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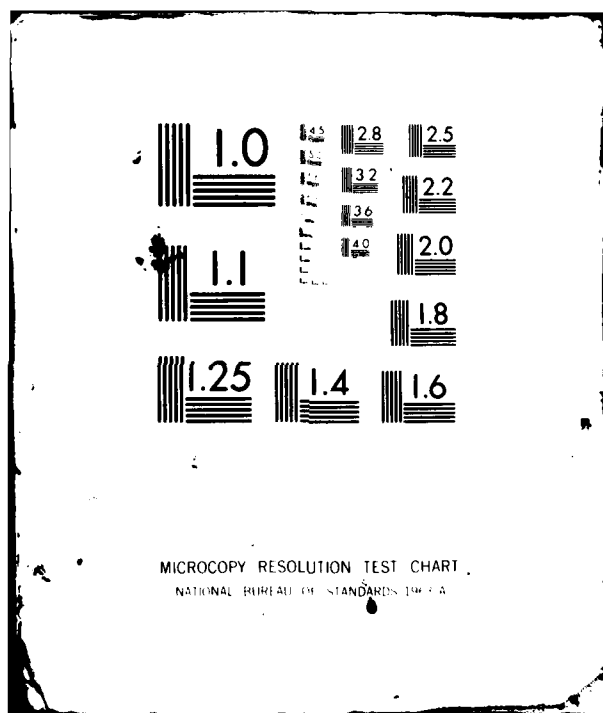
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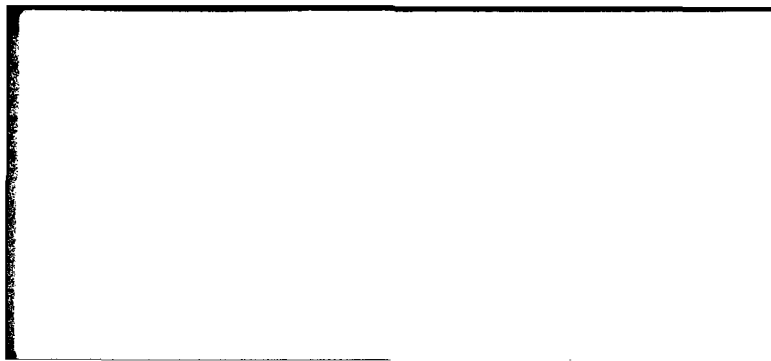
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FLUID DYNAMICS-REACTIVE
FLOW MODELING

Final Report

SAI-82-655-WA

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FLUID DYNAMICS-REACTIVE
FLOW MODELING

Final Report
SAI-82-655-WA

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GENERAL DISCUSSION

In the following discussion we will describe the work performed by Science Applications, Inc. (SAI) on contract number N00014-81-C-2085, SAI project number 1-157-18-265, entitled "Fluid Dynamics-Reactive Flow Modeling," which had a technical performance period of 1 December 1980 to 30 November 1981.

This work includes (1) adaptations of the FAST2D code for slow flow applications, (2) use of the FAST2D code to model vorticity and turbulence flow efficiently, (3) an analytical and computational study of the ignition and quenching of laminar flames in a premixed H_2 , O_2 , N_2 mixture, and (4) incorporation of the latest reactive flow computer packages into the NRL ionosphere code. Each of these topics will be described in the following paragraphs.

SAI has recently increased the flexibility and efficiency of FAST2D, a two dimensional hydrocode developed by The Laboratory for Computational Physics at NRL. The transport algorithm used for transporting density, momentum, energy, and chemical species has been altered to compute along as many as ten rows of computational cells at a time. The original algorithm could only accommodate one row at a time. The new algorithm was compared to the original using a cylindrical axisymmetric shear flow problem. Since no changes were made in the differencing scheme itself, the new algorithm gave exactly the same results as the original. A factor of five increase in computing speed was obtained.

In preparation for reactive slow flow modeling FAST2D's mechanism for following chemical species was altered. Number densities rather than fractional densities for all the species are transported in order to make FAST2D compatible with existing chemical reaction schemes and molecular diffusion packages. The revised version has been benchmarked in a non-reacting shear-flow problem similar to the one mentioned above. As a result, no significant numerical diffusion of chemical species occurred.

A project involving shock modeling was also completed using FAST2D. The object of the study was to accurately and efficiently capture the various structures in complex, non-steady shocks. The quasi-Lagrangian rezoning capabilities of FAST2D were sufficient for modeling two of the four cases studied, regular and single mach reflection. Complex and double mach reflections were modeled after an additional rezoning capability was added to FAST2D. The code was modified to allow the grid to expand about any arbitrary point within the computational system. In this way, grid and fluid motions were synchronized such that self-similar shock structures could grow naturally with the system. This work has been reported in Fry, M., et al., "Shock Capturing Using Flux-Corrected Transport Algorithms with Adaptive Gridding," NRL Memo Report 4629 (1981) and appears in this report as Appendix A. This new adaptive gridding technique allows one to more efficiently model vorticity and turbulence flows.

A theoretical and computational study of the ignition and quenching of laminar flames in a premixed $H_2:O_2:N_2$ mixture has been performed and a detailed report of the work, entitled "A Theoretical Study of the Ignition of Pre-Mixed Gases," is included as Appendix B. The objectives

of this work were: (1) to complete the calibration of the similarity solution model, and (2) to utilize the similarity solution model in conjunction with the NRL 1-D flame model to study the ignition, propagation and quenching of laminar flames in premixed gases.

The similarity solution model is based on an analytic similarity solution to the non-linear time-dependent slow flow equations. The similarity solution and the induction time for the fuel-oxidizer mixture as a function of temperature and pressure can be used to calculate whether or not a given energy source is adequate to ignite the system. This simple procedure is then calibrated using the NRL 1-D flame model which includes the thermo-physical properties of the mixture, a full chemical kinetics scheme, nonlinear convection, molecular diffusion and thermal conduction. The details of the calibration are given in Appendix B.

The similarity solution model predicts whether or not a mixture will ignite given the initial radius of energy deposition R_0 , the duration of the heating τ_0 and the total energy deposited in the system E_0 . If ignition is predicted, the model gives the time it takes for ignition to occur. In contrast, the NRL flame model not only predicts ignition, but also provides the structure of the propagating flame. The calculations presented in Appendix B show that the similarity solution predicts ignition accurately when the radius of energy deposition is larger than the quench radius. The NRL flame model is used to estimate the quench radius as well as to explain the discrepancy in the predictions of the two models for very small radii of energy deposition.

SAI has incorporated the latest reactive flow computer packages into the NRL computer code for the

numerical modeling of the mid-latitude ionosphere.⁽¹⁾ There are two significant additions to the code to improve speed and flexibility. Firstly, the ordinary differential equation (ODE) solver, IMPLCT, used to time advance the chemistry part of the continuity equations was replaced by one which takes advantage of the form of the equations. If there are N_z grid points in altitude, then the ODE's decouple into N_z systems since with the time-splitting algorithm used the chemistry at a given altitude will not depend on the chemistry at any other altitude within the one hydrodynamic time step. Doing many systems at once is an ideal situation for a vector computer like the TI-ASC. The computer package, VSAIM, developed at NRL does such a problem. Since the chemistry at one altitude may proceed faster than at another altitude, VSAIM allows each system to use its own time step. After each chemistry time step it terminates those that have reached the desired ending time and if necessary starts a new system thus keeping the vectors as optimally long as possible throughout the computation. VSAIM, like its predecessor, CHEMEQ,⁽²⁾ also tries to treat those equations it deems are difficult to solve with a special algorithm for stiff equations and those which are easy to solve with a simpler algorithm.

The second major incorporation into the 1D ionosphere code is a routine for the processing of chemical reactions and their reaction rates. Formerly these reactions and reaction rates were hard-wired with the program, requiring program modification for even the slightest change in reaction rate coefficients or the number of reactions. By using the automatic rate processor, ARTP, the chemical reactions and their corresponding reaction rates are input as data cards allowing great flexibility in the choice of the type of chemistry one elects to incorporate into the ionospheric model.

In order to make these modifications it was necessary to change the data structures used to store the densities of the various chemical species. Instead of using a distinct array for each specie present in the problem, one larger array indexed by the number of species in the problem is now used. An array of symbols is now used to distinguish one specie from another. These symbols are the data that ARTP uses to recognize which species are involved in each reaction it processes. By making the types of ions and minor neutrals input to the program, the user has a greater flexibility to test the effects of various chemical reactions and the importance of the various ions or minor neutrals on the resulting ionosphere.

While the modifications to the code were being made, documentation describing the variables used by the code was added. Furthermore, a separate piece of documentation was added to describe the input data to the program, making the whole program much more user oriented. In Appendix C we have included the revised versions of 2 subroutines - INITAL and RTCON. These subroutines supply all the information necessary for setting up the input required for making a run of the ionosphere code.

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Appendix A

SHOCK CAPTURING USING FLUX-CORRECTED TRANSPORT
ALGORITHMS WITH ADAPTIVE GRIDDING

SHOCK CAPTURING USING FLUX-CORRECTED
TRANSPORT ALGORITHMS WITH ADAPTIVE GRIDDING

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A numerical technique has been developed for capturing complex, nonsteady shock structures in multidimensions. The technique relies on moving the computational mesh with the shock wave so that the features of principal interest appear approximately stationary. The method has been implemented using coordinate-split Flux-Corrected Transport (FCT) algorithms which allow the mesh to evolve arbitrarily with respect to the fluid in each coordinate. The grid may thus be optimized in response to the needs of a given problem. Synchronizing the grid and fluid motions permits significant reduction of numerical transients and eliminates numerical diffusion. Shocks develop naturally, with no fitting. The method is illustrated by calculating complex, two-dimensional Mach reflection phenomena associated with airblasts and shock diffraction on wedges. The numerical results are in good agreement with available experimental data.

INTRODUCTION

Numerical solution of transient multidimensional gas dynamics problems is always nontrivial. When, in addition, the problem involves reflecting supersonic flows, large variations in length scales in both space and time, or phenomena for which neither analytic solutions nor detailed experimental observations are at hand, the state of the computational art is challenged. Such a problem arises in calculating the oblique reflection of shocks from solid surfaces in planar geometries (e.g. shock tube experiments) or axisymmetric geometries (e.g. airblasts). The complications arise mainly from the presence of Mach reflections which occur when a shock front impinges on a reflecting surface at angles of incidence sufficiently far from normal. The formation of a Mach stem and, consequently, of a slip surface intersecting the triple point (the confluence of the incident, Mach, and reflected waves) results from the requirement that the flow behind the reflected shock be parallel to the reflecting surface, which cannot be achieved through regular reflection.

Attempts to calculate the properties of the flow in Mach reflections date back at least to von Neumann¹ and the research which grew out of the wartime explosive studies²⁻⁴. For the simplest problem, that of a planar shock

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reflecting from a plane surface, Jones, Martin, and Thornhill⁵ noted that it is possible to reduce the number of independent variables to two by transforming to the similarity variables x/t , y/t , a device that was also used by Kutler, et al⁶. Ben-Dor⁷ developed a theory which used shock polars to explain some of the features of this problem, and solved the system of algebraic equations obtained by combining the jump conditions across the various discontinuities (Courant and Friedrichs)⁸ to describe the flow in the neighborhood of the triple point. To date, no satisfactory treatment of the complete flow field has been published, although some features (like the shape of various waveforms) are quite easy to model.

In connection with studies of both chemical and nuclear explosions there have been many attempts to model a spherical blast wave reflecting from the ground, the so-called height-of-burst (HOB) problem. The hydrodynamic phenomena in the two cases are identical, although nonideal effects (primarily explosive afterburn in the first instance and radiation preheating in the second) are different. Previous attempts to model two-dimensional complex shock reflection have suffered from restriction to describing part of the system, the use of a special assumption like that of self-similarity, or less than satisfactory agreement with experimental data.⁹

The calculations discussed here represent a step forward in overcoming these difficulties. They differ from previous numerical work in incorporating two important computational developments: Flux-Corrected Transport (FCT)¹⁰ and an adaptive regridding procedure, called "sliding rezone",¹¹ which optimizes the mesh point distribution and hence the resolution of surfaces of discontinuity.

FCT is a finite-difference technique for solving the fluid equations in problems where sharp discontinuities arise (e.g. shocks, slip surfaces and contact surfaces). It modifies the linear properties of a second- (or higher) order algorithm by adding a diffusion term during convective transport, and then subtracting it out "almost everywhere" in the antidiffusion phase of each time step. The residual diffusion is just large enough to prevent dispersive ripples from arising at the discontinuity, thus ensuring that all conserved quantities remain positive. FCT captures shocks accurately over a wide range of parameters. No information about the number or nature of the surfaces of discontinuity need be provided prior to initiating the calculation.

The FCT routine used in the present calculations, called JPBFACT (an advanced version of ETBFCT)¹², consists of a flexible, general transport module which solves 1-D fluid equations in Cartesian, cylindrical, or spherical geometry. It provides a finite difference approximation to the conservation laws of the general form:

$$\frac{\partial}{\partial t} \int_{\delta V(t)} \phi dV = - \int_{\delta A(t)} \phi (\underline{u} - \underline{u}_g) \cdot d\underline{A} + \int_{\delta A(t)} \tau dA \quad (1)$$

where ϕ represents the mass, momentum, energy or mass species in cell $\delta V(t)$, \underline{u} and \underline{u}_g represent the fluid and grid velocities, respectively, and τ represents the pressure/work terms. This formulation allows the grid to slide with respect to the fluid without introducing any additional numerical diffusion. Thus, knowing where the features of greatest interest are located, one can concentrate fine zones where they will resolve these features most effectively as the system evolves (Fig. 1).

In the next section we describe the computational techniques used to solve the wedge problem and present the results of four simulations carried out to reproduce experimental results of Ben-Dor and Glass.¹³ In Section III we present a parallel discussion for a HOB calculation. Finally, in Section IV we summarize our conclusions.

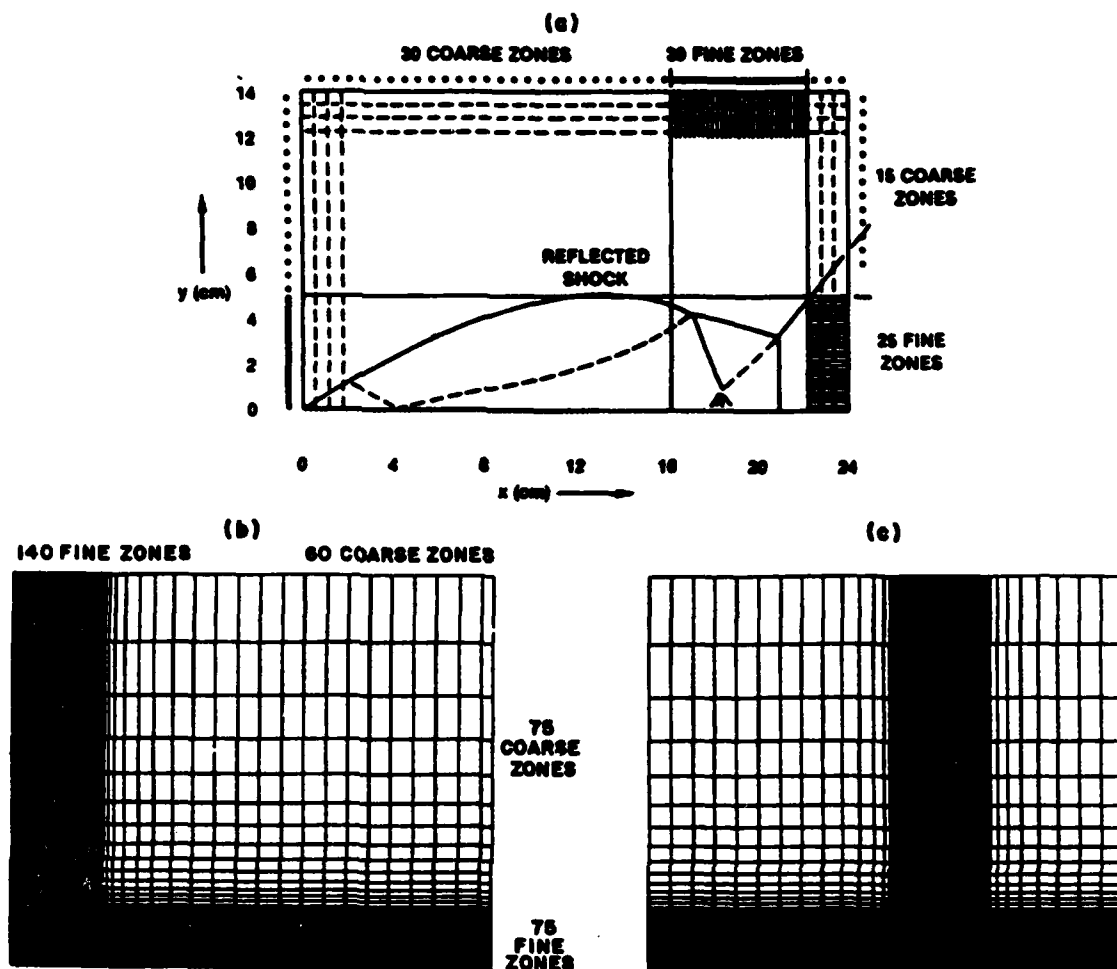


Fig. 1. Adaptive grids for a) planar shocks on wedge (double Mach shock features are indicated); b) and c) HOB problem initially and at transition point (grid lines in fine-zone region are indistinguishable).

SHOCK-ON-WEDGE CALCULATIONS

The JPBFACT algorithm was used in a 2-D Cartesian version of the FAST2D code to model the reflections of planar shocks from wedges of 20° to 60° and varying shock strengths. Four general classes which include regular, single, complex and double Mach reflection were calculated (referred to as cases a,b,c,d respectively). The bottom of the mesh, treated as a reflecting boundary, modeled the surface of the wedge. Quantities on the right hand boundary and on the top were set equal to the ambient values. The remaining boundaries were treated as permeable. In the single, complex, and double Mach reflection cases, the mesh was anchored on the left, essentially at the wedge tip where the incident shock first strikes, while the zones were stretched by a scaling factor proportional to t as soon as the reflection region filled a substantial portion of the grid. In case (d), the double Mach reflection case, the opening angle is so small that the incident shock has to traverse many zones before the mach stem has grown large enough to be well resolved. For this reason, the problem was solved on a uniform mesh in the frame of reference fixed

to the reflection point, with stretching being initiated after the first Mach stem reached ~ 20 cells in length. The timestep was recalculated at every cycle with a Courant number of 0.5.

Figure 2 shows the pressure and density contours and the velocity field for cases a,b,c,d. The pertinent shock phenomena can be easily identified: incident shock, contact surface, first and second Mach stems. As shown in Fig. 1, the zoning is particularly sparse except for the region of interest. Adequate resolution of the key surfaces (contact and second Mach stem) is obtained with 5 zones in each direction. The accuracy can be evaluated by comparing the experimental density distributions along the wall (Fig. 3).

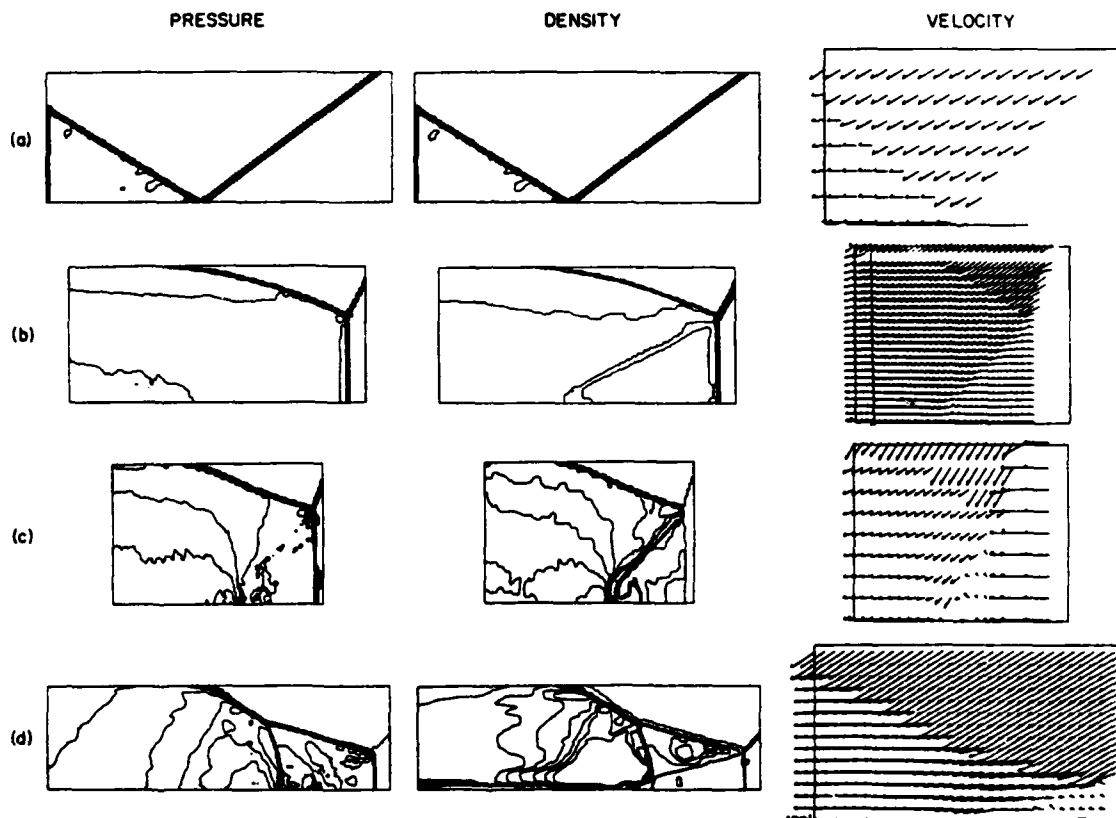


Fig. 2 - Pressure and density contours and flow velocity vectors (in frame of reflection point) for planar waves with Mach number M reflecting from wedges with angle θ for (a) $M=2.03$, $\theta=60^\circ$; (b) $M=2.82$, $\theta=20^\circ$; (c) $M=5.29$, $\theta=30^\circ$; (d) $M=7.03$, $\theta=50^\circ$

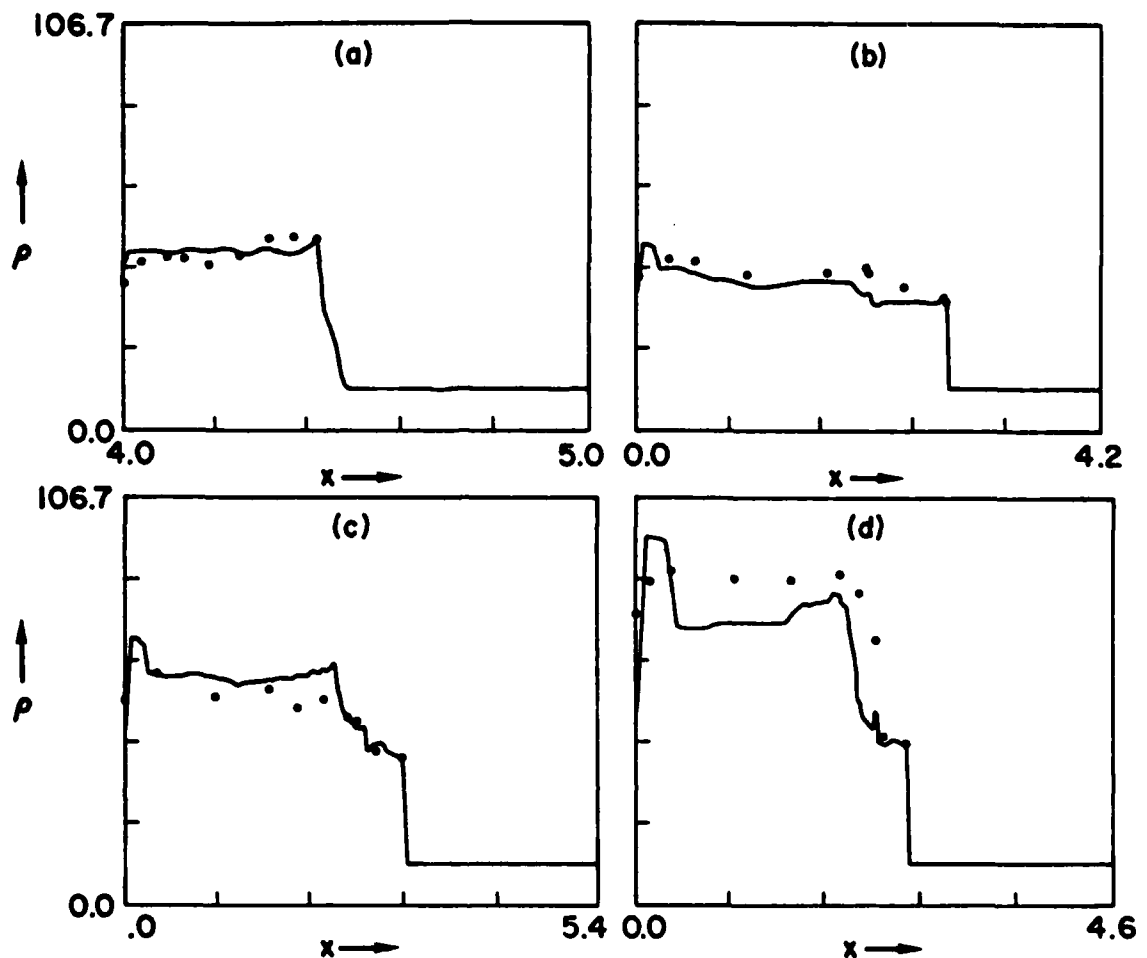


Fig. 3. Comparison of density (in units of ambient density ρ_0) for cases (a), (b), (c), (d) of Fig. 2 vs. distance from corner. Points are measured values reported in Ref. 13.

HEIGHT OF BURST CALCULATIONS

Next, we performed a numerical simulation of a 1KT nuclear detonation at 31.7 m HOB, a case which could be readily compared with high explosive data. A constant ambient atmosphere was used with a density of $1.22 \times 10^{-3} \text{ g/cm}^3$ and pressure $1.01 \times 10^6 \text{ dynes/cm}^2$. To relate the energy and density to the pressure, a real-air equation of state (EOS) was used. This table-lookup EOS was derived from theoretical calculations by Gilmore^{14,15} for equilibrium properties of air and has been vectorized for the Advanced Scientific Computer¹⁶. The internal energy density used in the call to the EOS is found by subtracting kinetic from total energy; this can be negative due to truncation (phase) errors. When this occurred, the value of the pressure was reset to zero.

The transition from regular reflection to double Mach reflection occurs at a ground range approximately equal to the HOB. The size of the mesh should

therefore be roughly twice the HOB in both directions. The upper boundary should be far enough away from the blast front to be non-interfering. We chose boundaries of 55 m for the radial direction and 103.5 m for the axial direction. The fine grid in the radial direction contained 140 out of 200 total zones, each 5 cm in length. The rightmost zones were 80 cm in length, and a smoothing involving 40 zones was performed between the regions to guarantee that the zone sizes varied slowly. In the axial direction the fine grid contained 75 out of 150 total zones, each 5 cm in length. Beyond that region the zones were geometrically increased by a factor of 1.112.

Placement of the fine grid at the origin of the mesh (ground zero, the point at which reflection first occurs) was determined to be optimum for capturing peak pressure in the airblast wavefront. Thus, as the expanding wave moves along the ground surface, the fine grid is always locked to it and each point along the blast front encounters the same spatial gridding as it approaches the ground. By treating each point of the incident front in the same manner, we insure that the calculation is internally consistent and that the computed transition point is accurate to within the limits of the resolution.

The initialization provides a strong shock with approximate Mach number $M=12$. This speed and the need for restart capability led to the choice of 200 timesteps as an interval for the spatial display (snapshots). The dump interval that resulted was $\Delta t \sim 0.3$ milliseconds (ms). These dumps were stored on magnetic tape and post-processed.

A fit to the 1-D nuclear blast flow field (Ref. 17) was used to initialize the energy and mass density and velocity field at 3.76 ms. The corresponding peak overpressure was 113 bars. After the 1 KT flow field was laid down inside a radius of 31.6 m, the fine-zone grid was activated to follow the peak pressure as it moved along the ground surface, modelled as a perfectly reflecting boundary. This region comprised 140 zones, and a switch was set to keep 40 of these zones ahead of the reflection point. Permeable boundary conditions are used on the top and right edges of the mesh, i.e., density, pressure and velocity are set equal to ambient preshock conditions. Reflecting conditions were applied to the left and bottom. The total elapsed physical time in the 2-D calculation, 7.6 ms, required 5600 cycles. Times are referred to $t=0$ at the start of the calculation.

The numerical simulation begins just before the shock first reflects from the ground. Fig. 4a indicates the pressure and density contours and velocity vectors at time 3.18 ms. In Fig. 4b the reflected shock is shown moving upward, the outward flow begins to stagnate at the ground (transition). Fig. 4c, $t=5.99$ ms, shows an enlargement of the shockfront, and the development of the Mach stem, slip surface and second Mach stem. The angle of the shock front with respect to the ground is increasing with time, so that the effective wedge angle is decreasing. From Ben-Dor and Glass¹⁸ one expects a transition to double Mach stem to occur at approximately 45° . The angle in Fig. 4b is about 45° and the shock front has entered the transition phase. Figure 4d shows the fully developed shock structure at 7.79 ms. Clearly visible is the second Mach stem and a vortex region behind the first Mach stem. Toeing out of the first Mach stem can be also seen in the contours of Fig. 4d and occurs as the fluid rolls forward where the slip line would otherwise intersect the ground. The velocity field in Fig. 4d also shows this detail.

One should also note the reflected shock properties. The reflected shock propagates rapidly through the high temperature fireball, due to the high local soundspeed. The shape of this reflected wave is a primary difference between the HOB case and the wedge case¹⁹. The other major difference, of course, is the spherically expanding blast wave which decreases in strength approximately proportional to r^{-2} .

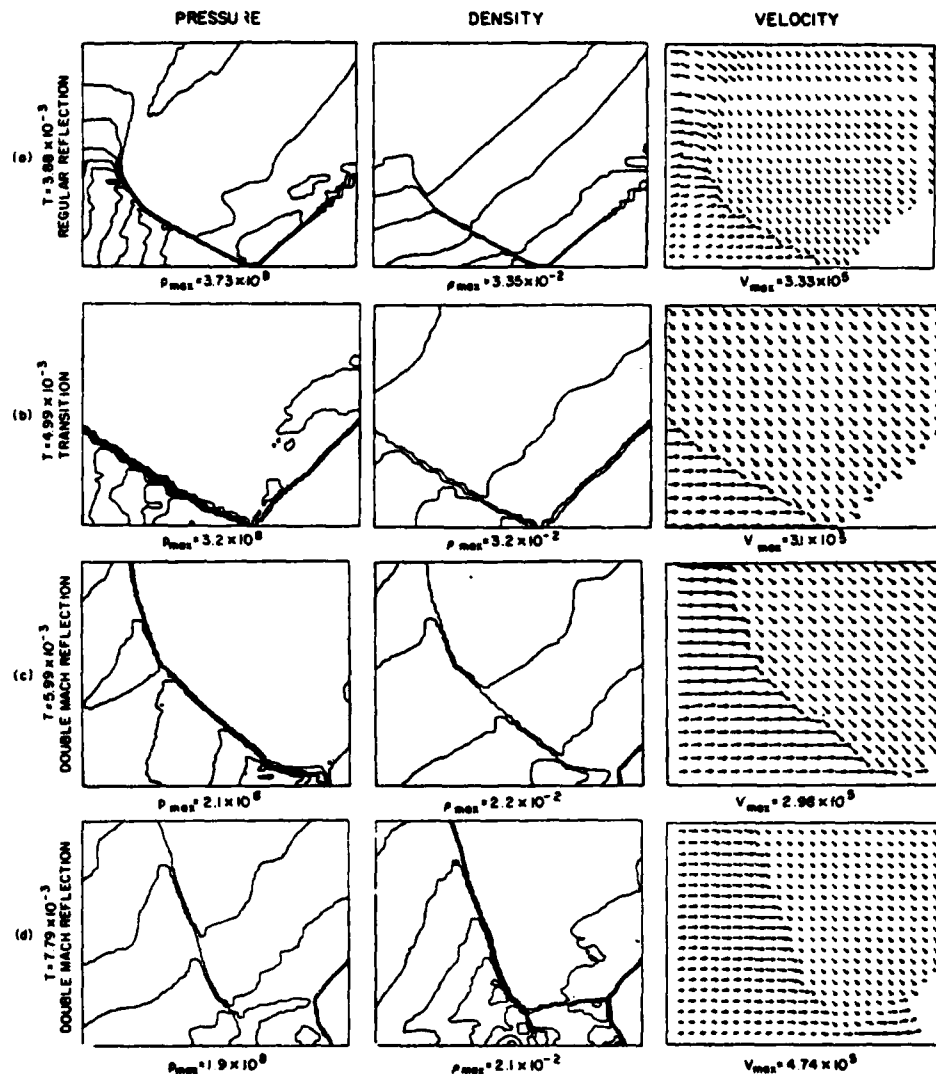


Fig. 4. Pressure, density, and velocity fields for HOB calculation (a) in regular reflection stage; (b) at transition to Mach reflection; (c) shortly afterward, when second peak has become larger than first; and (d) fully developed (note toe at base of first Mach stem).

Finally we consider the pressure/distance relation for the HOB case. In Fig. 5 we compare the results of the numerical simulation with the data of Carpenter and with empirical analysis. Carpenter's data are based upon careful HOB experiments with 8 lb PBX9404 spheres. The empirical analysis was based on a 1 KT nuclear free air curve and HOB construction factors. The calculated values in the regular reflection regime are 20% low and may be attributed to a combination of FCT clipping, the resolution of the grid, and inaccuracies in the initialization of the flow field. During and after Mach reflection, the peaks remain low until the Mach stem structure has grown large enough to be resolved on the mesh. By the time it occupies a region of 15 cells high and 35 cells wide, the peak pressures are in good agreement with the HE data and the empirical analysis.

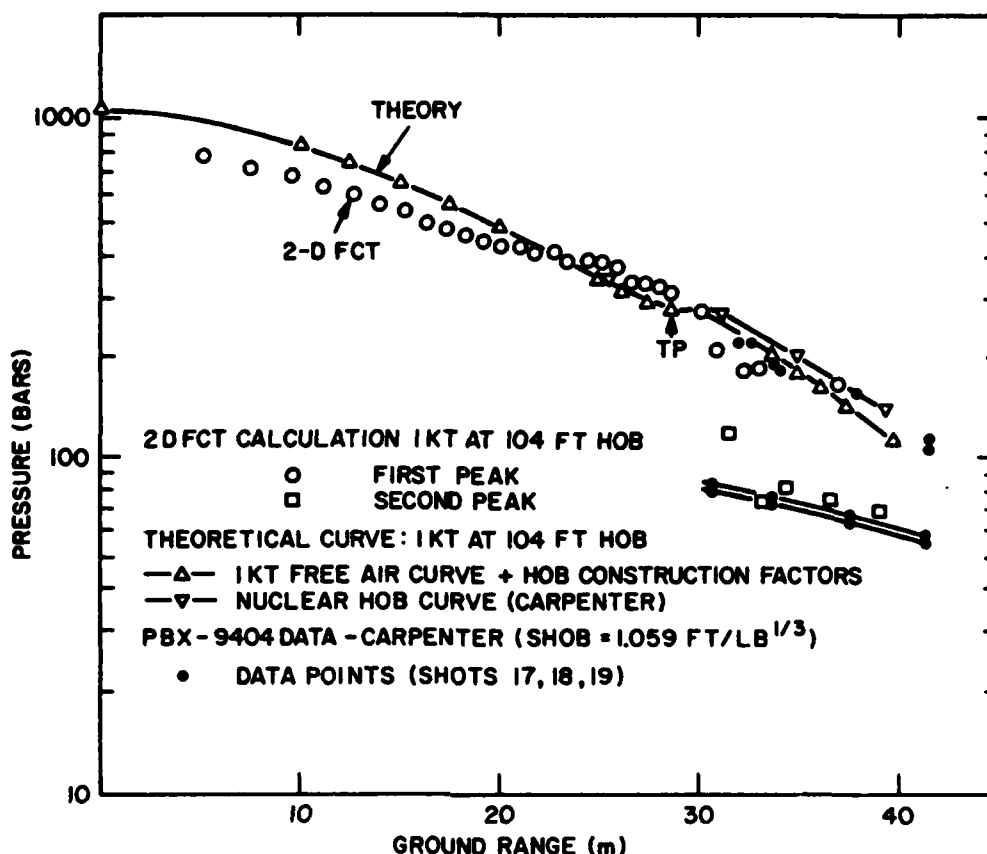


Fig. 5. Pressure-range curves for first and second (after transition - denoted by TP - to double Mach reflection) peaks.

SUMMARY AND CONCLUSION

The complex 2-D Mach reflection phenomena associated with shock diffraction on wedges and height-of-burst explosions have been modeled with the FAST2D computer code. Four wedge cases--regular, single, complex and double Mach reflection--have been calculated and the results compared to experiments. A nuclear detonation (1 KT at 31.7m HOB) was also simulated. The results give insight into the formation and subsequent evolution of the Mach stem, the triple point and the contact discontinuity. The transition from regular reflection to double Mach reflection is predicted. Excellent agreement with Ben-Dor's data is obtained. We suggest that the first signal for transition is the appearance of a second peak behind the shock front due to stagnation in the flow. Calculated first and second pressure peaks versus distance in the HOB case agree both with the HE data and analysis to within 20%.

The use of the adaptive regridding procedure, called "sliding rezone", along with the FCT algorithm allows one to accurately predict the nonsteady shock structures in two dimensions for diffractions on wedges and HOB cases. Comparison with data for both wedges and HOB yields the best results obtained to date.

ACKNOWLEDGEMENT

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Appendix B

A THEORETICAL STUDY OF THE
IGNITION OF PRE-MIXED GASES

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ABSTRACT

In this paper, time-dependent results obtained from both a simple but nonlinear analytic similarity solution and a detailed numerical simulation model are used to study the interactions between the fundamental processes occurring in the ignition of homogeneous premixed gases. The parameters which may be varied are the composition of the mixture, the initial radius of energy deposition R_0 , the duration of the heating T_0 , and the total energy deposited in the system E_0 . The similarity solution plus the induction time for the fuel-oxidizer mixture as a function of temperature and pressure can be used to calculate whether or not a given energy source is adequate to ignite the system. This simple procedure is then calibrated using a time-dependent detailed numerical reactive flow model which includes the thermophysical properties of the mixture, a full chemical kinetics scheme, nonlinear convection, molecular diffusion and thermal conduction. Calculations are presented for a selected mixture of $H_2-O_2-N_2$ for various values of R_0 and E_0 . These show that the similarity solution predicts ignition accurately when the radius of energy deposition is larger than the quench-radius. The detailed numerical reactive flow model is used to predict the quench-radius and the absolute minimum ignition energy associated with it.

NOMENCLATURE

A	Nonlinear amplitude in similarity solution
E	Energy
E_o	Total amount of energy deposited
I	Induction Parameter
k	Scale size in similarity solution
k_B	Boltzmann's constant
N	Total number density
n_j	Number density of species j
P	Pressure
P_j	Term representing production of species j
Q_D	Contribution to the heat flux vector due to diffusion
Q_j	Term representing loss of species j
R_o	Initial radius of deposition
R_c	Characteristic radius of energy deposition
r	Radial distance
T	Temperature
t	time
v	fluid velocity
v_j	Diffusion velocity of species j
γ	ratio of specific heats, c_p/c_v
η_m	mixture viscosity coefficient
λ_m	mixture thermal conductivity coefficient
ρ	mass density
τ_o	time period during which energy is deposited
τ_c	chemical-induction time

INTRODUCTION

An external source of energy can initiate interactions among the controlling convective, diffusive and chemical processes in a fuel-oxidizer mixture. Whether the interactions result in ignition of a deflagration or detonation wave depends on the intensity, duration, and volume affected by the external heat source. Ignition will also depend on the initial ambient properties of the mixture which determine the chemical induction time and the heat release per gram of material. Thus ignition is a complicated phenomena whose occurrence for a specific mixture of fuel and oxidizer depends strongly on diffusive and chemical parameters which are often very poorly known.

It is possible, in principle, to study flame ignition by performing detailed numerical simulations. This is a complicated, multi-dimensional, multi-species, time-dependent problem which has been solved in certain limited cases (see e.g., Ref. 1). Part of the complication and cost of such calculations arises from the multi-dimensional solution of the conservation equations, but at least as much arises from integrating the large number of ordinary differential equations describing the chemical reactions. This latter factor is further complicated by the fact that we usually do not have an adequate representation of the chemical reactions with which to work. Thus a convenient, inexpensive way to estimate whether a mixture will ignite given a heat source intensity, duration, and volume would be a very valuable laboratory tool and a useful learning device.

This paper represents an extension and clarification of the work described by Oran and Boris [1,2]. They presented a preliminary summary of a simplified, theoretical model of localized ignition of a homogeneous, premixed gas and explained how it could be calibrated by using a detailed simulation. In this paper the calibration of the simplified model is extended and the results are compared in detail to those of detailed, one-dimensional simulations. After a brief review of related literature, the essential properties of the detailed, time-dependent, numerical model are presented. Then a description is given of a closed form similarity solution for the nonlinear time-dependent slow flow equation which forms the basis for the simplified model of localized ignition. The similarity model avoids the integration of the ordinary differential equations describing the chemical reactions by defining an induction parameter. Two constants must be calibrated; the radius at which the thermal conductivity is evaluated and the radius at which the induction parameter is evaluated. Finally, comparisons between the two models are described for ignition of a $H_2-O_2-N_2$ mixture. The composition of the mixture and the duration of energy deposition are held constant but the total energy deposited and the radius of deposition are allowed to vary.

BACKGROUND

Ignition phenomena and the associated properties of minimum ignition energies and quench volumes have been studied both experimentally and theoretically. Lewis and von Elbe [3] have reported extensive experimental data on ignition by electric sparks. Weinberg and Wilson [4] and Kingdon and Weinberg [5] have compared the ignition energies required when a spark and a laser were the source of ignition. The former paper [4] concludes that the laser minimum ignition energy is very much less than that required by a spark for mixtures at low pressures or near the flammability limit. They have attributed this difference to the influence of the electrodes and the losses to them since the quenching distances are large under the above conditions. The latter paper [5] concludes that for short pulses applied to mixtures with small quenching distances, the energies required by the two ignition sources are not that different.

Dixon-Lewis and Shepherd [6] have used a time-dependent flame model to examine the effects of varying the initial radical concentration and of changing the geometry of the initial hot core. Their studies were done on a homogeneous premixed 60% hydrogen-air mixture in which energy was deposited instantaneously in the form of hydrogen atom radicals and temperature. They found that energy in the form of hydrogen atoms was more efficient at igniting a flame. Dixon-Lewis [7] then looked for a minimum quench volume in the same 60% hydrogen-air mixture in which one third of the added energy was in the form of hydrogen atoms.

Another point noted by both Overley et al. [8] and by Dixon-Lewis and Shepherd [6] is that the shape and size of the mixture core is important in determining the minimum ignition energy. The former paper presented a study of a hydrazine mixture in both spherical and prolate spheroidal coordinates. The latter paper considered both cylindrical and spherical systems. Both papers investigated the effects of flame curvature on burning velocity.

The work of Ballal and Lefebvre [9] is a detailed experimental investigation of the effects of pressure, velocity, turbulent intensity and scale, and mixture composition on the minimum ignition energy and quench distance in a flowing gas mixture. Using the data as a guide, they analyzed the important transport and turbulent processes and developed a highly simplified model for the quench distance in the limit of low and high turbulence. The data has allowed them to calibrate the model and determine important constants.

THE DETAILED NUMERICAL SIMULATION MODEL

This section describes the detailed numerical flame model which solves the time-dependent conservation equations for total mass ρ , momentum $\rho \underline{v}$, energy E , and individual species densities n_j [2,10]:

$$\frac{\partial \rho}{\partial t} = -\underline{\nabla} \cdot \rho \underline{v} \quad (1)$$

$$\frac{\partial n_j}{\partial t} = -\underline{\nabla} \cdot n_j \underline{v}_j - \underline{\nabla} \cdot n_j \underline{v} + P_j - Q_j n_j \quad (2)$$

$$\frac{\partial \rho \underline{v}}{\partial t} = -\underline{\nabla} \cdot (\rho \underline{v} \underline{v}) - \underline{\nabla} P + \underline{\nabla} \cdot \underline{\eta}_m [\underline{\nabla} \underline{v} + (\underline{\nabla} \underline{v})^T] \quad (3)$$

$$\frac{\partial E}{\partial t} = -\underline{\nabla} \cdot E \underline{v} - \underline{\nabla} \cdot (P \underline{v} - \frac{\lambda}{m} \underline{\nabla} T - \underline{Q}_D) \quad (4)$$

The technique for solving the various terms in these equations is based on the method of asymptotic timestep splitting in which the individual chemical and physical processes are integrated separately and then asymptotically coupled together [1]. The model permits a wide variety of geometric, initial, boundary and time-varying energy input conditions and was specifically developed to study the various physical and chemical processes which control flame initiation and quenching. [23].

The convective transport is solved by the algorithm ADINC, a Lagrangian hydrodynamic algorithm which solves implicitly for the pressures [11]. The method allows for arbitrary equations of state, gives an accurate representation of material interfaces, and allows steep gradients in species and temperature to be developed and maintained.

A number of tests of this algorithm have been documented by Boris [11] . An adaptive gridding method has been implemented in which cells are inserted or deleted according to externally specified physical conditions in the flow. The diffusion velocities are calculated using an iterative algorithm [12,1].

The chemical interactions are described by a set of nonlinear coupled ordinary differential equations. For this ignition study we have used the H_2-O_2 reaction scheme [13] given in Table 1 which involves the eight reactive species, H_2 , O_2 , O , H , OH , HO_2 , H_2O_2 , H_2O and diluent which is chosen to be N_2 . The thermochemical properties of these species were taken from the JANAF tables [14]. The ordinary differential equations describing the chemical kinetics are solved using a fully vectorized version of the selected asymptotic integration method, CHEMEQ, developed by Young [15,16].

Results from a typical flame calculation in spherical geometry are presented in Fig. 1. The figure depicts the time history of the temperature profile after 4mJ of energy is deposited over a period of 10^{-4} seconds. Even after the energy deposition is stopped the "core" temperature continues to increase due to the heat released in chemical reactions. With time, however, the temperature near the center decreases and the temperature away from the center increases due to heat conduction. In this case, since the rate of heat generation is greater than the rate of heat loss, the temperature profile develops into that of a typical flame temperature profile. Species profiles and details of the flame front have been presented elsewhere [2].

THE SIMILARITY SOLUTION

The similarity solution is derived from the slow flow approximation [1,17] and is predicated on the assumption that energy addition to the system is slow enough so that there is no shock heating. Thus the system is characterized by flow velocities which are small compared to the speed of sound, and an essentially constant pressure field. The energy and velocity equations may be written in terms of total derivatives as

$$\frac{dp}{dt} \approx 0 = -\gamma p \underline{\nabla} \cdot \underline{v} + \underline{\nabla} \cdot \gamma N k_B \kappa \nabla T + S(t) e^{-k^2(t)r^2} \quad (5)$$

and the continuity equation is written in the form

$$\frac{1}{p} \frac{dp}{dt} = -\underline{\nabla} \cdot \underline{v}. \quad (6)$$

In Eq. (5) γ is held constant, and κ is a function of the mixture thermal conductivity, λ_m ,

$$\kappa \equiv \frac{\gamma-1}{\gamma N k_B} \lambda_m(T). \quad (7)$$

The last term on the right hand side of Eq. (5) is the source term. Proper choice of $S(t)$ ensures that a given amount of energy, E_0 , is deposited in a certain time, τ_0 . It is the choice of this Gaussian profile which allows us to obtain the "closed" form similarity solution which is given below.

The details of the solution of Eqs. (5) and (6) are given in the Appendix at the end of this paper. The final results for the temperature and density as a function of time and position may be written as

$$T(r,t) = T_{\infty} e^{A(t)} e^{-k^2(t)r^2} \quad (8)$$

and

$$\rho(r,t) = \rho_{\infty} e^{-A(t)} e^{-k^2(t)r^2} \quad (9)$$

where T_{∞} and ρ_{∞} are the background temperature and density, respectively. In addition, two ordinary differential equations describing the evolution of $A(t)$ and $k(t)$ are required to complete the solution,

$$\frac{dk}{dt} = -kv_1 - 2kk^3 \quad (10)$$

$$\frac{dA}{dt} = \frac{S(t)}{\gamma P_{\infty}} - 2ck^2 A \quad (11)$$

where v_1 is an approximation to the velocity based on the assumption that $v(r,t) \equiv v_1(t)r$; and c is a constant which depends upon the configuration of the problem ($c = 1$ for cartesian, 2 for cylindrical and 3 for spherical coordinates). By comparing the results from this similarity solution model to those from the detailed numerical simulation model described earlier, we have seen that the linear dependence on r is a valid approximation before ignition occurs.

The model requires one further definition in order to predict ignition. The chemical induction time, which is a function of temperature and pressure, must be used to define the induction parameter,

$$I(T,P) = \int_0^t \frac{dt'}{\tau_c[T(r,t'), P(r,t')]} \quad (12)$$

For the work presented in this paper, pressure is constant throughout the calculation. Then $I(T, P_\infty)$ is integrated in time according to Eq. (12). Ignition "occurs" when $I(T, P_\infty) = 1$, which is an exact result in the limit of large heat source and constant temperature near the center of the heated region. Values of τ_c have been calculated [13] for a wide range of temperatures and pressures from the chemical rate scheme given in Table I. In general, τ_c as required in these calculations may be obtained from such detailed kinetic calculations, a few measured points, or from educated guesses. The concept of an induction parameter has been extended in scope and used extensively for reactive shock and detonation studies [e.g., 1, 18, 22].

The parameter κ in Eqs. (10) and (11) is found using the definition in Eq. (7). Determining the temperature (radius) at which κ is to be evaluated is part of the calibration to be done. For this, the derivation in the appendix was also done for the case where κ was assumed to be a function of radius (r). This analysis indicated that if κ is to maintain its similarity form and be a function of time alone, κ must be independent of r . Thus, within the framework of the similarity solution, the appropriate location at which to evaluate κ is at the center ($r = 0$). Determining the location at which the induction parameter, $I(T, P_\infty)$, should be evaluated is the second calibration to be done. This has been done by comparing the predictions of the two models and is discussed in the next section.

In summary, the approximations to Eqs. (1) - (4) which allows us to write Eq. (5) and obtain the solutions represented by Eqs. (8) - (11) are:

1. The flow velocities characteristic of the system are small compared to the speed of sound;
2. The pressure is essentially constant everywhere;
3. The ratio of specific heats, γ , is constant;
4. Molecular diffusion effects are not important until after ignition;
5. The velocity, $V(r,t)$ may be approximated by $V_1(t)r$;
6. The system is homogeneous and premixed;
7. The energy is input in a Gaussian form with a characteristic radius R_c which increases in time; and
8. The gas never gets hot enough to radiate away a significant fraction of its energy during the ignition period.

MODEL COMPARISONS

The calibration of the similarity model is complete when the location at which the induction parameter should be evaluated is determined. For this purpose, the results from detailed simulations are compared to those from the similarity model. Energy deposition in both models is linear in time at a rate determined by requiring an energy E_0 to be deposited in a time τ_0 . For all of the results discussed in this paper, τ_0 is taken to be 10^{-4} seconds. As in the similarity model, energy deposition in the detailed model is in the form of a Gaussian profile in space. The characteristic radius of the Gaussian, R_c , increases with time and is determined in the detailed simulation by the formula:

$$R_c^2 = \frac{2 \int r^2 \ln(T/T_\infty) dr}{\int \ln(T/T_\infty) dr} \quad (13)$$

The chemical model for these first tests was taken to be a mixture of $H_2:O_2:N_2$ in the ratio 2:1:10 at 1 atm and $T_\infty = 300^\circ K$. The induction time as a function of temperature for this mixture was derived from the detailed studies of the H_2-O_2 reaction mechanisms [13] and is shown in Fig. 2.

In the similarity model, κ was estimated by comparing the formula at $300^\circ K$,

$$\lambda_M^S = \frac{8.4 \times 10^3}{\bar{\sigma}^2} \sqrt{\frac{T(^{\circ}K)}{\bar{M}}} \frac{\text{erg}}{\text{cm sec } ^{\circ}K}, \quad (14)$$

which assumes that an average molecular distance $\bar{\sigma}$ and an average molecular weight \bar{M} may be found, to the more exact formulation

$$\lambda_m = \sum_j \lambda_j \left[1 + \frac{1}{2\sqrt{2}} \sum_{k \neq j} n_k W_{jk} \right]^{-1} \quad (15)$$

where W_{jk} is a function of $\{\lambda_j\}$ and the atomic masses $\{m_j\}$ suggested by Mason and Saxena [19]. This gives us

$$\bar{\sigma} = 3.16 \text{ A}$$

(16)

$$\bar{M} = 24.3.$$

This approximation is valid because the similarity solution is only accurate for ignition, that is, before any major amount of product or intermediates are formed. Then the parameter κ is found using the definition in Eq. (7). As discussed in the previous section, for the similarity solution κ is evaluated at the central ($r=0$) temperature. In contrast the detailed simulation uses Eq. (15) to evaluate the thermal conductivity at each cell at each time step.

In the first case studied, the initial radius of deposition, R_0 , was 0.1 cm and both models were configured for spherical symmetry. By varying E_0 and evaluating the induction parameter $I(T, P_\infty)$ at the central temperature ($r=0$) the similarity solution indicates that the minimum ignition energy is about 3.7mJ. Figure 3 shows the typical behavior of the amplitude, $A(t)$, and the characteristic radius, R_c , for this test case. If $I(T, P_\infty)$ is evaluated at $R = 0.06$ cm the minimum ignition energy predicted is about 5.1mJ, and if it is evaluated at R_c ignition is not predicted even when E_0 is raised to 8mJ. By comparing these predictions with those from the detailed simulation model we determine the location at which $I(T, P_\infty)$ must be evaluated. Results from the detailed simulation are shown in Fig. 4 for three values of E_0 . Ignition occurs when E_0 is greater than or equal to 3.7mJ. Therefore good agreement between the two models for the case under study is achieved by evaluating the induction parameter at the central temperature.

The central temperature and the induction parameter have been shown for three values of E_0 in Figs. 5 and 6 respectively. The time at which ignition occurs ($I=1.0$) is shown by a '*' in Fig. 6. A comparison with the

results from the detailed simulation (Fig. 4) tells us that both models predict ignition at essentially the same time for a range of input energies. The temperature profiles predicted by the two models are presented in Fig. 7. The agreement is very good except for long times when the detailed simulation predicts higher temperatures than those from the similarity model. This is primarily due to the heat released in chemical reactions which is not included in the similarity model. It is interesting to note that the effects of molecular diffusion included in the detailed simulation model are not considered in the similarity solution model. The results presented have shown that these effects are not as important as the effects of thermal conduction in determining the ignition characteristics of the system under investigation.

The models were then re-configured for cylindrical geometry and the case, $R_0 = 0.1\text{cm}$, was again investigated. By varying E_0 , the similarity solution indicates that the minimum ignition energy is about 3.5mJ/cm , not very different from the spherical case. The detailed simulation predicts that the minimum ignition energy is between 3.3 and 3.7mJ/cm , so again the predictions of both models are comparable when the induction parameter is evaluated at $r=0$.

EFFECT OF QUENCHING DISTANCE

As discussed in the previous section, good agreement between the predictions of the detailed simulation and the similarity solution is obtained for the case, $R_0 = 0.1$ cm. In order to determine if the agreement is good for other values of R_0 , various cases were studied and these have been summarized in Table II. Evaluating the induction parameter at the central temperature provides agreement between the ignition predictions of the two models for all the cases in which R_0 is greater than 0.1 cm. However, for radii smaller than 0.1 cm the similarity solution predicts a minimum ignition energy that is lower than for the $R_0 = 0.1$ case described above. In fact, as the initial radius of deposition decreases below 0.1 cm the similarity solution (with $I(T, P_\infty)$ evaluated at a fixed radius) predicts that the minimum ignition energy also decreases. The detailed simulation does not agree with this prediction. The radius 0.1 cm appears to be a "critical radius" below which the minimum ignition energy again increases. The above observation is similar to that made by Blanc, Guest, von Elbe and Lewis [20]. In their study of spark ignition, it was observed that there was a "critical electrode spacing" below which the minimum ignition energy increased. The critical electrode spacing was termed the "quenching distance".

To study the phenomena of "absolute" minimum ignition energies and quenching distances, the energy deposition in the detailed simulation needs to be modified. Up to this point energy was deposited in a Gaussian profile with a characteristic radius which increased with time. This was necessary in order to ensure that energy was deposited in a manner which closely matches the one derived from the similarity model. In the similarity model,

a Gaussian profile with characteristic radius increasing in time was essential to obtain the similarity solution described earlier. However, for studying the effect of the radius of deposition on the minimum ignition energy, it is confusing to have a varying radius of deposition. Therefore, for the results discussed below, energy is deposited in a Gaussian profile with a constant radius of deposition. As before, energy deposition is linear in time at a rate determined by requiring an energy E_0 to be deposited in a time τ_0 .

For a particular radius of deposition, a certain amount of energy is deposited and the computations are carried out for sufficient time until the existence (or absence) of a propagating flame is definite. By repeating the computations for different values of E_0 a bound for the minimum ignition energy for that particular radius is obtained. Similar calculations are performed for different values of the radius of deposition, R_0 . The results of such investigations are shown in Fig. 8. A propagating flame results when 3.8 mJ of energy is deposited in a sphere with a radius of 0.1 cm. However if the same amount of energy is deposited in a sphere of smaller radius, the rate of heat liberation is insufficient to compensate for the rate of heat loss and consequently there is no ignition. This radius, 0.1 cm, is the "quench-radius" for this particular mixture. For radii slightly larger than the quench-radius, the minimum ignition energy is almost constant and for larger radii (larger than 0.11 cm) the minimum ignition energy increases rapidly with increasing radii. Therefore for the system under study, the

absolute minimum ignition energy is about 3.7 mJ. These observations are in qualitative agreement with those of Lewis and von Elbe [21]. Quantitative comparisons are not possible since the composition of the mixture and the time for energy deposition are different.

This study of the "quench-radius" provides the insight needed to explain the discrepancy in the predictions of the similarity solution and the detailed model for small radii. We conclude that a volume smaller than the "quench-volume" needs to be maintained at a temperature T for a time which is longer than the corresponding induction time for ignition to occur. Therefore the concept of an induction parameter as it is used in the similarity solution is not valid for very small radii. If the absolute minimum ignition energy is deposited in a sphere of radius smaller than the quench radius, ignition will not occur since the heat generation rate within this smaller volume cannot compensate for the heat loss rate. This effect is not significant in measurements of induction time which are for larger radii. Therefore an agreement between the predictions of the two models can be forced for radii smaller than the quench-radius by evaluating the induction parameter at increasingly larger radii (i.e. lower temperatures). For example, when the initial radius of deposition is 0.08 cm, the detailed simulation predicts that the minimum ignition energy is between 3.4 and 5 mJ. The minimum ignition energy predicted by the similarity solution is 3.4 mJ if the induction parameter is evaluated at 0.06 cm and it is 5.1 mJ if the induction parameter is evaluated at 0.08 cm. For the case when the quench radius, $r_q = 0.1$ cm, the formula

$$r = r_q - Ae^{\frac{BR}{r_q}}; \quad (17)$$

$A = 2.84 \times 10^{-4}$ and $B = 58.78$ gives a good estimate for the radius at which to evaluate the induction parameter. We are currently seeking a more general formula to give this radius.

SUMMARY AND CONCLUSIONS

This paper describes a theoretical model for flame ignition based on a similarity solution which may be used to predict the ignition properties of a homogeneous mixture of gases. The model requires specification of the amount of energy input, E_0 , the length of time over which the energy is deposited, τ_0 , and the radius of energy deposition, R_0 . The model also requires basic information about the gas mixture which includes estimates of the thermal conductivity and the chemical induction time of the gas mixture as functions of temperature. Since a number of approximations have been applied to derive the model, it has been calibrated and its range of validity determined. This has been done by comparing its predictions to those of detailed numerical simulations.

The one-dimensional detailed numerical simulation used solves the set of coupled partial differential equations representing conservation of mass, momentum, and energy as well as individual species densities. For this study it was configured with an open boundary at one end to simulate an infinitely large system. Energy was deposited linearly with time, as it was done in the similarity solution, and the radius of deposition was chosen to mimic that determined by the characteristic radius in the similarity solution. The detailed model, however, contained calculations of the thermal conductivity and chemical kinetics which were much more accurate than the approximations used in the similarity solution. Furthermore, the detailed model contained the effects of molecular diffusion, which were not at all included in the similarity solution.

Predictions from the similarity model consist of an answer as to whether or not a given mixture would ignite given E_0 , τ_0 , and R_0 . Then if ignition is predicted, the model gives the time it takes for ignition to occur. In

contrast, the detailed simulation model not only predicts ignition, but also provides the structure of a propagating flame.

Comparisons of the predictions of the two models show that the system center is the optimal location for evaluation of an induction parameter, which is the indicator of ignition in the similarity model. Furthermore, the predictions of the similarity model are excellent when energy is deposited in a large enough volume. When the radius of deposition is less than the quench radius of the system, the similarity model is not accurate: the similarity model predicts ignition when the detailed model shows it does not occur. This can be compensated for by evaluating the induction parameter away from the system center. However, as with the value of the quench radius, the radius at which the induction parameter must be evaluated can be determined by comparisons with experiments or calculations performed with a detailed model.

After performing a series of studies which tested and calibrated the similarity model in cylindrical and spherical geometries, the detailed model was reconfigured to evaluate the quench radius and the minimum ignition energy of a particular gas mixture. This study provided insight into the source of the disagreement between the predictions of the similarity and detailed models at very small radii of energy deposition. The error occurred because the definition of an induction time is only valid for a volume of material that is large and homogeneous enough in temperature and pressure so that diffusive effects are not important. In the cases where the radii of deposition were very small, increased thermal conductivity due to a steep temperature gradient eroded the high temperature region too quickly. Thus in the competition between chemical energy release to heat a region and thermal conduction to cool it, thermal conduction dominated.

Further limits of validity of the simplified model should now be tested. These include investigating the sensitivity of predictions to time or mode of energy deposition, to variations in the chemical induction time, and to the effects of radiative losses discussed in the Appendix. These kinds of calibrations and determinations of the limitations and sensitivity of the similarity model are extremely important if we are to establish the level of accuracy required for input data. Once this has been done, the similarity model can be used with experimental input data to estimate quickly whether a material is flammable and if so, how much energy is required to ignite it. Another extension of the work presented here involves using the detailed simulation to investigate the effect of geometry and method of energy deposition on ignition energies and quenching distances. Both these studies are currently being pursued.

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APPENDIX

The derivation of the similarity solution model is discussed in detail here for the case of spherically symmetric geometry. Assuming that the pressure field is essentially constant and that no shocks are present, the conservation equations for momentum and energy may be combined to give

$$\frac{dP}{dt} \approx 0 = -\gamma P \underline{\nabla} \cdot \underline{v} + \underline{\nabla} \cdot \lambda n k_B \underline{\nabla} T + S(t) e^{-k^2(t)r^2} \quad (A1)$$

where κ and the Gaussian energy deposition term, $S(t)e^{-k^2 r^2}$, have already been discussed. The other equation required is the continuity equation,

$$\frac{1}{\rho} \frac{d\rho}{dt} = -\underline{\nabla} \cdot \underline{v} \quad (A2)$$

Assuming $dP/dt \approx 0$, Eq. (A1) gives an algebraic equation for $\underline{\nabla} \cdot \underline{v}$ which may be combined with Eq. (A2) to give

$$\frac{1}{T} \frac{dT}{dt} = \frac{S(t)}{P_\infty \gamma} e^{-k^2(t)r^2} + \underline{\nabla} \cdot \frac{\kappa}{T} \underline{\nabla} T \quad (A3)$$

where P_∞ is the background pressure. The solution is then

$$T(r,t) = T_\infty e^{A(t) e^{-k^2(t)r^2}} \quad (A4)$$

and

$$\rho(r,t) = \rho_\infty e^{-A(t) e^{-k^2(t)r^2}} \quad (A5)$$

where T_∞ and ρ_∞ are the background temperature and density, respectively.

Thus the nonlinear slow flow equations including expansions and contractions of the flow have been converted into a single equation which is linear in the logarithm of the temperature.

The total energy of the system at any instant is the sum of the internal energy and the work performed in expanding the heated region. It may be written

$$E(t) = \frac{P_{\infty} \gamma}{\gamma - 1} \int_0^{\infty} 4\pi r^2 dr \left[1 - \frac{\rho(r, t)}{\rho_{\infty}} \right] \quad (A6)$$

$$= \frac{\gamma P_{\infty}}{(\gamma - 1) k^3(t)} \int_0^{\infty} 4\pi x^2 \left[1 - e^{-Ax^2} \right] dx$$

$$= \frac{\gamma P_{\infty}}{(\gamma - 1) k^3(t)} F(A(t)). \quad (A7)$$

which defines the integral $F(A(t))$. Differentiating this we find that

$$\frac{dE}{dt} = \frac{\pi^{3/2} S(t)}{(\gamma - 1) k^3(t)} \quad (A8)$$

which may be equated to

$$\frac{dE}{dt} = \frac{\partial E}{\partial k} \frac{\partial k}{\partial t} + \frac{\partial E}{\partial A} \frac{\partial A}{\partial t}. \quad (A9)$$

Thus a consistency condition has been specified on the rates of change of the amplitude, $A(t)$, and the scale size $k^{-1}(t)$ for the heated region.

If the fluid velocity v is then expanded such that

$$v(r) \approx v_1(t) r, \quad (A10)$$

that is, only the linear term is kept, two coupled ordinary differential equations for k and A may be obtained,

$$\frac{dk}{dt} = -kv_1 - 2\kappa k^3 \quad (A11)$$

$$\frac{dA}{dt} = \frac{S(t)}{\gamma P} - 6\kappa k^2 A. \quad (A12)$$

Then the expression for v_1 may be written in terms of the integral $F(A)$

$$v_1 = \frac{S}{3\gamma P_{\infty}} \frac{F'(0) - F'(A)}{F(A)} + 2\kappa k^2 \frac{AF'(A) - F(A)}{F(A)} \quad (A13)$$

which results from using the principle of energy conservation and equating Eqs. (A8) and (A9).

EFFECT OF RADIATIVE LOSSES

When a large amount of energy is deposited in a small volume, the effect of radiative losses may be significant. Exact calculation of all the low temperature radiation effects is still beyond even the best detailed calculations today. An idealized model can be included in the similarity solution, however, to estimate these effects.

Black body radiation from a spherical surface at radius r takes energy out of the system at a rate

$$\frac{dE_{\text{rad}}}{dt} = 4\pi r^2 \sigma T^4(r). \quad (\text{A14})$$

In the similarity solution the temperature at any radius r is given by

$$T(r, t) = T_{\infty} e^{A(t)} e^{-k^2(t)r^2}. \quad (\text{A15})$$

Therefore,

$$\frac{dE_{\text{rad}}}{dt} = 4\pi \sigma T_{\infty}^4 r^2 e^{4A(t)} e^{-k^2(t)r^2}. \quad (\text{A16})$$

However at $t = 0$ ($A = 0$),

$$\frac{dE_{\text{rad}}}{dt} = 0. \quad (\text{A17})$$

Therefore the background radiation into the volume must be subtracted from (A 16) to give

$$\frac{dE_{\text{rad}}}{dt} = 4\pi \sigma T_{\infty}^4 r^2 e^{4A(t)} e^{-k^2(t)r^2} - 4\pi \sigma T_{\infty}^4 r^2. \quad (\text{A18})$$

The next step is to choose r such that Eq. A18 is maximized. By assuming that the loss from the system proceeds at the maximum rate possible, the model is sure to signal the onset of radiative loss effects at least as soon as they occur in the physical system itself.

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Table I. H_2-O_2 Elementary Reactive Mechanism

Reaction	$k_1 = AT^B \exp(-C/T)^{(a)}$			Reference
	A ^(b)	B	C ^(b)	
$H + HO \rightleftharpoons O + H_2$	1.40(-14) 3.00(-14)	1.00 1.00	3.50(+03) 4.48(+03)	[24] [24]
$H + HO_2 \rightleftharpoons H_2 + O_2$	4.20(-11) 9.10(-11)	0.00 0.00	3.50(+02) 2.91(+04)	[24] [24]
$H + HO_2 \rightleftharpoons HO + HO$	4.20(-10) 2.00(-11)	0.00 0.00	9.50(+02) 2.02(+04)	[24] [24]
$H + HO_2 \rightleftharpoons O + H_2O$	8.30(-11) 1.75(-12)	0.00 0.45	5.00(+02) 2.84(+04)	[25] $k_r = k_f/K_c$
$H + H_2O_2 \rightleftharpoons HO_2 + H_2$	2.80(-12) 1.20(-12)	0.00 0.00	1.90(+03) 9.40(+03)	[24] [24]
$H + H_2O_2 \rightleftharpoons HO + H_2O$	5.28(-10) 3.99(-10)	0.00 0.00	4.50(+03) 4.05(+04)	[24] $k_r = k_f/K_c$
$HO + H_2 \rightleftharpoons H + H_2O$	1.83(-15) 1.79(-14)	1.30 1.20	1.84(+03) 9.61(+03)	[26] [26]
$HO + HO \rightleftharpoons H_2 + O_2$	1.09(-13) 2.82(-11)	0.26 0.00	1.47(+04) 2.42(+04)	$k_f = k_r/K_c$ [27]
$HO + HO \rightleftharpoons O + H_2O$	1.00(-16) 3.20(-15)	1.30 1.16	0.00(+00) 8.77(+03)	[26] $k_r = k_f/K_c$
$HO + HO_2 \rightleftharpoons H_2O + O_2$	8.30(-11) 2.38(-10)	0.00 0.17	5.03(+02) 3.69(+04)	[28] $k_r = k_f/K_c$
$HO + H_2O \rightleftharpoons HO_2 + H_2$	1.70(-11) 4.70(-11)	0.00 0.00	9.10(+02) 1.65(+04)	[24] [24]
$HO + O_3 \rightleftharpoons HO_2 + O_2$	1.60(-12) 6.69(-14)	0.00 0.33	9.56(+02) 2.04(+04)	[25] $k_r = k_f/K_c$
$HO + H_2 \rightleftharpoons HO + H_2O$	1.20(-12) 1.33(-14)	0.00 0.43	9.41(+03) 3.62(+04)	[27] $k_r = k_f/K_c$
$HO_2 + HO_2 \rightleftharpoons H_2O_2 + O_2$	3.00(-11) 1.57(-09)	0.00 -0.38	5.00(+02) 2.20(+04)	[25] $k_r = k_f/K_c$

Table I. (continued)
H₂-O₂ Elementary Reactive Mechanism

Reaction	$k_1 = AT^B \exp(-C/T)^{(a)}$			Reference
	A ^(b)	B	C ^(b)	
O + HO \rightleftharpoons H + O ₂	2.72(-12) 3.70(-10)	0.28 0.00	-8.10(+01) 8.45(+03)	$k_f = k_r/K_c$ [24]
O + HO ₂ \rightleftharpoons HO + O ₂	8.32(-11) 2.20(-11)	0.00 0.18	5.03(+02) 2.82(+04)	[28] $k_r = k_f/K_c$
O + H ₂ O ₂ \rightleftharpoons H ₂ O + O ₂	1.40(-12) 5.70(-14)	0.00 0.52	2.12(+03) 4.48(+04)	[25] $k_r = k_f/K_c$
O + H ₂ O ₂ \rightleftharpoons HO + HO ₂	1.40(-12) 2.07(-15)	0.00 0.64	2.13(+03) 8.23(+03)	[25] $k_r = k_f/K_c$
H + H + M \rightleftharpoons H ₂ + M	1.80(-30) 3.70(-10)	-1.00 0.00	0.00(+00) 4.83(-04)	[24] [24]
H + HO + M \rightleftharpoons H ₂ O + M	6.20(-26) 5.80(-09)	-2.00 0.00	0.00(+00) 5.29(+04)	[24] [24]
H + O ₂ + M \rightleftharpoons HO ₂ + M	4.14(-33) 3.50(-09)	0.00 0.00	-5.00(+02) 2.30(+04)	[24] [24]
HO + HO + M \rightleftharpoons H ₂ O ₂ + M	2.50(-33) 2.00(-07)	0.00 0.00	-2.55(+03) 2.29(+04)	[24] [24]
O + H + M \rightleftharpoons HO + M	8.28(-29) 2.33(-10)	-1.00 0.21	0.00(+00) 5.10(+04)	[29] $k_r = k_f/K_c$
O + HO + M \rightleftharpoons HO ₂ + M	2.80(-31) 1.10(-04)	0.00 -0.43	0.00(+00) 3.22(+04)	[29] $k_r = k_f/K_c$
O + O + M \rightleftharpoons O ₂ + M	5.20(-35) 3.00(-06)	0.00 -1.00	-9.00(+02) 5.94(+04)	[24] [24]

- (a) Bimolecular reaction rate constants are given in units of cm³/(molecule sec).
Termolecular reaction rate constants are given in units of cm⁶/(molecule² sec).
- (b) Exponentials to the base 10 are given in parenthesis; i.e., 1.00(-10) = 1.00 X 10⁻¹⁰.

Table II

Case	Initial Radius of Deposition R_0 (cm)	Total Energy Deposited E_0 (mJ)	Ignition Prediction	
			Detailed Numerical Simulation	Similarity Solution
1	0.1	4.0	yes	yes
		3.7	yes	yes
		3.0	no	no
2	0.11	5.0	yes	yes
		3.0	no	no
3	0.12	7.0	yes	yes
		6.0	no	no
4	0.09	3.3	no	yes
5	0.08	3.3	no	yes

FIGURE CAPTIONS

- Figure 1 Time history of the temperature profile in a $H_2:O_2:N_2/2:1:10$ mixture as predicted by the detailed numerical simulation model.
- Figure 2 Temperature as a function of induction time for $H_2:O_2:N_2/2:1:10$ mixture evaluated using the chemical reaction scheme in Table I.
- Figure 3 The nonlinear amplitude, A , and the characteristic radius, R_c , as functions of time calculated using the similarity solution model.
- Figure 4 Calculations of the central temperature as a function of time for three values of E_0 using the detailed numerical simulation model.
- Figure 5 The central temperature as a function of time for three values of E_0 as predicted by the similarity solution model.
- Figure 6 Calculations of the induction parameter as a function of time for three values of E_0 using the similarity solution model. The "*" indicates the predicted time of ignition.
- Figure 7 Comparisons of the time history of the temperature profiles predicted by the detailed numerical model and the similarity solution model.
- Figure 8 The minimum ignition energy as a function of the radius of energy deposition calculated using detailed numerical simulations.

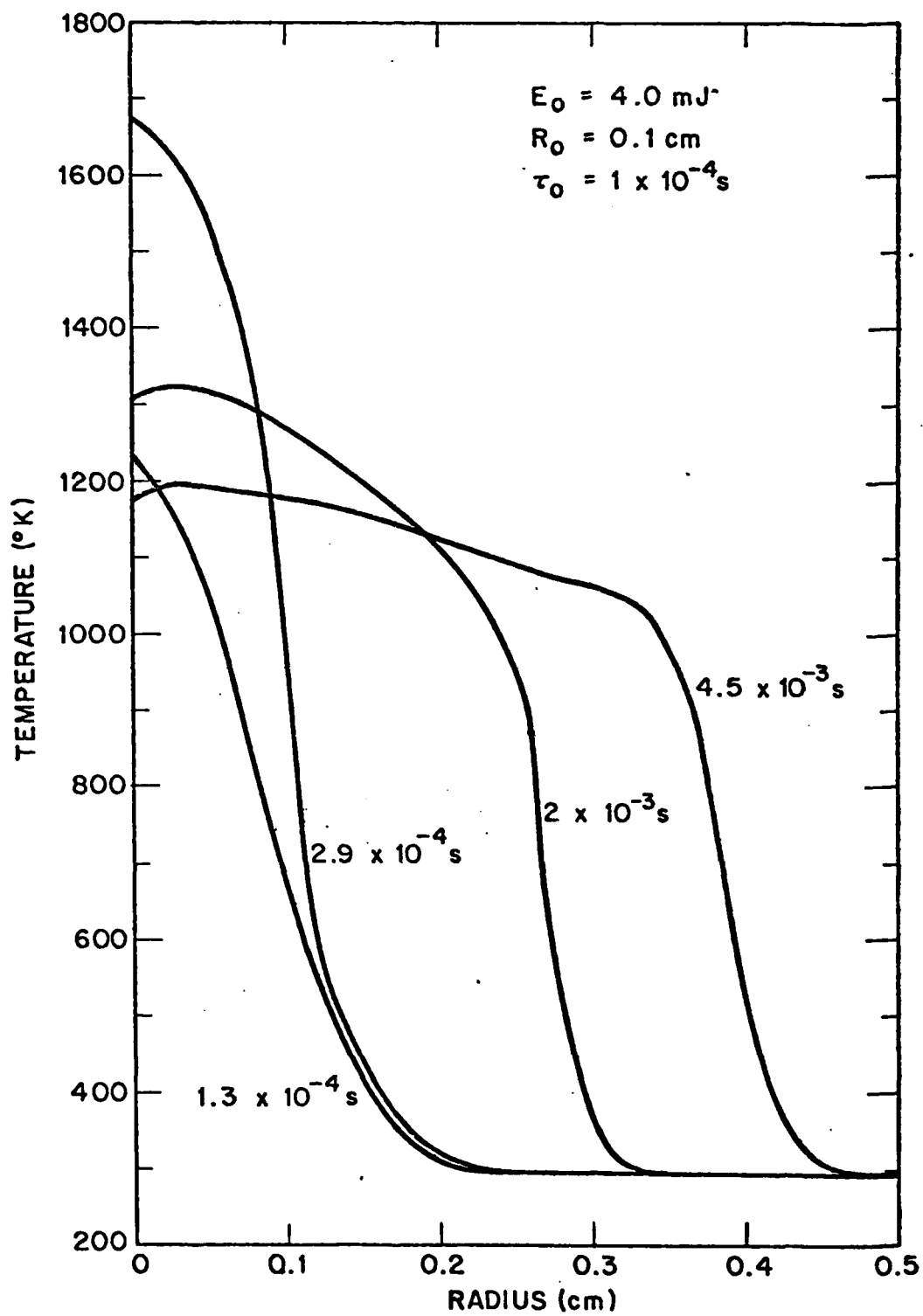


Figure 1

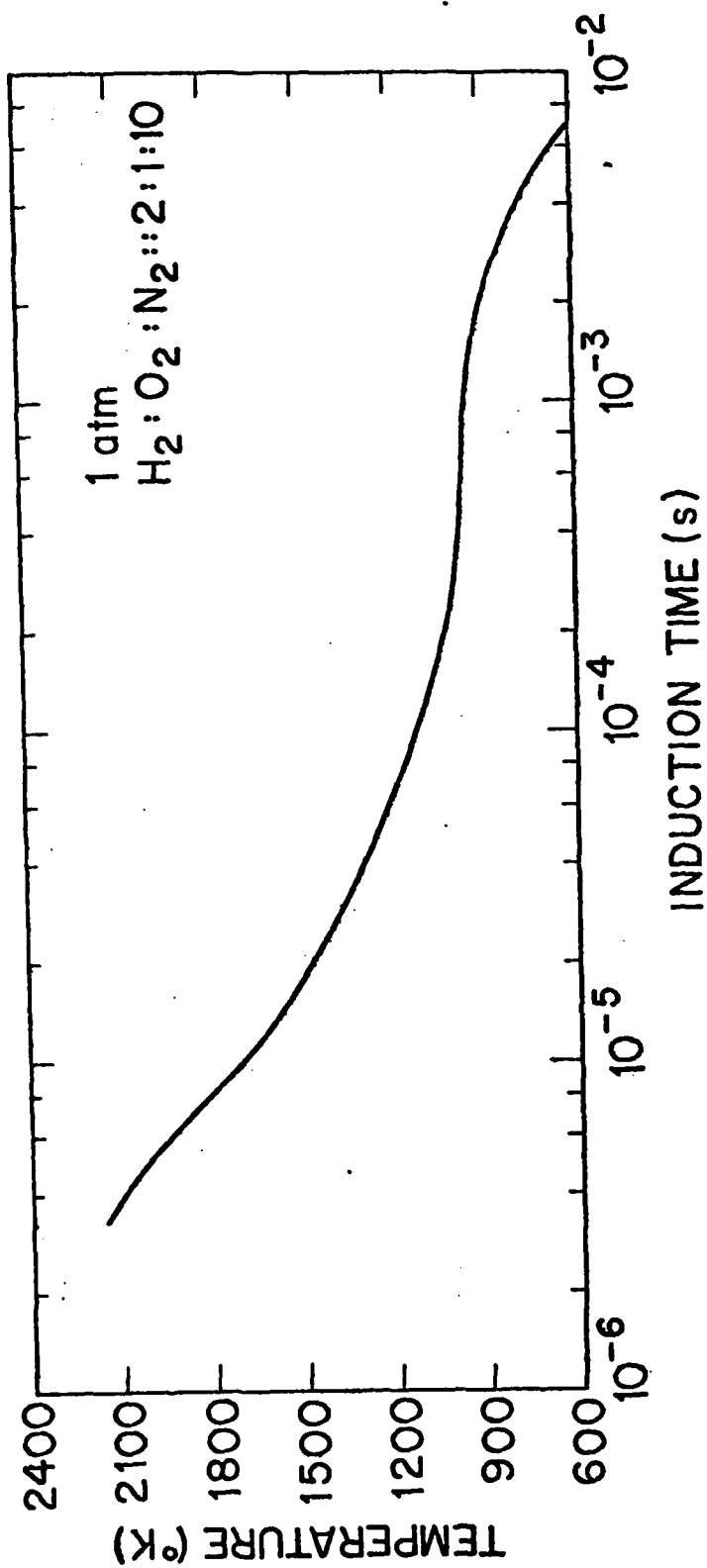


Figure 2

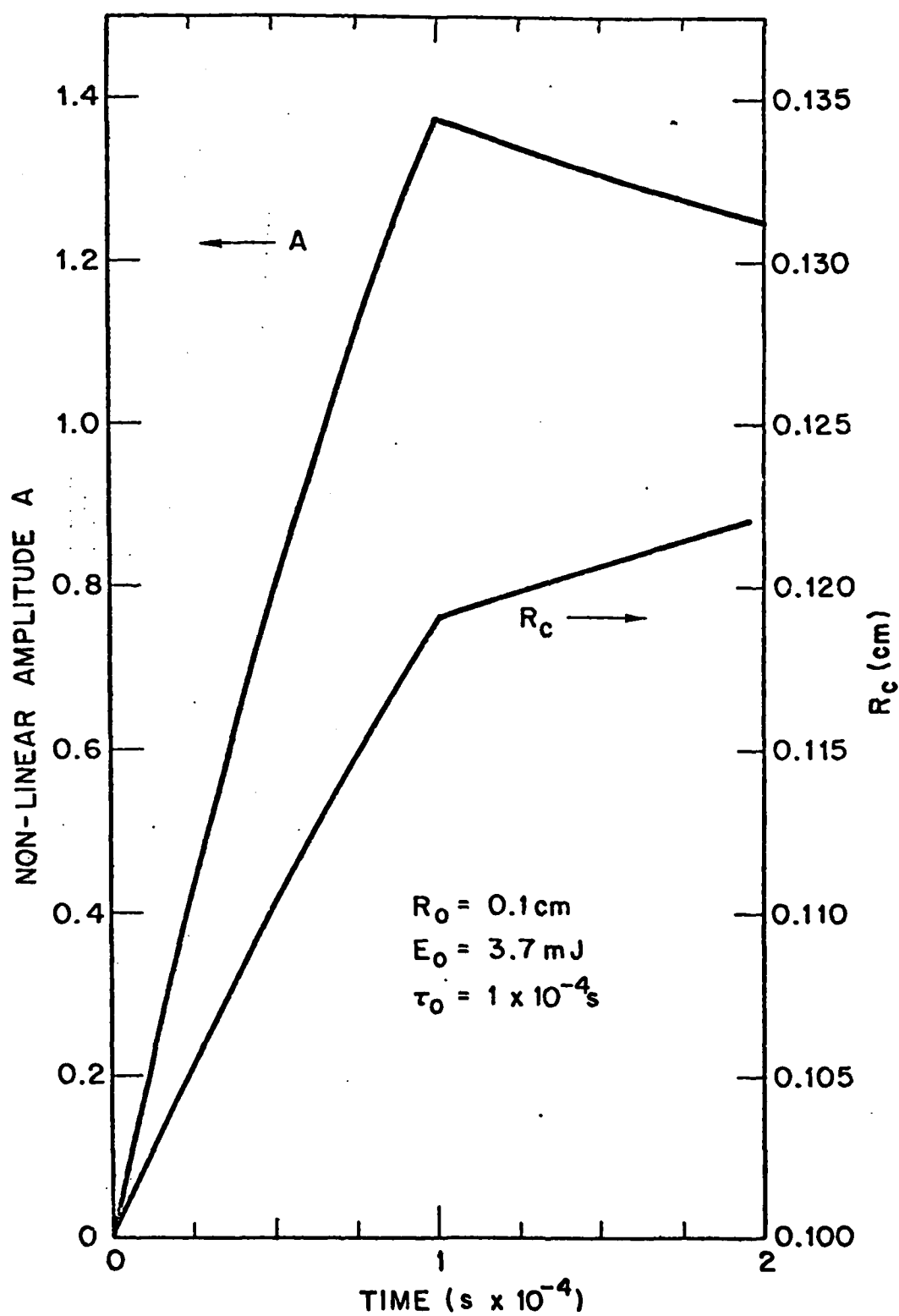


Figure 3

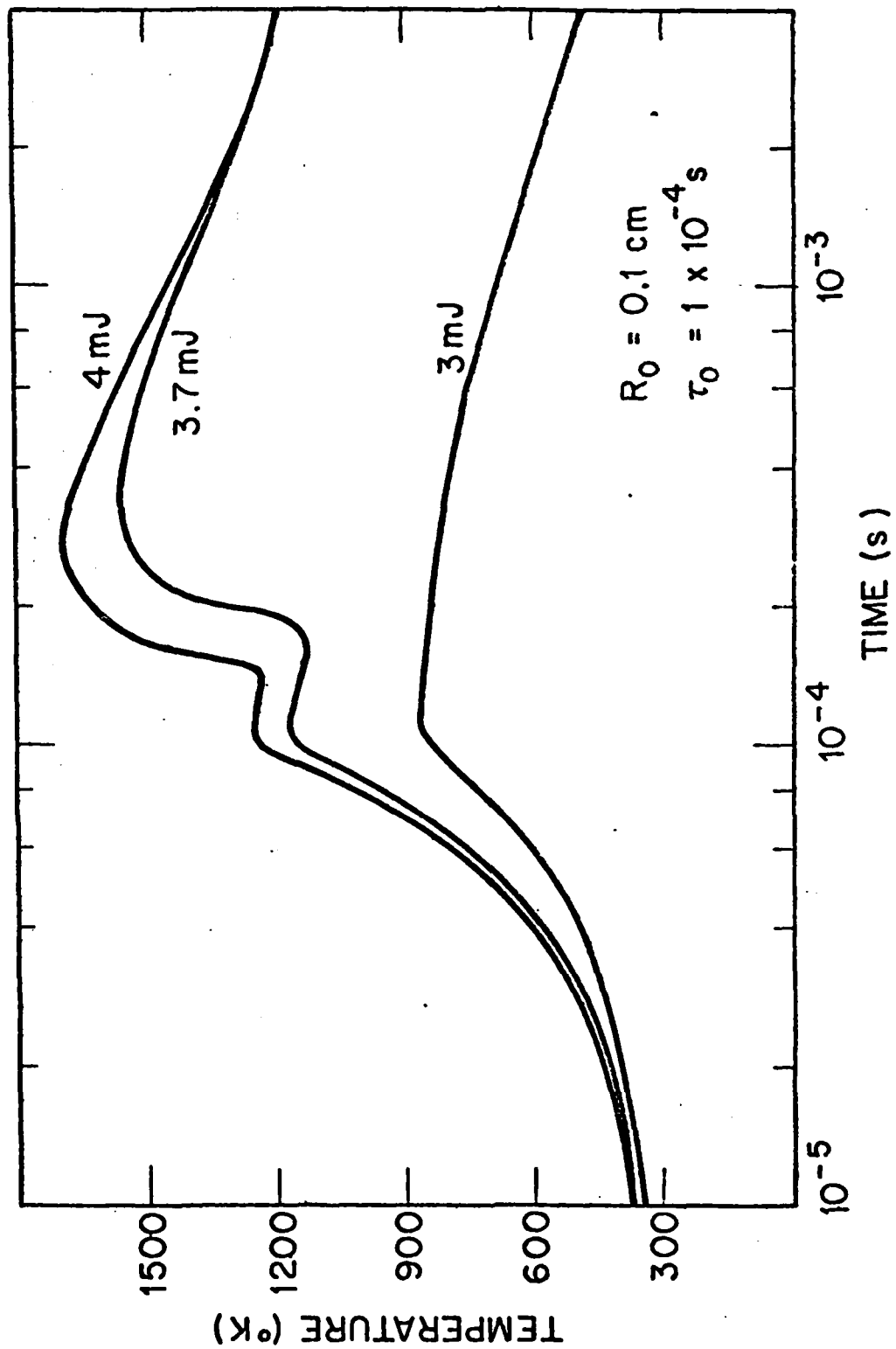


Figure 4

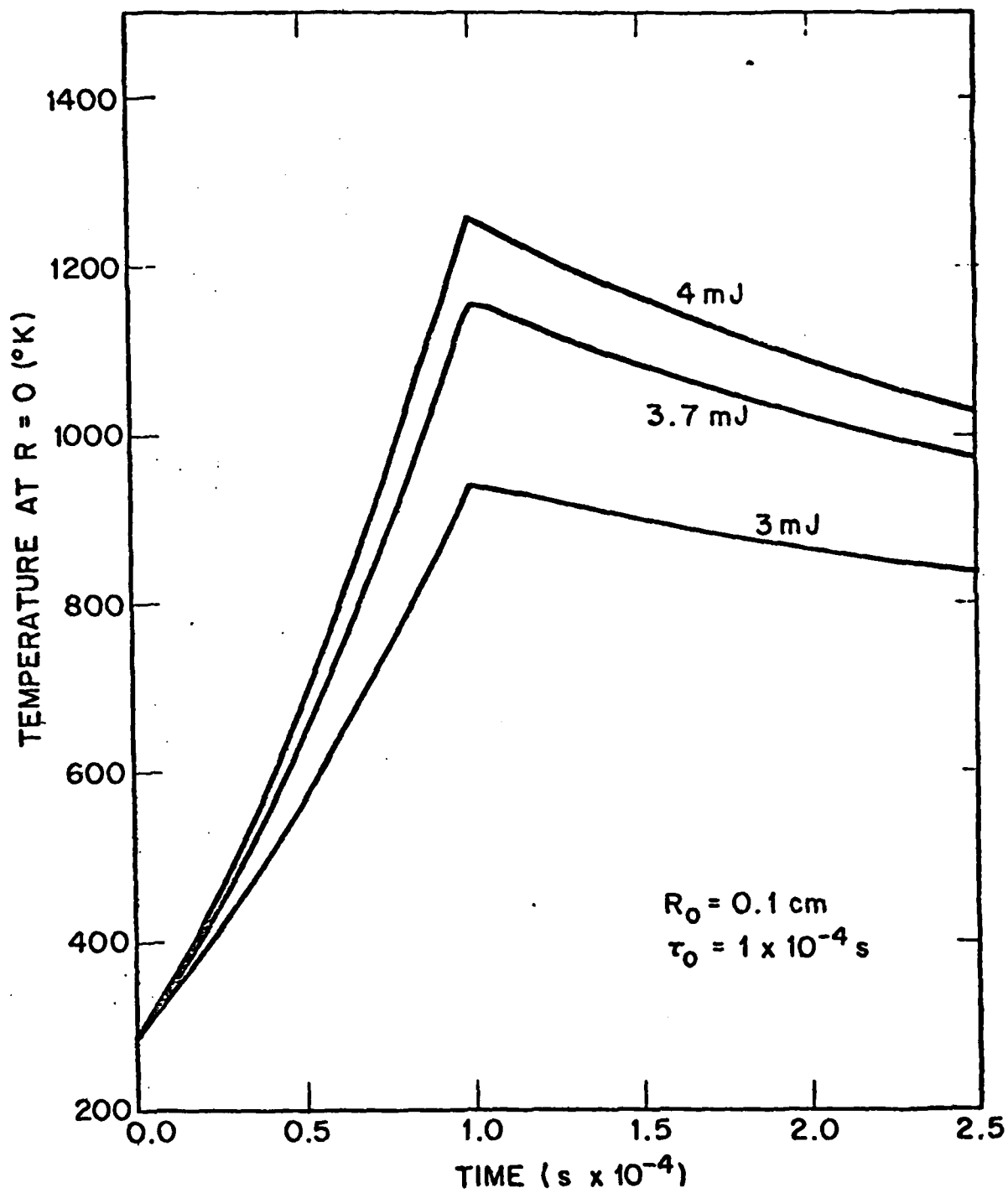


Figure 5

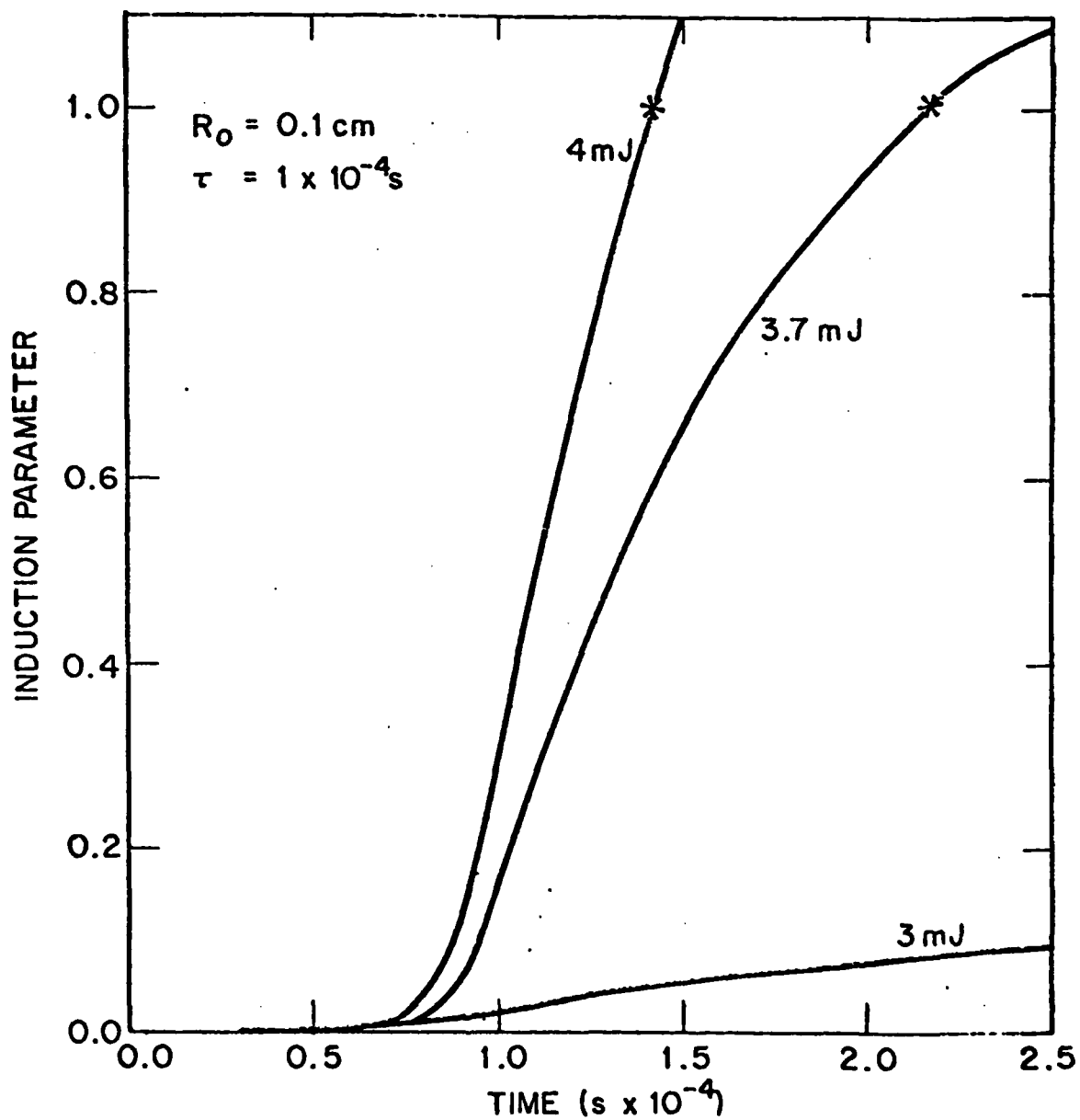


Figure 6

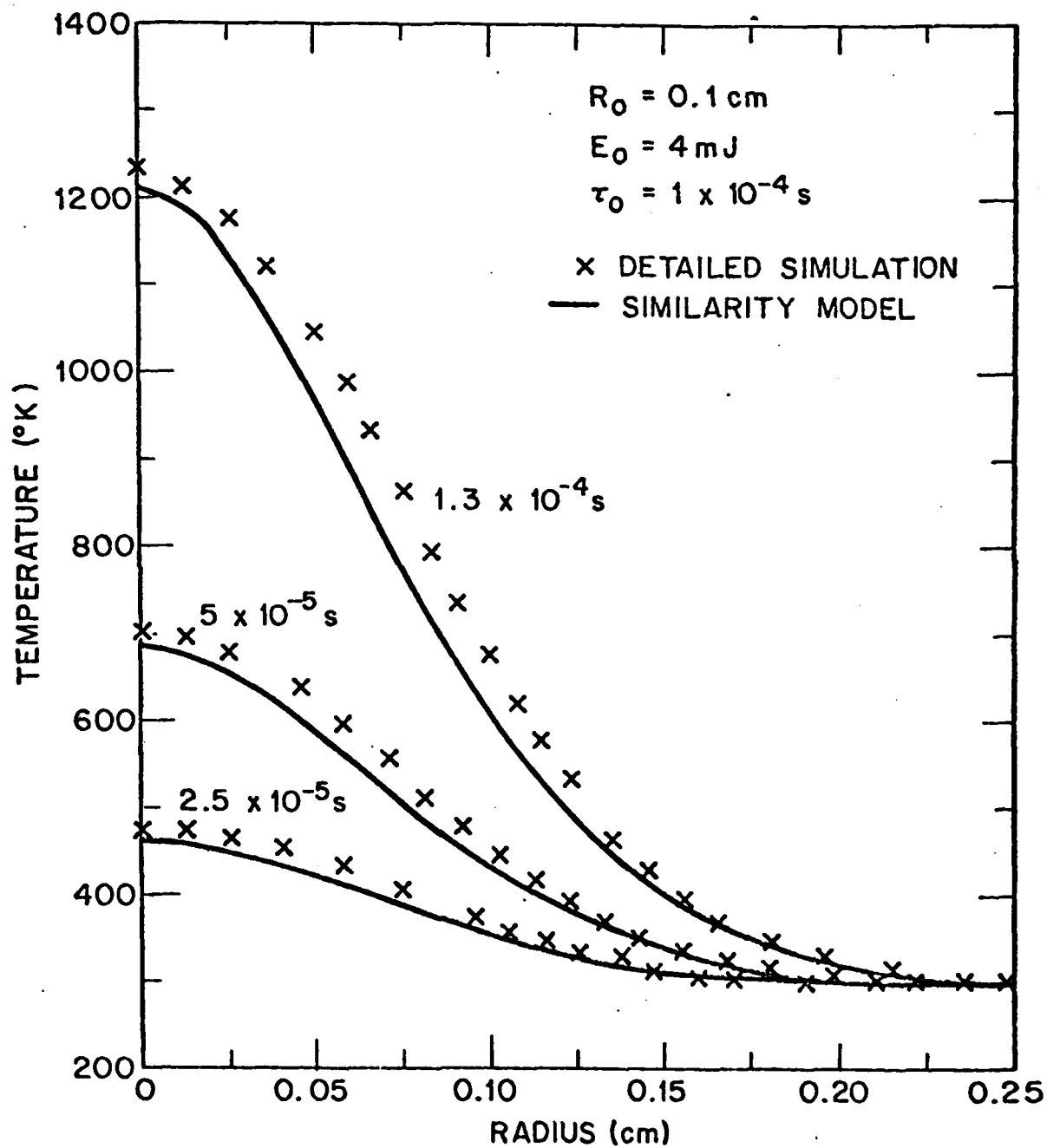


Figure 7

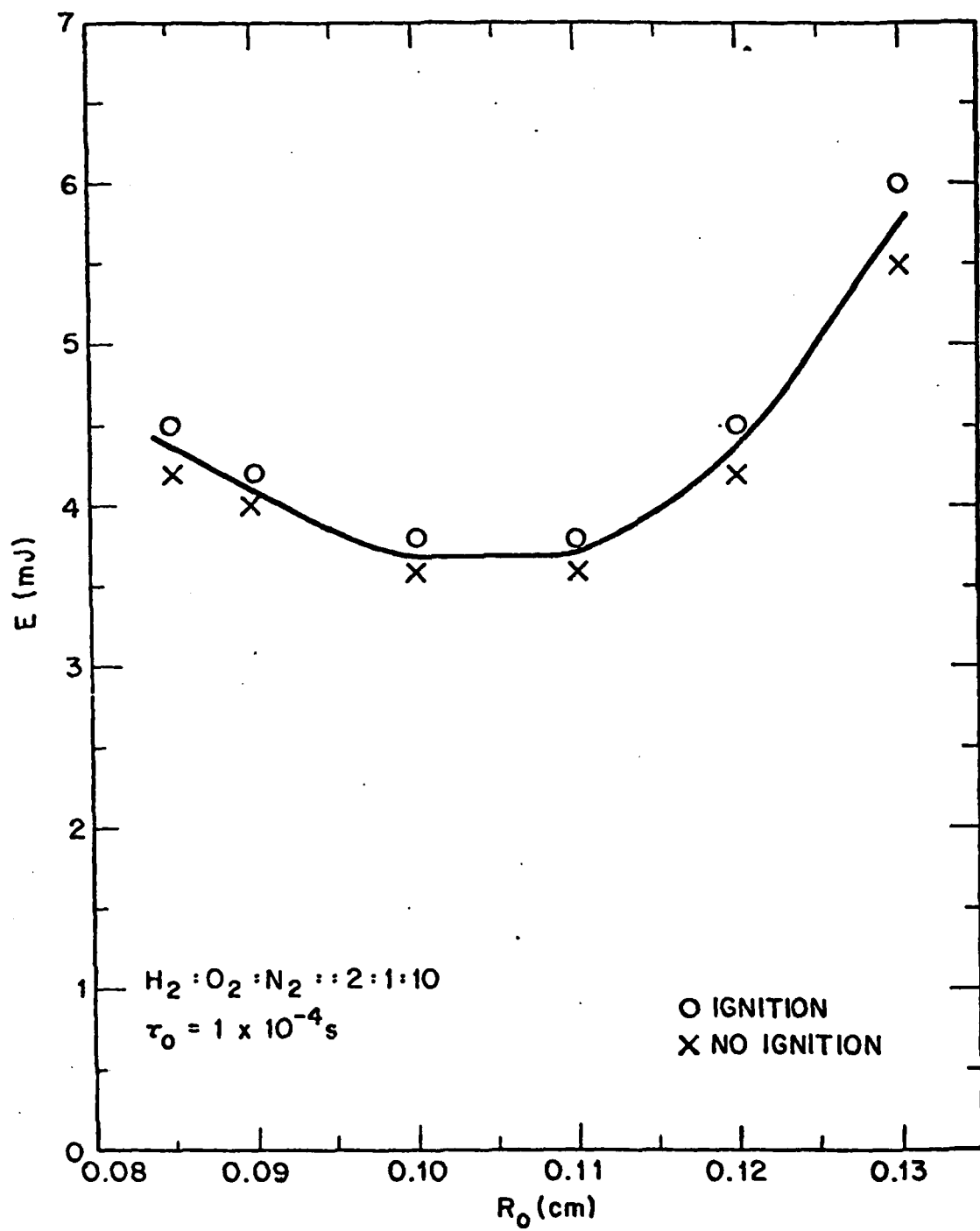


Figure 8

Appendix C
REVISED SUBROUTINES - INITAL AND RTCON

CIFER -- VERSION 06.03 DATE = 12/08/81 TIME = 10:24:52:97

..PRINT TEMP

```

*** MEMBER INITIAL      OLD DATA = 81.342    TIME = 10:20    CHECKSUM = 2F841888

14      SUBROUTINE INITIAL
15      C-----
16      C-----
17      C-----
18      C-----
19      C-----
20      C-----
21      C-----
22      C-----
23      C-----
24      C-----
25      C-----
26      C-----
27      C-----
28      C-----
29      C-----
30      C-----
31      C-----
32      C-----
33      C-----
34      C-----
35      C-----
36      C-----
37      C-----
38      C-----
39      C-----
40      C-----
41      C-----
42      C-----
43      C-----
44      C-----
45      C-----
46      C-----
47      C-----
48      C-----
49      C-----

```

INITIALIZE EVERYTHING IN SIGHT ***

THE ORDER OF INPUT ITEMS IS

1) PAUTLIST "SOLARP"

INPUT DATA WHICH DESCRIBE THE JACCHIA MODEL OF THE MAJOR NEUTRAL ATMOSPHERE

FRAP

F

RAY

KP

THOT

PAT

FOR

FCM2

FCO2

FWFO

2) PAUTLIST "CMTS"

INHS

MINHPS

HZ

ZBOT

ZTOP

DZN

ZPLT

DT

MCRTA

LAT

PCRAFA

MCNA

PCSTI

FFHX

FLUXF

JAXI

THE NUMBER OF ION SPECIE

THE NUMBER OF MINOR NEUTRAL SPECIE

THE NUMBER OF GRID POINTS IN ALTITUDE

THE BOTTOM OF THE MESH (LOWEST ALTITUDE IN KM)

THE TOP OF THE MESH (HIGHEST ALTITUDE IN KM)

THE SPACING BETWEEN THE TWO LOWEST GRID POINTS IN ALTITUDE

THE ALTITUDE AT WHICH TIME PLOTS ARE TO BE MADE (IN KM)

THE TIME STEP (IN SECONDS)

MAGNETIC DIP ANGLE (IN DEGREES)

THE (IN DEGREES) LATITUDE

THE STEP SIZE IN ALTITUDE FOR COMPUTATION

OF PRESSURE GRADIENTS (IN DEGREES) --

DEFAULT: 10.0

PHASE FACTOR FOR NEUTRAL WINDS

DEFAULT: 0.0

PRESSURE GRADIENT SCALE FACTOR --

DEFAULT: 1.0

ELECTRON HEATING EFFICIENCY SCALE FACTOR --

DEFAULT: 1.0

DAYTIME SOLAR FLUX SCALE FACTOR --

DEFAULT: 1.0

THE MAXIMUM NUMBER OF INTERVALS FOR THE

*** MEMORIAL INITIAL

OLD DATE = 81.342

TIME = 10:20 CHECKSUM = 2F001800

50* C

51* C

52* C

53* C

54* C

55* C

56* C

57* C

58* C

59* C

60* C

61* C

62* C

63* C

64* C

65* C

66* C

67* C

68* C

69* C

70* C

71* C

72* C

73* C

74* C

75* C

76* C

77* C

78* C

79* C

80* C

81* C

82* C

83* C

84* C

85* C

86* C

87* C

88* C

89* C

90* C

91* C

92* C

93* C

94* C

95* C

96* C

97* C

98* C

99* C

100* C

JAX"

3) PARELIST "CIRL"

PAXSTP

HPCAY

HPCAX

IAHNT

IDFF

ICHEM

TCHP

LIER

LATER

LPRIC

HSTART

LPCMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

LTPMP

4) ASYNPL AND RELATED DATA

THE DATA CARDS FOR IONS SHOULD PRECEDE THOSE FOR THE
 MAJOR NEUTRALS WHICH PRECEDE THOSE FOR THE LIVE (S)
 MAJOR NEUTRALS AND FINALLY THE ELECTRON. EACH CARD
 CONSISTS OF THE FOLLOWING FIELDS:

COLUMNS

1 - 6

7 - 14

A SIX CHARACTER SYMBOL IDENTIFYING THE
 SPECIE (LEFT JUSTIFIED)
 THE ATOMIC MASS OF THE SPECIE (P.1)

CIFER -- VERSION 06.03 DATE = 12/08/81 TIME = 10:20:52:97

*** MEMREF INITIAL OLD DATE = 81.342 TIME = 10:24 CHECKSUM = 2F0A188A

15 - 17 THE TYPE OF BOUNDARY CONDITION FOR THE CONTINUITY EQUATION TO USE AT THE HIGH ALTITUDE (133)

18 - 25 THE HIGH ALTITUDE AT WHICH THE BOUNDARY CONDITION IS APPLIED (F0.1)

26 - 33 FOR MINOR NEUTRALS, THE BOUNDARY VALUE (F0.1)

34 - 41 FOR MINOR NEUTRALS, A DIFFUSION COEFFICIENT (F0.1)

42 - 48 PLANY

49 A PLE CHARACTER SYMBOL TO USE ON PLOTS TO IDENTIFY THIS SPECIE (A1)

THE LAST CARD IN THIS SECTION GIVES THE ORDER IN WHICH THE CONTINUITY EQUATIONS ARE TO BE SOLVED WITH ALL THE IONS DONE BEFORE ANY MINOR NEUTRAL

5) INITIAL PROFILES

FOR EACH ALTITUDE AT WHICH INITIAL CONDITIONS ARE KNOWN THREE (3) CARDS ARE USED

THE FIRST CARD GIVES THE ALTITUDE (Z), THE TWO COMPONENTS OF THE NEUTRAL WINDS (UAV), AND THE VIBRATIONAL ENERGY OF H2 (EV3). (F0.1,7E0.1)

THE SECOND CARD GIVES THE ION DENSITIES (BX,7E0.1)

THE THIRD CARD GIVES THE MINOR NEUTRAL DENSITIES (PX,7E0.1)

6) OUTPUT CONTROL VARIABLES IN TWO NAMELISTS IN SUBROUTINE DSPLI

NAMELIST "PRINT"

LI A LOGICAL VARIABLE, .TRUE. IF THE HYDRODYNAMIC VARIABLES ARE TO BE PRINTED -- DEFAULT: .TRUE.

LV A LOGICAL VARIABLE, .TRUE. IF THE ION VELOCITIES ARE TO BE PRINTED -- DEFAULT: .FALSE.

LC A LOGICAL VARIABLE, .TRUE. IF THE CHEMISTRY VARIABLES ARE TO BE PRINTED -- DEFAULT: .TRUE.

LI A LOGICAL VARIABLE, .TRUE. IF THE IONIZATION RATES OF NEUTRALS ARE TO BE PRINTED -- DEFAULT: .FALSE.

LP A LOGICAL VARIABLE, .TRUE. IF SELECTED PRODUCTION/LOSS RATES ARE TO BE PRINTED -- DEFAULT: .FALSE.

PLT A LOGICAL VARIABLE, .TRUE. IF PLOTS OF TEMPERATURES VS ALTITUDE ARE TO BE MADE --

DATE = 12/08/81 TIME = 10120152197

CIFER -- VERSION 06.05

OLD DATE = 81.342 TIME = 10121 CHECKSUM = 2F801888

DEFAULTS .FALSE.
A LOGICAL VARIABLE, .TRUE. IF PLOTS OF
SELECTED DEPENDENCIES VS ALTITUDE ARE TO BE
MADE -- DEFAULT: .FALSE.
THE MINIMUM AND MAXIMUM ALTITUDE COVERED
IN THE PLOTS -- DEFAULT: 100.0, 5000.0
A LOGICAL VARIABLE, .TRUE. IF LOG-LPG
PLOTS ARE DESIRED
THE HOUR, DAY, AND INCREMENT IN ALTITUDE
INDEX AT WHICH TO PRODUCE PUNCHED OUTPUT
FOR USE AS INITIAL CONDITIONS
SELECTED HOURS OF THE DAY AT WHICH
PRINTED OUTPUT IS DESIRED
THE INCREMENT IN THE ALTITUDE INDEX FOR
PRINTED OUTPUT
THE NUMBER OF HOURS BETWEEN PRINTED OUTPUT
IS TO START
THE DAY THAT PRINTED OUTPUT IS TO START
A LOGICAL VARIABLE, .TRUE. IF PRINTED
OUTPUT IS TO BE GENERATED AFTER EVERY STEP
-- DEFAULT: .FALSE.

THE NEXT THREE ARE NOT CURRENTLY USED. THEY ARE ASSOCIATED
WITH MAKING PLOTS TO FILM WHICH HAS NOT BEEN IMPLEMENTED.

HPPLT
HPPLT
HPPLT

NAMELIST "RASTER"

OUTPUT VARIABLES FOR PLOTS TO FILM NOT CURRENTLY USED

PASXPL
PASXPR
PASXTL
PASXTR
PASYSB
PASYSI
XCORRL
XCORPR
XCORPT
SPC
WGT
HGT

7) CUMULATIVE REACTION RATES
THROUGH SUBROUTINE ACTP

*** MEMOIR INITIAL
152. C
153. C
154. C
155. C
156. C
157. C
158. C
159. C
160. C
161. C
162. C
163. C
164. C
165. C
166. C
167. C
168. C
169. C
170. C
171. C
172. C
173. C
174. C
175. C
176. C
177. C
178. C
179. C
180. C
181. C
182. C
183. C
184. C
185. C
186. C
187. C
188. C
189. C
190. C
191. C
192. C
193. C
194. C
195. C
196. C
197. C
198. C
199. C
200. C
201. C
202. C

*** MEMOIR INITIAL

OLD DATE = 01.342 TIME = 10:24 CHECKSUM = 2F8418B8

2034 C
2044 C
2054 C
2064 C
2074 C
2084 C
2094 C
2104 C
2114 C
2124 C
2134 C
2144 C
2154 C
2164 C
2174 C
2184 C
2194 C
2204 C
2214 C
2224 C
2234 C
2244 C
2254 C
2264 C
2274 C
2284 C
2294 C
2304 C
2314 C
2324 C
2334 C
2344 C
2354 C
2364 C
2374 C
2384 C
2394 C
2404 C
2414 C
2424 C
2434 C
2444 C
2454 C
2464 C
2474 C
2484 C
2494 C
2504 C
2514 C
2524 C
2534 C

SET "RTCON" FOR DESCRIPTION OF INPUT CARDS.

0) INITIALIZE DEPOSITION ROUTINES
THROUGH SUBROUTINE PEPHY

TABLELIST "TABLE"

VARIABLES USED TO MAKE A DEPOSITION TABLE, IF DESIRED.

LSPT THE UNIT NUMBER OF THE FILE CONTAINING OR
TO CONTAIN THE TABLE (SEE "MONTLU")
IDPT A TABLE IDENTIFIER -- DEFAULT: 0
DATE (DEFAULT GIVES NO TABLE SEE "MONTLU")
THE JACCHIA MODEL TO USE FOR COMPUTING THE
THE DEPOSITION TABLE
NDSMIN THE MINIMUM HOUR IN THE TABLE --
DEFAULT: 0.0
NDSMAX THE MAXIMUM HOUR IN THE TABLE --
DEFAULT: 24.0
THRS THE NUMBER OF TIME INTERVALS FOR THE TABLE
-- DEFAULT: 96
ALTMIN THE MINIMUM ALTITUDE IN THE TABLE --
DEFAULT: ZERO
ALTMAX THE MAXIMUM ALTITUDE IN THE TABLE --
DEFAULT: 2100
HALTS THE NUMBER OF ALTITUDE INTERVALS IN THE
TABLE -- DEFAULT: 12-1
OPT(2) THE TYPE OF GRID SPACING FOR THE TABLE
DEFAULT: 0, 1

THIS SECTION ALSO READS THE VARIOUS CROSS SECTIONS
FOR THE DAYTIME AND NIGHTTIME DEPOSITION

*** THE PROGRAM SIZE ***

THE PARAMETERS

NZ THE MAXIMUM NUMBER OF GRID POINTS

NACTIV THE MAXIMUM NUMBER OF ACTIVE SPECIES
(IONS PLUS "FREE NEUTRALS")

NATONS THE MAXIMUM NUMBER OF SPECIES
(NOT COUNTING ELECTRONS)

NE THE MAXIMUM NUMBER OF CHEMICAL REACTIONS

CITER -- VERSION 06.03 DATE = 12/00/81 TIME = 10120152197

*** MEMBER INITIAL OLD DATE = 81.302 TIME = 10120 CHECKSUM = 2F001008

2500 C (INCLUDING DEPOSITION)
 2550 C THE MAXIMUM NUMBER OF REACTIONS INVOLVING DEPOSITION
 2560 C
 2570 C
 2580 C THE MAXIMUM NUMBER OF REACTANTS PER REACTION
 2590 C
 2600 C

THE VARIABLES

2610 C THE ACTUAL NUMBER OF GRID POINTS USED
 2620 C
 2630 C
 2640 C THE ACTUAL NUMBER OF IONS
 2650 C
 2660 C IONSPI IONS + 1
 2670 C
 2680 C

2690 C THE ACTUAL NUMBER OF MINOR NEUTRAL SPECIES
 2700 C
 2710 C IONS + MINORS
 2720 C
 2730 C ICLUSK + 1
 2740 C
 2750 C

2760 C THE ACTUAL NUMBER OF MAJOR NEUTRAL SPECIES
 2770 C
 2780 C IPLUSK + MAJORS
 2790 C
 2800 C IATONS + 1
 2810 C
 2820 C

2830 C THE ACTUAL NUMBER OF CHEMICAL REACTIONS
 2840 C (INCLUDING DEPOSITION)
 2850 C
 2860 C THE ACTUAL NUMBER OF REACTIONS INVOLVING DEPOSITION
 2870 C
 2880 C THE ACTUAL MAXIMUM NUMBER OF REACTANTS PER REACTION
 2890 C
 2900 C

2910 C
 2920 C
 2930 C
 2940 C
 2950 C
 2960 C
 2970 C
 2980 C
 2990 C
 3000 C
 3010 C
 3020 C
 3030 C
 3040 C

PARAMETER MZ = 151
 PARAMETER MACTIV = 14
 PARAMETER MATONS = 20
 PARAMETER MATONS + 1
 PARAMETER MNR = 70
 PARAMETER MNR = 25
 PARAMETER MNR = 3

COMMENT / SIZE / IZ, IONS, IONSPI, MINORS, IPLUSK, IMAJORS,
 IATONS, ICLUSK, ICLUSK + 1, ICLUSK + 1, ICLUSK + 1, ICLUSK + 1

THE VARIABLES AND VARIOUS OTHER ASSOCIATED ITEMS ***

THE CIPHERITY VARIABLES:

ASYNPL A SIX CHARACTER SYMBOL TO IDENTIFY EACH SPECIES
 (INCLUDING ELECTRONS)

DATE = 12/08/81 TIME = 10:20:52:97

DATE = 12/08/81 TIME = 10:20:52:97

CIFER -- VERSION 06.03

OLD DATE = 01.342 TIME = 10:20:52:97

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CIFER -- VERSION 06.03

*** MEMBER INITIAL ***

305A C THE ATOMIC MASS OF EACH SPECIE

306A C THE ATOMIC SPECIES DENSITIES

307A C THE ELECTRON DENSITY AT THE OLD AND NEW TIME STEP

308A C THE MINIMUM VALUE THAT A DENSITY CAN HAVE

309A C AT A GRID POINT

310A C THE MINOR NEUTRALS, A BOUNDARY VALUE

311A C FOR THE MINOR NEUTRALS, A DIFFUSION COEFFICIENT

312A C FOR THE MINOR NEUTRALS, A DIFFUSION COEFFICIENT

313A C THE ORDER IN WHICH THE VARIOUS CONTINUITY EQUATIONS

314A C ARE SOLVED -- ALL ION EQUATIONS MUST BE SOLVED

315A C BEFORE ANY MINOR NEUTRAL EQUATION

316A C INTEGER ASYMOL(6, HATMP), LN(MACTIV), RORCEP(MACTIV)

317A C REAL**4 ASP (M2, HATONS), AN(PATONS), NE(M2, 2), DMRH(M2)

318A C REAL**4 UB(MACTIV), BV(MACTIV), AA(MACTIV)

319A C COMMON / CVAR / ASYPR, AM, ASP, ME, DMRH, LP, MR, BV, AA,

320A C PRCER

321A C THE HYDRODYNAMIC VARIABLES:

322A C T1 THE AMBIENT MAJOR NEUTRAL TEMPERATURE

323A C T2 THE ION TEMPERATURE AT THE OLD AND NEW TIME STEP

324A C T3 THE ELECTRON TEMPERATURE AT THE OLD AND NEW TIME STEP

325A C U1 THE MINOR ION VELOCITY IN THE X-DIRECTION

326A C V1 THE MINOR ION VELOCITY IN THE Y-DIRECTION

327A C EVID THE VIBRATIONAL ENERGY OF I2 -- NOT CURRENTLY USED

328A C PFCX THE PRESSURE GRADIENT IN THE X-DIRECTION

329A C PFCY THE PRESSURE GRADIENT IN THE Y-DIRECTION

330A C V1H ION NEUTRAL COLLISION FREQUENCY

331A C

332A C

333A C

334A C

335A C

336A C

337A C

338A C

339A C

340A C

341A C

342A C

343A C

344A C

345A C

346A C

347A C

348A C

349A C

350A C

351A C

352A C

353A C

354A C

355A C

DATE = 12/08/81 TIME = 10120152197

CIPER -- VERSION 06.03

*** MEMOFF INITIAL OLD DATE = 01.342 TIME = 10124 CHECKSUM = 2F041000

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356* C PTH VISCOSITY
357* C
358* C EYFFC EPOY DIFFUSION COEFFICIENT
359* C
360* C REAL*4 T1(NZ), T1(NZ,2), T1(NZ,2)
361* C REAL*4 U(NZ,2), V(NZ,2), EVIR(NZ)
362* C REAL*4 CPDX(NZ), CPDY(NZ), VIND(NZ), MEM(NZ),
363* C FDYDC(NZ)
364* C
365* C COMPOU / HVAR / TH, TL, TE, U, V, EVIR,
366* C OPDX, OPDY, VIN, VEM, FDYDC
367* C
368* C
369* C
370* C SOME POINTERS INTO THE ASP ARRAY
371* C
372* C PTH THE SECOND INDEX FOR ASP WHERE H BEGINS
373* C
374* C PTHF THE SECOND INDEX FOR ASP WHERE HE BEGINS
375* C
376* C PTH THE SECOND INDEX FOR ASP WHERE H BEGINS
377* C
378* C PTH2 THE SECOND INDEX FOR ASP WHERE H2 BEGINS
379* C
380* C PTH2 THE SECOND INDEX FOR ASP WHERE H2 BEGINS
381* C
382* C INTEGER PTH, PTHF, PTH, PTH2, PTH2
383* C
384* C COMPOU / ADPINT / PTH, PTHF, PTH, PTH2, PTH2
385* C
386* C
387* C THE GRID POINTS AND RELATED VALUES ***
388* C
389* C THE VARIABLES
390* C
391* C Z THE GRID POINTS --- ALTITUDE (IN KM)
392* C
393* C CPDZ INFORMATION ABOUT GRID SPACING
394* C
395* C PSC P*2, WHERE P IS THE RADIAL GEOCENTRIC DISTANCE
396* C
397* C RECSC RECIPROCAL OF PSC
398* C
399* C REAL*4 Z(NZ), CRKZ(NZ), PRSQ(NZ), RSD(NZ)
400* C
401* C COMPOU / HFSHA / Z, PWDZ, PRSQ, RSD
402* C
403* C THE SCALAR VARIABLES:
404* C
405* C PZM 07-1
406* C
407* C

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C-11

DATE = 12/08/81 TIME = 10:20:52:97

CIFER -- VERSION 06.03

*** MEMOFF INITIAL FILE DATE = 81.342 TIME = 10:24 CHECKSUM = 2F8018B8

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5094 C
5104 C
5114 C
5124 C*** PRINTERS FOR THE 04(20) REACTIONS
5134 C
5144 C THE REACTION WHOSE CHEMISTRY RATE COEFFICIENT IS 1
5154 C
5164 C THE NUMBER OF 04(20) REACTIONS
5174 C
5184 C IROP20(0) GIVES THE J-TH 0P20 REACTION
5194 C
5204 C IROP20(0) GIVES THE OTHER REACTANT (OTHER THAN 04(20) )
5214 C INVOLVED IN THE J-TH 0P20 REACTION
5224 C
5234 C
5244 C IYTCGP IROP20(MR), IROP20(MP)
5254 C
5264 C COMPM / 0P20R / LROP20, MROP20, IROP20, IROP20
5274 C
5284 C POINTPS FOR PRINTING ***
5294 C
5304 C ITP THE NUMBER OF PRODUCTION/LOSS TERMS TO PRINT
5314 C
5324 C ITP AN INTEGER ARRAY GIVING THE INDEX OF EACH
5334 C PRODUCTION/LOSS TERM TO PRINT
5344 C
5354 C
5364 C
5374 C IYTCGP ITP(MR)
5384 C
5394 C COMPM / CHEMP / MRP, IRP
5404 C
5414 C
5424 C*** SURFACE FOR THE DEPOSITION RATES ***
5434 C
5444 C THE VARIABLES:
5454 C
5464 C DEPRAT THE DEPOSITION RATES AT THE GRID POINTS
5474 C
5484 C SCI THE TOTAL ION PRODUCTION RATE
5494 C
5504 C SEC THE ELECTRON HEATING RATE
5514 C
5524 C
5534 C FFALAN DEPRAT(MZ,MFC)
5544 C FFALAN SCI(MZ), SEC(MZ)
5554 C
5564 C COMPM / DEPRM / DEPRAT, SCI, SEC
5574 C
5584 C*** PRINTERS TO VARIOUS TYPES OF DEPOSITION REACTIONS
5594 C

```

```

*** MEMREF INITIAL.
5600 C      PLC DATF = 81.302      TIME = 10120      CHECKSUM = 2FPA1888
5610 C      NFDI      THE NUMBER OF IONIZATION REACTIONS
5620 C      IFDC      THE NUMBER OF DISSOCIATION REACTIONS
5630 C      IFDI      THE NUMBER OF REACTIONS INVOLVING BOTH IONIZATION
5640 C      AND DISSOCIATION
5650 C      NFDUP      THE NUMBER OF REACTIONS INVOLVING DUPLICATES OF
5660 C      PREVIOUS PHOTO DEPOSITIONS
5670 C      NFNT      THE NUMBER OF REACTIONS INVOLVING NIGHT TIME
5680 C      OPPOSITIONS
5690 C      IFXPAY      THE NUMBER OF REACTIONS INVOLVED IN XRAY PRODUCTION
5700 C      OF IONS
5710 C      IFDI      AN INTEGER ARRAY GIVING THE INDEX IN THE ARRAY 'DEPRAT'
5720 C      FOR THE IONIZATION RATES
5730 C      IFDC      AN INTEGER ARRAY GIVING THE INDEX IN THE ARRAY 'DEPRAT'
5740 C      FOR THE DISSOCIATION RATES
5750 C      IFDI      AN INTEGER ARRAY GIVING THE INDICES FOR DISSOCIATION
5760 C      AND IONIZATION
5770 C      IFDC      AN INTEGER ARRAY GIVING THE INDICES FOR THE
5780 C      DUPLICATES
5790 C      IFNT      AN INTEGER ARRAY GIVING THE INDEX FOR NIGHT TIME
5800 C      OPPOSITION REACTIONS
5810 C      IFXPAY      AN INTEGER ARRAY GIVING THE INDICES FOR THE REACTIONS
5820 C      INVOLVED IN XRAY PRODUCTION OF IONS
5830 C
5840 C      INTEGER IFDI(MDR), IRDD(MDR), IRDI(MDR), IRDDUP(MDR)
5850 C      INTEGER IFNT(MDR), IPXRAY(MDR)
5860 C
5870 C      COMMON / SPDCP / HRFI, IRDD, IRDI, IRDDUP, NFNT, NRXPAY,
5880 C      IFDI, IFDC, IRDI, IPDD, IRDDUP, IFNT, IRXPAY
5890 C
5900 C      *** THE MAIN CONTROL PARAMETERS ***
5910 C
5920 C      MAXSTP      THE MAXIMUM NUMBER OF TIME STEPS TO COMPUTE
5930 C      IFMAX      THE MAXIMUM IONIC AND
5940 C      IFAY      WAY TO WHICH TO COMPUTE
5950 C
5960 C
5970 C
5980 C
5990 C
6000 C
6010 C
6020 C
6030 C
6040 C
6050 C
6060 C
6070 C
6080 C
6090 C
6100 C

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```

*** MEMBER INITIAL
611* C      ALP DATE = 81.302      TIME = 10120      CHECKSUM = 21841080
612* C      ISTEP      THE CURRENT STEP
613* C      IF      THE CURRENT HOUR
614* C      IFAY      THE CURRENT DAY
615* C      IPR      THE TIME STEP IN HOURS
616* C      IAT      THE YEAR FOR THE APPROPRIATE JACCHIA MODEL OF THE
617* C      AMBIENT NEUTRAL ATMOSPHERE
618* C      IAPPT      THE NUMBER OF TIME STEPS BETWEEN CALCULATIONS
619* C      OF THE AMBIENT NEUTRAL TEMPERATURE
620* C      AND THE MAJOR NEUTRAL DENSITIES
621* C      PGSC1      PRESSURE GRADIENT SCALE FACTOR
622* C      ICEP      THE NUMBER OF TIME STEPS BETWEEN CALCULATION OF
623* C      THE DEPOSITION RATES
624* C      ICHEN      A LOGICAL VARIABLE: .TRUE. IF CHEMISTRY IS DONE
625* C      .FALSE. IF CHEMISTRY IS NOT DONE
626* C      ITRN      A LOGICAL VARIABLE: .TRUE. IF TRANSPORT IS DONE
627* C      .FALSE. OTHERWISE
628* C      ITR      THE NUMBER OF ITERATIONS IT TOOK TO GET THE ION
629* C      EQUATIONS TO CONVERGE
630* C      CONVRG      A LOGICAL VARIABLE: .TRUE. IF THE IONS CONVERGED
631* C      .FALSE. IF THEY DID NOT
632* C      LOGICAL      ICHEN, ITRN, CONVRG
633* C      CONVMN / MCPL / MAXSTP, HRMAX, IDAY,
634* C      ISTEP, HR, IDAY,
635* C      DHR,
636* C      PAT, IAPBT, PGSC1,
637* C      IPEP, ICHEN,
638* C      TRIP, ITP, CONVRG
639* C
640* C
641* C
642* C
643* C
644* C
645* C
646* C
647* C
648* C
649* C
650* C
651* C
652* C
653* C*** THE OUTPUT CONTROL VARIABLES ***
654* C
655* C THE PLOTTING CONTROL VARIABLES:
656* C
657* C ICPLOT THE VALUE IF IDAY WHEN "PLOT" WAS LAST CALLED
658* C
659* C IITP
660* C
661* C IZPIT THE INDEX OF THE ALTITUDE AT WHICH 20-MICUP PLOTS

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```

*** MEMBER INITIAL
662* C
663* C
664* C
665* C
666* C
667* C
668* C
669* C
670* C
671* C
672* C
673* C
674* C
675* C
676* C
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696* C
697* C
698* C
699* C
700* C
701* C
702* C
703* C
704* C
705* C
706* C
707* C
708* C
709* C
710* C
711* C
712* C

APE TO RE PAGE
THE NUMBER OF SECONDS PER DAY
AN ARRAY OF SYMBOLS TO IDENTIFY A SPECIE ON THE
DENSITY PLOT
PSYMBL(NATMD1)
COMMON / PCTRL / INCLAY, INTP, SPDAY, HZPLT, PSYMBL

THE RESTART CONTROL VARIABLES:
LDRMP
LTDMP
LDUMP
TDUMP
INTECER DUMP, TDUMP
COMMON / DCTRL / LDRMP, LTDMP, DDUMP, TDUMP

CITEF DECLARATIONS ***
LOGICAL LPRIC, NSTART
INTEGER BLANK
REAL *4 MGRPA, KP
THIS COMMON BLOCK IS USED BY "DISPLAY" AND "RSTART"
COMMON / CPLY / UNT, FZ(121,5)
THIS COMMON BLOCK IS IN THE CITEF MACRO *SCF
COMMON / STOPT /
75(50), US(50), VS(50), EVS(50), ASPS(50, MATMNS)
THIS COMMON BLOCK IS USED BY "JACT1"
COMMON / INUT / FCO, FCI2, FCR2, EUVED
INITIALIZING FIXED CONSTANTS ***
DATA BLANK / ' ' /
DATA PIF / 3.141593 /, PM100 / 1.745320E-02 /
DATA SPDAY / 86400.0 /, SPMD / 3600.0 /

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CIPHER -- VERSION 66.03

DATE = 12/00/81

TIME = 10120152197

*** MEMREF INITIAL

CLP DATE = 81.342 TIME = 10120 CHECKSUM = 2F001008

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713* DATA CZERO / 980.665 /, RE / 6370.0 /
714* DATA DMAG / 0.25 /
715* DATA WITTS / 1.161490 /, ROLT / 1.38044E-16 /,
716* APV / 1.672521-20 /
717* C
718* DATAE LIST / LITS / INES, MINORS, IZ, ZBOT, ZTOP, DZO, ZPLOT,
719* DT, PGDHA, LAT, PCRAHA, KPHA, PGSC,
720* FCUX, FLUXF, JAXI, JAXN
721* C
722* DATA ZBOT / 70.0 /, ZTOP / 10000.0 /
723* DATA PCRAHA / 10. /
724* DATA KPHA / 0.0 /, PGSC / 1.0 /
725* DATA EFMX / 1.0 /, FLUXF / 1.0 /
726* DATA JAXI / 150 /, JAXN / 50 /
727* C
728* DATAE LIST / CTRL / MAXSTP, HRMAX, HDAY, IAHRT, IDEP, ICHEN,
729* TRHP, LINC, LOTCP, LPRIC, LSTART,
730* LDDHP, LTDHP, TDHP, OCUMP
731* C
732* DATA IAHRT / 2 /, IDEP / 2 /
733* DATA ICHEN / .TRUE. /, TRHP / .TRUE. /
734* DATA LINC / .TRUE. /
735* DATA LINC / 5 /, LOTCP / 6 /
736* DATA LSTART / .FALSE. /
737* C
738* DATAE LIST/SOLARP/EPAR, F, DAY, KP, TNOT, PAT,
739* FCO, FCR2, FCR2, FUVF
740* C
741* DATAE JAC65, JACT1
742* DATAE RYCRU
743* C
744* C*** INITIALISE ERROR ROUTINES ***
745* C
746* CALL CERRU
747* C
748* C*** INITIALISE ATMOSPHERIC ROUTINE ***
749* C
750* DATAE (5,SOLARP)
751* DATAE (6,SOLAPP)
752* IF (PAT .EQ. 1965) CALL IJAC65(EPAR, F, DAY, KP, TNOT, .TRUE.)
753* IF (PAT .EQ. 1971) CALL IJACT1(EPAR, F, DAY, KP, TNOT, .TRUE.)
754* C
755* C*** READ SOME CONTROL VARIABLES ***
756* C
757* DATAE (5,CTH)
758* DATAE (6,CTPL)
759* C
760* C*** READ SOME NUMERICAL AND PHYSICAL CONSTANTS ***
761* C
762* DATAE (5,CHIS)
763* DATAE (6,CHIS)

```


CIFER -- VERSION 06.03 DATE = 12/08/81 TIME = 10120152197

*** MEMBER INITIAL CLF DATE = M1,342 TIME = 10124 CHECKSUM = 2F841888

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764* MAJORS = 5
765* ICHSPI = IONS + 1
766* IFLUSH = IONS + ICHSPI
767* ICHSPI = IFLUSH + 1
768* MATOPS = IFLUSH + MAJORS
769* MATOPS = MATOPS + 1
770* C
771* C*** CHECK FOR UNDERDIMENSIONED ARRAYS ***
772* C
773* IF (MATOPS .GT. MATOPS) GO TO 1000
774* IF (M2 .GT. M2) GO TO 1010
775* C
776* C*** FLAG INFORMATION ABOUT THE ATOMIC VARIABLES ***
777* C
778* DO 3 J=1,MATOPS
779* DO 3 I=1,6
780* ASYHRL(I,J) = BLANK
781* C
782* DO 5 J=1,IFLUSH
783* READ(5,9) (ASYHRL(I,J),I=1,6), AN(J), LB(J),
784* UB(J), NV(J), AAC(J), PSYHRL(J)
785* C
786* CONTINUE
787* READ(5,12) (ASYHRL(I,J),I=1,6), AN(J), PSYHRL(J)
788* C
789* CONTINUE
790* READ(5,12) (ASYHRL(I,J),I=1,6), AN(J), PSYHRL(J)
791* READ(5,12) (ASYHRL(I,J),I=1,6), AN(J), PSYHRL(J)
792* READ(5,12) (ASYHRL(I,J),I=1,6), AN(J), PSYHRL(J)
793* READ(5,12) (ASYHRL(I,J),I=1,6), AN(J), PSYHRL(J)
794* READ(5,12) (ASYHRL(I,J),I=1,6), AN(J), PSYHRL(J)
795* C
796* C*** CHECK THE ORDER ARRAY ***
797* C
798* DO 30 J=1,IONS
799* IF (ORDER(J) .LT. 1) .OR. ORDER(J) .GT. IONS) GO TO 1100
800* IF (J .EQ. 1) GO TO 30
801* J1 = J - 1
802* DO 25 JJ=1,J1
803* IF (ORDER(J) .EQ. ORDER(JJ)) GO TO 1100
804* C
805* CONTINUE
806* DO 40 J=1,IONS,IFLUSH
807* IF (ORDER(J) .LT. ICHSPI) .OR. ORDER(J) .GT. IFLUSH)
808* GO TO 1100
809* J1 = J - 1
810* DO 35 JJ=1,ICHSPI,J1
811* IF (ORDER(J) .EQ. ORDER(JJ)) GO TO 1100
812* C
813* CONTINUE
814* C

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DATE = 12/08/81 TIME = 10120152197

CIFER -- VERSION 06.03

*** MEMBER INITIAL OLD DATE = 01.342 TIME = 10124 CHECKSUM = 2F001006

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0660      IS = L - 1
0670      IF (ZS(I) .GE. 7(I)) GO TO 200
0680      CONTINUE
0690      RAT = (Z(I) - ZS(LS))/ (ZS(LS+1) - ZS(LS))
0700      U(I,2) = US(LS) + RAT*(US(LS+1) - US(LS))
0710      V(I,2) = VS(LS) + RAT*(VS(LS+1) - VS(LS))
0720      W(I,1) = U(I,2)
0730      V(I,1) = V(I,2)
0740      FV(I,1) = EVS (LS)*(FVS (LS+1)/FVS (LS))*RAT
0750      D = 25 J=1, IPLUSM
0760      ASP(I,J) = ASPS(LS,J) * (ASPS(LS+1,J)/ASPS(LS,J))*RAT
0770      CONTINUE
0780      D = 25 J=1, IPLUSM
0790      ASP(I,J) = 0.0
0800      IF (I,2) = 0.0
0810      YI(I,2) = 0.0
0820      NI(I,2) = 0.0
0830      D = 25 J=1, IPLUSM
0840      IF (I,2) = NE(I,2) + ASP(I,J)
0850      YI(I,1) = TE(I,2)
0860      YI(I,1) = YI(I,2)
0870      NI(I,1) = NE(I,2)
0880      SPE(I) = 0.0
0890      SPI(I) = 0.0
0900      D = 30 J=1, IPLUSM
0910      FPRAT(I,J) = 0.0
0920      CONTINUE
0930      D(I,2) = 1.0E-05/PRDZ(I)
0940      PRINT 400, I, Z(I), DELIZ, IDYDC(I)
0950      FPRAT(SX,IS,IP12(10,3))
0960      CONTINUE
0970      INITIALIZE OUTPUT ROUTINE ***
0980      CALL PSCLI
0990      CALCULATE THE GEOMETRIC VARIABLES ***
1000      PIC = 23.5*SIH2*0.017*(DAY - 80.0)/365.0)
1010      CPER = COS(PH100*FC)
1020      STCR = SIN(PH100*FC)
1030      CLAT = COS(PH100*LAT)
1040      SLAT = SIN(PH100*LAT)
1050      CCR = 0.0*PIE/SPDAY*SIAT
1060      CIPA = PH100*GDDA
1070      SIPA = SIN(UTPA)
1080      CIPA = COS(UTPA)

```

DATE = 12/00/81 TIME = 10124152197

CIFLP -- VERSION 06.03

CHECKSUM = 2F8A1888

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*** MEMBER INITIAL
0170 C
0180 C
0190 C
0200 C*** INITIALISE CHEMISTRY ROUTINE ***
0210 C
0220 C
0230 C
0240 C
0250 C
0260 C
0270 C
0280 C
0290 C
0300 C
0310 C
0320 C
0330 C
0340 C
0350 C*** INITIALISE REPOSITION ROUTINE ***
0360 C
0370 C
0380 C
0390 C
0400 C
0410 C
0420 C*** INITIALISE PRESSURE GRADIENT ROUTINE ***
0430 C
0440 C
0450 C
0460 C*** INITIALISE TIME LOOP ***
0470 C
0480 C
0490 C
0500 C
0510 C
0520 C
0530 C
0540 C
0550 C
0560 C*** DECIDE ON A RESTART ***
0570 C
0580 C
0590 C
0600 C
0610 C
0620 C
0630 C
0640 C
0650 C
0660 C
0670 C

```

IF(.NOT. ICHM) GO TO 600

INITIALISE CHEMISTRY ROUTINE ***

IFRIC = 0

IF(LPRIC) IPRIC = 1

CALL IAPIC(0,0,0,IAPRIC)

CALL ARTIC(ITERM, ASYMP, 6, MATPFI, IPLUS, PAJPRS+1,

ICRATE, ICRT, IDRATE, IDRT, IU, IP, NPT, NR,

NR, NR)

IF = DET(1)

IF(ITERM - LT, 1) GO TO 500

IF(ITERM - LT, 1) OR. LAMP2F .GT. NR) GO TO 1200

IF(LPRIC) CALL RTCSFR

500

CALL VSAINF(0,0, 0,0F-03, NR+PAJPRS+1, 0,0, 0,0, -1,0E+03)

INITIALISE REPOSITION ROUTINE ***

CALL REINIT(FLOUT, CEMX, RE+ZTOP+1,0, RE+ZTOP-1,0, 1,0E-03,

JAXI, JAXI, LPRIC,

LINCR)

600 CONTINUE

INITIALISE PRESSURE GRADIENT ROUTINE ***

CALL PGPAUI(PGPAUA, KPHA)

INITIALISE TIME LOOP ***

IFAY = 1

ISTEP = 0

IF = 0

FIR = IT/STHR

ITR = 0

CONVPC = .THRE.

ITP = IFIX(SPDAY/(DT+120.0) + .0000000)

DECIDE ON A RESTART ***

IF(.NOT. IRESTART) RETURN

ITSAV = 0

CALL RESTART(LUPRD, LTRPD)

IF(CPS(ITSAV - IT)/IT .LT. 1.0E-04) GO TO 650

IF(IT - 0, ITSAV, IT

CONVPC = .THRE.

IF(IT - 0, ITSAV, IT

ITP = IFIX(SPDAY/(DT+120.0) + .0000000)

IT = ITSAV

FIR = IT/STHR

CIFER -- VERSION 26.03 DATE = 12/08/81 TIME = 10124152197

*** MEMBER INITIAL OLD DATE = 81.342 TIME = 10124 CHECKSUM = 2F8418B8

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0680      ISUP = IFIX(TIME/DT + .05)
0690      LPT = IFIX((IDAY*SDAY - TIME)/(DT*MAXO(1, 120 - NPT)))
0700      *      + .999999)
0710      LPTAY = IDAY
0720      C
0730      PRINT
0740      C
0750      C*** ERROR MESSAGES ***
0760      C
0770      IF NPT = 120 THEN
0780          PRINT 1001, MATOMS, NPT
0790          FORMAT(' INSUFFICIENT STORAGE FOR ATOMIC VARIABLES',
0800              ' YOU REQUESTED MATOMS = ',13,' WHEN MATOMS = ',13)
0810      STOP
0820      C
0830      IF NPT = 12
0840          PRINT 1011, N2, NPT
0850          FORMAT(' INSUFFICIENT STORAGE FOR PESH DEPENDENT VARIABLES',
0860              ' YOU REQUESTED N2 = ',13,' WHEN N2 = ',13)
0870      STOP
0880      C
0890      PRINT 1101, (RORDER(L), L=1, IFLUSH)
0900      FORMAT(' RORDER IS NOT AN ACCEPTABLE PERMUTATION',
0910          ' RORDER = ',2013)
0920      STOP
0930      C
0940      PRINT 1201
0950      FORMAT(5(/), ' RICHN WAS UNABLE TO FIND AN R+(2D) REACTION',
0960          ' WHOSE CHEMISTRY RATE WAS EQUAL TO 1')
0970      STOP
0980      C
0990      END

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*** MEMBER INITIAL COPIES -- 999 RECORDS, DATE = 81.342 TIME = 10124 CHECKSUM = 2F8418B8

CITER -- VERSION 07.03 DATE = 12/00/01 TIME = 10:20:52:97

*** REVERSE ORDER *** TIME = 01.302 CHECKSUM = 17278520

SIGNATURE SIGNATURE, SYM, MCF, MSY, FRN, LRN, INT

PLAN THE REACTION RATE CONSTANTS ASSOCIATED WITH THE CURRENT
REACTION BEING DECODED BY "ARTP"
ALL THE DEPOSITION REACTIONS MUST BE PLACED AT THE END OF THE
LIST OF REACTIONS

FOR EACH REACTION THE INPUT IS AS FOLLOWS

1) A CHARACTR CARD CONSISTING OF SEVERAL FOUR-CHARACTER SYMBOLS
INDICATING THE TYPE OF REACTION

A) THE FIRST SYMBOL IS 'CHEM' TO INDICATE REACTIONS
INVOLVING CHEMISTRY

B) THE SECOND SYMBOL IS 'DEPN' TO INDICATE REACTIONS
INVOLVING PHOTON DEPOSITION

C) FOR PHOTO-DEPOSITION REACTIONS THE THIRD SYMBOL IS
'I' FOR IONIZATION
'D' FOR DISSOCIATION
'IP' FOR IONIZATION AND DISSOCIATION
'DIP' FOR A COMBINATION OF THE PREVIOUS
REACTIONS

D) THE FOURTH SYMBOL IS 'M20' FOR REACTIONS
WITH $n \geq 20$ AS AN INTERMEDIATE PRODUCT

E) THE FIFTH SYMBOL IS 'INT' TO INDICATE THAT
THE DEPOSITION REACTION IS IMPORTANT AT
HIGH TIME

F) THE SIXTH SYMBOL IS 'XRAY' FOR THE TWO DEPOSITION
REACTIONS INVOLVED IN THE XRAY PRODUCTION
OF $n \geq 2$ AND $n \geq 4$

G) THE SEVENTH SYMBOL IS 'PRINT' IF THE PRODUCTION/LOSS
RATE CORRESPONDING TO THIS REACTION IS TO BE
PRINTED

2) FOR REACTIONS INVOLVING CHEMISTRY THE NEXT CARD CONTAINS
DATA ASSOCIATED WITH THE CHEMICAL REACTION

A) THE FIRST NUMBER IS AN INTEGER GIVING THE
APPROPRIATE REACTION LAW

B) THE NEXT THREE NUMBERS ARE THREE CONSTANTS TO
BE USED BY "CATER" TO COMPUTE THE

1A C
2A C
3A C
4A C
5A C
6A C
7A C
8A C
9A C
10A C
11A C
12A C
13A C
14A C
15A C
16A C
17A C
18A C
19A C
20A C
21A C
22A C
23A C
24A C
25A C
26A C
27A C
28A C
29A C
30A C
31A C
32A C
33A C
34A C
35A C
36A C
37A C
38A C
39A C
40A C
41A C
42A C
43A C
44A C
45A C
46A C
47A C
48A C
49A C
50A C
51A C

DATE = 12/00/01 TIME = 1012/152197

CITER -- VERSION 06.03

*** MEMBER RICHN OLD DATE = 01.302 TIME = 10120 CHECKSUM = 1F220528

APPROPRIATE REACTION RATE

57A C*** THE PROGRAM SIZE ***

58A C THE PARAMETERS

59A C N2 THE MAXIMUM NUMBER OF GRID POINTS

60A C IACTIV THE MAXIMUM NUMBER OF ACTIVE SPECIES
(IONS PLUS MINOR NEUTRALS)61A C IATONS THE MAXIMUM NUMBER OF SPECIES
(NOT COUNTING ELECTRONS)62A C IF THE MAXIMUM NUMBER OF CHEMICAL REACTIONS
(INCLUDING DEPOSITION)

63A C ICR THE MAXIMUM NUMBER OF REACTIONS INVOLVING DEPOSITION

64A C IR THE MAXIMUM NUMBER OF REACTANTS PER REACTION

THE VARIABLES:

65A C N2 THE ACTUAL NUMBER OF GRID POINTS USED

66A C IONS THE ACTUAL NUMBER OF IONS

67A C IONSP1 IONS + 1

68A C MINORS THE ACTUAL NUMBER OF MINOR NEUTRAL SPECIES

69A C IPLUS IONS + MINORS

70A C IPLUS1 IPLUS + 1

71A C IMAJORS THE ACTUAL NUMBER OF MAJOR NEUTRAL SPECIES

72A C IPLUS1 IPLUS + MAJORS

73A C IATONS1 IATONS + 1

74A C IR THE ACTUAL NUMBER OF CHEMICAL REACTIONS
(INCLUDING DEPOSITION)

75A C ICRP THE ACTUAL NUMBER OF REACTIONS INVOLVING DEPOSITION

76A C IR THE ACTUAL MAXIMUM NUMBER OF REACTANTS PER REACTION

102A C

*** WEPRLE PICON

OLF DATE = 01.302 TIME = 10:120 CHICKSUP = 11225528

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103*  PARAMETER P2 = 151
104*  PARAMETER PACTIV = 10
105*  PARAMETER PATONS = 20
106*  PARAMETER MATND1 = PATONS + 1
107*  PARAMETER PR = 70
108*  PARAMETER MDP = 25
109*  PARAMETER PH = 3
110*  C
111*  COMMON / SIZE / N2, IONS, IONSPI, NIBRS, IPIUS, IPIPI, MAJORS,
112*  PATONS, MATND1, PR, IOR, PR
113*  C
114*  C
115*  C*** AUXILIARY ARRAYS FOR THE COMPUTATION OF CHEMICAL RATES ***
116*  C
117*  C THE VARIABLELIST
118*  C
119*  C KCR1 THE NUMBER OF PRODUCTION TERMS IN EACH EQUATION
120*  C
121*  C ICRATF A ARRAY OF POINTERS TO THE PARTICULAR PRODUCTION
122*  C TERMS IN EACH EQUATION
123*  C
124*  C IPR1 THE NUMBER OF LOSS TERMS IN EACH EQUATION
125*  C
126*  C IPRATF A ARRAY OF POINTERS TO THE PARTICULAR LOSS
127*  C TERMS IN EACH EQUATION
128*  C
129*  C KPT(K) GIVES THE NUMBER OF REACTIONS WITH AT LEAST
130*  C K REACTANTS
131*  C
132*  C IF IPR(K,J) GIVES THE J-TH REACTANT
133*  C IN THE K-TH REACTION WITH AT LEAST J REACTANTS
134*  C
135*  C IF IPR(J,J) GIVES THE K-TH REACTION WITH AT LEAST
136*  C J+1 REACTANTS
137*  C
138*  C IFLAW A FLAG FOR EACH REACTION INDICATING WHICH
139*  C TEMPERATURE DEPENDENT REACTION RATE TO PURSUE
140*  C
141*  C FA,FO,FC THREE CONSTANTS TO BE USED IN THE APPROPRIATE
142*  C REACTION LAW
143*  C
144*  C IUTGER NCR1(MATND1), ICRATE(MATND1,MP),
145*  C NCR1(MATND1), ICRATE(MATND1,MP),
146*  C NCR1(MP), IPR(MP,PH), IPR(MP,PH), IFLAW(MP)
147*  C
148*  C COMMON / CHEM / NCR1, ICRATE, NCR1, IPRATE,
149*  C IPR, IPR, IPR, IPR, IPR, IPR
150*  C
151*  C
152*  C

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CIPR -- VERSION 06.03 DATE = 12/08/81 TIME = 1012/152197

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*** MEMBER PICON
154 C *** POSITIONS FOR THE 0+(2D) REACTIONS
155 C
156 C LROP2D THE REACTION WHOSE CHEMISTRY RATE COEFFICIENT IS 1
157 C
158 C NROP2D THE NUMBER OF 0+(2D) REACTIONS
159 C
160 C IROP2D(J) GIVES THE J-TH 0P2D REACTION
161 C
162 C IROP2D(J) GIVES THE OTHER REACTANT (OTHER THAN 0+(2D) )
163 C INVOLVED IN THE J-TH 0P2D REACTION
164 C
165 C
166 C IROP2D(MR), IROP2D(MR)
167 C
168 C CPMOIN / 0P2D / LROP2D, NROP2D, IROP2D, IROP2D
169 C
170 C *** POSITIONS FOR PRINTING ***
171 C
172 C IOP THE NUMBER OF PRODUCTION/LOSS TERMS TO PRINT
173 C
174 C IOP AN INTEGER ARRAY GIVING THE INDEX OF EACH
175 C PRODUCTION/LOSS TERM TO PRINT
176 C
177 C
178 C IOPCOP IOPCOP(MR)
179 C
180 C CPMOIN / CHEPPR / IOPCOP, IOP
181 C
182 C
183 C *** SURFACE FOR THE DEPOSITION RATES ***
184 C
185 C THE VARIABLES:
186 C
187 C DEPRAT THE DEPOSITION RATES AT THE GRID POINTS
188 C
189 C SCI THE TOTAL ION PRODUCTION RATE
190 C
191 C SCI THE ELECTRON HEATING RATE
192 C
193 C
194 C REATIN DEPRAT(M2,MRP)
195 C REATIN SCI(M2), SCI(M2)
196 C
197 C CPMOIN / DEPRAT / REPRAT, SCI, SCI
198 C
199 C *** POSITIONS TO VARIOUS TYPES OF DEPOSITION REACTIONS
200 C
201 C
202 C
203 C
204 C IOP THE NUMBER OF IONIZATION REACTIONS

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*** MEMREF RICON
2054 C      OLD DATE = 01.302      TIME = 10124      CHECKSUM = 11220528
2064 C      AOPD      THE NUMBER OF DISSOCIATION REACTIONS
2074 C      IOPD      THE NUMBER OF REACTIONS INVOLVING BOTH IONIZATION
2084 C      AND DISSOCIATION
2094 C      AOPDUP     THE NUMBER OF REACTIONS INVOLVING DUPLICATES OF
2104 C      PREVIOUS PHOTO DEPOSITIONS
2114 C      AENT      THE NUMBER OF REACTIONS INVOLVING NIGHT TIME
2124 C      DEPOSITIONS
2134 C      AXPAY      THE NUMBER OF REACTIONS INVOLVED IN XRAY PRODUCTION
2144 C      OF IONS
2154 C      IFDI      AN INTEGER ARRAY GIVING THE INDEX IN THE ARRAY 'DEPRAT'
2164 C      FOR THE IONIZATION RATES
2174 C      IFDP      AN INTEGER ARRAY GIVING THE INDEX IN THE ARRAY 'DEPRAT'
2184 C      FOR THE DISSOCIATION RATES
2194 C      IFDIP     AN INTEGER ARRAY GIVING THE INDICES FOR DISSOCIATION
2204 C      AND IONIZATION
2214 C      IFDUPUP    AN INTEGER ARRAY GIVING THE INDICES FOR THE
2224 C      DUPLICATES
2234 C      IFNT      AN INTEGER ARRAY GIVING THE INDEX FOR NIGHT TIME
2244 C      DEPOSITION REACTIONS
2254 C      IFXPAY     AN INTEGER ARRAY GIVING THE INDICES FOR THE REACTIONS
2264 C      INVOLVED IN XRAY PRODUCTION OF IONS
2274 C      IFDIPUR    IFDD(MDR), IFDID(MDR), IFDUP(MDR)
2284 C      IFDIFUR    IFDI(MDR), IFDIP(MDR), IFXPAY(MDR)
2294 C      COMMON / SPEED / IPFI, IOPD, IOPID, IOPDUP, IFNT, IXPAY,
2304 C      IPFI, IOPD, IOPID, IOPDUP, IFNT, IXPAY
2314 C      *
2324 C      *
2334 C      *
2344 C      *
2354 C      *
2364 C      *
2374 C      *
2384 C      *
2394 C      *
2404 C      *
2414 C      *
2424 C      *
2434 C      *
2444 C      *
2454 C      *
2464 C      *
2474 C      *
2484 C      *
2494 C      *
2504 C      *
2514 C      *
2524 C      *
2534 C      *
2544 C      *
2554 C      *

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DATE = 12/08/81 TIME = 10:20:52:97

CHECKSUM = 1F22R528

CIFER -- VERSION 06.03

*** MEMBER DICON ***

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2560 DATA DEPT / 'LIPD' // CHEMT / 'CHEM' /
2570 IONIZ / 'I' // IANCD / 'ID' //
2580 FISSC / 'I' // DUPLC / 'DUP' //
2590 CP2UT / 'CP2D' // HTRPT / 'HTR' //
2600 XRAYT / 'XRAY' //
2610 DATA PRINT / 'PRINT' /
2620 C
2630 C*** CHECK FOR FIRST CALL
2640 C
2650 IF (IPT .NE. 0) GO TO 50
2660 ICR = 0
2670 IFDI = 0
2680 ICRN = 0
2690 ICRD = 0
2700 ICRH = 0
2710 ICRY = 0
2720 ICRX = 0
2730 ICRP = 0
2740 ICRD = 0
2750 ICRP = 0
2760 ICRP = 0
2770 ICRP = 0
2780 ICRP = 0
2790 C
2800 C*** REAR THE CONTROL LINE FOR THE REACTION
2810 C
2820 50 REAR(5,110) (TEST(1),1=1,20)
2830 110 FORMAT(20A0)
2840 C
2850 C
2860 C*** IS THIS REACTION TO BE PRINTED ***
2870 C
2880 IF (TEST(7) .NE. PRINT) GO TO 120
2890 ICR = ICR + 1
2900 ICR(HPP) = IRT
2910 C
2920 C
2930 C*** DOES THIS REACTION INVOLVE CHEMISTRY
2940 C
2950 IF (TEST(1) .NE. CHEMT) GO TO 200
2960 C
2970 C*** A REACTION INVOLVING CHEMISTRY
2980 C
2990 ICR = ICR + 1
3000 C
3010 C*** REAR THE CHEMICAL REACTION RATE COEFFICIENTS
3020 C
3030 REAR(5,160) INAN(IPT), RA(IPT), CP(IPT), RC(IPT)
3040 FORMAT(100,310.2)
3050 C
3060 C

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*** MEMBER FROM OLD DATA = M1.342 TIME = 101241 CHECKSUM = 1F22R528

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3074 CAAA A REACTION INVOLVING CHEMISTRY (DEPOSITION ONLY)
3084 C
3094 C POC IF(LAM(IRT) = 0
3104 CA (IRT) = 1.0
3114 CP (IRT) = 0.0
3124 CC (IRT) = 0.0
3134 CFFOIVY = .TRUE.
3144 C
3154 CAAA WRITE OUT THE CHEMISTRY RATE COEFFICIENTS
3164 C
3174 C 250 IF(MOD(IRT,60) .EQ. 1) WRITE(6,260)
3184 C 260 FORMAT(10X, 'A', 9X, 'R', 9X, 'C', 10X,
3194 C 'REACTIONS -----> RESULTS')
3204 C WRITE(6,30) IRT, IFLAM(IRT), PA(IRT), MD(IRT), RC(IRT),
3214 C (REACT(J),J=1,60)
3224 C 300 FORMAT(1X,13,3X,13,1X,3E10.2,2X,60A1)
3234 C
3244 CAAA PUES THE REACTION INVOLVE DEPOSITION
3254 C
3264 C IF(TEST(2) .EQ. DEPT) GO TO 400
3274 C IF(CPMHLY) GO TO 2000
3284 C IF(REFM) GO TO 3000
3294 C RETURN
3304 C
3314 CAAA A REACTION INVOLVING DEPOSITION
3324 C
3334 C 400 ICR = ICR + 1
3344 C IF(ICR .GT. MDR) GO TO 5000
3354 C
3364 CAAA FIND OUT WHAT KIND OF REACTION IT IS
3374 C
3384 C IF(TEST(3) .EQ. IQU12) GO TO 410
3394 C IF(TEST(3) .EQ. IAHED) GO TO 430
3404 C IF(TEST(3) .EQ. DISC) GO TO 420
3414 C IF(TEST(3) .EQ. DUPLC) GO TO 440
3424 C
3434 CAAA BE LEACH HERE IF THERE IS AN ERROR
3444 C GO TO 1000
3454 C
3464 C
3474 CAAA INITIALIZATION
3484 C
3494 C 410 ICR = ICR + 1
3504 C IF(I(MPR)) = MPR
3514 C GO TO 500
3524 C
3534 CAAA DISSOCIATION
3544 C
3554 C 420 ICR = ICR + 1
3564 C IF(I(MPR)) = MPR
3574 C GO TO 500

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*** MEMBER CLEAN *** CLC DATE = 81.342 TIME = 10120 CHECKSUM = 1F22052A

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3500 C
3590 C*** IONIZATION AND DISSOCIATION
3600 C
3610 C  M3C  M3C = M3C + 1
3620 C  IF(M3C(M3C)) = M3C
3630 C  GO TO 500
3640 C
3650 C*** DUPLICATE
3660 C
3670 C  M4C  M4C = M4C + 1
3680 C  IF(M4C(M4C)) = M4C
3690 C  GO TO 500
3700 C
3710 C  M5C  M5C = M5C + 1
3720 C  IF(M5C(M5C)) = M5C
3730 C
3740 C*** LOCATE SMPT SPECIAL DEPOSITION REACTIONS
3750 C
3760 C
3770 C*** CHECK FOR M20 REACTIONS
3780 C
3790 C
3800 C
3810 C
3820 C
3830 C
3840 C
3850 C
3860 C
3870 C
3880 C
3890 C
3900 C*** FIND THE REACTIONS INVOLVED IN THE NIGHTTIME DEPOSITION
3910 C
3920 C
3930 C
3940 C
3950 C
3960 C
3970 C*** CHECK FOR XRAY PRODUCTION
3980 C
3990 C
4000 C
4010 C
4020 C
4030 C
4040 C
4050 C
4060 C
4070 C
4080 C

```

IT IS ASSUMED THAT THERE IS ONLY ONE SPECIE REACTING WITH
M20 IN THE CURRENT REACTION AND THAT REACTANT IS THE
SECOND ONE NAMED IN THE REACTION (THE FIRST BEING O)

IF (TEST(4) .NE. M20) GO TO 720
M20 = M20 + 1
IF(M20(M20)) = M20
IF(M20(M20)) = M20
IF (M20(M20)) .EQ. 0 .AND. M20(M20) .EQ. 1.0) LROP20 = M20
CONTINUE

FIND THE REACTIONS INVOLVED IN THE NIGHTTIME DEPOSITION

IF (TEST(5) .NE. M20) GO TO 740
M20 = M20 + 1
IF(M20(M20)) = M20
CONTINUE

CHECK FOR XRAY PRODUCTION

IF (TEST(6) .NE. M20) GO TO 760
M20 = M20 + 1
IF(M20(M20)) = M20
CONTINUE

ENDIF

ENDIF

CIPHER -- VERSION 06.03

DATE = 12/08/81

TIME = 10124152197

*** MEMBER PTCOM

PLC DATE = 01.342 TIME = 10124 CHECKSUM = 1F228528

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0090 C
0100 C
0110 C PRINT SOME ITEMS OF INTEREST THAT DID NOT GET PRINTED BY "ARIP"
0120 C
0130 C
0140 C
0150 C IF (LPROP2D .LT. 1) GO TO 990
0160 C WRITE(6, 910) LPROP2D
0170 C FORMAT(5(/), 1 LPROP2D = 1,15)
0180 C
0190 C WRITE(6, 920)
0200 C FORMAT(//, 1 REACTIONS WITH 0+(2D) AS AN INTERMEDIATE',
0210 C 1 PRODUCT-REACTANT', //
0220 C 1 NON-(R) REACTANT(//)
0230 C
0240 C IF (LPROP2D .EQ. 1) LPROP2D = 1
0250 C WRITE(6, 930) LPROP2D(1), LPROP2D(1)
0260 C FORMAT(216)
0270 C CONTINUE
0280 C
0290 C CONTINUE
0300 C RETURN
0310 C *** ERROR MESSAGES
0320 C
0330 C PRINT 1001, IRT, NDF
0340 C FORMAT(5(/), 1 REACTION #,13,1, DEPOSITION REACTION #,13,
0350 C 1 WAS NOT GIVEN A TYPE (3RD SYMBOL ON CONTROL',
0360 C 1 CARD))
0370 C STOP
0380 C
0390 C PRINT 2001, IRT
0400 C FORMAT(5(/), 1 REACTION #,13,1 WAS NOT IDENTIFIED AS EITHER',
0410 C 1 CHEMISTRY OR DEPOSITION))
0420 C STOP
0430 C
0440 C PRINT 3001, IRT
0450 C FORMAT(5(/), 1 REACTION #,13,1 WAS IDENTIFIED AS CHEMISTRY',
0460 C 1 ONLY WHEN A PREVIOUS DEPOSITION REACTION WAS',
0470 C 1 ENCOUNTERED',
0480 C 1 ALL PHOTO REACTIONS MUST BE AT THE END OF THE',
0490 C 1 REACTION LIST))
0500 C STOP
0510 C
0520 C PRINT 4001, IRT
0530 C FORMAT(5(/), 1 REACTION #,13,1 WAS LABELED A DUPLICATE',
0540 C 1 PHOTO REACTION WHEN NO PREVIOUS PHOTO REACTION',
0550 C 1 HAD BEEN ENCOUNTERED))
0560 C STOP
0570 C
0580 C PRINT 5001, IRT, NDF
0590 C

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*** MEMREF NICON          OLD DATE = 81.1362    TIME = 10124   CHECKSUM = 1F2A520
                                S701      INSUFFICIENT STORAGE FOR THE DEPOSITION ROUTINE./
                                q60#     , YOU REQUESTED NOR = ',13,' WHEN NOR = ',13)
                                q61#           STOP
                                q62# C
                                q63# C
                                q64#     FID
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*** NEPHER BYCON 464 RECORDS, DATE = 81.342 TINI. = 10124 CHECKSUM = 1f22520

**DA
FILM**