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**SOURCE EMISSION TESTING OF THE
MUNITIONS DEACTIVATION FURNACE,
KADENA AIR BASE, OKINAWA, JAPAN**

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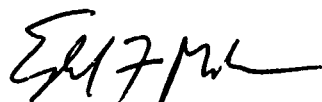
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13. ABSTRACT (Maximum 200 words) Source emission testing for total lead and particulates was conducted on the munitions deactivation furnace located in the 400th Munitions Squadron area of Kadena Air Base, Okinawa, Japan. Test results indicate that if most state or EPA standards were to apply, the munitions incinerator would exceed these standards. Total lead is also high, but there are no appropriate standards in which to compare. Recommendations are made as to the munitions furnace operation.		
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**SOURCE EMISSION TESTING OF THE MUNITIONS DEACTIVATION FURNACE
KADENA AB, OKINAWA, JAPAN**

INTRODUCTION

On 24-31 Sep 91, source emission testing for lead and particulate emissions was conducted on the munitions deactivation facility located in the 400th Munitions Maintenance Squadron (MMS) area of Kadena AB. Testing was performed by the Air Quality Function of Armstrong Laboratory. This survey was requested by the Chief, Bioenvironmental Engineering Services, 313th Medical Group (313 Med Gp/SGPB) to gather data necessary to satisfy an Environmental Compliance Assessment and Management Plan (ECAMP) deficiency. Personnel involved with on-site testing are listed in Appendix A.

Site Description

The deactivation furnace is a rotating kiln equipped with a small secondary burner/chamber at one end of the kiln (Fig. 1).



Figure 1. View of 400th MMS munitions deactivation furnace.

The incinerator is equipped with a continuous-feed conveyer which enters the incinerator just below the stack (Fig. 2). Emissions exit via a stack which extends through the roof and to 20.9 ft (6.38 m) above the ground (Fig. 3). Small arms ammunition, that is excess, no longer used, or out of date, is disposed of on a regular basis. Three different types of ammunition were used for the emission test which comprised 3 test runs: 20 mm high-explosive incendiary, 20 mm target tracer, and 7.62 mm and 5.56 mm ball cartridges.

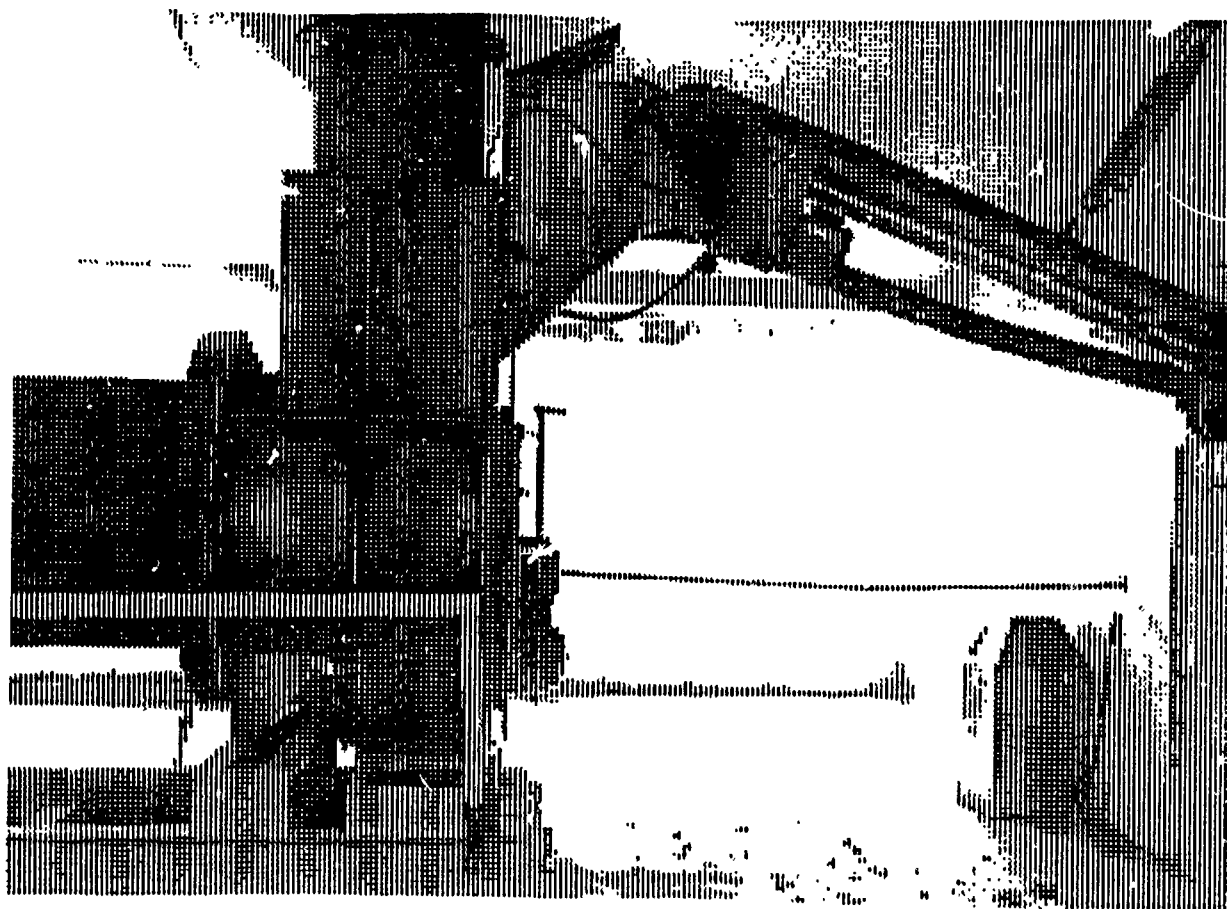


Figure 2. View of conveyer into incinerator.

Applicable Standards and Guidelines

There are no particulate or lead standards for this facility; however, in order to establish a baseline, particulate emission results are compared with Environmental Protection Agency (EPA) new source performance standard (NSPS) for incinerators which is 0.08 grains/dry standard ft³ (gr/dscf) (1). Emission standards in other states for existing facilities range from a high of 0.10 gr/dscf (229.22 mg/m³) in Alaska to a low of 0.04 gr/dscf (91.69 mg/m³) in New York (2). A comparable source standard for lead does not exist; however, the time weighted average-permissible exposure limit (TWA-PEL) for lead, which is 0.15 mg/m³, can be used to determine the relative risk with the appropriate dispersion model.

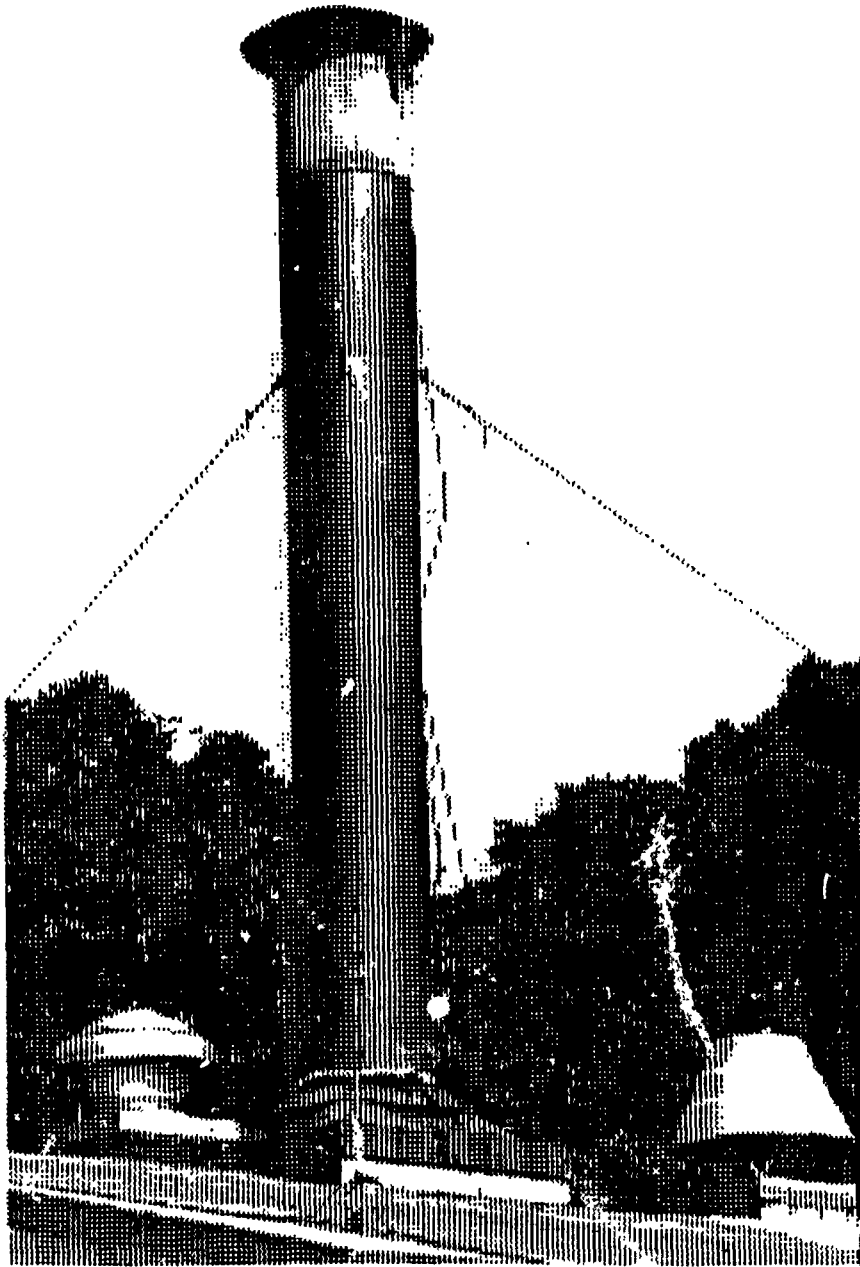


Figure 3. View of 400th MMS incinerator stack.

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METHODS AND MATERIALS

EPA Methods 1 through 5 and 12 were used for the sampling and analysis during this project.

Two sampling ports were installed at right angles in the stack. Ports were approximately 4 duct-diameters downstream and 3 duct-diameters upstream from any flow disturbance.

The inside stack diameter at the sampling port location is 23.5 in. (59.7 cm). Based on the duct-diameter, port location and type of sampling required (particulate), a total of 24 traverse points were determined for source emission evaluation.

Samples were collected using the sampling train of EPA Method 5. The train consisted of a button-hook probe nozzle, heated probe with stainless steel liner, a paper filter in a glass filter holder, impingers and pumping and metering device. Flue gas velocity pressure was measured at the nozzle tip using a Type-S pitot tube connected to a 10-in. inclined-vertical manometer. Type K thermocouples were used to measure flue gas as well as sampling train temperatures.

Prior to sampling, cyclonic flow was determined by using the Type S pitot tube and measuring the stack gas rotational angle at each traverse point. Flow conditions were considered acceptable since the arithmetic average of the rotational angles was less than 20°. A preliminary velocity pressure traverse was also accomplished at this time.

The total time for sampling run 1 was 60 min with sampling time for each traverse point at 2.5 min. Runs 2 and 3 had sampling times of 72 min with 3 min, respectively, for each sampling point.

A grab sample for Orsat analysis (measures oxygen and carbon dioxide for stack gas molecular weight determination) was taken during each sample run (1). Collected emission data and Orsat analysis data are in Appendix B. Calibration data are contained in Appendix C (3).

The emission calculations in Appendix B are made using "Source Testing Calculation and Check Programs for Hewlett-Packard 41 Calculators" developed by the EPA's Office of Air Quality Planning and Standards (4).

RESULTS AND DISCUSSION

Field Results

All 3 sampling runs were accomplished on 27 Sep 91. A summary of the field data from Appendix C is presented in Table 1.

The sampling time was modified after run 1 to draw a larger sample volume. A sample volume greater than 30 dscf is desirable and usually required for N₂SPS testing.

TABLE 1. FIELD DATA SUMMARY

Run #	Sampling Time (min.)	Meter Volume* (dscf)	Stack Flow Rate (dscfm)	Isokinetics %	O ₂ /CO ₂ %	Particulate Mass (mg)
1	60	28.708	1,041	101.5	13.3/5.6	2,170.3
2	72	35.900	1,130	97.6	13.9/5.2	958.5
3	72	40.042	1,290	95.3	13.2/5.7	1,346.0

* dscf is defined as dry standard cubic feet (1).
dscfm is defined as dry standard cubic feet per minute (1).

Isokinetics, which is the measure of the ratio sampling rate to the stack flow rate, is nominal for each run (3). The larger departure from 100% in runs two and three are not significant, and can be attributed to the increasing stack and ambient temperature as well as the rising atmospheric pressure associated with the departing typhoon Miriella.

Oxygen is slightly higher than required for excess air and may indicate too much ventilation or incomplete combustion.

A complete evaluation of the incinerator could not be accomplished without incinerator schematics and specifications; however, additional emission data (i.e., stack temperatures) from Appendix B with visual observations suggest that emissions are not adequately combusted.

Probe washes, impinger solutions, and blanks (7 samples) were left at Det 3, Armstrong Laboratory on 27 Sep 91. Samples were subsequently shipped to Armstrong Laboratory, Brooks AFB. Samples were received on 24 Oct 91 with the sample blank missing and the run 1 probe wash sample broken.

After gravimetric analysis to determine particulate concentrations, the samples were submitted for lead analysis to the Armstrong Laboratory, Occupational and Environmental Health Directorate, Analytical Services Division.

Analysis Results

All analyses were completed on 5 Dec 91. A summary of the laboratory results is presented in Table 2. The laboratory report is in Appendix D.

Particulate concentrations far exceed the allowable emissions of most states and those of the EPA's NSPS standard. Lead emissions are also high, but without an emission standard for comparison, the data cannot be adequately assessed. However, the data could be used within a dispersion model to determine ambient lead concentrations as well as deposition and accumulations in the surrounding area.

3. Quality Assurance Handbook for Air Pollution Measurement Systems - Volume III, Stationary Source Specific Methods, U.S. Environmental Protection Agency, EPA-600/4-77-027-b, Research Triangle Park, North Carolina, December 1984.
4. Source Test Calculation and Check Programs for Hewlett-Packard 41 Calculators. U.S. Environmental Protection Agency, EPA-304/1-85-018, Research Triangle Park, North Carolina, May 1987.

TABLE 2. ANALYSIS SUMMARY

Run #	Particulate Emissions		Lead Emissions	
	gr/dscf	mg/m ³	gr/dscf	mg/m ³
1*	1.167	2,670	0.0013	2.977
2	0.412	942.9	0.0013	2.931
3	0.519	1,187	0.0008	1.764
Average	0.700	1,600	0.0011	2.557

* The particulate emissions of run one have been corrected for the damaged sample. The lead emissions have not been corrected.

CONCLUSIONS AND RECOMMENDATIONS

The test results show the munitions incinerator at Kadena AB is not in compliance with the EPA or many states' particulate emission standards. Though there are no lead standards for incinerators, it is expected that new EPA regulations, as well as state regulatory agencies, will soon address incinerator lead emissions. In addition, the data in this report could be used in conjunction with other sampling which was performed concurrently and/or used in a dispersion model to give a more viable result.

Stack temperatures, oxygen values, and visual observations indicate incomplete combustion. Several alternatives exist to reduce these emissions. A secondary burner located at the base of the stack providing a chamber temperature between 1600-1800 °F would ensure more complete combustion. In addition, this approach would affect the excess air since more oxygen would be used for combustion, producing more carbon dioxide. It is questionable how much this modification would reduce emissions and whether the refractory could withstand these kinds of temperatures. Control equipment such as a wet scrubber is more expensive, but is guaranteed to reduce particulate emissions; a new incinerator is even more expensive, but may be more cost effective in the long term.

REFERENCES

1. "Standards of Performance for New Stationary Sources," Title 40, Part 60, Code of Federal Regulations, July 1, 1987.
2. "Alaska Air Quality Control Regulations," Title 18, Chapter 50, Alaska Administrative Code, June 2, 1988.

APPENDIX A
PERSONNEL

PERSONNEL

Armstrong Laboratory Stack Pack

Capt Paul T. Scott, Project Officer
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AL/OEBQ
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Phone: DSN 240-3305
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Det 3, Armstrong Laboratory Personnel

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APPENDIX B
FIELD DATA

PRELIMINARY SURVEY DATA SHEET N. 1
(Stack Geometry)

BASE <i>Kadena AFB</i>	PLANT <i>Munitions Incinerator</i>
DATE <i>27 Sept 91</i>	SAMPLING TEAM <i>May Cation / Capt Scott</i>
SOURCE TYPE AND MAKE <i>Incinerator</i>	
SOURCE NUMBER	INSIDE STACK DIAMETER <i>23.5 "</i> Inches
RELATED CAPACITY	TYPE FUEL
DISTANCE FROM OUTSIDE OF NIPPLE TO INSIDE DIAMETER <i>375 "</i> Inches	
NUMBER OF TRAVERSES <i>2</i>	NUMBER OF POINTS/TRVERSE <i>12</i>

LOCATION OF SAMPLING POINTS ALONG TRAVERSE

POINT	PERCENT OF DIAMETER	DISTANCE FROM INSIDE WALL (Inches)	TOTAL DISTANCE FROM OUTSIDE OF NIPPLE TO SAMPLING POINT (Inches)
<i>1</i>			<i>4.3</i>
<i>2</i>			<i>5.3</i>
<i>3</i>			<i>6.5</i>
<i>4</i>			<i>7.9</i>
<i>5</i>			<i>9.6</i>
<i>6</i>			<i>12.1</i>
<i>7</i>			<i>18.9</i>
<i>8</i>			<i>21.4</i>
<i>9</i>			<i>23.1</i>
<i>10</i>			<i>24.5</i>
<i>11</i>			<i>25.7</i>
<i>12</i>			<i>26.7</i>

PRELIMINARY SURVEY DATA SHEET NO. 2
(Velocity and Temperature Traverse)

BASE <i>Kadena AFB</i>	DATE <i>27 Sept 91</i>
BOILER NUMBER <i>Munitions Incinerator</i>	
INSIDE STACK DIAMETER <i>23 5"</i> Inches	
STATION PRESSURE <i>29.950</i> In Hg	
STACK STATIC PRESSURE <i>-(0.07)</i> In H2O	

SAMPLING TEAM
Major Eaton / Capt Scott

TRAVERSE POINT NUMBER	VELOCITY HEAD, V_p IN H2O	$\sqrt{V_p}$	STACK TEMPERATURE (°F)
1	0.015	0°	175
2	0.02	0°	202
3	0.02	0°	366
4	0.025	0°	434
5	0.03	0°	455
6	0.03	0°	461
7 (static pressure)	0.04	0°	472
8	0.035	0°	469
9	0.035	0°	467
10	0.04	0°	465
11	0.03	0°	463
12	0.03	0°	454
<i>Moisture = 5%</i>		<i>Molecular weight Wet = 29.63</i>	
<i>CO₂ = 12%</i>		<i>" " Dry = 30.24</i>	
<i>O₂ = 8%</i>		<i>Average FPS = 12</i>	
<i>Cp = 0.84</i>		<i>Average Temp = 107°F</i>	
<i>Nozzle = 0.5741 (calculated)</i>		<i>DSCFM = 1,263</i>	
		<i>A_p = 0.03</i>	
AVERAGE			

AII POLLUTION PARTICULATE ANALYTICAL DATA

BASE <i>Kadena AFB</i>	DATE <i>28 Sept 71</i>	RUN NUMBER <i>R41</i>
---------------------------	---------------------------	--------------------------

BUILDING NUMBER	SOURCE NUMBER <i>Munitions Incinerator</i>
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I. PARTICULATES			
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT PARTICLES (gm)
FILTER NUMBER	<i>1.4696</i>	<i>.2569</i>	<i>1.1727</i>
ACETONE WASHINGS (Probe, Front Hell Filter)	<i>Broken in shipment -</i>		<i>7.00</i> <i>6.07</i>
BACK HALF (if needed)	<i>99.1301</i>	<i>98.7532</i>	<i>0.3769</i>
Total Weight of Particulates Collected			<i>1.4696</i> <i>1.763 gm</i>

II. WATER			
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT WATER (gm)
IMPINGER 1 (H2O)	<i>128.5</i>	<i>100</i>	<i>28.5</i>
IMPINGER 2 (H2O)	<i>107.0</i>	<i>100</i>	<i>7</i>
IMPINGER 3 (Dry)	<i>.5</i>		<i>.5</i>
IMPINGER 4 (Silica Gel)	<i>209.9</i>	<i>200</i>	<i>9.9</i>
Total Weight of Water Collected			<i>45.9 gm</i>

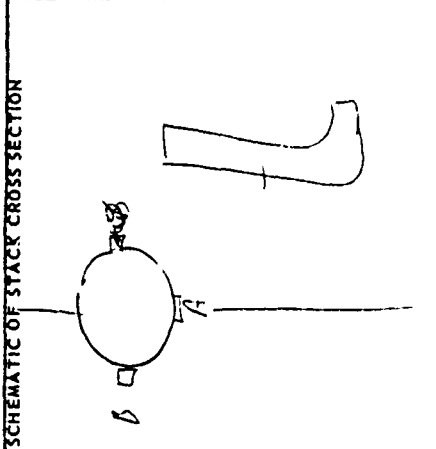
III. GASES (Dry)					
ITEM	ANALYSIS 1	ANALYSIS 2	ANALYSIS 3	ANALYSIS 4	AVERAGE
VOL % CO ₂	<i>5.6</i>	<i>5.6</i>	<i>5.6</i>		<i>5.6</i>
VOL % O ₂	<i>13.4</i>	<i>13.2</i>	<i>13.4</i>		<i>13.3</i>
VOL % CO					
VOL % N ₂					

Vol % N₂ = (100% - % CO₂ - % O₂ - % CO)

PARTICULATE SAMPLING DATA SHEET

AMBIENT TEMP 83 °F
 STATION PRESS 25.99 in Hg
 HEATER BOX TEMP 248 °F
 PROBE HEATER SETTING 248 °F
 PROBE LENGTH 6'
 NOZZLE AREA (A) 0.50 sq ft
 Cp 0.84
 DRY GAS FRACTION (F_d)

EQUATIONS
 $Q_R = Q_F + 460$
 $H = \left[\frac{5130 \cdot F_d \cdot C_p \cdot A}{C_o} \right]^2 \cdot \frac{T_m \cdot V_p}{T_s}$
 checked vacuum = 15 psi
 post check =
 pilot check = no leak (per check)
 pilot check = (post-leak)



RUN NUMBER A-1
 DATE 28 Sept 91
 PLANT Munitions Incinerator
 BASE Kaduna AFB
 SAMPLE BOX NUMBER 0
 METER BOX NUMBER 3551
 Qw/Qm
 Co

TRAVERSE POINT NUMBER	SAMPLING TIME (min)	STATIC PRESSURE (in H ₂ O) $\frac{W_{atm} \cdot V_{atm}}{W_{atm} \cdot V_{atm}}$	STACK TEMP		VELOCITY HEAD (V _p) (4)	ORIFICE DIFF. PRESS. (in)	GAS SAMPLE VOLUME (cu ft)	GAS METER TEMP		OUT (°F) (C)	SAMPLE BOX TEMP (°F)	IMPINGER OUTLET TEMP (°F)
			(°F)	(°R)				IN (°F) (C)	AVG (T _m) (°R)			
1	2.5	1.0	240		0.015	0.77	401.465	87		87	246	74
2	2.5	1.5	305		0.015	0.71	3-17	94		90	248	63
3	2.5	2.0	295		0.015	0.72	7-10	96		90	249	60
4	2.5	2.5	399		0.015	0.64		97		91	249	59
5	2.5	3.0	496		0.025	0.76		97		91	251	58
6	2.5	4.0	512		0.025	0.94	705.0	97		91	250	57
7	2.5	4.5	532		0.03	1.10		97		91	249	57
8	2.5	5.0	538		0.03	1.10		97		91	252	57
9	2.5	5.0	540		0.025	0.91		98		92	252	57
10	2.5	5.0	538		0.025	0.92		98		92	252	58
11	2.5	5.5	540		0.025	0.91		98		92	252	59
12	2.5	6.0	530		0.025	0.92	414.986	99		92	252	59

AI. POLLUTION PARTICULATE ANALYTIC/ DATA

BASE <i>Kadena AFB, OK</i>	DATE <i>28 Sept 91</i>	RUN NUMBER <i>2</i>
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BUILDING NUMBER <i>Munitions Incinerator</i>	SOURCE NUMBER
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I. PARTICULATES			
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT PARTICLES (gm)
FILTER NUMBER	<i>0.6652</i>	<i>.2937</i>	<i>0.3715</i>
ACETONE WASHINGS (Probe, Front Half Filter)	<i>105.8373</i>	<i>105.6039</i>	<i>0.2334</i>
BACK HALF (If needed)	<i>103.8432</i>	<i>103.4896</i>	<i>0.3536</i>
Total Weight of Particulates Collected			<i>0.9585 gm</i>

II. WATER			
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT WATER (gm)
IMPINGER 1 (H2O)	<i>121</i>	<i>100</i>	<i>21</i>
IMPINGER 2 (H2O)	<i>114</i>	<i>100</i>	<i>14</i>
IMPINGER 3 (Dry)	<i>20</i>	<i>-</i>	<i>20</i>
IMPINGER 4 (Silica Gel)	<i>217.8</i>	<i>200</i>	<i>17.8</i>
Total Weight of Water Collected			<i>54.8 gm</i>

III. GASES (Dry)					
ITEM	ANALYSIS 1	ANALYSIS 2	ANALYSIS 3	ANALYSIS 4	AVERAGE
VOL % CO ₂	<i>5.2</i>	<i>5.2</i>	<i>5.2</i>		<i>5.2</i>
VOL % O ₂	<i>13.8</i>	<i>14.0</i>	<i>14.0</i>		<i>13.9</i>
VOL % CO					
VOL % N ₂					

Vol % N₂ = (100% - % CO₂ - % O₂ - % CO)

PARTICULATE SAMPLING DATA SHEET

SCHEMATIC OF STACK CROSS SECTION

AMBIENT TEMP _____ OF
 STATION PRESS _____ in Hg
 HEATER BOX TEMP _____ OF
 PROBE HEATER SETTING _____
 PROBE LENGTH _____ in
 NOZZLE AREA (A) _____ sq ft
 Cp _____
 DRY GAS FRACTION (Fd) _____

EQUATIONS

$$^{\circ}R = ^{\circ}F + 460$$

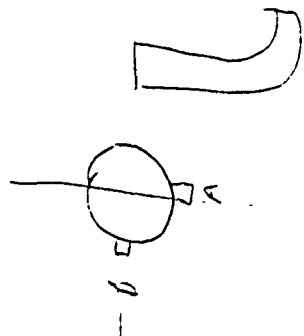
$$H = \left[\frac{5130 \cdot Fd \cdot Cp \cdot A}{Co} \right]^2 \cdot \frac{T_m \cdot V_p}{T_s}$$

RUN NUMBER **A-2**
 DATE **28 Sept 91**
 PLANT _____
 BASE _____
 SAMPLE BOX NUMBER _____
 METER BOX NUMBER _____
 Q_w/Q_m _____
 Co _____

TRAVERSE POINT NUMBER	SAMPLING TIME (min)	STATIC PRESSURE (in H ₂ O)	STACK TEMP		VELOCITY HEAD (Vp) (ft)	ORIFICE DIFF. PRESS. (H)	GAS SAMPLE VOLUME (cu ft)	GAS METER TEMP			SAMPLE BOX TEMP (OF)	IMPINGER OUTLET TEMP (OF)
			(OF)	(TS) (OR)				IN (OF)	AVG (Tm) (OR)	OUT (OF)		
1	3.0	3.5	280		.02	1.00	436.359	105		103	248	63
2	3.0	4.0	400		.025	1.08		107		103	249	58
3	3.0	4.0	377		.02	0.81		109		103	251	58
4	3.0	4.0	460		.02	0.75		109		104	251	60
5	3.0	4.0	525		.02	0.73		110		104	251	60
6	3.0	4.0	560		.02	0.73		111		105	251	61
7	3.0	4.0	593		.02	0.72		111		105	249	62
8	3.0	4.0	587		.02	0.72		111		106	250	64
9	3.0	4.0	589		.02	0.71		111		106	251	64
10	3.0	4.0	585		.02	0.72		111		105	249	64
11	3.0	4.0	574		.02	0.72		111		106	250	66
12	3.0	4.0	565		.02	0.73	473.886	111		106	251	67
Avg 494										105		
$\sqrt{8.575} = 4.9357$ $\sqrt{0.1} = 3.853$												

PARTICULATE SAMPLING DATA SHEET

RUN NUMBER	B-2
DATE	29 Sept 91
PLANT	
BASE	
SAMPLE BOX NUMBER	
METER BOX NUMBER	
Q_w/Q_m	
C_p	



$\Delta H_o = 1.921$
 $\Delta T = 90^\circ\text{F} + 460$
 $H = \left[\frac{5130 \cdot F_d \cdot C_p \cdot A}{C_o} \right]^2 \cdot \frac{T_m}{T_s} \cdot V_p$

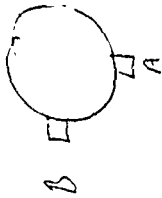
TRAVERSE POINT NUMBER	SAMPLING TIME (min)	STATIC PRESSURE (in H ₂ O)	STACK TEMP		VELOCITY HEAD (Vp) (ft)	ORIFICE DIFF. PRESS. (H)	GAS SAMPLE VOLUME (cu ft)	GAS METER TEMP			SAMPLE BOX TEMP (°F)	IMPINGER OUTLET TEMP (°F)
			(°F)	(°K)				IN (°F)	AVG (°F)	OUT (°F)		
1	3.0	2.0	265		0.03	1.53	435.137	101	100	100	243	70
2	3.0	2.0	309		0.03	1.44		102	100	100	243	70
3	3.0	2.0	314		0.02	0.96		104	100	100	241	70
4	3.0	2.5	328		0.03	1.41		106	100	100	253	70
5	3.0	2.5	530		0.03	1.13		107	101	101	252	70
6	3.0	2.5	571		0.035	1.26		107	101	101	255	70
7	3.0	3.0	578		0.04	1.43		107	101	101	254	70
8	3.0	3.5	580		0.04	1.43		107	101	101	256	70
9	3.0	4.0	578		0.04	1.43		108	102	102	251	70
10	3.0	3.5	573		0.03	1.08		108	102	102	251	70
11	3.0	3.5	570		0.03	1.08		108	101	101	252	67
12	3.0	3.5	561		0.025	0.91	456.359	109	102	102	252	65

AI. POLLUTION PARTICULATE ANALYTIC/ DATA					
BASE		DATE		RUN NUMBER 3	
BUILDING NUMBER			SOURCE NUMBER		
I. PARTICULATES					
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT PARTICLES (gm)		
FILTER NUMBER	9398	2909	0.6489		
ACETONE WASHINGS (Probe, Front Half Filter)	99.8668	99.4264	0.4404		
BACK HALF (if needed)	94.7806	94.5239	0.2567		
Total Weight of Particulates Collected			1.3460 gm		
II. WATER					
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT WATER (gm)		
IMPINGER 1 (H2O)	142	100	42		
IMPINGER 2 (H2O)	105	100	5		
IMPINGER 3 (Dry)	10	-	1		
IMPINGER 4 (Silica Gel)	212.8	200	12.8		
Total Weight of Water Collected			60.8 gm		
III. GASES (Dry)					
ITEM	ANALYSIS 1	ANALYSIS 2	ANALYSIS 3	ANALYSIS 4	AVERAGE
VOL % CO ₂	5.6	5.8	5.8		5.7
VOL % O ₂	13.2	13.2	13.2		13.2
VOL % CO					
VOL % N ₂					
Vol % N ₂ = (100% - % CO ₂ - % O ₂ - % CO)					

OEHL FORM 20
MAY 78

PARTICULATE SAMPLING DATA SHEET

SCHEMATIC OF STACK CROSS SECTION



RUN NUMBER: A-3

DATE: 28 Sept 91

PLANT: Munition

BASE: Kadana

SAMPLE BOX NUMBER: 3551

METER BOX NUMBER: 70m

Co: -

AMBIENT TEMP: 88°F

STATION PRESS: 30 In Hg

HEATER BOX TEMP: OF

PROBE HEATER SETTING: OF

PROBE LENGTH: IN

NOZZLE AREA (A): 0 sq ft

Cp: 0.84

DRY GAS FRACTION (Fd):

EQUATIONS

$$^{\circ}R = ^{\circ}F + 460$$

$$H = \left[\frac{5130 \cdot Fd \cdot Cp \cdot A}{Co} \right]^2 \cdot \frac{T_m}{T_s}$$

TRAVERSE POINT NUMBER	SAMPLING TIME (min)	STATIC PRESSURE (in H ₂ O)	STACK TEMP		VELOCITY HEAD (Vp)	ORIFICE DIFF. PRESS. (H)	GAS SAMPLE VOLUME (cu ft)	GAS METER TEMP			IMPINGER OUTLET TEMP (°F)	
			(°F)	(°R)				IN (°F)	AVG (Tm) (°R)	OUT (°F)		SAMPLE BOX TEMP (°F)
1	3.0	2.5	248	248	0.02	1.02	474.259	106	105	106	244	70
2	3.0	4.0	225	225	0.03	1.63		106	106	106	244	60
3	3.0	4.0	473	473	0.03	1.44		108	106	106	245	57
4	3.0	4.0	543	543	0.03	1.00		110	106	106	246	56
5	3.0	4.5	574	574	0.03	1.12		110	105	105	246	56
6	3.0	5.5	593	593	0.04	1.27		111	107	107	247	55
7	3.0	6.0	597	597	0.04	1.42		111	106	106	248	54
8	2.0	6.0	602	602	0.04	1.41		112	107	107	249	55
9	3.0	7.0	600	600	0.04	1.42		112	107	107	247	56
10	3.0	6.5	592	592	0.03	1.07		112	107	107	248	56
11	3.0	6.5	580	580	0.03	1.08	495.410	111	107	107	549	56
12												

PARTICULATE SAMPLING DATA SHEET

SCHEMATIC OF STACK CROSS SECTION

RUN NUMBER B-1

DATE 28 Sept 91

PLANT _____

BASE _____

SAMPLE BOX NUMBER _____

METER BOX NUMBER _____

Qw/Qm _____

Co _____

AMBIENT TEMP 85 °F

STATION PRESS _____ in Hg

HEATER BOX TEMP _____ °F

PROBE HEATER SETTING _____

PROBE LENGTH _____ in

NOZZLE AREA (A) _____ sq ft

DRY GAS FRACTION (FD) _____

OR = °F + 460

$$H = \left[\frac{-5130 \cdot FD \cdot Cp \cdot A}{Co} \right]^2 \cdot \frac{T_m}{T_8} \cdot Vp$$



TRAVERSE POINT NUMBER	SAMPLING TIME (min)	STATIC PRESSURE (in H2O)	STACK TEMP		VELOCITY w/HEAD (Vp)	ORIFICE DIFF. PRESS. (H)	GAS SAMPLE VOLUME (cu ft)	GAS METER TEMP			SAMPLE BOX TEMP (°F)	IMPINGER OUTLET TEMP (°F)
			(°F)	(Ts) (°R)				IN w (°F)	AVG (Tm) (°R)	OUT w (°F)		
1	3.0	6.0	275		0.02	1.02	495.610	108	106	106	248	62
2	3.0	6.5	354		0.03	1.15		110	107	107	248	55
3	3.0	7.5	420		0.03	1.28		111	107	107	248	53
4	3.0	9.5	486		0.04	1.19		112	107	107	250	53
5	3.0	13.0	536		0.04	1.51		112	107	107	248	52
6	3.0	13.0	541		0.04	1.43		112	107	107	247	54
7	3.0	16.0	588		0.04	1.61		111	107	107	250	55
8	3.0	16.5	593		0.04	1.60		111	107	107	249	56
9	3.0	17.0	591		0.04	1.60		111	107	107	250	57
10	3.0	13.0	529		0.03	1.14		111	107	107	246	57
11	3.0	14.5	467		0.03	1.41		110	106	106	250	58
12	3.0	17.0	454		0.03	1.23		110	106	106	248	58
							517.539					
							Avg 494					
							1.51					
							5.6398					
							VPTS					
							43.28					

XPOM "METH 5"		XPOM "METH 5"		XPOM "METH 5"	
RUN NUMBER		RUN NUMBER		RUN NUMBER	
THREE		TWO		ONE	
METER 60X V"	PUM	METER 60X V"	PUM	METER 60X V"	PUM
.9938	PUM	.9938	PUM	.9938	PUM
DELTA H"		DELTA H"		DELTA H"	
1.9248	PUM	1.9248	PUM	1.9248	PUM
BAR PRESS ?		BAR PRESS ?		BAR PRESS ?	
29.9002	PUM	29.9002	PUM	29.9002	PUM
METER VOL ?		METER VOL ?		METER VOL ?	
43.2888	PUM	78.5768	PUM	38.2288	PUM
MTR TEMP F?		MTR TEMP F?		MTR TEMP F?	
105.0000	PUM	105.0000	PUM	95.0000	PUM
STATIC HOH IN ?		% OTHER GAS REMOVED BEFORE DRY GAS METER ?		% OTHER GAS REMOVED BEFORE DRY GAS METER ?	
-.0700	PUM				
STACH TEMP.		STATIC HOH IN ?		STATIC HOH IN ?	
494.0000	PUM	-.0700	PUM	-.0700	PUM
ML. WATER ?		STACH TEMP.		STACH TEMP.	
60.9000	PUM	494.0000	PUM	481.0000	PUM
% CO2?		ML. WATER ?		ML. WATER ?	
5.7000	PUM	54.8000	PUM	45.9000	PUM
% OXYGEN?		% CO2?		% CO2?	
13.3000	PUM	5.3000	PUM	5.6000	PUM
% CO ?		% OXYGEN?		% OXYGEN?	
	PUM	13.9000	PUM	13.3000	PUM
MWD =25.44		% CO ?		% CO ?	
MW WET=28.68			PUM		PUM
		MOL WT OTHER?		MOL WT OTHER?	
			PUM		PUM
SQRT PETS ?		MWD =29.39		MWD =29.47	
5.6738	PUM	MW WET=29.62		MW WET=29.67	
TIME MIN ?					
72.0000	PUM	SQRT PETS ?		SQRT PETS ?	
NOZZLE DIA ?		4.9357	PUM	4.4069	PUM
.5000	PUM	TIME MIN ?		TIME MIN ?	
STK DIA INCH ?		72.0000	PUM	68.0000	PUM
23.5000	PUM	NOZZLE DIA ?		NOZZLE DIA ?	
	PUM	.5000	PUM	.5000	PUM
		STK DIA INCH ?		STK DIA INCH ?	
		23.5000	PUM	23.5000	PUM
* VOL MTR STD = 40.842		* VOL MTR STD = 35.908		* VOL MTR STD = 29.708	
STK PRES ABS = 29.89		STK PRES ABS = 29.89		STK PRES ABS = 29.89	
VOL HOH GAS = 2.98		VOL HOH GAS = 2.53		VOL HOH GAS = 2.15	
% MOISTURE = 6.67		% MOISTURE = 6.70		% MOISTURE = 7.08	
MOL DRY GAS = 0.973		MOL DRY GAS = 0.973		MOL DRY GAS = 0.978	
% NITROGEN = 81.10		% NITROGEN = 88.90		% NITROGEN = 81.10	
MOL WT DRY = 29.44		MOL WT DRY = 29.39		MOL WT DRY = 29.47	
MOL WT WET = 29.62		MOL WT WET = 29.62		MOL WT WET = 29.63	
VELOCITY FPS = 13.82		VELOCITY FPS = 12.13		VELOCITY FPS = 10.92	
STACK AREA = 3.91		STACK AREA = 3.81		STACK AREA = 3.91	
STACK ACFM = 1.503		STACK ACFM = 2.148		STACK ACFM = 1.955	
* STACK BSCFM = 1.248		* STACK BSCFM = 1.138		* STACK BSCFM = 1.041	
% ISOCHNETIC = 95.29		% ISOCHNETIC = 97.98		% ISOCHNETIC = 101.78	

END OF FIELD DATA

XROM "MASSFLO"		XROM "MASSFLO"		XROM "MASSFLO"	
RUN NUMBER		RUN NUMBER		RUN NUMBER	
ONE		TWO		THREE	
	RUN		RUN		RUN
VOL MTR STD ?		VOL MTR STD ?		VOL MTR STD ?	
28.70000	RUN	35.90000	RUN	40.04200	RUN
STACK DSCFM ?		STACK DSCFM ?		STACK DSCFM ?	
1,041.00000	RUN	1,130.00000	RUN	1,290.00000	RUN
FRONT 1/2 MG ?		FRONT 1/2 MG ?		FRONT 1/2 MG ?	
2,170.30000	RUN	958.50000	RUN	1,346.00000	RUN
BACK 1/2 MG ?		BACK 1/2 MG ?		BACK 1/2 MG ?	
	RUN		RUN		RUN
F GR/DSCF = 1.16665		F GR/DSCF = 0.41202		F GR/DSCF = 0.51875	
F MG/MMM = 2.669.70789		F MG/MMM = 942.85429		F MG/MMM = 1.187.06968	
F LB/HR = 10.40988		F LB/HR = 3.99075		F LB/HR = 5.73584	
F KG/HR = 4.72192		F KG/HR = 1.81020		F KG/HR = 2.60179	

XROM "MASSFLO"		XROM "MASSFLO"		XROM "MASSFLO"	
RUN NUMBER		RUN NUMBER		RUN NUMBER	
ONE PB		TWO PB		THREE PB	
	RUN		RUN		RUN
VOL MTR STD ?		VOL MTR STD ?		VOL MTR STD ?	
28.70000	RUN	35.90000	RUN	40.04200	RUN
STACK DSCFM ?		STACK DSCFM ?		STACK DSCFM ?	
1,041.00000	RUN	1,130.00000	RUN	1,290.00000	RUN
FRONT 1/2 MG ?		FRONT 1/2 MG ?		FRONT 1/2 MG ?	
2,42000	RUN	2,98000	RUN	2,00000	RUN
BACK 1/2 MG ?		BACK 1/2 MG ?		BACK 1/2 MG ?	
	RUN		RUN		RUN
F GR/DSCF = 0.00130		F GR/DSCF = 0.00128		F GR/DSCF = 0.00077	
F MG/MMM = 2.37587		F MG/MMM = 2.93136		F MG/MMM = 1.76395	
F LB/HR = 0.01161		F LB/HR = 0.01241		F LB/HR = 0.00952	
F KG/HR = 0.00527		F KG/HR = 0.00567		F KG/HR = 0.00387	

APPENDIX C
CALIBRATION DATA

NOZZLE CALIBRATION DATA FORM

Date _____ Calibrated by _____

Nozzle identification number	Nozzle Diameter ^a			ΔD, ^b mm (in.)	D _{avg} ^c
	D ₁ , mm (in.)	D ₂ , mm (in.)	D ₃ , mm (in.)		
	0.500	0.500	0.500	0	0

where:

^aD_{1,2,3} = three different nozzle diameters, mm (in.); each diameter must be within (0.025 mm) 0.001 in.

^b ΔD = maximum difference between any two diameters, mm (in.), ΔD ≤ (0.10 mm) 0.004 in.

^c D_{avg} = average of D₁, D₂, and D₃.

$$\frac{32 \text{ cf}}{24} = 1.33 \text{ cf/point}$$

~~$$12 \text{ fps} \left(\frac{0.50}{42} \right)^2 = 0.79 \text{ cf/s} = \frac{117.8}{24} = 4.9$$~~

Quality Assurance Handbook M5-2.6

$$\left(\pi \left(\frac{0.5}{12} \right)^2 \times 12 \right) \times \frac{60^2}{144} \times 2.5 \text{ air} = 2.45 \text{ cf/point (58.8 cf)}$$

$$\left(\pi \left(\frac{0.6}{12} \right)^2 \times 12 \right) \times 60 \times 2.5 = 3.53 \text{ cf/point}$$

$$(3.216) \times 24 = \boxed{77.65}$$



METER BOX CALIBRATION DATA AND CALCULATION FORM

(English units)

Primary Standard calibrated 19 July 90

Date 13 Aug 90 $V_{uc} = 5.0$ Meter box number Nutech 2
 Barometric pressure, $P_b = 30.12$ in. Hg Calibrated by Scott & Vaughn

Orifice manometer setting (ΔH), in. H ₂ O	Gas volume		Temperature				Time (θ), min	Y_i	$\Delta H\theta$, in. H ₂ O
	Wet test meter (V_w), ft ³	Dry gas meter (V_d), ft ³	Wet test meter (t_w), °F	Dry gas meter					
				Inlet (t_{d_i}), °F	Outlet (t_{d_o}), °F	Avg ^a (t_d), °F			
0.5	5	4.984	⁷⁹ ₈₅ 542.0	⁷⁹ ₈₈ 543.5	⁷⁶ ₈₁ 538.5	541.0	13.1	1.00001	1.948 1.948
1.0	5	5.006	⁸⁵ ₈₂ 543.5	⁸⁸ ₈₉ 548.5	⁸⁷ ₈₁ 541.0	544.8	9.2	0.9987	1.932
1.5	10	10.080	⁸² ₈₂ 542.0	⁸⁹ ₉₄ 551.5	⁸⁷ ₈₄ 547.5	547.0	15.0	0.9976	1.908
2.0	10	10.225	⁸² ₈₃ 542.5	⁹⁴ ₉₇ 555.5	⁸⁴ ₈₆ 545	550.75	13.1	0.9871	1.932
3.0	10	10.175	⁸³ ₈₃ 543.0	⁹⁷ ₁₀₀ 558.5	⁸⁶ ₈₈ 547	552.75	10.7	0.9932	1.928
^{V_{uc} = 7.0} 4.0	10	10.280	⁸³ ₈₃ 543.0	¹⁰⁰ ₁₀₀ 560	⁸⁹ ₈₉ 549	554.5	9.2	0.9838	1.8747
Avg								0.993	1.924

ΔH , in. H ₂ O	$\frac{\Delta H}{13.6}$	$Y_i = \frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\Delta H\theta_i = \frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) \theta}{V_w} \right]^2$
0.5	0.0368	$Y_i = \frac{(5)(30.12)(541)}{(4.984)(30.1568)(542.0)}$	$= \frac{(0.0317)(0.5)}{(30.12)(541)} \left[\frac{(542)(13.1)}{5} \right]^2 = 1.948$
1.0	0.0737	$Y_i = \frac{(5)(30.12)(544.75)}{(5.006)(30.1937)(543.5)}$	$= \frac{(0.0317)(1.0)}{(30.12)(544.8)} \left[\frac{(543.5)(9.2)}{5} \right]^2 = 1.932$
1.5	0.110	$Y_i = \frac{(10)(30.12)(547.0)}{(10.08)(30.230)(542.0)}$	$= \frac{(0.0317)(1.5)}{(30.12)(547)} \left[\frac{(542)(15)}{10} \right]^2 = 1.9076$
2.0	0.147	$= \frac{(10)(30.12)(550.75)}{(10.225)(30.267)(542.5)}$	$= \frac{(0.0317)(2.0)}{(30.12)(550.75)} \left[\frac{(542.5)(13.1)}{10} \right]^2 = 1.9320$
3.0	0.221	$= \frac{(10)(30.12)(552.75)}{(10.175)(30.341)(543.0)}$	$= \frac{(0.0317)(3.0)}{(30.12)(552.75)} \left[\frac{(543)(10.7)}{10} \right]^2 = 1.9288$
4.0	0.294	$= \frac{(10)(30.12)(554.5)}{(10.28)(30.414)(543)}$	$= \frac{(0.0317)(4)}{(30.12)(554.5)} \left[\frac{(543)(9.2)}{10} \right]^2$

^a If there is only one thermometer on the dry gas meter, record the temperature under t_d .

METER BOX CALIBRATION DATA AND CALCULATION FORM

(English units)

Date 23 Dec 91

Meter box number 2

Barometric pressure, $P_b = \underline{29.370}$ in. Hg Calibrated by C. Brice/Vayha

VAL

Orifice manometer setting (ΔH), in. H ₂ O	Gas volume		Temperature				Time (Θ), min	Y_i	$\Delta H @_i$ in. H ₂ O			
	Wet test meter (V_w), ft ³	Dry gas meter (V_d), ft ³	Wet test meter (t_w), °F	Dry gas meter								
				Inlet (t_{d_i}), °F	Outlet (t_{d_o}), °F	Avg ^a (t_d), °F						
4.8	0.5	5	69 70	69.5	70 72	71.5	69 70	69.5	70.5	12.642	1.011	1.823
4.8	1.0	5	70 71	70.5	72 76	74.5	71 70	70	72.25	9.084	1.020	1.886
4.8	1.5	10	71 71	71	76 72	79	70 72	71	75	15.054	1.029	1.934
4.9	2.0	10	71 71	71	78 79	89.5	77 79	78	83.75	13.19	1.037	1.947
5.1	3.0	10	71 71	71	85 88	86.5	74 77	78.5	81	10.750	1.025	1.950
7.0	4.0	10	71 71	71	91 96	93.5	79 82	80.5	87	9.251	1.042	1.965
								Avg	1.027	1.908		

ΔH , in. H ₂ O	$\frac{\Delta H}{13.6}$	$Y_i = \frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\Delta H @_i = \frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) \Theta}{V_w} \right]^2$
0.5	0.0368	$\frac{(5)(29.370)(70.5+460)}{(4.951)(29.370 + \frac{0.5}{13.6})(69.5+460)}$	$\frac{0.0317(0.5)}{29.370(70.5+460)} \left[\frac{(69.5+460)(12.642)}{5} \right]^2$
1.0	0.0737	$\frac{(5)(29.370)(72.25+460)}{(4.904)(29.370 + \frac{1.0}{13.6})(70.5+460)}$	$\frac{0.0317(1.0)}{29.370(72.25+460)} \left[\frac{(70.5+460)(9.084)}{5} \right]^2$
1.5	0.110	$\frac{(10)(29.370)(75+460)}{(9.754)(29.370 + \frac{1.5}{13.6})(71+460)}$	$\frac{0.0317(1.5)}{29.370(75+460)} \left[\frac{(71+460)(15.054)}{10} \right]^2$
2.0	0.147	$\frac{(10)(29.370)(83.75+460)}{(9.825)(29.370 + \frac{2.0}{13.6})(71+460)}$	$\frac{0.0317(2.0)}{29.370(83.75+460)} \left[\frac{(71+460)(13.19)}{10} \right]^2$
3.0	0.221	$\frac{(10)(29.370)(81+460)}{(9.867)(29.370 + \frac{3.0}{13.6})(71+460)}$	$\frac{0.0317(3.0)}{29.370(81+460)} \left[\frac{(71+460)(10.750)}{10} \right]^2$
4.0	0.294	$\frac{(10)(29.370)(87+460)}{(9.79)(29.370 + \frac{4.0}{13.6})(71+460)}$	$\frac{0.0317(4.0)}{29.370(87+460)} \left[\frac{(71+460)(9.251)}{10} \right]^2$

^a If there is only one thermometer on the dry gas meter, record the temperature under t_d .

APPENDIX D
LABORATORY REPORT

AIR FORCE
OCCUPATIONAL AND ENVIRONMENTAL HEALTH DIRECTORATE
BROOKS AFB, TEXAS, 78235-5000

REPORT OF ANALYSIS

BASE SAMPLE NO: GN910025 OEHL SAMPLE NO: 91061451
SAMPLE TYPE: NON-POTABLE WATER
SITE IDENTIFIER: FAMU227 DATE RECEIVED: 911126
DATE COLLECTED: 910928 DATE REPORTED: 911211
DATE REPRINTED: 920102
SAMPLE SUBMITTED BY: 18 MEDICAL GROUP/SGPB

RESULTS

<u>Test</u>	<u>Results</u>	<u>Units</u>
Lead	9669	ug/L

Analyzed by:

Aaron L. Forrest, Sgt, USAF
Occupational Analysis Technician

Reviewed by:

G. Cornell Long
Chief, Metals Analysis Function

TO:

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AL/OEBE
BROOKS AFB, TX 78235-5000

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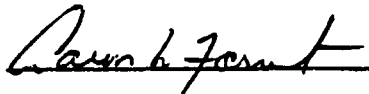
AIR FORCE
OCCUPATIONAL AND ENVIRONMENTAL HEALTH DIRECTORATE
BROOKS AFB, TEXAS, 78235-5000


REPORT OF ANALYSIS

BASE SAMPLE NO: GN910027 OEHL SAMPLE NO: 91061453
SAMPLE TYPE: NON-POTABLE WATER
SITE IDENTIFIER: FAMU227 DATE RECEIVED: 911126
DATE COLLECTED: 910928 DATE REPORTED: 911211
DATE REPRINTED: 920102
SAMPLE SUBMITTED BY: 18 MEDICAL GROUP/SGPB

RESULTS

<u>Test</u>	<u>Results</u>	<u>Units</u>
Lead	1661	ug/L

Analyzed by: 
Aaron L. Forrest, Sgt, USAF
Occupational Analysis Technician

Reviewed by: 
G. Cornell Long
Chief, Metals Analysis Function

TO:

AIR FORCE
OCCUPATIONAL AND ENVIRONMENTAL HEALTH DIRECTORATE
BROOKS AFB, TEXAS, 78235-5000

REPORT OF ANALYSIS

BASE SAMPLE NO: GN910029 OEHL SAMPLE NO: 91061455
SAMPLE TYPE: NON-POTABLE WATER
SITE IDENTIFIER: FAMU227 DATE RECEIVED: 911126
DATE COLLECTED: 910928 DATE REPORTED: 911211
DATE REPRINTED: 920102
SAMPLE SUBMITTED BY: 18 MEDICAL GROUP/SGPB

RESULTS

<u>Test</u>	<u>Results</u>	<u>Units</u>
Lead	6995	ug/L

Analyzed by:

Aaron L. Forrest, Sgt, USAF
Occupational Analysis Technician

Reviewed by:

G. Cornell Long
Chief, Metals Analysis Function

TO:

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