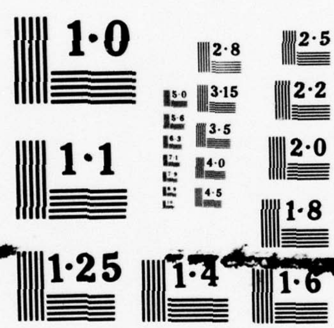
AD-A055 379 NAVAL POSTGRADUATE SCHOOL MONTEREY CALIF F/G 13/1
STATE VARIABLE ANALYSIS OF A BOILER SYSTEM.(U)
MAR 78 C SENANIKROM

UNCLASSIFIED NL

1 OF 2
ADA
055379



NATIONAL BUREAU OF STANDARDS
MICROCOPY RESOLUTION TEST CHART

NAVAL POSTGRADUATE SCHOOL

Monterey, California

THESIS

State Variable Analysis of a Boiler System

by

Chusakdi Senanikrom

March 1978

Thesis Advisor: T. M. Houlihan

Approved for public release; distribution unlimited.

SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

REPORT DOCUMENTATION PAGE		READ INSTRUCTIONS BEFORE COMPLETING FORM
1. REPORT NUMBER	2. GOVT ACCESSION NO.	3. RECIPIENT'S CATALOG NUMBER
4. TITLE (and Subtitle) State Variable Analysis of a Boiler System.		5. TYPE OF REPORT & PERIOD COVERED Master's Thesis; March 1978
		6. PERFORMING ORG. REPORT NUMBER
7. AUTHOR(s) Chusakdi Senanikrom		8. CONTRACT OR GRANT NUMBER(s)
9. PERFORMING ORGANIZATION NAME AND ADDRESS Naval Postgraduate School Monterey, California 93940		10. PROGRAM ELEMENT, PROJECT, TASK AREA & WORK UNIT NUMBERS
11. CONTROLLING OFFICE NAME AND ADDRESS Naval Postgraduate School Monterey, California 93940		12. REPORT DATE March 1978
		13. NUMBER OF PAGES 106
14. MONITORING AGENCY NAME & ADDRESS (if different from Controlling Office) Naval Postgraduate School Monterey, California 93940		15. SECURITY CLASS. (of this report) UNCLASSIFIED
		15a. DECLASSIFICATION/DOWNGRADING SCHEDULE

16. DISTRIBUTION STATEMENT (of this Report)

Approved for public release; distribution unlimited.

17. DISTRIBUTION STATEMENT (of the abstract entered in Block 20, if different from Report)

18. SUPPLEMENTARY NOTES

19. KEY WORDS (Continue on reverse side if necessary and identify by block number)

20. ABSTRACT (Continue on reverse side if necessary and identify by block number)

The state variable formulation of a Foster Wheller ESD-III boiler is developed from fundamental principles. The response of the model for various input signals is determined using CSMP-III, the IBM simulation

DD FORM 1473, 1 JAN 73 EDITION OF 1 NOV 65 IS OBSOLETE
(Page 1) S/N 0102-014-6601

SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

CONT

language. The sensitivity of the model to various coefficient values is noted as are the characteristics of various system states for small perturbation values.

ABSTRACT

ACCESSION for		
NTIS	White Section	☒
DDC	Buff Section	☐
UNANNOUNCED		☐
JUSTIFICATION		
BY		
DISTRIBUTION/AVAILABILITY CODES		
Dist.	AVAIL. and/or SPECIAL	
A		

DD Form 1473
1 Jan 73
S/N 0102-014-6601

STATE VARIABLE ANALYSIS OF A BOILER SYSTEM

by

Chusakdi Senanikrom
Lieutenant, Royal Thai Navy
B.S., Royal Thai Naval Academy, 1967

Submitted in partial fulfillment of the
requirements for the degree of

MASTER OF SCIENCE IN MECHANICAL ENGINEERING

from the

NAVAL POSTGRADUATE SCHOOL

March 1978

Author: Chusakdi Senanikrom.

Approved by: Thomas Houlihan, Thesis Advisor

_______________ Second Reader

Allen E Fuhs, Chairman, Department of Mechanical Engineering

George J. Haltiner, Dean of Science and Engineering

ABSTRACT

The state variable formulation of a Foster Wheeler ESD-III boiler is developed from fundamental principles. The response of the model for various input signals is determined using CSMP -III, the IBM simulation language. The sensitivity of the model to various coefficient values is noted as are the characteristics of various system states for small perturbation values.

TABLE OF CONTENTS

LIST OF FIGURES

NOMENCLATURE

A_s, A_r, A_D = superheater, riser and downcomer cross-sectional areas respectively (ft^2)

C = evaporation level proportionality constant (ft-sec/lb)

c_s, c_r, c_D = heat capacitance for superheater, riser and downcomer tubes respectively (BTU/lb-°R)

C_g = average heat capacitance of combustion gases times air-fuel ratio (BTU/lb-°R)

c_i = heat capacitance for feedwater(BTU/lb-°R)

c_{ps} = average heat capacitance of superheated steam (BTU/lb-°R)

f_s, f_r, f_D = friction coefficients for superheater, riser and downcomer tubes, respectively (sec^2/ft^5)

g = acceleration due to gravity (ft/sec^2)

h_B = enthalpy of saturated vapour corresponding to P_B (BTU/lb)

h_{wB} = enthalpy of saturated liquid corresponding to P_B (BTU/lb)

h_{wD} = enthalpy of liquid in mud-drum (BTU/lb)

h_w = enthalpy of drum and downcomer liquid (BTU/lb)

h_{fg} = enthalpy of evaporation corresponding to P_B (BTU/lb)

K_{as} = air cooling coefficient at superheater bank (BTU/sec)

K_{ar} = air cooling coefficient at riser bank (BTU/sec)

K_{gs}, K_s = heat-transfer coefficients from combustion gas to superheater tubes, and from superheater tubes to steam, respectively (BTU/lb-°R)

K_{gB}, K_r, K_g = heat-transfer coefficients from combustion gas to riser tubes and from riser tubes to boiling liquid respectively (BTU/lb-°R), (BTU/lb-°R^4), (BTU/lb-°R)

K_e = evaporation rate constant of drum liquid (lb/sec-°R)

K_T, K_B = constants for state equations of saturated steam (°R-ft^2/lb), (ft^{-1})

L_S, L_V, L_D = superheater, riser and downcomer tube lengths respectively (ft)

M = mass of drum liquid (lb)

M_S = mass of superheater tubes (lb)

M_B = mass of riser tubes (lb)

P_B = drum pressure (lb/ft^2)

P_S = superheater outlet pressure (lb/ft^2)

P_W = mud-drum pressure (lb/ft^2)

Q_S = heat-input rate from tube walls into the superheated steam (BTU/sec)

Q_{gS} = heat-input rate from hot gasses into superheater tube walls (BTU/sec)

Q_B = heat-input rate from riser tube walls into boiling liquid (BTU/sec)

Q_{gB} = heat-input rate from hot gasses into riser tube walls (BTU/sec)

T_i = feedwater temperature (°R)

T_B = saturation temperature corresponding to P_B (°R)

T_S = superheater outlet temperature (°R)

T_W = drum and downcomer liquid temperature (°R)

T_{SW} = superheater tube-wall temperature (°R)

T_{BW} = riser tube-wall temperature (°R)

T_{gS} = average gas temperature at superheater banks (°R)

T_{gB} = average gas temperature at riser banks (°R)

T_c = combustion gas temperature entering superheater banks (°R)

V_B = volume of vapor phase in drum (ft^3)

V_r = velocity of riser mixture (ft/sec)

V_w = velocity of downcomer water (ft/sec)

V = total drum volume (ft^3)

W_s = steam mass-flow rate at the superheater outlet (lb/sec)

W_f = fuel mass-flow rate (lb/sec)

W_i = feedwater mass-flow rate (lb/sec)

W_w = downcomer mass-flow rate (lb/sec)

W = riser mass-flow rate (lb/sec)

W_a = air mass-flow rate from blower (lb/sec)

W_{ac} = chemically correct +50% excess air rate (lb/sec)

W_e = mass-evaporation rate from drum liquid surface (lb/sec)

W_B = steam mass-flow rate from drum into superheater (lb/sec)

X = quality of mixture leaving riser

X_v = throttle opening (%)

y = drum liquid level (ft)

ρ_B = saturated vapor density corresponding to P_B (lb/ft^3)

ρ_S = superheater outlet density (lb/ft^3)

ρ_w = saturated liquid density corresponding to P_B (lb/ft^3)

ρ = density of liquid vapor mixture leaving riser (lb/ft^3)

η = evaporation level (ft)

I. INTRODUCTION

Boilers as understood by marine engineers are closed vessels containing water which by the application of heat is converted into steam at any designed pressure. This steam is then used for the production, through machinery, of useful work. A dynamic model of steam turbine machinery consists of a boiler model and a turbine model. The difficult part is the boiler, as a load change causes variations in some important properties such as boiler pressure, temperature and drum water level. The analysis in this paper will use Chien's dynamic analysis (1) of a boiler as a reference. Chien considered a naval boiler which for purposes of analysis was divided into four sections namely a superheater, a downcomer-riser loop, a drum and a gas path.

The principles of thermodynamics, heat-transfer and fluid mechanics were used to describe the dynamic behaviour corresponding to each section of the boiler and these were derived from equations of continuity, energy, heat-transfer, and momentum. The equations involve partial differentials as well as nonlinear terms. These equations were reduced to the ordinary linear equation form by applying small perturbation and difference equation techniques. Linear equations thus obtained were reduced to ten state variable equations and solved by digital computer techniques.

Since there is an increasing interest in boiler modelling, the objective of this thesis was to develop a comprehensive boiler simulation model in a form useful for modern control (i.e., multivariable control) analysis.

II. BOILER MODEL

A. BOILER CONSIDERATIONS

The control problems of high pressure boilers have become more and more critical, both from the operational and the economical points of view. A dynamic analysis is the method to be used for a control-system analysis. It consists of a complete understanding of the process to be controlled and the effects of physical and chemical changes. The analysis is not exact by any means but the results obtained should be in good qualitative agreement with actual tests. The major difficulty in boiler analysis is the fact that the whole system is very complex and contains numerous variables.

Chien(1) considered a naval boiler which for purposes of analysis was divided into four distinct sections namely a superheater, a downcomer-riser loop, a drum and a gas path. The detail of analysis is described in Part B of this section. The basic equations used in the analysis are those of continuity,energy(heat-transfer),momentum and the state equations. These equations involve partial differentiation as well as nonlinearities. Generally,the equations have the form

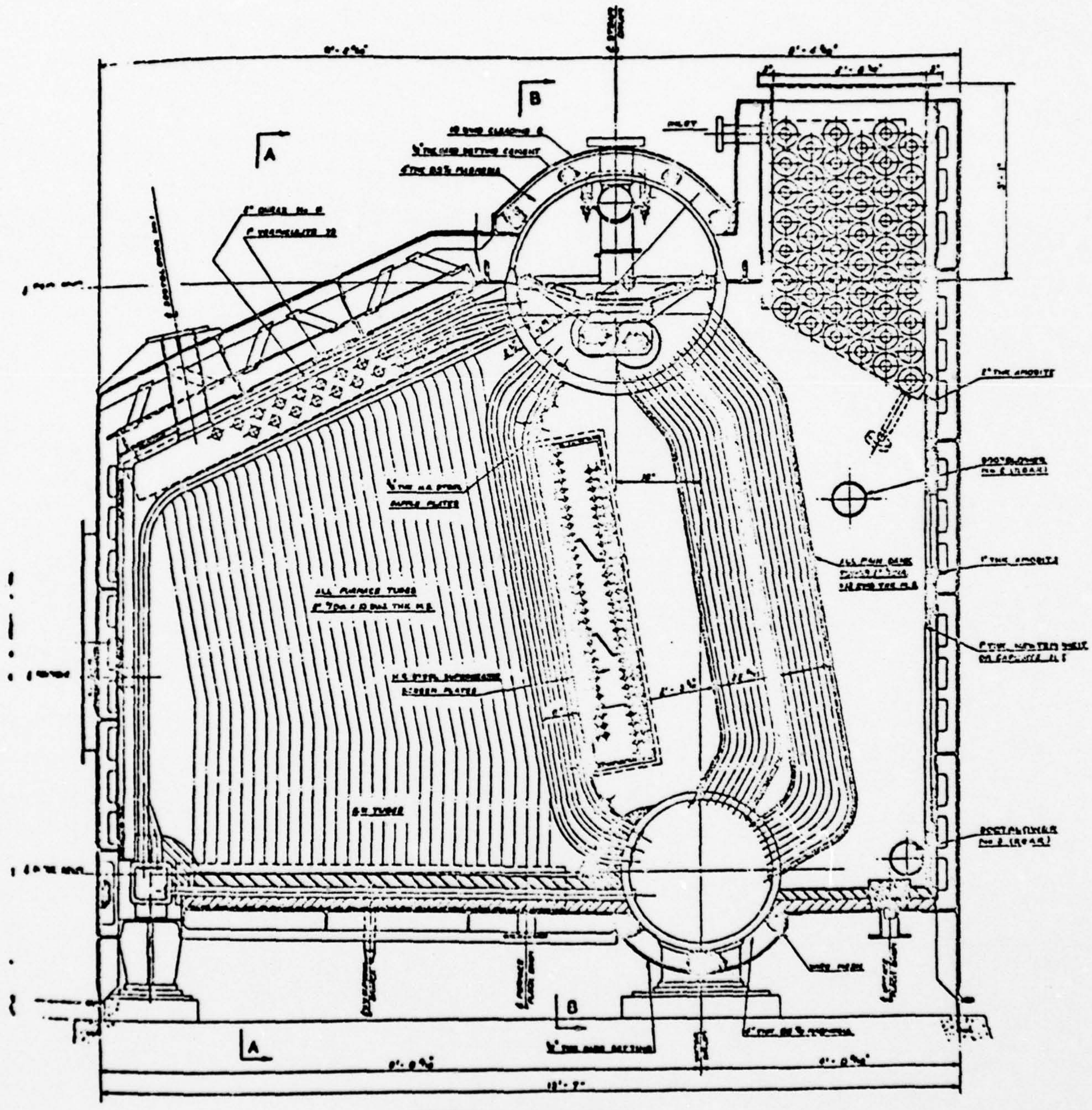
$$f(x, y, z, \cdots) = 0$$

To eliminate the nonlinearities one uses perturbation theory, which effectively approximates the response of the system to small signal changes about a chosen operating condition. Thus, the equation is perturbed about its steady state operating condition to give the linearized form.

Hence it can be written as

$$\frac{\partial f}{\partial x}\Delta x + \frac{\partial f}{\partial y}\Delta y + \frac{\partial f}{\partial z}\Delta z + \ldots = 0$$

The perturbed variables are ΔX, ΔY, ΔZ, etc. and the partial differentials ($\frac{\partial f}{\partial x}$, $\frac{\partial f}{\partial y}$, $\frac{\partial f}{\partial z}$, etc.) that form the coefficients of the perturbed variables are evaluated at steady state operating conditions. This technique was also followed by Whalley (2) in modeling the same boiler plant.



SECTIONAL ELEVATION

Figure 1 - A CROSS SECTIONAL ARRANGEMENT OF THE FOSTER WHEELER D-TYPE MARINE BOILER

B. BOILER ANALYSIS

The boiler studied in this analysis is a Foster Wheeler D-type marine boiler; which is an oil fired, two-drum, natural circulation unit having a rated output of 28,800 lbs/hour at 350 lbs/in^2 gauge, 1200°F. A cross sectional arrangement of the unit is shown in Figure 1. The following assumptions apply to the physical simplifications in each of four sections.

1. Superheater

(a) The inertial effects of superheated steam are neglected.

(b) The superheater tubes are assumed to be a single capacitance with restriction on the drum side and another restriction on the load side.

(c) Desuperheaters are not considered.

2. Downcomer riser loop

(a) Only natural circulation exists.

(b) No boiling takes place in the downcomers.

(c) Vapor and liquid velocities in the riser are identical.

(d) Heat-transfer rates to the boiling liquid from the tube walls are proportional to the cube of temperature difference between the wall and the liquid.

(e) Steam quality is uniform in the riser.

(f) Liquid temperature is always the same as the saturation temperature corresponding to drum pressure.

(g) Downcomer liquid temperature is the same as the drum liquid temperature.

3. Drum

(a) There is no temperature gradient across the drum vapor phase, and the temperature is always the saturation temperature corresponding to drum pressure.

(b) The liquid phase has no temperature gradient other than across a very thin boundary layer at the drum surface.

(c) Evaporation or condensation rate in the drum is proportional to the difference of liquid and saturation temperatures.

(d) Feedwater temperature is assumed to be constant.

(e) Liquid-level changes due to bubble formation in the drum are neglected.

4. Gas Path

(a) The air-fuel ratio is assumed to be constant.

(b) Temperature of combustion gas entering superheater is proportional to the firing rate.

(c) Waterwalls are lumped with the riser-banks.

(d) The heat-transfer rate at each tube bank is determined by the tube wall temperature and the average gas temperature.

(e) Inertia of the hot gases is neglected, that is, velocity changes take place instantaneously.

(f) Delays due to the heat capacitance of the hot gases are neglected, that is, temperature changes take place instantaneously in combustion gases.

(g) All heat transfer is due to turbulent convection and radiation.

The following steps are taken in developing the equations for each of the four sections. A simple schematic diagram of each sub-section is included at the beginning of each part of the analysis. A brief statement of the physical situation is included under the headings. The dummy coefficients such as a_1, b_1, C_{11}, D_{11}, were used for convenience, and their values are declared in the Appendices. The quantities such as $\bar{W}_B$, $\bar{h}_S$, $\bar{h}_B$, etc. are the steady state values of W_B, h_S, h_B, respectively. These values can be evaluated from the original unperturbed nonlinear equations by setting all derivative terms to zero and solving for the unknown values in term of known values.

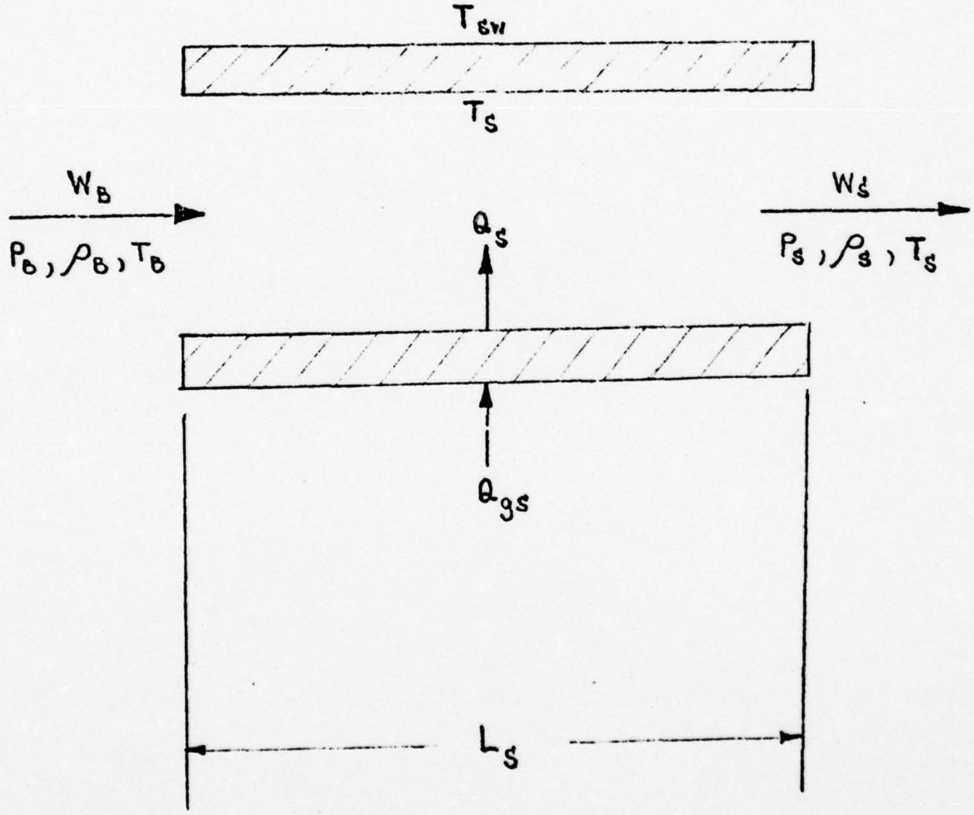


Figure 2 - SCHEMATIC DIAGRAM OF SUPERHEATER

5. <u>Superheater continuity</u>

Mass flow in - Mass flow out = Rate of change of enclosed mass

$$W_B - W_S = \frac{d}{dt}(L_S A_S \rho_S)$$

The perturbed equation is :

$$\Delta W_B - \Delta W_S = L_S A_S S \Delta\rho_S$$

or,

$$a_1 \Delta W_B + a_2 \Delta W_S = a_3 S \Delta\rho_S \qquad (1)$$

where S is the Laplace variable denoting differentiation with respect to time

6. <u>Superheater energy balance</u>

Heat input from tube wall + Heat in incoming steam - Heat with outgoing steam = Rate of change of internal energy

$$Q_S + W_B h_B - W_S h_S = \frac{d}{dt}(L_S A_S \rho_S h_S)$$

The perturbed equation is ;

$$\Delta Q_S + \bar{W}_B \Delta h_B + \bar{h}_B \Delta W_B - \bar{W}_S \Delta h_S - \bar{h}_S \Delta W_S = L_S A_S(\bar{\rho}_S S \Delta h_S + \bar{h}_S S \Delta\rho_S)$$

Since, $\Delta h_B = 0$, $\Delta h_S = C_{ps}\Delta T_S$ and $L_S A_S S \Delta\rho_S = \Delta W_B - \Delta W_S$

After substitution and rearrangement:

$$(L_S A_S \bar{\rho}_S C_{ps}) S \Delta T_S + (\bar{h}_S - \bar{h}_B)\Delta W_B - \Delta Q_S = -\bar{W}_S C_{ps} \Delta T_S \qquad (2)$$

or,

$$a_4 S \Delta T_S + a_5 \Delta W_B + a_6 \Delta Q_S = a_7 \Delta T_S$$

7. <u>Heat conduction across superheater walls</u>

Heat input to wall - Heat output from wall = Rate of change of energy stored in superheater wall

$$Q_{gs} - Q_s = \frac{d}{dt}(M_s C_s T_{sw})$$

The perturbed equation is :

$$\Delta Q_{gs} - \Delta Q_s = M_s C_s S \Delta T_{sw}$$

or,

$$a_8 \Delta Q_{gs} + a_9 \Delta Q_s = a_{10} S \Delta T_{sw} \qquad (3)$$

8. <u>Heat input to superheater wall</u>

The following empirical formula includes the cooling effect if air supply W_a differs from ideal air supply W_{ac} (Whalley (2)):

$$Q_{gs} = K_{gs} W_f^{0.6} (T_{gs} - T_{sw}) - K_{as}\left(1 - \frac{W_a}{W_{ac}}\right)^2$$

The perturbed equation is :

$$\Delta Q_{gs} = \frac{0.6 K_{gs}}{\bar{W}_f^{0.4}} (\bar{T}_{gs} - \bar{T}_{sw}) \Delta W_f + K_{gs} \bar{W}_f^{0.6} (\Delta T_{gs} - \Delta T_{sw}) + 2K_{as} \frac{(\bar{W}_{ac} - \bar{W}_a)}{\bar{W}_{ac}^2} \Delta W_a$$

or,

$$a_{11} \Delta Q_{gs} = a_{12} \Delta W_f + a_{13} (\Delta T_{gs} - \Delta T_{sw}) + a_{14} \Delta W_a \qquad (4)$$

9. Heat transfer across superheater wall

For turbulent gas flows:

$$Q_s = K_s W_B^{0.8} (T_{sw} - T_s)$$

The perturbed equation is :

$$\Delta Q_s = \frac{0.8}{\bar{W}_B^{0.2}} K_s (\bar{T}_{sw} - \bar{T}_s) \Delta W_B + K_s \bar{W}_B^{0.8} (\Delta T_{sw} - \Delta T_s)$$

or,

$$a_{15} \Delta Q_s = a_{16} \Delta W_B + a_{17} (\Delta T_{sw} - \Delta T_s) \qquad (5)$$

10. Heat transfer from combustion gas

Average gas temperature at superheater wall is T_{gs} where

$$T_{gs} = T_c - \frac{0.5\, Q_{gs}}{C_g W_f}$$

and C_g is related to the heat capacitance of the combustion gas by :

$$C_g = C_c \left(1 + \frac{W_a}{W_f}\right)$$

where C_c is constant

Thus ;

$$Q_{gs} = 2 C_c (W_f + W_a)(T_c - T_{gs})$$

The perturbed equation is :

$$\Delta Q_{gs} = 2 C_c \left[(\bar{W}_f + \bar{W}_a) \Delta T_c + (\bar{T}_c - \bar{T}_{gs}) \Delta W_f + (\bar{T}_c - \bar{T}_{gs}) \Delta W_a - (\bar{W}_f + \bar{W}_a) \Delta T_{gs} \right]$$

Rearranging:

$$\frac{1}{2C_c}\Delta Q_{gs} = (\bar{W}_f + \bar{W}_a)\Delta T_c + (\bar{T}_c - \bar{T}_{gs})\Delta W_f + (\bar{T}_c - \bar{T}_{gs})\Delta W_a - (\bar{W}_f + \bar{W}_a)\Delta T_{gs}$$

or,

$$a_{18}\Delta Q_{gs} = a_{19}\Delta T_c + a_{20}\Delta W_f + a_{21}\Delta W_a + a_{22}\Delta T_{gs} \qquad (6)$$

11. Superheater momentum

Neglecting the inertia of the steam:

$$(P_B - P_S)A_S - \left(\frac{f L_s V_B^2}{g D_s}\right) A_S \rho_B = 0$$

Since: $W_B = \rho_B A_S V_B$

$$(P_B - P_S) - \frac{f L_s}{g D_s}\left(\frac{W_B}{\rho_B A_S}\right)^2 \rho_B = 0$$

Substitute: $f_S = \dfrac{f L_s}{g D_s A_S^2}$

The perturbed equation is;

$$\Delta P_B - \Delta P_S = 2 f_S \frac{\bar{W}_B}{\bar{\rho}_B}\Delta W_B - f_S \frac{\bar{W}_B^2}{\bar{\rho}_B^2}\Delta \rho_B$$

Rearranging:

$$2 f_S \frac{\bar{W}_B}{\bar{\rho}_B}\Delta W_B + \Delta P_S - f_S \frac{\bar{W}_B^2}{\bar{\rho}_B^2}\Delta \rho_B = \Delta P_B$$

or,

$$a_{23}\Delta W_B + a_{24}\Delta P_S + a_{25}\Delta \rho_B = a_{26}\Delta P_B \qquad (7)$$

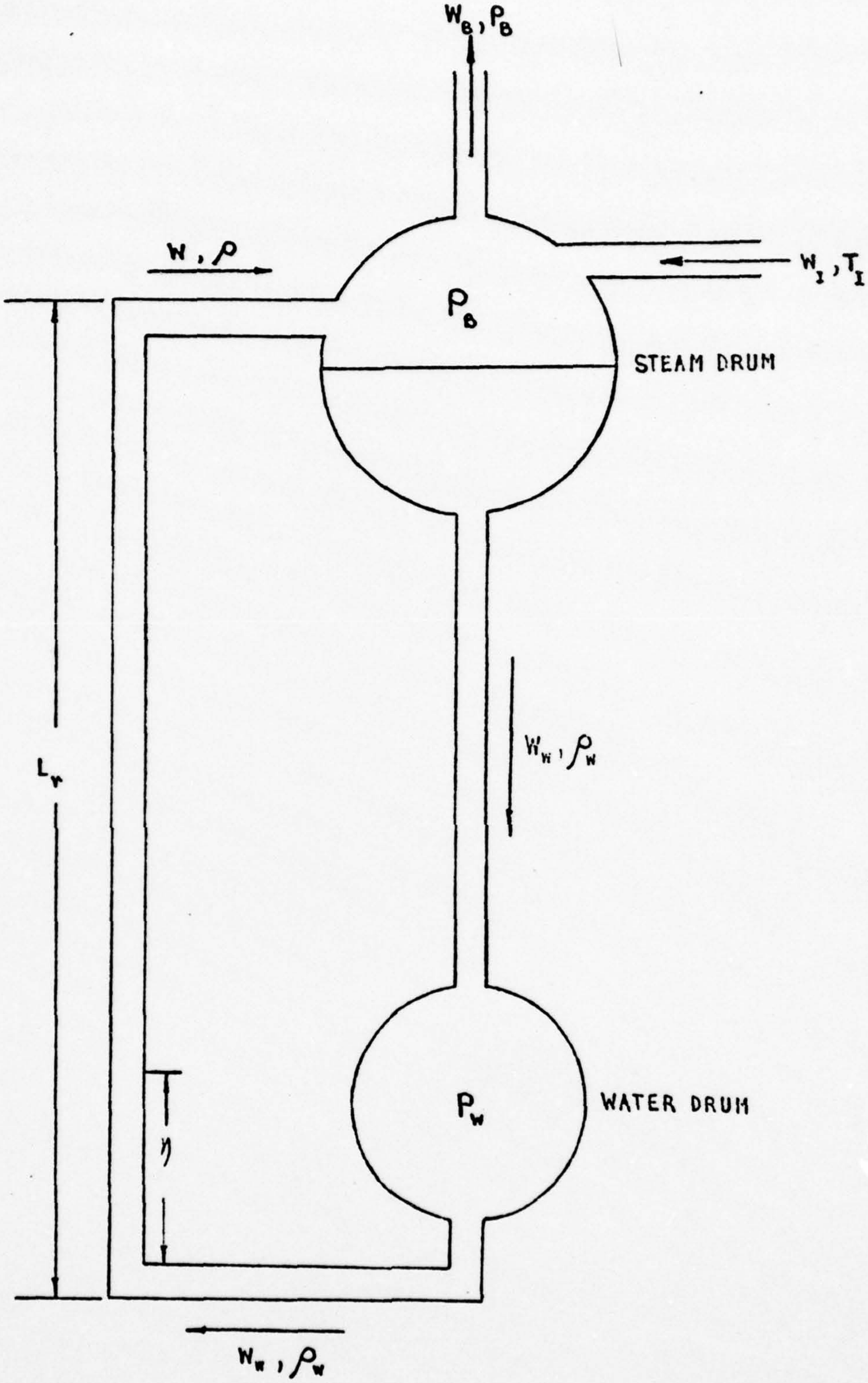


Figure 3 - SCHEMATIC DIAGRAM OF RISER-DOWNCOMER LOOP

12. Riser continuity equation

Mass flow into riser - Mass flow out = Rate of change of enclosed mass

$$W_w - W = \frac{d}{dt}\left[A_r(L_r - \eta)(\rho + \rho_w)/2\right]$$

The perturbed equation is :

$$\Delta W_w - \Delta W = \frac{1}{2}\left[A_r L_r S\Delta\rho - A_r(\rho + \rho_w)S\Delta\eta + A_r\bar{\eta}S\Delta\rho\right]$$

since

$$\frac{1}{\rho} = \frac{X}{\rho_B} + \frac{(1-X)}{\rho_w}$$

then,

$$\Delta\rho = \bar{\rho}^2\left(\frac{1}{\bar{\rho}_w} - \frac{1}{\bar{\rho}_B}\right)\Delta X + \frac{\bar{\rho}^2\bar{X}}{\bar{\rho}_B^2}\Delta\rho_B$$

If the starting point of evaporation in the riser tube is η above the water drum exit where ;

$$\eta = 1 - CW_w$$

then,

$$\Delta\eta = -C\Delta W_w$$

$A_r\bar{\eta}S\Delta\rho$ can be neglected since $\bar{\eta}$ is small

Substituting $\Delta\rho$ and $\Delta\eta$ and rearranging :

$$0.5A_rL_r\bar{\rho}^2\left(\frac{1}{\bar{\rho}_w} - \frac{1}{\bar{\rho}_B}\right)S\Delta X + 0.5A_rL_r\bar{X}K_B\left(\frac{\bar{\rho}^2}{\bar{\rho}_B^2}\right)S\Delta P_B$$

$$+ 0.5(\bar{\rho} + \bar{\rho}_w)CS\Delta W_w = \Delta W_w - \Delta W$$

or,

$$a_{27}S\Delta X + a_{28}S\Delta P_B + a_{29}S\Delta W_w = a_{30}\Delta W_w + a_{31}\Delta W \qquad (8)$$

13. Riser momentum equation

Pressure drop - frictional losses - gravity head - exit loss - momentum flux change = Inertia force

$$(P_W - P_B) A_r - \frac{f_r L_r W^2}{A_r^2 g D_r \rho^2} \cdot \rho A_r - A_r L_r \rho - \frac{W^2}{2g(\rho A_r)^2} \cdot \rho A_r$$

$$- \left[\frac{W^2}{g(\rho A_r)^2} \cdot \rho A_r - \frac{W_W^2}{g(\rho_W A_r)^2} \right] = \frac{L_r}{g} \frac{dW}{dt}$$

Therefore:

$$(P_W - P_B) - \left[\frac{1}{A_r^2 g} \left(\frac{f_r L_r}{D_r} + \frac{3}{2} \right) \right] \frac{W^2}{\rho} + \frac{W_W^2}{g \rho_W A_r^2} - L_r \rho = \frac{L_r}{g A_r} \frac{dW}{dt}$$

After perturbation and substitution for $\Delta\rho$ as done before in the Riser Continuity Equation, the perturbed equation is:

$$(\Delta P_W - \Delta P_B) - 2F \left[\left(\frac{1}{\bar{\rho}_B} - \frac{1}{\bar{\rho}_W} \right) \bar{W} \bar{X} + \frac{\bar{W}}{\bar{\rho}_W} \right] \Delta W - F W^2 \left(\frac{1}{\bar{\rho}_B} - \frac{1}{\bar{\rho}_W} \right) \Delta X$$

$$+ \frac{F \bar{X} \bar{W}^2}{\bar{\rho}_B^2 \Delta \rho_B} - L_r \left[\frac{\bar{X} \bar{\rho}^2}{\bar{\rho}_B^2 \Delta \rho_B} + \rho^2 \left(\frac{1}{\bar{\rho}_W} - \frac{1}{\bar{\rho}_B} \right) \right] \Delta X = \frac{L_r}{g A_r} S \Delta W$$

where:

$$F = \frac{\left(\frac{f_r L_r}{D_r} + \frac{3}{2} \right)}{A_r^2 g}$$

Rearranging:

$$\Delta P_W - \Delta P_B - (b_r + a_r S) \Delta W + b_X \Delta X - \frac{2 \bar{W}_W}{g A_r^2 \bar{\rho}_W} \Delta W_W + \propto \Delta \rho_B$$

where:

$$b_r = 2 \bar{W} \left(\frac{f_r L_r}{D_r} + \frac{3}{2} \right) / g A_r^2 \bar{\rho}$$

$$a_r = \frac{L_r}{g A_r}$$

$$b_x = \left(\frac{1}{\bar{\rho}_B} - \frac{1}{\bar{\rho}_W}\right)\left[\frac{\bar{W}^2}{g A_r^2}\left(\frac{f_r L_r}{D_r} + \frac{3}{2}\right) - \bar{\rho}^2 L_r\right]$$

$$\alpha = -\frac{\bar{X}}{\bar{\rho}_B^2}\left[\frac{\bar{W}^2}{A_r}\left(\frac{f_r L_r}{D_r} + \frac{3}{2}\right) + \bar{\rho}^2 L_r\right]$$ and is small enough to be neglected

Therefore :

$$\Delta P_W - \Delta P_B = b_v \Delta W + a_r S \Delta W + b_x \Delta X - \frac{2 W_W}{g A_r^2 \bar{\rho}_W} \Delta W_W$$

or,

$$a_{32} \Delta P_W + a_{33} \Delta P_B = a_{34} \Delta W + a_{35} S \Delta W + a_{36} \Delta X + a_{37} \Delta W \qquad (9)$$

14. Heat balance across riser tube wall

Heat from hot gas to riser tubes-Heat from tubes to mixture =Rate of change of internal energy stored in tubes

$$Q_{gB} - Q_B = \frac{d}{dt}\left(M_B C_B T_{BW}\right)$$

The perturbed equation is :

$$\Delta Q_{gB} - \Delta Q_B = M_B C_B S \Delta T_{BW}$$

or,

$$a_{38} \Delta Q_{gB} + a_{39} \Delta Q_B = a_{40} S \Delta T_{BW} \qquad (10)$$

15. Riser heat balance equation

Heat input to risers-Heat output from risers =Rate of change of internal energy

$$Q_B - W_w h_{WD} - Wh = \frac{d}{dt}\left[0.5 A_r (L_r - \eta)(\rho + \rho_w) h\right]$$

$$= \bar{h}\frac{d}{dt}\left[0.5 A_r (L_r - \eta)(\rho + \rho_w)\right] + A_r (L_r - \eta)(\bar{\rho} + \bar{\rho}_w)\frac{d}{dt}(h)$$

From the continuity equation ;

$$\frac{d}{dt}\left[0.5 A_r (L_r - \eta)(\rho + \rho_w)\right] = W_w - W$$

After substitution and perturbation ;

$$\Delta Q_B + \bar{W}_w \Delta h_{WD} + (\bar{h}_{WD} - \bar{h})\Delta W_w - \bar{W}\Delta h = 0.5 A_r L_r (\rho + \rho_w) S \Delta h$$

since :

$$h = h_{WB} + X h_{fg}$$

If changes in latent heat Δh_{fg} are neglected, then

$$\Delta h = \Delta h_{WB} + \bar{h}_{fg} \Delta X$$

From steam tables ;

$$\Delta h_{WB} = K_c \Delta P_B$$

$$\Delta h_{WD} = \Delta T_W$$

Therefore ;

$$0.5 A_r L_r (\bar{\rho} + \bar{\rho}_W) K_c S \Delta P_B + 0.5 A_r L_r (\bar{\rho} + \bar{\rho}_W) \bar{h}_{fg} S \Delta X - \Delta Q_B$$

$$= (\bar{h}_{WD} - \bar{h}) \Delta W_W - \bar{W} K_c \Delta P_B - \bar{W} \bar{h}_{fg} \Delta X + \bar{W}_W \Delta T_W$$

or,

$$a_{41} S \Delta P_B + a_{42} S \Delta X + a_{43} \Delta Q_B = a_{44} \Delta W_W + a_{45} \Delta P_B + a_{46} \Delta X + a_{47} \Delta T_W \qquad (11)$$

16. Riser heat transfer equation

An empirical formula that accounts for turbulent gas flow is adopted and gives :

$$Q_{gB} = K_{gB} W_f^{0.6} (T_{gB} - T_{BW}) - K_{ar}\left(1 - \frac{W_a}{W_{ac}}\right)^2 + K_r\left(T_{gB}^4 - T_{BW}^4\right)$$

The perturbed equation is :

$$\Delta Q_{gB} = \frac{0.6 K_{gB}(\bar{T}_{gB} - \bar{T}_{BW})}{W_f^{0.4}} \Delta W_f + K_{gB} \bar{W}_f (\Delta T_{gB} - \Delta T_{BW})$$

$$+ \frac{2 K_{ar}(\bar{W}_{ac} - \bar{W}_a)}{\bar{W}_{ac}^2} \Delta W_a + 4 K_r (T_{gB}^3 \Delta T_{gB} - T_{BW}^3 \Delta T_{BW})$$

Rearranging :

$$\Delta Q_{gB} - K_{gB} \bar{W}_f^{0.6} \Delta T_{gB} = - K_{gB} \bar{W}_f^{0.6} \Delta T_{BW} + \frac{0.6 K_{gB}(\bar{T}_{gB} - \bar{T}_{BW})}{\bar{W}_f^{0.4}} \Delta W_f$$

$$+ \frac{2 K_{ar}(\bar{W}_{ac} - \bar{W}_a)}{\bar{W}_{ac}^2} \Delta W_a + 4 K_r \bar{T}_{gB}^3 \Delta T_{gB}$$

$$- 4 K_r \bar{T}_{BW}^3 \Delta T_{BW}$$

hence :

$$\Delta Q_{gB} - (K_{gB} \bar{W}_f^{0.6} + 4 K_r \bar{T}_{gB}^3) \Delta T_{gB} = -(K_{gB} \bar{W}_f^{0.6} + 4 K_r \bar{T}_{BW}^3) \Delta T_{BW}$$

$$+ \frac{0.6 K_{gB} (\bar{T}_{gB} - \bar{T}_{BW})}{\bar{W}_f^{0.4}} \Delta W_f$$

$$+ \frac{2 K_{ar}(\bar{W}_{ac} - \bar{W}_a)}{\bar{W}_{ac}^2} \Delta W_a$$

or,

$$a_{48} \Delta Q_{gB} + a_{49} \Delta T_{gB} = a_{50} \Delta T_{BW} + a_{51} \Delta W_f + a_{52} \Delta W_a \qquad (12)$$

17. <u>Riser heat transfer to boiling fluid</u>

The heat transfer rate is assumed to be proportional to the cube of temperature difference between wall and mixture. Continuing to follow Whalley(2):

$$Q_B = K_g (T_{BW} - T_B)^3$$

The perturbed equation is :

$$\Delta Q_B = 3 K_g (\bar{T}_{BW} - \bar{T}_B)^2 (\Delta T_{BW} - \Delta T_B)$$

or,

$$a_{53} \Delta Q_B = a_{54} \Delta T_{BW} + a_{55} \Delta T_B \qquad (13)$$

18. <u>Downcomer momentum equation</u>

Σ Forces due to pressure difference-frictional loss +gravitational head-entrance loss = Inertia force

Hence :

$$(P_B - P_W) A_D - \frac{f_D L_D}{g D_D} (V_W)^2 \rho_W A_D + \rho_W A_D (L_D + 2) - \frac{(V_W)^2}{2g} \rho_W A_D$$
$$= \frac{d}{dt} \frac{(L_D A_D \rho_W V_W)}{g}$$

since : $W_W = \rho_W A_D V_W$

$$(P_B - P_W) - \frac{f_D L_D W_W^2}{g \rho_W D_D A_D^2} + \rho_W L_D - \frac{W_W^2}{2 g A_D \rho_W} = \frac{d}{dt} \frac{L_D}{g A_D} W_W$$

$$(P_B - P_W) - \left[\left(\frac{f_D L_D}{D_D} + 0.5 \right) \frac{1}{g \rho_W A_D^2} \right] W_W^2 + \rho_W L_D = \frac{L_D}{g A_D} \frac{d}{dt} (W_W)$$

The perturbed equation is ;

$$\Delta P_B - \Delta P_W = \left(b_W + a_W S \right) \Delta W_W - L_D \Delta \rho_W$$

where :

$$b_W = \frac{2\bar{W}_W}{g\bar{\rho}_W A_D^2}\left(\frac{f_D L_D}{D_D} + 0.5\right)$$

$$a_W = \frac{L_D}{g A_D}$$

Since flow is incompressible (ρ_W is constant both in time and space), then $\Delta\rho_W = 0$

Therefore ;

$$a_{56}\Delta P_B + a_{57}\Delta P_W = a_{58}\Delta W_W + a_{59} S \Delta W_W \qquad (14)$$

19. <u>Drum steam mass balance equation</u>

$\sum$ Vapor rates to/from drum = Rate of change of vapor mass in drum

Thus ,

Evaporation rate + vapor rate from risers-steam rate from drum = $\frac{d}{dt}(V_B \rho_B)$

Therefore :

$$W_e + X W - W_B = \frac{d}{dt}(V_B \rho_B)$$

The perturbed equation is :

$$\Delta W_e + \bar{X}\Delta W + \bar{W}\Delta X - \Delta W_B = \bar{V}_B S \Delta\rho_B + \bar{\rho}_B S \Delta V_B$$

Substituting for ;

$$\Delta V_B = - A \Delta y$$

$$\Delta \rho_B = K_B \Delta P_B$$

$$\Delta W_e = K_e(\Delta T_W - \Delta T_B)$$

gives :

$$\bar{V}_B K_B S \Delta P_B - \bar{\rho}_B A S \Delta y = K_e(\Delta T_w - \Delta T_B) + \bar{X}\Delta W + \bar{W}\Delta X - \Delta W_B$$

or,

$$a_{60} S \Delta P_B + a_{61} S \Delta y = a_{62}(\Delta T_w - \Delta T_B) + a_{63}\Delta W + a_{64}\Delta X + a_{65}\Delta W_B \quad (15)$$

20. Drum liquid heat balance equation

$\sum$ Heat to and from drum with liquid = Rate of change of the internal energy of the liquid

Hence :

Internal energy of riser liquid + heat transfered in feedwater - heat taken in by downcomer liquid - latent heat released with evaporating liquid $= \frac{d}{dt}$(drum liquid internal energy)

Therefore :

$$C_v(1-X)WT_B + C_i W_i T_i - C_D W_w T_w - W_e h_{BW} = \frac{d}{dt}(C_D M T_w)$$

But $C_v, C_i, C_D = 1$.

The perturbed equation is :

$$(1-\bar{X})\bar{T}_B \Delta W + (1-\bar{X})\bar{W}\Delta T_B - \bar{W}\bar{T}_B \Delta X + \bar{W}_i \Delta T_i + \bar{T}_i \Delta W_i - \bar{W}_w \Delta T_w$$

$$-\bar{T}_w \Delta W_w - \bar{W}_e \Delta h_{BW} - \bar{h}_{BW}\Delta W_e = \bar{M} S \Delta T_w + \bar{T}_w S \Delta M$$

Substituting for :

$$\Delta W_e = K_e(\Delta T_w - \Delta T_B)$$

$$\Delta h_{BW} = K_c \Delta P_B$$

$$\Delta M = A\rho_w \Delta y$$

and $T_i \approx$ constant, so $\Delta T_i \approx 0$

Thus:

$$(1-\bar{X})\bar{T}_B\,\Delta W + (1-\bar{X})\bar{W}\,\Delta T_B - \bar{W}\bar{T}_B\Delta X + \bar{T}_i\,\Delta W_i - \bar{W}_w\Delta T_w - \bar{T}_w\Delta W_w - \bar{W}_c K_c \Delta P_B$$

$$-\bar{h}_{BW} K_e(\Delta T_w - \Delta T_B) = \bar{M}\,S\,\Delta T_w + A\bar{\rho}_w \bar{T}_w S\,\Delta y$$

or,

$$a_{66}\,\Delta W + a_{67}\,\Delta T_B + a_{68}\,\Delta X + a_{69}\,\Delta W_i + a_{70}\Delta T_w + a_{71}\,\Delta W_w + a_{72}\,\Delta P_B$$

$$+\,a_{73}(\Delta T_w - \Delta T_B) = a_{74}\,S\,\Delta T_w + a_{75}\,S\,\Delta y \qquad (16)$$

21. <u>Drum liquid mass balance equation</u>

$\sum$ Liquid input/output rates = Rate of change enclosed mass of liquid

Hence:

feedwater input rate + riser liquid input rate-downcomer liquid rate-evaporation rate = $\frac{d}{dt}(M)$

Therefore:

$$W_i + (1-X)W - W_w - W_e = \frac{d}{dt}(M)$$

The perturbed equation is:

$$\Delta W_i + (1-\bar{X})\Delta W - \bar{W}\,\Delta X - \Delta W_w - \Delta W_e = S\,\Delta M$$

Substituting for:

$$\Delta W_e = K_e(\Delta T_w - \Delta T_B)$$

$$\Delta M = A\rho_w\,\Delta y$$

gives:

$$-K_e\,\Delta T_B + A\bar{\rho}_w S\,\Delta y = (1-\bar{X})\Delta W - \bar{W}\Delta X - \Delta W_w - K_e\Delta T_w + \Delta W_i$$

or,

$$a_{66}\,\Delta T_B + a_{77}\,S\,\Delta y = a_{88}\,\Delta W + a_{89}\,\Delta X + a_{90}\,\Delta W_w + a_{91}\Delta T_w + a_{92}\,\Delta W_i \qquad (17)$$

22. Equation from throttle valve

$$W_S = f_1(X_V, P_S, T_S)$$

The perturbed equation is :

$$\Delta W_S = \frac{\partial f_1}{\partial X} \Delta X_V + \frac{\partial f_1}{\partial P_S} \Delta P_S + \frac{\partial f_1}{\partial T_S} \Delta T_S$$

or,

$$a_{93} \Delta W_S = a_{94} \Delta X_V + a_{95} \Delta P_S + a_{96} \Delta T_S \qquad (18)$$

23. State equations

$$\Delta T_B = \frac{\partial T_B}{\partial P_B} \Delta P_B = K_T \Delta P_B$$

or,

$$\Delta T_B = a_{97} \Delta P_B \qquad (19)$$

$$\Delta \rho_B = \frac{\partial \rho_B}{\partial P_B} \Delta P_B = K_B \Delta P_B$$

or,

$$\Delta \rho_B = a_{98} \Delta P_B \qquad (20)$$

$$\Delta T_{gs} = \Delta T_{gs} \qquad (21)$$

$$\Delta h_{BW} = \frac{\partial h_{BW}}{\partial P_B} \Delta P_B = K_C \Delta P_B$$

or,

$$\Delta \dot{h}_{BW} = a_{99} \Delta P_B \qquad (22)$$

$$P_s = f_2(T_s, \rho_s)$$

$$\Delta P_s = \frac{\partial f_2}{\partial T_s} \Delta T_s + \frac{\partial f_2}{\partial \rho_s} \Delta \rho_s$$

or,

$$\Delta P_s = a_{100} \Delta T_s + a_{101} \Delta \rho_s \qquad (23)$$

$$\Delta T_c = K_f \Delta W_f$$

or,

$$\Delta T_c = a_{102} \Delta W_f \qquad (24)$$

C. STATE VARIABLE EQUATIONS

The following procedure is an algebraic method to reduce the twenty-four governing equations to ten state variable equations,that is, in standard matrix form of $\dot{X}(t) = AX(t) + BU(t)$

Here X(t) is the matrix of system state variables and U(t) is the matrix of system inputs.

From (1)

$$a_3 \Delta\dot{\rho}_s = a_1 \Delta W_B + a_2 \Delta W_s$$

$$\Delta\dot{\rho}_s = \frac{a_1}{a_3} \Delta W_B + \frac{a_2}{a_3} \Delta W_s$$

or,

$$\Delta\dot{\rho}_s = b_1 \Delta W_B + b_2 \Delta W_s \qquad (1.1)$$

From (2)

$$a_4 \Delta \dot{T}_s = -a_5 \Delta W_B - a_6 \Delta Q_s + a_7 \Delta T_s$$

$$\Delta \dot{T}_s = -\frac{a_5}{a_4} \Delta W_B - \frac{a_6}{a_4} \Delta Q_s + \frac{a_7}{a_4} \Delta T_s \qquad (1.2)$$

From (5)

$$\Delta Q_s = \frac{a_{16}}{a_{15}} \Delta W_B + \frac{a_{17}}{a_{15}} \Delta T_{sw} - \frac{a_{17}}{a_{15}} \Delta T_s \qquad (1.3)$$

Substituting Q_s from (1.3) in (1.2) and rearranging :

$$\Delta \dot{T}_s = \left(\frac{a_{15} \cdot a_{17}}{a_4 \cdot a_{15}} + \frac{a_7}{a_4}\right) \Delta T_s - \left(\frac{a_5}{a_4} + \frac{a_{16} \cdot a_{16}}{a_4 \cdot a_{15}}\right) \Delta W_B - \frac{a_6 \cdot a_{17}}{a_4 \cdot a_{15}} \Delta T_{sw}$$

or,

$$\Delta \dot{T}_S = b_3 \Delta T_S - b_4 \Delta W_B - b_5 \Delta T_{SW} \qquad (1.4)$$

From (3)

$$a_{10}\, S\, \Delta T_{SW} = a_8\, \Delta Q_{gs} + a_9\, \Delta Q_s$$

$$\Delta \dot{T}_{SW} = \frac{a_8}{a_{10}} \Delta Q_{gs} + \frac{a_9}{a_{10}} \Delta Q_s \qquad (1.5)$$

From (4)

$$\Delta Q_{gs} = \frac{a_{12}}{a_{11}} \Delta W_f + \frac{a_{13}}{a_{11}} \Delta T_{gs} - \frac{a_{13}}{a_{11}} \Delta T_{SW} + a_{14} \Delta W_a \qquad (1.6)$$

From (6)

$$\Delta Q_{gs} = \frac{a_{19}}{a_{18}} \Delta T_c + \frac{a_{20}}{a_{18}} \Delta W_f + \frac{a_{21}}{a_{18}} \Delta W_a + \frac{a_{22}}{a_{18}} \Delta T_{gs} \qquad (1.7)$$

Setting (1.6) = (1.7) and rearranging :

$$\Delta T_{gs} = -\frac{\left(\frac{a_{12}}{a_{11}} - \frac{a_{20}}{a_{18}}\right)}{\left(\frac{a_{13}}{a_{11}} - \frac{a_{22}}{a_{18}}\right)} \Delta W_f + \frac{\left(\frac{a_{13}}{a_{11}}\right)}{\left(\frac{a_{13}}{a_{11}} - \frac{a_{22}}{a_{18}}\right)} \Delta T_{SW}$$

$$- \frac{\left(a_{14} - \frac{a_{21}}{a_{18}}\right)}{\left(\frac{a_{13}}{a_{11}} - \frac{a_{22}}{a_{18}}\right)} \Delta W_a + \frac{\left(\frac{a_{19}}{a_{18}}\right)}{\left(\frac{a_{13}}{a_{11}} - \frac{a_{22}}{a_{18}}\right)} \Delta T_c \qquad (1.8)$$

Substituting $\Delta T_c = a_{102} \Delta W_f$ from (24) into (1.8) and rearranging :

$$\Delta T_{gs} = \frac{\left(\frac{a_{19} \cdot a_{102}}{a_{18}} - \frac{a_{12}}{a_{11}} + \frac{a_{20}}{a_{18}}\right)}{\left(\frac{a_{13}}{a_{11}} - \frac{a_{22}}{a_{18}}\right)} \Delta W_f + \frac{\left(\frac{a_{13}}{a_{11}}\right)}{\left(\frac{a_{13}}{a_{11}} - \frac{a_{22}}{a_{18}}\right)} \Delta T_{SW} - \frac{\left(a_{14} - \frac{a_{21}}{a_{18}}\right)}{\left(\frac{a_{13}}{a_{11}} - \frac{a_{22}}{a_{18}}\right)} \Delta W_a$$

or,

$$\Delta T_{gs} = b_6 \Delta W_f + b_7 \Delta T_{sw} - b_8 \Delta W_a \tag{1.9}$$

Substituting ΔT_{gs} from (1.9) into (1.6) and rearranging :

$$\Delta Q_{gs} = \left(\frac{a_{12}}{a_{11}} + \frac{a_{13} . b_6}{a_{11}}\right) \Delta W_f + \left(\frac{b_7 . a_{13}}{a_{11}} - \frac{a_{13}}{a_{11}}\right) \Delta T_{sw} + \left(a_{14} - \frac{b_8 . a_{13}}{a_{11}}\right) \Delta W_a$$

or,

$$\Delta Q_{gs} = b_9 \Delta W_f + b_{10} \Delta T_{sw} + b_{11} \Delta W_a \tag{1.10}$$

Substituting ΔQ_{gs} from (1.10) and ΔQ_s from (1.3) into (1.5) and rearranging :

$$\Delta \dot{T}_{sw} = \left(\frac{a_8 . b_9}{a_{10}}\right) \Delta W_f + \left(\frac{a_8 . b_{10}}{a_{10}} + \frac{a_9 . a_{17}}{a_{10} . a_{15}}\right) \Delta T_{sw} + \left(\frac{a_8 . b_{11}}{a_{10}}\right) \Delta W_a$$

$$+ \left(\frac{a_9 . a_{16}}{a_{10} . a_{15}}\right) \Delta W_B - \left(\frac{a_9 . a_{17}}{a_{10} . a_{15}}\right) \Delta T_s$$

or,

$$\Delta \dot{T}_{sw} = b_{12} \Delta W_f + b_{13} \Delta T_{sw} + b_{14} \Delta W_a + b_{15} \Delta W_B - b_{16} \Delta T_s \tag{1.11}$$

From (17)

$$\Delta \dot{y} = - \frac{a_{76}}{a_{77}} \Delta T_B + \frac{a_{88}}{a_{77}} \Delta W + \frac{a_{89}}{a_{77}} \Delta X$$

$$+ \frac{a_{90}}{a_{77}} \Delta W_w + \frac{a_{91}}{a_{77}} \Delta T_w + \frac{a_{92}}{a_{77}} \Delta W_i \tag{1.12}$$

Substituting ΔT_B from (19) into (1.12)

$$\Delta \mathring{y} = -\frac{a_{76}.a_{97}}{a_{77}} \Delta P_B + \frac{a_{88}}{a_{77}} \Delta W + \frac{a_{89}}{a_{77}} \Delta X$$

$$+ \frac{a_{90}}{a_{77}} \Delta W_w + \frac{a_{91}}{a_{77}} \Delta T_W + \frac{a_{92}}{a_{77}} \Delta W_i$$

or,

$$\Delta \mathring{y} = -b_{17} \Delta P_B + b_{18} \Delta W + b_{19} \Delta X + b_{20} \Delta W_w + b_{21} \Delta T_w + b_{22} \Delta W_i \qquad (1.13)$$

From (16)

$$\Delta \dot{T}_W = -\frac{a_{75}}{a_{74}} \Delta \mathring{y} + \frac{a_{66}}{a_{74}} \Delta W + \frac{(a_{67} - a_{73})}{a_{74}} \Delta T_B + \frac{a_{68}}{a_{74}} \Delta X$$

$$+ \frac{a_{69}}{a_{74}} \Delta W_i + \frac{(a_{70} + a_{73})}{a_{74}} \Delta T_W + \frac{a_{71}}{a_{74}} \Delta W_w + \frac{a_{72}}{a_{74}} \Delta P_B \qquad (1.14)$$

Substituting $\Delta \mathring{y}$ from (1.13) and ΔT_B from (19) into (1.14) and rearranging ;

$$\Delta \dot{T}_W = \left(\frac{a_{75}.b_{17}}{a_{74}} + \frac{a_{97}.a_{67}}{a_{74}} - \frac{a_{97}.a_{73}}{a_{74}}\right) \Delta P_B + \left(\frac{a_{66}}{a_{74}} - \frac{a_{75}.b_{18}}{a_{74}}\right) \Delta W$$

$$+ \left(\frac{a_{68}}{a_{74}} - \frac{a_{75}.b_{19}}{a_{74}}\right) \Delta X + \left(\frac{a_{71}}{a_{74}} - \frac{a_{75}.b_{20}}{a_{74}}\right) \Delta W_W$$

$$+ \left(\frac{a_{70} + a_{73}}{a_{74}} - \frac{a_{75}.b_{21}}{a_{74}}\right) \Delta T_W + \left(\frac{a_{69}}{a_{74}} - \frac{a_{75}.b_{22}}{a_{74}}\right) \Delta W_i$$

or,

$$\Delta \dot{T}_W = b_{23} \Delta P_B + b_{24} \Delta W + b_{25} \Delta X + b_{26} \Delta W_w + b_{27} \Delta T_W + b_{28} \Delta W_i \quad (1.15)$$

From (15)

$$\Delta P_B = -\frac{a_{61}}{a_{60}}\Delta\dot{y} + \frac{a_{62}}{a_{60}}\Delta T_W - \frac{a_{62}}{a_{60}}\Delta T_B + \frac{a_{63}}{a_{60}}\Delta W + \frac{a_{64}}{a_{60}}\Delta X + \frac{a_{65}}{a_{60}}\Delta W_B \quad (1.16)$$

Substituting $\Delta\dot{y}$ from (1.13) into (1.16) and rearranging :

$$\Delta\dot{P}_B = \left(\frac{a_{61}.b_{17}}{a_{60}} - \frac{a_{62}.a_{97}}{a_{60}}\right)\Delta P_B + \left(\frac{a_{63}}{a_{60}} - \frac{a_{61}.b_{18}}{a_{60}}\right)\Delta W + \left(\frac{a_{64}}{a_{60}} - \frac{a_{61}.b_{19}}{a_{60}}\right)\Delta X$$

$$-\left(\frac{a_{61}.b_{20}}{a_{60}}\right)\Delta W_W + \left(\frac{a_{62}}{a_{60}} - \frac{a_{61}.b_{21}}{a_{60}}\right)\Delta T_W$$

$$-\left(\frac{a_{61}.b_{22}}{a_{60}}\right)\Delta W_i + \left(\frac{a_{65}}{a_{60}}\right)\Delta W_B$$

or,

$$\Delta\dot{P}_B = b_{29}\Delta P_B + b_{30}\Delta W + b_{31}\Delta X - b_{32}\Delta W_W$$

$$+ b_{33}\Delta T_W - b_{34}\Delta W_i + b_{35}\Delta W_B \quad (1.17)$$

From (11)

$$\Delta\dot{X} = -\frac{a_{41}}{a_{42}}\Delta\dot{P}_B - \frac{a_{43}}{a_{42}}\Delta Q_B + \frac{a_{44}}{a_{42}}\Delta W_W + \frac{a_{45}}{a_{42}}\Delta P_B$$

$$+ \frac{a_{46}}{a_{42}}\Delta X + \frac{a_{47}}{a_{42}}\Delta T_W \quad (1.18)$$

From (13)

$$\Delta Q_B = \frac{a_{54}}{a_{53}}\Delta T_{BW} + \frac{a_{55}}{a_{53}}\Delta T_B$$

Substituting ΔT_B from (19)

$$\Delta Q_B = \frac{a_{54}}{a_{53}} \Delta T_{BW} + \frac{a_{55} . a_{97}}{a_{53}} \Delta P_B \qquad (1.19)$$

Substituting $\Delta \dot{P}_B$ from (1.17) and ΔQ_B from (1.19) into (1.18) and rearranging :

$$\Delta \dot{X} = \left(\frac{a_{45}}{a_{42}} - \frac{a_{41}. b_{29}}{a_{42}} - \frac{a_{43}. a_{55} . a_{97}}{a_{42} . a_{53}} \right) \Delta P_B - \left(\frac{a_{41} . b_{30}}{a_{42}} \right) \Delta W$$

$$+ \left(\frac{a_{46}}{a_{42}} - \frac{a_{41}. b_{31}}{a_{42}} \right) \Delta X + \left(\frac{a_{44}}{a_{42}} + \frac{a_{41}. b_{32}}{a_{42}} \right) \Delta W_W + \left(\frac{a_{47}}{a_{42}} - \frac{a_{41}. b_{33}}{a_{42}} \right) \Delta T_W$$

$$+ \left(\frac{a_{41} . b_{34}}{a_{42}} \right) \Delta W_i - \left(\frac{a_{41} . b_{35}}{a_{42}} \right) \Delta W_B - \left(\frac{a_{43} . a_{54}}{a_{42} . a_{53}} \right) \Delta T_{BW}$$

or,

$$\Delta \dot{X} = b_{36} \Delta P_B - b_{37} \Delta W + b_{38} \Delta X + b_{39} \Delta W_W$$

$$+ b_{40} \Delta T_W + b_{41} \Delta W_i - b_{42} \Delta W_B - b_{43} \Delta T_{BW} \qquad (1.20)$$

From (8)

$$\Delta \dot{W} = - \frac{a_{27}}{a_{29}} \Delta \dot{X} - \frac{a_{28}}{a_{29}} \Delta \dot{P}_B + \frac{a_{30}}{a_{29}} \Delta W_W + \frac{a_{31}}{a_{29}} \Delta W \qquad (1.21)$$

Substituting $\Delta \dot{X}$ from (1.20) and $\Delta \dot{P}_B$ from (1.17) into (1.21) and rearranging :

$$\Delta \dot{W}_W = -\left(\frac{a_{27}.b_{36}}{a_{29}} + \frac{a_{28}.b_{29}}{a_{29}}\right)\Delta P_B + \left(\frac{a_{27}.b_{37}}{a_{29}} - \frac{a_{28}.b_{30}}{a_{29}} + \frac{a_{31}}{a_{29}}\right)\Delta W$$

$$-\left(\frac{a_{27}.b_{38}}{a_{29}} + \frac{a_{28}.b_{31}}{a_{29}}\right)\Delta X + \left(\frac{a_{28}.b_{32}}{a_{29}} + \frac{a_{30}}{a_{29}} - \frac{a_{27}.b_{39}}{a_{29}}\right)\Delta W_W$$

$$-\left(\frac{a_{27}.b_{40}}{a_{29}} + \frac{a_{28}.b_{33}}{a_{29}}\right)\Delta T_W + \left(\frac{a_{28}.b_{34}}{a_{29}} - \frac{a_{27}.b_{41}}{a_{29}}\right)\Delta W_i$$

$$+\left(\frac{a_{27}.b_{42}}{a_{29}} - \frac{a_{28}.b_{35}}{a_{29}}\right)\Delta W_B + \left(\frac{a_{27}.b_{43}}{a_{29}}\right)\Delta T_{BW}$$

or,

$$\Delta \dot{W}_W = -b_{44}\,\Delta P_B + b_{45}\,\Delta W - b_{46}\,\Delta X + b_{47}\Delta W_W - b_{48}\,\Delta T_W$$

$$+ b_{49}\,\Delta W_i + b_{50}\,\Delta W_B + b_{51}\,\Delta T_{BW} \qquad (1.22)$$

Substituting $\Delta \dot{W}_W$ from (1.22) into (14) and rearranging :

$$\Delta P_W = \left(\frac{a_{58} + a_{59}.b_{47}}{a_{57}}\right)\Delta W_W - \left(\frac{a_{56} + a_{59}.b_{44}}{a_{57}}\right)\Delta P_B + \left(\frac{a_{59}.b_{45}}{a_{57}}\right)\Delta W$$

$$-\left(\frac{a_{59}.b_{46}}{a_{57}}\right)\Delta X - \left(\frac{a_{59}.b_{48}}{a_{57}}\right)\Delta T_W + \left(\frac{a_{59}.b_{49}}{a_{57}}\right)\Delta W_i$$

$$+\left(\frac{a_{59}.b_{50}}{a_{57}}\right)\Delta W_B + \left(\frac{a_{59}.b_{51}}{a_{57}}\right)\Delta T_{BW}$$

or,

$$\Delta P_W = b_{52}\Delta W_W - b_{53}\Delta P_B + b_{54}\Delta W - b_{55}\Delta X - b_{56}\Delta T_W$$

$$+ b_{57}\Delta W_i + b_{58}\Delta W_B + b_{59}\Delta T_{BW} \qquad (1.23)$$

From (9)

$$\Delta \dot{W} = \frac{a_{32}}{a_{35}}\Delta P_W + \frac{a_{33}}{a_{35}}\Delta P_B - \frac{a_{34}}{a_{35}}\Delta W - \frac{a_{36}}{a_{35}}\Delta X - \frac{a_{37}}{a_{35}}\Delta W_W$$

Substituting ΔP_W from (1.23) into (1.24) and rearranging :

$$\Delta \dot{W} = \left(\frac{a_{32}\cdot b_{52}}{a_{35}} - \frac{a_{37}}{a_{35}}\right)\Delta W_W + \left(\frac{a_{33}}{a_{35}} - \frac{a_{32}\cdot b_{53}}{a_{35}}\right)\Delta P_B + \left(\frac{a_{32}\cdot b_{54}}{a_{35}} - \frac{a_{34}}{a_{35}}\right)\Delta W$$

$$-\left(\frac{a_{32}\cdot b_{55}}{a_{35}} + \frac{a_{36}}{a_{35}}\right)\Delta X - \left(\frac{a_{32}\cdot b_{56}}{a_{35}}\right)\Delta T_W + \left(\frac{a_{32}\cdot b_{57}}{a_{35}}\right)\Delta W_i$$

$$+\left(\frac{a_{32}\cdot b_{58}}{a_{35}}\right)\Delta W_B + \left(\frac{a_{32}\cdot b_{59}}{a_{35}}\right)\Delta T_{BW}$$

or,

$$\Delta \dot{W} = b_{60}\Delta W_W + b_{61}\Delta P_B + b_{62}\Delta W - b_{63}\Delta X - b_{64}\Delta T_W$$

$$+ b_{65}\Delta W_i + b_{66}\Delta W_B + b_{67}\Delta T_{BW} \qquad (1.25)$$

From (10)

$$\Delta \dot{T}_{BW} = \frac{a_{38}}{a_{40}}\Delta Q_{yB} + \frac{a_{39}}{a_{40}}\Delta Q_B . \qquad (1.26)$$

From (12)

$$a_{48}\,\Delta Q_{gB} = a_{50}\,\Delta T_{BW} + a_{51}\,\Delta W_f + a_{52}\,\Delta W_a - a_{49}\,\Delta T_{gB} \qquad (1.27)$$

Since $\Delta T_{gB} = \Delta T_{gS}$ from (21), then substituting ΔT_{gS} From (1.9) into (1.27) and rearranging :

$$\Delta Q_{gB} = \frac{a_{50}}{a_{48}}\,\Delta T_{BW} + \left(\frac{a_{51} - a_{49}\cdot b_6}{a_{48}}\right)\Delta W_f + \left(\frac{a_{52} + a_{49}\cdot b_8}{a_{48}}\right)\Delta W_a - \left(\frac{a_{49}\cdot b_7}{a_{48}}\right)\Delta T_{SW} \qquad (1.28)$$

Substituting ΔQ_{gB} from (1.28) and ΔQ_B from (1.19) into (1.26) and rearranging :

$$\Delta \dot{T}_{BW} = \left(\frac{a_{38}\cdot a_{50}}{a_{40}\cdot a_{48}} + \frac{a_{39}\cdot a_{54}}{a_{40}\cdot a_{53}}\right)\Delta T_{BW} + \left(\frac{a_{38}}{a_{40}\cdot a_{48}}\right)\left(a_{51} - a_{49}\cdot b_6\right)\Delta W_f + \left(\frac{a_{38}}{a_{40}\cdot a_{48}}\right)\left(a_{52} + a_{49}\cdot b_8\right)\Delta W_a - \left(\frac{a_{38}\cdot a_{49}\cdot b_7}{a_{40}\cdot a_{48}}\right)\Delta T_{SW} + \left(\frac{a_{39}\cdot a_{55}\cdot a_{97}}{a_{40}\cdot a_{53}}\right)\Delta P_B$$

or,

$$\Delta \dot{T}_{BW} = b_{68}\,\Delta T_{BW} + b_{69}\,\Delta W_f + b_{70}\,\Delta W_a - b_{71}\,\Delta T_{SW} + b_{72}\,\Delta P_B \qquad (1.29)$$

From (7)

$$\Delta W_B = \frac{a_{26}}{a_{23}}\,\Delta P_B - \frac{a_{24}}{a_{23}}\,\Delta P_S - \frac{a_{25}}{a_{23}}\,\Delta \rho_B \qquad (1.30)$$

Substituting ΔP_S from (23) and $\Delta \rho_B$ from (20) into (1.30)

$$\Delta W_B = \left(\frac{a_{26}}{a_{23}} - \frac{a_{25} \cdot a_{98}}{a_{23}}\right) \Delta P_B - \left(\frac{a_{24} \cdot a_{100}}{a_{23}}\right) \Delta T_S - \left(\frac{a_{24} \cdot a_{101}}{a_{23}}\right) \Delta \rho_S$$

or,

$$\Delta W_B = b_{73} \Delta P_B - b_{74} \Delta T_S - b_{75} \Delta \rho_S \qquad (1.31)$$

From (18)

$$\Delta W_S = \frac{a_{94}}{a_{93}} \Delta X_V + \frac{a_{95}}{a_{93}} \Delta P_S + \frac{a_{96}}{a_{93}} \Delta T_S \qquad (1.32)$$

Substituting ΔP_S from (23) into (1.32)

$$\Delta W_S = \frac{a_{94}}{a_{93}} \Delta X_V + \left(\frac{a_{95} \cdot a_{100}}{a_{93}} + \frac{a_{96}}{a_{93}}\right) \Delta T_S + \frac{a_{95} \cdot a_{101}}{a_{93}} \Delta \rho_S$$

or,

$$\Delta W_S = b_{76} \Delta X_V + b_{77} \Delta T_S + b_{78} \Delta \rho_S \qquad (1.33)$$

Substituting ΔW_B from (1.31) and ΔW_S from (1.33) into (1.1) and rearranging :

$$\Delta \dot{\rho}_S = (b_2 \cdot b_{78} - b_1 \cdot b_{75}) \Delta \rho_S + (b_2 \cdot b_{77} - b_1 \cdot b_{74}) \Delta T_S$$

$$+ (b_1 \cdot b_{73}) \Delta P_B + (b_2 \cdot b_{76}) \Delta X_V$$

or,

$$\Delta \dot{\rho}_S = C_{11} \Delta \rho_S + C_{12} \Delta T_S + C_{13} \Delta P_B + D_{11} \Delta X_V \qquad (A)$$

Substituting ΔW_B from (1.31) into (1.4) and rearranging :

$$\Delta\dot{T}_S = b_4 \cdot b_{75}\,\Delta\rho_s + (b_3 + b_4 \cdot b_{74})\,\Delta T_s - b_5\,\Delta T_{sw} - b_4\,b_{73}\,\Delta P_B$$

or,

$$\Delta\dot{T}_S = C_{21}\,\Delta\rho_s + C_{22}\,\Delta T_s + C_{23}\,\Delta T_{sw} + C_{28}\,\Delta P_B \qquad (B)$$

Substituting ΔW_B from (1.31) into (1.11) and rearranging :

$$\Delta\dot{T}_{sw} = -b_{15} \cdot b_{75}\,\Delta\rho_s - (b_{15} \cdot b_{74} + b_{16})\,\Delta T_s + b_{13}\,\Delta T_{sw}$$

$$+ b_{15} \cdot b_{73}\,\Delta P_B + b_{12}\,\Delta W_f + b_{14}\,\Delta W_a$$

or,

$$\Delta\dot{T}_{sw} = C_{31}\,\Delta\rho_s + C_{32}\,\Delta T_s + C_{33}\,\Delta T_{sw} + C_{38}\,\Delta P_B$$

$$+ D_{32}\,\Delta W_f + D_{33}\,\Delta W_a \qquad (C)$$

Substituting ΔW_B from (1.31) into (1.20) and rearranging :

$$\Delta\dot{X} = b_{42} \cdot b_{75}\,\Delta\rho_s + b_{42} \cdot b_{74}\,\Delta T_s + b_{38}\,\Delta X - b_{37}\,\Delta W$$

$$+ b_{39}\,\Delta W_W - b_{43}\,\Delta T_{BW} + (b_{36} - b_{42} \cdot b_{73})\,\Delta P_B$$

$$+ b_{40}\,\Delta T_W + b_{41}\,\Delta W_i$$

or,

$$\Delta\dot{X} = C_{41}\,\Delta\rho_s + C_{42}\,\Delta T_s + C_{44}\,\Delta X + C_{45}\,\Delta W + C_{46}\,\Delta W_W$$

$$+ C_{47}\,\Delta T_{BW} + C_{48}\,\Delta P_B + C_{49}\,\Delta T_W + D_{44}\,\Delta W_i \qquad (D)$$

Substituting ΔW_B from (1.31) into (1.25) and rearranging ;

$$\Delta \dot{W} = -b_{66} \cdot b_{75} \Delta \rho_S - b_{66} \cdot b_{74} \Delta T_S - b_{63} \Delta X + b_{62} \Delta W + b_{60} \Delta W_W$$

$$+ b_{67} \Delta T_{BW} + (b_{66} \cdot b_{73} + b_{61}) \Delta P_B - b_{64} \Delta T_W + b_{65} \Delta W_i$$

or,

$$\Delta \dot{W} = C_{51} \Delta \rho_S + C_{52} \Delta T_S + C_{54} \Delta X + C_{55} \Delta W + C_{56} \Delta W_W$$

$$+ C_{57} \Delta T_{BW} + C_{58} \Delta P_B + C_{59} \Delta T_W + D_{54} \Delta W_i \qquad \text{(E)}$$

Substituting ΔW_B from (1.31) into (1.22) and rearranging ;

$$\Delta \dot{W}_W = -b_{50} \cdot b_{75} \Delta \rho_S - b_{50} \cdot b_{74} \Delta T_S - b_{46} \Delta X + b_{45} \Delta W$$

$$+ b_{47} \Delta W_W + b_{51} \Delta T_{BW} + (b_{50} \cdot b_{73} - b_{44}) \Delta P_B$$

$$- b_{48} \Delta T_W + b_{49} \Delta W_i$$

or,

$$\Delta \dot{W}_W = C_{61} \Delta \rho_S + C_{62} \Delta T_S + C_{64} \Delta X + C_{65} \Delta W + C_{66} \Delta W_W$$

$$+ C_{67} \Delta T_{BW} + C_{68} \Delta P_B + C_{69} \Delta T_W + D_{64} \Delta W_i \qquad \text{(F)}$$

From (1.29)

$$\Delta \dot{T}_{BW} = -b_{71} \Delta T_{SW} + b_{68} \Delta T_{BW} + b_{72} \Delta P_B + b_{69} \Delta W_f + b_{70} \Delta W_a$$

or,

$$\Delta \overset{\circ}{T}_{BW} = C_{73}\,\Delta T_{SW} + C_{77}\,\Delta T_{BW} + C_{78}\,\Delta P_B + D_{72}\,\Delta W_f + D_{73}\,\Delta W_a \qquad (G)$$

Substituting ΔW_B from (1.31) into (1.17) and rearranging :

$$\Delta \overset{\circ}{P}_B = -b_{35}\cdot b_{73}\,\Delta \rho_S - b_{35}\cdot b_{74}\,\Delta T_S + b_{31}\,\Delta X + b_{30}\,\Delta W$$

$$- b_{32}\,\Delta W_W + (b_{29} + b_{35}\cdot b_{73})\,\Delta P_B + b_{33}\,\Delta T_W - b_{34}\,\Delta W_i$$

or,

$$\Delta \overset{\circ}{P}_B = C_{81}\,\Delta \rho_S + C_{82}\,\Delta T_S + C_{84}\,\Delta X + C_{85}\,\Delta W + C_{86}\,\Delta W_W$$

$$+ C_{88}\,\Delta P_B + C_{89}\,\Delta T_W + D_{84}\,\Delta W_i \qquad (H)$$

From (1.15)

$$\Delta \overset{\circ}{T}_W = b_{25}\,\Delta X + b_{24}\,\Delta W + b_{26}\,\Delta W_W + b_{23}\,\Delta P_B + b_{27}\,\Delta T_W + b_{28}\,\Delta W_i$$

or,

$$\Delta \overset{\circ}{T}_W = C_{94}\,\Delta X + C_{95}\,\Delta W + C_{96}\,\Delta W_W + C_{98}\,\Delta P_B + C_{99}\,\Delta T_W + D_{94}\,\Delta W_i \qquad (I)$$

From (1.13)

$$\Delta \overset{\circ}{y} = b_{19}\,\Delta X + b_{18}\,\Delta W + b_{20}\,\Delta W_W - b_{17}\,\Delta P_B + b_{21}\,\Delta T_W + b_{22}\,\Delta W_i$$

or,

$$\Delta \overset{\circ}{y} = C_{104}\,\Delta X + C_{105}\,\Delta W + C_{106}\,\Delta W_W + C_{108}\,\Delta P_B + C_{109}\,\Delta T_W + D_{104}\,\Delta W_i \qquad (J)$$

The state variable equations from (A) to (J) were rewritten in matrix notation as shown in Figure 4. The state equations were solved for various percent step changes to input variables (ΔX_V , ΔW_F , ΔW_I),using the IBM simulation language CSMP - III as shown in the next section.

$$
\begin{bmatrix} \Delta\mathring{\rho}_s \\ \Delta\mathring{T}_s \\ \Delta\mathring{T}_{SW} \\ \Delta\mathring{X} \\ \Delta\mathring{W} \\ \Delta\mathring{W}_W \\ \Delta\mathring{T}_{BW} \\ \Delta\mathring{P}_B \\ \Delta\mathring{T}_W \\ \Delta\mathring{Y} \end{bmatrix}
=
\begin{bmatrix}
C_{11} & C_{12} & 0 & 0 & 0 & 0 & 0 & C_{18} & 0 & 0 \\
C_{21} & C_{22} & C_{23} & 0 & 0 & 0 & 0 & C_{28} & 0 & 0 \\
C_{31} & C_{32} & C_{33} & 0 & 0 & 0 & 0 & C_{38} & 0 & 0 \\
C_{41} & C_{42} & 0 & C_{44} & C_{45} & C_{46} & C_{47} & C_{48} & C_{49} & 0 \\
C_{51} & C_{52} & 0 & C_{54} & C_{55} & C_{56} & C_{57} & C_{58} & C_{59} & 0 \\
C_{61} & C_{62} & 0 & C_{64} & C_{65} & C_{66} & C_{67} & C_{68} & C_{69} & 0 \\
0 & 0 & C_{73} & 0 & 0 & 0 & C_{77} & C_{78} & 0 & 0 \\
C_{81} & C_{82} & 0 & C_{84} & C_{85} & C_{86} & 0 & C_{88} & C_{89} & 0 \\
0 & 0 & 0 & C_{94} & C_{95} & C_{96} & 0 & C_{98} & C_{99} & 0 \\
0 & 0 & 0 & C_{104} & C_{105} & C_{106} & 0 & C_{108} & C_{109} & 0
\end{bmatrix}
\begin{bmatrix} \Delta\rho_s \\ \Delta T_s \\ \Delta T_{SW} \\ \Delta X \\ \Delta W \\ \Delta W_W \\ \Delta T_{BW} \\ \Delta P_B \\ \Delta T_W \\ \Delta Y \end{bmatrix}
+
\begin{bmatrix}
D_{11} & 0 & 0 & 0 \\
0 & 0 & 0 & 0 \\
0 & D_{32} & D_{33} & 0 \\
0 & 0 & 0 & D_{44} \\
0 & 0 & 0 & D_{54} \\
0 & 0 & 0 & D_{64} \\
0 & D_{72} & D_{73} & 0 \\
0 & 0 & 0 & D_{84} \\
0 & 0 & 0 & D_{94} \\
0 & 0 & 0 & D_{104}
\end{bmatrix}
\begin{bmatrix} \Delta X_V \\ \Delta W_F \\ \Delta W_A \\ \Delta W_I \end{bmatrix}
$$

Figure 4 - STATE VARIABLE MATRIX

III. COMPUTER RESULTS

From Appendix A , it is seen that the a coefficients are in terms of steady state values. These values were determined from the data in Whalleys thesis (2) which are repeated in Appendix E. A Fortran IV program to find the a,b,C,D coefficients which appear in the CSMP program is shown in Appendix F, and the calculated values are shown in Appendix G. Appendix H is the IBM simulation language CSMP program that was developed. Only input variables were changed for each computer run. For example, results for a 5% step change of Δx_v, a 10% step change of ΔW_f and a 10% step change of ΔW_t were calculated. The output response curves were plotted using the NPS CALCOMP PLOTTER.

A. TRANSIENT RESPONSES FOLLOWING A STEP CHANGE IN THROTTLE SETTING OF 5%

At a particular steady state operating condition the throttle valve is suddenly opened while still keeping the previous air and fuel flow rates and feedwater flow rate constant. Because of bubble formation in the steam drum liquid,the steam drum water level (FIGURE 9) swells for about 40 seconds and then shows a steady falling in level at higher flow rates of steam. The steam drum pressure (FIGURE 8) immediately begins to fall. Following these sudden increases, the steam mass-flow rates from the steam drum and the superheater (FIGURES 10 and 11) show slight declines because of the effect of the decrease in steam drum pressure. The superheater outlet pressure (FIGURE 10) acts in a similar fashion to the steam drum pressure, that is ,it shows a steady decline to a new steady state condition but it is slightly lower than the steam drum pressure because of system pressure drops. The superheated steam temperature and superheater wall temperature (FIGURES 5 and 6) both decline, although the latter temperature is slightly lower. The riser tube wall temperature (FIGURE 8) and steam drum liquid temperature (FIGURE 9) also decrease due to the throttle change. The superheated steam density (FIGURE 5) shows a rising characteristic to counteract the loss in superheater pressure and temperature and the gain in steam mass-flow rate from the steam drum (FIGURE 11). The riser and downcomer flow rates (FIGURE 7) are reduced to a lower value but steam quality (FIGURE 6) is increased to a higher value than previously to preserve the energy balance.

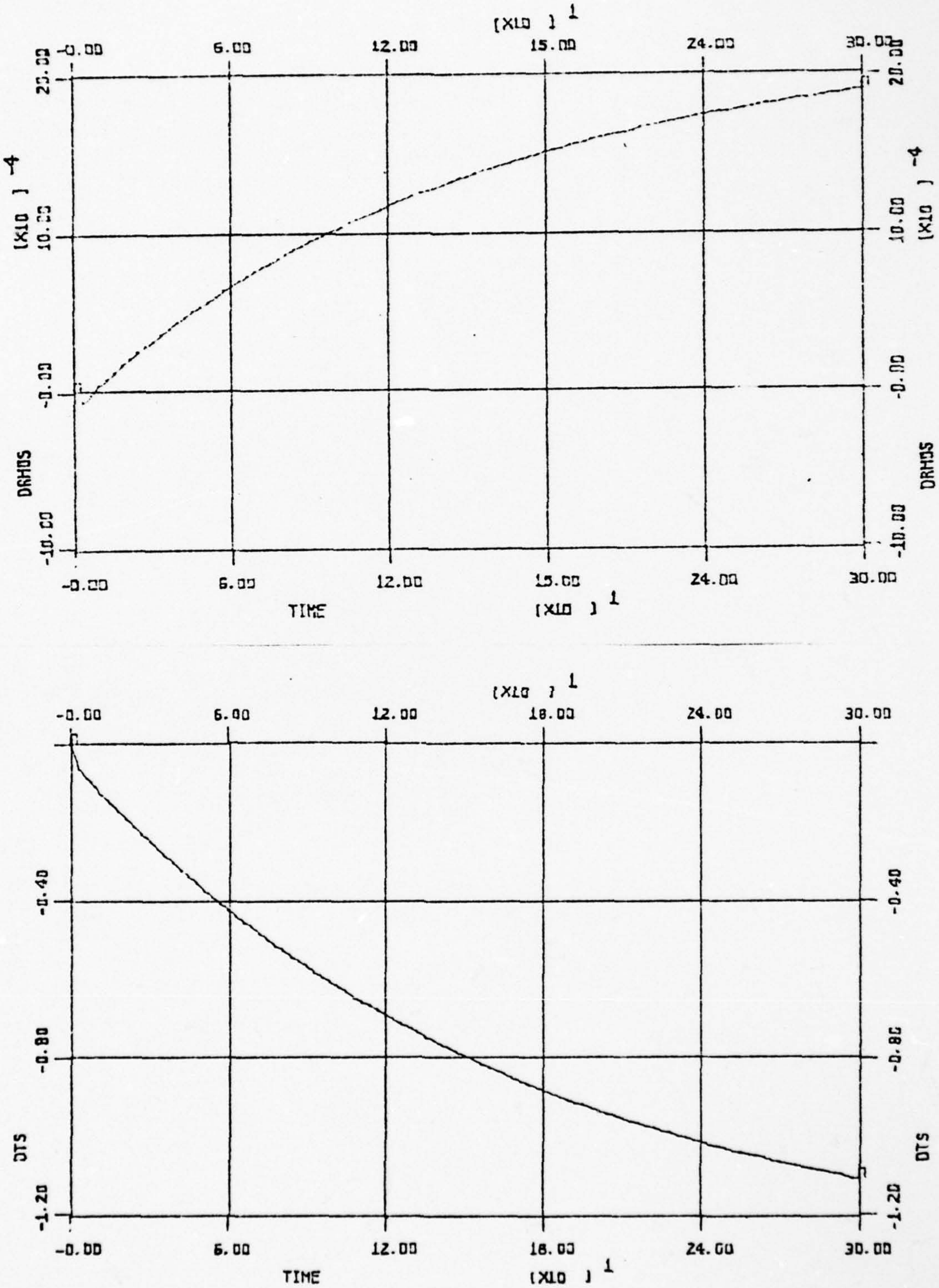


Figure 5 - SUPERHEATED STEAM DENSITY ($\Delta\rho_s$) VS TIME AND SUPERHEATED STEAM TEMPERATURE (ΔT_s) VS TIME

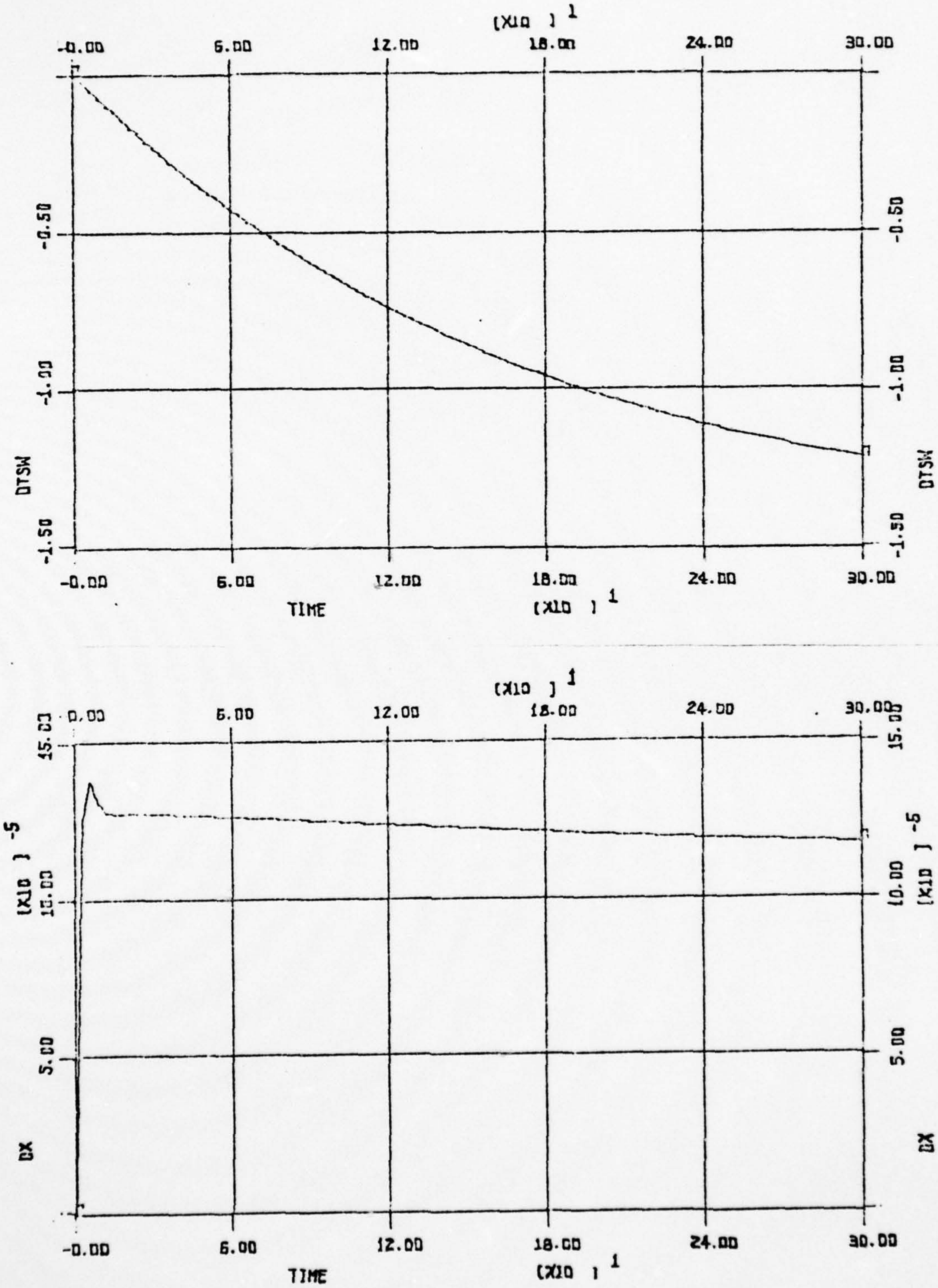


Figure 6 - SUPERHEATER WALL TEMPERATURE (ΔT_{SW}) VS TIME AND QUALITY OF MIXTURE LEAVING RISER (ΔX) VS TIME

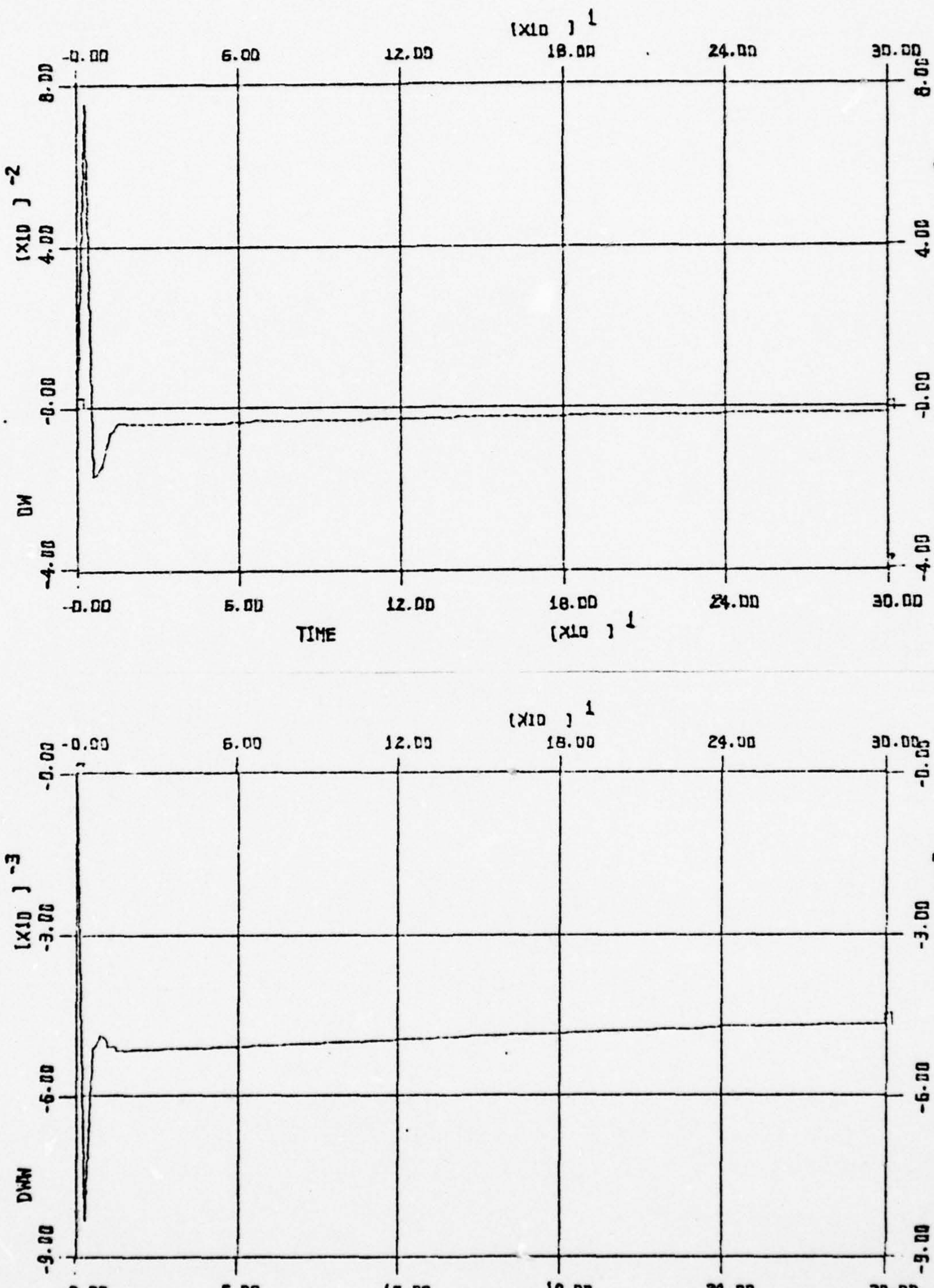
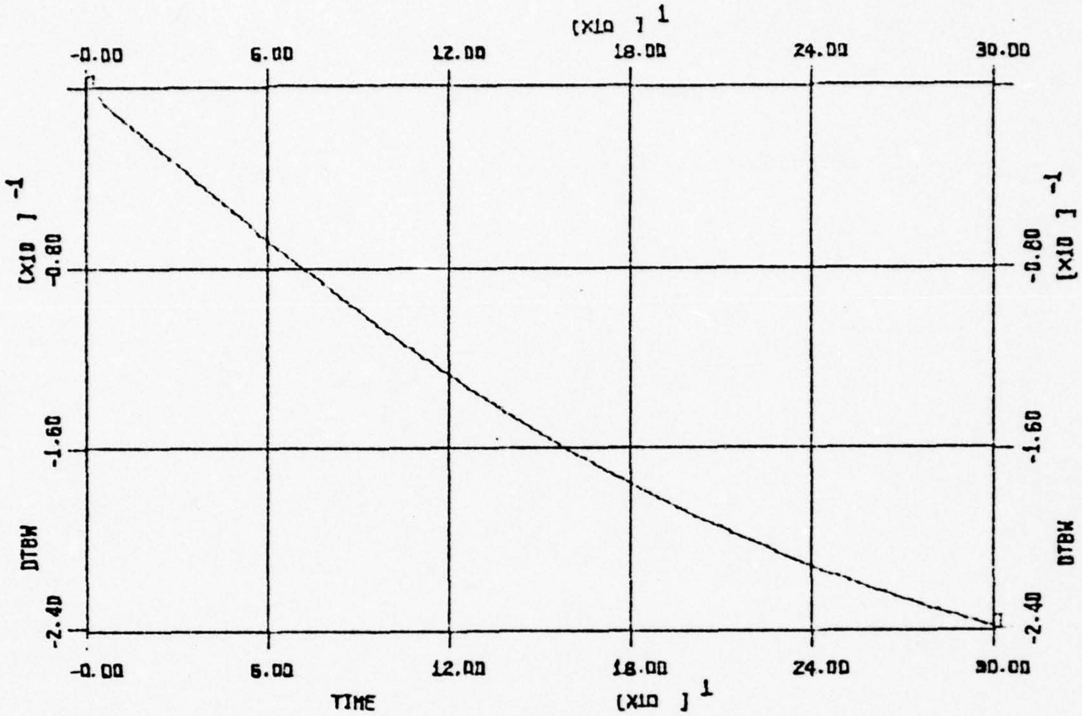


Figure 7 - RISER MIXTURE FLOW RATE (ΔW) VS TIME AND DOWNCOMER LIQUID FLOW RATE (ΔW_w) VS TIME



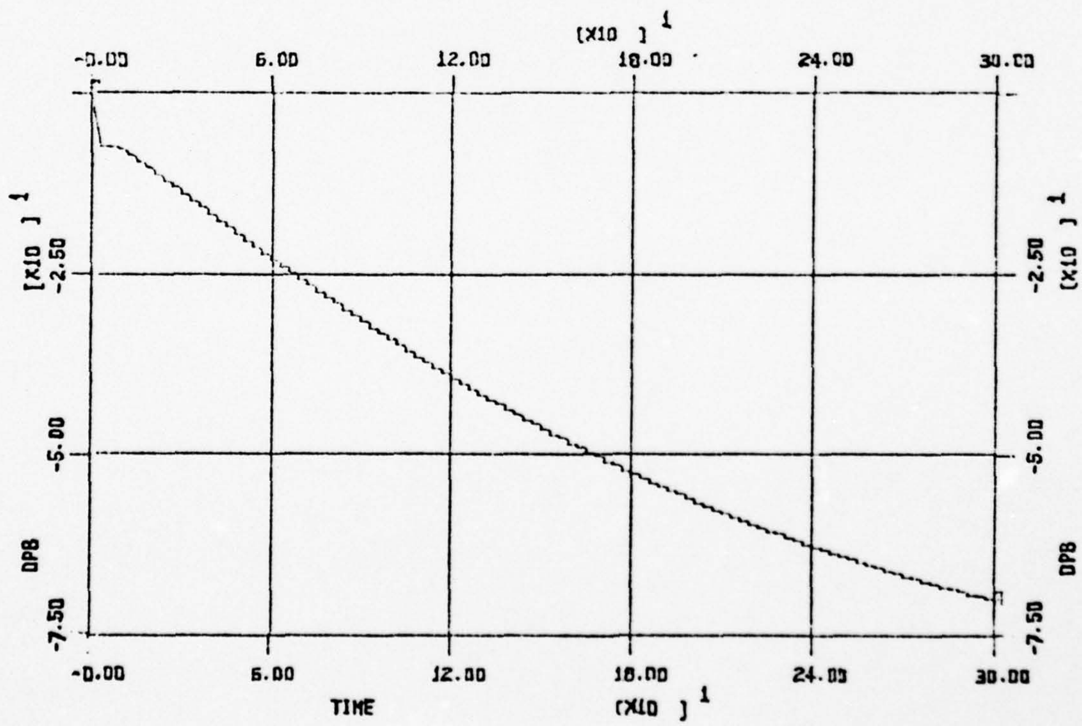


Figure 8 - RISER TUBE WALL TEMPERATURE (ΔT_{BW}) VS TIME AND STEAM DRUM PRESSURE (ΔP_B) VS TIME

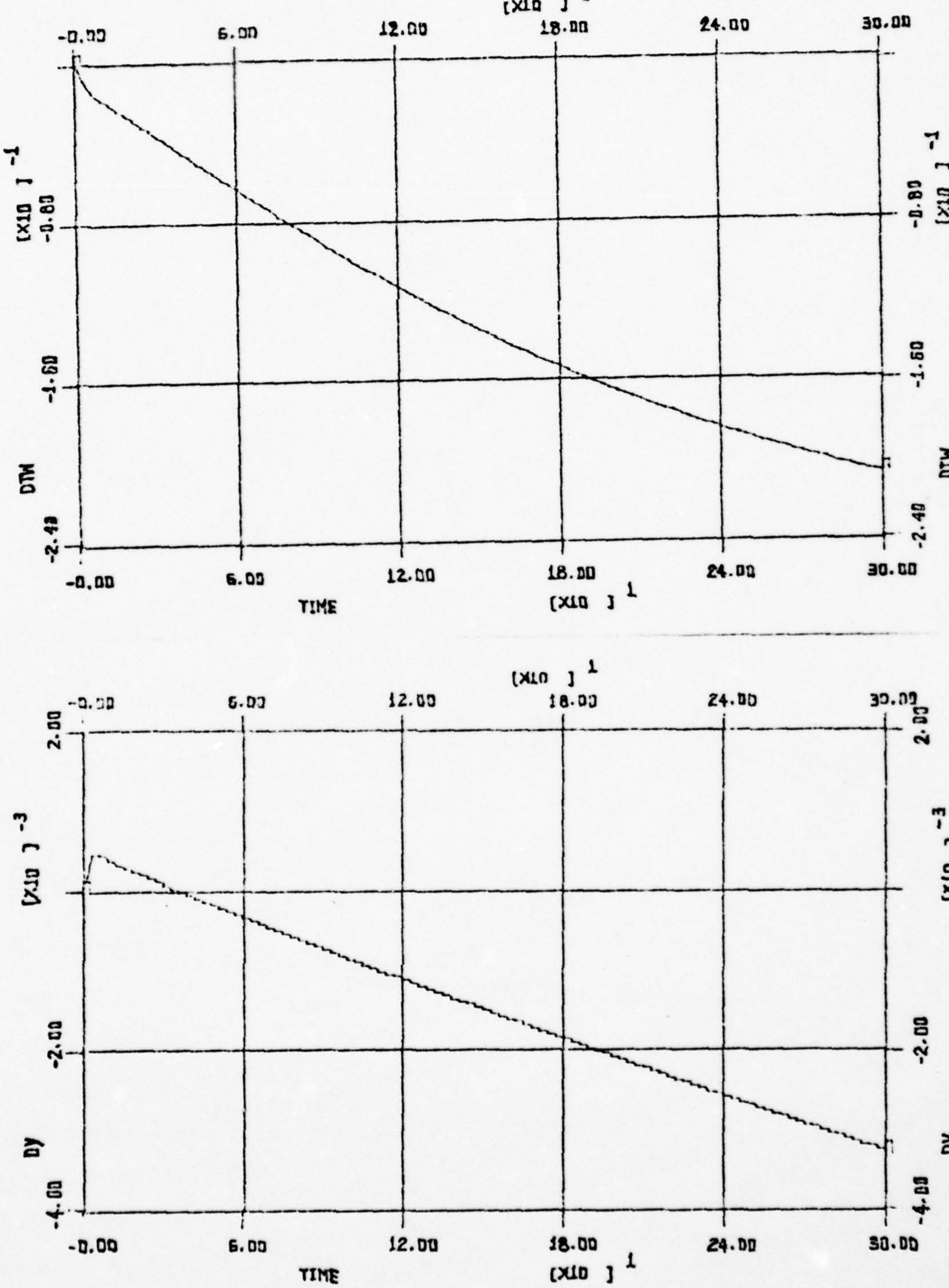
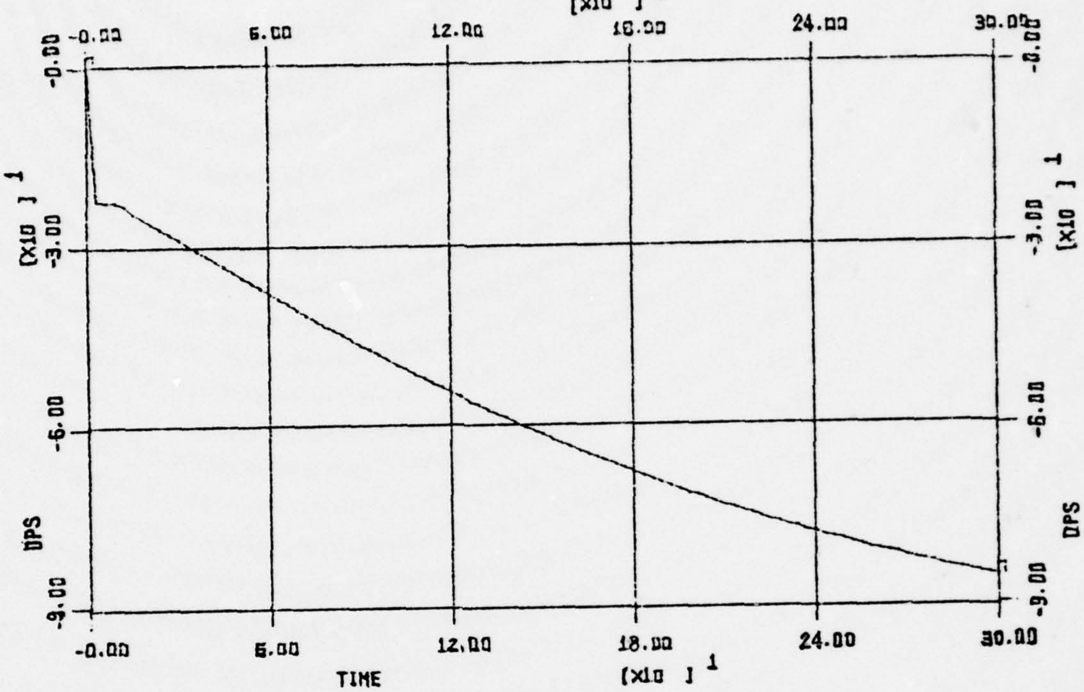


Figure 9 - STEAM DRUM LIQUID TEMPERATURE (ΔT_W) VS TIME AND STEAM DRUM WATER LEVEL (Δy) VS TIME



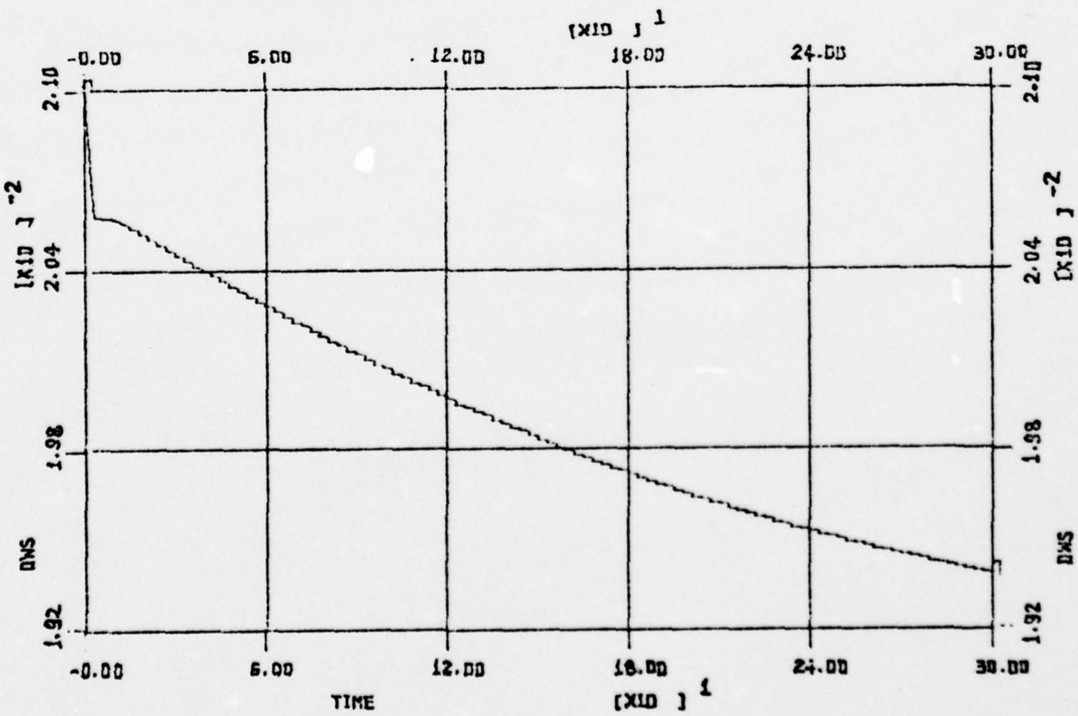


Figure 10 - SUPERHEATER OUTLET PRESSURE (ΔP_S) VS TIME AND STEAM FLOW RATE AT SUPERHEATER OUTLET (ΔW_S) VS TIME

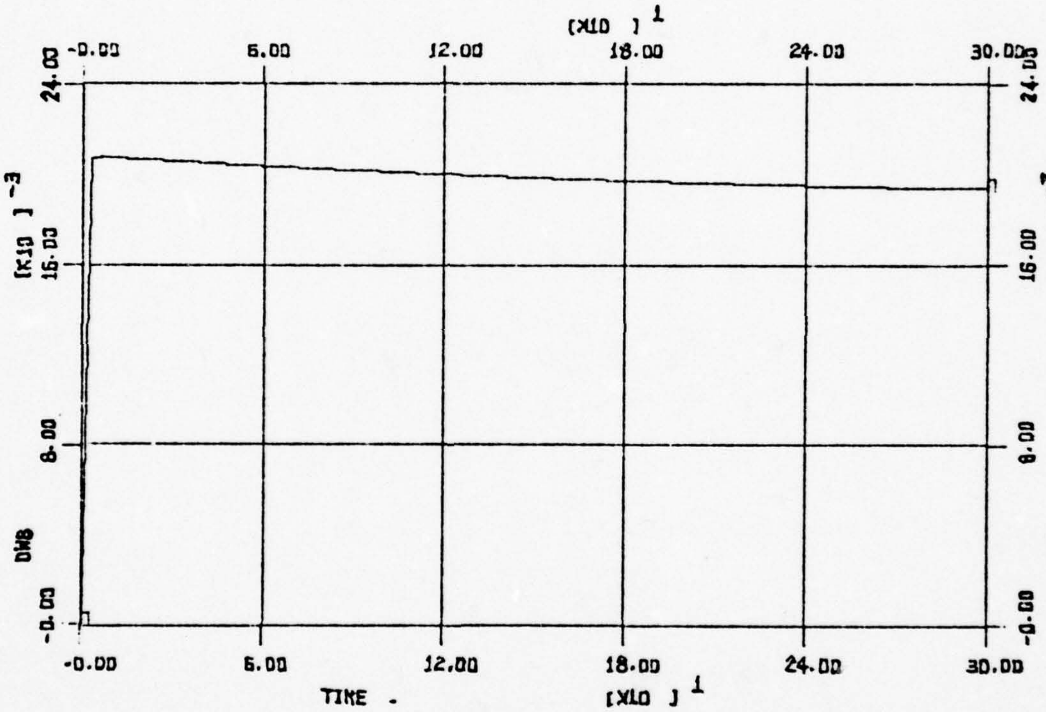
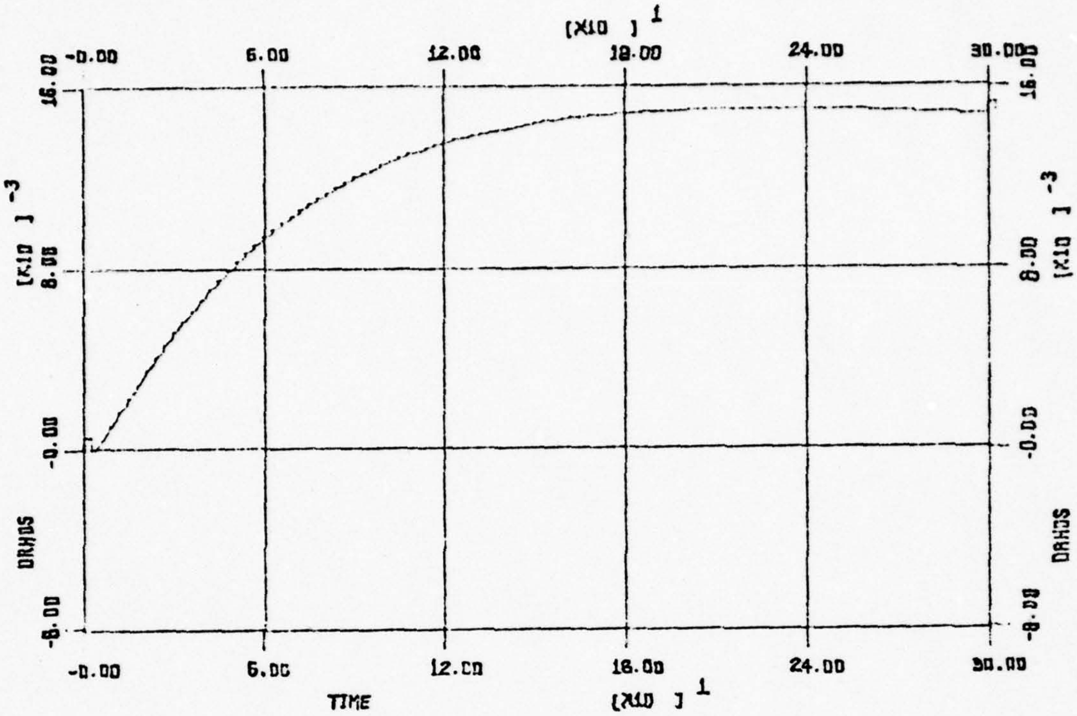


Figure 11 - STEAM MASS-FLOW RATE FROM STEAM DRUM TO SUPERHEATER (ΔW_8) VS TIME

B. TRANSIENT RESPONSES FOLLOWING A STEP CHANGE OF 10% IN FUEL FLOW RATE.

The effects due to a change in the fuel flow rate are less than those due to a change in the throttle valve setting. However,the system requires a longer period of time to reach a new steady state condition. Because the combustion rate is increased, the evaporation rate is also increased making both the steam mass-flow rate at the superheater (FIGURE 17) and the steam mass-flow rate from the steam drum (FIGURE 18) increase in a similar manner. Initially, density in the risers falls quickly in response to the increased firing rate which causes a rise in superheated steam density (FIGURE 12). An increase in steam flow from the steam drum without an increase in the feedwater flow rate results in a drop in steam drum water level (FIGURE 16).The steam drum pressure (FIGURE 15) and superheater outlet pressure (FIGURE 17) rise monotonically as time increases. Also superheated steam temperature (FIGURE 12) , superheater wall temperature (FIGURE 13) , riser tube wall temperature (FIGURE 15) and steam drum liquid temperature (FIGURE 16) all increase with increasing fuel flow rate. The abrupt fall in riser mixture flow rate (FIGURE 14) is probably due to the sudden drop in the level of the initial density change in the riser.



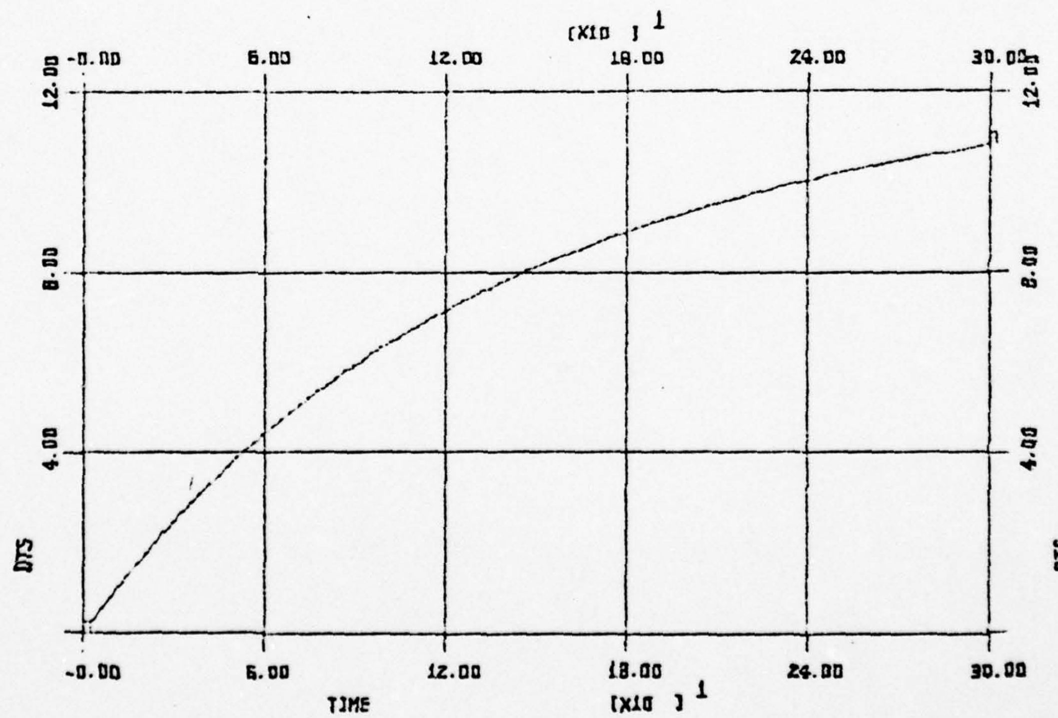


Figure 12 - SUPERHEATED STEAM DENSITY ($\Delta\rho_S$) VS TIME AND SUPERHEATED STEAM TEMPERATURE (ΔT_S) VS TIME

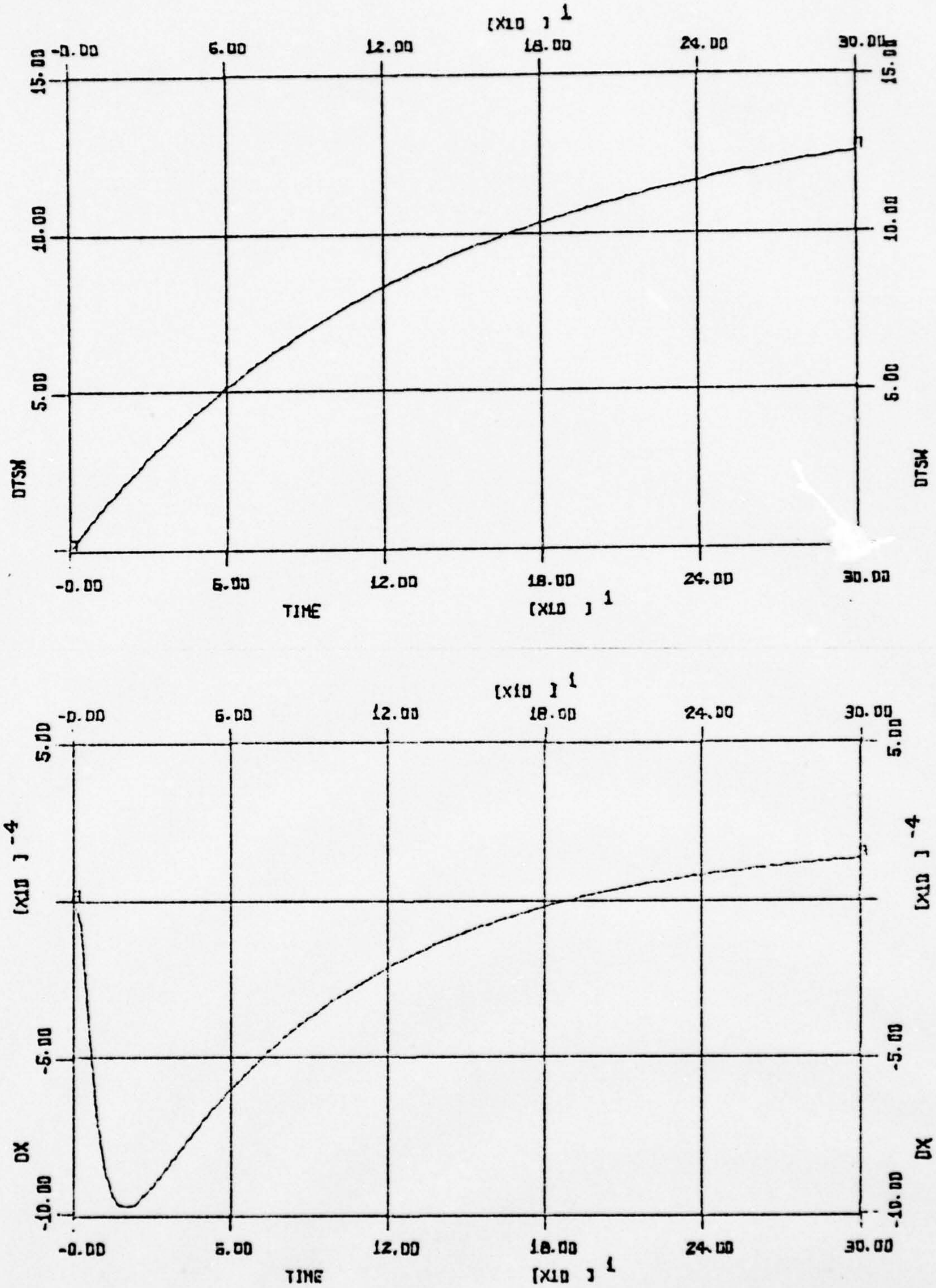


Figure 13 - SUPERHEATER WALL TEMPERATURE (ΔT_{SW}) VS TIME AND QUALITY OF MIXTURE LEAVING RISER (ΔX) VS TIME

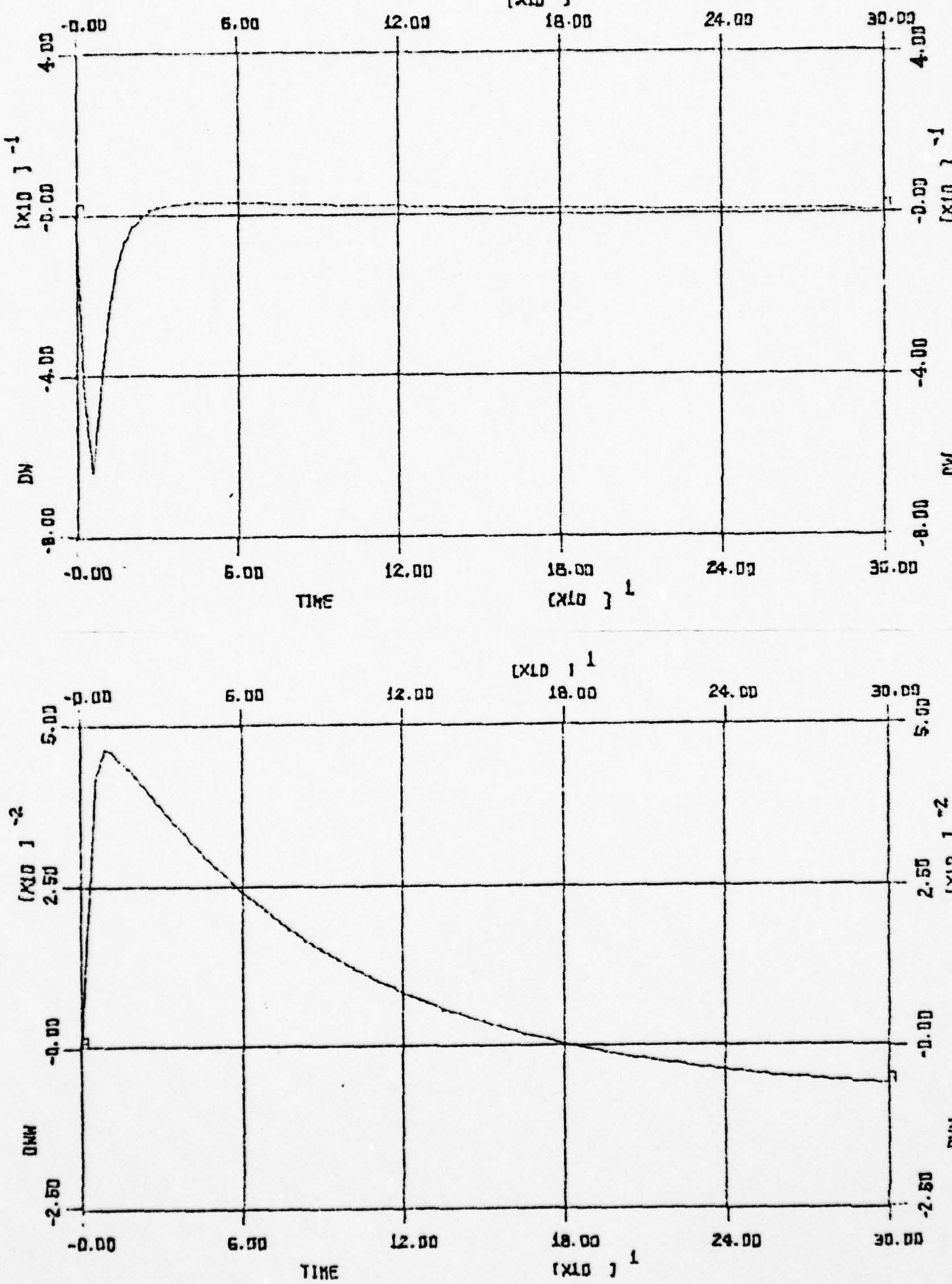


Figure 14 - RISER MIXTURE FLOW RATE (ΔW) VS TIME AND DOWNCOMER LIQUID FLOW RATE (ΔW_w) VS TIME

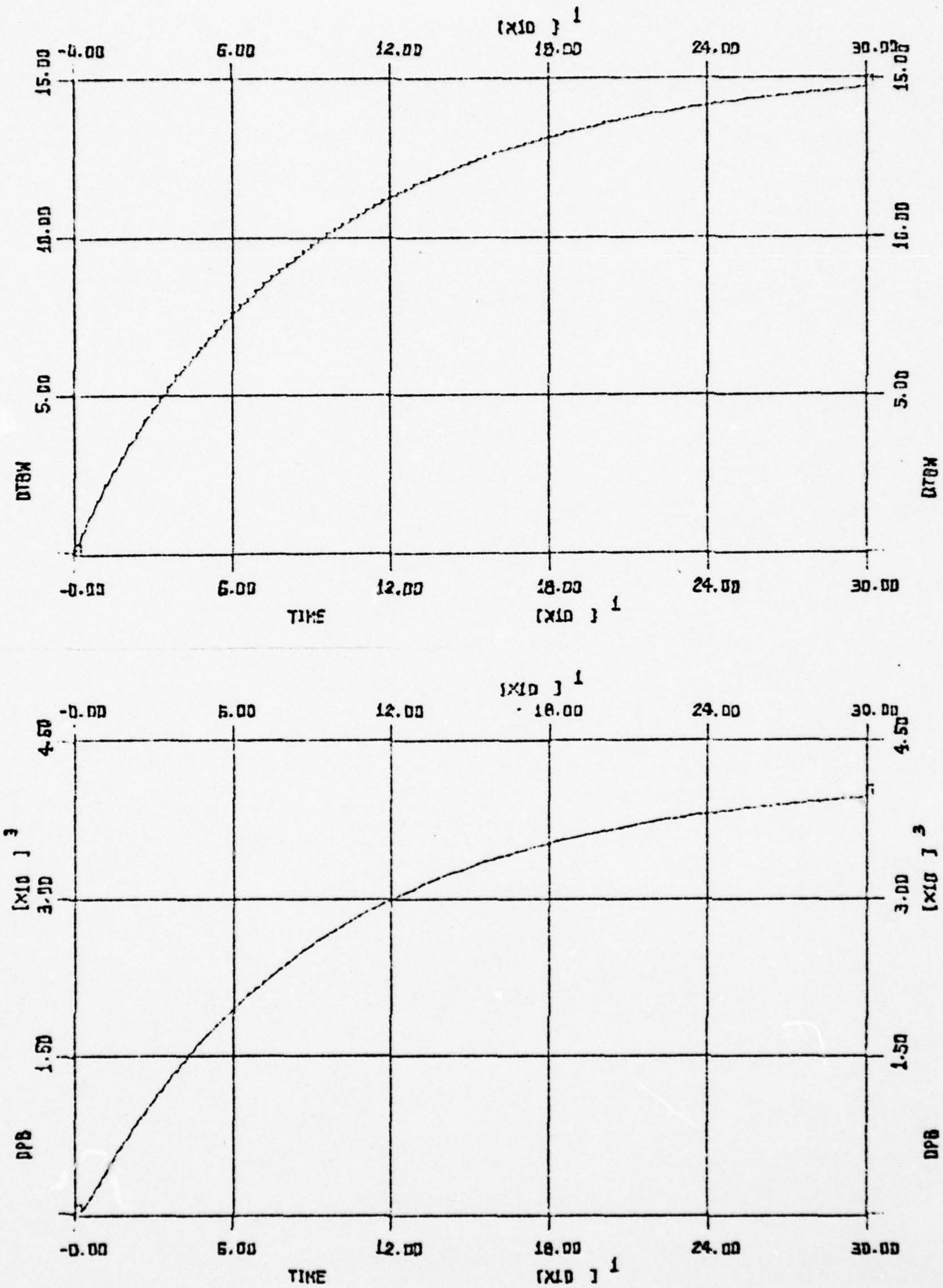


Figure 15 - RISER TUBE WALL TEMPERATURE (ΔT_{BW}) VS TIME AND STEAM DRUM PRESSURE (ΔP_B) VS TIME

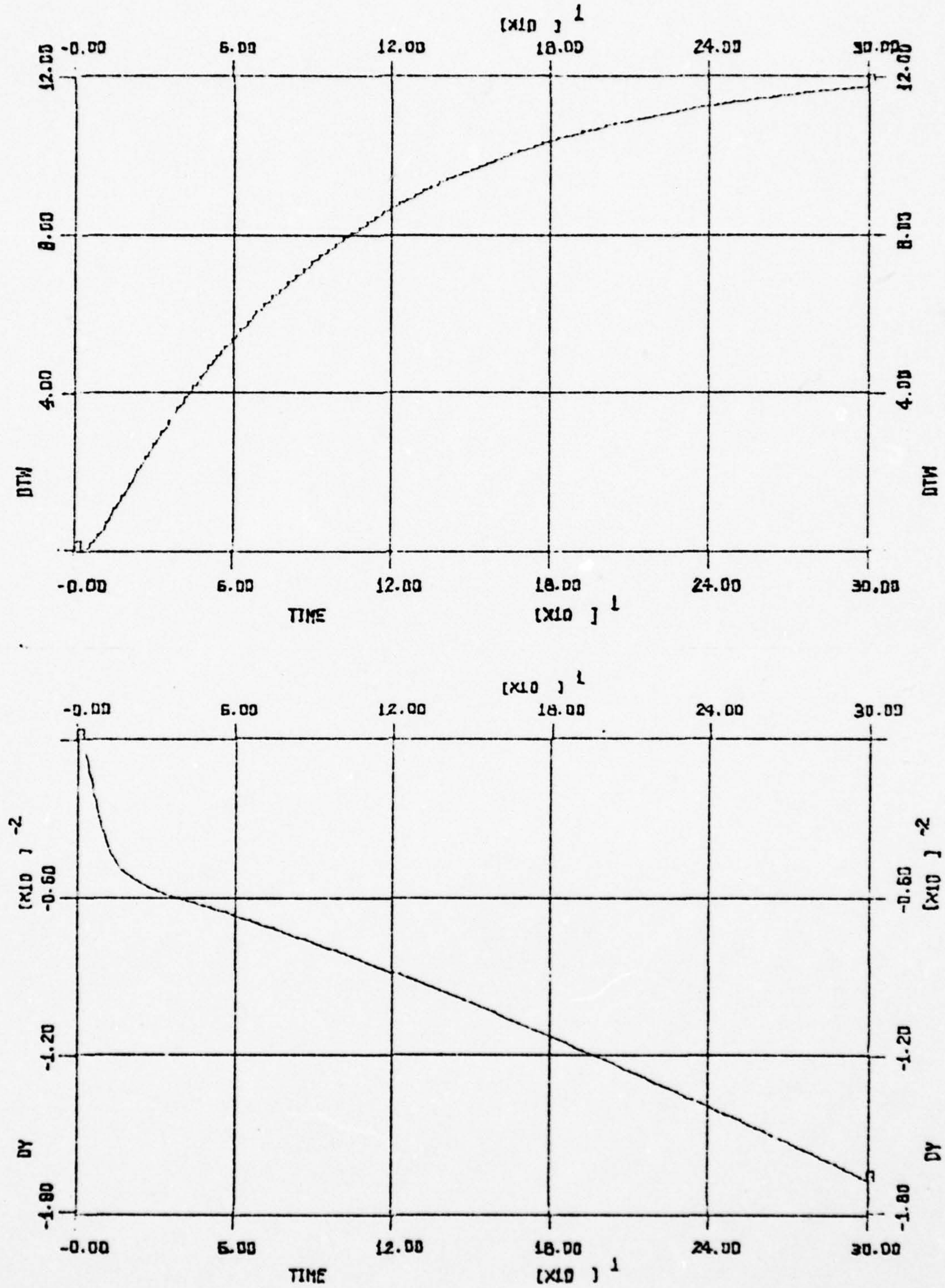
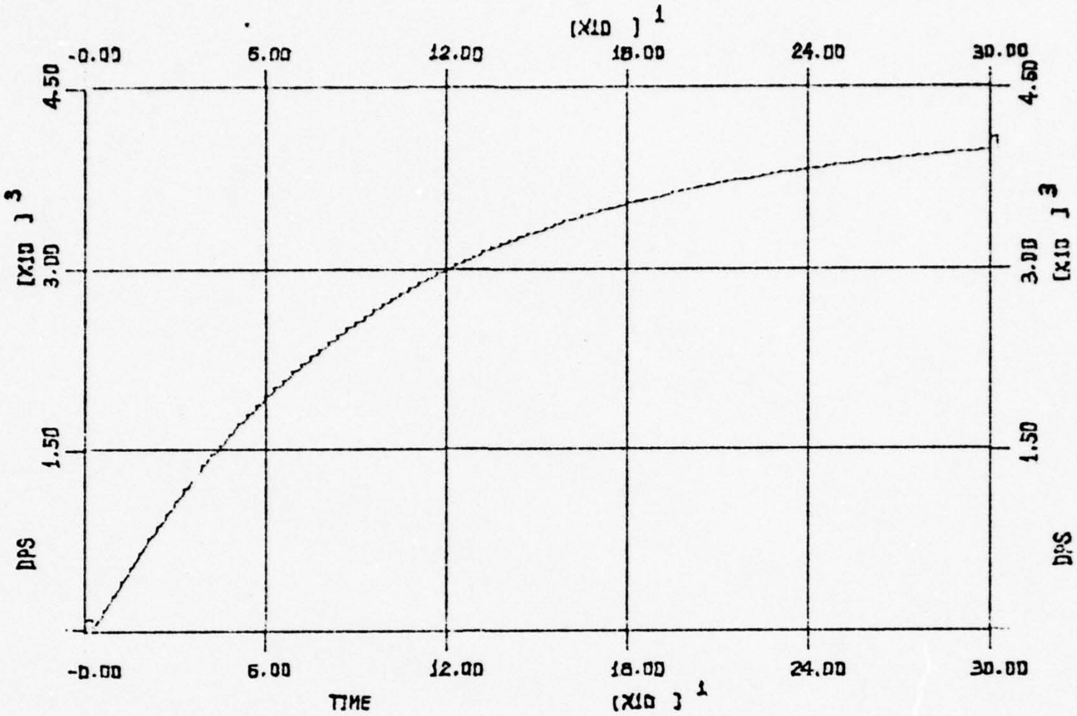


Figure 16 - STEAM DRUM LIQUID TEMPERATURE (ΔT_W) VS TIME AND STEAM DRUM WATER LEVEL (Δy) VS TIME



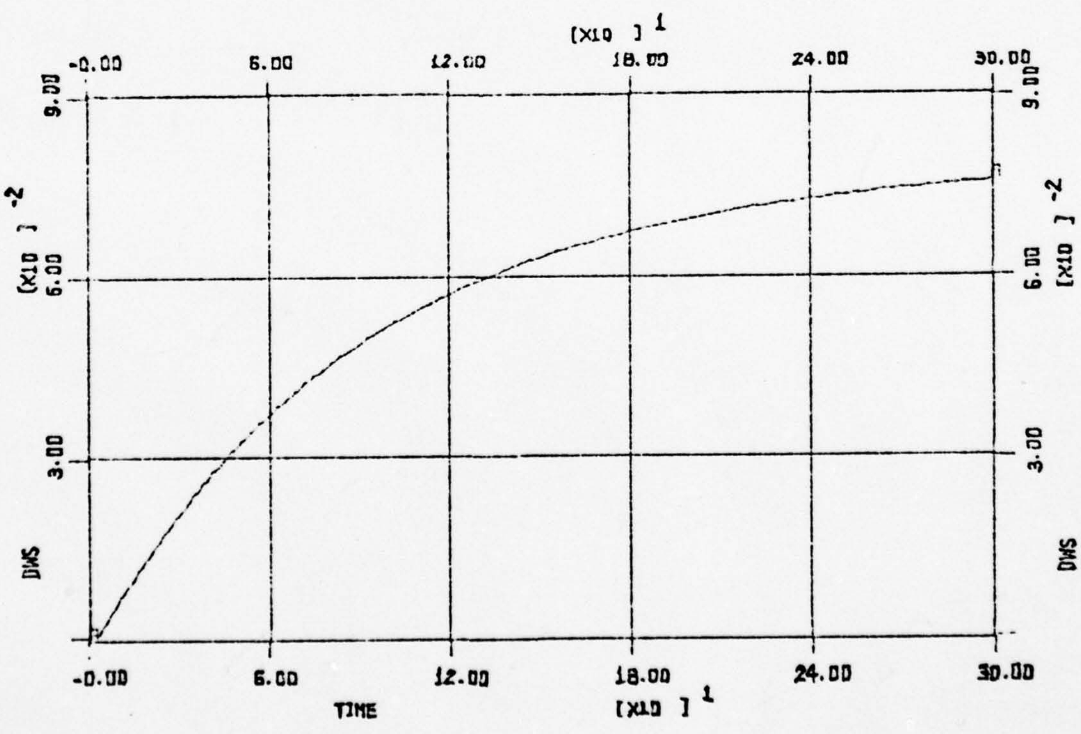


Figure 17 - SUPERHEATER OUTLET PRESSURE (ΔP_S) VS TIME AND STEAM FLOW RATE AT SUPERHEATER OUTLET (ΔW_S) VS TIME

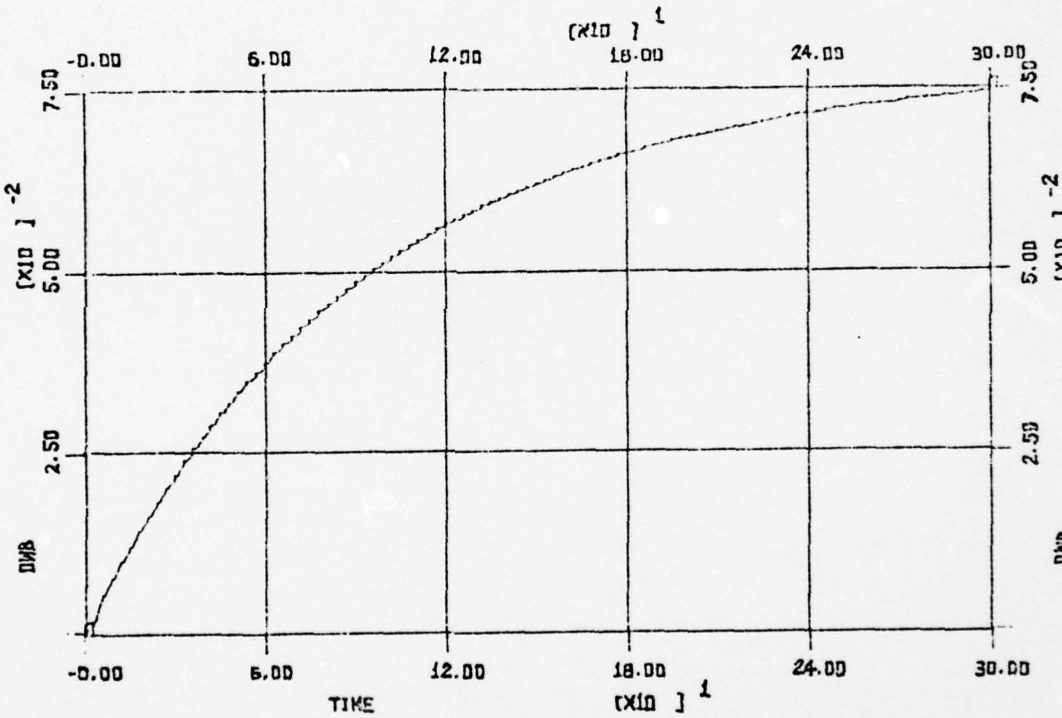


Figure 18 - STEAM MASS-FLOW RATE FROM STEAM DRUM TO SUPERHEATER (ΔW_B) VS TIME

C. TRANSIENT RESPONSES FOLLOWING A STEP CHANGE OF 10% IN FEEDWATER FLOW-RATE

The main effect of increasing feedwater flow rate while maintaining throttle setting and air-fuel flow rate constant is an increase in the steam drum water level (FIGURE23). Because feedwater is added into the steam drum, steam drum pressure (FIGURE22) suffers a small overshoot followed by a decline. As a result, a drop in both steam mass-flow rate from the steam drum (FIGURE25) and steam mass-flow rate at the superheater outlet (FIGURE24) occurs.Flow around the riser-downcomer loop (FIGURE21) is only slightly affected. Since the firing rate is unaltered,the riser tube wall temperature (FIGURE 22) and the steam drum liquid temperature (FIGURE23) decline. The superheated steam temperature (FIGURE19) and the superheater wall temperature (FIGURE20) rise because of a drop in steam mass-flow rate from the steam drum.The quality of steam (FIGURE20) shows a general lowering. The superheated steam density (FIGURE19) shows a decline which is similar in form to the drop in the superheater outlet pressure.

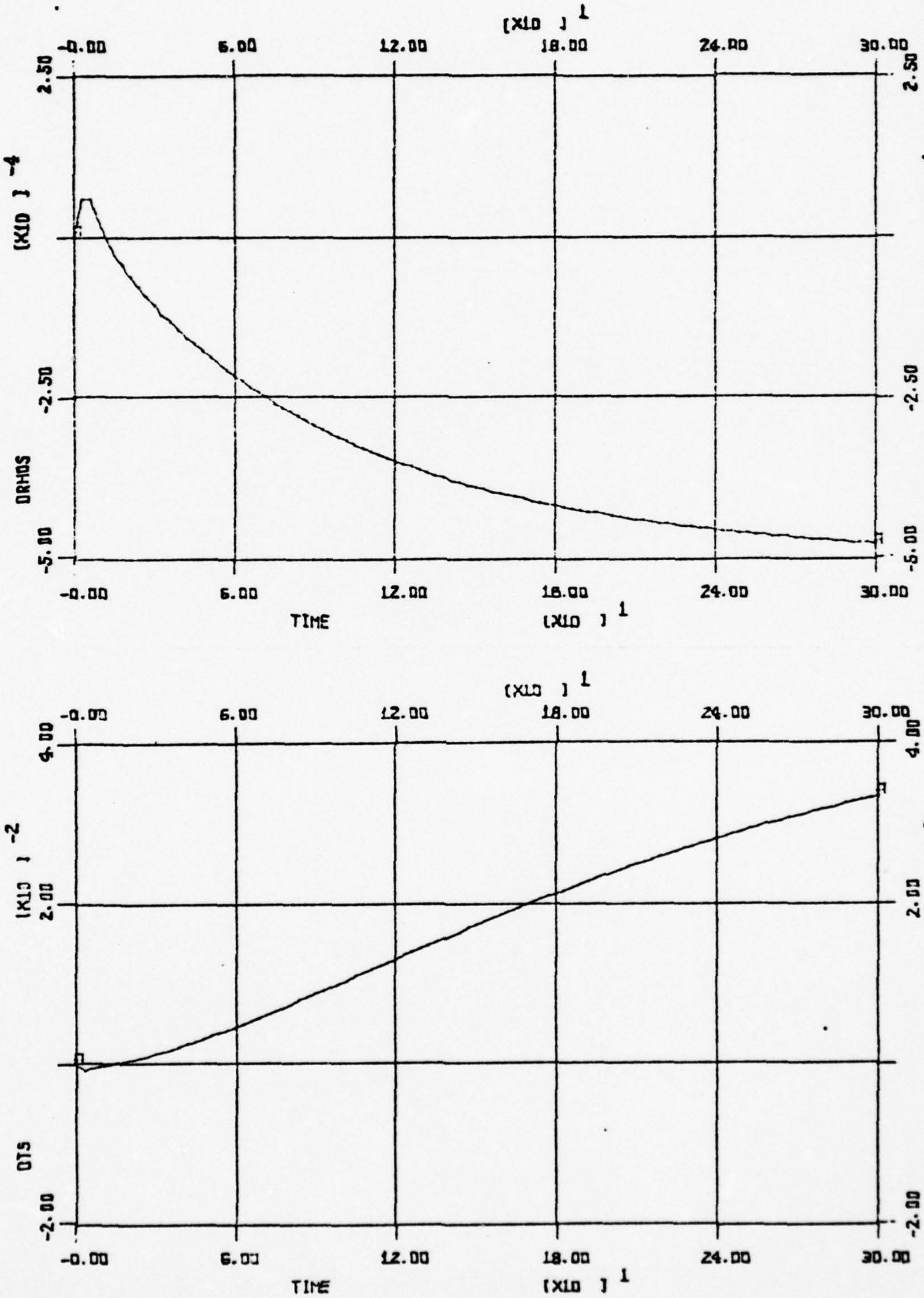
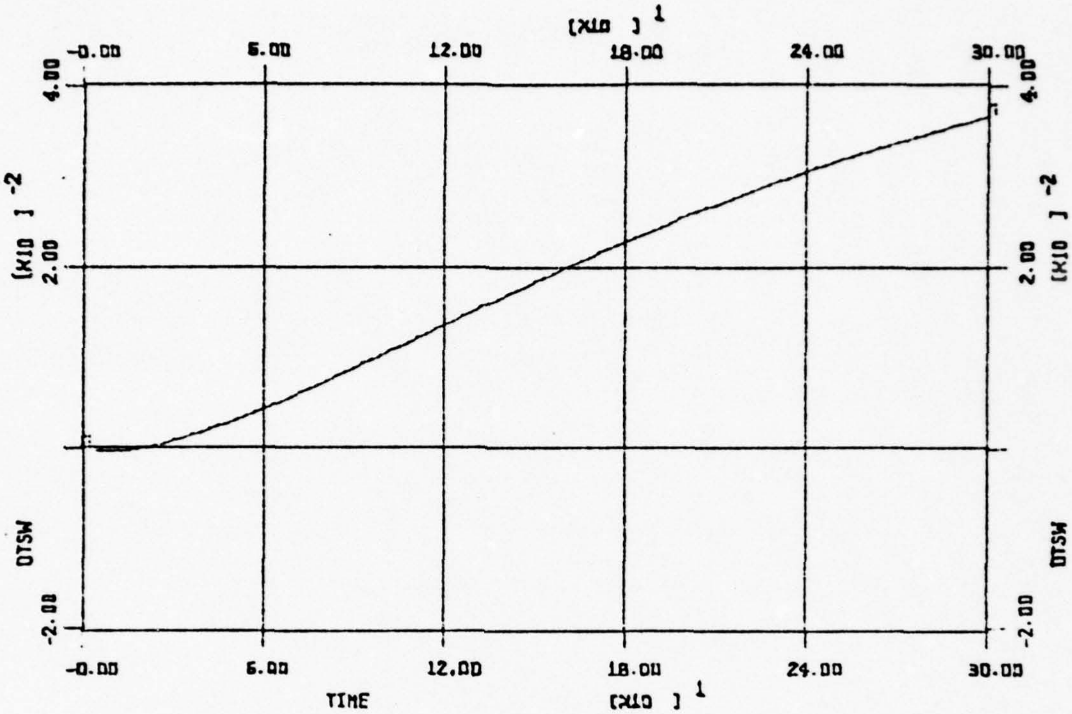


Figure 19 - SUPERHEATED STEAM DENSITY ($\Delta\rho_S$) VS TIME AND SUPERHEATED STEAM TEMPERATURE (ΔT_S) VS TIME



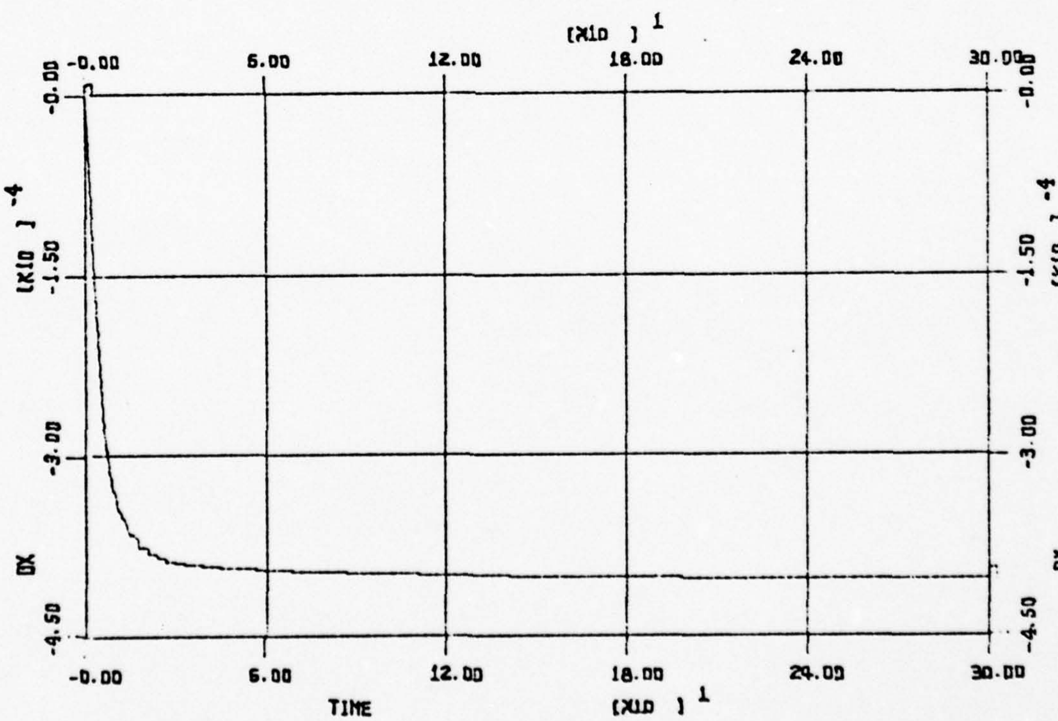


Figure 20 - SUPERHEATER WALL TEMPERATURE (ΔT_{SW}) VS TIME AND QUALITY OF MIXTURE LEAVING RISER (ΔX) VS TIME

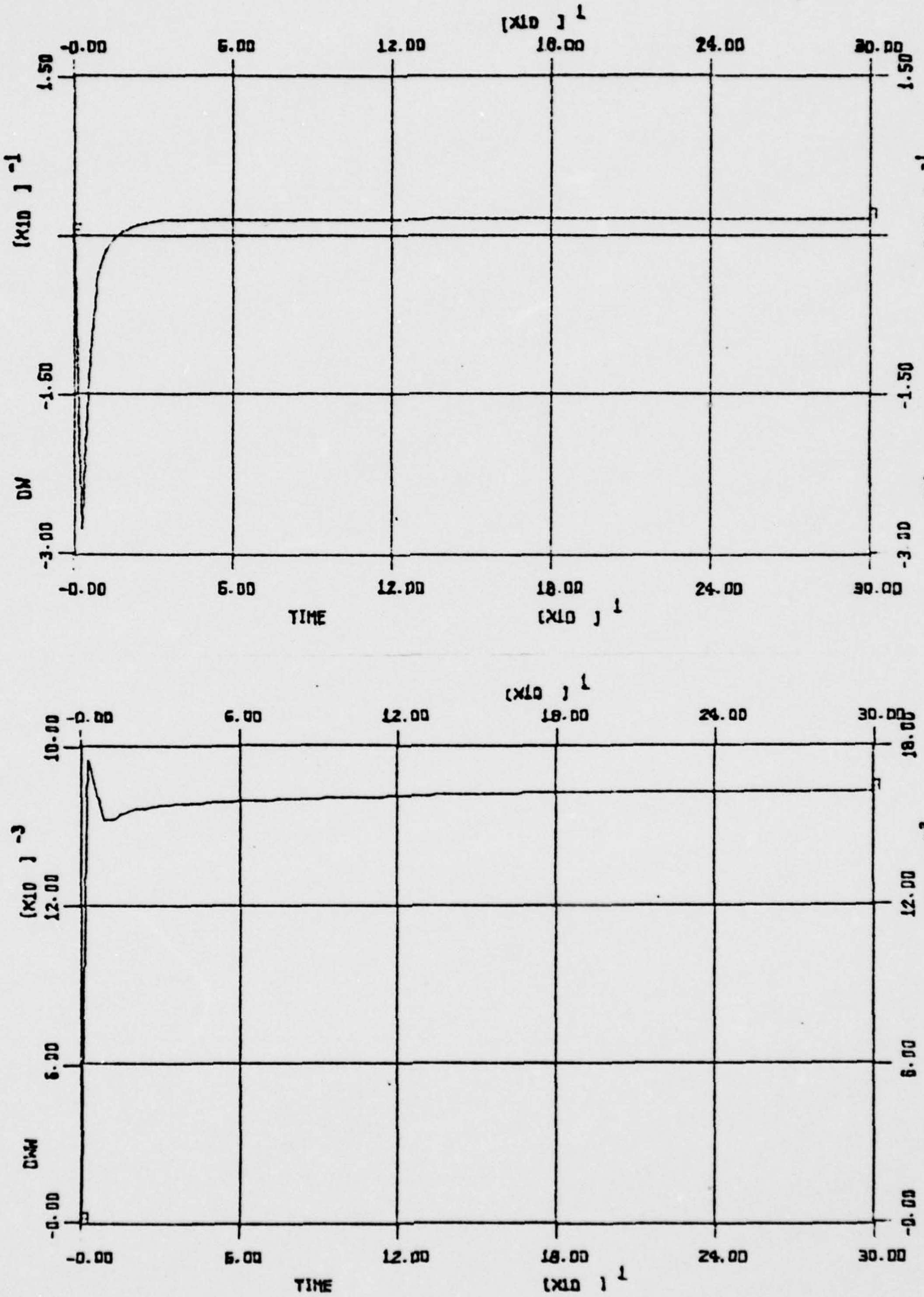


Figure 21 - RISER MIXTURE FLOW RATE (ΔW) VS TIME AND DOWNCOMER LIQUID FLOW RATE (ΔW_W) VS TIME

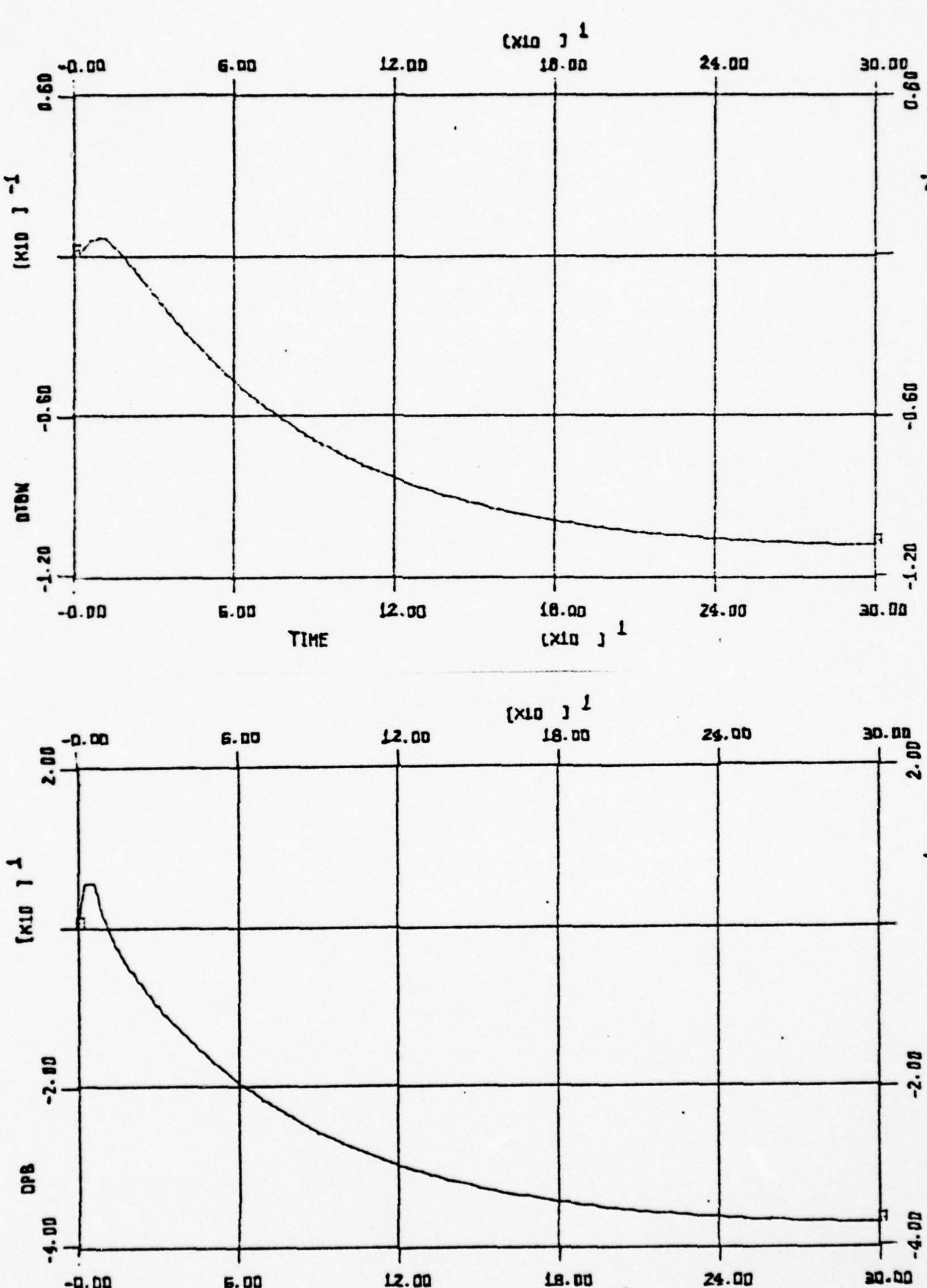


Figure 22 - RISER TUBE WALL TEMPERATURE (ΔT_{BW}) VS TIME AND STEAM DRUM PRESSURE (ΔP_B) VS TIME

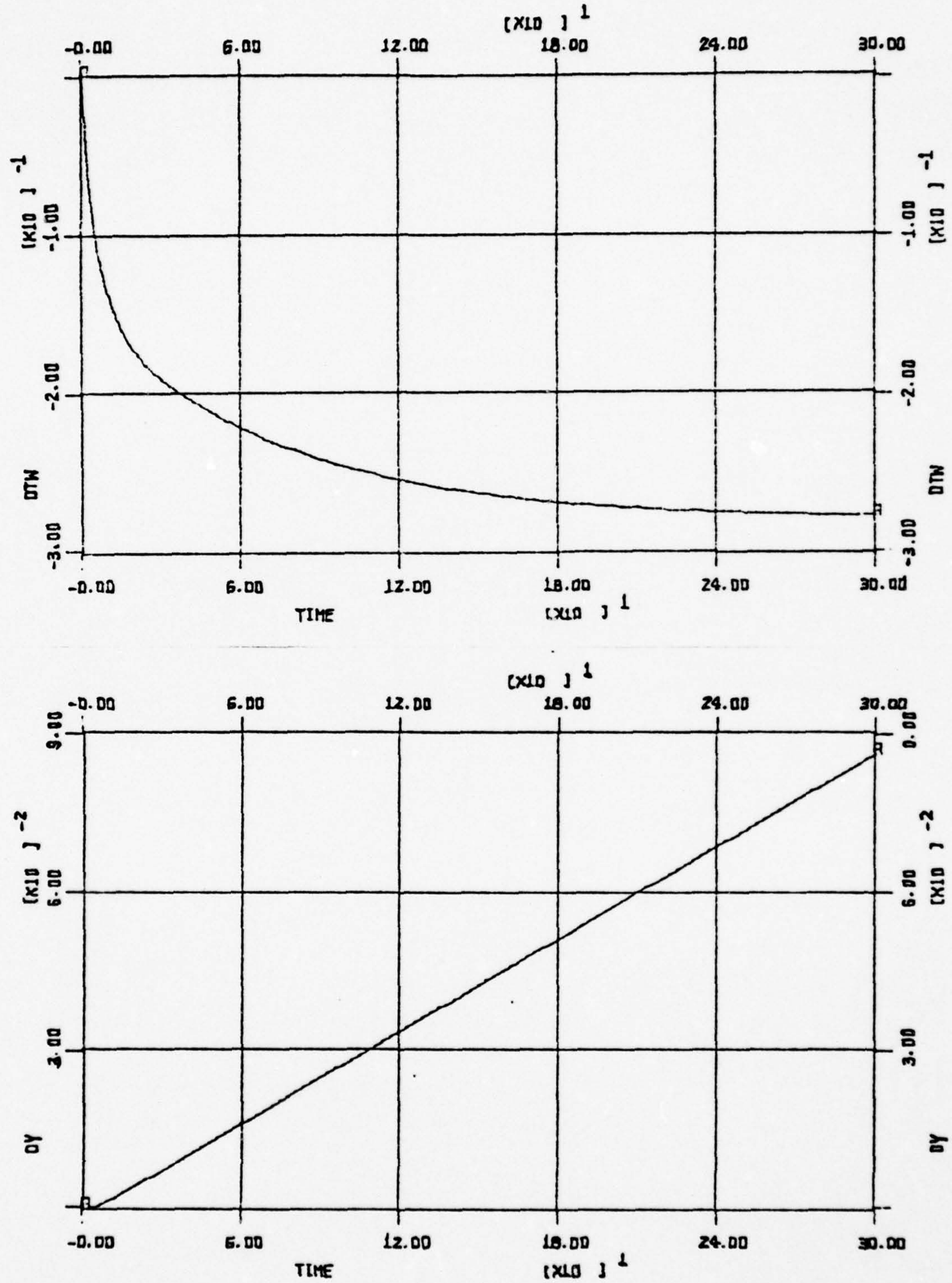
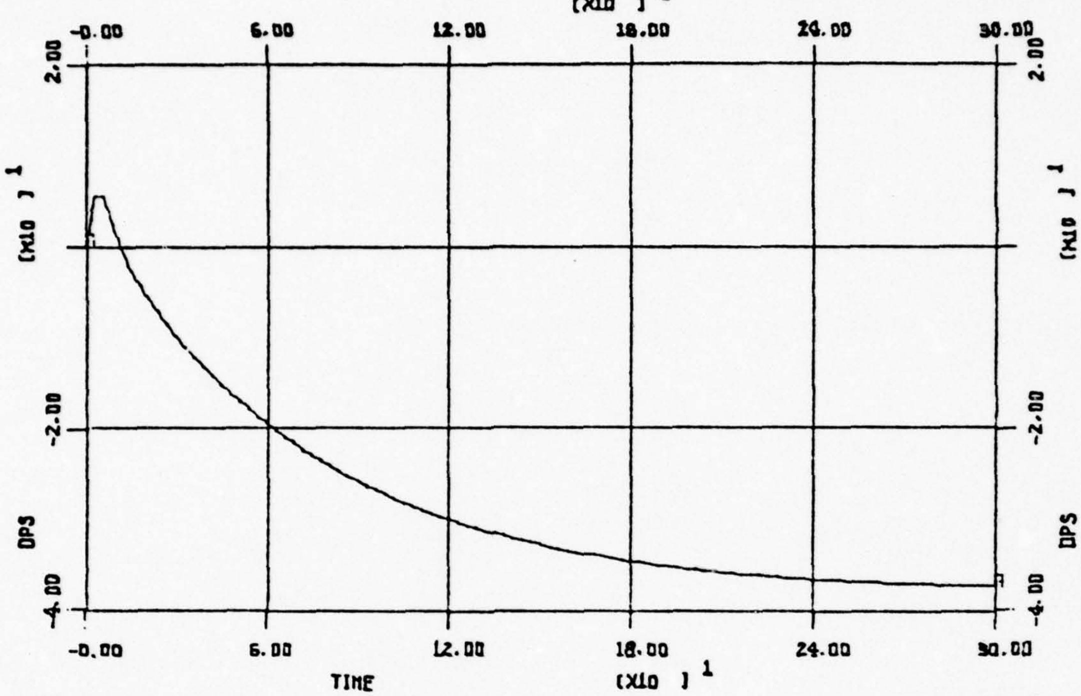


Figure 23 - STEAM DRUM LIQUID TEMPERATURE (ΔT_W) VS TIME AND STEAM DRUM WATER LEVEL (Δy) VS TIME



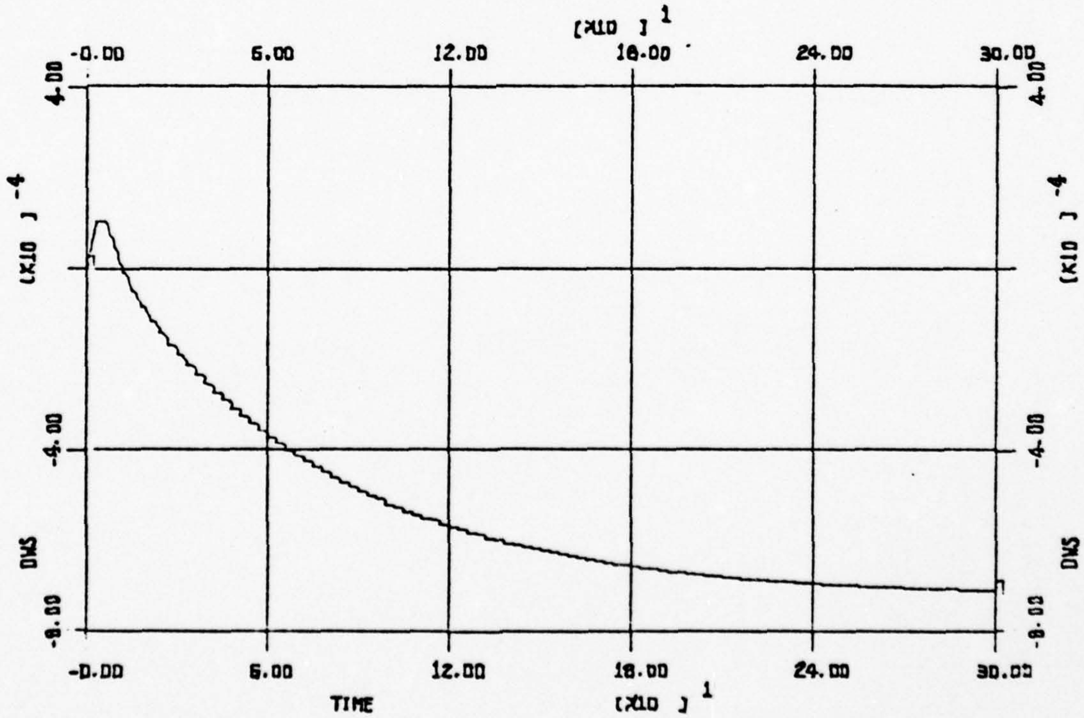


Figure 24 - SUPERHEATER OUTLET PRESSURE (ΔP_S) VS TIME AND STEAM FLOW RATE AT SUPERHEATER OUTLET (ΔW_S) VS TIME

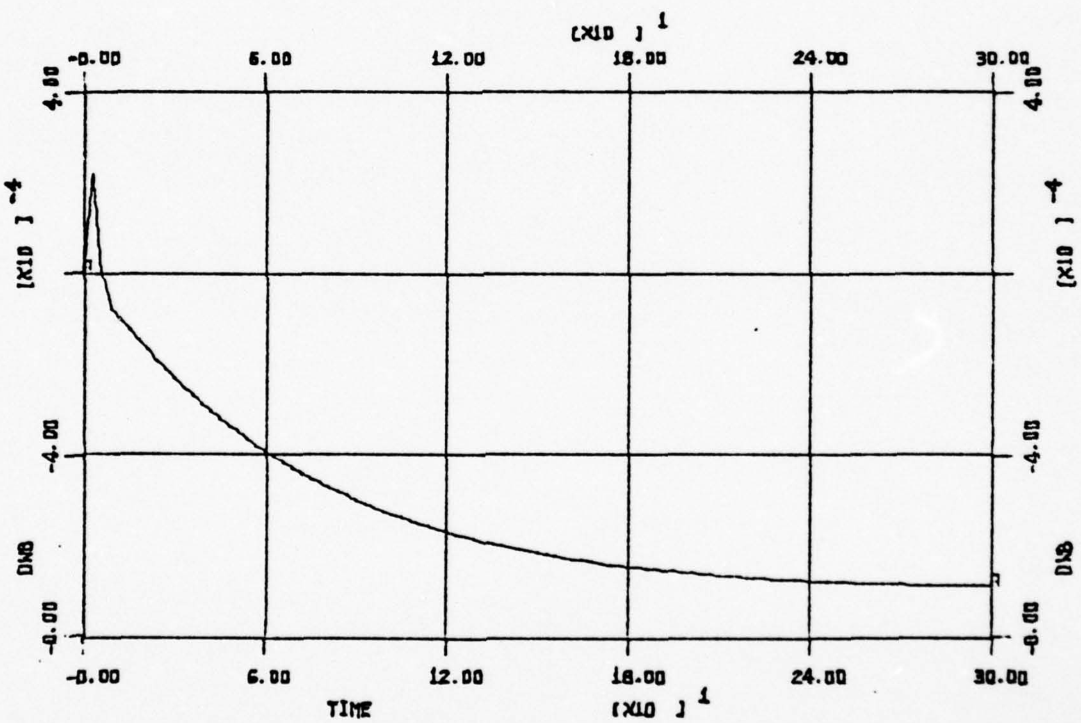


Figure 25 - STEAM MASS-FLOW RATE FROM STEAM DRUM TO SUPERHEATER (ΔW_B) VS TIME

IV. CONCLUSIONS

This analysis is only the initial step toward a better understanding of a naval steam generating plant both from the dynamic and from the control points of view. The analysis concerns a boiler system which is divided into four parts. The major difficulty in the analysis is the fact that the whole system is very complex and contains numerous variables which are extremely unwieldy to manipulate. Large numbers of relationships are non-linear so it is necessary to generate a linear form by the methods of perturbation theory. After setting up the state variable equations, the IBM simulation language CSMP-III was used to solve for the open loop transient response characteristics of the state variables due to variations in input variables. Throughout these calculations, all the variables appearing in the transient response curves are not absolute values. Rather, they represent a small incremental change from some particular steady state operating condition. Also, it is to be noted that trends in some of these results differ markedly in form from those appearing in Whalley (2). Future studies will be undertaken to determine the causes of these differences. Meanwhile, the benefit one may derive from this basic analysis is its use in the design and construction of a new type of boiler controller, that is, a multivariable control system.

APPENDIX A

LIST OF COEFFICIENTS A

$a_1 = 1$

$a_2 = -1$

$a_3 = L_S A_S \bar{\rho}_s C_{ps}$

$a_4 = L_S A_S$

$a_5 = \bar{h}_S - \bar{h}_B$

$a_6 = -1$

$a_7 = -\bar{W}_S C_{ps}$

$a_8 = 1$

$a_9 = -1$

$a_{10} = M_S C_S$

$a_{11} = 1$

$$a_{12} = \frac{0.6\, K_{gs}}{\bar{W}_f^{0.4}} (\bar{T}_{gs} - \bar{T}_{sw})$$

$$a_{13} = K_{gs}\, \bar{W}_f^{0.6}$$

$$a_{14} = 2\, K_{as} \frac{(\bar{W}_{ac} - \bar{W}_a)}{\bar{W}_{ac}^2}$$

$$a_{15} = 1$$

$$a_{16} = \frac{0.8\, K_S}{\bar{W}_B^{0.2}} (\bar{T}_{sw} - \bar{T}_S)$$

$$a_{17} = K_S\, \bar{W}_B^{0.8}$$

$$a_{18} = \frac{1}{2C_c}$$

$$a_{19} = (\bar{W}_f + \bar{W}_a)$$

$$a_{20} = (\bar{T}_C - \bar{T}_{gS})$$

$$a_{21} = (\bar{T}_C - \bar{T}_{gS})$$

$$a_{22} = -(\bar{W}_f + \bar{W}_a)$$

$$a_{23} = 2f_s \frac{\bar{W}_B^2}{\bar{\rho}_B^2}$$

$$a_{24} = 1$$

$$a_{25} = -f_s \frac{\bar{W}_B^2}{\bar{\rho}_B^2}$$

$$a_{26} = 1$$

$$a_{27} = 0.5 A_r L_r \bar{\rho}^2 \left(\frac{1}{\bar{\rho}_W} - \frac{1}{\bar{\rho}_B} \right)$$

$$a_{28} = 0.5 A_r L_r \bar{X} K_B \left(\frac{\bar{\rho}^2}{\bar{\rho}_B^2} \right)$$

$$a_{29} = 0.5 (\bar{\rho} + \bar{\rho}_W) C$$

$$a_{30} = 1$$

$$a_{31} = -1$$

$$a_{32} = 1$$

$$a_{33} = -1$$

$$a_{34} = \frac{2\bar{W}}{g A_r^2 \rho} \left(\frac{f_r L_r}{D_r} + \frac{3}{2} \right)$$

$$a_{35} = \frac{L_r}{g A_r}$$

$$a_{36} = \left(\frac{1}{\bar{\rho}_B} - \frac{1}{\bar{\rho}_W} \right) \left[\frac{\bar{W}^2}{g A_r^2} \left(\frac{f_r L_r}{D_r} + \frac{3}{2} \right) - \bar{\rho}^2 L_r \right]$$

$$a_{37} = \frac{-2 \bar{W}_W}{g A_r^2 \bar{\rho}_W}$$

$$a_{38} = 1$$

$$a_{39} = -1$$

$$a_{40} = M_B C_B$$

$$a_{41} = 0.5 A_r L_r (\bar{\rho} + \bar{\rho}_W) K_c$$

$$a_{42} = 0.5 A_r L_r (\bar{\rho} + \bar{\rho}_W) \bar{h}_{fg}$$

$$a_{43} = -1$$

$$a_{44} = (\bar{h}_{WD} - \bar{h})$$

$$a_{45} = -\bar{W} K_C$$

$$a_{46} = -\bar{W} \bar{h}_{fg}$$

$$a_{47} = \bar{W}_W$$

$$a_{48} = 1$$

$$a_{49} = -K_{gB} \bar{W}_f^{0.6} - 4 K_r \bar{T}_{gB}^3$$

$$a_{50} = -K_{gB} \bar{W}_f^{0.6} - 4 K_r \bar{T}_{BW}^3$$

$$a_{51} = \frac{0.6 K_{gB} (\bar{T}_{gB} - \bar{T}_{BW})}{\bar{W}_f^{0.4}}$$

$$a_{52} = \frac{2 K_{ar} (\bar{W}_{ac} - \bar{W}_a)}{\bar{W}_{ac}^2}$$

$$a_{53} = 1$$

$$a_{54} = 3K_g(\bar{T}_{BW} - \bar{T}_B)^2$$

$$a_{55} = -3K_g(\bar{T}_{BW} - \bar{T}_B)^2$$

$$a_{56} = 1$$

$$a_{57} = -1$$

$$a_{58} = b_W = \frac{2W_W}{g\bar{\rho}_W A_D^2}\left(\frac{f_D L_D}{D_D} + 0.5\right)$$

$$a_{59} = a_W = \frac{L_D}{g\,A_D}$$

$$a_{60} = \bar{V}_B K_B$$

$$a_{61} = -\bar{\rho}_B A$$

$$a_{62} = K_e$$

$$a_{63} = \bar{X}$$

$$a_{64} = \bar{W}$$

$$a_{65} = -1$$

$$a_{66} = (1-\bar{X})\bar{T}_B$$

$$a_{67} = (1-\bar{X})\bar{W}$$

$$a_{68} = -\bar{W}\bar{T}_B$$

$$a_{69} = \bar{T}_i$$

$$a_{70} = -\bar{W}_W$$

$$a_{71} = -\bar{T}_W$$

$$a_{72} = -\bar{W}_e K_C$$

$$a_{73} = -\bar{h}_{BW} K_e$$

$$a_{74} = \bar{M}$$

$$a_{75} = A\bar{\rho}_w \bar{T}_w$$

$$a_{76} = -K_e$$

$$a_{77} = A\bar{\rho}_w$$

$$a_{88} = (1-\bar{X})$$

$$a_{89} = -\bar{W}$$

$$a_{90} = -1$$

$$a_{91} = -k_e$$

$$a_{92} = 1$$

$$a_{93} = 1$$

$$a_{94} = \frac{\partial f_1}{\partial x_v}$$

$$a_{95} = \frac{\partial f_1}{\partial P_s}$$

$$a_{96} = \frac{\partial f_1}{\partial T_s}$$

$$a_{97} = K_T$$

$$a_{98} = K_B$$

$$a_{99} = K_C$$

$$a_{100} = \frac{\partial f_2}{\partial T_s}$$

$$a_{101} = \frac{\partial f_2}{\partial \rho_s}$$

$$a_{102} = K_f$$

APPENDIX B

LIST OF COEFFICIENTS B

$$b_1 = \frac{a_1}{a_3}$$

$$b_2 = \frac{a_2}{a_3}$$

$$b_3 = \left(\frac{a_6 . a_{17}}{a_4 . a_{15}} + \frac{a_7}{a_4} \right)$$

$$b_4 = \left(\frac{a_5}{a_4} + \frac{a_6 . a_{16}}{a_4 . a_{15}} \right)$$

$$b_5 = \left(\frac{a_6 . a_{17}}{a_4 . a_{15}} \right)$$

$$b_6 = \left(\frac{a_{13} . a_{162}}{a_{18}} - \frac{a_{12}}{a_{11}} + \frac{a_{20}}{a_{18}} \right) \Big/ \left(\frac{a_{13}}{a_{11}} - \frac{a_{22}}{a_{18}} \right)$$

$$b_7 = \left(\frac{a_{13}}{a_{11}} \right) \Big/ \left(\frac{a_{13}}{a_{11}} - \frac{a_{22}}{a_{18}} \right)$$

$$b_8 = \left(a_{14} - \frac{a_{21}}{a_{18}} \right) \Big/ \left(\frac{a_{13}}{a_{11}} - \frac{a_{22}}{a_{18}} \right)$$

$$b_9 = \left(\frac{a_{12}}{a_{11}} + \frac{a_{13} . b_6}{a_{11}} \right)$$

$$b_{10} = \left(\frac{b_7 . a_{13}}{a_{11}} - \frac{a_{13}}{a_{11}} \right)$$

$$b_{11} = \left(a_{14} - \frac{a_{13} . b_8}{a_{11}} \right)$$

$$b_{12} = \frac{a_8 . b_9}{a_{10}}$$

$$b_{13} = \left(\frac{a_8 . b_{10}}{a_{10}} + \frac{a_9 . a_{17}}{a_{10} . a_{15}} \right)$$

$$b_{14} = \frac{a_8 . b_{11}}{a_{10}}$$

$$b_{15} = \frac{a_9 . a_{16}}{a_{10} . a_{15}}$$

$$b_{16} = \frac{a_9 . a_{17}}{a_{10} . a_{15}}$$

$$b_{17} = \frac{a_{76} . a_{97}}{a_{77}}$$

$$b_{18} = \frac{a_{88}}{a_{77}}$$

$$b_{19} = \frac{a_{89}}{a_{77}}$$

$$b_{20} = \frac{a_{90}}{a_{77}}$$

$$b_{21} = \frac{a_{91}}{a_{77}}$$

$$b_{22} = \frac{a_{92}}{a_{77}}$$

$$b_{23} = \left(\frac{a_{75} . b_{17}}{a_{74}} + \frac{a_{97} . a_{67}}{a_{74}} - \frac{a_{97} . a_{73}}{a_{74}} + \frac{a_{72}}{a_{74}} \right)$$

$$b_{24} = \left(\frac{a_{66}}{a_{74}} - \frac{a_{75} . b_{18}}{a_{74}} \right)$$

$$b_{25} = \left(\frac{a_{68}}{a_{74}} - \frac{a_{75} . b_{19}}{a_{74}} \right)$$

$$b_{26} = \left(\frac{a_{71}}{a_{74}} - \frac{a_{75} . b_{20}}{a_{74}} \right)$$

$$b_{27} = \left(\frac{a_{70} + a_{73}}{a_{74}} - \frac{a_{75} . b_{21}}{a_{74}} \right)$$

$$b_{28} = \left(\frac{a_{69}}{a_{74}} - \frac{a_{75} . b_{22}}{a_{74}} \right)$$

$$b_{29} = \left(\frac{a_{61} . b_{17}}{a_{60}} - \frac{a_{62} . a_{97}}{a_{60}} \right)$$

$$b_{30} = \left(\frac{a_{63}}{a_{60}} - \frac{a_{61} . b_{18}}{a_{60}} \right)$$

$$b_{31} = \left(\frac{a_{64}}{a_{60}} - \frac{a_{61} . b_{19}}{a_{60}} \right)$$

$$b_{32} = \left(\frac{a_{61} . b_{20}}{a_{60}} \right)$$

$$b_{33} = \left(\frac{a_{62}}{a_{60}} - \frac{a_{61} . b_{21}}{a_{60}} \right)$$

$$b_{34} = \frac{a_{61} . b_{22}}{a_{60}}$$

$$b_{35} = \frac{a_{65}}{a_{60}}$$

$$b_{36} = \left(\frac{a_{45}}{a_{42}} - \frac{a_{41} . b_{29}}{a_{42}} - \frac{a_{43} . a_{53} . a_{97}}{a_{42} . a_{53}} \right)$$

$$b_{37} = \frac{a_{41} . b_{30}}{a_{42}}$$

$$b_{38} = \left(\frac{a_{46}}{a_{42}} - \frac{a_{41} . b_{31}}{a_{42}} \right)$$

$$b_{39} = \left(\frac{a_{44}}{a_{42}} + \frac{a_{41} . b_{32}}{a_{42}} \right)$$

$$b_{40} = \left(\frac{a_{47}}{a_{42}} - \frac{a_{41} \cdot b_{33}}{a_{42}}\right)$$

$$b_{41} = \frac{a_{41} \cdot b_{34}}{a_{42}}$$

$$b_{42} = \frac{a_{41} \cdot b_{35}}{a_{42}}$$

$$b_{43} = \frac{a_{43} \cdot a_{54}}{a_{42} \cdot a_{53}}$$

$$b_{44} = \left(\frac{a_{27} \cdot b_{36}}{a_{29}} + \frac{a_{28} \cdot b_{29}}{a_{29}}\right)$$

$$b_{45} = \left(\frac{a_{27} \cdot b_{37}}{a_{29}} - \frac{a_{28} \cdot b_{30}}{a_{29}} + \frac{a_{31}}{a_{29}}\right)$$

$$b_{46} = \left(\frac{a_{27} \cdot b_{38}}{a_{29}} + \frac{a_{28} \cdot b_{31}}{a_{29}}\right)$$

$$b_{47} = \left(\frac{a_{28} \cdot b_{32}}{a_{29}} + \frac{a_{30}}{a_{29}} - \frac{a_{27} \cdot b_{39}}{a_{29}}\right)$$

$$b_{48} = \left(\frac{a_{27} \cdot b_{40}}{a_{29}} + \frac{a_{28} \cdot b_{33}}{a_{29}}\right)$$

$$b_{49} = \left(\frac{a_{28} \cdot b_{34}}{a_{29}} - \frac{a_{27} \cdot b_{41}}{a_{29}}\right)$$

$$b_{50} = \left(\frac{a_{27} \cdot b_{42}}{a_{29}} - \frac{a_{28} \cdot b_{35}}{a_{29}}\right)$$

$$b_{51} = \frac{a_{27} \cdot b_{43}}{a_{29}}$$

$$b_{52} = \frac{a_{58} + a_{59} \cdot b_{47}}{a_{57}}$$

$$b_{53} = \frac{a_{56} + a_{59} \cdot b_{44}}{a_{57}}$$

$$b_{54} = \frac{a_{59} \cdot b_{45}}{a_{57}}$$

$$b_{55} = \frac{a_{59} \cdot b_{46}}{a_{57}}$$

$$b_{56} = \frac{a_{59} \cdot b_{48}}{a_{57}}$$

$$b_{57} = \frac{a_{59} \cdot b_{49}}{a_{57}}$$

$$b_{58} = \frac{a_{59} \cdot b_{50}}{a_{57}}$$

$$b_{59} = \frac{a_{59} \cdot b_{51}}{a_{57}}$$

$$b_{60} = \left(\frac{a_{32} \cdot b_{52}}{a_{35}} - \frac{a_{37}}{a_{35}} \right)$$

$$b_{61} = \left(\frac{a_{33}}{a_{35}} - \frac{a_{32} \cdot b_{53}}{a_{35}} \right)$$

$$b_{62} = \left(\frac{a_{32} \cdot b_{54}}{a_{35}} - \frac{a_{34}}{a_{35}} \right)$$

$$b_{63} = \left(\frac{a_{32} \cdot b_{55}}{a_{35}} + \frac{a_{36}}{a_{35}} \right)$$

$$b_{64} = \frac{a_{32} \cdot b_{56}}{a_{35}}$$

$$b_{65} = \frac{a_{32} \cdot b_{57}}{a_{35}}$$

$$b_{66} = \frac{a_{32} \cdot b_{58}}{a_{35}}$$

$$b_{67} = \frac{a_{32} \cdot b_{59}}{a_{35}}$$

$$b_{68} = \left(\frac{a_{38} \cdot a_{50}}{a_{40} \cdot a_{48}} + \frac{a_{39} \cdot a_{54}}{a_{40} \cdot a_{53}} \right)$$

$$b_{69} = \left(\frac{a_{38} \cdot a_{51}}{a_{40} \cdot a_{48}} - \frac{a_{38} \cdot a_{49} \cdot b_6}{a_{40} \cdot a_{48}} \right)$$

$$b_{70} = \left(\frac{a_{38} \cdot a_{52}}{a_{40} \cdot a_{48}} + \frac{a_{38} \cdot a_{48} \cdot b_8}{a_{40} \cdot a_{48}} \right)$$

$$b_{71} = \frac{a_{38} \cdot a_{49} \cdot b_7}{a_{40} \cdot a_{48}}$$

$$b_{72} = \frac{a_{33} \cdot a_{55} \cdot a_{97}}{a_{40} \cdot a_{53}}$$

$$b_{73} = \left(\frac{a_{26}}{a_{23}} - \frac{a_{25} \cdot a_{98}}{a_{23}} \right)$$

$$b_{74} = \frac{a_{24} \cdot a_{100}}{a_{23}}$$

$$b_{75} = \frac{a_{24} \cdot a_{101}}{a_{23}}$$

$$b_{76} = \frac{a_{94}}{a_{93}}$$

$$b_{77} = \left(\frac{a_{95} \cdot a_{100}}{a_{93}} + \frac{a_{96}}{a_{93}} \right)$$

$$b_{78} = \frac{a_{95} \cdot a_{101}}{a_{93}}$$

APPENDIX C

C MATRIX COEFFICIENTS

$C_{11} = (b_2 . b_{78} - b_1 . b_{75})$

$C_{12} = (b_2 . b_{77} - b_1 . b_{74})$

$C_{18} = b_1 . b_{73}$

$C_{21} = b_4 . b_{75}$

$C_{22} = (b_3 + b_4 . b_{74})$

$C_{23} = -b_5$

$C_{28} = -b_4 . b_{73}$

$C_{31} = -b_{15} . b_{75}$

$C_{32} = -(b_{15} . b_{74} + b_{16})$

$C_{33} = b_{13}$

$C_{38} = b_{15} . b_{73}$

$C_{41} = b_{42} . b_{75}$

$C_{42} = b_{42} . b_{74}$

$C_{44} = b_{38}$

$C_{45} = -b_{37}$

$C_{46} = b_{39}$

$C_{47} = -b_{43}$

$C_{48} = (b_{36} - b_{42} . b_{73})$

$C_{49} = b_{40}$

$C_{51} = -b_{66} \cdot b_{75}$

$C_{52} = -b_{66} \cdot b_{74}$

$C_{54} = -b_{63}$

$C_{55} = b_{62}$

$C_{56} = b_{60}$

$C_{57} = b_{67}$

$C_{58} = (b_{66} \cdot b_{73} + b_{61})$

$C_{59} = -b_{64}$

$C_{61} = -b_{50} \cdot b_{75}$

$C_{62} = -b_{50} \cdot b_{74}$

$C_{64} = -b_{46}$

$C_{65} = b_{45}$

$C_{66} = b_{47}$

$C_{67} = b_{51}$

$C_{68} = (b_{50} \cdot b_{73} - b_{44})$

$C_{69} = -b_{48}$

$C_{73} = -b_{71}$

$C_{77} = b_{68}$

$C_{78} = b_{72}$

$C_{81} = -b_{35} \cdot b_{75}$

$C_{82} = -b_{35} \cdot b_{74}$

$C_{84} = b_{31}$

$C_{85} = b_{30}$

$C_{86} = -b_{32}$

$C_{88} = (b_{29}+b_{35}\cdot b_{73})$

$C_{89} = b_{33}$

$C_{94} = b_{25}$

$C_{95} = b_{24}$

$C_{96} = b_{26}$

$C_{98} = b_{23}$

$C_{99} = b_{27}$

$C_{104} = b_{19}$

$C_{105} = b_{18}$

$C_{106} = b_{20}$

$C_{108} = -b_{17}$

$C_{109} = b_{21}$

APPENDIX D

D MATRIX COEFFIENTS

$D_{11} = b_2 . b_{76}$

$D_{32} = b_{12}$

$D_{33} = b_{14}$

$D_{44} = b_{41}$

$D_{54} = b_{65}$

$D_{64} = b_{49}$

$D_{72} = b_{69}$

$D_{73} = b_{70}$

$D_{84} = -b_{34}$

$D_{94} = b_{28}$

$D_{104} = b_{22}$

APPENDIX E

LIST OF CONSTANTS

$L_s = 45.0$

$A_s = 0.239$

$\bar{\rho}_s = 0.5$

$C_{ps} = 0.53$

$\bar{h}_s = 1390.0$

$\bar{h}_B = 1204.9$

$\bar{W}_s = 4.0$

$M_s = 1900.0$

$C_s = 0.23$

$K_{gs} = 0.94633$

$\bar{W}_f = 0.32$

$\bar{T}_{gs} = 2800.0$

$\bar{T}_{sw} = 1250.0$

$K_{as} = 0.0$

$\bar{W}_{ac} = 7.0$

$\bar{W}_a = 5.3$

$K_s = 4.8848$

$\bar{T}_s = 1200.0$

$\bar{W}_B = 4.0$

$C_C = 0.37$

$\bar{T}_C = 3200.0$

$f_S = 68.22$

$\bar{\rho}_B = 0.758$

$A_r = 2.95$

$L_r = 10.0$

$\bar{\rho} = 16.52$

$\bar{\rho}_W = 52.6$

$\bar{X} = 0.031933$

$K_B = 0.00001$

$C = 0.007637$

$\bar{W} = 178.97$

$f_r = 0.76095$

$D_r = 0.146$

$g = 32.2$

$\bar{W}_W = 178.97$

$M_B = 12000.0$

$C_B = 0.28$

$K_C = 0.00406$

$\bar{h}_{fg} = 390.0$

$\bar{h}_{WD} = 0.0$

$\bar{h} = 430.39$

$K_{gB} = 3.6632$

$K_r = 7.5E-10$

$\bar{T}_{gB} = 3000.0$

AD-A055 379 NAVAL POSTGRADUATE SCHOOL MONTEREY CALIF F/G 13/1

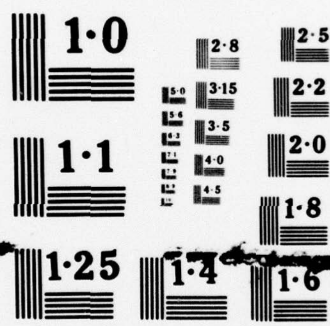
STATE VARIABLE ANALYSIS OF A BOILER SYSTEM.(U)

MAR 78 C SENANIKROM

UNCLASSIFIED NL

2 OF 2
ADA
055379

END
DATE
FILMED
8-78
DDC



NATIONAL BUREAU OF STANDARDS
MICROCOPY RESOLUTION TEST CHART

$\bar{T}_{bw} = 930.0$

$K_{ar} = 0.0$

$K_g = 0.059806$

$\bar{T}_B = 890.0$

$f_D = 2.7014$

$L_D = 10.0$

$D_D = 0.3$

$A_D = 0.426$

$\bar{V}_B = 40.0$

$A = 26.4$

$K_e = -0.39157$

$\bar{T}_i = 740.0$

$\bar{T}_W = 894.38$

$W_e = -1.7742$

$\bar{h}_{BW} = 405.0$

$M = 1680.0$

$K_T = 0.003$

$K_f = 500.0$

APPENDIX F

FORTRAN IV PROGRAM

```
$JOB
      IMPLICIT REAL*4 (A-Z)
      LS=45.0
      AS=0.239
      RHOS=0.5
      CPS=0.53
      HS=1390.0
      HB=1204.9
      WS=4.0
      MS=1900.0
      CS=0.22
      KGS=0.94633
      WF=0.32
      TGS=2800.0
      TSW=1250.0
      KAS=0.0
      WAC=7.0
      WA=5.3
      KS=4.8843
      TS=1200.0
      WB=4.0
      CC=0.37
      TC=3200.0
      FS=68.22
      RHOB=0.758
      AR=2.95
      LR=10.0
      RHO=16.52
      RHOW=52.6
      X=0.031933
      KB=0.00001
      C=0.007637
      W=178.97
      FR=0.76095
      DR=0.146
      G=32.2
      WW=178.97
      MB=12000.0
      CB=0.28
      KC=0.00406
      HFG=390.0
      HWD=0.0
      H=430.39
      KGB=3.6632
      KR=7.5E-10
      TGB=3000.0
      TBW=930.0
      KAR=0.0
      KG=0.059806
      TB=890.0
      FD=2.7014
      LD=10.0
      DD=0.5
      AD=0.426
      VB=40.0
      A=26.4
      KF=-0.39157
      TI=740.0
      TW=894.38
      WE=-1.7742
```

```
HBW=405.0
M=1680.0
KT=0.003
KF=500.0
A1=1.0
A2=-1.0
A3=LS*AS
A4=LS*AS*RHOS*CPS
A5=HS-HB
A6=-1.0
A7=-WS*CPS
A8=1.0
A9=-1.0
A10=MS*CS
A11=1.0
A12=(0.6*KGS)/(WF**0.4)*(TGS-TSW)
A13=KGS*WF**0.6
A14=(2.0*KAS/WAC**2)*(WAC-WA)
A15=1.0
A16=(0.8*KS/WB**0.2)*(TSW-TS)
A17=KS*WB**0.8
A18=1.0/(2.0*CC)
A19=WF+WA
A20=TC-TGS
A21=A20
A22=-(WF+WA)
A23=2.0*FS*WB/RHOB
A24=1.0
A25=-(FS*WB**2/RHOB**2)
A26=1.0
A27=0.5*AR*LR*RHO**2*(1.0/RHOW-1.0/RHOB)
A28=0.5*AR*LR*X*KB*(RHO**2/RHOB**2)
A29=0.5*C*(RHO+RHOW)
A30=1.0
A31=-1.0
A32=1.0
A33=-1.0
A34=2.0*W*(FR*LR/DR+1.5)/(G*AR**2*RHO)
A35=LR/(-G*AR)
A36=(1.0/RHOB-1.0/RHOW)*((W**2/(G*AR**2))*(FR*LR/DR+1.5)-
1(RHO**2*LR))
A37=-2.0*WW/(G*AR**2*RHOW)
A38=1.0
A39=-1.0
A40=MB*CB
A41=0.5*AR*LR*KC*(RHO+RHOW)
A42=0.5*AR*LR*HFG*(RHO+RHOW)
A43=-1.0
A44=HWD-H
A45=-W*KC
A46=-W*HFG
A47=WW
A48=1.0
A49=(-KGB*WF**0.6)-(4.0*KR*TGB**3)
A50=(-KGB*WF**0.6)-(4.0*KR*TBW**3)
A51=0.6*KGB*(TGB-TBW)/WF**0.4
A52=2.0*KAR*(WAC-WA)/WAC**2
A53=1.0
A54=3.0*KG*(TBW-TB)**2.0
A55=-A54
A56=1.0
A57=-1.0
A58=2.0*WW*(FD*LD/DD+0.5)/(AD**2.0*G*RHOW)
A59=LD/(G*AD)
A60=VB*KB
A61=-RHOB*A
A62=KE
A63=X
A64=W
A65=-1.0
```

```
A66=TB*(1.0-X)
A67=W*(1.0-X)
A68=-W*TB
A69=TT
A70=-WW
A71=-TW
A72=-WE*KC
A73=-HBW*KE
A74=M
A75=A*RHCW*TW
A76=-KE
A77=A*RHCW
A88=1.0-X
A89=-W
A90=-1.0
A91=-KE
A92=1.0
A93=1.0
A94=0.42
A95=0.000019
A96=-0.000005
A97=KT
A98=KB
A99=KC
A100=240.0
A101=95000.0
A102=KF
B1=A1/A3
B2=A2/A3
B3=(A6*A17)/(A4*A15)+(A7/A4)
B4=(A6*A16)/(A4*A15)+(A5/A4)
B5=(A6*A17)/(A4*A15)
B6=((A19*A102/A18)-(A12/A11)+(A20/A18))/((A13/A11)-(A22/A18))
B7=(A13/A11)/((A13/A11)-(A22/A18))
B8=(A14-(A21/A18))/((A13/A11)-(A22/A18))
B9=(A12/A11)+(A13*B6/A11)
B10=(B7*A13/A11)-(A13/A11)
B11=A14-(B8*A13/A11)
B12=A8*B9/A10
B13=(A8*B10/A10)+((A9*A17)/(A10*A15))
B14=A8*B11/A10
B15=(A9*A16)/(A10*A15)
B16=(A9*A17)/(A10*A15)
B17=A76*A97/A77
B18=A88/A77
B19=A89/A77
B20=A90/A77
B21=A91/A77
B22=A92/A77
B23=(A75*B17/A74)+(A97*A67/A74)-(A97*A73/A74)+(A72/A74)
B24=(A66/A74)-(A75*B18/A74)
B25=(A68/A74)-(A75*B19/A74)
B26=(A71/A74)-(A75*B20/A74)
B27=(A70+A73)/A74-(A75*B21/A74)
B28=(A69/A74)-(A75*B22/A74)
B29=(A61*B17/A60)-(A62*A97/A60)
B30=(A63/A60)-(A61*B18/A60)
B31=(A64/A60)-(A61*B19/A60)
B32=A61*B20/A60
B33=(A62/A60)-(A61*B21/A60)
B34=A61*B22/A60
B35=A65/A60
B36=(A45/A42)-(A41*B29/A42)-(A43*A55*A97/A42/A53)
B37=A41*B30/A42
B38=(A46/A42)-(A41*B31/A42)
B39=(A44/A42)+(A41*B32/A42)
B40=(A47/A42)-(A41*B33/A42)
B41=A41/A42*B34
B42=A41*B35/A42
```

```
B43=(A43*A54)/(A42*A53)
B44=(A27*B36/A29)+(A28*B29/A29)
B45=(A27*B37/A29)-(A28*B30/A29)+(A31/A29)
B46=(A27*B38/A29)+(A28*B31/A29)
B47=(A28*B32/A29)+(A30/A29)-(A27*B39/A29)
B48=(A27*B40/A29)+(A28*B33/A29)
B49=(A28*B34/A29)-(A27*B41/A29)
B50=(A27*B42/A29)-(A28*B35/A29)
B51=A27*B43/A29
B52=(A58/A57)+(A59*B47/A57)
B53=(A58/A57)+(A59*B44/A57)
B54=A59*B45/A57
B55=A59*B46/A57
B56=A59*B48/A57
B57=A59*B49/A57
B58=A59*B50/A57
B59=A59*B51/A57
B60=(A32*B52/A35)-(A37/A35)
B61=(A33/A35)-(A32*B53/A35)
B62=(A32*B54/A35)-(A34/A35)
B63=(A32*B55/A35)+(A36/A35)
B64=A32*B56/A35
B65=A32*B57/A35
B66=A32*B58/A35
B67=A32*B59/A35
B68=(A38*A50)/(A40*A48)+(A39*A54)/(A40*A53)
B69=(A38*A51)/(A40*A48)-(A38*A49*B6)/(A40*A48)
B70=(A38*A52)/(A40*A48)+(A38*A49*B8)/(A40*A48)
B71=(A38*A49*B7)/(A40*A48)
B72=(A39*A55*A97)/(A40*A53)
B73=(A26/A23)-(A25*A98/A23)
B74=A24*A100/A23
B75=A24*A101/A23
B76=A94/A93
B77=(A95*A100/A93)+(A96/A93)
B78=A95*A101/A93
C11=(B2*B78)-(B1*B75)
C12=(B2*B77)-(B1*B74)
C13=B1*B73
C21=B4*B75
C22=B3+(B4*B74)
C23=-B5
C28=-B4*B73
C31=-B15*B75
C32=-(B15*B74)-B16
C33=B13
C38=B15*B73
C41=B42*B75
C42=B42*B74
C44=B33
C45=-B37
C46=B39
C47=-B43
C48=B36-(B42*B73)
C49=B40
C51=-B66*B75
C52=-B66*B74
C54=-B63
C55=B62
C56=B60
C57=B67
C58=(B66*B73)+B61
C59=-B64
C61=-B50*B75
C62=-B50*B74
C64=-B48
C65=B45
C66=B47
C67=B51
C68=(B50*B73)-B44
C69=-B48
C73=-B71
```

```
      C77=B68
      C78=B72
      C81=-B35*B75
      C82=-B35*B74
      C84=B31
      C85=B30
      C86=-B32
      C88=B29+(B35*B73)
      C89=B33
      C94=B25
      C95=B24
      C96=B26
      C98=B23
      C99=B27
      C104=B19
      C105=B18
      C106=B20
      C108=-B17
      C109=B21
      D11=B2*B76
      D32=B12
      D33=B14
      D44=B41
      D54=B65
      D64=B49
      D72=B69
      D73=B70
      D84=-B34
      D94=B28
      D104=B22
      WRITE (6,100) A100,A101,B73,B74,B75,B76,B77,B78
100   FORMAT(1H1,8X,5HA100=,E15.8,5X,5HA101=,E15.8//,
     19X,5HB73 =,E15.8,5X,5HB74 =,E15.8,5X,5HB75 =,E15.8//,
     29X,5HB76 =,E15.8,5X,5HB77 =,E15.8,5X,5HB78 =,E15.8//)
      WRITE (6,200) C11,C12,C18,C21,C22,C23,C28,C31,C32,C33,C38,C41,
     1C42,C44,C45,C46,C47,C48,C49,C51,C52,C54,C55,C56,C57,C58,C59,
     2C61,C62,C64
200   FORMAT(1H0,8X,5HC11 =,E15.8,5X,5HC12 =,E15.8,5X,5HC18 =,E15.8//,
     19X,5HC21 =,E15.8,5X,5HC22 =,E15.8,5X,5HC23 =,E15.8//,
     29X,5HC28 =,E15.8,5X,5HC31 =,E15.8,5X,5HC32 =,E15.8//,
     39X,5HC33 =,E15.8,5X,5HC38 =,E15.8,5X,5HC41 =,E15.8//,
     49X,5HC42 =,E15.8,5X,5HC44 =,E15.8,5X,5HC45 =,E15.8//,
     59X,5HC46 =,E15.8,5X,5HC47 =,E15.8,5X,5HC48 =,E15.8//,
     69X,5HC49 =,E15.8,5X,5HC51 =,E15.8,5X,5HC52 =,E15.8//,
     79X,5HC54 =,E15.8,5X,5HC55 =,E15.8,5X,5HC56 =,E15.8//,
     89X,5HC57 =,E15.8,5X,5HC58 =,E15.8,5X,5HC59 =,E15.8//,
     99X,5HC61 =,E15.8,5X,5HC62 =,E15.8,5X,5HC64 =,E15.8/)
      WRITE (6,300) C65,C66,C67,C68,C69,C73,C77,C78,C81,C82,C84,C85,
     1C86,C88,C89,C94,C95,C96,C98,C99,C104,C105,C106,C108,C109
300   FORMAT(1H ,8X,5HC65 =,E15.8,5X,5HC66 =,E15.8,5X,5HC67 =,E15.8//,
     19X,5HC68 =,E15.8,5X,5HC69 =,E15.8,5X,5HC73 =,E15.8//,
     29X,5HC77 =,E15.8,5X,5HC78 =,E15.8,5X,5HC81 =,E15.8//,
     39X,5HC82 =,E15.8,5X,5HC84 =,E15.8,5X,5HC85 =,E15.8//,
     49X,5HC86 =,E15.8,5X,5HC88 =,E15.8,5X,5HC89 =,E15.8//,
     59X,5HC94 =,E15.8,5X,5HC95 =,E15.8,5X,5HC96 =,E15.8//,
     69X,5HC98 =,E15.8,5X,5HC99 =,E15.8,5X,5HC104=,E15.8//,
     79X,5HC105=,E15.8,5X,5HC106=,E15.8,5X,5HC108=,E15.8//,
     89X,5HC109=,E15.8//)
      WRITE (6,400) D11,D32,D33,D44,D54,D64,D72,D73,D84,D94,D104
400   FORMAT(1H0,8X,5HD11 =,E15.8,5X,5HD32 =,E15.8,5X,5HD33 =,E15.8//,
     19X,5HD44 =,E15.8,5X,5HD54 =,E15.8,5X,5HD64 =,E15.8//,
     29X,5HD72 =,E15.8,5X,5HD73 =,E15.8,5X,5HD84 =,E15.8//,
     39X,5HD94 =,E15.8,5X,5HD104=,E15.8//)
      STOP
      END
$GO
```

APPENDIX G

FORTRAN IV PROGRAM OUTPUT

```
A100= 0.24000000E 03      A101= 0.95000000E 05
B73 = 0.14152740E-02      B74 = 0.33333340E 00      B75 = 0.13194440E 03
B76 = 0.42000000E 00      B77 = 0.45549940E-02      B78 = 0.18049990E 01

C11 =-0.12436020E 02      C12 =-0.31416850E-01      C18 = 0.13159210E-03
C21 = 0.17133750E 04      C22 =-0.16096850E 01      C23 = 0.51956340E 01
C28 =-0.18585510E-01      C31 = 0.44709970E 02      C32 = 0.14683690E 00
C33 =-0.34865910E-01      C38 =-0.47957190E-03      C41 =-0.34339410E 01
C42 =-0.86752210E-02      C44 =-0.47662320E 01      C45 =-0.11941460E-02
C46 =-0.70738900E-03      C47 = 0.72198050E-03      C48 = 0.27080380E-05
C49 = 0.10494110E-01      C51 =-0.49093270E 06      C52 =-0.12402500E 04
C54 =-0.63842140E 05      C55 =-0.15757540E 03      C56 = 0.93258980E 03
C57 = 0.99146950E 02      C58 = 0.40967170E 00      C59 = 0.14977520E 04
C61 =-0.70394060E 05      C62 =-0.17910070E 03      C64 =-0.98256370E 05
C65 =-0.28442070E 02      C66 =-0.99339400E 01      C67 = 0.14317490E 02
C68 = 0.59159390E-01      C69 = 0.21628560E 03      C73 = 0.25403440E-02
C77 =-0.86705500E-01      C78 = 0.25631110E-03      C81 = 0.32986130E 06
C82 = 0.83333390E 03      C84 = 0.44097750E 06      C85 = 0.11470870E 03
C86 =-0.36026590E 02      C88 =-0.64373300E 00      C89 =-0.96481330E 03
C94 = 0.46655270E 00      C95 =-0.25236600E-02      C96 =-0.29802320E-06
C98 = 0.65586110E-03      C99 =-0.22059300E 00      C104=-0.12888150E 00
C105= 0.69713330E-03      C106=-0.72012910E-03      C108=-0.84594270E-06
C109= 0.28198090E-03

D11 =-0.39051580E-01      D32 = 0.34094850E 01      D33 = 0.69783800E-01
D44 =-0.37504610E-03      D54 =-0.53618420E 02      D64 =-0.77428660E 01
D72 = 0.73857530E 01      D73 = 0.15741700E 01      D84 = 0.36026590E 02
D94 =-0.91892480E-01      D104= 0.72012910E-03
```

APPENDIX H

CSMP - III PROGRAM

```
$$$CONTINUOUS SYSTEM MODELING PROGRAM III V1M3 TRANSLATOR OUTPUT$$$
      INITIAL
      CONSTANT A100=0.2400E+03,A101=0.[illegible]
      CONSTANT B73=0.1415E-02,B74=0.[illegible]+0[illegible],B75=0.1319E+03
      CONSTANT B76=0.4200E+00,B77=0.4555E-02,B78=0.1805E+01
      CONSTANT C11=-0.1[illegible]E+02,C12=-0.5[illegible]E-01,C18=0.1316E-03
      CONSTANT C21=0.1714E+04,C22=-0.1609E+01,C23=0.5195E+01
      CONSTANT C28=-0.1[illegible]E-01,C31=0.[illegible]471E+02,C32=0.1448E+00
      CONSTANT C33=-0.3486E-01,C38=-0.4796E-02,C41=-0.3434E+01
      CONSTANT C42=-0.8675E-02,C44=-0.4766E+01,C45=-0.1194E-02
      CONSTANT C46=-0.7070E-0[illegible],C47=0.7[illegible]E-0[illegible],C48=0.270[illegible]E-05
      CONSTANT C49=0.1049E-01,C51=-0.4[illegible]9E+06,C52=-0.1240E+04
      CONSTANT C54=-0.638[illegible]E+06,C55=-0.1575E+03,C56=0.9325E+03
      CONSTANT C57=0.9914E+02,C58=0.40[illegible]E+0[illegible],C59=0.14[illegible]E+04
      CONSTANT C61=-0.7039E+05,C62=-0.1791E+03,C64=-0.9325E+05
      CONSTANT C65=-0.2844E+02,C66=-0.[illegible]E+01,C67=0.14[illegible]E+02
      CONSTANT C63=0.5916E-01,C69=0.2162E+03,C73=0.2540E-02
      CONSTANT C77=-0.8670E-01,C78=0.256[illegible]E-0[illegible],C81=0.[illegible]E+06
      CONSTANT C82=0.8[illegible]E+03,C84=0.44[illegible]E+0[illegible],C85=0.1147E+03
      CONSTANT C86=-0.3603E+02,C88=-0.6437E+0[illegible],C89=-0.9648E+03
      CONSTANT C94=0.4665E+00,C95=-0.2534E-02,C96=-0.2930E-06
      CONSTANT C98=0.6598E-03,C99=-0.2206E+00,C104=-0.1288E+00
      CONSTANT C105=0.6971E-03,C106=-0.7201E-03,C108=-0.8459E-06
      CONSTANT C109=0.2[illegible]E-0[illegible]
      CONSTANT D11=-0.3905E-01,D32=0.340[illegible]E+01,D33=0.697[illegible]E-01
      CONSTANT D44=-0.3750E-03,D54=-0.5261E+02,D64=-0.7742E+01
      CONSTANT D72=0.7[illegible]E+01,D73=0.157[illegible]E+01,D84=0.36[illegible]E+0[illegible]
      CONSTANT D94=-0.9139E-01,D104=0.7201E-0[illegible]
      CONSTANT IC1=0.0,IC2=0.0,IC3=0.0,IC4=0.0,IC5=0.0
      CONSTANT IC6=0.0,IC7=0.0,IC8=0.0,IC9=0.0,IC10=0.0
      CONSTANT DXV=0.05,DWA=0.0,DWF=0.0,DWT=0.0
      DYNAMIC
      DRHOSD=C11*DRHOS+C12*DTS+C18*DPB+D11*DXV
      DRHOS=INTGRL(IC1,DRHOSD)
      DTSD=C21*DRHOS+C22*DTS+C23*DTSW+C28*DPB
      DTS=INTGRL(IC2,DTSD)
      DTSWD=C31*DRHOS+C32*DTS+C33*DTSW+C38*DPB+D32*DWF+D33*DWA
      DTSW=INTGRL(IC3,DTSWD)
      DXD=C41*DRHOS+C42*DTS+C44*DX+C45*DW+C46*DWW+C47*DTBW ...
      +C48*DPB+C49*DTW+D44*DWT
      DX=INTGRL(IC4,DXD)
      DWD=C51*DRHOS+C52*DTS+C54*DX+C55*DW+C56*DWW+C57*DTBW ...
      +C58*DPB+C59*DTW+D54*DWT
      DW=INTGRL(IC5,DWD)
      DWWD=C61*DRHOS+C62*DTS+C64*DX+C65*DW+C66*DWW+C67*DTBW ...
      +C68*DPB+C69*DTW+D64*DWT
      DWW=INTGRL(IC6,DWWD)
      DTBWD=C73*DTS+C77*DTBW+C78*DPB+D72*DWF+D73*DWA
      DTBW=INTGRL(IC7,DTBWD)
      DPBD=C81*DRHOS+C82*DTS+C84*DX+C85*DW+C86*DWW+C88*DPB+C89*DTW ...
      +D84*DWT
      DPB=INTGRL(IC8,DPBD)
      DTWD=C94*DX+C95*DW+C96*DWW+C98*DPB+C99*DTW+D94*DWT
      DTW=INTGRL(IC9,DTWD)
      DYD=C104*DX+C105*DW+C106*DWW+C108*DPB+C109*DTW+D104*DWT
      DY=INTGRL(IC10,DYD)
      DPS=A100*DTS+A101*DRHOS
      DWB=B73*DPB-B74*DTS-B75*DRHOS
      DWS=B76*DXV+B77*DTS+B78*DRHOS
```

```
PAGE HEIGHT=3,WIDTH=5
PAGE XYPLOT
OUTPUT TIME,DRHOS
LABEL DRHOS VS TIME
OUTPUT TIME,DTS
LABEL DTS VS TIME
OUTPUT TIME,DTSW
LABEL DTSW VS TIME
OUTPUT TIME,DX
LABEL DX VS TIME
OUTPUT TIME,DW
LABEL DW VS TIME
OUTPUT TIME,DWW
LABEL DWW VS TIME
OUTPUT TIME,DTBW
LABEL DTBW VS TIME
OUTPUT TIME,DPB
LABEL DPB VS TIME
OUTPUT TIME,DTW
LABEL DTW VS TIME
OUTPUT TIME,DY
LABEL DY VS TIME
OUTPUT TIME,DPS
LABEL DPS VS TIME
OUTPUT TIME,DWS
LABEL DWS VS TIME
OUTPUT TIME,DWB
LABEL DWB VS TIME
TIMER FINTIM=300.0,OUTDEL=3.0,PRDEL=3.0
END
CONSTANT DWF=0.032,DXV=0.0,DWA=0.0,DWI=0.0
END
CONSTANT DWI=0.4,DWA=0.0,DWF=0.0,DXV=0.0
END
STOP
```

BIBLIOGRAPHY

1. Chien, KL, Ergin, EI, Ling C and Lee, A, " Dynamic Analysis of a Boiler", _Trans Amer Soc Mech Engrs_, v. 80, p. 1809-1819, 1958.

2. Whalley, R, _The Control of Marine Propulsion Plant_, p. 1.1-4.28, PhD Thesis, University of Manchester, 1976.