence
- Turbulent mixing and reaction of chemical species
- Entrainment of droplets from working fluid

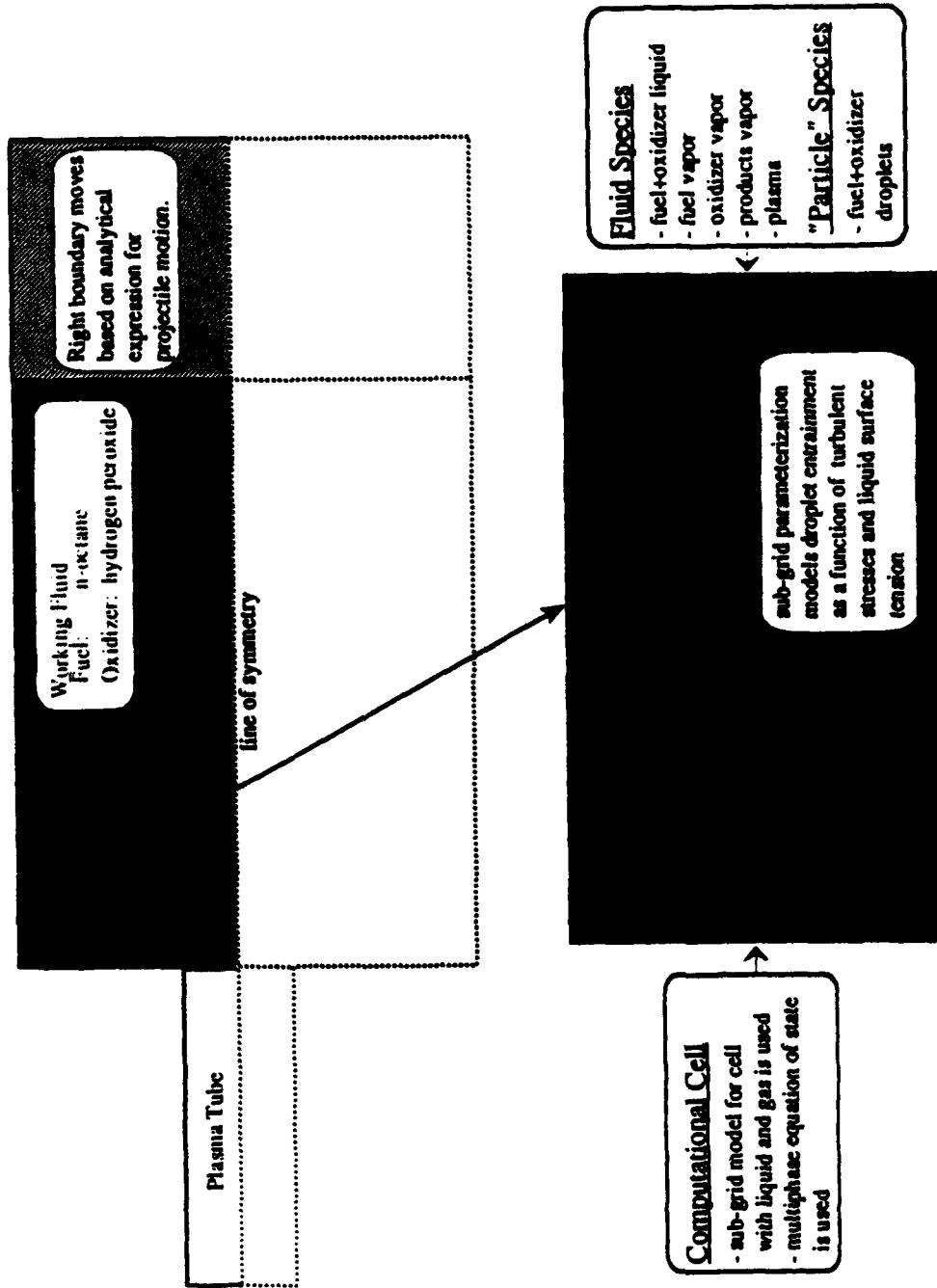


ETIC Gun Modeling Approach (continued)

- Model simply:
 - Addition of electrical energy to plasma
 - Chemical kinetics
 - Projectile motion

EIC Gun Modeling Approach Schematic

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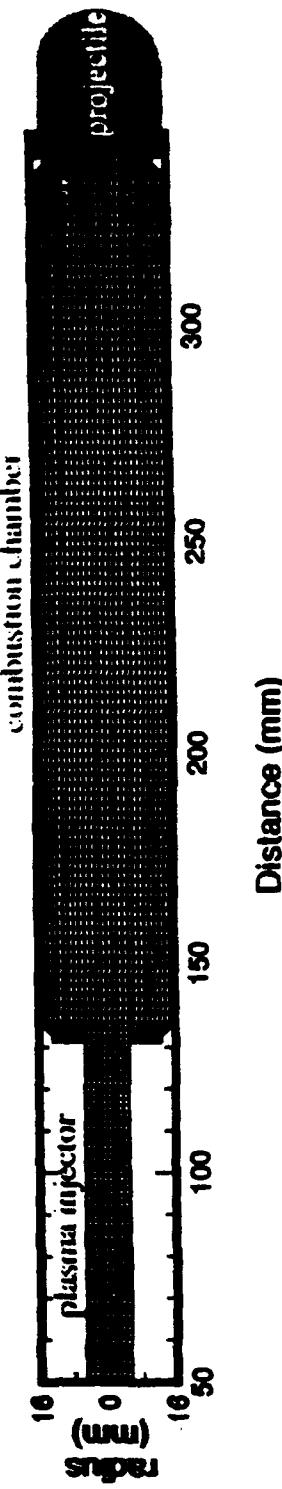




ETIC Gun Calculation Description

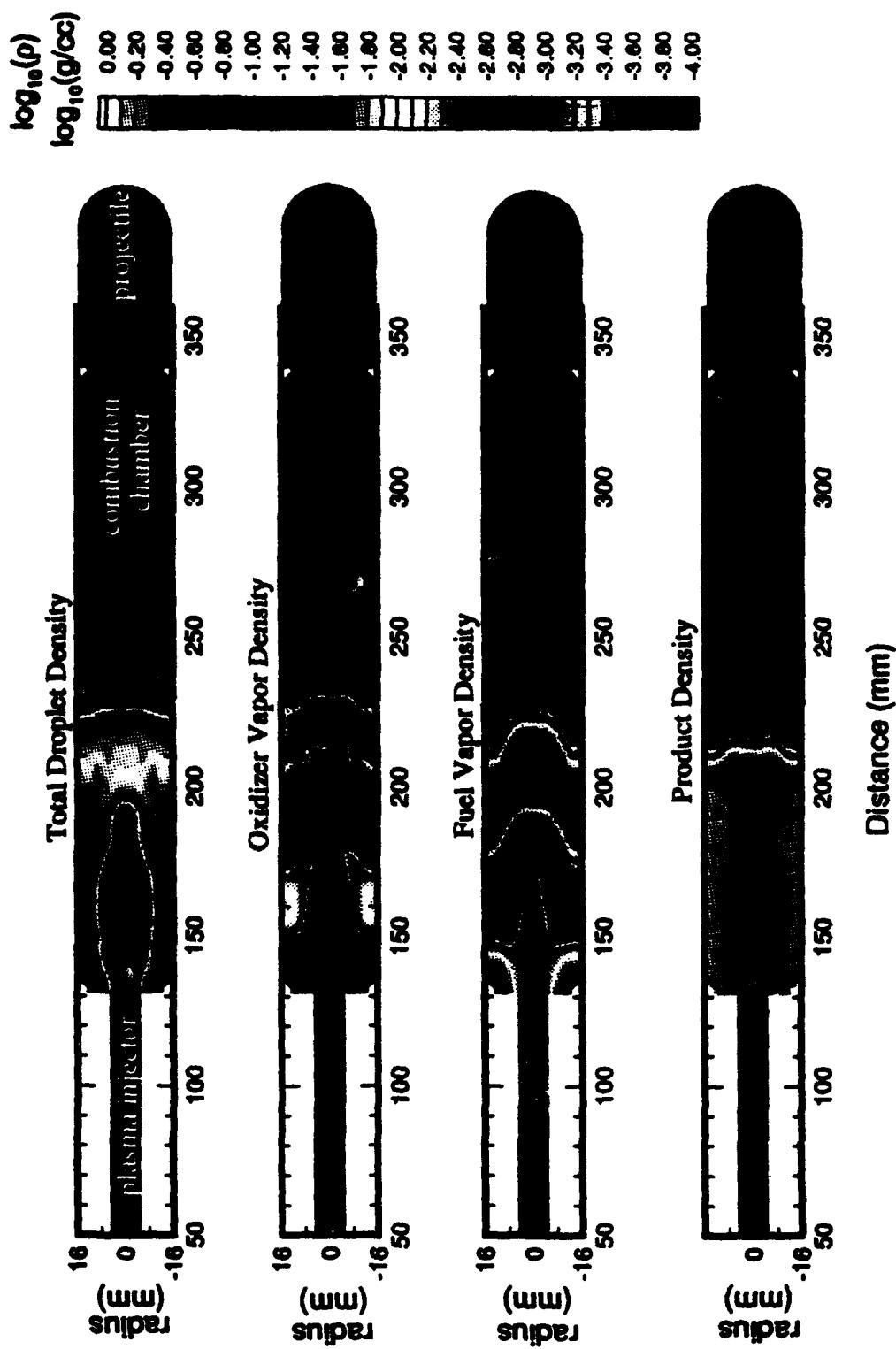
Features

- Simulation of DNA Shot #7
- 30mm nominal diameter, 57.4 caliber, projectile weight = 339 g
- Gun chamber is scaled version of 155mm gun chamber
- Propellant is 85% H₂O₂ by volume, 15% RJ4 (simulated by octane), 166 cc
- Total electrical energy input = 168 KJ, added over 1.1 msec
- 2-D MAZE code (axisymmetric)



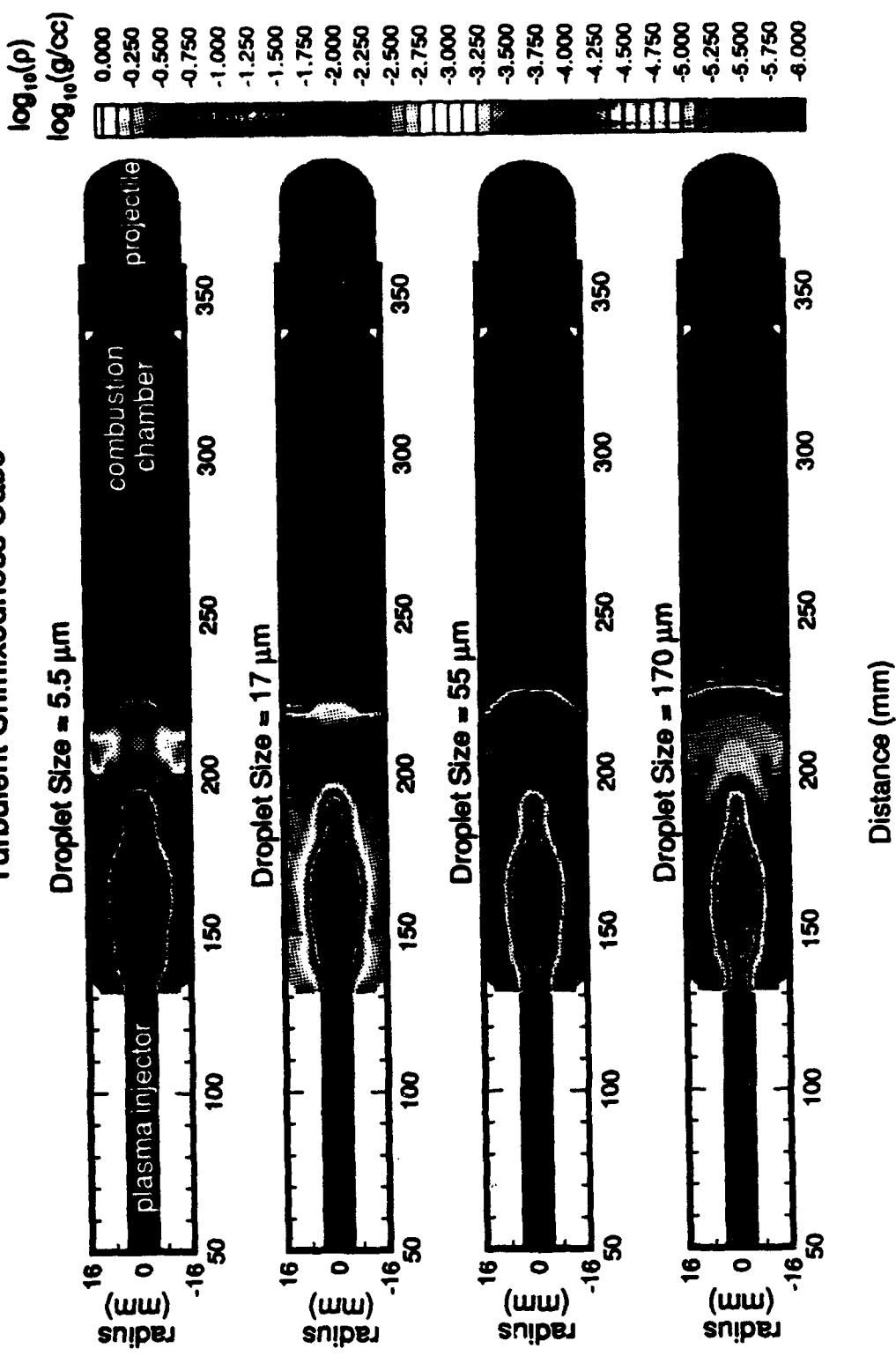
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MAZE Code Simulation of 30mm ETC Gun Test Selected Densities at 0.50 msec Turbulent Unmixedness Case



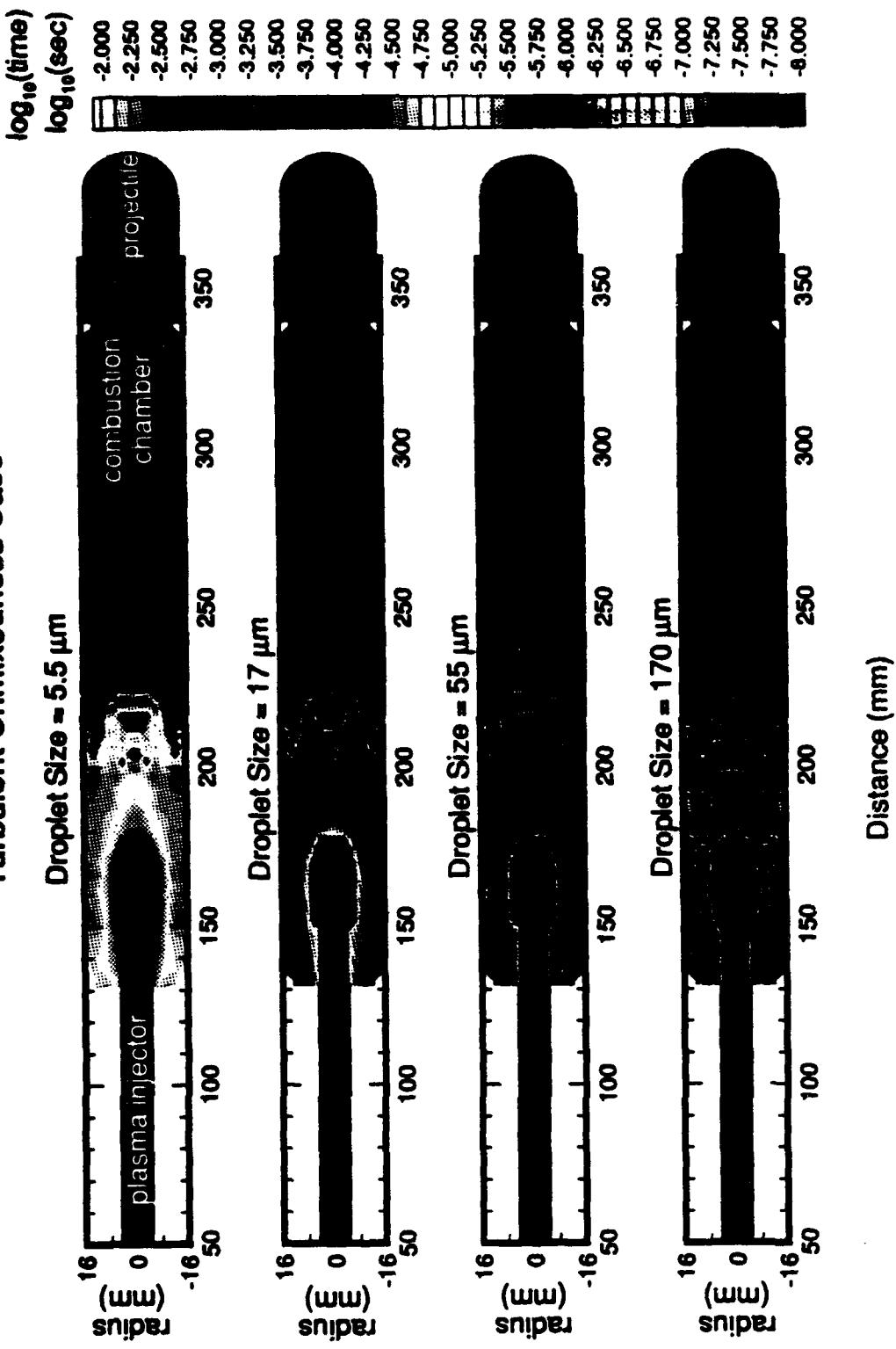
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MAZE Code Simulation of 30mm ETC Gun Test
Droplet Density Time = 0.50 msec
Turbulent Unmixedness Case

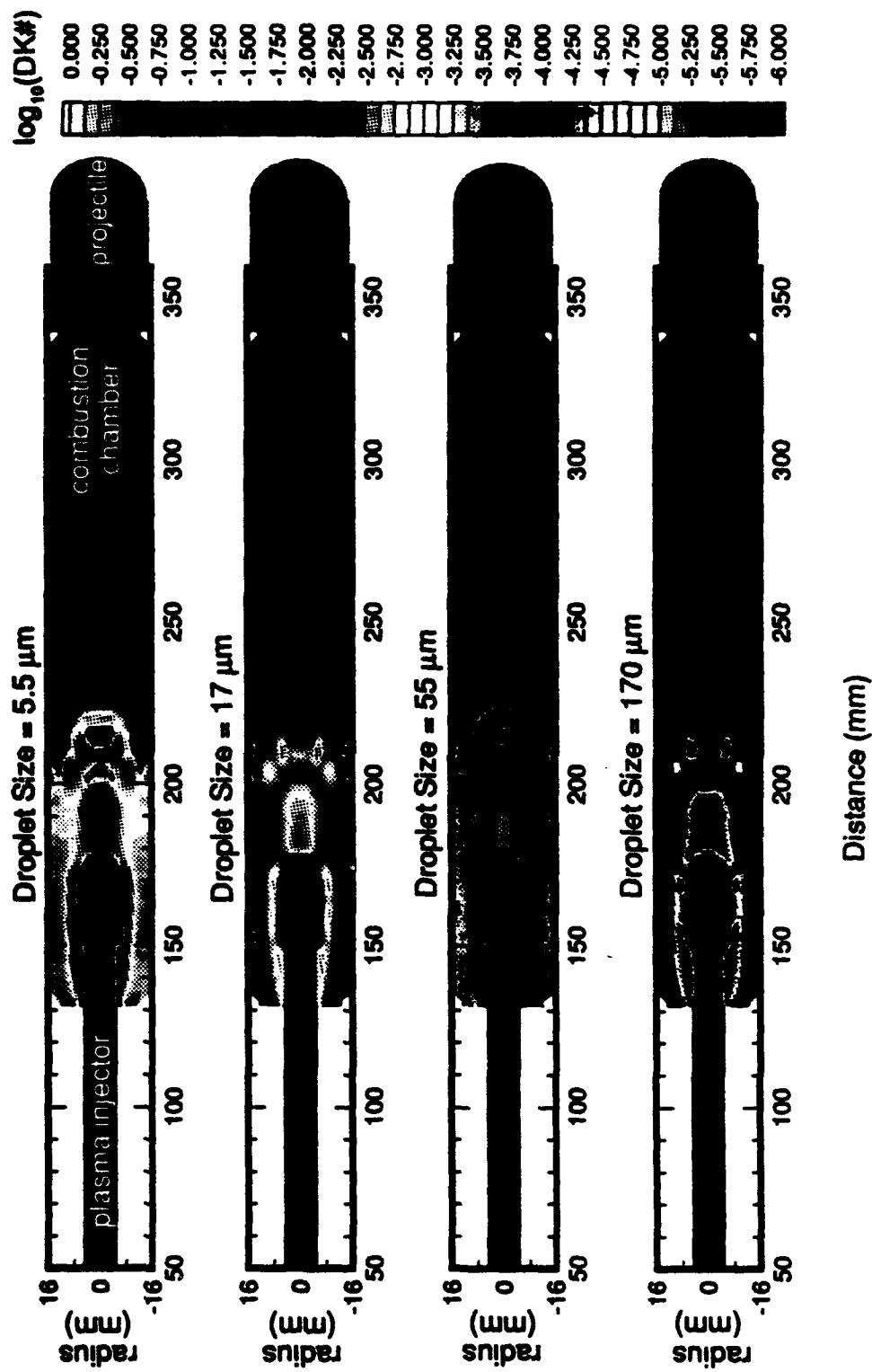


CF

MAZE Code Simulation of 30mm ETC Gun Test
Droplet Extinction Time Time = 0.50 msec
Turbulent Unmixedness Case



MAZE Code Simulation of 30mm ETC Gun Test
Turbulent Damköhler Number (t_{mix}/t_{evap}) Time = 0.50 msec
Turbulent Unmixedness Case



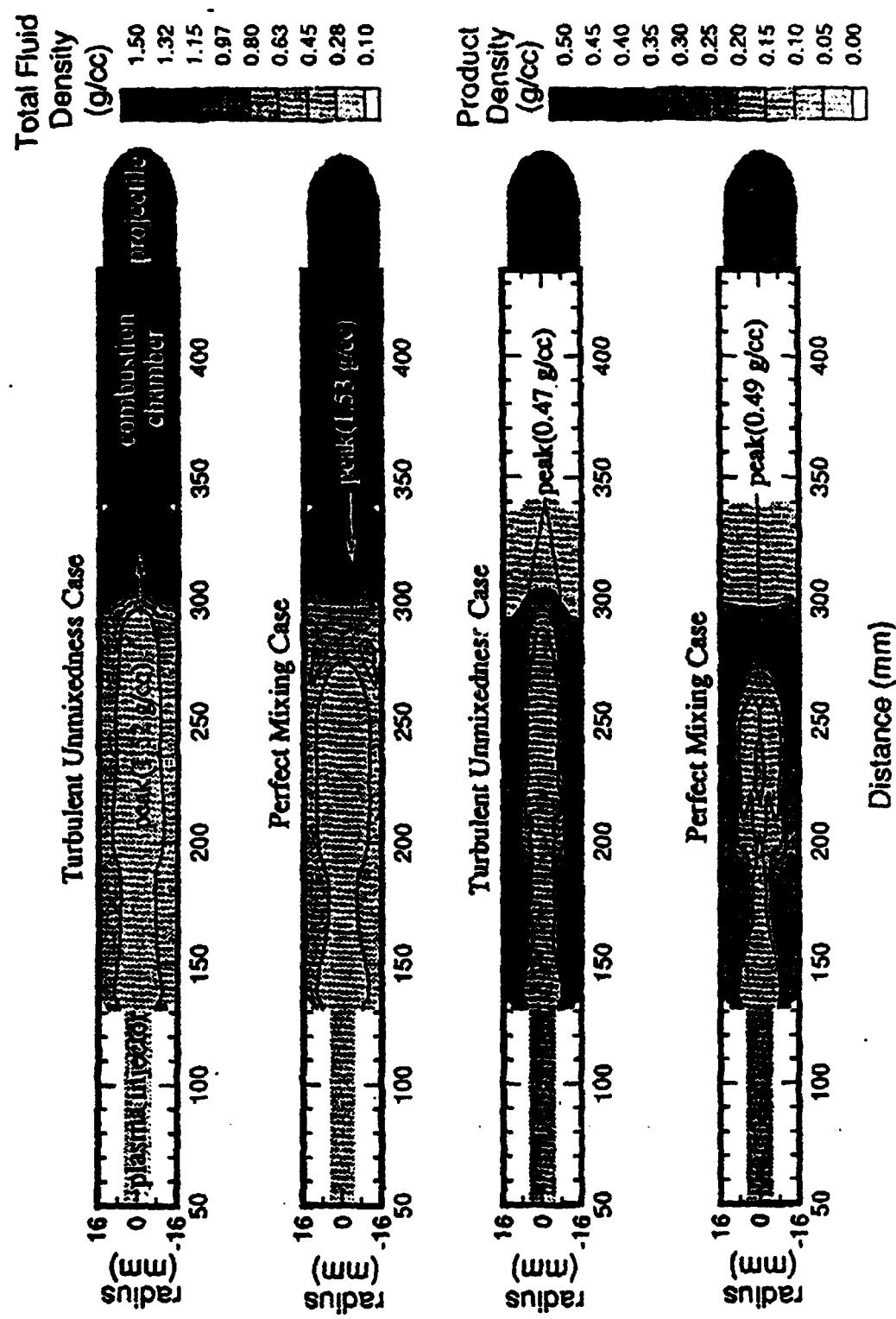


Figure 17. Comparison of turbulent unmixedness and perfect mixing cases at 1.1 msec: total fluid density and product density contours.

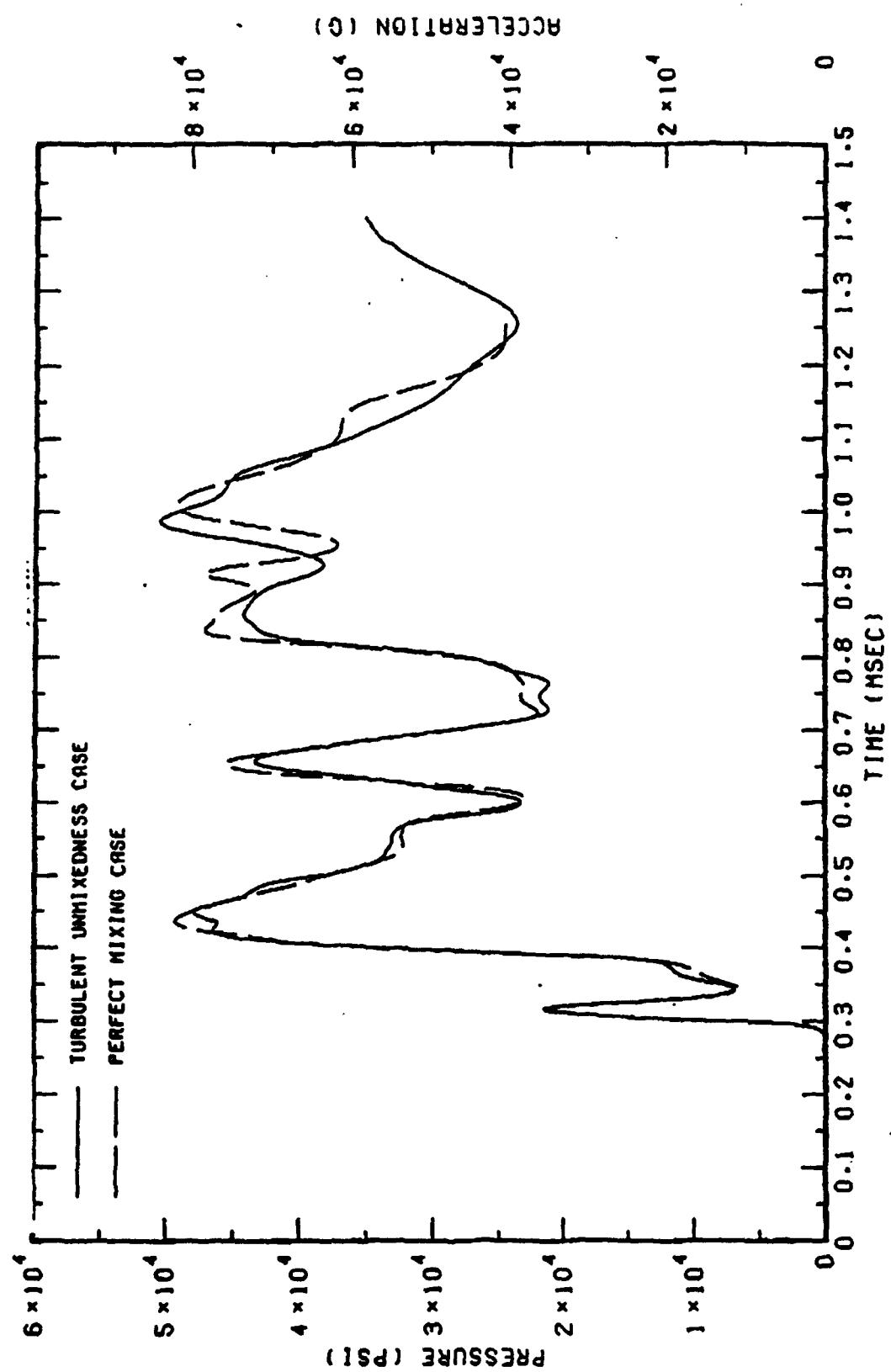
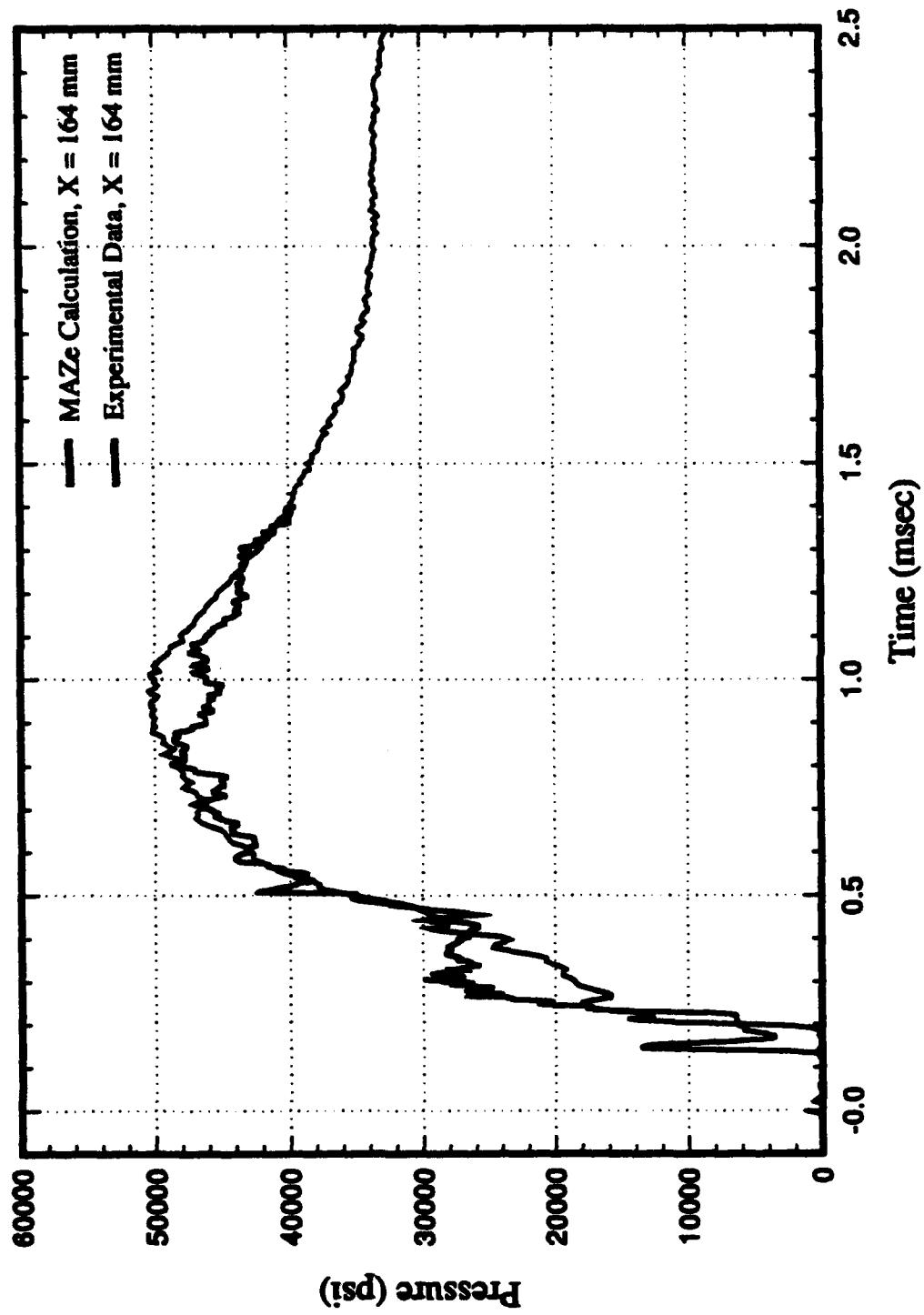


Figure 6. Projectile base pressure and acceleration time history.

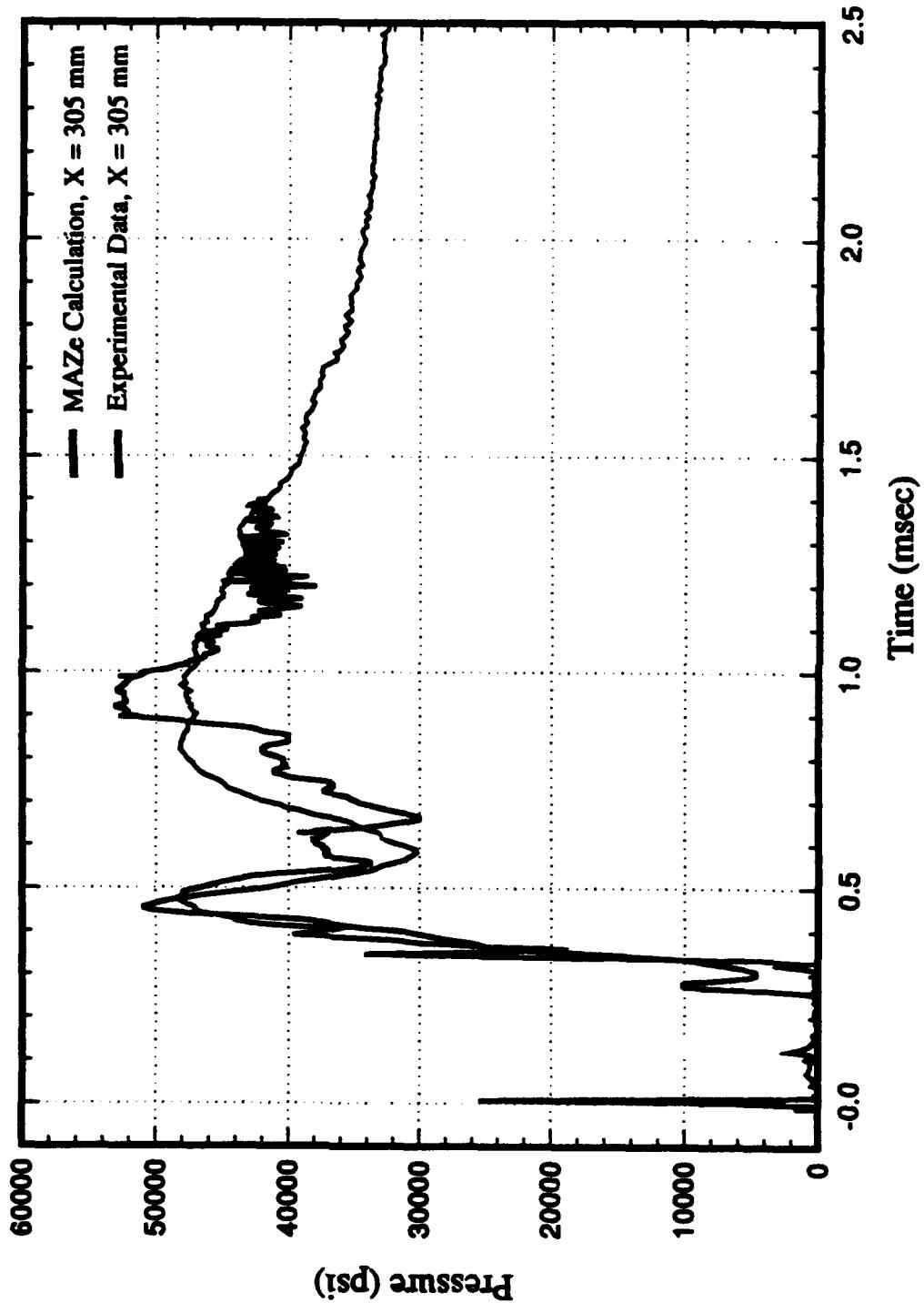
**MAZE Code Simulation of 30mm ETC Gun Test
Comparison with Experimental Overpressure Time-Histories**

Fig



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MAZE Code Simulation of 30mm ETC Gun Test Comparison with Experimental Overpressure Time-Histories



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