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**Integrated Component Fluidic Servovalves and
Position Control Systems**

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Prepared by

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Cambridge, MA 02139

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20. Abstract (Cont'd)

tion control system. Static and dynamic experimental evaluation of the servosystem has shown that its performance is comparable to that of a servo employing electrohydraulic components.

This development effort has demonstrated the capability to develop high performance, closed loop servo components from standard, integrated component fluidic elements.



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1. INTRODUCTION

Hydraulic control systems are widely used in applications where high force levels, fast response and high power to weight ratios are required. Aerodynamic control surface actuators, machine tool actuators, mobile equipment control systems and marine control systems frequently employ closed loop hydraulic control systems. Important performance criteria for these systems include maximum force and velocity capabilities, accuracy, repeatability, reliability, maintainability and cost.

The primary power modulation elements in high performance hydraulic systems are servovalves. In position and velocity control systems servovalves are utilized extensively as indicated in figure 1. Also shown in the figure are typical pressure-flow output characteristics of commercial sliding spool servovalves. Servovalves with linear flow gains and high pressure gains are desired to achieve accuracy and overcome actuator and load stiction.

Electrohydraulic servovalves consisting typically of a torque motor, a first stage flapper nozzle or jet-pipe valve and a final stage sliding spool valve are the dominant type of valves employed in high performance hydraulic systems.¹ In these valves the electromechanical interface and the sliding mechanical elements contribute to valve cost, sensitivity to contamination and sensitivity to failure due to radiation.

The high reliability, insensitivity to extreme environments and low cost associated with no moving part fluidic elements and the potential for weight and size reduction in comparison to conventional valves are attractive features for servovalves. In addition, the implementation of a closed loop control system employing only fluid and mechanical elements offers potential for reduction of sensitivity to radiation and increased reliability with the elimination of electro-mechanical interfaces. In systems where these attributes are important and where the quiescent power drain associated with open-center fluid valves can be accommodated, fluidic servovalves and pure fluid-mechanical control systems have high application potential.

The application potential of pure fluid servovalves and control systems

¹R. Deadwyler, Two Stage Servovalve Development Using a First-Stage Fluidic Amplifier, Harry Diamond Laboratories, HDL-TM-80-21 (July 1980).

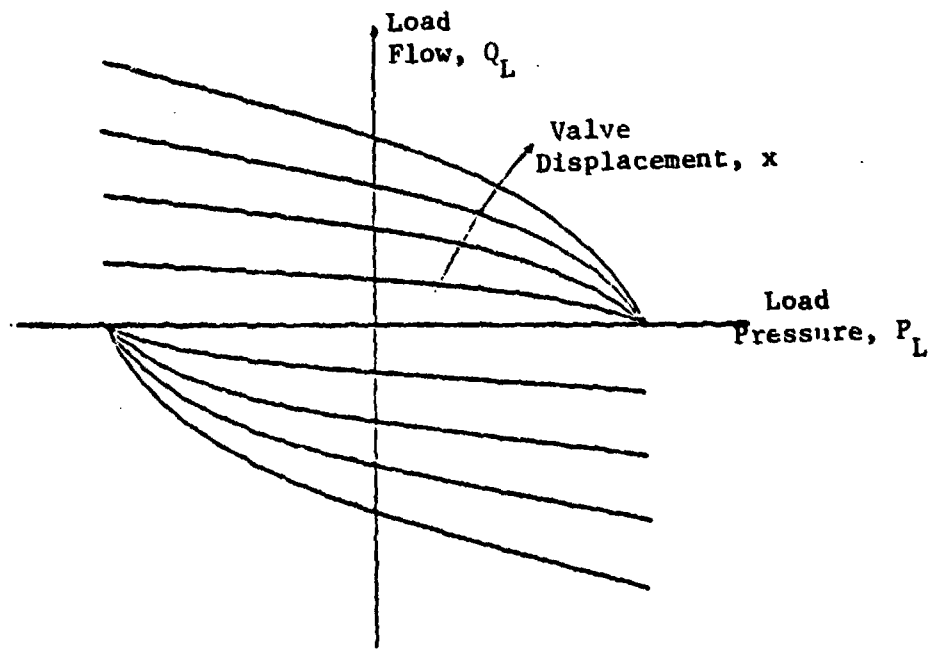
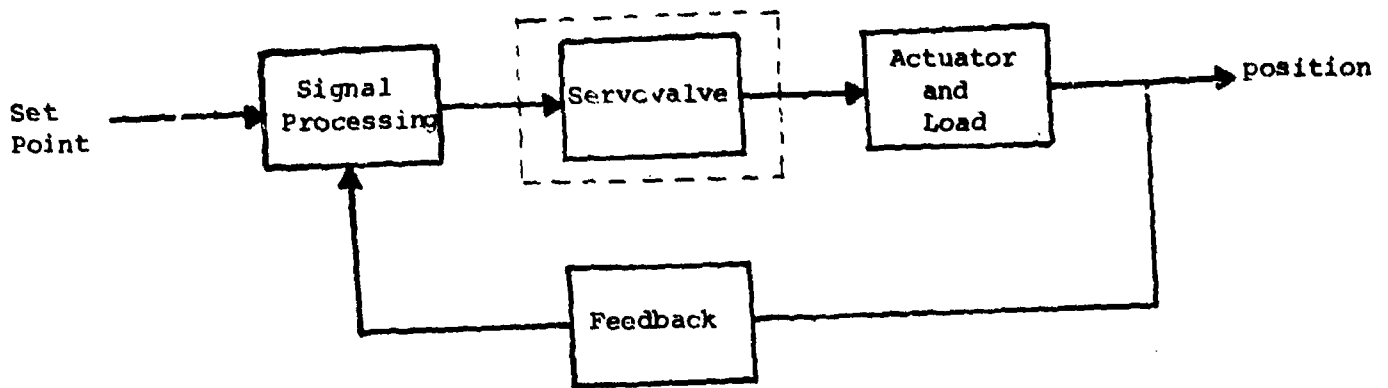


Figure 1. Closed loop position servo and servovalve output characteristics.

motivated a study² in which a pure fluid servovalve was constructed using laminar proportional amplifiers (LPA's) in a breadboard configuration. In the present study, development of pure fluid servovalves and servosystems has continued. Servovalves constructed from standard C format laminates³ and interconnecting elements have been developed to reduce packaging volume and weight, provide a basis for standardization and to improve valve dynamic response. The static and dynamic characteristics of the C format LPA elements individually and integrated into the servovalve have been measured including performance sensitivity to temperature. Finally the servovalve has been employed in a closed loop position control system which includes an actuator and fluidic position transducer for evaluation.

Two aspects of the influence of temperature are particularly addressed in this study, namely, the static characteristic performance and the laminar operating range of the LPA as a function of supply conditions.

In all tests described in this report, hydraulic oil Univis J-43 has been used. The properties and specifications of the fluid are summarized in table 1 and the kinematic viscosity as a function of temperature is shown in figure 2 in the range from 20°F to 140°F. Univis J-43 changes in viscosity over this typical temperature range. An exponential curve fit of the form:

$$v_o = v_o e^{-\lambda(T-T_o)} \quad (1)$$

where

- v = kinematic viscosity at temperature T ,
- v_o = kinematic viscosity at reference temperature, T_o
- λ = viscosity - temperature coefficient,

may be used to approximate the kinematic viscosity of the hydraulic oil Univis J-43 as a function of temperature

with $\lambda = 0.02862 \text{ 1/}^\circ\text{C} [0.0159 \text{ 1/}^\circ\text{F}]$

and $v_o = 21.78 \text{ cSt. evaluated at } 25^\circ\text{C} [77^\circ\text{F}]$

The exponential curve of equation (1) is a good approximation to the fluid viscosity as shown in figure 2.

²D.N. Wormley, D. Lee, and K-M Lee, Development of a Fluidic, Hydraulic Servovalve, HDL-CR-81-216-1, Harry Diamond Laboratories (February 1981).

³M.F. Cycon and D.J. Schaffer, Design Guide for Laminar Flow Fluidic Amplifiers and Sensors, HDL-CR-28-288-1, Harry Diamond Laboratories (April 1982).

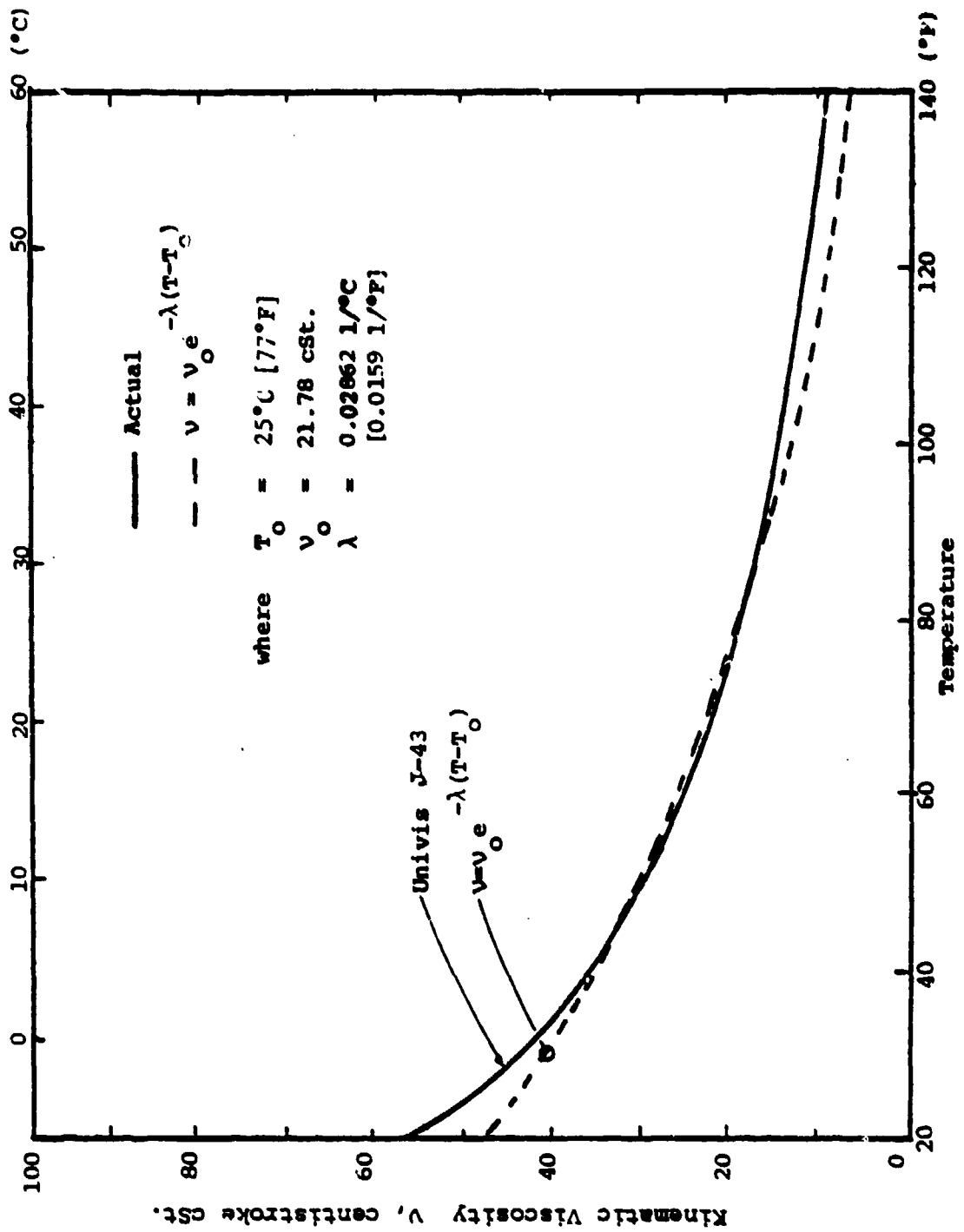


Figure 2. Kinematic viscosity as a function of temperature.

TABLE 1 HYDRAULIC OIL UNIVIS J-43 SPECIFICATION

Specific gravity: 0.8607

Temperature (°C)	Kinematic Viscosity (cSt.)
100	5.2
54	10.3
40	14.9
-18	102.7
-40	495.5
-54	2332.

2. FLUIDIC INTEGRATED COMPONENTS

Fluidic C format integrated components are basic elements in the servo-valve. The primary elements are the LPA and the channel resistance which are shown in figure 3. The secondary elements are vents, exhausts, spacers, transfers, base plate, input and valve manifolds. The primary elements are standardized in design and manufacturing and are thus well documented and have repeatable characteristics.

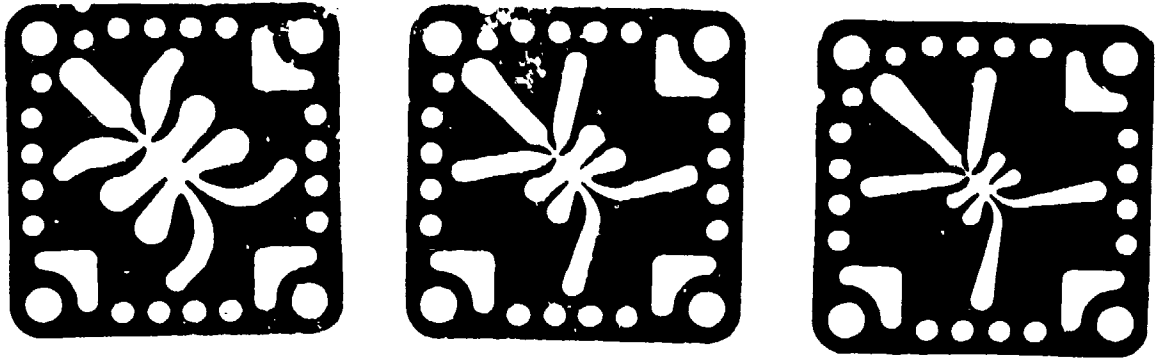
2.1 Laminar Proportional Amplifier

Laminar proportional amplifiers have been designed to operate in the laminar flow regime. The detailed geometry of a typical HDL integrated component laminar proportional amplifier with a summary of LPA characteristic dimensions are illustrated in figure 4.

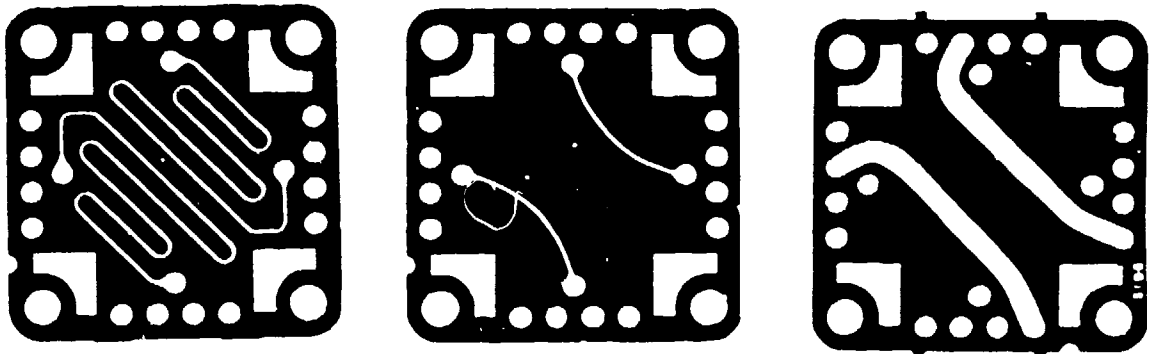
The LPA performance is influenced by the temperature of the operating fluid through its influence on the fluid viscosity.

The analytical design procedures which predict the performance of the laminar proportional amplifier based on the characteristic dimensions and the supply conditions have been discussed by Drzewiecki et al.⁴ The

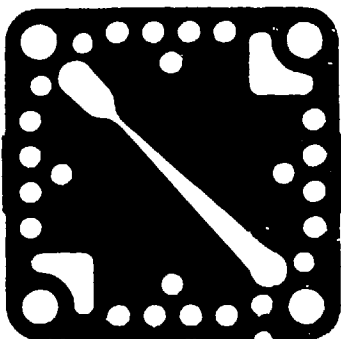
⁴T.M. Drzewiecki, D.N. Wormley and F.M. Manion, Computer Aided Design Procedure for Laminar Fluidic Systems, Journal of Dynamic Systems, Measurement and Control, 97, Series G, No. 4 (December 1975).



(a) laminar proportional amplifier (LPA)

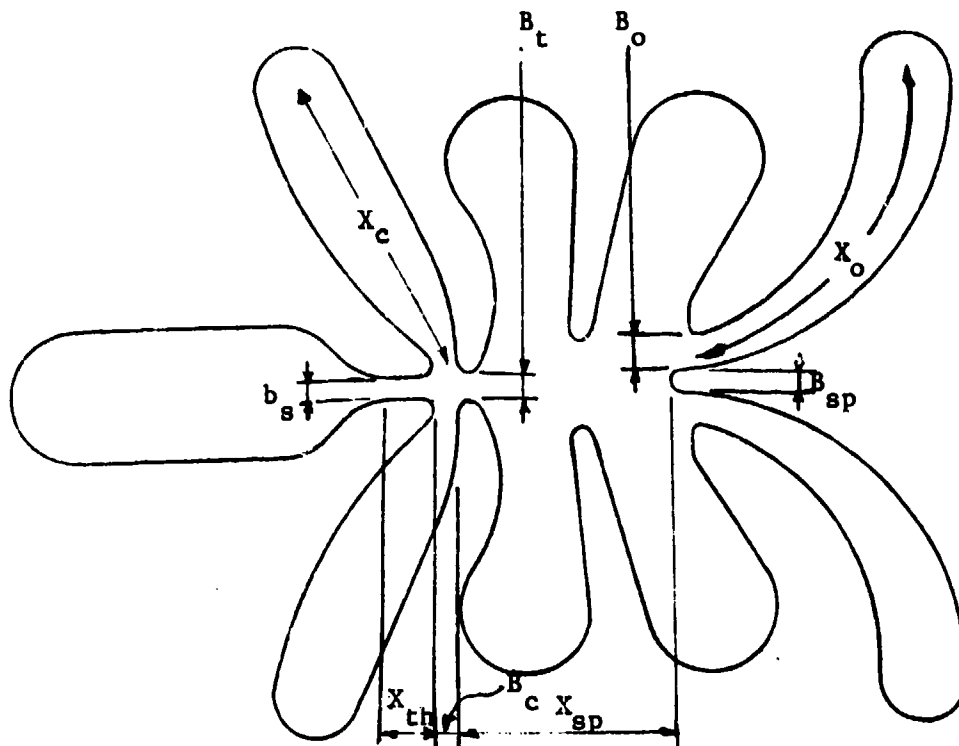


(b) linear channel resistance



(c) nozzle or nonlinear resistance

Figure 3. Primary fluidic C format integrated components.



- b_s = supply nozzle width
- σ = aspect ratio, h/b_s
- B_c = control port minimum width
- B_o = outlet port minimum width
- B_{sp} = splitter width
- B_t = downstream control edges spacing
- x_c = control port channel length
- x_o = outlet port channel length
- x_{th} = supply nozzle throat length
- x_{sp} = supply nozzle - splitter distance

Capitalized parameters are normalized to b_s .

Figure 4. Silhouette for $b_s = 0.5$ mm LPA in C Format

LPA's with aspect ratios less than one are commonly used in the design of multistage gain blocks. However, limited experimental data are available for LPA's of aspect ratio less than one. The work described in this section provides data and correlations for gain block and servovalve design using LPA's in this range of aspect ratios.

The supply condition of an LPA may be characterized by the modified Reynolds number

$$N'_R = \frac{N_R}{\left(1 + \frac{1}{\sigma}\right)^2 \left(1 + X_{th}\right)}$$

where

$$N_R = \frac{b_s}{v} \sqrt{\frac{2P_s}{\rho}}$$

ρ = fluid density

P_s = supply pressure, gage

σ = nozzle aspect ratio, h/b_s

Experimental data have been collected from three different C format LPA configurations (HDL 63020, HDL 72010 and HDL 61505) with aspect ratios of $\sigma = 0.667$, 0.55 and 0.333 and supply nozzle throat widths of 0.75 mm, 0.5 mm and 0.375 mm respectively. The characteristic dimensions are shown in Table 2. The LPA's have been tested under blocked-load conditions over a temperature range of 5.5°C (42°F) to 48°C (118°F) and a pressure range of 35 kPa (5 psi) to $11,032$ kPa (1600 psi). In all tests, the control bias pressures were adjusted to 5 percent of the supply pressure.

The analytical and experimentally measured blocked-load pressure gain are plotted against the modified Reynolds number in figure 5. The analytical model is based on the modified two-dimensional, incompressible, laminar jet deflection theory discussed by Drzewiecki et al.⁴ The experimental gains were determined from the slope of the blocked-load characteristics at the null position.

⁴T.M. Drzewiecki, D.N. Wormley and F.M. Manion, Computer Aided Design Procedure for Laminar Fluidic Systems, Journal of Dynamic Systems, Measurement and Control, 97, Series G, No. 4 (December 1975).

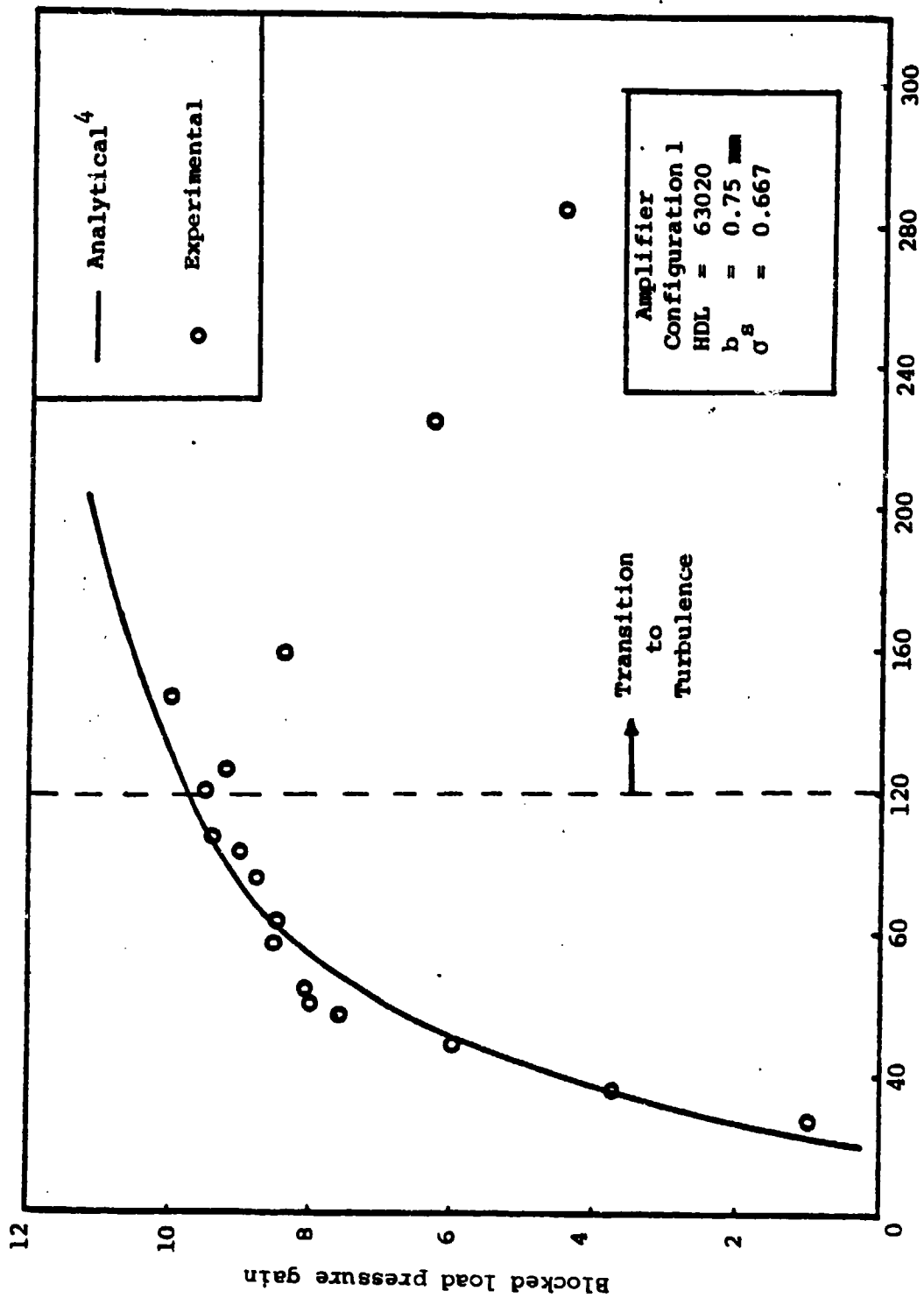


Figure 5. Comparison of theory and data of blocked load gain

TABLE 2 CHARACTERISTIC DIMENSIONS OF LPA's

HDL design	63020	72010	61505
b_s (mm)	0.75	0.5	0.375
	0.667	0.55	0.333
B_s	1.0	1.0	1.0
\bar{B}_c	3.08	4.0	4.733
x_c	8.875	13.312	21.
B_o	1.2	1.25	1.33
\bar{B}_o	2.667	2.875	3.6
X_o	14.875	16.56	22.08
B_t	1.25	1.125	1.167
B_{sp}	0.55	0.5	0.533
X_{th}	1.257	1.25	1.25
X_{sp}	8.0	8.0	8.0

The experimental data closely follow the analytical prediction up to $N'_R = 120$ beyond which transition-to-turbulence occurs and the theory based on laminar flow fails. In the turbulent flow regime, the flow noise increases, offset increases and the gain decreases. Therefore, the transition-to-turbulence establishes an upper design limit of operation for the LPA. In the laminar flow regime, the blocked-load pressure gain increases as the Reynolds number increases.

A guideline to determine the point of transition from laminar to turbulence for fluidic devices (when $X_{sp} = 8$ to 10) has been discussed by Drzewiecki et al.⁵

$$\frac{C_d N'_R}{\left(1 + \frac{1}{\sigma}\right)^2} = 200 \quad (2)$$

where C_d = volumetric discharge coefficient, $f(N'_R)$ or the expression may be written as

⁵T.M. Drzewiecki and F.M. Manion, Fluierics 40: LJARS, The Laminar Jet Angular Rate Sensor, HDL-TM-79-7, Harry Diamond Laboratories (December 1979).

$$C_d N'_R \Big|_{tr.} = \frac{200}{1+X_{th}} \quad (3)$$

For $X_{sp} = 8$ and $X_{th} = 1.25$, the point of transition from laminar to turbulence occurs at $N'_R \approx 120$.

The lower operating limit of the amplifier may be predicted from the information on the control edge clearance. The amplifier ceases to function if the jet cannot deflect. The distance from the control edge to the jet edge, based on the assumption that the jet spreads linearly, is given by Manion et al.⁶

$$B_v = \frac{1}{2} \left[B_t - 1 - \frac{B_c}{0.0278 C_d^3 N'_R / C_\theta} \right] \quad (4)$$

where

B_v = distance between control edge and jet edge
 C_θ = momentum flux coefficient.

With $C_\theta \approx 1.32 C_d^2$ and $B_v = 0$, the expression may be written as

$$C_d N'_R = \frac{47.5 B_c}{(B_t - 1) \left(1 + \frac{1}{\sigma}\right)^2 (1 + X_{th})} \quad (5)$$

The average value of $C_d N'_R$ for the three amplifier configurations is approximately equal to 10 and the point at which the LPA fails to function occurs at $N'_R \approx 22$.

The experimental data obtained for the blocked-load pressure gain of the three different LPA configurations are plotted in figure 6. The effect of the modified Reynolds number on the blocked-load pressure gain may be summarized by noting the four regions defined in the following paragraphs.

In region (1), $0 \leq N'_R < 40$, the blocked-load pressure gain is less than 50 percent of its maximum value. In all three different con-

⁶F.M. Manion and T.M. Drzewiecki, Analytical Design of Laminar Proportional Amplifiers, Proceedings of the HDL Fluidic State-of-the-Art Symposium, 1, Harry Diamond Laboratories (October 1974).

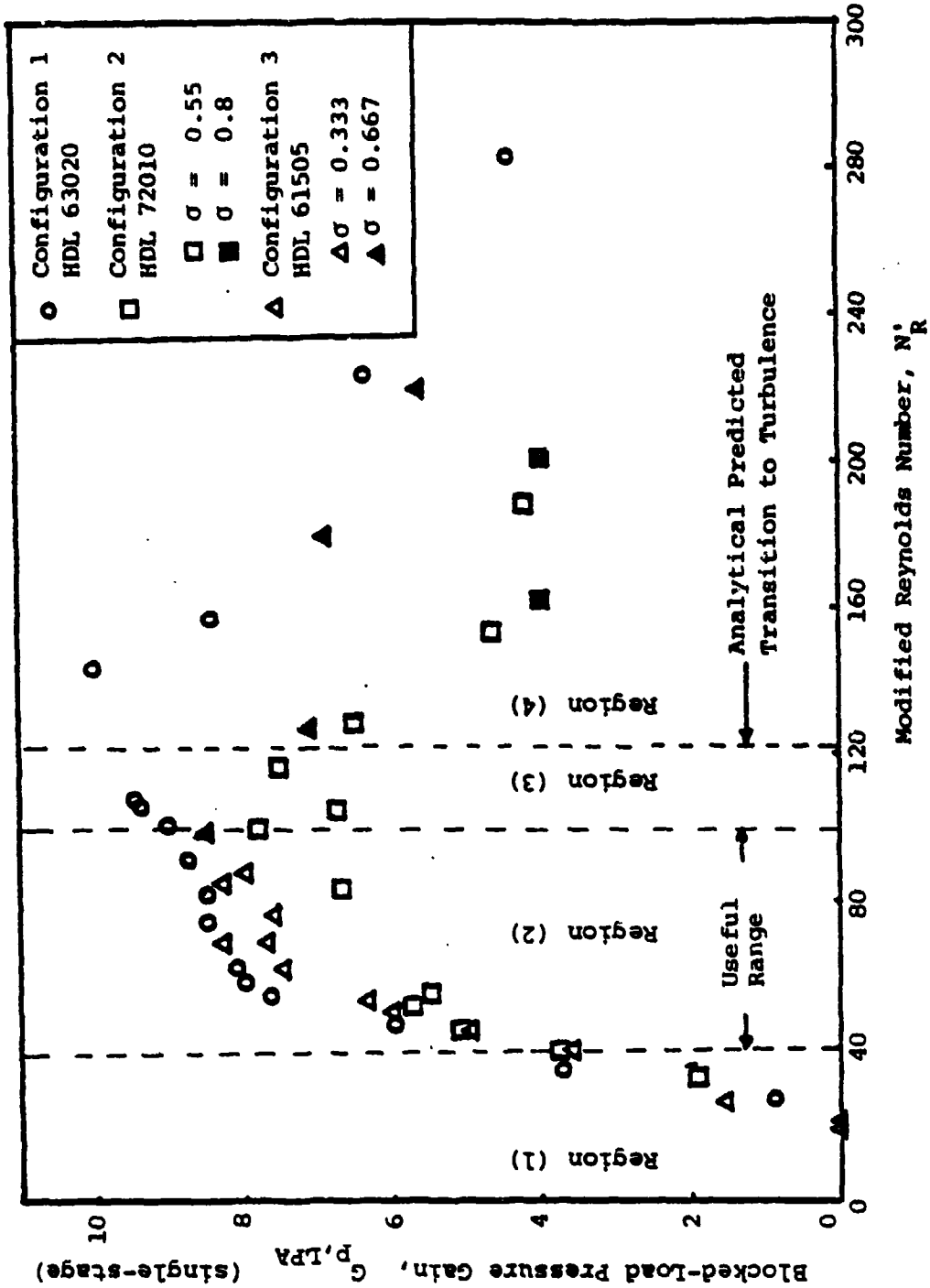


Figure 6. Experimental data illustrating the operating range of LPA.

figurations tested, the LPA gain is zero for $N'_R \leq 20$.

In region (2), $40 \leq N'_R \leq 100$, the typical LPA operating range is bounded by two limits, a lower limit below which the LPA gain is too low for use and an upper limit beyond which transition-to-turbulence occurs.

In region (3), $100 \leq N'_R < 120$, just before the analytical predicted point of transition-to-turbulence, the experimental data are scattered. This uncertainty suggests that the point of transition-to-turbulence is in this region.

In region (4), $N'_R \geq 120$, the blocked-load pressure gain decreases and noise increases since the LPA's are operated beyond the transition-to-turbulence.

2.2 Fluidic Channel Resistance

The channel resistor is one of the important elements in fluidic circuits. In general, the channel resistance may be represented as a laminar, fully-developed duct resistance. The channel resistance consists of a linear portion due to the fully developed viscous dissipative flow in the channel plus a nonlinear portion due to the entrance region pressure drop. A general expression for a channel resistance given by Drzewiecki⁷ is

$$R = \frac{12 \mu x}{(\bar{b}h)^2} \left[\sigma_c \left(1 + \frac{1}{\sigma_c^2} \right) + C \right] + \frac{0.475 \rho Q}{(bh)^2} \quad (6)$$

where

$$\text{for } 1 \leq \sigma_c \leq 2, \quad 0.35 \leq C \leq 0.5;$$

$$\text{for } \sigma_c > 2, \quad C = 0.5,$$

x = channel length in the direction of flow,

\bar{b} = average channel length,

b = minimum channel width,

Q = volumetric flow through duct,

σ_c = channel aspect ratio, $\frac{h}{b}$

⁷T.M. Drzewiecki, Fluierics 37. A General Planar Nozzle Discharge Coefficient Representation, HDL-TM-74-5, Harry Diamond Laboratories, (1974).

- μ = absolute fluid viscosity,
 C = empirical constant.

For the case where the channel length is much longer than the entrance length, the nonlinear term may be neglected. An analytical study on the hydrodynamic entrance length for incompressible flow in rectangular ducts has been performed by Han.⁸ The experiments to verify the analysis of Han for aspect ratios of 5 and 2 have been performed by Sparrow et al.⁹ The results of these studies to determine the entrance length may be summarized as

$$L_e = 0.055 \left(\frac{\sigma_c}{1 + \sigma_c} \right)^2 N_{R_c} \quad \text{for } \sigma_c = 5,$$

$$L_e = 0.127 \left(\frac{\sigma_c}{1 + \sigma_c} \right)^2 N_{R_c} \quad \text{for } \sigma_c = 2,$$

where

- L_e = normalized entrance length, l_e/b
 N_{R_c} = channel Reynolds number, referred to b .

For flow between parallel-plates, Schlichting¹⁰ has derived an expression for the entrance length as

$$\frac{L_e}{\sigma_c^2 N_{R_c}} = 0.04 \quad \text{for } b \gg h.$$

If the assumption of fully developed flow is justified and the entrance length can be neglected, the flow can be described by Poiseuille flow between parallel plates and the expression for the resistance may be stated as

$$R_c = \frac{12\mu x}{bh^3} \quad \text{for } b \gg h. \quad (7)$$

⁸L.S. Han, Hydrodynamic Entrance Lengths for Incompressible Flow in Rectangular Ducts, Journal of Applied Mechanics, 27, Trans. ASME (1960).

⁹E.M. Sparrow, C.W. Hixon and G. Shavitt, Experiments on Laminar Flow Development in Rectangular Ducts, Journal of Basic Engineering, Trans. ASME (March 1976).

¹⁰M. Schlichting, Boundary Layer Theory, McGraw-Hill, New York, New York, (1960).

The standard nozzle, 5221A-20 shown in figure 3, has been used as a channel resistor in the design of the gain block. Since the channel length is much longer than the entrance length of the flow for a wide range of Reynolds numbers, the quasi-fully-developed assumption is justified, and equation (6) may be applied. Normalizing equation (6) to the linear portion, the expression for resistance is

$$\bar{R} = 1 + \frac{0.475}{12} \left(\frac{\bar{b}}{b} \right)^2 \frac{\left(\sigma + \frac{1}{\sigma} + 2 \right)}{\left(\frac{h}{\bar{b}} + \frac{\bar{b}}{h} + c \right)} \cdot \frac{1 + X_{th}}{X} C_d N_R' \quad (8)$$

where

$$\bar{R} = \frac{R}{\left[\frac{12\mu x}{(\bar{b}h)^2} \left(\frac{h}{\bar{b}} + \frac{\bar{b}}{h} + c \right) \right]}$$

The nozzle resistance as a function of modified Reynolds numbers has been determined experimentally. The range of temperatures and the pressure drops across the nozzle are from 6°C to 48°C and from 5516kPa to 10170 kPa respectively. The experimentally determined nozzle resistance is compared with analytically predicted values using equation (8) as a function of modified Reynolds numbers in figure 7. The experimental data falls within 10 percent of the predictions in the range of N_R' tested.

3. FLUIDIC GAIN BLOCK AND SERVOVALVE

The fluidic servovalve consists of a multi-stage LPA gain block and a set of laminar flow resistors. The gain block is a basic power amplifier while the resistors are used to provide feedback and summing functions.

3.1 Gain Block Configuration and Characteristics

The analytical design of the fluidic gain block to predict the essential characteristics as a function of individual stage operating Reynolds number, control bias pressure and the detailed geometry of the LPA has been discussed by Manion et al.^{4,11}

⁴T.M. Drzewiecki, D.N. Wormley and F.M. Manion, Computer-Aided Design Procedure for Laminar Fluidic Systems, Journal of Dynamic Systems, Measurement and Control, 97, Series G, No. 4 (December 1975).

¹¹F.M. Manion and G. Mon, Fluercs 33: Design and Staging of Laminar Proportional Amplifiers, HDL-TR-1608, Harry Diamond Laboratories (September 1972).

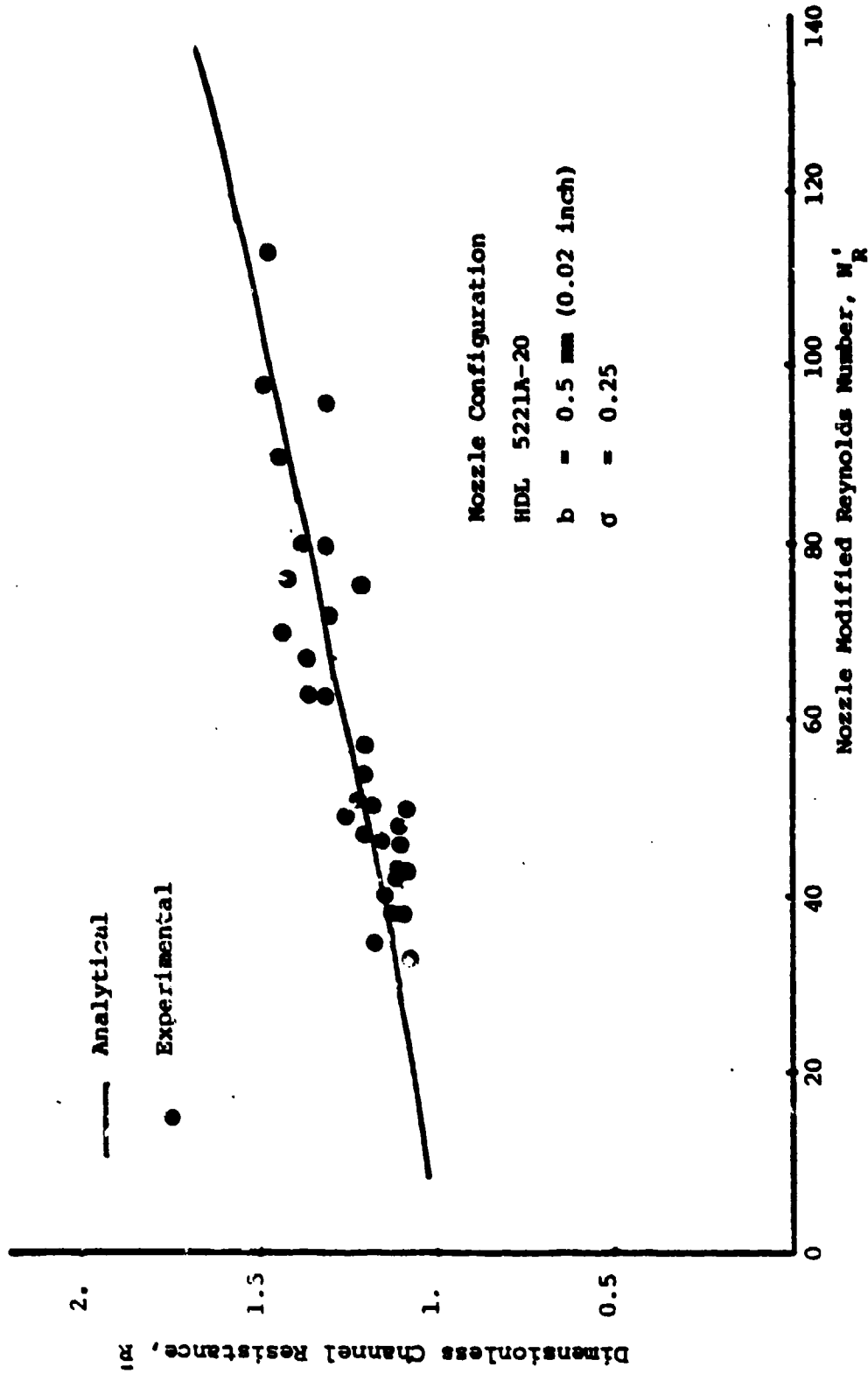


Figure 7. Comparison of analytical and experimental nozzle resistance.

The general design criteria of a gain block are as follows:

- (1) Maximize the laminar operating range by matching the modified Reynolds numbers, of each stage:

$$N'_{R1} = N'_{R2} = N'_{R3}.$$

- (2) Achieve 90° phase shift bandwidth requirement:

$$f_{90^\circ} = \frac{\left(\frac{\pi}{2}\right)}{2\pi \sum_{i=1}^3 \frac{4x_{sp}}{C_{di} \sqrt{\frac{2P_{si}}{\rho}}}}$$

- (3) Maximize the blocked-load pressure gain:

$$K_p = \frac{K_1 \cdot K_2 \cdot K_3}{\left(1 + \frac{R_{01}}{R_{12}}\right) \left(1 + \frac{R_{02}}{R_{13}}\right)}$$

where K_1 , K_2 and K_3 are blocked-load pressure gain of 1st, 2nd and 3rd stages LPA respectively. R_{01} and R_{02} are output resistance of the 1st and 2nd stages and R_{12} and R_{13} are input resistance of the 2nd and 3rd stages.

- (4) Maximize the input-to-output resistance ratio:

$$R_{i1}/R_{03}.$$

- (5) Minimize the quiescent flow draw:

$$Q_s = \sum_{i=1}^3 Q_{si},$$

where Q_{si} ($i = 1, 2, 3$) are supply flows of the 1st, 2nd and 3rd stages. An iterative design procedure is generally required to achieve a design which meets (if possible) the above design criteria.

The gain block shown in figure 8 has been designed using the guidelines cited above.

The supply pressure of the three stage gain block is connected directly to the final stage of the gain block. The first and second

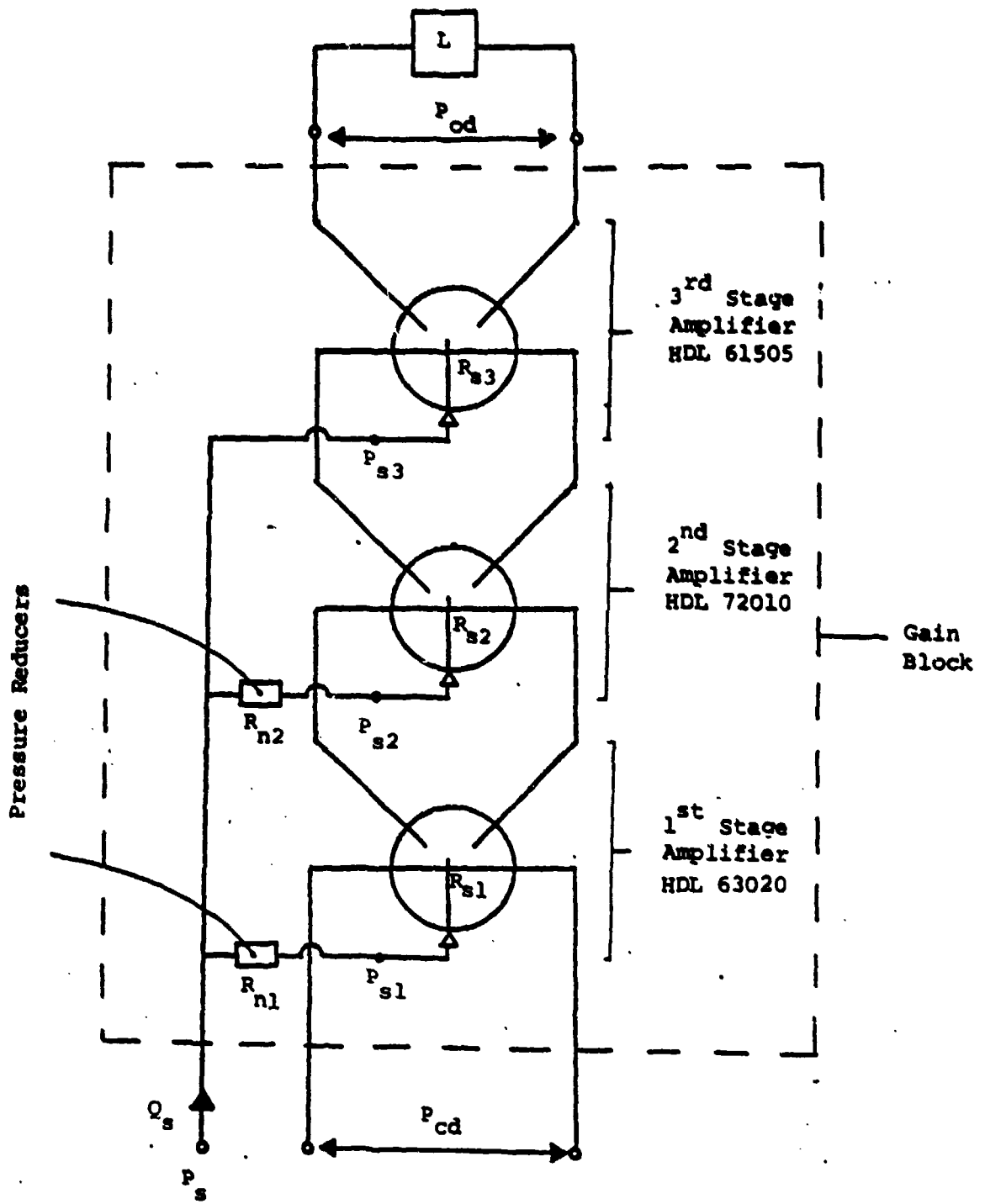


Figure 8. Gain block schematics.

stages are supplied by reducing the main pressure through the pressure reducers which are a number of nozzles in parallel.

The first and second stage supply pressures depend on the final stage supply condition with respect to the fluid properties. The supply pressure of i^{th} stage, P_{si} may be expressed as

$$\frac{P_{si}}{P_s} = \frac{1}{1 + \frac{m_i}{n_i} \frac{R_{ni}}{R_{si}}} \quad (9)$$

where

- m_i = no. of LPA's in parallel of i^{th} stage,
- n_i = no. of resistor nozzles in parallel of i^{th} stage,
- R_{si} = LPA supply resistance of i^{th} stage,
- R_{ni} = nozzle resistance of i^{th} stage.

As the nozzle resistance, R_{ni} , and the supply resistance, R_{si} are connected in series, the flow through R_{ni} and R_{si} are related by the continuity equation as

$$\frac{Q_{ni}}{Q_{si}} = \frac{m_i}{n_i} \quad (10)$$

With equation (10), the ratio of the nozzle resistance, R_{ni} , to the supply resistance, R_{si} , may be expressed as

$$\frac{R_{ni}}{R_{si}} = \frac{24 X_{ni}}{\bar{B}_{ni}^2} \left[\frac{\sigma_i}{H_{ni}^2} \right] \cdot \left[\frac{H_{ni}}{\bar{B}_{ni}} + \frac{\bar{B}_{ni}}{H_{ni}} + C \right] \cdot \frac{C_{di}}{N_{Ri}} + 0.95 \left[\frac{\sigma_i}{\bar{B}_{ni} H_{ni}} \right]^2 \frac{m_i}{n_i} C_{di}^2 \quad (11)$$

where

- σ_i = LPA aspect ratio,
- X_{ni} = normalized nozzle length, x_{ni}/b_{si} ,
- \bar{B}_{ni} = normalized nozzle average channel length, \bar{b}_{ni}/b_{si} ,
- B_{ni} = normalized nozzle throat width, b_{ni}/b_{si} ,
- H_{ni} = normalized nozzle height, h_{ni}/b_{si} ,

$$1 \leq \frac{H_{ni}}{\bar{B}_{ni}} \leq 2, \quad 0.35 \leq C \leq 0.5; \quad \frac{H_{ni}}{\bar{B}_{ni}} > 2, C = 0.5.$$

Subscript i refers to the i^{th} stage.

The Reynolds number of the first and second stage LPA may be related to that of the final stage as

$$N_{Ri} = \frac{b_{si}}{b_{sf}} \sqrt{\frac{P_{si}}{P_s}} N_{Rf} \quad (12)$$

where

- b_{si} = LPA supply nozzle throat width, i^{th} stage,
- b_{sf} = LPA supply nozzle throat width, final stage,
- N_{Ri} = Reynolds number of i^{th} stage,
- N_{Rf} = Reynolds number of final stage.

As the first and second stage supply pressures are an implicit function of the final stage Reynolds number, N_{Rf} , the first and second stage operating Reynolds numbers depend only on the final stage Reynolds number. In the following discussions, the gain block operating Reynolds number is referred to the operating Reynolds number of the final stage, N_{Rf} . The first and second stage Reynolds numbers can be related to the final stage by solving equations (9) through (12) simultaneously.

In the report by Wormley et al.² a hyperbolic tangent curve has been used to describe the nonlinear saturation characteristics of the gain block. The output pressure/flow characteristics of the gain block may be expressed as

$$\frac{Q_L}{Q_{Ls}} = \tanh \frac{P_{cd}}{P_{cds}} - \frac{P_{od}}{P_{ods}} \quad (13)$$

where

- Q_L = output load flow,
- P_{od} = amplifier output pressure differential,
- P_{cd} = amplifier input pressure differential,

²D.N. Wormley, D. Lee, and K-M Lee, Development of a Fluidic, Hydraulic Servovalve, HDL-CR-81-216-1, Harry Diamond Laboratories (February 1981).

Q_{Ls} = saturation output load flow,
 P_{ods} = saturation amplifier output pressure differential,

and where the saturation control pressure differential is defined as

$$P_{c ds} = \frac{P_{ods}}{K_f} = \frac{Q_{Ls}}{K_q} \quad (14)$$

with the incremental amplifier static pressure gain K_p and flow gain, K_q defined as

$$K_p = \left. \frac{\partial P_{od}}{\partial P_{cd}} \right|_{Q_L = 0} \quad (15)$$

$$K_q = \left. \frac{\partial Q_L}{\partial P_{cd}} \right|_{P_{od} = 0} \quad (16)$$

A three-stage fluidic gainblock with a single supply pressure based on the standard packaging technique was constructed and tested. The construction schematic of the gain block is shown in figure 9. The stacking order is listed in appendix A. The characteristic dimensions of the amplifier laminates and the three stage amplifier parameters, measured with Univis J-43 at a temperature of 27°C, are summarized in table 3. The experimental output characteristics are displayed in figure 10. The comparison between the predicted and the experimentally measured characteristics displayed in figure 11 shows that the analytical model with hyperbolic tanh curve closely matches the experimental data.

3.2 Fluidic Servovalve Configuration and Characteristics

The conceptualization, analysis and design of a fluidic servovalve constructed from the gainblock and fluidic resistance elements in a breadboard configuration are described by Wormley et al.². The flow feedback resistance in the case in which the net flow feedback is equal to zero can be eliminated. In order to minimize the loss of output flow due to feed-

²D.N. Wormley, D. Lee, and K-M. Lee, Development of a Fluidic, Hydraulic Servovalve, HDL-CR-81-216-1, Harry Diamond Laboratories (February 1981).

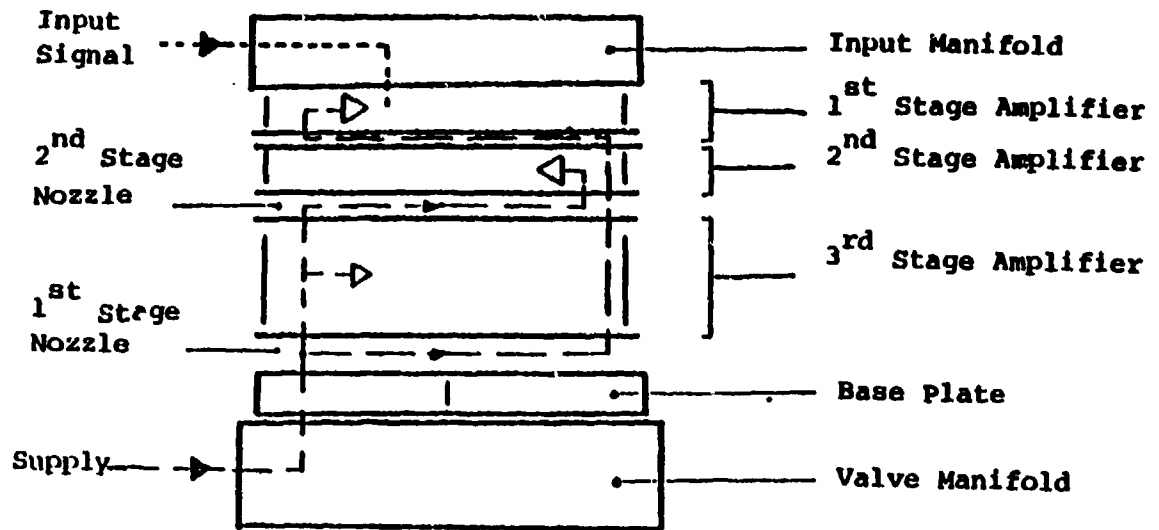


Figure 9. Gain block construction schematics.

TABLE 3 GAIN BLOCK CONFIGURATION AND INCREMENTAL PARAMETERS
LAMINATE DESCRIPTION

Stage	Design	b_s (mm)	$\sigma = h/b_s$	Number of Sections
1	HDL 63020	0.75	0.667	2
2	HDL 72010	0.5	0.55	3
3	HDL 61505	0.375	0.333	6
EXPERIMENTAL DATA				
P_s	6895	kPa	1000	psi
P_{ods}	2551	kPa	370	psi
Q_{Ls}	8×10^{-6}	m^3/sec	0.5	cis
$P_{c ds}$	8.72	kPa	35	in.H ₂ O
K_p	277			
K_q	8.6×10^{-7}	$m^3/sec/kPa$	0.35	cis/psi
R_a	5.80×10^{10}	$N-s/m^5$	140	psi/cis

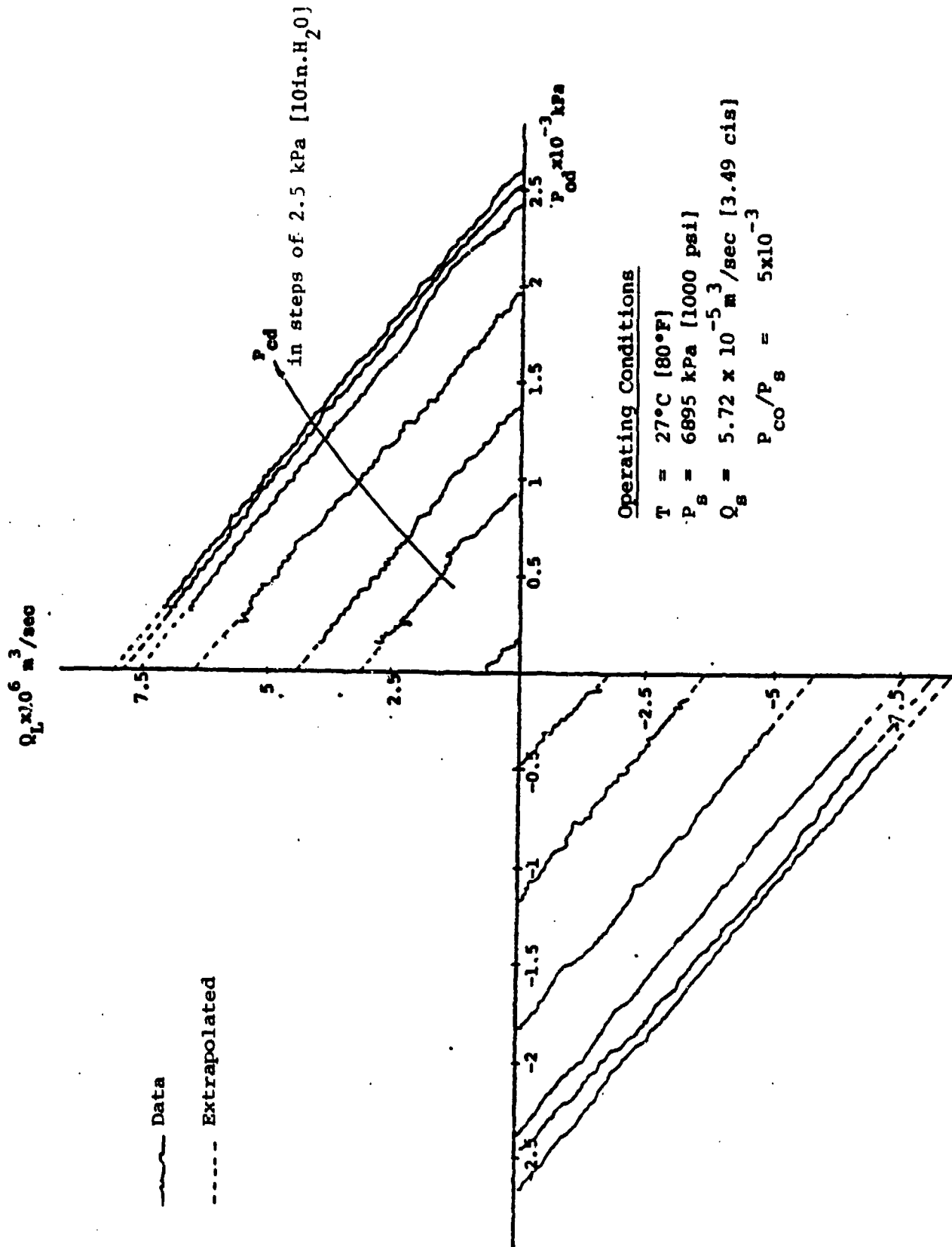


Figure 10. Experimental gain block output characteristics.

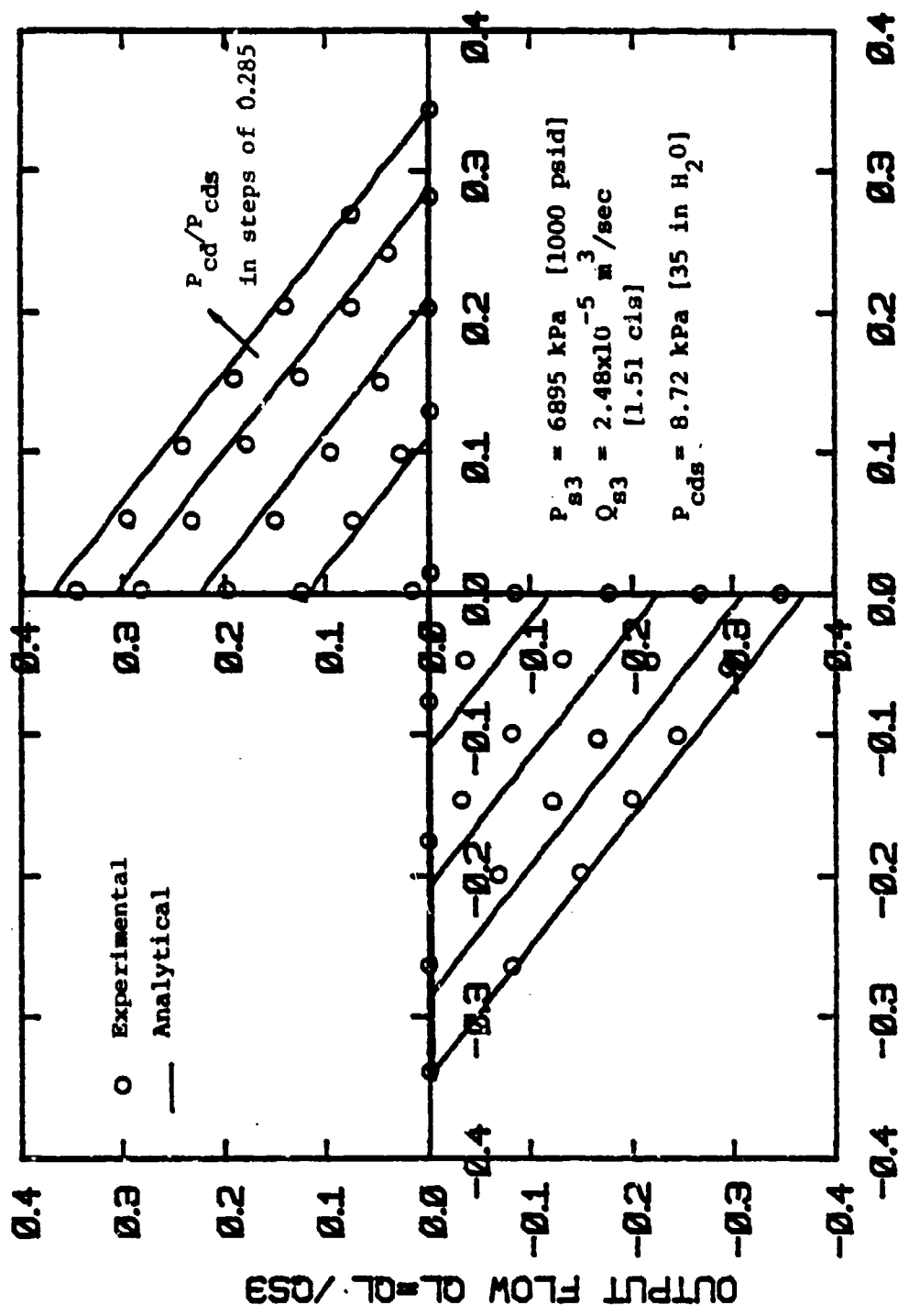


Figure 11. Comparison of computer-aid design prediction and experimental gain block output characteristics.

back and the complexity of the valve construction, the case of zero flow feedback is chosen for the performance evaluation. In this particular case, the resulting nonlinear normalized governing equation of the valve becomes

$$\frac{Q_L}{Q_{Ls}} + \frac{P_{od}}{P_{ods}} = \tanh \left[\alpha \frac{P_{id}}{P_{idm}} + \gamma \frac{P_{od}}{P_{ods}} \right] \quad (17)$$

where

P_{idm} = maximum input pressure differential

$$\alpha = \left(\frac{1}{1 + \frac{R_i}{R_a}} \right) \frac{P_{idm}}{P_{cds}} \quad \text{for } R_{fp} \gg R_i \quad (18)$$

$$\gamma = \frac{R_i}{R_{fp}} \left(\frac{1}{1 + \frac{R_i}{R_a}} \right) K_p \quad (19)$$

R_i = input resistance,

R_{fp} = pressure feedback resistance,

R_a = amplifier input deflection resistance.

The schematic drawing of the servovalve is shown in figure 12.

The fluidic servovalve steady state blocked-load pressure gain and no-load flow gain can be obtained from the linearized valve model as

$$G_{qs} = \left. \frac{\partial Q_L}{\partial P_{id}} \right|_{P_{od}=0} = \frac{K_q}{1 + \frac{R_i}{R_a}} \quad (20)$$

$$G_{ps} = \left. \frac{\partial P_L}{\partial P_{id}} \right|_{Q_L=0} = \frac{K_p}{(1-\gamma) \left(1 + \frac{R_i}{R_a} \right)} \quad (21)$$

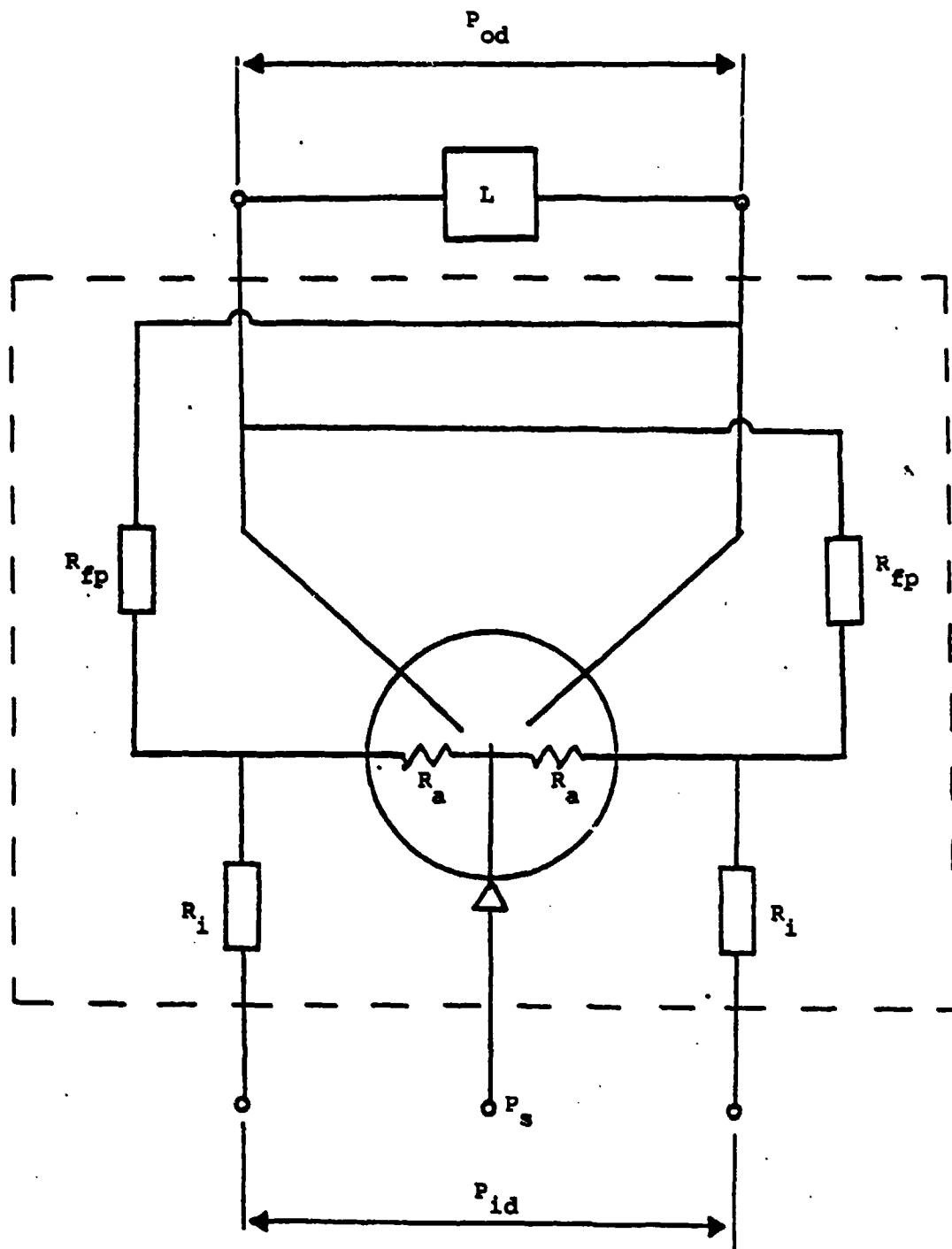


Figure 12. Servovalve schematic.

The steady state performance of the servovalve is characterized by the parameters α and γ . The valve parameter α indicates the flow gain linearity with respect to the maximum input pressure differential whereas the parameter γ provides information regarding the limit of servovalve stability.

As shown in equation (21), the servovalve pressure gain is sensitive to the valve parameter γ . The fluidic servovalve has a maximum pressure gain at γ equal to one and has a negative pressure gain for γ greater than one. The valve is unstable when the valve pressure gain curve has negative slope.

The effect of a variation in α is illustrated in figure 13. With $\gamma = 1$ to achieve maximum pressure gain, the servovalve flow gain becomes more non-linear as α is increased.

An integrated component fluidic servovalve has been constructed and tested. The gain block discussed in the preceding section has been used in the servovalve design. Two HDL 5196 capillaries are connected in series to form an input resistor R_i . The pressure feedback resistor R_{fp} consists of four parallel HDL 5026 capillaries in series, with a HDL 5027 capillary. The experimentally measured resistances at the temperature of 27°C (80.6°F) are:

$$R_i = 4.42 \times 10^{10} \text{ N-s/m}^5 \quad (105 \text{ psi/cis}) \text{ and}$$

$$R_{fp} = 7.52 \times 10^{12} \text{ N-s/m}^5 \quad (17850 \text{ psi/cis}).$$

The servovalve construction schematic is shown in figure 14. The stacking order is summarized in appendix A.

The experimental data obtained at a temperature of 27°C and a supply pressure of 6895 kPa (1000 psi) showing the output characteristics are displayed in figure 15 and compared with the analytical prediction in figure 16. Apart from the offset, the analytical prediction fits the experimental characteristics well.

3.3 Temperature Effects and Compensation

For incompressible flow, the working fluid temperature affects the Reynolds number, $N_R = (b_s / \nu) \sqrt{2P_s / \rho}$, through an influence on the fluid

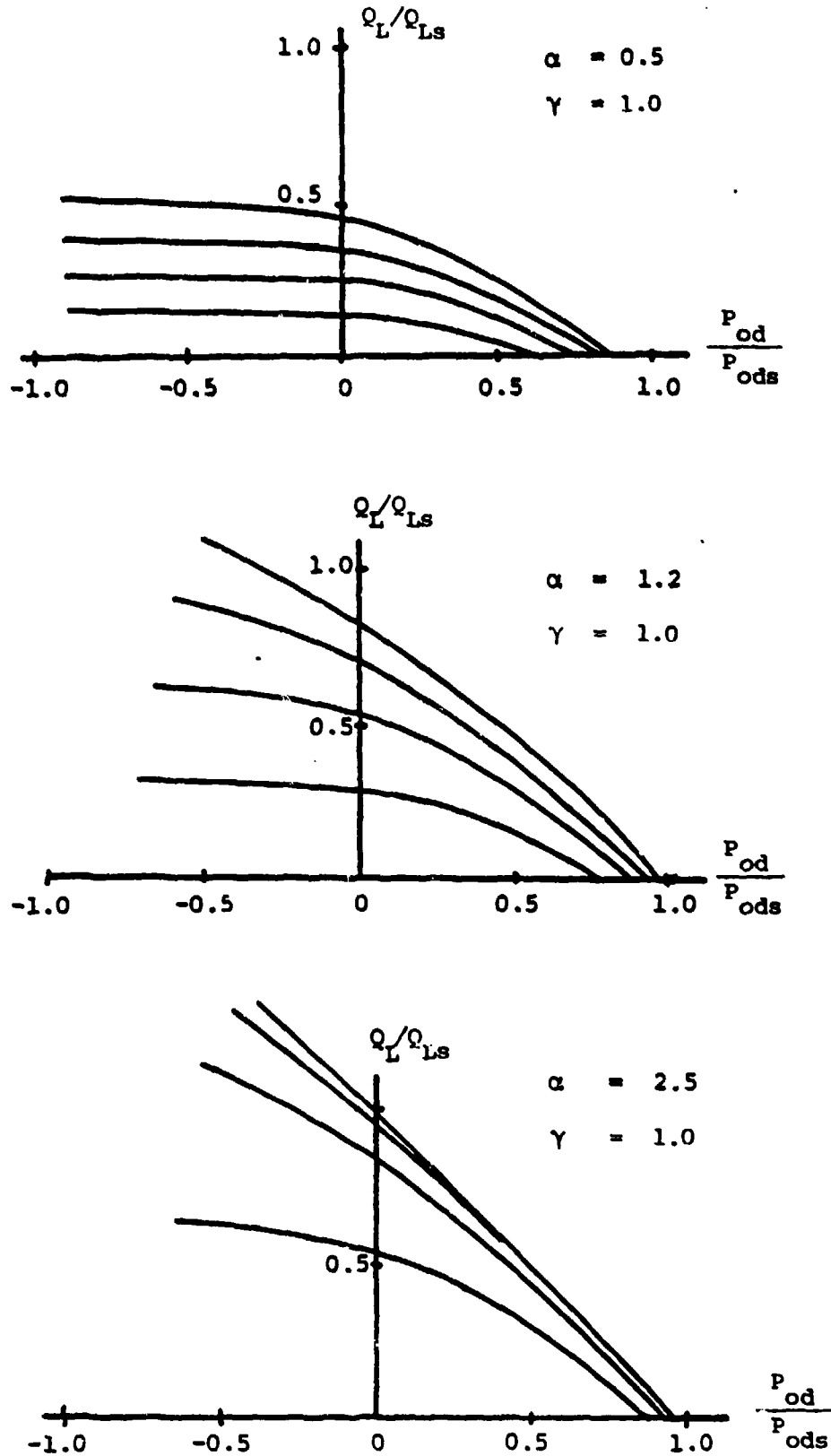


Figure 13. Effect of valve parameter α on Valve Characteristics.

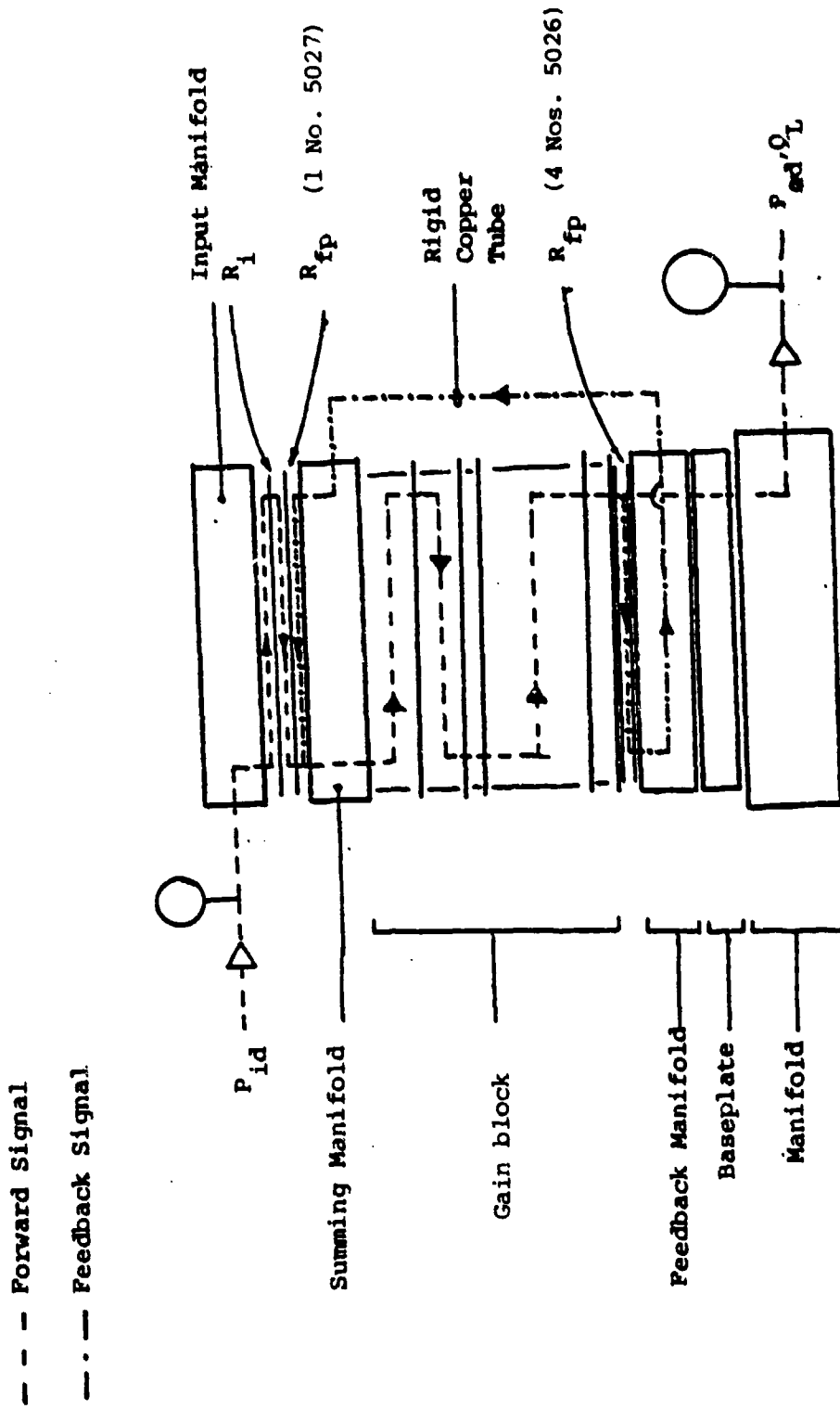


Figure 14. Servovalve construction schematics.

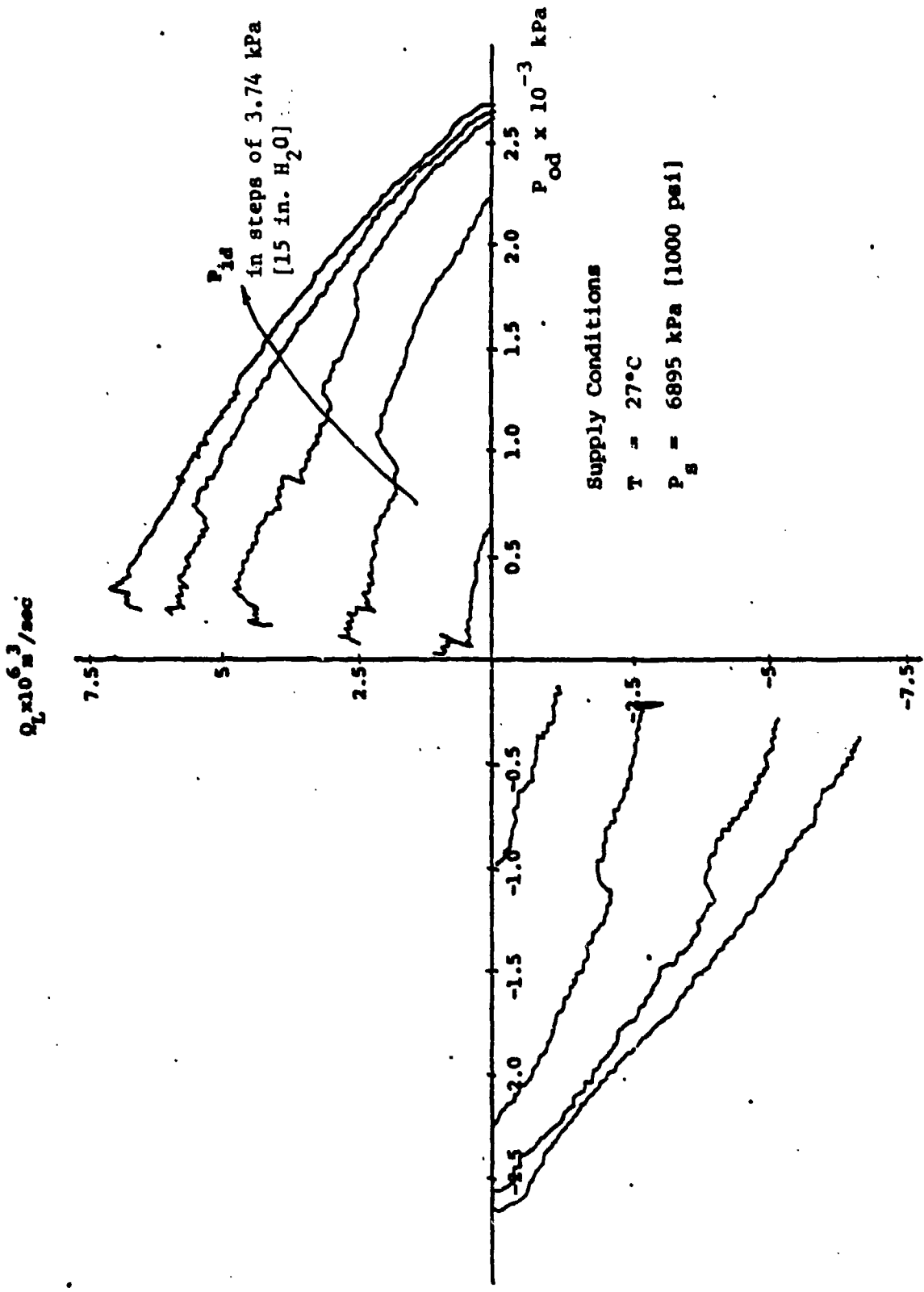


Figure 15. Experimental data of servovalve output characteristics.

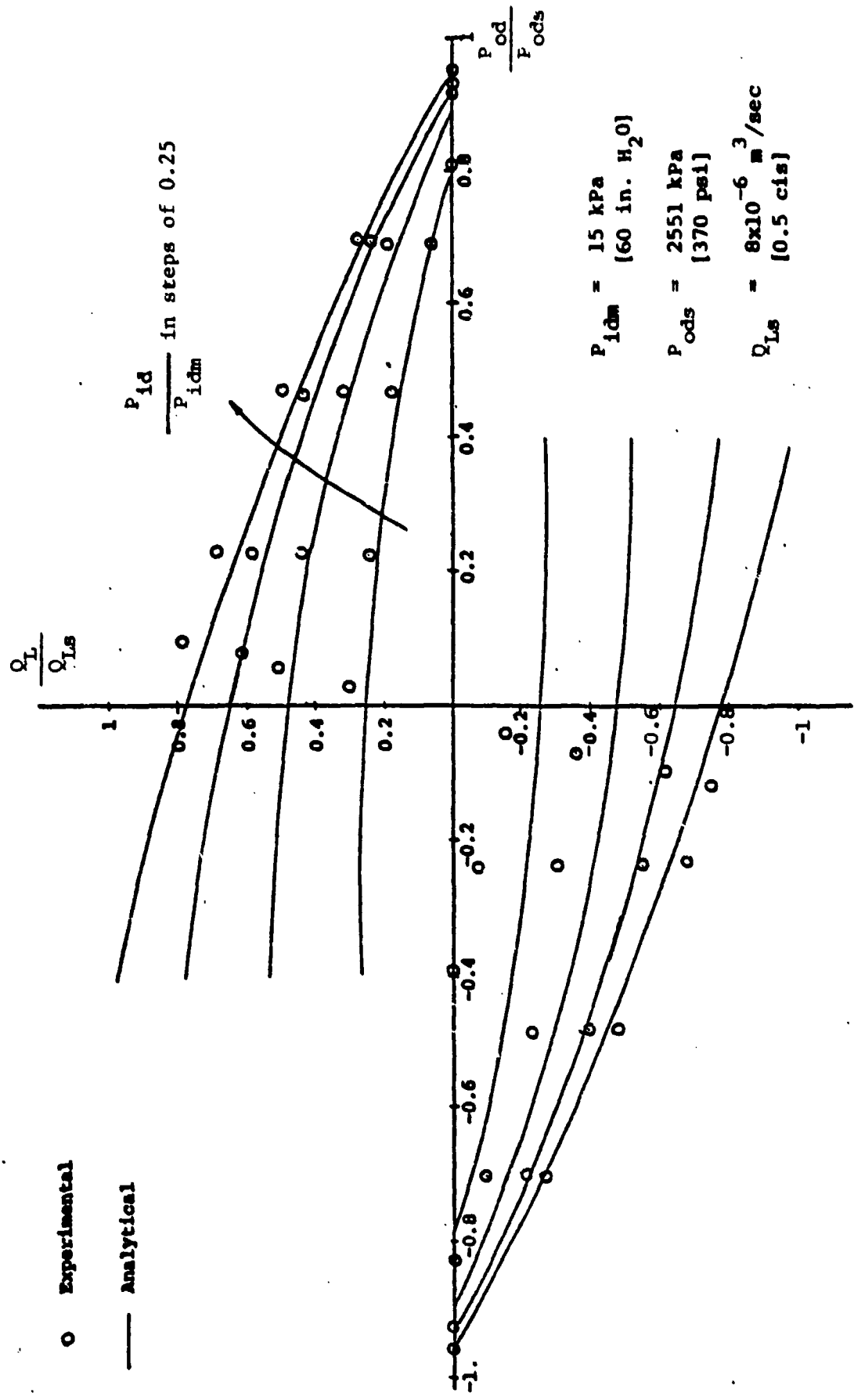


Figure 16. Comparison of experimental and analytical servovalve output characteristics.

viscosity. The effect of the change of operating Reynolds number on the blocked-load pressure gain of the LPA has been discussed in section 2.1.

The stability of the fluidic servovalve is primarily determined by the valve parameter γ which is a measure of the degree of positive pressure feedback. The value of γ can be increased by decreasing the pressure feedback resistance, or increasing the gain block pressure gain, K_p , or the value of input resistance to the point where γ is greater than one and the valve fails neutrally. The additional flow of the positive pressure feedback due to the increase in temperature tends to decrease the valve stability. On the other hand, if the positive feedback flow is reduced as a result of a decrease in temperature, the valve behaves as an amplifier with reduced feedback. To compensate for the temperature effects, the valve parameter γ must be kept at a desired constant value in the temperature range concerned. Since the ratio of two linear resistances is independent of fluid viscosity and the factor $1/(1 + R_i/R_a)$ is not significantly affected by temperature variations, the valve parameter γ is primarily dependent on the blocked-load pressure gain of the gain block, K_p .

The valve parameter α is proportional to the ratio of maximum input pressure differential, P_{idm} , to the saturation control pressure differential P_{cds} . The saturation control pressure differential, P_{cds} , decreases as the temperature increases. The maximum input pressure differential must be limited in order to keep the flow gain in a reasonable linear range. However, the linearity of the servovalve flow gain is maintained at the expense of the maximum input pressure differential, P_{idm} .

Since the gain block characteristic performance is primarily a function of final stage Reynolds number, this provides a means of temperature compensation by maintaining a constant operating Reynolds number, N_{Rf} . From the definition of the Reynolds number and the kinematic viscosity-temperature relation as written in equation (1), we have

$$\frac{N_{Rf}(T)}{N_{Rf}(T_o)} = \frac{v_o}{v} \sqrt{\frac{P_s(T)}{P_s(T_o)}} = e^{\lambda(T-T_o)} \sqrt{\frac{P_s(T)}{P_s(T_o)}} \quad (22)$$

If $N_{R_f}(T) = N_{R_f}(T_o) = \text{constant}$, then

$$\frac{P_s(T)}{P_s(T_o)} = e^{-2\lambda(T-T_o)}. \quad (23)$$

Hence, the supply pressure must be varied directly proportional to the square of the fluid viscosity in order to maintain a constant Reynolds number. To decrease the high pressure required at the low temperature operating condition, the supply pressure is scheduled as a linear function of temperature, i.e.

$$\frac{P_s(T) - P_s(T_o)}{T - T_o} = \lambda_o. \quad (24)$$

The choice of λ_o depends on the temperature range considered and the maximum of safe supply pressure imposed by the hydraulic plant at the lowest temperature of interest. As an example, consider the following,

Reference temperature, $T_o = 25^\circ\text{C} (77^\circ\text{F})$,

Reference pressure, $P_s(T_o) = 6895 \text{ kPa} (1000 \text{ psi})$,

Temperature range, $10^\circ\text{C} < T < 50^\circ\text{C}$, $(50^\circ\text{F} \leq T \leq 122^\circ\text{F})$,

Maximum supply pressure, $P_s \Big|_{\text{max}} = 11,032 \text{ kPa} (1600 \text{ psi})$,

It follows $\lambda_o = 275.8 \text{ kPa}/^\circ\text{C} [22.2 \text{ psi}/^\circ\text{F}]$.

The experimental data for linearly compensated and uncompensated gain block and servovalve blocked-load pressure gain as a function of temperature are shown in figures 17 and 18. The temperature compensation based on the supply pressure scheduling significantly reduces the temperature sensitivity of both the gain block and servovalve pressure gain and successfully extends the operating range of the servovalve beyond the design temperature.

3.4 Dynamic Response

The fluidic servovalve dynamic model for small derivatives may be expressed as

$$Q_L(s) = G_q(s)P_{id}(s) - G_{qp}(s)P_{od}(s) \quad (25)$$

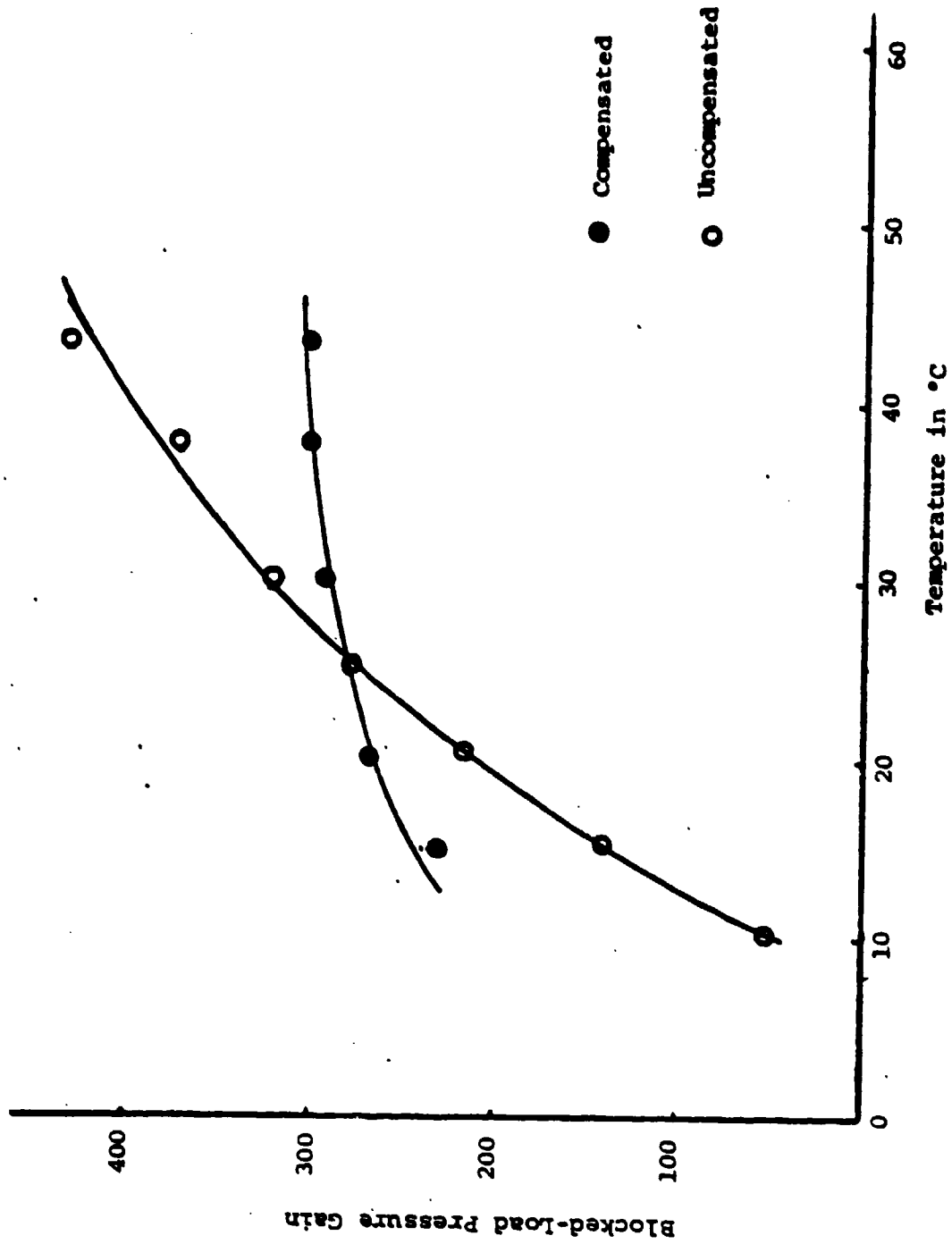


Figure 17. Gair block compensated and uncompensated blocked-load pressure gain.

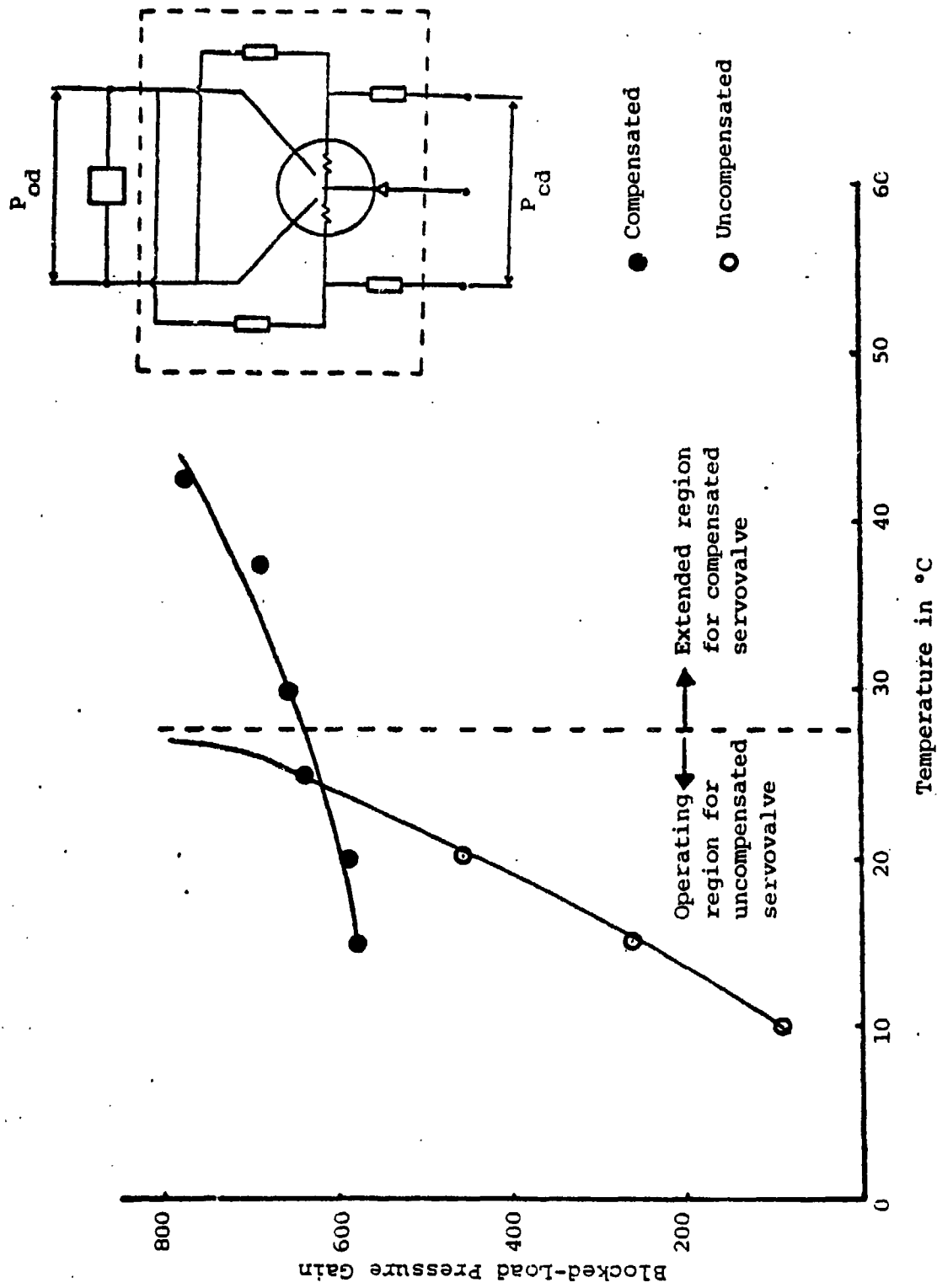


Figure 18. Fluidic servo valve compensated and uncompensated blocked-load pressure gain.

where

$$G_q(s) = \left[\frac{1}{1 + \frac{Z_i(s)}{Z_a(s)}} \right] K_q(s), \quad (26)$$

$$G_{qp}(s) = G_p(s)[1 - \gamma(s)]K_{qp}(s). \quad (27)$$

$$G_p(s) = \frac{K_p(s)}{[1 - \gamma(s)] \left[1 + \frac{Z_i(s)}{Z_a(s)} \right]}, \quad (28)$$

$$\gamma(s) = \frac{Z_i(s)}{Z_{fp}(s)} \cdot \frac{K_p(s)}{\left[1 + \frac{Z_i(s)}{Z_a(s)} \right]}, \quad (29)$$

s = Laplace operator.

The input $Z_i(s)$ and feedback $Z_{fp}(s)$ impedances consist of a resistance and inertance. The input deflection impedance of the gain block is $Z_a(s)$.

Two dynamic tests, flow frequency and pressure frequency response tests, have been conducted point by point on both the gain block and servovalve at a temperature of 27°C. The experimentally measured pressure and flow gain as a function of frequency are plotted in figures 19 and 20. The test data show that the flow gain of the valve reaches 90° phase shift at 80 Hz, the pressure gain reaches 90° phase shift at approximately 100 Hz and the experimentally measured pure delay time for both the pressure and flow gain is 1.1 ms.

The comparisons of the frequency response between the breadboard configuration and the integrated component fluidic servovalve are shown in figures 21 and 22. The elimination of the feedback line capacitance which is present in the breadboard configuration as described by Lee¹², leads to improved response in the integrated component fluidic servovalve. The data show that the pressure gain reaches 90° phase shift at 7 Hz for the bread-

¹²D. Lee, The Analytical and Experimental Development of a Fluidic Servovalve, Massachusetts Institute of Technology, Ph.D Thesis (April 1980).

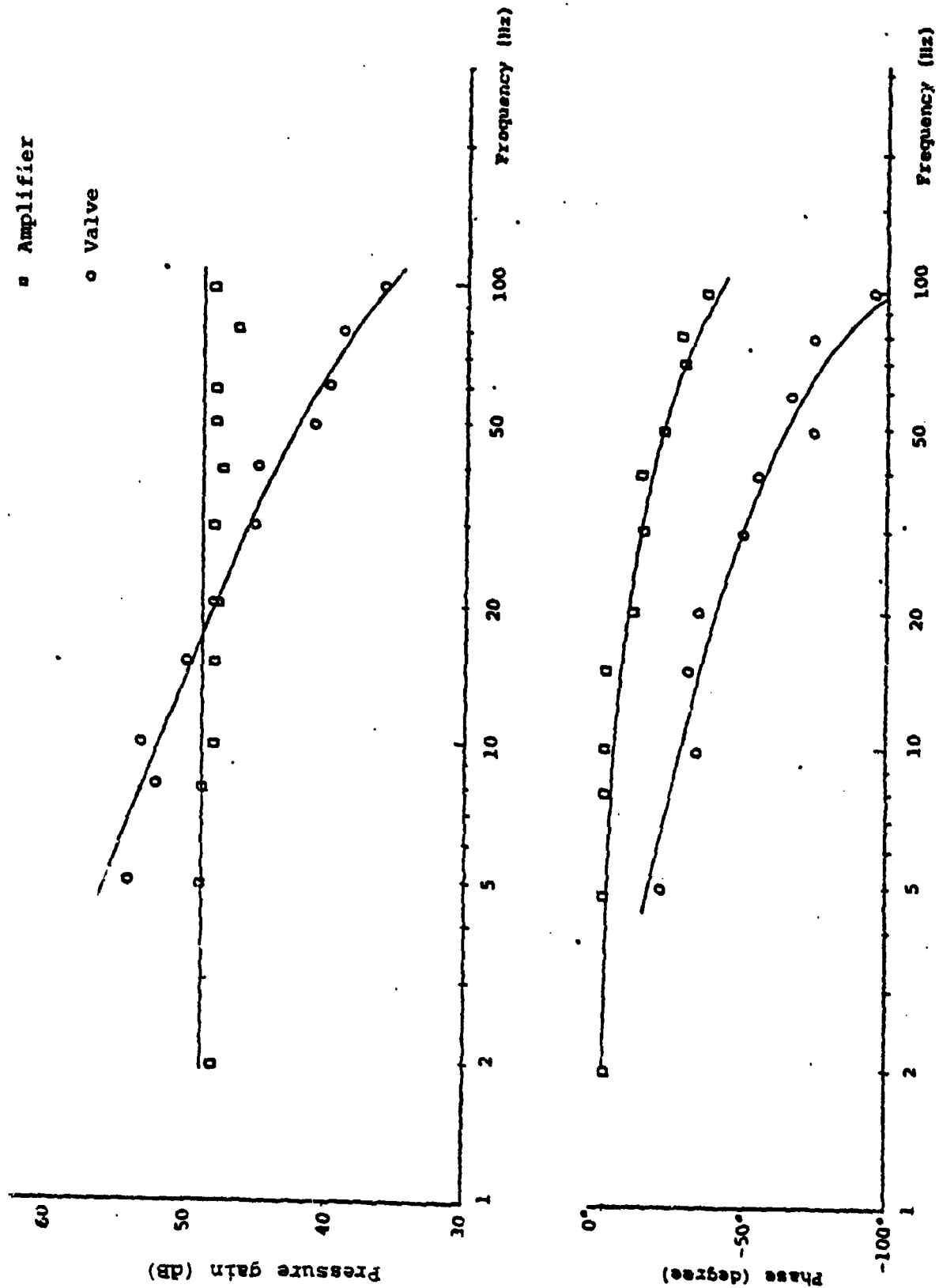


Figure 19. Gain block and servovalve blocked-load pressure gain.

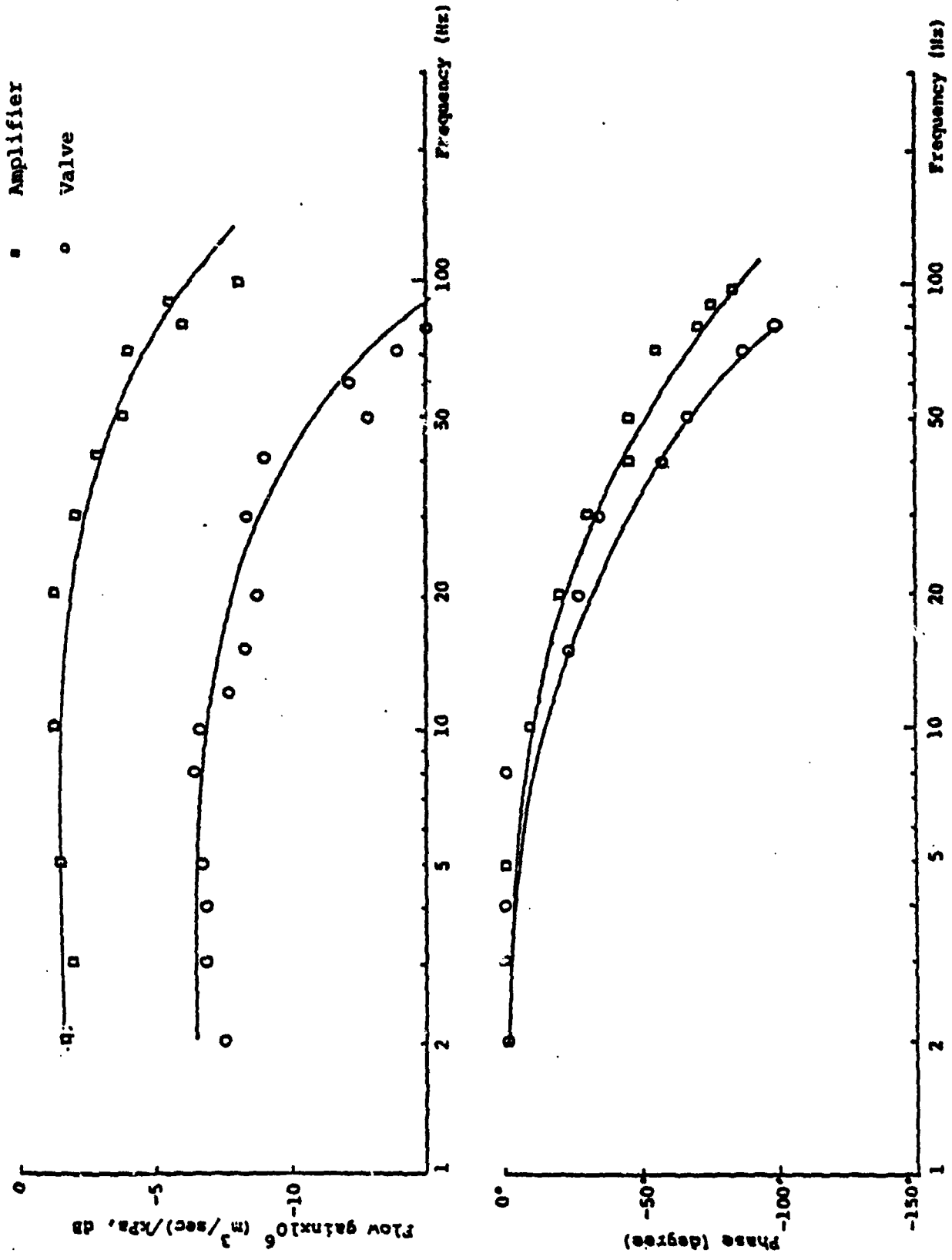


Figure 20. Gain block and servovalve no-load flow gain frequency response.

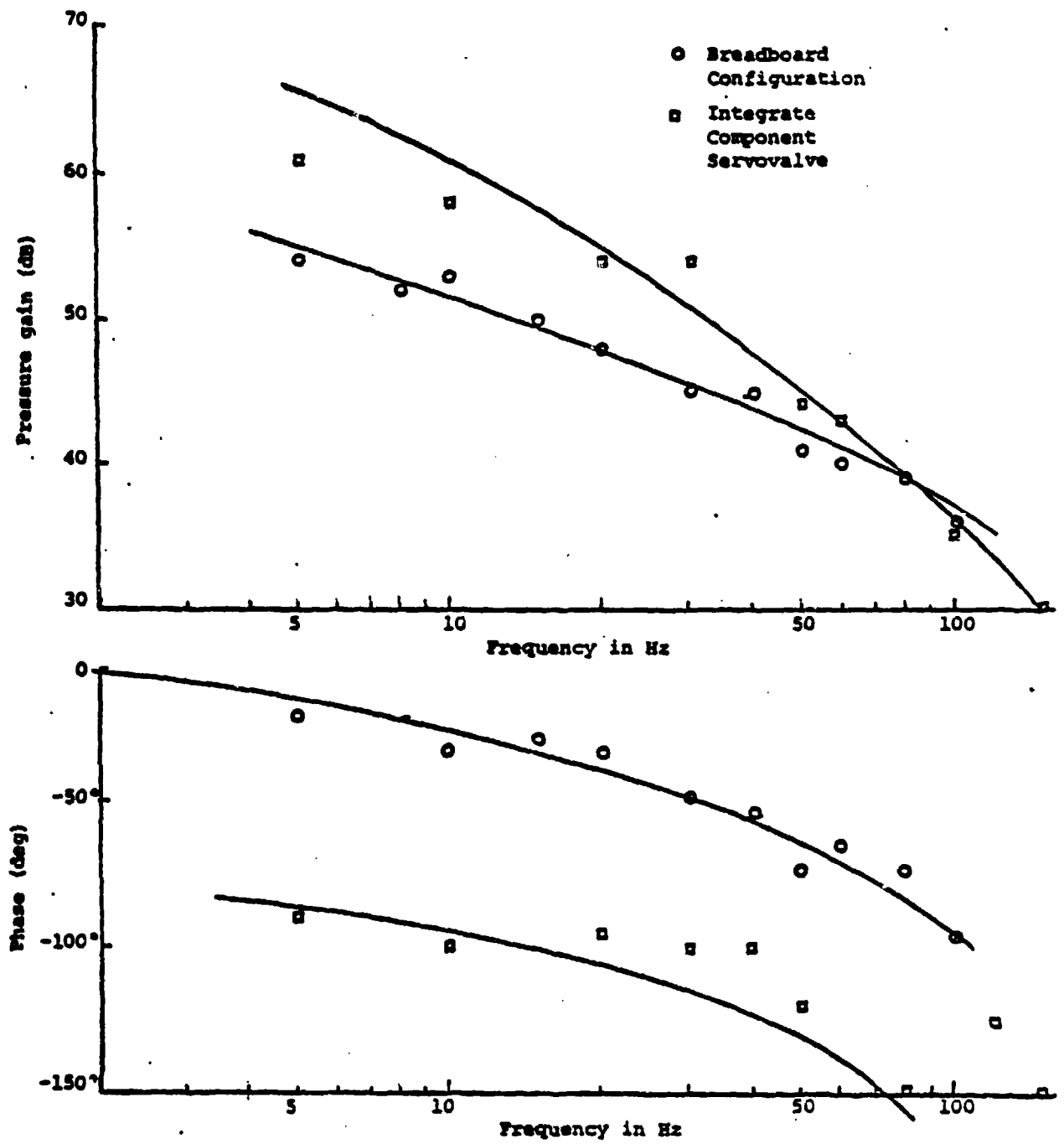


Figure 21. Comparison of blocked-load frequency response between integrated component servovalve and breadboard configuration servovalve.

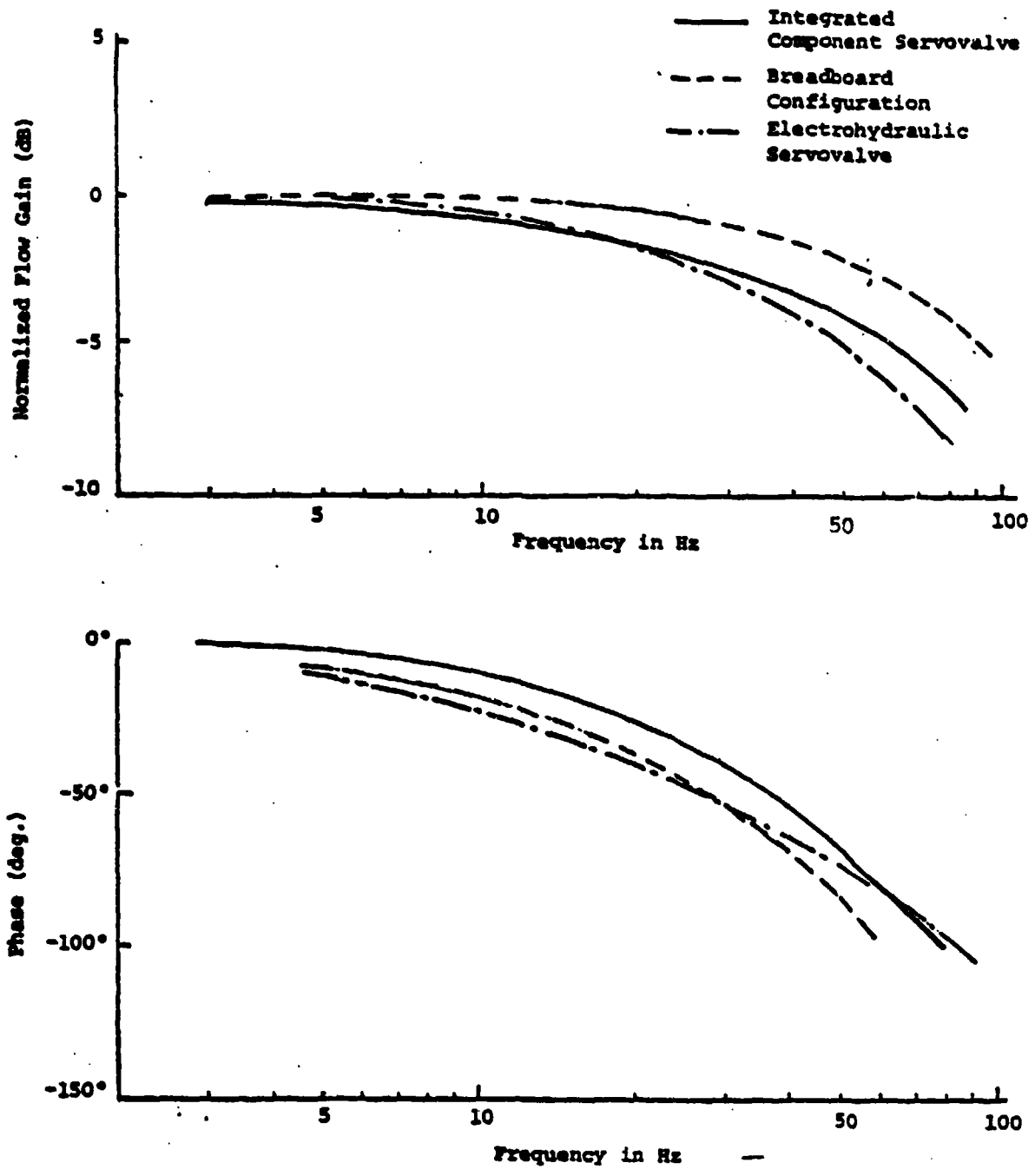


Figure 22. Comparison of no-load frequency response of integrated component servo valve, breadboard configuration and electrohydraulic servo valve.

board configuration and at 100 Hz for the integrated component configuration. figure 22 indicates that the flow gain reaches 90° phase shift at 60 Hz for the breadboard configuration and at 80 Hz for the integrated component configuration and electrohydraulic servovalve approximately. The comparison shows that a significant decrease in phase shift has been achieved and the dynamic performance of the fluidic servovalve is comparable to the electrohydraulic servovalve with standard packaging.

4. FLUIDIC POSITION SERVO

A closed-loop fluidic position servo has been constructed as shown in figure 23. An integrated component fluidic servovalve, similar to that discussed in the preceding section, has been used as a power modulation element. A fluidic summing amplifier is also used to perform signal processing. In addition, a fluidic feedback transducer has been developed so that the mechanical displacement sensing is feedback in the form of a fluidic signal. The elements in the control system are described in the following paragraphs.

4.1 Fluidic Summer

The fluidic summer is shown in figure 23. For low frequency applications, the transfer function of the fluidic summer may be expressed as

$$K_s(s) = K_{ss} e^{-\tau_s s} \quad (30)$$

where

$$K_{ss} = \frac{G_{p,LPA}}{2 + \frac{R_1}{R_{as}}}, \quad (31)$$

$G_{p,LPA}$ = LPA blocked-load pressure gain,

R_1 = Summer input resistance,

R_{as} = LPA deflection resistance,

τ_s = LPA pure time delay.

4.2 Mechanical-Fluidic Displacement Transducer

The mechanical-fluidic displacement transducer is essentially a position feedback sensor in which the mechanical translational displacement is transformed into a fluidic signal. The electrical equivalent and the construction schematic are shown in figure 24. The displacement trans-

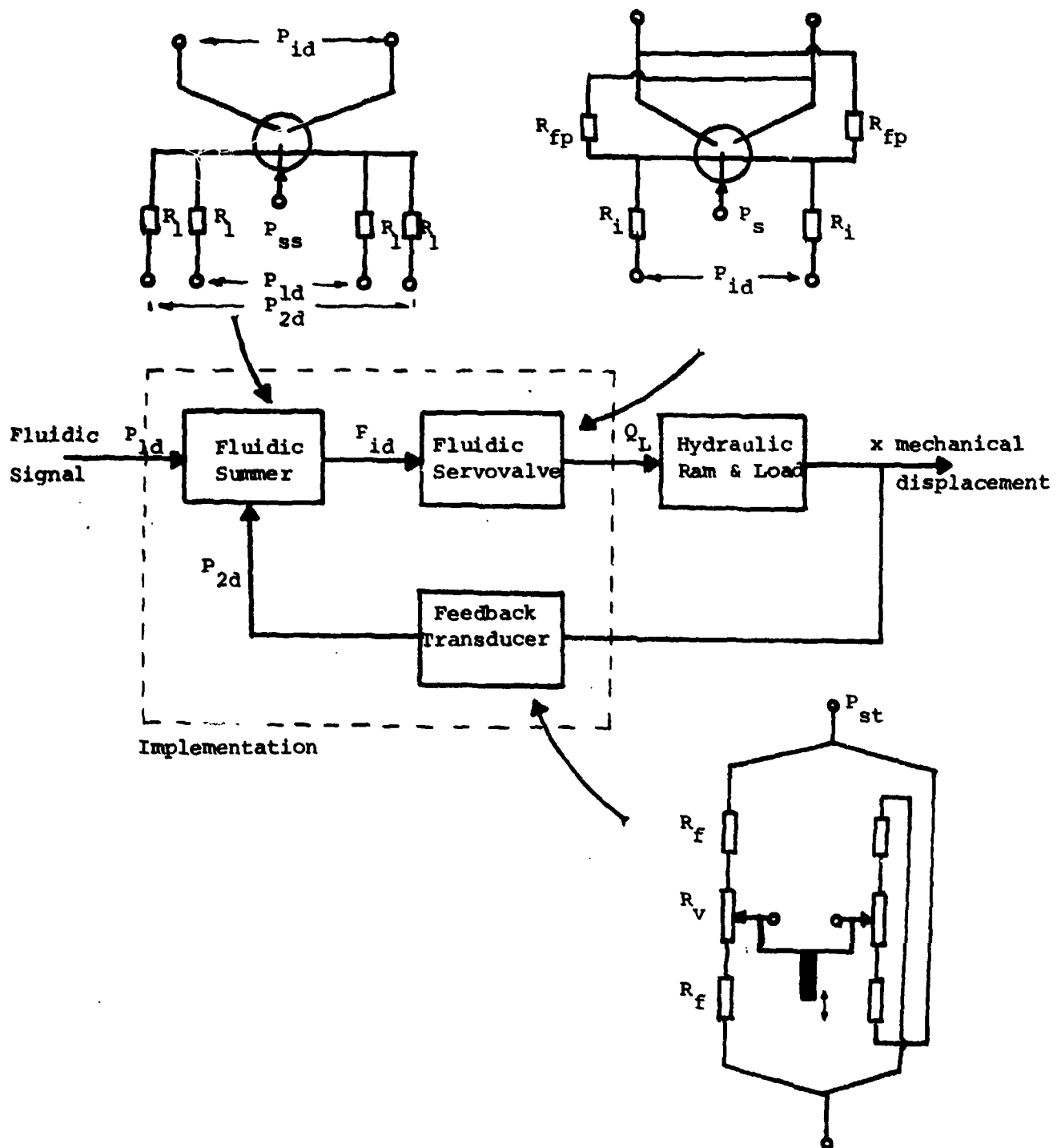
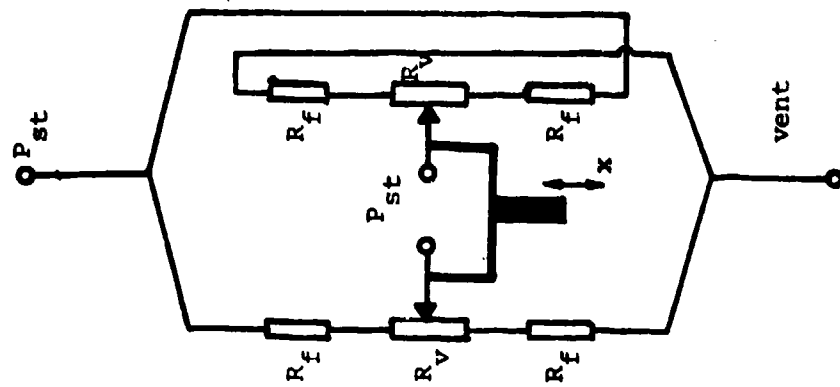
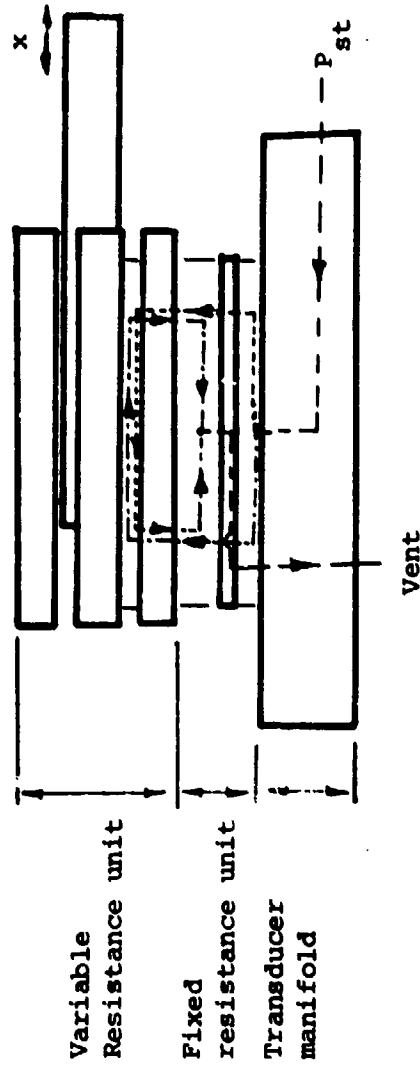


Figure 23. Fluidic position servo block diagram.

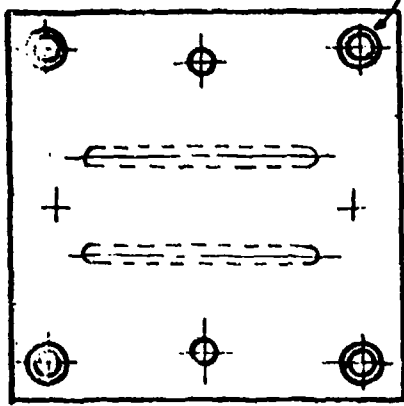


(a) Electrical equivalent

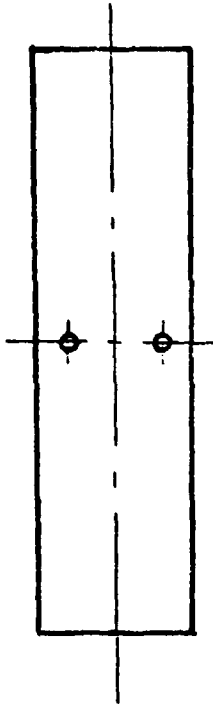


(b) Construction schematics

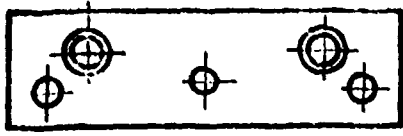
Figure 24. Mechanical-fluidic displacement transducer schematics.



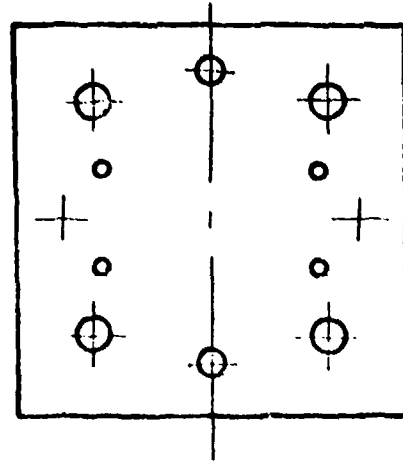
Component A



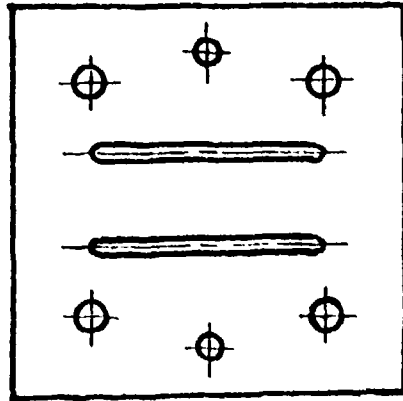
Component B



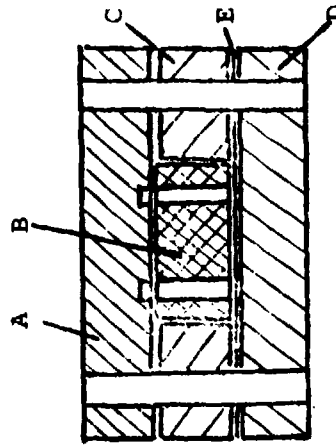
Component C



Component D



Component E



(c) Detail of variable resistance unit

Figure 24. Mechanical-fluidic displacement transducer schematic.

ducer may be considered as a fluidic resistance bridge. It consists of two pairs of fixed resistors and a pair of variable resistors.

The transducer sensitivity at blocked-load may be derived from circuit analysis

$$K_t(s) = \frac{P_{dt}(s)}{x(s)} = \frac{P_{st}}{x_m} \left[\frac{1}{1 + 2 \frac{R_f + sL_f}{R_v + sL_v}} \right] \quad (32)$$

where

- P_{dt} = output pressure differential of transducer,
- P_{st} = supply pressure of transducer,
- x = translational displacement,
- x_m = half stoke,
- R_f, R_v = fixed and variable resistance, respectively,
- L_f, L_v = fixed and variable inertance, respectively.

The resistance and inertance of the channel resistance are

$$\begin{aligned} R_c &= \frac{12\mu x}{bh^3} && \text{for } b \gg h, \\ L_c &= \frac{\rho x}{bh}, \end{aligned} \quad (33)$$

and the time constant of the channel resistance, τ_c , may be expressed as

$$\tau_c = \frac{L_c}{R_c} = \frac{h^2}{12\nu}. \quad (34)$$

If equal channel heights are chosen for both fixed and variable resistances, the transfer function of the mechanical-fluidic displacement transducer may be simplified from equations (32) and (34) as

$$K_t(s) = \left(\frac{1}{1 + 2 \frac{R_f}{R_v}} \right) \frac{P_{st}}{x_m} \quad (35)$$

and the dynamics of the transducer may be neglected.

4.3 Fluidic Servovalve

The characteristic performance of the fluidic servovalve has been discussed in section 3.2. In the application of the fluidic servovalve in

the position servo system, the output flow/pressure characteristics must be designed to meet the particular ram and load requirements. The actuator and load described as part of the position servo by Lee¹³ has been used in this study so that a step response between the fluidic position servo and a conventional electrohydraulic position servo may be compared directly.

From the characteristics of the fluidic servovalve and the parameters of the actuator and load, the dimensionless group

$$\frac{G_{qp} d}{A_r^2} \ll 1$$

and the time constant,

$$\frac{m}{d} < 1 \text{ second}$$

may be calculated

where

$$G_{qp}(s) = G_q(s)/G_p(s)$$

d = damping coefficient

A_r = area of ram,

m = mass of load.

As a result of the high pressure gain and small load mass and friction, the load dynamics for this particular system can be neglected and the dynamic flow gain of the servovalve is the dominant valve performance parameter. The experimentally determined flow gain from section 3.4 is

$$G_q(s) = \frac{Q_L(s)}{P_{id}(s)} = \frac{G_{qs} e^{-\tau_v s}}{(1 + \tau_q s)} \quad (36)$$

where

G_{qs} = steady state servovalve flow gain,

τ_v = pure time delay of the servovalve,

τ_q = first order time constant.

4.4 Closed-Loop Fluidic Position Servo

With the dynamic characteristic performance of the fluidic summer, fluidic feedback transducer and fluidic servovalve predicted in sections

4.1, 4.2 and 4.3 respectively, the fluidic position servo can be represented by the block diagram shown in figure 25. The open loop transfer function of position servo may be expressed as

$$GH(s) = \frac{Ke^{-\tau s}}{s(1+\tau_q s)} \quad (37)$$

where

$$K = \frac{K_t \cdot K_{ss} \cdot G_{qs}}{A_r}$$

$$\tau = \tau_v + \tau_s$$

The dynamic performance of the closed-loop position servo may be expressed in terms of two dimensionless parameters, namely, the normalized gain $K\tau$, and the normalized characteristic time constant τ/τ_q and may be analyzed by Root Locus analysis. Normalized gain for zero damping, which indicates the limit of closed-loop stability, and normalized gain for critical damping, which corresponds to a step response with no overshoot, are of particular interest. $K\tau$ corresponding to $\xi = 0$ and $\xi = 1$ are plotted as a function of τ/τ_q in figure 25. For simplicity and as a first-order guide in selecting the combination of $K\tau$ and τ/τ_q , the damping ratio ξ and normalized natural frequency, $\omega_n \tau$ are plotted against the normalized $K\tau$ with τ/τ_q as a parameter in figure 26.

4.5 Implementation

A fluidic position servo has been constructed and tested. The construction is shown in figure 27. A flapper-nozzle valve with an electrical torque motor has been used as a fluidic signal generator.

The gain block, used in the servo is a modified form of the gain block described in section 3 in which the steady state flow gain has been increased and the transport time delay has been reduced with no change in blocked-load pressure gain at the design temperature of 25°C. The increase of the no-load flow gain provides improved servo frequency response and has been achieved by increasing the number of sections in parallel in the final stage and by operating the servovalve at a higher supply pressure whereas the decrease of the pure time delay is achieved by using LPA's with smaller nozzle throat width ($x_{sp}/b_s = 8$) for first and second stages. The

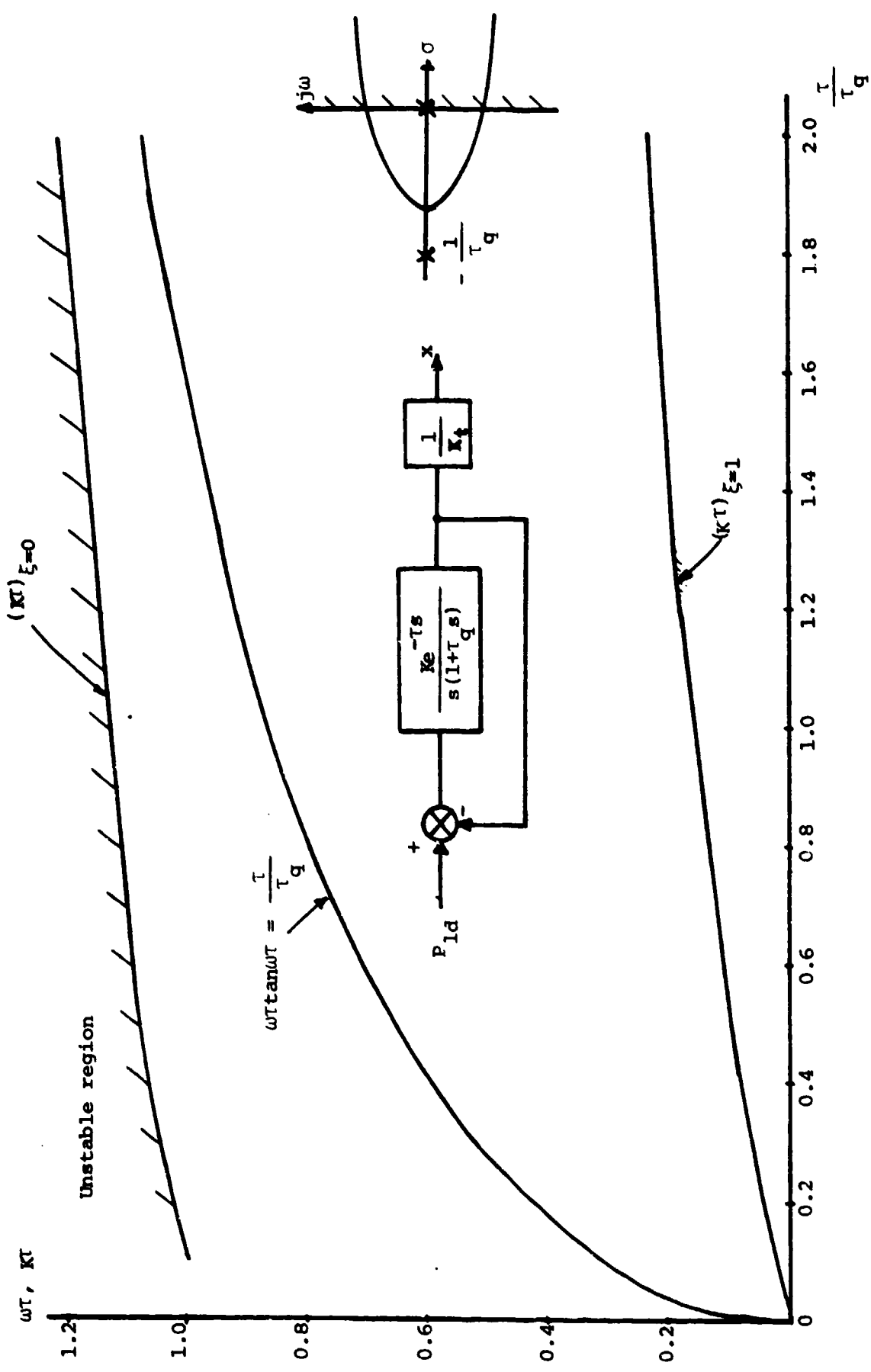


Figure 25. Root locus analysis of fluidic position servo.

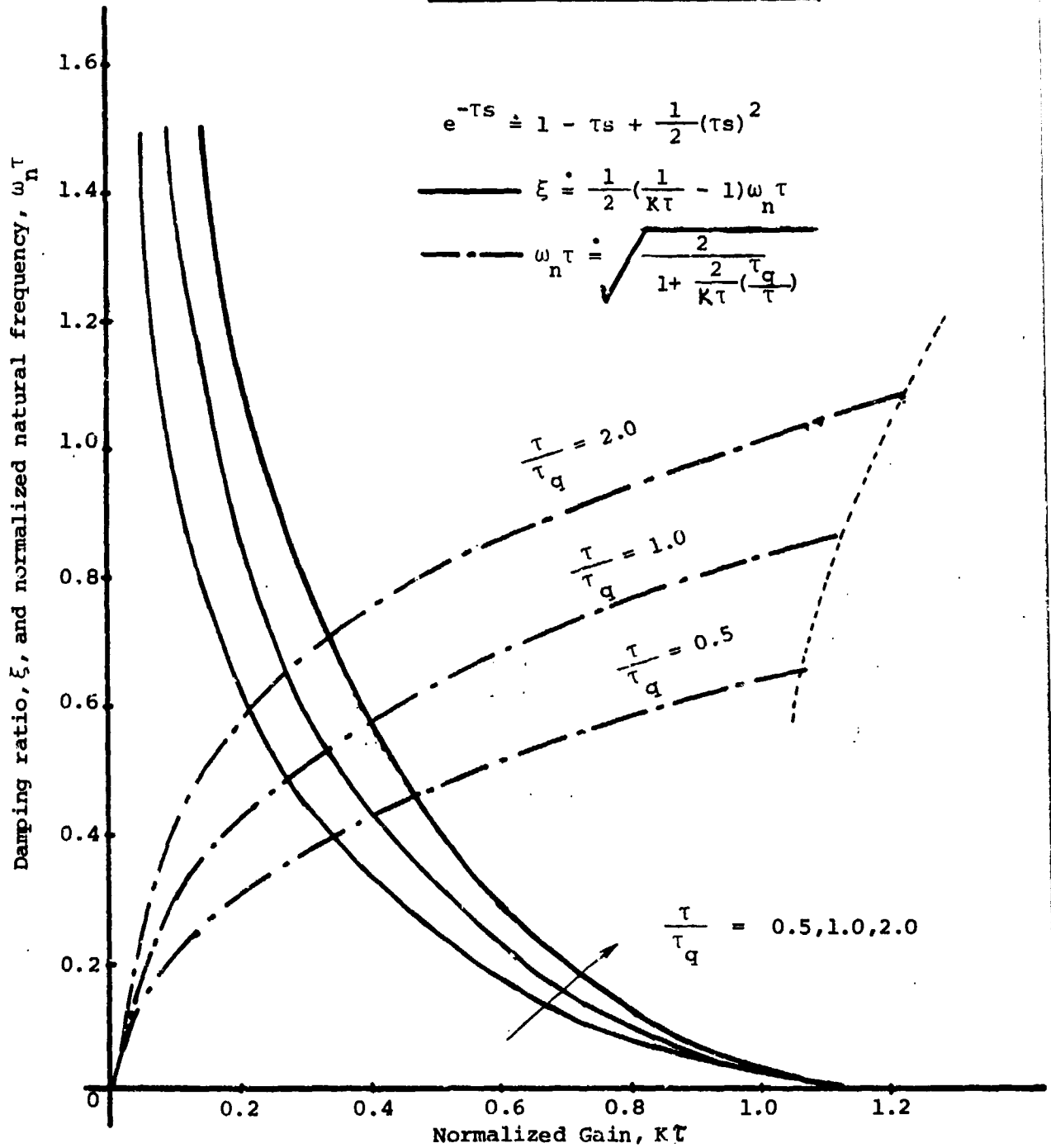
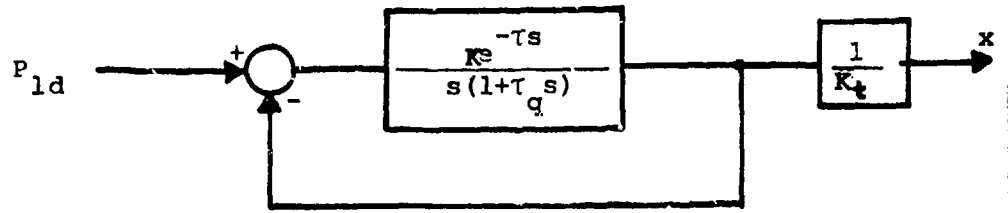


Figure 26. ξ and $\omega_n \tau$ of fluidic position servo.

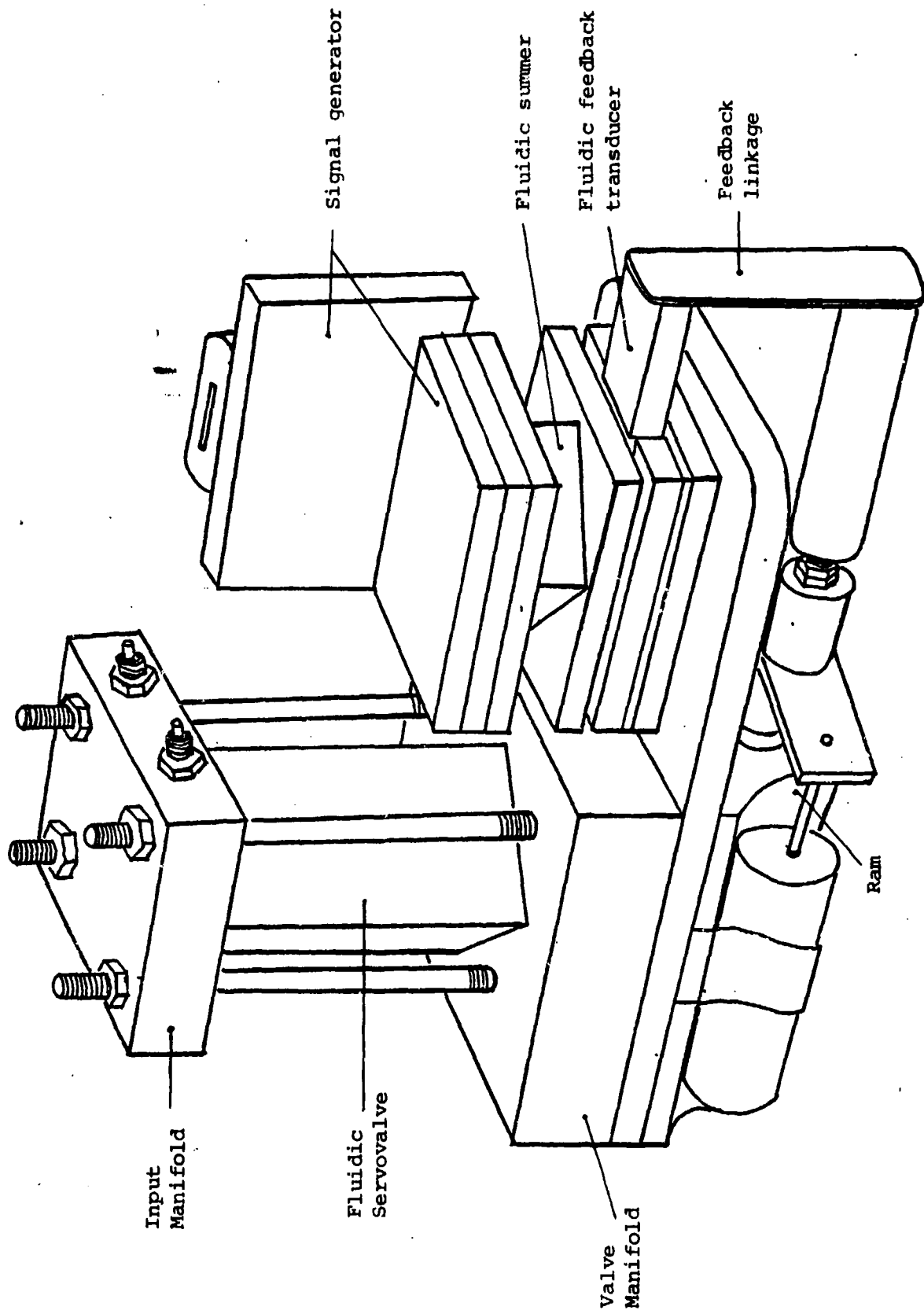


Figure 27. Fluidic position servo construction schematics.

increase in first and second stage gain, resulting from the higher aspect ratio, is designed to offset the additional pressure drop. Hence, K_p has not been varied significantly. The same input and feedback resistors as described in section 3.2 have been used to construct the servovalve.

The fluidic servo components are summarized in table 4. The components have been tested individually for both static and dynamic performance. The data are presented in figures 28 through 33 for the fluidic summer, displacement transducer and servovalve respectively. As shown in table 5, in which the essential servo component parameters are summarized, the servovalve flow gain has been increased by a factor of 2.2 and the pure time delay has been successfully reduced from 1.1 ms to 0.65 ms in comparison to the value of section 3. The displacement transducer exhibits a linear characteristic throughout the entire stroke tested in a blocked load condition and significantly solves the mechanical-to-fluidic interface problems encountered in the previous investigations.¹³

The fluidic position servo response has been calculated based on responses to step inputs. The experimental data, in figure 34 show that the fluidic position servo design with 5 percent overshoot exhibits performance comparable to the commercial electrohydraulic position servo and a significant improvement over the hydraulic position servo described by Lee and Wormley.¹³

Figure 35 compares the experimental and analytical step responses for the fluidic position servo. The preliminary analytical pure time delay based on the sum of LPA transport time lags in both the fluid in summer and servovalve is observed to be smaller than the measured time delay of the servo. Since the dynamic responses of the components have been measured individually, the additional time delay may be attributed to the interconnections between the components of the fluidic position servo.

5. SUMMARY AND CONCLUSIONS

The characteristic performance of HDL fluidic integrated components essential for servovalve design have been evaluated as a function of supply

¹³D. Lee and D.N. Wormley, Multistage Hydraulic Summing and Signal Processing Amplifiers and Fluidic Input Servovalve Development, Harry Diamond Laboratories, HDL-CR-76-233-1 (1976).

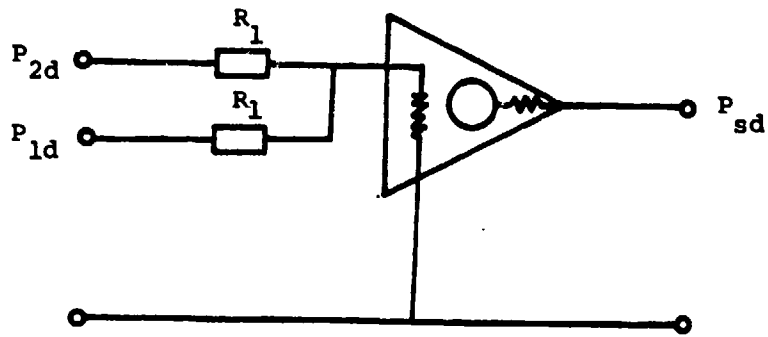
TABLE 4 FLUIDIC POSITION SERVO COMPONENT CONFIGURATION

FLUIDIC SUMMER			
LPA design	81505	$\sigma = 1.666$	$b_s = 0.375$ mm
$N'_R = 90$, $G_{p,LPA}$		10.5	
R_{as}		1.45×10^{11} N-s/m ⁵	350 psi/cis
Input resistance, R_1		6.863×10^9 N-s/m ⁵	16.5 psi/cis
MECHANICAL-FLUIDIC DISPLACEMENT TRANSDUCER			
Variable resistance, R_v		2.03×10^{10} N-s/m ⁵	49 psi/cis
Fixed resistance, R_f		1.491×10^{10} N-s/m ⁵	36 psi/cis
FLUIDIC SERVOVALVE *			
Amplifier			
Stage	LPA	σ	No. of sections
1	x1505	1.000	5
2	x61505	0.667	4
3	x61505	0.333	12
Pressure Reducer			
Stage	Nozzle	No. of sections	
1	5221A-20	6	
2	5221A-20	8	
3	direct supply	—	

* Supply pressure, $P_s = 10.343$ kPa (1500 psi)

TABLE 5 VALUES OF PARAMETERS OF FLUIDIC POSITION SERVO

ACTUATOR			
Area,	A_r	432 mm ²	0.67 in ²
Volume (single side)	V	8.19x10 ³ mm ³	0.5 in ³
Oil Bulk Modulus,	β	1.38x10 ⁶ kPa	2x10 ⁵ psi
LOAD			
Mass,	m	16.65 kg	0.095 lb-s ² /in
Damping constant,	d	29.6 N-s/m	0.169 lb-s/in
FLUIDIC SUMMER			
Steady state gain,	K_{ss}	5	
Pure time delay,	τ_s	0.35 ms	
MECHANICAL-FLUIDIC DISPLACEMENT TRANSDUCER			
Transducer sensitivity,	K_t	11 kPa/mm	40.5 psi/in
FLUIDIC SERVOVALVE			
Steady state flow gain,	G_{qs}	1.207x10 ⁻⁹ m ⁵ /N-s	0.5 cis/psi
Pure time delay,	τ_v	0.65 ms	
1 st order time constant,	τ_q	5.3 ms	



Fluidic Summer Schematic

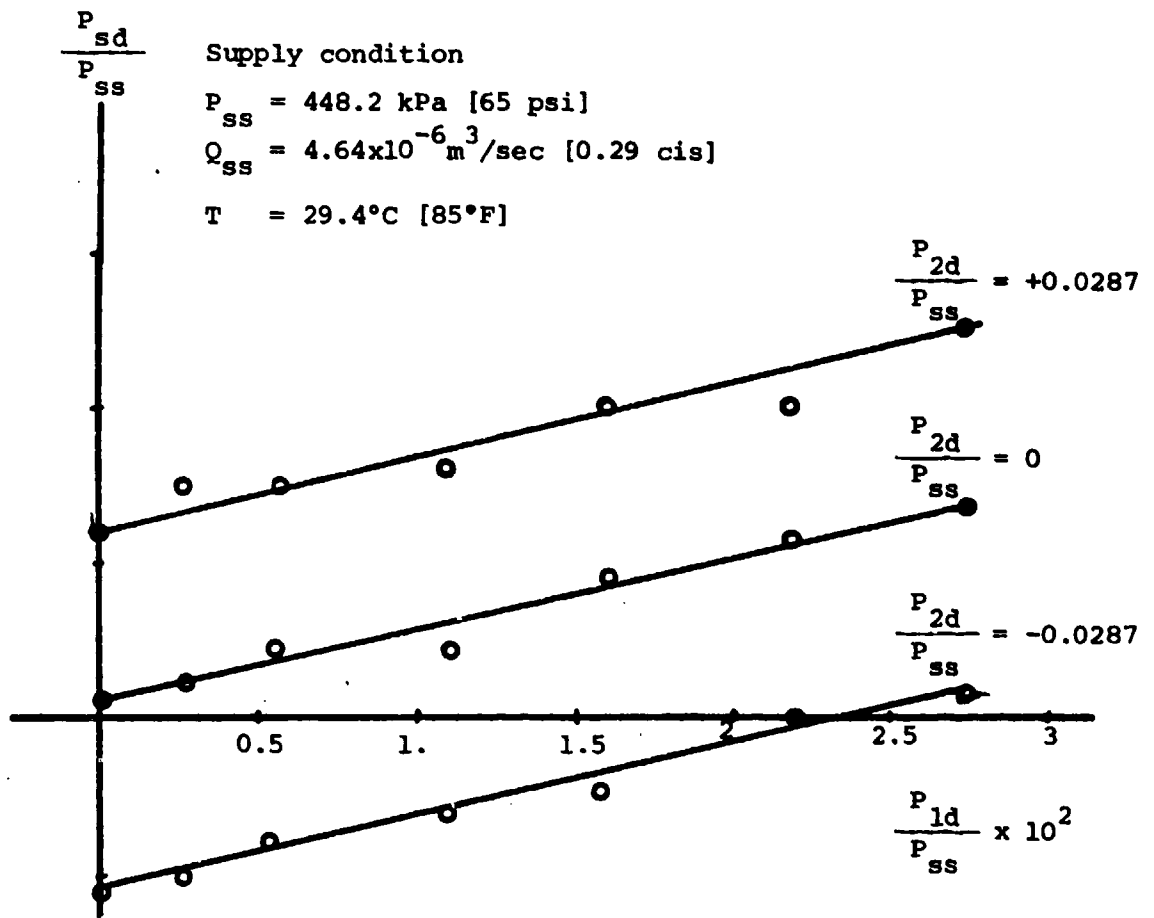


Figure 28. Fluidic summer schematic and static characteristics.

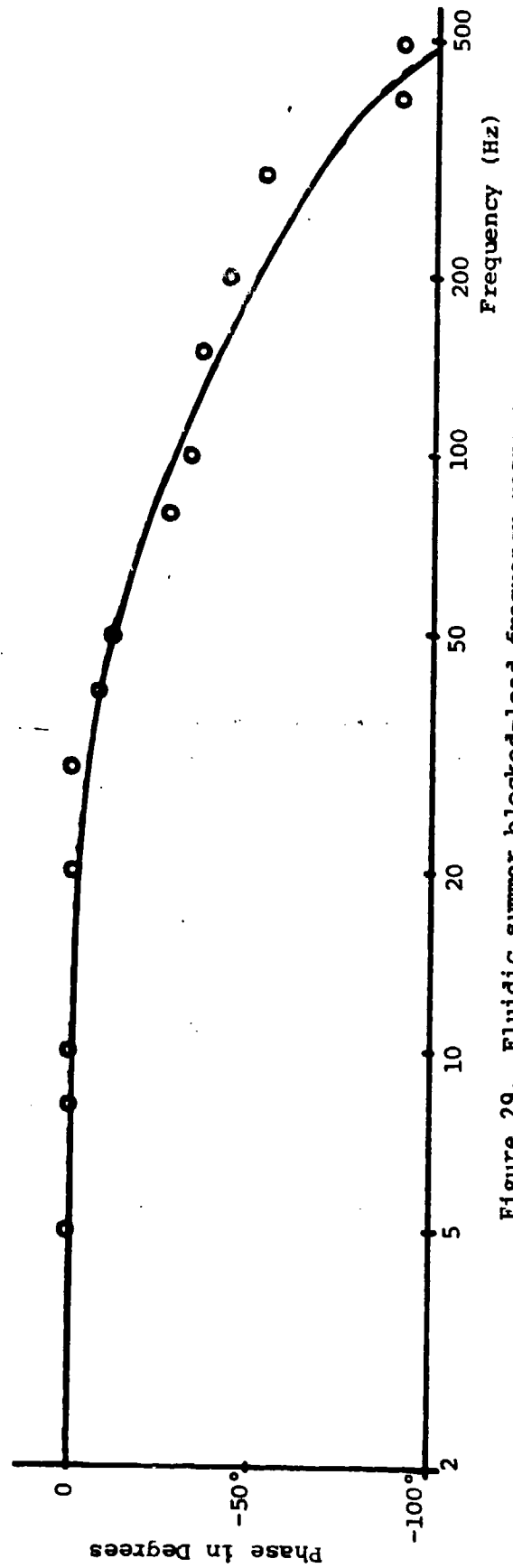
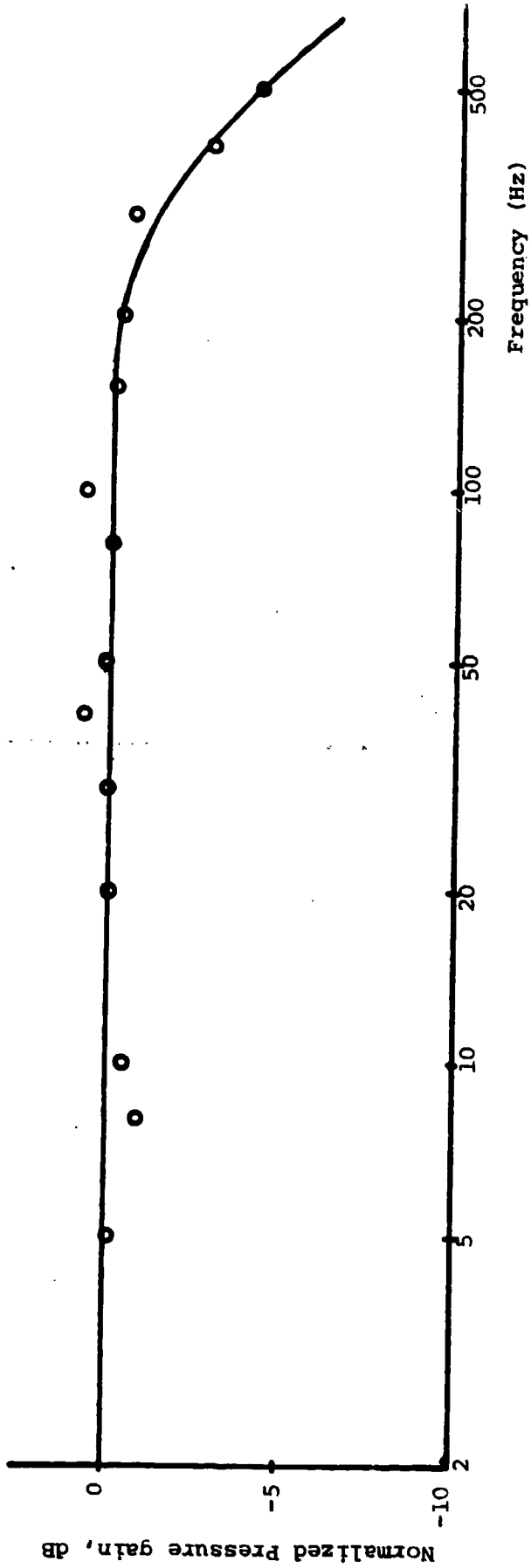


Figure 29. Fluidic summer blocked-load frequency response.

Temperature 29°C [84°F]
 Supply pressure 345 kPa
 Leakage flow $1.632 \times 10^{-5} \text{ m}^3/\text{sec}$
 [1.02 cis]
 $x_m = 12.7 \text{ mm}$
 [$\frac{1}{2}$ inch]

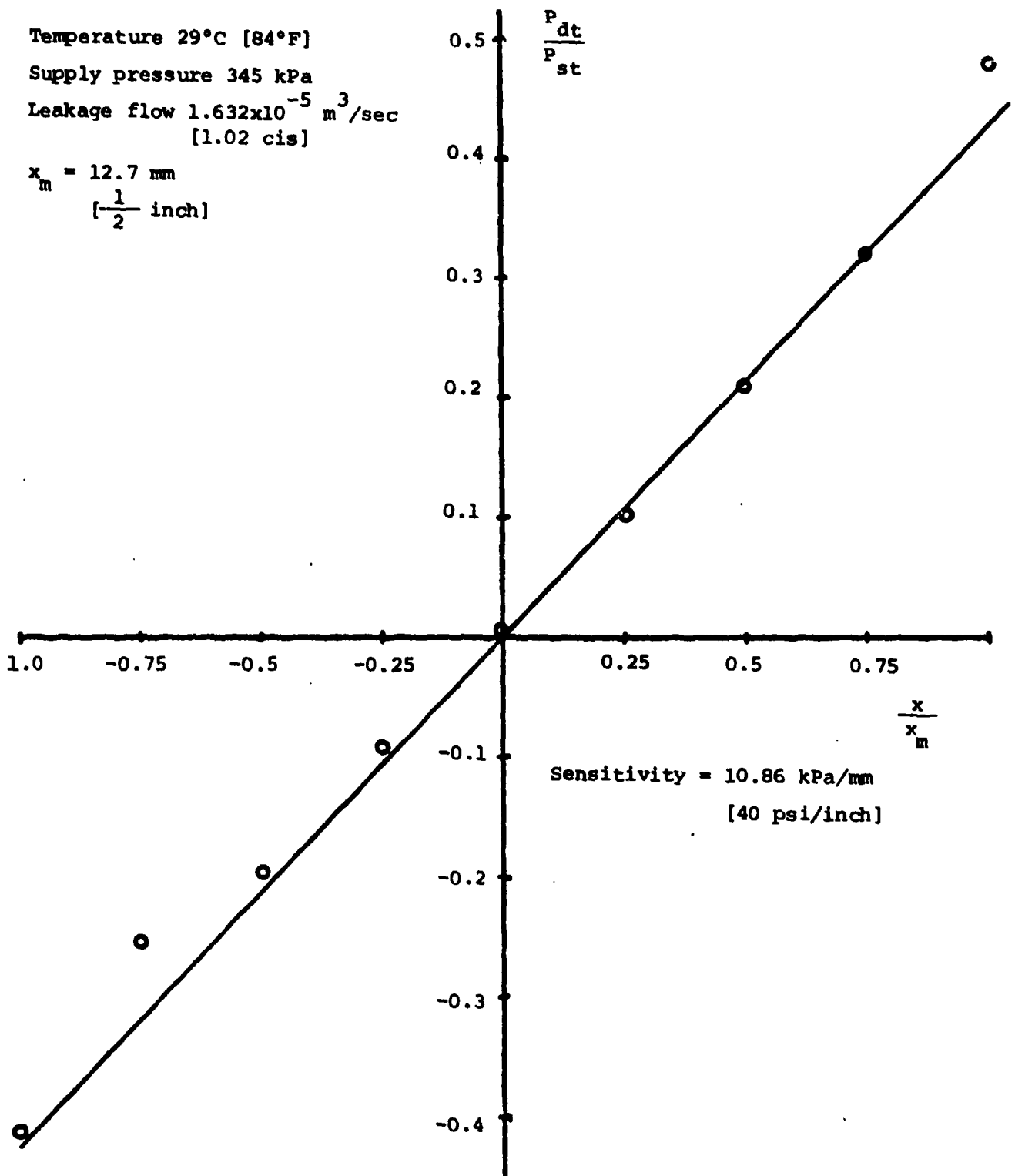


Figure 30. Displacement transducer blocked-load static characteristics.

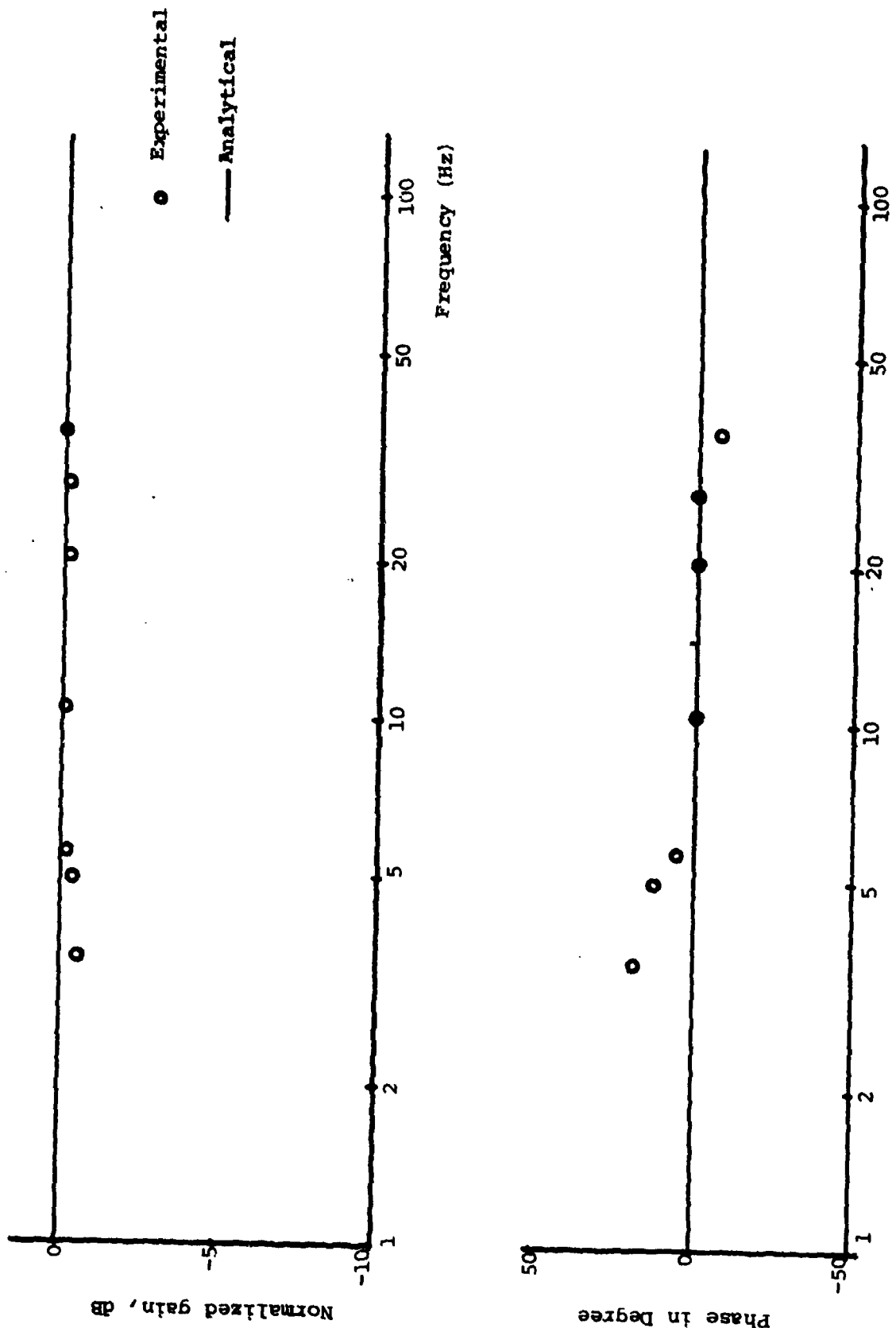


Figure 31. Displacement transducer blocked-load frequency response.

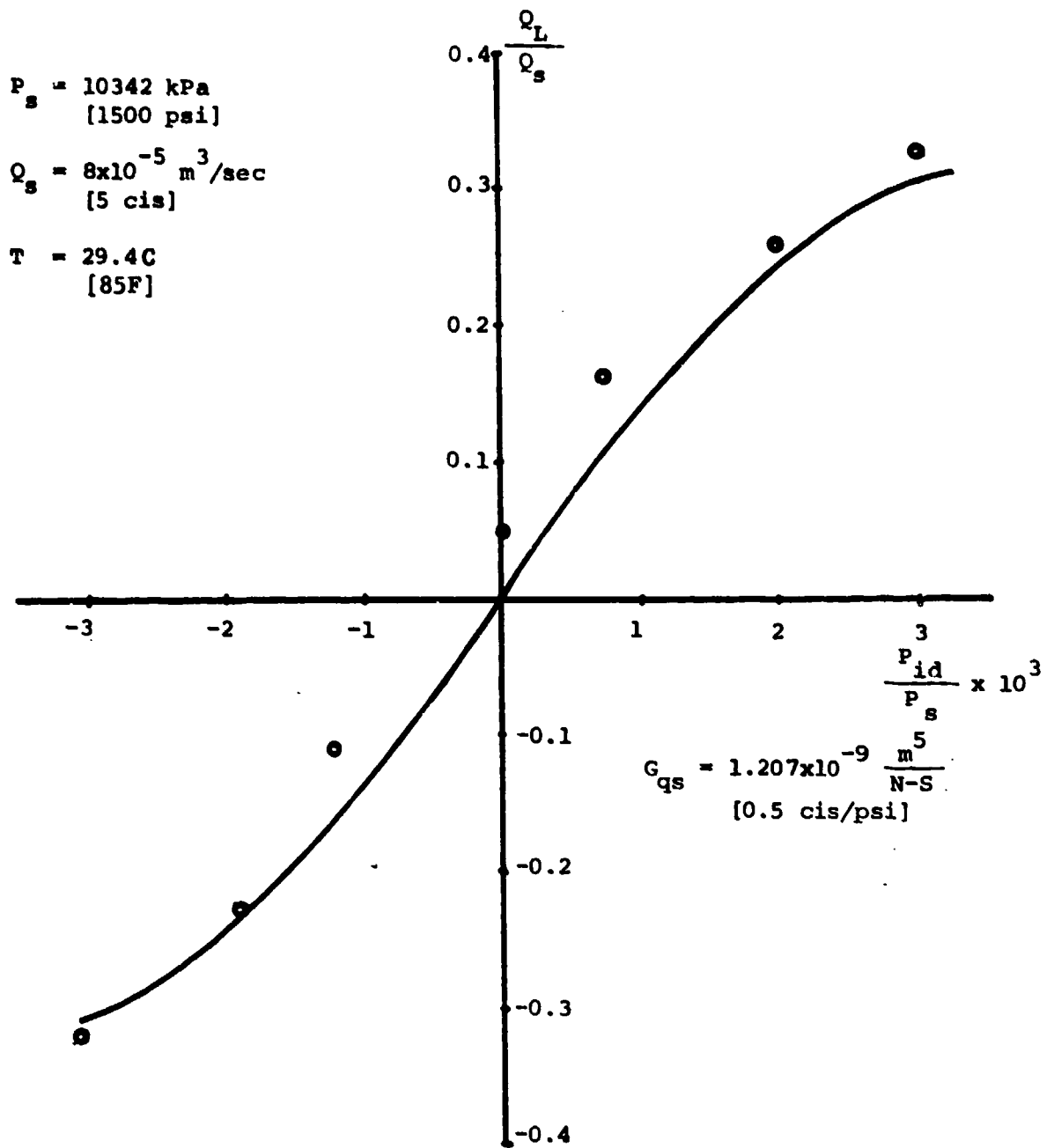


Figure 32. Fluidic servovalve no-load static characteristics.

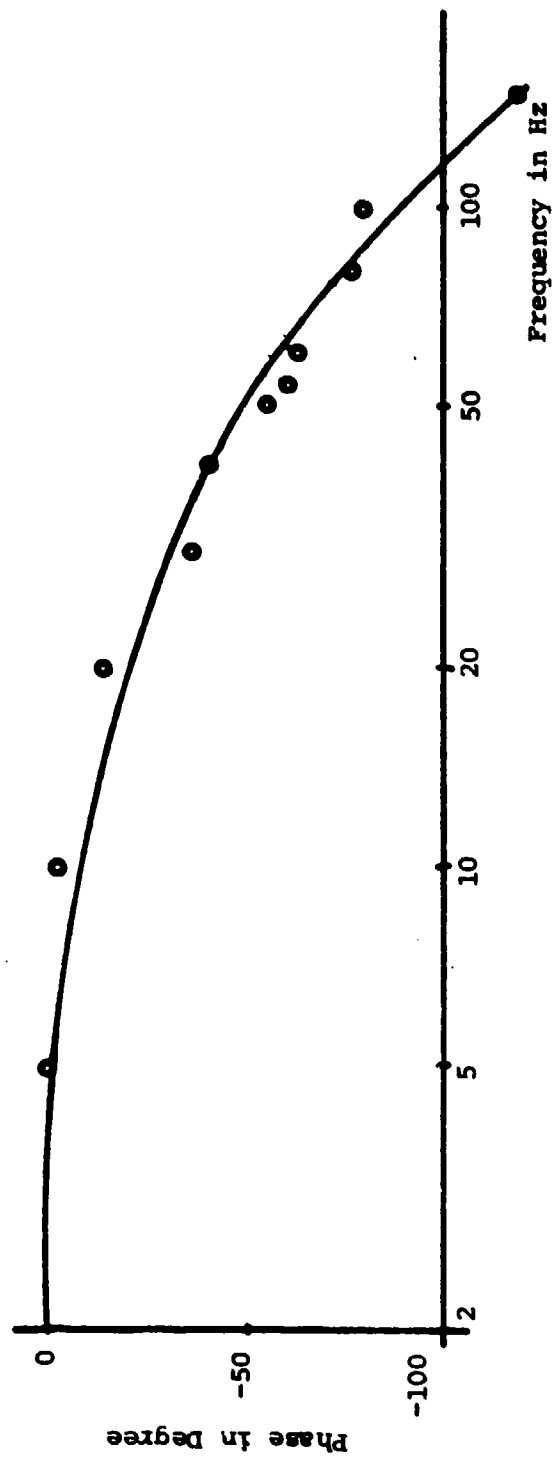
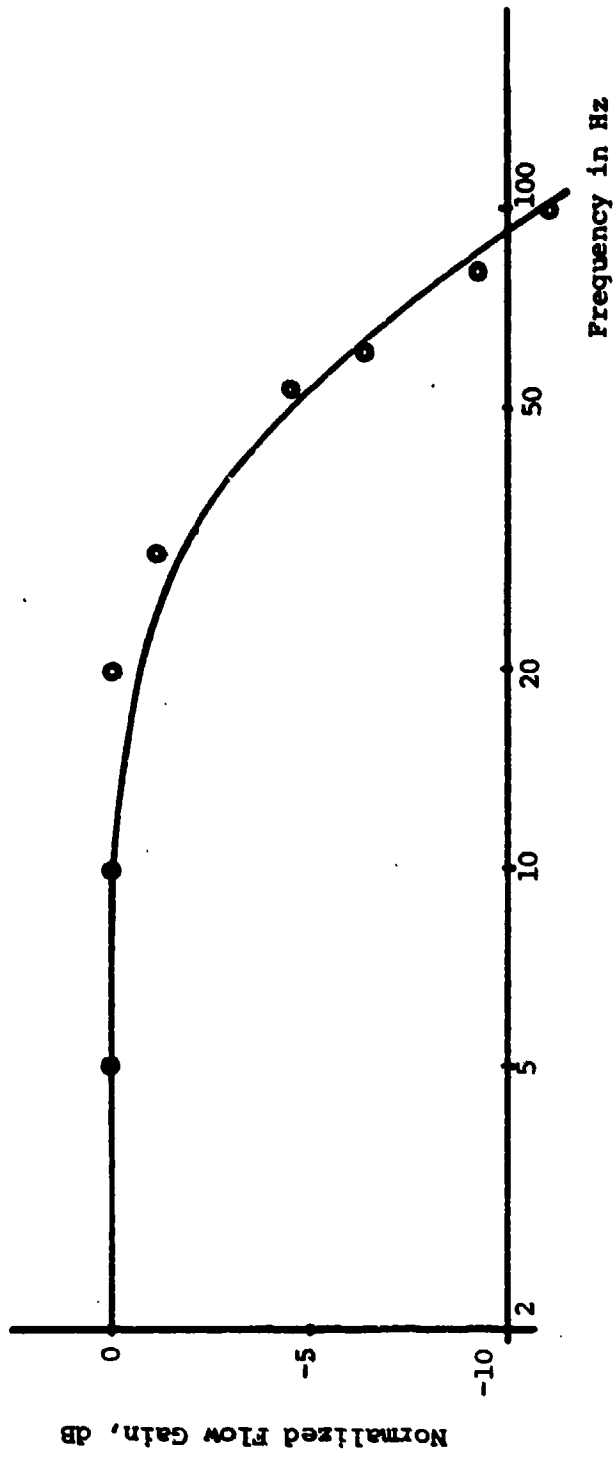


Figure 33. Fluidic servovalve no-load frequency response.

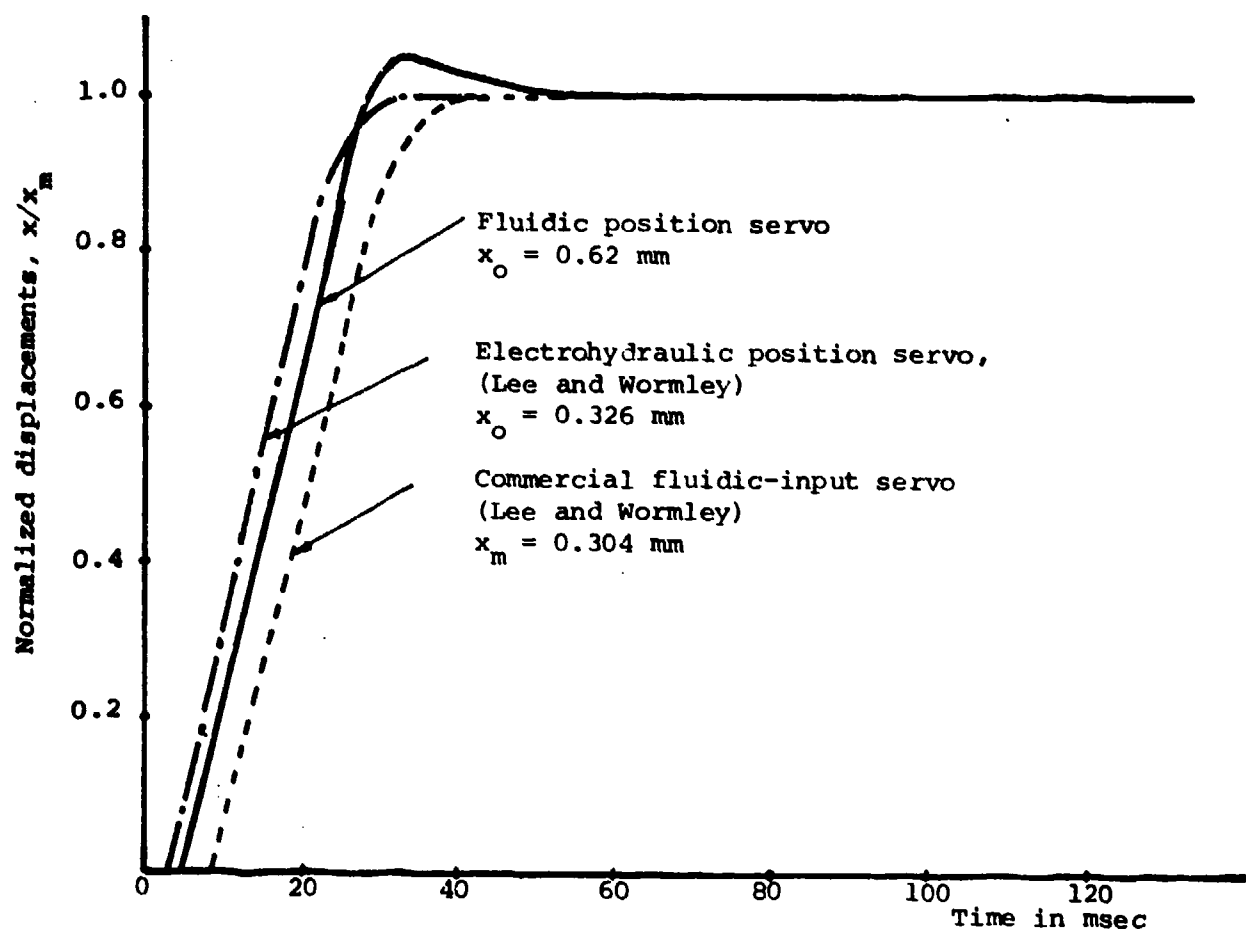
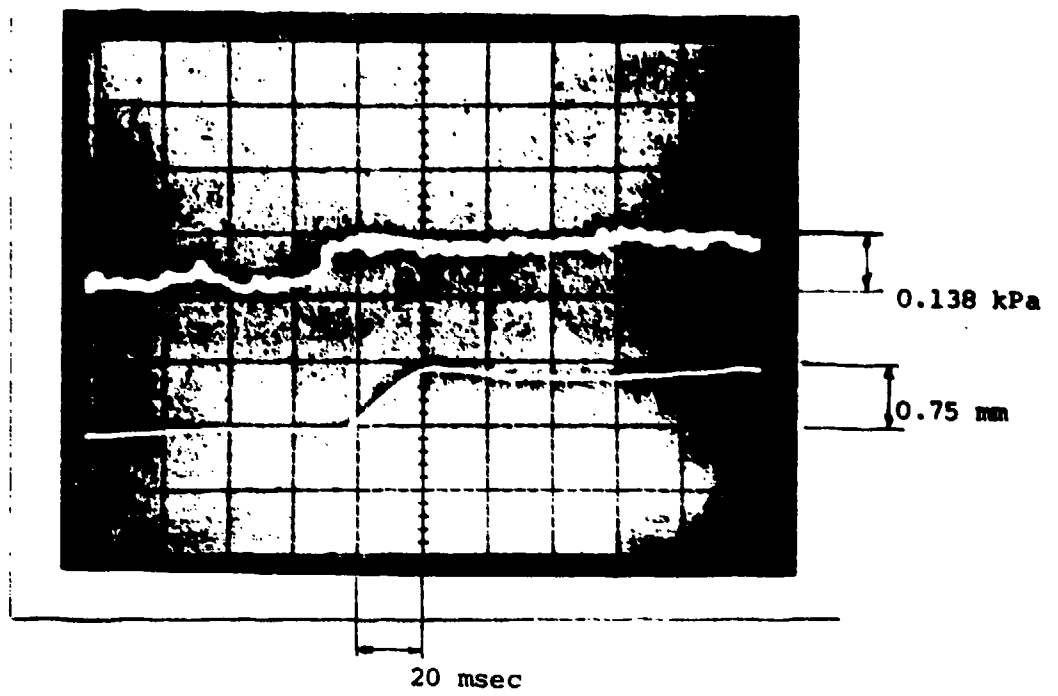


Figure 34. Comparison of step response between fluidic and commercial position servo.

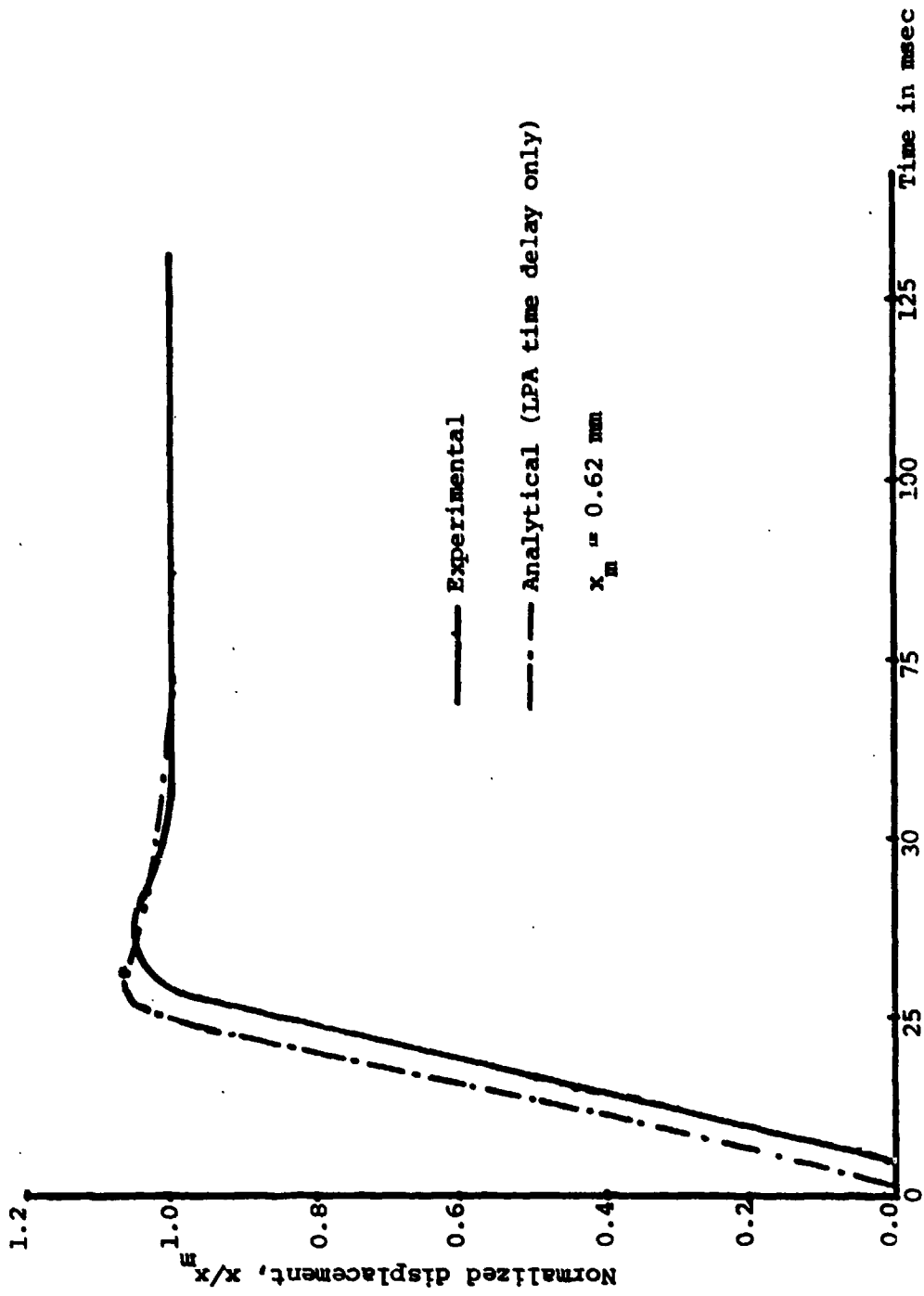


Figure 35. Comparison of experimental and analytical step response of fluidic position servo.

pressure and temperature which are characterized in terms of the modified Reynolds number. The point of transition-to-turbulence of three standard LPA configurations namely, HDL 63020, HDL 72010 and HDL 61505 occurs between modified Reynolds numbers of 100 and 120. The useful operating range of LPA's has been determined through the experimental program to be $40 \leq N'_R \leq 100$.

The relationship between the supply conditions of the individual stages and that of the final stage of the gain block has been derived and verified experimentally. Compensated fluidic gain blocks and servovalves are sensitive to temperature variation at constant supply pressure. The temperature compensation technique, based on the supply pressure scheduling to maintain an approximately constant final stage modified Reynolds number, significantly suppresses the temperature sensitivity of the blocked-load pressure gain of the gain block and servovalve.

The fluidic gain block, summing amplifier and feedback transducer have been used with an actuator and load mass to construct a closed loop position control systems. Static and dynamic tests of the servosystem have shown its performance comparable to an electrohydraulic servoloop. This development effort has demonstrated the capability to develop high performance position servo components from standard integrated component fluidic elements and to interconnect the components into a closed loop servo with performance comparable to high performance electrohydraulic commercial components.

In the current fluidic servo, the maximum load pressure differential and flow gain of the servovalve are primarily limited by the LPA characteristics. Future effort is merited to optimize the LPA design to achieve high pressure recovery, to reduce the ratio of quiescent to maximum load flow and to further minimize the overall power-to-weight ratio.

APPENDIX A. --GAIN BLOCK AND SERVOVALVE CONSTRUCTION DETAILS

In this appendix the gain block stacking order is summarized as given in tables A-1 and A-2 with the components shown in figure A-1.

TABLE A-1 GAIN BLOCK STACKING ORDER DESCRIPTIONS

Stacking Order	HDL Part No.	HDL Orientation	Quantity	Description
Valve Baseplate				
1	5018	C	(*)	
2	5047	G		
3	5221A-20	H	6 } pairs	First Stage Pressure Reducer
4	5040	F		
5	5221A-20	H	3 } pairs	
6	5018	H		
7	5200	C		
8	5200	H		
9	5021	F		
10	5216	F	2 } 6 sections 2	Third Stage Amplifier and Vent Assembly
11	5339A	F		
12	61505	F		
13	5339A	F		
14	5216	F		
15	5040	E		
16	5221A-20	C	7 } pairs	Second State Pressure Reducer
17	5018	F	2 } pairs	
18	5221A-20	C		
19	5021	C		
20	5046	B		
21	5021	D		
22	5216	C	2	
23	5216	H	2	
24	5046	D		
25	5018	A		
26	5046	B		
27	5046			
28	5239	H	} 3 sections	Second State Amplifier and Vent Assembly
29	5137	H		
30	72010	H		
31	5137	C		
32	5237	C		
33	5216	H		
34	5021	A		
35	5200	H		
36	5200	C		
37	5047	D		

* 1 unless otherwise stated

TABLE A-1 (Cont.)

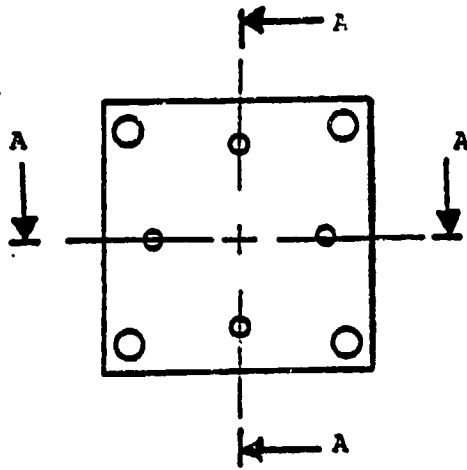
GAIN BLOCK STACKING ORDER AND DESCRIPTIONS

Stacking Order	HDL Part No.	HDL Orientation	Quantity	Description
38	5239	D	2	
39	5018	H		
40	5216	F	2	First Stage Amplifier and Vent Assembly
41	5237	F		
42	5236	F		
43	63020	F		
44	5236	F		
45	5237	F		
46	5216	A		
47	5237	A		
48	5236	A		
49	63020	F		
50	5236	F		
51	5237	F		
52	5216	F	2	
56	5046	E		
Input manifold				

TABLE A-2

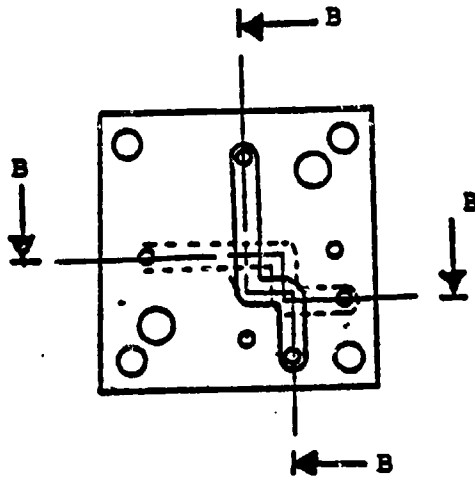
SERVOVALVE STACKING ORDER AND DESCRIPTIONS

Stacking Order	Part No.	Orientation	Quantity	Description
Supply/output manifold baseplate				
1.	SP5			
2.	SP3			feedback manifold
3.	HDL 5043		} 4 pairs	feedback resistors
4.	HDL 5026			
5.	HDL 5040			
6.	3 stage amplifier Refer to amplifier stacking order (1-56)			
7.	SP2			summing manifold
8.	HDL 5040			
9.	HDL 5027			feedback resistors
10.	HDL 5112		2	
11.	HDL 5196			input resistance
12.	HDL 5040			
13.	SP4			
14.	HDL 5040			
15.	HDL 5196			input resistor
16.	HDL 5040			
17.	HDL 5112		2	input manifold



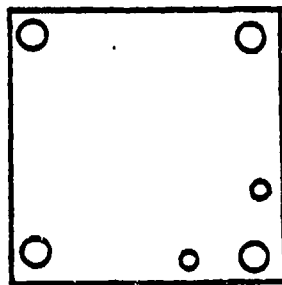
Section A-A

SP2 Summing Manifold (including cover)

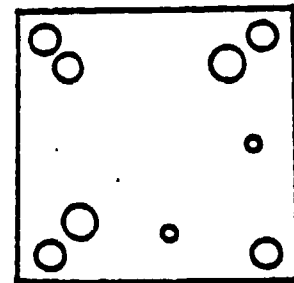


Section B-B

SP3 Feedback Manifold



SP4



SP5

Figure A-1. Servovalve components descriptions.

NOMENCLATURE

A_r	ram area
B_c	LPA control port minimum width
\bar{B}_c	LPA average control port channel width
B_{ni}	normalized nozzle throat width, b_n/b_{si} of i^{th} stage
B_o	LPA outlet port minimum width
\bar{B}_o	LPA average outlet port channel width
B_{sp}	LPA splitter width
B_t	LPA downstream control edges space
B_v	LPA jet-control edge space
\bar{B}_{ni}	normalized nozzle average channel width, \bar{b}_n/b_{si}
C	empirical constant in channel resistance model
C_d	discharge coefficient
C_{di}	discharge coefficient of i^{th} stage LPA
C_θ	momentum flux coefficient
G_p	servovalve blocked-load pressure gain
G_{ps}	servovalve blocked-load pressure gain at steady state
$G_{p,LPA}$	LPA blocked-load pressure gain
G_q	servovalve no-load flow gain
G_{qs}	servovalve no-load flow gain at steady state
G_{qp}	servovalve output admittance
H_{ni}	normalized nozzle height, h_n/b_{si}
K	fluidic servo open-loop steady state gain
K_i	i^{th} stage LPA blocked-load pressure gain, $i=1,2,3$
K_p	gain block blocked-load pressure gain
K_q	gain block no-load flow gain
K_s	fluidic summer gain
K_{ss}	fluidic summer steady state gain
K_t	displacement transducer sensitivity
L_e	normalized entry length, ℓ_e/b
L_c	channel fluid inertance
L_f	transducer fixed channel fluid inertance
L_v	transducer variable channel fluid inertance
N_R	Reynolds number
N_{Rc}	channel Reynolds number
N_{Rf}	gain block final stage Reynolds number

N_{Ri}	gain block i^{th} stage Reynolds number
N'_R	LPA modified Reynolds number
N'_{Rf}	gain block final stage modified Reynolds number
N'_{Ri}	gain block i^{th} stage modified Reynolds number
P_{cd}	control pressure differential
$P_{c ds}$	saturation control pressure differential
P_{co}	bias control pressure
P_{dt}	output pressure differential of transducer
P_{id}	input pressure differential
P_{idm}	maximum input pressure differential
P_L	defined in figure 1
P_{od}	output pressure differential
P_{ods}	saturation output pressure differential
P_s	main supply pressure
P_{sd}	defined in figure 28
P_{si}	supply pressure of i^{th} stage, $i = 1, 2, 3$
P_{ss}	supply pressure of summer
P_{st}	supply pressure of transducer
P_{1d}	input 1 of summer
P_{2d}	input 2 of summer
Q	volumetric flow rate
Q_L	load flow
Q_{Ls}	saturation load flow
Q_{ni}	flow through i^{th} stage nozzle
Q_s	supply flow
Q_{si}	supply flow of i^{th} stage LPA
R	channel resistance
\bar{R}	normalized resistance defined in equation (8)
R_a	gain block input deflection resistance
R_{as}	LPA input resistance for summer
R_f	fixed resistance in transducer
R_{fp}	servovalve feedback resistance
R_i	servovalve input resistance
R_{i1}	1 st stage input resistance
R_{i2}	2 nd stage input resistance
R_{i3}	3 rd stage input resistance

R_{ni}	nozzle resistance of i^{th} stage
R_{01}	1 st state output resistance
R_{02}	2 nd stage output resistance
R_{03}	3 rd stage output resistance
R_{si}	supply resistance of i^{th} stage
R_v	variable resistance in transducer
R_1	summer input resistance
T	temperature
T_o	reference temperature
X	channel length
X_c	LPA control port channel length
X_{ni}	normalized nozzle channel length of i^{th} stage
X_o	LPA outlet port channel length
X_{sp}	LPA supply nozzle-splitter distance
X_{th}	LPA supply nozzle throat length
Z_a	gain block input complex impedance
Z_i	servovalve input complex impedance
Z_{fp}	servovalve feedback complex impedance

Lower Case Letter

b	channel width
\bar{b}	average channel width
b_s	LPA supply nozzle throat width
b_{sf}	final state LPA supply nozzle throat width
b_{si}	i^{th} stage LPA supply nozzle throat width
d	damping coefficient
f	frequency
h	channel height
l_e	entry length
m	mass
m_i	number of LPA in parallel in i^{th} stage
n_i	number of nozzles in parallel in i^{th} stage
S	Laplace transform operator
x	valve input in section 1
	channel length in section 2
	displacement in section 4
x_m	half stroke, maximum travel

x_{sp} dimensional LPA supply nozzle-splitter distance

Greek Letter

α servovalve parameter, defined in equation (18)

β bulk modulus, table 5

γ servovalve parameter, defined in equation (19)

λ viscosity-temperature coefficient

λ_o defined in equation (24)

μ absolute viscosity of oil

ν kinematic viscosity of oil

ν_o kinematic viscosity at reference temperature

ξ damping ratio

ρ density

σ aspect ratio

σ_c channel aspect ratio, h/\bar{b}

σ_i aspect ratio of i^{th} stage

τ total time delay of fluidic servo

τ_c defined in equation (34)

τ_q 1st order time constant of $G_q(s)$

τ_s time delay of summer

τ_v time delay of servovalve

ω_n natural frequency

Subscripts

tr. transition

90° 90° phase shift

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