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FLAMMABILITY OF AIRCRAFT HYDRAULIC FLUIDS — A BIBLIOGRAPHY

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FLAMMABILITY OF AIRCRAFT HYDRAULIC FLUIDS - A BIBLIOGRAPHY (CRC Project No. CA-49-71)

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Prepared by the

Aviation Fluids Flammability Group



January 1986

Aviation Fuel, Lubricant, and Equipment Research Committee of the

Coordinating Research Council, Inc.

ABSTRACT

As part of an overall effort to collect flammability data on aircraft fluids, a critical survey was made of the aircraft hydraulic oil literature, with particular emphasis on flammability testing and flammability characteristics of existing and projected aircraft hydraulic fluids. Commercial aviation and military aviation fluids are treated separately, in view of their divergent development. Flammability test procedures are described. Flammability test results and other inspection tests are given for a variety of current and proposed aircraft hydraulic fluids.

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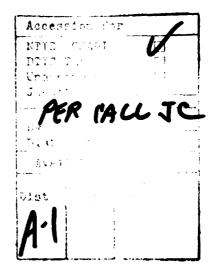


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I. BACKGROUND AND HISTORY

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As part of an overall effort to collect flammability data on aircraft fluids, a critical survey of the aircraft hydraulic oil literature was made by the Aviation Fluids Flammability Group of Coordinating Research Council, Inc. (CRC). Membership of the Group is detailed in Appendix A. Particular emphasis has been placed on flammability testing and flammability characteristics of existing and projected aircraft hydraulic fluids. Commercial aviation and military aviation fluids have been treated separately in the survey, in view of their divergent development.

For many years, hydraulic fluid power has been used effectively and efficiently to provide power transfer in complex hydraulic systems due to the extremely high efficiency, compact size, and light weight of hydraulic systems when compared with alternative methods including mechanical or electrical devices. Typical aircraft systems utilizing hydraulic power include primary flight controls and utility systems such as landing gears, brakes, accessory doors, and many others. The most widely used fluid in military aircraft over the last thirty-five years has been a light mineral-oil base meeting specification MIL-H-5606⁽¹⁾. This fluid or its preservative version, MIL-H-6083⁽²⁾, has provided excellent service over a temperature range of -54 to 135°C. The primary deficiency of this oil has been its high degree of flammability.

The flammability of MIL-H-5606 has prompted many government and private research programs to develop fluids of improved flammability characteristics. The most successful program of these years was the development and adoption of phosphate ester-based, fire-resistant hydraulic oils generally employed in today's jet-powered commercial aircraft(3,4). The phosphate esters have significantly improved resistance to ignition and flame propagation over the petroleum-based fluid; however, the different chemical characteristics of the phosphate esters make them incompatible with the elastomeric seals, wiring insulation, and various coatings developed for petroleum-based oils. Different materials for these purposes are thus required for compatibility with the phosphate esters. In addition, phosphate ester fluids are not capable of operating at the higher temperatures found in some military aircraft hydraulic systems. Silicate esters, another fluid type having better high-temperature oxidation stability than the phosphate esters, but also incompatible with petroleum oil systems, are employed in the supersonic Concorde (5). Silicate esters meeting MIL- $H-844\tilde{6}^{(6)}$ have also been employed in some military aircraft, but are no longer utilized because of hydrolytic stability problems.

While commercial aviation was able to adopt fluids requiring new system materials because of wholesale fleet replacements, the military, with a large inventory of existing aircraft, was unable to go the same route $^{(7)}$. One special high-temperature mineral oil, MIL-H-27601⁽⁸⁾, was developed for high-speed, high-temperature applications, but its poor low-temperature properties prevented its general adoption. In the early 1970's, a hydraulic fluid based on poly-alpha olefins with suitable additives, MIL-H-83282⁽⁹⁾, was developed by the US Air Force and private industry and flight tested by the US Navy to replace the more flammable MIL-H-5606 oil. The US Army developed a rust-inhibited version, MIL-H-46170⁽¹⁰⁾, to replace the corresponding MIL-H-6083 oil. Both fluids are completely compatible with systems currently serviced with petroleum-based fluids, and can be used in all mixture ratios with the petroleum fluids. The poly-alpha olefin based fluids are replacing the MIL-H-5606 type fluids in many military applications.

II. FLAMMABILITY HAZARD ASSESSMENT

Flammability testing of aircraft fluids continues to be empirical, because no single fundamental property adequately describes the flammability characteristics of a fluid. It is, therefore, necessary to analyze the hazard environment, and then to relate the results of various tests to that environment. The assessment of flammability hazards should address at least the following parameters:

Fluid Exposure

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Fluid system pressures and temperatures

Environmental air temperature, pressure, and velocity

Possible modes of fluid exposure such as misting, pooling, or wick material absorbancy

Ignition Sources

Type of source such as open flame, hot surface, or electric spark

Energy level of the ignition source

Location of ignition source

Size and shape of ignition source

Extreme temperatures in some modern military systems are illustrated in Table I which lists maximum bulk and surface temperatures experienced in different locations of various aircraft $^{(11,12)}$. The extreme temperatures of modern braking systems are obvious.

In addition to analyzing the above parameters during the design and testing of hydraulic systems, reductions in flammability hazards depend heavily upon investigations of accidents caused by hydraulic fluids. Such investigations pinpoint the most frequent sources of problems and can serve to prioritize changes. Sometimes, hazards can be reduced by parts redesign or relocation; however, performance requirements or material limitations often mitigate against such changes, and highlight the need for fluids with improved flammability characteristics.

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The results of accident investigations by various branches of the US Government have thus pointed out the need for better flammability features than exist in hydraulic oils meeting MIL-H-5606. (12) US Air Force and US Navy⁽¹³⁾ studies of non-combat fires between 1965 and 1975 are summarized in Table II. More detailed results of the studies are given in Appendix B. Out of some 3600 US Air Force and 2500 US Navy fires over the eleven-year period, 101 US Air Force and 101 US Navy fires were directly attributed to hydraulic fluid (MIL-H-5606), and another 184 US Air Force and 33 US Navy indicated hydraulic fluid involvement. The uncertainty arises from the fact that, depending upon the severity of the accident, pinpointing the exact cause may be very difficult, particularly since more than one combustible fluid is often involved in a fire. A further breakdown of data in Table III shows the wheel-well area to be very susceptible to hydraulic oil These tend to occur during landings or aborted takeoffs, due to maximum hydraulic system pressures and the very high temperatures reached on the braking surfaces. When hot engine surfaces in the nacelle are included in the analysis, some 80 percent US Air Force and 68 percent US Navy hydraulic fluid fires were the result of a hot surface acting as the ignition source. This is the type of information vital to giving direction to hydraulic fluid development and flammability test design. It also becomes reasonable to conclude that sprays on hot surfaces are an important test parameter to be addressed in hydraulic-fluid flammability abatement studies.

On the other hand, a survey⁽¹⁴⁾ of FAA Service Difficulty Reports, covering commercial jet transports operating in the US over the period 1975 to March 1984, disclosed a total of four reported "fires" involving hydraulic systems. (All such transports used phosphate ester fluids in the time period.) In two incidents, electrical sparks apparently ignited hydraulic fluid, one in a rear stairs compartment, the other in the wheel-well area. In another incident, smoke evolved from a hot engine surface; while in the fourth case, a hydraulic leak was involved, along with an overheat alarm, with no evidence of fire.

III. FLAMMABILITY TESTING

Aircraft accident investigations have indicated hydraulic oil fires usually are complex events, with the possibility of several release modes and several ignition sources. Quite often, hydraulic fluid is sprayed at high pressure, followed by leaking or seeping, forming pools of liquid. Liquid may be absorbed by porous materials such as insulation. The sprays, as well as the pools, may be exposed to hot surfaces, sparks, or open flames. Accurate assessment of a hydraulic fluid's flammability, therefore, cannot be established with a single test procedure, although testing may be simplified once major hazards have been identified. Flammability tests are often designed to incorporate specific parameters such as fluid pressure, hot surface temperature, and a specific ignition source, because these variables are intended to duplicate or closely relate to a field problem situation. On the other hand, fluid specifications usually include simpler, standardized flammability tests used primarily for manufacturing control. To better understand flammability characteristics of hydraulic fluids, a brief description of various flammability test methods follows, along with the significance of the method.

A. Flash Point and Fire Point

The flash point is the minimum temperature which a fluid must attain to generate sufficient vapor to ignite in the application of a small flame in a specific apparatus under closely controlled conditions. The fire point is the minimum temperature (usually higher than the flash point) at which ignition and continued burning take place. The most commonly specified flash and fire tester for hydraulic fluid is the Cleveland Open Cup, ASTM Test Method D $92^{(15)}$; however, MIL-H-5606E requires the Pensky Martens Closed Tester, ASTM Test Method D $93^{(15)}$.

The usefulness of flash point/fire point data is limited by the fact that they are based entirely upon vapor evolution, and are obtained under quiescent conditions at a fixed vapor-to-liquid volume ratio. Investigations⁽¹⁶⁾ have shown, however, that the flash point temperatures of petroleum products, particularly those of fuels, mark a relatively narrow transition region above which the flame speed over a pool of the fluid increases by several orders of magnitude. The flash test is also useful in the detection of hydraulic oil contamination by more flammable fluids.

B. Autoignition

Spontaneous ignition of a flammable fluid in the presence of an oxidant occurs only when the temperature is at or above that required to generate heat by oxidation at a rate which is greater than the rate of dissipation of this heat to the surroundings⁽¹⁷⁾. Autoignition has been defined as the ignition of a material commonly in air as the result of heat liberation due to an exothermic oxidation reaction in the absence of an external ignition source such as a spark or a flame (18). The autoignition temperature (or AIT) is the temperature at which autoignition occurs under the specified conditions of the procedure. test, a small quantity of liquid is injected and vaporized in a quiescent, uniformly heated, air-filled container. Time delays between injection and ignition are recorded as part of the results, and maximum ignition delays are specified in the procedure. If no reaction occurs, the unit is purged, the temperature is raised, and fluid is again injected. This process is repeated until ignition is observed. Cool flame reactions are also noted on occurrence. Standard AIT tests were formerly conducted per ASTM Test Method D 2155, which was replaced in 1980 by the revised procedure ASTM Test Method E $659^{(18)}$.

Test results obtained by this procedure should be used with caution because of apparatus and test condition effects (19). Results are influenced by apparatus size (larger vessels give lower results) and by the vessel material which may have catalytic effects. Vessel pressure and oxygen concentration have major effects on AIT, with pressures above atmospheric resulting in the lowering of AIT. Also, the test measures only vapor ignitability. The primary usefulness of the test is to furnish a relative rating scale, rather than produce absolute values which can be directly applied to problem solutions.

C. Hot Surface Ignition

To overcome some of the AIT test shortcomings, a number of "dynamic" tests have been developed. All include a heated metal surface and a method of delivering fluid to the hot surface. In some procedures, air is swept over the hot surface at controlled velocity and pressure. In the Hot Manifold Test per modified Federal Test Method 791B, Method 6053⁽²⁰⁾, illustrated in Figure 1, 10 ml of fluid is dripped with a buret at a flow rate of 10-15 ml/min on a 3-inch diameter stainless-steel tube heated to 704°C. This method has been modified by one researcher(21) to include sprays at varying pressure and a variety of atomizing nozzles. In a facility illustrated in Figure 2, another investigator (22) has used differing hot surface shapes, as well as varying air flows, to obtain differing residence times and differing test results. The same investigator has also examined the effect of two different metal compositions. Still others (23) have designed equipment to reach surface temperatures as high as 1649°C with induction-heated graphite specimens.

It can be argued that the closer the test equipment and operation approaches the real-life situation, the higher the reliability of the results. Such an approach may have to be taken in the early investigation of a major problem, and full-scale high-temperature brake tests have been conducted (11,24). Other investigators simulated fluid leakage into a closed, high-temperature compartment (24), studied pressure and volume effects in an actual aircraft compartment (26), or used a small wind tunnel to relate laboratory tests to design factors (28). High experimental costs tend to curb such approaches, however, and they are not necessarily feasible for engines or aircraft still in the design stage. Attempts to relate large-scale test results to smallscale laboratory procedures are limited by the heterogeneity of the air/fluid mixtures in all these experiments. Several investigators (22,23,27) point out that it is the temperature of a critical air/fluid vapor mixture which determines ignition, rather than the temperature of the igniting surface; however, very few of the tests are able to measure temperatures in these vapor zones which are seldom stationary.

D. Flame Propagation

In fluid flammability safety studies, flame propagation often refers to "pool burning," or burning above a liquid layer typical of a spill. The propagation of a flame, after ignition, can be very slow or fast enough to cause detonation depending upon a number of factors, including the composition of the fluid, bulk fluid temperature, air velocity, and other factors. The speed with which the flame front travels above the quiescent liquid is directly related to the vaporization characteristics of the fluid, with drastic increases of flame speed when fluid temperatures are above the fluid's flash point (29,30). This phenomenon is illustrated in Figure 3 for several fuels. Because only vaporized fluid can be ignited and burned, the low volatility of most hydraulic fluids usually tends to prevent pool burning.

Under certain conditions, however, even very low volatility fluids will maintain a steady flame once ignited. In one such test, the liquid is absorbed on a porous substrate or wicking material and ignited. A schematic of the apparatus is shown in Figure 4. The procedure takes advantage of the decrease in fluid viscosity adjacent to the flame to promote wicking and reduce the required ignition source intensity. This type of test, of course, is the equivalent of a wax candle. Several variations of this approach are being used to measure comparative propagation rates of fluids with a variety of non-combustible substrates, including ceramic fiber cord (9), or asbestos string wicks (7). Results from these tests can rate the relative ability of hydraulic fluids to sustain a flame when insulation or some other porous material has become soaked with the fluid and is ignited by a flame or fire.

In a different evaluation of flame propagation, hydraulic fluid is sprayed from a nozzle under designated conditions. A flame, usually fed by oxy-acetylene, is moved into the spray a prescribed distance away from the nozzle, and the tendency of the spray to ignite and maintain a flame after removal of the ignition source is measured. Such a procedure is described in Federal Test Method 791B, Method $6052^{(31)}$. A recent study $^{(32)}$ systematically investigated the parameters of this procedure and noted that air velocity, fluid temperature, and nozzle pressure all required close control. Spray nozzles should be standardized and preselected for improved test precision. Ambient air temperature appeared to have little effect on test results.

A test which measures the effect of evaporation on flammability is described in Federal Test Method Standard 791B, Method 352⁽³³⁾. An absorbent wick, soaked in the test fluid, is repeatedly passed through a flame. The test criterion is the average number of cycles necessary for a self-sustaining flame to be established.

E. Ignition Sources

Aside from the above-mentioned hot surfaces and oxy-acetylene flames, one author $^{(19)}$ summarizes the effect of hot wire and hot gas ignition sources in terms of heat-source diameter, in that ignition temperatures decrease with increasing heat-source diameter. Ignition temperature differences between these ignition sources were noted below source diameters of 2.5 mm. Other ignition sources used to evaluate military fluids include ballistic rounds of various types $^{(24)}$.

F. Heat of Combustion

The heat of combustion or specific energy is not directly related to a potential hazard, and is not a measure of flammability. It is a measure of the heat generated during combustion after ignition and is, therefore, considered a significant factor in the overall flammability characteristics of a fluid. The higher the heat of combustion, the greater the energy releases into the bulk fluid while it is burning. Heat of combustion is normally determined by ASTM Test Method D $240^{\left(34\right)}$.

IV. FLAMMABILITY CHARACTERISTICS OF HYDRAULIC FLUIDS

As pointed out earlier, the flammability of hydraulic oils is checked by a battery of tests, not all of which are fully standardized. Table IV presents such a listing for hydraulic fluids in current use. The results reflect that, for a given fluid, an improvement in one test does not necessarily cause similar improvements in other flammability characteristics. Thus, while the alpha-olefin fluid meeting MIL-H-83282 had an AIT some 80°C higher than the MIL-H-5606 oil, its hot manifold ignition temperature was 66°C below that of the MIL-H-5606 product. These results follow earlier findings $^{(19)}$ that more volatile products tend to have higher hot surface ignition temperatures than less volatile fluids of similar chemical composition. On the other hand, careful control of test parameters in the spray/oxy-acetylene test showed a significant difference between these two fluids in favor of the alpha-olefins $^{(32)}$. AIT and hot manifold minimum ignition temperatures on a wide variety of fluids are given in Appendix C.

As a result of the findings with the alpha-olefin type products, the Air Force has issued the flammability criteria for new technology hydraulic fluids shown in Table V. $^{(24,25)}$ Criterion A was developed to insure nonignition of the hydraulic fluid when exposed to all anticipated ignition sources aboard current and future aircraft. Criterion B covers all anticipated ignition sources except overheated carbon brakes resulting from an emergency rejected takeoff. Test results for two experimental materials are compared with the near term goals of Criterion B in Table VI. The two fluids are a tetrachlorophenylmethyl siloxane (Nadraul MS-6) $^{(13)}$ and a chlorotrifluoroethylene oligomer (CTFE) $^{(25)}$. The reduction in flammability over existing fluids is noteworthy.

The performance of differing fluids in a dynamic hot surface $test^{(22)}$ is illustrated in Figure 5. In this procedure, the fluid is sprayed on the heated surface from a high-pressure nozzle, while air velocity is varied from 0.8 to about 40 meters per second. The marked effect of air velocity on ignition temperature is noteworthy, as are the significant differences among the fluids tested. Changing metal composition from stainless steel (Figure 5) to titanium decreased ignition temperatures 25 to 75°C in the same test, as illustrated in Figure 6.

The American Standards Institute (ANSI) and the International Standards Organization (ISO) have developed a classification system of fire-resistant hydraulic oils. Except for one category, these "oils" contain water and/or glycol, and are not suitable for aircraft. A description of the classification system can be found in Appendix D.

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FIGURES

TABLE I

TYPICAL MAXIMUM OPERATIONAL TEMPERATURES IN MILITARY AIRCRAFT*

(All Temperatures in °C)

0i1	Bulk	Tempera	tures

<u>Aircraft</u>			Temperatures
F-104	F-111	AWACS	
F-105	A-7	HH-53B	Between 107 and 135
F-106	F-15	B-1	

Brake Temperatures

<u> Aircraft</u>	Normal_	Rejected Takeoff
F-15 and C5A (Beryllium)	200 - 260	650
F-16 (steel brakes)	370 - 430	1260
B-1 (carbon brakes)	600 - 650	1650

Engine Temperatures

Aircraft	Forward of Firewall	Aft of Firewall	Accessory
F-4, F-5, F-105, A-10		700	
B-1, F-15, F-16	260 max.		
C-5		700	400
C-141		650	410

^{*} Taken from Reference 12.

TABLE II

MILITARY HYDRAULIC FIRE SUMMARY NON-COMBAT EXPERIENCE*

Fire History	1965 -	<u> 1970 - 1975</u>	
	USAF	USN	USAF
Total Non-Combat Fires	3634	2500	1807
Hydraulic Fluid Related	101	101	46
Other (fuel, tires, electrical, etc.	3533**	2399***	1761****

^{*} Taken from Reference 12.

^{** 184} may have been hydraulic fluid related.

^{*** 33} may have been hydraulic fluid related.

^{**** 25} may have been hydraulic fluid related.

TABLE III

MILITARY HYDRAULIC FLUID IGNITION SOURCE HISTORY

NON-COMBAT EXPERIENCE*

	1965 -	1975	1970-1975	1975- <u>March 1978</u>
	USAF	USN	USAF	USAF
Hot Surface Ignition				
Engine	39	33	13	3
Brakes	36	20	21	11
Bleed Air Ducts	2	0	0	0
Other	3	15	12	2
Runway Friction Sparks	9	0	-	2
Engine Ingestion	3	0	-	0
Electrical Arcing	2	16	-	4
Combustor Burn-Through	1	0	-	0
Unknown	6	15	-	4
Incendiary	0	2	-	-

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AND PRODUCED TOURSESS PRODUCES PRODUCES PRODUCES PRODUCES PRODUCES PRODUCES AND PRODUCES PRODUCES AND PRODUCES PRODUCES

^{*} Taken from Reference 12.

TABLE IV

FLAMMABILITY OF CURRENT HYDRAULIC FLUIDS*

(All Temperatures in °C)

Test	Test Method	MIL-H-5606	MIL-H-83282	Phosphate Esters**	Silicate Esters***
Flash Point, Open Cup	ASTM D 92	99	224	182	215
Auto-Ign. Temp.	ASTM D 2155	241	371	510	404
Linear Flame Propagation Rate, cm/sec	MIL-H-83282	0.76	0.33	-	-
Hot Manifold Ign.					
Drip	FS 791-6053	430	315	780	-
High Press Spray	FS 791-6053 [#]	816*	816*	-	-
High Press Spray	FS 791-6053	760**	700**	815**	-
Spray Ign. Temp.	AMS 315°C				
Low Pressure	(SAE)	increases flame	carries flame	extinguishes flame	s -
High Pressure	co	ignites & intinues to bur	ignites, s n extinguish		-
Heat of Combus., kJ/kg	ASTM D 240	4.2×10^4	4.2×10^4	3.0×10^4	-

^{*} Taken from Reference 13.

^{**} Taken from Reference 24.

^{***} Taken from Reference 5.

[#] Same spray conditions as used in AMS 3150C, high pressure spray.

TABLE V

US AIR FORCE FLAMMABILITY CRITERIA FOR

NONFLAMMABLE HYDRAULIC FLUID*

Requirement	Test Method (Re	Criterion A ejected Takeoff)	Criterion B (Minimum Acceptable)
Heat of Combustion	ASTM D 240	0 kJ/kg	1.16 x 10 ⁴ kJ/kg
Hot Manifold Ign.	Modified Fed. Method Std. 791, Method 6053**	1650°C (3000°F)	930°C (1700°F)
Min. Autogenous Ignition Temp.	ASTM E 659 Modified to include air circulation	1430°C (2600°F)	700°C (1300°F)
Atomized Fluid Flammability Test	020.7×10 ⁵ Pa and 17 <u>+</u> 6°C		
(a) Arc/Spark	6 J and 20 kV	Fluids may f self-ext	lash but must inguish
(b) Propane/Air Flame	15-1/4 cm high flame premixed stoichiometric propane air flame from 1.9 cm ID burner	back to nozz extinguishin	g when ignition
(c) Incendiary Ignition	-	Fluids may f self-ext	lash but must inguish

^{*} Taken from References 24 and 25.

^{**} Taken from Reference 21.

TABLE VI

FLAMMABILITY OF CANDIDATE AIRCRAFT HYDRAULIC FLUIDS*

Test	Near Term Goal	Siloxane (Nadraul MS-6)	CTFE
Heat of Combustion	<2.78 cal/g	5.41	1.33
Auto Ignition Temperature, °C	>705	410	643
Hot Manifold Ignition, °C			
Stream	>927	482	927
Spray	>927	538	>927
Atomized Spray, Open Flame, °C	non-reactive	extinguishes	non-reactive

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^{*} Taken from Reference 24.

TABLE VII

TYPICAL TESTS FOR COMMERCIAL AIRCRAFT HYDRAULIC FLUIDS

	P	Silicate Ester		
Test	Skydrol LD-4*	Skydrol 500B-4*	Hyjet IV**	Hydaulic Fluid M2-V***
Viscosity, cs -54°C -38°C 100°C 232°C	1158 11.42 3.93	2765 11.51 3.78	1375 10.58 3.57	2450 16.9 5.25
Pour Point, °C	<-62	<-62	<-62	<-79
Relative Density, 25/25°C	1.009	1.057	0.999	0.946
Coeff. Expansion, x 10 ⁻⁴ /°C	9.18	8.46	8.28	9.0
Moisture, wt %	0.1-0.3	0.1-0.3	0.2	<0.01
Acidity	0.10 max	0.10 max	0.07	0.04
Bulk Modulus, MPa @38°C, 435 kPa	1738	1944	1631	1282****
Specific Heat, Cal/g/°C 38°C 149°C 260°C	0.437 0.507	0.418 0.487	- - -	0.44 0.54 0.64
Thermal Conduct, W/m/°C 38°C 149°C 260°C	0.132 0.116	0.132 0.116	- - -	0.145 0.121 0.097
Electr. Conduct, pS/m	43	42	130	-

^{*} Taken from Reference 3.

NOTE: Test procedures used for these determinations were not identified in the referenced documents.

^{**} Taken from Reference 4.

^{***} Taken from Reference 5.

^{****} Isothermal secant bulk modulus taken from Reference 38.

TABLE VIII

RADITIONAL PROPERTIONS WAS INVESTIGATED AND AND AND STREET TO THE CONTRACTOR OF THE PARTY OF THE

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MILITARY HYDRAULIC FLUID SPECIFICATIONS

TABLE IX

NONFLAMMABLE FLUID REQUIREMENTS AND CHARACTERISTICS*

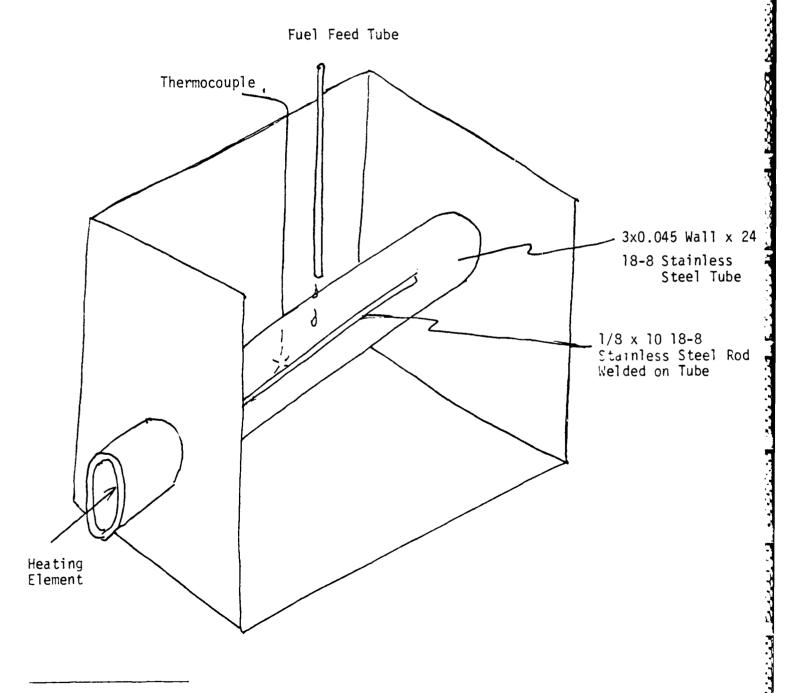
Test	Test Method	Target Requirements*	MIL-H-5606**	CTFE*
Kin. Viscosity, cs -54°C 135°C	ASTM D 445	2500 max 1.5 min	2000 3.0	2231
Pour Point, °C	ASTM D 97	-62 min	<-65	<-65
Four Ball Wear Scar, mm 10 kg 40 kg	ASTM D 2260	0.5 max 1.0 max	- -	- 0.55#
Specific Heat, KCal/kg/°C @38°C @93°C	ASTM D 2766	<u>.</u>	0.47 0.52	0.23 0.24
Thermal Conduct., W/m/°C @38°C @93°C	ASTM D 2717	- -	0.135 0.131	0.074 0.067
Bulk Modulus, Isoth. Secant, Pa x 10 ⁸ @38°C & 2.09 x 10 ⁷ Pa	MIL-H-23282	>14	14.5	12.1
Vapor Pressure, mm Hg @ 149°C	ASTM D 2879	-	56***	71***
Coeff. Expansion, x 10 ⁻⁴ /°C	-	-	7.2***	9.0***
Density @ 25°C, g/cc	ASTM D 287	1.7 max	0.84	1.836

^{*} Taken from References 24 and 25.

^{**} Taken from Reference 13.

^{***} Taken from Reference 36.

FIGURE 1
HOT MANIFOLD TEST*



^{*} Adopted from Reference 20.

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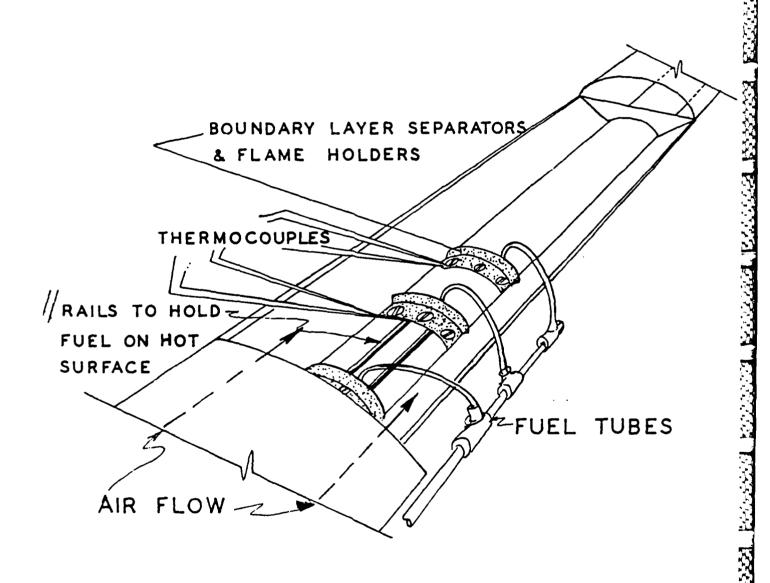
k.

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FIGURE 2

FIRE SIMULATION FACILITY *



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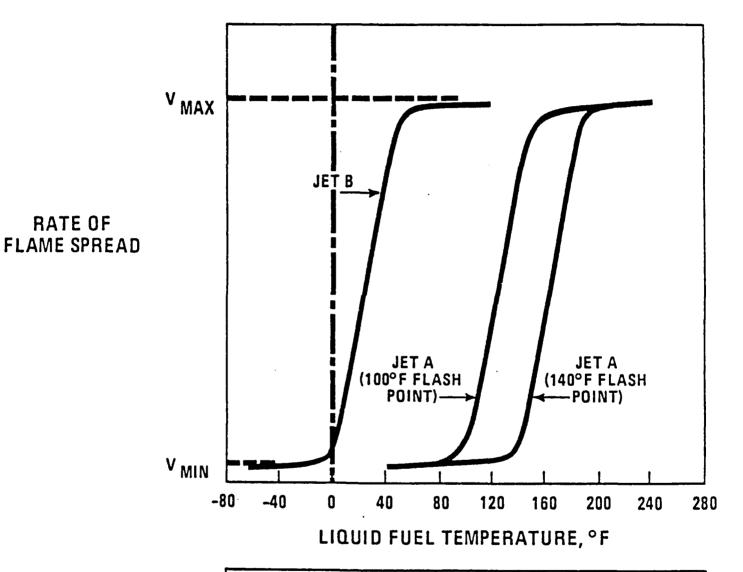
13.23

^{*} Taken from Reference 22.

*

RATE OF FLAME SPREAD VS. LIQUID FUEL TEMPERATURE FOR JET A

AND JET B TYPE FUELS IN AIR AT ATMOSPHERIC PRESSURE*



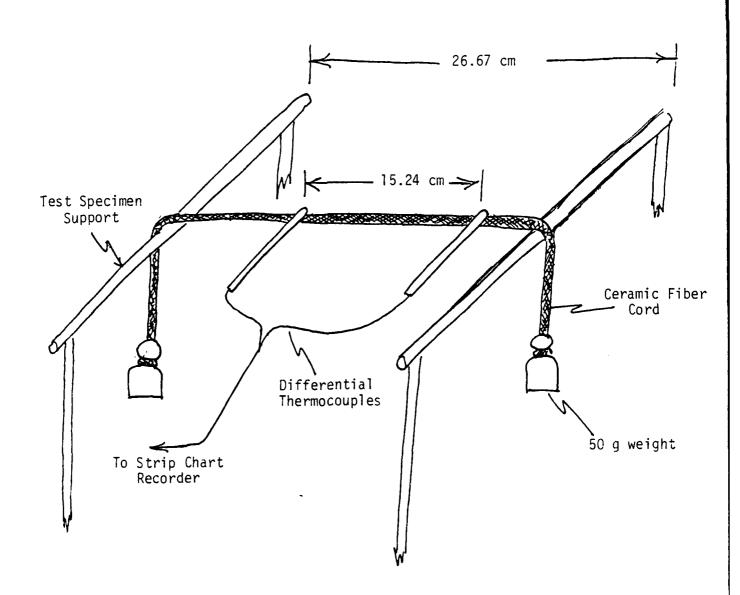
Reference	Fuel	Flame Spread V MIN $(T < T_{f,p.})$	Rate Ft./Min. V_{MAX} $(T > T_{f,p.})$
Weatherford and Schaekel ⁽²⁹⁾	JET A JET B	3.5	248 ± 10
Kuchta Et Al ⁽³⁰⁾	JET A JET B	0.6	438 ± 30

^{*} Taken from Reference 16.

FIGURE 4

APPARATUS FOR DETERMINATION OF LINEAR FLAME PROPAGATION RATE*

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Thermocouple junctions are held 2 mm above ceramic fiber cord.

^{*} Taken from References 7 and 9.

FIGURE 5

EFFECT OF AIR VELOCITY ON FLUID AUTOIGNITION TEMPERATURES

Stainless Steel Surface

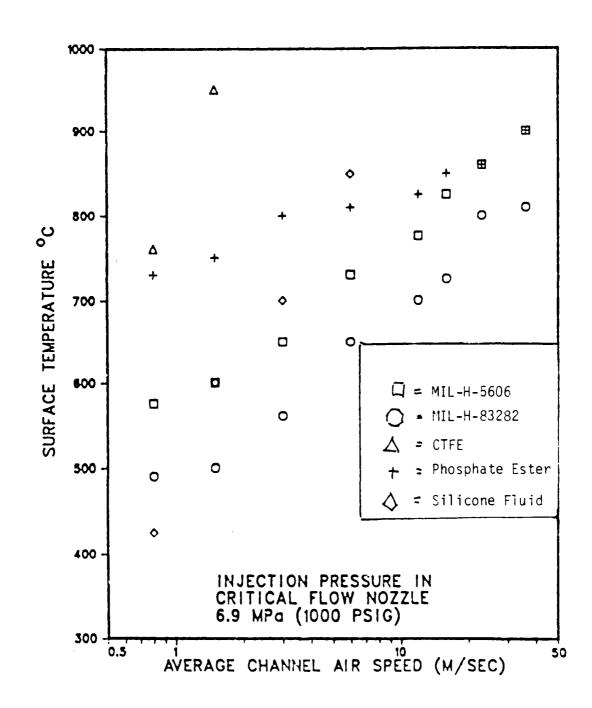
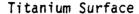
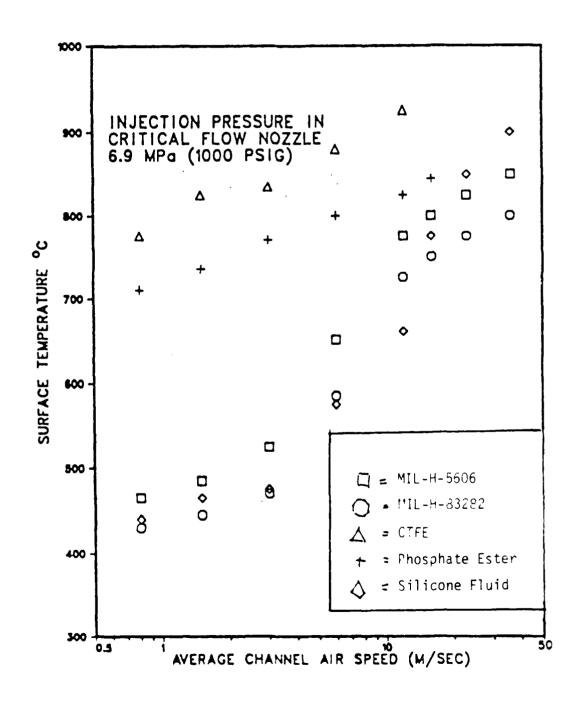


FIGURE 6

EFFECT OF AIR VELOCITY ON FLUID AUTOIGNITION TEMPERATURES





APPENDIX A

MEMBERSHIP OF THE

CRC AVIATION FLUIDS FLAMMABILITY GROUP

MEMBERSHIP OF THE

CRC AVIATION FLUIDS FLAMMABILITY GROUP

Name	Affiliation					
B. R. Wright, Leader A. A. Conte G. S. Economy G. W. Gandee L. Gardner H. L. Hepplewhite R. W. McQuaid D. F. Mearns C. J. Nowack E. L. Richardson C. E. Snyder H. F. Sullivan F. F. Tolle E. W. Wiggins	Southwest Research Institute Naval Air Development Center U.S. Air Force - Norton AFB Air Force Aero Propulsion Lab National Research Council of Canada Mobil Research & Development Corp. Naval Research & Development Center Naval Air Systems Command Naval Air Propulsion Center General Electric Company U.S. Air Force - AFML University of Waterloo Boeing Military Airplane Company McDonnell-Douglas Corporation					
Project Officers						
A. V. Churchill M. E. LePera	U.S. Air Force - AFWAL U.S. Army - Ft. Belvoir					

REPORT-WRITING PANEL

<u>Name</u>	Affiliation				
K. H. Strauss	Consultant				
B. R. Wright	Southwest Research Institute				

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APPENDIX B

DETAILED US AIR FORCE AND US NAVY ACCIDENT FINDINGS

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TABLE B-1

AIRCRAFT HYDRAULIC FIRE PHASE OF OPERATION HISTORY

	1965 -	1975	1970-1975
	USAF	USN	USAF
Parked	10	31	5
Taxi (to takeoff & from landing)	26	10	20 (7/13)
Takeoff Roll	5	2	2
Initial Climb	16	11	8
Inflight	15	18	4
Final Approach	1	0	0
Landing Roll	17	11	7
Ground Run	11	18	0

TOTAL	101	101	46

TABLE B-2

HYDRAULIC COMPONENT FAILURE FIRE HISTORY

Ø

	<u> 1965 -</u>	1975	1970-1975
	USAF	<u>USN</u>	USAF
Lines & Fittings	43	66	14
Brakes	16	0	15
Seals	12	16	5
Pump	3	6	2
Valve	3	0	3
Other	24	13	7
TOTAL	101	101	46

APPENDIX C

FLAMMABILITY DATA ON VARIOUS FLUIDS

TABLE C-1 PHYSICAL AND OTHER PROPERTIES OF LUBRICATING OILS, ENGINE OILS, AND HYDRAULIC FLUIDS*

Mineral Oils Mineral Oil 32,2 5,8 0.85 -430 665 (5)				scosity, cs	Gravity	Point,	Point.	Autoignition b Temperature,	Temperatu
MIL-1919 Mileral oil	Fluid	Compound or Chemical Class	100 F	210 F	(Water=1) <u>F</u>	<u>_</u> F	<u>F</u>	F
Jammory 44 (Call) Mineral oil \$7.5 9.8 9.8 ~460 \$60 (5) \$60 (1) Millor-1977 Mineral oil apabhenic			***			444			
MULD-737 Miceal OII - apathenic									
Mill-19-274 Milleral all - paphthenic Mill-19-274 Milleral all - paphthenic Mill-19-274 Milleral all - paphthenic Mill-19-274 Milleral all 14 3.15 0.88 385 430 700 (288) 725 747 740	•								
Ministral of June Partiffica February Ministral of Partiffica Ministral of Partiffica Partiff									640 (29
Mobil DTE-103 Mineral oil 124 3.15 0.28 385 430 700 (281 ~20 ~20 Mil. +1-60826 Mineral oil 124 8.74-10.2 0.22 309 ~7 702(281 ~20 ~20 Mil. +1-60826 Mineral oil ~ ~ ~ ~ ~ ~ ~ ~ 125 ~ ~ ~ 470 (40) ~ ~ ~ ~ ~ ~ ~ ~ ~ 175 700 (281 ~20 ~20 ~20 ~20 ~20 ~20 ~20 ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~		•	**					464 (40)	725 (31
Mobil UTF-103 Mineral oil 194 8.74-10.2 0.92 200 702,675 (40) Mineral oil 55 5- 477 (43) Mineral oil 477 (43) Mineral oil 477 (43) Mineral oil 477 (43) Mineral oil Mineral oil	MLO-60-294	• .							
Millerari Oil 255 470 (42) Millerari Oil 255 470 (42) Millerari Oil 195 225 437 (2) Millerari Oil 195 235 437 (2) 195 235 437 (2) 195 235 437 (2) 195 235 437 (2) 195 235 437 (2) 195 235 437 (2) 195 235 437 (2) 195 235 437 (2) 195 235 437 (2) 195 235 437 (2) 195 235 437 (2)		•						•	~620 (31
Milerar Mile			124						••
Olycola and Water Clycola Clycol Glycol								• • •	**
Care									
Empleine Glycol Glycol 19.6 200 235 856 (36) 10 200 235 835 (36) 8 200 235 835 (36) 8 200 235 835 (36) 8 200 235 835 (36) 8 200 235 835 (36) 8 200 235 835 (36) 8 200 235 835 (36) 8 200 235 835 (36) 8 200 235 835 (36) 8 200 235 835 (36) 8 200 235 835 (36) 8	•							101 (2)	
Propyten Giycol Giycol Giycol 19.6 230 235 833 (36) 10.00	•	a				040		050 (00)	
Ethylene Glycol + 9.9 M Mater Water-glycol	• •	•							
	• •	•							
Houghto-Safe 529 Mater-glycol 43.2 25.1 (1307) 1.075	•								
Linughno-Safe 620 Water-glycol and additives 41	•							• •	
Nyuka 20 (Mobil) Water-Qiron and additives 41	9	Water-glycol						**	
Tus 90 (Shell)	Houghto-Safe 620		43.2	29.8 (150F)	1.055	••			
Decon Solid=2600 Polysiklylene glycol Se	Nyvac 20 (Mobil)	Water-glycol and additives	41		1.07		••	750 (41)	
Loos 194-80	Irus 902 (Shell)	Water-oil emulsion	97.4	51	0.93			709 (41)	
Decom LB-400-X	Ucon 50HB-260	Polyalkylene glycol	56			455	500	743 (36)	
	Ucon 50HB-280-X	, , , ,				500	600	743 (20)	••
Description Triary Description Triary	-	, , , ,	10.7	•=		310	325		
Houghto Safe 1010				, 					••
Houghto Safe 1010	harabata Estar	•							
Houghto-Safe 1055	•	Total about the control	100	• •		505	670	31000 //13	
Houghto-Safe 1115	•	• • •							
		• • •						— · ·	
	•	• •							
MIL-1-19451 (Type 1)		• • •	•						
Tricretyl Phosphate Triaryl phosphate ener Triaryll phosphate	-	• • •						, ,	
Triceryi Phosphate Trialkyl phosphate ester 549 (12) Triberyl Phosphate Trialkyl phosphate ester 549 (12) Triberyl Phosphate Trialkyl phosphate ester 549 (12) Triberyl Phosphate ester-Chlorinated Triberyl Phosphate ester	MIL-H-19457 (Type 1)	Triaryl phosphate exer		••				1040 (19)	
TrilallyI, phosphate exter Pydraul AC Phosphate exter Pydraul AC Phosphate exter-chlorinated hydrocarbon 88.8 8.0 1.36 450 745 1148 (5)	Tricresyl Phosphate	Triaryl phosphate ester	38.3	4.48	1.17	470		1110 (12)	680 (3
Phosphate exter-chlorinated hydrocarbon So.9 So.9 1.36 450 745 1148 (5)	Trioctyl Phosphate	Trialkyl phosphate ester			0.926	405	••	545 (13)	~380 (29
Pydraul F-9	Trihexyl Phosphate	Trialkyl phosphate ester			,			549 (12)	
Pydraul F-9	Pydraul AC	Phosphate ester-chlorinated							
Celiulube 220 (Shell S.F.R.) Phosphate ester 43.4 4.9 1.145 455 665 1038 (5)		hydrocarbon	88.8	5.0	1.36	450	745	1148 (5)	
Celiulube 220 (Shell S.F.R.) Phosphate exer 43.4 4.9 1.145 455 665 1038 (5) Pydraul 150 (Monsanto) Phosphate exter 30.5 7.9 1.125 380 470 975 (41) Skydrol Phosphate exter 30.5 7.9 1.125 380 470 975 (41) Skydrol Phosphate exter 30.5 7.9 1.125 380 470 975 (41) Skydrol Phosphate exter 30.5 7.9 1.125 380 470 975 (41) Skydrol Phosphate exter 30.5 7.9 1.125 380 470 975 (41) Skydrol Phosphate exter 30.5 7.9 1.125 380 470 975 (41) Skydrol Phosphate exter 30.5 7.9 1.125 380 470 975 (41) Skydrol Phosphate exter 30.5 7.9 1.250 380 470 975 (41) Plexol 244 Di-isooctyl adipate 12.7 3.31 0.912 420 450 Plexol 273 Polyener 1250 108 1.023 540 620 Mill-L-7808 (0-60-18, Esso 4040) Sebacate-adipate diester 12.1 3.1 437 460 728,486 (7) 490 (Mill-L-7808 (1-1026) Di-2-ethylhexyl sebacate 12.58 3.3 755 (40) 575 (Mill-L-9236 (0-60-27, TP-6538) Trimethylol propane exter 15.1 3.4 430 475 738,491 (7) ~650 (Mill-L-9236 (0-60-23) Trimethylol propane exter 15.78 3.59 435 485 Mill-L-9236 (0-60-23) Trimethylol propane exter 15.78 3.59 470 525 Mill-L-92368 Trimethylol propane exter 15.78 3.59 435 475 738,491 (7) ~650 (Mill-54-581 (Texaco, TL-2456) Diexer 435 475 734 (2) P/10 (Esso 4275) Polyerer 705,507 (40) P/10 (Esso 4275) Polyerer 8.04 0.951 510 711,500 (40) P/10 (Esso 4275) Polyerer	Pydraul F-9	Phosphate ester-chlorinated							
Pydraul 150 (Monsanto) Phosphate ester Phosphate ester Phosphate ester Phosphate ester Phosphate ester Plexol 201 Plexol 201 Di-2-bexyl sebacate 12.7 1.3.31 0.912 420 450 Plexol 273 Plexol 273 Plexol 273 Plexol 79 Plexol 80 (-60-18, Euso 4040) NILL-1-7808 (-60-18, Euso 4040) NILL-1-7808 (1-1026) Di-2-ethylheryl sebacate 12.1 3.1		hydrocarbon	50.9	5.9	1.285	430	675	1100 (41)	**
Pydraul 150 (Monsanto)	Ccilulube 220 (Shell S.F.R.)	Phosphate ester	43.4	4.9	1.145	455	665	1038 (5)	
Skydrol Phosphate ester 360 470 >1300 (41)	Pydraul 150 (Monsanto)	•		7.9	1.125	380	470		
Plexol 201 Di-2-hexyl sebacate 12.7 3.31 0.912 420 450 Plexol 244 Di-Isooctyl adipate 9.64 2.77 0.926 400 445 712 (12) Plexol 273 Di-Isodecyl adipate 14.5 3.56 0.920 425 460 Polyester 1250 108 1.023 540 620		•							
Piexol 201 Di-2-hexyl sebacate 12.7 3.31 0.912 420 450 Piexol 244 Di-Issooctyl adipate 9.64 2.77 0.926 400 445 712 (12) 7 Piexol 273 Di-Issodecyl adipate 14.5 3.56 0.920 425 460 7	dono - and Dibasic Acid Esters								
Piexol 273 Di-isodecyl adipate 14.5 3.56 0.920 425 460 Piexol 79 Polyester 1250 108 1.023 540 620		Di-2-hexyl sebacate	12.7	3.31	0.912	420	450	••	••
Plexol 273 Di-Isodecyl adipate 14.5 3.56 0.920 425 460 Plexol 79 Polyeser 1250 108 1.023 540 620 MILL-1-7808 (10-60-18, Esso 4040) Sebacate-adipate diester 12.1 3.1 437 460 728.486 (7) 490 (MILL-1-7808 (11-1026) Di-2-ethylhexyl sebacate 12.58 3.3 755 (40) 57	Plexol 244	•		2.77	0.926	400	445	712 (12)	
Piexol 79									
MILL-L-7808 (0-60-18, Esso 4040) Sebacate adipate diester 12.1 3.1 437 460 728,486 (7) 490 (MIL-L-7808 (H-1026) Di-2-ethylhexyl sebacate 12.58 3.3 755 (40) 575 (MILL-L-92368 (0-60-7, TP-6538) Trimethylol propane exter 15.1 3.4 430 475 738,491 (7)650 (MILL-L-9236 (0-60-27) Trimethylol propane exter 15.99 3.62 470 525 MILL-19236 (0-60-23) Trimethylol propane exter 15.78 3.59 490 535 MILL-19236 (0-61-17) Trimethylol propane exter 15.78 3.59 490 535 MILL-19236 (0-61-17) Trimethylol propane exter 16 3.2 0.97 425 510 >800 (41)650 (MILL-192368 Trimethylol propane exter 16 3.2 0.97 425 510 >800 (41)650 (MILL-192368 (Texaco, TL-2456) Diexer 435 475 743 (2) 470 525 (40) 705,507 (40)		•							
MIL-L-7808 (H-1026) Di-2-ethylhexyl sebacate 12.58 3.3 755 (40) 575 (MIL-L-92368 (0-60-7, TP-6538) Trimethylol propane ester 15.1 3.4 430 475 738.421 (7)650 (MIL-L-9236 (0-60-27) Trimethylol propane ester 14.8 3.45 435 485 MIL-L-9236 (0-60-23) Trimethylol propane ester 15.99 3.62 470 525 MIL-L-9236 (0-61-17) Trimethylol propane ester 15.78 3.59 490 535 MIL-L-92368 Trimethylol propane ester 16 3.2 0.97 425 510 >800 (41)650 (MILO-54-581 (Texaco, TL-2456) Diester 435 475 743 (2) TP-6538 (Hey, Newport) Trimethylol propane ester 70.97 705.507 (40) Polyester 8.04 0.951 510 711.500 (40) MILO-60-50 Trimethylol propane ester 606 (Trimethyolpropane Tri- Trimethylol propane ester 606 (Trimethylol propane ester 606 (MILO-54-408C Tetra dodecyl silane 37.2 6.2 530 580 690 (17) >680 (MILO-56-578 Octadecyl trioctyl silane 37.2 6.2 530 580 690 (17) >680 (MILO-56-578 Octadecyl trioctyl silane 33.9 6.8 545 595 750 (17) MILO-56-611 Didodecyl dioctyl silane 26.4 5.6 535 575 750 (17) MILO-56-611 Didodecyl dioctyl silane 23.1 5.0 520 565 750 (17)		•							
NIL-L-92368 (0-60-7, TP-6538) Trimethylol propane exer 15.1 3.4 430 475 738,491 (7) ~650 (1) MIL-L-9236 (0-60-27) Trimethylol propane exer 14.8 3.45 435 485 NIL-L-9236 (0-60-23) Trimethylol propane exer 15.99 3.62 470 525 NIL-L-9236 (0-61-17) Trimethylol propane exer 15.78 3.59 490 535 NIL-L-92368 Trimethylol propane exer 16 3.2 0.97 425 510 >800 (41) ~650 (1) NIL-92368 Trimethylol propane exer 16 3.2 0.97 425 510 >800 (41) ~650 (1) NIL-92368 (Hey. Newport) Trimethylol propane exer 1 435 475 743 (2) TP 6538 (Hey. Newport) Trimethylol propane exer 1 435 475 743 (2) TP 6538 (Hey. Newport) Trimethylol propane exer 1 70.97 1 705.507 (40) 1- P/1) (Esso 4275) Polyexer 1- 8.04 0.951 510 1- 711.500 (40) 1- NILO-60-50 Trimethylol propane exer 1- 1- 1- 1- 1- 1- 1- 1- 1- 1- 1- 1- 1-	•	•							
MIL-L-9236 (0-60-27)	• •	· -							
MIL-L-9236 (0-60-23)		• • •						_	-
MIL-L-9236 (0-61-17) Trimethylol propane exer 15.78 3.59 490 535 MIL-L-92368 Trimethylol propane exer 16 3.2 0.97 425 510 >800 (41) ~650 (500 (41) 550	•								
MIL-L-92368 Trimethylol propane exer 16 3.2 0.97 425 510 >800 (41) ~650 (41) ~650 (41) MILO-54-581 (Texaco, TL-2456) Diexer 435 475 743 (2) TP 5538 (Hey. Newport) Trimethylol propane exer 70.97 705, 507 (40) P/D (5x80 4275) Polyexer 8.04 0.951 510 711, 500 (40) MILO-60-50 Trimethylol propane exer 748 (71, 500 (40) 748 (71, 500 (40) (40) (40) (40) (40) (40) (40) (4	, ,	Trimethylol propane exer						••	
MLO-54-581 (Texaco, TL-2456) Dieser 435 475 743 (2) TP 6538 (Hey. Newport) Trimethylol propane ester 70.97 705.507 (40) P/I) (Esso 4275) Polyester 8.04 0.951 510 711.500 (40) MLO-60-50 Trimethylol propane ester 748 (70.000	MIL-L-9236 (0-61-17)		15.78						
TP 6538 (Hey. Newport) Trimethylol propane exer 70.97 705.507 (40) P/D (Esso 4275) Polyester 8.04 0.951 510 711.500 (40) MLO-60-50 Trimethylol propane exer 748 (Trimethylol propane exer 606 (Polyester		Trimethylol propane exer	16	3.2	0.97	425		>800 (41)	~650 (2
P/I) (Esso 4275)	MLO-54-581 (Texaco, TL-2456)	Diester			••	435	475	743 (2)	••
Mico-60-50 Trimethylol propane exter	TP 6538 (Hey, Newport)	Trimethylol propane exer	••	••	~0.97			705, <u>507</u> (40)	
Mt.O-60-50	P/O (Esso 4275)	Polyester		8.04	0.951	510		711,500 (46)	••
Trimethyolpropane Tripelargonate Trimethyolpropane exer 606 (pelargonate Ilanes NLO-54-408C Tetra dodecyl silane 34.58 6.37 555 625 775 (17) 6588 (MLO-56-280 Diphenyl di-n-dodecyl silane 37.2 6.2 530 580 690 (17) >680 (MLO-56-578 Octadecyl trioctyl silane 27.5 5.76 520 590 790 (17) (MLO-56-582 Octadecyl tridecyl silane 33.9 6.8 545 595 750 (17) (MLO-56-610 Dodecyl tridecyl silane 26.4 5.6 535 575 750 (17) (MLO-56-611 Didodecyl dioctyl silane 23.1 5.0 520 565 750 (17) (*					••		••	748 (3
NILO-54-408C Tetra dodecyl silane 34.58 6.37 555 625 775 (17) 688 MLO-56-280 Diphenyl di-n-dodecyl silane 37.2 6.2 530 580 690 (17) >680 MLO-56-578 Octadecyl trioctyl silane 27.5 5.76 520 590 790 (17) MLO-56-582 Octadecyl tridecyl silane 33.9 6.8 545 595 750 (17) MLO-56-610 Dodecyl tridecyl silane 26.4 5.6 535 575 750 (17) Alla)-56-611 Didodecyl dioctyl silane 23.1 5.0 520 565 750 (17)	· · · · · · · · · · · · · · · · · · ·		••			••	••		606 (2
NLO-54-408C Tetra dodecyl silane 34.58 6.37 555 625 775 (17) 688 MLO-56-280 Diphenyl di-n-dodecyl silane 37.2 6.2 530 580 690 (17) >680 MLO-56-578 Octadecyl trioctyl silane 27.5 5.76 520 590 790 (17) MLO-56-582 Octadecyl tridecyl silane 33.9 6.8 545 595 750 (17) MLO-56-610 Dodecyl tridecyl silane 26.4 5.6 535 575 750 (17) NLO-56-611 Didodecyl dioctyl silane 23.1 5.0 520 565 750 (17)	ilanes								
MLO-56-280 Diphenyl di-n-dodecyl silane 37.2 6.2 530 580 690 (17) >680 MLO-56-578 Octadecyl trioctyl silane 27.5 5.76 520 590 790 (17) MLO-56-582 Octadecyl tridecyl silane 33.9 6.8 545 595 750 (17) MLO-56-610 Dodecyl tridecyl silane 26.4 5.6 535 575 750 (17) Allc)-56-611 Didodecyl dioctyl silane 23.1 5.0 520 565 750 (17)		Tetra dodecyl silane	34.58	6.37	••	555	625	775 (17)	658 (1
MLO-56-578 Octadecyl trioctyl silane 27.5 5.76 \$20 590 790 (17) MLO-56-582 Octadecyl tridecyl silane 33.9 6.8 545 595 750 (17) MLO-56-610 Dodecyl tridecyl silane 26.4 5.6 535 575 750 (17) AllO-56-611 Didodecyl dioctyl silane 23.1 5.0 520 565 750 (17)		•					580		>680(1
MLO-56-582 Octadecyl tridecyl silane 33.9 6.8 545 595 750 (17) MLO-56-610 Dodecyl tridecyl silane 26.4 5.6 535 575 750 (17) MLO-56-611 Didodecyl dioctyl silane 23.1 5.0 520 565 750 (17)									
MLU-56-610 Dode:yi tridecyl silane 26.4 5.6 535 575 750 (17) MLU-56-611 Didodecyl dioetyl silane 23.1 5.0 520 565 750 (17)		* *							
NIL(1)-56-611 Didodecyl dioctyl stiane 23.1 5.0 520 565 750 (17)		• •							
,									
MLO-57-9 Tetra undecyl silane 29.26 6.11 545 600 760 (17)									

^{*} Taken from Reference 19.

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TABLE C-1 (Continued)

		Viscosity, cs		Specific	Flash	Fire	Autoignition	Decomposition
Fluid	Companyed at Chamterl Class		<u></u>	Gravity	Point	Point.	•	Temperature.
riuid	Compound or Chemical Class	100 F	200 F	(Water=1)	F	<u> </u>	F	F
Silicates and Silicones								
Tetra (2-ethylhexyl) Silicate	Ethyl hexyl silicate				••		••	638 (29)
Onsli B.F.1	(2-ethylhexyl) silicate						~570 (12)	
Oronite 8200	Silicate ester	31.75	11.14		385	440	716 (2)	
Oronite 8515	Silicate ester	24.3	8.11		390	450	710 (40)	
MLO-54-645	85% oronite and 15% plexol	••	••		340	455	716 (2)	
MLO-54-540 (Monsanto OS-45)	Silicate exer				325	430	703 (2)	••
MLO-54-856 (Hollingshead,					323	430	100(2)	
72073C)	Silicate estet				315	440	716 (2)	
Versilube F-50	Silicone	52	16	1.045	550	11 0	110 (2)	
Versilube F-44	Silicone	55	17	1.045	550		000 (40)	>400.444
Dow Coming 190	Polymethyl siloxane	22.6				640	900 (40)	>600 (41)
Dow Corning 400	Polymethyl siloxane				240	540	900 (40)	>600 (41)
Dow Corning 500	• •	10.9			255	••	860 (36)	
•	Polyethyl siloxane	44.9			470	280	610 (36)	
Dow Corning 550	Silicone	65 - 87		1.065	600		900 (36)	
Dow Coming 700	Poly (methyl. phenyl)					••		740 (29)
	siloxane	2.8			305			
Dow Corning 710	Methyl phenyl silicone	220		1.112	520	325	940 (36)	
MLO-59-98	50% methyl phenyl silicone						••	589 (15)
	(DC 258) plus 50% TMP							
	adipate tetracoproate	61.8	13.5			••		625 (31)
								` .
Halogenated Silicones and Hydrocar	bons							
MLO-53-446 (GE 81406)	Chlorinated silicone				580	710	786 (2)	514 (15)
MLO-59-287 (GE F-50)	Chlorophenyl methyl silicone						••	630 (31)
Fluorolube F-S	Polytrifluoroch loroethylene	5		1.86		••	~1205 (12)	>620 (41)
Pydraul A-200	Chlorinated hydrocarbon	43.8	5.0	1.42	350	680	1200 (41)	••
Arochlor-1248	Tetrachlorodiphenyl	43.0	3.2	1.41	380	None	~1185 (12)	••
Arochlor-1242	Trichlorodiphenyl	17.7			350	633	1230 (36)	
Arochlor-1254	Chlorinated hydrocarbon		•-	••			~1085 (12)	••
							1003 (12)	
Aromatic Ethers								
OS-124 (Monsanto, 5P4E)	5 ring polyphenyl ether	363	13.1	1.20	550	660	1112 (40)	> 020 /211
MCS-293 (Monsanto)	Atomatic ether	25.2	4.13	1.19	428	518	914 (40)	>830 (31)
MLO-59-692 (Monsants)	Bis (phenoxyphenoxy) benzene	23.4	4. 13	1.19		210	914 (40)	675
mm-4P4E	Bis(m-phenoxyphenyl) ether	-60.9						942 (31)
pp-4P3E			5.98		465		1095 (17)	~835 (17)
mmm-5P4E	Bis(p-phenoxyphenyi) ether	2.83(300F)			516	585	1040 (17)	~835 (15)
5P4E	m-Bis(m-phenoxyphenoxy) benzene		12.7		540	660	1050 (17)	870 (17)
	Bis(phenoxyphenoxy) benzene	380	13.4		560	660	1130. <u>1030</u> (7)	870 (27)
pppp-6P5E	Bis (p-(p-phenoxyphenoxy)phenyl)							
	ether	4.20(400F)	1.55 (600F)		635	••	1030 (17)	773 (15)
Marahan (asila)								
hosphonitriles								
NLO-63-24	Hexaphenyltriphosphonitrile	••	••	••		•-	••	810 (31)
MLO-63-25	Phenoxy base triphosphonitrile							905 (31)
K488 (Olin Mathleson)	Tetrameric octylfluoroamyl							
	phosphonitrilate				••	••	900 (19)	
discellaneous Oils								
Lard oll				< 1	395		833 (38)	••
Linseed off			••	0.95	435	535	820 (38)	••
Lube oil, cylinder			••	<1	••	535	783 (38)	••
Lube oil, light machine			••	<1	318	370	**	••
Lube oil, spindle				<1	169	260		
Menhaden oil		••	••	0.927	435	200		••
Mineral seal oil			••	0.521	170		828 (38)	••
Olive oil		••		0.91	437	255	926 (28)	••
Palm oil		••		0.91	421	••	826 (38)	••
Pine oti		••	••				650 (38)	••
Rapesced otl	•			0.86	172	175	••	
Rosin oli				0.915	325	550	836 (38)	
•				0.98-1.1	266	••	648 (38)	••
Soybean oll			••	0.925	540		833 (38)	
T								
Tung oil				0.94	552		855 (38)	••
Turkey-red oil			••	••	476		855 (38) 833 (38)	••

Autoignition and decomposition temperature data from references cited in parentheses. Viscosity, specific gravity, flash point, and fire point data mainly from vendor's literature.

bignition evidenced by visible flame except for underlined values where sudden pressure rise was used. Bureau of Mines data (Refs. 2, 4, 5, 7, and 40) were obtained using reaction vessels >200 cc. Values listed for other references were determined in reaction vessels <12

APPENDIX D

INTERNATIONAL STANDARDS

CATEGORIES FOR FIRE-RESISTANT HYDRAULIC FLUIDS

ACCOUNTS REPORTED TO SECOND AND SECOND DESCRIPTION OF SECOND PROPERTY OF SECOND PROPERTY

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ISO Standard 6743/4, 1982

Class L Classification

Family H (Hydraulic Systems)

(Note: This family does not include automotive brake fluids or aircraft hydraulic fluids.)

General classification of fire-resistant fluid types:

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Fluid Category HFA: Solution or emulsions containing more than 80 percent water. Service temperature +5° to +50°C (+41° to +122°F).

Fluid Category HFB: Water in oil emulsion. Service temperature +5° to +60°C (+41° to +140°F).

Fluid Category HFC: Water polymer solutions or water-glycol containing less than 80 percent water. Service temperature -20° to +60°C (-4° to+140°F).

Fluid Category HFD: Synthetic fluids containing no water. Service temperature -20° to +150°C (-4° to +302°F).

Category HFA: Two major subdivisions of this class are: HFAS-Solutions and HFAE-Emulsions with continuous water phase.

HFA fluids are generally unsuitable for use in highly rated systems due to their low viscosity and poor lubricity. Suitable paints and coatings are necessary to prevent rust and corrosion of components above the liquid level. Most HFA fluids have a viscosity level comparable to that of water. For such fluid systems, changes in water content will not be accompanied by a significant change in viscosity, and viscosity control is not required. Where solution-type fluids containing thickeners are used, the viscosity will vary in service with water content and thickener integrity. The viscosity of these fluids should be monitored and maintained in accordance with pump manufacturer's and fluid supplier's recommendations. Consult supplier for recommended procedures for adding make-up water.

Category HFB: HFB fluids are dispersions of finely divided water droplets in a continuous phase of mineral oil with special emulsifiers, stabilizers, and inhibitors. They normally contain approximately 40 percent water. Changes in water content will change viscosity, stability, and/or fire resistance.

HFB fluids have viscosity grades similar to normal mineral hydraulic oil and exhibit quite good lubricating and anticorrosive properties. The fluid is non-Newtonion, and the operational viscosity may vary from one part of a system to another according to the shear forces applied (stated viscosity may be higher than effective viscosity). Because of this viscosity characteristic and high vapor pressure, pump inlet conditions have to be carefully designed so as to avoid cavitation.

Since viscosity and fire resistance vary with water content, fluid viscosity should be measured at regular intervals during the initial period of operation to determine the water content. Fluid viscosities should be selected and maintained in accordance with pump manufacturer's and fluid supplier's recommendations. Excessive loss of water should be avoided since this reduces fire resistance and causes a decrease in viscosity. Adding excessive amounts of water should be avoided as this will increase the fluid viscosity and may cause operating problems.

Avoid contamination by acids, alkalis, hard water, inorganic salts, solvents, HFC fluids, or HFD fluids since emulsion stability (phase separation) may occur.

Category HFC: HFC fluids are true solutions, derive their fire resistance from the presence of approximately 45 percent water, and have viscosity characteristics similar to mineral oil. Because viscosity and fire resistance vary with water content, measure fluid viscosity at regular intervals during the initial period of operation to determine the water content. Select and maintain fluid viscosities in accordance with pump manufacturer's and fluid supplier's recommendations.

Avoid excessive loss of water since this reduces fire resistance and causes an abnormally high viscosity.

Category HFD: The water-free HFD fluids such as phosphate esters are fire-resistant by virtue of their chemical composition, are available in viscosity grades similar to mineral hydraulic oils, and are suitable for higher operating temperatures than HFA, HFB, and HFC fluids. The various HFD fluids differ in low-temperature capability; elastomer, paint, and metal compatibility; specific gravity; and toxicity. The two major subdivisions of these fluids are distinguished by the nature of the synthetic products and are designated by HFD-R (phosphate esters) and HFD-U (other compositions). Manufacturers should be consulted regarding these characteristics.

It is readily apparent from reviewing the classifications that the fluids used by aircraft manufacturers and users as well as other military applications are almost exclusively the HFD fluids. It should be noted, however, that many of the same flammability procedures are applicable both to water containing fluids and also nonwater-containing fluids.

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