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ABSTRACT

This report describes the application of Reynolds-Averaged Navier-Stokes (RANS) codes to viscous-flow problems associated with marine propulsors. The theory behind RANS codes is described, and the numerical solution methods typically applied to solve the RANS equations are discussed. A description of the strengths and limitations of applying RANS codes to predict real fluid effects is given. Careful scrutiny and engineering judgment must be exercised in the interpretation of predictions based on the turbulence models typically embodied in RANS codes. Two benchmark computations using DTNS3D, a typical RANS code, are presented to illustrate interpretation concerns. The examples include flow over a pipe expansion and flow over the leading edge of a blunt rectangular plate.

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INTRODUCTION

In the design of fluids engineering devices that use slender bodies and lifting surfaces as their components, the application of potential flow methods are useful. This fact is particularly true in the design and performance evaluation of marine propulsors. In the analysis of slender bodies or lifting surfaces viscous effects are assumed to be confined to thin boundary-layers adjacent to the solid surfaces of the body that moves (or is propelled) through a fluid. The flow field exterior of the boundary-layers is assumed to be potential. These assumptions are known to be realistic for propulsors operating in an irrotational free-stream (or onset flow). In many design scenarios, however, the propulsor operates in the wake of the ship it is designed to propel. In these situations the inflow is rotational, i.e., it has finite vorticity or internal shear stresses. When the propulsor is designed to operate in a sheared onset flow it is still a reasonable approximation to assume that the propulsor is a potential flow producer. In this case the effects of the propulsor's induced flow on the distortion of the inflow vorticity must be taken into account. It is taken into

account by computing an effective inflow either empirically or by applying a computational method that computes the additional induced velocities associated with the stretching and turning of the vorticity in the onset flow when it is acted upon by the propulsor. In conventional propulsor-design practice, this distorted onset flow is called the effective wake. The wealth of successful experience in the design of wake adapted propellers provides substantial support for these assumptions.

Why would we need Reynolds-Averaged Navier-Stokes (RANS) codes in the analysis of marine propulsor designs? In the conventional procedure for the design of ship hulls, the hull shape is selected without regard to the detailed geometric configuration of the propulsor. The hull is selected based on low tow resistance; hence, a nonseparating bare hull is typically designed. If hulls with fuller stern shapes are desirable, then the potential for suppressing flow separation with the propulsor cannot be ignored. In order to examine the propensity for a full stern hull to cause flow separation and to examine the effect of propulsor design on suppressing flow separation, a RANS code should be considered. This is because flow separation is primarily a real (or viscous) flow effect. Additional opportunities for RANS analysis occur on the complex surfaces of propulsor components.

This report presumes that there is an interest in applying a Navier-Stokes or (real fluid) viscous flow code to evaluate a given propulsor design. In addition, it also presumes that time-averaged flow properties are required. From a practical point of view a RANS code should provide reasonable approximations of the time-averaged flow properties in high Reynolds number flows around complex geometries.

What is involved in selecting and using a RANS code? It is this question that is considered in this report. The theory of turbulence modeling typically implemented in RANS codes is described. This description is followed by a description of the computational methods required to solve the RANS equations. The selection of grids and other issues related to the application of a RANS code are discussed. Finally, two RANS codes that could be used by the marine propulsor designer are described.

In the next section of this report the theory that describes the flow of water is presented. This theory is the foundation on which the models to predict the time-averaged flow properties of a turbulent flow are built.

THEORY

It is well known in the fluid mechanics community that the Navier-Stokes equations are the equations that model the dynamics of water and air (at low Mach number, less than 0.3). The Navier-Stokes (N-S) and continuity equations in nondimensional form are as follows:

$$\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} = -\nabla P + \frac{1}{\mathcal{R}} \nabla^2 \mathbf{u}, \quad (1)$$

and

$$\nabla \cdot \mathbf{u} = 0. \quad (2)$$

The parameter $\mathcal{R} = UL/\nu$ is the Reynolds number, where U is the characteristic velocity of the flow problem, e.g., the uniform speed of a ship, L is the characteristic length of the flow problem, e.g., the overall length of a ship, and ν is the kinematic viscosity of the fluid, e.g., for fresh water $\nu = 1.0 \times 10^{-6} \text{ m}^2\text{s}^{-1}$ at 20° C . Equations (1) and (2) are a set of four equations in four unknowns, viz, the three components of the velocity vector $\mathbf{u} = (u, v, w)$ and the dynamic pressure $P = p/(\rho U^2)$. The density and kinematic viscosity are assumed to be constant. These are reasonable assumptions for the flow of water at relatively high Reynolds numbers. Typical values of the Reynolds number in flows of practical interest are within the range $10^6 < \mathcal{R} < 10^9$.

The inverse of \mathcal{R} is the coefficient of the viscous term in the N-S equations; it is obviously small as compared to the coefficients of the other terms. The importance of viscosity in high Reynolds number flows is evident for two reasons. The first reason is the physically realistic no-slip boundary condition that must be imposed at the solid boundaries adjacent to the fluid. This boundary condition causes large gradients in the mean velocity distribution near the boundaries; hence, viscous boundary-layers are formed near the solid boundaries. The second reason is the fact that the flow induced by the relative motion of a solid boundary with a viscous fluid is highly unsteady (i.e., turbulent) in the high Reynolds number flows of practical interest. The no-slip condition and turbulence are viscous flow phenomena; without the viscous terms in the N-S equations these phenomena do not exist.

The no-slip boundary condition completes the mathematical statement of the flow problem of a body moving through an incompressible fluid of infinite extent. Let us consider the flow field induced by a body moving at constant speed through an incompressible fluid. From the

viewpoint of a reference frame attached to the body, we observe a stationary body in a uniform stream $U\bar{i}$; see Fig. 1. The boundary condition on S_B may be written as follows:

$$\mathbf{u} = 0 \text{ on } S_B. \quad (3)$$

This condition states that both the normal and tangential velocity components at the solid boundary are equal to zero in the body fixed frame.

Equations (1) and (2) with the no-slip condition, (3), completely describe the flow induced by a moving body, S_B , in an incompressible, viscous fluid of infinite extent. However, for high \mathcal{R} flows around arbitrarily shaped bodies this set of equations is intractable even by computational methods with present day digital computers. This fact has led the engineering community to seek other methods to predict the time-averaged flow properties in flows of practical interest. Two of the more well known models for high Reynolds number turbulent flows are described in the next section.

TURBULENCE MODELING

Viscous flows at large values of \mathcal{R} are in general unsteady (i.e., turbulent). The design conditions for most hydrodynamic devices are imposed at a steady characteristic speed, e.g., at a prescribed ship speed or onset flow. Therefore, a computational analysis method is desirable that allows the engineer to obtain approximate solutions for the time averaged flow properties in high Reynolds number turbulent flows.

Reynolds, in 1895, proposed the following decomposition of the flow properties. He assumed that the velocity field can be decomposed into a mean, $\bar{\mathbf{u}}$, and a random fluctuation, \mathbf{u}' , such that

$$\mathbf{u} = \bar{\mathbf{u}} + \mathbf{u}', \quad (4)$$

where

$$\bar{\mathbf{u}} = \lim_{T_T \rightarrow \infty} \frac{1}{T_T} \int_{t_0}^{t_0 + T_T} \mathbf{u} \, dt,$$
$$\bar{\mathbf{u}}' = \lim_{T_T \rightarrow \infty} \frac{1}{T_T} \int_{t_0}^{t_0 + T_T} (\mathbf{u} - \bar{\mathbf{u}}) \, dt = 0$$

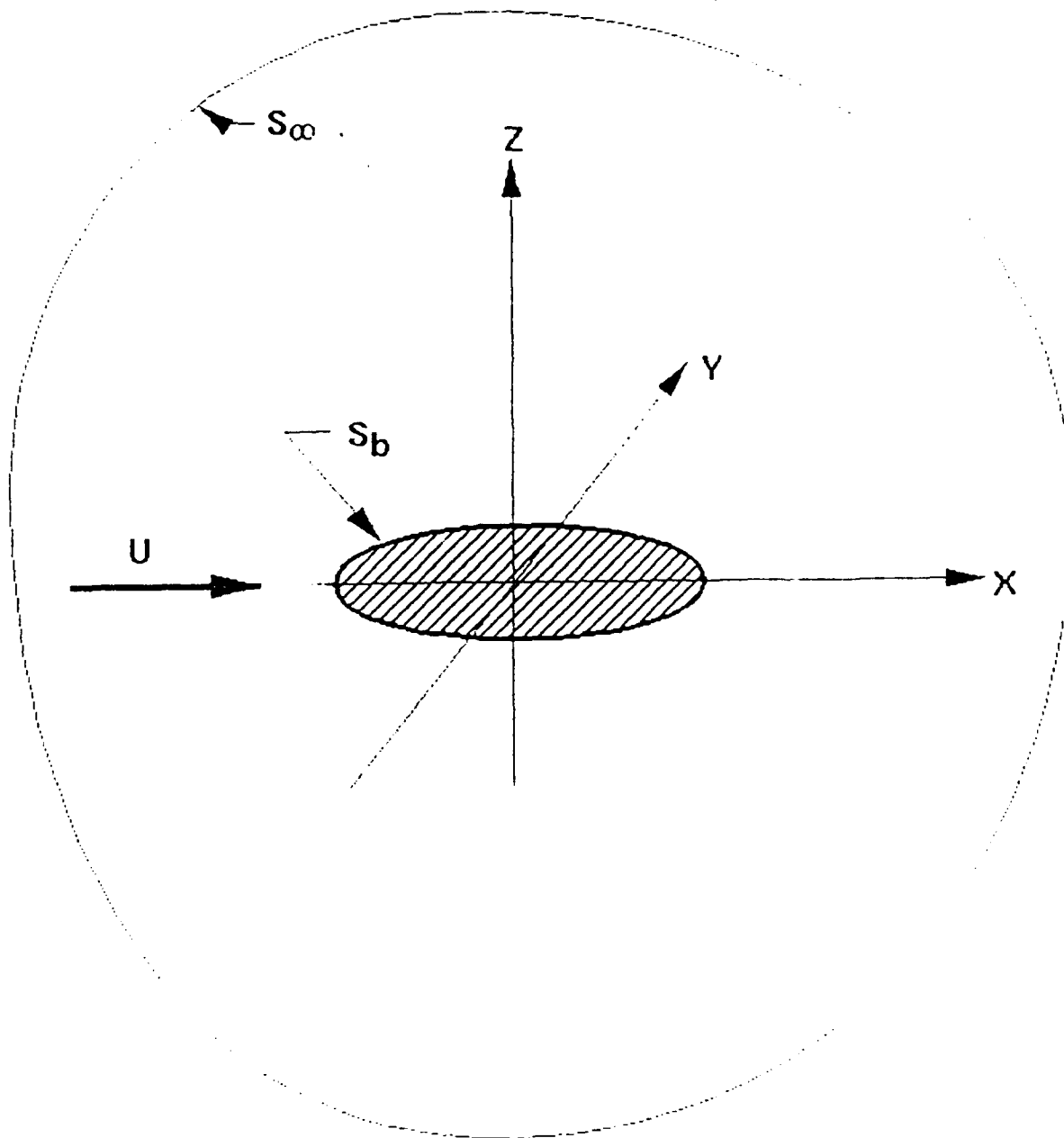


Fig. 1. Illustration of the boundary-value problem of a body in a uniform stream.

Similarly,

$$P = \bar{P} + P'. \quad (5)$$

Substituting (4) and (5) into (1) and (2) and taking the time average (as defined above) of the resulting equations, we obtain the Reynolds-Averaged N-S (RANS) equations, viz:

$$\frac{\partial \bar{u}_i}{\partial t} + \bar{u}_j \frac{\partial \bar{u}_i}{\partial x_j} = -\frac{\partial \bar{P}}{\partial x_i} + \frac{1}{\mathcal{H}} \frac{\partial^2 \bar{u}_i}{\partial x_j \partial x_j} - \frac{\partial \overline{u'_i u'_j}}{\partial x_j}, \quad (6)$$

where, of course, $\partial \bar{u}_i / \partial t = 0$; however, the time derivative is included for two reasons. The first reason is that artificial time-stepping is used as the iteration procedure for solving steady-state problems in many of the available RANS codes. The second reason is to provide the option of considering slowly varying unsteady flows, i.e., $\bar{\mathbf{u}} = \bar{\mathbf{u}}(\mathbf{x}, t)$, in which the time scales of the solid boundary oscillations are significantly longer than the time scales, T_T , of the turbulence velocity fluctuations. In this report it is for the first reason that the time derivatives are retained. (Note that Equation (6) is in component form in which Cartesian tensor notation with Einstein's summation convention is used. The velocity components implied by this equation are $u_i = u, v$ and w for $i = 1, 2$, and 3 , respectively.)

From Equation (6) we see that a total stress tensor acting on the flow may be written in the following, nondimensional form:

$$\tau_{ij} = -P\delta_{ij} + \frac{1}{\mathcal{H}} \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) - \overline{u'_i u'_j}.$$

The latter term is known as the Reynolds stress. Hence, the only effect of the random velocity fluctuations on the time averaged flow properties is the contribution of an additional stress system.

The time averaged form of the continuity equation is:

$$\frac{\partial \bar{u}_i}{\partial x_i} = 0 \quad (7)$$

Equations (6) and (7) are a set of equations for the mean flow properties $\bar{u}_i = \bar{u}, \bar{v}, \text{ or } \bar{w} = 1, 2$ or 3, respectively, and \bar{P} . However, the quantities $\overline{u'_i u'_j}$ are additional unknowns that arise from the application of Reynolds decomposition. The fact that the components of the Reynolds stress tensor are additional unknowns is an illustration of the well known closure problem of turbulence.

The decomposition of the flow into a mean flow and turbulent velocity fluctuations isolates the effects of the turbulent fluctuations on the mean flow. However, as pointed out above and discussed in detail by Tennekes and Lumley (1974), there are additional unknowns that must be determined. If we sought to derive additional equations for the components of the Reynolds stress tensor from the original N-S equations, additional unknowns of the form $\overline{u'_i u'_j u'_k}$ are generated by the nonlinear inertia terms. According to Tennekes and Lumley, this problem is characteristic of all nonlinear stochastic systems. This is the closure problem; the system of equations describing the mean flow cannot be closed without additional assumptions even though the N-S equations and the continuity equation form a complete mathematical statement of the actual time-dependent flow problem.

To attempt to solve the closure problem many engineering investigators have judiciously guessed in attempts to find a relationship between

$$\overline{u'_i u'_j} \text{ and } \frac{1}{2} \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right).$$

These attempts are by analogy (in some sense) with the constitutive relationship for a Newtonian fluid, viz:

$$\frac{\sigma_{ij}}{\rho U^2} = -\frac{p}{\rho U^2} \delta_{ij} + \frac{\nu}{UL} \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right).$$

The equation for σ_{ij} , which is the stress tensor for a Newtonian fluid in component form, is a phenomenological law which states that the stress at a point is the sum of the normal stress due to pressure plus the viscous stress, which is linearly dependent on the rates of strain (deformation) of the fluid. This equation for σ_{ij} is the constitutive equation used to derive the N-S equations from the transport theorem; see for example Newman (1977). It is this equation that connects the microscopic behavior of a liquid to its macroscopic behavior. (It is a well known fact that this equation describes the behavior of water; see Truesdell, 1974.)

One of the most popular models that arises from judicious guessing is the 'standard' $k - \epsilon$ model originally proposed by Launder and Spalding (1974). The 'standard' model, which is the model presented below, is not very general. It must be extended to include the effects of curvature, low Reynolds number, near wall, etc. Some of the extensions examined in the literature to handle complex flow fields are discussed by Nallasamy (1987) among others. The 'standard' model mainly applies to nearly parallel, high Reynolds number flows. The 'standard' $k - \epsilon$ model is called a two-equation turbulence model since two additional differential equations must be solved along with Equations (3) and (4). Because it does not handle near-wall flows, a wall-function model is required to satisfy the no-slip boundary condition at solid walls. The 'standard' $k - \epsilon$ model with the wall-function boundary condition works adequately as long as the assumptions inherent in the model are not greatly violated; numerous successful applications of this model in studies of a wide variety of flow problems have been reported in the literature. The mathematical statement of this two-equation turbulence model is given in the next subsection.

The algebraic turbulence model reported by Baldwin and Lomax (1978) is an alternative model. It is simpler than the two-equation model already described and, for high Re flows, has a wider range of applicability. Models of this type have found successful application in the prediction of separated flows; see for example Gee, Cummings and Schiff (1990). These models work well in flows where viscous effects are confined to boundary-layers and the external flow is primarily inviscid in nature with or without finite vorticity. The problems of marine hydrodynamics are generally of this type. The mathematical statement of this model is given in a subsequent subsection.

The selection and application of a turbulence model is indeed an art. Once an appropriate model has been selected, a computational method must also be selected to solve the model equations. The selection and application of a computational method also requires judgment. The issues that arise in the selection and implementation of a computational method to solve the RANS equations will be discussed in a subsequent section of this report.

Note that the turbulence models to be presented next are to a great extent ad hoc. They are tractable models that provide a means to estimate the time averaged flow fields of high Reynolds number turbulent flows. They are not models of the complete physics of flow as are Equations (1) and (2). The models are simplifications that attempt to provide the engineer with a set of model equations that can be solved with today's computational technology. Considering the successful experience with careful applications of turbulence models reported in the literature, RANS codes should find successful application in the evaluation of flows of engineering interest and, in particular, in the evaluation of some of the flow problems that arise in the design of

advanced marine propulsors. The experience to date, that has been reported in the engineering literature, supports this contention.

TWO-EQUATION, $k - \epsilon$ MODEL

The two equation model originally proposed by Launder and Spalding (1974) may be derived from a rational mechanics viewpoint that includes considerations of the energy equation and the second-law of thermodynamics; see Tannous, Ahmadi and Valentine (1989) and Tannous, Valentine and Ahmadi (1990). It is a "phenomenological" model that assumes an eddy viscosity analogous to the kinematic viscosity, i.e., it assumes

$$-\overline{u_i' u_j'} = \frac{\nu_T}{UL} \left(\frac{\partial \overline{u}_i}{\partial x_j} + \frac{\partial \overline{u}_j}{\partial x_i} \right).$$

If we define an effective viscosity as follows,

$$\nu_c = \nu + \nu_T$$

and note that ν_T is not a constant, we may rewrite Equation (6), i.e., the RANS equations, as follows:

$$\frac{\partial \overline{u}_i}{\partial t} + \overline{u}_j \frac{\partial \overline{u}_i}{\partial x_j} = -\frac{\partial \overline{P}}{\partial x_i} + \frac{\partial}{\partial x_j} \left[\frac{1}{\mathcal{R}_c} \left(\frac{\partial \overline{u}_i}{\partial x_j} + \frac{\partial \overline{u}_j}{\partial x_i} \right) \right], \quad (8)$$

where

$$\mathcal{R}_c = \frac{UL}{\nu_c}$$

In this system of equations the effective viscosity is an unknown because ν_T is an unknown; thus, the effective Reynolds number, \mathcal{R}_c , is an unknown.

In two-equation turbulence models the Prandtl-Kolmogorov hypothesis is usually invoked. It relates the turbulent viscosity, ν_T , to the turbulent kinetic energy, $k = \frac{1}{2} \overline{u_i' u_i'}$ and the turbulent dissipation function, ϵ . The Prandtl-Kolmogorov expression is, in dimensionless form, as follows:

$$\frac{1}{\mathcal{R}_c} - \frac{1}{\mathcal{R}} = \frac{v_T}{UL} = C^\mu \frac{k^2}{\varepsilon}$$

In order to close the system of equations we need equations for k and ε .

The transport equations for the turbulent kinetic energy, k , and the turbulent dissipation function, ε , were originally reported by Launder and Spalding (1974). They are, in dimensionless form:

$$\begin{aligned} \frac{\partial k}{\partial t} + \bar{u}_i \frac{\partial k}{\partial x_i} &= \frac{\partial}{\partial x_i} \left[\left(\frac{\sigma_k - 1}{\sigma_k} \frac{1}{\mathcal{R}} + \frac{1}{\sigma_k \mathcal{R}_c} \right) \frac{\partial k}{\partial x_i} \right] - \varepsilon \\ &+ \left(\frac{1}{\mathcal{R}_c} - \frac{1}{\mathcal{R}} \right) \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) \frac{\partial \bar{u}_i}{\partial x_j}, \end{aligned} \quad (9)$$

and

$$\begin{aligned} \frac{\partial \varepsilon}{\partial t} + \bar{u}_i \frac{\partial \varepsilon}{\partial x_i} &= \frac{\partial}{\partial x_i} \left[\left(\frac{\sigma_\varepsilon - 1}{\sigma_\varepsilon} \frac{1}{\mathcal{R}} + \frac{1}{\sigma_\varepsilon \mathcal{R}_c} \right) \frac{\partial \varepsilon}{\partial x_i} \right] - C^{\varepsilon_1} \frac{\varepsilon^2}{k} \\ &+ C^{\varepsilon_2} \left(\frac{1}{\mathcal{R}_c} - \frac{1}{\mathcal{R}} \right) \frac{\varepsilon}{k} \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) \frac{\partial \bar{u}_i}{\partial x_j}, \end{aligned} \quad (10)$$

where the constants are as follows:

$$C^\mu = 0.09, \quad C^{\varepsilon_1} = 1.45, \quad C^{\varepsilon_2} = 1.90, \quad \sigma_k = 1.0, \quad \sigma_\varepsilon = 1.5.$$

These constants are *not* meant to be changed; they are assumed to be universal. This completes the mathematical statement of the flow field equations for the 'standard' $k - \varepsilon$ model. Equations (7), (8), (9) and (10) are a set of 6 equations in 6 unknowns, viz, the three components of velocity, $(\bar{u}, \bar{v}, \bar{w})$, the pressure, \bar{P} , the turbulent kinetic energy, k , and the turbulence dissipation, ε .

Since near-wall flows are not appropriately modeled with this formulation, a wall-function boundary condition or other near-wall treatment must be applied. In the near-wall region the boundary conditions may be imposed in the logarithmic layer of the near-wall boundary layer

by invoking the universal law-of-the-wall. Using this logarithmic law and the assumption of local equilibrium, equations that provide the necessary boundary values for k and ϵ have been developed. Modifications to this approach have also been reported in the literature to extend the near-wall model in conjunction with extending the $k - \epsilon$ model to handle complex flows.

If the two-equation model just described does not predict a particular flow field correctly, then the flow field most likely violates the assumptions made in the derivation of the model. Again, we must keep in mind that this model is not expected to work in highly curved flows, in near wall flows among other complex flows. There are a wealth of proposed modifications that are reported in the engineering literature from which to choose an appropriate modification of this two-equation model when it is required. It is up to the user to select the appropriate turbulence model.

BALDWIN-LOMAX ALGEBRAIC MODEL

The Baldwin-Lomax model has been used extensively since its introduction because of its computational efficiency and accuracy; see Baldwin and Lomax (1978). This model was patterned after the model developed by Cebeci et al (1977). This and four similar models were applied and compared by Gee et al (1990) to investigate the flow about a prolate spheroid at high angle of attack. For bodies that are at high angles of attack (27 to 30 degrees) the Baldwin-Lomax model requires modification. For flows of practical interest to the marine hydrodynamicist at or near design points in which flow separation is not expected to occur, this model is useful. In fact, the recent experience of C.I. Yang (1991)¹ with this model on problems of interest to the marine propulsor designer is encouraging. The turbulence model equations for the Baldwin-Lomax formulation are presented next.

This model is also an eddy viscosity model that assumes an effective kinematic viscosity, i.e.,

$$\nu_e = \nu + \nu_T.$$

The turbulent flow is assumed to be divided into an inner and outer region with a different set of equations used in each region to determine the turbulent eddy viscosity, ν_T . The value of ν_T is defined as follows:

¹ Personal communication.

$$v_T = \min \left[(v_T)_{\text{inner}}, (v_T)_{\text{outer}} \right]. \quad (11)$$

In the inner region the Prandtl-Van Driest formulation is used to determine v_T . This formula is

$$(v_T)_{\text{inner}} = l^2 \Omega,$$

where

$$l = ky \left[1.0 - e^{-(y^*/A^*)} \right],$$

$$y^* = \frac{u_* y}{v_*} = \frac{(\tau_w / \rho)^{1/2} y}{v_*}$$

and

$$\Omega = \left[\left(\frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} \right)^2 + \left(\frac{\partial v}{\partial z} - \frac{\partial w}{\partial y} \right)^2 + \left(\frac{\partial w}{\partial x} - \frac{\partial u}{\partial z} \right)^2 \right]^{1/2},$$

the latter of which is the magnitude of the local vorticity.

In the outer region, for attached boundary-layers, the turbulent viscosity is given by

$$(v_T)_{\text{outer}} = KC_{cp} F_{\text{wake}} F_{\text{Kleb}}(y)$$

where

$$F_{\text{wake}} = \min \left[(y_{\text{max}} F_{\text{max}}), (C_{wk} y_{\text{max}} u_{\text{dif}}^2) \right],$$

in which u_{dif} is the difference between the maximum and minimum total velocity in the local profile, i.e.,

$$u_{\text{dif}} = \left(\sqrt{u^2 + v^2 + w^2} \right)_{\text{max}} - \left(\sqrt{u^2 + v^2 + w^2} \right)_{\text{min}}$$

and

$$F_{Klcb}(y) = \left[1.0 + 5.5 \left(\frac{C_{Klcb} y}{y_{max}} \right)^6 \right]^{-1}$$

F_{max} is defined as the maximum value of the function,

$$F(y) = y\Omega \left[1.0 - e^{-(y^*/A^*)} \right]$$

for each streamwise location along the wall at y_{max} , which is the normal distance from the surface at which this maximum occurs.

The constants in the model (which are assumed to be universal) are as follows:

$$A^* = 26, \quad k = 0.4, \quad C_{cp} = 1.6,$$

$$K = 0.0168, \quad C_{Klcb} = 0.3, \quad C_{wk} = 0.25.$$

This completes the mathematical statement of the Baldwin-Lomax algebraic turbulence model. The model provides a method to compute the turbulent viscosity, ν_T and, hence,

$$\frac{1}{\mathcal{R}_c} = \frac{\nu + \nu_T}{UL}$$

which is the only other unknown in the eddy viscosity version of the RANS equations. Hence, Equations (7), (8) and (11) are a set of five equations in five unknowns, viz, the three components of velocity, $(\bar{u}, \bar{v}, \bar{w},)$ the pressure, \bar{P} , and the eddy viscosity, ν_T .

COMPUTATIONAL METHODS

The boundary-value problems described in the previous section cannot in general be solved by analytical methods. If we are interested in solving these equations we must resort to approximate, computational methods that may be implemented on a digital computer. One class of computer methods is finite difference methods. (There are several other well-known classes of computational methods, viz., finite-element methods, spectral methods, and equivalent-vortex

methods.) A relatively large class of finite difference methods fall into the category of finite volume, finite difference methods. The derivation of a finite volume scheme assumes that the flow domain is discretized into small control volumes within which integral forms of the the model equations are satisfied. The approximations associated with the application of computational methods may be illustrated by a derivation of one-dimensional methods. Such a derivation is presented to illustrate the assumptions required to develop a computational method.

A two-dimensional finite difference method is subsequently presented that is a generalization of the one-dimensional method described. The two-dimensional method is presented to illustrate the problems associated with going to higher dimensions.

DERIVATION OF FDM

The transport equations of the turbulence models, viz, Equations (6), (9) and (10), have the following structure (in component form):

$$\frac{\partial f}{\partial t} + u_i \frac{\partial f}{\partial x_i} = \frac{\partial}{\partial x_i} \left(D \frac{\partial f}{\partial x_i} \right) + S, \quad (12)$$

or (in the Gibbs vector notation form):

$$\frac{\partial f}{\partial t} + \mathbf{u} \cdot \nabla = \nabla \cdot (D \nabla f) + S, \quad (13)$$

where $f = u, v, w, k, \text{ or } \epsilon$. Utilizing the continuity equation, $\nabla \cdot \mathbf{u} = 0$, we may write (13) in the following, so-called conservative or divergence form:

$$\frac{\partial f}{\partial t} + \nabla \cdot (\mathbf{u}f) = \nabla \cdot (D \nabla f) + S, \quad (14)$$

To solve a differential equation of the form (14) we must, of course, integrate. This is done next by a finite difference method.

Consider the elemental control volume illustrated in Fig. 2. This control volume is assumed to be a discrete subdomain of the flow field of interest. Integrating Equation (14) over this arbitrarily selected control volume, $C.V.$, we obtain:

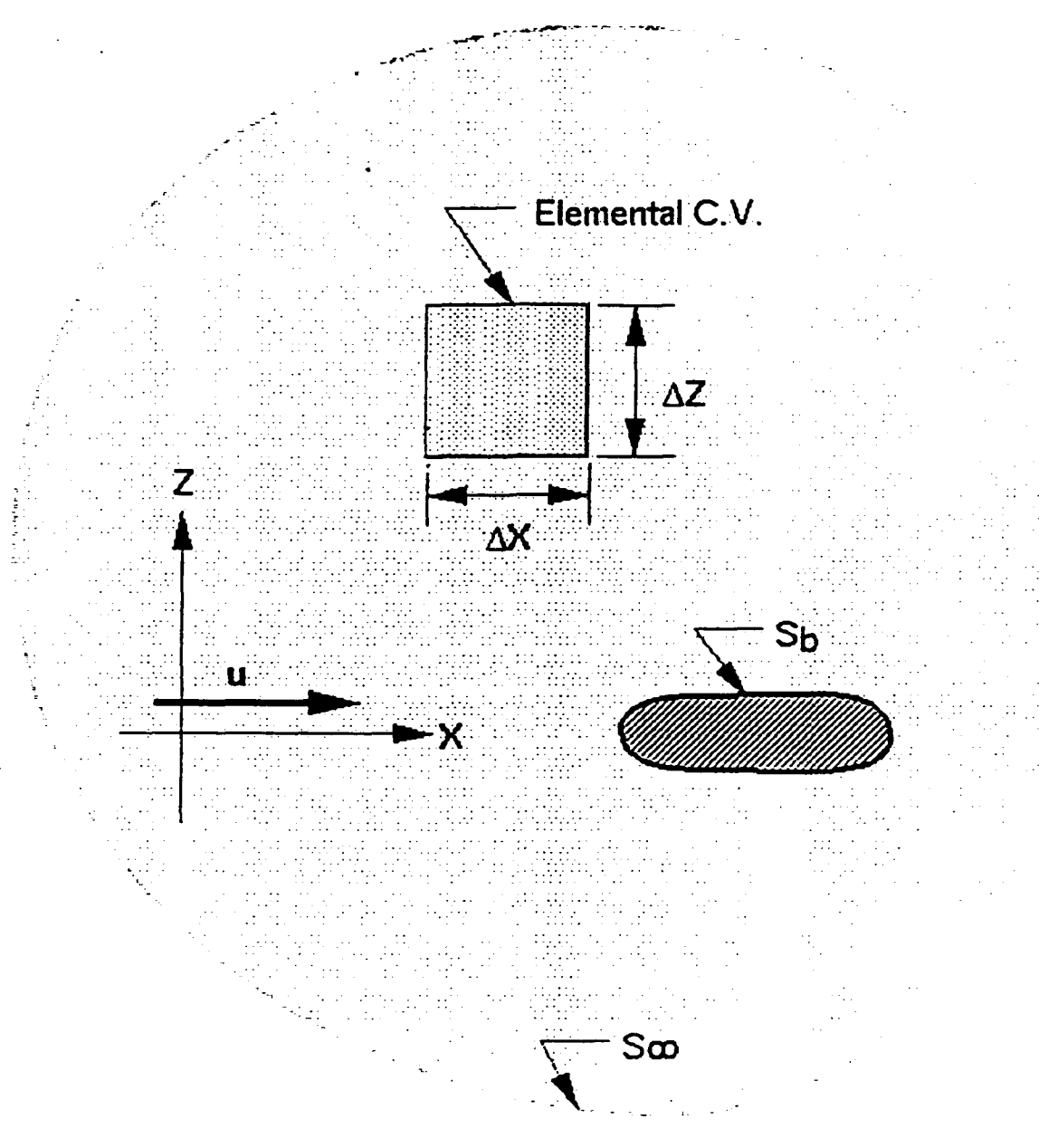


Fig. 2. Illustration of an elemental control volume for two-dimensional problems.

$$\iiint_{C.V.} \frac{\partial f}{\partial t} dV = \iiint_{C.V.} [-\nabla \cdot (uf) + \nabla \cdot (D\nabla f) + S] dV. \quad (15)$$

Equation (15) is the form of the transport equation from which the finite difference method is derived.

Let us consider the one-dimensional problem illustrated in Fig.3. In this case we assume that $\mathbf{u} = u \mathbf{i}$, $f = f(x,t)$ and $S = S(x,t)$. In this case, after applying the theorem of Leibnitz, Equation (15) reduces to

$$\frac{d}{dt} \iiint_{C.V.} f dV = \iiint_{C.V.} \left[-\frac{\partial(uf)}{\partial x} + \frac{\partial}{\partial x} \left(D \frac{\partial f}{\partial x} \right) + S \right] dV, \quad (16)$$

in which $dV = dx dy dz$. Next, we integrate over unit distances in the y and z directions, and in the x direction from $x_i - \Delta x/2$ to $x_i + \Delta x/2$. Integrating, we get

$$\frac{d}{dt} \int_{x_i - \Delta x/2}^{x_i + \Delta x/2} f dx + (uf)_R - (uf)_L = \int_{x_i - \Delta x/2}^{x_i + \Delta x/2} \left[\frac{\partial}{\partial x} \left(D \frac{\partial f}{\partial x} \right) + S \right] dx. \quad (17)$$

Finally, we may write Equation (17) as follows:

$$\frac{d\bar{f}}{dt} = -\frac{(uf)_R - (uf)_L}{\Delta x} + \frac{1}{\Delta x} \left[\left(D \frac{\partial f}{\partial x} \right)_R - \left(D \frac{\partial f}{\partial x} \right)_L \right] + \bar{S} \equiv F(t), \quad (18)$$

where \bar{f} and \bar{S} are the spatial averages of f and S , respectively, over the control volume, $C.V.$

The functions f_R, f_L , and their derivatives are the instantaneous values of f and its derivative on the right, R , and left, L , faces of the surface of the control volume. Integrating (14) from t to $t+\Delta t$, we obtain

$$\bar{f}^{n+1} - \bar{f}^n = \int_t^{t+\Delta t} F(t) dt, \quad (19)$$

where the superscript $n+1$ identifies the value of the function at time $t+\Delta t$ and the superscript n identifies the value of the function at time t . The Euler-explicit or forward-time approximation to this integral is

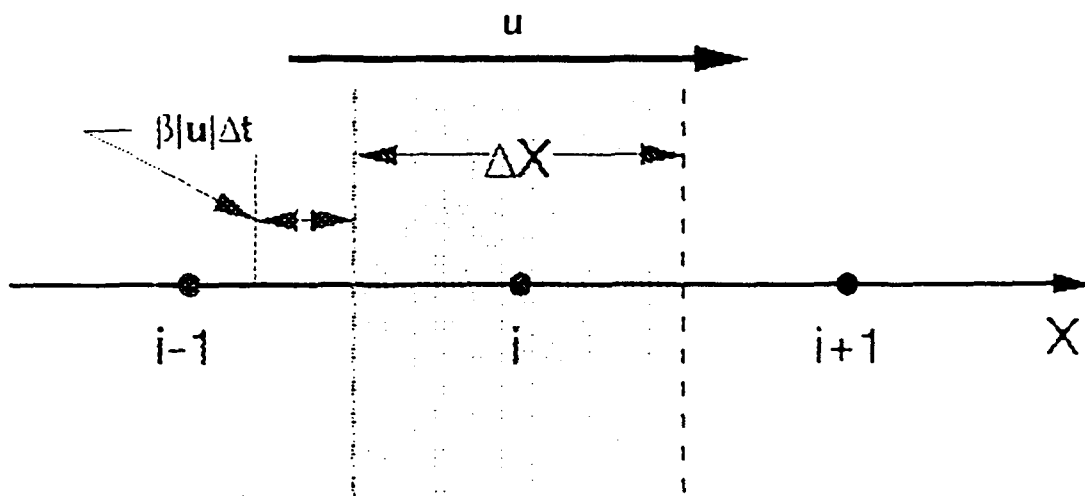


Fig. 3. One-dimensional finite-difference grid structure.

$$\bar{f}^{n+1} - \bar{f}^n = \bar{F} \Delta t, \quad (20)$$

where \bar{F} is a suitable average of the right-hand-side of Equation (18) over the time interval Δt . In the classical Euler-explicit method it is assumed to be constant over the interval Δt and equal to its initial value, i.e., $\bar{F}^n = F^n$. (This is the first approximation made in this derivation. Other schemes could have been applied, e.g., the trapezoidal rule of numerical integration or one of a number of Runge-Kutta schemes.)

The problem now is to find a suitable expression for \bar{F}^n and \bar{f} . The latter is assumed to be the value of f at the center of the control volume, i.e., $\bar{f}^n = \bar{f}_i^n$ and $\bar{f}^{n+1} = \bar{f}_i^{n+1}$, where the subscript, i , in the computational scheme refers to the center of the i th control volume.

Substituting (18) into (19) and integrating according to (20), we get

$$\bar{f}^{n+1} - \bar{f}_i^n = \frac{\Delta t}{\Delta x} [(\bar{u}f)_R - (\bar{u}f)_L] + \frac{1}{\Delta x} \left[\left(D \frac{\partial \bar{f}}{\partial x} \right)_R - \left(D \frac{\partial \bar{f}}{\partial x} \right)_L \right] + \bar{S}_i^n \Delta t. \quad (21)$$

In the one-dimensional problem illustrated in Fig. 3, the velocity u and the diffusion coefficient D are assumed to be constant. (This is the second approximation made in this derivation, i.e., we assumed that the local velocity and the local 'eddy' diffusion coefficient are approximately constant in the vicinity of the i th grid or cell.) In this case we may write

$$\bar{f}_i^{n+1} - \bar{f}_i^n = \frac{u\Delta t}{\Delta x} [\bar{f}_R - \bar{f}_L] + \frac{D\Delta t}{\Delta x} \left(\frac{\partial \bar{f}}{\partial x} \Big|_R - \frac{\partial \bar{f}}{\partial x} \Big|_L \right) + \bar{S}_i^n \Delta t. \quad (22)$$

Over the time interval Δt , f is physically transported from a point $u\Delta t$ upstream of the cell (or control volume) to the cell face as illustrated in Fig. 3. The quantity $u\Delta t$ times a unit width times a unit height represents the volume of fluid transported through a cell face over the time interval Δt . A suitable average value of f for this volume of fluid, which is transported across a cell face in the time interval Δt , is assumed to be the value of f at time t at a distance $\beta u\Delta t$ upstream (or upwind) of the face of the cell (or control volume) within the volume $u\Delta t$, i.e., $0 \leq \beta \leq 1$. Thus, for $u \geq 0$ and using linear interpolation, we may write

$$\bar{f}_i = \left(\frac{1}{2} - \frac{\beta u \Delta t}{\Delta x} \right) f_i + \left(\frac{1}{2} + \frac{\beta u \Delta t}{\Delta x} \right) f_{i-1}.$$

or

$$\bar{f}_L = \left(\frac{1}{2} - \beta C\right) f_{i+1} + \left(\frac{1}{2} + \beta C\right) f_i$$

(This is the third approximation, i.e., a linear interpolation function was selected to estimate the upwind value of f .) Similarly,

$$\bar{f}_R = \left(\frac{1}{2} - \beta C\right) f_{i+1} + \left(\frac{1}{2} + \beta C\right) f_i$$

Thus,

$$\bar{f}_R - \bar{f}_L = \left(\frac{1}{2} - \beta C\right) f_{i+1} + 2\beta C f_i - \left(\frac{1}{2} + \beta C\right) f_{i-1} \quad (23)$$

Substituting Equation (23) into (22) and applying second-order central differences to the $\partial/\partial x$ terms in (22), we get the finite difference analog of the transport equation, Equation (14), viz:

$$f_i^{n+1} = (1 - 2\beta C^2 - 2r) f_i^n + \left(\beta C^2 + \frac{C}{2} + r\right) f_{i-1}^n + \left(\beta C^2 - \frac{C}{2} + r\right) f_{i+1}^n + \bar{S}_i^n \Delta t, \quad (24)$$

where the choice of β distinguishes between various schemes. This class of Euler-explicit β schemes was investigated by Valentine (1987,1988). The parameter $C = u\Delta t / \Delta x$ is the Courant number. The parameter $r = D\Delta t / (\Delta x)^2 = C / \mathcal{R}_{\Delta x}$ is the Courant number divided by the cell Reynolds number. The cell Reynolds number is $\mathcal{R}_{\Delta x} = u\Delta x / D$, where D is the local diffusion or effective viscosity coefficient. The local Courant number and the local cell Reynolds number play an important role in determining the stability of the computational method.

Equation (24), by virtue of the parameter β , contains a number of well known finite difference schemes. If $r = 0$, $C = 0$, and $S = 0$, $f_i^{n+1} = f_i^{n+1}$, which means there is no motion and no internal sources of f . If $C \rightarrow 0$, $C^2 \ll C$, then for $\beta = 0.5$, this scheme reduces to the forward-time centered-space difference scheme. Other relatively well known schemes that are embodied in this equation are as follows. If $\beta = 1/(2C)$, then the advection (or convection) term reduces to the second upwind (or donor-cell) advection scheme. If $\beta = 1/2$ and $\mathcal{R}_{\Delta x} \rightarrow \infty$, which means $r \rightarrow 0$, the scheme is the Lax-Wendroff scheme. If $\beta = 1/2$, for $C = 1$ the equation is pure

upwind and exact for pure advection (no diffusion, i.e., $r = 0$, and no internal sources, i.e., $S = 0$). If $C \rightarrow 0$ the scheme approaches the second-order centered difference scheme. Finally, if $\beta = \alpha/(2C)$, where $0 < \alpha < 1$ is a weighting parameter, the scheme reduces to the weighted-upwind scheme. The special cases cited above of the scheme given by Equation (24) are in the textbook by Roache (1972) on computational fluid dynamics. Other variations of the Euler-explicit β scheme are reported by Valentine (1988).

To examine the problems associated with selecting and implementing a computational method it is instructive to study the modified equation that corresponds to the difference equation, Equation (24). If we nondimensionalize (24) in terms of the local characteristic scales, i.e.,

$$x^* = \frac{x}{\Delta x}, \quad t^* = \frac{t}{\Delta t},$$

and let

$$s = \frac{f - f_r}{f_o - f_r},$$

we may write the modified equation for the scheme given by Equation (24) as follows:

$$\begin{aligned} \frac{\partial s}{\partial t} + C \frac{\partial s}{\partial x} - r \frac{\partial^2 s}{\partial x^2} - S^* = C^2 \left(\beta - \frac{1}{2} \right) \frac{\partial^2 s}{\partial x^{*2}} + C \left[r + \frac{C^2 - 1}{6} \right] \frac{\partial^3 s}{\partial x^{*3}} \\ + \left[\frac{C^2}{12} \left(\beta - \frac{C^2}{2} \right) + \frac{r}{2} \left(\frac{1}{6} - r - C^2 \right) \right] \frac{\partial^4 s}{\partial x^{*4}} + \dots, \end{aligned} \quad (25)$$

where the terms on the right-hand-side are the truncated terms (or *truncation error*) of the scheme explicitly exposed. This equation is derived by substituting the Taylor series approximations of the terms not in the center of the i th cell and not at time t in terms of the value of s and its derivatives at time t and at the center of the i th cell, viz, in terms of $s = s_i^n$. The truncation error shows that Equation (24) is a first-order upwind scheme if $\beta \neq 1/2$; if $\beta = 1/2$, then the scheme is a second-order scheme.

The second derivative truncation error produces numerical (or false) diffusion that is analogous to physical diffusion. The third derivative truncation error produces wave-like behavior or 'wiggles' in the solution near steep gradients, i.e., at locations in the flow field where s changes nearly discontinuously so that $\partial^3 s / \partial x^{*3}$ is relatively large. This error is an error of inconsistency of

the difference scheme in that it actually approximates an equation with a third derivative term by virtue of the truncation error instead of the original differential equation for which the right-hand-side of (25) is identically zero. Fine mesh or more grid points where gradients of s are large will tend to suppress the wiggles because the third derivative of s will be reduced. It is reduced when the mesh is refined because s is a continuous function. The modified equation was nondimensionalized in terms of the grid size deliberately to illustrate this computational problem. Hence, *a fine mesh is required in regions of the flow where s is expected to have large gradients.*

The selection of grid size, Δx , in conjunction with the selection of the time step, Δt (which may be viewed as the selection of the iteration step for problems in which the steady solution is sought), is not completely arbitrary. The Courant number is proportional to $\Delta t/\Delta x$ and the cell Reynolds number is proportional to Δx ; hence, they are measures of the time step and the grid size. It can be shown from heuristic and von Neumann stability considerations that the following restriction is imposed on the selection of these parameters:

$$C \leq \frac{\mathcal{R}_{\Delta x}}{2(1 + \beta C \mathcal{R}_{\Delta x})}. \quad (26)$$

For the case in which $\mathcal{R}_{\Delta x} \rightarrow \infty$, this restriction on C reduces to

$$C^2 \leq \frac{1}{2\beta}. \quad (27)$$

If $\beta = 1/2$, then Equation (27) reduces to the well known CFL (or Courant-Friedrichs-Lewy) condition.

Within the framework of the last three equations, let us examine the effects of increasing grid resolution. If $\Delta x \rightarrow$ small, then $\mathcal{R}_{\Delta x} \rightarrow$ small. Because $C \leq \mathcal{R}_{\Delta x}/2$ (approximately) from Equation (26), $r \approx 1/2$. Hence, for small grid size or high resolution of rapidly varying values of s the local or cell Reynolds number is small which leads to a relatively large coefficient, r , of the diffusion term and a relatively small value of C . This means that locally physical diffusion will smooth the solution at the expense of smaller time steps (or iteration steps). Of course, this is not unexpected; if more accuracy is required, then the computational effort required must increase. For small values of Δx , the value of C is reduced and, hence Δt is reduced. This shows that a greater number of equations over a greater number of time steps are required to reach a steady solution.

There have been a number of successful extensions to the second-order scheme just described that reduces the problems associated with the truncation error for relatively coarse grids. The schemes go by the names flux-corrected transport (or FCT) and total variation diminishing (or TVD) schemes. These refinements are designed to modify first- and second-order schemes to suppress the problems that are associated with the second and third derivative truncation errors particularly in the vicinity of step gradients of s . In the preliminary stages of a computational investigation it may be useful to use the lower-order schemes with greater numerical damping when the grid selection and debugging process is underway. If large gradients in s are anticipated from the results of preliminary investigations and/or experience, then finer grid structures in these regions along with the implementation of an FCT or TVD scheme would be useful. For practical purposes, these refinements should be sufficient to handle most of the practical problems confronted by the marine propulsor designer today. (In addition, before more complex models and computational methods are used, experience with the set of tools described in this report would be useful and, at least, an important first step in the implementation of CFD-RANS codes in hydrodynamic design.)

TWO-DIMENSIONAL COMPUTATIONAL METHODS

Many two- and three-dimensional methods implement one-dimensional methods, that are similar to the method just described, in each of the coordinate directions with the assumption that the local flow field is nearly perpendicular to one of the grid faces. The experience reported in the literature indicates that even if the flow is not necessarily perpendicular to one of the finite difference cell faces the methods as constructed this way still provide reasonable approximations of the solutions sought. The primary purpose of this section is to present a logical extension of the one-dimensional method to illustrate the increase in complexity associated with coding multidimensional methods. The extension presented is the simplest two-dimensional method for which a rectangular mesh is assumed. As one can easily imagine, even without computational fluid dynamics experience, the algebra involved in deriving nonrectangular grid approximations would indeed be more complex particularly if the same order accuracy is to be maintained.

Let us consider the two-dimensional flow problem illustrated in Fig. 2. The characteristic length, L , and the characteristic velocity, U , are identified in the figure. The two-dimensional version of the model transport equation for f is

$$\frac{\partial f}{\partial t} + \frac{\partial uf}{\partial x} + \frac{\partial wf}{\partial z} = \frac{\partial}{\partial x} \left(D \frac{\partial f}{\partial x} \right) + \frac{\partial}{\partial x} \left(D \frac{\partial f}{\partial z} \right) + S. \quad (28)$$

The two-dimensional extension of Equation (24) as applied to (28) is as follows:

$$f_{i,j}^{n+1} = f_{i,j}^n + \frac{\Delta t}{h} \left[u_R \bar{f}_R - u_L \bar{f}_L + w_T \bar{f}_T - w_B \bar{f}_B \right] + \frac{D_{i,j}^n \Delta t}{h^2} \left[f_{i+1,j}^n + f_{i-1,j}^n + f_{i,j+1}^n - 4f_{i,j}^n \right] + \bar{S}_{i,j}^n. \quad (29)$$

The finite difference cell for this formulation is illustrated in Fig. 4. The grid, for illustration purposes, is assumed square, i.e., $\Delta x = \Delta z = h$. The local diffusion coefficient is assumed to be constant (or slowly varying locally). Note that $D_{i,j}^n$ is the local value of D . Three methods to estimate \bar{f}_R , \bar{f}_L , \bar{f}_T , and \bar{f}_B are described next. They are identified by the numbers 1, 2 and 3 in Fig. 5. They are called: (1) Second-upwind. (2) Skew-upwind. (3) Euler-explicit β scheme (with $\beta = 1/2$). The parameter $|u|$ is the magnitude of the velocity vector in the direction of the arrow in the figure. Case 1 is an extension of the donor-cell method to two-dimensional problems; it is described in the book by Roache (1972). The proper extension of the one-dimensional donor-cell method is Case 2, or the skewed-upwind scheme (as it has been called in the literature). It requires, in addition to the same numerical operations in the x and z directions as Case 1, the linear interpolation of f between the grid points $(i-1, j)$ and $(i-1, j-1)$ for the example illustrated in the figure. The method of Case 3 requires bilinear interpolation between these points and points (i, j) and $(i, j-1)$. Case 3 is the proper two-dimensional extension of the one-dimensional β scheme. The important point to note here is that the proper extensions require additional computations; hence, they require more than a proportional increase in computational effort as compared to their one-dimensional counterparts. The method typically used to extend one-dimensional methods is analogous to Case 1. The modifications that improve the numerical performance of the second-upwind scheme that goes by the names FCT and TVD are invariably applied along the direction of the grid lines. Hence, there is an implicit assumption made by this procedure, viz, the flow is in the direction of the vertical or horizontal grid lines. In fact, nonuniform grid methods are usually designed with this assumption applied. This assumption is important because it reduces the computational effort required; without this assumption the computational effort is indeed increased as was illustrated by Cases 2 and 3.

The stability criteria for multidimensional schemes are known to be more restrictive than for one-dimensional schemes; see, for example, Hirt (1968) or Roache (1972). The fact that the selection of grid size and time-step size is restricted by numerical stability considerations in addition to accuracy requirements is important. If a selection is made that exceeds the stability

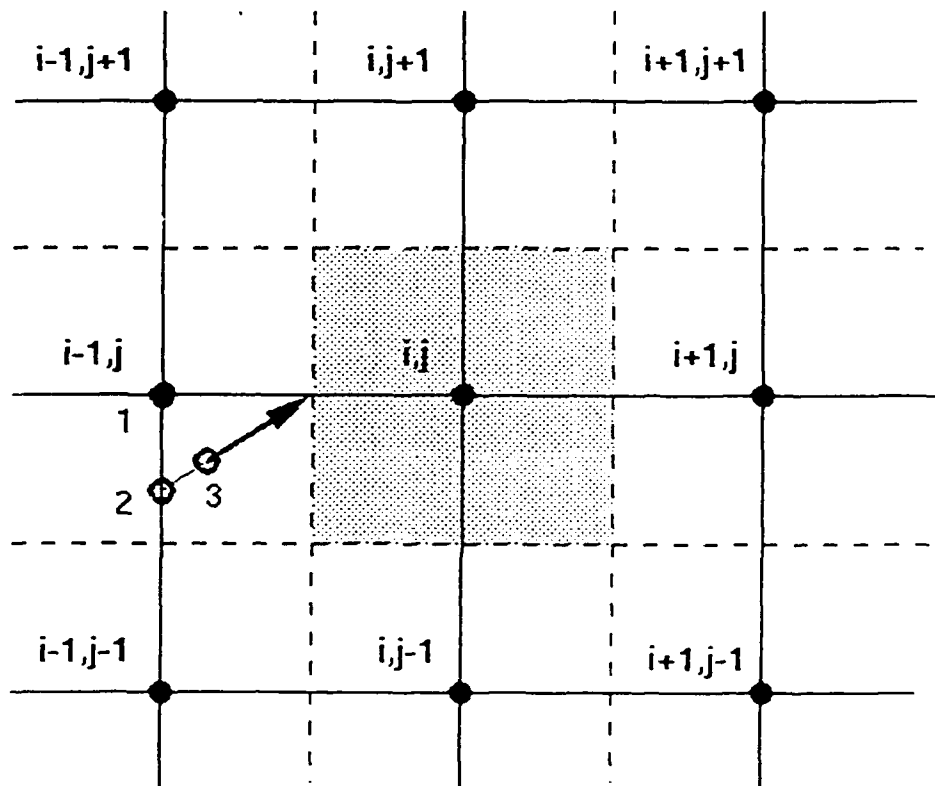


Fig. 4. Two-dimensional finite-difference grid structure.

bounds, the solution blows up rapidly; hence, precise knowledge of the stability bounds is not particularly important. In addition, accuracy requirements tend to demand much finer meshes as compared to the stability restrictions. Finally, the effects of the nonlinearities in the original differential equation prevent an exact assessment of the stability bounds of the nonlinear algebraic system of equations. Fortunately, the wealth of experience in applying a variety of computational fluid dynamics methods to multidimensional problems that have been reported in the literature illustrates that these issues are not the main problems in implementing computational methods. The primary concerns are to ensure accuracy by comparing solutions to known solutions, comparing solutions with solutions found using different methods and comparing solutions with experimental data. The principal objectives of a computational study are: (1) to demonstrate that the computational method produces reasonable approximations of the model equations; (2) to demonstrate that the turbulence model is the appropriate model for the kind of flow problem to be solved; (3) to provide a computational solution of the problem posed to help make engineering decisions about hydrodynamic devices.

We cannot expect that all fluids engineers with a need for turbulent flow approximations be experts in the development and implementation of computational turbulence models. However, we can expect the fluids engineer, because of his or her academic background, to use existing tools successfully. The application of the relatively crude RANS tools by the engineering community has and will continue to help the research community in their quest to modify the methods to more suitably handle particular classes of flows. In the area of the design of marine propulsors there is a need to determine the usefulness of existing turbulence models. What computational tools or computer programs are available to the marine propulsor engineer? This question is considered in the next section.

RANS CODES

The codes described in this section fall into two categories. The first set are "user friendly" in the sense that the author of the code does not have to be directly involved in its implementation. Such a code is DTNS3D which has an accompanying grid generation code that can be used to help grid the flow domain to be analyzed. This code has been used successfully to solve flows of interest to the marine hydrodynamicist; see Gorski, Coleman and Haussling (1990). Other commercially available codes in the user friendly category may be found in numerous advertisements in, for example, any issue of *Mechanical Engineering* (1990).

The second set of codes requires the direct involvement of their original authors. These codes are "research" codes that have been developed to investigate the capabilities of a particular

computational method and a particular turbulence model in the solution of problems of interest to the marine hydrodynamicist. Three examples that have been used at CDNSWC are the Yang code, the Sung code and the Iowa code. The second set of codes has been successfully used to investigate fairly complex flows of interest to the marine hydrodynamicist; see Yang (1990), Sung and Yang (1988) and Chen and Patel (1985). However, in order to implement them, the originators must prepare the input data and run them. The latter set may be used in some of the initial applications of the former set to provide confidence in the user oriented codes. It is with this in mind that the advantages and disadvantages of each tool are discussed below.

The DTNS3D code is available at CDNSWC to solve the RANS equations for incompressible turbulent flows. It utilizes a finite difference method based on a finite volume derivation such that the computational domain is discretized into a finite number of small rectangular volumes. It is a multiblock code that allows the user to break up an arbitrarily shaped flow domain into a number of separately gridded zones. This may have an advantage in attempting to optimize grid structure. To help generate the computational grid, the program NUGGET is available. The documentation for the flow code and the grid generation code is crude; however, since it exists, it is an advantage. Also, the original authors are at CDNSWC to help in instructing the users in its application. The user selects a computational method from a set of five, the highest order of which is a third-order upwind difference TVD scheme applied to the convection terms and a second-order central difference scheme applied to the diffusion terms. The time marching scheme is a Runge-Kutta scheme which may be viewed as the iteration scheme applied for time-averaged flow solutions. Several numerical approximations of the boundary conditions are at the users' disposal which is an advantage in the debugging process inherent in selecting the correct grid for a given problem. The two turbulence models described in this report are also coded in DTNS3D.

Two-dimensional (DTNS2D) and axisymmetric (DTNSA) versions of this code are available for execution on CDNSWC workstations. Because of the tremendous increase in computational effort required in going from a 2D or axisymmetric problem to a full 3D problem, the computer required changed. A superminicomputer, such as is available in the CDNSWD Hydrodynamics/Hydroacoustics Technology Center, is a minimum requirement. Using supercomputers like the Cray-XMP or the Cray-YMP becomes essential when full 3D flows around arbitrarily shaped boundaries is required. Grids with over 10^6 grid points are not unrealistic. This is because of the large number of grid points required to resolve the flows within the boundary-layers. The CPU time required to compute complex 3D RANS solutions will be of the order of hours on Cray computers. These tools are *not* production run tools like the lifting line

and simple streamline curvature methods that are currently used in the preliminary design of marine propulsors. They are not even production tools like the lifting surface potential-flow codes used by marine propulsor designers which can be run on workstations within a CPU hour for complex 3D flows.

The tools developed by Yang, Sung, and Chen and Patel are discussed next. These codes are not designed for use by others. They are tools that require the direct involvement of the authors of the codes. From the research and engineering experiences gained with these tools and, in particular, the experience on marine propulsor problems due to Yang (1990), the potential usefulness of codes that solve the turbulence model equations for making design decisions has been demonstrated (to some extent). This work in conjunction with the experience gained in using codes like DTNS3D should provide the encouragement required for the marine propulsor community to take a more active part in exercising these tools. This is a new area of engineering application in the design process of marine propulsors. There is sufficient knowledge about the limitations of the model equations that our expectations in what the results can provide should not be overzealously stated. However, there is sufficient experience to indicate that these methods can be helpful and, hence, useful in analyzing the capabilities of designs.

PROPULSOR MODELING

There are two problems that arise in the design of marine propulsors that are unique to the analysis of turbomachinery. They are the analysis of the flow through rotating (impeller) and stationary (stator) blades, and the interaction between the flow induced by the blades and the flow past the solid boundaries adjacent to them. The latter problem is the first problem for which RANS codes would be useful in the analysis of marine propulsor designs. The design of blading systems that produce acceptable distributions of forces is relatively well established within the framework of lifting-surface theory and streamline-curvature methods. The RANS codes provide a useful set of tools in the investigation of the propulsor/hull interaction problem particularly when the determination of flow separation and/or excessive secondary flows are required in a design evaluation to ensure that these flow problems are avoided. Recent experience on this problem has been reported by Dai, Gorski and Haussling (1991). They compared turbulence model predictions with experimental data for the flow field produced by an integrated ducted propulsor propelling a fine stern axisymmetric body. Their predictions were made using DTNSA, the axisymmetric version of DTNS3D. Their predictions of the time-averaged pressure and velocity fields compared favorably with the data; thus, they provide a verification of the procedure for analyzing the interaction between propulsor and vehicle. The two turbulence

models presented in this report were used by Dai et al. Because the axisymmetric body they examined had a fine stern, it was encouraging to see that the predictions based on the two turbulence models were essentially the same.

In their investigation, Dai et al. modeled the blades of the ducted propulsor with an "actuator disk." This model is an important element that must be included in RANS codes designed to investigate flows around marine propulsors. The actuator disk model for a system of blades (rotors and stators) is described next.

The impeller applies thrust and torque forces to the fluid at the location of the blades. The thrust produced by the propulsor must of course balance the resistance of the vehicle it is designed to propel. To model the effect of the time-averaged values of the forces applied by the propulsor, it is assumed that the radial distribution and the integral value of these forces are known. The radial distribution can be estimated from the procedure given by Pelletier and Schetz (1986) or it can be predicted by lifting surface theory as was done by Dai et al. (1991). The total thrust is a given requirement at the design point. The importance of meeting the self-propulsion operating condition at the design point goes without saying; however, if the RANS code is used to predict the effective inflow into the propulsor's blade rows, then an iterative procedure is required between the RANS code calculations of the effective inflow and the lifting surface method predictions of the forces acting on and the velocity field induced by the blading system on the total inflow. A major assumption in this procedure is that the induced velocity field due to the blading system singularities are accurately determined by the lifting surface, potential flow theory. This is important to note because it is this set of induced velocities that must be subtracted from the total velocity vectors computed with the RANS code to obtain a measure of the effective inflow just upstream of the blades. This effective flow (or "effective wake") is what the blade designer requires as input to the lifting surface analysis.

To illustrate the application of the actuator disk in RANS calculations, the model presented by Pelletier and Schetz (1988) will be described. Their model provides a useful model for preliminary design considerations of open propellers. Extension of the model for hub-and-tip loaded ducted rotors is straightforward. The incorporation of lifting surface design predictions into the model of the actuator disk is straightforward and can only be done when these results are available. The latter procedure has been successfully applied by Dai et al. (1991) and Yang et al. (1990).

Let us consider the model of the impeller or rotor blades next. (The same model can be used for the stator blades as well; hence, only the model for the rotor is presented here.) The rotor is modeled by a disk of radius equal to the radius of the rotor and a thickness Δx , roughly equal to

the physical thickness or axial extent of the blades. The thrust and torque are allowed to vary radially but are constant in the tangential direction. This model assumes that the integral values of thrust and torque acting on the blades are known from the design conditions imposed by the designer. For simplicity Pelletier and Schetz (1986) suggested the following radial distribution of thrust for open propellers:

$$\begin{aligned}
 T(r) &= 0 & r \text{ in } [0, r_1], \\
 T(r) &= T_M \frac{r - r_1}{r_2 - r_1} & r \text{ in } [r_1, r_2], \\
 T(r) &= T_M & r \text{ in } [r_3, R], \\
 T(r) &= T_M \frac{R - r}{R - r_3} & r \text{ in } [r_3, R], \\
 T(r) &= 0 & r > R,
 \end{aligned}$$

where T_M is the maximum value of the thrust and R is the radius of the rotor. Values of r_1 , r_2 , and r_3 were set in Pelletier and Schetz's calculations to $0.25R$, $0.7R$, and $0.85R$, respectively. This is a trapezoidal load distribution. For ducted propellers a uniform distribution may be desirable or some other distribution may be selected with finite hub and tip loading.

The trapezoidal distribution just described was also used by Pelletier and Schetz for the distribution of the force q that produces the swirl. The maximum value of q is denoted by q_M . The integration of these distributions leads to the following expressions for the net thrust and torque produced by the rotor (or actuator disk), i.e.,

$$T = 0.3075(2\pi R^2)T_M$$

$$Q = 0.2218(2\pi R^3)q_M$$

where T and Q are the thrust and torque, respectively. The integrated values are assumed to be given by the design conditions. It is from these equations that the values of T_M and q_M are determined. Then the trapezoidal load distribution equations are used to determine the radial distribution of the corresponding body force to be imposed in the computer code.

The corresponding body forces used in the finite volume, finite difference equations that are coded are obtained by dividing the thrusting and swirling forces by the thickness of the rotor disk. How are these body forces implemented in a RANS code? This issue is considered next.

The body forces are represented by additional terms in the RANS equations that are zero everywhere except within the actuator disk. The RANS equations, Equation (8), are recast as follows:

$$\frac{\partial \bar{u}_i}{\partial t} + \bar{u}_j \frac{\partial \bar{u}_i}{\partial x_j} = \frac{\partial \bar{P}}{\partial x_i} + \frac{\partial}{\partial x_j} \left[\frac{1}{R_e} \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) \right] + F_i, \quad (30)$$

where F_i is the "body force" that represents the vector components of the thrusting and swirling components of the body force, where

$$F_i = \frac{f}{\rho U^2 / L}$$

is the nondimensional form of the body force representation in which f_i is in units of force per unit volume. This force must be added to the source term $\bar{S}_{i,j}^n$ in the computational scheme; see, for example, Equation (29). It is added such that it is zero everywhere except within the volume occupied by the actuator disk.

This type of model has already been incorporated into DTNS3D; see, for example, Dai et al. (1991). Successful comparison of predictions with measurements was presented by Dai et al. (1991). The propeller model was also used in the Yang code; Yang et al. (1990)* reported results that are also quite encouraging. The predictions of the velocity field are very good. The predictions of the pressure field are reasonable. This experience provides a validation of the actuator disk model based on a body force representation of the blading system of propulsors.

SUMMARY

The Navier-Stokes (N-S) equations are the equations that describe the motion of water at speeds of practical interest to the marine propulsor engineer. At high Reynolds numbers, the flows of practical interest are turbulent, which means they are highly unsteady. Since it is well known that the N-S equations cannot be solved analytically or numerically for high Reynolds numbers, the engineer must consider solving the Reynolds-Averaged Navier-Stokes (RANS) equations with an appropriately selected turbulence model in order to predict time-averaged flow properties. If the effects of turbulence and the no-slip boundary conditions on flow field

* Also, Yang, C.-I., private communication (1991)

predictions are important, then a RANS solver is required. However, because the RANS solvers require turbulence model equations to close the system of equations, great care must be exercised in interpreting the numerical solutions.

One of the principal difficulties with RANS/turbulence model solvers (or RANS codes) is that they do *not* solve the N-S equations. They solve model equations that are at best a crude (yet useful) approximation of the N-S equations. Recall the additional assumptions about the flow physics that were made in the derivation of the RANS equations that are typically coded: for example, the introduction of the concept of an "eddy" viscosity, ν_T (this concept was originally developed by Taylor, Prandtl, and others). As pointed out in Tennekes and Lumley (1972), this concept is based on a superficial resemblance between the way molecular motions transfer momentum and the way turbulence velocity fluctuations transfer momentum. This concept was proposed as an expedient method to obtain engineering estimates of the time averaged flow properties of turbulent flows. Although the models are crude representations of the effects of turbulence on the time-averaged flow field, there is a large body of literature that presents relatively successful experience with the application of RANS codes to predict time-averaged flow field measurements. This experience provides the support for further investigations and applications of RANS codes in the analysis of designs and, in particular, marine propulsor designs.

If the necessary care is taken in selecting the grid to be used and finer grid calculations are planned to ensure that a reasonably accurate solution to the model equations is computed, then should we expect good comparison with experimental data? *Not necessarily!* If the predictions and experimental data compare favorably, then either the turbulence terms are relatively small or the flow field is part of the class of flows for which the original turbulence model was designed to handle. If they do not compare favorably, then a closer study of the flow field geometry should reveal the missing pieces that are not handled by the turbulence model used. The next step, of course, would be to select the appropriate turbulence model for the class of flows under consideration (if it indeed exists). Finally, it is the engineers' responsibility to determine at the outset of any computational investigation the RANS code to be used. If a qualitative assessment of the flows typically encountered in the design of marine propulsors is required, the RANS methods described in this paper should be useful. Actually, for the typical flows of interest to the marine propulsor designer, the methods discussed herein should provide results that are sufficiently accurate for engineering purposes. This is true primarily because the flows typically of interest to the marine propulsor designer are in the class of flows for which the models were developed.

Finally, there are three other issues that are important to the marine propulsor designer that may or may not require a RANS equations model to predict results of engineering significance. They are the calculation of flow through the actual blading system, the consideration of free-surface effects in the calculation, and the calculation of unsteady flows. There is experience using RANS codes that has been reported in the literature on problems that are similar to these three issues; it is not as extensive as the experience reported on time-averaged flow predictions. Hence, the technology exists to extend existing RANS codes to handle these problems; albeit, it is not a trivial task to implement the extensions. When the designer or researcher is considering the application of a computational prediction tool in a particular flow field investigation there are two primary questions that must be answered. They are: What fluid dynamical phenomena do I wish to predict? What are its characteristic scales? The number of grid points (temporal and spatial), the grid structure, and the boundaries of the flow domain to be modeled including how the boundary conditions are to be handled will be dictated by the answer to these questions. Preliminary computations may, of course, be required to answer these questions. The limitations of the computer to be used will also play a role in the decisions to be made in selecting the appropriate computational tools for a given flow problem. We must also keep in mind that the selection of a RANS code must be made after one is convinced that potential flow solvers and boundary-layer solvers are not useful in answering the particular engineering question raised in a given design problem.

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