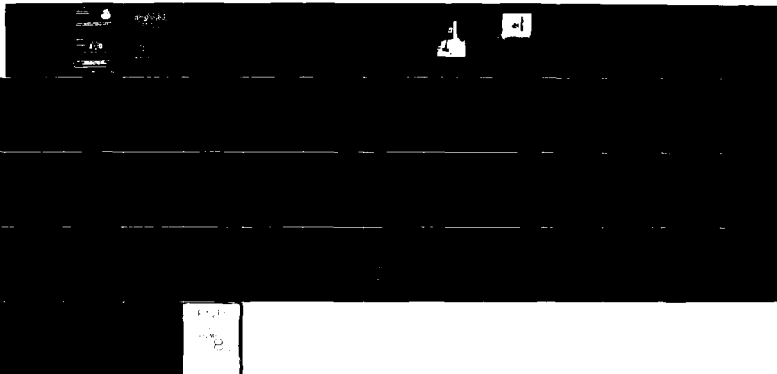
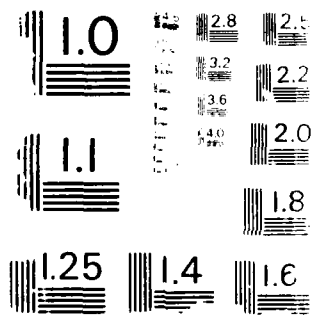


AD-A209 500

SOURCE EMISSION TESTING OF CLASSIFIED WASTE INCINERATOR I/I
GRIFFISS AFB NEW. (U) AIR FORCE OCCUPATIONAL AND
ENVIRONMENTAL HEALTH LAB BROOKS AF.. P I SCOTT APR 89
USAF OENL-89-031EQ0079FEI F/G 24/1 NL

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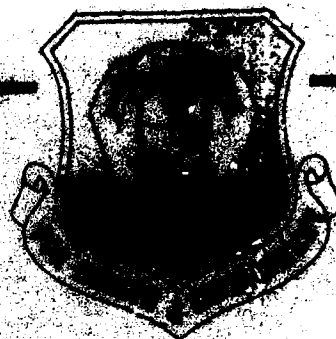




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USAF OEHF REPORT
89-031EG0070DEF



AD-A209 500

**SOURCE EMISSION TESTING OF CLASSIFIED
WASTE INCINERATOR, GRIFFISS AFB NY**

PAUL T. SCOTT, Capt, USAF, BSC

April 1989

Final Report

DTIC
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JUN 28 1989
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Distribution is unlimited; approved for public release

Environmental Health Laboratory

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The Public Affairs Office has reviewed this report, and it is releasable to the National Technical Information Service, where it will be available to the general public, including foreign nations.

This report has been reviewed and is approved for publication.

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JAMES C. BUCK, Colonel, USAF, BSC
Commander

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SECURITY CLASSIFICATION OF THIS PAGE

REPORT DOCUMENTATION PAGE				Form Approved OMB No 0704-0188	
1a. REPORT SECURITY CLASSIFICATION Unclassified			1b. RESTRICTIVE MARKINGS N/A		
2a. SECURITY CLASSIFICATION AUTHORITY N/A			3. DISTRIBUTION / AVAILABILITY OF REPORT Approved for public release. Distribution is unlimited.		
2b. DECLASSIFICATION / DOWNGRADING SCHEDULE N/A					
4. PERFORMING ORGANIZATION REPORT NUMBER(S) AFOEHL Report 89-031EQ0079DEF			5. MONITORING ORGANIZATION REPORT NUMBER(S)		
6a. NAME OF PERFORMING ORGANIZATION AF Occupational and Environmental Health Laboratory.		6b. OFFICE SYMBOL (If applicable) ECO	7a. NAME OF MONITORING ORGANIZATION		
6c. ADDRESS (City, State, and ZIP Code) Brooks AFB TX 78235-5501			7b. ADDRESS (City, State, and ZIP Code)		
8a. NAME OF FUNDING / SPONSORING ORGANIZATION Same as 6a		8b. OFFICE SYMBOL (If applicable)	9. PROCUREMENT INSTRUMENT IDENTIFICATION NUMBER		
8c. ADDRESS (City, State and ZIP Code) Same as 6c			10. SOURCE OF FUNDING NUMBERS		
			PROGRAM ELEMENT NO	PROJECT NO	TASK NO
					WORK UNIT ACCESSION NO
11. TITLE (Include Security Classification) Source Emission Testing of Classified Waste Incinerator, Griffis AFB NY					
12. PERSONAL AUTHOR(S) Capt Paul T. Scott					
13a. TYPE OF REPORT Final		13b. TIME COVERED FROM 19-23 Sep 88 TO	14. DATE OF REPORT (Year, Month, Day) April 1989		15. PAGE COUNT 53
16. SUPPLEMENTARY NOTATION					
17. COSATI CODES			18. SUBJECT TERMS (Continue on reverse if necessary and identify by block number)		
FIELD	GROUP	SUB-GROUP			
			Emission Testing		
			Classified Waste		
			Compliance Testing		
			Air Quality		
19. ABSTRACT (Continue on reverse if necessary and identify by block number)					
At the request of 416 Strategic Hospital/SGPB, personnel of the AFOEHL Air Quality Function conducted source emission testing for particulates, HCl, and opacity on the classified waste incinerator at Griffiss AFB. The New York Department of Environmental Conservation (NYDEC) required testing for permit compliance. Particulate Emissions were well above the emission limits allowed by the State of New York. Action is recommended to bring the classified waste incinerator into compliance.					
20. DISTRIBUTION / AVAILABILITY OF ABSTRACT ☐ UNCLASSIFIED/UNLIMITED ☒ SAME AS RPT ☐ DTIC USERS			21. ABSTRACT SECURITY CLASSIFICATION Unclassified		
22a. NAME OF RESPONSIBLE INDIVIDUAL Capt Paul T. Scott			22b. TELEPHONE (Include Area Code) (512) 536-2891		22c. OFFICE SYMBOL USAF0EHL/ECO

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I. INTRODUCTION

On 19-23 Sep 88, a stationary source sampling survey for opacity, particulate emissions, and hydrogen chloride emissions was conducted on the new classified waste incinerator at Griffiss AFB NY by personnel from the Air Quality Function of the AF Occupational and Environmental Health Laboratory (AFOEHL). This survey was requested by the 416 Strategic Hospital/SGPB via HQ SAC/SGPB to meet permit requirements established by the New York State Department of Environmental Conservation (NYSDEC). Personnel involved with on-site testing are listed in Appendix A.

II. DISCUSSION

A. Background: Griffiss AFB had an accumulated amount of classified waste material which needed to be destroyed. A shredding machine had been used, but was inadequate; and, the accumulation was considered a potential security risk. Before placing a new classified waste incinerator on line, the NYSDEC ordered compliance testing as a condition for obtaining an operating permit. Compliance testing included opacity, particulate emissions, and hydrogen chloride (HCl) emissions. HCl was a concern because of the potential for incinerating small percentages of classified microfiche and other chlorinated plastics.

B. Site Description: The classified waste incinerator is located in a separate building approximately 50 yards east of bldg 19. Figure 1 is a photograph of the incinerator building and stack. The incinerator, Model CAI-750-MI, was manufactured by Advanced Combustion Systems, Bellingham, Washington and has no pollution control equipment. A view of the incinerator can be seen in Figure 2. The following are operating parameters:

1. Two-chamber design
2. Fired by #2 fuel oil
3. Load capacity
 - a. 500 lbs/hr for type 0 waste
 - b. 750 lbs/hr for type 1 waste

C. Applicable Standards: The monitoring requirements and regulations for opacity and particulates are defined under Codes, Rules, and Regulations of the State of New York, Title 6, Chapter III--Air Resources, Subchapter A--Prevention and Control of Air Contamination and Air Pollution, Part 219. Appendix B has a copy of the applicable state laws. Particulate emissions are based on a charge of 300 lbs per hour and are extrapolated from Figure 1 of Appendix 2 in Part 219. There are no applicable standards for chloride emissions but testing for chlorides was requested. Proposed new incinerator emission standards (Part-219.5) do not apply to existing Type 0 waste incinerators. The following is a summary of the applicable standards:

1. Particulate emissions: 0.85 lbs/hr
2. Opacity: not to exceed 20% or No. 1 on the Ringleman Chart

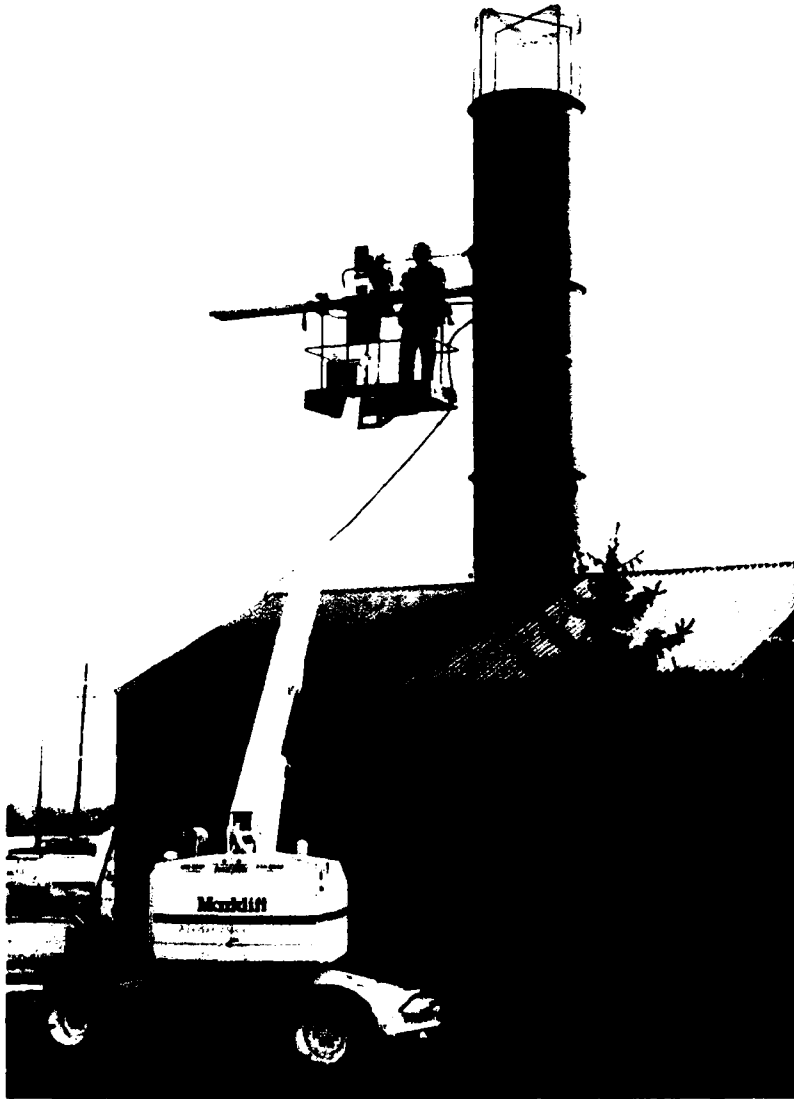


Figure 1: Classified Waste Incinerator Building and Stack

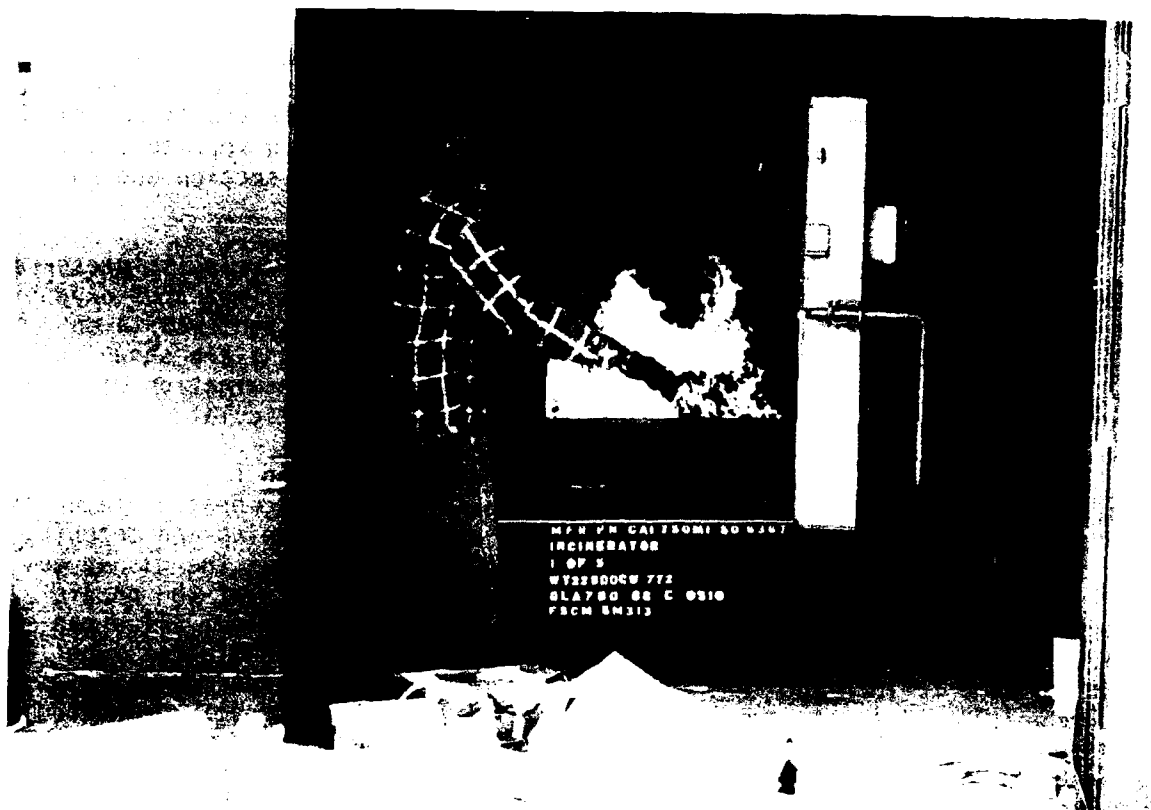


Figure 2: View of Incinerator

D. Sampling Methods and Procedures

New York State Codes, Rules, and Regulations, Title 6, Chapter III--Air Resources, require that emission testing be conducted in accordance with Appendix A to Title 40, Code of Federal Regulations, Part 60 (40 CFR 60). Therefore, sample train preparation, sampling and recovery, calculations and quality assurance were done in accordance with the methods and procedures outlined in 40 CFR 60, Appendix A.

For testing purposes, the incinerator was operated with Type 0 waste at a load rate of 300 lbs/hr, although the maximum rated load was 500 lbs/hr. Griffiss AFB personnel were unable to provide an estimate of the amount or frequency in which they would burn, since they had not operated the

incinerator previously. It was determined that 300 lb/hr would be more than a sufficient charge. This change was coordinated with the State with the stipulation that the load rate used for testing would be the maximum load rate for future incinerator use.

Sampling ports were already in place approximately 4.5 duct diameters downstream and 1.5 duct diameters upstream from any flow disturbance. Based on the inside stack diameter, port locations, and type of sample (particulate), 24 four traverse points (12 per diameter) were used to collect a representative particulate sample. Appendix C shows a typical stack cross section and the actual traverse point locations for each stack surveyed.

Prior to testing, cyclonic flow was determined and a velocity pressure traverse was accomplished. A grab sample for Orsat analysis (measures oxygen and carbon dioxide for stack gas molecular weight determination) was taken during each sample run. Orsat sampling and analysis equipment are shown in Figures 3 and 4. Flue gas moisture content, needed for determination of flue gas molecular weight determination, was obtained during particulate sampling.

Particulate samples were collected using the sampling train shown in Figure 5. The train consisted of a button-hook probe nozzle, heated stainless steel probe liner, heated glass filter, impingers, and a pumping and metering device. The nozzle was sized prior to each sample run so that the gas stream could be sampled isokinetically; in other words, the velocity at the nozzle tip was the same as the stack gas velocity at each point sampled. Flue gas velocity pressure was measured at the nozzle tip using a Type-S pitot tube connected to a 10-inch inclined-vertical manometer. Type K thermocouples were used to measure flue gas as well as sampling train temperatures. The heated, stainless steel-lined probe was used due to the extremely high stack temperature. The heated filter was used to collect particulates and pass condensable materials. The impinger train (first, third and fourth impingers were modified Greenburg-Smith type; second impinger standard Greenburg-Smith design) was used as a condenser to collect stack gas moisture and condensable particulates. The first and second impingers were filled with 200 ml each of 0.100 N sodium carbonate to collect any HCl. The third and fourth impingers were empty and contained 200 grams of indicating silica gel, respectively, to collect any remaining moisture. The pumping and metering system was used to control and monitor the sample gas flow rate. Each of the three tests were 84 minutes in duration.

Emission calculations were done using "Source Test Calculation and Check Programs for Hewlett-Packard 41 Calculators" (EPA-340/1-85-018) developed by the EPA Office of Air Quality Planning and Standards, Research Triangle Park NC. All field data and resulting emission calculations are presented in Appendix D. Calibration Data is presented in Appendix E.

III. CONCLUSIONS

The emission survey results did not satisfy the New York State's emission limits. Opacity was well within limits and did not exceed 5% at any time during the test. However, particulate emissions were well above the limit.

The high particulate emissions were somewhat of a surprise since the opacity averaged near zero. The average particulate emission was 2.6677 lbs/hr compared to the limit of 0.85 lbs/hr. The average HCl emission rate was 0.01579 lbs/hr. The stack emission test results can be found in Table 2.

IV. RECOMMENDATIONS

The Classified Waste Incinerator is not in compliance with particulate emission limits. Considering the incinerator is new and of good design, it is not obvious where the problem may lie. The particulate collected was primarily a white ash so incineration was complete. However, it was observed that forced air to the primary chamber caused turbulence in the chamber and could be sending ash up the stack. The design of the chamber should limit exit gas velocities such that nonoxidized particulate matter and ash are not entrained in the exhaust gases and carried up to the secondary chamber and out the stack. Perhaps an adjustment here might alleviate the problem. Also, further reducing the charge rate may bring emissions below standards. Finally, we recommend a re-evaluation of the incinerator after NYSDEC action or any procedural or equipment adjustments have been accomplished.

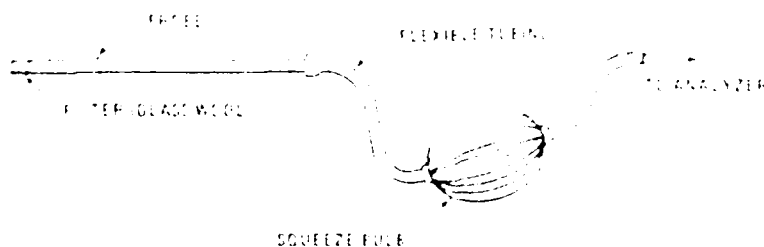


Figure 3: Schematic of Grab Bag Sampling Train

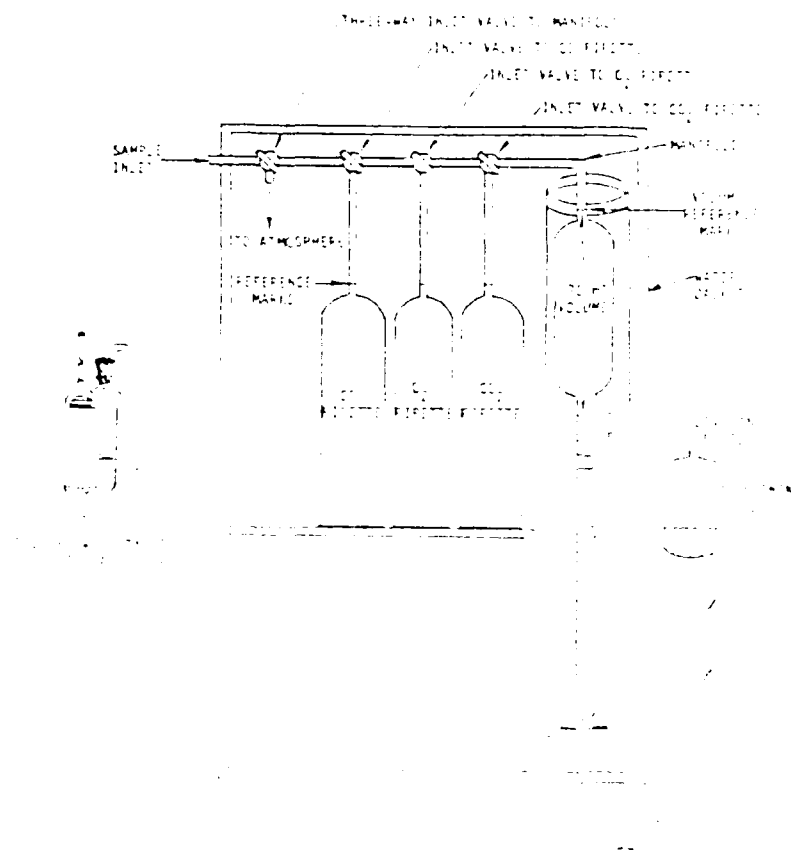


Figure 4: Schematic of ORSAT Apparatus

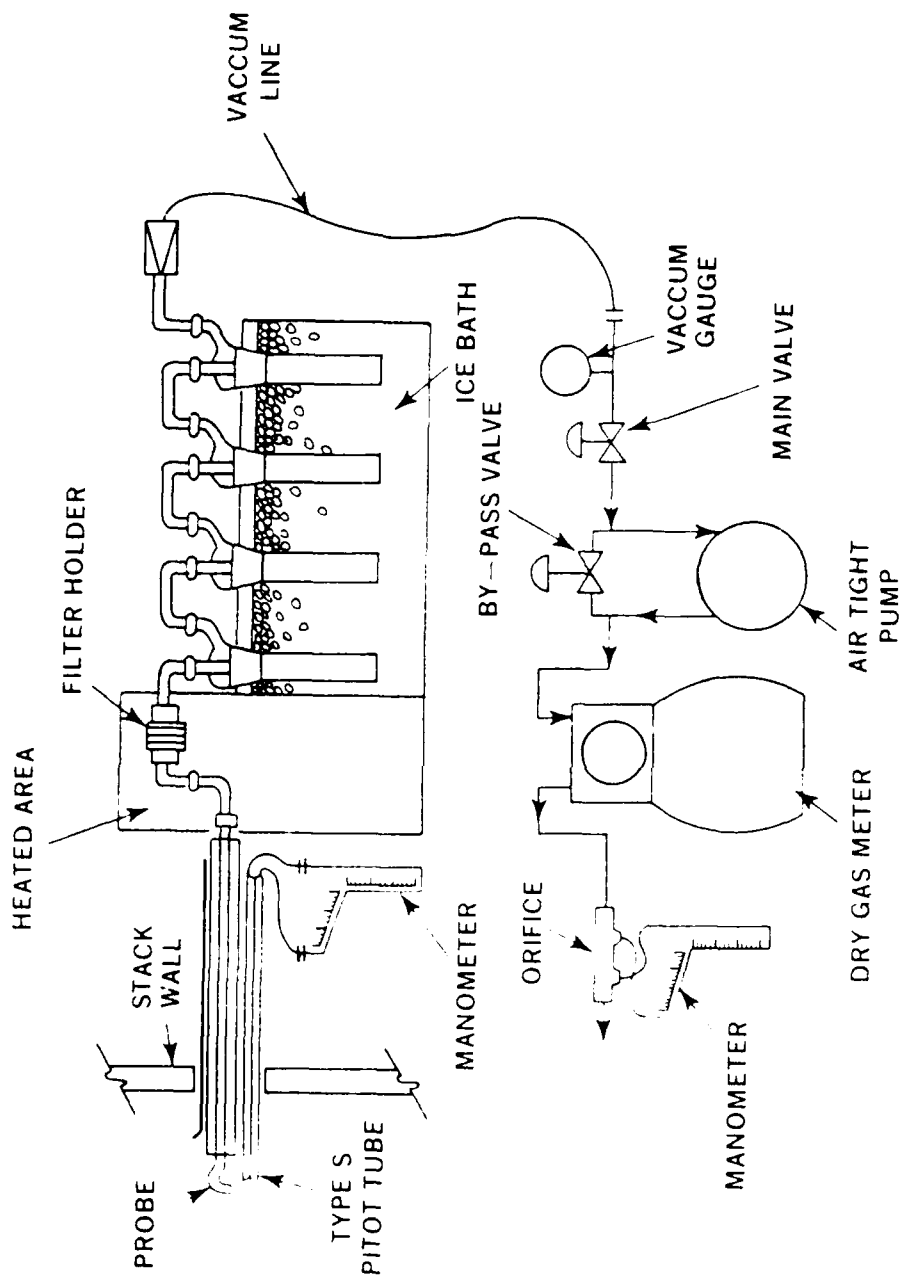


Figure 5: Schematic of Particulate Sampling Train

TABLE 1

SUMMARY OF EMISSION DATA

RUN #	CHARGE RATE (lbs/hr)	PERCENT ISOKINETICS (%)	SAMPLE VOLUME (dscf)	STACK GAS FLOW RATE (dscfm)	PARTICULATE CATCH (mg)	CHLORIDE CATCH (mg)
1	300	98.85	34.3610	1255	683.5	2.7824
2	300	99.62	35.4670	1293	603.1	3.4282
3	300	102.87	33.2880	1168	444.4	3.7504

TABLE 2

STACK EMISSION TEST RESULTS
GRIFFISS AFB CLASSIFIED WASTE INCINERATOR

RUN #	STACK GAS		PARTICULATE EMISSIONS (lbs/hr)	HCl EMISSIONS (lbs/hr)	PASS STANDARDS (Y or N)
	%O ₂	%CO ₂			
1	8.7	10.6	3.3021	0.01344	N
2	10.3	9.0	2.9083	0.01653	N
3	9.5	9.4	2.0626	0.01741	N
AVERAGE			2.6677	0.01579	N

REFERENCES

1. Code of Federal Regulations. Vol 40, Parts 53-60, The Office of the Federal Register National Archives and Records Service, General Services Administration, Washington DC, July 1987.
2. Quality Assurance Handbook for Air Pollution Measurement Systems - Volume III, Stationary Source Specific Methods, US Environmental Protection Agency, EPA-600/4-77-027-b, Research Triangle Park, North Carolina, December 1984.
3. Source Test Calculation and Check Programs for Hewlett-Packard 41 Calculators, US Environmental Protection Agency, EPA-340/1-85-018, Research Triangle Park, North Carolina, May 1987.

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APPENDIX A
Test Participants

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1. AFOEHL Test Team

Maj James A. Garrison, Chief, Air Quality Function
Capt Paul T. Scott, Consultant, Air Quality Meteorologist
TSgt Benjamin Hernandez, Environmental Quality Technician
SSgt Daniel Schillings, Industrial Hygiene Technician

AFOEHL/ECQ
Brooks AFB TX 78235-5501

Phone: AUTOVON 240-2891
Commercial (512) 536-2891

2. Griffiss AFB On-site Representatives

Capt Richard Tourjee	416 Strategic Hospital Griffiss/SGPB
MSgt Donald Watkins	AUTOVON 587-3617

Ms Gilda Bielba	416 CSG/DAD
Mr Ryan Ziminski	AUTOVON 587-7708

Mr Bruce Mero	416 CSG/DEEV
Mr Fred Conover	AUTOVON 587-2098

Mr Walt Hyde	416 CSG/DEMM
--------------	--------------

3. New York State Department of Environmental Conservation (Region 6)

Mr David Prosser, PE (via phone)
Regional Air Pollution Engineer
(315) 785-2513

Mr David Hathaway
Principal Engineering Technician
(315) 793-2554

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APPENDIX B
State Incinerator Regulations

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PART 218 VEHICLES PROPELLED BY DIESEL ENGINES

(Effective May 1, 1972; May 10, 1981)

Section 218.1 Applicability. This Part shall apply to all vehicles propelled by a diesel engine, excluding marine vessels.

218.2 Prohibitions. (a) No person who owns, operates or leases a vehicle propelled by a diesel engine, or who owns, leases or occupies land and has actual or apparent dominion or control over the operation of a vehicle propelled by a diesel engine which is present on said land, shall operate said vehicle or allow or permit it to be operated, in such a manner that exhaust emissions of a shade of blue, black or grey equal to or greater than Number 1 on the Ringelmann chart or equivalent standard acceptable to the Commissioner are produced for a continuous period of more than five seconds, when the vehicle is in motion.

(b) No person who owns, operates or leases a bus or truck, the motive power for which is provided by a diesel engine or who owns, leases or occupies land and has the actual or apparent dominion or control over the operation of a bus or truck present on such land, the motive power for which said bus or truck is provided by a diesel engine, shall allow or permit the diesel engine of such bus or truck to idle for more than five consecutive minutes when the bus or truck is not in motion, except as otherwise permitted by section 218.3.

218.3 Exceptions. The prohibitions of subdivision (b) of Section 218.2 shall not apply when:

(a) A bus or truck is forced to remain motionless because of traffic conditions over which the operator thereof has no control;

(b) Regulations adopted by federal, state or local agencies having jurisdiction require the maintenance of a specific temperature for passenger comfort. The idling time specified in subdivision (b) of section 218.2 may be increased but only to the extent necessary to comply with such regulations;

(c) A diesel engine is being used to provide power for an auxiliary purpose, such as loading, discharging, mixing or

processing cargo; controlling cargo temperature; construction; lumbering; oil or gas well servicing; farming; or when operation of the engine is required for the purpose of maintenance.

(d) Fire, police and public utility trucks or other vehicles are performing emergency services.

(e) Trucks owned or operated by persons engaged in mining and quarrying are used within the confines of such persons' property.

(f) A truck is to remain motionless for a period exceeding two hours, and during which period the ambient temperature is continuously below twenty-five degrees Fahrenheit.

PART 219 INCINERATORS (Effective May 1, 1972)

Section 219.1 Title. These rules shall be known as the New York State rules to prevent air pollution from incinerators.

219.2 Applicable geographical area. This Part shall apply to the entire State of New York.

219.3 Definitions. (a) Incinerator. Any structure or furnace in which combustion takes place and type 0, 1, 2, 3, or 4 refuse is used as fuel, alone or in conjunction with fossil fuel.

(b) Refuse. All waste material, including but not limited to, garbage, rubbish, incinerator residue, street cleanings, dead animals, and offal. Refuse is classified in accordance with Table 1, Appendix 2.

(c) Smoke. An air contaminant consisting of small gas-borne particles emitted by an air contamination source in sufficient number to be observable.

219.4 Emission limits. (a) All incinerators having a capacity of 2,000 lb/hr or less and built and installed after January 1, 1968, shall be designed, built, installed and operated to meet the emission limits of figure 1*.

(b) No incinerator larger than 2,000 lb/hr capacity and built after January 1, 1970, shall be operated so as to produce

particulate emissions which exceed the amount shown in figure 1*.

(c) No incinerator having a capacity of 2,000 lb/hr or less and built or installed between April 1, 1962, and January 1, 1968, shall be operated so as to produce particulate emissions which exceed 0.5 lb/hr for every 100 lb/hr of refuse charged, unless a final order by the commissioner provides otherwise.

(d) Any incinerator having a capacity of 2,000 lb/hr or less and built or installed prior to April 1, 1962, shall either meet the requirements of 219.4(c) or shall be equipped with adequate control devices or redesigned and rebuilt so as to meet the requirements of 219.4(a) by January 1, 1969.

(e) No incinerator larger than 2,000 lb/hr capacity and built between April 1, 1962, and January 1, 1970, shall be operated so as to produce particulate emissions which exceed 0.5 lb/hr for every 100 lb/hr of refuse charged, unless a final order by the commissioner provides otherwise.

(f) Any incinerator larger than 2,000 lb/hr capacity and built prior to April 1, 1962, shall either meet the requirements of 219.4(e) or shall be equipped with adequate control devices or redesigned and rebuilt so as to meet the requirements of 219.4(b) by January 1, 1970.

219.5 Smoke emissions. (a) No incinerator, built or installed after January 26, 1967, regardless of size, shall emit smoke of an opacity denser than 20 percent or No. 1 of the Ringelmann chart or equivalent, under normal operating conditions.

(b) No incinerator built or installed prior to January 26, 1967, regardless of size, shall be operated so as to emit smoke of an opacity denser than 40 percent or No. 2 of the Ringelmann chart or equivalent, under normal operating conditions.

219.6 Tests. (a) All incinerators larger than 2,000 lb/hr capacity shall be tested using isokinetic sampling techniques in accordance with test procedures acceptable to the commissioner.

(b) All incinerators built or installed after January 1, 1968, and having a capacity of 2,000 lb/hr or less shall be tested in

*See Appendix 2

accordance with special test procedures promulgated by the commissioner. Units which are representative models may be tested instead of an actual installation, in accordance with special test procedures promulgated by the commissioner.

219.7 Abatement. (a) Where the commissioner has reason to believe that an incinerator installation is violating the emissions standards of section 219-4, he

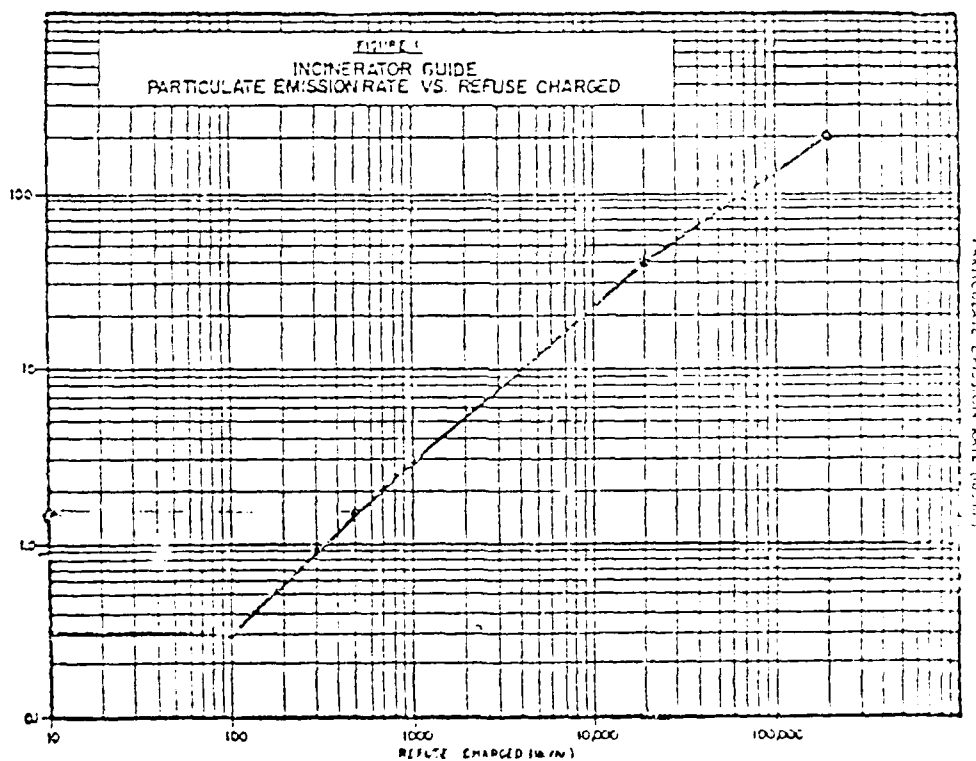
may have tests conducted. The owner shall provide, at his expense, sampling holes and pertinent allied facilities as needed, at the request of the commissioner.

(b) If such tests indicate a contravention of the emission limits, the commissioner may require the installation of appropriate control equipment or he may seal the incinerator if such equipment is not installed within the time limit specified by the commissioner.

(c) The commissioner may order the cleaning, repair, replacement or alteration of any equipment or control equipment which causes it is operated so as to cause a violation of this Part.

(d) The commissioner may order a change in the manner of operation of any incinerator which is operated so as to cause a violation of this Part.

APPENDIX 2



APPENDIX 2

TABLE 1

Classification of Refuse

(1)	(2)	(3)	(4)	(5)	(6)
	Refuse from residential areas, including refuse from hotels, motels, and other transient accommodations, and refuse from commercial and industrial sources.	Approximate Moisture Content, by weight	Approximate Solid Content, by weight	Approximate P.L.U. per pound of refuse	
1	Public collection of refuse from residential areas, including refuse from hotels, motels, and other transient accommodations, and refuse from commercial and industrial sources.	Approximate Moisture Content, by weight	Approximate Solid Content, by weight	Approximate P.L.U. per pound of refuse	
2	Refuse from residential areas, including refuse from hotels, motels, and other transient accommodations, and refuse from commercial and industrial sources.	Approximate Moisture Content, by weight	Approximate Solid Content, by weight	Approximate P.L.U. per pound of refuse	
3	Refuse from residential areas, including refuse from hotels, motels, and other transient accommodations, and refuse from commercial and industrial sources.	Approximate Moisture Content, by weight	Approximate Solid Content, by weight	Approximate P.L.U. per pound of refuse	
4	Refuse from residential areas, including refuse from hotels, motels, and other transient accommodations, and refuse from commercial and industrial sources.	Approximate Moisture Content, by weight	Approximate Solid Content, by weight	Approximate P.L.U. per pound of refuse	
5	Refuse from residential areas, including refuse from hotels, motels, and other transient accommodations, and refuse from commercial and industrial sources.	Approximate Moisture Content, by weight	Approximate Solid Content, by weight	Approximate P.L.U. per pound of refuse	
6	Refuse from residential areas, including refuse from hotels, motels, and other transient accommodations, and refuse from commercial and industrial sources.	Approximate Moisture Content, by weight	Approximate Solid Content, by weight	Approximate P.L.U. per pound of refuse	

PART 220

PORTLAND CEMENT PLANTS

(Effective March 16, 1973; May 10, 1984)

Section 220.1 Definitions. (a) For the purpose of this Part, the general definitions of Part 200 of this Title apply.

(b) For the purpose of this Part, the following definitions also apply:

(1) Dry process portland cement plant. A portland cement plant where the raw material kiln feed entering the kiln in a powder form has a moisture content of one percent or less by weight.

(2) Feed to the kiln. The weight of all materials, excluding fuels and uncombined water, introduced into the kiln during the time when a stack sample is being taken to determine compliance with sections 220.2 and 220.3 of this Part.

(3) Upset condition. Any unavoidable

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APPENDIX C
Sampling Port Location

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DETERMINATION OF MINIMUM NUMBER OF TRAVERSE POINTS

Stack ID: 200-500-0000 Stack diameter at ports: 3.4 (ft)

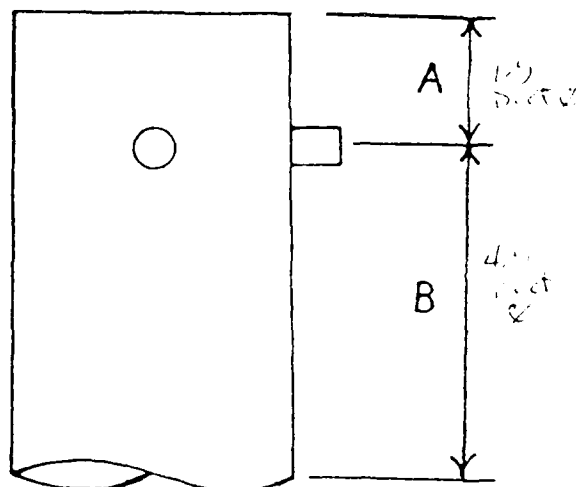
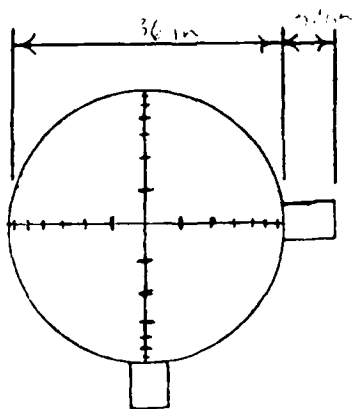
Distance A (ft) 4.4 (duct diameters) 1.6

Recommended number of traverse points as determined by
distance A: 24

Distance B (ft) 3.4 (duct diameters) 1.4

Recommended number of traverse points as determined by
distance B: 24

Number of traverse points used: 24



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APPENDIX D
Sampling Data and Calculations

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PRELIMINARY SURVEY DATA SHEET NO. 2
(Velocity and Temperature Traverse)

BASE Griffiss AFB	DATE 21 Sept 66
BOILER NUMBER Clarified Waste Incinerator	
INSIDE STACK DIAMETER 36.0 Inches	
STATION PRESSURE 29.396 In Hg	
STACK STATIC PRESSURE -0.05 In H2O	

SAMPLING TEAM

OETHL

TRAVERSE POINT NUMBER	VELOCITY HEAD, V_p IN H ₂ O	$\propto \sqrt{V_p}$	STACK TEMPERATURE (°F)
1	.014	0	1364
2	.010	0	1351
3	.024	2	1394
4	.015	0	1400
5	.014	0	1412
6	.045	0	1419
7	.041	0	1446
8	.01	0	1425
9	.02	5	1426
10	.03	5	1416
11	.03	5	1401
12	.03	5	1398
13			
			$\bar{T} = 1376$
			FP5 = 13
			FPA = 76.2
			$\bar{V} = .02$
AVERAGE			

AIR POLLUTION PARTICULATE ANALYTICAL DATA

BASE		DATE		RUN NUMBER	
Griffiss AFB		22 Sept 88		ONE	
BUILDING NUMBER			SOURCE NUMBER		
Classified Waste Incinerator			Model CAI-750-MI		
I. PARTICULATES					
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT PARTICLES (gm)		
FILTER NUMBER	521.3	286.6	0.2347		
ACETONE WASHINGS (Probe, Front Half Filter)	98.5648	98.1164	0.4488		
BACK HALF (if needed)					
		Total Weight of Particulates Collected		68.35 gm	
II. WATER					
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT WATER (gm)		
IMPINGER 1 (H2O)	242.0	200.0	42.0		
IMPINGER 2 (H2O)	210.0	200.0	10.0		
IMPINGER 3 (Dry)	0.0	0.0	0.0		
IMPINGER 4 (Silica Gel)	207.2	200.0	7.2		
		Total Weight of Water Collected		59.2 gm	
III. GASES (Dry)					
ITEM	ANALYSIS 1	ANALYSIS 2	ANALYSIS 3	ANALYSIS 4	AVERAGE
VOL % CO ₂	10.6	10.6	10.6		10.6
VOL % O ₂	8.8	8.8	8.6		8.7
VOL % CO					
VOL % N ₂					
Vol % N ₂ = (100% - % CO ₂ - % O ₂ - % CO)					

PARTICULATE SAMPLING DATA SHEET											
SCHEMATIC OF STACK CROSS SECTION				EQUATIONS				AMBIENT TEMP			
RUN NUMBER CNE				$^{\circ}\text{R} = ^{\circ}\text{F} + 460$				STATION PRESS 37.42			
DATE 22 Sept 88				$H = \left[\frac{5130 \cdot F_d \cdot C_p \cdot A}{C_o} \right]^2 \cdot \frac{T_m}{T_s} \cdot V_p$				HEATER BOX TEMP 25.4			
PLANT Clayton's Coast Inc								PROBE HEATER SETTING 218			
BASE Critch								PROBE LENGTH 218			
SAMPLE BOX NUMBER N 24								NOZZLE AREA (A) 34			
METER BOX NUMBER N 24								DRY GAS FRACTION (F _d) 34			
Q _w /Q _m											
Co											
<i>Posil leak check at 5:00 PM</i>											
TRAVERSE POINT NUMBER	SAMPLING TIME (min)	STATIC PRESSURE (in H ₂ O)	STACK TEMP		VELOCITY HEAD (Vp)	ORIFICE DIFF. PRESS. (in H ₂ O)	GAS SAMPLE VOLUME (cu ft)	GAS METER TEMP		SAMPLE BOX TEMP (°F)	IMPINGER OUTLET TEMP (°F)
			(°F)	(T _s) (°R)				IN (°F)	AVG (T _m) (°R)	OUT (°F)	
1	0	2.4	1210		0.001	0.06	736.072	75		74	726
2	3.5	2.4	1370		0.005	0.81		79		75	230
3	7.0	2.4	1390		0.005	0.86		80		76	240
4	10.5	2.7	1451		0.015	0.83		81		77	250
5	14.0	2.5	1466		0.012	0.66		83		77	242
6	17.5	2.4	1486		0.005	0.27		81		77	242
7	21.0	2.4	1479		0.005	0.27		81		77	251
8	24.5	2.4	1486		0.005	0.55		83		78	231
9	28.0	3.0	1481		0.024	1.09		82		78	235
10	31.5	3.4	1479		0.024	1.10		83		78	256
11	35.0	3.6	1476		0.026	1.19		84		78	259
12	38.2	3.7	1464		0.015	0.83	252.274	84		78	249
T _m = 75 T _s = 1421 ΔH = 4.71 T _{PS} = 4.6773											
C _o FT = 32.164											

PARTICULATE SAMPLING DATA SHEET												
SCHEMATIC OF STACK CROSS SECTION				EQUATIONS								
				$^{\circ}R = ^{\circ}F + 460$ $H = \left[\frac{5130 \cdot F \cdot C_p \cdot A}{C_o} \right]^2 \cdot \frac{T_m}{T_s} \cdot V_p$ $56 H_2O \cdot 8 \psi$ $1600 \cdot 275$								
				AMBIENT TEMP 60 $^{\circ}F$ 55443 STATION PRESS 28.1 $^{\circ}F$ HEATER BOX TEMP 275 $^{\circ}F$ PROBE HEATER SETTING 170 PROBE LENGTH 48 NOZZLE AREA (A) .651 Cp .84 DRY GAS FRACTION (Fd)								
				Static $Q = 0.54$ GDT $T_{m,s} = 0.54$ GDT								
TRAVERSE POINT NUMBER	SAMPLING TIME (min)	STATIC PRESSURE (in H ₂ O)	STACK TEMP		VELOCITY READ (Vp)	ORIFICE DIFF. PRESS. (H)	GAS SAMPLE VOLUME (cu ft)	GAS METER TEMP		SAMPLE BOX TEMP	IMPINGER OUTLET TEMP	
			($^{\circ}F$)	(T_s) ($^{\circ}R$)				IN ($^{\circ}F$)	AVG (T_m) ($^{\circ}R$)	OUT ($^{\circ}F$)		
A 1	0	2.2	1405		4.2	4.14	270.110	66		64	245	55
2	35	2.4	1350		4.05	4.21		70		66	248	56
3	30	2.1	1412		4.1	4.56		71		66	248	56
4	10.5	2.5	1424		4.15	4.83		73		68	251	56
5	10.6	2.3	1411		4.15	4.82		73		68	225	58
6	17.5	2.2	1453		4.02	4.82		74		69	230	55
7	21.6	2.0	1447		4.05	4.11		75		69	227	57
8	24.7	2.0	1497		4.15	4.27		76		70	230	56
9	28.0	2.5	1468		4.25	4.82		77		71	242	56
10	31.5	3.0	1470		4.25	1.47		77		72	248	56
11	35.0	3.4	1467		4.25	1.37		78		72	244	56
12	38.5	3.4	1466		4.25	1.37	236.472	79		73	240	56
stop												

Run#1 Calculations

XROM METH 5"

RUN NUMBER 1.0000 RUN

METER BOX V³ 1.0078 RUN

BELTA H² .7100 RUN

BAP PRESS² 30.0300 RUN

METER VOL³ 32.1640 RUN

MTR TEMP F¹ 75.0000 RUN

% OTHER GAS REMOVED BEFORE DRY GAS METER¹ RUN

STATIC HOH IN² -1.0500 RUN

STACK TEMP¹ 1.421.0000 RUN

ML. WATER² 59.0000 RUN

% CO₂¹ 10.0000 RUN

% OXYGEN¹ 8.0000 RUN

% CO¹ RUN

MOL WT CORR¹ RUN

MW = 78.24

MW MET = 19.14

SOFT PRESS¹ 4.6077 RUN

TIME MIN² 84.0000 RUN

MIDDLE IIP² 1.0540 RUN

STR IIP INCH² 30.0000 RUN

* VOL MTR STD = 74.361

STD PRESS DEG = 20.40

VOL RAW DGS = 0.79

% MOISTURE = 7.50

MOL DGM DGT = 0.905

% NITROGEN = 20.70

MOL WT DRY = 78.24

MOL WT MET = 19.14

WT NITRY EG = 11.74

STD PRESS = 1.07

STD DGM = 1.07

* STD. DGM = 1.055

% ISOETHANE = 19.15

END OF FIELD DATA

RUN NUMBER 1.0000 RUN

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VISIBLE EMISSION OBSERVATION FORM

No. RUN #1

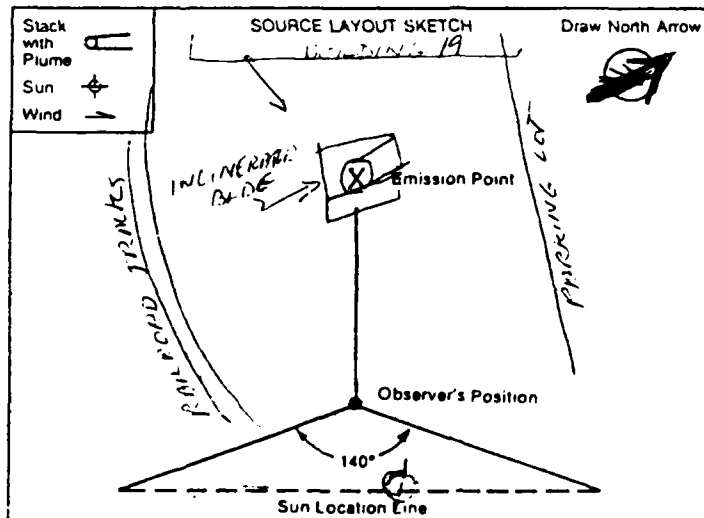
COMPANY NAME GRIFFISS HEB		
STREET ADDRESS		
CITY ROME	STATE NY	ZIP
PHONE (KEY CONTACT)	SOURCE ID NUMBER CLASS. WASTE INCINERATOR	

PROCESS EQUIPMENT 2 STAGE INCINERATOR	OPERATING MODE BATCH 300 LB
CONTROL EQUIPMENT NONE	OPERATING MODE -

DESCRIBE EMISSION POINT STEEL 3.5' OD STACK WITH LINDER	
SCREEN APPROX 2' HIGH	
HEIGHT ABOVE GROUND LEVEL 28'	HEIGHT RELATIVE TO OBSERVER Start 28' End ✓
DISTANCE FROM OBSERVER Start 100' End ✓	DIRECTION FROM OBSERVER Start NN End ✓

DESCRIBE EMISSIONS Start HEAT WAVES - NO CLOUDS End ✓	
EMISSION COLOR Start NONE End ✓	IF WATER DROPLET PLUME Attached ☐ Detached ☐
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED Start 5' ABOVE STACK End ✓	

DESCRIBE PLUME BACKGROUND CLEAR - NO HAZE	
Start RED 17-18-19 End ✓	
BACKGROUND COLOR Start BLUE/GRAY End ✓	SKY CONDITIONS Start SCATTERED End ✓
WIND SPEED Start 3 K End ✓	WIND DIRECTION Start SW End ✓
AMBIENT TEMP Start 60 End ✓	WET BULB TEMP 55
	RH. percent



OBSERVATION DATE		START TIME		END TIME	
22 SEPT 85		0850		0920	
SEC	0	15	30	45	COMMENTS
MIN					
1	0	0	0	0	300 LB- CHARGE
2	0	0	0	0	LOSS PAPER
3	0	0	0	0	SHEETS IN COMPLETE
4	0	0	0	0	PAPER ETC.
5	0	0	0	0	NO CAPACITY- CND
6	0	0	0	0	HEAT WAVES. START
7	0	0	0	0	at ABOUT 1452' F.
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	5	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	STACK WAS MONITOR
25	0	0	0	0	FOR REMAINDER
26	0	0	0	0	OF STACK TEST.
27	0	0	0	0	SUBSEQUENT
28	0	0	0	0	READINGS
29	0	0	0	0	REMAINED THE SAME
30	0	0	0	0	

OBSERVER'S NAME (PRINT) JAMES A. GARRISON	
OBSERVER'S SIGNATURE <i>James A. Garrison</i>	DATE 22 SEPT 85
ORGANIZATION USAFUEL/ECG BRIGADS HEB 14	
CERTIFIED BY TEXAS AIR CONTROLS	DATE 16 SEPT 85

CONTINUED ON VEO FORM NUMBER

ADDITIONAL INFORMATION

FUEL NO 2 FUEL OIL

CAPACITY. 300 LB

1412

2. LABORATORY PERFORMING ANALYSIS			063116			CN881265			
SAMPLE COLLECTION INFORMATION						1. DATE RECEIVED BY LAB 7 Oct 88		3. DATE ANALYSIS COMPLETED 17 Oct 88	
7. SITE DESCRIPTION 15 25									
8. SITE LOCATION NO		9. FLOWRATE AT SITE 00246 GAL/MIN		10. WEATHER		11. WATER TEMP (°F)		12. WIND DIR	
13. COLLECTION DATE PERIOD				14. COLLECTION TIME		15. REFERENCE TO OTHER ON-SITE ANALYSIS			
16. SAMPLING TECHNIQUE				17. ANALYST NAME					
18. REASON FOR SAMPLE SUBMISSION									
NEEDS									
ANALYSES REQUESTED AND RESULTS									
PRESERVATION GROUP A			PRESERVATION GROUP B			PRESERVATION GROUP C			
PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	MG/L
DISSOLVED OXYGEN Demand	0.34		ARSENIC	0.0010		BORON	01022		
TOTAL ORGANIC CARBON as C	0008		HARDNESS	100	1000	BORON, Dissolved	01020		
			CADMIUM	00024	00027	CHLORIDE	00940		47
PRESERVATION GROUP E			PRESERVATION GROUP F			PRESERVATION GROUP G			
PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	MG/L
COD & BPL (Free Chlorine Method)	005		CHROMIUM	0.03	0.04	COLOR	00080		
			COPPER	0.04	0.042	FLUORIDE	00951		
PRESERVATION GROUP C			PRESERVATION GROUP D			PRESERVATION GROUP H			
PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	MG/L
AMMONIA as N	00610		IRON	01040	01043	Residue Extractable IDS	00515		
NITRATE as N Cd Reduct. Method	00620		LEAD	01049	01051	Residue Non-Extractable	00530		
NITRITE as N	00615		MANGANESE	01050	01055	Residue Volatile	00505		
TOTAL KJELDAHL NITROGEN as N	00624		MERCURY	01090	01095	Specific Conductance	00095		
PHOSPHORUS (Ortho) as P	00510		NICKEL	01065	01067	SULFATE as SO4	00545		
PHOSPHORUS (Total) as P	00614		SELENIUM	01140	01147	SURFACTANTS MBAS as LAS	38200		
			SILVER	01070	01077	TURBIDITY	00074		
PRESERVATION GROUP D			PRESERVATION GROUP E			PRESERVATION GROUP I			
PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	MG/L
CYANIDE	00020		CALCIUM as Ca	00015	00016				
CYANIDE Free Chlorine as Cl2	00001		MAGNESIUM as Mg	00015	00017				
			POTASSIUM	00010	00010				
PRESERVATION GROUP E			PRESERVATION GROUP F			PRESERVATION GROUP J			
PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	MG/L
PHENOLS	3273		SODIUM	00013	00014				
19. ORGANIZATION REQUESTING ANALYSIS						20. CHEMIST JSC			
ECQ						21. REVIEWED BY			
						22. APPROVED BY			

AIR POLLUTION PARTICULATE ANALYTICAL DATA

BASE <i>Griffiss</i>		DATE <i>22 Sept 88</i>		RUN NUMBER <i>TWØ</i>	
BUILDING NUMBER <i>Classified Waste Incinerator</i>			SOURCE NUMBER <i>Model CAI-750-MI</i>		
I. PARTICULATES					
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT PARTICLES (gm)		
FILTER NUMBER	<i>.478Ø</i>	<i>.2862</i>	<i>.1918</i>		
ACETONE WASHINGS (Probe, Front Half Filter)	<i>1Ø5.18Ø8</i>	<i>1Ø4.7695</i>	<i>.4113</i>		
BACK HALF (if needed)					
			Total Weight of Particulates Collected <i>.6Ø31 gm</i>		
II. WATER					
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT WATER (gm)		
IMPINGER 1 (H2O)	<i>245.Ø</i>	<i>2ØØ.Ø</i>	<i>45.Ø</i>		
IMPINGER 2 (H2O)	<i>2Ø4.Ø</i>	<i>2ØØ.Ø</i>	<i>4.Ø</i>		
IMPINGER 3 (Dry)	<i>Ø.Ø</i>	<i>Ø.Ø</i>	<i>Ø.Ø</i>		
IMPINGER 4 (Silica Gel)	<i>2Ø7.2</i>	<i>2ØØ.Ø</i>	<i>7.2</i>		
			Total Weight of Water Collected <i>56.2 gm</i>		
III. GASES (Dry)					
ITEM	ANALYSIS 1	ANALYSIS 2	ANALYSIS 3	ANALYSIS 4	AVERAGE
VOL % CO ₂	<i>9.Ø</i>	<i>9.Ø</i>	<i>9.Ø</i>		<i>9.Ø</i>
VOL % O ₂	<i>1Ø.4</i>	<i>1Ø.4</i>	<i>1Ø.4</i>		<i>1Ø.3</i>
VOL % CO					
VOL % N ₂					
Vol % N ₂ = (100% - % CO ₂ - % O ₂ - % CO)					

Page 1 of 2

Run Number: 1W0

Date: 22 Sept 83

Plant: Classifex Waste Inc

Base: Civifex AFB

Sample Box Number:

Meter Box Number: Nutech

Qw/Qm:

Co:

PARTICULATE SAMPLING DATA SHEET

SCHEMATIC OF STACK CROSS SECTION

EQUATIONS

$0R = 0F + 460$

$H = \left[\frac{5130 \cdot Fd \cdot Cp \cdot A}{Co} \right]^2 \cdot \frac{Tm \cdot Vp}{Ts}$

$Mux = 29.5$

Stack C/P = -05

$\%H_2O \approx 8.8$

Pre leak check good and 15 in Hg

AMBIENT TEMP

STATION PRESS

HEATER BOX TEMP

PROBE HEATER SETTING

PROBE LENGTH

NOZZLE AREA (A)

Cp

DRY GAS FRACTION (Fd)

TRAVERSE POINT NUMBER	SAMPLING TIME (min)	STATIC PRESSURE (in H ₂ O)	STACK TEMP		VELOCITY HEAD (Vp)	ORIFICE DIFF. PRESS. (in)	GAS SAMPLE VOLUME (cu ft)	GAS METER TEMP		SAMPLE BOX TEMP (°F)	IMPINGER OUTLET TEMP (°F)
			(°F)	(Ts) (°R)				IN (°F)	OUT (°F)		
A 1	0	2.0	1232		0.10	0.62	252.514	76	76	246	56
2	3.5	2.0	1340		0.10	0.54		76	76	247	57
3	7.0	2.0	1420		0.15	0.84		77	76	247	56
4	10.5	2.5	1395		0.12	0.68		75	77	247	56
5	14.0	2.5	1394		0.15	0.85		79	76	251	56
6	17.5	2.5	1506		0.20	1.08		81	76	251	56
7	21.0	2.0	1502		0.05	0.27		80	76	251	57
8	24.5	2.0	1410		0.00	0.57		81	76	251	57
9	28.0	2.0	1450		0.10	0.55		81	77	251	57
10	31.5	2.0	1500		0.15	0.81		81	77	254	58
11	35.0	2.5	1419		0.20	1.13		81	77	254	58
12	38.5	3.4	1506		0.20	1.08		81	77	254	60
	42.0 stop										

PARTICULATE SAMPLING DATA SHEET															
SCHEMATIC OF STACK CROSS SECTION				EQUATIONS				AMBIENT TEMP							
				$^{\circ}R = ^{\circ}F + 460$ $H = \left[\frac{5130 \cdot F_d \cdot C_p \cdot A}{C_o} \right]^2 \cdot \frac{T_m \cdot V_p}{T_s}$				STATION PRESS		HEATER BOX TEMP		PROBE HEATER SETTING		PROBE LENGTH	
								in Hg		in Hg		in			
								sq ft							
								Cp							
								DRY GAS FRACTION (F _d)							
RUN NUMBER: <u>Page 2 of 2</u> DATE: <u>22 Sept 88</u> PLANT: <u>Chaparral Center</u> BASE: <u>Griffiss</u> SAMPLE BOX NUMBER: METER BOX NUMBER: <u>Nickel</u> Q _w /Q _m : Co:				S.O.P. page 1 of 2 Post leak check-out Sunday											
TRAVERSE POINT NUMBER	SAMPLING TIME (min)	STATIC PRESSURE (in H ₂ O)	STACK TEMP		VELOCITY HEAD (V _p)	ORIFICE DIFF. PRESS. (in)	GAS SAMPLE VOLUME (cu ft)	GAS METER TEMP		SAMPLE BOX TEMP (°F)	IMPINGER OUTLET TEMP (°F)				
			(°F)	(T _s) (°R)				IN (°F)	AVG (T _m) (°R)	OUT (°F)					
1	5	1.5	1256		0.001	0.460	269.510	76		75	253	57			
2	3.5	2.4	1392		0.010	0.57		76		75	249	63			
3	7	2.5	1460		0.015	0.83		78		75	252	54			
4	10.5	2.5	1485		0.012	0.63		79		76	252	54			
5	14.0	2.0	1485		0.010	0.54		81		76	253	55			
6	17.5	2.0	1504		0.010	0.54		82		77	255	56			
7	21	2.0	1517		0.005	0.27		83		77	257	59			
8	24.5	2.4	1460		0.015	0.83		83		78	252	64			
9	28	3.0	1506		0.020	1.08		83		78	255	55			
10	31.5	3.0	1409		0.020	1.14		84		78	257	55			
11	35	3.0	1410		0.020	1.14		84		78	257	57			
12	38.5	3.0	1492		0.010	0.55	285.898	85		79	260	57			
42.5 min T _m = 78 T _s = 1436 ΔH = 0.72 V _{STP} = 4.8196 C _u F _t = 3.2284															

10. *Journal of the American Medical Association*, 1990; 263: 2503-2506.

$\bar{F} = 0.0012$
 $\bar{M} = 0.0012$
 $\bar{F} = 0.0012$
 $\bar{M} = 0.0012$

δ DE TMS = 0.00 ppm
 δ H₂O = 3.47 ppm
 δ CDCl₃ = 7.26 ppm
 δ Me₂SO = 2.50 ppm

VISIBLE EMISSION OBSERVATION FORM

No. RUN # 2

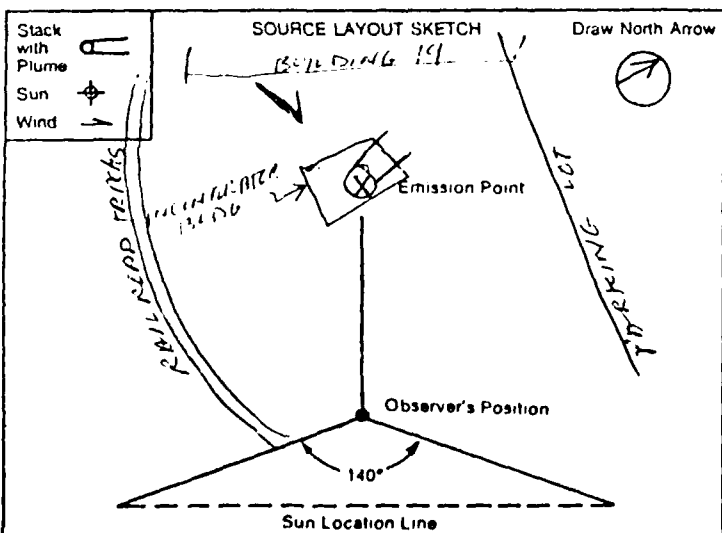
COMPANY NAME <u>GRIFFISS AFB</u>		
STREET ADDRESS		
CITY <u>Rome</u>	STATE <u>NY</u>	ZIP
PHONE (KEY CONTACT)	SOURCE ID NUMBER <u>CLISS. WASTE INCINERATOR</u>	

PROCESS EQUIPMENT <u>2 STAGE INCINERATOR</u>	OPERATING MODE <u>BATCH 300 lb</u>
CONTROL EQUIPMENT <u>NONE</u>	OPERATING MODE

DESCRIBE EMISSION POINT <u>STEEL 3.5' OD STACK WITH CINDER/ASH</u>	
<u>SCREEN APPROX 2' HIGH</u>	
HEIGHT ABOVE GROUND LEVEL <u>25'</u>	HEIGHT RELATIVE TO OBSERVER Start <u>25'</u> End ☒
DISTANCE FROM OBSERVER Start <u>100</u> End	DIRECTION FROM OBSERVER Start <u>NW</u> End

DESCRIBE EMISSIONS Start <u>HEAT WAVES - VISIBLE PLUME AFTER 8:40.</u> End ☒	
EMISSION COLOR Start <u>LIGHT BROWN</u> End ☒	IF WATER DROPLET PLUME Attached ☐ <u>N/A</u> Detached ☐
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED Start <u>5' FROM STACK</u> End	

DESCRIBE PLUME BACKGROUND Start <u>SKY OVERCAST</u> End	
BACKGROUND COLOR Start <u>GRAY</u> End ☒	SKY CONDITIONS Start <u>OVERCAST</u> End ☒
WIND SPEED Start <u>SL</u> End ☒	WIND DIRECTION Start <u>SL</u> End ☒
AMBIENT TEMP Start <u>62</u> End ☒	WET BULB TEMP RH, percent



OBSERVATION DATE 22 SEPT 88		START TIME 1120		END TIME 1150	COMMENTS
SEC	0	15	30	45	
1	0	0	0	0	300 LB CHARGE
2	0	0	0	0	LESS PAPER
3	0	0	0	0	SHEETS, COMPUTER
4	0	5	5	5	PAPER, FORMS ETC
5	5	5	5	5	PLUS APPROX 100 LB
6	5	5	5	5	MICROFICHE.
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	STACK MONITORED
25	0	0	0	0	DURING REMAINDER
26	0	0	0	0	OF STACK TEST,
27	0	0	0	0	SUBSEQUENT VIS
28	0	0	0	0	EMISSIONS
29	0	0	0	0	REMAINED THE
30	0	0	0	0	SAME.

OBSERVER'S NAME (PRINT) <u>JAMES A. GARRISON</u>		DATE <u>22 SEPT 88</u>
OBSERVER'S SIGNATURE <u>James A. Garrison</u>		ORGANIZATION <u>USAFORHL/ECR BROOKS AFB</u>
CERTIFIED BY <u>TEXAS AIR CONTROL BOARD</u>		DATE <u>16 SEPT 88</u>
CONTINUED ON VEO FORM NUMBER		

ADDITIONAL INFORMATION <u>FUEL: NO 2 FUEL OIL</u>
<u>CAPACITY: 500 LB/H</u>

STACK #2 14.12

2. LABORATORY PERFORMING ANALYSIS OEHL			063117			1. REQUESTOR SAMPLE NO CN881266			
SAMPLE COLLECTION INFORMATION						3. DATE RECEIVED BY LAB 702.88		4. DATE ANALYSIS COMPLETED 1702.88	
7. SITE DESCRIPTION 25						ON-SITE ANALYTICAL RESULTS			
8. SITE LOCATION NO		9. FLOWRATE AT SITE 00054 GAL/MIN		10. WEATHER		12. WATER TEMP 00110 °F		16. DISS SOL 00300 MG/L	
11. COLLECTION DATE/PERIOD				12. COLLECTOR'S NAME		14. RESULTS OF OTHER ON-SITE ANALYSES			
13. SAMPLING TECHNIQUE				14. PHONE NUMBER					
15. REASON FOR SAMPLE SUBMISSION NPDES									
ANALYSIS REQUESTED AND RESULTS									
PRESERVATION GROUP A			PRESERVATION GROUP F			PRESERVATION GROUP G			
PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	MG/L
Chemical Oxygen Demand	00340	.	ARSENIC	01001	01002	BORON	01022	.	61
Total Organic Carbon as C	00651	.	BARIUM	01005	01007	BORON, Dissolved	01020	.	61
		.	CADMIUM	01025	01027	CHLORIDE	00940	.	61
PRESERVATION GROUP B			PRESERVATION GROUP F			PRESERVATION GROUP G			
PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	MG/L
OIL & GREASE FREON-IR Method	00500	.	CHROMIUM	01030	01034	COLOR	00080	Units	
		.	CHROMIUM Hexavalent		01031	FLUORIDE	00451	.	
PRESERVATION GROUP C			PRESERVATION GROUP F			PRESERVATION GROUP G			
PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	MG/L
AMMONIA as N	00610	.	COPPER	01040	01042	Residue Filterable (FDS)	00515	.	
NITRATE as N Cd Reduct. Method	00620	.	IRON	01040	01045	Residue Non-Filter (SS)	00530	.	
NITRITE as N	00615	.	LEAD	01049	01051	Residue	00500	.	
TOTAL KJELDAHL NITROGEN as N	00625	.	MANGANESE	01056	01055	Residue Volatile	00505	.	
PHOSPHORUS Ortho PO4 as P	70507	.	MERCURY	71900	71900	Specific Conductance	00095	µmhos	
PHOSPHORUS as P	0665	.	NICKEL	01065	01067	SULFATE as SO4	00945	.	
		.	SELENIUM	01145	01147	SURFACTANTS MBAS as LAS	38200	.	
PRESERVATION GROUP D			PRESERVATION GROUP F			PRESERVATION GROUP G			
PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	MG/L
CYANIDE	00727	.	SILVER	01075	01077	TURBIDITY	00076	Units	
CYANIDE Free, Amenable to Cl2	00721	.	ZINC	01090	01092				
		.	CALCIUM as Ca	00415	00416				
PRESERVATION GROUP E			PRESERVATION GROUP F			PRESERVATION GROUP G			
PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	PARAMETER	TOTAL	MG/L	MG/L
PHENOLS	32737	.	MAGNESIUM as Mg	00925	00927				
		.	POTASSIUM	00925	00927				
		.	SODIUM	00930	00929				
1. ORGANIZATION REQUESTING ANALYSIS Griffiss A.F.B.						CHEMIST JSO			
						REVIEWED BY			
						APPROVED BY [Signature]			

AIR POLLUTION PARTICULATE ANALYTICAL DATA

BASE <i>Griffiss</i>		DATE <i>22 Sept 88</i>		RUN NUMBER <i>THREE</i>	
BUILDING NUMBER <i>Classified Waste Incinerator</i>		SOURCE NUMBER <i>Model CAI-750-MI</i>			
I. PARTICULATES					
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT PARTICLES (gm)		
FILTER NUMBER	<i>.4284</i>	<i>0.2874</i>	<i>.1410</i>		
ACETONE WASHINGS (Probe, Front Half Filter)	<i>103.1077</i>	<i>102.8043</i>	<i>.3034</i>		
BACK HALF (If needed)					
			Total Weight of Particulates Collected <i>4444 gm</i>		
II. WATER					
ITEM	FINAL WEIGHT (gm)	INITIAL WEIGHT (gm)	WEIGHT WATER (gm)		
IMPINGER 1 (H2O)	<i>246.0</i>	<i>200.0</i>	<i>46.0</i>		
IMPINGER 2 (H2O)	<i>206.0</i>	<i>200.0</i>	<i>6.0</i>		
IMPINGER 3 (Dry)	<i>0.0</i>	<i>0.0</i>	<i>0.0</i>		
IMPINGER 4 (Silica Gel)	<i>206.6</i>	<i>200.0</i>	<i>6.6</i>		
			Total Weight of Water Collected <i>58.6 gm</i>		
III. GASES (Dry)					
ITEM	ANALYSIS 1	ANALYSIS 2	ANALYSIS 3	ANALYSIS 4	AVERAGE
VOL % CO ₂	<i>9.4</i>	<i>9.4</i>	<i>9.4</i>		<i>9.4</i>
VOL % O ₂	<i>9.4</i>	<i>9.6</i>	<i>9.6</i>		<i>9.5</i>
VOL % CO					
VOL % N ₂					
Vol % N ₂ = (100% - % CO ₂ - % O ₂ - % CO)					

XROM *METH 5*

RUN NUMBER

3.0000 RUN

METER BOX M?

1.0770 RUN

DELTA H?

.6100 RUN

BAP PRESS ?

30.0200 RUN

METER VOL ?

31.3070 RUN

MTR TEMP ?

77.4000 RUN

% OTHER GAS

REMOVED BEFORE

DRY GAS METER ?

RUN

STATIC HIGH IN ?

-0.0500 RUN

STACK TEMP.

1,443.1700 RUN

ML. WATER ?

50.6000 RUN

% CO2

0.4000 RUN

% OXYGEN?

0.5000 RUN

% CO ?

0.4000 RUN

MOL WT OTHER?

0.0000 RUN

MWD =29.00

MW MET=28.90

SOFT PDS ?

4.4000 RUN

TIME MIN ?

04.0000 RUN

NOZZLE DIA ?

.6540 RUN

STA DIA INCH ?

36.0000 RUN

Run #3

XROM *METH 5*

RUN NUMBER

3.0000 RUN

Page 1 of 2

PARTICULATE SAMPLING DATA SHEET

RUN NUMBER: **THREE**

DATE: **22 Sept 88**

PLANT: **Claymire Wick**

BASE: **Criffiss**

SAMPLE BOX NUMBER: _____

METER BOX NUMBER: _____

Qw/Qm: _____

Co: _____

SCHEMATIC OF STACK CROSS-SECTION

EQUATIONS

$^{\circ}R = ^{\circ}F + 460$

$H = \left[\frac{5130 \cdot F \cdot C_p \cdot A}{C_o} \right]^2 \cdot \frac{T_m \cdot V_p}{T_s}$

$M_{w_0} = 27.5$

$A_{m_0} = 8.0$

$Q_{w_0} = 2.07$

$AP_0 = 1.05$

START

1336 EST

TRAVERSE POINT NUMBER	SAMPLING TIME (min)	STATIC PRESSURE (in H ₂ O)	STACK TEMP		VELOCITY HEAD (Vp)	ORIFICE DIFF. PRESS. (in)	GAS SAMPLE VOLUME (cu ft)	GAS METER TEMP		SAMPLE BOX TEMP (°F)	IMPINGER OUTLET TEMP (°F)
			(°F)	(Ts) (°R)				IN (°F)	OUT (°F)		
A 1	0	2.0	1322		0.00	0.60	286.63	76	76	244	56
2	3.5	2.0	1359		0.01	1.57		76	76	246	56
3	7.0	2.0	1405		0.01	1.55		78	77	247	56
4	10.5	2.0	1423		0.01	1.56		79	76	248	56
5	14.0	2.0	1517		0.01	1.53		79	76	240	55
6	17.5	2.0	1489		0.05	1.27		80	76	242	55
7	21.0	2.0	1475		0.05	1.28		80	76	243	56
8	24.5	2.5	1487		0.15	1.82		84	77	247	56
9	28.0	2.5	1446		0.24	1.11		86	78	243	57
10	31.5	3.0	1476		0.26	1.10		81	77	249	53
11	35.0	3.0	1448		0.24	1.11		81	77	249	54
12	38.5	3.0	1472		0.20	1.16		81	77	250	55
42 Stop											
THREE											

PARTICULATE SAMPLING DATA SHEET												
SCHEMATIC OF STACK CROSS SECTION				EQUATIONS				AMBIENT TEMP				
				$H = \left[\frac{5130 \cdot F \cdot C_p \cdot A}{C_o} \right]^2 \cdot \frac{T_m}{T_s} \cdot V_p$				$OR = ^\circ F + 460$				
								STATION PRESS				
								HEATER BOX TEMP				
								PROBE HEATER SETTING				
								PROBE LENGTH				
								NOZZLE AREA (A)				
								Cp				
								DRY GAS FRACTION (Fd)				
TRaverse POINT NUMBER	SAMPLING TIME (min)	ST. PRESS (in H ₂ O)	STACK TEMP (°F)	STACK TEMP (°R)	VELOCITY HEAD (Vp)	ORIFICE DIFF. PRESS. (H)	GAS SAMPLE VOLUME (cu ft)	IN (°F)	AVG (Tm) (°R)	OUT (°F)	SAMPLE BOX TEMP (°F)	IMPINGER OUTLET TEMP (°F)
1	0	2.0	1326		0.001	0.006	302.478	77		73	747	57
2	3.5	2.0	1406		0.001	0.57		77		73	250	57
3	7	2.0	1436		0.001	0.56		77		73	226	57
4	10.5	2.0	1436		0.012	0.68		76		74	230	57
5	14	2.0	1403		0.012	0.57		76		74	236	57
6	17.5	2.0	1403		0.010	0.11		77		76	243	61
7	21	2.0	1445		0.002	0.42		78		76	246	62
8	24.5	2.5	1537		0.008	0.54		80		76	252	62
9	28	2.5	1504		0.010	0.80		81		77	252	62
10	31.5	2.5	1516		0.015	0.86		81		77	252	62
11	35	2.5	1587		0.015	0.65	317.470	81		77	252	62
12	38.5	2.5	1487		0.012		296.163			71		
$TPSTS = 4.40$												
$T_s = 1443.17$												
$T_m = 77.4$												
$\Delta H = 0.60$												

Post leak check

TPH Cu FE = 31307

VISIBLE EMISSION OBSERVATION FORM

No. 1204 # 3

COMPANY NAME GRIFFISS AFB		
STREET ADDRESS		
CITY ROME	STATE NY	ZIP
PHONE (KEY CONTACT)	SOURCE ID NUMBER CLASS WASTE INCINERATOR	

PROCESS EQUIPMENT 2 STAGE INCINERATOR	OPERATING MODE BATCH 300 lb
CONTROL EQUIPMENT NONE	OPERATING MODE

DESCRIBE EMISSION POINT STEEL 3.5' OD STACK WITH LINER/ASIT	
SCREEN APPROX 2' HIGHER	
HEIGHT ABOVE GROUND LEVEL 28'	HEIGHT RELATIVE TO OBSERVER Start 28' End
DISTANCE FROM OBSERVER Start 100 End ☒	DIRECTION FROM OBSERVER Start S End ☒

DESCRIBE EMISSIONS Start LT BROWN WITH VISIBLE End ☒	
EMISSION COLOR Start LT BROWN End ☒	IF WATER DROPLET PLUME Attached ☐ N/A Detached ☐
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED Start 13' FROM STACK End ☒	

DESCRIBE PLUME BACKGROUND Start OVERCAST SKY - NO HAZE End ☒	
BACKGROUND COLOR Start GRAY End ☒	SKY CONDITIONS Start OVERCAST End ☒
WIND SPEED Start 5K End ☒	WIND DIRECTION Start WEST End ☒
AMBIENT TEMP Start 61 End ☒	WET BULB TEMP RH, percent

Stack with Plume	SOURCE LAYOUT SKETCH		Draw North Arrow
Sun			
Wind			

ADDITIONAL INFORMATION FUEL: NO 2 FUEL OIL CAPACITY: 500 lb/hr
--

OBSERVATION DATE 22 SEPT 88				START TIME 1340	END TIME 1410
SEC	0	15	30	45	COMMENTS
1	0	0	0	0	300 lb. CHARGE
2	5	5	5	5	LOGIC PROPER, COMPUTE
3	0	0	0	5	12 TC
4	5	5	5	5	
5	5	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	STACK MONITORED
25	0	0	0	0	FOR REMAINDER OF
26	0	0	0	0	STACK TEST:
27	0	0	0	0	SUBSEQUENT VIS.
28	0	0	0	0	EMISSIONS REMAIN
29	0	0	0	0	THE SAME.
30	0	0	0	0	

OBSERVER'S NAME (PRINT) JAMES A. GARRISON		DATE 22 SEPT 88
OBSERVER'S SIGNATURE James A. Garrison		ORGANIZATION USAFORTH/ECR, BROOKS AFB TX.
CERTIFIED BY TEXAS AIR CONTROL BOARD		DATE 16 SEPT 88

2. LABORATORY PERFORMING ANALYSIS

CEHL

063118

STACK RUN #3

17.1

REQUESTOR SAMPLE NO

LN 88/1267

00029

SAMPLE COLLECTION INFORMATION

7. SITE DESCRIPTION

7 001 15 25

8. DATE RECEIVED BY LAB

7 Oct. 88

9. DATE ANALYSIS COMPLETED

17 Oct. 88

ON-SITE ANALYTICAL RESULTS

10. SITE LOCATION NO

11. FLOWRATE AT SITE
00256
GAL/MIN

12. WEATHER

13. WATER TEMP
0010
°C14. F.W.
0040
UNITS15. DISS O₂
0030
MG/L

16. COLLECTION DATE PERIOD

17. COLLECTOR NAME

18. RESULTS OF OTHER ON-SITE ANALYSES

19. SAMPLING TECHNIQUE

20. PHONE NUMBER

21. REASON FOR SAMPLE SUBMISSION

NPDES

ANALYSES REQUESTED AND RESULTS

063118

291

PRESERVATION GROUP A

PARAMETER	TOTAL	MG/L
Chemical Oxygen Demand	01340	.
Total Organic CARBON as C	0064	.

PRESERVATION GROUP B

PARAMETER	TOTAL	MG/L
OIL & GREASE FREDON-IR Method	00507	.

PRESERVATION GROUP C

PARAMETER	TOTAL	MG/L
AMMONIA as N	00610	.
NITRATE as N Cd Reduct. Method	00620	.
NITRITE as N	00615	.
TOTAL KJELDAHL NITROGEN as N	00625	.
PHOSPHORUS Ortho PO ₄ as P	70507	.
PHOSPHORUS as P	00665	.

PRESERVATION GROUP D

PARAMETER	TOTAL	MG/L
CYANIDE	00727	.
CYANIDE Free, Amenable to Cl ₂	00721	.

PRESERVATION GROUP E

PARAMETER	TOTAL	MG/L
PHENOLS	32737	.

PRESERVATION GROUP F

PARAMETER	TEST	TOTAL	MG/L
ARSENIC	01006	01002	.
BARIUM	01005	01007	.
CADMIUM	01025	01027	.
CHROMIUM	01030	01034	.
CHROMIUM Hexavalent		01032	.
COPPER	0104	01042	.
IRON	01047	01045	.
LEAD	01049	01051	.
MANGANESE	01056	01055	.
MERCURY	71890	71900	.
NICKEL	01065	01067	.
SELENIUM	01145	01147	.
SILVER	01075	01077	.
ZINC	01090	01092	.
CALCIUM as Ca	00915	00916	mg/l
MAGNESIUM as Mg	00925	00927	mg/l
POTASSIUM	00935	00937	mg/l
SODIUM	00930	00929	mg/l

PRESERVATION GROUP G

PARAMETER	TOTAL	MG/L
BORON	01022	mg/l
BORON, Dissolved	01020	mg/l
CHLORIDE	00940	64
COLOR	00080	Units
FLUORIDE	00951	.
Residue Fil- terable (TDS)	00515	.
Residue Non- Filt (SS)	00530	.
Residue	00500	.
Residue Volatile	00505	.
Specific Conductance	00095	µmhos
SULFATE as SO ₄	00945	.
SURFACTANTS MPAS as LAS	38260	.
TURBIDITY	00076	Units

1. ORGANIZATION REQUESTING ANALYSIS

Griffiss & F.B.

CHEMIST

J30

REVIEWED BY

APPROVED BY

D. J. J. J.

APPENDIX E
Calibration Data

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NOZZLE CALIBRATION DATA FORM

Wright Patterson

Date Dec 85 Calibrated by Cavan

Nozzle identification number	Nozzle Diameter ^a			ΔD , ^b mm (in.)	D_{avg} ^c
	D_1 , mm (in.)	D_2 , mm (in.)	D_3 , mm (in.)		
	.6524	.654	.653	.652 .001	.654

where:

^a $D_{1,2,3}$ = three different nozzles diameters, mm (in.); each diameter must be within (0.025 mm) 0.001 in.

^b ΔD = maximum difference between any two diameters, mm (in.),
 $\Delta D \leq (0.10 \text{ mm}) 0.004 \text{ in.}$

^c D_{avg} = average of D_1 , D_2 , and D_3 .

Quality Assurance Handbook M5-2.6

METER BOX CALIBRATION DATA AND CALCULATION FORM

(English units)

Date 12 Jul 88

Meter box number 2010 NUTECH

Barometric pressure, $P_b =$ 29.119 in. Hg Calibrated by Fagin & Scott

Orifice manometer setting (ΔH), in. H_2O	Gas volume		Temperature				Time (θ), min	Y_i	$\Delta H\theta$ in. H_2O
	Wet test meter (V_w), ft^3	Dry gas meter (V_d), ft^3	Wet test meter (t_w), $^{\circ}F/R$	Dry gas meter					
				Inlet (t_{d_i}), $^{\circ}F/R$	Outlet (t_{d_o}), $^{\circ}F/R$	Avg. (t_d), $^{\circ}F/R$			
0.5	5	4.668	78 79 538	76 83 539.5	78 78 536.5	538	13.1	1.070	2.010
1.0	5	4.674	78 78 538	84 81 546.5	78 81 539.5	543	9.3	1.078	2.008
1.5	10	9.390	78 78 538	90 96 553	82 86 544	548.5	15.5	1.082	2.070
2.0	10	9.455	79 80 539.5	96 101 558.5	87 90 548.5	553.5	13.5	1.070	2.087
3.0	10	9.470	80 81 540.5	101 106 563.5	90 93 559.5	557.5	11.1	1.081	2.109
4.0	10.1	9.590	81 81 541	106 109 567.5	94 96 555	561.3	9.8	1.082	2.138
							Avg	1.077	2.070

ΔH , in. H_2O	$\frac{\Delta H}{13.6}$	$Y_i = \frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\Delta H\theta_i = \frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) \theta}{V_w} \right]^2$
0.5	0.0368	$Y_1 = \frac{(5)(29.119)(538)}{(4.668)(29.119 + \frac{0.5}{13.6})(538)}$	$H\theta_1 = \frac{(0.0317)(0.5)}{29.119(538)} \left[\frac{(538)(13.1)}{5} \right]^2$
1.0	0.0737	$Y_2 = \frac{(5)(29.119)(543)}{(4.674)(29.119 + \frac{1.0}{13.6})(543)}$	$H\theta_2 = \frac{(0.0317)(1)}{29.119(543)} \left[\frac{(538)(9.3)}{5} \right]^2$
1.5	0.110	$Y_3 = \frac{(10)(29.119)(548.5)}{(9.390)(29.119 + \frac{1.5}{13.6})(548.5)}$	$H\theta_3 = \frac{(0.0317)(1.5)}{29.119(548.5)} \left[\frac{(538)(15.5)}{10} \right]^2$
2.0	0.147	$Y_4 = \frac{(10)(29.119)(553.5)}{(9.455)(29.119 + \frac{2.0}{13.6})(553.5)}$	$H\theta_4 = \frac{(0.0317)(2.0)}{29.119(553.5)} \left[\frac{(539.5)(13.5)}{10} \right]^2$
3.0	0.221	$Y_5 = \frac{(10)(29.119)(557.5)}{(9.470)(29.119 + \frac{3.0}{13.6})(557.5)}$	$H\theta_5 = \frac{(0.0317)(3)}{29.119(557.5)} \left[\frac{(540.5)(11.1)}{10} \right]^2$
4.0	0.294	$Y_6 = \frac{(10.1)(29.119)(561.3)}{(9.590)(29.119 + \frac{4.0}{13.6})(561.3)}$	$H\theta_6 = \frac{(0.0317)(4)}{29.119(561.3)} \left[\frac{(541)(9.8)}{10.1} \right]^2$

^a If there is only one thermometer on the dry gas meter, record the temperature under t_d .

POSTTEST DRY GAS METER CALIBRATION DATA FORM (English units)

Test numbers 1, 2, 3 Date 17 Oct 88 Meter box number Nutech Plant Griffiss (Post)
 Barometric pressure, $P_b = 29.305$ in. Hg Dry gas meter number Rockwell Pretest Y 1.077 ($\pm .0539$)

Orifice manometer setting, (ΔH), in. H_2O	Gas volume		Temperature			Time (θ), min	Vacuum setting, in. Hg	Y_i	$V_w P_b (t_d + 460)$ $V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)$
	Wet test meter (V_w), ft^3	Dry gas meter (V_d), ft^3	Wet test meter (t_w), $^{\circ}F$	Inlet (t_d), $^{\circ}F$	Outlet (t_d), $^{\circ}F$				
$\phi .6$	10	9.252	76 536	76 541	77 541.5	23.40	4.0	1.090	$60(29.305)(541.25)$ $9.252(29.305 + \frac{1.090}{13.6})(536)$
$\phi .6$	10	9.277	76 536	76 545	83 544.5	24.10	4.0	1.095	$60(29.305)(545.0)$ $9.277(29.305 + \frac{1.095}{13.6})(536)$
$\phi .6$	10	9.317	76 536	76 548	84 544.5	25.6	4.0	1.091	$60(29.305)(545.75)$ $9.317(29.305 + \frac{1.091}{13.6})(536)$
								$Y = 1.092$	

^a If there is only one thermometer on the dry gas meter, record the temperature under t_d .

V_w = Gas volume passing through the wet test meter, ft^3 .
 V_d = Gas volume passing through the dry gas meter, ft^3 .
 t_w = Temperature of the gas in the wet test meter, $^{\circ}F$.
 t_{d_i} = Temperature of the inlet gas of the dry gas meter, $^{\circ}F$.
 t_{d_o} = Temperature of the outlet gas of the dry gas meter, $^{\circ}F$.

t_d = Average temperature of the gas in the dry gas meter, obtained by the average of t_{d_i} and t_{d_o} , $^{\circ}F$.
 ΔH = Pressure differential across orifice, in H_2O .

Y_i = Ratio of accuracy of wet test meter to dry gas meter for each run.
 Y = Average ratio of accuracy of wet test meter to dry gas meter for all three runs;
 tolerance = pretest $Y \pm 0.05Y$

P_b = Barometric pressure, in. Hg.
 θ = Time of calibration run, min.

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