

Orbital Transfer Rocket Engine Technology

High Velocity Ratio Diffusing Crossover

Contract NAS3-23773-Task B.2

FINAL REPORT

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NASA-Lewis Research Center Cleveland, Ohio 44135 G. P. Richter, Program Manager



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FOREWORD

The work represented by this final report was completed from December 1983 to December 1988 by personnel from engineering functional units at Rocketdyne, a division of Rockwell International, under Contract NAS3-23773. Mr. Dean Scheer, Lewis Research Center, was the NASA Project Manager. At Rocketdyne, Messrs. Ronald Pauckert, Project Manager, Timothy Harmon, Project Engineer, and Brian Lariviere, Development Engineer were responsible for the technical progress and administration of the program.

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SUMMARY

The effort conducted herein was sponsored by the Space Propulsion Technology Division, NASA Lewis Research Center, Cleveland, Ohio, under Contract NAS3-23773, "Orbit Transfer Rocket Engine Technology Program." The technical effort of this contract was completed from December 1983 through December 1988.

The overall objective of this task was to experimentally evaluate the performance of the high velocity ratio diffusing crossover used in the first and second stages of the MK49-F high pressure fuel turbopump, which is used on the RS-44 Orbital Transfer Vehicle rocket engine. With the diffuser inlet conditions generated by a scaled up model of the MK49-F inducer and impeller, the performance of these pumping elements and the high velocity ratio diffusing crossover were determined using water and air as the pumped fluids. The air tests were included to obtain performance data over a wide range of Reynolds number. These performance surveys were to be used to verify the design of the high velocity ratio diffusing crossover, and correct any design deficiencies that were found. Since the MK49-F was tested prior to the completion of this test program, the data from the MK49-F was used as a comparison for the water and air test data.

To complete the technical requirements of this program, a tester, utilizing a 2.85 times scale inducer, impeller, and diffuser crossover system, was designed, fabricated, and tested in both air and water.

The design of the high velocity ratio diffusing crossover was based on integrating the scaled up MK49-F first stage components with the existing SSME HPFTP tester. By using the existing tester hardware, design and fabrication costs were saved. Additional costs were saved by fabricating the new crossover tester components from common aluminum alloys to minimize the machining complexities and procurement costs.

A total of nine (9) tests were conducted on the north powerhead of the Pump Test Facility at the Engineering Development Laboratory from September 1988 to October 1988. The first two (2) tests of the diffusing crossover were conducted in air, while the remaining seven (7) tests were conducted in water. Both, the air and water tests were conducted at a shaft speed of 6322 rpm. In air, the head versus flow (H-Q) test data determined that the upcomer diffuser in the crossover was stalled for all the flow conditions attempted. The stall was caused by increased boundary layer blockage due to the low Reynolds number resulting in the impeller discharge flow entering the diffuser inlet at an angle and velocity, which would produce a flow separation in the diffuser. Air test data compared well with the analytic predictions and MK49-F hydrogen data for the impeller and the inducer head performance, clearly showing that the stall was in the diffuser.

H-Q tests in water, from 65 to 140% of design flow, were conducted. The overall stage head measured these tests was only 4% lower than the prediction. Again, the performance of the inducer and impeller were compared with the available resources. During the H-Q tests, the upcomer diffuser stall point was determined to be at a slightly lower flow than predicted, and the hysteresis region was clearly evident. The head loss during stall was not severe which was indicative of a diffuser leading edge stall characteristic. Internal pressure distributions were also examined to evaluate the inducer, impeller, and various positions within the diffuser crossover system. Suction performance tests from 80% to 124% of design flow were conducted, which established the minimum inlet Net Positive Suction Head (NPSH). The performance was lower than the ideal potential, but a lower performance was expected with the design characteristics scaled from the smaller MK49-F. The performance of the tester, however, exceeded the minimum design requirements established for the MK49-F turbopump.

The test data showed 95% of the overall diffusion being accomplished by the upcomer portion of the crossover passage, as predicted. By calculating the required diffuser intet boundary layer blockage to match the test data and using the Loss Isolation program to determine the vaneless area diffusion, the mean pressure recovery coefficient from the test data compared favorably with the predictions.

The technique generated to analyze the data will be beneficial for the design and analysis of future diffusing crossover passages. The data generated in this test program verified the methods used at Rocketdyne to design and predict the performance of pumping elements and high velocity ratio diffusing crossovers. The data generated in this program will also be of value in further anchoring the predictive codes of other designs.

INTRODUCTION

Multistage pumps require the use of crossover passages to convey the fluid from the exit of one impeller to the inlet of the next impeller. The MK49-F, which is used on the 15,000 lbf thrust Orbital Transfer Vehicle (OTV) engine, is a three stage centrifugal high-pressure liquid hydrogen turbopump. A cross-section of the MK49-F turbopump is presented in Figure 1 showing the location of the two interstage crossovers. The MK49-F uses seventeen continuous passage crossovers between each centrifugal impeller stage. Each passage consists a radially out diffuser called the "upcomer", followed by a radially inward diffuser called the "downcomer". A low turning loss section, called the transition, connects the two diffuser sections.

To develop the 4600 psia discharge pressure required by the advanced expander cycle OTV engine, a high impeller exit velocity is required. However, relatively low velocity is required at the inlet of the next impeller for the best overall pump performance. The result is a large diffuser inlet velocity to exit velocity ratio through the crossover.

The MK49-F design uses a velocity ratio of 6.23, which approaches the diffusion limit for stable efficient design. Previous diffusing crossover designs, at Rocketdyne, used velocity ratios that were lower, for example, 5.46 for the MK48-F, and 3.0 for the SSME HPFTP (MK38-F). With these high diffusion rates, the boundary layer flows must be carefully controlled to preclude stall, while operating over the wide range of pump flows required by the engine system.

The design of the crossover passages was based on advanced analytical procedures anchored by tests of stationary two-dimensional diffusers with steady flow. In the case of centrifugal pumps, however, the flow leaving the rotating impeller appears to the stationary diffusion system as an unsteady non-uniform flow field with potential inlet boundary layers even larger than normally encountered in laboratory tests of static diffusers. To accurately assess the design of the high velocity ratio diffusing crossover, it was required that the impeller flow be accurately simulated. This could only be achieved by using a scaled-up version of the MK49-F impeller.

A highly instrumented tester was designed and fabricated which would simulate the MK49-F first stage pumping elements and crossover passages. To take advantage of existing test facility hardware, a scaled up model of the stage was chosen with a scale factor of 2.85. This scaled up model also served to increase the Reynolds number for

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the model test to bring it closer to the Reynolds number of operation in hydrogen of the full scale MK49-F.

Table 1 gives the basic dimensions and operating parameters of both the MK49-F pump for full speed operation in hydrogen and the scale up model for the subject test program.

Tests of the high velocity ratio diffusing crossover tester with unsteady whirling flow from the exit of the scaled up impeller, were conducted to evaluate the influences of the large-scale turbulence, non-uniform velocity profile, and non-steady velocity on the MK49-F stage performance and efficiency. Tests were conducted in two fluids, water and air, to determine the effects on performance over a wide range of Reynolds number.

	MK49-F Turbopump	Crossover Tester		
Parameter	LH ₂	Water	Air	
Inducer Tip Diameter (inch)	1.95	5.56	5.56	
Impeller Tip Diameter (inch)	3.90	11.124	11.124	
Diffuser Inlet Diameter (inch)	4.30	12.25	12.25 -	
Number of Blades: Inducer Impelier Diffuser Inducer Flow Coeff. (\$=Cm/Ut)* Design Speed (rpm) Design Flow (gpm) Reynolds Number **	4 4+4 17 0.10 110,000 436 7.6x10 ⁷	4 4+4 17 0.10 6322 583 2.31x10 ⁷	4 - 4+4 17 0.10 6322 583 1.65x10 ⁸	

Table 1 - Basic Parametric Information MK49-F Turbopump versus Crossover Test Rig

Inter Flow Coefficient, ϕ , where C_m is the meridional fluid velocity and U_t is the inducer tip speed.

Reynolds number based on impeller diameter and speed.

* * * At 33,400 rpm, Reynolds number drops to 2.31x107.

TECHNICAL DISCUSSION

DESIGN AND FABRICATION

Tester Configuration & Layout

Analytical and computer predictions determined that, for optimum performance of the RS-44 advanced expander cycle engine, an interstage diffusion of 6.23 for the MK49-F would result. However, there was little published data on multistage pump crossovers having high diffusion velocity ratios. Rocketdyne's experience was limited to a maximum diffusion velocity ratio of 5.46 used in the MK48-F turbopump. The high diffusion rate of the MK49-F was sufficiently beyond the current experience base that a test program to evaluate the performance of the high velocity ratio diffusing crossover was required. The overall objective was to design a tester and experimentally evaluate the performance of the high velocity ratio diffusing crossover used in the first and second stages of the MK49-F high pressure fuel turbopump.

The high velocity ratio diffusing crossover tester, shown in Figure 2, was designed with two major design requirements imposed. The first requirement was to design the crossover tester around the dimensions of the existing SSME HPFTP tester interfaces to minimize the tester design and fabrication costs. The second requirement was to incorporate as much internal instrumentation as possible to maximize the information obtained during testing of the diffusing crossover passage and MK49-F pumping elements.

A scale factor of 2.85 was determined from the SSME HPFTP impeller tester hardware. The crossover tester layout was then generated by maintaining these interface geometries and directly scaling the MK49-F turbopump pump elements. Figure 3 shows the cross-section of the HPFTP tester shaft, discharge manifold, bearing carrier, face seal, and bearing assembly which were used by the crossover tester. The hardware parts list for the High Velocity Ratio Diffusing Crossover tester are shown in Table 2.

The MK49-F inducer, impeller, and crossover housing, components were scaled up to mate with the HPFTP tester discharge manifold. A scale factor of 2.85 was used to increase the size of the MK49-F impeller from 3.900 inches in diameter to a size of 11.124 inches. With this scale factor established, the crossover, the impeller, and the inducer were designed.

Figure 2 - Crossover Tester Cross-Section







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Table 2 - Crossover Tester Parts List

HIGH VELOCITY RATIO DIFFUSING CROSSOVER TESTER PARTS LIST

FRAT NV.	DESCRIPTION	ONTY
7R0017922-5	TUBE	6
7R0017923-3	HOUSING. FUMP END	ĩ
7R0017924-3	COVER PLATE. BEARING PRELOAD	ī
7R0017925-3	CROSSOVER HOUSING	ī
7R0017927-3	FACE SEAL MATING RING	ī
7R0017927-5	THRUST DISK	ī
7R0017928-3	THRUST DISK SEAL	1
7R0017928-5	RETAINER, THRUST DISK SEAL	1
7R0017930-1	IMPELLER	1
7R0017931-1	INDUCER	1
7R0017932-3	NUT (INDUCER)	1
7R0017933-3	LOCK (INDUCER)	1
7R0017934-3	SPACER	1
7R0017935-3	Lock (Impeller)	1
7R0017936-3	SPACER	1
7R0017938-3	RETAINER	1
7R0017940-3	SEAL, LABY	· · 1
7R0017940-5	RETAINER, LABY SEAL	1
7R0017941-3	NUT (IMPELLER)	1
7R0017942-3	SPACER	1
7R0017943-3	SCREEN	1
7R0017944-1	INLET	1
780017945~3	SPACER	1
7R0017950+3	TUBES	2
780033904-3	SPACER	1
NS 9390-580	PIN	3
T-5100073-120	FACE SEAL. SEALOL: 3-3-B002B0-44	1
T-5100073-108	SPACER	1
T-5100073-104	NUT	-
T-5100073-501	SLEEVE	1
T-5100073-801	COLLAR	1
T-5100073-104	SCREW, SET	2
	•	
SRF 7214 BEA	BEARING	2
EWR307280-007	MAINFOLD	1
EWR306802-003	SHAFT	1
EWR306803-003	BEARING CARRIER	1

High Velocity Ratio Diffusing Crossover

A pair of straight channel type vaned diffusers, with square cross-section separated by a variable cross-section turning channel, were chosen for the MK49-F. The same concept was chosen for the lower area ratio SSME HPFTP diffusion system which had demonstrated an outstanding efficiency.

For a straight channel diffuser design, maximum performance requires a uniform flow field at the diffuser iniet, or throat. To improve the inlet flow field and reduce the perturbations produced by the passing impeller blades, a vaneless entrance region, just upstream of the diffuser throat, was included in the design. A detailed vane leading edge geometry and flow pattern relationship was investigated, using available analytical codes, to determine the diffuser inlet flow angle and velocity from the impeller. From this information, the inlet vane angle, throat area, and number of crossover passages were determined. Once the inlet geometries were satisfied and the throat flow field established, the diffuser geometry was produced.

At the exit of the upcomer diffuser, a three-dimensional transition section turns the flow radially inward to the inlet of the downcomer diffuser, forming a continuous crossover passage, as seen in Figure 4. The turning channel cross-section changes continuously through the turn to minimize the static pressure gradient across the passage. These pressure gradients, created by the centrifugal force of the fluid in the turn would induce secondary flows which would reduce the overall crossover performance. The design of the turning channel required the use of computer-aided design (CAD) to produce the three dimensional lay out.

Figure 5 shows the ceramic casting core assembly of the seventeen crossover passages of the MK49-F turbopump. The High Velocity Ratio Diffusing Crossover tester passages were scaled up directly from the coordinates generated on GAD for the MK49-F crossover.

Initial blds for casting the aluminum crossover housing resulted in only one bidder response at a cost three times greater than the estimated costs based on the MK49-F crossover cores. It was decided that casting the crossover from e high strength plastic would save both cost and schedule. By casting with a plastic, costs would be saved in raw materials and "hard" tooling which are required for metal castings. A plastic, FR-40/5481C epoxy, crossover housing was designed, with an aluminum reinforcing ring.

HIGH VELOCITY RATIO DIFFUSING CROSSOVER





Figure 5 - MK49-F Turbopump Crossover Casting Core

Rockwell International Rocketoyne Division Tri-Models was placed under contract to construct the core and tooling required to produce the plastic crossover housing, while the actual pouring of the part would be conducted at Rocketdyne. However, when Tri-Models completed the core box, their costs exceeded the purchase agreement. As a result, Rocketdyne took delivery of the core box only.

Using the core box and FR-40/5481C epoxy provided by Rocketdyne, A & M Model Makers was contracted to cact the crossover housing. Wax cores were successfully made and assembled into a "negative" of the crossover. The plan was to pour the plastic into the mold surrounding the cores, and then return the crossover to Rocketdyne for elevated temperature curing, which would promote the greatest strength of the epoxy. The pouring technique was designed to slowly cure the casting at an elevated temperature to reduce risk of cracking the crossover housing. However, when the pour of the plastic proceeded, cracks began to appear almost immediately. By the completion of the pour, the housing was riddled with cracks. The cracking was caused by normal shrinkage of the plastic, the aluminum reinforcement ring restricting any movement by the shrinking plastic.

The crossover housing drawing, 7R0017925, was modified to fabricate the part from aluminum alloy 356. Burrows Pattern Works was contracted to fabricate a set of ceramic cores from the existing core box. The cores were dimensionally inspected and found to be within the tolerance of the drawing. Enough cores were fabricated by Burrows Pattern Works to produce four crossover housings. The ceramic cores and the core box were delivered to Wellman Dynamics for casting. Figure 6 shows one of seventeen crossover cores which were assembled for each crossover housing pour.

Upon the attempt to cast the crossover housing, Wellman found that the Burrows Pattern Works cores were unusable. The long thin crossover inlet necessitated a high percentage of core binder. During the pour, the binder vaporized at the temperatures of molten aluminum, causing blows and cold shuts, ruining the casting. Wellman was forced to make their own cores using alumina sand and glass reinforcing rods running through the center of each core. Figure 7 shows the completed Wellman core assembly. Prior to the first pour by Wellman, the passage cores were dimensionally inspected and were found to meet the tolerance requirements of the drawing. In seven attempts to cast the crossover, only one good crossover housing was produced. Figure 8 shows the diffuser inlet vanes of this crossover housing. Rocketdyne released Wellman of the requirement for two castings, because of the excessive costs required to achieve a useable product.



Figure 7 - Assembled Casting Cores for Crossover Tester by Wellman





Impeller

The crossover tester impeller design, 7R0017930, maintained the critical dimensions of the MK49-F, such as blade geometry, inlet area, exit area, tip width, and shroud contours. However, the MK49-F impeller was machined in two pieces from titanium in the form of a pre-impeller and main impeller. The aluminum alloy 6061-T6 impeller was also designed and fabricated in two pieces, but in the form of a shroudless impeller and a front shroud. The impeller blades and face were numerical control (NC) machined to produce the complicated flow passage. The scaled-up impeller with the front shroud removed can be seen in Figure 9. Once the impeller blades were machined and dimensionally inspected, the front shroud was bonded to the impeller face using a furnace braze process. At the completion of the furnace braze operation, the impeller was machined to final dimensions and is shown in Figure 10.

Inducer

The crossover tester inducer, 7R0017931, was NC machined from aluminum alloy 7075-T73. The inducer blade coordinates, hub contour, and leading edge contours were also scaled directly from the MX49-F inducer using CAD. The crossover tester inducer is shown in Figure 11.

Dynamic Soft Wear Ring Seals

To gain some experience with the soft seal technology, being developed concurrently in task B.5 of this contract, cast in place polyurethane seals were incorporated in the inducer tunnel and the impeller interstage seal. The inducer seal was centrifugally cast by pouring the seal material, Hexcel 3125, in the inducer tunnel, while rotating the part on a lathe for several hours. A similar technique was used to cast the interstage seal in the inner diameter of the crossover housing. The seals were then machined to final bore dimensions after the casting and curing processes were completed. The casting and subsequent machining techniques were very successful. A photograph of the soft seal material in the inducer tunnel, 7R0017944, is shown in Figure 12.

The impeller front wear ring labyrinth seal and thrust disk seal also used soft seal technology and were machined from Kel-F stock. These seals went through several curing cycles before they were machined to their final dimensions. The clearances for the inducer tunnel, interstage seal, and the front wear ring labyrinth seal were also scaled by 2.85 from the MK49-F design, as shown in Table 3.









Diametral C	<u>learance (inch</u>)
Clearance Location	Crossover Tester	MK49-F Turbopump
Impeller Tip	0.710	0.250
Impeller Front Hub Labyrinth	0.023	0.008
Inducer Tip	0.029	0.010
Interstage Seal	0.023	800.0

Table 3 - Operating Clearance ComparisonCrossover Tester vs.MK49-F

Thruat Disk

Hydrodynamic analysis of the test pump showed the potential of large loads with some uncertainty of the load direction due to the lack of definitive pressure profiles around the impeller shrouds. With moderate changes in the effective vortex strengths in these shroud areas, the total net axial force could change direction and magnitude. To better handle this potential load variation the drive end bearing stop was replaced with a belleville spring to accommodate the thrust without unloading. Also, a thrust compensating disk, 7R0017927, as seen in Figure 13, was added to the design. To cross the gap between the volute manifold and the bearing carrier, transfer tubes, 7R0017922, were designed to allow the thrust disk back pressure to be vented through a control valve overboard. By allowing some of the crossover discharge flow to leak past the thrust disk tip seal into the thrust disk drain cavity, the pressure behind the disk could be regulated to produce the desired resultant axial thrust. Blank transfer tubes (no through holes) were also designed to return the manifold to its SSME test condition.

A thermodynamic computer model of the pump was developed to predict the axial load Nor the anticipated test range. The pressure of 461 psia in the thrust disk drain cavity as selected to preclude the direction of the axial thrust at the 80% design flow towards the drive end. This pressure yields a uniform thrust cirection with a maximum amplitude of 3555 tb. toward the pump inlet at 120% design flow as shown in Table 4. Also seen in Table 4, the loads produced at 60 and 70 percent of design flow are larger than at 80 percent because of the predicted stall characteristic of the pump. The axial load in air was considered negligible.



	% of Design Flow Q _d (583 gpm)					
Tester Location	60%	7.0%	80%	100%	110%	120%
Inducer Inlet Pr	94.3	94.3	94.3	94.4	94.3	94.3
Inducer Discharge Pr	163	160	156	141	129	114
Impeller Discharge Pr	558	556	553	541	528	509
Imp Front Shroud Hub Pr	365	362	360	347	335	315
Imp Rear Shroud Hub Pr	529	527	523	512	499	480
Crossover Disch Pr	711	708	741	710	685	649
Thrust Disk Front Pr	724	720	751	718	693	658
Thrust Disk Rear Pr	461	461	461	461	461	461
Axial Thrust (lbf) *	1336	1474	43	1333	2273	3555

Table 4 - Hydrodynamic Performance and Axial Load Predictions Crossover Tester Internal Static Pressures (psia) in Water

Positive Load towards the Pump Inlet.

Ball Bearings and Shaft Support System

In addition to adding the thrust disk, a redesign of the pump bearing system was also required. The original 70mm bore conrad ball bearings, used in the SSME HPFTP tester, could not be used due to the high variations in axial load for the flow ranges to be tested. The maximum axial load capacity calculated for these bearings was 2500 lb. It was therefore necessary to increase the ball bearing axial load capacity. As a result, a pair of 70mm J type angular contact ball bearings were procured to replace the original conrad bearings. Mechanical preloading was used to obtain the appropriate radial stiffness and accommodate axial translation.

DESIGN SUPPORT ANALYSIS

Rotordynamics

In early 1984, the preliminary MK49-F crossover tester design, without the thrust disk, was analyzed to predict the critical speeds, shaft mode shapes, and shaft deflection. The rotating assembly consisted of a single stage inducer and impeller subassembly cantilevered on a shaft supported by two ball bearings. The finite element model of the rotor is shown in Figure 14. The rotor was segmented into 10 weight groups and 25 finite elements. The bearings were represented as translational springs to ground (rigid casing), and the assembly drive coupling shaft was assumed to add weight but no radial stiffness to the system.



MK-49F CROSSOVER TESTER ROTATING ASSEMBLY MODEL CR-194447

The first three critical speeds of the rotor, pumping water and air respectively, are shown in Figures 15 and 16 as a function of bearing stiffness. The mode shapes corresponding to these critical speeds, for a bearing stiffness of 500,000 lb/in., are given in Figure 17. For the tester running in water, the operating speed is 6,322 rpm. Observing the normal rotordynamic practice of not operating within 20% of a critical speed, a first critical speed of at least 7590 rpm is required. According to Figure 15, if the bearings have a minimum stiffness of approximately 440,000 lb/in., the first critical speed would be over 7590 RPM, and the machine could operate safely at 6,322 RPM. The preloaded angular contact ball bearings easily met these radial stiffness requirements.

With air as the pumped fluid, a similar critical speed analysis was conducted with proposed operating speeds of 6,322 rpm and 14,000 rpm. This analysis was required because in the previous analysis, water being pumped adds mass and damping to the rotor system, while air, due to its low density and compressibility, provides less mass and virtually no damping. Again, a 20% margin on critical speeds was maintained and no critical speeds were found between 5,000 and 7,500 rpm and between 11,670 and 17,500 rpm for the predicted bearing stiffnesses, as seen in Figure 16. It was noted for the 14,000 rpm case, that the tester would run between the first and second critical speeds and below twice the first critical speed eliminating the requirement for a rotor stability analysis. The critical speed analysis showed that this machine could operate safely at either of the desired shaft speeds.

Due to the overhung nature of the crossover tester design, an unbalance response analysis was performed to determine the potential rubbing due to rotor deflection. Figure 18 and 19 show the predicted inducer and impeller deflections, respectively, as a function of rotor speed with 500,000 lb/in bearing stiffnesses. At 6,322 rpm, the predicted deflections were significantly less than the radial clearances built into the tester as shown earlier in Table 2. Figures 20 and 21 show similar inducer and impeller deflections, respectively, with air as the pumped fluid, as a function of shaft speed for bearing stiffnesses of 500,000 lb/in. As shown in these figures, large deflections would be incurred if the tester speed dwelled around the first critical speed of 8,000 rpm.

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RI/RD89-111 -27CRITICAL SPEED (RPM)





Figure 18 - Inducer Deflections in Water

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$$K_{\rm B} = 500,000 \, \text{LB/IN}$$

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• Y AXIS • Z AKIS

UNIALANCED RESPONSE OF 1849F DIFFUSING CROSSOVER TESTER 1 GH-IN UNDAL ON IMPELLER. OPERATING IN MATER



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DISPLACEMENT (IN.)
Figure 19 - Impeller Tip Deflections in Water

 $K_{\rm B} = 500,000 \, \text{LB/IN}$

• Y AKIS • Z AKIS

UNINANCED RESPONSE OF HK49F DIFFUSING CROSSOVER TESTER 1 SH-IN UNINL ON INPELLER, OPERATING IN WATER



RPN

Operating Speed

CR-194447

Figure 20 - Inducer Deflections in Air

$$K_{\rm B}$$
 = 500,000 LB/IN

• Y AKIS • Z AKIS

LIGALANCED RESPONSE OF MK49F DIFFUSING CROBBOVER TESTER 1 SM-IN LIGAL ON IMPELLER, OPERATING IN AIR



Operating Speed

RPN

Operating Spe

CR-194447

Figure 21 - Impeller Tip Deflections in Air

$$K_{\rm B} = 500,000 \, \text{LB/IN}$$

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• Y AKIS • Z AKIS

UNIMALANCED RESPONSE OF 19649F DIFFUSING CROSSOVER TESTER 1 GH-IN UNIME, ON INPELLER, OPERATING IN AIR



As discussed earlier, the design for the High Velocity Ratio Diffusing Crossover tester was modified to incorporate the thrust disk, however, this was accomplished after the initial rotordynamic analyses were completed. To determine if this modification would significantly alter the rotordynamic characteristics of the tester, the finite element model of the rotor was updated and its critical speeds, operating in water, were recalculated. Close comparison of this critical speed map with that of the old design showed that the first critical speed was virtually unaffected by the addition of the thrust disk because of its close proximity to the pump end bearing.

Structural Analysis

An analysis of the Crossover Tester assembly was performed for operating conditions of 6322 rpm for water testing and 14500 rpm for air testing, and for a maximum discharge pressure of 1111 psia in water. The analysis covered the major hydrodynamic test components, including the inducer, impeller, inlet, and crossover. In addition, new hardware required by the bearing support system redesign effort, including bearing preload belleville spring sizing and face seal retainer deflections, were analyzed.

Because of the geometric similarity between the tester inducer, impeller and crossover and their counterparts from the MK49-F turbopump, stresses in these tester parts were determined by applying scaling factors to the MK49-F part stresses. Scale factors accounting for differences in tester and turbopump tip speeds, fluid densities, material densities, and static pressures were used as appropriate. Centrifugal stresses in the inducer and impeller were tess than 10% of those in the turbopump. Fluid pressure stresses on the inducer and impeller blades and on the crossover were 38% of those occurring in the turbopump. Although the aluminum alloy, 6061-T6, used on the tester components, has significantly lower strength than the Inconel 718 (inducer), titanium (impeller) and inconel 625 (crossover) used on the turbopump, the tester parts were shown to have higher factors of safety because of the lower loading.

TEST PLAN

Test Matrix

The planned high velocity ratio diffusing crossover tests were divided into four parts; H-Q tests in water, crossover stall mapping in water, suction performance tests in water, and H-Q tests in air. These tests were run to establish the diffusion capability of the crossover passage, as well as, verify the performance and efficiency of the scaled up model of the MK49-F first stage pumping elements. The planned test matrix is shown in Table 5. The yaw probe survey tests described in Table 5 were later deleted f(\bigcirc m the test matrix due to cost and schedule constraints coupled with the fact that these results were not critical to accomplishing the basic objectives of the program. Only in the event of a serious stall in the downcomer would the yaw data become critical.

Test Instrumentation

Instrumentation for the High Velocity Ratio Diffusing Crossover tests consisted of those parameters necessary to determine pressure, temperature, flowrate, speed, torque, and acceleration. In addition, adequate instrumentation was required of the facility to solve conduct the proposed tests and provide the information required for facility diagnostics. The low and high frequency data recorded provided the information necessary to investigate the performance and efficiency of the $\Delta K49$ -F turbopump high velocity ratio diffusing crossover and its pumping elements.

The instrumentation used, including parameter nomenclature, transducer ranges, redline limits, recording device, and parameter displays, for the water test series are shown in Table 6. Redundancy on all critical parameter systems were maintained. Figure 22 shows the locations of the various instrumentation types available on the crossover hardware. The three Kiel probes at the discharge of the crossover are located at three different radial heights: 1/4 passage, mid-height, 3/4 passage, from hub to tip.

The instrumentation used for the air test series are shown in Table 7. The air tests required less instrumentation to obtain the necessary performance information.

All low frequency data was recorded on a Digital Data Acquisition System (DDAS). The DDAS also provides test sequence control and redline monitoring, in addition to recording the low frequency data and facility events.

Some selected parameters were recorded in real-time on strip charts, as seen on the instrumentation lists in Tables 6 and 7, shown previously. During suction performance (cavitation) tests, monitoring of inlet pressure decay rate and pump differenties) pressure, ΔP , were essential to successfully and safely control the test.

Provision was also made in the hardware design for laser velocimeter measurements at the impeller discharge (diffuser inlet). The measurements would have been able to define the blade-to-blade flowfield leaving the impeller at different planes from the tip

]	TEST NO.	3T 7E	TEST FLUID	FLOW (GPM)	TEST DESCRIPTION	SPEED (RPM)	DATA SAMPLING	PROBE TYPE
	1	CHECK OUT	H20	582	ESTAB AXIAL LOAD	6322	20 scans	KIEL
	2	HEAD VOL FLOW	H20	408-694	H-Q W/ PROBE	5528	20 SCANS	KIEL
	3	H-Q STALL NAPPING	N20	233-408	No 60-90X0	6322	20 SCANS	KIEL
	4	CAVITATION	H20	582	NPSH a 100%a	6322	CONTINUOUS	KIEL
	5	GAVITATION	H20	640	NPSH & 110%	6322	CONTINUOUS	KIEL
	6	CAVITATION	H20	698	NPSH a 120Xa	6322	CONTINUOUS	KIEL
	7	CAVITATION	H20	523	NPSH & 90XQ	6322	CONTINUOUS	KIEL
	8	CAVITATION	H20	465	NPSH & BOXA	6322	CONTINUOUS	KIEI.
	9	CAVITATION	H20	407	NPSH 0 7C	6322	CONTINUOUS	KIEL
	10	CAVITATION	H20	349	NPSH & 60XQ	6322	CONTINUOUS	KIEL
	11	PROBE SURVEY POS#1	H20	408-694	NG 70-120XG	6322	20 SCANS	WAY
	12	PROBE SURVEY POSH2	H20	408-694	HQ 70-120XQ	6322	20 scans	WAN
	13	PROSE SURVEY POLIS	H20	408-694	HQ 70-120XQ	6322	20 scans	WAY
	test No.	TEST TYPE	TEST FLUID	FLOW (CFS)	TEST DESCRIPTION	SPEED (RPH)	DATA SAMPLING	PROBE TYPE
	14	HEAD vs. FLOW	AIR	0.91-1.56	H-G W/ PROCE	6322	20 scans	KIEL
	188866							

Table 5 - Crossover Planned Test Matrix

* These tests were later deleted

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Table 6 - Water Test Instrumentation List

PARAMETER	PARAMETER NAME	RANGE	REDLINE	I	DATA RECOR	DING AND DIS	PLAY
NUMBER		PSIG	NIN/MAX	DIGITAL	STRP CHRT	CRT	HF DIGITAL
	23328222222222882338282222	2222222222 73					
1	INLET STATIC PRESS #1	100 PSIA		X	X	1	
2	INLET STATIC PRESS #2	100 PSIA		X	1	1	
3	INDUCER DISCH PRESS #1	0-500		L X	1	l X	1 1
4	INDUCER DISCH PRESS #2	0-500		X	ł	1	1 1
5	INP FRNT SHRD PR #1	0-2000		X	ł	1	
6	IMP FRNT SHRD PR #2	0-1000		X	1	1	
7	REAR SHRD PR #1	0-1000		X	I	1	
8	REAR SHRD PR #2	0-2000		X	l	1	!
9	INP DISCH PR O	0-1000		X	1	ł X	l !
10	INP DISCH PR 45	0-2000		X	I	ł	l l
12	UPC CONST SEC PR #2	0-2000		X	1	l	!!!
13	UPC CONST SEC PR #3	0-2000		X		1	
14	UPC CONST SEC PR #4	0-2000		X	i	l	1
15	TRANSITION PR #1	0-2000		L X	ł	L X	
18	DWN DIFF DISCH PR #2	0-3000		L X	I	ł	
19	DUN MID-DIFFUSR PR #1	0-2000		X	I	1	
20	DUN MID-DIFFUSR PR #1	0-2000	l i	L X	1	ł	
21	XOVR DISCH STATIC	0-2000		X	1	L X	
24	BAL PSTN SHP DRN PR	0-500		X	1	1	
25	INP DISCH TOTAL PR	0-2000		X	1	1	I I
26	TRANSITION TOTAL PR	0-2000	}	X	1	l	1 1
27	XOVR EXIT YOTAL PR #1	0-2000		j X	l X	1	
28	XOVR EXIT TOTAL PR #2	0-2000		X	1	l	
29	XOVR EXIT TOTAL PR #3	0-2000		X	1	1	l 1
* 30	PUNP DELTA-PR	0-3000		X	X	X	
		1	i I		1	ł	1 1
31	WATER INLEY TEMP F	0-100		X	1	1	
34	LUBE OIL OUT TEMP F	0-200		X	1	ł X	1 1
35	THRUST DISK FLOW	0-200		X	1	X	1 1
36	WATER FLOW GPH	0-1284		X	j X	X I	
37	LUBE OIL FLOWRATE GPH	0-4		X	ł	i X	
38	SNAFT SPEED - APN	0-10,000		X	I X	1	I X I
39	TORQUE - IN-LUS	0-20000		X	l	i	
40	RADIAL O ACCEL	0-10 GRHS	5	• .	ł	1	×
41	RADIAL 90 ACCEL	0-10 GRHS	5		1	ł	×
42	AXIAL ACCEL	0-10 GHIS	5		ĺ	1	X
*********		**********	**********	**********		***********	**********

* USE XOVE DISCH TOTAL PR #1 TO INLET STATIC #2 PR FOR DELTA-P





Table 7 - Air Test Instrumentation List

					DATA RECOR	DÌNG AND DIS	PLAY
PARAMETER	PARAMETER NAME	RANGE	REDLINE	1			
NUMBER		PSIG	HIH / MAX	DIGITAL	STRP CHRT	CRT	HF DIGITAL
********	₽¥₽¥₽₽₽₽₽₽₽¥¥₽₽₽₽₽₽₽₩¥₽₽₽₽					*==*==*=*=*=	*********
1	INLET STATIC PRESS #1	0-1		X		1	
2	INLET STATIC PRESS #2	0-1	1	I X	1	!	1 1
3	INDUCER DISCH PRESS #1	0-5	1	X	l	1	1 1
4	INDUCER DISCH PRESS #2	0-5	I	l X	l	1	1 1
5	INP FRNT SHRD PR #1	0-5	l	L X	1	l	1 1
6	REAR SHRD PR #1	0-5	1	X	1	1	
8	INP DISCH PR O	0-5	I	i x	I	l x	1 1
9	UPC CONST SEC PR #2	0-5	1	L X	1	X	1 1
10	UPC CONST SEC PR #3	0-5	l	l X	l I	l	1
11	TRANSITION PR #1	0-5	l	X	1	1 X	1
12	DWN DIFF DISCH PR #2	0-5	l	X	1	l X	1 1
13	DWN CONST SEC PR #2	0-5	1	L X	1	X I	
14	DWN MID-DIFF PR #1	0-5	1	X	1	l x	1 1
15	XOVR DISCH. #1	0-5		X	[X	i x	1 1
17	INLT ORF U/S PR	0-1	I	L X	I X	l X	1 1
18	INLT ORF D/S PR	0-1	l i	I X	l x	X	1 1
19	INP DISCH TOTAL PR	0-5	l	X	1	1	1 1
20	TRANSITION TOTAL PR	0-5	1	l X	1	l	1 1
21	XOVR EXIT TOTAL PR#1	0-5	1	l X	1	I	1 1
22	XOVR EXIT TOTAL PR#2-	0-5		I . X	1	l	1
23	XOVR EXIT TOTAL PR#3	0-5		X	1	1	
• 24	PUNP DELTA-PR	0-5		 X	X	1	
18	INLT ORF DELTA-PR	0-1	1	X	X	X	1 1
25	AIR INLEY TENP F	0-100		l X		1	
26	INLT ORF U/S TEMP	0-100	1	i x	i	Ì	1 1
30	LUBE OIL OUT TEMP F	0-200	- / 150	X	İ		i i
31	LUBE OIL FLOWRATE GPN	0-10	1/-	x	Ì	ĺ	ÌÌ
32	SHAFT SPEED - RPH	0-10,000	t t	l X	l X	l	
33	TORQUE - IN-LES	0-5000		X	İ	Ī	i i
34	RADIAL O ACCEL	0-10 CRHS	5	Ì	i		i x i
35	RADIAL 90 ACCEL	0-10 CRMS	5		i	-	I X I
36	ANIAL ACCEL	0-10 GRMS	5	į	İ	-	I X I

* USE XOVR DISCH TOTAL PR #1 TO INLET STATIC PR #2 FOR PUNP DELTA-P

RI/RD89-111 -39shroud to the rear shroud. Had the diffuser-crossover system shown poor performance, this would permit valuable diagnostic data to be obtained relative to the uniformity of the fluid entering the diffuser. For example, such measurements could potentially differentiate between an impeller stall problem and a diffuser stall problem. A second laser window was designed for the transition section of the diffuser between the upcomer and downcomer diffusers. This too could be valuable for diagnostics to differentiate between stall in the various parts of the diffusing system.

Test Procedures

The first test scheduled for the high velocity ratio diffusing crossover tester was a system check out at 6322 rpm and 100% of design flow (582 gpm). This test, in water, was designed to verify the soundness of the tester assembly, to verify the instrumentation systems, and to determine the pump pressure distributions and axial loads. One major goal of this test was to establish the hydrodynamically produced axial loads, compare them to the current prediction, and modify the thrust disk back pressure to accommodate these loads. A secondary goal was to rotate the total pressure Kiel probes within the flow passages, to align the sensor with the fluid velocity vector. (Kiel probes will measure the total pressure accurately within ± 40 degrees of the mean streamline for velocities ranging from 4 ft/sec to Ma 1 in air)

Following the check out test, the performance tests were to evaluate the diffusing crossover tester by mapping the delivered head as a function of flow. Tests were to be run from 70% to 120% of design flow in 10% increments, while maintaining a constant thrust disk back pressure to ensure the net axial thrust direction would always be towards the inlet. To establish the H-Q map, the tester is brought to the proper inlet conditions and ramped to speed, as stated in the program test plan. By adjusting the pump discharge throttle valve, the tester flowrate was changed to the various set points described by the test plan, and the resulting pump pressure distribution recorded. At each H-Q set point, the data system was allowed to take twenty (20) scans and average the results before continuing to the next point. This method reduced the opportunity for erroneous data.

Once the H-Q map had been determined, the stall region of the crossover was explored. Starting at a nominal flow condition, as determined by the previous test, the flow would be decreased in 2% to 5% flow increments until diffuser stall was clearly defined. Again, the data was recorded at the steady state set points. The flow was then increased in similar increments until the diffuser performance returned to the nominal H-Q map.

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Determining the diffuser stall point, in the decreasing flow direction, and the diffuser reattachment point, in the increasing flow direction, is important for the engine system operating conditions.

The final test series in water were the suction performance tests used to determine the iniet head at which pump discharge head breaks down. These tests were to be run at the 60% to $120\%Q_d$ conditions, in 10% flow increments, in the order described by the test matrix. The suction performance tests were initiated when the desired flow conditions were met. At this point, the inlet pressure was slowly reduced until a minimum 10% breakdown in discharge pressure was observed. Immediately thereafter, the inlet to the tester would be pressurized to the initial conditions. The thrust disk drain valve, during these tests, was to be maintained in a constant position. Data were recorded continuously during the cavitation tests.

The H-Q test in air was designed to verify the tester assembly function, set the total pressure Kiel probe angular positions, verify all instrumentation was operational, and obtain an H-Q curve for the pump from 70% to 120% of design flow, in 10% increments. The H-Q tests in air were conducted similarly to the H-Q tests in water.

Test Facility Description

The test program for the high velocity ratio diffusing crossover was conducted at the Pump Test Facility in Rocketdyne's Canoga Main Building. Both water and air tests were conducted at this facility on the north powerhead. The tester was driven by a 4000 hp reversible, synchronous electric motor. The 1200 rpm output of the motor was increased through a oil lubricated gearbox to 6322 rpm. The water and air tests were remotely conducted from the control center, shown in Figure 23.

The water and air tests were conducted at the 6322 rpm speed to stay well below the first undamped critical speed for this rotating assembly which lies between 8000 and 9400 rpm for the predicted bearing stiffnesses, as shown in the rotordynamic analysis. The air tests were originally going to be run at 14,000 rpm in a separate air test rig, but it was more economical to run the tests on the same rig as the water test. Also, at the lower speed in air the Reynolds number is even further reduced from that in water yielding a stronger contrast to characterize Reynolds number effects.

The water test facility and hardware interface schematic for the high velocity ratio diffusing crossover was configured as shown in Figure 24. The water flowed from the

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8000 gallon tank through the tester and returned to the tank in a recirculation mode. The tank pressurizing and vacuum systems were capable of maintaining a constant pressure at the pump inlet during the head versus flow maps and could also ramp the inlet pressure to less than 5 psia during the suction performance runs.

A hydraulically operated pump discharge valve, using flowrate feedback, was installed downstream of the tester. This valve was used to vary the water flowrate during the H-Q tests and maintain a constant flowrate during the suction performance test series. This valve utilized the flowmeter downstream of the tester to react to the requested changes in the flow conditions. Since the flowmeter was located downstream of the pump, a flowmeter was added to the thrust disk drain system so the actual pumped flow could be measured. Later a flowmeter was placed in the inlet line reduce measurement error created by adding the output of two separate flowmeters (see Figure 24).

A 40 micron (minimum) mesh filter was installed in the inlet duct to protect the hardware from any debris in the facility lines. A 100 micron filter was installed downstream of the hardware to collect any debris which emanated from the tester. The tester bearings were lubricated by a pump-fed 2 gpm oil jet supply and drain system, also provided by the facility. A photograph of the lubrication system and hardware interface is shown in Figure 25.

The air tests were conducted at the same pump position as the water tests. The fluid supply system, however, was significantly different. A six inch diameter pipe, ten feet long, with an eight-inch to six-inch pipe reducer at the entrance was used as the inlet duct to channel the atmospheric air into the inducer. Within the inlet duct, a 2.000 inch diameter orifice was used, in coordination with the upstream pressure and temperature and orifice ΔP , to calculate mass flow. There were no appreciable axial loads predicted for these tests, so the thrust disk back pressure system was plugged. Like the water test, pump flow was controlled using throttiling valve in the pump discharge line. A schematic of the air test facility is shown in Figure 26.

There are two digital data acquisition systems that were used to record and reduce test data at the Pump Test Facility. The system consists of two digital computers forming a multi-user display and data processing system. The test control and data acquisition system for the water test facility consists of an analog-to-digital conversion subsystem tied into the Data General MV4000 computer as seen in Figure 27. The analog subsystem can acquire 128 analog signals, such as pressure, delta pressure, temperature, torque,







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speed, acceleration, flow, and displacement transducer outputs. All analog signals are filtered and sampled within 80 microseconds (1st sample to the 128th sample). While performing test control, the computer simultaneously accepts the digitized data from the analog subsystem and passes the data every 0.1 second to the hard disk storage for post test processing. After all data channels are acquired, the data is converted to specified engineering units and sent to the various display monitors. At the conclusion of the test, the data is transmitted to an Apollo computer format via BLAST software. The data is then further reduced and analyzed by the Rotating Machinery Analysis groups.

For the air test facility, the Pressure System Incorporated (PSI) system was used. The four major components of the PSI system are the Data Acquisition and Control Unit (DACU), Pressure Calibration Unit (PCU), pressure sensor modules, and the system controller. The DACU provides the control and data acquisition functions for the pressure sensor modules. An eight bit microprocessor executing firmware programs controls the DACU. The PCU consists of pneumatic valves and high accuracy quartz pressure transducers. The pressure transducers ranged from 1 psig to 15 psig, with accuracies to 0.5%. Under DACU control, the PCU switches the calibration value within the sensor to calibrate position and then applies a three point pressure calibration to all transducers. The calibration data is then reduced by the DACU. The main purpose of the system controller, an IBM PS/2 Model 80 computer, is to program the DACU and direct data flow within the acquisition system. Additional functions of the computer are data reduction, data display, and permanent data storage. A photograph of the Air test data controller and display are shown in Figure 28. When the test condition is met, the PSI system averages twenty scans of data and stores the data in specified angineering units on a 3.5 Inch floppy diskette. The test information is then anasterred from the data file into a Lotus 1-2-3 spreadsheet where the data is further reduced.

TEST DESCRIPTION

Test Summary

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Tests of the high velocity ratio diffusing crossover were conducted between September 1988 and October 1988. During that period, tests were conducted in air and water for the purpose of obtaining performance data at two Reynolds Numbers and determining the stall and cavitation characteristics of the crossover tester. Since the design of the crossover tester and the MK49-F are geometrically similar, this data can be easily scaled for comparison.



Table 8 prosents a summary of the nine tests actually performed. Test 1, in air, provided a successful check out of the tester mechanical operation and facility systems. Figure 29 shows the crossover tester installed in the air test configuration at the Pump Test Facility. Test 2 was repeated the set points of Test 1 while rotating the Kiel probes to find the maximum total pressure. No effects were observed. Typical facility start up and mechanical problems occurred in tests 3, 5, 6, and 7 primarily related to the balance pressure drum operation which had not been used before in this facility and the tests vacuum system operation required for the suction performance test. The only instrumantation test during the tests was the Kiel probe at the impeller discharge which fueld early in Test , however, some good H-Q data were still achieved. This Kiel probe to logated in a region of Large dynamic variations due to the normal blade-to-blade "howfield in the rotating impeller and is likely to have experienced a high-cycle fatigue failure.

Saple	8	•	High	Velocity	Ratio	Diffusing	Crossover	Test	Summary
-------	---	---	------	----------	-------	-----------	-----------	------	---------

Test	Test Number	Test Fluid	Test Objectives	Comments
1	•	Air	Check Out & HQ	Objectives Achleved
	•	Air	HQ with Klel Probe	Objectives Achieved
3	T88A092	Water	Check Out @ 100 Qd	Test Cut - Redline
-	T88AD93	Water	Check Out @ 100% Qd	Objectives Achieved
5	788 A094	Water	HQ and Stall Map	Facility Issue
P	T881095	Wøter	Detailed Mapping	Facility Issue
7	785 4094	Water	Suction Performance	Limited Data Achieved
u	T88A097	Water	HQ & Stall Mapping	Objectives Achieved
S.	TBJÅØØ()	Water	Suction Performance	Redline Cut. Data Achlaved - Tester Failed

Was very successful and several H-Q points were achieved, diffuser stail was moded, and some stabiling performance tests completed. In Test 8, the remaining suction which manoe della points were completed. Test 8, however, was terminated prematurely in the realise mutoit. At the line of cutoff, the cavitation test at 80% design flow have just here completed and the inter line was being re-pressurized. During the automatic, shumehower sequence, the one-inch diameter quill shaft failed. Tester the managed is the pump end bearing had failed and the impeller front shroud have push sequence. Post test analysis of the pressure parameters



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indicated that the axial thrust of the pump had dramatically changed due to shifting pressures caused by the deep cavitation in the pump. Figure 30 shows the axial loads calculated for the test where the failure occurred. With the pressures changing so rapidly, the accuracy of calculating this load is in question because it is obtained by vector addition of large forces which yield a relatively small residual. However, the trend is certainly correct. As can be seen from the Figure 30, the thrust suddenly changed direction at the end of the test by a magnitude of over 6,000 lb. resulting in an unloaded pump end ball bearing. Subsequent pressurization of the inlet and recovery from cavitation would then force the bearing back into a highly loaded condition which caused the bearing failure.

Hardware Disassembly

At the conclusion of the final test, the high velocity ratio diffusing crossover tester was disassembled and the condition of the major components documented. Two major observations were noted. First, there was significant rubbing on all the close radial clearance locations, and second, the shaft had translated axially toward the inlet sufficiently enough to rub the impeller.

When the axial load reversed during the 90% and 80% Qd cavitation tests, the pump end bearing was unloaded, providing no radial support to the shaft. The rotor proceeded to whirl with amplitudes sufficient enough to cause the rotor to rub in the soft seal areas. Most of the damage incurred was at the inducer/tunnel, impeller hub/interstage seal, and thrust disk/seal interfaces.

The inducer tunnel and interstage seals were made with Hexcel 3125 polyurethane as described earlier. The interstage seal was badly damaged, including large cracks and significant material loss. However, there was no damage found on the inside diameter of the crossover housing. The rubbing velocity at the interstage seal was approximately 110 feet per second.

The inducer tip seal was moderately damaged. The inducer tip seal showed scratches from rubbing of the aluminum inducer blades, as well as pitting caused by the deep cavitation. Some minor damage to the inducer blade tips were also noted, but were considered superficial and easily repairable. The rubbing velocity at the inducer tip seal was approximately 154 feet per second.



RI/AD89-111 -53Further investigation into the survivability of Hexcel 3125 as a soft seal material is required to fully evaluate the findings of the post test disassembly. The condition of these seals were documented for the data base being compiled under the Soft Wear Ring Seal Technology Program, Task B.5.

The thrust disk, made from A-286, also rubbed the Kel-F thrust disk seal during the bearing unloading. The wear track in the Kel-F was not uncommon for this seal/rotor combination. Some heat generation was noted on the disk tip. The rubbing velocity in this location was approximately 235 feet per second.

The soft seal materials, though heavily damaged, were very successful. One of the main goals of this type of seal is to tolerate rubbing without damaging the rotor or stationary housings. In each case, the seals were worn, but did not cause severe damage to the rotating part or the soft seal retainer system. This was important because if significant rubbing were observed in an actual turbopump, only the soft seal material would have to be replaced and not the expensive rotor or seal retainer parts. This was evident in the interstage seal area. If a metallic seal would have been used in this application (and not uncommon) the impeller and the crossover as well as the soft seal would have to be replaced. During the crossover tests, however, neither the impeller hub nor crossover were damaged.

The axial rubbing damage caused by the axial translation of the shaft was much more severe than the radial rubbing damage. Some of the damaged parts included the impeller, front shroud carbon face seal, bearing sleeve, and labyrinth seal retainer.

The axial travel that was witnessed during the failure was over .025 inch towards the inlet. This was caused when the axial load returned towards the inlet after unloading the bearing during the 80% Qd test. When the thrust reversed the bearing seized, and the power of the motor kept turning the tester shaft. The tester shaft rotated inside the inner ring of the failed bearing heating the shaft sleeve and bearing area. With the 3,000 lb. load towards the inlet the high frictional heating in this area, the sleeve between the bearings started to deform allowing the shaft to travel until the impeller shroud started to rub on the pump and housing. At some point, the torque from the rubbing of the shaft and impeller was enough to shear the quill shaft. Excessive damage was incurred to the front shroud of the impeller, tester shaft and bearing separator sleeve. A list documenting the current damage status of the tester parts and the action required to fix the tester are shown in Table 9.

RI/RD89-111 -54TABLE 9: CROSSOVER TESTER POST TEST PARTS STATUS

PART NO.	DESCRIPTION	DAMAGE	ACTION	(N)EW (R)EWORK (U)SE AS IS
7R0017923-3	INLET HOUSING	Rub at Seal Retainer	Clean Up with Lathe	er
7R0017924	COVER	None	None	Э
7R0017925	CROSSOVER	Interstage Seal Worn	Replace Interstage Seal	ű
7R0017927	THRUST DISK	Tp Rub	None	Э
7R0017928-1	THRUST DISK SEAL	Seal Worm	Replace Seal	Z
7R0017930-3	IMPELLER	Tip Rub, Front Shroud Rub	Remove Stroud & Braze New	æ
7R0017331-3	INDUCER	Blade Tip Rub	Sharpen Plade Tips	œ
7R0017940-3	IMP LABY SEAL	None	None	Э
7R0017940-5	LABY RETAINER	Severely Rubbed by Impeller	Replace Retainer	z
7R0017944-1	INLET TUNNEL	Minor Rubbing/Cavitation Damage	Replace Seal	œ
T-5100073-120	FACE SEAL	Nomally Wom	None	Þ
T-5100073-501	BEARING SPACER	Severely Damaged	Replace Sleave	z
SKF 7214	BALL BEARINGS	One Failure/One Good Condition	Replace (buy 2 minimum)	z
EWR3072086-007	VOLUTE MANIFOLD	None	None	Þ
EWR306802-003	SHAFT	Severe Pubbing from Bearing	Grind, Plate, Grind	œ
EWR305803-003	BEARING CARRIER	Bore Scratches from Bearing	Polish Bore	œ
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TEST DATA ANALYSIS

Data from the two air tests and four of the seven water tests were compiled to determine the performance of the crossover tester. The tester performance was analyzed to review the crossover as well as the pumping element performance (inducer and impeller). In this section, the crossover test results of head and efficiency, axial thrust, critical NPSH, and crossover pressure recovery will be discussed and compared with the analytical models used to design this tester and the MK49-F LH₂ turbopump. Data from the MK49-F turbopump tests conducted in 1986 will also be compared with these results. The raw data for the Air Tests 1 and 2 can be found in Appendix A and the water test data from tests T88a094, T88a096, and T88a097 can be seen in Appendix B.

Stage Head and Efficiency versus Flow Results

The overall stage head was determined using the crossover exit total pressure measurements and the calculated inlet total pressure where the latter was based on the measured static pressure and the calculated velocity head from the measured flowrate. At the crossover exit, three total pressures were measured at different radii representing the V4, V2, and 3/4 blade height positions. These three total pressures were in excellent agreement as can be seen in Figure 31 (notice the suppressed zero to expand the scale). This was the expected result and shows that the crossover exit flow was relatively uniform hub-to-tip as designed. If there had been a significant separation at the hub or tip, a variation in total pressure would have been seen.

Data from two water tests (T88A094 and 096) were combined in Figure 32 to show the stage head-flow relationship for the water test in comparison with the predicted head. The predicted head was calculated using Rocketdyne's Loss Isolation Program for centrifugal pumps with the actual dimensions and fluid properties for the water test configuration. This program accounts for the Reynolds number change for the test set up versus that for hydrogen testing of the MK49-F. The comparison between measured and predicted values was good, with the measured values of head being approximately 4 percent low at the design flow (Qd). Tests of the 3-stage MK49-F hydrogen pump had also shown the head low by about 8.0 percent. With a known overboard seal teakage problem partially contributing to the low head, a direct comparison of the tester and the MK49-F turbopump could not be made. Based on the water data, however, it appears that the stage performance of the hydrodynamic design was slightly lower than predicted. Figure 32 also shows the stall characteristic. The analysis had predicted the stall to occur at approximately 80 percent of design flow with a rather moderate decrease in head. The Loss Isolation program only predicts stall due to leading edge flow angle





mismatch. The water test data shows that the stall initiates at approximately 76% Q_d while the flow was decreased. While increasing the flow, the stalled condition persisted until approximately 100% Q_d . This is known as the stall hysteresis effect.

The stall hysteresis phenomena could have important implications in the engine start sequence. For example, if the pump operated at a low Q/N (flow-speed ratio) during the start transient and the diffuser stalled, then the pump may remain in the stalled condition if the pump operated at a Q/N lower than 100%. This scenario is being reviewed for the MK49-F turbopump performance issues on the Integrated Component Evaluator (ICE) completed under Task F.4 of this contract.

The total head loss due to the stall was not severe and was only approximately 9% lower than the predicted head at 70% Q_d in the "unstalled" condition. This low head loss is characteristic of leading edge type stall in a centrifugal pump.

To determine the pump stage efficiency, the power absorbed by the rotating axial thrust balance disk was subtracted from the measured power (torque and speed) to arrive at the pump absorbed pump power. The thrust balance disk power was calculated using the Daily and Nece friction coefficients (Ref. 1). Figure 33 shows the resulting pump efficiency for the water test as a function of flow and compares it with predicted values. Near design flow, the efficiency was approximately 3 percentage points lower than predicted. The lower calculated efficiency was due in part to the accuracy of the calculated and measured power terms. The general shape of the curve again agrees well with prediction. As was the case with the head characteristic, the measured stall initiated later than the predicted stall.

The effect of Reynolds No. on head was larger than expected. Figure 34 shows the headflow relationship for the stage from the air test, again comparing the measured to predicted values. The measured head near 100% Qd was about 18 percent lower than predicted even though the predicted curve in air was 18 percent less than the prediction in water. Also, note that the air data does not show any stall characteristic in the curve. Data to be presented below will actually show that the diffuser was stalled over the full range of flow for the air test, so that the head characteristic in the data presented was the stalled head.

The stage efficiency could not be determined from the air test because of the low power absorption compared to the system tare torque. Table 10 presents the predicted and



Figure 33 - Tester Stage Efficiency in Water Test Versus Predicted ¥

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Figure 34 - Tester Stage Static Head in Air Test Versus Predicted

Table 10 - Head & Efficiency versus Flow - Air, Water,and LH2 Measured & Predicted

-		D	licer		-	nducer	+ [mpall	91	Stag	e - Ind+	Imp+Xo	/er
••••••••••••••••••••••••••••••••••••••	Static H	(ii) bee	Effic	lency	Static H	ead (ft)	Effic	lency	Static H	lead (ft)	Effic	lency
	Pred	Meas	Pred	Meas	Pred	Meas	Pred	Meas	Pred	Meas	Pred	Meas
Crossover Tester (Water)	100 1	5	78%	•	1037	1074	91.3%	•	1461	1420	56.5%	55.4%
Crossover Tester (Air)	8	8	*	4	8	1065	85.0%	•	1203	1011	45.7%	1
MK49-F Turborump in LI & at 60,000 rpm	1362	1235	4	•	11693	12029	92.9%	•	16882	15768	69.7%	•

measured head and efficiency of the crossover tester in water and air with those data available from the MK49-F turbopump testing.

Internal Pressure Distributions

With the numerous internal pressures used in the test, the performance of indivicuum components of the pump was estimated.

For the air test, the total pressure at the impeller discharge was measured using a sine f. Kiel probe. Using this, the total head across the inducer-impeller combination we be determined. The measured hoad was actually slightly higher than the predicted. The results are shown in Figure 35. This was consistent with the observations of stage head efficiency reported above. The water data had shown the head closer percentage-will to the prediction than the efficiency. This could be obtained if the impeller head were higher than predicted, and the losses in the diffusion system were higher than predicte. The two effects tend to cancel each other in the stage head but the higher losses show a direct effect on the efficiency.

Another interesting feature in Figure 35 was the difference between the two air tests. The first air test was started at a lower Q/N which apparently put the impeller interstall, and due to hysteresis the impeller did not come out of stall until approximately Qd was achieved. Once out of stall, the flow could be decreased to 70% Qd without initiating stall. On the second air test, the pump was started at a higher flow but still began in an apparent stalled condition but, even more surprising, never got out of the "stalled" condition. This behavior has not been explained. The stage head characteristic in air did not show the same trends from test one to test two. In Figure 34, the two tests were shown to give about the same head value, and in fact, the data for the second test was higher than for the first test. With severe stall in the diffuser system, the stage performance results are not necessarily expected to be consistent.

Figures 36 and 37 show the static-to-static pressure rise across the inducer-impeller for the air and water, respectively. The air data (Figure 36) shows the same general features as the total head curve, but the difference between measured and predicted was much higher for the static rise. This was possible if there was some diffusion in the vaneless space due to the difference in radial position between the impeller diameter and the sensing port diameter. For the water data, the prediction and measurement are closer but the measured value was still higher. Note that for the water, the predicted



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Figure 36 - Inducer + Impeller Static Head in Air Test Versus Predicted



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static pressure was actually 14 percent higher than for air, but the measured values are essentially the same.

Figure 38 shows the static-to-static pressure rise across the inducer only for both air and water tests. Again, the second air test gave lower results. This could be indicative of inducer "stall" in the second test which would have aggravated the impeller stall. However, it was still not clear why the inducer would not come out of stall at the higher flows. The water data agreed with the data from the first air test. The air test data did not show a definitive stall, although there was some indication of hysteresis between 65% and 75% Qd. The predicted inducer discharge static pressure was close to the measured value for the air test at the design flow using the Loss Isolation Program. The predicted inducer discharge static pressure, for the water tests, was slightly higher.

To show the diffuser performance, plots of static-to-static head rise from pump inlet through crossover exit were prepared showing the intermediate stations through the diffuser-crossover system. The water test data pressure distribution at various flowrates are shown in Figure 39. The measurement stations (1 through 9) are delineated on the cross section of the pump in Figure 40. Note the significant increase in static pressure from station 3 to 4. This figure clearly shows the majority of the diffusion occurring in the upcomer diffuser. In the transition and the downcomer diffuser, little diffusion can be achieved because the boundary layers are already large before entering these sections. Figure 39 also shows the stall occurring in the upcomer diffuser at the 70% Q_d flow. Note that the pressure at station 3 (Impeller exit) was still high at this flow but the pressure at station 4 decreases.

The two air tests gave similar results so only those of the second air test were shown in Figure 41. The majority of the diffusion should be occurring in the upcomer diffuser, station 3 to station 4, as was seen in the water test data. The static pressure, however, for most flows significantly decreases from stations 3 to 4. Thus, the inlet to the upcomer diffuser was the point of initiation of the stall. The diffusion system never recovers from this stall. The stall was caused by increased boundary layer blockage due to a low Reynolds number. This effect resulted in an impeller discharge flow which entered the diffuser at a velocity and angle which would produce flow separation at the leading edge.


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Single Stage Scaled-Up MARK49F



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Figure 38 - Inducer Static Head in Water and Air Test Versus Predicted

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σ i i :1 IMP 0.0. - 11.124 IN. N - 6322 RPM DD - 583 GPM TEST FLUID - WATER Ø r MEASUREMENT STATION (REF FIG. G Scaled-Up MARK49F Single Stage ŝ n N ŧ 1 ł l 1.50 1.40 1.30 1.20 1.10 0.50 1.00 0.90 0.80 0.70 0.60 0.40 0.30 0.00 0.20 0.10 STATIC HEAD (FT) RI/RD89-111

Figure 39 - Static Head vs. Tester Location in Water

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Figure 41 - Static Head vs. Tester Location in Air

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Pump Suction Performance

Suction performance data were obtained from 80% to 124% Q_d at approximately 10% Q_d increments. It was during the 80% Q_d flow test when the tester bearing failure occurred. By this point in the test program all flow conditions had been tested. Some data points, including the design flow point, would have been repeated because less than 3% head loss was seen. However, enough data existed to project reasonable estimates of the suction performance for all flows.

The test data were typically reduced by plotting stage head as a function of NPSH (Net Positive Suction Head) for each constant flow condition. Flow was held constant during these test via the pump discharge throttle valve. Typical results were shown in Figure 42 through 50, beginning at 80% and increasing to 124% Q_d .

At the lower flows, the head was seen to hold relatively constant and drop sharply once cavitation effects were seen. Figure 43, at 87% Q_d , shows a very interesting characteristic in that the head drops noticeably into stall as the NPSH was decreased. It can be said that the ensuing cavitation phenomena was a sufficient disturbance to drop the head to the lower level of the stall hysteresis characteristic.

As mentioned, in Figure 44 and 45, the tests were terminated before significant head loss occurred. The resulting suction specific speed values could not be accurately determined. Unfortunately, the failure occurred before these key points could be repeated.

As the flow was increased, the head was seen to drop at a higher NPSH, as expected. However, head loss was less severe before eventually dropping into super-cavitation, as seen Figures 46 through 50, which was indicative of the inception of impeller stall. This phenomena has been seen in other centrifugal pumps like Rocketdyne's MK29-F (used on the J2S Engine). Inducer performance was seen to be lower than expected and may have also contributed to this situation.

Using the Head versus NPSH data, suction specific speed curves were generated to compare with the design predicted value. These curves are given in Figure 51 for 3, 5, and 10 percent head fall off. Suction specific speed was defined as:

Suction Specific Speed =
$$N_{40} = \frac{NYQ}{(NPSH)^{75}}$$
 (1)









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I-I SINGE HEAD, FEET

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Single Stage

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Figure 45 - Suction Performance Test at 101%Od



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I-I STAGE HEAD, FEET

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Figure 46 - Suction Performance Test at 108% Od





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Figure 48 - Suction Performance Test at 116%Qd

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Figure 49 - Suction Performance Test at 119%Qd

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Stage

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where the parameters were speed (N) in rpm, flow (Q) in gpm, and NPSH in feet. Also shown in the figure was the predicted ideal capability at 3% head fall off based on the design flow coefficient and inlet hub/tip diameter ratio of the inducer. The ideal suction specific speed in water without thermodynamic suppression head (TSH) benefit was nearly 29,000. The suction specific speed calculated from the water data was only about 18,000. The low Nss could have been caused by several factors: (1) leading edge of inducer not fabricated to print, particularly with regard to thickness, (2) tip clearance of the inducer and leading edge thickness too large, (3) large hub-to-tip diameter ratio of the inducer, or (4) design deficiency. The latter does not appear to be the problem based on review of the hydrodynamic design. With the size of the MK49-F inducer being so small, the parameters typically controlled for good suction performance could not be scaled down. Consequently, the inducer tip clearance and leading edge radii, used in this tester, when scaled up from the small MK49-F, were larger than the ideal dimensions used on a turbopump of similar size. By scaling up these dimensions, suction performance would be reduced from the ideal case, hence the lower performance found during the tests.

It should be noted that the results of Figure 51 were for a single stage and with no TSH benefit. For a 3-stage pump in hydrogen the results would be much better. For example, 10 percent head loss on the first stage would represent only about 3 percent over all for the 3-stage design. The 10% head fall off curve was not defined in Figure 51 at design flow but the suction specific speed (N_{SS}) could easily reach 25,000. With added TSH benefits, the suction specific speed capability in hydrogen could be much higher than 30,000.

At the time the MK49-F was designed, the required suction specific speed was only 10,000 at design flow. This value was exceeded even in water for a single stage. Thus, the operating requirements would be met even though the performance was down from the predicted potential at the design flow coefficient.

Using the inducer and impeller discharge static pressures, the relative performance of the inducer and impeller can be distinguished over the flow and NPSH range tested. Figure 52 shows the inducer static pressure head rise above inlet total at 87% Q_d, and Figure 53 shows the corresponding static pressure head differential across the impeller. Obviously, at this flow the inducer was determining the suction performance of the stage while the impeller continues to generate the static pressure head until the inducer performance drops. In Figure 53, note the very interesting result of the stall that was

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also seen to occur at an NPSH of approximately 140 ft. in Figure 43. Although the impeller experienced a significant discharge pressure oscillation during pump stall, it did not lose head, showing that the pump stall occurred in the diffuser. The static pressure head was actually varying by 250 feet, peak-peak. With a stage head rise of only 1400 feet this was a peak-peak variation of over 15 percent of the stage head. Operation under such a large dynamic oscillation would not be recommended.

In contrast to Figure 52 and 53, Figure 54 and 55 present the same two parameters at 109% Q_d . At this flow the impeller can be seen to slowly lose static pressure head as NPSH was decreased even though the inducer static head remains the same. As the inducer head decays the effect was also seen in the impeller, but the impeller began losing head earlier. Even at this flow however, the super-cavitation point was determined by the inducer, not the impeller. This was, of course, typical. At higher flows, the impeller suction performance was most critical while at design flow and below, the inducer determined the suction performance.

Shroud Vortex Strength

Static pressure measurements were made on the front and rear shroud of the impeller to permit evaluation of the vortex strength in these regions. The pressure distribution on these shrouds, which are strongly affected by these vortices, determine both the axial thrust and the shroud leakage rates. Data from the water tests was used to establish the front and rear shroud pressure distributions. Figure 56 presents an illustration of the impeller shroud pressure distributions and the direction of leakage flow.

The front shroud flow enters from the impeller outer diameter and down the shroud cavity to the impeller labyrinth seal. This leakage combine with the inducer discharge flow before re-entering the impeller eye. Because the front shroud flow enters at the impeller tip, the fluid already has a strong tangential velocity. According to the Loss Isolation program results, the fluid tangential velocity to impeller tip velocity ratio, defined as Cu/Ut, at the design flow is 0.63. This velocity ratio varies from 0.67 to 0.61 at the 80% to 120% design flow, respectively. Since the impeller discharge static pressure was measured 0.213 inch radially outboard from the impeller outside diameter, the static pressure at the impeller tip was calculated, using the velocity ratio and assuming no total pressure loss per the following;

$$P_{tp} = P_{tases} + \frac{1}{2g} C \frac{\Gamma_{tp}}{\Gamma_{meas}} + 1$$
 (2)



Figure 54 - Inducer Static Head Loss at $Q/Q_d = 109\%$

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The effective ratio of fluid to wheel velocity, K, in the front shroud region was determined from the relationship,

$$\Delta P = \frac{\rho K^2 N^2 (d_2^2 \cdot d_1^2)}{144 (2g) (229.2)^2}$$
(3)

where ρ was the specific weight in pounds per cubic feet, g was acceleration due to gravity (ft/sec²), N was the shaft speed in rpm, d₂ and d₁ (in inches) are the diameters at the pressures measurements (d₂ being at the impeller tip) and ΔP was the differential pressure in psi from d₂ to d₁. The constants in the denominator were used for engineering unit conversion. A predicted front shroud velocity ratio, K_{fs}, of 0.7 was selected based on the high tangential velocity entering the cavity and from turbopump data with similar geometries, such as the SSME HPFTP. As seen in Table 11, the measured values of K_{fs}, ranged from 0.72 to 0.68 from 80% to 120%Q_d, respectively, and were in excellent agreement with this prediction. Because of the higher than predicted impeller discharge pressure at 80% and 100%Q_d, a modest increase in axial thrust, 824 and 808 pounds, respectively, was calculated.

For the impeller rear shroud, the flow field was very different. In this case, the flow originates from the crossover exit with very low tangential velocity, flows through the interstage seal, and up the rear face of the impeller. Analysis had predicted the K value on this face to be as low as 0.23 due to the low entering velocity. The test data showed, however showed that the rear shroud velocity ratio, K_{rs} , to be between 0.36 to 0.33. The higher value may have been due to a higher than expected angular velocity exiting the interstage seal.

If the flow were low, a value close to 0.5 would be expected (this being the average value for a rotating flat disk in a stationary housing with no through-flow). A higher K_{rs} would tend to reduce the axial force on this face, as seen in the 100% and 120%Q_d calculations, where a reduction of 694 and 1626 lbf, respectively, was seen. At the low flow condition, 80%Q_d, the higher than predicted impeller discharge pressure overwhelmed the influence of K_{rs} on axial thrust, and therefore, a slightly higher value (340 lbf) was calculated. The K factor information generated will be used to recalculate the axial loads of the MK49-F turbopump. Table 11 - Shroud Vortex Strength - Predicted versus Measured

High Velocity Ratio Crossover Tester Pump Parameters	Predicted 80%	Measured 80%	Predicted 100%	Measured 100%	Predicted 120%	Measured 120%
Impeller Discharge Tap Pr (psia)	•	591	٠	571	•	521
impeller Tip Press * (psia)	549	567	536	550	504	501
imp Front Shroud Pr (psia)	•	475	•	462	t	417
Imp Frnt Shrd Hub Pr. (psla)	355	364	. 343	356	311	316
impeller Rear Shrd Pr (psia)	•	548	•	526	ŀ	481
Imp Rear Shid Hub Pr. (psia)	520	510	507	478	475	440
imp Front Shroud K factor, Kis	0.70	0.72	0.70	0.70	0.70	0.68
Front Shroud Axial Force (Ibf)	27,409	28,233	26,663	27,471	24,718	24,765
A Fint Shid Axial Force (Ibf)	ŧ	824	٩	808	•	47
Imp Rear Shroud K factor, Krs	0.23	0.32	0.23	0.36	0.23	0.33
Rear Shroud Axial Force (b)	45,224	45,564	44,183	43,489	41,467	39,841
A Rear Shrd Axial Force (101)	•	340	٠	-694	•	-1,626
Net Ax Thrust Toward Inlet (Ibf)	17,815	17,331	17,519	16,017	16,749	15,076

Imp Tip pressure calculated from measured Imp discharge pressure assuming rCu constant. · · Hub Pressures calculated using measured K Factors

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(See Figure 22 for Pressure Tap Locations)

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Diffuser Crossover System Design Verification

The diffuser-crossover system plays an important part in the operation of a high efficiency multistage pump. The diffuser and crossover (DC) system consists of a vaneless space upstream of two straight mean line diffusers with a constant area turning channel in between, Figure 57.

The vaneless space was necessary for the suppression of pressure and velocity perturbations from the impeller blade wakes. These perturbations cause local variations in the diffuser inlet flow angle resulting in dynamic loads on the leading edges of the diffuser vanes. The gap size was restricted since increasing the gap size above the minimum necessary will reduce efficiency and increase diameter and weight.

Design of the first diffuser of the DC system, the upcomer, requires one of the most critical calculations in diffuser design: the calculation of the effective blockage at the diffuser throat. This calculation requires estimation of the boundary layer growth up to the throat in the following regions:

- 1) Along the side walls in the vaneless space
- 2) Along the side walls in the diffuser inlet region represented by the triangular section DEF (Figure 58)
- 3) Along the vane suction surface (line DE in Figure 58)

The boundary layer displacement thicknesses were simply added to arrive at a total area blockage at the throat. The blockage formula can be stated as:

$$\frac{BlG_{4*}2\delta_{SW}+\delta_{44}}{b_4}$$

and represented in Figure 58. Note that eq. (4) double counts the boundary layer blockage in the corners, which tends to overestimate blockage, but this was assumed to partially account for 3-D boundary layer interaction effects not represented in the simple 1-D displacement thickness calculations. Coincidentally, double counting the boundary layer blockage in the corners may compensate for the actual metallic blockage due to corner radii or fillets.



Figure 57 - Diffusing Crossover System





Determination of the throat blockage has been correlated with the pressure recovery from the diffuser inlet to the throat (Ref. 2, 3):

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$$\frac{\Delta P}{q_3} = \frac{(P_4 - P_3)}{q_3} \tag{5}$$

where P_3 and P_4 were the static pressures at diffuser inlet and throat and q_3 was the inlet dynamic pressure defined as:

$$q_{\beta} = \frac{1}{2}\rho C_{3}^{2}$$
 (6)

where C₃ was the diffuser inlet flow velocity. Figure 59 shows the correlation plotted at various inlet blade angles, α . As expected, the smaller the blade angle the larger the blockage due to the increased length of the fluid path to the diffuser throat. Since these curves were developed for a Reynolds number of 1×10^5 , a correction for significant variation in the Reynolds number was derived:

$$CR = 10 Re^{-0.2}$$
 (Ref. 2) (7)

The blockage was read from the curves in Figure 59 and multiplied by CR to determine the effective throat blockage. This blockage was then used to determine the pressure recovery of the dilfuser channel from the 2-D diffuser performance Cp maps; an example of which was given in Figure 60.

The diffuser pressure recovery can be defined in various ways. The pressure recovery as defined by the diffuser maps described above was:

$$\mathbf{C}_{p} = \frac{2(\mathbf{P}_{d} - \mathbf{P}_{l})}{\mathbf{p}\mathbf{C}^{2}} \tag{8}$$

where $P_d - P_t$ was the static pressure difference between the diffuser discharge and the diffuser throat and C_t was the velocity at the throat including any throat flow blockage due to the boundary layers. Since the blockage was not known, a priory in this case, an alternate form of the pressure recovery factor was defined by not including the blockage

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Figure 59 - Curve Fits of Blockage Factor for Diffuser Angles (Ref. 3)



RI/RD89-111 -95in the velocity term:

$$C_{p} = \frac{2(P_{d} - P_{1})}{\rho C_{t}^{2}}$$
(9)

where P_d and P_1 were the static pressure at the inlet and discharge to the diffuser and C_t was the mean velocity in the diffuser throat calculated only from the flowrate and the diffuser throat area. It was felt that this coefficient was the most representative to compare the analysis calculations to the data results because it allowed direct comparison between experimental and analytical results. The original design criteria was for no diffusion between the inlet and the throat of the upcomer. The test results were compared to this analysis and then the required throat blockage and leading edge suction surface diffusion required to match the test data were calculated. Similarly for the downcomer the pressure recovery was predicted analytically and then the throat blockage was calculated from the measured pressure recovery.

Data analysis for the upcomer involved using the same techniques as those utilized during the design analysis, but using the data results to calculate the amount of inlet blockage and the diffusion occurring in the inlet section of the diffuser. The analysis required iteration of the inlet pressure recovery, $\Delta P/q_3$, to determine the blockage from Figure 58 This blockage was then used to determine the predicted throat velocity for calculation of the throat Reynolds number defined as:

$$R_{\theta} = \frac{C_{i}W_{1}}{\upsilon}$$
(10)

where C₁ was the throat velocity including the predicted blockage, W₁ was the throat width, and v was the kinematic viscosity. The blockage term as determined from Figure 58 was then corrected for Reynolds number using the correlation previously determined in eq. (3). This value of blockage was then used to find the L/8^{*}, where L was the effective diffuser channel length from throat to discharge and 8^{*} was an effective blockage determined from the Reynolds number corrected blockage. This term was necessary for the determination of the diffuser pressure recovery from Figure 60. The obtained Cp can easily be transformed to a mean pressure recovery, $\overline{C_9}$, by adjusting the throat velocity in the denominator by the predicted blockage. The inlet pressure recovery term was then converted to a common denominator by multiplying by the ratio of the throat dynamic pressure,

$$q_t = \frac{1}{2}\rho \overline{G}_t^2 \tag{11}$$

to the inlet dynamic pressure, q_3 . This ratio was determined by assuming a "lossless" core flow in the diffuser inlet section. This is an often used assumption for 2-D diffuser analysis and assumes that the boundary layers do not merge. The q_3/q_1 ratio was:

$$\frac{\mathbf{q}_{3}}{\mathbf{q}_{t}} = \left(1 - \frac{\Delta P}{\mathbf{q}_{3}}\right)^{-1} \tag{12}$$

The Cp calculated from the data can be compared to the analysis Cp,

$$\overline{C}_{p} = \frac{C_{p}}{(1 - BLG_{4})^{2}} + \left(\frac{\Delta P}{q_{3}}\right) \frac{q_{3}}{q_{4}}$$
(13)

The analysis was then completed by iterating on the inlet pressure recovery until the data and analysis mean pressure recoveries were matched. From this analysis, it was possible to obtain a good estimate of the actual throat blockage.

Data was available in three test mediums: hydrogen, water and air. One speed was selected from the hydrogen turbopump tests (60K rpm) giving data at three Reynolds numbers. As will be shown, the data predicted that the diffuser was stalled in air, allowing the diffuser performance predictions to be verified at two Reynolds numbers and the stall prediction to be checked for the third.

Hydrogen test data of the complete turbopump showed that the upcomer had a mean pressure recovery, $\overline{C_P}$, of 0.749 at 60,000 rpm. Design analysis predicted a $\overline{C_P}$ of 0.684 and a throat blockage of 8%. Analysis of the data indicated that diffusion had occurred in the diffuser inlet. The analysis showed that the inlet $\Delta P/q_3$ was 9.07 and the throat blockage 10.8% to match the test data $\overline{C_P}$. This analysis of the design was confirmed by comparing the inlet velocity of the analysis to that which was predicted by Rocketdyne's Loss Isolation program for centrifugal impeller design. The velocities were very close: 620.7 ft/sec from the data analysis and 619.7 ft/sec from the Loss Isolation program. The amount of diffusion represented by the $\Delta P/q_3$ was only 3.6% of the inlet velocity and probably represents the time average effect of the unsteady flow at the upcomer inlet. Table 12 gives a summary of the analysis results.

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	C _p Data		∆P/q3	BLG4	Re	Cp	C₽	C3 Analysis	C3 Loss Prgm
Design	•	0.866	0	0.08	2.6x10 ⁶	0.58	0.684	-	619.7
Data Analysis	0.749	0.866	0.07	0.108	2.85x10 ⁶	0.52	0.748	620.2	619.7

Table 12 - MK49-F Turbopump Crossover Data Analysis (LH₂)

Note: C₃ in feet per second.

Water test data showed that the upcomer had a mean pressure recovery of 0.81. Analysis showed that to achieve this amount of pressure recovery there was approximately 6% diffusion in the diffuser inlet. This indicates that the inlet $\Delta P/q_3$ was 0.12 and the throat blockage was 17.8%. This analysis was substantiated by a comparison of the inlet velocity calculated from the data analysis with that predicted by the Loss Isolation program. The values agree within 5% as shown in Table 13. The increased throat blockage was expected since the lower Reynolds number of the water test, compared to the hydrogen tests, would tend to increase the boundary layer growth on the diffuser walls.

Table 13 - Crossover Tester Data Analysis (Water)

C _p Data	Cpl	AP/q3	BLG4	Re	Ср	C3	C3 Analysis	C3 Loss Prgm
0.81	0.866	0.12	0.178	4.32x10 ⁵	0.41	0.808	194.6 (fps)	181.8 (fps)

The diffusion system turning channel was designed for minimum tosses. Rocketdyne data has shown that it was best to avoid diffusion in the turning channel, achieving all the diffusion in the radial inflow or outflow sections of the passage. Design of the turning channel for no diffusion and to minimize the losses does not simply mean designing for a constant cross section duct. Losses arising from secondary flows developed in the turning channel due to the centrifugal forces of the fluid flowing around the bend must be minimized. An area distribution to achieve this was developed by the Southwest Research Institute (Ref. 5). A correction factor was applied to the duct height as a

function of radius to minimize the migration of boundary layer fluid from the outside to the inside of the bend.

The effectiveness of the turn-around duct could not be determined directly due to the complexity of the flow in the bend which would have required extensive flow measurements. An estimate of the effectiveness was found from the data analysis of the second diffuser inlet blockage as compared to the discharge blockage of the first diffuser.

Design analysis of the second diffuser, the downcomer, was much the same as the upcomer although there was no inlet blade section. Again, accurate calculation of the inlet blockage was essential to the design. A first approximation of the inlet blockage can be made by assuming a loss-less flow from the upcomer discharge through the turning channel. Thus, the inlet, or throat, blockage of the downcomer would be equivalent to the discharge blockage of the upcomer. This analysis indicates that the inlet blockages for hydrogen and water would be 55% and 61%, respectively. Using these blockages the mean pressure recoveries were predicted to be 0.57 in hydrogen and 0.76 in water. Data showed that the pressure recoveries were actually 0.867 in hydrogen and 0.586 in water. The necessary throat blockanes to match the data were found to be 65% for hydrogen and 55% for water. The data analysis for the hydrogen shows that the blockage only grew by a factor of 10% in the turnaround duct. The water data indicated that the blockage decreased from that predicted by the "lossless" flow approximation which was probably due to experimental and analytical inaccuracies. The analysis, however, does show the criticality of predicting the throat blockage in calculating diffuser performance, and also that the turnaround duct has achieved its purpose of minimizing the increase in blockage from the upcomer discharge to the downcomer inlet. The results were summarized in Table 14.

Test Fluid	Cpi	BLG4	Ċp	Cp Analysis
LH2 (Loss-Less Core Analysis)	0.866	0.55	0.115	0.572
LH ₂ Oata Analysis	0.866	0.65	0.106	0.865
Water (Loss-Less Core Analysis)	0.866	0.61	0.10	0.755
Water Data Analysis	0.868	0.55	0.12	0.593

Table 14 - Crossover Analysis Data (Water and LH₂)

The effectiveness of the overall diffusion system can be measured by assuming that the system was one diffuser. Determination of the ideal pressure recovery, Cpl:

$$\overline{C_{pi}} = 1 - (AR)^2 \tag{14}$$

where AR was the area ratio of the diffuser as defined by the downcomer discharge area to the unblocked upcomer throat area. The calculated overall $\overline{C_{P}}$ was 0.982, and for each individual diffuser it was 0.866. The data analysis shows the overall $\overline{C_{P}}$ to be .853 in hydrogen and 0.887 in water. Calculation of the effectiveness ($\overline{C_{P}}/\overline{C_{P}}$), which was an indication of the diffuser efficiency, was 0.887. This was of the order expected for a diffuser with the calculated area ratio and length to throat width, L/W₁. Table 15 gives a summary of the mean pressure recoveries computed from the data and the analysis. Figure 60 shows the first stage diffusion system operation at 60K and 87K rpm in hydrogen and the current test at 6,322 rpm in water, plotted as a static pressure rise normalized via the tip speed of the impeller versus the position in the diffuser. The performance loss in the impeller probably caused by excessive overboard teakage.

Table	15 -	· Crossover	Overall	Performance	(Weter	and	LH ₂)	
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`	Total Pressure Loss (P ₆ -P ₃)				
Test Fluid	Cpi	Cp Analysis	C _p Data	Data (psis)	Anaiyala (paia)
MK49-F Turbopump (LH ₂)	0.982	0.853	0.854	u	•
Crossover Tester (Water)	0.982	0.887	0.888	90,16	101.24

Note: No total pressures measurements were taken during the MK49-F Turbopump tests.

A method of verifying the analysis was to compare the total pressure loss through the system as determined by the analysis and the data. This information was recorded in the water test and was found to be 90.2 psia as determined by the calculated impeller exit total pressure and the measured crossover exit total pressure. The analysis predicted that the total pressure loss would be 101.2 psia. The system performed better than predicted by the analysis.

Results from the air test (Figure 61) show a static pressure loss in the upcomer, indicating a stall either at the leading edge or in the 2-D diffuser. Analysis showed that the pressure recovery for the upcomer in air should have been 0.29, which was very low, but does not represent a stalled condition. The pressure recovery was low due to the boundary layer blockage of the upcomer throat, approximately 30% as extrapolated from the hydrogen and water data analysis. This was much larger than in the water and hydrogen tests because the Reynolds number of the air test was only of the order of 1×10^4 , two orders of a magnitude less than the hydrogen test. This data and analysis indicates that the stall occurred at the diffuser leading edge.

The leading edge stall model was based on modeling the flow incidence angle and blade geometry of the diffuser inlet vane suction surface as a 2-D channel diffuser (Ref. 2). The diffuser blade row can be approximated as shown in Figure 62, where the transition region ABCD can be treated as a 2-D diffuser. The 2-D diffuser stall model was used to predict a leading edge stall, Figure 63, using line a-a. Using the diffuser geometry and the expected inlet flow angle as determined by the Loss isolation program, stall was predicted at a flow angle of 4.5 degrees or an incidence angle of 4.9 degrees. The expected flow angle was 7.65 degrees, which corresponds to an incidence angle of 1.75 degrees which was below the predicted stall angle. It was expected that the stall incidence would increase with decreasing Reynolds number, and making a correction based on variations of peak diffuser pressure recovery with Reynolds number and inlet blockage, the stall incidence was predicted to be 3.5 degrees, corresponding to an 0.6a-a line on Figure 62. Again, stall was not predicted, but the tendency for stall to occur in the case of air was evident. A compressor performance prediction code should be used to calculate the rotor exits conditions and, hence, may predict the stall. More analysis is required to evaluate the stall model for high blockage and low Reynolds number flows. In addition, an investigation is required to evaluate the dynamic effects of the varying incidence angle due to the impeller blade wakes on the mean stall incidence.

The DC system has been shown to achieve the required pressure recovery with lower total pressure loss than predicted. The test series was designed to verify the analytical approach and prove the usefulness in future design efforts. As was shown, the analysis does well provided that the throat blockage can be adequately predicted. The difficulty for the upcomer was trying to predict the time-averaged effect of an unsteady inlet flow field due to the impeller blade wakes. This may account for the difference between the original design and the data analysis results as determined in this report. The downcomer design was dependent on the correct estimation of the upcomer exit blockage



DELP/(RH0+U^2)+10%

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Figure & - Flow Regime Chart for Two-Dimensional Diffuser . (Ref. 4)

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and determination of the extent of the boundary layer growth in the turnaround duct. The design approach for the constant area turnaround was verified. This was critical for designing effective downcomers with high diffusion upcomers.

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APPENDIX A - AIR TEST DATA TEST 1 AND TEST 2

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		Inlet Orf	Intet Orf	Intet Orf	Inducer	Shaft	Inducer	Inducer
	900	U/S Pr	ÅP	U/S Temp	In #1 Pr	Speed	In #2 Pr	Out Pr #1
Record #	•	psia	psd	ĉ	psia	rpm	psia	psia
~	80.2	14.2598	0.0486	538.3	14.312	6322	14.312	14.3771
8	80.7	14.3599	0.0431	538.6	14.312	6322	14.312	14.3773
6	71.5	14.3601	0.0384	539.3	14.323	6322	14.323	14.3948
10	71.9	14.3600	0.0389	538.5	14.323	6322	14.323	14.3948
11	81.8	14.3600	0.0504	539.5	14.312	5322	14.312	14.3761
12	81.8	14.3599	0.0503	539.8	14.312	6322	14.312	14.3782
13	91.1	14.3589	0.0825	539.6	14.299	6322	14.299	14.3563
14	80.3	14.3598	0.0614	540.1	14.300	6322	14.300	14.3572
15	102.3	14.3598	0.0787	540.6	14.286	6322	14.286	14.3332
16	102.5	14.3597	0.0792	540.1	14.286	6322	14.286	14.3329
17	110.9	14.3596	0.0925	541.5	14.271	6322	14.271	14.3087
18	110.6	14.3587	0.0919	542.3	14.272	6322	14.272	14.3101
19	119.4	14.3598	0.1073	541.2	14.257	6322	14.257	14.2835
20	120.4	14.3598	0.1087	542.5	14.256	6322	14.256	14.2834
21	111.4	14.3598	0.0927	544.8	14.273	6322	14.273	14.3108
22	111.5	14.3587	0.0929	545.0	14.273	6322	14.273	14.3108
23	101.7	14.3598	0.0772	545.4	14.290	6322	14.290	14.3399
24	100.9	14.3598	0.0759	545.4	14.290	6322	14.290	14.3395
25	92.1	14.3599	0.0632	545.0	14.302	6322	14.303	14.3590
26	92.0	14.3598	0.0631	545.4	14.303	6322	14.303	14.3601
27	81.4	14.3600	0.0493	545.0	14.319	6322	14.319	14.3847
28	81.9	14.3601	0.0500	544.8	14.318	6322	14.318	14.3836
29	70.8	14.3589	0.0370	547.1	14.331	6322	14.331	14.4125
30	72.4	14.3600	0.0389	547.1	14.330	6322	14.330	14.4093

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Inducer	Impeller Frnt	Impeller Aft	Implir Disch	Upcorner Const	Upcomer Const	Transition	Downcomer	Downcomer
Out Pr #2	Shrd #1 Pr	Shrd #1 Pr	Static Pr	Area Pr #2	Area Pr #3	Static Pr #1	Disch Pr #2	Cnst Area #2
psia	psia	psia	psia	psia	psia	psia	psia	psia
14.3726	14.7336	14.8064	14.8721	14.8598	14.8371	14.8693	14.8600	14.8351
14.3724	14.7335	14.8066	14.8721	14.8592	14.8372	14.8691	14.8600	14.8351
14.3905	14.7577	14.8387	14.8991	14.9109	14.8890	14.9176	14.9067	14.8872
14.3904	14.7581	14.8366	14.8993	14.9103	14.8883	14.9169	14.9062	14.8866
14.3717	14.7317	14.8043	14.8698	14.8547	14.8331	14.8649	14.8565	14.8304
14.3744	14.7332	14.8058	14.8706	14.8585	14.8374	14.8685	14.8587	14.8337
14.3523	14.7040	14.7686	14.8383	14.7974	14.7758	14.8088	14.8039	14.7718
14.3534	14.7050	14.7701	14.8389	14.7986	14.7774	14.8117	14.8057	14.7739
14.3286	14.6874	14.7211	14.8185	14.7227	14.7155	14.7546	14.7468	14.7101
14.3290	14.6873	14.7213	14.8179	14.7212	14.7148	14.7536	14.7462	14.7098
14.3050	14.6573	14.6864	14.7842	14.6497	14.6442	14.6899	14.6794	14.6396
14.3059	14.6587	14.6887	14.7856	14.6532	14.6483	14.6943	14.6830	14.6434
14.2798	14.6253	14.6518	14.7488	14.5701	14.5661	14.6203	14.6064	14.5624
14.2794	14.6255	14.6518	14.7482	14.5688	14.5657	14.6195	14.6057	14.5612
14.3068	14.6585	14.6905	14.7859	14.6568	14.6524	14.6980	14.6869	14.6466
14.3069	14.6589	14.6901	14.7857	14.6579	14.6523	14.6982	14.6874	14.6476
14.3356	14.6938	14.7329	14.8258	14.7397	14.7322	14.7698	14.7630	14.7269
14.3358	14.6936	14.7321	14.8255	14.7396	14.7321	14.7705	14.7632	14.7274
14.3563	14.7183	14.7854	14.8540	14.7868	14.7781	14.8132	14.8066	14.7736
14.3572	14.7197	14.7669	14.8554	14.7901	14.7807	14.8154	14.8089	14.7761
14.3828	14.7527	14.8137	14.8921	14.8444	14.8311	14.8631	14.8545	14.8268
14.3816	14.7505	14.8116	14.8899	14.8410	14.8271	14.8604	14.8517	14.8235
14.4070	14.7927	14.8494	14.9386	14.8960	14.8807	14.9030	14.9006	14.8770
14.4048	14.7875	14.8459	14.9318	14.8942	14.8795	14.9028	14.8994	14.8756

Jowncomer	Xover Disch	Implir Disch	Transition	Xover Exit-Mid	Xover Exit	Xover Exit	Inlet Orf	Pump Inlet	Salculated
Aid Diff #1	Static Pr #1	Tolal Press	Total Press	Mid Pass Pr	Mid Pass Pr	Inner Hub Pr	Disch Pr	Temp	nlet Flov
psia	psia	psiat	psiat	psiat	psiat	psiat	psia	Å	lbm/sec
14.8630	14.8634	15.1460	14.8551	14.8752	14.8630	14.8645	14.3147	77.05	1.043
14.8634	14.8635	15.1449	14.8547	14.8747	14.8630	14.8645	14.3148	77.38	1.049
14.9116	14.9115	15.1797	14.8053	14.9222	14.9113	14.9130	14.3256	77.08	0.929
14.9115	14.9112	15.1798	14.9051	14.9210	14.9111	14.9128	14.3253	77.16	0.934
14.8588	14.8595	15.1419	14.8513	14.8714	14.8590	14.8609	14.3144	77.99	1.064
14.8619	14.8632	15.1428	14.8538	14.8733	14.8627	14.8642	14.3155	78.13	1.063
14.8031	14.8048	15.1009	14.7941	14.8168	14.8044	14.8032	14.3026	78.42	1.184
14.8041	14.8065	15.1027	14.7957	14.8184	14.8062	14.8051	14.3030	78.57	1.174
14.7452	14.7465	15.0889	14.7345	14.7588	14.7448	14.7486	14.2893	79.23	1.330
14.7446	14.7458	15.0892	14.7342	14.7585	14.7443	14.7482	14.2892	78.82	1.333
14.6779	14.6790	15.0432	14.6548	14.6927	14.6766	14.6814	14.2750	80.11	1.442
14.6819	14.6827	15.0461	14.6684	14.6963	14.6805	14.6849	14.2759	80.35	1.438
14.6043	14.6056	14.9973	14.5883	14.6200	14.6036	14.6079	14.2606	80.89 \	1.553
14.6039	14.6047	14.9967	14.5874	14.6192	14.6029	14.6068	14.2603	80.52	1.565
14.6862	14.6860	15.0448	14.6720	14.6998	14.6837	14.6887	14.2773	82.93	1.448
14.6858	14.6868	15,0451	14.6717	14.7002	14.6842	14.6889	14.2771	83.58	1.450
14.7608	14.7618	15.0970	14.7504	14.7747	14.7593	14.7644	14.2941	83.11	1.322
14.7613	14.7623	15.0978	14.7503	14.7748	14.7595	14.7648	14.2939	83.34	1.312
14.8046	14.8064	15.1288	14.7949	14.8179	14.8035	14.8082	14.3059	83.87	1.197
14.8075	14.8089	15.1292	14.7961	14.8191	14.8054	14.8099	14.3065	83.83	1.196
14.8570	14.8590	15.1686	14.8473	14,8685	14.8556	14.8598	14.3217	84.05	1.058
14.8531	14.8555	15.1865	14.8446	14.8657	14.8532	14.8568	14.3209	83.78	1.065
14.9060	14.9052	15.2074	14.8971	14.9156	14.8052	14.9070	14.3335	86.72	0.917
14.9034	14.9036	15.2052	14.8954	14.9137	14.9031	14.9043	14.3324	85.42	0.941

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Test
Air

Inducar	Impeller	Transition	Downcomer	Crossover	Transition	Downcomer	Crossover	Calc
Static AP	Static AP	Static AP	Static AP	Static AP	Total AP	Total AP	Total AP	In Dens
psi	þsi	psi	ps i	psi	psi	psi	psi	tbm/ft3
0.0651	0.4950	-0.0028	0.0059	-0.0087	0.2909	0.0201	0.2708	0.0720
0.0553	0.4948	-0.0030	0.0056	-0.0086	0.2902	0.0200	0.2702	0.0720
0.0718	0.5043	0.0185	0.0046	0.0124	0.2744	0.0169	0.2575	0.0719
0.0718	0.5045	0.0176	0.0041	0.0119	0.2747	0.0159	0.2588	0.0720
0.0641	0.4937	-0.0049	0.0065	-0.0103	0.2906	0.0201	0.2705	0.0719
0.0662	0.4924	-0.0021	0.0048	-0.0074	0.2890	0.0195	0.2695	0.0718
0.0573	0.4820	-0.0295	0.0080	-0.0335	0.3068	0.0227	0.2841	0.0718
0.0572	0.4817	-0.0272	0.0067	-0.0324	0.3070	0.0227	0.2843	C.0718
0.0472	0.4853	-0.0639	0.0042	-0.0720	0.3544	0.0243	0.3301	0.0717
0.0469	0.4850	-0.0643	0.0049	-0.0721	0.3550	0.0243	0.3307	0.0718
0.0377	0.4755	-0.0943	0.0028	-0.1052	0.3784	0.0279	0.3505	0.0716
0.0381	0.4755	-0.0913	0.0020	-0.1029	0.3777	0.0279	0.3498	0.0715
0.0265	0.4653	-0.1285	-0.0003	-0.1432	0.4090	0.0317	0.3773	0.0716
0.0274	0.4648	-0.1287	-0.0003	-0.1435	0.4093	0.0318	0.3775	0.0715
0.0378	0.4751	-0.0879	0.0018	-0.0339	0.3728	0.0278	0.3450	0.0712
0.0378	0.4749	-0.0875	0.0020	-0.0989	0.3734	0.0285	0.3449	0.0711
0.0499	0.4859	-0.0560	0.0049	-0.0640	0.3466	0.0243	0.3223	0.0711
0.0495	0.4860	-0.0550	0.0043	-0.0632	0.3473	0.0245	0.3228	0.0711
0.0570	0.4950	-0.0408	0.0047	-0.0476	0.3339	0.0230	0.3109	0.0711
0.0571	0.4953	-0.0400	0.0037	-0.0465	0.3331	0.0230	0.3101	0.0711
0.0657	0.5074	-0.0290	0.0054	-0.0331	0.3213	0.0212	0.3001	0.0711
0.0656	0.5083	-0.0295	0.0053	-0.0344	0.3219	0.0211	0.3008	0.0711
0.0815	0.5281	-0.0356	0.0126	-0.0334	0.3103	0.0185	0.2918	0.0709
0.0793	0.5225	-0.0290	0.0109	-0.0282	0.3098	0.0183	0.2915	0.0709

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		Inie Or	Iniel Ort	Inlet Orf	Inducer	Shaft	Inducer	Inducer
	80	U/S Pr	ą.b	U/S Temp	In #1 Pr	Speed	In #2 Pr	Out Pr #1
Record #	٠	pala	psi	ů.	psia	ndı	psia	psia
**	100.3	14.3396	0.0757	539.9	14.262	6322	14.262	14.3068
ຸດ	100.2	14.3395	0.0754	540.4	14.262	6322	14.262	14.3070
n	111.3	14.3384	0.0931	541.2	14.244	6322	14.244	14.2765
4	111.0	14.3394	0.0926	541.0	14.244	6322	14.244	14.2769
S	122.6	14.3393	0.1128	541.8	14.224	6322	14.224	14.2432
9	122.2	14,3394	0.1122	541.3	14.224	6322	14.224	14.2437
~	80,6	14.3397	0.0613	542.7	14.277	6322	14.277	14.3308
8	90.4	14.3397	0.0610	543.2	14.277	6322	14.277	14.3307
ġ	80.7	14.3397	0.0485	543.8	14.287	6322	14.287	14.3470
10	80.6	14.3397	0.0484	544.1	14.287	6322	14.287	14.3475
11	69.8	14.3397	0.0363	543.6	14.301	6322	14.301	14.3704
12	70.8	14,3399	0.0373	544.5	14.301	6322	14.301	14.3698
13	98.3	14.3397	0.0722	543.7	14.265	6322	14.265	14.3105
14	98.5	14.3396	0.0725	543.6	14.265	6322	14.265	14.3109
15	110.3	14.3396	0.0908	544.4	14.245	6322	14.245	14.2773
16	110.4	14.3394	0.0909	544.8	14.246	6322	14.246	14.2773

Inducer	Impeller Frnt	Impeller Aft	Implir Disch	Upcomer Const	Upcomer Const	Transition	Downcomer	Downcomer
Out Pr #2	Shrd #1 Pr	Shrd #1 Pr	Static Pr	Area Pr #2	Area Pr #3	Static Pr #1	Disch Pr #2	Cnst Area #2
psia	psia	psia	psiæ	psia	psia	psia	psia	psia
14.3033	14.6514	14.6983	14.7802	14.7228	14.7135	14.7501	14.7455	14.7107
14.3033	14.6508	14.6988	14.7800	14.7223	14.7130	14.7493	14.7451	14.7103
14.2730	14.6134	14.8526	14.7370	14.6357	14.6303	14.6721	14.6668	14.6268
14.2728	14.6132	14.6526	14.7374	14.6359	14.6301	14.6724	14.6670	14.6270
14.2395	14.5724	14.6085	14.6919	14.5336	14.5307	14.5814	14.5728	14.5294
14.2400	14.5724	14.6067	14.6923	14.5352	14.5318	14.5820	14.5735	14.5295
14.3275	14.6767	14.7419	14.8103	14.7589	14.7476	14.7829	14.7759	14.7469
14.3273	14.6764	14.7417	14.8096	14.7588	14.7469	14.7831	14.7761	14.7465
14.3444	14,6979	14.7674	14,8333	14.8069	14.7940	14.8283	14.8190	14.7934
14.3440	14.6978	14.7681	14.8344	14.8077	14.7946	14.8289	14.8194	14.7937
14.3676	14.7285	14.8056	14,8586	14.8741	14.8594	14.8888	14.8772	14.8578
14.3869	14.7282	14.8050	14.8673	14.8739	14.8592	14.8884	14.8764	14.8579
14.3069	14.6525	14.7001	14.7819	14.7323	14.7234	14.7580	14.7536	14.7194
14.3072	14.8528	14.6998	14.7819	14.7321	14.7235	14.7583	14.7534	14.7194
14.2737	14.6117	14.6516	14.7348	14.6367	14.6312	14.6718	14.6664	14.6269
14.2743	14.6120	14.6518	14,7356	14.6372	14.6321	14.6733	14.6675	14.6281

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Downcomer	Xover Disch	Implir Disch	Transition	Xover Exit-Mid	Xover Exit	Xover Exit	Inlet Orf	Puma Inle
Mid Diff #1	Static Pr #1	Total Press	Total Press	Mid Pass Pr	Mid Pass Pr	Inner Hub Pr	Disch Pr	Temp
psia	psia	psiat	psiat	psiat	psiat	pslat	psla	ų
14.7427	14.7421	15.0346	14.7374	14.7657	14.7549	14.7460	14.2654	78.40
14.7426	14.7418	15.0342	14.7394	14.7656	14.7549	14.7455	14.2656	78.80
14.6635	14.5632	14.9759	14.6575	14.6881	14.6768	14.6666	14.2478	79.20
14.6637	14.6634	14.8760	14.6571	14.6882	14.6765	14.6666	14.2482	79.40
14.5703	14.5693	14.9187	14.5603	14.5973	14.5834	14.5736	14.2281	80.50
14.5700	14.5698	14.9192	14.5612	14.5979	14.5835	14.5744	14.2283	79.60
14.7759	14.7779	15.0690	14.7709	14.7980	14.7887	14.7806	14.2801	81.10
14.7752	14.7774	15.0681	14.7702	14.7971	14.7883	14.7802	14.2800	81.70
14.8200	14.8216	15.1007	14.8161	14.8394	14.8311	14.8247	14.2902	81.80
14.8208	14.8220	15.1005	14.8162	14.8393	14.8319	14.8247	14.2904	82.40
14.8816	14.8821	15.1433	14.8778	14.8964	14.8906	14.8849	14.3037	82.30
14.8812	14.8817	15.1430	14.8773	14.8963	14.8898	14.8843	14.3038	82.40
14.7503	14.7503	15.0382	14.7443	14.7723	14.7613	14.7533	14.2685	81.90
14.7504	14.7501	15.0387	14.7442	14.7718	14.7610	14.7534	14.2687	82.50
14.6631	14.6624	14.8729	14.6553	14.6874	14.6752	14.6659	14.2495	83.30
14.6643	14.6634	14.9731	14.6555	14.6875	14.6752	14.6669	14.2494	82.90

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Calculated	Inducer	Impeller	Transition	Downcomer	Crossover	Transition	Downcomer	Crossover
Inlet Flow	Static AP	Static AP	Static AP	Static AP	Static AP	Total AP	Total AP	Total AP
lbm/sec	psi	psi	İsq	psi	psi	psi	psi	psi
1.304	0.0448	0.4734	-0.0301	0.0156	-0.0381	0.2972	0.0283	0.2689
1.302	0.0450	0.4730	-0.0307	0.0163	-0.0382	0.2948	0.0262	0.2686
1,448	0.0325	0.4605	-0.0649	0.0160	-0.0738	0.3184	0.0306	0.2878
1.443	0.0329	0.4605	-0.0650	0.0158	-0.0740	0.3189	0.0311	0.2878
1.594	0.0192	0.4487	-0.1105 -	0.0159	-0.1226	0.3584	0.0370	0.3214
1.588	0.0197	0.4486	-0.1103	0.0159	-0.1225	0.3580	0.0367	0.3213
1.177	0.0538	0.4795	-0.0274	0.0151	-0.0324	0.2981	0.0271	0.2710
1.175	0.0537	0.4789	-0.0265	0.0140	-0.0322	0.2979	0.0269	0.2710
1.049	0.0600	0.4883	-0.0050	0.0111	-0.0117	0.2846	0.0233	0.2613
1.048	0.0605	0.4869	-0.0055	0.0104	-0.0124	0.2843	0.0231	0.2612
0.907	0.0694	0.4982	0.0202	0.0076	0.0135	0.2655	0.0186	0.2469
C.920	0.0588	0.4875	0.0211	0.0079	0.0144	0.2657	0.0190	0.2467
1.278	0.0455	0.4714	-0.0239	0.0143	-0.0316	0.2919	0.0280	0.2639
1.281	0.0459	0.4710	-0.0236	0.0135	-0.0318	0.2925	0.0276	0.2649
1.433	0.0323	0.4575	-0.0630	0.0156	-0.0724	0.3176	0.0321	0.2855
1.435	0.0313	0.4583	-0.0623	0.0142	-0.0722	0.3176	0.0320	0.2856

APPENDIX B - WATER TEST DATA

TEST NUMBER T88A094 TEST NUMBER T88A096 TEST NUMBER T88A097

INFORMATION FOR READING DATA TABLE SUMMARY AND DATA TABLES:

- MDS: Measurement Data Sequence. Data record within a particular test.
- NSCANS: Number of Scans in the data record.
- TYPE: Type of data recorded;
 - TYPE =1 Data are recorded at steady state operating conditions, e.g., HQ. The data are averaged based on the number of scans in the MDS.
 - TYPE = 2 Data are recorded continuously for transient tests,e.g. start/shutdown transients and suction performance tests.

Data in tables are averaged over the number of scans and are presented by MDS number. All TYPE 2 data, since they are averaged, should be disregarded. Due to the volumes of suction performance data, it was considered too cumbersome for this report. These data can be made available upon request. .

DIRI EDF	ECTORY HDR:	FILE: CROSS	RUN NU SOVER H	M: 88A Q AND	094 CAV TE	.st '	DATE:	10/ 5	5/88, 1	N MDS≖	17, N	CPS=
IC	P:	1 231 818 838 4	801 806 120 900 953	2 807 819 901 850	228 808 820 903 851	229 809 821 902 926	802 810 822 904	803 811 826 905	804 812 7 950	805 813 5 951	230 815 3 952	
MDS 1 2 3 4 5 6 7 8 9 10	NSCANS 20 181 20 20 20 20 20 20 20 20	TYPE 1 PF 2 SJ 1 HC 1 HC	H RE TEST CARTUP 2 0640 2 0699 2 0640 2 0640 2 0582 2 0524 2 0524 2 0466 2 0407 2 0466	EADER STATIC TRANSI FLOW FLOW FLOW FLOW FLOW FLOW FLOW	C @ 91 ENT	. 2 PSJ	ĨĂ					
10 11 12 13 14 15 16 17	20 20 345 3 579 701 20	$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	2 6466 2 6524 2 6582 2 6582 2 6582 2 6582 2 6582 2 7 2 6524 2 6466 2 7 2 7 2 6466 2 7 2 6466 2 6524 2 6 2 6 2 6 2 6 2 6 2 6 2 6 2 6 2 6 2 6	FLOW FLOW FLOW FLOW FLOW FLOW T STAT	IC (9)) PSIA						
T S N ID N	TIME: WS= 70 W: 23 81 95 -10 -80	14:59:3 , N W 1 803 1 806 6 818 3 838 2 4 1 -106 1 -808	S.90, STAT= 807 120 900 953 5 -107 -809	P DAT 74, 228 808 819 901 850 -34 -810	E: 10/ N STAJ 229 809 920 903 951 -193 -811	06/88, 12 802 810 821 926 926 927 926 927	P TI 2 803 0 811 1 822 904 5 -152 4 -195 2 -813	ME: 07 8 804 812 826 905 -25 -202 8 -814	7:30:0 4 80 2 81 5 95 -2 2 -20 4 -81	7 5 23(3 815 7 5 0 95 6 -10(3 -80) 5 -81) 5 1 0 0 6	
IW	STAT:	1 231 815 5 951 -100 -203 -814	801 806 816 3 952 -101 -800 -152	2 807 818 838 4 -106 -801 -815	228 808 120 900 953 -107 -152 -816	229 809 819 901 850 -34 -808	802 810 820 903 851 -152 -809	803 811 821 902 926 -193 -810	804 812 822 904 -152 -194 -811	805 813 826 905 -25 -195 -812	230 802 7 950 -26 -272 -272	
M W	1 REC:	3 364	23 384	204 404	224 7 (9	244 752	264 1331	284 2032	304	324	344	
IN	STAT:	1 10	0 11	2 0	3 0	4 0	5 0	6 12	7	8	9	

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AVERAGED DATA ON MEASUREMENT DATA SETS CROSSOVER HQ AND CAV TEST

HEADER:

FWD TMP AFT IMP AFT DUD P SHROUD P SHROUD P P R #1 R #2	171 74.296 75.943 333 358.11 338.57 93 448.27 436.68 58 427.57 417.53 81 475.71 436.96 17 483.57 436.20 17 483.57 450.20 75 501.95 459.23 66 572.78 471.08	39 502.02 460.97 83 482.71 450.72 83 467.86 446.04 48 402.28 383.44 96 489.48 455.49 407.93 377.34 70 452.63 407.04 133 74.567 75.913	LO 811 812 NSITI DWN DIFF DWN DIFF ST PR DISCH P DISCH P R #1 R #2	115 75.249 74.193 46 570.53 568.13 43 532.91 532.16 43 533.91 532.16 43 533.91 532.16 67 586.01 585.91 67 606.10 601.06 67 606.10 601.06 15 589.94 590.65 33 577.65 625.98 15 589.94 590.65 15 569.94 590.65 32 579.56 510.25 32 593.51 590.65 32 593.51 590.25 512.47 512.47
BUZ BUZ BU IMP FWD IMP J SHROUD P SHROI R #1 R #2	75.242 333.70 298. 386.14 399.66 391. 399.66 391. 399.45 477.95 402. 402. 402. 402.	478.78 454.06 437.12 437.12 451.10 461.10 406. 379.34 379.34 324. 379.34 324. 74.876 76.4	809 81 UPC CONS TRAN T SEC PR ON S #4	75.945 399.325 565.55 565.55 565.60 565.60 563.51 562.42 582.42 582.42 582.42 582.42 582.42 572.55 582.42 572.55 582.42 572.55 575.55 5
229 D/S STAT . PRESS. IND #2	77,348 92,410 92,730 92,730 92,661 101,30 101,30 101,49		808 UPC CONS T SEC PR	45440,000 66440,000 66440,000 66440,000 66400,000 66400,000 66400,000 6660,000 6660,000 6600,0000 6600,000
228 D/S STAT . PRESS. IND #1	222 222 222 222 222 222 222 222 222 22	11126.314 1066.314 11.223 11.233 11.233 11.233 11.233 11.233 11.233 11.233 11.233 11.233 11.233 11.235 11.2555 11.2555 11.2555 11.2555 11.2555 11.2555 11.2555 11.2555 11.2555 11	807 UPC CONS T SEC PR 13	766.25 766.25 766.25 766.25 771.12 766.25 775.75 775 775 775 775 775 775
2 Flommete R f 1	6.3538 564.3538 564.353 733.24 733.24 734.95 673.53 673.58 75 75 75 75 75 75 75 75 75 75 75 75 75	620.82 676.67 676.67 674.05 617.62 617.62 563.46 15050	17 3310 114 110 114 110	74.81 561 561 562 562 562 562 562 562 562 562 562 562
801 INLET ST ATIC PR 82	91.475 91.475 91.475 91.333 91.124 91.124 91.124 91.124	99999999 111919999 199999 19999 19999 19999 19999 19999 19999 19999 19999 19999 1997 1	231 D/S STAT . Press. IMP 4 2	4 4 4 8 8 8 8 8 8 9 9 9 9 9 9 9 9 9 9 9
1 INLET ST ATIC PRE SSURE, F	991.36 991.36 991.36 991.36 995.45 9931.65 9931.55 995.4 9531.5 9531.5 9531.5 9531.5 955.5	99999 9999 9999 9999 9999 9999 9999 9999	230 D/S STRT PRESS. IMP 41	22222222222222222222222222222222222222
P/F ID † MDS † TYFE			P/F ID † Mds † type	ミンちゅうりょうりょう うっての ないしょう うってい うちょう うっちょう うっちょう うっちょう うちょう うちょう うちょう う

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AVERAGED DATA ON HEASUREMENT DATA SETS

HEADER: Test 88 a 094	CROSSOVER B TEST	IQ AND CAV TE START TIME 1	ST 0/ 5/88 - 14:	59:35.90	PROCESS TIME	10/12/88	14:03:21		
P∕F ID∳ TYPE	230 D/S STAT . Press. IMP &1	231 D/S STAT - PRESS. IMP #2	17 4310 014 NMO 908	807 UPC CONS T SEC PR £ 3	808 UPC COVS T SEC PR	B09 UPC CONS T SEC PR	610 TRANSITI ON ST PR	811 DWN DIFF DISCH P R #1	812 DWN DIFF DISCH P R #2
16 2	51 9.77	521.79	553.05	540.06	523.23	534.33	539.65	550.85	552.82
17 1	7 7.832	76.940	74.303	76.670	74,788	75.619	74.366	75.199	74.655
3477 ¥20M	813	802	815	gis	120	819	820	821	822
	DMN CONS	IMP FMD	KOVER DI	Thrust d	D/S TOT	Turisiti	XJVER EX	XOVER EX	XOVER EX
	T SEC PR	Shroud P	SCR ST P	ISK drat	PRESS. 1	Or fotal	IT TOTAL	IT TOTAL	IT TOTAL
	#1	R 41	R f 1	N Pr	IMP \$1	Pr	PR #1	PR #2	PR #3
-000-000-00-00-00-00-00-00-00-00-00-00-	55555555555555555555555555555555555555	400.20 400.20	570 6 6 6 6 7 7 8 6 7 7 8 6 7 7 8 6 7 7 8 6 7 7 8 6 7 7 8 6 7 7 8 6 7 7 8 6 7 7 8 6 7 7 8 6 7 7 7 7	50.68 50.68 50.68 641.92 687.21 686.24 693.70 636.64 651.88 651.88 651.88 651.88 651.90 6	22222222222222222222222222222222222222	55555 55555 55555 55555 55555 5551 5551 5551 5555 5555 5555 5555 5	427.907 5482.907 5483.46 586.28 602.77 624.79 624.79 624.15 595.02 595.02	48.702 544.62 544.68 544.68 598.61 598.61 604.27 618.96 619.06 613.02 603.02 590.07	425.123 5425.73 545.08 545.08 561.84 663.15 663.06 617.08 617.08 617.08 617.08
199992	689.55	370.49	510.40	413.69	301.95	4 68.42	527.71	521.79	525.02
	573.55	870.49	595.98	492.07	381.33	551.43	614.86	608.36	608.81
	691.40	870.10	512.66	414.46	301.21	471.92	530.77	524.24	524.73
	530.95	825.53	552.65	48.38	336.52	514.62	571.94	565.87	562.20
	76.116	78.876	76.301	78.838	779	75.857	77.497	76.922	76.744

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HEADER: Test 88A094	CROSSOVER I TEST	HQ AND START	CAV T TIME	AU 10/	ERAGEL 5/88	14:59	он :35.	MEASU 90	REMENT D PROCESS	ATA S TIME	ETS 10/12/88	14:03
6∕E ID€	826	i	2	l	ŝ			9	838	I	006	

																														1							
	902 LUBE OIL TEMP #2		96.359	101.09	112.60	111.11	112.57	116.11	117.63	118.53	119.00	119.15	118.40	117.44	115.11	117.12	117.35	117.49	101.06	851	GBOX OIL	PR		46.547	34.603	23.402	22.603	21.930	CC5.12	20.953	20.698	C44.07	20.184	100.01	19 140	18.562	17.872
	903 LUBE OIL TEMP #1		93.201	105.05	116.17	117.92	117.38	123.05	126.12	131.69	133.49	133.95	126.35	124.10	123.05	126.00	126.73	131.89	10.101	850	FLEX FLO	N PR		914.20	963.05	944.04	943.58	942.60	CZ . 294	941.72	941.56	940.03	940.80 620 00	030.00	0.00 0.00	11.12	936.09
4:03:21	901 FWD TORQ UE TEMP		70.209	72.333	80.900	81.670	82.355	83.066	85.484	87.145	87.897	88.905	89.488	90.069	91.762	94.922	97.095	101.15	99.598	953	LUBE OIL	FLOW		21.215	21.719	20.007	19.902	19,890	17.21	19.951	106.901	10,000	202.21	10 01	20. 267	20.733	20.647
10/12/88 1	900 REAR TOR QUE TEMP		70.673	73.109	81.688	82.474	83.197	83.835	84.846	85.808	86.619	87.409	87.389	88.317	90.072	91.858	93.952	97.322	94.359	4	SPEED			-1.7116	4986.8	6318.9	631/.9	6320.5	C'ATCO	6318.9	6320.2	0.11CO	2.02cg	2.1100	6318 6	6318.6	6318.6
PROCESS TIME	838 Thrust d Isk drai	N FLOW	4.4700	62.269	92.914	85.819	92.928	94.229	94.810	96.105	97.893	96.212	54.954	93.564	91.162	95.392	92.338	95.856	-0.154828-01	952	ACCEL 2	AXIS		0.26343E-01	0.15718	0.21661	0.42381	C6122-0	U.1880D	0.21291	0.22909	16202.0	C 20211	0 21160	0.23215	0.22019	0.27875
59:35.90	3 Floumete R f 2		0.75280	503.98	655.26	706.91	657.03	597.86	538.88	£79.79	€18.57	479.62	539.45	597.91	597.71	538.96	539.00	479.50	0.95945E-01	195	ACCEL Y	SIXU		0.79573E-01	0.15707	0.57703	0.2005/	0.1//01	177/1.0	0.16375	0.15310		0.15450	0 15783	0.15736	0.14956	0,16506
0/ 5/88 14:	5 Torque f 1		-1.7035	3242.0	4355.6	4408.5	4350.4	1249.4	4130.8	4015.5	3364.8	4020.1	(129,9	1260.0	4171.3	£139.6	4034.8	3957.7	5.6784	950	ACCEL X	AXIS		0.555258-01	0.28876	0.32515	0.01011	0.44261	ポカクロデーン	0.41847	0.24286	0.0000	0.26305	10002	0.22744	0.30932	0.32048
START TIME 1	7 In. Temp Erature		67.405	66.452	66.667	66.736	66.924	67.119	67.247	67.372	67.476	67.612	67.697	67.860	68.254	68.652	69.054	69.737	70.228	305	LUBE OIL	SUP T		92.108	91.525	100 NOU	205.16	611.2A		92.150	92.24 97.24		787.14 03 260	0000000	0.0.00	92.892	121.421
TEST	826 Pump del Ta Pr		0.75468	334.32	489.74	453.77	490.37	507.80	513.93	528.96	549.56	530.03	512.51	498.88	477.29	518.67	694.80	529.86	1.3902	¥06	GEAR CAS	E TEMP		73.766	74.084		50.103 20.000	99.720 107 05		105.69	108.28	07 711	25.211	115 66	120.53	125.02	129.02
rest 88A094	/F ID#	ACS I TYPE		2	1 M	-		9 9	e-4	8	1 6	10 1	11 1	12 1	13 2	14 2	15 2	16 2	17 1	/F ID#			MDSH TYPE	1	~			-1 - 1 -				7 - N C	1 1		13	14 2	15 2

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GBOX OIL PR -194 SCALED F LOW IND. 17.298 23.145 -85.634 78.611 66.678 71.918 66.736 60.736 54.694 48.658 42.412 48.678 54.737 60.730 60.689 54.703 54.685 54.685 851 Ţ. 0.44755E+12 0.52580E+11 8010.5 FLEX FLO W PR SCALED N PSH IND. 934.33 932.79 8027.1 8015.3 7994.0 7966.7 7981.6 7992.3 8010.2 7995.1 8003.3 4034.7 8006.6 2792.3 3430.2 850 -193 14 953 LUBE OIL FLOW FLOW 1 R ATIO IND 1 41 21.591 22.411 18.234 5.7014 1.2605 1.2615 1.2615 1.2615 1.2647 1.2640 1.0660 0.96855 0.96855 0.96905 1.1636 1.1588 1.0673 1.0618 0.96851 -0.54076 1.0670 -152 PROCESS TIME 10/12/88 14:03:21 D/S PRES S. PIPE 92.644 93.013 93.013 93.013 93.013 92.455 92.725 92.613 92.613 92.613 92.613 92.613 92.613 92.643 92.643 0.31601 0.16592 0.26610 6319.6 0.515572-01 0.775192-01 0.226192-01-0.23337 speed Ee-AVERAGED DATA ON MEASUREMENT DATA SETS EAD 2 IM P. #1 **4.2**122 **480.39 683.62 683.62 685.36 685.36 685.36 743.63 743.63 743.63 743.63 743.63 743.63 631.49 632.07 632.07 632.07 632.07 632.07 632.03 6455 636.63 636.63 636.63 636.63 636.63 636.63 636.63 636.63 636.63 636.63 636.63 636.63 636.63 636.63 636.63 636.63 637.64 637.65 647.6565 647.6565 656565** ST-TOT H 952 Accel z Axis -107 -0. 2278.1 2278.7 3046.8 3046.8 3046.8 3046.8 3046.8 2034.6 2804.6 28033.5 28033.5 28033.5 28033.5 2805.5 2000.5 2 HSS IND. 951 Accel Y Axis CROSSOVER HO AND CAV TEST TEST START TIME 10/ 5/88 14:59:35.90 -26 OHI BSAN 950 Accel X Axis -25 FLOH 1 R ATIO IND 905 LUBE OIL SUP T 18.234 5.7014 1.2605 1.2605 1.2605 1.2605 1.2605 1.2605 1.26647 1.163647 1.163647 1.16368 1.1637 1.065733 1.065733 1.065733 1.0 93.645 92.712 11522 . . 904 Gear cas e temp G-BOX TE MP ALARM 133.87 926 HEADER: Test 82A094 MDS# TYPE TYPE 2 401 3/a ₽/F ID∯ MDSE 110 500 000 -00-500 00-500

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-105.69

0.31593E+12

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text.output:10/12/88 2:15 PM

- 18 -

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PROCESS TIME 10/12/88 14:03:21 AVERAGED DATA ON MEASUREMENT DATA SETS CROSSOVER HQ AND CAV TEST TEST START TIME 10/ 5/88 14:59:35.90 PROCESS TIME 10/ HEADER: Test 88A094

0 1031		C 1031	NT 7011 1491			Frocess 11115		17.00-61		
P/F ID		-195	-800	-801	-152	-808	-809	-810	-811	-812
	,	SCALED H	INDUCER	INDUCER	FLOH 1 R	IMP STAT	XOVR U/S	XOVR D/S	XOVR D/S	XOVR D/S
		EAD IND.	TOT-ST H	TOT-ST H	ATIO IND	IC HEADR	T-T HEA	TT READ	TT HEAD	TT HEAD
NDS4	TYPE	£ 1	EAD #1	EAD #2	•	ISE	DRISE	RISE #1	RISE #2	RISE #3
,	-	0.66111E410	0.35421 -	-0.75170	18.234	-0.57728	-2.0294	4.5761	1.7916	2.7644
2	~~	0.27447E+09	38.310	28.612	5.7014	729.37	185.39	113.07	111.12	110.02
. (* 1	-	43232.	41.212	34.072	1.2605	913.21	313.14	138.27	129.86	130.03
-	-	40207.	21.478	15.033	1.3417	889.64	266.09	153.71	142.62	143.36
- vh	-	43370.	40.466	32.923	1.2615	913.58	317.04	139.28	128.85	129.01
Q	. 4	4859.	63.301	54.302	1.1647	916.81	242.79	151.46	141.86	139.99
2		45382.	87.747	69.776	1.0660	1042.3	297.33	138.11	124.20	121.61
œ	•-•	4 6611.	112.69	85.105	0.96852	1081.8	425.50	136.88	123.41	119.06
a	-	6 8383.	130.90	100.62	0.86855	1092.2	321.27	148.04	132.78	121.09
10	-	46593.	112.54	84.832	0.96905	1078.4	387.37	138.97	127.21	122.52
	-	65279.	68.753	68.862	1.0670	1054.0	372.98	138.61	121.68	125.05
2	-	4160.	65,810	51.252	1.1636	1031.5	365.63	142.20	130.75	137.71
13	~	12221.	66.841	53.292	1,1588	977.86	377.86	137.35	123.68	131.13
14	2	15708.	88.083	67.016	1.0673	1067.0	393.23	146.92	131.88	132.92
15	~	(3677.	86.346	67.406	1.0618	1014.0	394.67	136.34	121.23	122.37
16	2	46613.	107.27	84.394	0.96851	1064.6	411.77	132.81	118.78	110.30
17		-0.162558+10	0.64980E-01	-1.0191	-0.54076	-0.67307	-2.1304	4.0739	2.7443	2.3316

HOI J/d	-813	-152	-815	-816	-817	-818	-819	
	STAGE T-	FLOW 1 R	XOVR TT	PUMP TT	RESULTAN	RESULTAN	NET AXIA	
	T HEADRI	ATIO IND	HEADRISE	HEADRISE	T AXIAL	T AXIAL	L LOAD	
YT SOM	.be se	. 4 2	# 2		LOAD (-)	LOAD (+)		
	3.2246	18.234	-0.23779	3.4653	10385.	9978.8	406.29	
2	805.48	5.7014	296.51	509.47	6 6393.	50000.	-3607.3	
1	1160.7	1.2605	643.00	718.33	59570.	63603.	-4033.4	
4	1079.1	1.3417	11.804	670.99	56438.	60276.	-3837.9	
5	1165.0	1.2615	445.89	719.72	59518.	63563.	-4045.2	
9	1204.6	1.1647	384.65	820.63	61603.	66346.	-4742.7	
	1218.4	1.0660	421.53	797.57	63608.	67898.	-4290.2	
- 60	1251.9	0.96852	548,91	703.60	65844.	70260.	-4415.9	
0	1.298.1	0,86855	454.05	845.08	68407.	73036.	-4628.6	
10 1	1251.4	0,96905	514.58	737.43	.65999.	70378.	-4378.4	
	1215.0	1.0670	494.65	720.88	63296.	67641.	-4344.2	
12	1184.8	1.1636	496.38	689.00	61697.	65821.	-4123.4	
13	1133.4	1.1588	501.56	632.34	52455.	56631.	-4176.6	
-	1227.0	1.0673	525.11	702.40	64060.	68549.	-4488.2	
10	1172.5	1.0618	515.90	657.02	52248.	56959.	-4711.2	

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-819

-818

-817

- 19 -

	14:03:21	-819 Net a y
ST	10/12/88	-818 Resultan
REMENT DATA SE	PROCESS TIME	-817 Resultan
DATA ON MEASU	£:59;35.90	-816 PUMP TT
AVERAGED	5T 0/ 5/88 1	-815 Xour 7t
	IQ AND CAV TE Start Time 1	-152 FION 1 R
	CROSSOVER H	-813 57100 4-
	HEADER: Test 802094	₽/F ID∳

-819 NET AXIA L LOAD		-5162.7 421.72
-818 RESULTAN T AXIAL	(+) GNOI	62801. 9967.0
-817 RESULTAN T AXIAL	LOAD (-)	57638. 10389.
-816 PUMP TT HEADRISE		721.55 -1.5031
-815 Xovr TT Headrise	4 2	530.56 0.61385
-152 FLOH 1 R ATIO IND		0.96851 -0.54076
-813 STAGE T- T HEADRI	35	1251.7 -0.88846
*	TYPE	25
oI <i>al</i> a	₩DS	16 17

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EDF.DIR				- :	1
DIRECTORY EDF HDR:	FILE: RUN XOVER HQ	NUM: 88A096 CAV TEST	,	T	D

8:03 PM

EDF.DIR	- 1 -	edf.diz_10/09/8	8
DIRECTORY FILE: RUN NUM: 88A096 EDF HDR: XOVER HQ CAV TEST	, T DATE: 10/	8/88, N MDS= 37, N CPS	×
ICP: 1 801 2 228 231 806 807 808 818 120 819 820 838 900 901 903 4 953 850 851	229 802 803 809 810 811 821 822 826 902 904 905 926	804 805 230) 812 813 815 7 5 3 950 951 952	
MDS NSCANS TYPE HEADER 1 20 1 PRE STATIC 90 2 158 2 START UP 3 20 1 582 GFM HQ 4 20 1 582 GPM HQ 5 20 1 640 GPM HQ 6 20 1 640 GPM HQ 7 20 1 582 GPM HQ 8 20 1 524 GPM HQ 9 20 1 466 GPM HQ 10 20 1 437 GPM HQ 11 20 1 349 GPM HQ 13 20 1 349 GPM HQ 14 20 1 347 GPM HQ 15 20 1 524 GPM HQ 16 20 1 524 GPM HQ 21 <			
T S TIME: 7:26:17.20, P DATE: 10 N WS= 70, N W STAT= 74, N ST ID W: 1 801 2 228 2: 231 806 807 808 80 816 818 120 819 80 938 900 901 90 952 4 953 850 80 -101 -106 -107 -34 -1 -801 -808 -809 -810 -8	0/09/88, P P TIME: 1 AT= 37 29 802 803 80 09 810 811 81 20 821 822 81 03 902 904 90 51 926 -152 -1 93 -194 -195 -2 11 -812 -813 -802	19:25:39 04 805 230 12 813 815 26 7 5 05 950 951 25 -26 -100 02 -203 -800 14 -815 -816 805 230	

2	158	2 ST	ART UE)							
3	20	1 58	2 GFM	HQ							
4	20	1 58	2 GPM	HQ							
5	20	1 69	8 GPM	HQ							
6	20	1 64	0 GPM	HQ							
7	20	1 58	2 GPM	HQ			•				
8	20	1 54	4 GPM	HQ							
10	20	1 43	7 CDM	NG NG							
11	20	1 40	7 GPM	HO							
12	20	1 37	8 GPM	HO							
13	20	1 34	9 GPM	HQ							
14	20	1 34	9 GPM	HQ							
15	20	1 37	8 GPM	HQ							
16	20	1 40	7 GPM	HQ							
17	20	1 43	7 GPM	HQ							
18	20	1 46	6 GPM	HQ							
73	20	1 54	4 GPM	HQ HQ							
20	20	1 64	A COM	HQ HQ							
22	20	1 69	A GPM	HO							
23	972	2 58	2 GPM	CAV							
24	824	2 64	0 GPM	CAV							
25	128	2 69	8 GPM	CAV							
26	531	2 58	2 GPM	CAV							
27	847	2 52	4 GPM	CAV							
20	035	2 40	O GPM	CAV							
30	181	2 20	n Staf	07 110							
31	934	2 58	2 GPM	CAV							
32	913	2 40	7 GPM	CAV							
33	20	1 20	ST STA	TTC 80	1						
34	200	2 38	D STAF	T JP							
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31	20	7 50	21 211	1110 BO	1						
* 5	TTME -	7 . 26 . 1	7 20.	p har	E. 10/	09/88.	דידי מ	NE - 10	.25.30		
้ทั้ง	wS= 70.	NW	STAT	74.	N STAT	₩ 37		-9 Held 4 - 42 4/	160100		
ID V	N: 1	801	2	229	229	802	803	804	805	230)
·	231	806	807	808	809	810	811	812	813	815	3
	816	818	120	819	820	821	. 822	826	1	<u>ب</u>	5
		838	900	901	. 903	902	904	905	950	951	L
	952	4	953	850	851	926	-152	-29	-26	-100	2
	-101	-106	-107	-34	-193	-194	-195	-202	-203	900)
	-801	808	~805	-810		~812	2 -81J	-814	-813	-810	220
IW	STAT:	1	801	2	228	229	802	803	804	805	230
		231 916	000	0U/ 910	808 190	810	820	831 831	822 822	013 013	0UZ 7
		04J 5	2	848	900	901	9020	902	904	905	950
		951	952	4.00	953	850	851	926	-152	-25	-26
		-100	-101	-106	-107	-34	-152	-193	-194	-195	-202
		-203	-800	-801	-152	-808	-809	-810	-811	-812	-813
		-814	-152	-815	-816						
M W	1 REC:	З	23	181	201	221	241	261	281	301	321

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AVERAGED DATA ON MEASUREMENT DATA SETS

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			AVENANEU UAL	ADGADE ND AL	IC UTUR INTUR	212				
HEAUEK: Test 88A096	TEST TEST	AV TEST START TIME I	10/ 8/88 7:2	16:17.20	PROCESS TIME	01/05/89	13:05:42			
401 3 /a	-813	-152	-815	-816	-817	-818	-819	-814	-820	
	STAGE T-	FLOW 1 R	XOVR TT	PUMP TT	RESULTAN	RESULTAN	NET AXIA	STAGE EF	CMOMENTL	
MDS& TYPE	55 52	1		7ct 1/1/20	LOAD (+)	(-) GYOT	TYOT T			
1	1.9290	-0.18862	0.608612-01	1,8699	6639.7	9647.2	-3007.5	-0.11455	0.51631E-06	
5	1051.7	1.2422	477.59	575.05	£9007.	4 8067.	519.13	0.45537	25.738	
3	1226.1	1.2643	554.44	672.76	5 5798.	61582.	-5784.7	0.51964	31.937	
	1300.8	1.1827	593.40	708.63	58527.	63470.	-4942.9	0.52546	27.928	
 	1148.9	1.3421	513.28	636.72	52814.	59047.	-6233.1	0.51275	35.969	
7 9	1226.0	1.2651	554.78	672.29	55766.	61747.	-5981.3	0.52198	31.954	
7	1300.6	1.1836	594.52	707.23	58538.	63400.	-4862.1	0.52636	27.968	
8	1362.9	1.0977	632,36	731.79	60964.	64957.	-3993.1	0.52641	24.065	
5	1420.3	1.0126	650.48	771.08	63212.	66368.	-3156.5	0.52409	20.481	
10	1434.7	0.98131	646,98	789.01	63966.	68159.	-4193.8	0.51588	19.227	
	1465.3	0.92781	664.85	801.76	65205.	69548.	-4342.7	0.50956	17.179	
12	1486.6	0.88381	677.78	810.10	66087.	70544.	-4457.1	0.50228	15.593	
13	1500.9	0.83499	684.58	817.57	66702.	71269.	-4566.6	0.49087	13.919	
	1499.7	0.83558	687.03	813.92	66731.	71341.	-4610.0	0.49073	13.935	
15	1390.6	0.87895	573.57	BI8.33	63942.	69375.	-5433.4	0.46361	15.421	
-1-	1380.9	0.92462	572,80	15.909	63436.	68946.	-5510.1	0.47536	17.062	
1 1	1430 A	0.98620	679.10	758.45	64128.	69329.	-5201.0	0.51538	19.400	
18	1410.0	1.0341	668.43	742.66	63125.	68314.	-5189.1	0.51990	21.334	
1 51	1367.7	1.1253	639,62	11.602	60562.	66095.	-5532.9	0.52508	25.284	
20	1279.3	1.2180	601.69	678,63	57802.	63313.	-5511.4	0.52478	29.585	
21 1	1194.3	1.3076	548,68	646.63	54650.	60278.	-5627.1	0.51777	34.136	
22	1137.8	1.3612	513.50	625.20	52566.	60131.	-7565.7	0.50985	37.012	
23 23	1157.8	1.1602	586.03	582.60	42188	50401.	-8212.7	0.48706	27.046	
24 2	1017.1	1.2453	529.70	.88.00	36486.	44132.	-7645.9	0.45308	31.177	
2 42	347.86	1.3288	486.78	461.66	36023.	43497.	-7473.4	0.43815	35.303	
26	740.82	1.3083	337 13	323.76	23594.	30117.	-6522.5	0.36293	34.502	
	1.508.9	1580.1	634.16	670.49	1 8387.	56761.	-8374.4	0.51179	23.468	
200			50° T/0			. 0292C	-1620.0	0.51642	20.415	
20	200 DO	0.78004	081,10	*****	60175.	65972.	8.1916-	U.51634	19.433	
20 20	939.29	2.8127	634.9 4	504.91	.0111	50149.	-5679.8	-0.48905	25.136	
31	1161.0	1.1631	584,87	576.80	£ 2386.	50589.	-8202.6	0.48363	27.107	
32 22	1456.5	0.92327	706.23	741.08	54122.	60927.	-6804.7	0.50684	16.915	
	1648.2-	27.257	0.51741	-3.3700	. 6355.8	9435.1	-3079.3	-18.538	0.12027E-02	
	11004			20.025		.11010	-1717-	-U.JJ618	P85.02	
-1 C	1402.4	G. 7.3 / 84	635.55	757.72	64159. 74000	69997.	-5837.7	0.41975	10.876	
30	1,282.4	0.61349	603.20	786.69	55033.	61861.	-7827.2	0.44800	13.045	
37 1	-1.8889	22.021	0.98010	-2.8719	6268.6	9340.7	-3072.1	-11.587	0.13436E-02	

loads:01/04/89 5:48 F

SOAD3

1 91 1

PROCESS TIME 01/04/99 17:23:31 AVERAGED DATA ON MEASUREMENT DATA SETS 6607.3 335205. 335205. 335205. 3375991. 3375991. 460503. 465533. 465533. 465533. 3355261. 3375223. 337522. 337522. 33752. 33752. 337522. 337522. 337522. 3375. 33752. 33752. 33752. 3375. 33752. 33752. 33752. 3375. 33752. 33752. 33752. 3375. 33752. 33752. 33752. 33752. 3375. 33752. 33752. 33752. 3375. 33752. 33752. 3375. 3375. 33752. 3375. 35 -825 AIMPL TDLAFTL 6014.5 66014.5 7:26:17.20 -823 TDUAFTL Particle participation pa XOVER HO CAV TEST TEST START TIME 10/ 8/88 -822 FIMPL -821 TOFHDL 3085.0 20480 203398 203398 203398 203398 20339 20359 20050 20359 20050 20050 20 22153 223377 225947 19695 225565 245565 245565 263811 26381 26381 26381 \$.0795 HEADER: Test 88A096 TYPE ~~~~ **₽**/5 10 **HSQU** 4500

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NSOVOT

AVERAGED DATA ON MEASUREMENT DATA SETS XOVER HO CAN TEST

HEADER:	-1	KOVER HO CA	U TEST U				
TEST 881	9601	TEST	START TIME	10/ 8/88	7:26:17.20	PROCESS TIME 01/05/89	13:05:42
P/F ID		-821	-822	-823	-824	-825	
		TOFNDL	LUMIS	TDUAFTL	TDLAFTL	AIMPL	
λ⊥ ∦ SGM	BE.						
* - 1		3085.0	-1006.4	1304.8	593.62	6607.3	
2	.	20452.	20589.	5468.6	6056.5	35205.	
сч (М		23391.	23962.	9369.8	11175.	39694 .	
4		24661.	25047.	5460.3	11294.	41277.	
ي م		22074.	22683.	0.48.00	10753.	37997.	
••		23393.	23926.	9441.0	11269.	39694.	
7 1		24564.	25054.	9431.8	11257.	41273.	
8		25706.	26114	5440.I	11268.	\$2723.	
6		26668.	27076.	9430.9	11256.	44 066.	
10		26910.	27511.	9923.7	11902.	44703.	
		27433.	28058.	10174.	12231.	€5465.	
12		27793.	28449.	10334.	12441.	4 6052.	
13		28039.	28715.	10437.	12576.	46503.	
14 1	_	28025.	28752.	LOAA6.	12588.	(6553.	
15 15		26172.	28139.	10013.	12019.	45621.	
16		26011.	27899.	4.7222	11999.	4 5272.	
		26933.	27697.	10294.	12388.	45040.	
81		26506.	27255.	10137.	12182.	4 430.	
19		25456.	26050,	9887.4	11855.	42861.	
20		24268.	24857.	9436.0	11262.	£1225.	
21 1		22825 .	23573.	6954.4	10630.	39406,	
22		21859.	22724.	5431.3	11256.	38224.	
23 23		19679.	17850,	8161.9	2.888.2	31349.	
	• /	17209.	15092.	7436.2	6638.5	27523.	
20		16544.	1521	7212.7	6345.4	27333.	
26 2		12009.	9117.8	5060.0	5520.7	19267.	
21		22153.	20929.	9326.1	1119.	35628.	
28	- /	23377.	22162.	9386.0	11197.	37332.	
23 17 17 17	_	25947.	25958.	9376.9	11973.	{ 2685.	
30		18600.	18378.	7571.6	8816.5	32492.	
31		19695.	17942.	8481.7	10011.	314 90.	
32		24566.	23550.	5493.3	11338.	39261.	
33	•	2984.3	-1130.5	1289.3	573.11	6453.7	
34		19082.	18526.	7837.8	9165.7	33234.	
50		26381.	28042.	10265.	12350.	<pre>45602.</pre>	
36 2		23639.	24291.	9425.7	11249.	4 0251.	
37 1		2970.4	-1173.1	1278.2	5 58.63	6391.1	

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EDF.DIR		- 1 -		edf.d:	Lr_10/11/38	8:03 AM
DIRECTORY FILE: RU EDF HDR: CROSSOV	IN NUM: 88A097 Ver Test	, T DATE	: 10/10/88,	N MDS-	46, N CPS=	45
ICP: 1 80 231 80 818 12 838 90 4 95	2 228 6 807 808 20 819 820 30 901 903 33 850 851	229 802 809 810 821 822 902 904 926	803 804 811 812 . 826 7 905 950	805 813 5 951	230 815 3 952	
MDS NSCANS TYPE	HEADER					
1 20 1 PRE 2 139 2 STAR 3 132 2 4 20 1 463 5 20 1 582 6 20 1 524 7 20 1 495 8 20 1 466 9 20 1 437 10 20 1 407 11 189 2 2ND 12 20 1 442 13 20 1 400 14 20 1 375 15 20 1 359 16 20 1 331	STATIC (90 PSIA RT UP GPM GPM GPM GPM START UP				·	
17 20 1 302 19 20 1 272						
19 20 1 243						
20 20 1 21 97 2 38D	START IIP					
22 252 2 4TH	START UP					
23 300 2 5TH 24 183 2 6TH	START UP STARTUP					
25 20 1 441						
27 20 1 375						
28 20 1 359 29 20 1 331						
30 20 1 302						
31 20 1 272 32 20 1 243						
33 20 1 243 34 20 1 272						•
35 20 1 302						
36 20 1 331 37 20 1 359						
36 20 1 375 39 20 1 400						
40 20 1 442						
41 681 2 442 42 14 2	gpm					
43 188 2 7TH	START UP					
44 182 2 STAR 45 175 2 STAR	T UP					
46 717 2 375	CAV					
T S TIME: 14:37:48.	70, P DATE: 10/	11/88, P T	NE: 07:42:5	8		
NWS= 70, NWST IDW: 1 801	AT- 74, N STAT 2 229 229	₩ 46 802 803	804 80	5 230		
231 806 816 818 3 838 952 4 -101 -106 -901 -909	807 808 809 120 819 820 900 901 903 953 850 851 -107 -34 -193	810 811 821 822 902 904 926 -152 -194 -195	$ \begin{array}{cccccccccccccccccccccccccccccccccccc$.3 815 7 5 60 951 6 -100 93 -800		

EDF.DIR

HA 89:5 68/90/01/01/01/02

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AVERAGED DATA ON MEASUREMENT DATA SETS 7:26:17.20 XOVER HO CAV TEST TEST START TIME 10/ 8/88 HEADER: Test 83A096

PROCESS TIME 01/04/89 17:23:31

	-813 87AGE T-	-152 FLOW 1 R	-BIS Xovr TT	-816 Pump TT	-817 Resultan	-818 Resultan	-819 Net Axia	-814 STAGE EF	-820 Cmomentl
T HEADRI Se		ATIO IND	HEADRISE 42	HEADRISE	T AXIAL LOAD (-)	T AXIAL LOAD (+)	L LOAD	FICIENCY	
1.9290		-0.18862	0.608612-01	1.8699	10687.	10145.	541.90	-0.11455	0.51631E-06
1051.7		1.2422	<77.59	575.05	53056.	4 8566.	4490.4	0.45537	25.738
1226.1		1.2643	554.44	672.76	59848.	62081.	-2232.6	0.51964	31.937
1300.8		1.1827	593.40	708.63	62577.	63968.	-1390.8	0.52546	27.928
1148.9		1.3421	513.28	636.72	56865.	59546.	-2681.1	0.51275	35.969
1226.0		1.2651	554.78	672.29	53816,	62246.	-2429.4	0.52198	31.954
1300.6		1.1836	594.52	707.23	62588.	63898.	-1310.2	0.52636	27.968
1362.9		1.0977	632.36	731.79	65015.	65456.	-441.23	0.52641	24.065
1420.3		1.0126	650.48	771.28	67262.	66856.	395.31	0.52409	20.481
1436.7		0.98131	646.98	789.01	68016.	68658.	-641.98	0.51588	19.227
1465.3		0.92781	664.85	801.76	69255.	70046.	-791.00	0.50956	17.179
1485.6		0.88381	677.78	810.10	70137.	71042.	-905.48	0.50228	15.593
1500.9		0.83495	684.58	817.57	70752.	71767.	-1015.0	0.49087	13.919
1499.7		0.83558	687.03	813.92	70781.	71839.	-1058.4	0.49073	13.935
1390.6		0.87896	573.57	618.33	67992.	69873.	-1881.9	0.46361	15.421
1380.9		0.92462	572.80	609.31	67486.	69445.	-1958.6	0.47536	17.062
1436.4		0.98620	679.10	758.45	68178.	69827.	-1649.5	0.51538	19.400
1410.0		1,0341	668.43	742.66	67175.	68813.	-1637.6	0.51990	21.334
1347.7		1.1253	639.62	709.11	64611.	66593.	-1981.5	0.52508	25.284
1279.3		1.2180	601.69	678.63	61851.	63811.	-1960.0	0.52478	29.585
1194.3		1.3076	548.68	646,63	58700.	60776.	-2075.8	0.51777	34.136
1137.8		1.3612	513.50	625.20	56615.	60630.	-4014.4	0.50985	37.012
1167.8		1.1602	586.03	582.60	€ 6237.	50699.	-4661.6	0.48708	27.046
1017.1		1.2453	529.70	488.00	(0535.	44630.	-4095.2	0.45308	31.177
947.86		1.3288	486.78	4 61.66	€0072.	6 3995.	-3922.9	0.43815	35.303
740.82		1.3083	\$17.45	323.76	27643.	30615.	-2972.1	0.36293	34.502
1308,9		1.0831	634.15	675.49	52435.	57259.	-4824.2	0.51179	23.468
1388.4		1.0111	671.89	717.27	55042.	59118.	-4076.1	0.51642	20.415
1429.9		0.98664	687.10	743.54	64222.	66470.	-2248.0	0.51634	19.433
939.29		2.8127	434.94	504.91	(8517.	50647.	-2130.0	-0.48905	25.136
1161.0		1.1631	584.87	576.80	46435 .	51087.	-4652.2	0.48363	27.107
1446.5		0.92327	706.23	741.08	58170.	61425.	-3254.6	0.50684	16.915
-2.8491		27.257	0.51/41	-3.3700	10404.	9 933.1	470.44	-18.538	0.12027E-02
968.13		3.3650	448.01	520.68	49646.	52015.	-2369.2	-0.53618	25.384
1402.4		0.73784	635.55	767.72	68207.	70495.	-2287.7	0.41975	10.876
1389.4		0,81349	603.50	786.69	58081.	62359.	-4277.5	0.44800	13.045
-1.8889		22.021	0.98010	-2.8719	10316.	9038.7	477.43	-11.587	0.13436E-02

EQNO1

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AVERAGED DATA ON MEASUREMENT DATA SETS

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NET AXIA L LOAD 541.90 -819 12:53:52 -818 RESULTAN T AXIAL LOAD (+) PROCESS TIME 10/12/88 -817 RESULTAH T AXIAL LOAD (-) -816 PUMP TT Headrise 7:26:17.20 -815 Xovr TT Beadrise 12 0.98010 XOVER HQ CAV TEST TEST START TIME 10/ 8/88 -152 FLOW 1 R ATIC IND . 41 -813 Stage T-T headri 33 HEADER: Test Bea096 JAYT P/F ID **HDS**

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- 32 -

HEADER:		CROSSOVER .	Test	AVTRAGED I	DATA ON MEASU	REMENT DATA S	ETS			
TEST 85	3A097	TEST	START TIME	10/10/88	1:37:48.70	PROCESS TIME	10/12/88	12:39:00		
P/F ID	- 141	230	231	806	807	808	608	810	811	812
		D/S STAT	D/S STAT	DIM NMD	UPC CONS	UPC CONS	UPC CONS	TRANSITI	DWN DIFF	DWN DIFI
		. PRESS.	. PRESS.	DIFF #1	T SEC PR	T SFC PR	T SEC PR	ON ST PR	DISCH P	DISCH H
NDS¥ 1	IYPE	INP #1	IMP #2		# 3	#2	5 #		R #1	R #2
26	-1	562.64	562.10	702.89	697.48	692.52	699.77	697.61	705.33	704.04
27	-	567.66	567.36	711.38	706.44	701.69	708.63	706.10	713.65	712.43
28	1	569.95	569.69	715.31	710.63	706.29	712.82	710.19	717.52	716.47
29	-	574.08	574.48	722.44	718.82	714.38	719.97	716.93	724.38	723.62
30		579.27	579.04	729.91	727.96	721.68	727.50	724.81	731.53	731.18
31		572.57	569.10	679.15	672.57	667.63	673.56	671.68	681.78	681.05
32	1	579.33	580.49	683.11	676.82	671.97	675.83	676.50	686.02	684.89
33	1	582.61	580.63	682.21	675.48	672.14	675.35	675.13	685.52	684.51
34	-	573.87	575.49	678.93	672.13	666.75	672-63	E71.36	601.55	600.77
30	7	571.30	571.58	677.01	670.03	665.51	669.58	669.42	679.87	679.29
36	-1	566.13	568.36	676.03	668.63	653.01	670.06	668.51	679.17	678.53
ጦ. የጎ	-	562.67	562.51	673.40	666.76	660.35	666,35	€ ⁶ 5.80	676.08	675.64
36	 4	559.78	559.35	670.85	663.55	658.14	663.43	6 .4.10	673.90	673.42
đ۱ ۳	~	557.89	553.52	667.24	659.66	653.87	659.12	658.36	670.28	669.65
40	1	550.78	549.13	675.98	669.11	661.76	671.59	668.08	678.97	677.73
	2	474.81	472.89	614.64	610.38	604.79	611.50	610.11	617.59	617.08
- Z	2	79.528	77.562	75.980	77.549	77.213	77.392	75.298	77.932	77.552
(Y) -	2	456.26	455.49	561.95	556.99	551.85	558.10	556.07	564.53	563.45
	2	491.36	450.38	609.15	603 .94	598.42	605.29	603.16	611.69	610.56
υ) Έ	2	484.43	483.59	598.32	591.95	586.42	592.84	591.07	600.80	599.72
4 6	3	398.80	396.36	482.47	477.98	474.15	478.54	476.64	&84.92	484.44
. •										
D/2 The		613	803	212	818 8	100	010	000	100	с с о
	L .	DEN CONS	TMD FLD	XOUPP DI	TRPNST N	77 TOT	TTT TAL	AJ GANUA	AD 170	770 770
			SHRCHD P	SCH ST P	ISK DEAT	PRESS. 1	ON TOTAL	TT TOTAT.	TT TOTAL	TT TOTAL
I ∦ SGN	347.	1	R #1	R 41	N PK	IH HI	PR	PR #1	PR #2	PR #3
		77.195	76.880	76.757	76.647	15.778	74.832	74.306	75.278	75.319
2	2	78.439	78.714	78.410	77.879	77.235	75.538	75.972	J6 .971	76.774
m	2	524.82	372.29	533.44	420.65	327.41	493.29	543.60	541.10	543.60
बहो । इ	.	617.17	411.67	626.15	472.74	371.93	587.15	636.58	632.98	635.74
ŝ	-1	689.83	447.60	693.45	514.41	402.42	667.98	702.47	693.55	700.10
Ś		711.95	456.98	714.41	527.49	405.6	696.57	723.40	715.35	720.16
~ (i ,	11	438.34	111.10	300.00	50,005	649.68 222 22	120.021	20 911	20.52/
Ċ,	.	726.35	462,98	726.18	536.23 503 27	409.01 01.00	713.56	735 . 61	727.93	731.65
л¢	-4	613.6r	0 + / QCV	041.10	- 05-10C	422.80 112 50	655 01	688.82 601 62	020 - 20 200 - 50	CC./89
	4 (*					200 60		553 1A	550 1A	10.000 NC 144
4	4	プラ・ファロ		こうちょう				ドイ・コンク		ドー・の しつ

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		5	AVERAGED DA	NTA ON MEASU	REMENT DATA S	ETS			
reauck: Test 88A097	CROSSOVER	VEST START TIME	10/10/88 14:	:37:48,70	PROCESS TIME	10/12/88 1	00:6E:2	·	
p/f ID#	1 INLET ST ATIC PRE SSURR. P	801 INLET ST ATIC PR 62	2 Flohmzte R §1	228 D/S STAT , PRESS. YND 41	229 D/S STAT . PRESS. TND #2	802 IMP FRD SHROUD P R #1	803 IMP FWD Shroud P B 4 2	804 IMP AFT Shroud P P #1	805 IMP AFT Shkoud P B #2
1	<u>50.968</u>	90.812	579.49	115.95	115.61	443.36	396.21	508.66	507.33
	27.024	26.766 92.504	5.2102 4.2102	16.15/ 76.256	48.505 78.433	364.69	326.05 70.438	430.52	431.05
2 C C C C	91.112	92.159 92.159	51 44 N 01 V 14 V 14 V 14 V 14 V 14 V 14 V 14 V 1	10/.13	110.73	394.96	326.41	453.78 453.78	421.90
4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	91.071 61.197	51.703	380.89	106.36 81.473	106.41 81.361	389.38 321.12	353.51	446.16 365.75	446.62 366.30
			,	•					
₽/F ID∯	230 D/G 5785	231	806 Duni 147D	807 000 COUS	808 TDC 2013	809 1100 0010	810 205N6721	811 Dian Dian	812 Dem D TOP
	ere eress.	PRESS.	TH AALG	T SEC PR	T SEC PR	T SEC PR	TITENAAL	DISCH P	DISCH P
MDS# TYPE	INP 41	IMP #2	, , ,		1	5		R #1	R #2
c	78.274	77.140	105-55 205-55	76.705	76.108	76.984	75.402	76.868	76.758
9 0 9 0	100, 201 141 25		630.663		51. 440 516 75	10.040 501 05	503 76	10.6/1 535 75	CCI.07
) w	510.79	507.99	625.40	615.43	609.41	616.52	616.14	628.35	627.12
ын 4 40 Ч	556.66	555.71	693 .58 25 . 56	687.10	681.49	689.00	687.36	695.54	694.55
-1 + 4 -	570.01	571 67	L5 212 TT-571	14.201	704.15	711.80	709.08	716.29	715.25
• œ	17.113	577.71	725.69	722.93	717.48	724.06	721.23	728.02	727.06
ы Э.	571.75	569.59 111	679.30	672.11	666.07	673.11	671.55	681,91	681.24
7 7 7	212.54 142.54	10.144	245.19	539.62	534.42 534.43	540.45 540.45	539.03 539.03	682.48 547.55	683.UU 546.20
12	550.58	549.54	669.42	683.85	677.53	685.62	683.90	691.99	690.73
	563.76	563.37	706.19	700.90	695.54	703.19	701.44	708.47	707.25
-4	571 22	1000 C 1000	718 04	312.28	709.36	215.07	712 35	720 50	719 53
1	571.53	567.04	675.96	668.51	663.44	669.33	668.55	678.85	677.80
17 1	569.62	573.61	678.27	671.86	666.94	672.63	670.02	680.94	680.04
	579.87	577.24	680.53	674.43	669.83	673.88	672.03	684.16	683.02
	76.730	15.403	12.054	74.614	191.197	74.811	72.820	75,103	74.448
24	258.96	258.43	285.53	283.40	281.01	283.83	281.79	287.70	287.21
22 22	339.11	337.31	375.69	374.37	372.31	374.23	371.22	377.26	376.56
0 0 01 0	161.00	159.04	178.70	178.09	176.14	178.11	176.06	180.92	180.43
22 52	550.52	549.06	589.11	583.25	677.35	584.98	682.83	691.76	690.54

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AVERAGED DATA ON MEASUREMENT DATA SETS

PROCESS TIME 10/12/88 12:39:00 CROSSOVER TEST Test Start Time 10/10/88 24:37:48.70 HEADER: TEST 88A097

MILEY ST TALONGETE D/S STAT T/S STAT	P/2 104		801	N	228	229	802	803	804	805
Dote True Arric Free Arric Free Arric Frees. Freeses. Freeseseseseses Freeseses Free		TRLET ST	TRIET ST	BLOWNER	D/S STAT	D/S STAT	UME EMD	IMP EWD	IMP AFT	IMP AFT
1 1 0.64 1.10 0.125 1.11 0.45 1.11 0.45 1.11 0.45 1.11 0.45 1.11 0.41 1.4 1.11 0.45 1.11 0.45 1.11 0.45 1.11 0.41 1.11 1.11 1.11 1.11 1.11 1.11 1.11 1.11 1.11 1.11 1.11 1.11 1.11 1.11 1.11 1.11 1.11<		ATIC PRE	ATIC PR	R #1	. PRESS.	. PRESS.	SHROUD P	SHROUD P	SHROUL P	SHROUD P
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	HOSE TYPE	SSURE, P	1 2		IND FI	IND #2	R #1	R #2	R #1	R #2
2 91.235 91.444 56.123 75.445 75.33 75.445 75.33 6 1 50.757 711.67 719.675 717.652 79.666 717.65 717.75 759.737 758.34 757.35 75	1	90.861	31,100	0,13083	77.611	77.060	76.880	74.766	73.596	77.950
7 91 70 91 70 91 70 91 70 91 </td <td></td> <td>91,265</td> <td>91.424</td> <td>54.122</td> <td>76.495</td> <td>76.539</td> <td>78.714</td> <td>76.834</td> <td>75.339</td> <td>79.847</td>		91,265	91.424	54.122	76.495	76.539	78.714	76.834	75.339	79.847
4 9.671 90.672 91.672 91.675 91.755 91.675 91.755	- CN	91.236	91.227	0E.2ET	91.131	90.700	372.29	349.32	418.49	418.19
5 1 90.759 90.076 57.65 56.47 6 1 90.759 90.076 572.15 115.05 <td></td> <td>90.871</td> <td>90.672</td> <td>711.62</td> <td>\$7.562</td> <td>97.676</td> <td>411.67</td> <td>390.37</td> <td>469.85</td> <td>457.79</td>		90.871	90.672	711.62	\$7.562	97.676	411.67	390.37	469.85	457.79
6 1 90.885 90.875 91.676 513.55 124.13 132.120 456.98 434.67 528.26 15 90.375 90.375 90.486 513.55 127.13 137.10 465.67 228.47 533.40 533.40 533.40 534.67 533.41 5	- SJ	937.06	90.881	578.63	116.03	115.32	447.60	427.51	512.05	511.36
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$		90.855	969.09	51.01.0	124 13	123.20	456.98	434.67	526.44	525.29
6 1 27.5 90.705	-	127.02	91.060	502.19	124.78	124.10	458.34	435.81	528.20	526.91
9 1 0.000 000	 30	50. 735	90.109	466.67	128.24	127.54	461.98	424.72	534.16	532.68
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$		69,850	90.420	435.40	132.34	132.08	467.48	471.95	529.10	533.12
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	19	50.108	88.340	402.81	135.14	134.24	476.12	434.51	539.15	534.22
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	11 2	181.08	\$00.05	526.59	101.52	102.03	357.84	338.37	409.37	411.48
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	12 1	69.630	89.491	578.57	115.62	115.65	440.93	438.33	508.79	509.91
16 180.702 90.664 513.52 123.12 125.33 455.36 417.86 534.55 17 1 90.702 90.792 90.792 90.779 457.36 417.86 534.55 17 1 91.772 96.779 456.00 122.374 457.36 417.86 537.55 18 1 91.470 322.11 123.74 137.30 477.31 436.65 537.55 20 1 91.470 322.12 132.57 455.13 440.49 537.55 20 1 91.470 322.14 137.30 477.31 440.49 537.55 21 22 90.473 327.12 139.62 139.62 440.49 537.55 21 22 90.779 327.51 139.62 139.62 139.69 537.65 22 20.65 119.65 119.65 119.65 119.65 139.67 340.27 343.28 22 90.076 54.67 55.6	13 1	\$2.024	90.886	539.61	120.23	119.65	451.86	448.82	519.36	519.03
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	14 1	90.702	9 0.68∉	513.52	123.12	122.28	455.38	417.86	524.57	524.21
16 90.072 90.0814 467.00 129.33 466.41 436.65 524.75 18 1 90.795 90.795 470.31 135.65 524.75 533.65 524.75 18 1 90.795 90.470 135.65 132.12 135.65 524.75 440.49 557.55 20 1 88.500 91.470 382.17 146.88 135.65 524.75 440.49 557.55 21 22 92.355 90.470 382.17 146.88 135.65 527.55 440.49 557.75 440.49 557.75 440.49 557.55 543.87 75.713 312.00 27.717 72.707 22 90.025 91.475 95.65 119.65 115.47 115.36 319.00 27.67 319.00 27.67 319.00 27.67 319.00 27.61 127.71 319.00 27.71 27.717 212.10 27.717 212.10 27.717 212.10 27.717 219.00 27.65 </td <td>15 1</td> <td>\$0.902</td> <td>361,796</td> <td>500.01</td> <td>124.48</td> <td>123.74</td> <td>457.36</td> <td>427.79</td> <td>527.30</td> <td>526.74</td>	15 1	\$0.902	361,796	500.01	124.48	123.74	457.36	427.79	527.30	526.74
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	16	90.072	90. BI4	467.00	129.92	129.33	466.41	436.65	524.75	521.05
18 1 69.589 90.454 607.83 135.45 134.30 477.65 440.49 535.63 535.63 535.66 535.66 535.713 340.49 535.713 240.49 535.73 53.46 73.76 53.73 53.763 53.66 73.766 73.763 53.737 224.07 212.21 242.40 72.703 232.66 73.763 236.633 139.63 139.63 139.63 139.70 272.71 242.631 242.407 212.212 242.407 224.07 224.07 224.07 224.07 222.6317 236.533 239.238 299.238 299.238 299.238 299.238 299.238 299.238 299.238 299.238 299.238 299.238 299.236 2392.238 2392.240 2322.240 <	1 1 1	231.182	561.04	438.88	132.12	132.01	470.31	436.98	527.55	530.17
19 16.500 91.470 382.17 146.88 139.62 485.13 443.28 543.81 27.107 21 2 92.575 92.474 $2.57.563$ 19.658 95.266 19.673 92.4713 70.419 72.707 22 2 92.575 92.474 $2.57.563$ 119.65 119.65 110.73 232.10 242.72 243.75 70.419 72.707 212.21 242.76 319.00 266.63 390.71 212.21 242.76 319.00 266.61 319.65 319.76 319.70 212.71 212.21 242.75 319.00 276.41 265.26 118.93 410.54 390.10 508.60 506.61 319.76 319.70 218.77 321.68 399.19 518.77 329.29 399.23 399.23 399.26 399.26 518.77 329.26 518.77 329.26 518.77 329.26 518.77 329.26 518.77 339.26 518.77 339.26 518.77 339.26 518.77 524.60 526.61 526.61 526.61 526.61 526.61 526.61 526.61 <td>18 1</td> <td>635, 239</td> <td>90.454</td> <td>407.83</td> <td>135.45</td> <td>134.30</td> <td>477.65</td> <td>440.49</td> <td>535.50</td> <td>533.43</td>	18 1	635, 239	90.4 54	407.83	135.45	134.30	477.65	440.49	535.50	533.43
20 1 89.793 89.874 6.6683 75.545 75.821 75.713 70.419 72.707 21 2 90.655 95.031 25.46 75.45 115.21 242.40 72.707 23 2 90.655 95.260 75.46 15.564 120.69 240.71 212.21 242.40 25 90.655 90.711 189.45 79.436 115.38 95.031 231.77 321.68 399.33 25 1 90.026 90.722 579.66 115.47 115.38 440.54 399.19 518.77 26 1 90.026 90.274 95.255 115.47 319.16 399.13 319.40 27 91.201 687.50 95.256 115.47 115.38 440.54 399.19 518.77 27 91.201 92.273 89.45 122.43 455.55 460.75 524.01 524.61 526.61 526.61 526.61 526.61 526.61 526.61 526.61 526.61 526.61 526.61 556.65 530.16 526.61<	19 1	68.508	91.430	382.17	140.88	139.62	485.13	443.28	543.81	539.48
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	20	89,793	89.874	6.6583	75,545	75.821	75.713	70.419	72.707	76.241
22 50.655 95.260 75.663 119.63 120.09 295.09 276.31 319.00 24 2 90.635 90.711 189.45 79.433 79.565 140.77 321.68 399.19 508.60 25 1 90.022 579.65 115.47 115.38 440.54 390.10 508.60 26 1 90.022 579.65 119.65 119.65 119.65 310.10 508.60 26 1 90.022 579.65 119.65 119.65 119.65 309.19 508.60 27 51.71 530.50 121.84 115.47 321.68 399.19 518.77 27 51.61 125.65 119.65 118.93 450.77 321.68 399.19 518.77 27 51.73 30.20.65 122.63 121.84 456.77 321.68 399.19 518.77 28 90.374 90.274 122.63 122.64 122.32 456.11 530.66 533.66 28 1 126.03 127.33 381.51	21 2	92.355	92.440	257.98	95.248	95.031	224.07	212.21	242.40	244.42
23 2 90.635 90.711 189.45 79.439 79.565 140.89 130.65 149.75 24 2 91.202 91.202 579.66 115.47 115.47 321.68 399.33 25 1 90.825 90.825 95.252 69.825 351.77 321.68 399.33 26 1 90.825 90.875 579.66 119.65 119.65 390.10 518.77 27 31.251 50.977 539.56 119.65 128.47 390.10 518.77 27 31.1 90.876 514.97 122.66 123.43 454.28 121.84 454.32 400.27 524.08 530.55 531.77 321.66 530.55 526.61 531.67 524.08 530.55 531.66 531.77 524.08 530.25 435.16 530.25 435.16 531.77 524.08 531.66 531.66 531.66 531.66 531.66 531.66 531.66 531.66 531.66 531.66 531.66 531.66 531.67 531.67 531.67 531.67 531.67 </td <td>63 64</td> <td>\$0.855</td> <td>95.260</td> <td>75.663</td> <td>119.63</td> <td>120.09</td> <td>295.09</td> <td>276.31</td> <td>319.00</td> <td>322.25</td>	63 64	\$0.855	95.260	75.663	119.63	120.09	295.09	276.31	319.00	322.25
24 2 91.202 547.50 96.252 89.825 351.77 321.68 399.33 25 1 90.025 90.222 579.66 115.47 115.38 440.54 390.10 508.60 26 1 91.251 50.947 513.55 115.47 115.38 440.54 390.10 508.60 27 1 91.251 90.376 514.59 122.65 118.93 450.77 321.68 399.33 28 1 91.251 50.970 514.97 122.65 123.43 456.72 524.66 524.66 526.66 526.66 526.66 536.23 530.55 536.29 536.	52	90.635	50.711	189.45	79.439	79.565	140.89	130.85	149.75	153.08
25 1 90.825 90.822 579.65 115.47 115.38 440.54 390.10 508.60 26 1 90.875 50.477 539.59 119.65 118.93 450.79 399.19 518.77 27 1 91.251 50.947 539.59 119.65 118.93 450.79 399.19 518.77 27 5 91.251 534.97 122.69 121.84 456.73 399.19 518.77 28 1 91.274 530.55 139.01 122.44 339.19 518.77 29 31 90.87 532.55 139.01 125.55 450.77 524.08 20 1 90.87 126.01 126.01 125.55 450.11 530.55 30 1 89.87 36 452.07 440.46 536.61 533.66 31 1 89.490 90.47 126.07 125.41 455.65 534.67 534.67 32 1 89.490 90.77 381.51 134.16 469.55 540.67 536.61	24 2	91.202	50.14	697.50	98.252	69.825	351.77	321.68	399.33	401.16
26 1 90.892 50.947 539.59 119.65 118.93 450.79 399.19 518.77 26 1 91.251 90.874 539.59 119.65 121.84 454.32 402.27 524.08 26 1 91.874 514.97 122.69 121.84 454.32 402.27 524.08 26 1 91.874 512.67 122.63 121.84 455.55 435.96 530.55 27 91.71 90.374 90.283 473.07 126.04 125.36 455.55 436.11 536.661 524.08 28 1 90.374 90.283 473.07 126.04 125.36 455.55 436.11 530.55 534.66 534.66 536.661 536.61 536.661 536.661 536.661 524.08 536.661<		90.025	90.222	579.65	115.47	115.38	440.54	390.10	508.60	509.62
27 1 \$90.374 \$90.870 \$14.97 122.63 121.84 454.32 402.27 524.08 26 1 \$1.011 90.874 502.06 124.28 123.43 455.55 436.11 530.55 27 1 \$1.011 90.874 502.06 126.04 125.36 456.61 526.61 27 502.06 \$124.28 125.36 456.13 455.55 436.11 530.55 30 1 \$10.97 \$126.04 126.04 125.36 456.11 530.55 31 1 \$20.394 \$00.876 \$45.07 126.04 126.11 530.55 31 1 \$0.999 \$130.00 129.36 \$462.07 \$460.05 536.61 32 1 \$0.999 \$31.51 \$34.16 \$469.58 \$460.05 536.61 530.55 33 1 \$29.49 \$00.334 \$465.71 \$333.66 \$36.61 \$36.61 \$36.61 \$36.66 \$36.66 \$36.66 \$36.66 \$36.66 \$36.66 \$36.66 \$36.66 \$36.66	74	90.893	\$0.947	539.59	119.65	118.93	450.79	399.19	518.77	519.17
26 1 \$1.011 90.874 502.06 124.28 123.43 455.55 435.96 526.61 25 1 90.374 90.374 90.374 90.374 500.083 473.07 126.04 125.36 458.43 436.11 530.55 30 1 87.495 90.374 90.374 90.374 90.374 500.05 536.29 31 1 87.495 97.77 409.27 126.04 125.36 460.05 536.29 32 1 87.368 97.77 409.27 134.16 460.05 536.29 33 1 87.368 91.71 381.51 134.25 133.07 479.17 460.05 533.67 33 1 87.368 134.28 133.00 474.12 429.53 540.97 35 1 90.548 91.012 468.46 136.51 533.67 528.16 35 1 90.548 91.012 435.96 130.39 474.12 422.97 538.67 35 1 90.548 130.97	102	91.25L	50.970	514.97	122.69	121.84	454.32	402.27	524.08	524.24
25 1 90.374 90.374 90.374 90.374 90.374 90.374 90.374 90.374 90.374 30.55 30.55 30 1 89.409 90.477 409.27 126.04 129.36 462.07 440.46 536.29 31 1 89.909 90.477 409.27 134.16 469.58 460.05 533.66 32 1 87.368 91.771 381.51 140.25 139.98 479.17 440.46 540.63 33 1 87.368 91.771 383.61 133.57 138.41 480.49 440.63 540.63 34 29.5944 90.333 408.46 134.28 133.00 474.12 422.97 540.97 35 1 90.548 91.012 457.47 129.05 130.39 465.31 417.72 528.14 36 1 50.548 130.39 130.39 456.55 456.56 405.78 520.41 37 90.579 531.055 125.59 456.56 405.78 517.32 539.49 <t< td=""><td>26 1</td><td>51.011</td><td>30,874</td><td>502.05</td><td>124.28</td><td>123.43</td><td>455.55</td><td>435.96</td><td>526.61</td><td>526.47</td></t<>	26 1	51.011	30,874	502.05	124.28	123.43	455.55	435.96	526.61	526.47
30 1 0.5,00 129.36 462.07 440.46 536.29 31 1 89.909 90.477 409.27 134.16 469.58 460.05 533.66 32 1 89.909 90.477 409.27 134.16 469.58 460.05 533.66 33 1 87.368 91.71 383.63 134.16 469.58 460.05 533.67 34 25.946 90.333 498.46 134.28 133.57 138.41 480.49 540.63 35 1 90.503 381.61 134.28 133.57 138.41 480.49 540.63 35 1 90.548 91.012 498.46 136.28 133.39 417.12 422.97 528.14 35 1 90.548 91.012 457.47 129.06 125.63 125.59 456.21 411.43 528.14 36 1 90.549 510.65 125.63 125.65 456.56 405.78 520.41 37 1 90.579 536.48 127.65 125.65		\$12.02	90.083	£73.07	126.04	125.36	458.43	436.11	530.55	529.74
11 1 89.909 90.477 409.27 134.16 469.58 460.05 533.66 22 1 87.368 91.771 383.51 140.25 139.98 479.17 445.04 540.63 33 1 87.368 91.771 383.83 139.98 479.17 445.04 540.63 34 25.944 90.333 408.46 134.28 133.00 474.12 422.97 533.67 35 1 90.509 90.333 408.46 134.28 133.00 474.12 422.97 533.67 35 1 90.548 91.012 467.47 129.05 130.39 469.31 411.72 528.14 36 1 90.548 91.012 467.47 129.05 125.59 466.28 411.05 520.41 37 90.579 536.68 123.65 123.66 455.67 405.78 528.14 38 1 90.579 90.579 399.49 517.32 517.32 39 1 90.579 536.48 120.70 455.97 <td>30</td> <td>557 63</td> <td>365, 36</td> <td>443.85</td> <td>130.00</td> <td>129.36</td> <td>462.07</td> <td>440.46</td> <td>536.29</td> <td>535.25</td>	30	557 63	365, 36	44 3.85	130.00	129.36	462.07	440.46	536.29	535.25
22 1 67.368 91.733 381.51 140.25 139.98 479.17 445.04 540.63 33 1 92.91 96.971 383.83 139.57 138.41 445.04 540.63 34 2 25.944 90.333 408.46 134.28 133.00 474.12 422.97 533.67 35 1 90.503 408.46 136.58 133.00 474.12 422.97 533.67 35 1 90.503 408.46 136.58 133.00 474.12 422.97 533.67 35 1 90.548 91.012 467.47 129.06 130.39 469.31 411.72 528.14 36 1 90.548 91.012 467.53 125.63 125.59 456.28 411.05 520.41 37 1 90.579 96.576 123.64 455.67 455.67 517.32 38 1 90.579 90.576 123.67 399.49 517.32 38 1 90.579 536.48 121.56 120.70 <td< td=""><td></td><td>626.68</td><td>90.477</td><td>409.27</td><td>134.30</td><td>134.16</td><td>469.58</td><td>460.05</td><td>533.66</td><td>535.40</td></td<>		626.68	90.477	409.27	134.30	134.16	469.58	460.05	533.66	535.40
33 1 02.01 90.771 303.63 139.57 138.41 480.49 429.53 540.97 54 50.594 50.333 488.46 134.28 133.00 474.12 422.97 533.67 35 1 90.503 90.333 439.69 130.39 469.31 417.72 528.14 36 1 90.548 91.012 467.47 129.06 128.45 466.28 411.43 525.74 37 1 90.548 91.012 467.47 129.06 128.45 466.28 411.43 525.74 37 1 90.579 531.06 125.63 125.59 456.26 405.78 517.32 38 1 90.579 90.579 536.48 517.32 517.32 39 405.79 90.579 90.579 905.49 513.33	22	87.368	91.733	381.51	140.25	139.98	479.17	445,04	540.63	543.16
24 295.944 90.333 408.46 134.28 133.00 474.12 422.97 533.67 35 1 90.903 30.332 439.69 130.39 469.31 417.72 528.14 36 1 90.548 91.012 467.47 129.06 128.45 466.28 411.43 525.74 37 1 90.537 93.711 496.53 125.63 125.59 456.21 411.05 520.41 38 1 90.579 531.06 123.64 456.56 405.78 517.32 38 1 90.579 936.48 121.06 123.64 455.97 399.49 513.33	1	85.041	36.771	303.83	139.53	138.41	480.49	429.53	540.97	539.07
35 1 90.503 30.332 439.69 130.39 469.31 417.72 528.14 36 1 90.548 91.012 467.47 129.06 128.45 466.28 411.43 525.74 37 1 90.548 91.012 467.47 129.06 128.45 466.28 411.43 525.74 37 1 90.578 93.771 496.53 125.63 125.59 456.26 411.05 520.41 38 1 96.579 93.757 536.48 123.64 456.56 405.78 517.32 39 1 90.579 90.579 536.48 121.50 120.70 455.97 399.49 513.33	44 44	55.944	90.3 33	408.46	134.28	133.00	474.12	422.97	533.67	534.46
36 1 90.548 91.012 467.47 129.06 128.45 466.28 411.43 525.74 37 1 90.537 90.771 496.53 125.63 125.59 458.21 411.05 520.41 38 1 90.579 90.579 511.06 123.64 456.56 405.78 517.32 39 1 90.579 90.579 536.48 121.50 120.70 455.97 399.49 513.33	35 1	505.06	30.332	439.65	130.99	130.39	469.31	417.72	528.14	529.44
27 1 90.337 90.771 696.53 125.63 125.59 458.21 411.05 520.41 38 1 90.679 90.579 90.579 517.32 517.32 35 1 90.579 90.579 536.48 121.50 120.70 455.97 399.49 513.33	36 1	90.548	91.012	467.47	129.06	128.45	.466.28	411.43	525.74	524.36
38 1 80.671 \$2.296 511.06 123.54 123.64 456.56 405.78 517.32 39 1 90.579 90.579 536.48 121.50 120.70 455.97 399.49 513.33	14 - C. C.	50.327	117.02	696.53	125.63	125.59	458.21	411.05	520.41	522.77
39 1 90.57B 90.57B 536.48 121.50 120.70 455.97 399.49 513.33	38 . 1	20.671	\$2.236	511.06	123.54	123.64	456.56	405.78	517.32	519.82
	36	90.579	90.757	536.48	121.50	120.70	455.97	399.49	513.33	515.61

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TUTT. OUTPUT

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AVERAGED DATA ON MEASUREMENT DATA SETS XOVER HO CAV TEST Test Start Time 10/ 8/88 7:26:17.20

PROCESS TIME 10/12/88 12:53:52 HEAD2R: Test 242096

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F/F ID		106	305	950	951	952	Ţ	953	850	851	
		GEAR CAS	LUBE OIL	ACCEL X	ACCEL Y	ACCEL 2	SPEED	LUBE OIL	FLEX FLO	GBOX OIL	
1 1504	2473	1 1 ECF	1 200	CTYY	CTYN	CT74		E LOW	2 7 7 7	лх	
÷			COT C0	10-809CC1 0	10- 000199 V	-10- <i>4116</i> 21 V		033 66	36 640		
-1 6	- 6		221.25		C. COLSSE-UL	0.512995-01-	0.01144 PF116.0	200 . 1 2	95.146	120.04	
	N	71.458	84.713	0.19817	0.14/34	0.16290	0.32.0	26.838	939.84	32.023	
(m)	-1	79.708	85.005	0.24620	0.28518	0.25991	6323.2	26.777	937.86	26.844	
Y		82.573	65.103	0.20897	0.14574	0.18550	6323.2	26.754	937.57	25.812	
ŝ	-	88.654	85.293	0.44809	0.55748	0.40748	6323.2	26.732	936.27	24.041	
Q		90.724	84.608	0.29548	0.34509	0.28366	6322.5	26.744	936.23	23.405	
~	-	93.280	84.746	0.22252	0.14628	0.19356	6322.6	26.772	935.94	22.976	
8		95.981	85.308	0.25120	0.14860	0.20455	6322.4	26.776	935.44	22.533	
0		98.453	85.094	0.26146	0.14531	0.21050	6322.8	26.762	934,86	22.104	
10	1	102.71	84.968	1.0966	0.54314	0.45076	6323.3	26.782	934.33	21.383	
11	· e=4	105.21	85.034	1.1546	0.57229	0.35895	6321.9	26.774	933.79	20.973	
12	~	108.14	85.737	1.1521	0.56924	0.44810	6322.9	26.762	933.17	20.540	
13		109.95	85.617	1.1086	0.55102	0.45039	6322.1	26.769	933.06	20.280	
4	-1	111.50	85.078	1.1240	0.55678	0.47432	6322.3	26.760	932.55	20.156	
15		112.86	85.884	0.40793	0.22899	0.25445	6322.5	26.761	932.07	19.829	
16		114.83	85.991	0.57571	0.30002	0.35654	6322.9	26.770	931.56	19.483	
17	1	116.64	85.821	1.1567	0.57323	0.54485	6322.5	26.781	931.40	19.246	
18		118.16	85,502	I.1233	0.54835	0.57097	6322.8	26.781	930.77	19.052	
19	 1	120.06	85.514	0.23107	0.14787	0.20412	6324.5	26.789	930.02	18.913	
50	~~1	120.97	86.146	0.22121	0.15059	0.18938	6322.3	26.802	930.00	18.781	
21		121.86	86.148	0.36558	0.39454	0.35535	6324.6	26.804	929.84	18.635	
22	-1	122.80	85.648	0.47110	0.55373	0.44895	6325.2	26.856	929.61	18.483	
23	~	128.08	86.492	0.20699	0.18005	0.27671	6322.5	26.935	927.51	18.175	
24	ŝ	133.89	87.494	0.21844	0.18278	0.29545	6324.3	27.328	924.37	17.574	
ŝ	2	136.97	87.439	0.20159	0.15978	0.25789	6322.7	27.296	922.25	17.166	
26	2	137.94	88.046	0.34979	0.27073	0.28555	6324.0	27.242	921.65	17.243	
27	2	140.35	88.355	0.20060	0.17312	0.26348	6322.5	27.407	919.56	16.980	
28	2	142.40	88.925	0.18953	0.14838	0.24430	6322.9	27.161	917.21	16.815	
525	~	143.32	88.837	0.22313	0.15698	0.27386	6323.9	27.121	915.73	16.709	
30	2	112.71	89.901	0.18653	0.15018	0.13381	5152.9	26.761	901.60	27.855	
31	~	109.86	90.075	0.20696	0.17646	0.23437	5322.1	26.638	900.49	22.576	
32	2	121.16	90.354	0.70488	0.35120	0.34457	6322.0	26.711	898.12	18.981	3
3	1	125.76	90.4 29	0.49253E-01	0.71387E-01	0.16207E-01	1.1290	26.779	895.48	28.319	
40	2	112.29	92.248	0.18557	0.14707	0.13040	5238.9	26.704	687.70	27.173	
51 19		110.47	91.518	0.23168 .	0.16756	0.19863	6324.7	26.749	887.40	24.106	
36	્ત	115.48	92.005	0.28278	0.17704	0.33150	6323.5	26.312	885.83	20.097	
37	ы	121.48	92.556	0.463842-01	0.71021E-01	0.17397E-01	0.42823	26.945	884.23	27.200	

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AVERAGED DATA ON MEASUREMENT DATA SETS

PROCESS TIME 10/12/88 12:53:52 XOVER HO CAV TEST TEST START TIME 10/ 8/88 7:26:17.20 HEADER: Test 88A096

P/F II	# 0	526	2	S	m	838	006	901	603	902
		PUMP DEL TA PR	IN. TEMP ERATURE	Torgue 4 1	elowmete R e2	IHRUST D ISK DRAI	REAR TOR OUE TEMP	FWD TORQ UE TEMP	TEMP #1	LUBE OIL TEMP #2
#SOM	затт			ŀ	•	N FLOW				
-1	7	0.26863	66.346	-1.8460	-0.64277E-01-	0.12035E-01	72.844	72.005	88.141	88.967
~	2	434.50	61.300	3741.1	584.37	74.661	76.236	74.100	88.771	99.471
m	-1	518.57	58.846	4371.7	653.50	94.924	77.882	77.436	97.957	104.05
*	1	550.92	58.944	1290.8	593.82	106.06	79.048	78.642	87.622	105.38
ഹ	-1	485,21	59.187	4407.2	704.24	010.02	80.897	80.777	94.291	105.13
Q	~	518.83	59.285	4354.5	652.81	95.822	81.271	81.468	95.435	105.23
-	gui	551.19	59.406	<pre>{285.8</pre>	593.83	106.57	81.683	82.264	91.399	106.88
ŝ	-	577.88	59.541	4164.8	535.96	113.73	81.964	83.088	86.170	107.46
ch.		602.04	55.630	6 021.5	479.33	120.05	82.202	83.558	95.395	107.26
9	r-1	608.07	59.852	3999.2	449.51	131.22	82,935	84.189	112.68	112.58
	,	621.49	59.937	3309.8	415.22	133.72	83.270	84.820	114.99	112.98
12	7	630.55	60.172	3833.1	388.35	134.64	83.620	85.603	116.45	113.65
13	-1	637.35	60.247	3741.1	358.88	135.25	83,963	86.243	117.70	113.94
14	-	637.33	60.338	3741.8	358.78	135.63	64.432	87.054	116.59	114.18
15	~1	588.46	60.427	3863.4	388.36	131.74	64.783	87.274	110,92	113.96
16	-	584.90	60.562	3935.7	415.19	131.90	85.457	87.928	113.69	114.05
17	~	609.64	60.702	£027.5	449.47	133.89	85.656	88.791	121.65	114.94
18		598.34	60.786	4103.4	£79.25	132.50	86.183	89.458	123.44	115.06
1 3		571.54	60.973	£232.0	535.92	130.07	86.854	90.109	95.810	111.01
20	1	541.54	61.058	4350.7	593.84	126.57	87.189	90.067	95.868	109.89
21		504.82	61.161	4419.4	653.02	120.83	87.431	90.367	95.161	109.00
22	-1	481.15	61.312	4450.7	705.74	100.05	87.784	168.06	97.116	108.60
M N	2	494.05	61.968	4073.8	595.57	93.176	90.047	93.098	107.52	106.87
24	2	429.69	62.892	4088.9	654.5I	85.049	93.223	95.876	107.72	106.00
52	~	400.59	53.554	4209.4	704.96	82.088	96.015	97.345	110.42	106.09
26	2	310.72	63.766	3908.1	708.31	69.763	96.709	98.238	110.59	106.31
27	~	555.43	64.399	4057.2	535.98	105.60	99.305	99.952	106.48	106.22
28	2	589.80	65.002	3981.3	€ 78.99	119.49	102.16	101.76	105.11	107.58
29	2	608.09	65.393	4001.6	€8.8 } ₽	135.07	103.61	102.63	97.649	108.61
30	N	397.49	65.231	3450.2	523.42	94.207	93. 339	91.357	101.54	100.67
31	ŝ	493.00	63.795	4087.6	594.78	94.776	97.696	96.441	115.88	108.98
32	3	615.80	64.790	3859.7	413.56	131.16	100.78	101.34	118.11	114.03
33		-0.23896	65.438	-4.6860	-0.25827E-01	4.6179	96.079	98.602	96.305	99.522
¥ m	~	4 10.13	65.370	3519.3	528.12	95.777	94.056	93.209	103.32	99.989
5 10	-1	597.86	64.894	3610.8	301.48	135.39	97.349	95.820	116.61	110.77
36	2	590.37	65.530	3695.3	355.28	122.87	99.684	99.815	120.00	115.76
37	-	-0.37835	66.040	-3.9760	-0.664162-01	4.9213	96.208	98.404	99.098	102.11

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TEXT. OUTPUT

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PROCESS TIME 10/12/88 12:53:52 AVERAGED DATA ON MEASUREMENT DATA SETS XOVER HO CAV TEST TEST START TIME 10/ 8/83 7:26:17.20 HEADER: Test 08A096

	• •	
822 XOVER EX IT TOTAL FR #3	78.782 535.32 535.32 643.55 643.55 643.55 643.55 643.55 669.87 727.47 727.53 669.43 669.43 669.43 669.43 669.43 669.43 669.43 669.43 614.27 513.15 514.27 514.27 514.27 514.27 514.27 514.27 514.27 514.27 514.27 514.27 514.27 514.27 514.27 515.17 515.17 515.17 515.17	75.759 499.39 686.44 614.64 75.628
821 XOVER EX IT TOTAL PR #2	532 532 532 532 532 532 532 532 532 532	75.919 496.39 683.06 612.53 75.677
820 Xover ex It Total Pr #1	78.033 529.033 644.594.033 644.594.39 644.594.39 644.593.30 644.594.39 644.594.59 644.59 644.59 7714.55 641.33 681.96 693.00 800.00 800.00 800.00 800.00 800.00 800.000 800.000 800.000 800.000 800.000 800.000 800.000 800.000 800.000 800.000 800.000 800.000 800.000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.0000 800.00000 800.00000 800.00000000	75.915 498.72 684.94 615.59 75.626
819 TRANSITI ON TOTAL PR	77 77 77 77 77 77 77 77 77 77	14.935 456.77 653.21 578.96 74.767
120 D/S TOT PRESS. 1 IMP #1	738888888999993333333333333333333333333	75.815 302.64 408.14 351.50 75.375
818 THRUST D ISK DRAI H PR	444444444446666666664644466466444464464	11,923 385,69 499,76 460.31 77,400
815 Xover di Sch St P R f i	73 73 73 74 75 75 75 75 75 75 75 75 75 75	76.619 489.91 677.30 606.90 76.263
802 IMP FHD SHROUD P R ∉1	22222222222222222222222222222222222222	75.661 328.61 461.15 392.43 75.394
813 DWN CONS T SEC PR	2202224445566666666723222 2202224445566666667232 220222328887 220222328887 220222328887 2202233847 220223847 220223887 22022387 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 2202237 220257 220257 220257 220257 220257 220257 220257 220257	40.414 479.94 668.05 597.37 75.179
p/f 10 4 PDS4 TYPE		- 2 - 2 - 3 - 2 - 2 - 3 - 2 - 2 3 - 2 3 3 3

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- 27 -

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PROCESS TIME 10/12/88 12:53:52 7:26:17.20 XOVER HQ CAV TEST TEST START TIME 10/ 8/88 HEADER: Test 88A096

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812 DWN DIFF DISCH P R #2	76.94 525.94 525.94 5666.53 5666.53 719.59 561.04 551.04 5	222 222 202 202 202 203 203 203 203 203
811 DWN DIFF DISCH P R #1	77 526 634 634 634 634 634 634 634 634 704 704 704 70 704 706 651 720 71 706 651 720 71 720 71 720 71 720 71 720 71 720 71 720 71 720 720 720 720 720 720 71 70 720 71 70 720 71 70 720 71 70 720 71 70 720 71 70 720 71 70 70 70 70 70 70 70 70 70 70 70 70 70	423,22 423,24 5600.64 667.53 667.53 667.53 678.44 78.44 78.44 78.47 78.47 78.90 79.90 71.994 71.994
810 Transiti On St Fr	77.845 5908.09 5555.855.85 659.05 659.05 659.03 659.30 714.82 659.30 659.33 714.82 659.33 714.82 659.33 714.82 659.33 714.82 659.33 714.82 715.10 710	2413.32 5610.03 5610.03 653.61 653.61 653.61 467.92 647.92 74.061 73.627 73.627 627 627 627
809 UPC CONS T SEC PR	78.486 518.486 518.486 559.51 554.51 554.51 554.51 554.51 654.51 717.55 613.56	241.03 5624.87 5625.52 5651.81 661.81 666.73 75.829 482.829 596.93 75.473 75.473 75.473
808 UPC CONS T SEC PR €2	4822 11 4827 13 4827 14 4827 19 4827 19 4827 19 4827 19 4827 19 4827 19 4827 10 488 100 488 100 488 100 488 100 488 100 488 100000000000000000000000000000000000	2803.42 5525.33 5525.33 5555.63 5651.89 461.30 461.30 461.30 415.494 475.494 475.494 475.494 791 74.791
807 UPC CONS T SEC PR	722 316 523 51 523 523 513 120 513 120 5552 555 555 555 555 555 555 555 555 55	2522 2522 2522 2522 2522 2522 2522 252
806 DMN MID D <i>IFF</i> <u>\$</u> 1	77.557.533 554.153 554.155 554.155 554.155 554.155 554.155 556.55 659.23 7102.84 659.23 7102.84 659.23 7102.84 7102.84 659.23 7102.84 659.23 7102.84 7102.84 659.23 7102.84 7102.84 7102.83 755.50 7102.84 7002.74 7000.74 700	441.53 566.53 566.53 598.61 598.61 665.21 665.21 74.23 615.33 615.33 74.288 603.87 74.288
231 D/S STAT · PRESS. IMP £2	L 4 4 7 4 4 8 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 	74566740 94749994 94949 94966 9405 9405 9405 9405 9305 9305 9305 9305 9305 9305 9305 93
230 D/S STAT . PRESS. IMP #1		256 256 266 266 266 266 266 267 267 267 267 26
P∕F ID∳ MDS∳ TYPE		~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~

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TEXT. OUTPUT

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AVERAGED DATA ON MEASUREMENT DATA SETS

PROCESS TIME 10/12/88 12:53:52 7:26:17.20 XOVER HO CAV TEST TEST START TIME 10/ 8/88 HEADER: Test 88A096

toi 3/a		801	~	228	229	802	803	804	805
	INLET ST	INLET ST	FLOMETE	D/S STAT	D/S STAT	IMP FWD	IMP FWD	IMP AFT	IMP AFT
	ATIC PPE	ATIC PR	R #1	. PRESS.	PRESS.	SHROUD P	SHROUD P	SHROUD P	SHROUD P
LT. LONN	rk ssuke, P	4 2		15 DNT	ZA GNT	1 4 X	K 52	R #1	R #2
1 1	171.19	93.243	-0.49547E-01	78.957	79.059	77.372	78.349	75.878	79.217
3	91.176	92.858	646.44	95.565	95.164	350.39	343.47	395.28	397.15
 	91,230	93.257	735.96	96.046	95,806	392.33	385.63	445.69	448.62
4	91.161	93.021	688.44	104.14	103.92	405.89	398.33	465.19	467.16
 	91.180	92.850	781.27	88.068	87.827	378.31	367.80	426.70	429.06
1 9	91.323	92.969	736.36	96.083	95.774	392.52	377.46	446.28	447.54
1	91.212	93.039	688.93	104.15	103.83	405.54	397.70	464.99	465.94
8	50.907	52.777	638.89	111.64	111.11	417.68	410.65	481.77	481.94
6	91.058	92.725	589.42	EI-911	118.42	430.32	421.78	497.63	497.37
10 1	91.256	92.914	571.24	120.39	119.41	4 36.89	425.72	505.51	504.68
77	91.061	93.053	539.98	124.46	123.47	443.67	431.14	514.49	513.37
12	91.106	92.8 92	514.45	127.71	126.45	448.83	442.86	521.90	520.41
13 1	91.022	93.035	485.97	130.73	129.71	451.59	458.29	528.18	525.64
14 1	91.147	92.966	486.33	I30.85	129.70	451.97	446.68	528.75	526.41
15 1	51.000	92.875	511.60	128.15	127.75	453.89	447.92	516.84	517.89
16 1	91.197	92.878	538.21	124.43	124.32	448.43	445.07	512.55	513.82
17 1	90.688	516.16	574.01	118.45	117.57	440.54	433.61	510.40	510.34
18 1	91.192	92.474	601.94	114,92	113.82	434.73	433.64	503.27	503.48
1 61	91.304	92.468	655.20	108.66	107.67	.417.68	413.62	486.09	486.63
20 1	91.382	92.288	708.92	065. 66	99,049	403.22	395.08	467.13	468.14
21 1	91.106	92.267	761.32	91.299	50.4 00	388.33	380.25	445.31	447.26
22	91.430	92.018	792.60	85.580	84.656	378.34	371.22	431.41	433.51
23 23	20.716	21.566	675.32	32.889	32.108	294.17	290.66	349.21	351.76
24	23.387	23,584	725.02	27.450	26.981	256.65	245.20	304.47	306.91
25 25	36.869	36.514	773.43	33.510	32.732	257.13	266.60	302.80	304.53
26	9.0136	9.0783	761.69	4.9378	5.3683	170.88	175.82	207.98	210.60
27 2	23.450	23.493	630.42	40.536	40.506	334.22	334.54	399.69	398.72
28	20.246	20.202	588.54	41.971	4 2.995	349.66	353.58	419.62	419.80
29	68.520	68.588	574.40	95.595	95.704	410.32	414.73	483.50	483.80
30 2	91.318	91.227	607.60	89.773	89.824	321.35	323.50	367.71	369.99
31 2	24.001	23.679	676.92	33.605	34,289	295.54	294.33	351.19	352.80
32 2	24.835	24.714	537.34	52.947	53.475	369.62	368.89	442.31	443.26
33 1	91.181	175.19	4.5953	77.048	77.194	75.661	71.099	74.287	77.233
31 2	91.246	91.165	613.49	90.646	90.727	328.61	302.89	376.20	379.25
35 1	90.146	89.820	\$29.60	133.00	132.95	461.15	474.59	518.04	537.66
36 2	25.271	25.218	473.56	61,436	61.760	392.43	360.97	453.48	451.48
37 1	90.527	93.742	4.8763	76,518	76.709	75.394	71.275	73.517	76.663

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TEXT. OUTPUT

AVERAGED DATA ON MEASUREMENT DATA SETS

PROCESS TIME 10/12/88 12:53:52 XOVER NO CAV TEST TEST START TIME 10/ 8/88 7:26:17.20 HEADER: Test 88A096

P/F 10	-	90 <i>K</i>	1 1 1	96 .	-9 F	201-	45-	-160	50 L T	101-
•	•	G-BOX TE	FLOW 1 R	CHI HSAN	WSS IND.	ST-TOT H	D/S PRES	FLOW 1 R	SCALED N	SCALED F
Hore	TYPE	HP ALARM	ATIO IND	. 81		EAD 2 IM P. #1	S. PIPE	ATIO IND	PSH IND.	LOW IND.
•	•									
	-4 1		79881.0-	213,85	-0.512/08-03	CI2/ .I-	105.26	-0.18862	0.124598+12	-50.725
N	2	3.3122	1.2422	214.53	2643.5	533.98	92.742	1.2422	22348.	67.349
ጣ	2	3.3127	1.2643	214.79	3057.4	630.22	92.856	1.2643	7989.5	66.758
¢	-1	3.3116	1.1827	214.49	2960.1	647.00	92.726	1.1827	7978.5	60.649
ŋ		3,3129	1.3421	214.81	3149.9	612.70	92.862	1 3421	0001	71 983
9		3.3132	1.2651	215.01	3055.6	630.07	92.948	1.2651	7999.4	66 712
 ~	I	3.3128	1.1836	214.61	2959.7	645.95	92.777	1 1836	0 000L	60 650
- UJ	ا	3.3128	1.0977	213.78	2858.4	652.85	92.420	1.0977	7954.0	50.603
O	i	3.3118	1.0126	214.02	2743_3	675.43	92.524	1.0126	7962.0	48.880
10	 -1	3.3118	0.98131	214.43	2697.1	691.47	92.699	0.98131	7975.9	45.819
11		3.3122	0.92781	213.92	2626.3	694.33	92.480	0 92781	7960 A	40 213
23	a=4	3.3128	0.88381	213.99	2563.3	695.83	92.508	0.88381	7960.4	39.551
13	-1	3.3121	0.83499	213.75	2493.2	695.55	92.406	0.83499	7953.7	36.526
14		3.3131	0.83558	214.04	2491.6	692.20	92.531	0.83558	7964.0	36.523
15	1	3.3129	0.87896	213.74	2559.0	700.83	92.402	0.87896	7952.1	39.557
16	**	3.3125	0.92462	216.24	2622.1	700.24	92.617	0.92462	7969.8	42.309
1	i ş -i	3.3128	0.98620	213.12	2715.7	663.94	92.131	0.98620	7929.0	45.832
18	***	3.3120	1,0341	214.33	2769.3	658.06	92.658	1.0341	7973.6	48.832
19	1	3.3124	1.1253	214.70	2886.3	639.15	92.816	1.1253	7982.8	54.666
20		3.3117	1.2180	215.00	2998.1	628.94	92.948	1.2180	7.999.7	60.643
21		3.3138	1.3076	214.50	3113.4	616.47	92.731	1.3076	7975.5	66.673
22	-	3.3119	1.3612	215.39	3167.3	609.23	93.114	1.3612	8006.7	72.084
23	2	3.3123	1.1602	51.527	12606.	524.48	22.281	1.1602	1916.9	60.614
24	~	3.3131	1.2453	57.843	12117.	448.21	25.011	1.2453	2151.8	66.610
25	~	3.3133	1.3288	89.164	6165.0	£ 39,93	38.551	1.3288	3317.2	71.970
26	2	3.3127	1.3083	24.725	17304.	301.08	10.696	1.3083	919.60	72.015
51	2	3,3128	1.0831	57.727	11033.	604.19	24.961	1.0831	2147.6	54.632
28	2	3.3129	1.0111	50.208	11065.	632.69	21.711	1.0111	1867.9	48.821
29	2	3.3128	0.98664	161.83	3385.3	648.66	69.962	0.98664	6018.0	45.718
30	2	3.3129	2.8127	214.79	2424.7	476.76	92.854	2.8127	0.11589E+11	140.28
31	~	3.3130	1.1631	59.125	LI448.	521.34	25.566	1.1631	2200.0	60.607
32	2	3.3132	0.92327	60.717	9519.3	642.75	26.254	0.92327	2259.5	42.284
33	1	3.3130	27.257	213.94	0.43254E-01	-2.6200	92.458	27.257	0.13122E+12	33815.
34	2	3.3125	3.3690	214.63	2467.7	£90.28	92.784	3.3690	0.11142E+11	60.234
5	,	3.2131	0.73754	211.65	2362.9	636.48	91.499	0.73784	7869.2	30.614
96	2	3.3124	0.81349	61,645	8684.8	670.14	26.655	0.81349	2292.4	36.496
5	٦	3.3124	22.021	212.42	0.16740E-01	-2.5197	91.832	22.021	0.13029E+12	32558.

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TLAT. OUTPUT

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AVERAGED DATA ON MEASUREMENT DATA SETS

HEADER	••	XOVER HO CAV	TEST							
TEST 6	360V33	TEST &	TART TIME	10/ 8/88	1:26:17.20	PROCESS TIME	10/12/88	2:53:52		
e/f ID	-	-195	-800	-801	-152	-808	608-	-810	-811	-812
		SCALED H	INDUCER	INDUCER	FLOH 1 R	IMP STAT	XOVR U/S	XOVR D/S	XOVR D/S	XOVR D/S
		EAD IND.	TOT-ST H	TOT-ST H	ATIO IND	IC HEADR	T-T HEA	TT HEAD	TT HEAD	TT HEAD
NDS	TYPE	8 1	EAD #1	EAD #2	eri 4	ISE	DRISE	RISE #1	RISE #2	RISE #3
-		0.804795+09	3.4162	3.6517	-0.18862	0.80728 '	-1.5992	1.8549	1.6601	3.5841
2	~	42279.	41.162	40.236	1.2422	785.94	385.49	85 606	80 CB	960 90
(**)		45605	42,013	41.459	1.2643	905.24	44.05	120.09	110.38	LA ALL
	-	48387	61 047	60.501	1 1877	931 54	494 12	107 71	00 075	10.011
5	l g-4	2737	0 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	20.084	1092 1	877.62	241 RG	131 55	01.101	120.65
ø	-	5612.	61.885	41.170	1.2651	906.99		10.01	111 20	119 98
r ~		4 8387.	60.952	60.214	1.1836	932.29	495.21	108.59	90 305	106.211
8	-	50709.	79.100	77.864	1.0977	955.14	545.15	96.312	87 204	23.255
0	-	52338.	96.191	94.543	1.0126	977.52	572.17	85.609	28 410	000 18
10		53365	98,700	96.427	0.98131	592.54	566.34	87,083	80.631	82.647
21	~	54527.	108.62	106.32	0.42781	1003.7	592.66	78,788	70 101	74 555
12	. 0	55302.	116.06	113.16	0.88381	1012.4	609.70	75.117	68.081	69.896
13		55847.	123.29	120.92	0.83499	1014.1	622.58	70.360	61.998	63.514
11	•-1	55799.	123.29	120.63	0,83558	1015.4	623.54	72.064	63.495	65.781
15		51737.	117.33	116.40	0.87896	996.51	484.46	95.650	89.111	92.353
16		51369.	108.23	107.98	0.92462	90.166	485.58	94.806	87.218	91.699
17	-	53442.	95.526	93.489	0.98620	1004.9	595.19	91.421	83.916	86.636
18	~	52453.	86.124	83.586	1.0341	9 95.93	578.30	99.143	90.126	94.044
19		50108.	71.284	68.999	1.1253	962.70	541.91	107.11	97.705	104.37
20	m i	1599.	50.923	48.748	1.2180	935.77	490.10	119.65	111.59	117.85
21	-	44407.	31.320	29.239	1.3076	905,85	\$24.35	132.65	124.34	131.32
22	-	4 2295.	17.206	15.068	1.3612	887.14	382.19	139.88	131.31	137.81
23	2	43448.	59.172	57.365	1.1602	823.83	488.25	106.68	97.778	101.94
2	0	37821.	40.275	39.148	1.2453	728.32	423.93	114.44	105.77	110.65
ŝ	2	35263.	22.973	21.172	1,3288	708.68	370.37	124.60	116.41	122.00
0	N 1	27550.	21.313	22.309	1.3083	549.71	310.78	114.32	106.68	111.32
27	2	48697.	70.662	70.593	1.0831	922.86	548.45	92.899	85.715	90.175
5 8	2	51648.	81.502	63.872	1.0111	967.38	597,90	80.885	73.994	77.600
60	2	53175.	93.932	94.183	0.98664	05.199	613.78	79.615	73.320	76.630
30	Ň	-0.126962+09	27.506	27,624	2.8127	711.84	345.26	94.409	89.675	96.329
3	~	43198.	53.232	54.814	1.1631	822.31	489.41	104.77	95.459	101.18
32	2	53825.	96.385	97.605	0.92327	996.57	642.28	72.015	63.955	66.536
() ()	-	-0.17930E+10	-1.0867	-0.74895	27.257	-1.5363	-2.0270	2.5367	2.5444	2.1753
	N	-0.14261E+09	29.688	29.874	3,3690	730.52	356.17	97.234	91.840	98.777
ŝ	•	52141.	130.65	130.52	0.73784	1000.6	566.29	73.613	69.254	77.080
30	~	51676.	115.09	115.84	0.81349	1000.0	525.65	84.929	77.852	82.718
37	~	-0.123402+10-	0,79349	-0.35118	22.021	-2.0121	-1.4039	2.2646	2.3840	2.2697

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TEXT. OUTPUT

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AVERAGED DATA ON MEASUREMENT DATA SETS

CROSSOVER TEST

XOVER EX IT TOTAL PR #3 696.43 719.24 719.24 719.24 6683.67 6686.59 6686.59 712.53 67 6686.59 712.53 712.53 6686.59 7121.59 720 720.59 720. 822 XOVER EX IT TOTAL 694.76 7111.06 7111.06 6824.76 6824.76 6824.75 6824.97 6824.97 7195.59 7326.57 7326.52 7326.52 6628.22 PR #2 82 i XOVER EX IT TOTAL PR #1 698.42 715.24 715.24 7722.53 7722.53 7722.53 7722.53 7722.63 698.17 7724.76 698.37 7724.76 698.37 6682.66 688.70 6682.66 6882.66 6882.66 6882.66 6882.66 6882.70 75.462 616.59 606.14 490.07 569.41 820 PROCESS TIME 10/12/88 12:39:00 TRANSIFI ON TOTAL 6662.85 6683.76 6683.76 6683.76 6683.76 6683.76 6683.76 66855.75 76855.75 773.05 76855.75 773.05 76855.75 773.05 773.05 7555.75 773.05 7555.75 773.05 775.05 819 PR 120 D/S TOT PRESS. 1 IMP #1 818 Thrust d Isk drai N Pr TEST START TIME 10/10/88 14:37:48.70 eis Xover di Sch st p R #1 802 IMP FWD Shroud P R #1 T SEC PR 813 HEADER: Test 888097 TYPE FUI 3/9 **§**SGM うらもとてもいめるとの気をしなすいめのとうなみをごとしめるとうらかをことするかをしているのとの気をしたてのののとうです。

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TEXT. OUTPUT

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text.output:10/12/88 12:49 P

		6	AVERAGED	DATA ON MEASUR	REMERT DATA SE	S1.2			
TEST 88A097	CROSSOVEN '	START TIME	10/10/88	\$:37:48.70	PROCESS TIME	10/12/88 1	2:39:00		
₽/F ID₩	826 PUMP DEL	7 In. Temp	5 Torçue 4	3 FLOMARTE	838 THRUST D	900 REAR TOR	901 FWD TORQ	903 LUBE OIL	902 LUBE OIL
APS& TYPE	TA PR	ERATURE	-1	R #2	ISK DRAI N FLOW	QUE TEMP	UE TEMP	TEMP #1	TEMP #2
1	1.1449	68,464	8.0963	-0.11805	-0.154702-01	75.662	75.707	90.640	96.493
2	0.84515	67.578	52.482	40.986	5.7271	75.879	75.845	103.03	106.89
(N) -	451.86	65,773	6254.5	644.70	106.75	79.538	77.673	100.31	108.12
1 -	547.88	65.270	6374.6	593.86	129.75	83.019	80.260	107.24	112.86
 n 4	613.8U	50. V3.	0.858 0.858 0.858	401-045	139.40	66 . 15U	88.447	117,83	121.40
•••	637.95	67.182	3810.8	371.46	139.43	91.118	93.827	118.70	124.97
8	646.77	67.316	3688.4	333.80	140.88	91.921	95.256	121.14	124.91
	600.30	67.631	3630.8	305.52	136.03	93.174	96.766	120.54	124.14
10 1	603.08	67.835	3536.0	273.07	136.41	94.186	97.626	125.50	124.56
~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	465.81	67.802	3365.4	424.68	110.21	85.877	84.584 06 252	101.66	110.34
7 77	611.65 626 66	50, 500 500 500 500 500 500 500 500 500 500	a 0000	400 45	12/.12 120 04	50,505 00 640	80.JJJ	17.0UL	12.911
	624 B1	65 610		282.77	138.67	90.216 90.216	89.155	114 51	120.66
	639.25	65.694	3812.3	367.99	139.46	90.805	90.371	115.84	122.43
16 1	598,40	65.721	3733.1	338.05	135.82	91.120	91.204	116.39	123.51
17 1	597.23	65.811	3652.2	309.12	136.20	91.498	91.830	117.65	123.73
18 1	602.35	65.889	3549.0	277.19	136.34	91.840	92.474	129.57	124.89
19	606.41	65.962	3486.0	250.44	136.68	92.426	93.322	125.23	125.45
20	-0.10951	66.051	-0.42611	-0.959142-01	. f.5120	89.378	90.213	106.82	113.70
2	204.54	66.685	1.999. 1.000	1977, 724 1977, 724 1977, 724	62.476	85.689	85.454	100.61	107.63
200	291.55 103 57	66,885 65 583	1380.3 844 32	-6.12300	14.913 103	64.645 63.673	84.584 83.601	103.12	107.32
24	439.79	65.239	3873.4	587.36	111.78	82.357	82.599	103.32	105.52
25	610.98	65.264	4044.0	451.12	138.17	84.315	84.388	104.89	111.74
26 1	624.12	65.260	<b>3</b> 931.7	€10.0€	138.35	85.316	85.282	114.01	116.39
27	632.15	65.289	3846.5	383.62	139.97	86.264	85.581	113.69	117.45
1 82	636.42	65.344	1.05/17	11.992	20°191	86.119 01 101	67.139 00 000	111.28	50.8TT
7 52	643.94	65,405	3713.6	339.12		88.190	195.88	110.40	121.32
1 .	651.08	60.42C			57	61.400 61 Feb	027.48	111.19	00.221
51 F	604 79	176.ED		513.15	50.074 574 575	07.026	000.00	06 211	04.271
				21 136		001.00	00 460	07.1TT	30 501
	501 - 50 501 - 50	65.843	3573.0	277.07	137.73	88.552	91.141	114.14	123.57
35 1	597.73	65.936	3655.9	309.97	136.77	88.730	91.613	123.90	124.16
36 I	597.20	65.972	3746.0	339.15	135.99	89.018	92.013	123.20	123.76
37 I	594.10	66.060	3829.9	368.81	135.87	89.209	92.387	118.24	124.00
000 000 000	591.89 588.24	66.125 66.192	3867.8 3929.9	383.76 410.12	135.97 135.03	89.431 89.661	92.788 93.155	116.93 112.40	123.81 123.08

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TUTTUO TXT

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AVERAGED DATA ON MEASUREMENT DATA SETS

HEADER :	CRCSSOVER	TEST				)			
TEST EBAC	197 TES1	START TIME	10/10/88 14:	37:48.70	PROCESS TIME	10/12/88 1	12:39:00		
toi 3/8	826	•	S	ŝ	838	006	106	<b>9</b> 03	902
	PUMP DEL Tà pr	IN. TEMP FRATIOR	TORQUE	FLOWMETE D 10	THRUST D	REAR TOR	FWD TORO	LUBE OIL TEMP #1	LUBE OIL
IYT ISCM	ы a		à	1	R FLOW			-	71 HIT
40 1	591.93	66,284	<b>4</b> 029.9	452.91	136.24	89.906	93.438	109.48	121.46
41 2	600.12	66.978	3936.1	449.99	135.61	91.459	94.911	108.84	115.87
<b>4</b> 2 <b>2</b>	-0.24178	67.400	12.378	-0.10540	4.0012	89,609	93.498	102.78	107.31
43	480.08	67.411	3332.6	\$26.25	116.90	88,056	89.450	104.91	110.96
<b>~</b> u	527.06	66.307	3571.4	<b>6</b> 29, 73	124.69	86.442	86.736	106.22	106.48
5 7 7 9 7 9	434.96	62.522	2801.0	284.83	101.26	84.366	86.936	109.00	114.58
P/F IDS	904	905	950	951	95.2	4	953	RSD	851
	GEAR CAS	LUBE OIL	ACCEL X	ACCEL Y	ACCEL 2	SPEED	LUBE OIL	FLEX FLO	GBOX OIL
ITT ASCH	10 x r w	1 300	CTV4	21VU	0170		MOT 4	1 L L	2
~	75.804	94.559	0.482808-01	0.713202-01	0.198698-01	1.0119	26.372	945.06	42.860
N (		403°0A	0.690238-01	0.823502-01	U.19538E-U1	249.41	19.059	16.298	39.736
•	12.20	1111 11 1111 111	0.1881.0	0.12219	0.15252	6287.8	19.114	942.40	28.292
-4 yr		230.52 23 033	C.14075		0.19160	0.1250	19.006	25.144	10/ .22
4 <del>-</del>	110 45	270.50 778 50	1.1002	C. 21.50	0.10414	1.2250	10.016	90. 454 62 020	052.12
	121.67	60 - 235			0.456 C	6300 R	901 01	62,026	
. a	123.97	93.632	0.95253	0.70893	0.4264	6320.9	19.401	936.41	18.419
	127.94	94.429	0.17099	0,12522	0.23754	6322.3	19.682	935.29	18.098
10 1	130.23	93.851	0.16529	0.12445	0.19853 r	6323.8	19.763	934.87	17.913
11 2	89.155	93.656	0.16312	0.13518	0.12475	5262.4	20.282	912.95	28.499
	025.33	93,590	0.17069	0.13678	0.14949	6321.7	20.231	912.81	26.548
		771 - 7A	10505.0	0./0483	2 - 50 - 10 - 10 - 10 - 10 - 10 - 10 - 10	0.2220	CUP.UZ	912.83 010 67	196.C2
امبر ق آلو ه نمبر 9	63.053	94.097	0.88731	0.25212	0.55483	6321.5	20.201	912.55	23.878
10	94.843	94.160	0.23499	0.13620	0.23992	6321.8	20.052	912.13	23.250
17 1	97.269	94.147	0.21964	0.12228	0.22445	6322.0	20.207	911.82	22.659
16	55.556	020. 15	0.18528	0.11939	0.19713	6322.4	20.139	911.63	22.142
67	102.54	94,354	0.17060	0.11167	0.23366	6321.6	20.194	911.37	21.582
107	20.01	121.14	0.393992-01	0.645072-01	0.16847E-01	0.97300	20.454	11.116	28.991
N 0 0 0 1	50 - 100 50 - 100	41.174 00 459	0.11413 0 12001	0.1174	0.11458 A 15216	2225.5	162.02	901.90 688 47	31.U/4 31 537
10 14 14	020 40	179 60	0 745359405	0 001760 U	0.110110 0 515500-01		161 14	50 73	LVL VE
24 10 10	78.355	93.678	0.20683	G: 16696	0.28566	5834.4	31.084	723.17	27.774
25	79.139	53,783	0.17365	0.14209	0.16597	6321.7	26.121	739.53	27.077

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TEXT OUTPUT

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. 630333	. 444025080	6734	AVERAGED DA	TA ON MEASURI	as vlvg lning	SL			
TEST 88A097	1531	START TIME	10/10/88 14:	37:48.70 E	PROCESS TIME	10/12/88	12:39:00		
€dI 3/a	904 GEAR CAS	TID SOS	950 ACCEL X	A 13000	352 ACCEL 2	0234S	953 LUBE OIL	B50 FLEX FLO	851 GBOX OIL
3477 <del>1</del> 204	L TEME	T ANS	AXIS	AXIS	VXIS		FLOW	84 <b>M</b>	Яđ
26 1	80.359	93.432	1.1544	16275.0	0.54543	6321.6	24.084	736.57	26.547
27 1	81.968	94.061	1.0835	0.56001	0.52028	6322.3	19.848	734.41	25.909
20 20 20	83.444 85 671	261.5 <b>8</b>		0.52522	0.55724	6321.2	19.167	733.64	25.260 24 501
	67.837	977 - E 6	1.0395	0.56647	0.30059	6321.5	26.820	732.30	23,842
1	90.290	94.193	0.18839	0.12265	0.21764	6321.5	26.279	731.71	23.236
32 1	£15 . 25	94.455	0.17801	0.12970	0.29812	6320.7	28.876	731.28	22.815
33	94.541	93.831	0.19815	0.10779	0.21407	6320.2	31.084	731.27	22.510
	97.331	93.556	0.19214	0.11572	0.23076	6321.5	31.084	731.17	21.987
50	662.65	94.267	0.23206	0.11432	0,25286	6321.6	28.517	713.83	21.697
-1- 	100.99	409'05 111'05	0.20942	0.12555	0.22085	6321.1	28.532 20 AEC	715.61	21.390
	104.24	11. 11. 12. 15.	0.0400	0.13125	0.64641	1.1007	000 CC	717 36	071.12 021.12
	106.14	617 × 6	0.0000			5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.100 5.1000 5.1000 5.1000 5.1000 5.1000 5.1000 5.1000 5.1000 5.1000 5.1000 5.1000 5.1000 5.1000 5.1000 5.1000 5.10000 5.1000 5.10000000000	27. R33	717.68	20.570
1	107.62	93.665	19161.0	0,10883	0.20537	6321.8	27.314	728.10	20.297
<b>6</b> 1 2	118.88	94.248	0.19672	0.13763	0.19769	6321.8	29.509	718.09	19.050
42 2	123.97	94.373	0.435412-01	0.654502-01	0.216262-01	1.3900	19.805	748.73	26.942
6 6 7	108,74	93.758	0.11367	0.85801E-01	0.18385	5471.7	27.045	740.98	27.088
	94,306	93.149	0.17509	0.13562	0.14257	5776.3	23.945	736.47	27.776
2 2 2 2 2	78.946	50.00 50.00 50.00 50.00	0.17369	0.13628	0.14816	5797.8	24.026	777.37	28.817
2 9	672, 52	480.14	0.35418	95612.0	6.20062	5050.0	CON. 02	108.32	8nc.12
				.: •	•		•		
P/F 104	926	-152	-25	-26	-107	е С	-152	-193	-194
• . •	G-BOX TE	B I MOLT	NPSH IND	NSS IND.	H TOT-12	D/S PRES	FLOW I R	SCALED N	SCALED F
	MP ALARM	ATIC LAD	-1+	1.	EAD 2 IM	S. PIPE	ATIO IND	DANI HSA	TOM IND.
HDS# TYPE		- 41	-		-4 	4	 ##*	1	1
1 1	SETE.E	0.19632	213.14	0.388512-02	-2,4010	92.141	. 0.19632	0.55227E+11	49.669
2	3.3134	9.2647	213.95	63,316	2.1726	92.490	9.2647	0.34463E+11	476.61
c9 -	3.3134	1.2372	214.80	3044.5	547.53	92.859	1.2772	8080.9	66.204
		1.2231	213.82	3016.3 2375 0	534.32	52.435	1.2231	7957 3 7020 c	60.594 AF 60:
 n -2	2535.5	0.889.7		5 - 1 - 1 5 - 1 - 1 7 - 1 - 1 7 - 1 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7 - 1 7		400 000 400 000	0 88237	9.5561	100.05
• • •	3.3134	0.86276	213.25	9K39.1	654.42	92.188	0.86276	7933.0	37.749
- <b>6</b>	3.3130	0.401.94	213.05	2448.7	651.36	92,104	0.60198	7930.5	33.911
еч Ф.	3134	0.71808	210.97	2383.9	672.69	91.205	0.74808	7849.9	31.154
10		0.69193	211.53	2293.9	01.517	195.16	0.69193	7867.0	27.716
2 11	3515.5	1.3531	211.93	2314.1	210.42	91.628	1.525/	0.449606+10	242.90

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text.output:10/12/88 12:49 PM

- 37 -

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TEXT. OUTPUT

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PROCESS TIME 10/12/88 12:39:00 AVERAGED DATA ON MEASUREMENT DATA SETS HEADER: CROSSOVER TEST .... HEADER: CROSSOVER TEST ..... TEST 88A097 TEST START TIME 10/13/88 14:37:48.70

	<pre>K FLOW 7 R ATIO IND . #1 0.99432 0.99432 0.85919 0.85919 0.85919 0.85919 0.85919 0.85919 0.70070 0.70070 0.70070 0.85719 0.85719 0.82719 0.88479 0.88479</pre>	WPSH IND 41 41 41 41 41 41 41 41 41 41	NSS IND. 11 2750.6 2569.0 2569.0 2569.0 2569.0 2559.3 2319628-01 1058.8 672.13 672.13 672.13 672.13 672.13 672.555.3 2755.5 2755.5 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1058.8 1	ST+TCT EAD - 2 IM P. <b>#</b> 1 655.34 655.11 652.10 652.10 672.49 672.49 672.33 356.62 356.62 356.62 120.30 519.51 519.51 519.51	Р/S 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	FLOW 1 R ATTO IND . #1 18 . #1 0.99432 0.994339 0.922117 0.859139 0.75409 0.75409 0.75409 0.75409 0.75409 11.955 2.11995 6.71995 1.1995 2.11995 1.2907 0.2907	SCALED N FSH IND. #1 7838.1 7938.1 7945.2 7945.2 7945.2 7945.2 7945.2 7935.6 7733.6 0.57430E+11 0.57430E+11 0.87440E+10	SCALED F LOW IND. #1 45.963 39.022 331.506 51.799 69.737 51.799 69.737 111.232 111.232 551 551 551 551 551 551 551 551 551 55
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	0.70070 0.65669 11.953 2.1185 2.1185 6.1185 6.1185 0.9201 0.82719 0.88479	210.34 207.81 2136.75 218.75 218.75 218.58 211.58 211.58 213.58	2319.0 2293.7 2293.7 0.37962E-01 1058.8 672.13 662.27 2755.3 2755.3	693.97 701.32 -3.3381 264.02 356.62 319.51 519.51 642.29	90.931 89.838 91.073 92.135 92.135 91.39 92.35	0.70970 0.65669 11.953 1.3372 2.1195 6.7096 6.7096	7826.1 7733.6 0.57438E+11 0.86463E+06 0.87440E+10	28.258 25.554 51.799 69.737 11.233 79.551 79.551
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	0.88479		2628.8	040.040	92.313	0.92719	7947,0	41.771
		214.31	2561.5	649.70	92.549	0.88479	1974.1	39.034
	0.86277	213.74	2534.4	647.96	92.401	0.86277	7955.5	37.582
	0.81286	212.23	2474.6	644.81	91.747	0.81286	7.1697.7	34
	0.76268	210.17	2416.2	646.06	90.856	0.76268	7821.6	31
	0.70327	211.08	2325.9	676.92	91.251	0.70327	7855.8	25
3.3132 3.3132 3.3135 3.3135 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.31355 3.31355 3.31355 3.31355 3.3135555555555	0.65564	205.17	2333.1	685.88	88.698	0.65534	7637.8	25 4 4
3.3132 3.3135 3.3135 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3134 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3155 3.3155 3.3155 3.3155 3.3155 3.31555 3.315555 3.315555555555	0.65968	209.05	2260.6	696.13	90.372	0.65968	7783.3	25.581
1 3.3135 3.3134 3.3134 3.3134 3.3134 3.3134 3.3133 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3135 3.3155 3.3135 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.3155 3.31555 3.31555 3.315555 3.315555555555	0.70188	225.04	2215.6	682.40	97.286	0.70188	8375.3	28.192
1 3.3133 1 3.3134 1 3.3134 1 3.3134 1 3.3133	0.75553	213.43	2374.8	675.92	92.266	0.75553	7942 F	31.533
1 3.3134 1 3.3133 1 3.3133	0.80334	212.63	2455 3	669.57	91.920	0.80334	7914.4	34.508
1 3.3133 3.3136 3.3136	0.85315	212.32	2534.1	663.60	91.786	0.85315	7900.6	37.540
1 3.3136	0.87815	212.97	2563.9	659.68	92.069	0.87815	7925	£\$0. <b>6</b>
A ( ) ( A )	0.92185	212.80	2628.2	655.61	91.994	0.92189	7920	061.15
1 3.43.54	0.99573	213.77	2722.3	654.73	92.412	0.99573	7955.0	46.1
2 3 3134	0.99068	65.836		611.89	28.467	0.99068	2450.1	45.893
3.3141	12,559	213.37	0	)423	92,243	12.559	0.49889E+11	65.432
2 3138	1.096	214.50	311 4	. LE, 93	92.728	1.0965	26826.	52.755
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	-812	TT HEED	RISE 13	1.4079	3.1387	116.55	112.58	74.501	54.808	54.399	42.098	75.744	78.560	74.142	77.896	66.319	59.935	56.533	81.231	77.248	75.655	75.026	-0.88656	33.387	23.764	23.530	104.09	76.219	68.405	59.503	55.421	48.911	38.126	74.351	71.274	75.903	78.109	78.659	81.154	82.820	84.936	T/T'/0
	-811	PEAD	RISE #2	1.3120	3.5935	110.76	106.20	59.369	43.695	43.835	33.502	72,983	77.902	70.424	74.024	63.392	57.955	54.136	80.273	73.120	74.910	74.094	1.7236	33.722	24.693	24.015	99.643	72.602	66.146	56.322	53.204	46.424	37.971	71.131	69.474	76.126	76.118	76.376	78.593	19.011	81.630 03 710	271 20
	-810	TT HEAD	RISE #1	-0.93450	1.2831	116.54	114.50	79.983	62.300	62.558	51.240	78.670	84.705	75.054	82.476	73.041	67.769	65.088	67.009	77.563	80.051	78.366	-0.72593	37.224	25.246	24.260	105.40	81.727	75.351	66.435	64.466	57.327	46.595	77.750	75.875	82.221	83.739	83.112	86.137	84.015	B7.220	50.00
	-809-	T-T HEA	DEISE	-2.1876	-3.9228	383.35	497.35	613.70	672.26	676.51	703.72	536.38	491.22	455.80	618.57	642.85	665.33	678.63	513.18	532.47	511.50	503.28	-2.5363	151.12	205.90	90.495	389.14	623.93	646.54	667.32	678.04	698.83	715.49	527.07	516.63	502.10	519.86	527.46	534.51	540.67	541.23 FAT 26	00.340
	-608	IC READR	ISE	0.18367	6.0927	654.07	346.18	1017.8	1032.9	1034.9	1040.5	1011.3	1019.7	783.70	1602.7	1025.4	1031.6	1034.7	1011.5	1020.6	1023.7	1023.3	-0.96464	377 . 66	502.07	183.67	796.13	1002.2	1024.1	1029.5	1631.3	1037.9	1039.2	1005.1	1018.0	1022.0	1022.6	1019.6	1016.6	1009.8	1007.0	20001
	-152	AL DIND	1944 1944	<b>9.156</b> 32	2.2647	1.2772	1.2233	0.59403	0.88237	0.86276	0.80198	0.74808	0.69193	1.3537	0.99432	0.92717	0.88239	0.85919	0.80243	6.75409	0.70076	0.65669	11.953	1.3372	2.1195	6.7096	1.2907	0.99601	6.92719	0.88479	0.86277	0.81286	0,76253	0.70327	0.65564	0.65968	0.70188	0.75553	0.80334	0.85315	0.87815 0 60100	כייקיים
-	198-	TOT-51 J	EFD 42	≈0 25512	-2.2676	29, 539	46.737	83.017	106.14	108.46	116.52	129.19	133.64	58,685	91.532	97.570	104.45	107.40	122.29	124.56	134.96	149.63	-0.65682	37.694	99.300	5.9160	27.781	89.955	56.197	102.17	106.41	112.40	123.71	133.91	153.26	145.76	117.25	122.84	119.14	112.83	107.66	
	-8()#) -6()#)	TCT-57 H	13 Gv3	-0-36831	a <2,6700	30.635	ିଟେ " 4 ଅନ୍	.€ ≥ <b>3</b>	108.28	110.04	118.24	129.80	135,71	3 58.432	91.465	<b>58.517</b>	106.40	109.10	123.63	124.87	137.62	152.71	1-1.2878	38.196	1 <u>\$8.230</u>	5.6248	28.768	90.162	57.368	103.13	108.38	113.96	125.18	134.22	153.90	1.98.44	120.22	124.21	120.56	112.92	107.44	12.021
	47.95 € €3467 s	ERD L'IG	ert Min.	-r .9021 3E +09	*', 56928E~'	£0283.	476≎6.	53028.	54901.	55175.	56025.	52506.	52653,	-0.53844E+06	53238.	<b>54</b> 516.	55180.	55532.	52215.	52197.	52655.	53156.	-0.15136E+10	15410.	-0.169192+03	-0.60252E+09	<b>\$2041.</b>	53167.	54267.	56896.	55292.	55907.	56634.	52435.	53051.	52868.	12615	52195.	52174.	51947.	51732.	
	5',1 J/ 5		Daf Tree	l I	2 2	4) (~4		-1 -2	6 1	1	6 1	••4 69	10 1	11	1. 22	. 13 1	14 1	15 1	-4 94	1 1	18 1	1 61	20 1	21 2	22 22	23	24	- 25 1	26 1	1	28	29 1	30	31 15	32 1	33		35	36 1	37 1	00 0 00 0 01 0	4

text.output:10/12/88 12:49

AVERAGED DATA ON MEASUREMENT DATA SZTS

- 39 -

TEXT. OUTPUT

CROSSOVER TEST HEADER:

TEST BUAUS	7 TEST	START TIME	10/10/28 14	:37:48,70 E	ROCESS TIME	10/12/88	12:39:00		
P/F ID#	-195 Scaled H Ead 180.	-600 INDUCER TOT-ST H	-801 INDUCER TOT-ST H	-152 FLON 1 R ATIO IND	-808 IMP STAT IC READR	-809 Xovr 0/S T-T Hea	-810 Xovr D/S TT HEAD	-811 XOVR D/S TT HEAD	-812 XOVR D/S TT HEAD
	si si si	TX NVA	EAU 52	-1	201	ALIXU	NISE FI	K18% FZ	RISE #3
	52142.	89.079 60.143	808. 808 805. 808	0.99573	1001.9	515.93	90-155	81.164	84.167
	-0.339522+09	2.2762	2.6857		20128		-0.55441	1/0.20	66,304 -0 57587
5	50255.	67.942	67.559	1.0965	805.60	483.20	70.747	64.231	66.753
44	51807.	76.810	76.693	1.0292	877.43	538.66	72.688	66.404	69.017
20 10 10 10 10 10 10 10 10 10 10 10 10 10 1	56405. -0.222516+69	66.612 78.376	66.737 78.117	1.0838 1.9613	871.56 727,72	519-01 211-51	81.967 61.59%	74.700 55.24r	78.370
					1			2	
101 3/4	-613	-152	-815	-816	-817	-81 81 1	-819		
• •	STAGE T-	FLOW 1 R	KOVR TT	LL JANA	RESULTAN	RESULTAN	NET AXIA		
HDSE TYPE	T HEADEL	ATTO INU	HEADRISK \$2	HEADELSE	T AXIAL LOAD (-)	T AXIAL LCAD (+)	L LOAD		
-1 (	-3.5303	0.19632	-0.87555	-2.6567	16409.	9845.8	562.85		
N 0	-0.42128	9.2647	-0-32830 	-0.921998-01	10622.	10070.	551.10 006 0		
1 1 	1284.6	1.2231	603.55	681.76	040100. 67178	64659.	-2480.7		
	1425.1	0.99403	673.07	752.79	68410.	70654.	-2244.6		
	1475.4	0.88237	715.96	760.21	70346.	72568.	-2222.4		
~ 8	1483.1	0.86276 0.80198	720.35	763.55	71416	73662.	-2267.9		
0	1411.1	0.74808	609.36	802.43	69142.	71861.	-2718.9		
101	1415.8	0.69193	569.13	e47.31	69748	72672.	-2924.1		
	5 0611	1.3537	226.22	000 100 100	5	106498. 106498.	-2095.4		• •
-1 e-4	1465.1	0.92717	712.24	753.60	69512	71748.	-2236.2		
14 1	1482.8	0.88239	723.28	760.25	70214	72461.	-2250.5		:
15	1492.1	0.85919	732.76	760.17	70590.	72840.	-2250.2		
	1403.1	0.80243	593.46	610.69	68939.	71578.	-2638.9		-
1 21	1402.7	0.75409	605.59	36.262	69906.	71762.	-2695.9	. •	
	1415.2	0.70070	506.41 577 37	829.64 851.82	69803 70530	73504	-2817.6		
50	1556. 1-	11.953	-0.81272	-3.9907	10179.	9648.8	530.44		
21 2	486.53	1.3372	184.84	301.96	31450.	32370.	-920,03		
22	696.42	2.1195	230.59	466.25	49928.	42440.	-1511.9	•	
() () () ()	240.72	6.7096	114.51	126,33 E43 05	20222.	20367.	-164.62		
1 44 1 40 1 44	1428.7	0.99601	696,53	132.94	67815.	70874.	-3058.7		

text.output:10/12/88 12:49

AVERAGED DATA ON NEASOREMENT DATA SETS

- 0

TTATO OUTPUT

PROCESS TIME 10/13/85 RT TTME 10/50/88 14:37:48 70 HEADER: CROSSOVER TEST TEST 88A097 7857 5741

						ANLENS LINE	00/27/07	00265321
L ald	<b>*</b> 0	-813	-152	-815	-816	-817	-818	-819
·		STAGE T-	FLOW 1 R	XOVR TT	LL annd	RESULTAN	RESULTAN	NET AXIA
		T HEADRI	ATIO IND	BEADRISE	HEADRISS	T AXIAL	T AXIAL	L LOAD
NDS	TYPE	35	. 41	(J	•	LOAD (-)	(+) GYOT	
26	<b>.</b>	1458.2	0.92719	712.69	746.29	69299	71903	-2503 6
27	<b>~~1</b>	1475.4	0.88479	723.64	752.57	70047.	72316.	-2569.4
28		1485.5	0.86277	731.24	755.06	70404.	73084.	-2680.3
50	~	1502.3	0.81286	745.25	757.90	70974.	73663.	-2689.1
	-4	1523.1	0.76268	753.46	770.45	71694.	- E3457	-2758.7
	~1	1408.9	0.70327	598.20	611.54	69239.	72460.	-5221.5
32	<b>r</b> 4	1425.1	0.65564	586.10	839.86	69911.	73254.	-3342.9
39		1420.0	0.65968	578.22	842.60	70118.	73397.	-3279.3
3		1395.5	0.70188	595.98	800.34	69474.	72563.	-3088.7
5	<b>-</b> -1	1402.5	0.75553	603.83	799.45	69020.	72103.	-3083.0
ର ମ		1401.7	0.80334	613.11	789.38	68603.	71781.	-3178.3
(** (*)	-	1396.0	0.85315	613.68	777.09	68175.	71275.	-3099.7
92) (*1)	-1	1390.1	0.87815	622.86	767,99	67361.	70948.	-3086.6
U) M	Į.	1381.6	0.92189	625.03	757.30	67528.	70555.	-3026.9
0		1400.1	0.99573	657.13	743.67	67322.	70401.	-3079.3
	3	1405.5	0.55068	712.44	653 . 56	56852.	60211.	-3359.3
V W	0	-1.1318	12.559	0.46576	-1.6590	10571.	10048.	523.25
	¢ł.	1133.8	1.0965	547.44	583,82	56174.	58725.	-2553.8
-	2	1240.3	1.0292	605.06	- 635.86	60516.	63357.	-2841.7
1	~	1215.9	1.0838	16-265	622.88	59510.	62308.	-2798.1
9	ି ବ୍ୟ	1016.7	1.9613	466.76	550.71	47840.	50219.	-2378.5
		•						

	Report Do	cumentation F	'age	
1. Report No. CR-194447	2. Government Acce	ssion No.	3. Recipient's Cat	alog No.
4. Title and Subtitle Orbital Transfer Vehicle Er	aine Technology		5. Report Date December 19	92
High Velocity Ratio Diffusir	g Crossover		6. Performing Org	anization Code
7. Author(s) Brian W. Lariviere	<u>, , , , , , , , , , , , , , , , , , , </u>		8. Performing Org RI/RD89-11	anization Report No. 1
			10, Work Unit No.	
9. Performing Organization Nam Rockwell International Rocketdyne Division P.O. Box 7922 Canoga Park, California 9130	and Address		11. Contract or Gr NAS3-2377	ant No. 3 - Task B.2
12. Sponsoring Agency Name an	d Address		Final Report	- 12/83 to 12/89
National Aeronautic Space Lewis Reseach Center Cleveland, Ohio 44135	Administration		14. Sponsering Ar NASA-LeRC	Jency Code
15 Supplementary Notes				A
<ul> <li>16. Abstract</li> <li>High speed, high efficiency effectively convey the pumpe Orbital Transfer Vehicle (OTV velocity ratio diffusing crossor the operating conditions requisated on advanced analystic steady flow. To secure the or characteristics produced by a MK49-F turbopumps first stag</li> <li>Water and air tests were com- velocity on the pump and cro flow were completed in water and air tests were compared to</li> </ul>	head rise multistage d fluid from the exit of hit fluid from the exit of the MK49-F, a three er. This velocity ratio red by the OTV syste al techniques anchore lesign and the analyt impeller. A tester was e, including the induce pleted to evaluate the soover head and efficito to assess these pump with the actual MK49-f	e pumps require lone impeller to e stage high pre- e approaches the m. The design of od by previous to ical techniques, as designed and er, impeller, and e large scale tu ilency. Suction o characteristics. F test data in lim	e continuous passage the iniet of the next imp ssure liquid hydrogen tu diffusion limits for stabl of the high velocity ratio asts of stationary two-dir tests were required wit fabricated using a 2.85 the diffusing crossover. rbutence, non-uniform v performance tests from Pump and diffuser perf uid hydrogen.	diffusing crossovers to beller. On Rocketdyne's rbopump, utilizes a 6.23 e and efficient flow over diffusing crossover was mensional diffusers with h the unsteady whirling times scale model of the relocity, and non-steady 80% to 124% of design formance from the water
17 Knu Wards (Suggested by Au	hartall		Charles and a	
Orbital transfer Vehicle Engine; O Hydrogen Tuibopump; Multi-stage Crossover.	TV; OTVE; Liquid pump; Dilluser,	Unclassified Subject Cate	- Unlimited gory 20	
19. Security Classif. (of this repor Unclassified	) 20. Security Classi Unclassified	i. (of this page)	21. No. of Pages 151	22. Price

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