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LAMINARISCENT TURBULENT BOUNDARY LAYERS: EXPERIMENTS ON NOZZLE --ETC(U)

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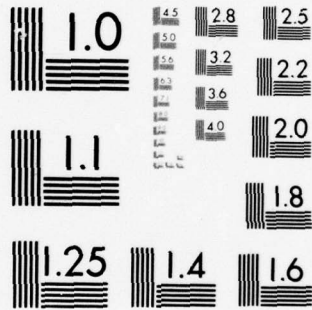
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PROJECT SQUID

TECHNICAL REPORT SMU-2-PU

LAMINARISCENT TURBULENT BOUNDRY LAYERS: EXPERIMENTS ON NOZZLE FLOWS

by

ROGER L. SIMPSON AND C. R. SHACKLETON
SOUTHERN METHODIST UNIVERSITY
DALLAS, TEXAS

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A COOPERATIVE PROGRAM OF FUNDAMENTAL RESEARCH
AS RELATED TO JET PROPULSION
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LAMINARISCENT TURBULENT BOUNDARY LAYERS:
EXPERIMENTS ON NOZZLE FLOWS

by

Roger L. Simpson* and C. R. Shackleton**

ABSTRACT

Because a turbulent boundary layer in a nozzle undergoes strong acceleration, a laminariscient boundary layer with the benefit of a lower surface heat transfer rate can result for some short distance. Here and in a previous report (Simpson and Wallace, 1975) several phenomena which accompany laminariscence produced by strong acceleration are examined for nozzle-flow and sink-flow accelerational distributions, respectively. Several different type measurements of the structure of two nozzle-type flows are reported to determine how an initially normal turbulent boundary layer approaches the laminar-like state, including mean velocity and Reynolds stresses profiles, spectra, turbulent/non-turbulent interfacial structure, and wall bursting and sublayer spanwise spatial structure.

As a result of these experiments, it appears that the surface skin-friction is not reduced to laminar values in sink flows unless $K(=vU_{\infty}^2 du/dx)$ is greater than about 3.6×10^{-6} . In nozzle-type flows, K must also be greater than this value over a short distance in order to produce a short relaminarized region downstream. The large-eddy structure of the outer region governs the bursting frequency, the intermittent bulge passage frequency, and influences the wall flow behavior downstream. After the cessation of entrainment of free-stream fluid, these frequencies approach constant values. The wall spanwise structure appears to lag behind local conditions and to reflect upstream flow behavior. After retransition to a low acceleration turbulent boundary layer downstream, much larger spanwise scale structures are observed.

The entrainment rate of non-turbulent fluid decreases to zero at about the streamwise location at which the shape factor reaches a minimum value. The cessation of entrainment by the eruption and

* Professor of Mechanical Engineering, Southern Methodist University.
** Research Assistant, Dept. of Mechanical Engrg., Southern Methodist University.

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and engulfment action of the large eddies can be traced to the reduction of available turbulence energy for diffusion to free-stream fluid. This reduction of available energy is due to the negative normal stresses turbulence energy production term. Spectral distributions of the streamwise fluctuation $F(n)$ possess a frequency region where $nF(n)$ is constant for laminar-like boundary layers at large K values.

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NOMENCLATURE

A, B, C, D	constants.
$C_f/2$	$= \tau_w/\rho U_\infty^2$, friction factor.
E, e	mean and fluctuation voltages.
F(n)	spectral density defined by equation (9).
F, F_δ	defined by equations (18) and (20), respectively.
f, f'	U/U_∞ and $\partial f/\partial \eta$, respectively.
H	$= \delta^*/\theta$, shape factor.
K	$= \frac{v}{U_\infty^2} \frac{dU_\infty}{dx}$; also a constant in equation (12).
L_z	integral length scale defined by equation (14).
M	constant.
m	exponent in split-film calibration curve.
n	frequency, Hz.
n_{iY}	frequency of intermittent bulge passage at \bar{Y} .
dP/dx	pressure gradient.
$\frac{Q_i}{q}$	power dissipation in split-film sensor i. $= \overline{u^2} + \overline{v^2} + \overline{w^2}$.
$\hat{sR}_{\tau\tau}(z, T_s)$	normalized spatial cross-correlation of two τ surface fluctuation signals during sample time T_s .
$\hat{sR}(z)$	$\hat{sR}(z, T_s)$ as T_s becomes very large.
Re_θ	$= U_\infty \theta/\nu$, momentum thickness Reynolds number.
Re_λ	$= \frac{(\overline{u^2})^{1/2} \lambda}{\nu}$, microscale Reynolds number.
T_s	length of sample time.
t	time delay; time.

U_τ	$= (\tau_w/\rho)^{1/2}$, shear velocity.
$u, v, w,$	velocity fluctuations in the streamwise, normal, and spanwise directions.
U, V, W	mean velocities in the streamwise, normal, and spanwise directions.
$-\overline{uv}$	kinematic Reynolds shearing stress.
V_E	entrainment velocity.
x, y, z	cartesian co-ordinates in the streamwise, normal, and spanwise directions, respectively.
\bar{Y}	distance from the wall to where $\gamma = 0.5$.

SUBSCRIPTS

b	denotes "bursting" value.
eff	denotes effective cooling velocity.
i	split-film sensor index.
l	denotes linearized signal.
w	denotes wall value.
∞	free-stream condition.

GREEK

α	constant in equation (10); split-film probe yaw parameter.
γ	intermittency, long-time averaged fraction of time that the flow is turbulent.
δ	$\delta_{0.99} = y$ where $f = 0.99$; $\delta_{0.995} = y$ where $f = 0.995$.
δ^*	$= \int_0^\infty \left(1 - \frac{U}{U_\infty}\right) dy$, displacement thickness.
ϵ	dissipation rate
η	$= yU_\infty/\nu$
θ	$= \int_0^\infty \frac{U}{U_\infty} \left(1 - \frac{U}{U_\infty}\right) dy$, momentum thickness.

λ	$= (15\overline{vu^2}/\epsilon)^{1/2}$, a turbulence microscale.
λ_z	spanwise wavelength in wall sensors cross-correlations.
λ_{z1}^+ , λ_{z2}^+	defined by equations (15).
ν	kinematic viscosity.
ρ	density.
σ	standard deviation for intermittency distribution.
τ	shearing stress.
ϕ	angle of flow incidence to split-film probe.
Ω	logarithmic equation (5) constant.

1. INTRODUCTION

The strong acceleration of turbulent boundary layers in a nozzle can produce the benefit of a substantially reduced convective heat transfer rate when relaminarization occurs (Moretti and Kays, 1965). The accelerational parameter K , defined as $\nu U_\infty^{-2} dU_\infty/dx$, must increase to a value in excess of about 3.6×10^{-6} (Kline et al., 1967) for relaminarization to occur. The practical consideration that flow acceleration extends over a finite length then requires that K decrease to zero downstream. Narasimha and Sreenivasan (1973) reexamined the behavior of this type of flow from the time-averaged results of many previous experiments. However, there is little information on the flow structure that would explain the mechanisms for relaminarization. Exceptions are the space-time correlations of Blackwelder and Kovaszny (1972) for the large-scaled motion and the wall region structure reported by Schraub and Kline (Kline, et al., 1967).

The work described here is the second part of a program to provide experimental flow structure information for strongly-accelerated turbulent boundary layers under different K distributions. In the first part (Simpson and Wallace, 1975) results were obtained for two asymptotic sink-flow type turbulent boundary layers with constant K distributions (flow A, $K = 2.17 \times 10^{-6}$; flow B, $K = 3.19 \times 10^{-6}$). Here results are presented for a flow in which K increases linearly with x (flow C) and a flow in which K increases linearly with x to a maximum value, stays constant at this level for a short distance, and then decreases linearly with x (flow D). Flow C models the rapid increase

in K encountered in nozzles while flow D models both the increase and decrease in K . Since the acceleration of both flows took place in the same length of wind tunnel test section, dK/dx for the increasing K portion of flow D was more than double dK/dx for flow C.

The type of measurements reported here for flows C and D are similar to those obtained for flows A and B. In addition to mean velocity and Reynolds' stresses measurements, spectra of the streamwise fluctuations were obtained. This was partly motivated by the presence of a flat $nF(n)$ spectrum for flow B and the question as to whether this behavior accompanies true relaminarization. Other measurements are the turbulent/non-turbulent interfacial intermittency and frequency of passage of intermittent turbulent bulges, the wall "bursting" frequencies or rate of passage of eddies over the wall, and the spanwise spatial structure at the wall. This latter group of measurements provides further insight as to the roles that the bursting behavior, spanwise structure, and intermittency play in relaminarization. Since these measurements have been obtained for four different K distribution flows on the same apparatus, the effect of the K distribution on the developing flow structure can be determined.

2. EXPERIMENTAL APPARATUS

In general, all of the apparatus and instrumentation described by Simpson and Wallace (1975) for flows A and B were used for flows C and D. The SMU wind tunnel with a sixteen feet long, three feet wide, test section was used to produce the desired boundary layer on the flat bottom wall by adjusting the plexiglas top wall. In the current

experiments the freestream flow upstream of the acceleration was uniform within 0.066% in the spanwise direction and within 1% in the vertical direction, with a streamwise turbulence intensity of 0.6% at 9.1 fps. At the tunnel exit the free-stream streamwise turbulence intensity dropped to below 0.55% and 0.5% for flows C and D, respectively. Of this intensity, about 0.5% was due to unsteadiness at about 20 Hz. Figure 1 is a side view schematic of the test section with the upper wall locations for flows A, C, and D. In all four flows the flat upper wall was 15 inches above the test wall at the entrance and 19.5 inches above it at the 96 inches location. For flow C the parabolic-shaped upper wall section began at 96 inches and was 1.72 inches above the test wall at the exit at 190.8 inches. For flow D the antisymmetric ogee-shaped upper wall began at 96 inches and was 1.84 inches above the test wall at 189.7 inches. All experimental data were obtained with the temperature maintained constant at $77 \pm 1/2^\circ\text{F}$ and a constant stagnation pressure at the exit.

The 1/4 inches blunt leading edge trip on the test wall and the boundary layer smoke injection arrangement upstream of the trip were the same as used for flows A and B. The same smoke generation system with a mean particle size of about 1 micron was used when smoke was used to mark turbulent fluid upstream of relaminarization. For these intermittency measurements the optics and traversing equipment of the SMU laser anemometer were used as for flows A and B.

Standard Thermo-Systems, Inc., model 1050 constant temperature anemometers, model 1055 linearizers, model 1057 signal conditioners,

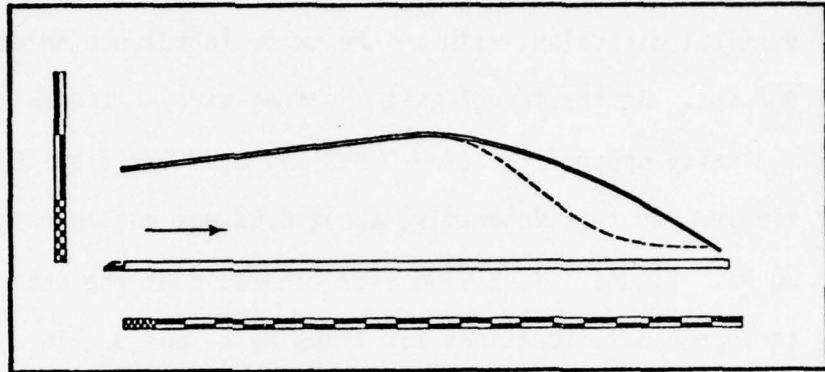


Figure 1. Sideview schematic of the test section: solid line, flow C; dashed line, flow D. Major divisions on abscissa and ordinate: 10 inches. Note 2:1 scale ratio.

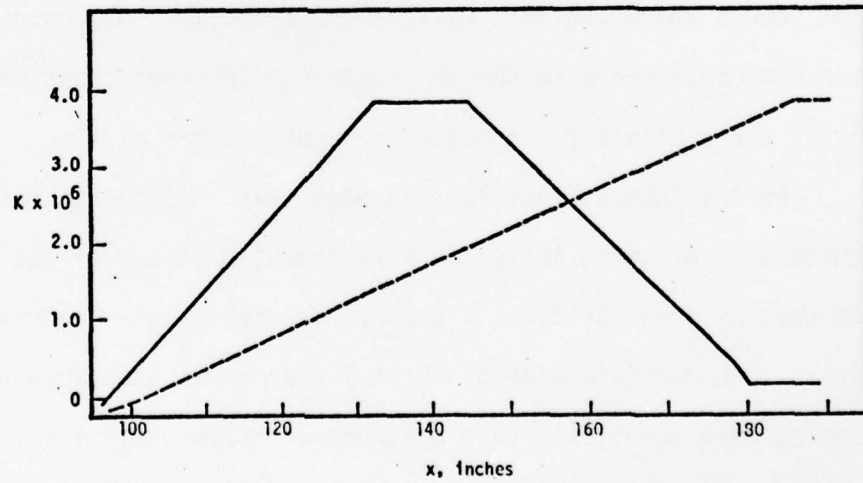


Figure 2. K distributions for flows C and D: flow C - dashed line; flow D - solid line.

and model 1015C correlator were used. A TSI model 1274-10 boundary layer hot-film probe was used in measuring the mean and streamwise fluctuation velocities in flow C while a model 1218-T1.5 boundary layer hot-wire probe was used for flow D. The sensing element for the hot-film is a 0.001 inches diameter platinum coated quartz rod with a sensing length of 0.04 inches. The 0.00015 inches diameter platinum-plated tungsten wire had a 0.05 inches sensing length. Based on the Collis and Williams (1959) equation for the anemometer bridge output calibration, the linearizers were adjusted. The linearizer output was directly checked with the known calibrator velocity for accuracy and linearity, the maximum tolerable deviation being less than about 1/2%. Consequently, the uncertainty on velocity measurements is about $\pm 1/2\%$.

The split-film probe (TSI model 1287) was used to determine U , V , $\overline{u^2}$, $\overline{v^2}$, and $-\overline{uv}$ for flow C. This relatively new hot-film probe was selected because of its relatively small size since the boundary layers under study were thin. The split-film sensor is a modification of the basic platinum coated cylindrical film sensor. Two electrically independent films each cover one-half of the circumference of a 0.006 inches diameter quartz rod. Each film is operated by a separate constant temperature circuit. The non-uniform heat transfer distribution around a constant temperature cylinder is utilized to measure the fluctuating components of the instantaneous velocity vector. To avoid thermal variations in the substrate the sensors must be held at closely identical temperatures. The resulting output

voltages are used in the same manner as those from an x-wire probe to determine mean and fluctuation quantities.

Using a right-handed coordinate system, the plane of the two splits that separate the two platinum films from one another are in the x-z plane, being nominally parallel to the test wall in these experiments. Following Spencer and Jones (1971), the power dissipated in each film can be related to the velocity by

$$Q_i = (A + BU_{\text{eff}}^m)(1 + \alpha_i \frac{V}{U_{\text{eff}}}) \quad i = 1, 2$$

neglecting axial cooling. The constants A, B, and m were obtained by velocity calibration as done for a single sensor probe; α_i was determined by azimuthal yaw calibration. The power dissipated is proportional to the square of the anemometer bridge output minus the zero flow voltage:

$$E_i = M_i(Q - Q_0)_i = M_i U_{\text{eff}}^m (1 + \alpha_i \frac{V}{U_{\text{eff}}})$$

The voltage E_i can be linearized directly in terms of U_{eff} using $m = 0.5$. Thus

$$E_{\ell i} = M_{\ell i} E_i^{1/m} = M U_{\text{eff}} (1 + \alpha_i \frac{V}{U_{\text{eff}}})^2$$

or when neglecting higher ordered terms the instantaneous voltage is

$$E_{\ell i} + e_{\ell i} = M U_{\text{eff}} [1 + \frac{u}{U_{\text{eff}}} + 2\alpha_i \frac{(V + v)}{U_{\text{eff}}}]$$

When calibrated in a steady flow

$$\frac{(E_{\ell i})_{\phi}}{(E_{\ell i})_{\phi=0}} = 1 + 2\alpha_i \sin\phi$$

Second order effects, which occur for angles larger than 20° , are negligible for this particular flow.

The following calibration procedure was repeated before and after each velocity profile was obtained. The probe was mounted in a specially constructed support with orientation adjustment, the "dial calibrator," that permitted a $\pm 50^\circ$ rotation of the split-film sensor about a fixed location. The sensor was supported over the potential core of the near jet produced by a TSI model 1125 calibrator. The dial calibrator was used for both the velocity and azimuthal yaw calibrations. The uncertainty in the angle was less than 0.2° . The use of the split-film probe requires closely equal temperatures of the films, so that very fine overheat adjustment of one film is mandatory to match temperatures.

Both films were exposed to 77° air flow directed along the plane of splits. Cold resistances were measured and found to be about 11 and 12 ohms. Both films were then overheated by a factor of 0.5. One film was left without further adjustment while the other film overheat was adjusted using a 1 ohm precision ten turn potentiometer. The temperature matching was achieved when the ratio of the two output bridge voltages remained constant (within 0.2%) as the velocity directed along the plane of the splits was varied from 9 fps to 70 fps. Temperature matching was checked again immediately after taking data from flow C in order to estimate any possible anemometer drift.

The bridge outputs were then each linearized and checked with the known calibrator velocity. A calibration equation of the form:

$$E_{\ell i} = C_i U_{\text{eff}} + D_i$$

was determined from a least squares fit with less than 4% standard deviation. The background noise level in the steady laminar calibrator flow was also measured. This noise took the form of a triangular wave with no phase change between channels. We suspect the noise was due to vortex shedding off of the relatively large diameter sensor. The probe was then calibrated for several azimuthal yaw angles to determine α_i . Yaw characteristics were found to be independent of the magnitude of U_{eff} .

The equations governing the split film are a combination of the above equations

$$E_{\ell i} + e_i = C_i U_{\text{eff}} [1 + u/U_{\text{eff}} + 2\alpha_i(V + v)/U_{\text{eff}}] + D_i$$

$$i = 1, 2$$

or
$$E_{\ell 1} = C_1 [U_{\text{eff}} + 2\alpha_1 V] + D_1$$

and
$$E_{\ell 2} = C_2 [U_{\text{eff}} + 2\alpha_2 V] + D_2$$

Since C_i , D_i , and α_i are known from calibration, then $E_{\ell 1}$ and $E_{\ell 2}$ are measured and U_{eff} and V are derived. The angle of flow, ϕ , at a point is then found from

$$\sin\phi = V/U_{\text{eff}}$$

Similarly, the fluctuation quantities are found from:

$$\overline{(e_{\ell 1})^2} = C_1^2 \overline{u^2} + 4C_1^2 \alpha_1 \overline{uv} + (2C_1 \alpha_1)^2 \overline{v^2}$$

$$\overline{(e_{\ell 1} + e_{\ell 2})^2} = (C_1 + C_2)^2 \overline{u^2} + 4(C_1 \alpha_1 + C_2 \alpha_2)(C_1 + C_2) \overline{uv} + 4(C_1 \alpha_1 + C_2 \alpha_2)^2 \overline{v^2}$$

$$\overline{(e_{\ell 1} - e_{\ell 2})^2} = (C_1 - C_2)^2 \overline{u^2} + 4(C_1 \alpha_1 - C_2 \alpha_2)(C_1 - C_2) \overline{uv} + 4(C_1 \alpha_1 - C_2 \alpha_2)^2 \overline{v^2}$$

$\overline{e_1^2}$, $\overline{(e_{\lambda 1} + e_{\lambda 2})^2}$, and $\overline{(e_{\lambda 1} - e_{\lambda 2})^2}$ were measured, corrected for the above mentioned noise, and used to solve simultaneously for $\overline{u^2}$, $-\overline{uv}$, and $\overline{v^2}$ using the latter equations. These results are discussed in section 3.4 below.

The traversing mechanism used for the boundary layer velocity measurements was mounted on the supporting frame for the upper wall and provided for precise positioning of the probe sensors as described by Strickland and Simpson (1973). A cathetometer was used to accurately locate the probe sensor from the wall within an uncertainty of about ± 0.001 inches. The detailed streamwise free-stream velocity distributions were obtained using a TSI model 1210-20 hot-film probe (0.002 inches diameter platinum-coated quartz rod) attached to a probe support rod inserted from the tunnel exit or mounted on the toy racing car shown in figure 3 of Simpson and Wallace (1975). The car was easily positioned along the flow by fishing line. It could not be used near the exit since substantial flow blockage effects would have been produced.

The flush surface mounted hot-film sensors for the wall "bursting" and spanwise measurements are described in detail by Strickland and Simpson (1973). The basic sensing part is a very thin layer of platinum (Engelhard Ind. Liquid Bright Platinum #05) fired on the end of a 2mm diameter quartz rod. Gold leads (Engelhard Ind. Gold Alloy Paste A-1199) were fired on the sides of the rod and short wire leads were soldered to the gold. A casing made from 1/4 inch diameter plexi-glas rod was used to protect the sensor from damage due to handling.

The resulting unit was mounted in the wind tunnel wall with the platinum portion flush with the test wall. A unit containing two flush surface 0.020 inches diameter platinum sensors was also fabricated to permit one of the sensors to be traversable. This unit was used in the surface spanwise structure measurements and is described in more detail by Simpson and Wallace (1975). All of these sensors were operated at an overheat ratio of 0.03 in the current experiments. A higher overheat ratio would have permanently damaged the sensors. The constant temperature frequency response for each sensor was determined to be down 3 db at 4 KHz using the method of Freymuth (1967).

Other electronic equipment included Krohn-Hite model 3202 and 330B filters, HP model 400E rms voltmeters, an Anadex model CF-600 timer-frequency counter, a SAICOR model 41 digital correlation and probability analyzer, an Applied University Research four-channel FM tape recorder (response down 3 db at 2 KHz), a voltage comparator or schmitt trigger using an operational amplifier integrated circuit and a multiplier using an Analog Devices AD533 JH integrated circuit trimmed to within $\pm 1\%$ fullscale nonlinearity error. A true integrating voltmeter consisting of a voltage-controlled oscillator (Tektronix FG501 Function Generator) and a digital counter (Tektronix DC503 Universal Counter) was found to be superior to RC-type meter circuits used in most voltmeters. A HP 5451A/71A Fast Fourier Analyzer System was used to process data recorded on the tape recorder.

For the intermittency measurements in flow C, the laser optics, and photo-multiplier tube of the SMU laser anemometer (Simpson, et al., 1974) was used to scatter light from the smoke filled boundary layer

and collect the signal. A focal volume of 0.32 mm diameter and 3.56 mm long was produced from a laser beam 1.1 mm in diameter at the $1/e^2$ intensity locations. Since the laser anemometer is mounted on a single traversable cart, accurate location of the focal volume could be determined.

3. EXPERIMENTAL RESULTS

3.1 Description of the test flows

Because of the strong influence of acceleration on these boundary layers, careful measurements of the freestream velocity were made every one inch along the test section using the rake and car probe mounts. For flow C the following velocity and K distributions were obtained:

$$1/U_{\infty} = -1.525 \times 10^{-2} + (2.307 \times 10^{-3})(x) - (1.133 \times 10^{-5})(x^2)$$

for $96 \leq x \leq 178$ inches and

$$1/U_{\infty} = 4.273 \times 10^{-1} - (2.466 \times 10^{-3})(x) + (1.473 \times 10^{-6})(x^2)$$

for $178 \leq x \leq 190$ inches with

$$K = -4.622 \times 10^{-6} + (4.5427 \times 10^{-8})(x)$$

for $96 \leq x \leq 185$ and $K = 3.83 \times 10^{-6}$ for $186 \leq x \leq 191$ inches. U_{∞} is in fps and x is in inches. The maximum deviation of U_{∞} data from these equations is less than 0.4% while the rms deviation is about 0.1%. The different x ranges for the $1/U_{\infty}$ distributions and their respective K distribution reflect the fact that the upstream velocity equation produces K values in closer agreement with data for $178 < x < 185$ inches. The single-sample uncertainty (Kline and McClintock, 1953) in K at 20:1 odds is about 2%.

For flow D, with both increasing and decreasing K regions, the following velocity and K distributions are presented:

$$1/U_{\infty} = 9.898 \times 10^{-2} + (6.568 \times 10^{-5})(x)$$

for $64 < x < 96$ inches

$$1/U_{\infty} = -1.449 \times 10^{-1} + (5.167 \times 10^{-3})(x) - (2.675 \times 10^{-5})(x^2)$$

for $96 < x < 132$ inches

$$1/U_{\infty} = 3.243 \times 10^{-1} - (1.917 \times 10^{-3})(x)$$

for $132 < x < 144$ inches

$$1/U_{\infty} = 8.497 \times 10^{-1} - (9.1869 \times 10^{-3})(x) + (2.5138 \times 10^{-5})(x^2)$$

for $144 < x < 180$ inches and

$$1/U_{\infty} = 2.475 \times 10^{-2} - (7.8147 \times 10^{-5})(x)$$

for $180 < x < 190$ inches.

$$K = -1.32 \times 10^{-7} \text{ for } 64 < x < 96 \text{ inches}$$

$$K = -1.037 \times 10^{-5} + (1.0737 \times 10^{-7})(x) \text{ for } 96 < x < 132 \text{ inches}$$

$$K = 3.85 \times 10^{-6} \text{ for } 132 < x < 144 \text{ inches}$$

$$K = 1.8438 \times 10^{-5} - (1.009 \times 10^{-7})(x) \text{ for } 144 < x < 179 \text{ inches}$$

$$K = 1.568 \times 10^{-7} \text{ for } 180 < x < 190 \text{ inches}$$

The maximum deviation of U_{∞} data from these equations is less than 1% while the rms deviation is about 0.2%. The discontinuity in K at the ends of each region is of the order of 10^{-7} . The single-sample uncertainty in K is about 4%. The smoothed K distributions for both flows C and D are shown in figure 2.

As was done for flows A and B, observations were made to assess the three-dimensionality of flows C and D. Because of the care used in adjusting the spanwise elements of the upper wall parallel to the

test wall, the thin boundary layers in a large aspect ratio channel, and the fact that the flow was accelerating, minimal three-dimensional effects were expected. At the 88 inches location there was less than 1% spanwise difference in the momentum thickness, so no gross three-dimensionality due to the upstream flow was present. The side wall boundary layers of the converging section for each flow tended to remain at about a constant thickness due to the reduction of the side wall surface area simultaneously with acceleration of the freestream. Thus convergence or divergence effects on the test wall boundary layer by the side wall boundary layers appears to be negligible.

As discussed in section 3.3 below, the skin friction was deduced by analyzing mean velocity profiles near the wall. The smoothed "best estimate" skin friction coefficients and other required and experimentally deduced quantities were used to check the balance of terms in the two-dimensional momentum integral equation. In both flows C and D this equation was balanced well within the uncertainty of the most uncertain term, $d\theta/dx$, or about 5% of that term.

3.2 Mean velocity profile measurements

Figure 3 shows the mean velocity profile results for flow C. A distinct logarithmic region exists for each upstream profile, with the last evidence of any logarithmic region occurring at about station 160 inches. As shown in figure 4, the shape factor H is near a minimum at station 165 inches. The wake-like tail of each profile near the freestream is observed to progressively decrease in wake strength,

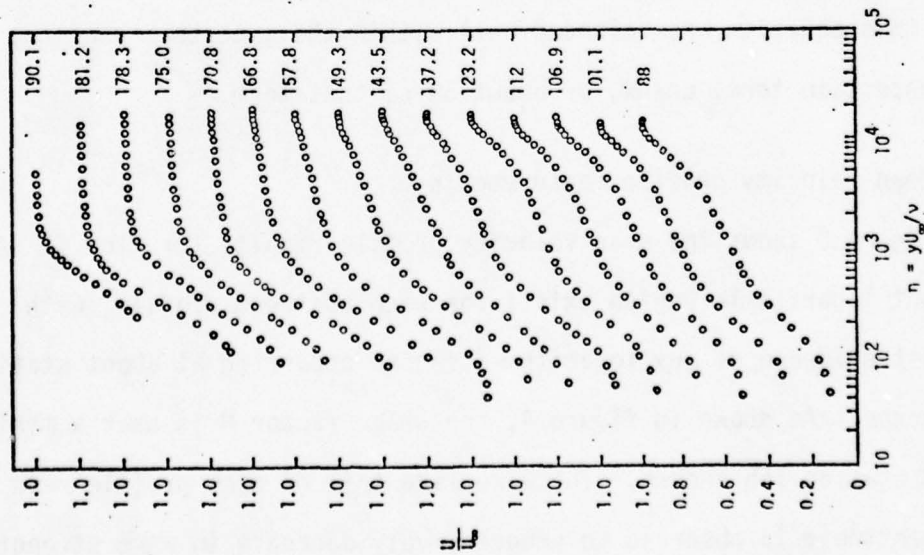


Figure 3. Experimental mean velocity profiles for flow C. linearly increasing K. Note displace ordinates. Station position in inches at right of each profile.

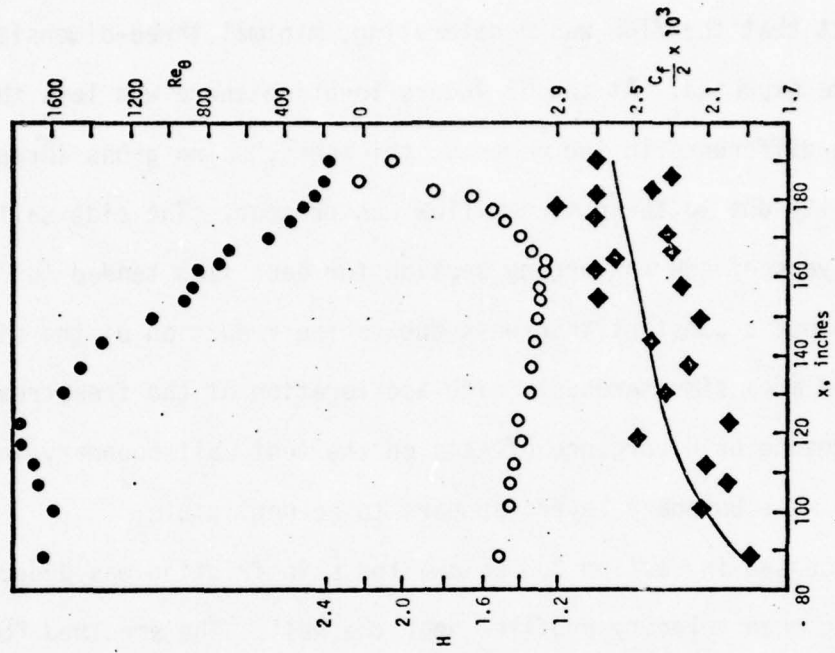


Figure 4. Re_δ , H , and $C_f/2$ for flow C. Friction factors from table 1: solid symbols - wall profile results; line - best estimate curve.

Station (inches)	U_{∞}^a (fps)	$(K \times 10^6)^b$	Re_{θ}	H	$\delta_{0.99}$ (inches)	$\frac{C_f}{2} \times 10^3$	
						wall profile $\pm 15\%$	best estimate ^c $\pm 15\%$
88.0	8.94	-0.59	1647	1.505	2.62	1.90	1.93 ^d
101.1	8.51	-0.029	1600	1.456	2.81	2.15	2.14 ^d
106.9	8.59	0.234	1681	1.450	2.91	2.04	2.20
112.0	8.80	0.466	1698	1.437	2.90	2.12	2.23
117.9	9.27	0.733	1765	1.388	2.91	2.48	2.27
123.2	9.71	0.974	1778	1.407	2.89	2.01	2.30
130.6	10.06	1.31	1546	1.344	2.74	2.32	2.34
137.2	10.79	1.61	1465	1.341	2.62	2.2	2.38
143.5	11.42	1.90	1353	1.320	2.53	2.40	2.41
149.3	12.10	2.16	1096	1.313	2.24	2.15	2.44
154.5	13.36	2.40	923	1.290	2.02	2.7	2.46
157.8	14.00	2.55	890	1.307	1.94	2.25	2.48
162.0	15.53	2.74	868	1.274	1.77	2.7	2.50
164.2	16.67	2.84	747	1.262	1.60	2.6	2.51
166.8	17.89	2.96	697	1.335	1.47	2.30	2.52
170.8	20.42	3.14	484	1.407	1.09	2.32	2.54
175.0	23.98	3.33	373	1.481	0.698	2.70	2.56
178.3	29.62	3.48	314	1.559	0.395	2.9	2.57
181.2	33.12	3.61	257	1.647	0.302	2.7	2.58
182.3	36.11	3.66	264	1.850	0.197	2.4	2.58
185.8	44.46	3.82	201	2.223	0.098	2.3	2.60
190.1	80.30	3.83	182	2.049	0.048	2.7	2.61

- (a) measured when velocity profile measured.
(b) from least squares fit of rake and cart data.
(c) with exceptions noted, from faired curve of data on figure 4.
(d) determined from logarithmic velocity profile, equation (5).

Table 1. Values of parameters along flow C.

the wake strength being defined as the maximum deviation of the measured velocity profile from the extrapolated logarithmic region profile. Downstream of the location of the minimum H the velocity profiles take on an increasingly more laminar-like character, although the streamwise fluctuation measurements clearly show that a relatively large turbulence intensity still exists. Since the last 5 inches of the test flow has a constant K of about 3.83×10^{-6} , this is the only region where constant K asymptotic velocity profile similarity of $f(=U/U_\infty)$ and $\eta(=yU_\infty/\nu)$ is possible. In this region the velocity profiles for $\eta > 1000$ are similar well within a deviation of 0.01 f. However, the streamwise fluctuation intensity profiles discussed in section 3.4 do not possess similarity in this region and H and Re_θ do not reach constant values, as required for true asymptotic similarity (Simpson and Wallace, 1975). Re_θ drops well below the value of about 360 (Kays 1966) where normal transition from a laminar to turbulent boundary layer occurs, so true laminar behavior could be expected downstream had the test section been longer and the level of acceleration maintained.

Flow D also has a linearly increasing K distribution but only for $x < 132$ inches. dK/dx is more than twice that for flow C. As in flow C, the initial upstream logarithmic velocity profile progressively decays downstream. Figure 5 shows that the wake strength also decreases to zero near the minimum H location, shown at about 135 inches in figure 6. The location of the minimum H occurs in the region where K is a maximum, while in flow C it occurs at a much

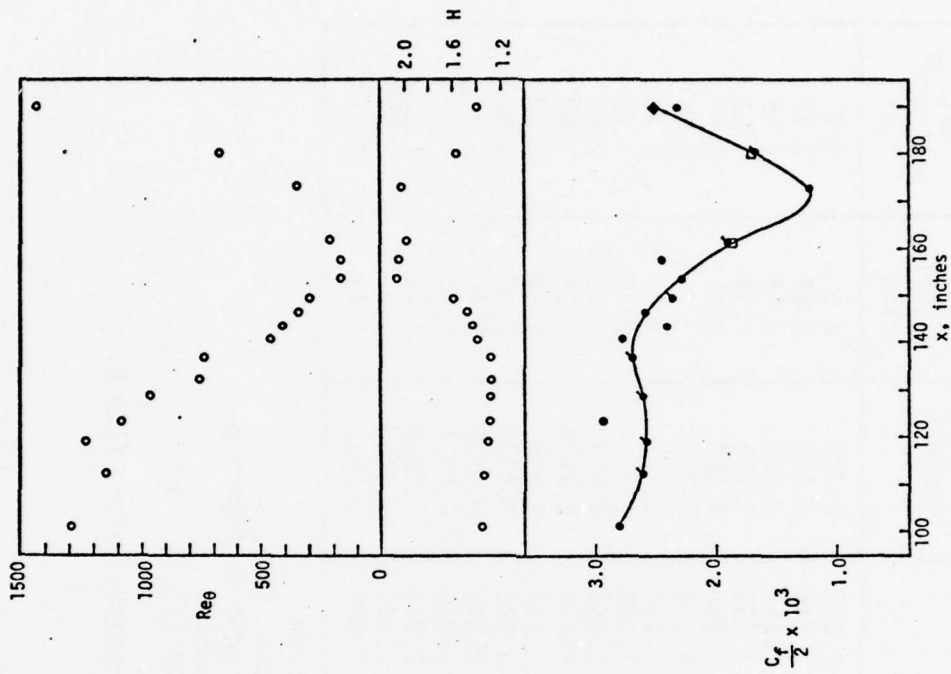


Figure 6. Re_θ , H , and $C_f/2$ for flow D. $C_f/2$ values from table 2: \circ , unshifted wall profile; \bullet , shifted wall profile; \diamond , logarithmic profile with $K = 0.4$; \square , momentum integral equation.

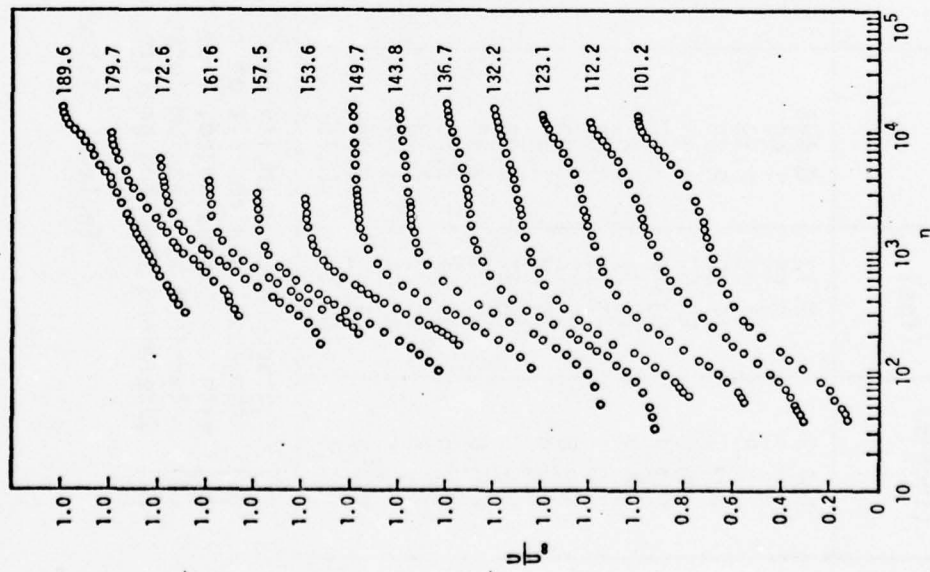


Figure 5. Mean velocity profiles for flow D. Streamwise location in inches to right of each profile. Note displaced ordinate scales.

Station (inches)	U_{∞}^a (fps)	$(K \times 10^6)^b$	Re_{θ}	H	$\delta_{0.99}$ (inches)	$\frac{C_f}{2} \times 10^3$	
						wall profile $\pm 10\%$	best estimate ^c $\pm 10\%$
101.2	9.12	0.495	1294	1.352	2.409	2.9	2.9
112.2	9.55	1.68	1156	1.346	2.243	2.62	2.62
118.8	11.26	2.39	1236	1.311	2.168	2.58	2.58
123.1	11.22	2.85	1087	1.293	2.053	2.94	2.58
128.6	13.53	3.44	965	1.286	1.889	2.61	2.61
132.2	13.72	3.85	761	1.264	1.756	?	2.65
136.7	16.71	3.85	740	1.281	1.477	2.70	2.70
140.7	17.75	3.85	464	1.388	1.113	2.79	2.70
143.8	21.02	3.85	419	1.436	0.908	2.42	2.65
146.8	22.67	3.62	347	1.478	0.7544	2.60	2.59
149.7	26.37	3.33	307	1.583	0.535	2.37	2.49
153.6	30.68	2.94	168	2.069	0.1183	2.30	2.32
157.5	37.81	2.55	166	2.043	0.0900	2.46	2.12
161.6	48.39	2.13	219	1.980	0.0871	1.91	1.87 ^d
172.6	83.55	1.02	355	2.028	0.0984	1.22	1.22 ^d
179.7	94.82	0.306	677	1.567	0.1436	1.67	1.72 ^d
189.6	102.1	0.157	1432	1.408	0.2477	2.43	2.54 ^e

- (a) measured when velocity profile measured.
- (b) from least squares fit of rake and cast data.
- (c) with exceptions noted, from faired curve on figure 6.
- (d) determined by momentum integral equation.
- (e) determined from log profile, equation (5), $\Omega = 0.40$.

Table 2. Values of parameters along flow D.

lower K value. Downstream the profiles assume an increasingly more laminar-like character as Re_θ drops below 360 until about 157.5 inches, even though K decreases downstream of 144 inches. No profile similarity is observed.

Between 157.5 inches and about 172.6 inches the momentum and displacement thicknesses, θ and δ^* , remain about constant, giving rise to about a constant shape factor ($H \equiv \delta^*/\theta$) of about 2.0. As noted in section 3.7 below, intermittency measurements downstream of 157.5 inches indicate that considerable turbulence is redeveloping. At the 189.6 inches location a thick logarithmic region $500 < \eta < 5000$ is observed, so that this flow is developing into a typical low acceleration turbulent boundary layer. The wake strength is also observed to be increasing.

Simpson and Wallace (1975) found that for each of flows A and B the location of the H minimum was closely related to where the wake strength was zero and where entrainment of free-stream fluid ceased. For flows C and D, the mass flux in each boundary layer as reflected by $U_\infty(\delta - \delta^*)$ increases until about 165 inches and 135 inches, respectively, as shown in figures 7 and 8. This parameter decreases downstream in both flows but again increases downstream of about 157.5 inches in flow D as a low acceleration turbulent boundary layer develops. These plots of experimentally deduced values indicate that there was entrainment of non-turbulent fluid into each boundary layer until the minimum H locations. As in the cases of flows A and B, the intermittency measurements discussed below indicate that after the

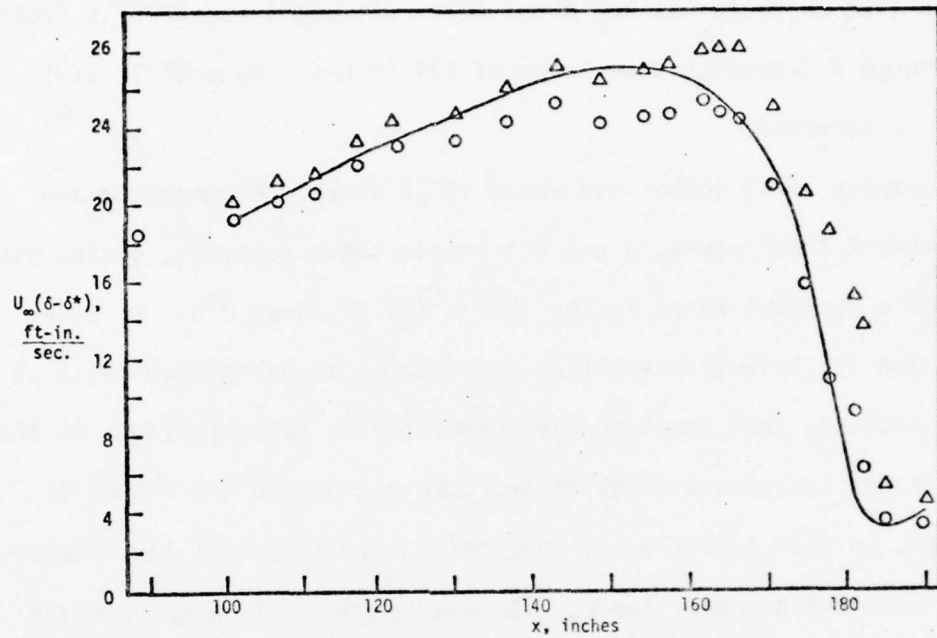


Figure 7. Mass flux in boundary layer of flow C, $U_\infty(\delta - \delta^*)$: \circ , $\delta = \delta_{0.99}$; \triangle , $\delta = \delta_{0.995}$.
 Solid line - equation (21) results.

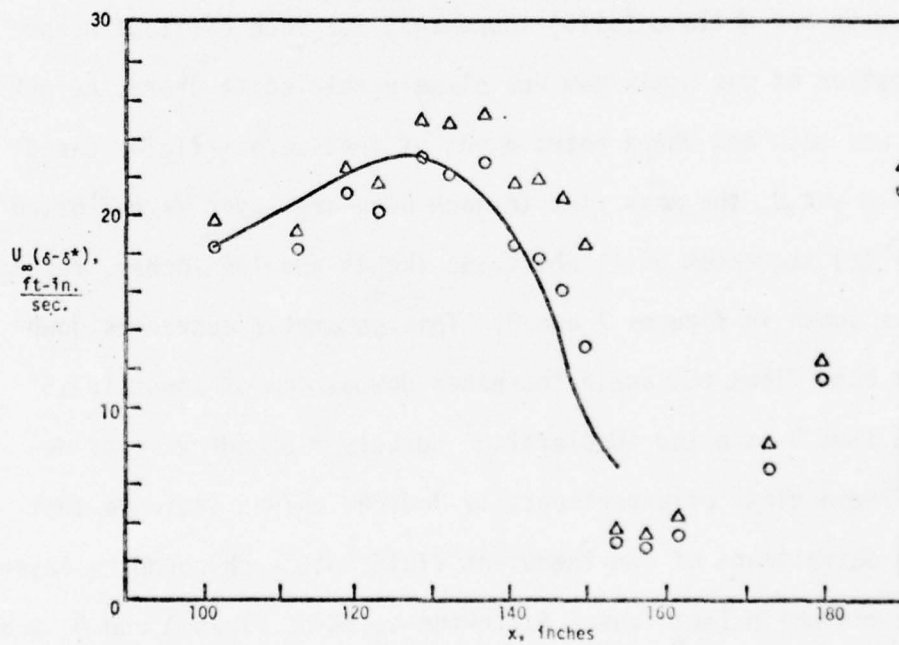


Figure 8. Mass flux in boundary layer of flow D, $U_\infty(\delta - \delta^*)$: \circ , $\delta = \delta_{0.99}$; \triangle , $\delta = \delta_{0.995}$.
 Solid line - equation (21) results.

cessation of entrainment the intermittent turbulent/non-turbulent region lies outside δ . Thus there is no mean velocity gradient $\partial U/\partial y$ and no wake-like tail in this region and no mechanism for engulfment of non-turbulent fluid by the intermittent bulges is possible. The model proposed by Simpson and Wallace for the entrainment process in a strongly accelerated boundary layer is discussed in section 4 below.

3.3 Skin-friction results

The skin-friction coefficient $C_f/2$ was primarily determined by two methods: the velocity profile near the wall and the logarithmic velocity profile relationship for unaccelerated flow regions. The momentum integral equation

$$\frac{C_f}{2} = \frac{d\theta}{dx} + KRe_\theta (2 + H) \quad (1)$$

was used some for flow D when both terms of the right side were positive and relatively certain.

The velocity profile near the wall can be derived from the differential momentum equation, neglecting the convective and turbulent transport terms:

$$\nu \frac{\partial^2 U}{\partial y^2} = \frac{1}{\rho} \frac{dP}{dx} = \frac{-U_\infty^3 K}{\nu} \quad (2)$$

Integrating equation (2) produces

$$\frac{C_f}{2} = \frac{\partial f}{\partial \eta} + K\eta \quad (3)$$

and the velocity profile upon integration of equation (3)

$$\frac{U}{U_\infty} = f = \frac{C_f}{2} \eta - \frac{K\eta^2}{2} \quad (4)$$

Equation (4) was used with experimental velocity measurements for $5 \leq y^+ = \eta\sqrt{C_f/2}$ to determine $C_f/2$. Oka and Kostić (1972) noted that hot-film and hot-wire measurements are strongly influenced by conduction to the test wall for $y^+ < 4$. For velocity profiles with logarithmic regions it is known that equation (4) does not well describe the velocity profile for $y^+ > 6$, so only points in the range $5 < y^+ < 6$ were used. For the more laminar-like profiles experimental data with $y^+ > 6$ were also used.

Logarithmic velocity profiles in unaccelerated or weakly accelerated flow regions are described by the relation

$$\frac{U}{U_\infty \sqrt{\frac{C_f}{2}}} = \frac{1}{\Omega} \ln \left| \eta \left(\frac{C_f}{2} \right)^{1/2} \right| + C \quad (5)$$

where $\Omega = 0.40 (Re_\theta/6000)^{-1/8}$ (Simpson, 1970) for low Reynolds number boundary layers with $Re_\theta < 6000$. A fit of equation (5) to experimental data was made for the two upstreammost profiles of flow C and to the downstreammost profile of flow D. In the latter case $\Omega = 0.40$ was used since a large logarithmic region that normally accompanies high Reynolds number boundary layers was observed. Results using this latter method are about $\pm 10\%$ uncertain.

For flow C the 0.001 inches diameter cylindrical hot-film sensor was located from the test wall within an uncertainty of about 0.001 inches. Considering the $\pm 1/2\%$ uncertainty of the velocity, the $C_f/2$ values shown in figure 4 appear to be about $\pm 15\%$ uncertain at 20:1 odds. This uncertainty value seems reasonable due to the scatter

of the data. The logarithmic velocity profile results from equation (5) are in close agreement with these results.

For flow D the 0.00015 inches diameter hot-wire sensor was located from the test wall with somewhat more uncertainty than for flow C since the wire was more difficult to illuminate and to observe by the cathetometer. This more fragile sensor was located at a safe distance of about 0.005 inches from the wall to prevent breaking the wire. Data from this smaller diameter sensor are less susceptible to velocity gradient effects so the near wall velocity profiles for $y^+ > 4$ are believed to be of higher quality than those of flow C. For each velocity profile point a least squares fit of equation (4) to the five surrounding data points was made to deduce the slope $\partial f/\partial n$ at that point. $C_f/2$ can be eliminated from equations (3) and (4) to produce

$$\eta = \frac{-\frac{\partial f}{\partial n} + \sqrt{\left(\frac{\partial f}{\partial n}\right)^2 + 2Kf}}{K} \quad (6)$$

from which the proper sensor distance from the test wall could be computed from K , f , and $\partial f/\partial n$. For flow D equation (6) was used to determine the required change in the y direction for a self-consistent velocity distribution near the wall. Values within about 5% of one another were obtained for successive points in a given velocity profile. As given in Appendix B these shifts in the y direction are no more than ± 0.005 inches and therefore are reasonable.

Figure 6 shows relatively less scatter in the wall profile results than shown for flow C, thus an estimated uncertainty of $\pm 10\%$

seems reasonable. The logarithmic profile $C_f/2$ result at 189.6 inches is in good agreement with the $C_f/2$ result from equation (4) with no y direction shifting. Results from equation (1) at 161.6 and 179.7 inches are also in good agreement with the wall profile results.

Smooth curves of "best estimate" values for $C_f/2$ are shown on figures 4 and 6 with values given in Tables 1 and 2. While these curves were just faired among the points shown on those figures within about 15% and 10%, respectively, they are probably representative of the variation of $C_f/2$ along each flow. From the laminar sink flow (Schlichting, 1968), i.e. a constant K flow, one can obtain the expression

$$\frac{C_f}{2} = \sqrt{\frac{4}{3}} K \quad (7)$$

so for the maximum K of about 3.83×10^{-6} achieved in these two flows, $C_f/2 = 2.26 \times 10^{-3}$. Near the maximum K for each of flows C and D the experimental $C_f/2$ values are above this value as they should be since considerable turbulent momentum transport is still present. While one cannot exactly compare results from different K distributions, it is interesting that the experimental results shown in figure 6 for flow D are always greater than or about equal to those given by equation (7) with the local K value. In the region near 165 inches where the turbulence intermittency is near zero at the wall, as discussed in section 3.7 below, the skin friction values are about equal. Downstream of this region the experimental $C_f/2$ values increase rapidly as turbulence redevelops.

3.4 Reynolds stresses distributions

Figures 9 and 10 show intensity $\sqrt{u^2}/U_\infty$ profiles for flows C and D from the fluctuation portion of the linearized hot-film and hot-wire signals. In flow C the maximum intensity remains at about 0.1 and is located in the range of $300 < \eta < 400$ up until $K > 3.6 \times 10^{-6}$ at about 181 inches, after which the normalized intensity decays and the maximum intensity location moves to a greater η value. The hump in the outer region of the upstream intensity profiles vanishes just downstream of the cessation of entrainment at about 165 inches. Between 165 inches and 181 inches the acceleration of the wall region flow alone is apparently sufficient to maintain the same level of turbulence production as upstream. In other words the entrainment of high momentum free-stream fluid performs no role.

Flow D exhibits the same behavior but the outer region hump does not completely vanish until about 143.8 inches. The maximum intensity is located in the range of $200 < \eta < 400$. Beginning at about 153.6 inches, where $C_f/2$ begins to drop rapidly, the value and η location of the maximum intensity decreases. After retransition to a low acceleration turbulent boundary layer begins, the maximum intensity remains at about 0.08 but the η location of the maximum increases. At 189.6 inches the intensity profile of a normal low acceleration turbulent boundary layer is emerging.

The split-film probe was used to determine $\overline{u^2}$, $\overline{v^2}$, and $-\overline{uv}$ for flow C. No split-film probe measurements were attempted for flow D. The mean velocity profiles showed very good agreement with those

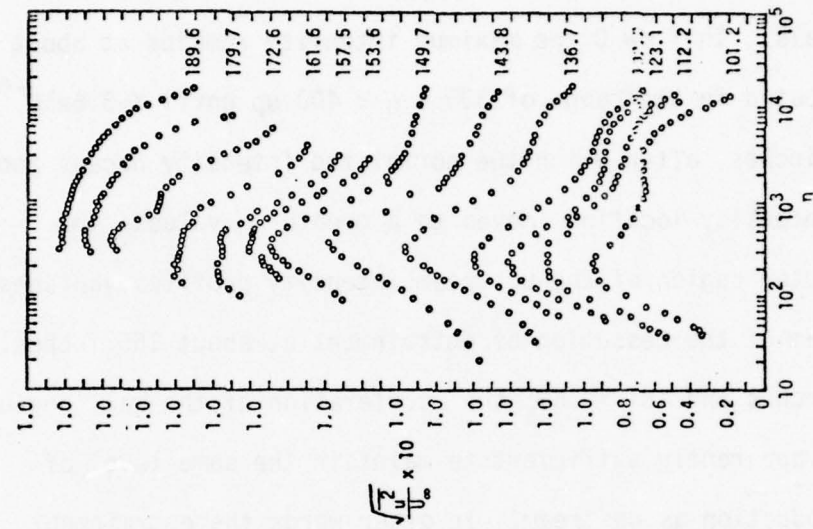


Figure 9. Streamwise intensity profiles for flow C. Note displaced scales. Station position in inches at right of each profile.

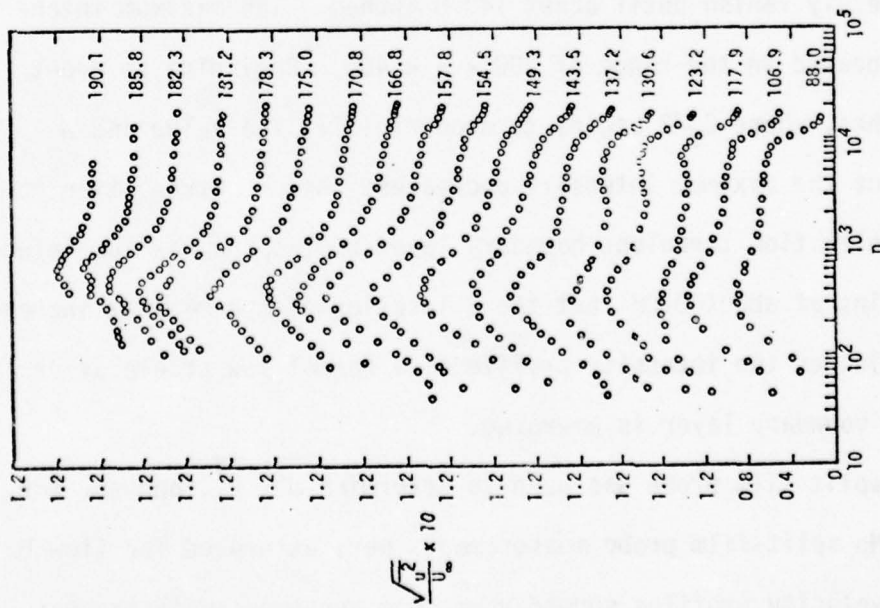


Figure 10. Streamwise intensity profiles for flow D. Note displaced scales. Station position in inches at right of each profile.

measured with a single film boundary layer probe. The deviation was within the uncertainty of the calibration except at locations 171.3, 178.8, and 187.6 inches. At these locations the mean velocities below $\eta = 10^3$ were as much as 47% high nearest the wall yet were less than 2% high at $\eta=10^3$ and were less than 0.5% high at $\eta = 1300$ and beyond. At locations 101.7, 137.8, 149.6 and 162.4 inches, the mean velocity deviated from the single film probe by less than 3% from the wall to the freestream. The large deviation near the wall at higher freestream velocities may be due to the significantly greater velocity gradient effects which tend to cool the top film more than the bottom film.

The V component of velocity, when normalized against U_{eff} allowed comparison of the angle of flow ϕ with respect to the test wall since $\sin \phi = V/U_{eff}$. After accounting for the angle of the plane of the splits with the test wall, the angle of flow measured by the split-film probe at a point in the freestream was at worst within 1.4° of the flow angle at that point derived from the displacement thickness gradient and freestream velocity gradient. This difference is beyond 0.6° uncertainty in computing ϕ from the calibration equations plus the 0.2° uncertainty in ϕ due to approximation of the displacement thickness gradient. However, for 6 of the 8 profiles taken, the angles measured agree within that 0.6° uncertainty in ϕ .

The $\overline{u^2}$ fluctuations, as seen in figure 11, tend to show very poor agreement with those measured with the single film probe for $\eta < 10^3$. At $x = 137.8$ and 149.6 the discrepancy is apparent to

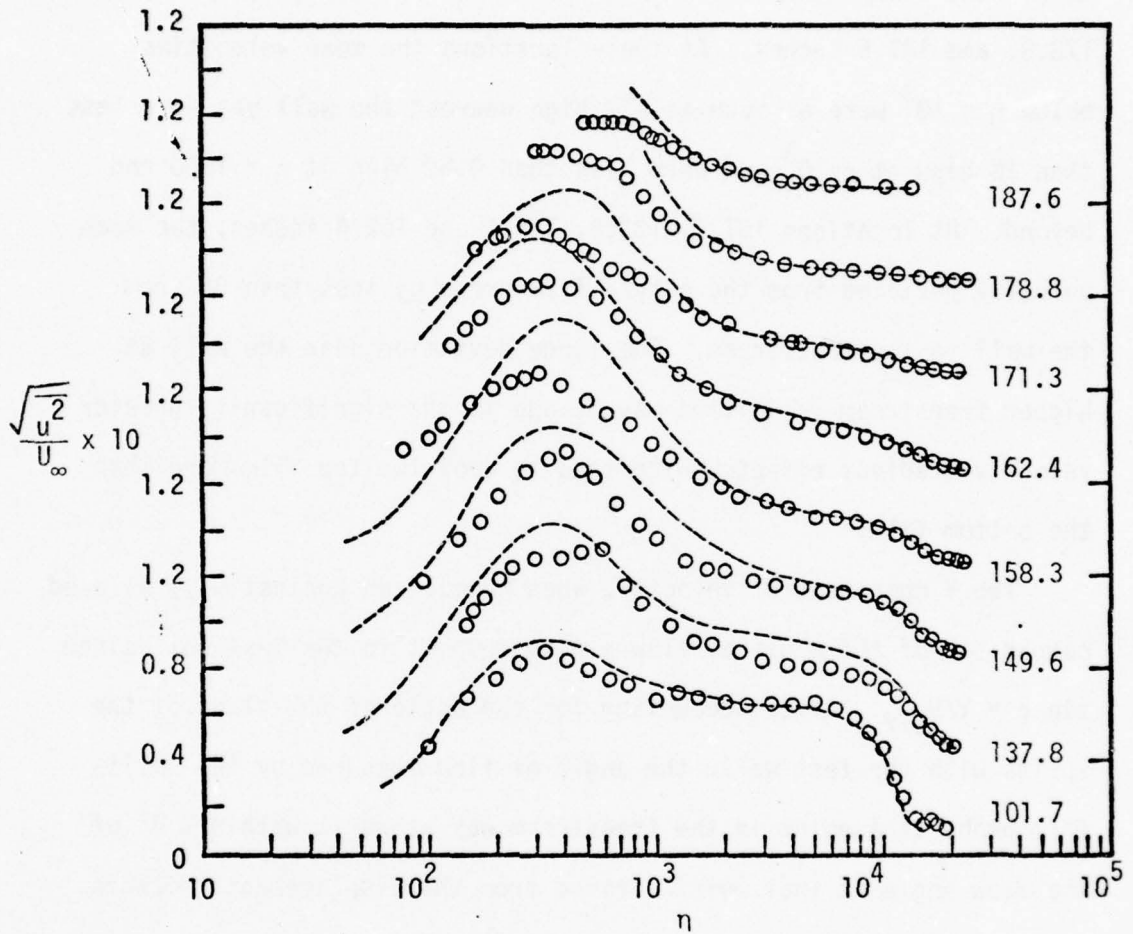


Figure 11. Streamwise fluctuation distributions from the split-film sensor for flow C. Profile location in inches at right of each profile. Dashed lines - normal hot-film results from figure 9 for nearby location. Note displaced ordinate scales.

$\eta = 10^4$. In all other cases the agreement is good from $\eta = 10^3$ to the freestream except at $x = 158.3$ where agreement is poor until η reaches 5000. The kinematic Reynolds shearing stress $-\overline{uv}$ also shares the $\eta = 10^3$ cutoff above which the data begin to seem reasonable. There is a rapid decrease in $-\overline{uv}$ as the flow accelerates as shown in figure 12. Also shown on this figure is the shearing stress profile for 190.1 inches generated from the momentum equation and U/U_∞ vs. η similarity. The outer region mean velocity profiles at 185.8 and 190.1 inches are similar well within 0.01 in U/U_∞ and K is constant. Thus the similarity assumptions are met for an asymptotic flow and the equation

$$\frac{-\overline{uv}}{U_\infty^2} = K \int_{\eta}^{\infty} (1 - f^2) d\eta - \frac{df}{d\eta} \quad (8)$$

describes the Reynolds shearing stress (Simpson and Wallace, 1975). The agreement must be considered good for $\eta > 2600$. Thus the results from the split-film for $-\overline{uv}$ are credible at least in locations where $\overline{u^2}$ is credible. The $\overline{v^2}$ quantities measured by the split-film are high in the viscous sublayer due to the high velocity gradient there. The data in the outer region, $\eta > 3000$, are more believable.

Many problems were encountered in using the split-film sensor. The calibration process was time-consuming and frequent checks were required to overcome anemometer drift. Anemometer drift at times caused the films to operate with different temperatures, thus producing thermal interference between films as well as introducing a slight velocity dependence on the yaw characteristics. The resistance

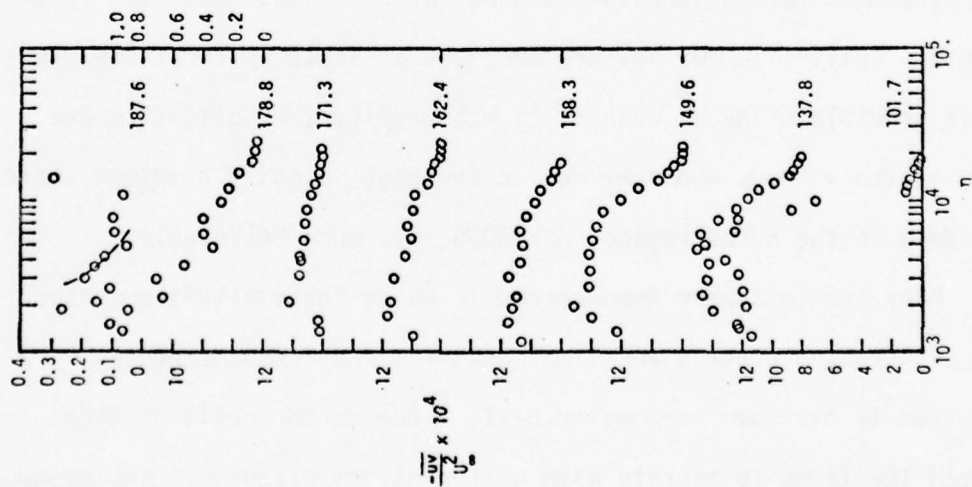


Figure 12. Reynolds shearing stress distributions from split-film sensor for flow C. Profile location in inches at right of each profile. Dashed line - mean velocity profile similarity result from eqn. (8). Note displaced ordinate scale.

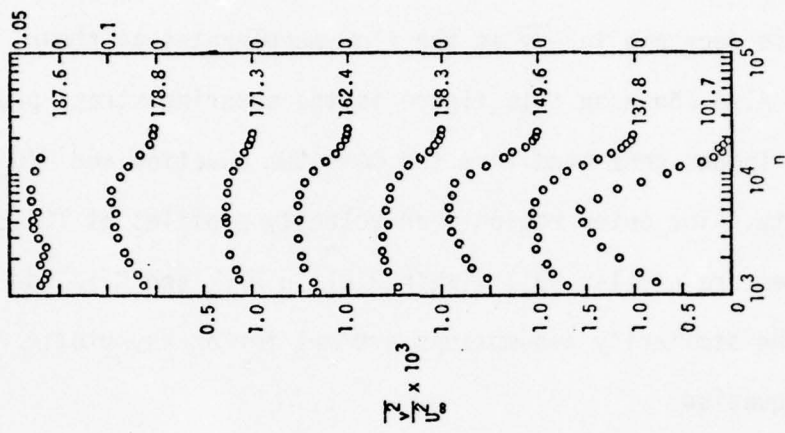


Figure 13. \bar{v}^2/U_0^2 distributions from the split-film sensor for flow C. Profile location in inches at right of each profile. Note displaced ordinate scales.

of the probe support structure sometimes changed when the probe was unplugged and then replaced in its support. Vortex shedding from the sensors produced high noise levels at increasing velocities. This noise introduced greater uncertainty in the fluctuation quantities. Velocity gradients near the wall produced unusually high V values at those points where V should be lowest. Several schemes were tried to correct for the influence of the high velocity gradient. Unfortunately, those corrections did not produce consistent results.

This experience with the split-film probe seems to be reasonably consistent with that of Sandborn (1976). He found $\sqrt{\overline{u^2}}/U_\infty$ to be closely the same as that measured by a single hot wire parallel to the test wall. $-\overline{uv}$ values from split-film data appeared to be close to the estimated true shear stress profile away from the wall where velocity gradients are sufficiently small. On the other hand, Young (1976) found that the split-film probe consistently produced a low $\sqrt{\overline{u^2}}$ by about 22% and a low $-\overline{uv}$ by about 26% in a two-dimensional channel flow. Thus, clearly the split-film results should be critically compared with results from other sensors for consistency.

3.5 Spectra measurements and dissipation estimates

The spectrum function $F(n)$ of $\overline{u^2}$ was obtained throughout each boundary layer at several streamwise locations, where

$$\overline{u^2} \int_0^\infty F(n) dn = \overline{u^2} \quad (9)$$

and n is the frequency in Hz. Simpson and Wallace (1975) discovered that a portion of $F(n)$ varied like n^{-1} for locations in the region $n > 1000$ after the cessation of entrainment in flow B. They found that Tchen's high mean vorticity spectral model (Hinze, 1975) relating $F(n)$ to the turbulence dissipation ϵ by

$$\frac{\epsilon v}{U_\infty^4} = \frac{3}{2} \alpha [nF(n)] \left[\frac{\overline{u^2}}{U_\infty^2} \right] \frac{\partial f}{\partial n} \quad (10)$$

seemed to hold.

Their data indicate that α is about 0.77 for flow B. Data from flow B were reanalyzed using equation (10) above. Equation (21) of Simpson and Wallace should have contained $\overline{u^2}$. The spectral data of Laufer (1954) in the logarithmic region of a pipe flow indicate that $\alpha \approx 0.88$ while Klebanoff's (1955) flat plate turbulent boundary layer produced flat $nF(n)$ spectra with $\alpha \approx 0.80$. In both of these latter cases, ϵ was evaluated by the equilibrium relationship

$$\epsilon = -\overline{uv} \frac{\partial U}{\partial y} \quad (11)$$

that is applicable for the logarithmic velocity profile region (Rotta, 1962). Here we wish to examine the spectra obtained for flows C and D and the range of applicability of equation (10) using $\alpha = 0.8$.

Representative first moments of the spectra $nF(n)$ for flows C and D are presented in figures 14 through 23. The hot-film and hot-wire sensor response was down 5% at 15 KHz, and 25 KHz, respectively. The data were recorded on tape and processed on the fast Fourier analyzer with a bandwidth of 2 Hz and 50 seconds record times. The

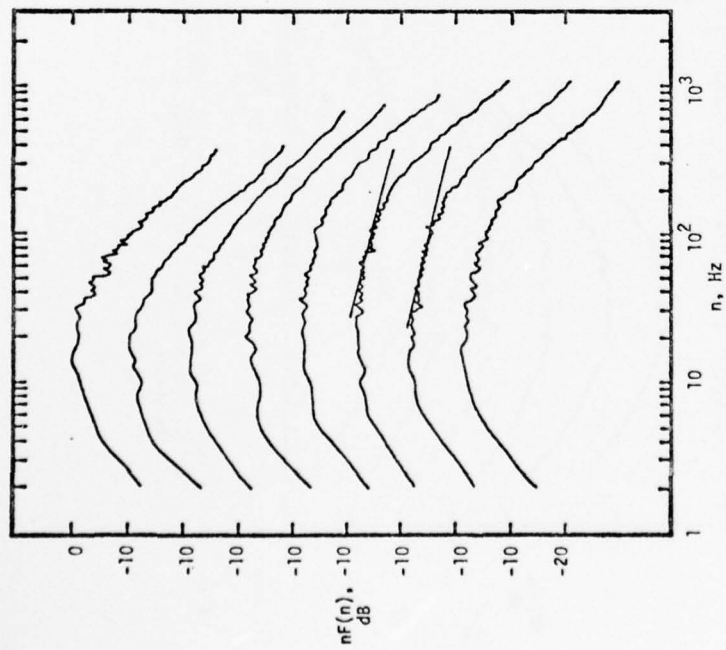


Figure 14. \bar{u}^2 spectra for flow C at 137.2 inches; from top to bottom $n = 54, 108, 350, 673, 1346, 2154, 4307, \text{ and } 8076$. Note displaced ordinate scales. Straight lines, $n^{-2/3}$ slope.

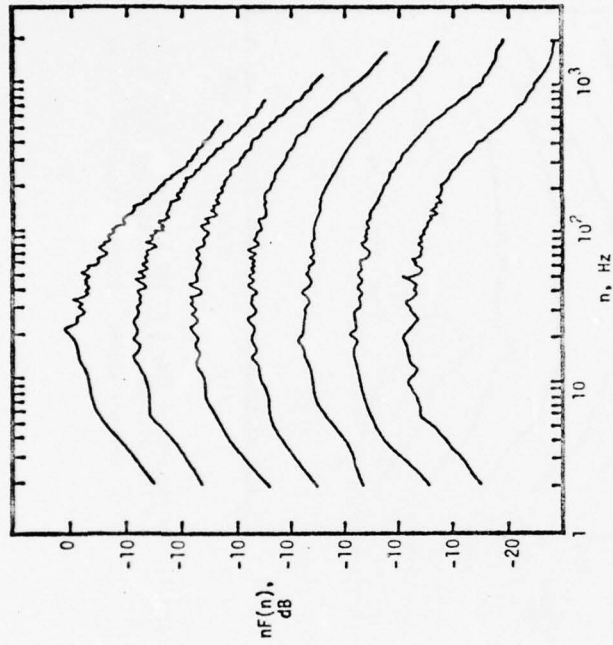


Figure 15. \bar{u}^2 spectra for flow C at 157.8 inches; top to bottom $n = 70, 454, 873, 1397, 2794, 5589, \text{ and } 8733$. Note displaced ordinate scales.

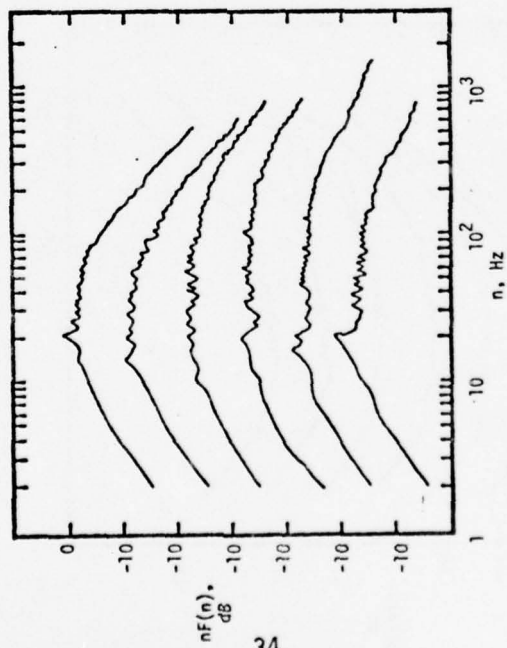


Figure 16. u^2 spectra for flow C at 170.8 inches; top to bottom $n = 153, 306, 815, 1528, 3057, \text{ and } 8152$. Note displaced ordinate scales.

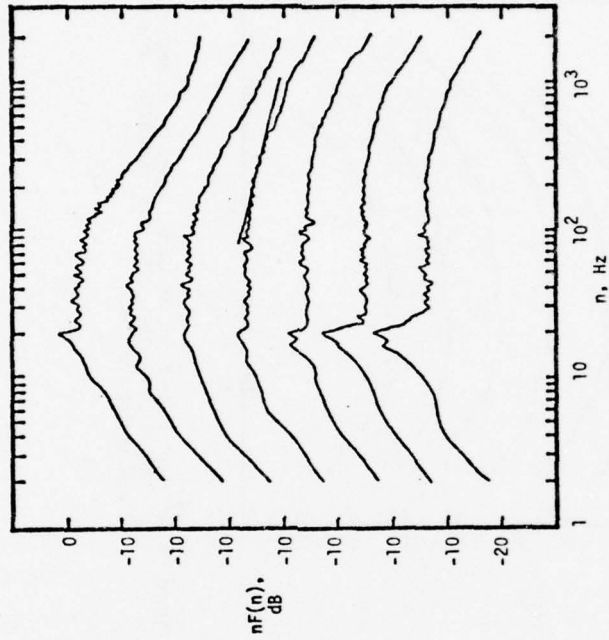


Figure 17. u^2 spectra for flow C at 182.3 inches; top to bottom $n = 180, 541, 901, 1532, 2252, 3604 \text{ and } 7208$. Note displaced ordinate scales. Straight line, $n^{-2/3}$ slope.

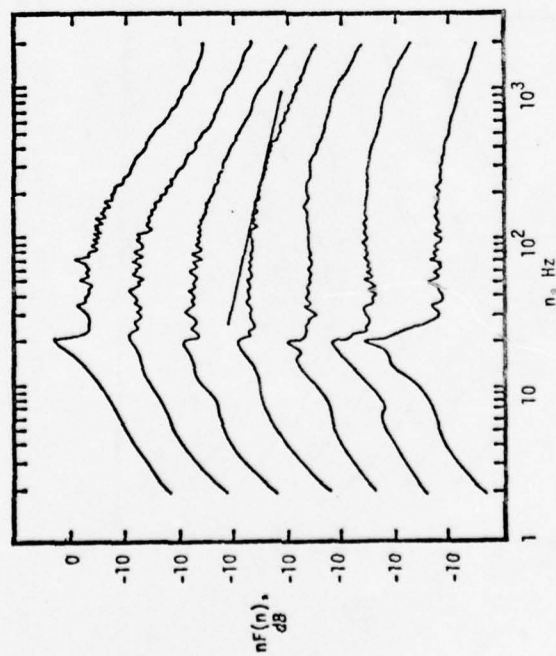


Figure 18. $\overline{u^2}$ spectra for flow C at 185.8 inches; top to bottom $n = 222, 444, 887, 1331, 1866, 2662, \text{ and } 7765$. Note displaced ordinate scales. Straight line, $n^{-2/3}$ slope.

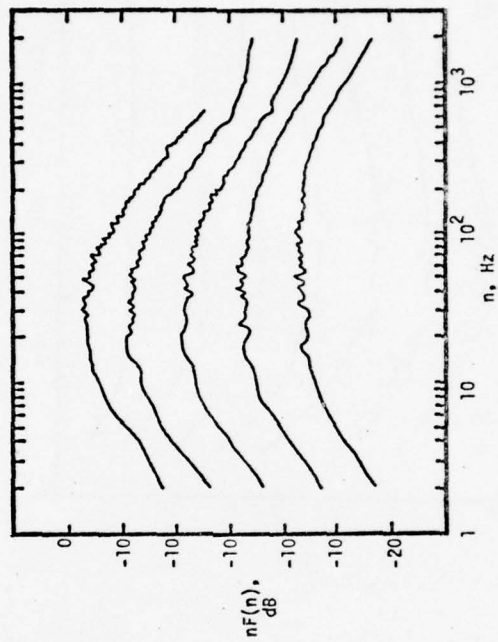


Figure 19. $\overline{u^2}$ spectra for flow D at 153.6 inches; from top to bottom $n = 153, 367, 673, 1131, \text{ and } 2201$. Note displaced ordinate scales.

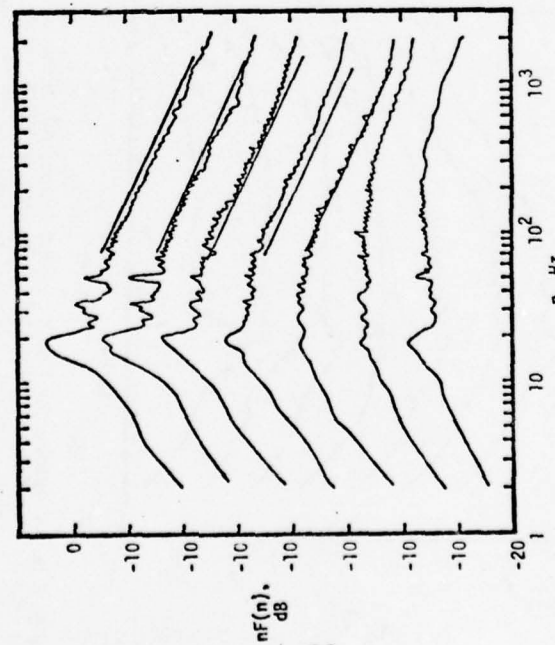


Figure 20. \bar{u}^2 spectra for flow D at 161.6 inches; from top to bottom $n = 135, 231, 328, 473, 834, 1919$ and 3848 . Note displaced ordinate scales. Straight lines, $n^{-1.3}$ slope.

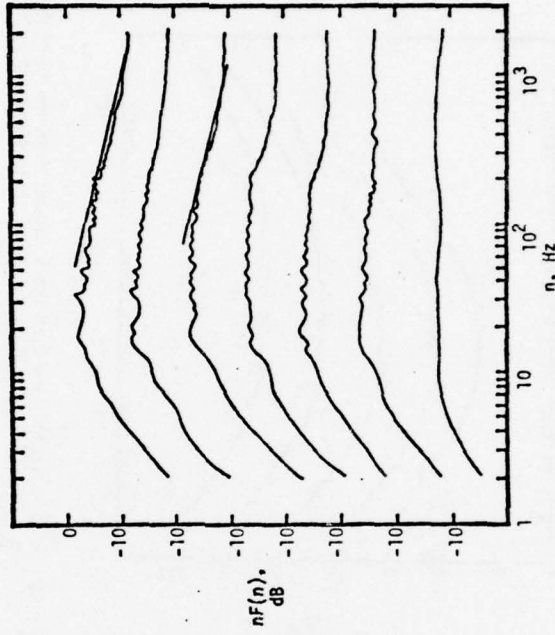


Figure 21. \bar{u}^2 spectra for flow D at 172.6 inches; from top to bottom $n = 333, 791, 1166, 1582, 2623, 4288$ and 6786 . Note displaced ordinate scales. Straight lines, $n^{-2/3}$ slope.

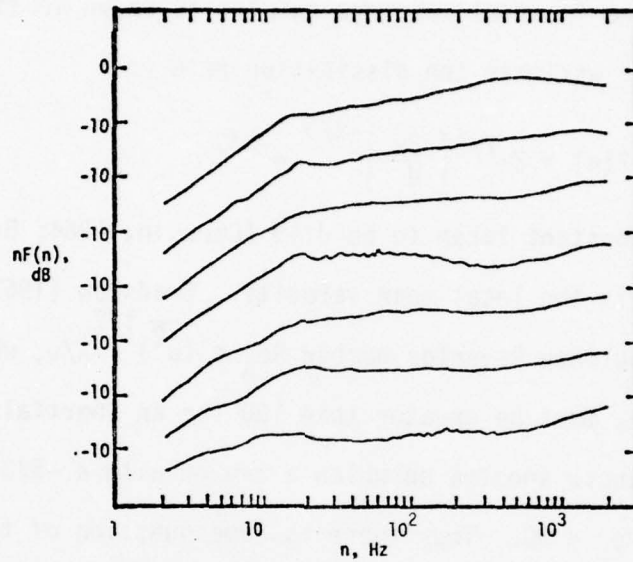


Figure 22. $\overline{u^2}$ spectra for flow D at 179.7 inches; from top to bottom $\eta = 283, 945, 1890, 3780, 5669, 7559,$ and 9449 . Note displaced ordinate scales.

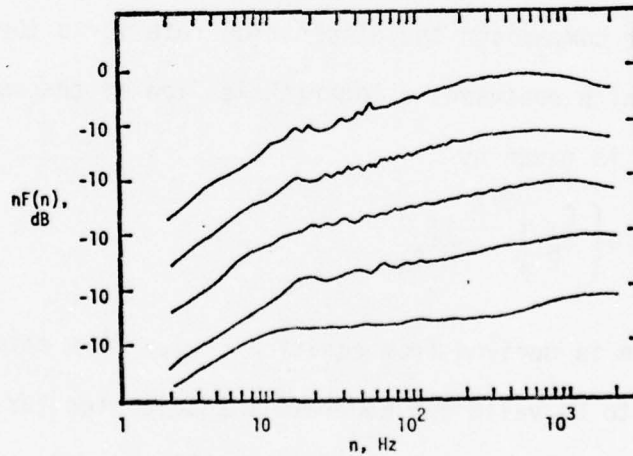


Figure 23. $\overline{u^2}$ spectra for flow D at 189.6 inches; from top to bottom $\eta = 305, 2034, 4069, 8138,$ and 15259 . Note displaced ordinate scales.

2 KHz upper frequency limit on the analyzer was not a serious limitation except for the data at the downstream stations in flow D.

For several of the spectral distributions, a small range of the -5/3 law of the inertial subrange existed as shown in figure 14, so it was used to estimate the dissipation rate ϵ :

$$\overline{u^2} F(n) = K\epsilon^{2/3} \left(\frac{2\pi}{U} \right)^{-2/3} n^{-5/3} \quad (12)$$

Here K is a constant taken to be 0.49 (Corrsin, 1964; Bradshaw, 1967a) and U is the local mean velocity. Bradshaw (1967b) suggested that the turbulence Reynolds number $Re_\lambda = (\overline{u^2})^{1/2} \lambda/\nu$, where $\lambda^2 = 15\nu \overline{u^2}/\epsilon$, must be greater than 100 for an inertial subrange to exist. For those spectra on which a region with a -5/3 slope was found, $35 < Re_\lambda < 80$. Thus there is some question of the validity of equation (12) even for these cases.

Figures 24 and 25 show the dissipation rate results for flows C and D. For comparison the dissipation rate for a turbulent boundary layer which possesses a logarithmic "law of the wall" mean velocity profile is given by

$$\frac{\epsilon\nu}{U_\infty^4} = \left(\frac{C_f}{2} \right)^{3/2} \frac{1}{0.4\eta} \quad (13)$$

This equation is derived from equation (11). This result would also be expected to be valid for moderately accelerated turbulent boundary layers since a logarithmic mean velocity profile would still exist. At the upstream stations the dimensionless dissipation $\epsilon\nu/U_\infty^4$ is the same order of magnitude for each flow from equations (10),

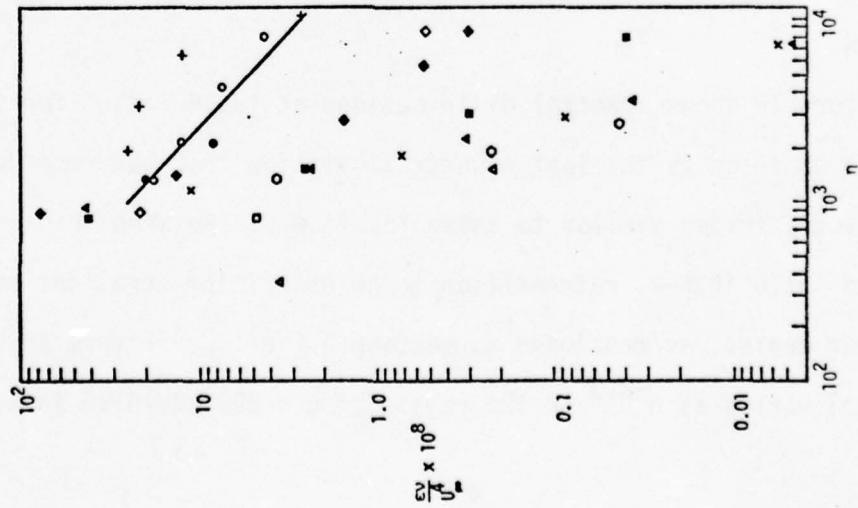


Figure 24. Dissipation results for flow C. Eqn. (12) results: + 106.9, ○ 137.2, ◇ 157.8, □ 170.8, △ 182.3. Eqn. (10) results: ● 137.2, ◆ 157.8, ■ 170.8, × 178.3, ▲ 182.3. ○ 185.8. Solid line - eqn. (13) with $C_f \times 10^3 = 2.2$.

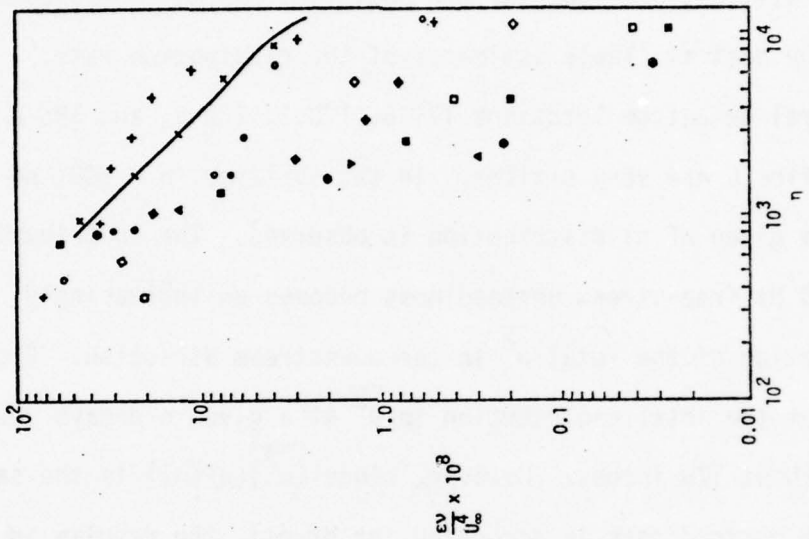


Figure 25. Dissipation results for flow D. Eqn. (12) results: + 101.2, × 112.2, ○ 123.1, ◇ 132.2, □ 140.7. Eqn. (10) results: ● 123.1, ◆ 132.2, ■ 140.7, ◆ 140.7, ● 146.8, ▲ 153.6, ▼ 161.1. Solid line - eqn. (13) with $C_f/2 \times 10^3 = 2.9$.

(12), and (13). The results from equation (12) for each flow near the 100 inches location are closely the same. At 137.2 inches in flow C the results from equations (10) and (12) are reasonably close for a given η when $\alpha = 0.8$ is used. Since the $nF(n)$ spectra at downstream stations are flat for $\eta > 800$, the results from equation (10) are the best available estimates of the dissipation rate.

Spectral data from locations 170.8, 178.3, 182.3, and 185.8 inches of flow C are very similar. In the sublayer, $\eta < 800$, no flat region of a given $nF(n)$ distribution is observed. The contribution from the 20 Hz free-stream unsteadiness becomes an increasingly greater portion of the total $\overline{u^2}$ in the downstream direction. Figure 9 shows that the total contribution to $\overline{u^2}$ at a given η decays downstream of about 178 inches. However, since $(\overline{u^2})(nF(n))$ is the same whether the unsteadiness is accounted for or not, the results in figure 24 should be unaffected. For a given η in the outer region, $\epsilon\nu/U_\infty^4$ decreases two orders of magnitude from 137.2 inches to 170.8 inches. Thereafter the decrease is much slower. In the inner region, $\eta < 1000$, $\epsilon\nu/U_\infty^4$ remains about the same order of magnitude all along the flow.

Figure 19 shows spectral distributions at 135.6 inches for flow D. This location is the last downstream station that was recorded with spectra shapes similar to those for flow C. Between this location and 161.6 inches, retransition to an entraining turbulent boundary layer begins, as mentioned in section 3.7 below. Figure 20 shows that $F(n)$ varies as $n^{-2.3}$ in the region of $\eta < 800$ at 161.6 inches,

where the intermittency is about 0.01. In the outer region at this location flat $nF(n)$ spectra are found. Note the relative importance of the 20 Hz unsteadiness. Downstream where the intermittency is progressively increasing, the spectral distributions are flatter. At 179.7 and 189.7 inches the peaks shift progressively toward 1 KHz as the low accelerated turbulent boundary layer redevelops. Notice that 20 Hz unsteadiness does not dominate the near wall spectra.

The dissipation results for flow D from equations (10) and (12) are in reasonably good agreement at 123.1 inches and in fair agreement at 132.2 and 140.7 inches. Between 132.2 and 161.1 inches the results from equation (10) are considered the best available estimates of the dissipation rate. For a given η in the outer region, $\epsilon\nu/U_\infty^4$ decreases two orders of magnitude from 123.1 to 161.1 inches, as was observed for flow C. As for flow C, $\epsilon\nu/U_\infty^4$ remains about the same order of magnitude in the inner region along this length of flow. Certainly the spectral behavior downstream of retransition needs further research.

3.6 Wall bursting frequencies and spanwise structure

The more or less periodic lift off or bursting process in the viscous sublayer has become accepted as the sequence of events that create the Reynolds shearing stress near the wall (Wallace et al., 1972; Nychas et al., 1973; Willmarth, 1975). On a short-time basis the velocity fluctuations in the sublayer produced by the bursting process vary across the sublayer in the spanwise direction. The data of Gupta et al. (1971) indicate that the short-record-time

normalized cross-correlation of fluctuations $\hat{sR}_{uu}(z, T_s)$ could be represented by a spanwise periodic function. Their results indicate that the short-record-time T_s over which the cross-correlation is averaged must be less than about 20 bursting periods in order for the periodic spanwise structure to be detectable. Simpson and Wallace (1975) measured the average frequency of bursting and the long-time spanwise cross-correlation of fluctuations for two sink-flow type strongly accelerated turbulent boundary layers, flows A and B. Here the results from flows C and D are presented.

Strickland and Simpson (1973, 1975) assumed that the short-time autocorrelation time scale from a flush wall hot-film sensor and the bursting period were equal. Histograms of the frequency characterized by the time to the first peak on these autocorrelations were constructed and the corresponding frequency of the peak of each histogram was taken as the characteristic frequency. The histograms appeared to have a log-normal probability distribution, so this peak frequency was also the median frequency. They also proved a one to one correspondence between this characteristic frequency and the peak of the first moment of the wall shearing stress spectra $nF(n)$. Also, examination of spectral data from zero pressure gradient boundary layers produced bursting frequencies in agreement with those previously reported. More recently, Simpson (1976) used a pattern recognition algorithm to determine the average bursting frequency from flush surface hot-film signals produced in the Max-Planck-Institut für Strömungsforschung oil channel. This average bursting

frequency closely agreed with the peak of the $nF(n)$ spectral distribution of these signals.

As was done for flows A and B, the peak of each $nF(n)$ curve for flows C and D was deduced as the bursting frequency for a given wall spectral distribution. The results are given in table 3. As it is clear from figures 26 and 27, it is difficult to select a precise single frequency at which $nF(n)$ is a maximum for a given distribution. Consequently, a range over which the peak frequency definitely occurs is also presented in table 3.

Two types of non-dimensionalizing parameters have been used in previous bursting frequency studies, inner variables and outer variables. Inner variables are the shear velocity U_τ for the velocity scale and ν/U_τ for the length scale. This scaling does not correlate other available bursting data. The bulk of available bursting frequency results for turbulent boundary layers correlate using the outer flow velocity and length scales, U_∞ and δ . For zero pressure gradient boundary layers $U_\infty/\delta n_D$ is about 5 (Rao et al., 1971) and varies between 11.7 and 8.35 for the separating turbulent boundary layer of Simpson et al. (1974). It should be noted that this large eddy outer variables scaling continued even after the boundary layer separated.

For flow A presented by Simpson and Wallace (1975), $U_\infty/\delta n_D$ started at about 5 at 89.2 inches, decreased to about 3.5 at about 139 inches or the location of minimum H, and then monotonically increased to a value above 50 at the last measurement station. The

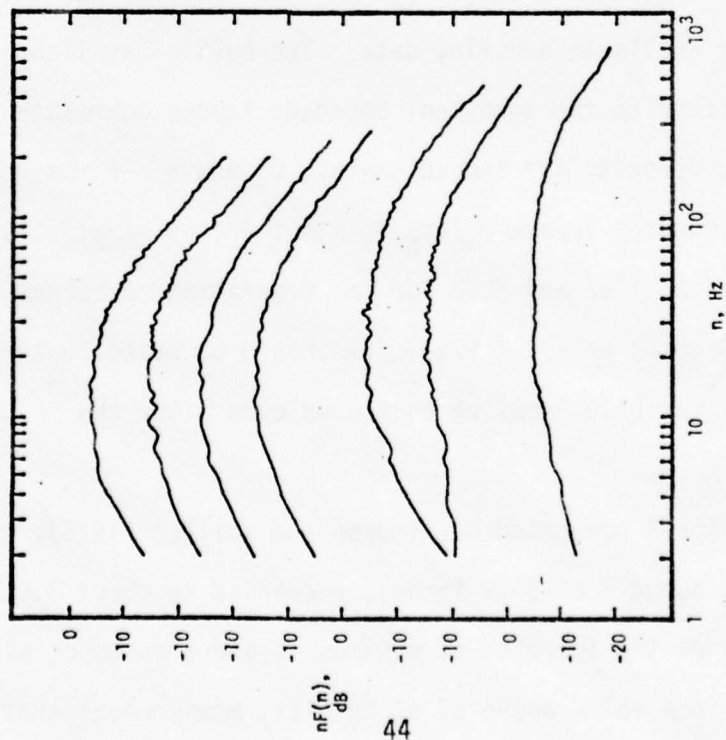


Figure 26. Typical flush-wall hot-film spectra, flow C. Station location from top to bottom: 105.0, 122.0, 135.5, 156.3, 171.8, 184.2, and 186.2. Record times 100 sec. Note displaced ordinate scale.

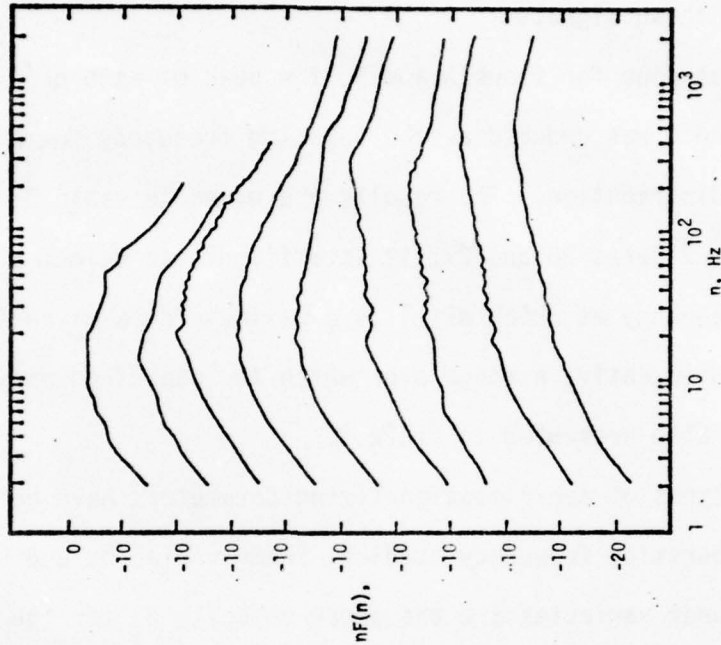


Figure 27. Typical flush-wall hot-film spectra, flow D. Station location from top to bottom: 122.0, 135.5, 158.3, 171.8, 175.2, 177.4, 182.0, 184.2, and 186.2. Record times 50 sec. Note displaced ordinate scale.

bursting frequency n_b apparently reached about a constant value after the asymptotic condition was achieved, so an increasing $U_\infty/\delta n_b$ reflects the fact that U_∞ increases and δ decreases faster than n_b increases. For flow B $U_\infty/\delta n_b$ remained nearly constant at about $3(\pm 1)$ until the location of a minimum in H , downstream of which it also increased monotonically to a value of about 90 at the last measurement station. The bursting frequency n_b was virtually constant all along flow B. The outer variables parameter $U_\infty/\delta n_b$ was no better a correlation parameter for these data.

The results for flow C indicate that the bursting frequency increased up to about 165.3 inches or where H was about a minimum and where entrainment ceased. The plateau on the $nF(n)$ spectral distributions existed over an increasingly wider frequency range at downstream locations. The low frequency end of the plateau remained at about 25 Hz. The results from these three flows indicate that they are non-equilibrium flows at least up until the cessation of entrainment. Thus no equilibrium non-dimensional parameter such as $U_\infty/\delta n_b$ should have a constant value upstream of the minimum in H . Downstream of the minimum H location there was no entrainment, so the large eddy structure and the intermittent turbulent/non-turbulent outer region flow were not creating new bulges. Thus the bursting frequency and the frequency of passage of the intermittent bulges (see section 3.7 below) were constant in this downstream region.

For flow D the bursting frequency increased until near the location where H was a minimum, after which it remained constant until

Flow C			Flow D		
Station (inches)	Peak frequency, n_b , Hz	Range of peak, Hz	Station (inches)	Peak frequency, n_b , Hz	Range of peak, Hz
90.2	15	13-18	105.0	12	10-15
105.0	12	10-15	110.4	15	10-20
110.4	13	10-20	122.0	15	10-20
117.3	15	10-20	129.9	19	15-25
122.0	16	13-20	133.5	18	15-25
129.9	16	11-20	135.5	18	15-20
131.6	16	11-20	139.7	20	15-25
135.5	20	14-22	147.6	20	15-25
138.6	16	10-20	158.3	25	20-30
139.7	16	10-20	171.8	20	15-30
147.6	20	15-30	175.2	25	20-40
156.3	20	15-20	177.4	300	250-350
158.3	20	15-25	182.0	200	150-250
165.3	25	20-30	184.2	500	400-700
171.8	25	20-30	186.2	500	400-700
175.2	25	15-35	189.6	500	400-700
177.4	26	20-30			
182.0	26	20-30			
184.2	--	20-45			
186.2	--	20-100			

Table 3. Peak frequencies of $nF(n)$ spectral distributions from flush surface hot-film sensors.

Station (inches)	Z_{max}, mm	λ_{Z1}^+	Z_{min}, mm	λ_{Z2}^+	L_Z, mm	L_Z^+	$\frac{1}{2t_{min-max}}, Hz$
117.3	7.62	6.7	5.59	99	4.88	43.4	19
138.6	---	---	7.11	151	4.46	47.3	16
156.3	10.16	135	5.33	142	3.23	43.0	--
165.3	9.40	157	3.56	119	1.42	23.8	--
182.0	8.38	302	3.86	278	1.79	64.5	28
126.3	14.48	179	5.33	132	2.70	33.3	22
138.6	9.40	160	4.83	164	2.60	44.3	21
156.3	8.38	274	2.41	158	1.11	36.4	22
165.3	7.87	332	3.30	279	3.61	152.5	--
182.0	---	---	21.6	3480	12.50	1007	--

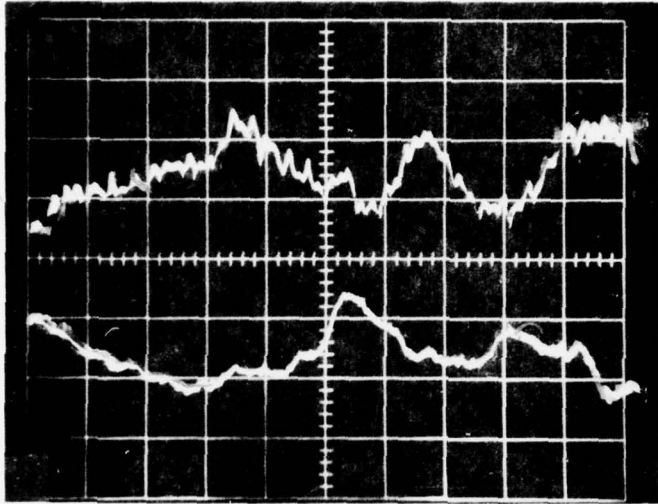
Table 4. Experimental results from the wall spanwise spatial cross-correlatives. First five entries, flow C; second five, flow D.

the beginning of retransition to a low accelerated turbulent boundary layer. As discussed in section 3.7 below, high velocity pulses are first detected at about 165.3 inches. Figure 27 shows that the wall sensor spectra are not appreciably affected until about 175.2 inches.

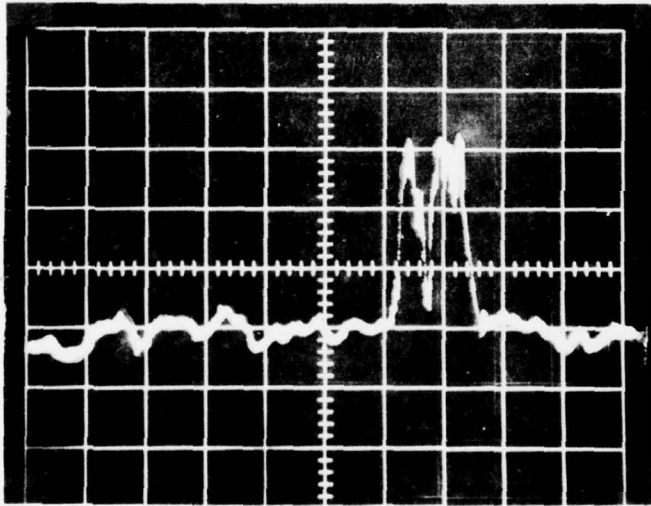
Figure 28(c) shows a typical signal trace for this location. Between 175.2 and 182.0 inches, a distinct local peak is observed in the spectra at frequencies an order of magnitude higher than observed upstream. This indicates that the high frequency oscillations that are contained in the higher velocity pulses are increasingly important. Downstream of 184.2 inches the laminar-like low velocity regions such as seen in figure 31 for 182.0 inches were no longer observed on signal traces. Thus the flow at the wall was always turbulent. Peak frequencies are observed in figure 27 to occur at an even higher frequency of about 500 Hz.

Several researchers have proposed that during the bursting process a hairpin or horseshoe vortex with trailing legs is formed (Willmarth, 1975). With this model, the counter-rotating trailing legs would produce fluctuations in the sublayer that are periodic in the spanwise or z direction on a short-time basis. Simpson (1976) noted that this model suggests motions too coherent to be consistent with experimental observations.

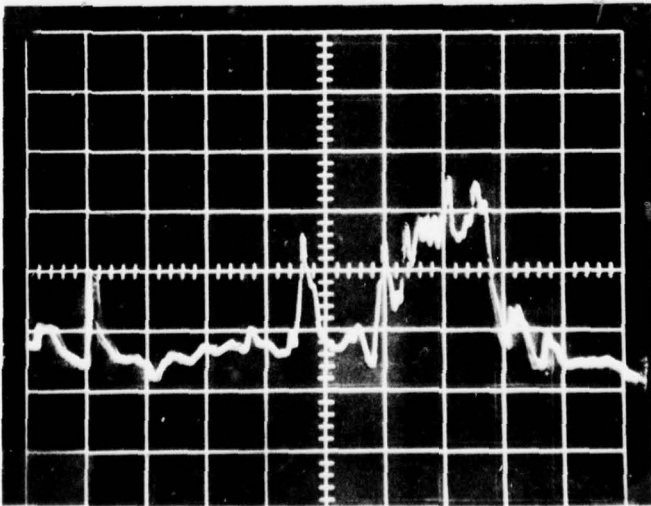
He alternatively proposed that "fingers" of high velocity fluid come from the outer region at a velocity much higher than sublayer mean velocities toward the wall and displace the low velocity fluid



(a)



(b)



(c)

Figure 28. Flush surface hot-film signals for flow D. Top photo: 138.6 inches, $\Delta Z = 4.83$ mm; top trace-movable sensor, 500 Hz low pass filtered, lower trace-fixed sensor, 1 kHz low pass filtered; 10 msec/div. Middle photo: 171.5 inches, 20 msec/div. Bottom photo: 175.0 inches, 5 msec/div.

t →

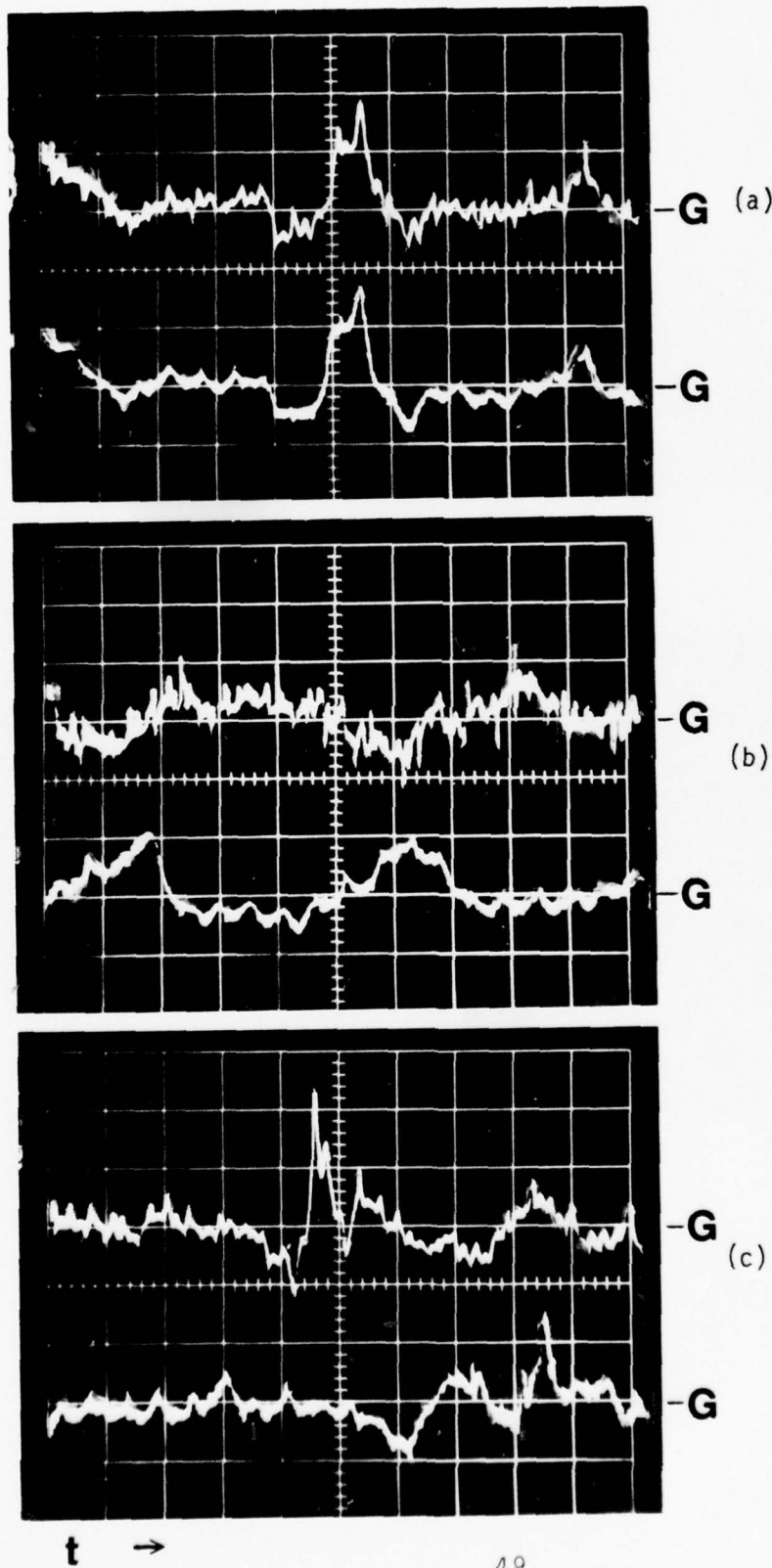


Figure 29. Flush surface hot-film signals from two-sensor unit at 156.3 inches for flow D. Top trace of each photo - moveable sensor; bottom trace - fixed sensor. From top to bottom $Z = 0$ mm, 2.29 mm, and 8.38 mm. Abscissa - 10 msec/div. Low pass filter: 500 Hz moveable sensor; 2 kHz - fixed sensor. G denotes mean signal level.

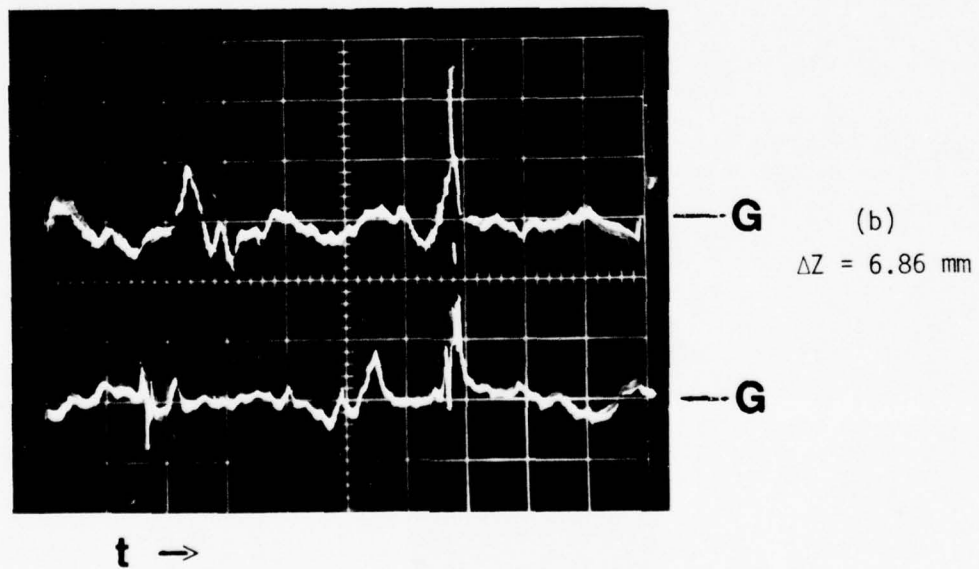
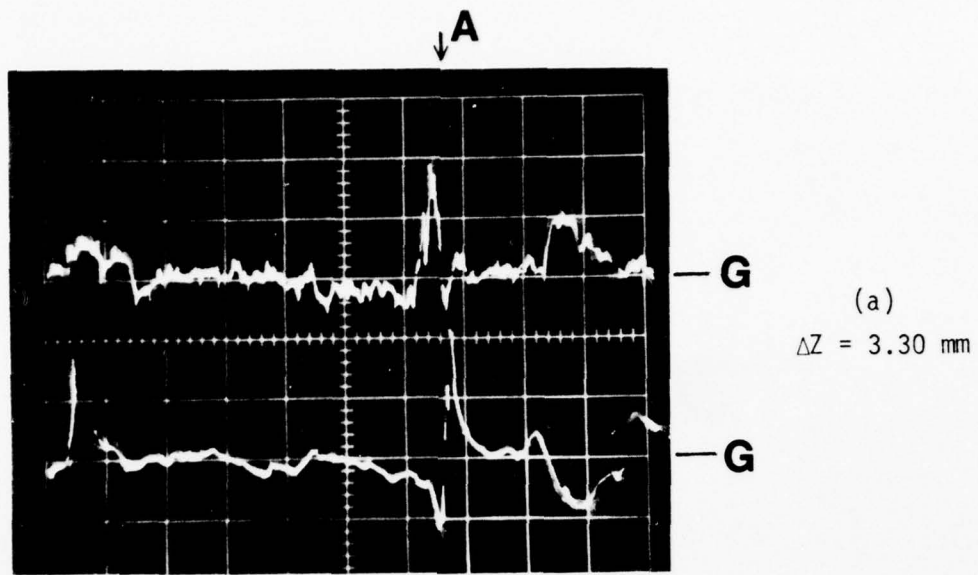


Figure 30. Flush surface hot-film signals from two-sensor unit at 165.3 inches for flow D. Top trace of each photo - moveable sensor; bottom trace - fixed sensor. Abscissa - 10 msec/div. low pass filtered at 2 kHz. G denotes mean signal level.

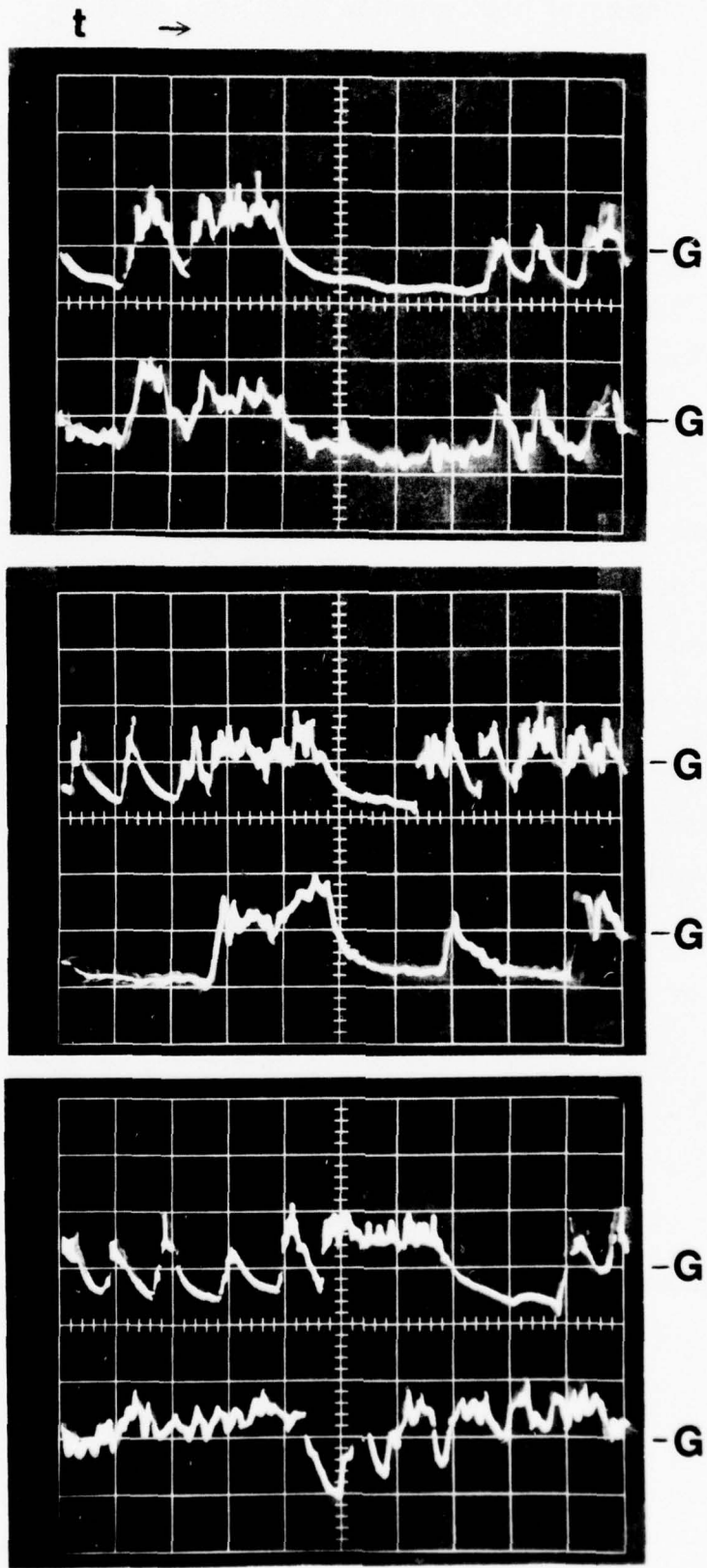


Figure 31. Flush surface hot-film signals from two-sensor unit at 182.0 inches for flow D. Top trace of each photo - fixed sensor; bottom trace - movable sensor. From top to bottom $\Delta Z = 0$ mm, 8.13 mm, and 19.56 mm. Abscissa - 5 msec/div. Low pass filter: 1 kHz - movable sensor; 5 kHz - fixed sensor. G denotes mean signal level.

to each side. These fingers of high velocity fluid were found for the MPI oil channel flow to be no less than $\Delta z^+ \approx 11$ nor greater than about $\Delta z^+ \approx 44$ in size and are spaced spanwise across the flow at average distances of about $\lambda_z^+ \approx 100$. There are curved fronts on these higher velocity fluid fingers so that the low velocity fluid just downstream at that instant must move aside to satisfy continuity requirements. Thus low velocity fluid trapped between two high velocity fluid fingers must move outward from the wall.

After the low velocity fluid has been "ejected" away from the wall, the two adjacent higher velocity fluid fingers coalesce. Since this fluid now occupies the wall region it progressively gives up its momentum until new high velocity fingers from the outer region force this fluid away from the wall and the process is repeated downstream. The spanwise locations of these high velocity fingers vary randomly for successive burst occurrences.

An interesting point is that these high velocity fingers must be formed so that the low velocity fluid can be ejected between them. Otherwise a blanket of higher velocity fluid would trap the low velocity fluid beneath. Stability considerations then require regions of high velocity fluid separated by low velocity ejections. The bulk of available experimental results for low pressure gradient flows show that the most preferred spacing of these higher velocity regions is $\lambda_z^+ \approx 100$. It appears unlikely that streamwise vortices that rotate more than one revolution are produced by the ejection process.

Some characteristics of the spanwise sublayer spatial structure for flows C and D were determined using the two sensor wall unit

described by Simpson and Wallace (1975). The unit was located spanwise across the tunnel with the direction of travel of the slider plate perpendicular to the streamwise flow direction. The signals from the two sensors were time-delay cross-correlated using the SAICOR model 41 correlator, with the record time for a given z-spacing time-delayed correlation being 65.5 seconds. For zero time delay, normalized spanwise cross-correlations $\hat{sR}_{\tau\tau}(z)$ such as shown in figures 32 and 34 result. Three characteristic lengths were deduced, the distance to the first correlation maximum z_{\max} , the distance to the first correlation minimum z_{\min} , and the integral length scale

$$L_z = 2 \int_0^{z_i} \hat{sR}(z) dz \quad (14)$$

The limit of integration z_i was taken as the largest available location for which data were available.

Figure 32 and table 4 indicate that for flow C the integral length scale progressively decreased until 165.3 inches and slightly increased thereafter. The parameters z_{\min} and z_{\max} are relatively easy to interpret, within 10% for the former and 20% for the latter. The results of Gupta et al. (1971) and Simpson (1975) indicate that z_{\min} is a somewhat more reliable spatial parameter than z_{\max} . These two parameters are normalized by the wall length scale ν/U_τ to produce the quantities

$$\lambda_{z1}^+ = \frac{U_\tau z_{\max}}{\nu} \quad \text{and} \quad \lambda_{z2}^+ = \frac{2U_\tau z_{\min}}{\nu} \quad (15)$$

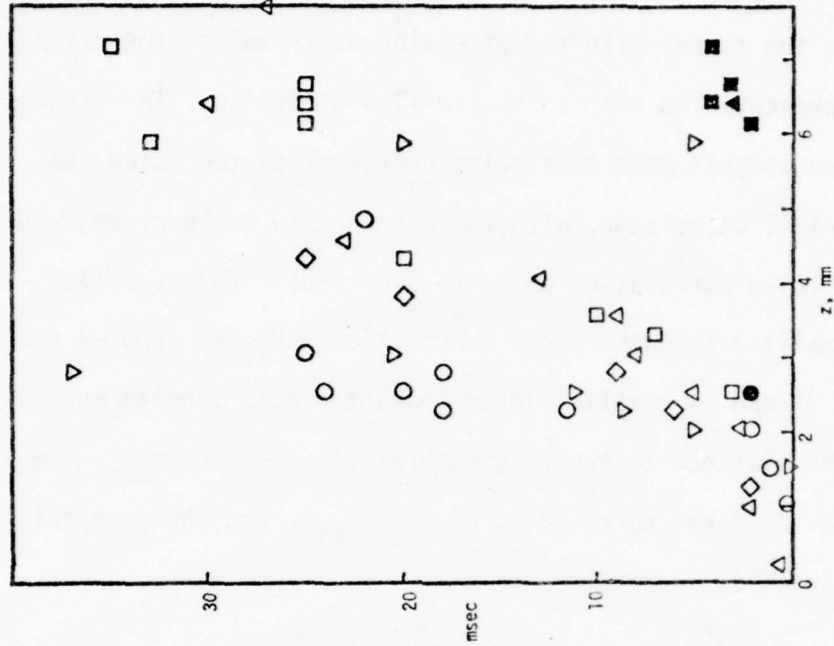


Figure 33. Observed minima and maxima from $\hat{R}_{tt}(z,t)$ data, flow C. Open symbols - maxima; solid symbols - minima: Δ , 117.3; \square , 138.6; \diamond , 156.3; ∇ , 165.3; \circ , 182.0.

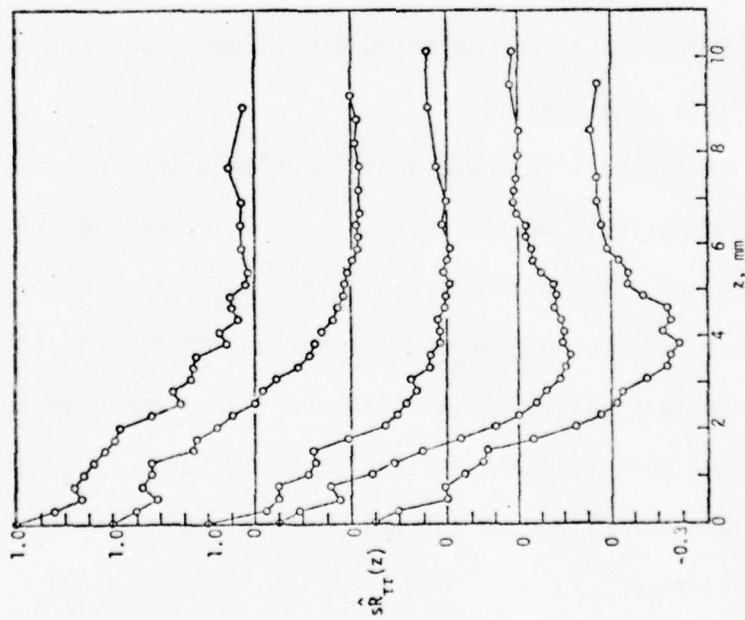


Figure 32. Normalized long time-averaged spanwise correlation $s\hat{R}_{tt}(z)$ results at the wall for flow C. Station locations from top to bottom: 117.3, 138.6, 156.3, 165.3, and 182.0 inches. Note displaced ordinate scales.

which have the value of about 100 for zero pressure gradient boundary layers. Only at 182.0 inches does λ_{z2}^+ increase appreciably from this value. At the two downstream locations, $\hat{sR}_{\tau\tau}(z)$ behaves more like the low Reynolds number cross-correlation computed by Simpson (1976). He used the Gupta et al. spanwise spacing probability distribution to compute $\hat{sR}_{\tau\tau}(z)$ when no large eddy outer region structures were present, i.e. $L_z/z_{\min} \rightarrow 0$.

Figure 34 and table 4 indicate the same type of behavior for flow D up to 156.3 inches with $L_z/z_{\min} \approx 1/2$. Figures 28(a) and 29 shows typical simultaneous signal traces for the two sensors. For the two downstream stations, the signals contained high velocity pulses intermittently as shown in figures 30 and 31 and as discussed in section 3.7 below. The length scale ratio L_z/z_{\min} was about 1.1 at 165.3 inches and 0.579 at 182 inches. The parameter λ_{z2}^+ is significantly larger than 100 at these two stations.

Several different models were examined in an attempt to correlate these λ_{z2}^+ results. As attempted for flows A and B, λ_{z2}^+ was compared with the data of Schraub and Kline(1965) when presented versus K. Just as Schraub and Kline found, λ_{z2}^+ is of the order of 300 for $K \approx 3 \times 10^{-6}$. However, for lower K values λ_{z2}^+ varied rather randomly between 100 to 164. In flow D λ_{z2}^+ remained only at about 158 at 156.3 inches even after the flow had been subjected to a K of 3.85×10^{-6} and K was decreasing. After retransition to a low accelerated turbulent boundary layer had begun λ_{z2}^+ was very large even though K was of the order of 10^{-6} . It does not appear that λ_{z2}^+

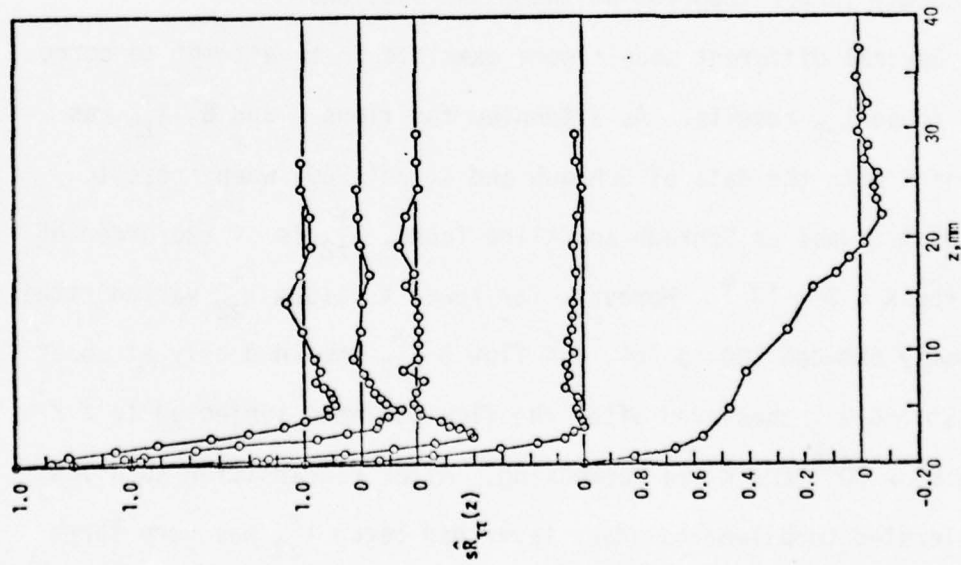


Figure 34. Normalized long time-averaged spanwise correlation $\hat{s}R_{tt}(z)$ results at the wall for flow D. Station locations from top to bottom: 126.3, 138.6, 156.3, 165.3, and 182.0 inches. Note displaced ordinate scales.

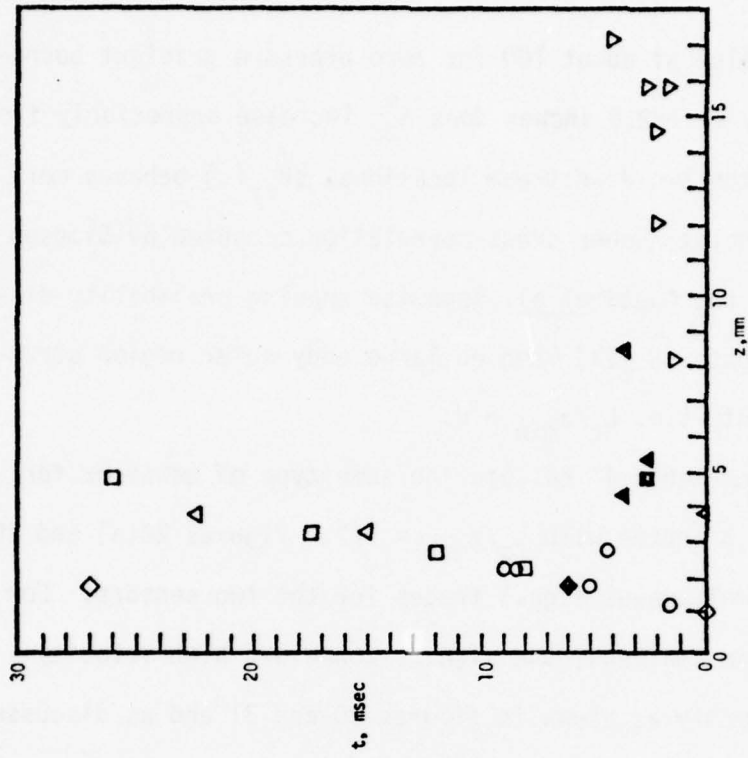


Figure 35. Observed minima and maxima for $\hat{s}R_{tt}(z, t)$. Maxima: \triangle 126.3, \square 138.6, \diamond 156.3, \circ 165.3, ∇ 182.0; Minima: \blacktriangle 126.3, \blacksquare 138.6, \blacklozenge 156.3

is solely a function of K . After retransition began, the flow character with high velocity pulses is entirely different than that found upstream.

Simpson et al. (1974) found that for adverse pressure gradient turbulent boundary layers, the maximum turbulent shearing stress should be used in the velocity scale in order to produce $(-\overline{uv}_{\max})^{1/2} z_{\max}/\nu$ values of about 100. This model was not successful for flows A and B (Simpson and Wallace). Unfortunately the split-film results for $-\overline{uv}$ presented in section 3.4 are not reliable in the wall region where it is a maximum. Since $-\overline{uv}/U_{\infty}^2$ decreases along a strongly accelerated flow, $(-\overline{uv}_{\max})^{1/2} z_{\max}/\nu$ would also decrease. This parameter would fall well below 100 since $(-\overline{uv}_{\max})/\tau_w$ would be below 1/4 at say, 156.3 inches. Another correlation parameter, $(KU_{\infty}^2/\nu n_b)(C_f/2)^{-1/2}$, used by Simpson et al. was also not successful in correlating these data.

It appears that the λ_z^+ spacing lags behind local conditions. In other words, the spatial parameters z_{\max} and z_{\min} remain large due to upstream conditions in these non-equilibrium flows. For example, at 182.0 inches in flow C, U_{τ}/ν is more than twice that at 165.3 inches but z_{\min} and z_{\max} are only slightly different. In retrospect, there is no reason to expect flows C and D to possess equilibrium characteristics.

Figures 33 and 35 show the local maxima and minima from the time-delayed cross-correlations for a given z spacing which were clearly distinguishable from noise. The wavelike nature of the

viscous sublayer behavior is illustrated by the fact that the maximum correlation at a given z spacing is time-delayed. The bursting frequency results given in table 3 above are somewhat crudely supported by the frequency corresponding to twice the time delay between the first minima and the first maxima, as given in table 4. In other words, if there is a repetitive wave-like nature of the sublayer flow in both z and t , the time-averaged characteristic bursting frequency should be approximately the same at all z sensor spacings.

For flow D figures 29(b) and 30(a) show that for the z spacings of sensors at which the spanwise cross-correlations were a minimum, the two signals were strongly out of phase. At time A in the latter oscilloscope photograph a short period of high velocity fluid passed over the moveable sensor. At the same time lower velocity fluid passed over the fixed sensor. A short time later, of the order of 3 msec, high velocity fluid passed over the fixed sensor while low velocity fluid passed over the moveable sensor. About 15 msec later the two traces again appear to be strongly out of phase. These data are consistent with the observations of Simpson (1976) regarding fingers of high velocity fluid as mentioned above.

3.7 Intermittency measurements

The intermittency factor γ , or the fraction of time that the flow is turbulent at a given spatial location, was determined for flow C using smoke in the boundary layer as the marker of turbulent fluid and scattered light from this smoke at a given location as the detected signal, using the optical apparatus described in section 2

above. Due to the large-scale mixing in the turbulent region the smoke is rapidly diffused while smoke is carried across the turbulent/non-turbulent interface by the much slower process of molecular diffusion. Thus, the smoke was assumed to be effectively confined to the turbulent regions of the flow. Fiedler and Head (1966) verified that values obtained by this method agree with those obtained by analysis of hot-wire signals.

The signal passed from the photomultiplier tube through a trigger circuit which produced positive rectangular pulses when the input was above a preset discrimination level. The discrimination level was set at approximately 10% of the peak PM tube sign amplitude. The counter-timer determined the fraction of time the positive pulses were present, which is the intermittency. Due to the steep slope of the PM output pulses, γ was not very sensitive to slightly different discriminator levels. Preliminary data taken in a zero pressure gradient flow were found to be in close agreement with the data of Klebanoff (1954).

The intermittency factor γ of this turbulent/non-turbulent interface has been previously found to be well represented by the integral of the normal distribution curve

$$\gamma = \frac{1}{\sqrt{2\pi} \sigma} \int_{\xi}^{\infty} \exp \left[-\frac{1\xi^2}{2\sigma^2} \right] d\xi \quad (16)$$

where $\xi = y - \bar{Y}$, \bar{Y} is the mean distance from the wall to the interface where $\gamma = 0.5$, and σ is the deviation from the mean. If this interface is viewed as a wavy pattern moving approximately at the

free-stream velocity, then σ characterizes the amplitude of this pattern. γ was in good agreement with equation (16) for flow C. Table 5 presents the characterizing parameters which describe these intermittency distributions.

The results of Fiedler and Head (1966) showed that the parameters \bar{Y}/δ^* and σ/δ^* are strongly dependent on the shape factor H for values of H less than about 2. This dependence is quite strong as the lower limiting value of H is approached. The minimum H found for flow C was about 1.26 at about 165 inches. Upstream of the minimum in H for flow C, at 130.6 and 149.3 inches, values of these parameters were well within the scatter of the Fiedler and Head results for their "normally developing" boundary layers. As pointed out in section 3.2 above, no entrainment of non-turbulent fluid takes place after the minimum H value occurs so it is not unexpected that \bar{Y}/δ^* and σ/δ^* downstream do not follow the results of Fiedler and Head.

The celerity and mean velocity profile measurements for flows A and B reveal that when there is no entrainment, the entire intermittent region is moving with the free-stream velocity. This means that there cannot be any relative streamwise motion of the intermittent region nor any engulfment of non-turbulent fluid by turbulent bulges. $U_\infty(\bar{Y} - \delta^*)$ and $U_\infty\sigma$ remain approximately constant downstream. As for flows A and B, the intermittent region plays no role in the momentum transport after entrainment.

Measurements of the frequency with which turbulent bulges pass a fixed point were made by counting the number of pulses per unit

Station (inches)	$\bar{\gamma}$, inches	σ , inches	$\eta_{\gamma} \times 10^{-4}$	$\frac{\sigma U_{\infty}}{\nu} \times 10^{-3}$	$n_{i\gamma}$, Hz
130.6	3.00	0.491	1.506	2.465	47.7
149.3	2.55	0.417	1.540	2.518	45.4
164.2	1.93	0.440	1.605	3.660	50.2
170.8	1.59	0.437	1.620	4.453	53.0
178.3	1.19	0.306	1.759	4.523	54.8
185.8	0.704	0.193	1.562	4.281	58.7

Table 5. Intermittency parameters for flow C.

Station, inches	γ
165.3	0.02
171.8	0.15
175.2	0.55
177.4	0.78
182.0	0.96
184.2	1.0
186.2	1.0

Table 6. Surface intermittency parameters for flow D.

time from the schmitt trigger output. A serious problem with this method arises due to the fact that several short duration pulses may occur as the probe volume enters and leaves the turbulent bulge thus giving rise to frequencies which are perhaps an order of magnitude higher than the actual.

In order to reduce the effects of this problem, the signal from the schmitt trigger was processed through a low pass filter which attenuated the short duration pulses responsible for the higher frequency. It was found that the resulting frequency obtained was quite dependent on the filter setting, so the filter setting was obtained by visual comparison of the unfiltered PM tube signal with the filtered schmitt trigger signal on a dual trace storage oscilloscope. Typical signal and oscilloscope traces from this method are given by Strickland and Simpson (1973). The filter was set such that there was a single zero crossing from negative to positive for each "significant" peak on the unfiltered PM tube signal. The filter setting chosen for all the results here was 300 Hz.

Figure 33 of Simpson and Wallace (1975) shows a typical bell-shaped frequency distribution such as obtained for flow C. The frequency distributions across the intermittent region for flow C are rather similar when the frequency is normalized on the frequency at \bar{Y}, n_{iY} . As for flows A and B, the peak frequency for each profile occurred at about the location where $\gamma = 0.6$. The n_{iY} for flow C was about twice the bursting frequency n_b when tables 3 and 5 are compared. Since the technique used to obtain the intermittency

frequency requires a certain amount of arbitrary judgment, as do techniques using hot-wires, it cannot be determined if the absolute values of these measurements are accurate. However, since for each flow n_b was proportional to $n_{i\gamma}$, it appears that the large motion influencing the intermittency also influences the wall bursting frequency even downstream of the cessation of entrainment. Strickland and Simpson (1973) also found n_b to be proportional to $n_{i\gamma}$ for an adverse pressure gradient turbulent boundary layer. Thus, apparently this proportionality is present in turbulent boundary layers over a wide range of pressure gradient conditions.

For flow D the intermittency at the surface was determined for the retransition region downstream from the flush-surface hot-film signals. The taped signals were examined for high frequency content since considerable mixing and high frequency oscillations are associated with turbulent fluid. These signals were passed through the model 330B filter with a 200 Hz-2KHz bandpass and then through the multiplier used as a squarer in order to rectify the negative portions. This signal was low-pass filtered at 300 Hz using the model 3202 filter and passed through a schmitt trigger. The resultant pulses were visually compared with the original signals on a storage oscilloscope for validity as regions of high frequency content. These pulse periods were accumulatively counted for 50 sec. by the digital timer-counter. The fraction of time pulses were present was the intermittency γ . These results are presented in table 6. These same signals were processed by using the schmitt trigger on the

output signal of the model 330B filter. The resulting fraction of time positive pulses were present was doubled to get the intermittency since contributions from negative pulses had not been rectified. These latter results were within 5% of the results of table 6.

The results in table 6 follow a curve of the form of the integral of the normal distribution curve. γ increases slowly from about 165.3 inches to 171.8 inches, increases more rapidly up to 177.4 inches, and thereafter increases slowly to unity at about 184.2 inches. Upstream of 165.3 inches the flow had low frequency oscillations as shown in figures 28(a) and 29. It is clear in figures 30 that higher amplitude pulses were occasionally present at 165.3 inches. Figures 28(b) and (c) show the relatively high frequency oscillations in the high velocity pulses at 171.5 and 175.0 inches. The clearest oscilloscope traces are shown in figures 31 for 182.0 inches. The higher velocity regions contain high frequency oscillations. Regions of laminar-like flow follow each high velocity pulse. These velocity signals slowly decay, not because of limited sensor response but because of temporarily high velocity laminar flow that follows the turbulent pulses.

It is clear that in the low velocity wall regions downstream of the cessation of entrainment in flow D, the flow became progressively more laminar-like. The magnitude of the oscillations in these regions progressively decreased. However, beginning at 165.3 inches, high velocity fluid moved in toward the wall. The average frequency of occurrence of high velocity pulses in this downstream region was

about 25 Hz, as determined by counting these pulses. Further analysis of these data is planned.

4. DISCUSSION

Many aspects of flows C and D are similar to previous results reported by other investigators and by Simpson and Wallace (1975). In flow D and in the flow of Blackwelder and Kovaszny (1972), K increased to a value which exceeded 3.8×10^{-6} and decreased downstream to zero. In both flows, a local maximum in $C_f/2$ occurred at the same streamwise position as the K maximum; the minimum in $C_f/2$ occurred downstream of the minimum of the intermittency at the wall; the maximum H occurred upstream of the $C_f/2$ minimum and approximately at the minimum intermittency at the wall.

In all four flows measured in this research program, the behavior of the turbulent boundary layer after the beginning of strong acceleration was very similar. An initially normal low-pressure-gradient boundary layer first became distorted. The wake-like tail of the mean velocity profile became progressively weaker until at the cessation of entrainment none remained. It appears that the shape factor H is about a minimum at this location. The bursting frequency and intermittent bulge passage frequency downstream either increased or remained about constant along this length. The surface spanwise structure was not appreciably different from a low Reynolds number low-pressure-gradient boundary layer. Downstream the entire intermittent turbulent/non-turbulent interface was outside the

boundary layer thickness δ and the celerity of this region was the free-stream velocity.

Simpson and Wallace (1975) showed that normal stresses production was important in the mean turbulence kinetic energy balance

$$\frac{1}{2} \left\{ U \frac{\partial \overline{q^2}}{\partial x} + v \frac{\partial \overline{q^2}}{\partial y} \right\} + \frac{\partial}{\partial y} \left[\frac{\overline{pv}}{\rho} + \frac{1}{2} \overline{q^2} v \right] + \epsilon = -\overline{uv} \frac{\partial U}{\partial y} - (\overline{u^2} - \overline{v^2}) \frac{\partial U}{\partial x} \quad (17)$$

Here the terms are from left to right: advection, turbulent diffusion, dissipation, shear production, and normal stresses production. This last term is of opposite sign to the shear production term in strongly accelerated flows. The net turbulence energy production is less than the shear production by the factor

$$F = 1 - \frac{(\overline{u^2} - \overline{v^2}) \partial U / \partial x}{(-\overline{uv}) \partial U / \partial y} \quad (18)$$

which represents total production to shear production.

They also found that the normal stresses term reduces the diffusion of turbulence kinetic energy into the freestream, or the entrainment of non-turbulent fluid into the boundary layer. The velocity difference between turbulent fluid in the intermittent region and the irrotational freestream fluid approaches zero with strong acceleration. Thus, velocity profile instabilities which produce the eruption and eventual engulfment of free-stream fluid are eliminated. There could be no creation or merging of adjacent large eddies that accompanies the entrainment process. This also explains why the intermittency and bursting frequencies for all four flows remained about constant after cessation of entrainment.

Simpson and Wallace found that

$$V_E = 10F_\delta (-\overline{uv})_{\max} / U_\infty \quad (19)$$

described the entrainment velocity upstream of cessation for flows A and B. This scale characterizes the large eddy structure that is not only largely responsible for the various turbulence intensity levels in the turbulent fluid, but is directly responsible for the entrainment. When the negative normal stresses turbulence energy production term arises under strong acceleration, the available turbulence kinetic energy in the outer region is reduced so less large eddy energy is available for entrainment. This equation reduces to Bradshaw's relation for low acceleration boundary layers when $F_\delta = 1$. F_δ is given by equation (18) with all quantities evaluated at the boundary layer thickness δ . Using the relations $-\overline{uv} \approx 0.15 \overline{q^2}$, $\overline{u^2} \approx \frac{1}{2} \overline{q^2}$, and $\overline{v^2} \approx 0.2 \overline{q^2}$, which apply to entraining flows, they obtained

$$F_\delta = 1 - \frac{2K}{(\partial f / \partial \eta)_\delta} \quad (20)$$

Figure 36 shows this quantity along flows C and D. Note that negative values of F_δ occur after engulfment of non-turbulent fluid ceases. This does not mean that turbulent fluid is instantaneously reverting to a laminar state, but simply that progressively more turbulent fluid lies outside the δ location.

Figures 7 and 8 show the results obtained by integrating equation (19)

$$U_\infty (\delta - \delta^*) \Big]_{x_0}^x = \int_{x_0}^x V_E dx \quad (21)$$

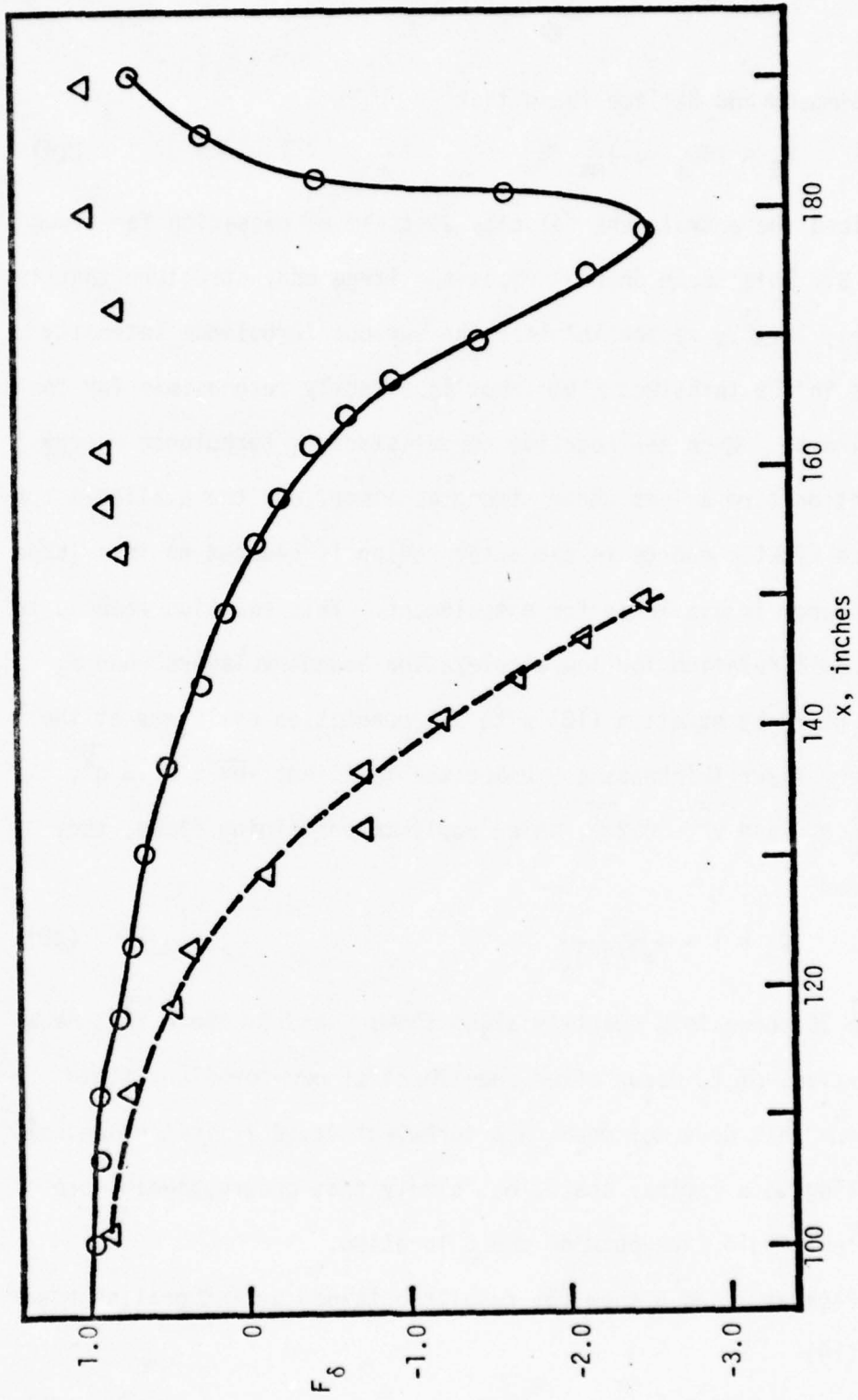


Figure 36. F_δ vs. x . Experimental values in eqn. (20): \circ , flow C; Δ , flow D. Lines for visual aid only.

For these computations the relation $(-\overline{uv})_{\max} \approx 0.3(\overline{u^2})_{\max}$ was used with experimental $(\overline{u^2})_{\max}$ values. The results are in good agreement with values determined directly from the mean velocity profiles, especially for flow C. Thus the growth and decline of the mean flow boundary layer is fairly well predicted by this model, at least to just downstream of the cessation of entrainment.

The observed flat $nF(n)$ region for $\overline{u^2}$ spectra emerges after some length of acceleration. The streamwise location where this behavior is first noticed does not seem to be directly related to the location where entrainment ceases. For flow A with $K = 2.17 \times 10^{-6}$, the $nF(n)$ spectra examined by Simpson and Wallace had no flat region, even downstream of the cessation of entrainment. For flow B with $K = 3.19 \times 10^{-6}$, no flat region was present in the spectra obtained upstream of the minimum H, while such a region was observed for spectra downstream. In flow C presented here, the flat region in some spectra began at about 137 inches while the cessation of entrainment did not occur until about 165 inches. Similarly for flow D entrainment ceased at about 132 inches while the flat $nF(n)$ region began at about 123 inches. A preliminary exploration of this behavior is that with strong acceleration, progressively weaker new low frequency oscillations are produced by the large-scaled motion while the higher frequency oscillations are produced by the breakdown of the more intense upstream large-scaled motions. Further analysis of these data is needed.

In flows A and B, asymptotic similarity flows were approached near the downstream end of the test section. This means that $\sqrt{u^2}/U_\infty$ vs. η similarity was present for $K < 3.19 \times 10^{-6}$. For flow C when $K > 3.6 \times 10^{-6}$, $\sqrt{u^2}/U_\infty$ profiles decayed. This means that had this K level been maintained downstream, true relaminarization would have eventually resulted, as suggested by Kline et al. (1967). Since there is a much shorter distance from the beginning of acceleration to the maximum K in flow D, the intensity $\sqrt{u^2}/U_\infty$ did not begin to decay near the wall until about 157 inches. At 161.6 inches, as shown in figure 20, a considerable amount of the intensity was due to unsteadiness rather than turbulence. Since K decreased downstream of 144 inches, retransition to a low acceleration turbulent boundary layer began at about 165 inches. In this region the flow possessed a highly laminar-like behavior, so $-\overline{uv}$ was extremely small. Evidently $\sqrt{v^2}$ decays considerably. As mentioned above, the surface spanwise structure upstream of the onset of decay of $\sqrt{u^2}/U_\infty$ was not appreciably different from that of a low Reynolds number low pressure gradient boundary layer. After the onset of decay of $\sqrt{u^2}/U_\infty$, λ_z^+ increased. Evidently the upstream λ_z values in these non-equilibrium flows persist downstream, so when normalized with a higher U_τ/ν , λ_z^+ is higher.

In the relaminarizing nozzle-type flow of Schraub and Kline (Kline et al. 1967), λ_z^+ was reported for the region of maximum K to be of the order of 200 for $K = 2.75 \times 10^{-6}$ and of the order of 300 for $K = 3.25 \times 10^{-6}$. On the surface, it would appear that they found

λ_z^+ to vary directly with K . However, their estimates of $C_f/2$ for these two streamwise locations seem high by about a factor of two when compared to the $C_f/2$ behavior in flow D and in the Blackwelder and Kovasznay (1972) nozzle flow. In that case, values of about 150 and 220 for λ_z^+ would result, respectively, and would agree reasonably well with the flow D results in the vicinity of the maximum K .

Schraub and Kline did not present λ_z results downstream of the K maximum, so the data from flow D are the only available on this downstream structure. λ_z^+ is still of the order of 300 while K decreases below 2×10^{-6} . After retransition to a low-accelerated low-pressure-gradient turbulent boundary layer begins, λ_z^+ is an order of magnitude greater. This behavior is as yet incompletely explained, so further analysis of these data is needed.

5. CONCLUSIONS AND RECOMMENDATIONS

The following conclusions can be made about turbulent boundary layers subjected to strong acceleration.

- a. The parameter K must be greater than about 3.6×10^{-6} for the decay of the upstream generated turbulence.
- b. For practical use in a nozzle only one short region downstream of the maximum K will possess a laminar-like behavior with significantly lower $C_f/2$ and heat transfer coefficients.
- c. The large eddy structure of the outer region governs the bursting frequency, the intermittent bulge passage frequency, and influences the wall flow behavior downstream. These frequencies

seem to approach constant values after the cessation of entrainment of non-turbulent fluid.

d. The wall spanwise structure appears to lag behind local conditions and to reflect upstream flow behavior. λ_z^+ seems to steadily increase to about 300 even after K has dropped below its maximum value in a nozzle flow. After retransition to a low accelerated turbulent boundary layer, a large λ_z^+ of the order of 3000 is observed.

e. The proposed modified entrainment model accounts for the reduction of available turbulence kinetic energy by the negative normal stresses production term of the turbulence kinetic energy equation.

f. A $nF(n)$ spectral distribution of $\overline{u^2}$ for $\eta > 1000$ appears to possess a flat region for laminar like boundary layers at large K values.

As a result of the large quantity of experimental data provided by the research program, the following recommendations for future work are suggested.

a. Further analysis of these data, some of which was not presented in this report because of the lack of time. Afterwards a manuscript should be submitted for journal publication. At that time a more intelligent assessment for future work can be made.

b. A generalized computational effort incorporating flow models reflected by all available data should be undertaken. Communication between the senior author and predictors has begun, but no results are yet available.

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APPENDIX A - Mean velocity and streamwise fluctuation intensity $(\bar{u}^2)^{1/2}/U_\infty$ profile data, flow C,
linearly increasing K

K = 101.2			K = 112.2			K = 118.8			K = 123.1		
N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY
27.	.1227	0.0339	36.	.1152	0.0337	22.	.1172	0.0258	56.	.1604	0.0464
32.	.1382	0.0381	43.	.1245	0.0384	28.	.1288	0.0288	61.	.1693	0.0525
39.	.1493	0.0392	48.	.1351	0.0436	34.	.1292	0.0327	67.	.1863	0.0570
45.	.1608	0.0464	52.	.1445	0.0478	43.	.1439	0.0409	81.	.2282	0.0648
57.	.2039	0.0549	62.	.1644	0.0549	56.	.1599	0.0457	95.	.2674	0.0752
65.	.2412	0.0651	71.	.1864	0.0614	70.	.1874	0.0538	109.	.3204	0.0811
91.	.3136	0.0776	83.	.2157	0.0692	84.	.2174	0.0620	123.	.3431	0.0867
114.	.3717	0.0883	95.	.2482	0.0778	112.	.2457	0.0802	151.	.4091	0.0954
136.	.4112	0.0922	119.	.3014	0.0902	140.	.3032	0.0898	179.	.4773	0.0997
182.	.4979	0.0947	143.	.3561	0.0951	168.	.4136	0.0950	207.	.5178	0.0999
227.	.5329	0.0959	167.	.4241	0.0996	224.	.4840	0.1021	235.	.5588	0.1024
273.	.5636	0.0940	194.	.4335	0.1035	281.	.5453	0.1020	291.	.6094	0.1007
344.	.6053	0.0950	239.	.4901	0.1035	337.	.5688	0.1011	347.	.6504	0.0952
454.	.6223	0.0904	254.	.5313	0.1035	412.	.6443	0.0949	454.	.6872	0.0875
545.	.6535	0.0784	381.	.5827	0.1004	561.	.6621	0.0868	570.	.7226	0.0813
627.	.6721	0.0736	476.	.6354	0.0897	701.	.7114	0.0795	710.	.7467	0.0859
909.	.6875	0.0708	575.	.6670	0.0891	842.	.7291	0.0726	850.	.7602	0.0661
1134.	.7077	0.0669	714.	.6869	0.0853	1122.	.7549	0.0646	1129.	.7825	0.0598
1362.	.7171	0.0657	982.	.7194	0.0752	1467.	.7735	0.0576	1497.	.7768	0.0551
1580.	.7215	0.0661	1190.	.7814	0.0696	1693.	.7842	0.0549	1688.	.8102	0.0524
1818.	.7257	0.0667	1428.	.7860	0.0653	2244.	.8078	0.0519	1964.	.8197	0.0516
2272.	.7372	0.0667	1665.	.7717	0.0637	2805.	.8162	0.0506	2247.	.8314	0.0498
2726.	.7443	0.0673	1903.	.7842	0.0626	4488.	.8579	0.0502	2896.	.8396	0.0497
3435.	.7471	0.0658	2379.	.7989	.0597	5610.	.8619	0.0523	3365.	.8425	0.0468
4444.	.8072	0.0599	2895.	.8136	0.0583	6732.	.8619	0.0515	4484.	.8708	0.0460
5453.	.8429	0.0510	3897.	.8408	0.0576	7859.	.9236	0.0494	5602.	.8948	0.0467
6362.	.8404	0.0511	4758.	.8649	0.0548	8977.	.9432	0.0462	6720.	.9166	0.0448
7271.	.9178	0.0525	5710.	.8889	0.0519	10899.	.9615	0.0408	7878.	.9365	0.0416
8179.	.9408	0.0474	6662.	.9110	0.0516	12821.	.9767	0.0340	8956.	.9572	0.0372
9298.	.9627	0.0421	7612.	.9330	0.0494	14826.	.9947	0.0264	10074.	.9742	0.0306
10274.	.9828	0.0333	8565.	.9518	0.0467				11192.	.9875	0.0233
11348.	.9934	0.0289	9517.	.9717	0.0444				12590.	.9973	0.0157
12496.	.9999	0.0204	10766.	.9937	0.0379				13987.	1.0000	0.0103
13632.	1.0000	0.0203	11896.	1.0000	0.0275						

Y shift = 0.002

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X = 128.4			X = 132.2			X = 136.7			X = 140.7		
Z	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY
27.	-1.109	0.0198	42.	-1.982	0.0551	33.	-1.217	0.0265	115.	-2.952	0.0731
36.	-1.168	0.0246	46.	-2.156	0.0618	42.	-1.413	0.0304	124.	-3.132	0.0788
40.	-1.271	0.0311	75.	-2.259	0.0523	50.	-1.508	0.0343	133.	-3.306	0.0754
54.	-1.523	0.0400	82.	-2.456	0.0559	67.	-1.607	0.0415	138.	-3.701	0.0787
67.	-1.626	0.0481	92.	-2.618	0.0727	82.	-2.116	0.0514	168.	-4.112	0.0818
81.	-2.086	0.0554	109.	-3.302	0.0609	108.	-2.470	0.0584	186.	-4.402	0.0869
94.	-2.449	0.0645	126.	-3.724	0.0671	117.	-2.696	0.0657	203.	-4.794	0.0932
108.	-2.712	0.0705	144.	-4.174	0.0919	133.	-3.293	0.0705	224.	-5.149	0.0910
121.	-3.045	0.0764	178.	-4.680	0.0963	136.	-3.698	0.0763	248.	-5.532	0.0923
135.	-3.333	0.0801	212.	-5.129	0.0994	167.	-4.059	0.0797	292.	-6.149	0.0928
152.	-3.822	0.0950	246.	-6.137	0.0998	187.	-4.516	0.0839	336.	-6.718	0.0928
165.	-3.976	0.0998	280.	-6.931	0.0946	208.	-4.957	0.0873	360.	-7.138	0.0915
232.	-4.955	0.092	348.	-7.114	0.0998	250.	-5.577	0.0941	449.	-7.714	0.0824
317.	-6.169	0.1009	411.	-7.622	0.0921	281.	-6.134	0.0947	531.	-8.133	0.0745
404.	-6.649	0.0990	554.	-7.915	0.0919	333.	-6.678	0.0949	734.	-8.652	0.0604
531.	-7.102	0.0905	648.	-8.171	0.0741	410.	-7.499	0.0918	911.	-9.045	0.0613
674.	-7.675	0.0817	867.	-8.618	0.0656	509.	-7.708	0.0870	1132.	-9.625	0.0561
842.	-8.073	0.0730	1032.	-8.657	0.0600	668.	-8.223	0.0813	1353.	-9.777	0.0490
1011.	-8.404	0.0674	1374.	-8.695	0.0508	833.	-8.510	0.0699	1755.	-9.524	0.0360
1345.	-8.703	0.0573	1716.	-8.612	0.0457	1041.	-8.888	0.0606	2208.	-9.414	0.0280
1695.	-8.655	0.0506	2058.	-8.885	0.0405	1248.	-8.833	0.0408	2685.	-9.524	0.0244
2022.	-8.664	0.0470	2399.	-8.956	0.0373	1685.	-8.943	0.0407	3122.	-9.577	0.0251
2357.	-8.662	0.0445	2741.	-8.952	0.0373	2081.	-8.937	0.0360	3504.	-9.611	0.0248
2697.	-8.944	0.0432	3425.	-9.155	0.0354	2498.	-9.182	0.0335	4449.	-9.796	0.0232
3371.	-8.625	0.0408	4108.	-9.229	0.0343	2914.	-9.144	0.0316	5333.	-9.713	0.0228
4044.	-8.905	0.0382	4792.	-9.308	0.0378	3316.	-9.184	0.0300	7102.	-9.775	0.0222
5303.	-9.267	0.0357	5476.	-9.375	0.0318	4153.	-9.276	0.0280	8871.	-9.685	0.0167
6741.	-9.577	0.0344	6643.	-9.426	0.0293	4996.	-9.378	0.0267	10839.	-9.621	0.0154
8499.	-9.798	0.0317	8210.	-9.657	0.0257	6661.	-9.519	0.0249	12428.	-9.677	0.0090
9696.	-9.626	0.0288	9577.	-9.627	0.0226	8326.	-9.559	0.0216	14177.	-1.4668	0.0065
16786.	-9.791	0.0250	10945.	-9.654	0.0170	9901.	-9.755	0.0196			
12135.	-9.807	0.0132	12312.	-9.913	0.0129	11656.	-9.874	0.0159			
13463.	-9.998	0.0132	13819.	-9.956	0.0093	13321.	-9.970	0.0122			
15148.	-1.4668	0.0100	15388.	-1.4660	0.0071	14987.	-9.962	0.0090			
						16652.	-1.4660	0.0072			

Y WHITE = 0.003

Y WHITE = 0.001

BEST AVAILABLE COPY

λ = 143.8				λ = 146.7				λ = 152.6			
H	F	INTENSITY	H	F	INTENSITY	H	F	INTENSITY	H	F	INTENSITY
18.	.1195	0.0134	74.	.2916	0.0467	153.	.3481	0.0452	202.	.9725	0.0170
21.	.1222	0.0170	76.	.2954	0.0490	42.	.2213	0.0513	166.	.3677	0.0468
24.	.1268	0.0232	182.	.2792	0.0523	185.	.2449	0.0553	183.	.3794	0.0497
42.	.1418	0.0391	113.	.2722	0.0551	137.	.2924	0.0628	199.	.4221	0.0725
52.	.1591	0.0346	124.	.2668	0.0646	156.	.3391	0.0694	214.	.4449	0.0732
73.	.1759	0.0448	136.	.2336	0.0518	184.	.3876	0.0743	249.	.4723	0.0742
94.	.2079	0.0528	152.	.3159	0.0657	218.	.4410	0.0802	282.	.5212	0.0744
115.	.2576	0.0593	181.	.4217	0.0726	237.	.4839	0.0832	290.	.5327	0.0812
136.	.2894	0.0657	209.	.4786	0.0742	243.	.5218	0.0874	309.	.5177	0.0812
157.	.3496	0.0717	237.	.5404	0.0805	246.	.5458	0.0883	327.	.4446	0.0796
182.	.3929	0.0727	265.	.5823	0.0845	328.	.6489	0.0899	405.	.4974	0.0790
204.	.4377	0.0730	294.	.6217	0.0864	394.	.6826	0.0889	453.	.7194	0.0795
242.	.5353	0.0718	322.	.6648	0.0874	482.	.7353	0.0857	482.	.7424	0.0785
314.	.6624	0.0783	358.	.6716	0.0846	526.	.7884	0.0813	520.	.7424	0.0785
367.	.6876	0.0791	487.	.7472	0.0843	657.	.8517	0.0788	520.	.7424	0.0785
471.	.7558	0.0746	451.	.7499	0.0784	766.	.8921	0.0676	596.	.8384	0.0758
576.	.8173	0.0812	920.	.8356	0.0720	1891.	.9328	0.0443	872.	.8785	0.0770
786.	.8792	0.0882	576.	.8516	0.0745	1319.	.9176	0.0378	749.	.8948	0.0690
995.	.9177	0.0945	489.	.8827	0.0657	1977.	.9432	0.0261	829.	.9175	0.0619
1204.	.9482	0.0532	482.	.9487	0.0558	1894.	.9089	0.0270	918.	.9449	0.0528
1414.	.9334	0.0331	915.	.9422	0.0500	2187.	.9725	0.0243	1131.	.9615	0.0446
1622.	.9424	0.0353	1141.	.9376	0.0434	2395.	.9766	0.0222	1286.	.9716	0.0414
1831.	.9477	0.0349	1387.	.9493	0.0352	2628.	.9766	0.0202	1500.	.9853	0.0307
2042.	.9419	0.0317	1593.	.9534	0.0305	2956.	.9888	0.0164	1896.	.9922	0.0253
2264.	.9453	0.0201	1819.	.9594	0.0280	3285.	.9810	0.0172	2261.	.9918	0.0214
2496.	.9486	0.0276	2044.	.9634	0.0251	3462.	.9823	0.0155	2567.	.9927	0.0194
2694.	.9493	0.0287	2276.	.9654	0.0230	3756.	.9871	0.0132	2872.	.9880	0.0171
4137.	.9789	0.0222	2557.	.9678	0.0214	4576.	.9976	0.0128			
5180.	.9718	0.0197	2815.	.9676	0.0200	7893.	.9917	0.0119			
6232.	.9764	0.0175	3466.	.9746	0.0194	18511.	.9982	0.0099			
8324.	.9842	0.0150	4527.	.9788	0.0180	13139.	.9989	0.0080			
10421.	.9924	0.0132	5637.	.9819	0.0152	15187.	1.0000	0.0064			
12516.	.9971	0.0102	6787.	.9859	0.0140						
14610.	1.0000	0.0077	7918.	.9889	0.0124						
			8648.	.9912	0.0125						
			11287.	.9956	0.0100						
			13584.	.9987	0.0076						
			15825.	1.0000	0.0060						

γ shift = 0.006

γ shift = 0.001

BEST AVAILABLE COPY

X = 157.5			X = 161.6			X = 172.6			X = 179.7		
N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY
100.	.2346	0.0660	135.	.3216	0.0769	291.	.3290	0.0924	283.	.4745	0.0665
119.	.2677	0.0719	159.	.3513	0.0806	333.	.3512	0.0944	331.	.4903	0.0832
138.	.3145	0.0768	183.	.3868	0.0789	375.	.3852	0.0959	378.	.5119	0.0899
156.	.3523	0.0775	207.	.3775	0.0811	416.	.4200	0.0954	425.	.5133	0.0895
175.	.3912	0.0779	231.	.3947	0.0789	458.	.4622	0.0938	472.	.5333	0.0895
213.	.4650	0.0780	256.	.4212	0.0788	500.	.5034	0.0911	567.	.5766	0.0867
251.	.5242	0.0753	280.	.4528	0.0784	541.	.5356	0.0899	601.	.6095	0.0849
289.	.5759	0.0753	328.	.5232	0.0775	624.	.5972	0.0816	756.	.6376	0.0838
326.	.6266	0.0756	376.	.5844	0.0773	708.	.6451	0.0749	850.	.6649	0.0825
364.	.6762	0.0764	424.	.6212	0.0762	791.	.6865	0.0712	945.	.7026	0.0834
401.	.7054	0.0761	473.	.6565	0.0760	874.	.7229	0.0693	1065.	.7262	0.0813
448.	.7464	0.0754	532.	.7146	0.0731	957.	.7566	0.0691	1181.	.7451	0.0797
495.	.7844	0.0733	593.	.7495	0.0714	1042.	.7957	0.0682	1417.	.7727	0.0768
532.	.8321	0.0658	714.	.8105	0.0708	1164.	.8221	0.0684	1654.	.7943	0.0746
684.	.8789	0.0606	834.	.8543	0.0668	1374.	.8727	0.0558	1850.	.8152	0.0723
778.	.9053	0.0566	955.	.8981	0.0614	1582.	.9099	0.0620	2362.	.8547	0.0687
966.	.9492	0.0460	1196.	.9415	0.0504	1790.	.9263	0.0589	2835.	.8849	0.0659
1155.	.9838	0.0384	1437.	.9626	0.0426	2204.	.9516	0.0497	3307.	.9121	0.0624
1512.	.9462	0.0282	1919.	.9872	0.0259	2623.	.9679	0.0414	3780.	.9360	0.0573
1908.	.9944	0.0217	2401.	.9944	0.0187	3038.	.9776	0.0347	4724.	.9412	0.0492
2245.	.9979	0.0177	2884.	.9965	0.0145	3455.	.9828	0.0278	5669.	.9677	0.0403
2682.	.9922	0.0153	3366.	.9986	0.0116	3872.	.9883	0.0219	6614.	.9871	0.0307
3039.	1.0000	0.0137	3848.	1.0000	0.0102	4288.	.9917	0.0179	7559.	.9991	0.0155
						5120.	.9969	0.0122	8504.	1.0000	0.0104
						5953.	1.0000	0.0091			

y shift = -0.0004

y shift = 0.0013

y shift = 0.003

BEST AVAILABLE COPY

N	F	INTENSITY
305.	.4986	0.0836
356.	.5214	0.0818
407.	.5436	0.0816
458.	.5585	0.0812
509.	.5732	0.0809
610.	.6020	0.0811
712.	.6162	0.0798
814.	.6277	0.0789
916.	.6451	0.0783
1017.	.6560	0.0773
1144.	.6687	0.0767
1272.	.6782	0.0760
1399.	.6956	0.0753
1526.	.7065	0.0743
1780.	.7224	0.0727
2034.	.7362	0.0710
2543.	.7596	0.0684
3052.	.7809	0.0661
3560.	.7999	0.0640
4069.	.8127	0.0620
4578.	.8351	0.0594
5086.	.8472	0.0576
6103.	.8759	0.0532
7121.	.8865	0.0501
8138.	.9105	0.0461
9155.	.9312	0.0423
10172.	.9537	0.0362
11444.	.9793	0.0283
12715.	.9904	0.0217
13987.	.9963	0.0152
15259.	1.0000	0.0112

APPENDIX B - Mean velocity and streamwise fluctuation intensity $(\bar{u}^2)^{1/2}/U$ profile data, flow D, nozzle flow

X = 88.0			X = 101.10			X = 106.90			X = 112.0		
N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY
65.	.1175	0.0190	64.	.1375	0.0288	43.	.1199	0.0170	66.	.1341	0.0263
67.	.1454	0.0320	65.	.1657	0.0388	64.	.1420	0.0284	68.	.1705	0.0398
69.	.1723	0.0407	127.	.2503	0.0648	66.	.1735	0.0408	132.	.2444	0.0635
134.	.2372	0.0623	170.	.3150	0.0802	129.	.2410	0.0618	176.	.3137	0.0790
178.	.2942	0.0789	212.	.3643	0.0897	171.	.3062	0.0810	219.	.3763	0.0909
223.	.3446	0.0863	276.	.4266	0.0926	214.	.3597	0.0892	285.	.4320	0.0939
290.	.4405	0.0897	340.	.4642	0.0947	279.	.4261	0.0928	351.	.4843	0.0948
357.	.4459	0.0885	425.	.5089	0.0941	343.	.4410	0.0945	439.	.5161	0.0899
446.	.4424	0.0896	531.	.4430	0.0874	429.	.5006	0.0926	549.	.4604	0.0862
558.	.5124	0.0834	637.	.5676	0.0834	536.	.5425	0.0889	658.	.5820	0.0820
649.	.5320	0.0821	849.	.5900	0.0792	643.	.5623	0.0833	878.	.6093	0.0745
892.	.5616	0.0766	1062.	.6099	0.0746	857.	.5972	0.0755	1097.	.6298	0.0709
1227.	.5980	0.0725	1274.	.6276	0.0710	1179.	.6310	0.0711	1317.	.6468	0.0668
1561.	.6198	0.0702	1698.	.6628	0.0700	1500.	.6496	0.0678	1756.	.6695	0.0633
2097.	.6467	0.0683	2123.	.6928	0.0656	1929.	.6740	0.0634	2145.	.6923	0.0614
2676.	.6791	0.0669	2760.	.7122	0.0637	2572.	.6997	0.0627	2853.	.7127	0.0608
3548.	.7194	0.0649	3397.	.7310	0.0629	3429.	.7322	0.0609	3512.	.7389	0.0590
4460.	.7580	0.0649	4246.	.7815	0.0623	4206.	.7625	0.0598	4390.	.7662	0.0608
5575.	.8011	0.0628	5308.	.8039	0.0594	5358.	.7951	0.0571	5447.	.8048	0.0585
6600.	.8469	0.0614	6369.	.8415	0.0588	6430.	.8300	0.0547	6585.	.8355	0.0579
7805.	.8893	0.0576	7431.	.8779	0.0558	7501.	.8673	0.0534	7682.	.8696	0.0574
8920.	.9275	0.0516	8492.	.9143	0.0531	8573.	.9034	0.0529	8779.	.9020	0.0551
10035.	.9588	0.0403	9554.	.9425	0.0438	9644.	.9336	0.0451	9877.	.9344	0.0495
11150.	.9834	0.0270	10615.	.9696	0.0346	10716.	.9639	0.0357	10974.	.9611	0.0397
12265.	.9969	0.0173	11677.	.9872	0.0227	11788.	.9814	0.0233	12072.	.9823	0.0264
13380.	.9997	0.0130	12738.	.9960	0.0159	12859.	.9942	0.0176	13149.	.9947	0.0201
14495.	1.0000	0.0111	13800.	1.0000	0.0138	13931.	.9988	0.0140	14267.	.9991	0.0141
			14851.	.9994	0.0114	15002.	1.0000	0.0107	15364.	1.0000	0.0117
			15923.	.9969	0.0107				16462.	.9991	0.0103

BEST AVAILABLE COPY

BEST AVAILABLE COPY

X = 137.20

N	F	INTENSITY
43.	.1788	0.0122
54.	.1297	0.0165
65.	.1446	0.0242
81.	.1705	0.0373
106.	.2132	0.0559
135.	.2623	0.0658
162.	.3142	0.0765
188.	.3531	0.0837
215.	.3939	0.0903
269.	.4541	0.1020
350.	.5236	0.1043
431.	.5737	0.1016
538.	.6237	0.0944
672.	.6817	0.0849
808.	.6877	0.0787
1077.	.7146	0.0680
1346.	.7368	0.0629
1615.	.7525	0.0606
2154.	.7720	0.0588
2692.	.7905	0.0565
3500.	.8100	0.0531
4267.	.8324	0.0526
5304.	.8545	0.0510
6730.	.8680	0.0491
8076.	.9110	0.0451
9422.	.9206	0.0425
10768.	.9510	0.0377
12115.	.9703	0.0399
13461.	.9852	0.0252
14807.	.9944	0.0177
16153.	.9981	0.0116
17499.	1.0000	0.0107
18645.	.9991	0.0097

X = 130.60

N	F	INTENSITY
50.	.2098	0.0138
66.	.1452	0.0251
75.	.1701	0.0348
100.	.2246	0.0541
125.	.2904	0.0706
151.	.3461	0.0786
201.	.4286	0.0887
251.	.4863	0.0918
326.	.5579	0.0872
401.	.6007	0.0837
502.	.6325	0.0794
627.	.6684	0.0714
753.	.6743	0.0691
1003.	.6962	0.0635
1505.	.7230	0.0561
2007.	.7469	0.0537
2614.	.7638	0.0555
3261.	.7777	0.0573
4014.	.7996	0.0592
5017.	.8235	0.0574
6272.	.8593	0.0561
7526.	.8891	0.0540
8781.	.9150	0.0489
10035.	.9408	0.0436
11289.	.9597	0.0366
12544.	.9776	0.0272
13798.	.9926	0.0194
15052.	.9975	0.0137
16307.	1.0000	0.0108
17310.	.9975	0.0096

X = 123.15

N	F	INTENSITY
48.	.1215	0.0172
73.	.1637	0.0359
97.	.2203	0.0531
121.	.2348	0.0567
145.	.2739	0.0664
194.	.3521	0.0813
242.	.4077	0.0885
315.	.4664	0.0946
389.	.5096	0.0933
445.	.5467	0.0906
606.	.5969	0.0835
727.	.6054	0.0746
949.	.6353	0.0685
1444.	.6703	0.0600
1939.	.6919	0.0560
2544.	.7136	0.0541
3150.	.7331	0.0560
3877.	.7547	0.0575
4846.	.7825	0.0589
6058.	.8196	0.0608
7269.	.8474	0.0579
8481.	.8814	0.0566
9693.	.9154	0.0501
10904.	.9452	0.0423
12116.	.9668	0.0345
13327.	.9843	0.0240
14539.	.9936	0.0170
15750.	.9989	0.0125
16720.	1.0000	0.0107

X = 117.90

N	F	INTENSITY
46.	.1142	0.0348
69.	.2622	0.0541
92.	.3324	0.0650
119.	.4122	0.0751
145.	.4737	0.0771
231.	.5083	0.0812
301.	.5363	0.0801
378.	.5601	0.0792
462.	.5795	0.0767
578.	.5903	0.0740
694.	.6043	0.0708
925.	.6237	0.0658
1159.	.6442	0.0648
1387.	.6476	0.0607
1850.	.6708	0.0613
2312.	.6964	0.0567
3005.	.7198	0.0568
3699.	.7457	0.0557
4624.	.7683	0.0571
5780.	.8072	0.0585
6936.	.8417	0.0614
8082.	.8751	0.0576
9249.	.9001	0.0533
10405.	.9409	0.0432
11561.	.9641	0.0335
12717.	.9824	0.0246
13873.	.9938	0.0169
15029.	.9942	0.0125
16185.	1.0000	0.0103
17341.	.9996	0.0096

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X = 143.50			X = 149.30			X = 154.50			X = 157.80		
N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY
57.	.1461	0.0294	40.	.1380	0.0198	53.	.1497	0.0288	42.	.1293	0.0161
55.	.1998	0.0500	41.	.1815	0.0404	67.	.1704	0.0406	56.	.1343	0.0202
114.	.2600	0.0630	121.	.2394	0.0570	83.	.2193	0.0514	70.	.1493	0.0289
142.	.3126	0.0765	151.	.3024	0.0731	100.	.2560	0.0585	87.	.1743	0.0398
171.	.3537	0.0829	181.	.33635	0.0864	133.	.3256	0.0744	105.	.2150	0.0501
228.	.4316	0.0930	242.	.4402	0.0960	167.	.3780	0.0850	140.	.2830	0.0676
285.	.4895	0.0950	302.	.5222	0.1035	200.	.4356	0.0923	175.	.3643	0.0829
370.	.5568	0.0956	362.	.5742	0.1073	233.	.4405	0.1019	210.	.4221	0.0954
456.	.6085	0.0934	423.	.6164	0.1039	267.	.5240	0.1059	279.	.5193	0.1056
570.	.6549	0.0917	483.	.6552	0.1038	333.	.5891	0.1084	349.	.5930	0.1126
712.	.6899	0.0833	604.	.7040	0.0966	433.	.6639	0.1088	454.	.6757	0.1089
855.	.7074	0.0769	755.	.7403	0.0875	533.	.7180	0.0978	559.	.7229	0.1006
1140.	.7275	0.0723	906.	.7643	0.0775	667.	.7522	0.0877	689.	.7707	0.0911
1425.	.7512	0.0688	1208.	.7913	0.0654	833.	.7882	0.0772	873.	.8021	0.0759
1710.	.7748	0.0523	1510.	.8155	0.0567	1000.	.8189	0.0693	1048.	.8307	0.0626
2200.	.8002	0.0505	1812.	.8207	0.0551	1333.	.8428	0.0582	1397.	.8550	0.0544
2850.	.8212	0.0522	2416.	.8461	0.0469	1667.	.8593	0.0599	1747.	.8693	0.0534
3705.	.8440	0.0480	3020.	.8634	0.0450	2000.	.8743	0.0461	2066.	.8829	0.0409
4560.	.8600	0.0454	3926.	.8808	0.0406	2667.	.8915	0.0400	2794.	.8957	0.0356
5700.	.8825	0.0435	4832.	.8973	0.0388	3333.	.9019	0.0364	3493.	.9071	0.0329
7125.	.9044	0.0405	6039.	.9146	0.0362	4333.	.9139	0.0319	4541.	.9229	0.0305
8549.	.9245	0.0370	7549.	.9328	0.0336	5333.	.9251	0.0314	5569.	.9336	0.0279
9974.	.9453	0.0336	9059.	.9510	0.0303	6667.	.9386	0.0297	6986.	.9457	0.0266
11399.	.9648	0.0289	10549.	.9675	0.0277	8333.	.9543	0.0277	8733.	.9593	0.0259
12824.	.9779	0.0229	12079.	.9807	0.0225	10000.	.9678	0.0254	10479.	.9714	0.0226
14249.	.9901	0.0169	13549.	.9907	0.0164	11667.	.9798	0.0213	12226.	.9836	0.0186
15674.	.9960	0.0116	15099.	.9962	0.0131	13333.	.9895	0.0177	13972.	.9914	0.0139
17099.	.9999	0.0092	16609.	.9999	0.0110	15000.	.9963	0.0127	15719.	.9979	0.0106
18524.	1.0000	0.0082	18114.	1.0000	0.0077	16667.	.9993	0.0093	17465.	1.0000	0.0087
19949.	.9992	0.0079	19628.	.9986	0.0069	18333.	1.0000	0.0079	19212.	1.0000	0.0079
						20000.	.9993	0.0078			

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X = 170.80

N	F	INTENSITY
82.	.1792	0.0289
162.	.2179	0.0382
127.	.2688	0.0465
143.	.3262	0.0550
178.	.3766	0.0647
264.	.4231	0.0712
255.	.5113	0.0784
366.	.5916	0.0828
357.	.6533	0.0851
468.	.7081	0.0860
459.	.7434	0.0877
569.	.7742	0.0833
611.	.8252	0.0763
713.	.8570	0.0668
815.	.8795	0.0596
1019.	.9069	0.0497
1274.	.9216	0.0395
1529.	.9314	0.0346
2030.	.9472	0.0207
2547.	.9519	0.0252
3057.	.9564	0.0230
4076.	.9647	0.0200
5095.	.9706	0.0195
6623.	.9760	0.0170
8182.	.9814	0.0161
10180.	.9873	0.0146
12228.	.9927	0.0123
14265.	.9971	0.0105
16303.	.9990	0.0088
18341.	1.0000	0.0079
20379.	.9990	0.0072

X = 166.80

N	F	INTENSITY
89.	.1902	0.0397
134.	.2723	0.0559
179.	.3624	0.0723
223.	.4422	0.0879
268.	.5136	0.0958
312.	.5754	0.0994
357.	.6167	0.0975
446.	.6922	0.0933
536.	.7380	0.0866
625.	.7780	0.0829
759.	.8163	0.0757
893.	.8448	0.0692
1116.	.8672	0.0564
1339.	.8862	0.0493
1785.	.9057	0.0412
2231.	.9189	0.0367
2678.	.9259	0.0314
3570.	.9359	0.0276
4461.	.9454	0.0224
5601.	.9555	0.0234
7140.	.9626	0.0213
8925.	.9726	0.0199
10710.	.9822	0.0174
12495.	.9880	0.0147
14280.	.9932	0.0131
16065.	.9973	0.0100
17850.	.9991	0.0092
19635.	1.0000	0.0083
21420.	.9990	0.0078

X = 164.20

N	F	INTENSITY
87.	.1854	0.0415
131.	.2710	0.0438
164.	.3424	0.0511
125.	.3137	0.0611
166.	.4379	0.0816
208.	.5584	0.0876
250.	.6159	0.0876
291.	.6637	0.0816
333.	.7259	0.0744
416.	.7750	0.0672
499.	.7990	0.0630
582.	.8152	0.0606
707.	.8162	0.0558
832.	.8479	0.0529
1040.	.8668	0.0505
1248.	.8764	0.0475
1664.	.8962	0.0427
2080.	.9034	0.0380
2496.	.9100	0.0350
3327.	.9239	0.0321
4159.	.9346	0.0299
5067.	.9456	0.0273
6655.	.9544	0.0259
8318.	.9628	0.0234
10306.	.9706	0.0213
12478.	.9868	0.0175
14557.	.9948	0.0129
16637.	.9982	0.0106
18716.	1.0000	0.0091
20795.	.9994	0.0088

X = 162.00

N	F	INTENSITY
78.	.2014	0.0650
97.	.2840	0.0657
116.	.3143	0.0728
136.	.3434	0.0760
155.	.3823	0.0876
184.	.4624	0.0998
232.	.5139	0.1075
271.	.5712	0.1108
310.	.5982	0.1108
347.	.6736	0.1082
504.	.7302	0.0998
620.	.7721	0.0799
775.	.8114	0.0721
968.	.8371	0.0617
1142.	.8500	0.0513
1550.	.8681	0.0449
1977.	.8758	0.0410
2712.	.9015	0.0359
3875.	.9190	0.0303
5037.	.9305	0.0290
6199.	.9408	0.0274
7749.	.9531	0.0266
9686.	.9666	0.0243
11624.	.9788	0.0207
13561.	.9904	0.0158
15498.	.9962	0.0132
17435.	.9985	0.0107
19373.	1.0000	0.0090
19922.	.9992	0.0088

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X = 175.00			X = 178.30			X = 181.20			X = 182.30		
N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY	N	F	INTENSITY
99.	.2848	0.0465	89.	.2660	0.0626	116.	.3040	0.0438	106.	.1698	0.0215
120.	.3203	0.0556	118.	.318*	0.0699	132.	.3273	0.0462	144.	.2312	0.0338
144.	.3524	0.0638	146.	.3656	0.0775	165.	.3892	0.0547	180.	.2924	0.0388
179.	.4159	0.0795	185.	.4247	0.0864	207.	.4680	0.0652	225.	.3691	0.0460
209.	.4754	0.0783	222.	.4868	0.0925	248.	.5402	0.0707	270.	.4544	0.0562
239.	.5138	0.0805	259.	.5375	0.0993	289.	.6042	0.0776	315.	.5204	0.0579
289.	.5997	0.0909	286.	.5982	0.1047	311.	.643*	0.0800	360.	.5768	0.0640
359.	.6610	0.0980	370.	.6604	0.1053	413.	.7337	0.0830	414.	.6405	0.0712
419.	.7023	0.0938	443.	.7022	0.0982	486.	.8046	0.0812	468.	.6959	0.0720
479.	.7460	0.0965	517.	.7448	0.0955	578.	.8439	0.0728	541.	.7591	0.0715
598.	.8098	0.0847	591.	.7944	0.0955	661.	.8786	0.0658	631.	.8084	0.0698
718.	.8486	0.0751	739.	.8477	0.0841	744.	.8989	0.0595	721.	.8457	0.0629
838.	.8799	0.0651	867.	.8980	0.0699	826.	.9185	0.0522	811.	.8776	0.0579
957.	.9020	0.0609	1035.	.9237	0.0523	982.	.9402	0.0399	901.	.9009	0.0526
1107.	.9286	0.0482	1162.	.9436	0.0419	1157.	.9526	0.0335	1041.	.9313	0.0443
1496.	.9441	0.0393	1478.	.9588	0.0299	1405.	.9639	0.0246	1261.	.9499	0.0377
1765.	.9543	0.0337	1649.	.9700	0.0242	1653.	.9719	0.0206	1532.	.9665	0.0296
2303.	.9646	0.0279	2217.	.9743	0.0210	2066.	.9765	0.0179	1802.	.9729	0.0241
2902.	.9712	0.0245	2956.	.9808	0.0176	2479.	.9804	0.0149	2252.	.9806	0.0201
3590.	.9762	0.0223	3695.	.9838	0.0158	3305.	.9858	0.0125	2703.	.9858	0.0173
4786.	.9824	0.0188	4684.	.9872	0.0132	4132.	.9873	0.0113	3604.	.9903	0.0147
5983.	.9859	0.0171	5912.	.9902	0.0127	5784.	.9925	0.0100	4505.	.9920	0.0138
7179.	.9892	0.0156	7300.	.9919	0.0112	7437.	.9943	0.0092	5406.	.9939	0.0129
9573.	.9917	0.0142	9647.	.9946	0.0107	9000.	.9964	0.0096	7208.	.9947	0.0116
11966.	.9962	0.0126	11824.	.9973	0.0098	11569.	.9982	0.0086	9910.	.9967	0.0112
14359.	.9996	0.0103	14780.	.9993	0.0095	14048.	1.0000	0.0078	12613.	.9992	0.0107
16752.	1.0000	0.0093	17737.	1.0000	0.0078	17353.	1.0000	0.0068	15316.	1.0000	0.0099
19146.	1.0000	0.0084	20693.	1.0000	0.0073				18019.	.9992	0.0092

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X = 185.80			X = 190.10		
N	F	INTENSITY	N	F	INTENSITY
133.	.1849	0.0204	240.	.5442	0.0303
155.	.2049	0.0236	260.	.5803	0.0301
177.	.2443	0.0241	321.	.6177	0.0306
222.	.3153	0.0295	401.	.6787	0.0296
277.	.4013	0.0346	481.	.7298	0.0330
333.	.4917	0.0412	561.	.7796	0.0390
388.	.5749	0.0488	641.	.8207	0.0400
444.	.6374	0.0493	721.	.8580	0.0372
510.	.7024	0.0486	801.	.8842	0.0352
577.	.7569	0.0511	902.	.9128	0.0338
644.	.8169	0.0553	1002.	.9340	0.0305
710.	.8700	0.0538	1202.	.9577	0.0242
847.	.9098	0.0477	1402.	.9738	0.0198
900.	.9330	0.0394	1603.	.9838	0.0163
1109.	.9505	0.0355	2003.	.9913	0.0124
1331.	.9746	0.0277	2653.	.9964	0.0095
1553.	.9829	0.0232	3206.	.9973	0.0089
1806.	.9861	0.0178	4007.	.9984	0.0081
2219.	.9906	0.0149	5009.	1.0000	0.0076
2662.	.9933	0.0131	6010.	.9994	0.0079
3106.	.9951	0.0122			
3641.	.9969	0.0107			
4437.	.9969	0.0103			
5546.	.9984	0.0097			
7765.	.9991	0.0091			
10538.	.9996	0.0083			
13311.	1.0000	0.0082			

APPENDIX C

ERRATA FOR REPORT SMU-1-PU

page	line	
10	bottom	"96 inches" should "93 inches"
11	6	" $3.1672 \times 10^{-4}(x)$ " should be " $3.1627 \times 10^{-4}(x)$ "
11	6	" $6.5931 \times 10^{-6}(x^2)$ " should be " $6.5931 \times 10^{-7}(x^2)$ "
11	8	" $1.1944 \times 10^{-5}(x^2)$ " should be " $1.1994 \times 10^{-5}(x^2)$ "

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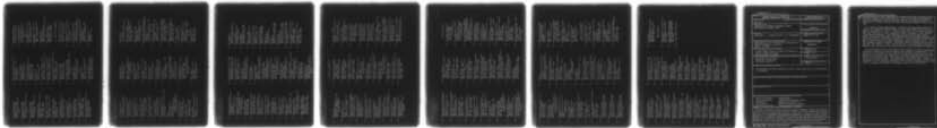
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ATTN: R.E. Smith, Jr., Chief
T-Cells Division
Engine Test Facility
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13. Air Force Aero Propulsion Laboratory
Wright-Patterson AFB, Ohio 45433
ATTN: AFAPL/TBC
Francis R. Ostidek
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Department of Defense
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ATTN: LKCG (Mr. Selph)
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(SAVDL-EU-PP)
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Moffett Field, California 94035
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23. NASA Ames Research Center
Aerodynamics Branch 227-8
Moffett Field, California 94305
ATTN: Mr. Ira R. Schwartz
24. NASA Lewis Research Center
21000 Brookpark Road
Cleveland, Ohio 44135
ATTN: D. Morris, Mail Stop 60-3
25. NASA Lewis Research Center
Hypersonic Propulsion Section
Mail Stop 6-1
21000 Brookpark Road
Cleveland, Ohio 44135
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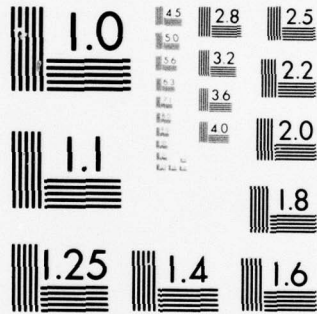
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LAMINARISCENT TURBULENT BOUNDARY LAYERS: EXPERIMENTS ON NOZZLE --ETC(U)
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ATTN: Dr. F.B. Gessner
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20. ABSTRACT (Continue on reverse side if necessary and identify by block number) Because a turbulent boundary layer in a nozzle undergoes strong acceleration, a laminariscent boundary layer with the benefit of a lower surface heat transfer rate can result for some short distance. Here, and in a previous report (Simpson and Wallace, 1975) several phenomena which accompany laminarescence produced by strong acceleration are examined for nozzle-flow and sink-flow accelerational distributions, respectively. Several different type measurements of the structure of two nozzle-type flows are reported to determine how an initially normal		

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20. turbulent boundary layer approaches the laminar-like state, including mean velocity and Reynolds stresses profiles, spectra, turbulent/non-turbulent interfacial structure, and wall bursting and sublayer spanwise spatial structure.

As a result of these experiments, it appears that the surface skin-friction is not reduced to laminar values in sink flows unless $K(=\nu U_{\infty}^{-2} dU_{\infty}/dx)$ is greater than about 3.6×10^{-6} . In nozzle-type flows, K must also be greater than this value over a short distance in order to produce a short relaminarized region downstream. The large-eddy structure of the outer region governs the bursting frequency, the intermittent bulge passage frequency, and influences the wall flow behavior downstream. After the cessation of entrainment of free-stream fluid, these frequencies approach constant values. The wall spanwise structure appears to lag behind local conditions and to reflect upstream flow behavior. After retransition to a low acceleration turbulent boundary layer downstream, much larger spanwise scale structures are observed.

The entrainment rate of non-turbulent fluid decreases to zero at about the streamwise location at which the shape factor reaches a minimum value. The cessation of entrainment by the eruption and engulfment action of the large eddies can be traced to the reduction of available turbulence energy for diffusion to free-stream fluid. This reduction of available energy is due to the negative normal stresses turbulence energy production term. Spectral distributions of the streamwise fluctuation $F(n)$ possess a frequency region where $nF(n)$ is constant for laminar-like boundary layers at large K values.

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