## FINAL REPORT

## Electrokinetic-Enhanced (EK-Enhanced) Amendment Delivery for Remediation of Low Permeability and Heterogeneous Materials

## ESTCP Project ER-201325

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This project demonstrated and validated electrokinetic(EK)-enhanced amendment delivery for in-situ bioremediation (EK-BIO) via enhanced reductive dechlorination (ERD) of a tetrachloroethene source area in clay. The EK-enhanced amendment delivery technology entails the establishment of an electric field in the subsurface using a network of electrodes. The electrical current and voltage gradient established across a direct-current electric field provide the driving force to transport remediation amendments, including electron donors, chemical oxidants, and even bacteria, through the subsurface. This project showed that EK could achieve relatively uniform transport in low-permeability materials. This technology also represents a remedial alternative with excellent environmental performance.

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| A | amp |
| :--- | :--- |
| AC | alternate current |
| cm | centimeter |
| cm/sec | centimeter per second <br> CVOC <br> chlorinated volatile organic compounds <br> cis-1,2-dichloroethene <br> ke |
| coefficient of electroosmotic permeability |  |


| low-K | low-permeability |
| :---: | :---: |
| $\mu \mathrm{g} / \mathrm{g}$ | microgram per gram |
| $\mu \mathrm{g} / \mathrm{L}$ | microgram per Liter |
| $\mathrm{mg} / \mathrm{kg}$ | milligram per kilogram |
| mV | millivolts |
| m | minutes |
| MMO | mixed metal oxide |
| NAS | Naval Air Station |
| NAVFAC | Naval Facilities Engineering Command |
| OU3 | Operable Unit 3 |
| ORP | oxidation-reduction potential |
| POC | points of contact |
| PVC | Polyvinyl chloride |
| $\mathrm{K} 2 \mathrm{CO}_{3}$ | potassium carbonate |
| PSV | pressure safety valve |
| PLC | programmable logic controller |
| qPCR | quantitative polymerase chain reaction |
| $\mathrm{cm}^{2}$ | square centimeter |
| TTA | target treatment area |
| PCE | tetrachloroethene |
| TCE | trichloroethene |
| TOC | total organic carbon |
| USACE | United States Army Corps of Engineers |
| VC | vinyl chloride |
| vcrA | vinyl chloride reductase |
| VFA | volatile fatty acid |
| VOC | volatile organic compound |
| V | volts |
| V/m | Volts per minute |
| $w / w$ | weight per weight |
| XRD | X-Ray Diffraction |

## EXECUTIVE SUMMARY

This Demonstration/Validation (Dem/Val) project was conducted at Naval Air Station (NAS) Jacksonville, Florida, to assess and validate the performance of an electrokinetic (EK) technique to promote uniform and effective distribution of remediation amendments (e.g., electron donors, electron acceptors, chemical oxidants) in low-permeability (low-K) and heterogeneous subsurface materials. Recent advances in the understanding of mass distribution in subsurface environments has highlighted that in many cases a significant portion of the source mass is held in storage in low-K materials. The main limitation of current in situ remediation applications in low-K materials using conventional hydraulic recirculation or injection techniques is the inability to effectively deliver the required amendments to the target contaminant mass. The EK-enhanced amendment delivery technology entails the establishment of an electric field in the subsurface using a network of electrodes. The electrical current and voltage gradient established across a direct-current (dc) electric field provide the driving force to transport remediation amendments, including electron donors, chemical oxidants, and even bacteria, through the subsurface.

The EK Dem/Val system consists of nine (9) electrode wells and eight (8) supply wells located within a target treatment area (TTA) measuring approximately 40 feet by 40 feet. The remediation amendments distributed by the EK remediation system included electron donor (lactate provided as potassium lactate), pH control reagents (potassium carbonate), and a dechlorinating microbial consortium (KB-1 ${ }^{\circledR}$ ) containing Dehalococcoides (Dhc). Following the system startup, initial site conditioning, and bioaugmentation of the site, the Dem/Val included two (2) separate stages, 5month each, of active operation with a 6-month incubation period between the two active stages.

The overall goal of this Dem/Val is to demonstrate and validate EK-enhanced amendment delivery for in-situ bioremediation (EK-BIO) via enhanced reductive dechlorination (ERD) of a tetrachloroethene (PCE) source area in clay. Several performance objectives were identified and assessed based on the performance monitoring data collected:
I. Demonstrate uniform distribution of the amendments and relative uniformity of the established electrical field.
This Dem/Val met this objective by meeting the success criteria, including:

- At groundwater monitoring locations within the TTA after the completion of active EK operation, post-EK concentration of total organic carbon (TOC) was at least 5x baseline; and
- No local focusing of electric field was observed within the TTA.
II. Demonstrate effectiveness of treatment established by EK-BIO operation within the TTA.

This Dem/Val met this objective by meeting the success criteria, including:

- $>60 \%$ reduction in average PCE concentrations was achieved in soil and groundwater within the TTA. While groundwater data also showed coupled and comparable increases of dechlorination daughter and end products, no such apparent increases of degradation products were observed in soil samples;
- Ethene was detected at $100 \%$ of groundwater monitoring wells within the TTA; and
- $>10 \mathrm{x}$ increases of Dh from baseline was observed at $>60 \%$ of soil and groundwater samples collected from within the TTA.


## III. Demonstrate suitability of this technology for full-scale implementation.

This Dem/Val met this objective by meeting the success criteria, including:

- System operation conditions (voltage and current) were maintained within $\pm 50 \%$ of the designed target conditions;
- Amendment supply up-time was $>75 \%$ of target; and
- Energy consumption was within $\pm 30 \%$ of design estimates.

This Dem/Val showed that a critical and distinct advantage of the EK-enhanced amendment delivery over other conventional advective flow-based approaches is that EK can achieve relatively uniform transport in low-K materials. EK-enhanced delivery is a safe and relatively more controllable approach compared to high-pressure/fracturing injection and thermal approaches. This technology also represents a remedial alternative with excellent environmental performance. The electrical energy consumed during the active EK operation period in this Dem/Val was equivalent to operating two $100-\mathrm{W}$ lightbulbs over the same time interval.

Based on the information and experience obtained from this Dem/Val, there are three main cost drivers to consider when evaluating implementation costs in future projects, including: (1) footprint, depth interval, and volume of target treatment zone and contaminant mass; (2) presence and location of above-ground and subsurface utilities; and (3) site geochemistry, particularly pH and iron. These are also the same cost drivers for many other in-situ remediation technologies and not unique to EK technology implementation.

A cost comparison was developed and showed that EK-BIO could be potentially more cost favorable to an in situ thermal treatment approach, electrical resistance heating (ERH). It is also noted that the significant difference in the electrical energy needed for these two technologies indicating a much more favorable environmental performance of EK-BIO over ERH. The cost comparison also showed that EK-BIO approach is slightly more cost favorable to direct-injection enhanced in situ bioremediation (EISB) and fracturing enhanced zero-valent iron (ZVI) direct injection. However, at sites where low-K material and/or high-degree of heterogeneity likely preclude the consideration for direct injection, EK-BIO provides a cost-effective solution for implementing in situ bioremediation.

While EK-BIO is mainly a variation on standard EISB whereby EK is used to more effectively deliver the required amendments through low-K materials, some areas where additional attention, beyond those typically considered for EISB, may be required on a site-specific basis include:

- Safety considerations related to potential stray current/voltage to surface. To address this question, we checked the current and voltage at the manhole steel cover located within the treatment area while the EK system was in operation to confirm that there was no safety concern. Depending on project site, and for sensitive and active facilities with dedicated safety departments, additional design and explanation effort may be required for project approvals.
- Iron fouling of filters and valves along the catholyte (well water from cathode wells) extraction line. In this Dem/Val, we re-plumbed the system to minimize potential flow restriction points. Scaling of the cathodes also required maintenance actions to clean the cathode surface. As indicated above, this issue diminished over the course of the Dem/Val.
- Corrosion of metallic parts in the manifold system \& wellhead fittings due to elevated chloride concentrations. In this Dem/Val, we replaced most metallic contacting parts with plastic parts upon discovering that chloride levels were far higher than initially known.
- The technology implementation did not require specialized/proprietary equipment. We used only standard commercial off-the-shelf equipment. We designed the manifold and control system and had a remediation system vendor assemble the system per design, but the overall system was similar to other "typical" in-situ remediation systems.
- If the technology is to be implemented near (laterally and/or vertically) utilities that are "sensitive" to electric interference or corrosion concerns, some protection measures, such as cathodic protection, may be considered.
- No special regulatory requirements or permits beyond what are typical for other EISB or ISCO projects such as UIC permit. Depending on the locality-/facility-specific requirements, local or facility power/electrical departments should be consulted.

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### 1.0 INTRODUCTION

This Draft Final Report summarizes the approach, methodology and results of a field Demonstration / Validation (Dem/Val) project conducted to assess and validate the performance of an electrokinetic (EK) technique to promote uniform and effective distribution of remediation amendments (e.g., electron donors, electron acceptors, chemical oxidants) in low-permeability (low-K) and heterogeneous subsurface materials, for the purposes of improving remediation success at low-K sites. This project was conducted in collaboration with Naval Facilities Engineering Command (NAVFAC) and the United States Army Corps of Engineers (USACE) Engineer Research \& Development Center (ERDC).

### 1.1 BACKGROUND

Decades of remediation experience have shown that in-situ remediation approaches are more successful and cost effective than most ex-situ remediation methods. However, in-situ remedies, such as enhanced in-situ bioremediation (EISB) and in-situ chemical oxidation (ISCO), while capable of treating various contaminants in permeable sandy aquifers, often fail to effectively target contaminants in silt and clay materials, or combinations of sand and low-K materials. Recent advances in the understanding of mass distribution in subsurface environments has highlighted that in many cases a significant portion of the source mass is held in storage in low-K materials, and that the release rate from low-K storage is many times slower than the original contaminant loading rate. The main limitation of EISB and ISCO applications in low-K materials is the inability to effectively deliver the required amendments to the target contaminant mass contained within the low-K material using conventional hydraulic recirculation or injection techniques.

While hydraulic fracturing has shown some promise in improving amendment distribution in lowK materials, the success of this approach has been limited by site access constraints, surface structure impact concerns, high cost, and consistency and predictability of induced fractures. Other technologies such as large diameter auger mixing and thermal treatment have shown promise in low-K materials. However, these approaches have been expensive and are also limited by site access and re-use limitations. Conventional thermal remediation approaches also face the challenges of removing and treating gaseous phase contaminants. Lower cost, and ideally more environmentally-sustainable remediation approaches or improvements to existing technologies are required to reduce overall remediation costs at Department of Defense (DoD) and defense contractor sites.

The EK-enhanced amendment delivery technology entails the establishment of an electric field in the subsurface using a network of electrodes. The electrical current and voltage gradient established across a direct-current (dc) electric field provide the driving force to transport remediation amendments, including electron donors, chemical oxidants, and even bacteria, through the subsurface. One reason why EK represents a fundamentally more effective delivery technique compared to an advective hydraulic approach is the relatively uniform electrical property of various soil materials. As a result, EK-enhanced amendment delivery technology can achieve effective and uniform amendment distribution at sites where heterogeneous subsurface materials often limit the applications of hydraulic methods.

### 1.2 OBJECTIVE OF THE DEMONSTRATION

The overall goal of this project is to Dem/Val the use of EK-enhanced amendment delivery to achieve uniform and effective distribution of remediation amendments into and through low-K and heterogeneous materials in the subsurface, thereby improving the effectiveness of in-situ remediation (in this case, EISB) and reducing the costs of remediation at DoD sites impacted by chlorinated and recalcitrant contaminants. The specific technical objectives for this Dem/Val project are as follows:
i) demonstrate and quantify the ability to uniformly distribute remediation amendments (in this case, lactate and Dehalococcoides (Dhc) microorganisms) across a target treatment area (TTA) using a dc electric field;
ii) demonstrate the ability to promote and sustain effective biodegradation within the TTA as a result of amendment delivery by EK;
iii) evaluate EK system operational parameters and resolve potential operational issues (e.g., scaling of electrodes) to allow engineering design and implementation of full-scale EK systems; and
iv) develop costing information for technology evaluation by DoD and remediation practitioners.

### 1.3 REGULATORY/TECHNICAL/COST DRIVERS

In 2011, a SERDP/ESTCP-sponsored workshop on Investment Strategies to Optimize Research and Demonstration Impacts in Support of DoD Restoration Goals identified treatment of contaminants in low-K subsurface materials (i.e. silts, clays, and bedrock) as a high-priority area for additional investment. The workshop participants noted that treatment of low-K zones would require adoption of cost-effective techniques that can target delivery of remedial agents to these regions and prevent continued back-diffusion of contaminants.

Estimated costs to DoD for adopting hydraulic containment at more than 3,000 chlorinated hydrocarbon sites could surpass $\$ 100$ million annually, with estimated life-cycle costs of more than $\$ 2$ billion (SERDP/ESTCP, 2006). EISB has generally been considered as one of the more cost-effective remedial options available for chlorinated solvent sites. However, there are sites where the effectiveness of EISB is limited by the presence of low-K zones, or sites where more expensive alternatives are the presumed options due to the concerns of low-K materials. Improved delivery of remediation amendments can reduce the overall duration and cost of EISB, as well as allow the consideration of lower cost EISB options at more DoD sites where low-K zones represent a limiting factor in remedy selection and success.

### 2.0 TECHNOLOGY

This section provides an overview of the EK-enhanced amendment delivery technology that was demonstrated in this project. Advantages and potential limitations associated with this technology are also discussed.

### 2.1 TECHNOLOGY DESCRIPTION

The EK-enhanced amendment delivery technology entails the use of electrodes and dc electrical power to establish an electric field in the subsurface. The voltage gradient established across the $d c$ electric field is then the driving force for transporting remediation reagents, including electron donors for microorganisms, chemical oxidants, and even bacteria, through low-K soils or uniformly through heterogeneous formations. The EK transport process relies on three mechanisms which occur with the application of the electric field:

- Electromigration (or ion migration) - the movement of charged dissolved ions through an aqueous medium in response to the applied electric field. The direction of ion migration is toward the electrode with a polarity opposite of the ion's charge;
- Electroosmosis - the movement of pore fluid (and dissolved constituents) within a porous medium in response to the applied electric field. The direction of electroosmotic flow is usually from the anode toward the cathode; and
- Electrophoresis - the movement of charged particles, such as clay particles or bacteria, through an aqueous medium in response to the applied electric field. Similar to electromigration, the direction of ion migration is toward the electrode with a polarity opposite to that of a particle's net charge.

This Dem/Val project focused on the amendment transport facilitated by electromigration and electroosmosis. While ion migration phenomenon is readily apparent and understandable as it reflects basic electrochemistry, electroosmosis is a more complex EK phenomenon. Certain subsurface materials, such as clays, have a negative surface charge due to their mineral contents and crystal lattice structures. Porewater surrounding these soil particles, containing mixtures of cations and anions, forms a boundary layer system (i.e., double layer) around these negatively charged soil particles consisting of an inner immobile zone (Stern layer) and an outer mobile zone (Diffuse layer). The electrical potential at the interface between the two zones is known as the zeta potential. Upon the application of a voltage gradient, the surface of the Stern layer (positively charged layer in this case) allows the movement of cations drawing along the surrounding water molecules toward the negatively charged electrode (i.e., cathode). The value of the zeta potential is dependent on the pore fluid's ionic strength and pH .

The rate of electroosmotic flow is proportional to the coefficient of electroosmotic permeability $\left(\mathrm{k}_{\mathrm{e}}\right)$, which is a measure of the rate of fluid flow per unit area under a unit voltage gradient. The value of $\mathrm{k}_{\mathrm{e}}$ is a function of the zeta potential of the soil particle surface, viscosity of the pore fluid, porosity, and electrical permittivity of the medium.

One reason why EK represents a fundamentally more effective delivery technique for low-K and heterogeneous soils compared to an advective hydraulic approach is the relatively uniform electrical property of various soil materials. For example, as presented in Figure 2-1, while the hydraulic conductivity of fine sand and kaoline materials can vary by several orders of magnitude, the coefficient of electroosmotic permeability of fine sand ( $4.1 \mathrm{E}-05 \mathrm{~cm}^{2} / \mathrm{sec}-\mathrm{V}$ ) is comparable to that of kaoline ( $5.7 \mathrm{E}-05 \mathrm{~cm}^{2} / \mathrm{sec}-\mathrm{V}$ ) and clayey till ( $5.0 \mathrm{E}-05 \mathrm{~cm}^{2} / \mathrm{sec}-\mathrm{V}$ ). Therefore, the EKenhanced amendment delivery technology can achieve effective and uniform amendment distribution at sites where heterogeneous subsurface materials often limit the applications of hydraulic methods.


Figure 2-1. Hydraulic and Electrical Properties of Various Soils (rev. Mitchell, 1993)

The application of electric current will also result in electrolytic reactions at the electrodes. If inert electrodes (such as graphite or ceramic-coated electrodes) are used, water oxidation produces oxygen gas and acid $\left(\mathrm{H}_{3} \mathrm{O}^{+}\right)$at the anode (positively charged electrode), while water reduction produces hydrogen gas and base $\left(\mathrm{OH}^{-}\right)$at the cathode (negatively charged electrode). Electrolytic reactions of water are shown below in Equations 1 and 2,

$$
\begin{array}{cll}
2 \mathrm{H}_{2} \mathrm{O} & ==>4 \mathrm{e}^{-}+4 \mathrm{H}^{+}+\mathrm{O}_{2} & \\
2 \mathrm{H}_{2} \mathrm{O}+2 \mathrm{e}^{-} & ==>2 \mathrm{OH}^{-}+\mathrm{H}_{2} &  \tag{2}\\
\text { (at Anode) } \\
\text { (at Cathode) }
\end{array}
$$

Faraday's law for equivalence of mass and charge can be used to calculate the rate of redox reactions that will occur at the electrodes (Koryta and Dvorak, 1987). Therefore, it is possible to engineer and control the electrolytic processes at the electrodes to produce hydrogen $\left(\mathrm{H}_{2}\right)$ and oxygen $\left(\mathrm{O}_{2}\right)$ or to control pH conditions, depending on the system design objectives.

To implement the EK-enhanced delivery technology in the field, remediation amendments are added to electrode wells and potentially additional supply wells located intermediary to the electrode wells, mainly to shorten amendment travel distance versus consumption rate (Figure 22). Electrodes of selected inert materials are installed in electrode wells and connected to a dc power source. The power supply unit will supply electrical energy to electrodes at designed settings of voltage and/or current. The electrical field will transport the amendments from the electrode wells and supply wells into and through the formation materials to achieve a relatively uniform transport and distribution. Cross-circulation and pH -balancing can be employed at the electrode wells to overcome the effects of water electrolysis, and retain the natural in-situ pH of the system (as required). Slight subsurface heating may occur with application of the electrical field. However, results from field trials have shown that temperature increases are minor (less than $10^{\circ} \mathrm{C}$. A modest increase in temperature often results in an improvement in the bioremediation process, as has been shown for Dhc during trichloroethene (TCE) dechlorination, where dechlorination was faster at $30^{\circ} \mathrm{C}$ than $15^{\circ} \mathrm{C}$ (Friis et al., 2007).


Figure 2-2. Schematic of EK-Enhanced Amendment Delivery Technology

### 2.2 TECHNOLOGY DEVELOPMENT

Results from many studies conducted at both bench-scale and field-pilot scale have shown the potential of EK-enhanced amendment transport (Mao et al., 2012; Gent, 2001; Wu et al., 2007; Reynolds et al., 2008; Hodges et al., 2011; SERDP ER-1204). Bench-scale studies conducted at ERDC effectively delivered acetate through loess soil ( $\mathrm{K}=10^{-7} \mathrm{~cm} / \mathrm{s}$ ) and vertically deposited clay ( $\mathrm{K}=10^{-9} \mathrm{~cm} / \mathrm{s}$ ) at rates of 2.1 and $2.5 \mathrm{~cm} /$ day, respectively, with a voltage gradient near $0.5 \mathrm{~V} / \mathrm{cm}$ (Gent, 2001).

An average lactate transport rate of $3.4 \mathrm{~cm} /$ day under a unit voltage gradient of $1 \mathrm{~V} / \mathrm{cm}$ was achieved in a bench-scale study conducted using a silty clay ( $\mathrm{K}=10^{-7} \mathrm{~cm} / \mathrm{s}$ ) (SERDP ER-1204). The observed EK-enhanced transport rate in that SERDP study was more than 120 times higher than the transport rate achievable in the same type of soil but under a unit hydraulic gradient. The use of EK-enhancement for ISCO has also been demonstrated at the bench scale in both column and sandbox experiments (Roach et al., 2006; Reynolds et al., 2008; Robertson, 2009; Hodges et al., 2011). Common oxidants such as permanganate and persulfate are charged compounds, and will migrate under the driving force of the imposed electric gradient. Migration rates of monovalent and divalent oxidants have been measured in the laboratory at levels in excess of 500 times higher than that achievable through diffusion alone.

Geosyntec, in collaboration with ERDC, completed a field pilot test of EK-enhanced delivery for in-situ bioremediation (EK-BIO) at a site in Denmark, which achieved a lactate transport rate between 2.5 and $5 \mathrm{~cm} /$ day through clay materials. The pilot test involved simultaneous biostimulation (using lactate) and bioaugmentation (using dechlorinating culture KB-1 ${ }^{\circledR}$ ) targeting a PCE source area. Active EK operation for lactate distribution was conducted for approximately 8 weeks, followed by 16 weeks of post-EK monitoring. Results from the pilot test (both groundwater samples and clay cores) indicated general uniformity of distribution of electron donor, rapid establishment and growth of the bioaugmented Dhc within the clay, and rapid dechlorination of PCE, TCE, and cis-1,2-dichloroethene (cDCE) to vinyl chloride (VC) and ethene. Results from both laboratory studies and the field pilot test for this site showed that the applied electrical field had no deleterious impacts on the microorganisms or subsurface conditions. During the EK field pilot test, the average groundwater temperature in the demonstration area increased from $17^{\circ} \mathrm{C}$ to $25^{\circ} \mathrm{C}$, which was believed to provide improved conditions for PCE dechlorination by the introduced Dhc.

### 2.3 ADVANTAGES AND LIMITATIONS OF THE TECHNOLOGY

A critical and distinct advantage of the EK technology over most other approaches is that EK can achieve relatively uniform transport in inter-bedded clays and sands, even when the hydraulic conductivities of the subsurface materials vary by orders of magnitude. EK-enhanced transport, which relies primarily on the electrical properties of aquifer materials instead of the hydraulic properties, represents a solution to the limitations of preferential pathways facing conventional advective-based hydraulic technologies.

EK-enhanced delivery is a safer, and more controllable approach compared to current highpressure/fracturing injection and thermal approaches. The migration of remediation reagents is directed by the electrical field established between electrodes, and no high injection pressures are involved.

EK-enhanced delivery also represents a remediation technology with good environmental performance. Unlike other technologies that repeatedly deliver/flush amendments through a small number of preferential pathways in the subsurface, the EK technology can uniformly deliver the amendments, maximizing treatment effectiveness and reducing treatment cost and duration. When coupled with existing in situ remediation technologies (i.e., EISB and ISCO), EK-BIO and EK-ISCO can achieve direct treatment and destruction of target contaminants in situ instead of transferring contaminants to the gas phase, which requires additional containment/collection and treatment.

The electrical energy usage of EK-enhanced delivery is relatively low compared to current thermal remediation technologies. The EK-BIO field pilot test conducted by Geosyntec in Denmark required less than 100 volts (V) and $15 \mathrm{amp}(\mathrm{A})$ of electrical power to sustain the EK operation. The energy usage of the EK-BIO pilot test was equivalent to the energy needed to power approximately ten 100-watt light bulbs, reflecting the small carbon footprint and excellent environmental performance of this technology. As discussed in Section 6.1 of this report, the electrical power used in this Dem/Val (maintained at $<30 \mathrm{~V}$ and $<10 \mathrm{~A}$ ) also demonstrated the excellent energy efficiency of this technology.

There are several aspects of this technology that will require appropriate considerations and control measures:

- Safety considerations related to potential stray current/voltage to ground surface.
- If the technology is to be implemented near (laterally and/or vertically) utilities that are sensitive to electric interference or corrosion concerns, some protection measures, such as cathodic (grounding) protection, may be required. Depending on the locality / facilityspecific requirements, local or facility power/electrical departments should be consulted.
- Although conceptually there is no depth limit for this technology, shallow treatment zones too close to the ground surface and/or utilities, or in a vadose zone, can limit the feasibility of this technology.
- Certain site hydrogeology or geochemical conditions may limit the applications or impact the costs of this technology, including
- Very high levels of sulfate or nitrate that challenge the supply of electron donors for promoting and sustaining reductive dechlorination. This limitation is not specific to EK amendment delivery, instead, it is a limitation for anaerobic in situ bioremediation.
- High natural groundwater flow velocity in the permeable portion of a target treatment zone may potentially limit the EK transport in the direction against the natural groundwater flow.
- High levels of chloride and/or iron that require particular engineering control measures (e.g., corrosion protection) or more operational maintenance efforts for fouling controls. Iron fouling is also a common challenge to other in situ remediation technologies.

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### 3.0 PERFORMANCE OBJECTIVES

The overall goal of this Dem/Val is to demonstrate and validate EK-enhanced amendment delivery for in-situ bioremediation via enhanced reductive dechlorination (ERD) of a PCE source area in clay. Performance objectives were identified and approved by ESTCP to provide the basis for evaluating the performance and costs of the Dem/Val technology. Table 3-1 presents a summary of the quantitative and qualitative performance objectives, which are further discussed in the following subsections.

Table 3-1. Performance Objectives

| Performance Objective | Data Requirements | Success Criteria | Assessment |
| :---: | :---: | :---: | :---: |
| Quantitative Performance Objectives |  |  |  |
| I. Demonstrate uniform distribution of the amendments and relative uniformity of the established electrical field | - Pre- and post-EK monitoring of the concentrations of amendments <br> - Monitoring of voltage and electrical current within the EK system during operation | - At groundwater monitoring locations within the TTA after the completion of active EK operation - post-EK concentration of TOC is $5 x$ baseline, or 10x detection limit if baseline is below detection <br> - No local focusing of electric field within the TTA - no electrical potential gradient between any individual pair of cathode-anode is $5 x$ the average electrical gradient between all pairs of electrodes <br> - Electrical potential gradient between electrode pairs maintained at level no more than 5x target gradient at design current | Objective Met <br> (see Section 3.1) |
| II. Demonstrate effectiveness of treatment established by EK-BIO operation within the TTA | - Pre- and post-EK concentrations of chlorinated ethenes in soil and groundwater <br> - Pre- and post-EK concentrations of ethene in groundwater <br> - Pre- and post-EK concentrations of biomarker (qPCR analysis of Dhc and/or vinyl chloride reductase [vcrA]) in soil and groundwater | - $>60 \%$ reduction in average PCE concentrations in soil and groundwater within the TTA, with coupled and comparable molar concentration increases of dechlorination daughter and end products <br> - Ethene/ethane detected at > 75\% of groundwater monitoring wells within the TTA before the completion of post-EK monitoring <br> - > 10x increases of Dhc from baseline at $>50 \%$ of soil and groundwater samples collected from within the TTA before the completion of post-EK monitoring | Objective Met <br> (see Section 3.2) |
| III. Demonstrate suitability of this technology for full-scale implementation | - EK system operational parameters, amendment usage, and energy consumption | - System operation conditions (voltage and current) within $\pm 50 \%$ of the designed target conditions <br> - Amendment supply up-time $>75 \%$ of target <br> - Energy consumption within $\pm 30 \%$ of design estimates | Objective Met <br> (see Section 3.3) |
| Qualitative Performance Objectives |  |  |  |
| Performance Objective | Data Requirements | Success Criteria | Assessment |
| IV. Safe and reliable operation | - Monitoring of system operational parameters | - Operation conditions remain stable within the normal designed ranges over the course of the demonstration period <br> - No lost-time incidents | Objective Met <br> (see Section 3.4) |
| V. Ease of implementation | - Feedback from field personnel on installation and operation of technology and system | - Ability to construct using conventional techniques and contractors <br> - A single field technician able to effectively monitor and maintain normal system operation | Objective Met <br> (see Section 3.4) |

### 3.1 PERFORMANCE OBJECTIVE: DEMONSTRATE UNIFORM DISTRIBUTION OF AMENDMENT

The main objective of the EK technology is to achieve uniform distribution of the remediation amendments in the subsurface upon injection under the established electric field conditions. The effective distribution of the amendments (electron donor and Dhc,) is essential to the success of the technology (EISB via ERD in this project).

### 3.1.1 Data Requirements

Uniform distribution of remediation amendments was determined by measuring concentrations of remedial reagents at all monitoring locations in the TTA. Groundwater and soil core samples were collected and analyzed in accordance with the sampling plan. Additionally, measurements of electric current and voltage were taken during system operation to assess the uniformity of the electrical field.

### 3.1.2 Success Criteria

This objective is considered achieved upon observing evidence of amendment (represented by TOC) transport at monitoring locations (5x baseline or 10x detection limit if baseline is below detection). Potential variability associated with the baseline data was assessed through calculating the arithmetic average and standard deviation.

For successful achievement of a uniform electric field at design levels, the electrical gradient between any individual pair of cathode-anode should not be more than 5 times the average electrical gradient between all pairs of electrodes. Moreover, the electrical potential gradient between electrode pairs should be maintained at a level no more than 5 times the target gradient.

### 3.1.3 Performance Objective Assessment

As presented in Table 6-4, every monitoring well within the TTA had TOC concentrations $>8 \mathrm{x}$ baseline levels (for each well) during Stage 1 and/or Stage 2 operation, with the exception of EKMW04 where the maximum TOC detected was $1.8 x$ of the baseline. However, at EKMW-04 the maximum VFA detected was $>9 \mathrm{x}$ its baseline. With respect to VFAs, all but one monitoring well (EKMW-05) had concentrations $>9 x$ baseline levels. As such, the Dem/Val has met this criterion in the EK was able to substantially increase electron donor concentrations across the entire TTA.

As presented in Figure 6-2, the voltage measured at discrete locations within the TTA were between 5.3 V and 6.2 V , with a standard deviation of $0.31 \mathrm{~V}(5 \%)$. Voltage gradients were calculated between locations of closest pairs shown in Figure 6-2 and range between 0.1 to 0.26 $\mathrm{V} / \mathrm{m}$. The calculated voltage gradients between these pairs are within 3 x of each other and within 2 x of the average gradients $(0.13 \mathrm{~V} / \mathrm{m})$ indicating no local focusing of electric field within TTA. The Dem/Val has met this criterion.

The EK system was designed and operated at a constant current, determined after the start-up period, during the Dem/Val. As presented in Figure 6-1, during Stage 1 and Stage 2 operation, the voltage required of the power supply unit was generally consistent at between 15 V and 30 V , except for a few occasions when electrodes were in need of replacement. The electrical current supplied to individual wells during each stage of operation was generally steady (variation within $37 \%$ of average).

Given that (1) soil electrical resistivity is a soil property not expected to vary over the course of Dem/Val, and (2) the voltage output by the power supply unit and the current supplied to individual electrodes were generally steady, the electrical potential between electrode pairs within the TTA should maintain within 5 x of target during operation. The Dem/Val has met this criterion.

### 3.2 PERFORMANCE OBJECTIVE: PROMOTE AND SUSTAIN EFFECTIVE BIODEGRADATION

The success of biodegradation depends on a sustained supply of remediation amendments such as electron donor. The benefit of the EK technology is its ability to facilitate transport of the remediation agents into hard-to-reach contaminant storage (low-K) areas/zones, thereby creating conditions that stimulate microbial activity and accomplish contaminant degradation.

### 3.2.1 Data Requirements

The effectiveness of EK in promoting biodegradation in the TTA was evaluated on the basis of concentrations of chlorinated ethenes in groundwater and soil, and ethene/ethane concentrations in groundwater in the TTA. Pre- and post-EK groundwater and soil core samples were collected and analyzed to assess the changes in chlorinated ethenes and ethene concentrations in the TTA. A baseline characterization event was performed to assess the pre-EK concentrations and establish the baseline conditions within the TTA.

### 3.2.2 Success Criteria

This objective is considered achieved through the observation of a $60 \%$ average reduction in PCE concentrations in groundwater and soil, coupled with comparable molar concentration increases of dechlorination daughter and end products at monitoring locations in the TTA. In addition, detection of ethene/ethane in more than $75 \%$ of groundwater monitoring wells within the TTA is indicative of successful attainment of this objective. Sustained biodegradation was successfully demonstrated by observing an increasing trend, or sustained elevated levels, of degradation intermediates and end products in the groundwater monitoring wells within the TTA for as long as sufficient (e.g., greater than 5 times the baseline concentration) electron donor was present.

### 3.2.3 Performance Objective Assessment

For each of the six monitoring wells located within the TTA, decreases of $>80 \%$ in PCE concentration were achieved at the end of either Stage 1 and/or Stage 2. Also presented in Figure 6-3 and Table 7-1, the decreases of PCE from baseline at each well within the TTA were coupled with evident increases of dechlorination daughter products and/or ethene. The Dem/Val has met this criterion for groundwater.

Figure 6-5 presents a comparison of soil chlorinated volatile organic compounds (CVOC) at corresponding locations between the three (3) sampling events. The data presented in Figure 6-5 are arranged per individual locations and sampling depths. Overall, soil PCE concentrations of all samples collected from 18.5 feet below ground surface ( ft bgs ) at the nine (9) locations within the TTA decreased by $78 \%$ (C6) to $99 \%$ (C3) from baseline to post-Stage 2, with an average decrease of $88 \%$.

It was also noted that while C6 was the only location with evident baseline PCE concentration at 21 ft bgs ( $5.5 \mathrm{mg} / \mathrm{kg}$ ), the PCE concentration at this depth and location decreased to $0.21 \mathrm{mg} / \mathrm{kg}$ ( $96 \%$ reduction) and below in subsequent post-operation sampling events. As such, the Dem/Val met the PCE soil reduction criterion.

As presented in Figure 6-3 and Table 7-1, every (100\%) monitoring well within the TTA showed increased concentrations of ethene (up to $>1,000 \mu \mathrm{~g} / \mathrm{L}$ ) during the Dem/Val. The Dem/Val has met this criterion. Figure 6-3 also shows that every monitoring well within the TTA showed significant increases (several orders of magnitude) of Dhc and vcrA. The Dem/Val has met this criterion for groundwater.

As presented in Table 6-9, among the nine post-Stage 2 soil samples collected from within the TAA, six samples were reported with quantifiable levels, plus one with estimated level, of Dhc, while all baseline soil samples did not contain detectable levels of Dhc. Of the seven samples with detected Dhc, five samples (C2, C3, C5, C7, and C9) showed functional genes for VC dechlorination. Thus, while not as impressive as the groundwater results, the Dem/Val has met this criterion for soil.

### 3.3 PERFORMANCE OBJECTIVE: DEMONSTRATE SUITABILITY FOR FULLSCALE IMPLEMENTATION

For this project, the application of EK technology is focused on and limited to the TTA. The information obtained from this Dem/Val was used to assess the suitability of EK for full-scale operation at this and other sites.

### 3.3.1 Data Requirements

The suitability of the EK technology for full-scale implementation was assessed by measuring the electrical input (voltage/current) to achieve and maintain the desired electric field, by measuring operational parameters for maintaining consistent operation, and by determining the overall energy consumption within the TTA.

### 3.3.2 Success Criteria

This objective is considered achieved if system operational conditions are within $\pm 50 \%$ of the designed target voltage and current. Additionally, successful accomplishment of this objective includes amendment supply up-time to be greater than $75 \%$ of target and the energy consumption to be within $\pm 30 \%$ of the design estimate.

### 3.3.3 Performance Objective Assessment

The EK system was designed and operated at a constant current, determined after the start-up period, during the Dem/Val. As discussed in Section 7.1 (criterion related to electrical gradient) and presented in Figure 6-1, the operating voltage and current remained relatively steady except when electrodes were in need of replacement. There were three occasions when different electrodes needed to be replaced: late October/early November 2015 and late January/early February 2016 during Stage 1 operation; and December 2016 during Stage 2 operation. Prior to electrode replacement, the system voltage readings would indicate the operating conditions were becoming unsteady.

As discussed in Section 6.1, excluding the temporary unstable readings during the three periods shortly before the electrode replacement, the overall system operation conditions were steady and within $50 \%$ of the average during each normal operation period. The Dem/Val has met this criterion.

Other than the scheduled major O\&M events between the two stages of operation, there were only three occasions when the system was shut down to allow replacement of electrodes. Overall, the system up-time was well $>75 \%$ during the Dem/Val. The Dem/Val has met this criterion.

Figure 6-1 presents cumulative energy consumption during each stage of operation. Given that the energy consumption is a function of voltage and current and as discussed above regarding the steady system operation condition criterion, excluding the temporary unstable voltage conditions during the three short periods before the electrode replacement, the overall system operations were steady within $\pm 30 \%$ and, thus, the energy usage as well. The Dem/Val has met the energy consumption criterion.

### 3.4 QUALITATIVE PERFORMANCE OBJECTIVES: DEMONSTRATE SAFETY, RELIABILITY, EASE OF IMPLEMENTATION

In addition to quantitative objectives discussed above, qualitative objectives are also identified for this Dem/Val and include demonstrations of the safety, reliability, and ease of technology implementation.

### 3.4.1 Data Requirements

The suitability of the EK technology for full-scale implementation should include the considerations of safety and reliability of technology implementation. Operation records, including system operation monitoring records and field operators' notes, are the primary data for assessing the safety and reliability. For ease of implementation criterion, field operation logs and records documented the utilization of field technician efforts for system operation and maintenance.

### 3.4.2 Success Criteria

This objective will be considered achieved if operational conditions remain stable over the course of the demonstration period and no lost-time incidents occur. The ease of technology implementation will be demonstrated if a single field technician is able to effectively monitor and maintain normal system operation.

### 3.4.3 Performance Objective Assessment

As discussed in Sections 7.1 and 7.3 above, the overall operation conditions remained relatively steady over the course of system operation. The Dem/Val has met this criterion. There were no safety-related lost-time incidents. The Dem/Val has met the safety criterion.

The Dem/Val involved only conventional field construction techniques, including well drilling, well installation, and trenching and piping, as well as remediation system assembly performed by regular, qualified subcontractors. The Dem/Val has met this criterion.

During the operation, one field technician performed routine system O\&M tasks twice per week with approximately 2 to 3 hours per visit. During the routine O\&M visit, the tasks primarily included system visual inspections, recording the system operational parameters (voltage, current, amendment flow and pressure), and replenishing amendment solutions as needed. Other than sampling groundwater, there were fewer than 5 scheduled O\&M events that involved two field technicians. The Dem/Val has met this criterion.

### 4.0 SITE DESCRIPTION

The target area for this Dem/Val is located within Operable Unit 3 (OU3) at Naval Air Station (NAS) Jacksonville in Duval County, Florida (Figures 4-1 and 4-2). The Site Selection Memorandum was accepted by ESTCP on 27 November 2013. This section provides a summary of site information most relevant to this technology Dem/Val.

### 4.1 SITE LOCATION AND HISTORY

The EK-BIO Dem/Val was conducted at NAS Jacksonville, which is located on the west bank of the St. Johns River in Duval County, Florida (Figure 4-1). The Dem/Val area is in OU3 in the vicinity of former Building 106, where the station's dry-cleaning facility once existed (Figure 42). The results of previous site characterizations in OU3 indicate that a PCE source zone exists in this area above and partially into a clay unit underneath the shallow sand unit.

NAS Jacksonville was commissioned in October 1940 to provide facilities for pilot training and a Navy Aviation Trades School for ground crewmen. The buildings in OU3 are industrial, consisting of administrative space, workshops, storage, and aircraft hangars. The majority of the buildings were constructed in the 1940s with several additions and re-fabrications taking place since then. Over 90 percent of OU3 is covered with buildings and thick (greater than 1 foot) concrete pavement.

The contamination within OU3 that is the focus of this Dem/Val is associated with PSC 48, the former station's dry-cleaning facility located in former Building 106. PSC 48 encompasses the footprint and immediate surrounding area of former Building 106. PCE was released at former Building 106 through occasional spills and leaks, resulting in contamination of the shallow aquifer. PCE and its dechlorination daughter products, including TCE, cDCE, and VC, have been detected in this area in permeable sand layers within the shallow aquifer ( 5 to 16.5 ft bgs ). Moreover, site characterization results also indicate that CVOC mass present in the low-K clay layer beneath the shallow sand aquifer can serve as a long-term source of contamination to the shallow aquifer (EISB Workplan, Geosyntec, 2013). This low-K clay layer beneath the shallow sand aquifer is the target for this EK technology Dem/Val.

### 4.2 SITE GEOLOGY/HYDROGEOLOGY

Site geology was characterized as part of a previous ESTCP Project (ER-0705), as described in the Data Analysis Report for Field Event 4: NAS Jacksonville (ESTCP, 2012b). Lithology at OU3 consists of inter-bedded layers of sand, clayey sand, sandy clay, and clay. Soil cores collected and logged at OU3 (ESTCP, 2012a) indicate that the site lithology generally consists of:

- 0.5 to 5
- 5 to 7.5
- 7.5 to 16.5
- 16.5 to 18.5
- 18.5 to 25
- 25 to 30
ft bgs:
ft bgs:
ft bgs:
ft bgs:
ft bgs:
ft bgs:

Fine sand with gravel and silt/clay;
Clay with trace sand and organic matter;
Fine sand/silt to fine sand with silt/clay;
Clay/silt with trace fine sand;
Clay with trace sand; and
Fine sand with silt/clay to fine sand.


Figure 4-1. Site Location


Figure 4-2. Target Dem/Val Area

A transition layer between the shallow sand and clay layers has been observed in some soil cores, generally between 13 and 16.5 ft bgs. A soil core, OU3-4 (location shown in Figure 4-2), exhibiting the lithology representative of the target area is presented below in Figure 4-3. The same lithology was again observed during this Dem/Val with a representative soil core collected from within the TTA during monitoring well installation (EKMW-02) also presented in Figure 43. The EK-BIO Dem/Val specifically targeted the CVOCs (predominately PCE) in the clay layer between approximately 16.5 to 24 ft bgs underneath the shallow sand unit in this area.


Figure 4-3. Lithology of the Target Dem/Val Area
(OU3-4 from ESTCP ER-201032; EKMW-02 from this Dem/Val)
Prior to the Dem/Val, depth to groundwater measurements local to the test area were collected in August 2009, January 2011, June 2011, and September 2011. Groundwater in this area was first encountered approximately 5 ft bgs, and flows towards the east with gradients ranging from 0.005 to 0.02 (ESTCP, 2012b). Past hydraulic testing estimated the mid-range hydraulic conductivity of the shallow sand aquifer at $5 \times 10^{-3} \mathrm{~cm} / \mathrm{s}$ (ESTCP, 2012b). The linear groundwater velocity was estimated as high as $101 \mathrm{ft} /$ year (using a gradient of 0.005 and the mid-range conductivity).

ESTCP Project ER-0705 conducted depth-discrete, aquifer specific-capacity tests at various locations in this area, including along a transect from ASU-2 through ASU-7 shown in Figure 42. Depth-discrete hydraulic conductivity estimates for the clay unit beneath the shallow sand aquifer showed that at approximately 17 ft bgs the average K was $4 \times 10^{-5} \mathrm{~cm} / \mathrm{sec}$ (September 2011 data); however, there was not enough water at 6 of the 7 locations tested at the depth of 22 ft bgs to provide steady-state flow rates needed for the specific-capacity testing. Based on the soil core lithology observation and the orders of magnitude decrease of K from the shallow sand ( $5 \times 10^{-3}$ $\mathrm{cm} / \mathrm{s})$ to the clay at a depth of $17 \mathrm{ft}\left(4 \times 10^{-5} \mathrm{~cm} / \mathrm{sec}\right)$, it is believed that the clay material below 17 ft bgs has a hydraulic conductivity lower than $10^{-5} \mathrm{~cm} / \mathrm{sec}$.

### 4.3 CONTAMINANT DISTRIBUTION

Site investigations prior to the Dem/Val showed that PCE and degradation daughter products (TCE, cDCE, and VC) were present in permeable sand layers within the shallow aquifer ( 5 to 16.5 ft bgs). Chlorinated ethenes have also migrated, in part through molecular diffusion, into the clay layer (generally from 16.5 to 24 ft bgs ) present beneath the shallow sandy aquifer. PCE is the dominant groundwater CVOC in this area, with TCE, cDCE and VC detected at lower concentrations. The groundwater quality data collected in January 2013 before this Dem/Val (Tetra Tech, 2013) indicate that groundwater monitoring wells screened in the shallow aquifer within the target area have total chlorinated ethene concentrations ranging from $194 \mu \mathrm{~g} / \mathrm{L}$ in well PZ-04 to $51,000 \mu \mathrm{~g} / \mathrm{L}$ in well PZ-02 (Figure 4-4).


Figure 4-4. Total Chlorinated Ethenes in Select Groundwater Monitoring Wells in Shallow Sand Aquifer
(January 2013; concentration unit: $\mu \mathrm{g} / \mathrm{L}$ )

Previous SERDP/ESTCP projects have profiled the distribution of CVOCs across both the sand and clay units in the target Dem/Val area (Figures 4-5 and 4-6). Figure 4-5 presents the distribution of CVOCs in groundwater along a north-south cross section just to the east (downgradient) of the target Dem/Val area (transect along ASU2 through ASU7 shown in Figure 4-2).


Figure 4-5. Profile of Groundwater CVOC Distribution

As shown in Figures 4-2 and 4-5, previous sampling location OU3-3 is located within the target Dem/Val footprint. Figure 4-6 presents a conceptualized geologic cross section derived from highresolution coring conducted at OU3-3 (ESTCP project ER-201032). At OU3-3, the vertical distribution of PCE, TCE, and cDCE in soil and groundwater at depths above, within, and below the clay unit depicts a classic PCE diffusion profile, with PCE penetration into approximately the upper 5 feet of the clay unit. Porewater PCE concentrations detected at OU3-3 at various depths across the clay unit ranged from 15,000 to $40,000 \mu \mathrm{~g} / \mathrm{L}$, indicating significant contamination within the depth interval targeted by the Dem/Val ( $\sim 16.5$ to 24 ft bgs ).


Figure 4-6. Profiles of Soil and Groundwater CVOC Concentrations at OU3-3
(Source: ESTCP Project ER-201032)

Based on the site characterization results discussed above, the CVOCs residing in the clay unit in the proximity of OU3-3 represent a long-term continuing source for groundwater CVOC contamination in this area. Previous efforts to obtain water samples from the clay unit using conventional approaches were reported to be difficult, highlighting the expected limitations that would be encountered in an attempt to hydraulically migrate remediation amendments into this clay unit. Therefore, the Dem/Val footprint (as shown in Figure 4-2) and the target depth interval of 16.5 ft bgs to 24 ft bgs are deemed appropriate for this Dem/Val. Subsequent characterization data collected during the Dem/Val baseline characterization are presented in Section 5.3.

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### 5.0 TEST DESIGN

This section provides the details pertaining to the design, installation, and implementation of the EK-BIO technology in the target Dem/Val area.

### 5.1 CONCEPTUAL EXPERIMENTAL DESIGN

As presented in Figure 5-1, the overall EK system consists of nine (9) electrode wells [E1 through E9] and eight (8) supply wells [S1 through S8] located within a TTA measuring approximately 40 feet by 40 feet. Also presented in Figure 5-1, are seven (7) monitoring wells [EKMW1 through EKMW-7] located within the TTA and four (4) located outside the TTA.

The remediation amendments distributed by the EK system included electron donor (lactate provided as potassium lactate), pH control reagents (potassium carbonate), and a dechlorinating microbial consortium (KB- $1^{\circledR}$ ) containing Dhc. The power supply unit, amendment supply units and manifolds, and system operation monitoring and control unit were housed in a shed located adjacent to an existing utility building approximately 35 feet south of the TTA. Amendment conveyance tubing and electrical wiring conduit were installed along a trenched corridor to connect the EK control/amendment supply system to the well network in the TTA.

Table 5-1 presents a summary of major project milestones for this Dem/Val. To support the Dem/Val design, a bench-scale EK column test was conducted. The bench test and test results are discussed in Section 5.2. A baseline characterization event was conducted prior to the system construction and installation. Baseline characterization results are presented in Section 5.3. After the completion of system construction/installation and system startup, the overall Dem/Val involved two separate stages of EK operations. Each stage was operated with varying anode and cathode configurations to alter the primary direction of electric fields. Figures 5-2 and 5-3 present conceptual orientations of the electric field established during each EK operational stage. Bioaugmentation of the TTA with reductive dechlorination culture (KB-1 ${ }^{\circledR}$ ) was conducted during Stage 1 operation. There was an incubation period of approximately 6 months between the two stages of active operation. Following the completion of the second EK operation stage in March 2017 and a subsequent incubation period of 3 months, a post-EK performance monitoring event was conducted in June 2017 to complete the Dem/Val.

During each stage of operation, the EK system was operated to achieve and maintain a constant current supplied to the overall electrode network. The voltage that was required to achieve and sustain this constant current is a site-specific characteristic related to the electrical resistance of the subsurface materials.


Figure 5-1. Well Network for Dem/Val

Table 5-1. Major Project Milestones

| Well Installation | September 2014 |
| :--- | :--- |
| Baseline Characterization | October 2014 |
| System Fabrication / Field Construction / System Installation <br> \& Shakedown | October 2014 - June 2015 |
| System Startup \& Initial Field Conditioning | June - August 2015 |
| Stage 1 Operation Period | August 2015 - Mach 2016 |
| Bioaugmentation (Supply Wells and Electrode Wells) | October 29, 2015 |
| End-of-Stage 1 Monitoring Event | March 2016 |
| Post-Stage 1 Incubation Period | March - September 2016 |
| Stage 2 Operation Period | October 2016 - March 2017 |
| End-of-Stage 2 Monitoring Event | March 2017 |
| Post-Stage 2 Incubation Period | March - June 2017 |
| Final Sampling Event | June 2017 |



Figure 5-2. $\quad$ Stage 1 Conceptual Electric Field


Figure 5-3. $\quad$ Stage 2 Conceptual Electric Field
Potassium lactate was used to provide electron donor for ERD of CVOCs. Lactate was supplied to all electrode wells and all supply wells during the system operation. In addition to lactate, potassium carbonate $\left(\mathrm{K}_{2} \mathrm{CO}_{3}\right)$ was added to all supply wells during EK operation as a pH buffer due to the low baseline $\mathrm{pH}(<6)$ in the TTA (which is not optimal for ERD). The EK system would also cross-circulate electrolytes (fluids in electrode wells) between cathodes and anodes, as well as provide supplemental acid or base, as needed, to individual electrode wells for overall pH control. The following sections provide specific details of individual phases completed under this Dem/Val.

### 5.2 TREATABILITY OR LABORATORY STUDY RESULTS

Preliminary characterization of the aquifer materials from the target Dem/Val area was performed to support design of the EK system. The descriptions of testing are provided in Appendix B. Approximately 24 feet of soil core was obtained from the vicinity of the target area with direct push approaches. Mineralogical analysis of the core through X-Ray Diffraction (XRD) indicated that the clay is predominantly kaolinite (61\%), with smaller amounts of illite (1.4\%), chlorite (11.9\%), and smectite (15.3\%). These fractions are within the range of soils encountered at other EK field sites.

Zeta potential measurements were conducted on samples from the soil cores by the University of Toronto. Zeta potential is a soil characteristic affecting electroosmosis of bulk water through soil pores under an applied electric potential. Two sets of testing were performed at various pH values. A flat zeta potential curve was measured, with values of approximately -25 mV above a pH of 4.5 , suggesting that the EK system design should target pH control in electrode wells to levels above pH 5 to maintain operational efficiency. The zeta potential of the site soil is similar to that of the materials from sites previously tested for other EK projects.

A bench-scale EK column test was also conducted using the core material from the site to estimate the migration rate of amendments. Three $10-\mathrm{cm}$ sections of the core materials were individually compacted using a piston into a $10-\mathrm{cm}$ PVC column (3-inch diameter). A filter assembly was used at each end of the PVC column to connect the soil column to the electrode cells. A conservative bromide tracer ( $1 \mathrm{~g} / \mathrm{L}$ of sodium bromide solution) was added to the cathode cell reservoir. Sodium phosphate solution ( $1.3 \mathrm{~g} / \mathrm{L}$ ) was added to both cathode and anode cells as electrolyte and buffer. The electrodes were connected to a dc power supply unit. A constant current of 25 mA was applied during the EK column test. The voltage needed to sustain this target current varied from the initial reading of 69.8 V after 29 hours to a lower reading of 54.3 V after 72 hours indicating the core material in the column became more electrically conductive.

At the completion of 72 hours of testing, the column was detached from the electrode cells and frozen. The frozen core was subsequently cut into a total of eight 1-cm sections along the direction from anode toward cathode. These samples, plus a background soil sample, were analyzed for bromide concentrations. The results presented in Table 5-2 show that bromide migrated across the entire length of the $10-\mathrm{cm}$ column from the cathode to the anode within 72 hours. These results suggest a minimum electromigration rate of $3.3 \mathrm{~cm} /$ day .

Table 5-2. Bromide Tracer Test Results

| Sample | Background <br> Soil | 3-cm from <br> cathode | 5-cm from <br> cathode | 7-cm from <br> cathode | 10-cm from <br> cathode |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Bromide <br> $(\mathrm{mg} / \mathrm{kg})$ | $<1$ | 295 | 158 | 157 | 284 |

### 5.3 BASELINE CHARACTERIZATION

As discussed in Section 4, several previous SERDP/ESTCP projects (ER-0705, ER-1740, and ER201032) have characterized the geology, hydrogeology, and contaminant distribution in the area that encompasses the target Dem/Val area. To establish the baseline geochemical conditions, microbial conditions, and contaminant distribution specifically within the Dem/Val footprint, a baseline characterization event was performed in October 2014 following the completion of well installation. Table 5-3 presents a summary of the overall monitoring program for the Dem/Val, including the baseline characterization discussed in this section. Specific activities and details for the monitoring activities performed during system operation are discussed in Section 5.5.

### 5.3.1 Baseline Groundwater Sampling

Groundwater samples were collected from the 11 groundwater monitoring wells (EKMW-01 through EKMW-11; seven within and four outside the TTA) shown on Figure 5-1. Baseline geochemical characterization of groundwater included measurements of field parameters (dissolved oxygen [DO], oxidation-reduction potential [ORP], conductivity, and temperature) and laboratory analyses for metals, inorganic anions (chloride, sulfate and nitrate), CVOCs, total organic carbon (TOC), volatile fatty acids (VFAs), and dissolved hydrocarbon gases (DHGs: methane, ethene and ethane). Baseline measurement of various carbon indicators, such as TOC and VFAs, allowed the subsequent tracking of electron donor distribution.

Baseline groundwater microbial characterization included quantitative analysis of Dhc and Dehalobacter (Dhb), as well as the key biomarker, vcrA. These microbial characterization data were collected to establish the baseline conditions regarding the specific microbiological capacity within the Dem/Val footprint.

Field sampling and laboratory analyses were performed in accordance with the sampling and analysis methods presented in Section 5.6. Field sampling forms are provided in Appendix D. The baseline groundwater sampling results of select key parameters are summarized in Table 54a and presented in Figure 5-4a and 5-4b. Baseline data indicated that groundwater within the TTA was generally acidic and slightly oxidizing with low DO between 0.2 to $0.6 \mathrm{mg} / \mathrm{L}$. Baseline TOC and VFAs were relatively low (mostly below $6 \mathrm{mg} / \mathrm{L}$ ), and, with the exceptions of EKMW01 and EKMW-05, there was no detectable levels of Dhc, Dhb, and vcrA. Additional detailed discussions of groundwater baseline characterization results are presented in Section 6.3.

Table 5-3. Summary of Monitoring Program

| Phase | Matrix | Frequency | Analyses | Location |
| :---: | :---: | :---: | :---: | :---: |
| Baseline Characterization | Soil | Three depths ${ }^{(1)}$ per boring | VOCs ${ }^{(2)}$, Metals ${ }^{(3)}$, Microbial (Dhc, Dhb \& $v c r A$ ), Grain-size | 9 locations within the target treatment area (TTA) and 2 locations outside the TTA |
|  | Groundwater | One Time | VOCs, DHGs ${ }^{(4)}$, VFAs $^{(5)}$, <br> Metals, Anions ${ }^{(6)}$, TOC, Field Geochemistry ${ }^{(7)}$, Microbial (Dhc, Dhb \& $v c r A$ ) | All 11 monitoring wells (EKMW-01 through EKMW-11) |
| System Start-up Phase | Groundwater | Weekly | Field Geochemistry, Electric Field ${ }^{(8)}$ | 7 Monitoring wells within TTA |
| Stage 1 Operations | Groundwater | Weekly | Electric Field | 6 Monitoring wells within the TTA (EKMW-01 through EKMW-07 except EKMW-06) |
|  |  | Monthly | TOC, VFAs |  |
| End of Stage 1 Operation \& End of Incubation Period between Stage 1 and Stage 2 Operations | Soil | Two depths ${ }^{(1)}$ per boring | VOCs, Microbial (Dhc, Dhb \& $v c r A$ ) | 9 select locations within the TTA and 1 location outside the TTA |
|  | Groundwater | One Time | VOCs, DHGs, VFAs, Metals, Anions, TOC, Field Geochemistry, Microbial (Dhc, Dhb \& vcrA) | All 10 monitoring wells (EKMW-01 through EKMW-11 except EKMW-06) |
| Stage 2 Operations | Groundwater | Weekly | Electric Field | 6 Monitoring wells within TTA (EKMW-01 through EKMW-07 except EKMW-06) |
|  |  | Monthly | TOC, VFAs |  |
| Post-Operation Final Monitoring (3 months) | Soil | End of 3-month post-operation incubation period; Two depths ${ }^{(1)}$ per boring | VOCs, Microbial (Dhc, Dhb \& vcrA); <br> and <br> Metals | 9 locations within TTA and 1 location outside TTA |
|  | Groundwater | End of 3-month post-operation incubation period | Field Geochemistry; TOC, VOCs, DHGs Metals, Microbial (Dhc, Dhb \& $v c r A$ ) | All 10 monitoring wells, including 6 Monitoring wells in TTA |

(1) Baseline event: discrete soil samples collected from approximately 18.5, 21, and 23 ft bgs. Subsequent events: two sampling depths per location at 18.5 and 21 ft bgs.
(2) VOCs: PCE, TCE, cDCE, and VC.
(3) Iron, Manganese, Calcium, and Magnesium.
(4) Methane, Ethene, and Ethane.
(5) Lactate, Acetate, Propionate, Formate, Butyrate, and Pyruvate.
(6) Nitrate, Sulfate, and Chloride.
(7) Conductivity, Temperature, Redox, pH , and Dissolved Oxygen.
(8) Voltage measurements taken at select wells. Readings of electric currents to individual electrodes recorded at wellhead using portable current clamp.

Table 5-4a. Analytical Results in Groundwater-baseline Sampling Event OU3, NAS Jacksonville

| Analyte | Units | EKMW-01 | EKMW-02 | EKMW-03 | EKMW-04 | EKMW-05 | EKMW-06 | EKMW-07 | EKMW-08 | EKMW-09 | EKMW-10 | EKMW-11 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Volatile Organic Compounds |  |  |  |  |  |  |  |  |  |  |  |  |
| 1,1-DCE | $\mu \mathrm{g} / \mathrm{L}$ | 25 U | 4 I | 2 I | 1 I | 5 U | 1 I | 2 U | 2 U | 25 U | 2 | 0.2 U |
| cis-1,2-DCE | $\mu \mathrm{g} / \mathrm{L}$ | 1,190 | 950 | 760 | 380 | 773 | 120 | 970 | 90 | 288 | 260 | 10 |
| PCE | $\mu \mathrm{g} / \mathrm{L}$ | 7,640 | 170 | 190 | 250 | 1,800 | 640 | 1,300 | 1,600 | 5,220 | 120 | 160 |
| trans-1,2-DCE | $\mu \mathrm{g} / \mathrm{L}$ | 323 | 11 | 2 I | 4 | 81 | 21 | 44 | 4 I | 50 | 3 | 0.2 U |
| TCE | $\mu \mathrm{g} / \mathrm{L}$ | 1,670 | 150 | 150 | 130 | 344 | 130 | 260 | 77 | 482 | 170 | 8 |
| VC | $\mu \mathrm{g} / \mathrm{L}$ | 33 U | 6 I | 1 U | 3 | 7 U | 9 | 89 | 2 U | 33 U | 5 | 0.4 I |
| Dissolved Hydrocarbon Gases |  |  |  |  |  |  |  |  |  |  |  |  |
| Methane | $\mu \mathrm{g} / \mathrm{L}$ | 190 | 1200 | 330 | 54 | 270 | 29 | 110 | 110 | 120 | 1300 | 10 U |
| Ethene | $\mu \mathrm{g} / \mathrm{L}$ | 15 | 10 U | 10 U | 10 U | 73 | 10 U | 11 | 10 U | 10 U | 10 U | 10 U |
| Ethane | $\mu \mathrm{g} / \mathrm{L}$ | 10 U | 10 U | 10 U | 10 U | 10 U | 10 U | 10 U | 10 U | 10 U | 10 U | 10 U |
| Microbial |  |  |  |  |  |  |  |  |  |  |  |  |
| Dhc | cell/L | $8.0 \mathrm{E}+05$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+05$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $4.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $4.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $4.0 \mathrm{E}+03 \mathrm{U}$ |
| Dhb | cell/L | $3.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $4.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $4.0 \mathrm{E}+03 \mathrm{U}$ | $3.0 \mathrm{E}+03 \mathrm{U}$ | $4.0 \mathrm{E}+03 \mathrm{U}$ |
| vcrA | gene copy/L | $3.0 \mathrm{E}+03$ | -- | -- | -- | $4.0 \mathrm{E}+05$ | -- | -- | -- | -- | -- | -- |
| Volatile Fatt Acids |  |  |  |  |  |  |  |  |  |  |  |  |
| Lactate | $\mathrm{mg} / \mathrm{L}$ | 0.96 | 0.39 U | 0.52 | 0.39 U | 0.39 U | 0.41 | 0.39 U | 0.39 U | 0.39 U | 0.46 | 0.55 |
| Acetate | $\mathrm{mg} / \mathrm{L}$ | 2.3 | 1.6 | 0.54 U | 1.9 | 1.8 | 4.6 | 2.2 | 3.1 | 2.3 | 1.3 | 0.81 |
| Propionate | $\mathrm{mg} / \mathrm{L}$ | 0.31 U | 0.31 U | 0.74 | 0.31 U | 0.31 U | 0.31 U | 0.31 U | 0.31 U | 0.31 U | 0.31 U | 0.31 U |
| Formate | $\mathrm{mg} / \mathrm{L}$ | 0.22 U | 0.22 U | 0.22 U | 0.22 U | 0.22 U | 1 | 0.22 U | 0.22 U | 0.22 U | 0.32 | 0.22 U |
| Butyrate | $\mathrm{mg} / \mathrm{L}$ | 0.41 U | 0.41 U | 0.41 U | 0.41 U | 0.41 U | 0.41 U | 0.41 U | 0.41 U | 0.41 U | 0.41 U | 0.41 U |
| Pyruvate | $\mathrm{mg} / \mathrm{L}$ | 0.69 U | 0.69 U | 0.69 U | 0.69 U | 0.69 U | 0.69 U | 0.69 U | 0.69 U | 0.69 U | 0.69 U | 0.69 U |
| Total VFAs | $\mathrm{mg} / \mathrm{L}$ | 3.26 | 1.6 | 1.26 | 1.9 | 1.8 | 6.01 | 2.2 | 3.1 | 2.3 | 2.08 | 1.36 |
| Other Organics and Inorganics |  |  |  |  |  |  |  |  |  |  |  |  |
| TOC | mg/L | 2.5 | 2.5 | 2.5 | 3.6 | 1.7 | 1.4 | 6.8 | 2.3 | 1.6 | 1.9 | 3.1 |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 3400 | 550 | 520 | 570 | 1900 | 1700 | 790 | 1000 | 2800 | 570 | 170 |
| Nitrate (as Nitrogen) | $\mathrm{mg} / \mathrm{L}$ | 0.17 U | 0.17 U | 0.17 U | 0.17 U | 0.17 U | 0.05 U | 0.17 U | 0.17 U | 0.17 U | 0.25 U | 0.17 U |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 57 | 27 | 24 I | 45 | 50 | 23 | 140 | 38 | 36 | 21 I | 16 I |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 350 | 100 | 89 | 120 | 400 | 400 | 150 | 150 | 460 | 140 | 130 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 130 | 57 | 58 | 47 | 160 | 61 | 23 | 67 | 130 | 49 | 2.9 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 98 | 30 | 27 | 31 | 110 | 100 | 21 | 45 | 130 | 42 | 0.74 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 2.8 | 0.86 | 0.79 | 0.99 | 3.3 | 3.1 | 0.48 | 1.1 | 4.1 | 1.2 | 0.015 |
| Field Parameters |  |  |  |  |  |  |  |  |  |  |  |  |
| pH | unit | 4.7 | 5.8 | 5.8 | 4.9 | 5.2 | 5.1 | 5.1 | 5.7 | 5.0 | 6.0 | 10.6 |
| ORP | mV | 54 | -21 | -21 | 42 | 64 | 81 | 34 | 12 | 100 | -27 | -9 |
| DO | $\mathrm{mg} / \mathrm{L}$ | 0.6 | 0.2 | 0.2 | 0.2 | 0.3 | 0.9 | 0.5 | 0.4 | 1.2 | 0.6 | 0.1 |

otes:
CE - Tetrachloroethene
CE - Trichloroethene
,1-1
is-1,2-DCE - cis-1,2-Dichloroethene
rans-1,2-DCE - trans-1,2-Dichloroethene
V - Vinyl Chloride
Dhb - dehalobacter
VFA - volatile fatty acid
TOC - Total organic carbon
ORP - oxidation reduction potential
DO - dissolved oxygen
$\mu \mathrm{g} / \mathrm{L}$ - microgram per lite

- liter
mg/L - milligram per liter
mV - millivolt
crA - vinyl chloride reductase
U - The compound was analyzed for but not detected
I - The reported value is between the laboratory method detection limit and the laboratory practical quantitation limit
(a) gene copy per liter is generally equivalent to cell per liter

Table 5-4b. Analytical Results in Soil - Baseline Sampling Event OU3, NAS Jacksonville

| Soil Boring | Sample <br> Depth <br> (ft bgs) | Volatile Organic Compounds (mg/kg) |  |  |  | Inorganics |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | PCE | TCE | cis-1,2-DCE | vC | Calcium | Iron | Magnesium | Manganese |
| Cl | 18.5 | 16 | 0.42 | 0.38 I | 0.032 | 2500 | 20000 | 3400 | 60 |
|  | 21 | 0.029 | 0.032 | 0.006 | 0.0013 U | -- | -- | - | - |
|  | 23 | 0.04 | 0.061 | 0.0077 | 0.0014 U | 2200 | 17000 | 2700 | 54 |
| C2 | 18.5 | 15 | 0.27 I | 0.16 | 0.012 | 1200 | 8000 | 1600 | 27 |
|  | 21 | 0.028 | 0.017 | 0.006 | 0.0011 U | -- | -- | - | - |
|  | 23 | 0.082 | 0.067 | 0.0083 | 0.0014 U | 2400 | 16000 | 3100 | 62 |
| C3 | 18.5 | 6.9 | 0.42 | 1.9 | 0.077 U | 1200 | 8100 | 1600 | 26 |
|  | 21 | 0.084 U | 0.07 U | 0.099 I | 0.084 U | -- | -- | - | - |
|  | 23 | 0.084 U | 0.07 U | 0.097 U | 0.084 U | 2200 | 13000 | 2800 | 49 |
| C4 | 18.5 | 4.7 | 0.17 | 0.14 | 0.023 | 2400 | 18000 | 3300 | 56 |
|  | 21 | 0.081 | 0.018 | 0.0082 | 0.0015 U | -- | -- | -- | - |
|  | 23 | 0.01 | 0.04 | 0.014 | 0.0014 U | 2700 | 21000 | 3600 | 71 |
| C5 | 18.5 | 12 | 0.14 I | 0.12 I | 0.083 U | 2200 | 15000 | 2800 | 47 |
|  | 21 | 0.022 | 0.007 | 0.0046 I | 0.00057 U | -- | -- | - | - |
|  | 23 | 0.047 | 0.043 | 0.0067 I | 0.0011 U | 2300 | 15000 | 2800 | 57 |
| C6 | 18.5 | 10 | 0.27 I | 0.16 | 0.027 | 3100 | 29000 | 4500 | 84 |
|  | 21 | 5.5 | 0.18 | 0.12 | 0.017 | -- | -- | -- | - |
|  | 23 | 3.1 | 0.18 | 0.11 | 0.016 | 2700 | 20000 | 3300 | 70 |
| C7 | 18.5 | 0.08 U | 0.067 U | 3.3 | 0.08 U | 2200 | 20000 | 3200 | 58 |
|  | 21 | 0.027 | 0.0025 I | 0.11 | 0.00052 U | -- | -- | - | - |
|  | 23 | 0.011 | 0.011 | 0.011 | 0.00056 U | 2800 | 19000 | 3800 | 71 |
| C8 | 18.5 | 7.6 | 0.12 | 0.86 | 0.2 | 2900 | 27000 | 4100 | 75 |
|  | 21 | 0.025 | 0.024 | 0.0058 | 0.0045 | -- | -- | - | - |
|  | 23 | 0.021 | 0.062 | 0.0062 | 0.0011 U | 2100 | 16000 | 2600 | 51 |
| C9 | 18.5 | 14 | 0.3 I | 0.22 I | 0.037 | 1800 | 13000 | 2200 | 42 |
|  | 21 | 0.035 | 0.0096 | 0.0018 I | 0.0015 U | -- | -- | -- | - |
|  | 23 | 0.0013 U | 0.03 | 0.0066 | 0.0012 U | 2400 | 17000 | 2900 | 61 |
| $\mathrm{C} 10^{(\mathrm{a})}$ | 18.5 | 45 | 0.1 | 0.031 | 0.00052 U | 1500 | 12000 | 2000 | 38 |
|  | 21 | 11 | 0.015 | 0.004 I | 0.00055 U | -- | -- | - | - |
|  | 23 | 2.6 | 0.0076 | 0.0016 I | 0.0005 U | 2500 | 18000 | 3200 | 34 |
| $\mathrm{Cl1}{ }^{(2)}$ | 18.5 | 4.9 | 0.024 | 0.0082 | 0.0015 I | 2700 | 19000 | 2900 | 69 |
|  | 21 | 0.034 | 0.0014 U | 0.0014 U | 0.0017 U | -- | -- | -- | -- |
|  | 23 | 0.097 U | 0.081 U | 0.11 U | 0.097 U | 4100 | 24000 | 4400 | 260 |

Notes:
PCE - Tetrachloroethene
TCE - Trichloroethene
cis-1,2-DCE - cis-1,2-Dichloroethene
VC - Vinyl Chloride
Dhc - dehalococcoides
$\mathrm{mg} / \mathrm{kg}$ - milligram per kilogram
mg - The - milligram per kilogram
U - The compound was analyzed for but not detected
I - The reported v
(a) Sampling locations C10 and C11 are outside the target treatment area.


Figure 5-4. Baseline Characterization

### 5.3.2 Baseline Soil Sampling

Soil cores were collected from nine (9) locations within the TTA and two (2) locations outside the TTA (Figure 5-4c). At each location, a soil core was collected using Direct Push Technology (DPT) to a target depth of 24 feet. With each collected soil core, three (3) discrete soil samples were collected from approximately 18.5, 21, and 23 ft bgs.

Baseline soil characterization included laboratory analyses for metals and CVOCs, as well as quantitative analyses of $D h c$, $D h b$, and $v c r A$. In addition, the baseline soil characterization included soil grain size analysis.

Field sampling and laboratory analyses were performed in accordance with the sampling and analysis methods presented in Section 5.6. Field sampling forms and chain of custody forms are provided in Appendices D \& E. The baseline soil sampling results of select key parameters are summarized in Table 5-4b and the soil PCE data are presented in Figure 5-4c. The baseline soil characterization data indicated that there was very little apparent reductive dechlorination activities within the TTA prior to the Dem/Val. The data also suggested that the majority of soil PCE within the TTA appeared to be present above the depth of 21 ft . Additional detailed discussions of soil baseline characterization results are presented in Section 6.2.

### 5.4 DESIGN AND LAYOUT OF TECHNOLOGY COMPONENTS

The locations of the electrode wells, supply wells, and monitoring wells are shown in Figure 5-1. System components and equipment for amendment supply and cross-circulation were housed in an equipment enclosure located adjacent to an existing utility building to the south of the TTA. Given the operational needs of NAS Jacksonville, the wellhead components and the connections between electrode/supply wells and the equipment enclosure (conveyance piping, electrical wiring, instrumentation wiring) were installed below ground. Prior to field construction and installation, a comprehensive utility locate and survey was conducted in the proposed Dem/Val area. The Dem/Val system design and well network was adjusted based on the results of these surveys. The following sections describe the specifics of individual system components.

### 5.4.1 Electrode Wells

A total of nine (9) electrode wells (E1 through E9) were installed by hollow-stem auger drilling in the treatment area. Electrode well construction details are provided in Figure 5-5. Each electrode well was constructed with 4 -inch diameter PVC casing and 0.01 -inch slotted screen. The screened interval was generally between 19 and 23 ft bgs across the clay unit (which was expected to be observed between approximately 16.5 to 25 ft bgs). A medium sand filter pack was placed around the screen from the bottom of the borehole up to the top of the screen and topped by a fine sand filter pack up to $1 / 2$ foot above the screened interval. A 2 -foot thick ( $\sim 16.5$ to 18.5 ft bgs) bentonite seal was installed above the sand pack by placing bentonite chips and hydrating for at least one hour. Grout, consisting of cement and bentonite powder, was then added to fill the remaining annulus up to the bottom of the well vault.

Figure 5-6 presents the details of the electrode well vault. Locking well vaults (traffic-rated, $2-\mathrm{ft}$ x $2-\mathrm{ft} x 2-\mathrm{ft}$ ) were installed with concrete protection around the vault and a gravel base. The electrode well casing was completed at the top with the installation of a PVC flange.


Figure 5-5. Electrode Well Details


Figure 5-6. Electrode Well Vault Details

Access ports were installed in the flange for installation of the electrode, electrical cable, tubing, and a pressure safety valve (PSV). Additional descriptions of the conveyance system and control instrumentation are provided in Sections 5.4.5 through 5.4.8.

### 5.4.2 Supply Wells

A total of eight (8) supply wells (S1 through S8) were installed by hollow-stem auger drilling in the treatment area. Supply well construction details are provided in Figure 5-7. Each supply well was constructed with 4 -inch diameter PVC casing and 0.01 -inch slotted screen. The screened interval was across the clay unit at depths between 19 and 23 ft bgs. Construction details for supply wells are the same as electrode wells. Figure 5-8 presents the details of the supply well vaults. Additional descriptions of the conveyance system and control instrumentation are provided in Sections 5.4.5 through 5.4.8.

### 5.4.3 Monitoring Wells

A total of 11 monitoring wells were installed by hollow-stem auger drilling within and around the treatment area (Figure 5-1). Monitoring wells were constructed as double-casing wells each with a 6-inch PVC surface casing installed to 18 ft bgs and grouted in place (Figure 5-9). Each 2-inch diameter monitoring well was then constructed by drilling through the bottom of grouted 6-inch casing to install 0.01 -inch slotted screen section at depths between 19 and 23 ft bgs. A medium (20/30) sand filter pack was placed around the screen from the bottom of the borehole up to $1 / 2 \mathrm{ft}$ above the top of the screened interval. A 2-foot thick bentonite seal was installed above the sand pack by placing bentonite chips and hydrating for at least one hour. Grout, consisting of cement and bentonite powder was then added to fill the remaining annulus up to the bottom of the well vault.

### 5.4.4 Power Supply and Electrodes

The power supply unit for the EK system was a Magna XR250-24/240 dc power supply unit with input power from 3-phase alternate current (AC) 240 V . This 6 kW unit has a capacity to output 0 to 250 V and 0 to 24 A . The power supply was operated in constant current mode with varying voltage automatically adjusted to the changes in soil conductivity.

During each EK operational stage, six (6) electrode wells were used as cathodes and three (3) electrode wells as anodes. The electrode arrangements for Stage 1 and Stage 2 operations are shown in Figures 5-2 and 5-3, respectively. The electrodes consisted of a titanium rod (3/4-inch diameter; 4-ft long) with mixed metal oxide (MMO) coating (TELPRO tubular anodes manufactured by Titanium Electrode Products, Inc., Stafford, TX). The coating consists of $\mathrm{IrO}_{2} / \mathrm{Ta}_{2} \mathrm{O}_{5}$ and is suitable for use in soils, carbonaceous backfill, fresh and brackish water, and seawater.

### 5.4.5 Amendment Supply System

Electron donor solution was prepared by adding $60 \%(\mathrm{w} / \mathrm{w})$ potassium lactate (WILCLEAR ${ }^{\circledR}$ ) to 250-gallon totes for transfer to supply wells and electrode wells by the amendment supply system. Buffer solution was prepared by adding potassium carbonate (anhydrous power, 99\%) to 250gallon totes for transfer to supply wells by the amendment supply system. The amendment supply was performed as short-duration pulsed injections using feed pumps controlled by timers. The duration and flow rate of each pulse injection cycle were programmed so that each injection event generally introduced less than $1 / 2$ gallon of solution to each well.


Figure 5-7. Supply Well Details




Figure 5-8. $\quad$ Supply Well Vault Details


Figure 5-9. Monitoring Well Details


NOTES:

1. SURFACE TO BE REPAIRED TO PRE-CONSTRUCTION CONDITIONS. WHERE GRASS IS REQUIRED, SEED TO BE USED.

CONDUIT TRENCH DETAILS
Geosyntec ${ }^{D}$
consultants
DATE: DECEMBER 2013 DOD PROU. NO. ESTCP ER-201325 GCI PROJN FILE NO. FIGURE NO.

Figure 5-10. Conduit Trench Details

### 5.4.6 Cross-Circulation and Electrode Well pH Control System

Electrolysis of water in electrode wells produces acid (anode) and base (cathode) resulting in pH changes in the wells. Cross-circulation of electrolytes between anodes and cathodes can balance pH to an extent and reduce the amount of supplemental pH -adjusting reagents needed. Crosscirculation between cathode wells and anode wells was achieved by transferring electrolyte from individual cathode wells to individual anode wells and vice versa. During a given programmed cross-circulation event, the system extracted catholyte from a cathode well to a catholyte holding tank, while at the same time extracting anolyte from an anode well to an anolyte holding tank. Extraction was performed by peristaltic pumps controlled by timers. In-line monitoring stations monitored the pH of the extracted electrolytes. Following the extraction event, the system pumped the extracted electrolyte in the holding tank back to the electrode well of opposite polarity (i.e., catholyte to anode well and vice versa). Depending on the pH reading of the extracted electrolyte, supplemental lactic acid solution (for cathode well) or sodium hydroxide solution (for anode well) was added to the electrolyte injection tubing during the re-injection cycle when electrolyte was pumped from the holding tank back to an electrode well.

### 5.4.7 Process Monitoring and Controls

The EK system was constructed with instrumentation and controls to monitor and operate the system automatically using a programmable logic controller (PLC). Overall operation of the pumps for amendment supply and electrolyte cross-circulation was controlled by timers in the PLC. The PLC also controlled solenoid valves at the central manifold in the equipment shed to direct flows from and to individual wells.

In-line water quality stations installed on the electrolyte extraction lines monitored the pH of the electrolyte coming from an individual electrode well. A data acquisition system was used to record the pH monitoring data collected.

### 5.4.8 Conveyance Piping and Utilities

Dedicated conveyance piping was run between the system equipment enclosure and the well network through a combined conduit. The conduit was installed in shallow trenches as shown in a typical trench detail (Figure 5-10). Additional conduits were placed in the trenches for the installation of electrical wires to electrodes.

### 5.5 FIELD TESTING

This section provides a description of each significant phase of operation and the activities conducted during that phase. A schedule illustrating the sequence and duration of individual phases of operation is presented in Table 5-5.

Table 5-5. Dem/Val Field Testing Phases

| System Startup \& Initial Field Conditioning | June 2015 - August 2015 |
| :--- | :--- |
| Stage 1 Operation | August 2015 - Mach 2016 |
| * During Stage 1 Operation - Bioaugmentation <br> (Supply Wells and Electrode Wells) | $*$ October 29, 2015 |
| * End-of-Stage 1 | * March 2016 |
| Post-Stage 1 Incubation Period (no operation) | March 2016 - September 2016 |
| Stage 2 Operation | October 2016 - March 2017 |
| * End-of-Stage 2 | March 2017 |
| Post-Stage 2 Incubation Period (no operation) | March 2017 - June 2017 |

### 5.5.1 System Start-Up

EK system Start-Up commenced following the installation and shakedown of the system components described above in Section 5.4. During the start-up, carbonate ( $\mathrm{Na}_{2} \mathrm{CO}_{3}$ ) solution was delivered to the supply wells in order to condition the pH in the formation around the supply wells prior to the addition of electron donor in the next phase. The duration of the start-up period for buffer addition was approximately 60 days. Buffer addition continued during the subsequent two active EK operational phases (Stage 1 and Stage 2) together with lactate amendment supply.

During the start-up operation, daily remote-monitoring of PLC data and weekly system field inspections were conducted to monitor system operations. The distribution of the electric field within the TTA was confirmed by lowering an insulated reference electrode into a given monitoring well and using a hand-held voltage meter to measure the voltage difference between that location and a universal reference cathode, which in our case was the power supply unit in the system shed. The field personnel wore rubber boots and rubber gloves when performing this task. As discussed in Section 6.1, relatively uniform electric field was confirmed based on the voltage measurements taken at all monitoring wells within the TTA.

### 5.5.2 Stage 1 EK Operations and Monitoring

Following system start-up, electron donor (lactate solution) was added to the TTA during Stage 1 EK operation. This operational stage included 2 segments - before bioaugmentation and after. The electrode polarity arrangement for Stage 1 operation is shown in Figure 5-2 with E2, E5, and E8 as anodes.

Lactate solution was supplied to all electrode wells and all supply wells as individual short pulses several times a day. Other system operation activities included buffer amendment to supply wells, cross-circulation between electrodes, and supplemental acid and base addition, as needed, to electrode wells.

## Bioaugmentation

Bioaugmentation of the TTA with dechlorination microbial culture containing Dhc was performed to establish adequate reductive dechlorinating populations. After approximately 75 days of active operation when geochemistry monitoring data indicated anaerobic and reducing conditions at supply wells and monitoring wells within the TTA, the system was shut down 48 hours prior to the bioaugmentation event, which occurred on 29 October 2015. To bioaugment the TTA, 4 liters of KB- $1^{\circledR}$ culture (SiREM Laboratory, Ontario, Canada) was added to each supply well, and 1.5 liters to each electrode well. The KB- $1^{\circledR}$ culture selected for this project contain Dhc that are capable of fully degrading chlorinated ethenes under mildly acidic (i.e., $\mathrm{pH}<6.0$ ) conditions. The system operation resumed 48 hours after the bioaugmentation event.

The Stage 1 operation continued for approximately 5 months following bioaugmentation and was completed in March 2016. During the operation, system inspections were conducted generally twice a week by a field operator to monitor and record system operational conditions and perform routine maintenance, mainly related to filter cleaning/replacement and amendment stock solution replenishment. The distribution of electric field within the TTA was confirmed by measuring voltages at monitoring wells as described above. Groundwater sampling and analysis for performance monitoring was conducted in accordance with Table 5-3 and the sampling methods presented in Section 5.6.

### 5.5.3 Post-Stage 1 Incubation

Following the completion of Stage 1 operations, the system was shut down and the project entered a 6 -month post-Stage 1 incubation period. An end-of-Stage 1 monitoring event was completed in March 2016 immediately following the system shut down. An end-of-post Stage 1 incubation monitoring event was completed in September 2016. Sampling and analysis for these monitoring events were performed in accordance with Table 5-3 and the methods presented in Section 5.6.

### 5.5.4 Stage 2 EK Operations and Monitoring

After the 6-month post-Stage 1 incubation, the electrode polarity arrangement was adjusted to start Stage 2 operation (Figure 5-3) with E4, E5, and E6 as anodes. The system operational program for electron donor amendment, buffer addition, cross-circulation between electrodes, and supplemental acid and base addition essentially followed the same approach as that of Stage 1 operation. There was no bioaugmentation in Stage 2 operation.

The Stage 2 operation continued for approximately 5 months from October 2016 through March 2017. During the operation period, system inspections and maintenance, as well as field measurements, were conducted following the same program and procedures as described above for the Stage 1 operation.

### 5.5.5 Post-Stage 2 Incubation

Following the completion of Stage 2 operations, the system was shut down and the project entered a 3 -month post-Stage 2 incubation period. An end-of-Stage 2 monitoring event was completed in March 2017 immediately following the system shut down. An end-of-post Stage 2 incubation monitoring event (also as the final performance monitoring event) was completed in June 2017.

Sampling and analysis for these monitoring events were performed in accordance with Table 5-3 and the methods presented in Section 5.6.

### 5.5.6 Decommissioning

NAS Jacksonville and NAVFAC are currently in the process of preparing a Feasibility Study (FS) for remediation of the OU3 area, which encompasses the Dem/Val TTA. It is anticipated that EKBIO will be retained in the FS as a technology in consideration for treatment of impacts in the clay layer outside of the Dem/Val TTA. As such, the Dem/Val infrastructure will remain in place until the FS is completed, and a decision rendered on remedy, in the event that the decision is to expand the EK-BIO remedy to the wider source zone. Should EK-BIO not proceed further, Geosyntec will then remove the surface infrastructure (i.e., EK Control Center and solution tanks) from the site, while NAS Jacksonville will complete final disposition of the wells. Details will be provided in a separate letter.

### 5.6 SAMPLING METHODS

In addition to operational data related to the system (i.e., electrical current and voltage, flow rates of amendments and cross-circulation), an overall field monitoring and sampling program for the Dem/Val is presented in Table 5-3. Table 5-3 presents the sample matrix (i.e., soil and groundwater), the locations and frequencies, and the analytical parameters performed during each phase of this Dem/Val.

### 5.6.1 Sampling and Analytical Methods

As presented in Table 5-3, the Dem/Val monitoring program included both measurements of field parameters and collection of environmental samples (soil and groundwater) for laboratory analyses. Table 5-6 summarizes the laboratory analytical methods. The methods for field sample collection and field parameter measurements are described in this section.

Table 5-6. Analytical Methods for Sample Analysis

| Matrix | Analyte | Method | Container | Preservative ${ }^{1}$ | Holding Time |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Soil | VOCs | 8260B | 3x 10-gram <br> Terra Cores | 2 with NaHSO4; <br> 1 with methanol; $4 \pm 2^{\circ} \mathrm{C}$ | 14 days |
|  | Metals (Ca, Fe, Mn, Mg) | 6010B | 2-oz glass jar | $4 \pm 2^{\circ} \mathrm{C}$ | 6 months |
|  | Tracer ( $\mathrm{Br}^{-}$) | 300.0 | 2-oz glass jar | $4 \pm 2^{\circ} \mathrm{C}$ | 28 days |
|  | Biomarkers (Dhc, Dhb, and vcrA) | Gene-Trac ${ }^{\circledR}$ Method | 50 mL conical tube provided by laboratory | $4 \pm 2^{\circ} \mathrm{C}$ | 14 days |
| Groundwater | VOCs | 8260B | 40 mL VOA vial | $\mathrm{HC} 1 ; 4 \pm 2^{\circ} \mathrm{C}$ | 14 days |
|  | VFAs | Ion Chromatography | 40 mL VOA vial | $4 \pm 2^{\circ} \mathrm{C}$ | 14 days |
|  | DHGs (methane, ethane, ethane) | RSK-175 | 40 mL VOA vial | $\mathrm{HC1} ; 4 \pm 2^{\circ} \mathrm{C}$ | $14 \text { days }$ |
|  | Total Metals (Ca, Fe, Mn, Mg) | 6010B | 250mL polyethylene | $\mathrm{HNO}_{3} ; 4 \pm 2^{\circ} \mathrm{C}$ | 6 months |
|  | Anions ( $\mathrm{NO}_{3}{ }^{-}, \mathrm{SO}^{-2}, \mathrm{Cl}^{-}$) and Tracer ( $\mathrm{Br}^{-}$) | 300.0 | 250mL polyethylene | $4 \pm 2^{\circ} \mathrm{C}$ | 28 days (except $\mathrm{NO}_{3}$ - at 48 hours) |
|  | TOC | 9060A | 125 mL amber glass | HC1, $4 \pm 2^{\circ} \mathrm{C}$ | 28 days |
|  | Biomarkers (Dhc, Dhb, and vcrA) | Gene-Trac ${ }^{\circledR}$ Method | 500 mL polyethylene | $4 \pm 2^{\circ} \mathrm{C}$ | 14 days |

For soil sampling, soil cores were collected using DPT tooling. For each soil sampling event, one continuous core from ground surface to approximately 24 feet bgs was collected from each of the 11 soil sampling locations (C1 through C11) shown in Figure 5-11. Soil cores were collected in acetate sleeves for observation and sampling. Discrete soil samples were collected for laboratory analyses from the selected depths. For the baseline event, samples were collected at each location from approximately 18.5 , 21, and 23 ft bgs. The field personnel documented that clay was the predominant geologic material at all the locations and all these sampling depths. As discussed in Section 6.2, based on the baseline soil sampling results, subsequent soil sampling events only collected samples from 18.5 and 21 ft bgs, since CVOCs were not typically present below 21 ft bgs. For VOC analysis, Terra Core samplers were used to minimize volatilization loss. Upon completion of soil sampling, each borehole was backfilled with bentonite chips and surface repaired in accordance with NAS Jacksonville requirements.


Figure 5-11. Soil Sampling Locations (C1 through C11)
The groundwater monitoring well network for the Dem/Val is presented in Figure 5-1. Groundwater elevation was measured for each monitoring well prior to sampling. After opening each well, the groundwater elevation was allowed to equilibrate with atmospheric conditions before taking a water level measurement. The depth to groundwater was measured using a Solinst interface meter (or equivalent) in 0.01 -foot increments, relative to a permanently marked survey point located at the top of the well casing and recorded on the purge log field form. The water level meter was decontaminated between wells.

Groundwater sampling was conducted following low-flow purging protocols with the use of a peristaltic pump and dedicated tubing. With the low-flow sampling, the intake of the sampling tube was placed mid-way between the top and bottom of the well screen. The water level was monitored during purging to measure drawdown and determine the appropriate flow rate for the well. During purging, in-line water quality parameters were monitored continuously in a flowthrough cell for temperature, pH , specific conductance, DO, and ORP. Purging was considered complete when a minimum of one casing volume of water had been removed with collection of at least three sets of field measurements spaced at two (2) to three (3) minute intervals, or when groundwater field parameters stabilized. The indicator parameters were considered stabilized when three consecutive readings met the following criteria:

- Temperature $\pm 0.2^{\circ} \mathrm{C}$
(i.e., the second and third reading must be within $0.2^{\circ} \mathrm{C}$ of the first reading);
- $\mathrm{pH} \pm 0.2 \mathrm{pH}$ units;
- Specific Conductance $\pm 5 \%$ units; and
- $\mathrm{DO} \pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater).

Readings of stabilized parameters were recorded on the field sampling log forms. Following stabilization of indicator parameters, groundwater samples were collected into the appropriate laboratory prepared and preserved sample containers. Sampling containers, holding times, and preservation methods associated with each method are presented in Table 5-6. The sample containers were clearly labeled and placed in an insulated cooler with ice for shipping to laboratories following proper chain-of-custody protocols.

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### 6.0 SAMPLING RESULTS AND DISCUSSIONS

This section presents a detailed summary and discussions of all monitoring/sampling results. While baseline characterization results have already been presented in Section 5.2, select baseline characterization data are incorporated in this section, as appropriate, with other performance monitoring data to support analyses and discussions related to changes of soil and groundwater conditions during the Dem/Val.

### 6.1 SYSTEM OPERATION MONITORING

Figure 6-1 presents the power usage over the course of Stage 1 and Stage 2 operations. The voltage (V) and current (A) readings recorded at the power supply unit over the duration of operation are used to calculate the electrical power usage (kilowatt-hour [kW-hr]). The system was designed and operated to supply a constant current, determined after the start-up phase, and the power supply unit would then operate at a voltage level that was required in response to field electrical resistivity in order to maintain the supply of constant current.

Figure 6-1 shows that the power supply unit's voltage output remained generally steady between approximately 18 V and 28 V (Stage 1) and 12 V and 20 V (Stage 2 ). There were three occasions when different electrodes needed to be replaced, including late October/early November 2015 and late January/early February 2016 during Stage 1 operation, as well as December 2016 during Stage 2 operation. Prior to the electrode replacement, the system voltage readings would indicate the operating conditions were becoming unsteady. By inspecting the electrodes, it was determined that the initial shakedown/start-up operations at the start of Stage 1 operation, particularly an initial conservative electrode polarity reversal program, overly stressed the anode leading to damage of the electrode surface coatings. The polarity reversal program was corrected after the start-up operation in June/July 2015, however, the initial damages to the electrodes shortened the life-span of the anodes leading to the need to replace them during the operation. Other than the periods when electrodes were in need of replacement, the power supply unit operating conditions were relatively steady.

The total power consumption was calculated for Stage 1 at $1,037 \mathrm{~kW}-\mathrm{hr}$ and Stage 2 at 548 kW hr. Calculations for Stage 1 include the initial start-up operation (June-July 2015) and the initial buffering/conditioning operation (July-October 2015) preceding the 5-month Stage 1 full EK-BIO operation (October 2015-March 2016) counting after the TTA bioaugmented with the dechlorination culture. Stage 2 operation included only the 5-month full operation (October 2016March 2017). As a comparison, the total energy usage by the EK system during the 14 active months of the Dem/Val ( $1,585 \mathrm{~kW}-\mathrm{hr}$ ) is equivalent to operating two 100-W lightbulbs over the same time interval, or operating a single 100-W lightbulb for approximately 660 days ( 22 months).



Figure 6-1. Power Usage During System Operation

In addition to monitoring the power supply unit, field measurements were taken to confirm the establishment of electric field within the TTA. Figure 6-2 presents the field measurements made in October 2015 when electrode wells, E2, E5, and E8 were anodes.


Figure 6-2. Voltage Measurements (V) at Monitoring Wells Within TTA
The voltage measurements taken at individual monitoring wells were used to assess if a uniform electric field was established within the TTA. Voltage measurements at individual wells relative to a common cathode reference at the EK control system were between 5.3 V and 6.2 V with an average of 5.6 V and a standard deviation of 0.31 V ( $5 \%$ variation from the average) indicating that an electric field was established in the area between electrode wells. Voltage gradients between discrete locations of closest pairs are also calculated and summarized below.

| Well Pairs |  <br> MW-3 |  <br> MW-3 |  <br> MW-6 |  <br> MW-6 |  <br> MW-7 |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Voltage <br> Gradient (V/m) | 0.12 | 0.26 | 0.1 | 0.1 | 0.1 |

The calculated voltage gradients between these pairs are within 2 x of the average gradients (0.13 $\mathrm{V} / \mathrm{m}$ ) measured also suggesting no local focusing of electric field within TTA.

Table 6-1 below presents the average and standard deviation calculated for the electrical current to individual wells during each stage of operation. The data show that the current supply to individual electrode well was generally steady (variation within $37 \%$ of average). Given that (1) soil electrical resistivity is a soil property not expected to vary over the course of Dem/Val, and (2) the voltage output by the power supply unit and the current supplied to individual electrodes were generally steady, the electrical potential between electrode pairs within the TTA should maintain within 5 x of target during operation.

Table 6-1. Electrical Current to Electrode Wells

| Stage 1 | Cathodes |  |  |  |  |  | Anodes |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | E1 | E3 | E4 | E6 | E7 | E9 | E2 | E5 | E8 |
| Avg | 1.5 | 1.0 | 1.4 | 1.5 | 1.8 | 1.3 | 3.2 | 2.3 | 3.1 |
| Std Dev | 0.2 | 0.3 | 0.1 | 0.3 | 0.3 | 0.2 | 0.5 | 0.6 | 0.4 |
| Stage 2 | Cathodes |  |  |  |  |  | Anodes |  |  |
|  | E1 | E2 | E3 | E7 | E8 | E9 | E4 | E5 | E6 |
| Avg | 1.4 | 1.7 | 0.8 | 1.5 | 1.7 | 1.1 | 2.3 | 2.9 | 2.2 |
| Std Dev | 0.1 | 0.3 | 0.2 | 0.2 | 0.1 | 0.2 | 0.8 | 0.3 | 0.6 |

Table 6-2 summarizes the amendment supplied to the TTA and the energy usage throughout the Dem/Val. The duration and quantity reported for Stage 1 operation include the initial start-up operation and buffering/conditioning operation prior to bioaugmentation of the field when the 5month full EK-BIO remediation operation was considered to start.

Table 6-2. EK System Operation Summary

| Stage 1 Operation | Lactate to 8 Supply Wells | Lactate to 9 Electrode Wells | K-Carbonate to All Wells | Energy Usage |
| :---: | :---: | :---: | :---: | :---: |
| June 2015 - <br> March 2016 | 80 kg via 370 gal | $\begin{gathered} 158 \mathrm{~kg} \text { via } \\ \text { gal } \end{gathered} \quad 620$ | $\begin{gathered} 35 \mathrm{~kg} \text { via } \\ \text { gal } \end{gathered}$ | 985 kW-hr |
|  | $10 \mathrm{~kg} /$ well via gal/ well | $17.5 \mathrm{~kg} / \mathrm{well}$ via $69 \mathrm{gal} / \mathrm{well}$ |  |  |
| Stage 2 Operation | Lactate to 8 <br> Supply Wells | Lactate to 9 Electrode Wells | K-Carbonate to All Wells | Energy Usage |
| October 2016 - <br> March 2017 | 105 kg via 520 gal | $\begin{gathered} 212 \mathrm{~kg} \text { via } \\ \text { gal } \end{gathered} \quad 1,038$ | $\begin{array}{r} 16 \mathrm{~kg} \text { via } \\ \text { gal } \end{array}$ | $548 \mathrm{~kW}-\mathrm{hr}$ |
|  | $13.1 \mathrm{~kg} /$ well via 65 gal/ well | 23.5 kg/well via $115 \mathrm{gal} / \mathrm{well}$ |  |  |
| Dem / Val Total | Lactate to 8 Supply Wells 185 kg / 890 gal ( $23 \mathrm{~kg} /$ well via 112 gal/well) | Lactate to 9 Electrode Wells 370 kg / 1,658 gal (41 kg/well via $184 \mathrm{gal} / \mathrm{well}$ ) | K-Carbonate to All Wells <br> $51 \mathrm{~kg} / 960 \mathrm{gal}$ | Total Energy Usage 1,533 kW-hr |

It should be noted that in this Dem/Val, amendment delivery was driven by electric field and not hydraulic pressure. The total volume of lactate amendment solution delivered throughout the Dem/Val was approximately 2,550 gallons. This accounts for only $16 \%$ to $22 \%$ of the total pore volume within a treatment zone of $35 \mathrm{ft} \times 35 \mathrm{ft} \times 5 \mathrm{ft}$ at $25 \%$ to $35 \%$ total porosity.

Therefore, amendment distribution and the resulted biotreatment achieved within the TTA, as discussed below based on the monitoring data collected, should be recognized as the results of enhanced amendment delivery beyond diffusion mechanism.

### 6.2 GROUNDWATER SAMPLING RESULTS

Groundwater monitoring data are summarized, per sampling event, and provided in Appendix F. The locations of groundwater monitoring wells are presented in Figure 5-1. One monitoring well within the TTA, EKMW-06, was later found to not produce sufficient groundwater volume for sampling likely due to blockage. Therefore, EKMW-06 was not included in the monitoring program.

### 6.2.1 Groundwater Geochemistry

Groundwater geochemistry data, including the baseline characterization results, are summarized in Table 6-3. The baseline groundwater geochemistry data are also presented in Figure 5-4. The discussion in this section is organized by three separate areas - upgradient of the TTA, within the TTA, and downgradient of the TTA. For each area, data collected from the baseline event and subsequent performance monitoring events are discussed.

Monitoring well EKMW-09 is located upgradient of the TTA. Baseline data indicated that groundwater in this area was acidic ( pH at 5), oxidizing (ORP at 100 mV and DO at $1.2 \mathrm{mg} / \mathrm{L}$ ), with high chloride ( $2,800 \mathrm{mg} / \mathrm{L}$ ), and high iron ( $130 \mathrm{mg} / \mathrm{L}$ ). Throughout the Dem/Val, groundwater remained acidic ( pH below 5.2) and slightly oxidizing (ORP above 60 mV with low DO). The chloride concentration decreased from baseline to below $1,800 \mathrm{mg} / \mathrm{L}$ post-Stage 2, the reasons for the decline are unknown. Iron concentrations decreased from baseline to below $80 \mathrm{mg} / \mathrm{L}$.

Within the TTA, baseline characterization data showed that groundwater was acidic ( pH 4.7 at EKMW-01 to pH 5.8 at EKMW-02 and EKMW-03), slightly oxidizing (ORP at 34 to 64 mV , except -21 mV at EKMW-02 and EKMW-03) with low DO at 0.2 to $0.6 \mathrm{mg} / \mathrm{L}$. Other notable baseline geochemical conditions included:

- Three relatively distinct baseline chloride levels - EKMW-01 at 3,400 mg/L; EKMW-05 and EKMW-07 at 1,900 and $790 \mathrm{mg} / \mathrm{L}$, respectively; and EKMW-02, -03, and -04 at 520 $-570 \mathrm{mg} / \mathrm{L}$.
- Sulfate at $140 \mathrm{mg} / \mathrm{L}$ at EKMW-07, while at 24 to $57 \mathrm{mg} / \mathrm{L}$ at all other wells.
- Relatively high iron at EKMW-01 (130 mg/L) and EKMW-05 (160 mg/L), while generally at $60 \mathrm{mg} / \mathrm{L}$ for iron at other wells.

Based on baseline chloride, and iron concentrations, groundwater at EKMW-01 and EKMW-05 seemed to have similar geochemistry as that of upgradient well EKMW-09. While EKMW-01 is located near the upgradient edge of the TTA, EKMW-05 is near the down-/side-gradient edge of the TTA.

Table 6-3. Groundwater Geochemistry Data Summary

| EKMW-01 |  | Baseline (October 2014) | July 2015 | October 2015 | December 2015 | March 2016 | September 2016 | December 2016 | March 2017 | June 2017 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| pH | S.U. | 4.7 | 5.1 | 5.0 | 6.4 | 5.6 | 5.74 | 5.9 | 5.5 | 5.7 |
| ORP | mV | 54 | 130 | -170 | -50 | -103 | -120 | -76 | -79 | -161 |
| Dissolved Oxygen | $\mathrm{mg} / \mathrm{L}$ | 0.6 | 2.1 | 0.1 | 0.6 | 0.2 | 0.13 | 0.1 | 0.1 | 1.1 |
| Analyte | Units | Result | Result | Result | Result | Result | Result | Result | Result | Result |
| Bromide | $\mathrm{mg} / \mathrm{L}$ | 4.0 I | NA | NA | NA | 2.3 | NA | NA | NA | 4.5 I |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 3400 | NA | NA | NA | 1450 | NA | NA | NA | 1950 |
| Nitrate (as N) | $\mathrm{mg} / \mathrm{L}$ | 0.17 U | NA | NA | NA | 0.1 | NA | NA | NA | NA |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 57 | NA | NA | NA | 13.2 | NA | NA | NA | 15 U |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 350 | NA | NA | NA | 210 | NA | NA | NA | 229 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 130 | 100 | NA | NA | 87.4 | NA | NA | NA | 93.4 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 98 | NA | NA | NA | 61.9 | NA | NA | NA | 57.7 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 2.8 | NA | NA | NA | 1.96 | NA | NA | NA | NA |
| Potassium | $\mathrm{mg} / \mathrm{L}$ | NA | 8.1 | 5.7 | 5.2 | 5.43 I | NA | NA | NA | 5.9 I |


| EKMW-02 |  | Baseline (October 2014) | July 2015 | October 2015 | December 2015 | March 2016 | September 2016 | December 2016 | March 2017 | June 2017 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| pH | S.U. | 5.8 | 6 | 6.0 | 6.6 | 5.9 | 6.3 | 5.8 | 5.0 | 6.4 |
| ORP | mV | -21 | 51 | -21 | -35 | -34 | -22 | 13 | -58 | -70 |
| Dissolved Oxygen | $\mathrm{mg} / \mathrm{L}$ | 0.2 | 0.3 | 0.1 | 0.5 | 0.1 | 0.1 | 0.1 | 0.2 | 0.7 |
| Analyte | Units | Result | Result | Result | Result | Result | Result | Result | Result | Result |
| Bromide | $\mathrm{mg} / \mathrm{L}$ | 0.06 U | NA | NA | NA | 3.3 I | NA | NA | NA | 2.6 I |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 550 | NA | NA | NA | 664 | NA | NA | NA | 756 |
| Nitrate (as N) | $\mathrm{mg} / \mathrm{L}$ | 0.17 U | NA | NA | NA | NA | NA | NA | NA | NA |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 27 | NA | NA | NA | 10.7 | NA | NA | NA | 6 U |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 100 | NA | NA | NA | 177 | NA | NA | NA | 202 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 57 | 9.5 | NA | NA | 121 | NA | NA | NA | 103 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 30 | NA | NA | NA | 53.7 | NA | NA | NA | 54.4 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 0.86 | NA | NA | NA | 1.74 | NA | NA | NA | NA |
| Potassium | $\mathrm{mg} / \mathrm{L}$ | NA | 2.1 | 4.1 | 4 | 4.46 I | NA | NA | NA | 4.94 I |

Table 6-3. Groundwater Geochemistry Data Summary (Continued)

| EKMW-03 |  | Baseline (October 2014) | July 2015 | October 2015 | December 2015 | March 2016 | September 2016 | December 2016 | March 2017 | June 2017 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| pH | S.U. | 5.8 | 5.8 | 5.8 | 6.5 | 5.6 | 5.8 | 6.1 | 5.8 | 6.3 |
| ORP | mV | -21 | 0.4 | -1.3 | -53 | -5 | -56 | -77 | -43 | -79 |
| Dissolved Oxygen | $\mathrm{mg} / \mathrm{L}$ | 0.2 | 1.1 | 0.1 | 0.5 | 0.1 | 0.1 | 0.1 | 0.1 | 1.4 |
| Analyte | Units | Result | Result | Result | Result | Result | Result | Result | Result | Result |
| Bromide | $\mathrm{mg} / \mathrm{L}$ | 0.06 U | NA | NA | NA | 1.2 U | NA | NA | NA | 1.2 U |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 520 | NA | NA | NA | 674 | NA | NA | NA | 717 |
| Nitrate (as N) | $\mathrm{mg} / \mathrm{L}$ | 0.17 U | NA | NA | NA | NA | NA | NA | NA | NA |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 24 I | NA | NA | NA | 15.6 | NA | NA | NA | 7.7 |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 89 | NA | NA | NA | 208 | NA | NA | NA | 174 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 58 | 70 | NA | NA | 101 | NA | NA | NA | 99 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 27 | NA | NA | NA | 62.9 | NA | NA | NA | 53 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 0.79 | NA | NA | NA | 1.85 | NA | NA | NA | NA |
| Potassium | $\mathrm{mg} / \mathrm{L}$ | NA | 4.2 | 4.1 | 4.2 | 6.16 I | NA | NA | NA | 5.86 I |


| EKMW-04 |  | Baseline (October 2014) | July 2015 | October 2015 | December 2015 | March 2016 | September 2016 | December 2016 | March 2017 | June 2017 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| pH | S.U. | 4.9 | 5.8 | 5.7 | 6.3 | 5.9 | 5.6 | 5.8 | 5.5 | 6.9 |
| ORP | mV | 42 | 3 | -54 | -27 | -20 | 0.1 | -3 | 4.5 | -173 |
| Dissolved Oxygen | $\mathrm{mg} / \mathrm{L}$ | 0.2 | 0.7 | 0.2 | 0.5 | 3.5 | 1.2 | 0.1 | 0.1 | 1.5 |
| Analyte | Units | Result | Result | Result | Result | Result | Result | Result | Result | Result |
| Bromide | $\mathrm{mg} / \mathrm{L}$ | 0.06 U | NA | NA | NA | 0.6 U | NA | NA | NA | 0.6 U |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 570 | NA | NA | NA | 462 | NA | NA | NA | 465 |
| Nitrate (as N) | $\mathrm{mg} / \mathrm{L}$ | 0.17 U | NA | NA | NA | NA | NA | NA | NA | NA |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 45 | NA | NA | NA | 15.3 | NA | NA | NA | 17 |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 120 | NA | NA | NA | 126 | NA | NA | NA | 115 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 47 | 56 | NA | NA | 59.6 | NA | NA | NA | 56.3 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 31 | NA | NA | NA | 35.6 | NA | NA | NA | 31.3 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 0.99 | NA | NA | NA | 1.28 | NA | NA | NA | NA |
| Potassium | $\mathrm{mg} / \mathrm{L}$ | NA | 4.5 | 5.3 | 6.3 | 7.1 I | NA | NA | NA | 3.6 I |

Table 6-3. Groundwater Geochemistry Data Summary (Continued)

| EKMW-05 |  | Baseline (October 2014) | July 2015 | October 2015 | December 2015 | March 2016 | September 2016 | December 2016 | March 2017 | June 2017 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| pH | S.U. | 5.2 | 5.4 | 5.5 | 5.9 | 6.2 | 5.6 | 5.3 | 4.8 | 5.7 |
| ORP | mV | 64 | 74 | 17 | NA | -118 | -1 | -10 | 4.9 | -39 |
| Dissolved Oxygen | $\mathrm{mg} / \mathrm{L}$ | 0.3 | 0.4 | 0.1 | 0.5 | 4 | 1.0 | 0.1 | 0.3 | 0.4 |
| Analyte | Units | Result | Result | Result | Result | Result | Result | Result | Result | Result |
| Bromide | $\mathrm{mg} / \mathrm{L}$ | 1.2 U | NA | NA | NA | 1.2 U | NA | NA | NA | 3.0 U |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 1900 | NA | NA | NA | 1240 | NA | NA | NA | 1570 |
| Nitrate (as N) | $\mathrm{mg} / \mathrm{L}$ | 0.17 U | NA | NA | NA | NA | NA | NA | NA | NA |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 50 | NA | NA | NA | 11.5 I | NA | NA | NA | 27.3 I |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 400 | NA | NA | NA | 259 | NA | NA | NA | 229 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 160 | 130 | NA | NA | 131 | NA | NA | NA | 92.4 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 110 | NA | NA | NA | 72.5 | NA | NA | NA | 55.8 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 3.3 | NA | NA | NA | 2.39 | NA | NA | NA | NA |
| Potassium | $\mathrm{mg} / \mathrm{L}$ | NA | 7.4 | 3.8 | 3.5 | 6.12 I | NA | NA | NA | 6.2 I |


| EKMW-07 |  | Baseline (October 2014) | July 2015 | October 2015 | December 2015 | March 2016 | September 2016 | December 2016 | March 2017 | June 2017 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| pH | S.U. | 5.1 | 6.5 | 6.0 | 6.6 | 6.2 | 6.6 | 5.8 | 5.9 | 6.2 |
| ORP | mV | 34 | 67 | -63 | NA | -114 | -56 | -53 | -75 | -88 |
| Dissolved Oxygen | $\mathrm{mg} / \mathrm{L}$ | 0.5 | 0.3 | 0.1 | 0.5 | 3.1 | 0.1 | 0.1 | 0.1 | 0.9 |
| Analyte | Units | Result | Result | Result | Result | Result | Result | Result | Result | Result |
| Bromide | $\mathrm{mg} / \mathrm{L}$ | 0.06 U | NA | NA | NA | 1.2 U | NA | NA | NA | 3.0 U |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 790 | NA | NA | NA | 975 | NA | NA | NA | 1670 |
| Nitrate (as N) | $\mathrm{mg} / \mathrm{L}$ | 0.17 U | NA | NA | NA | NA | NA | NA | NA | NA |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 140 | NA | NA | NA | 8.9 I | NA | NA | NA | 15 U |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 150 | NA | NA | NA | 275 | NA | NA | NA | 419 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 23 | 30 | NA | NA | 52.9 | NA | NA | NA | 85.1 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 21 | NA | NA | NA | 34 | NA | NA | NA | 56.9 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 0.48 | NA | NA | NA | 1.09 | NA | NA | NA | NA |
| Potassium | $\mathrm{mg} / \mathrm{L}$ | NA | 8.4 | 4.9 | 5.7 | 9.9 I | NA | NA | NA | 16.3 |

Table 6-3. Groundwater Geochemistry Data Summary (Continued)

| EKMW-08 |  | Baseline <br> (October 2014) | September 2016 | June 2017 |
| :--- | :---: | :---: | :---: | :---: |
| pH | $\mathrm{S} . \mathrm{U}$. | 5.7 | 5.5 | 5.4 |
| ORP | mV | 12 | NA | -57 |
| Dissolved Oxygen | $\mathrm{mg} / \mathrm{L}$ | 0.4 | 0.1 | 1.2 |
| Analyte | Units | Result | Result | Result |
| Bromide | $\mathrm{mg} / \mathrm{L}$ | 0.06 U | NA | 1.2 U |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 1000 | NA | 1300 |
| Nitrate $(a s \mathrm{~N})$ | $\mathrm{mg} / \mathrm{L}$ | 0.17 U | NA | NA |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 38 | NA | 15.5 |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 150 | NA | 258 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 67 | NA | 80.9 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 45 | NA | 72 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 1.1 | NA | NA |
| Potassium | $\mathrm{mg} / \mathrm{L}$ | NA | NA | NA |


| EKMW-09 |  | Baseline (October 2014) | July 2015 | March 2016 | September 2016 | December 2016 | March 2017 | June 2017 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| pH | S.U. | 5.0 | 4.5 | 4.5 | 4.8 | 4.9 | 3.8 | 5.2 |
| ORP | mV | 100 | 163 | 201 | 102 | 74 | 62 | 109 |
| Dissolved Oxygen | $\mathrm{mg} / \mathrm{L}$ | 1.2 | 0.8 | 4.1 | 0.1 | 1.7 | 1.4 | 0.5 |
| Analyte | Units | Result | Result | Result | Result | Result | Result | Result |
| Bromide | $\mathrm{mg} / \mathrm{L}$ | 6.0 U | NA | 0.38 I | NA | NA | NA | 3.0 U |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 2800 | NA | 2190 | NA | NA | 1790 | 1630 |
| Nitrate (as N) | $\mathrm{mg} / \mathrm{L}$ | 0.17 U | NA | NA | NA | NA | NA | NA |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 36 | NA | 18.4 | NA | NA | 22.8 I | 23.4 I |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 460 | NA | 431 | NA | NA | 295 | 296 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 130 | NA | 125 | NA | NA | 79.2 | 78.1 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 130 | NA | 128 | NA | NA | 85.3 | 77.8 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 4.1 | NA | 4.48 | NA | NA | 2.9 | NA |
| Potassium | $\mathrm{mg} / \mathrm{L}$ | 9.4 | 9 | 8.55 I | 10.3 | 7.4 I | 6.3 I | 5.9 I |
| Total Dissolved Solids (Filterable) | $\mathrm{mg} / \mathrm{L}$ | 5700 | 6900 | 5760 | 6190 | 4400 | 2950 | 3890 |

Table 6-3. Groundwater Geochemistry Data Summary (Continued)

| EKMW-10 |  | Baseline (October 2014) | July 2015 | March 2016 | September 2016 | December 2016 | March 2017 | June 2017 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| pH | S.U. | 6.0 | 6 | 5.8 | 7.2 | 5.7 | 5.3 | 6.3 |
| ORP | mV | -27 | 10 | -5.9 | -630 | -92 | 30 | -101 |
| Dissolved Oxygen | $\mathrm{mg} / \mathrm{L}$ | 0.6 | 0.6 | 3.6 | 0.1 | 0.1 | 0.2 | 0.1 |
| Analyte | Units | Result | Result | Result | Result | Result | Result | Result |
| Bromide | $\mathrm{mg} / \mathrm{L}$ | 0.06 U | NA | 0.32 I | NA | NA | NA | 1.2 U |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 570 | NA | 788 | NA | NA | NA | 793 |
| Nitrate (as N) | $\mathrm{mg} / \mathrm{L}$ | 0.25 U | NA | NA | NA | NA | NA | NA |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 21 I | NA | 12 | NA | NA | NA | 22.9 |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 140 | NA | 193 | NA | NA | NA | 166 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 49 | NA | 53.3 | NA | NA | NA | 49.5 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 42 | NA | 59.3 | NA | NA | NA | 47.7 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 1.2 | NA | 1.62 | NA | NA | NA | NA |
| Potassium | $\mathrm{mg} / \mathrm{L}$ | 7.8 | 6.1 | 16.1 | 11.7 | 23.6 | 12.4 | 21.4 |
| Total Dissolved Solids (Filterable) | $\mathrm{mg} / \mathrm{L}$ | 1700 | 3000 | 2290 | 2280 | 1980 | 1230 | 2040 |


| EKMW-11 |  | Baseline <br> (October 2014) | September 2016 | March 2017 | June 2017 |
| :--- | :---: | :---: | :---: | :---: | :---: |
| pH | $\mathrm{S} . \mathrm{U}$. | 10.6 | 5.6 | 5.2 | 5.6 |
| ORP | mV | -9.2 | 35 | 114 | 11 |
| Dissolved Oxygen | $\mathrm{mg} / \mathrm{L}$ | 0.1 | 1.4 | 0.1 | 0.1 |
| Analyte | Units | Result | Result | Result | Result |
| Bromide | $\mathrm{mg} / \mathrm{L}$ | 0.06 U | NA | NA | 6.0 U |
| Chloride | $\mathrm{mg} / \mathrm{L}$ | 170 | NA | 2430 | 2220 |
| Nitrate (as N) | $\mathrm{mg} / \mathrm{L}$ | 0.17 U | NA | NA | NA |
| Sulfate | $\mathrm{mg} / \mathrm{L}$ | 16 I | NA | 36.5 I | 41.8 I |
| Calcium | $\mathrm{mg} / \mathrm{L}$ | 130 | NA | 386 | 345 |
| Iron | $\mathrm{mg} / \mathrm{L}$ | 2.9 | NA | 95.5 | 104 |
| Magnesium | $\mathrm{mg} / \mathrm{L}$ | 0.74 | NA | 86.3 | 73.7 |
| Manganese | $\mathrm{mg} / \mathrm{L}$ | 0.02 | NA | 4.1 | NA |
| Potassium | $\mathrm{mg} / \mathrm{L}$ | NA | NA | 8.1 I | NA |

## Notes:

S.U. Standard Units
mV millivolts
$\mathrm{mg} / \mathrm{L}$ milligrams per Liter
NTU Nephelometric Turbidity Unit

NA Not analyzed
U The compound was analyzed for but not detected.
I The reported value is between the laboratory method detection limit and the laboratory practical quantitation limit

Geochemistry data collected from within the TTA in October 2015 following approximately 3 months of system operation adding buffering reagent showed pH increases at all wells from baseline to between pH 5.5 and pH 6 , except at EKMW-01 where pH increased from baseline pH 4.7 to pH 5 . The data showed negative ORP at all wells, except at EKMW-05 where ORP changed from 64 mV baseline to 17 mV . DO was at or below $0.2 \mathrm{mg} / \mathrm{L}$ at all wells. Bioaugmentation with low-pH KB- ${ }^{\circledR}$ dechlorination culture was conducted at the end of October 2015.

Within the TTA following bioaugmentation and through Stage 1 and Stage 2 operations, groundwater pH generally remained between 5.5 and 6.6 and ORP was mostly negative after the Stage 1 and Stage 2 operations. Notable changes of certain geochemical conditions over the duration of Dem/Val include:

- Chloride - At EKMW-01, the concentration decreased from a baseline of 3,400 mg/L to $1,950 \mathrm{mg} / \mathrm{L}$ post-Stage 2, and at EKMW-05 from 1,900 to $1,570 \mathrm{mg} / \mathrm{L}$. However, at EKMW-02 and -03, concentrations increased from baseline levels of $520-550 \mathrm{mg} / \mathrm{L}$ to $717-750 \mathrm{mg} / \mathrm{L}$, and at EKMW-07 from 790 to $1,670 \mathrm{mg} / \mathrm{L}$. Relatively smaller changes were observed at EKMW-04 ( 570 to $465 \mathrm{mg} / \mathrm{L}$ ). These data suggest that some migration and redistribution of chloride (and likely other anions) might have occurred within the TTA as a result of the EK application.
- Sulfate - concentrations at all wells decreased from baseline levels of around $50 \mathrm{mg} / \mathrm{L}$ (except $140 \mathrm{mg} / \mathrm{L}$ baseline at EKMW-07) to 9 to $15 \mathrm{mg} / \mathrm{L}$, including at EKMW-07, at end of Stage 1 operation. Sulfate concentrations generally remained low thereafter. These data are indicative of sulfate reduction in the TTA.
- Iron - concentrations decreased from baseline at EKMW-01 and EKMW-05, the two wells with the highest baseline iron, to approximately $90 \mathrm{mg} / \mathrm{L}$ at post-Stage 2 incubation. However, at EKMW-02, -03, and -07, iron concentrations doubled or more from their baseline levels to $85-100 \mathrm{mg} / \mathrm{L}$. These data suggest that some migration and redistribution of iron (and likely other cations) occurred within the TTA as a result of the EK application.

At downgradient well EKMW-10, baseline conditions were slightly acidic ( pH at 6 ) and reducing (ORP at -27 mV and DO at $0.6 \mathrm{mg} / \mathrm{L}$ ). Baseline chloride ( $570 \mathrm{mg} / \mathrm{L}$ ), sulfate ( $21 \mathrm{mg} / \mathrm{L}$ ), and iron ( $49 \mathrm{mg} / \mathrm{L}$ ) concentrations were consistent with those observed in most of the wells in the TTA. Over the duration of Dem/Val, groundwater pH generally remained close to pH 6 , while ORP became more reducing ( -101 mV post-Stage 2). Chloride increased from $570 \mathrm{mg} / \mathrm{L}$ baseline to over $780 \mathrm{mg} / \mathrm{L}$ post-operation. Sulfate decreased after Stage 1 operation, but increased to baseline level after Stage 2. Relatively minimum changes (less than $8 \mathrm{mg} / \mathrm{L}$ in changes) in iron concentrations occurred throughout the Dem/Val.

### 6.2.2 Groundwater Chemical and Microbial Analytical Results

The discussion of groundwater sampling results is organized in this section with respect to assessment of (1) amendment distribution and (2) reductive dechlorination of CVOCs.

## Amendment Distribution

Groundwater TOC and VFA concentrations at monitoring wells provided an assessment of amendment distribution across the TTA. While lactate was provided as the amendment, it was expected that lactate would biodegrade as it was transported in the subsurface. Therefore, total VFAs were considered as an appropriate indicator of amendment distribution. Table 6-4 presents a summary comparing the baseline TOC and VFA concentrations detected at individual monitoring wells to the maximum concentrations of each detected during the Dem/Val.

Table 6-4. Groundwater TOC and VFA Summary
(Baseline vs. Maximum During Stage 1 / Stage 2)

| Well ID | TOC <br> (baseline) | TOC <br> S1/S2) | (max <br> (baseline) | VFA* <br> S1/S2) |
| :---: | :---: | :---: | :---: | :---: |
| EKMW-01 | 2.5 | $12.8 / 20.1$ | 3.2 | $60.7 / 57.6$ |
| EKMW-02 | 2.5 | $36.2 / 4.30$ | 1.6 | $141 / 2.50$ |
| EKMW-03 | 2.5 | $57.9 / 4.60$ | 1.2 | $233 / 11.3$ |
| EKMW-04 | 3.6 | $6.70 / 3.50$ | 1.9 | $18.3 / 8.20$ |
| EKMW-05 | 1.7 | $15.9 / 2.30$ | 1.8 | $6.60 / 1.00$ |
| EKMW-07 | 6.8 | $12.5 / 57.0$ | 2.2 | $21.7 / 204.7$ |
| EKMW-09 | 1.6 | $1.40 / 1.90$ | 2.3 | $1.40 /$ NA |
| EKMW-10 | 1.9 | $1.50 / 10.1$ | 2.1 | $1.40 / \mathrm{NA}$ |

* VFA = total of lactate, acetate, propionate, formate, butyrate, and pyruvate.

Units: mg/L.

With respect to TOC data, every monitoring well within the TTA saw an increase in TOC concentration $>8 x$ baseline levels, with the exception of EKMW-04 where the maximum TOC detected was $1.8 x$ the baseline. With respect to VFA data, every monitoring well within the TTA saw an increase in VFA concentration $>9 x$ baseline levels, with the exception of EKMW-05 where the maximum VFA detected was 4 x the baseline. These data show substantial increase in TOC and VFA concentrations across the TTA affected by EK application.

TOC and VFA concentrations at the two background monitoring wells, EKMW-09 and EKMW10, did not show apparent increases from their baseline levels, with the exception of TOC detected at $10.1 \mathrm{mg} / \mathrm{L}$ at EKMW-10 during the final post-Stage 2 sampling event. EKMW-10 is located downgradient of the TTA approximately 20 ft from electrode well E6. It is possible that some migration of TOC from the TTA occurred to affect this well in its final sampling event.

It is recognized that concentrations of TOC and VFA at certain locations within the TTA may be dynamic in nature given the microbial activities occurring in the subsurface. While it is apparent that amendment provided from the supply wells and electrode wells was distributed to all the monitoring well locations during the Dem/Val, the data suggest that certain monitoring well locations received different amounts of amendment between Stage 1 and Stage 2 operations.

For example, EKMW-02 and EKMW-03 appeared to receive more amendment in Stage 1 than in Stage 2, while EKMW-07 received more in Stage 2 than in Stage 1. This is likely due to the different orientations of electric fields established during the two stages of operations affecting the amendment transport patterns within the TTA. This observation suggests that future design should consider electrode network arrangements that will allow operations of various electric field orientations to enhance amendment delivery efficiency.

Noting that there was not a monitoring well located between the supply well network and electrode well E5, which was an anode during both Stage 1 and Stage 2 (i.e., electron donor would have always been migrating from the supply wells towards E5 in each stage), grab groundwater samples were collected during the final post-Stage 2 sampling event at several DPT soil sampling locations (C2, C3, C6, C7, and C9 in Figure 5-11). These samples were collected at each location generally from the depth of 21 ft , which approximately corresponded to the mid-screen interval of the monitoring wells within the TTA. The TOC results of these grab groundwater samples are presented in Table 6-5 below.

Table 6-5. Groundwater TOC at Select DPT Sampling Locations (from 21 ft bgs )

| Location | C2 | C3 | C6 | C7 | C9 |
| :---: | :---: | :---: | :---: | :---: | :---: |
| TOC (mg/L) | 950 | 160 | 3.4 | 820 | 790 |

Significant TOC concentrations ( 160 to $950 \mathrm{mg} / \mathrm{L}$ ) were detected at all three sample locations (C2, C3, and C7) between the supply wells and electrode well E5. These data confirmed that significant amendment had been distributed to this interior area. As a comparison, location C6 at the upgradient edge of the TTA did not appear to receive much amendment, likely due to its exterior position relative to supply wells and electric field orientation.

TOC concentrations in the sample collected from C9, located in the vicinity of unused monitoring well EKMW-06, indicate that the area received substantial electron donor. Thus, while EKMW06 failed to provide data, C9 provided valuable replacement data confirming the amendment distribution to this portion of the TTA.

## Enhanced Reductive Dechlorination

Figure 6-3 presents a comparison of groundwater CVOC and biomarker monitoring results at six monitoring wells within the TTA and two outside the TTA. The overall tabulated groundwater monitoring data are provided in Appendix F. Figure 6-3 presents the data collected from five (5) milestone events: baseline event in October 2014; end of Stage 1 operation in March 2016; end of post-Stage 1 incubation in September 2016; end of Stage 2 operation in March 2017; and end of post-Stage 2 incubation in June 2017.




Legend:
$\Longrightarrow$ Ethene
$\longleftarrow V C$
$\square C D C E$
毋TCE
$\square$ PCE
$\rightarrow$ vhc
$\square-$ vcrA
ESTCP ER-201325
Groundwater CVOC \& Biomarkers
OU3, NAS Jacksonville

| Geosyntec <br> consultants |  | Figure |
| :---: | :---: | :---: |
| Columbia, Maryland | November 2017 | $6-3$ |

Figure 6-3. Groundwater CVOC \& Biomarkers

EKMW-09 and EKMW-10 are located outside the TTA (Figure 5-1). The upgradient well, EKMW-09, is in the general area of the suspected PCE source (the former Building 106 area). The PCE concentrations at EKMW-09 remained above the baseline level during the Dem/Val, with no apparent increase of reductive dechlorination intermediates, and no detectable levels of biomarkers (below 1E+03 cell/L) throughout the Dem/Val.

At downgradient well EKMW-10, the baseline cis-1,2-DCE concentration was $260 \mu \mathrm{~g} / \mathrm{L}$, while the baseline methane concentration was $1,300 \mu \mathrm{~g} / \mathrm{L}$, both indicative of some natural reductive biological activity in this area prior to the Dem/Val. Between the baseline event and the post-Stage 2 event, no significant changes in PCE and other PCE dechlorination intermediate concentrations were observed, with the exception of an increase in vinyl chloride from $5 \mu \mathrm{~g} / \mathrm{L}$ to $157 \mu \mathrm{~g} / \mathrm{L}$. It is also noted that while biomarkers were below detection in the baseline event, a low level of Dhc ( $1.6 \mathrm{E}+03$ cell per L) was detected at EKMW-10 in the post-Stage 2 event. This level of Dhc was close to the method detection limit, and vcrA in that sample was still below detection limit. Overall, the data at EKMW-10 appear to suggest slight influence from the operation in the TTA approximately 20 ft away (to electrode well E6). As a comparison, the upgradient well EKMW09 is located approximately 25 ft away from the closest electrode well E4.

Among the monitoring wells within the TTA, EKMW-01, located closest to the upgradient edge of the TTA, contained the highest baseline PCE concentration at $7,640 \mu \mathrm{~g} / \mathrm{L}$. While there were baseline PCE dechlorination intermediates (cis-1,2-DCE $>1,000 \mu \mathrm{~g} / \mathrm{L}$ and VC at $33 \mu \mathrm{~g} / \mathrm{L}$ ) at EKMW-01, low levels of baseline methane ( $190 \mu \mathrm{~g} / \mathrm{L}$ ), ethene ( $15 \mu \mathrm{~g} / \mathrm{L}$ ), and VFAs ( $2.3 \mathrm{mg} / \mathrm{L}$ ) suggested limited reductive dechlorination activities in the vicinity prior to the Dem/Val. It is noted that Dhc and vcrA were detected in the baseline event at $8 \mathrm{E}+05$ cell/L and $3 \mathrm{E}+03$ gene copies/L, respectively. As presented in Figure 6-3, significant PCE dechlorination at EKMW-01 was observed in both post-Stage 1 and post-Stage 2 monitoring events. PCE concentrations decreased from the baseline level by $90 \%$ and $95 \%$ in the two events, respectively, while dissolved ethene concentrations were 15 x and 85 x ( $228 \mu \mathrm{~g} / \mathrm{L}$ and $1,280 \mu \mathrm{~g} / \mathrm{L}$, respectively) the baseline level. There was a transitory increase of cis-1,2-DCE from baseline to end of Stage 1 operation followed by its continuing decrease through the post-Stage 2 sampling event. Methane concentrations remained generally at a similar level as baseline throughout the Dem/Val (75 to $399 \mu \mathrm{~g} / \mathrm{L}$ ). Both biomarkers increased by $1,000 \mathrm{x}$ or more from the baseline levels to the postStage 1 detections ( $10^{7}$ and $10^{8}$ cell/gene copies per L), with continued increases through the postStage 2 event ( $10^{8}$ and $10^{9}$ cell/gene copies per L ).

The data for monitoring wells EKMW-02, -03 , and -04 , were relatively similar, with baseline PCE concentrations ranging from 170 to $250 \mu \mathrm{~g} / \mathrm{L}$, and low to no detectable baseline VC ( $<6 \mu \mathrm{~g} / \mathrm{L}$ ), ethene (all below detection), and biomarkers (all below detection). While enhanced reductive dechlorination was evident at all these wells, one noticeable difference between this group of wells and EKMW-01 was the significant increases of methane throughout the Dem/Val (see below).

| Methane at | Baseline | End of Stage 1 | Post-Stage 1 | End of Stage 2 | Post-Stage 2 |
| :---: | :---: | :---: | :---: | :---: | :---: |
| EKMW-01 | 190 | 102 | 132 | 164 | 399 |
| EKMW-02 | 1,200 | 1,850 | 6,380 | 7,890 | 8,740 |
| EKMW-03 | 330 | 2,850 | 6,270 | 5,480 | 7,930 |
| EKMW-04 | 54 | 401 | 1,930 | 4,100 | 5,010 |

Unit: $\mu \mathrm{g} / \mathrm{L}$

Both biomarkers at all these three wells increased by >1,000x from non-detect baseline levels to above $1 \mathrm{E}+06$ at the end of Stage 1 operation, and were generally maintained at such levels throughout the Dem/Val. Dissolved ethene concentrations increased from non-detect baseline levels to the ranges of 120 to $170 \mu \mathrm{~g} / \mathrm{L}$ at EKMW-02, 50 to $78 \mu \mathrm{~g} / \mathrm{L}$ at EKMW-03, and up to 32 $\mu \mathrm{g} / \mathrm{L}$ at EKMW-04. The sum of chlorinated ethenes decreased by 78\% at EKMW-02, 54\% at EKMW-03, and 46\% at EKMW-04 over the course of Dem/Val.

EKMW-05 and EKMW-07 had relatively high baseline PCE concentrations at 1,800 and 1,300 $\mu \mathrm{g} / \mathrm{L}$, respectively. At EKMW-07 PCE concentrations significantly decreased from baseline to the end of Stage 1 operation ( $1,300 \mu \mathrm{~g} / \mathrm{L}$ to $202 \mu \mathrm{~g} / \mathrm{L}$ ) and remained relatively stable during the 6month post-Stage 1 incubation period (slight increase to $253 \mu \mathrm{~g} / \mathrm{L}$ ). In Stage 2, PCE concentrations decreased further ( $253 \mu \mathrm{~g} / \mathrm{L}$ to $55 \mu \mathrm{~g} / \mathrm{L}$ ) during active EK, and rebounded slightly during postStage 2 incubation (up to to $92 \mu \mathrm{~g} / \mathrm{L}$ ). Methane concentrations at EKMW-07 increased significantly throughout the Dem/Val ( $110 \mu \mathrm{~g} / \mathrm{L}$ baseline to over $7,000 \mu \mathrm{~g} / \mathrm{L}$ post-Stage 1 and over $8,000 \mu \mathrm{~g} / \mathrm{L}$ post-Stage 2), while Dhc and $v c r$ A increased from non-detect levels to over $1 \mathrm{E}+08$ cell/L and $1 \mathrm{E}+06$ gene copies/L, respectively, and dissolved ethene continued to increase from baseline ( $11 \mu \mathrm{~g} / \mathrm{L}$ ) through post-Stage 1 incubation ( $161 \mu \mathrm{~g} / \mathrm{L}$ ) and again through post-Stage 2 incubation ( $260 \mu \mathrm{~g} / \mathrm{L}$ ).

At EKME-05, PCE concentrations significantly decreased from baseline ( $1,800 \mu \mathrm{~g} / \mathrm{L}$ ) to end of Stage 1 operation ( $180 \mu \mathrm{~g} / \mathrm{L}$ ) but then rebounded during the 6 -month post-Stage 1 incubation period (to $2,280 \mu \mathrm{~g} / \mathrm{L}$ ). During the post-Stage 1 incubation (no active EK operation) when PCE rebounded, methane and ethene both increased from 210 to $587 \mu \mathrm{~g} / \mathrm{L}$ and 144 to $255 \mu \mathrm{~g} / \mathrm{L}$, respectively, indicating continuing methanogenic and reductive dechlorination activities in the area. During Stage 2 operation, PCE concentrations decreased from $2,280 \mu \mathrm{~g} / \mathrm{L}$ to $603 \mu \mathrm{~g} / \mathrm{L}$, but again rebounded (to $3,540 \mu \mathrm{~g} / \mathrm{L}$ ) during post-Stage 2 incubation. The reason for this rebound is unclear, but may indicate the presence of some residual PCE mass in this area. Methane concentrations further increased from post-Stage 1 incubation to post-Stage 2 incubation (from to $987 \mu \mathrm{~g} / \mathrm{L}$ ). Both biomarkers increased by almost 100 x to $10,000 \mathrm{x}$ from baseline ( $1 \mathrm{E}+05 \mathrm{cell} / \mathrm{gene}$ copies per L) through Stage 1 operation, and remained above $1 \mathrm{E}+06$ to $1 \mathrm{E}+07$ cell/gene copies per L throughout the Dem/Val.

As presented in Table 6-6, DPT groundwater samples collected from select interior locations during the post-Stage 2 event were analyzed for CVOCs, dissolved gases, and biomarkers to supplement the monitoring data collected at monitoring wells. The three samples from the interior locations (C2, C3, and C7; see Figure 5-11) between the supply wells and anode E5 showed the most significant methanogenesis and reductive dechlorination. Methane concentration were more than $2,400 \mu \mathrm{~g} / \mathrm{L}$, and dissolved ethene concentrations ranged between 474 and $1,880 \mu \mathrm{~g} / \mathrm{L}$. Biomarkers, Dhc and vcrA, were detected at levels between $1 \mathrm{E}+05$ and $2 \mathrm{E}+07$ cell/gene copies per liter. These observations are consistent with the soil sampling results for these three locations discussed in Section 6.3 below (see Figure 6-5 for soil CVOC and Table 6-9 for soil microbial analyses).

Table 6-6. Groundwater CVOC and Biomarker at Select DPT Sampling Locations (from 21 ft bgs)

| Location | C2 | C3 | C6 | C7 | C9 |  |
| :---: | :---: | ---: | ---: | ---: | ---: | ---: |
| PCE | $\mu \mathrm{g} / \mathrm{L}$ | 11 | 160 | 1,400 | 28 | 250 |
| TCE | $\mu \mathrm{g} / \mathrm{L}$ | 5 | 430 | 660 | 29 | 67 |
| cis-1,2-DCE | $\mu \mathrm{g} / \mathrm{L}$ | 86 | 3,700 | 2,600 | 220 | 1,900 |
| VC | $\mu \mathrm{g} / \mathrm{L}$ | 1,200 | 570 | 380 | 330 | 5,000 |
| Methane | $\mu \mathrm{g} / \mathrm{L}$ | 2,490 | 3,840 | 634 | 4,090 | 259 |
| Ethene | $\mu \mathrm{g} / \mathrm{L}$ | 1,710 | 474 | 100 | 1,880 | 402 |
| Ethane | $\mu \mathrm{g} / \mathrm{L}$ | 18 | 12 | 5 | 6 | 3 |
| $\boldsymbol{D h c}$ | cell / L | $5 . \mathrm{E}+06$ | $2 . \mathrm{E}+05$ | $2 . \mathrm{E}+03$ | $2 . \mathrm{E}+07$ | $<4 \mathrm{E}+04$ |
| $\boldsymbol{t c e}$ | gene copies / L | $1 . \mathrm{E}+06$ | $5 . \mathrm{E}+04$ | $<3 \mathrm{E}+04$ | $4 . \mathrm{E}+06$ | NA |
| $\boldsymbol{b v c}$ | gene copies / L | $5 . \mathrm{E}+05$ | $4 . \mathrm{E}+03$ | $<3 \mathrm{E}+04$ | $1 . \mathrm{E}+06$ | NA |
| $\boldsymbol{v c r}$ | gene copies / L | $4 . \mathrm{E}+06$ | $1 . \mathrm{E}+05$ | $<3 \mathrm{E}+04$ | $1 . \mathrm{E}+07$ | NA |
| $\boldsymbol{D h b}$ | cell / L | $1 . \mathrm{E}+04$ | $<4 \mathrm{E}+03$ | $<3 \mathrm{E}+04$ | $3 . \mathrm{E}+05$ | $<4 \mathrm{E}+04$ |

With the C6 sample, although methane concentrations over $600 \mu \mathrm{~g} / \mathrm{L}$, together with low levels of ethene ( $100 \mu \mathrm{~g} / \mathrm{L}$ ) and Dhc ( $2 \mathrm{E}+03 \mathrm{cell} / \mathrm{L}$ ), were detected, overall the data suggest that the area near the upgradient edge of the TTA likely received less treatment due to the location relative to the supply well network and electric field orientation, which would move the amendment more effectively towards the interior of the TTA.

Location C9 was in the vicinity of a former monitoring well EKMW-06 which was not included in the monitoring program. The DPT groundwater data of C9 showed significant TOC concentration ( $790 \mathrm{mg} / \mathrm{L}$ ) and evident reductive dechlorination with ethene concentration at 402 $\mu \mathrm{g} / \mathrm{L}$. As discussed below in Section 6.3, soil CVOC and soil microbial analyses of C9 also indicated reductive dechlorination activities in that area.

Collectively, with the evident reductive dechlorination observed in the groundwater samples collected from the interior portion of the TTA ( $\mathrm{C} 2, \mathrm{C} 3$, and C 7 locations) and the area of C9, as well as the network of Dem/Val monitoring wells, EK application clearly promoted substantial dichlorination and treatment within the overall TTA.

### 6.3 SOIL SAMPLING RESULTS

There were three (3) rounds of soil sampling over Dem/Val: baseline event (September 2014), post-Stage 1 event (April 2016), and post-Stage 2 event (June 2017). The 11 soil sampling locations are presented in Figure 5-11.

### 6.3.1 Soil Chemical Analyses Results

Table 6-7 presents a summary of soil chemical analytical results, including the baseline characterization results. For the baseline event, at each sampling location three (3) samples were collected each from discrete depths. The baseline data showed that within the TTA, PCE was the only chlorinated ethene detected at a concentration above $1 \mathrm{mg} / \mathrm{kg}$, with the exception of cis-1,2DCE at $1.9 \mathrm{mg} / \mathrm{kg}$ and $3.3 \mathrm{mg} / \mathrm{kg}$ at locations C3 ( 18.5 ft bgs ) and C7 ( 18.5 ft bgs ), respectively. The baseline data indicated that there was no apparent reductive dechlorination activity within the TTA soil prior to the Dem/Val. It was also noted that PCE concentrations decreased significantly with depth from 18.5 ft to 23 ft . PCE concentrations were below $0.08 \mathrm{mg} / \mathrm{kg}$ in all samples collected from the 21 and 23 ft bgs depths, with the exception of location C6 $(5.5 \mathrm{mg} / \mathrm{kg}$ at 21 ft bgs and $3.1 \mathrm{mg} / \mathrm{kg}$ at 23 ft bgs ) located on the upgradient limit of the TTA and closest to the expected PCE source in the general area of former Building 106 (Figure 5-11). Based on the finding that PCE was overwhelmingly present only at the 18.5 ft bgs sample interval, subsequent soil sampling events collected samples only from 18.5 ft bgs and 21 ft bgs.

The baseline soil sampling event also included soil grain size analysis to allow an assessment of whether the initial soil CVOC distribution was related to the heterogeneity of soil grain sizes. This was conducted, in response to a request by ESTCP during Demonstration Plan development, to assess whether CVOC concentrations, electron donor migration, and CVOC treatment could be correlated to grain size (a question related to uniformity of treatment). Table 6-8 presents the grain size analysis of the samples from within the TTA at 18.5 and 21 ft bgs.

Table 6-7. Summary of Soil Chemical Analytical Results

| Analyte (mg/kg) | C1-18.5 |  |  | C1-21 |  |  | C1-23 | C2-18.5 |  |  | C2-21 |  |  | C2-23 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) |
| Tetrachloroethene | 16 | 11 | 1.9 | 0.029 | 0.41 | 0.056 U | 0.04 | 15 | 0.63 | 1.9 | 0.028 | 0.043 | 0.11 | 0.082 |
| Trichloroethylene | 0.42 | 0.077 | 0.31 | 0.032 | 0.081 | 0.047 U | 0.061 | 0.27 I | 0.054 | 0.19 | 0.017 | 0.004 U | 0.015 | 0.067 |
| cis-1,2-Dichloroethene | 0.38 I | 0.084 | 0.75 | 0.006 | 0.1 | 0.31 | 0.0077 | 0.16 | 0.37 | 1.1 | 0.006 | 0.051 | 0.19 | 0.0083 |
| Vinyl Chloride | 0.032 | 0.0045 U | 0.043 U | 0.0013 U | 0.0044 U | 0.056 U | 0.0014 U | 0.012 | 0.0039 U | 0.24 | 0.0011 U | 0.0048 U | 0.036 | 0.0014 U |
| Calcium | 2500 | 2700 | 2400 | NA | NA | NA | 2200 | 1200 | NA | NA | NA | NA | NA | 2400 |
| Iron | 20000 | 19000 | 15000 | NA | NA | NA | 17000 | 8000 | NA | NA | NA | NA | NA | 16000 |
| Magnesium | 3400 | 3300 | 2600 | NA | NA | NA | 2700 | 1600 | NA | NA | NA | NA | NA | 3100 |
| Manganese | 60 | 59 | 55 | NA | NA | NA | 54 | 27 | NA | NA | NA | NA | NA | 62 |
| Total Organic Carbon | NA | 520 | 91 I | NA | 430 I | NA | NA | NA | NA | 170 I | NA | NA | NA | NA |


| Analyte (mg/kg) | C3-18.5 |  |  | C3-21 |  |  | C3-23 | C4-18.5 |  |  | C4-21 |  |  | C4-23 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | Baseline (October 2014) | April 2016 [1] | June 2017 [1] | Baseline (October 2014) | April 2016 [1] | June 2017 [1] | Baseline (October 2014) |
| Tetrachloroethene | 6.9 | 0.037 | 0.009 | 0.084 U | 0.0047 U | 0.2 | 0.084 U | 4.7 | 0.31 | 0.075 | 0.081 | 0.011 | 0.23 | 0.01 |
| Trichloroethylene | 0.42 | 0.0045 U | 0.001 U | 0.07 U | 0.0039 U | 0.084 | 0.07 U | 0.17 | 0.015 | 0.015 | 0.018 | 0.0027 U | 0.03 | 0.04 |
| cis-1,2-Dichloroethene | 1.9 | 0.87 | 0.007 | 0.099 I | 0.28 | 0.31 | 0.097 U | 0.14 | 0.027 | 1.2 | 0.0082 | 0.0037 U | 0.037 | 0.014 |
| Vinyl Chloride | 0.077 U | 0.029 | 0.67 | 0.084 U | 0.0047 U | 0.063 U | 0.084 U | 0.023 | 0.0022 U | 0.22 | 0.0015 U | 0.0032 U | 0.008 | 0.0014 U |
| Calcium | 1200 | NA | NA | NA | NA | NA | 2200 | 2400 | NA | NA | NA | NA | NA | 2700 |
| Iron | 8100 | NA | NA | NA | NA | NA | 13000 | 18000 | NA | NA | NA | NA | NA | 21000 |
| Magnesium | 1600 | NA | NA | NA | NA | NA | 2800 | 3300 | NA | NA | NA | NA | NA | 3600 |
| Manganese | 26 | NA | NA | NA | NA | NA | 49 | 56 | NA | NA | NA | NA | NA | 71 |
| Total Organic Carbon | NA | 360 I | 120 I | NA | 400 I | NA | NA | NA. | NA | 440 I | NA | NA | NA | NA |


| Analyte (mg/kg) | C5-18.5 |  |  | C5-21 |  |  | C5-23 | C6-18.5 |  |  | C6-21 |  |  | C6-23 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) |
| Tetrachloroethene | 12 | 2 | 0.73 | 0.022 | 0.06 | 0.099 | 0.047 | 10 | 9.6 | 2.2 | 5.5 | 0.088 | 0.21 | 3.1 |
| Trichloroethylene | 0.14 I | 0.031 | 0.23 | 0.007 | 0.004 U | 0.015 | 0.043 | 0.27 I | 0.028 | 0.21 | 0.18 | 0.01 I | 0.044 | 0.18 |
| cis-1,2-Dichloroethene | 0.12 I | 0.032 | 1.1 | 0.0046 I | 0.0056 U | 0.065 | 0.0067 I | 0.16 | $0.015 \mathrm{J4}$ | 0.27 | 0.12 | 0.0049 U | 0.055 | 0.11 |
| Vinyl Chloride | 0.083 U | 0.0028 U | 0.34 | 0.00057 U | 0.0048 U | 0.009 | 0.0011 U | 0.027 | 0.0053 U | 0.053 U | 0.017 | 0.0042 U | 0.023 | 0.016 |
| Calcium | 2200 | NA | NA | NA | NA | NA | 2300 | 3100 | 3000 | 2200 | NA | NA | NA | 2700 |
| Iron | 15000 | NA | NA | NA | NA | NA | 15000 | 29000 | 21000 | 11000 | NA | NA | NA | 20000 |
| Magnesium | 2800 | NA | NA | NA | NA | NA | 2800 | 4500 | 3500 | 2200 | NA | NA | NA | 3300 |
| Manganese | 47 | NA | NA | NA | NA | NA | 57 | 84 | 63 | 46 | NA | NA | NA | 70 |
| Total Organic Carbon | NA | 420 I | 52 U | NA | 480 I | NA | NA | NA | NA | 73 I | NA | NA | NA | NA |


| Analyte (mg/kg) | C7-18.5 |  |  | C7-21 |  |  | C7-23 | C8-18.5 |  |  | C8-21 |  |  | C8-23 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) |
| Tetrachloroethene | 0.08 U | 0.1 | 0.012 | 0.027 | 0.0025 U | 0.001 U | 0.011 | 7.6 | 1.9 | 1.6 | 0.025 | 0.058 | 0.13 | 0.021 |
| Trichloroethylene | 0.067 U | 0.0045 U | 0.001 U | 0.0025 I | 0.0021 U | 0.001 U | 0.011 | 0.12 | 0.046 | 0.24 | 0.024 | 0.0068 U | 0.02 | 0.062 |
| cis-1,2-Dichloroethene | 3.3 | 0.81 | 0.024 | 0.11 | 0.087 | 0.17 | 0.011 | 0.86 | 0.15 | 0.63 | 0.0058 | 0.0094 U | 0.047 | 0.0062 |
| Vinyl Chloride | 0.08 U | 0.0054 U | 0.096 | 0.00052 U | 0.0025 U | 0.061 | 0.00056 U | 0.2 | 0.026 | 0.058 U | 0.0045 | 0.0081 U | 0.025 | 0.0011 U |
| Calcium | 2200 | NA | NA | NA | NA | NA | 2800 | 2900 | NA | NA | NA | NA | NA | 2100 |
| Iron | 20000 | NA | NA | NA | NA | NA | 19000 | 27000 | NA | NA | NA | NA | NA | 16000 |
| Magnesium | 3200 | NA | NA | NA | NA | NA | 3800 | 4100 | NA | NA | NA | NA | NA | 2600 |
| Manganese | 58 | NA | NA | NA | NA | NA | 71 | 75 | NA | NA | NA | NA | N.A | 51 |
| Total Organic Carbon | NA. | NA | 480 I | NA | NA | NA | NA. | NA | 350 I | 490 I | NA | 360 I | NA | NA |

Table 6-7. Summary of Soil Chemical Analytical Results (Continued)

| Analyte (mg/kg) | C9-18.5 |  |  | C9-21 |  |  | C9-23 | C10-18.5 [2] |  |  | C10-21 [2] |  |  | C10-23 [2] |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | Baseline (October 2014) | April 2016 | June 2017 | Baseline (October 2014) | April 2016 | June 2017 | $\begin{array}{\|c\|} \hline \text { Baseline } \\ \text { (October 2014) } \\ \hline \end{array}$ |
| Tetrachloroethene | 14 | 0.28 | 1.9 | 0.035 | 0.039 | 0.13 | 0.0013 U | 45 | 48 | 8.2 | 11 | 14 | 0.99 | 2.6 |
| Trichloroethylene | 0.3 I | 0.0068 U | 0.086 | 0.0096 | 0.0019 U | 0.019 | 0.03 | 0.1 | 0.19 | 0.58 | 0.015 | 0.037 | 0.04 U | 0.0076 |
| cis-1,2-Dichloroethene | 0.22 I | 0.0095 U | 0.21 | 0.0018 I | 0.0026 U | 0.025 | 0.0066 | 0.031 | 0.034 | 0.55 | 0.004 I | 0.0035 U | 0.055 U | 0.0016 I |
| Vinyl Chloride | 0.037 | 0.0081 U | 0.014 | 0.0015 U | 0.0023 U | 0.007 | 0.0012 U | 0.00052 U | 0.0047 U | 0.11 | 0.00055 U | 0.003 U | 0.048 U | 0.0005 U |
| Calcium | 1800 | NA | NA | NA | NA | NA | 2400 | 1500 | 2600 | 620 | NA | NA | NA | 2500 |
| Iron | 13000 | NA | NA | NA | NA | NA | 17000 | 12000 | 15000 | 4500 | NA | NA | NA | 18000 |
| Magnesium | 2200 | NA | NA | NA | NA | NA | 2900 | 2000 | 3000 | 850 | NA | NA | NA | 3200 |
| Manganese | 42 | NA | NA | NA | NA | NA | 61 | 38 | 49 | 15 | NA | NA | NA | 34 |
| Total Organic Carbon | NA | NA | 480 I | NA | NA | NA | NA | NA | 510 | 510 | NA | 460 I | NA | NA |


| Analyte (mg/kg) | C11-18.5 [2] | C11-21 [2] | C11-23 [2] |
| :--- | :---: | :---: | :---: |
|  | Baseline <br> (October 2014) | Baseline <br> (October 2014) | Baseline <br> (October 2014) |
| Tetrachloroethene | 4.9 | 0.034 | 0.097 U |
| Trichloroethylene | 0.024 | 0.0014 U | 0.081 U |
| (is-1,2-Dichloroethene | 0.0082 | 0.0014 U | 0.11 U |
| Vinyl Chloride | 0.0015 I | 0.0017 U | 0.097 U |
| Calcium | 2700 | NA | 4100 |
| Iron | 19000 | NA | 24000 |
| Magnesium | 2900 | NA | 4400 |
| Manganese | 69 | NA | 260 |
| Total Organic Carbon | NA | NA | NA |

Notes:
$\mathrm{mg} / \mathrm{kg}$ milligram per kilogram
NA Not analyzed.
U The compound was analyzed for but not detected.
I The reported value is between the laboratory method detection limit and the laboratory practical quantitation limit.
J4 Estimated result.
[1] Baseline (October 2014) C4 location corresponds to the C12 location in 2016 and 2017 events.
[2] Sampling locations $\mathrm{C10}$ and $\mathrm{Cl1}$ are outside the target treatment area.

Table 6-8. $\quad$ Soil Grain Size Analysis (Baseline Event)

| Location / <br> Depth | \% Fines (Silt + Clay) |  | \% Silt |  | \% Clay |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathbf{1 8 . 5} \mathbf{f t}$ | $\mathbf{2 1 ~ f t}$ | $\mathbf{1 8 . 5} \mathbf{f t}$ | $\mathbf{2 1 ~ f t}$ | $\mathbf{1 8 . 5} \mathbf{f t}$ | $\mathbf{2 1 ~ f t}$ |  |
| C1 | 61.0 | 76.8 | 16.2 | 31.2 | 44.8 | 45.6 |
| C2 | 53.8 | 77.8 | 18.1 | 35.0 | 35.7 | 42.8 |
| C3 | 80.7 | 80.5 | 26.4 | 30.1 | 54.3 | 50.4 |
| C4 | 88.8 | 71.0 | 20.6 | 22.9 | 68.2 | 48.1 |
| C5 | 77.5 | 84.5 | 22.1 | 34.3 | 55.4 | 50.2 |
| C6 | 80.1 | 85.0 | 23.1 | 35.9 | 57.0 | 49.1 |
| C7 | 76.5 | 75.4 | 21.3 | 24.7 | 55.2 | 50.7 |
| C8 | 75.0 | 90.0 | 18.8 | 30.2 | 56.2 | 59.8 |
| C9 | 80.2 | 88.4 | 19.7 | 36.0 | 60.5 | 52.4 |
| Avg. | 74.6 | 81.0 | 20.6 | 31.1 | 54.0 | 49.9 |
| Std. Dev. | 11.5 | 6.40 | 3.20 | 4.80 | 9.90 | 4.70 |

As presented in Figure 6-4, no evident linear relationships between soil PCE concentrations and \% fine-grained materials were observed, with $\mathrm{R}^{2}$ values ranging between 0.33 and 0.57 . Furthermore, the correlation coefficients between these parameters did not indicate any strong correlation with coefficients of 0.75 between PCE concentration and \% Fines, 0.57 between PCE concentration and $\%$ Silt, and 0.69 between PCE concentration and $\%$ Clay. Given these analyses, soil grain size analysis was not included in the subsequent soil sampling events.


Figure 6-4. $\quad$ Soil PCE Concentration vs. Soil Grain Size (Baseline; 18.5 ft bgs)

Figure 6-5 below presents a comparison of soil CVOC concentrations at corresponding locations between the three (3) sampling events. The data presented in Figure 6-5 are arranged per individual locations and sampling depths. Overall, soil PCE concentrations of all samples collected from 18.5 ft bgs at the nine (9) locations within the TTA decreased by $78 \%$ (C6) to $99 \%$ (C3) from baseline to post-Stage 2, with an average decrease of $88 \%$. With the exceptions of C1 and C6, the decreases of PCE concentrations were already significant ( $75 \%$ at C8 to $99 \%$ at C3) from the baseline event to the post-Stage 1 event. Both C 1 and C 6 showed evident PCE decrease from the post-Stage 1 event to the post-Stage 2 event. It was also noted that while C6 was the only location with a significant baseline PCE concentration at 21 ft bgs ( $5.5 \mathrm{mg} / \mathrm{kg}$ ), the PCE concentration at 21 ft bgs of the C6 corresponding sampling location decreased to $0.21 \mathrm{mg} / \mathrm{kg}$ and below in subsequent post-operation sampling events.

Location C10 was in the general area of former Building 106 and approximately 35 ft from the upgradient edge of the TTA. No decreases in PCE concentrations were observed at C10 at 18.5 ft bgs or 21 ft bgs between the baseline and post-Stage 1 events. PCE concentrations declined at both depths at this location from the post-Stage 1 event to the post-Stage 2 event. While the reason for the decline is unclear and may be due to heterogeneity (attempts were made to repeat boreholes as close as possible to prior co-located borings), a slight increase in dichlorination intermediates was observed in the 18.5 ft bgs sample, suggesting some increase in biological activity in this area over time.

While the decreases in soil PCE concentrations over the Dem/Val are evident, significant, and generally consistent among all sampling locations within the TTA, there were no clear, corresponding increases of dechlorination intermediates in the soil samples. Additional assessment of the effects of EK-BIO remediation on soil quality is further discussed below based on soil microbial analysis.




Figure 6-5. Soil CVOC Data - Comparisons Between Events

### 6.3.2 Soil Microbial Analytical Results

Soil samples from all three (3) events were analyzed for multiple biomarkers: reductive dechlorination bacteria Dehalococcoides (Dhc) and functional genes for TCE and VC dechlorination. The analyses of all soil samples collected during the baseline and post-Stage 1 events did not detect any of these biomarkers above the detection limit ( $6 \mathrm{E}+03$ to $8 \mathrm{E}+03$ enumeration or gene copies per gram). Given the observed PCE distributions and the lack of biomarkers in the first two events, only the soil samples from 18.5 ft bgs from the post-Stage 2 event were submitted for biomarker analyses and the results are summarized in Table 6-9.

Table 6-9. $\quad$ Soil Microbial Analytical Data (Post-Stage 2 Samples; 18.5 ft bgs)

| Location / <br> Parameter | Dhc (baseline)* | vcrA | bvcA | tceA |
| :---: | :---: | :---: | :---: | :---: |
| C1 | $\begin{gathered} 2 \mathrm{E}+03 \mathrm{~J} \\ \text { (below } 8 \mathrm{E}+03 \text { ) } \end{gathered}$ | Below 7E+03 | Below 7E+03 | Below 7E+03 |
| C2 | $\begin{gathered} 7 \mathrm{E}+04 \\ \text { (below } 8 \mathrm{E}+03 \text { ) } \end{gathered}$ | $1 \mathrm{E}+04$ | $2 \mathrm{E}+04$ | 3E+03 J |
| C3 | $\begin{gathered} 9 \mathrm{E}+05 \\ \text { (below } 8 \mathrm{E}+03 \text { ) } \end{gathered}$ | $1 \mathrm{E}+05$ | $1 \mathrm{E}+05$ | $3 \mathrm{E}+05$ |
| C4 | $\begin{gathered} 7 \mathrm{E}+03 \\ \text { (below } 8 \mathrm{E}+03 \text { ) } \\ \hline \end{gathered}$ | Below 8E+03 | Below 8E+03 | Below 8E+03 |
| C5 | $\begin{gathered} 5 \mathrm{E}+04 \\ \text { (below } 8 \mathrm{E}+03 \text { ) } \end{gathered}$ | $4 \mathrm{E}+04$ | 2E+03 J | 7E+03 |
| C6 | Below 8E+03 | NA | NA | NA |
| C7 | $\begin{gathered} 4 \mathrm{E}+04 \\ \text { (below } 7 \mathrm{E}+03 \text { ) } \end{gathered}$ | Below 8E+03 | 1E+04 | Below 8E+03 |
| C8 | Below 7E+03 | NA | NA | NA |
| C9 | $\begin{gathered} 7 \mathrm{E}+03 \\ \text { (below 6E+03) } \end{gathered}$ | 1E+03 J | Below 7E+03 | Below 7E +03 |
| C10 | Below 8E+03 | NA | NA | NA |

* For the samples with detected Dhc, the baseline Dhc data were provided in ( ).

Dhc: Dehalococcoides (enumeration/gram); vcrA: VC Reductase (gene copies/gram)
bcvA : BAV1 VC Reductase (gene copies/gram) tceA : TCE Reductase (gene copied/gram)
J : Estimated quantity between the method detection limit and quantitation limit.
NA : Not applicable because Dhc was not detected.

Among the nine (9) post-Stage 2 samples from within the TAA, six (6) samples were reported with quantifiable levels, plus one with estimated level, of Dhc. Of these seven (7) samples with detected Dhc, five (5) samples, C2, C3, C5, C7, and C9, were detected with functional genes for VC dechlorination. Among all the locations within the TTA, location C3 appeared to have the most established Dhc populations with VC reductase genes, followed by locations C2 and C5.

It is noted that these are the locations in the interior of the TTA generally between supply wells and electrode well E5 which was an anode during both Stage 1 and Stage 2 operation. Electron donor would have been consistently migrating towards electrode well E5 during both Stages, and as such, it is not unexpected that the best electron donor availability and microbial growth would be detected in this area.

Overall, the soil sampling results presented in this section indicate that the EK-BIO operation resulted in significant decreases of PCE in clay soil across the TTA. The data also showed that microbial populations capable of reductive dechlorination of chlorinated ethenes, including VC, were established within the clay materials in at least part of the TTA.

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### 7.0 PERFORMANCE ASSESSMENT

This section provides an assessment of the performance of the Dem/Val relative to the performance objectives previously discussed in Section 3. Each subsection discusses the performance relative to an individual performance objective.

### 7.1 DEMONSTRATE UNIFORM DISTRIBUTION

The success criteria for this performance objective include:

## Criterion

At groundwater monitoring locations within the TTA, groundwater TOC is at least 5x baseline, or 10x detection limit if baseline is below detection.

As presented in Table 6-4, every monitoring well within the TTA had TOC concentrations $>8 \mathrm{x}$ baseline levels (for each well) during Stage 1 and/or Stage 2 operation, with the exception of EKMW-04 where the maximum TOC detected was 1.8x of the baseline. However, at EKMW-04 the maximum VFA detected was $>9 \mathrm{x}$ its baseline. With respect to VFAs, all but one monitoring well (EKMW-05) had concentrations >9x baseline levels. As such, the Dem/Val has met this criterion in the EK was able to substantially increase electron donor concentrations across the entire TTA. Of note, TOC concentrations were more than 100x average baseline levels in groundwater samples located between the supply wells and central anode (E5), indicating the electrode layout and electrical field design as important parameters in achieving optimal electron donor distribution across the TTA.

## Criterion

No local focusing of electric field within the TTA - no electrical potential gradient between any individual pair of cathode-anode is $5 x$ the average electrical gradient between all pairs of electrodes.

As presented in Figure 6-2, the voltage measured at discrete locations within the TTA were between 5.3 V and 6.2 V , with a standard deviation of 0.31 V ( $5 \%$ ). Voltage gradients were calculated between locations of closest pairs shown in Figure 6-2 and range between 0.1 to 0.26 $\mathrm{V} / \mathrm{m}$. The calculated voltage gradients between these pairs are within 3 x of each other and within 2 x of the average gradients $(0.13 \mathrm{~V} / \mathrm{m})$ indicating no local focusing of electric field within TTA. The Dem/Val has met this criterion.

## Criterion

Electrical potential gradient between electrode pairs maintained at level no more than 5x target gradient at design current.

The EK system was designed and operated at a constant current, determined after the start-up period, during the Dem/Val. As presented in Figure 6-1, during Stage 1 and Stage 2 operation, the voltage required of the power supply unit was generally consistent at between 15 V and 30 V , except for a few occasions when electrodes were in need of replacement. The electrical current supplied to individual wells during each stage of operation was generally steady (variation within $37 \%$ of average).

Given that (1) soil electrical resistivity is a soil property not expected to vary over the course of Dem/Val, and (2) the voltage output by the power supply unit and the current supplied to individual electrodes were generally steady, the electrical potential between electrode pairs within the TTA should maintain within 5 x of target during operation. The Dem/Val has met this criterion.

### 7.2 DEMONSTRATE TREATMENT EFFECTIVENESS

The success criteria for this performance objective include:

## Criterion

> 60\% reduction in average PCE concentrations in soil and groundwater within the TTA, with coupled and comparable molar concentration increases of dechlorination daughter and end products.

Figure 6-3 presents a comparison of groundwater CVOC and biomarker monitoring results. The \% decrease of PCE concentration and \% increases of concentrations of dechlorination daughter products and ethene from the baseline levels are summarized in Table 7-1.

Table 7-1. Changes of Groundwater CVOC and Ethene Concentrations*

|  | EKMW-01 |  | EKMW-02 |  | EMKW-03 |  | EKMW-04 |  | EKMW-05 |  | EKMW-07 |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Stage 1 | Stage <br> 2 | Stage <br> 1 | Stage <br> 2 | Stage 1 | Stage <br> 2 | Stage 1 | Stage <br> 2 | Stage 1 | Stage 2 | Stage <br> 1 | Stage <br> 2 |
| PCE <br> Decrease | 90\% | 95\% | 86\% | 74\% | 70\% | 83\% | 89\% | 72\% | 90\% | 67\% | 84\% | 93\% |
| Increase of Products | 310\% | 410\% | 65\% | -41\% | -13\% | -24\% | -18\% | -34\% | 160\% | 200\% | 140\% | 200\% |
| Increase <br> of <br> Ethene** | 14x | 84x | 58x | 47x | 30x | 26x | 11x | 3.8x | 1x | 1.6x | 13x | 22x |

* Calculations for each well are based on molar concentrations and comparing between Baseline to End-of-Stage 1 and Baseline to End-of-Stage 2. Calculations for increases of products include TCE, cis-1,2-DCE, VC, and ethene.

For each of the six monitoring wells located within the TTA, decreases of $>80 \%$ in PCE concentration were achieved at the end of either Stage 1 and/or Stage 2. Also presented in Figure 6-3 and Table 7-1, the decreases of PCE from baseline at each well within the TTA were coupled with evident increases of dechlorination daughter products and/or ethene. The Dem/Val has met this criterion for groundwater.

Figure 6-5 presents a comparison of soil CVOC at corresponding locations between the three (3) sampling events. The data presented in Figure 6-5 are arranged per individual locations and sampling depths. Overall, soil PCE concentrations of all samples collected from 18.5 ft bgs at the nine (9) locations within the TTA decreased by $78 \%$ (C6) to $99 \%$ (C3) from baseline to post-Stage 2 , with an average decrease of $88 \%$. It was also noted that while C6 was the only location with evident baseline PCE concentration at 21 ft bgs ( $5.5 \mathrm{mg} / \mathrm{kg}$ ), the PCE concentration at this depth and location decreased to $0.21 \mathrm{mg} / \mathrm{kg}$ ( $96 \%$ reduction) and below in subsequent post-operation sampling events. As such, the Dem/Val met the PCE soil reduction criterion.

While the decreases of soil PCE concentrations over the period of Dem/Val were evident, significant, and generally consistent among all sampling locations within the TTA, there were no corresponding increases of dechlorination intermediates in the soil samples. The reason for the general lack of intermediates in the soil samples is unclear, particularly since these degradation intermediates were clearly present in the groundwater samples. Thus, while this criterion was not clearly met for soils, this may not be an appropriate performance metric for the soils.

## Criterion

Ethene/ethane detected at > 75\% of groundwater monitoring wells within the TTA before the completion of post-EK monitoring.

As presented in Figure 6-3 and Table 7-1, every (100\%) monitoring well within the TTA showed increased concentrations of ethene (up to $>1,000 \mu \mathrm{~g} / \mathrm{L}$ ) during the Dem/Val. The Dem/Val has met this criterion.

## Criterion

> 10x increases of Dhc from baseline at >50\% of soil and groundwater samples collected from within the TTA before the completion of post-EK monitoring.

For the groundwater, Figure 6-3 shows that every monitoring well within the TTA showed significant increases (several orders of magnitude) of Dhc and $v c r A$. The Dem/Val has met this criterion for groundwater.

As presented in Table 6-9, among the nine post-Stage 2 soil samples collected from within the TAA, six samples were reported with quantifiable levels, plus one with estimated level, of Dhc, while all baseline soil samples did not contain detectable levels of Dhc. Of the seven samples with detected Dhc, five samples (C2, C3, C5, C7, and C9) showed functional genes for VC dechlorination. Thus, while not as impressive as the groundwater results, the Dem/Val has met this criterion for soil.

### 7.3 DEMONSTRATE SUITABILITY FOR FULL-SCALE IMPLEMENTATION

The success criteria for this performance objective include:

## Criterion

System operation conditions (voltage and current) within $\pm 50 \%$ of the designed target conditions.

The EK system was designed and operated at a constant current, determined after the start-up period, during the Dem/Val. As discussed in Section 7.1 (criterion related to electrical gradient) and presented in Figure 6-1, the operating voltage and current remained relatively steady except when electrodes were in need of replacement. There were three occasions when different electrodes needed to be replaced: late October/early November 2015 and late January/early February 2016 during Stage 1 operation; and December 2016 during Stage 2 operation. Prior to electrode replacement, the rising system voltage readings would indicate the operating conditions were becoming unsteady. As discussed in Section 6.1, excluding the temporary unstable readings during the three periods shortly before the electrode replacement, the overall system operation conditions were steady and within $50 \%$ of the average during each normal operation period. The Dem/Val has met this criterion.

## Criterion

## Amendment supply up-time $>75 \%$ of target.

Other than the scheduled major O\&M events between the two stages of operation, there were only three occasions when the system was shut down to allow replacement of electrodes. Overall, the system up-time was well $>75 \%$ during the Dem/Val. The Dem/Val has met this criterion.

## Criterion

## Energy consumption within $\pm 30 \%$ of design estimates.

The EK system was designed and operated at a constant current, determined after the start-up period, during Stage 1 and Stage 2 operation. Figure 6-1 presents cumulative energy consumption during each stage of operation. Given that the energy consumption is a function of voltage and current and as discussed above regarding the steady system operation condition criterion, excluding the temporary unstable voltage conditions during the three short periods before the electrode replacement, the overall system operations were steady and, thus, the energy usage as well. The Dem/Val has met this criterion.

### 7.4 SAFE AND RELIABLE OPERATION

The success criteria for this performance objective include:

## Criterion

Operation conditions remain stable within the normal designed ranges over the course of the demonstration period.
As discussed in Sections 7.1 and 7.3 above, the overall operation conditions remained relatively steady over the course of system operation. The Dem/Val has met this criterion.

## Criterion

No lost-time incidents.
There were no safety-related lost-time incidents. The Dem/Val has met this criterion.

### 7.5 EASE OF IMPLEMENTATION

The success criteria for this performance objective include:

## Criterion

Ability to construct using conventional techniques and contractors.
The Dem/Val involved only conventional field construction techniques, including well drilling, well installation, and trenching and piping, as well as remediation system assembly performed by regular, qualified subcontractors. The Dem/Val has met this criterion.

## Criterion

A single field technician is able to effectively monitor and maintain normal system operation.
During the operation, one field technician performed routine system O\&M tasks twice per week with approximately 2 to 3 hours per visit. During the routine O\&M visit, the tasks primarily included system visual inspections, recording the system operational parameters (voltage, current, amendment flow and pressure), and replenishing amendment solutions as needed. Other than sampling groundwater, there were fewer than 5 scheduled O\&M events that involved two field technicians. The Dem/Val has met this criterion.

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### 8.0 COST ASSESSMENT

This section provides cost information that a remediation professional could use to reasonably estimate the costs for implementing EK-BIO at a given site. The cost analysis is based on actual costs of the tasks completed for this Dem/Val, and supplemented with reasonable estimates based on team's experience from similar projects.

### 8.1 COST MODEL

Table 8-1 presents a summary of cost elements and the cost tracking. Select cost elements are briefly discussed.

Table 8-1. Cost Model for EK-enhanced Amendment Delivery In-Situ Remediation
(for a Source Area Measuring 35 ft by 35 ft by 5 ft Thick)

| Cost Element | Tracked During the Demonstration | Costs |
| :---: | :---: | :---: |
| Bench-scale EK tracer test | - Aquifer sediment materials provided by NAS Jacksonville. <br> - Laboratory bench-scale EK column tracer tests - $\$ 25 \mathrm{~K}$ | \$25K |
| Remedial Design | - System design and demonstration plan - professional labor \$80K | \$80K |
| Remediation Construction | - Well driller - 17 electrode/supply wells and 10 monitoring wells; \$40K <br> - EK system construction subcontractor - \$120K <br> - Site construction subcontractor - \$127K <br> - Field construction oversight and system shakedown professional labor (~ 7 weeks) - \$40K | \$327K |
| Baseline characterization | - Field staff labor - \$6K <br> - Laboratory analytical costs - $\$ 28 \mathrm{~K}$ | \$34K |
| Remediation System Operation \& Maintenance | - Field O\&M subcontractor - over 14 months of active operation, \$45K <br> - Materials - lactate, $\$ 6 \mathrm{~K}$ <br> - Materials - buffer and other chemicals, $\$ 3 \mathrm{~K}$ <br> - Materials - system parts \& consumables, $\$ 4 \mathrm{~K}$ <br> - Professional labor for startup and scheduled O\&M visits - $\$ 20 \mathrm{~K}$ | $\begin{gathered} 78 \mathrm{~K} \\ \text { (about } \\ \$ 6 \mathrm{~K} / \text { month) } \end{gathered}$ |
| Field Sampling (soil / <br> groundwater) | - 4 rounds of comprehensive sampling events and 4 rounds of limited scale sampling events <br> - Standard soil and groundwater sampling activities <br> - Field sampling staff labor (partially provided by NAS Jacksonville) <br> - Laboratory analytical costs (partially provided by NAS Jacksonville) | - |
| Waste disposal | - NAS Jacksonville provided waste disposal; no cost tracking | - |
|  <br> Other Compliance <br> Requirements | - Project reporting and meetings. | - |

## Cost Element - Bench-scale EK Column Testing

For this Dem/Val, the team conducted a bench-scale EK column tracer test to estimate the transport rate as a design basis. It is recommended that such bench-scale testing be considered as part of the remedial design for an EK-enhanced remedy. The scope of bench testing can vary depending on the test objectives. For example, the bench test can be designed to estimate EK transport rate only or to include assessment of treatment effectiveness facilitated by the enhanced amendment delivery, and the need for bioaugmentation. The costs of bench testing, therefore, vary based on the scope and objectives, but will typically range in cost between $\$ 15,000$ to $\$ 40,000$.

## Cost Element - Remediation Construction

For this Dem/Val, no special drilling or field construction methods were required. The EK system, including an amendment supply system, a power supply system, and electrolyte crosscirculation system, was constructed by a remediation system vendor in accordance with the project-specific design. No special equipment or parts, other than off-the-shelf commercial products, were required for the EK system. The electrodes and power supply unit were also commercially available products. The EK system construction costs will vary depending on the project scale (e.g. number of electrode wells needed to cover a treatment area, number of electrodes used, etc.) and site conditions (e.g., the extent of instrument automation due to site access, iron fouling and control measures due to geochemistry, etc.). However, the cost increase for expanding the EK system constructed for this Dem/Val will only be marginal, primarily related to additional parts (e.g., electrode (\$240 each), valves, and pipe fittings, etc.). The EK control center used for this Dem/Val could have been capable of incorporating up to 13 electrodes, thereby expanding the treatment footprint (on the electrode spacing used) by approximately $45 \%$.

## Cost Element - Remediation System Operation \& Maintenance

The system O\&M costs can vary depending on the extent of instrument automation and site conditions and restrictions. For this Dem/Val, routine O\&M tasks were performed by regular remediation field technicians without needing special personnel. The material costs for chemicals and system consumables are project-specific but generally scalable. Professional labor costs for this Dem/Val were related to initial system start-up operation and a system conditioning during the re-start transition from the end of Stage 1 incubation to Stage 2 operation.

### 8.2 COST DRIVERS

Based on the information and experience obtained from this Dem/Val, there are three main cost drivers to consider when evaluating implementation costs in future projects, including: (1) footprint, depth interval, and volume of target treatment zone and contaminant mass; (2) presence and location of above-ground and subsurface utilities; and (3) site geochemistry, particularly pH and iron. These are also the same cost drivers for many other in-situ remediation technologies and not unique to EK technology implementation. Each of these cost drivers is discussed below.

## Cost Driver - Target Treatment Zone and Contaminant Mass

As for most remediation technologies, the size and volume of the target treatment zone as well as the amount of contaminant requiring treatment significantly affects the overall remediation costs.

Particularly, the drilling and well installation costs for system wells (electrode wells and supply wells) vary based on the number and depth of these wells needed to adequately address the treatment zone. The spacing between electrode wells designed for this Dem/Val was approximately 18 ft , with supply wells located within the electrode well network. This level of well spacing, coupled with the phased operation program and the duration of operations, can be considered as within ranges of normal design for this technology. For this Dem/Val, active EK operation following bioaugmentation lasted approximately 10 months (two separate 5-month stages) and achieved an average soil PCE reduction of $88 \%$. The overall duration of an EK remedy implementation will depend on the contaminant mass and the required mass reduction goal.

While there is no technical limit for applying EK technology in terms of depth, the costs for well construction increase as the depth of target treatment zone. The depth interval (thickness) of target treatment zone may affect the number of electrodes within an electrode well and, therefore, the overall number of electrodes needed. A target treatment zone of shallow depth may need additional measures and costs related to utility protection as discussed below. This technology is suitable mainly in saturated formations; treatment within the vadose zone represents a challenge which is discussed in Section 9.

## Utilities

As with other active remediation technologies, a power source is required for this technology. Although not yet tested, the energy demand and the electrical operation conditions (voltage and current) demonstrated in this Dem/Val suggest that solar energy with battery units may be a feasible option.

Special considerations are warranted at sites with metallic subsurface infrastructure or subsurface utilities that may be electrically conductive. This evaluation should take into account the vertical separation of the electric field and the utility of concern. If needed, cathodic protection measures can be considered which can increase the implementation costs. In general, the EK technology is best suited for sites where the target treatment zone is deeper than 8 ft bgs (i.e., below utilities and conduits) and the groundwater table below 5 ft bgs, otherwise special design considerations are needed.

## Site Geochemistry

Concentrations of iron and other major cations (e.g., calcium and magnesium) in groundwater is an important factor that can affect the costs of system construction and O\&M. While this geochemical parameter is an important factor for most in-situ remediation technologies, it requires a special consideration when implementing an EK remedy because the electric field will result in, at least temporarily, concentrated iron and cations in cathode wells which attract cations in groundwater. The EK system for sites with elevated concentrations of these cations will need to be sized and equipped with adequate units for handling the anticipated amount of precipitates. More robust O\&M programs and efforts will also need to be considered for such sites. Over the course of implementation, the O\&M issues related to these do diminish.

### 8.3 COST ANALYSIS

For cost assessment, Table 8-2 provides a cost comparison between EK-BIO, conventional directinjection EISB, hydraulic fracturing DPT injection of ZVI, and electrical resistance heating (ERH) thermal treatment for a typical CVOC source site in low-K materials. The key characteristics of the framework site are as follows:

- The site characterization and conceptual site model have been completed. The characterization of the target treatment area is sufficient and no additional pre-design investigation data are needed to support the remedial design;
- The footprint of target treatment zone is approximately $80 \mathrm{ft} x 80 \mathrm{ft}$;
- The depth interval of target treatment zone is between 10 and 30 ft bgs ;
- Geology consisting of mainly fine-grained clayey material with low permeability (<1.0E$06 \mathrm{~cm} / \mathrm{sec}$ );
- CVOC mass (chlorinated ethenes) is approximately 500 lbs;
- Treatability testing is already completed to support bioremediation design. The site will require bioaugmentation of dechlorination cultures, which will completely dechlorinate target CVOCs to innocuous end product;
- The site has available potable water supply and adequate power utility; and
- No concerns for site access, subsurface obstruction, electrical interference or corrosion.

Table 8-2 presents estimated full-scale implementation costs and key assumptions associated with each technology on which the estimated costs are developed. Given that performance monitoring requirement is highly project-specific, the estimated costs are presented as with and without the costs for performance monitoring. These estimates are prepared at the level of a feasibility study (e.g., $+50 \% /-30 \%$ ) for a cleanup site.

For baseline comparison, the costs of excavation with offsite disposal was also estimated. The feasibility-level cost estimate for an excavation-disposal option is in the range of $\$ 1,300,000$ to $\$ 1,500,000$. One variable in cost estimation for excavation is the quantity of excavated soil that may need to be managed as hazardous waste. This can significantly increase the cost of this option.

Based on the cost estimates presented in Table 8-2, EK-BIO can be potentially more cost favorable to ERH remedy ( $\$ 688 \mathrm{~K}$ to $\$ 1,183 \mathrm{~K}$ before accounting for monitoring costs) and excavationdisposal. The cost saving of EK-BIO compared to ERH is smaller when factoring in the monitoring costs because ERH can complete the remediation within a shorter timeframe ( $\sim 6$ months with ERH compared to $\sim 2$ to 3 years with EK-BIO for the framework site). It is noted the significant difference in the electrical energy needed for these two technologies indicating a much more favorable environmental performance of EK-BIO over ERH.

The feasibility and effectiveness of direct-injection EISB approach is highly dependent on whether direct injection can achieve a reasonable injection rate and a reasonable radius of influence (ROI). For cost estimating purpose, an injection rate of 0.75 gpm to 1 gpm and a ROI of 7 ft are assumed.

The estimated costs for direct-injection EISB are presented in Table 8-2 as a range based on injection rates. It should be noted that it is possible that at certain low-K sites these assumed injection rates and ROI may not be achievable. As presented in Table 8-2, the estimated cost for EK-BIO approach is comparable to that of direct-injection EISB when factoring in the costs for reinjections (assumed two reinjections over five years). When further accounting the performance monitoring costs, which depends on the overall timeframe of individual remedy, EK-BIO is potentially a more cost favorable alternative to direct-injection EISB. Therefore, at sites where low-K material and/or high-degree of heterogeneity limits the feasibility of applying direct injection, EK-BIO provides a cost-effective solution for implementing in situ bioremediation.

Fracturing DPT injection has an overall estimated cost slightly higher than EK-BIO. Certain site conditions may present more constraints for fracturing DPT injection than EK-BIO, such as sensitive subsurface utilities, shallow treatment zone close to the ground surface, or oxidizing geochemical conditions requiring more site conditioning to facilitate reductive treatment. While fracturing DPT technology can enhance aquifer permeability, if a target treatment zone is in a heterogeneous formation, the fracturing technique may still result in non-uniform distribution of injected amendment. Alternately, the depth interval for fracturing will need to be reduced, with associated increased costs to achieve uniform distribution.

Table 8-2. Cost Model for Full-Scale Implementation of Select Source Area Remediation Technologies

| Cost Element | Tasks | Excavation Disposal | EK-BIO | Injection EISB | Hydraulic Fracturing ZVI <br> Injection | ERH | Descriptions / Assumptions |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Remedial Design and Permitting | Design, project workplans, UIC permit <br> ERH - also needs air permit, water discharge permit | \$50K | \$70K | \$50K | \$65K | \$80K | NA |
| Remedial Construction <br> (* Excavation-disposal and hydraulic fracturing ZVI injection costs presented only in Remediation System Operation \& Maintenance below) | EK-BIO - <br> 1. Well installations <br> 2. Site construction; utilities <br> 3. EK system \& control center fabrication / mobilization / field connections <br> 4. Professional field oversight and system shakedown/startup |  | 1. $\$ 53 \mathrm{~K}$ <br> 2. $\$ 140 \mathrm{~K}$ <br> 3. $\$ 160 \mathrm{~K}$ <br> 4. $\$ 60 \mathrm{~K}$ |  |  |  | - 25 electrode wells and 15 supply wells; all 4-inc PVC wells <br> - Electrode well spacing at $\sim 18 \mathrm{ft}$ <br> - Two electrodes vertically spaced in each electrode well <br> - One EK control / amendment supply system |
|  | Injection EISB - <br> 1. Well installations <br> 2. Site construction; utilities <br> 3. Injection system mobilization / field connections <br> 4. Professional field oversight and system shakedown/startup |  |  | 1. $\$ 70 \mathrm{~K}$ <br> 2. $\$ 35 \mathrm{~K}$ <br> 3. $\$ 20 \mathrm{~K}$ <br> 4. $\$ 40 \mathrm{~K}$ |  |  | - 49 injection wells; 2 -inch PVC wells <br> - Injection well spacing at $\sim 13 \mathrm{ft}$ <br> - Injection ROI at $\sim 7 \mathrm{ft}$ <br> - Up to three injection manifolds are constructed <br> - Area is accessible during injection, and no trenching is required |
|  | ERH - <br> 1. Well installations <br> 2. Site construction; utilities <br> 3. ERH system mobilization / field connection / system shakedown/startup <br> 4. Professional field oversight |  |  |  |  | 1. $\$ 92 \mathrm{~K}$ <br> 2. $\$ 180 \mathrm{~K}$ <br> 3. $\$ 190 \mathrm{~K}$ <br> 4. $\$ 60 \mathrm{~K}$ | - 25 electrode wells and 25 co-located vapor recovery wells <br> - Electrode well spacing at $\sim 18 \mathrm{ft}$ <br> - A surface cap will not be required <br> - Include a $20-\mathrm{hp}$ vapor extraction blower <br> - Adequate power supply is available for a $500-\mathrm{kW}$ power unit |
| Remediation System <br>  <br> Maintenance | Excavation with Off-site Disposal - <br> 1. Excavation <br> 2. Dewatering <br> 3. Off-site disposal of soil and water <br> 4. Backfill <br> 5. Professional field oversight | $\begin{aligned} & \$ 1,250 \mathrm{~K}- \\ & \$ 1,450 \mathrm{~K} \end{aligned}$ |  |  |  |  | - 7,000 CY excavated volume <br> - 150,000 gallons dewater volume <br> - $50 \%$ excavated volume as hazardous <br> - 25 miles to disposal facility |


| EK-BIO - <br> 1. Materials - chemicals <br> 2. Materials - parts and supplies <br> 3. Labor $-\mathrm{O} \& \mathrm{M}$ operator <br> 4. Labor-professional <br> 5. Utilities - water and electrical power |  | 1. $\$ 60 \mathrm{~K}-$ \$75K <br> 2. $\$ 25 \mathrm{~K}-$ \$40K <br> 3. $\$ 65 \mathrm{~K}-$ \$95K <br> 4. $\$ 50 \mathrm{~K}-$ \$75K <br> 5. $\$ 5 \mathrm{~K}-\$ 8 \mathrm{~K}$ |  |  |  | - Lactate as electron donor; also supply buffer and bioaugmentation culture <br> - Approximately up to 3A current between each pair of cathode and anode <br> - Four stages of operation over two years; each stage is four months of active EK operation followed by two months of incubation; alternate electric field orientation between each stage; a $3^{\text {rd }}$ year is assumed for contingency <br> - Less than $5,000 \mathrm{~kW}$-hr electrical energy required for EK operation <br> - Weekly visit by a system operator; up to three major O\&M events |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  | 1. $\$ 20 \mathrm{~K}$ to \$26K* <br> 2. $\$ 55 \mathrm{~K}$ <br> 3. $\$ 60 \mathrm{~K}$ to \$90K* <br> 4. $\$ 5 \mathrm{~K}$ <br> 5. $\$ 120 \mathrm{~K}$ to \$180K* x 2 events |  |  | - Emulsified vegetable oil (EVO) as the electron donor, also inject buffer and bioaugmentation culture <br> - Achievable injection rate from 1 gpm to 0.75 gpm <br> - Up to two re-injection events over a period of five years |
| DPT Hydraulic Fracturing ZVI <br> Injection - <br> 1. Injection vendor all labor/material inclusive costs <br> 2. Professional oversight |  |  |  | 1. $\$ 695 \mathrm{~K}$ to \$845K <br> 2. $\$ 30 \mathrm{~K}$ |  | - 25 DPT injection points; ROI $\sim 12 \mathrm{ft}$; spacing $\sim 20 \mathrm{ft}$ <br> - 7 fractures per DPT location $(\sim 3 \mathrm{ft}$ depth interval per fracturing) <br> - $1.5 \%$ wt ZVI to soil mass (total ZVI mass $=210,000 \mathrm{lbs}$ ) <br> - 20 to 25 days of field injection |
| ERH - <br> 1. System rental and system operator <br> 2. Labor - professional oversight <br> 3. Utilities - electrical power <br> 4. Permit monitoring (air and condensate) <br> 5. Waste (activated carbon) disposal |  |  |  |  | $\begin{array}{ll} \text { 1. } & \$ 360 \mathrm{~K} \\ \text { 2. } & \$ 24 \mathrm{~K} \\ \text { 3. } & \$ 114 \mathrm{~K} \\ \text { 4. } & \$ 30 \mathrm{~K} \\ \text { 5. } & \$ 53 \mathrm{~K} \end{array}$ | - Total heating time of 180 days <br> - Approximately $142,000 \mathrm{~kW}$-hr electrical energy needed <br> - Approximately $8,000 \mathrm{lb}$ of activated carbon for regeneration/disposal <br> - Vapor and condensate sampling and analysis in compliance with permits |
| Estimated Total (no performance monitoring costs) | $\begin{gathered} \$ 1,300 \mathrm{~K}- \\ \$ 1,500 \mathrm{~K} \end{gathered}$ | $\begin{gathered} \$ 688 \mathrm{~K}- \\ \$ 776 \mathrm{~K} \end{gathered}$ | $\$ 355 \mathrm{~K}$ to $\$ 386 \mathrm{~K}^{*}$ +2 reinjections $\$ 595 \mathrm{~K}$ to $\$ 746 \mathrm{~K}^{*}$ | $\begin{gathered} \$ 790 \mathrm{~K}- \\ \$ 940 \mathrm{~K} \end{gathered}$ | \$1,183K |  |


|  EK-BIO - <br> Semi-annual groundwater monitoring <br> for 3 to 4 years; Final soil sampling <br> Injection EISB - <br> Remediation <br> Performance <br> Monitoring <br> Semi-annual groundwater monitoring <br> for 5 years; Final soil sampling  <br> Hydraulic fracturing DPT ZVI  <br> Injection -  <br> Semi-annual groundwater monitoring  <br> for 3 years; Final soil sampling  <br> ERH -  <br> Two semi-annual groundwater  <br> following the active operation; Final  <br> soil sampling  |  | $\begin{aligned} & \$ 190 \mathrm{~K}- \\ & \$ 240 \mathrm{~K} \end{aligned}$ | \$290K | \$190K | \$90K | For costing purpose, assuming <br> $\$ 25 \mathrm{~K}$ per semi-annual groundwater monitoring event; <br> $\$ 40 \mathrm{~K}$ for final soil sampling event. |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Estimated Total (with performance monitoring costs) | $\begin{gathered} \$ 1,300 \mathrm{~K}- \\ \$ 1,500 \mathrm{~K} \end{gathered}$ | $\begin{aligned} & \$ 878 \mathrm{~K}- \\ & \$ 1,016 \mathrm{~K} \end{aligned}$ | $\underset{\$ 1,036 \mathrm{~K}^{*}}{\$ 885}$ | $\begin{aligned} & \$ 980 \mathrm{~K}- \\ & \$ 1,130 \mathrm{~K} \end{aligned}$ | \$1,273K |  |

### 9.0 IMPLEMENTATION ISSUES

EK-BIO is mainly a variation on standard EISB whereby EK is used to more effectively deliver the required amendments (electron donors, buffers and microbes) through low-K materials. As such, there are very few additional requirements or implementation issues that needed to be addressed beyond those typically encountered with a standard EISB implementation. Some areas where additional attention may be required, on a site-specific basis, include:

- Safety considerations related to potential stray current/voltage to surface. To address this question, we checked the current and voltage at the manhole steel cover located within the treatment area while the EK system was in operation to confirm that there was no safety concern. Depending on project site, and for sensitive and active facilities with dedicated safety departments, additional design and explanation effort may be required for project approvals.
- Iron fouling of filters and valves along the catholyte (well water from cathode wells) extraction line. In this Dem/Val, we re-plumbed the system to minimize potential flow restriction points. Scaling of the cathodes also required maintenance actions to clean the cathode surface. As indicated above, this issue diminished over the course of the Dem/Val.
- Corrosion of metallic parts in the manifold system \& wellhead fittings due to elevated chloride concentrations. In this Dem/Val, we replaced most metallic contacting parts with plastic parts upon discovering that chloride levels were far higher than initially known.
- The technology implementation did not require specialized/proprietary equipment. We used only standard commercial off-the-shelf equipment. We designed the manifold and control system and had a remediation system vendor assemble the system per design, but the overall system was similar to other "typical" in-situ remediation systems.
- If the technology is to be implemented near (laterally and/or vertically) utilities that are "sensitive" to electric interference or corrosion concerns, some protection measures, such as cathodic protection, may be considered.
- No special regulatory requirements or permits beyond what are typical for other EISB or ISCO projects such as UIC permit. Depending on the locality-/facility-specific requirements, local or facility power/electrical departments should be consulted.

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## APPENDIX A POINTS OF CONTACT

| Point of Contact <br> Name | Organization <br> Name <br> Address | Phone <br> Fax <br> Email | Role in Project |
| :---: | :---: | :---: | :---: |
| Evan Cox | Geosyntec Consultants, Guelph, ON, Canada | 519-514-2235 <br> ECox@Geosyntec.com | PI <br> Supervising the project |
| David Gent | US Army ERDC <br> Environmental Lab Vicksburg, MS | 601-634-4822 <br> David.B.Gent@usace.army.mil | Co-PI <br> Technical direction |
| James Wang | Geosyntec Consultants Columbia, MD | 410-910-7622 <br> JWang@Geosyntec.com | Performer <br> Technical design and execution |
| David Reynolds | Geosyntec Consultants Kingston, ON, Canada | 519-515-0883 DReynolds@Geosyntec.com | Performer Data analysis |
| Michael Singletary | NAVFAC Southeast Jacksonville, FL | $904-542-4204$ <br> Michael.a.singletary@navy.mil | Site coordination, technical review |

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## APPENDIX B TREATABILITY TEST MEMORANDUM

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# Geosyntec ${ }^{\triangleright}$ 

# Memorandum 

Subject: Results of Laboratory Testing of NAS Jacksonville Samples for Potential Application of Electrokinetic Remediation

ESAT TOA 601218

## BACKGROUND

Geosyntec Consultants Inc. (Geosyntec), in conjunction with Naval Facilities Engineering Command (NAVFAC) and the Army Engineer Research and Development Center (ERDC), submitted a proposal to ESTCP for pilot testing electrokinetic-enhanced remediation at Operable Unit 3 (OU3) NAS Jacksonville. To develop site-specific data supporting the preparation of the ESTCP proposal, soil samples were collected from the vicinity of proposed pilot test area at OU3, and sent to Geosyntec for bench-scale laboratory testing. The bench-scale testing was funded through a Rapid Response Task (task order number 601218-03). Geosyntec has developed this memorandum to document the test completed and report the test results.

## SCOPE OF WORK

The scope of work for the bench-scale electrokinetic (EK) testing program included the following tasks:

1) Mineralogical analysis of the supplied soil
2) Zeta potential testing of the supplied soil
3) Non-reactive tracer testing of the supplied soil

## RESULTS

## Mineralogical Analysis

A sample of the soil from NAS Jacksonville was sent to GR Petrology Consultants Inc. (GRP) in Calgary, Alberta, Canada for bulk and glycolated clay x-ray diffraction (XRD) analysis. The sample was found to contain $80.1 \%$ non-clay minerals and $19.9 \%$ clay minerals in the bulk XRD fraction. Quartz was the principal mineral detected, forming $61.3 \%$ of the bulk fraction. The high percentage of non-clay minerals is likely due to the selected subsample containing multiple sand grains, as the overall visual bulk soil was classified as sandy-clay.

NAS Jacksonville EK Bench-scale Testing
Page 2

The clay fraction was primarily composed of kaolinite ( $63 \%$ of the clay fraction), with smaller portions of illite, chlorite, and smectite.

## Zeta Potential Testing

A sample of the soil from NAS Jacksonville was sent to the University of Toronto for measurement of zeta potential. Zeta potential is a key parameter which in part controls the rate of electroosmosis of bulk water through soil pores under an applied electric potential. Two sets of measurements were performed at various pH values, the first (run 1) immediately after pH adjustment and the second (run 2) after the solutions had been allowed to equilibrate overnight. The results are presented in Figure 1.


Figure 1 - Zeta Potential Results

NAS Jacksonville EK Bench-scale Testing
Page 3

## Tracer Testing

A conservative tracer test was conducted on a $10-\mathrm{cm}$ long soil core using the EK testing apparatus (Figure 2). Under a process known as electromigration, anions and cations in bulk solution will migrate towards the oppositely charged electrode when an electrical potential is applied (independent of the effects of electroosmosis). Bromide was added to the cathode reservoir of the EKTA at a concentration of $1.0 \mathrm{~g} / \mathrm{L}$ (as NaBr ), and a constant current of 25 mA was applied to the soil core. The test was run for 72 hours. Following the test, the soil core was frozen and then sectioned into $1-\mathrm{cm}$ long increments. The samples were sent to Maxxam Analytics (Maxxam) for analysis of bromide concentrations in the soil. Table 1 presents the distribution of bromide in the soil as a function of distance from the cathode reservoir.


Figure 2 - EK Column Test Apparatus

Table 1 - Bromide Analytical Results in Samples Collected Along the Soil Column

| Sample | Background <br> Soil | 3-cm <br> from <br> cathode | 5-cm <br> from <br> cathode | 7-cm <br> from <br> cathode | 10-cm <br> from <br> cathode |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Bromide <br> $(\mathrm{mg} / \mathrm{kg})$ | $<1$ | 295 | 158 | 157 | 284 |

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## APPENDIX C BORING LOGS AND WELL CONSTRUCTION LOGS

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## WELL CONSTRUCTION LOG STANDARD FLUSH MOUNT

Well I.D.: $\quad$ s
Drilling Company: EDS
Driller(s): J.R., Mitch; seen
Geologist/Eng./Tech.: Bmu Zindyrof
Signature:


Site: NAS Jax
Project Number: TRO482
Installation Method:_HSA
Casing Installation Date:_10/15/14
Well Type: supply
Well Completion Method: flosh mount

## Well Completion

| Guard Posts (Y / N) Date: | $/ 7 \mid 14$ |  |
| :--- | :--- | :--- | :--- |
| Surface Pad Size: | 3 | $\mathrm{ftx} \frac{3}{\mathrm{St}}$ |

Protective Casing or Cover
Diameter/Type: $2^{\prime} \times 2^{\prime}$ stul vauit
Depth BGS: $\quad 2^{\prime}$ Weep Hole (Y/

## Grout

Composition/Proportions: pactland cenent type
Placement Method: $\qquad$
Seal Date: 10/15/14

Type: Pel-plug peatonite pellets
Source: $\quad 5$ gel buchet
Set-up/Hydration Time: 30 mm
Placement Method: drrect par
Vol. Fluid Added: $\frac{\text { no thid edded due to existing }}{\text { water in borehole }}$
Filter Pack
Type: 20/30 sillica sead, zolbs villea sand
Source: 50 it bags
Amount Used: 3 bags 20/30; 16 bag 30/65
Placement Method: tremmic pipe
Well Riser Pipe
Casing Material: schetwe 40 PVC
Casing Inside Diameters: $\qquad$ 4 $\qquad$ in.

## Screen

Material: chelure 40 PVC
Inside Diameter: 4
4
Screen Slot Size:: 0.010 in.
Percent Open Area: $\quad 0$
Sump or Bottom Cap ( $(\infty / \mathrm{N}$ )
Type/Length: cop / 0.25
Total Water Volume During Construction Introduced (Gal): 0 Recovered
(Gal): $\qquad$

## Reviewed

By:
Date: $\qquad$

## Comments

10/17114 13:25 Developient begins.~ ~20 gel milky brown to deer, then gues dy 10/20/14 $16: 11$ Developinent antinves. 28 gol clear

## WELL CONSTRUCTION LOG STANDARD FLUSH MOUNT

Well I.D.: $\qquad$
Drilling Company: EDS
Driller(s):


Geologist/Efig./Tech::Bunu Zinclegraf
Signature:


Site: $\qquad$
Project Number: TRO482
Installation Method: HSA
Casing Installation Date: $10 / 15 / 14$
Well Type: $\qquad$
Well Completion Method: fwoh mount

## Well Completion



## Protective Casing or Cover

Diameter/Type: $2^{\prime} \times 2^{\prime}$ steel vault
Depth BGS: 21 Weep Hole (Y/\$)

## Grout

Composition/Proportions: fortland cement type 1-
Placement Method: _remonic pupe


Filter Pack
Type: $20 / 30$ silica sand, $30 / 65$ sllice sond Source: 50 ib bags
Amount Used: 3 bags 20/30; 16 by $30 / 65$
Placement Method: tremmie plipe
Well Riser Pipe
Casing Material: schedrle 40 PVC
Casing Inside Diameters: $\qquad$ 4 $\qquad$ in.

## Screen

Material: schedre 40 PレC
Inside Diameter: 4
Screen Slot Size: $\quad 0.010$ in.

Percent Open Area: $\quad 0$
Sump or Bottom Cap ( $(\otimes / \mathrm{N}$ )
Type/Length:

## cop $/ 025^{\circ}$

| Total Water Volume During Construction |  |  |
| :--- | :--- | :--- |
| Introduced (Gal): | 0 | Recovered |
| (Gal): | 0 |  |
| Reviewed |  |  |
| By: |  |  |

By: Date: $\qquad$

## Comments

$10 / 17 / 14$ 13:05 Develwpiment begins. $\sim 18 \mathrm{gyt}$, Nillyy briwn to dear then gever dey $10 / 20 / 14$ 16:00 sevelepent cuntimes. $\sim 10$ gel clear.

## WELL CONSTRUCTION LOG <br> STANDARD FLUSH MOUNT

Well I.D.: $\quad 53$
Drilling Company: EDS
Driller(s): J.R., sean, Miteh
Geologist/Eng./Tech.: Bnqu Zinckgr. F
Signature:

Site: NAS Jox
Project Number: TROY\&2
Installation Method: HSA
Casing Installation Date: 10/15/14
Well Type: $\qquad$ suppy
Well Completion Method: flush mount

## Well Completion

Guard Posts (Y /
Surface Pad Size: $3 \quad \mathrm{ft} \mathrm{x} 3 \mathrm{ft}$

## Protective Casing or Cover

Diameter/Type: $2^{\prime} \times 2^{\prime}$ steal voult
Depth BGS: $\quad 2^{\prime}$ Weep Hole (Y/ ND

## Grout

Composition/Proportions: partiond cement type 1
Placement Method: $\qquad$


## Screen

Material: schoduce 40 pvc
Inside Diameter: 4

Screen Slot Size:: 0.010 in.
Percent Open Area: $\quad 0$
Sump or Bottom Cap ( $\triangle / \mathrm{N}$ )
Type/Length: cep / 0.25'
Total Water Volume During Construction Introduced (Gal): $\qquad$ Recovered (Gal): 0

## Reviewed

By: $\qquad$ Date: $\qquad$


## WELL CONSTRUCTION LOG <br> STANDARD FLUSH MOUNT



Site: NAS Jox
Project Number: TRO482
Installation Method: HSA
Casing Installation Date: $10 / 16 / 14$
Well Type: supди
Well Completion Method: Flush mount

## Well Completion

| Guard Posts (Y / D) Date: $\frac{11 / 7 / 14}{}$ |  |  |
| :--- | :--- | :--- | :--- |
| Surface Pad Size: |  |  |
| ft x | 3 | ft |

Surface Pad Size: _ 3 ft x $\quad 3 \quad \mathrm{ft}$

## Protective Casing or Cover

Diameter/Type: $2^{\prime} \times 2^{\prime}$ steel veuit Depth BGS: $\quad 2^{\prime} \quad$ Weep Hole (Y/

## Grout

Composition/Proportions: puthend cement type I
Placement Method: $\qquad$

Casing Material: sededele 40 PVC
Casing Inside Diameters: 4

## Screen

Material: $\frac{\text { cheerie } 40}{} \mathrm{PVC}$
Screen Slot Size:: $\quad 0.010$ in
Percent Open Area: $\quad 0$

Sump or Bottom Cap ( $\otimes / \mathrm{N}$ )
Type/Length: $\qquad$
Total Water Volume During Construction
Introduced (Gal): $\qquad$ Recovered
(Gal): $\qquad$
Reviewed
By:
Date: $\qquad$
Comments
1017 $10: 55$ Deaclopenent kegins. ~ 15 gel, withy bown to light bown, then goves dy 10120/14 14:30 Development continves. ~ 10 gal, lisht 6.0win to clear. Devzelopment ends.

## WELL CONSTRUCTION LOG <br> STANDARD FLUSH MOUNT



Site: NAS Tav
Project Number: TRO 482
Installation Method: HSA
Casing Installation Date: $10 / 15 / 14$
Well Type: supply
Well Completion Method:_fwosh mosat

## Well Completion

Guard Posts ( Y /
Surface Pad Size:
(N)

## Protective Casing or Cover

Diameter/Type: $2^{\prime \prime} \times 2^{\prime}$ stal voult
Depth BGS: $\quad 2^{\prime} \quad$ Weep Hole (Y/ $\Delta$ )

## Grout

Composition/Proportions: partiond cement type 1

Placement Method: $\qquad$
Well Riser Pipe
Casing Material: $\qquad$ schatuce 40 PVC
Casing Inside Diameters: $\qquad$ 4 $\qquad$ in.
Screen
Material: sudule 40 pve
Inside Diameter: 4
Screen Slot Size:: 0.010 in.
Percent Open Area: $\quad 0$

Sump or Bottom Cap ( $8 / \mathrm{N}$ )
Type/Length: $\qquad$

| Total Water Volume During Construction |  |
| :--- | :--- |
| Introduced (Gal): $\quad 0$ | Recovered |
| (Gal): $\quad 0$ |  |
| Reviewed |  |
| By:_ |  |

$\qquad$

## Comments

i0/17/14 11:23 Development bagins. ~ 12 gal , milky bown to light brown, then gues dy 10120/14 15:12 Development contimes $\sim 10 \mathrm{gal}$, light baun to clear. Dexchopunt ends.

## WELL CONSTRUCTION LOG <br> STANDARD FLUSH MOUNT

Well I.D.: $\quad 56$
Drilling Company: EDS
Driller(s): J. R, Mitch, sean
Geologist/Eng./Tech.: Byee Zindegrf
Signature:


Site: $\qquad$
Project Number: TRO482
Installation Method:_HSA
Casing Installation Date: $10 / 16 / 14$
Well Type: supply
Well Completion Method: fwsh mout

Well Completion


## Protective Casing or Cover

Diameter/Type: $2^{\prime} \times 2^{\prime}$ steel voult
Depth BGS: $\quad 2^{\prime}$ Weep Hole (Y/ (N)
Grout
Composition/Proportions: pertiand ceant have 1
Placement Method: tramene pre
Seal
Date:
Type: Pel-plog Bentonite peluets
Source: 5 gel buckent
Set-up/Hydration Time: 30 min
Placement Method: $\qquad$


## Filter Pack

Type: 20130 siliza end $30 / 65$ stiven sand

Source: 50 U. begs
Amount Used: 3 6ags $20 / 30,1 \mathrm{tag} 30 / 65$
Placement Method: tremmic pype
Well Riser Pipe
Casing Material: Scheduh 40 pve
Casing Inside Diameters: $\quad 4$
Screen
Material: $\frac{\text { schoelole } 40 \text { PVC }}{\text { Inside Diameter: } 4} 4$ in.

Screen Slot Size:: 0010 in.
Percent Open Area: _o

Sump or Bottom Cap ( $\Phi / \mathrm{N}$ )
Type/Length: ${ }^{32}$ cap $/ 0.25^{\prime}$
Total Water Volume During Construction
Introduced (Gal): 0 Recovered
(Gal): $\quad 0$

## Reviewed

By: $\qquad$ Date: $\qquad$
10./17114 10:32 Dewdopiment 6egins. ~ 12 gyls, milky brown to light brown then goas dyy 1012011413.46 Develupivent continves. $\approx 15 \mathrm{goy}$, light b.own to dear Developpreat ends.

## WELL CONSTRUCTION LOG STANDARD FLUSH MOUNT

| Well I.D.: 57 |
| :---: |
| Drilling Company: EDS |
| Driller(s): TR, mitch; seen |
| Geologist/Eng./Tech.: Buce Zinder.f |
| Signature: $\qquad$ 361 |

Site: $\qquad$
Project Number: TRO482
Installation Method: ASA
Casing Installation Date:___10/16/14
Well Type: $\qquad$
Well Completion Method:_ flush mount

## Well Completion

Guard Posts (Y / $11 / 7 / 14$

Surface Pad Size: $\qquad$
Protective Casing or Cover
Diameter/Type: $2^{\prime} \times 2^{\prime}$ steal vail
Depth BGS: __ $2^{\prime \prime}$ Weep Hole (Y/ (D)

## Grout

Composition/Proportions: pattend uent tyee 1
Placement Method: $\qquad$


## Comments

Ground Surface


By: $\qquad$ Date: $\qquad$

10/17/14 i0:10 Developpent iegins. च 12 gal, dark millyy bown to dear, then goes dey


## WELL CONSTRUCTION LOG <br> STANDARD FLUSH MOUNT

Well I.D.:
Drilling Company: EDS
Driller(s):


Geologist/Eng./Tech.:-Bque Zindeg. F
Signature:


Site: $\qquad$
Project Number: TROH 82
Installation Method: HSA
Casing Installation Date: $10 / 16 / 14$
Well Type: $\qquad$
Well Completion Method: flush mount

## Well Completion

Guard Posts (Y/N) Date: い ( ) / M
Surface Pad Size: $\qquad$ ft x $\qquad$ ft

## Protective Casing or Cover

Diameter/Type: $2^{\prime} \times 2^{\prime}$ stecl vault
Depth BGS: $\quad z^{\prime}$ Weep Hole (Y/ D)

## Grout

Composition/Proportions: portend cavent tyme I
Placement Method: $\qquad$

| Seal | Date: $10 / 16 / 14$ |
| :---: | :---: |
| Type: Pel-pwg Beatonite Seal |  |

Source: $\frac{5}{}$, buchet
Set-up/Hydration Time: $\qquad$
Placement Method: $\qquad$
Vol. Fluid Added: $\qquad$
Filter Pack
Type: 20/30 stlica sedi $30 / 65$ silica send

Source: $\frac{5016 \text { beys }}{}$
Amount Used: $3 \mathrm{begs} 20130,16 \mathrm{geg} 30 / 65$
Placement Method: tremmie phe

## Well Riser Pipe

Casing Material: | seledwle 40 pve |
| :--- |
| Casing Inside Diameters: 4 |$\quad$ in.

## Screen

Material: sehadule 40 PVC
Inside Diameter: $\quad 4$
Screen Slot Size:: $\quad 0.010$ in.
Percent Open Area: $\quad 0$

Sump or Bottom Cap ( $8 / \mathrm{N}$ )
Type/Length: cap / 0.25'
Total Water Volume During Construction
Introduced (Gal): $\qquad$ Recovered
(Gal): $\qquad$
Reviewed
By:
Date: $\qquad$


## Comments

 10/20/14 i7:08 Developunt continves. ~ 10 gal , light brown to clear

## WELL CONSTRUCTION LOG STANDARD FLUSH MOUNT



Site: NAS Jax
Project Number: TRO482
Installation Method: MSA
Casing Installation Date:_10/14/14
Well Type:_ electrode
Well Completion Method: fwith mount

## Well Completion

Guard Posts (Y / D) Date: $\frac{11 / 7 \mid 14}{} \begin{aligned} & \text { St x } 3 \\ & \text { Surface Pad Size: } \\ & 3\end{aligned} \quad \mathrm{ft}$

## Protective Casing or Cover

Diameter/Type: $z^{\prime} \times 2^{\prime}$ steel voult
Depth BGS: $\quad 2^{\prime}$ Weep Hole ( $\left.\mathrm{Y} / \Phi\right)$
Grout
Composition/Proportions: portiand cement type 1-
Placement Method: $\qquad$
Seal
Type: Pel-plog Bentonite peluts $10 / 14 / 14$
Date

Source: 5 gel buchet
Set-up/Hydration Time: 30 min
Placement Method: sirect pour
Vol. Fluid Added: on flid added the to existing
Filter Pack
Type: 20/30 cilica condi $30 / 65$ silica sand
Source: 50 ib bags
Amount Used: 3 begs 20/30; $16 \mathrm{gy} 30 / 65$
Placement Method:
tremmie pipe
Well Riser Pipe
Casing Material: _scheolule 40 PVC
Casing Inside Diameters: $\qquad$ in.
Screen
Material: $\frac{\text { schecule }}{} 40 \mathrm{PVC}$
Inside Diameter: $\quad 4$
in.
Screen Slot Size:: 0.010 in.
Percent Open Area: $\quad 0$

Sump or Bottom Cap ( $\varnothing / \mathrm{N}$ )
Type/Length: cop / $0.25^{\prime}$

| Total Water Volume During Construction |  |  |
| :--- | :--- | :--- |
| Introduced (Gal): | 0 | Recovered |
| (Gal): | 0 |  |
| Reviewed |  |  |
| By: |  |  |

## Comments

Ground Surface

io117/14 14:50 Development byens. $\sim 20$ gal

By.
By

## WELL CONSTRUCTION LOG <br> STANDARD FLUSH MOUNT

Well I.D.: E2
Drilling Company: EDS
Driller(s): J.R., seen, with
Geologist/Eng./Tech.: Bque Zinckgraf
Signature:


Site: NAS Jax
Project Number: TRO482
Installation Method: HSA
Casing Installation Date: $\qquad$
Well Type: Euctrode
Well Completion Method: fwsh mount

## Well Completion



## Protective Casing or Cover

Diameter/Type: $2^{\prime} \times 2^{\prime}$ sicel vait
Depth BGS: $\quad 2^{\prime}$ Weep Hole ( $\mathrm{Y} / \mathbb{\otimes}$ )

## Grout

Composition/Proportions: portiend cement type 1
Placement Method: tremmie pipe

| Seal | Date: $10 / 14 / 14$ |
| :---: | :---: |
| Type | Bentorite pellets |
| Sour | bucte |

Set-up/Hydration Time: 30 man
Placement Method: direct parr
Vol. Fluid Added: ©o flid celded due to existing water
Filter Pack
Type: 20/30 stlice sead; 30/65 silica sand
Source: 50 is bags
Amount Used: 4 begs 20/30; 1 heg $30 / 65$
Placement Method:
tremanie pipe
Well Riser Pipe
Casing Material: schedule 40 PVC
Casing Inside Diameters: $\quad 4$ in
Screen
Material: scheowle 40 PVC
Inside Diameter: 4 in.
Screen Slot Size:: 0.010 in.

Percent Open Area: $\quad 0$
Sump or Bottom Cap ( $\varnothing / \mathrm{N}$ )
Type/Length: cop / 0.25
Total Water Volume During Construction
Introduced (Gal): $\frac{0}{0}$ Recovered
(Gal):
Reviewed

By: $\qquad$ Date: $\qquad$ 10/20/14 16:32 Develpaent continves. 210 goi, cleer

## WELL CONSTRUCTION LOG STANDARD FLUSH MOUNT

Well I.D.: E3
Drilling Company: EDS
Driller(s) $\qquad$
Geologist/Eng./Tech.: Bmu Zinalgraf
Signature:


Site: NAS Jux
Project Number: TROY82
Installation Method: HSA
Casing Installation Date: $10 / 14 / 14$
Well Type: Electrode
Well Completion Method: fivis mount

## Well Completion



## Protective Casing or Cover

Diameter/Type: $z^{\prime} \times 2^{\prime}$ steel vart Depth BGS: $\quad z^{\prime}$ Weep Hole (Y/ ©)

## Grout

Composition/Proportions: portind cement bype I
Placement Method: $\qquad$
Sea
Date: $10 / 14 / 14$

Casing Inside Diameters: 4 in.

## Screen

Material: _scheevke 40 PVC
Inside Diameter: $\frac{4}{}$ in
Screen Slot Size:: 0.010 in.

Percent Open Area: $\quad 0$
Sump or Bottom Cap ( $\delta / \mathrm{N}$ )
Type/Length:
cap $10.25^{\prime}$
Total Water Volume During Construction
Introduced (Gal): _ O Recovered
(Gal): $\quad 0$
Reviewed
By: $\qquad$ Date: $\qquad$ io/i7/14 14:05 Sevelopment begins. $\sim 22 \mathrm{gal}$ milly bown to cher Development ends.
$\qquad$
$\qquad$

## WELL CONSTRUCTION LOG STANDARD FLUSH MOUNT

Well I.D.: $\qquad$
Drilling Company: EDS
Driller(s): JR, Mitch, seen
Geologist/Eng./Tech.: Bye Zinckgr of
Signature:


Site: $\qquad$
Project Number:TRO48,7
Installation Method: HSA
Casing Installation Date: $\quad 10 / 16 / 14$
Well Type:

- electroda

Well Completion Method: flush momt

Well Completion
Guard Posts (Y / D ) Date: _1/フ/14 Surface Pad Size: 3

## Protective Casing or Cover


Depth BGS: $\quad 2^{\prime}$ Weep Hole (Y/ (N)

## Grout

Composition/Proportions: partind cement type 1


## Filter Pack

Type: 20/30 slied sand; 30/65 whea send
Source: 50 ib begs
Amount Used: 3 bogs $20 / 30 ; 16 \mathrm{yg} 30 / 65$
Placement Method: tremmic pipe
Well Riser Pipe
Casing Material: Scheale 40 pue
Casing Inside Diameters: $\qquad$ 4 in.
Screen
$\qquad$
Inside Diameter: 4 in
Screen Slot Size:: 0.010 in.
Percent Open Area: $\quad 0$
Sump or Bottom Cap ( $\Phi / \mathrm{N}$ )
Type/Length: $\qquad$
Total Water Volume During Construction Introduced (Gal): _ o Recovered
(Gal): $\qquad$

## Reviewed

By: $\qquad$ Date: $\qquad$

10/17114 10:45 Dreelupment begins. $\sim 8$ gel milky brown then gues dyy 10i20/14 14:05 Develepment continves. ~ i5 gel, light boinn to elear. Developent ends.

## WELL CONSTRUCTION LOG <br> STANDARD FLUSH MOUNT

Well I.D.: $\qquad$ E5
Drilling Company: EDS
Driller(s): J.R., Mitch, Sear
Geologist/\&ng./Tech.: Bnqu ZindegraF
Signature:


Site: $\qquad$ NAS Jax
Project Number: TRO482
Installation Method: $\qquad$
Casing Installation Date: $\qquad$ $10 / 16 / \mathrm{m}$
Well Type: electrode
Well Completion Method $\qquad$

## Well Completion



## Protective Casing or Cover

Diameter/Type: $2^{\prime} \times 2^{\prime}$ steal voutt
Depth BGS: $2^{\prime} \quad$ Weep Hole (Y/

## Grout

Composition/Proportions: $\qquad$
Placement Method: $\qquad$
Sea
Date: $10 / 16 / 14$
Type: Pel-plug Bentorite Pellets
Source: 5 ouckets
Set-up/Hydration Time: 30 mm
Placement Method: $\qquad$
Vol. Fluid Added:


Filter Pack
Type: $20 / 30$ silice sand; $30 / 65$ silice send
Source: 5016 6ege
Amount Used: 3 beys $20130 ; 16$ y 30165
Placement Method: remmes ape
Well Riser Pipe
Casing Material: $\quad$ scheewhe 40 PVC
Casing Inside Diameters: $\qquad$ in.
Screen
Material: schence 40 PVC
Inside Diameter: 4
Screen Slot Size:: 0.010 in.
Percent Open Area: 0

Sump or Bottom Cap ( $\varnothing / \mathrm{N}$ )
Type/Length: $\qquad$
Total Water Volume During Construction
Introduced (Gal)
0 Recovered
(Gal):


## Reviewed

By: $\qquad$ Date: $\qquad$


## WELL CONSTRUCTION LOG <br> STANDARD FLUSH MOUNT

Site: NAS Jaw

Well Completion Method: fwosh mom


Project Number: TRO 482
Installation Method: HSA
Casing Installation Date: $10 / 25 / \mathrm{m}$
Well Type: electrode

Well Completion

| Guard Posts (Y / Date: | $/ 7 / 14$ |
| :--- | :--- | :--- |
| Surface Pad Size: | 3 |

## Protective Casing or Cover

Diameter/Type: $2^{\prime} \times 2^{\prime}$ steel verit
Depth BGS: $\quad 2^{\prime} \quad$ Weep Hole ( $\mathrm{Y} / \Phi$ )

## Grout

Composition/Proportions: partlend ceavent type 1
Placement Method: $\qquad$

Casing Material: sehedule 40 Puc
Casing Inside Diameters: 4


Percent Open Area: 0
Sump or Bottom Cap $(\nabla / \mathrm{N})$
Type/Length: sop / 0.25'

| Introduced (Gal): 0 | Recovered |
| :---: | :---: |
| (Gal): 0 |  |
| Reviewed |  |
| By: | Date: |

By: Date: $\qquad$

## Comments

10177/14 11.44 Developient begins. $\sim 8 \mathrm{gai}$, miltay brown to light brown, then goes dyy Lo/20/14 15:25 Develperent continves. ~ 20 gel, 1 git bown to cuar.

## WELL CONSTRUCTION LOG STANDARD FLUSH MOUNT

Well I.D.: $\qquad$ E7
Drilling Company: EDS
Driller(s):


Geologist/Eigg./Tech.:-Buque Zunclegr. F
Signature:


Site: $\qquad$
Project Number:_TRO482
Installation Method: HSA
Casing Installation Date:_10/17/14
Well Type: electrode
Well Completion Method: fwish mount

## Well Completion

 Protective Casing or Cover Diameter/Type: $2^{\prime} \times 2^{\prime}$ steal vait Depth BGS: $2^{\prime}$ Weep Hole ( $\mathrm{Y} / \mathbb{N}$ )

## Grout

Composition/Proportions: partiond cement type 1
Placement Method: $\qquad$

| Seal | Date: $10 / 17 / 14$ |
| :--- | :--- |
| Type: Pel-Pluy Bentanite Pellets |  |
| Source: $\frac{5}{}$ gol buekets |  |

Set-up/Hydration Time: 30 min
Placement Method: direct par
Vol. Fluid Added: $\frac{\text { no fluid added due to enis/ang }}{\text { water in borehoce }}$
Filter Pack
Type: $20 / 30$ rilico sandi 30165 silicen sand
Source: 50 t bags
Amount Used: 3 lags $20 / 30$; 1 bay $30 / 65$
Placement Method: tremmic pipe
Well Riser Pipe
Casing Material: schelve 40 PVC
Casing Inside Diameters $\qquad$ in.
Screen
Material: $\frac{\text { sedudule } 40 \text { PVC }}{\text { Inside Diameter: } 4} 4$. in
Screen Slot Size:: 0.010 in.
Percent Open Area: $\quad 0$
Sump or Bottom Cap ( $/ \mathrm{N}$ )
Type/Length: cap / 0.25
Total Water Volume During Construction
Introduced (Gal): $\qquad$ Recovered
(Gal):

## Reviewed

By: $\qquad$ Date: $\qquad$


## WELL CONSTRUCTION LOG STANDARD FLUSH MOUNT

Well I．D．：F8
Drilling Company：EOS
Driller（s）：J．R．，Mitch，seen
Geologist／Eng／Tech．：Bince Zinckgr．F
Signature：


Site：NAS Jax
Project Number：＿TRO482
Installation Method：HS A
Casing Installation Date： $10 / 17 / 14$
Well Type：＿electrode
Well Completion Method：swoh mount

## Well Completion

Guard Posts（Y／N）Date：い17／14
Surface Pad Size： $3 \quad \mathrm{ftx} 3 \mathrm{~K}^{\mathrm{ft}}$

## Protective Casing or Cover

Diameter／Type： $2^{\prime \prime} \times 2^{\prime}$ sheel voult
Depth BGS：$\quad 2^{\prime}$ Weep Hole（Y／$⿴ 囗 十$

## Grout

Composition／Proportions：partind cereat bype 1
Placement Method：tremmie pipe
Seal Date： $10 / 17 / 14$

Type：Pel－Plug Bentorate pellets
Source： 5 gel buthet
Set－up／Hydration Time： 30 ．．．n
Placement Method：direet pour
Vol．Fluid Added：no fincd codoled due to ekesting－

## Filter Pack

Type：20／30 silica sand； $30 / 65$ sitico send Source： 50 it lage
Amount Used： 3 logs 20／30； $1 \operatorname{lng} 30 / 65$
Placement Method：tremmic pipe

## Well Riser Pipe

Casing Material：scheedule 40 PVC
Casing Inside Diameters： $\qquad$ 4

## Screen

Material：schedule 40 PVC
Inside Diameter： 4 in
Screen Slot Size：： 0.010 in．

Percent Open Area： 0
Sump or Bottom Cap（ $\triangle / \mathrm{N}$ ）
Type／Length：cap／0．25＇
Total Water Volume During Construction
Introduced（Gal）： $\qquad$ Recovered
（Gal）：

## Reviewed

By： $\qquad$ Date： $\qquad$
 i0／20／k4 $16: 54$ sevelop．unt cantinvei．$\sim 7$ gel puapedi lisht brown to cleari then dyy

## WELL CONSTRUCTION LOG STANDARD FLUSH MOUNT

Well I．D．：Eq
Drilling Company：EDS
Driller（s）：J．R．，Seen，Mitch
Geologist／Eng／Tech．：Bryce Zuncho－F
Signature：


Site：NAS Jax
Project Number：TRO482
Installation Method：HSA
Casing Installation Date： 10 ／17／14
Well Type：electrode
Well Completion Method：fwih mount

## Well Completion

Guard Posts（Y／N）Date：いいつ／14
Surface Pad Size： 3 ft x $\quad 3 \quad \mathrm{ft}$
Protective Casing or Cover
Diameter／Type： $2^{\prime} \times 2^{\prime}$ steel voult
Depth BGS：$\quad 2^{\prime}$ Weep Hole（Y／©）

## Grout

Composition／Proportions：portlond cement tyrea 1
Placement Method：treamie pipe
Seal Date： $10 / 17 / 14$
Type：Pel－Plug Bentonite Pelets
Source： 5 gel buivect
Set－up／Hydration Time： $30 \min$
Placement Method：direct pur
Vol．Fluid Added：
no fivid odeled ave io exishing
Filter Pack waser in borenole
Type： $20 / 30$ sliea send； $30 / 65$ sitice sand
Source： 50 it langs
Amount Used： 3 begs $20 / 30$ ； 1 beg 30165
Placement Method：tremmie pipe
Well Riser Pipe
Casing Material：＿scherwie 40 PVC
Casing Inside Diameters： $\qquad$ in．

## Screen

Material： $\qquad$ schedule 40 PVC
Inside Diameter： 4
Screen Slot Size：： 0.010 in．
Percent Open Area：$\quad 0$
Sump or Bottom Cap（ $\overline{/} / \mathrm{N}$ ）
Type／Length：cop／0．25＇
Total Water Volume During Construction
Introduced（ Gal ）： $\qquad$ Recovered
（Gal）： $\qquad$

## Reviewed

By： $\qquad$ Date： $\qquad$


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## APPENDIX D GROUNDWATER SAMPLING FORMS

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## GROUNDWATER SAMPLING LOG

| SITE <br> NAME： NAS JOX | SITE | LOCATION：Jacksonville，FL |  |  |
| :--- | :--- | :--- | :--- | :--- | :--- |
| WELL NO： | EKMW－O1 | SAMPLEID： | EKMW－O1 | DATE： $10101 / 2014$ |

## PURGING DATA



## SAMPLING DATA

| SAMPLED BY（PRINT）／AFFILIATION： Bipu Zinckgraf／Geosyntec |  |  |  |  |  |  | SAMPLING <br> Initiated at：09：35 | SAMPLING <br> ENDEDAT：09：リて |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| PUMP OR TUBING DEPTH IN WELL（feet）： |  | 20.5 |  |  |  | FIELD－FILTERED：Y ©D Filtration Equipment Type： |  | FILTER SIZE：＿＿＿$\mu \mathrm{m}$ |  |
| FIELD DECONTAMINATION： |  |  | PUMP Y $\triangle$ | TUBING $Y$ N（treplaced） |  |  | DUPLICATE： | ND |  |
| SAMPLE CONTAINER SPECIFICATION |  |  |  | SAMPLE PRESERVATION |  |  | INTENDED ANALYSIS AND／OR METHOD | SAMPLING EQUIPMENT CODE | SAMPLE PUMP FLOW RATE （mL per minute） |
| $\begin{aligned} & \text { SAMPLE } \\ & \text { IDCOE } \end{aligned}$ | $\begin{gathered} \# \\ \text { CONTAINERS } \\ \hline \end{gathered}$ | $\begin{gathered} \text { MATERIAL } \\ \text { CODE } \end{gathered}$ | VOLUME | $\begin{gathered} \hline \text { PRESERVATIVE } \\ \text { USED } \\ \hline \end{gathered}$ | $\begin{gathered} \text { TOTAL VOL } \\ \text { ADDED IN FIELD }(\mathrm{mL}) \\ \hline \end{gathered}$ | $\begin{gathered} \text { FINAL } \\ \mathrm{pH} \\ \hline \end{gathered}$ |  |  |  |
| EKMW－O | 1 | PE | $1 し$ | none | － | － | Gene Trac | APP | $<100$ |
| ＂ | 2 | CG | 40 mL | nome | － | － | VFAS | APP | $\angle 100$ |
| ＂ | 3 | C G | 40 ml | nune | － | － | $\mathrm{DHG}_{5}$ | APP | ＜100 |
| ＂ | 1 | PE | 250 ml | $\mathrm{HNO}_{3}$ | － | － | metals | APP | $<100$ |
| ＂ | 1 | PE | 150 mL | none | － | － | anions | APP | 100 |
| ＂ | 1 | PE | 150 mL | nowe | － | － | lodide | APP | ＜100 |

REMARKS：

> MATERIAL CODES: $\quad \mathrm{AG}=$ Amber Glass; $\quad \mathrm{CG}=$ Clear Glass; $\quad \mathrm{PE}=$ Polyethylene; $\quad \mathrm{PP}=$ Polypropylene; $\quad \mathrm{S}=$ Silicone; $\quad \mathrm{T}=$ Teflon; $\quad \mathrm{O}=$ Other (Specify) SAMPLING EQUIPMENT CODES: APP = After Peristaltic Pump; B = Bailer; BP = Bladder Pump; ESP = Electric Submersible Pump; RFPP = Reverse Flow Peristaltic Pump; $\quad$ SM $=$ Straw Method (Tubing Gravity Drain); $\quad \mathbf{O}=$ Other (Specify)

NOTES：1．The above do not constitute all of the information required by Chapter 62－160，F．A．C．
2．STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS（SEE FS 2212，SECTION 3）
$\mathrm{pH}: \pm 0.2$ units Temperature：$\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance：$\pm 5 \%$ Dissolved Oxygen：all readings $\leq 20 \%$ saturation（see Table FS 2200－2）； optionally，$\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$（whichever is greater）Turbidity：all readings $\leq 20$ NTU ；optionally $\pm 5$ NTU or $\pm 10 \%$（whichever is greater）

Form FD 9000-24

| SITE <br> NAME: NAS Jox | SITE | LOCATION: Jeck-som,ike, FL |  |
| :--- | :--- | :--- | :--- | :--- |
| WELLNO: EKMW-02 | SAMPLEID: | EKMW -02 | DATE: |

## PURGING DATA



## SAMPLING DATA



## NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.

2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212. SECTION 3)
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2{ }^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS 2200 - 2 ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)

# GROUNDWATER SAMPLING LOG 

| SITE NAME: | UAS Jan |  | LITE LOCATION: Jacksonville, FL |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| WELL NO: | EKMW-03 | SAMPLEID: | Ekmw-03 | DATE: | 10101/14 |

## PURGING DATA

| WELL <br> DIAMETER (inches): 2 | TUBING <br> DIAMETER (inches): $1 / 4$ | WELL SCREEN INTERVAL <br> DEPTH: 19 feet to 23 | STATIC DEPTH <br> TO WATER (feet): 3.75 | PURGE PUMP TYPE OR BAILER: |
| :--- | :--- | :--- | :--- | :--- | :--- | WELL VOLUME PURGE: 1 WELL VOLUME = (TOTAL WELL DEPTH - STATIC DEPTH TO WATER) $X$ WELL CAPACITY (only fill out if applicable)





| INITIAL P DEPTH IN | OR TUBI <br> LL (feet): | 21 | FINAL PUMP DEPTH IN W | OR TUBIN LL (feet): | 21 | PURGIN INITIAT | $\text { D AT: } 10: 10$ | PURGING ENDED AT: | $11: 20$ | TAL VOLUME URGED (gallon | $4.80$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| TIME | VOLUME <br> PURGED <br> (gallons) | CUMUL. VOLUME PURGED (gallons) | PURGE RATE (gpm) | DEPTH TO WATER (feet) | $\begin{gathered} \mathrm{pH} \\ \text { (standard } \\ \text { units) } \end{gathered}$ | TEMP. $\left({ }^{\circ} \mathrm{C}\right)$ | COND. <br> (circle units) $\mu \mathrm{mhos} / \mathrm{cm}$ or 1551 em | $\begin{aligned} & \text { DISSOLVED } \\ & \text { OXYGEN } \\ & \text { (circle units) } \\ & \text { \% gaturation } \\ & \hline \end{aligned}$ | TURBIDITY <br> (NTUs) | COLOR <br> (describe) | $\begin{aligned} & \text { ORP } \\ & (\mathrm{mV}) \end{aligned}$ |
| 10:15 | 0.50 | 0.50 | 0.10 | 6.50 | 5.78 | 27.77 | 1770 | 0.38 | 31.9 | cleor | $-18.8$ |
| 10:18 | 0.25 | 0.75 | 0.08 | 6.82 | 5.81 | 27.73 | 1781 | 0.29 | 40.2 | 1 | -19.8 |
| 10:30 | 1.00 | 1.75 | 0.08 | 7.10 | 5.87 | 27.10 | 1854 | 0.60 | 173 | Light brown | $-32.7$ |
| 10:40 | 0.75 | 2.50 | 0.075 | 7.14 | 4.99 | 27.08 | 1811 | 0.22 | 95.7 | ${ }^{\prime}$ | 17.5 |
| 10:50 | 0.50 | 3.00 | 0.05 | 7.14 | 5.72 | 26.95 | 1781 | 0.33 | 64.8 | い | $-10.4$ |
| 11:05 | 1.00 | 4.00 | 0.067 | 7.03 | 5.78 | 27.11 | 1785 | 0.15 | 31.6 | clear | $-23.0$ |
| 11:10 | 0. 25 | 4.25 | 0.05 | 7.01 | 5.78 | 27.11 | 1783 | 0.15 | 29.3 | 1 | $-24.6$ |
| 11:15 | 0.25 | 4.50 | 0.05 | 6.97 | 5. 78 | 27.18 | 1783 | 0.15 | 19.6 | い | -25.9 |
| 11:17 | 0.15 | 4.65 | 0.075 | 6.94 | 5.78 | 27.18 | 1783 | 0.16 | 18.4 | " | $-22.3$ |
| 11:19 | 0.15 | 4.80 | 0.075 | 6.91 | 5.78 | 27.19 | 1782 | 0.16 | 18.3 | * | $-21.7$ |
| $\begin{array}{llllllllll}\text { WELL CAPACITY (Gallons Per Foot): } & 0.75^{\prime \prime}=0.02 ; & 1^{\prime \prime}=0.04 ; & 1.25^{\prime \prime}=0.06 ; & 2^{\prime \prime}=0.16 ; & 3^{\prime \prime}=0.37 ; & 4^{\prime \prime}=0.65 ; & 5^{\prime \prime}=1.02 ; \quad 6^{\prime \prime}=1.47 ; & 12^{\prime \prime}=5.88 \\ \text { TUBING INSIDE DIA. CAPACITY (Gal./Ft.): } & 1 / 8^{\prime \prime}=0.0006 ; & 3 / 16^{\prime \prime}=0.0014 ; & 1 / 4^{\prime \prime}=0.0026 ; & 5 / 16^{\prime \prime}=0.004 ; & 3 / 8^{\prime \prime}=0.006 ; & 1 / 2^{\prime \prime}=0.010 ; & 5 / 8^{\prime \prime}=0.016\end{array}$ |  |  |  |  |  |  |  |  |  |  |  |
| PURGING EQUIPMENT CODES: B |  |  | B = Bailer: | BP = Bladder Pump; |  | ESP = Electric Submersible Pump: |  | PP $=$ Peristaltic Pump; |  | $\mathrm{O}=$ Other (Specify) |  |

SAMPLING DATA


NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.

## 2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)

$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)

# Form FD 9000-24 <br> GROUNDWATER SAMPLING LOG 



## PURGING DATA



## SAMPLING DATA



NOTES: 1. The above do not constitute all of the information required by Chapter $\mathbf{6 2 - 1 6 0 , ~ F . A . C . ~}$
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3 )
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS 2200-2); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)

## GROUNDWATER SAMPLING LOG

| SITE NAME: | NAS Jax |  | SITELOCATION: Jocksunvilu, FL |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| WELL NO: | Ekmw - 05 | SAMPLE ID: | EKMNW-OS | DATE: | 10/01/2014 |

## PURGING DATA



## SAMPLING DATA

| SAMPLED BY (PRINT) / AFFILIATION: <br> Byu Zinckgraf / Geosyntee |  |  |  |  |  |  | SAMPLING <br> INITIATED AT: 14:00 | SAMPLING ENDED AT: |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| PUMP OR TUBING <br> DEPTH IN WELL (feet): <br> 21.5 |  |  |  |  |  | FIELD-FILTERED: Y $\mathbb{Q}$ FILTER SIZE: ___ $\quad$ +Filtration Equipment Type: |  |  |  |
| FIELD DECONTAMINATION: |  |  | PUMP $Y$ | TUBING Y N(reptaged) |  |  | DUPLICATE: $\quad$ Y | N |  |
| SAMPLE CONTAINER SPECIFICATION |  |  |  | SAMPLE PRESERVATION |  |  | INTENDED ANALYSIS AND/OR METHOD | $\qquad$ | SAMPLE PUMP FLOW RATE ( mL per minute) |
| $\begin{aligned} & \hline \text { SAMPLE } \\ & \text { ID CODE } \end{aligned}$ | CONTAINERS | $\begin{gathered} \text { MATERIAL } \\ \text { CODE } \\ \hline \end{gathered}$ | VOLUME | $\begin{gathered} \text { PRESERVATIVE } \\ \text { USED } \\ \hline \end{gathered}$ | $\begin{gathered} \text { TOTAL VOL } \\ \text { ADDED IN FIELD (mL) } \end{gathered}$ | FINAL pH |  |  |  |
| Exanw-05 | 1 | PC | 12 | Nore | - | - | Gene Trac | APP | $<100$ |
| $\cdots$ | 2 | $C G$ | 40 arc | nome | - | - | $V$ FAS | $\checkmark$ | 11 |
| $\cdots$ | 1 | PE | 250ML | $\mathrm{MNO}_{3}$ | - | - | metal 5 | " | 11 |
| $\cdots$ | 1 | PE | 150~L | none | - | - | anions | $n$ | * |
| 4 | 1 | PE | $150 \sim 6$ | none | - | - | iodide | " | " |
| " | 3 | CG | 40 ac | nome | - | - | DHG 5 | " | ' ${ }^{\prime}$ |
| REMARKS |  |  |  |  |  |  |  |  |  |

REMARKS:

MATERIAL CODES: $\quad$ AG = Amber Glass; $\quad C G=$ Clear Glass; $\quad P E=$ Polyethylene; $\quad P P=$ Polypropylene; $\quad S=$ Silicone; $\quad T=T e f l o n ; \quad O=O t h e r(S p e c i f y) ~$
SAMPLING EQUIPMENT CODES: $\quad$ APP = After Peristaltic Pump; $\quad$ B = Bailer; $\quad$ BP = Bladder Pump; $\quad$ ESP = Electric Submersible Pump;
RFPP = Reverse Flow Peristaltic Pump; $\quad$ SM = Straw Method (Tubing Gravity Drain); $\quad 0=$ Other (Specify)
NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
pH: $\pm 0.2$ units Temperature: $\pm 0.2{ }^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)

# GROUNDWATER SAMPLING LOG 

| SITE NAME: | NAS Jax |  | SITE LOCATION: |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| WELL NO: | EKMW-07 | SAMPLE ID: | EKMW-O7 | DATE: | $10 / 02 / 2014$ |

## PURGING DATA



## SAMPLING DATA



NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
pH: $\pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)

| SITE NAME: | NAS Jox |  | SITE <br> LOCATION: | Jacksonville, FL |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL NO: | Ekun - 08 | SAMPLE ID: | EKMNW-08 |  | DATE: | 10/02/2014 |

## PURGING DATA



## SAMPLING DATA



## NOTES: 1. The above do not constitute all of the information required by Chapter $\mathbf{6 2 - 1 6 0 , ~ F . A . C . ~}$

2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
pH: $\pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS 2200-2); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)


## SAMPLING DATA

| SAMPLED BY (PRINT) / AFFILIATION: Brqu Zinctgraf / Geosyntec |  |  |  |  |  |  | SAMPLING <br> INITIATED AT: $14: 08$ | SAMPLING ENDED A | $\begin{aligned} & \frac{\mathrm{G}}{\mathrm{~T}:} 14: 20 \\ & \mathrm{ZE}: \ldots \quad \ldots \mathrm{m} \end{aligned}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| PUMP ORTUBING DEPTH IN WELL (feet): |  | $22$ |  |  |  | FIELD-FILTERED: Filtration Equipment Type: |  | FILTER SIZE: $\qquad$ $\mu \mathrm{m}$ |  |
| FIELD DECONTAMINATIO |  |  |  | TUBING $Y$ N(replaced) |  |  | DUPLICATE: Y © |  |  |
| SAMPLE CONTAINER SPECIFICATION |  |  |  | SAMPLE PRESERVATION |  |  | INTENDED ANALYSIS AND/OR METHOD | SAMPLING EQUIPMENT CODE | SAMPLE PUMP FLOW RATE (mL per minute) |
| $\begin{aligned} & \text { SAMPLE } \\ & \text { ID CODE } \end{aligned}$ | $\begin{gathered} \# \\ \text { COIANERS } \\ \hline \end{gathered}$ | MATERIAL CODE | VOLUME | $\begin{aligned} & \text { PRESERVATIVE } \\ & \text { USED } \end{aligned}$ | TOTAL VOL ADDED IN FIELD (mL) | $\begin{gathered} \text { FINAL } \\ \mathrm{pH} \end{gathered}$ |  |  |  |
| EKMW-09 | 1 | PE | 12 | none | - | - | Genc Trac | APP | $<100$ |
| * | 2 | $e G$ | 40mL | none | - | - | VFAs | " | , |
| " | 3 | $C G$ | 40 mL | none | - | - | DHGs | $\cdots$ | " |
| * | , | OE | 250 mL | $\mathrm{HNO}_{3}$ | - | - | metals, K | " | $\cdots$ |
| " | 1 | PE | 150 al | nome | - | - | anions | ', | " |
| " | 1 | PE | 150 mL | none | - | - | iodide | ' | ${ }^{\prime}$ |
| REMARKS | 1 | PE | Soom | none | - | - | TDS | ' | ' |
| MATERIAL | CODES: | AG = Ambe | Glass; CG | = Clear Glass; PE | E = Polyethylene; PP = | olypropy | e; S S Silicone; $\quad$ T | = Teflon; $\quad 0=$ | ther (Specify) |
| SAMPLIN | EQUIPMENT | CODES: | $\begin{aligned} & \text { APP }=\text { After } \\ & \text { RFPP }=\text { Reve } \end{aligned}$ | eristaltic Pump; se Flow Peristaltic $P$ | $\begin{aligned} & \mathrm{B}=\text { Bailer; } \quad \mathrm{BP}=\text { Blad } \\ & \text { ump; } \quad \mathrm{SM}=\text { Straw Meth } \end{aligned}$ | r Pump: (Tubing | $\begin{gathered} \text { ESP = Electric Subm } \\ \text { ravity Drain); } \quad 0=6 \end{gathered}$ | rsible Pump; ther (Specify) |  |

NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212. SECTION 3 )
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS 2200-2); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTU; optionally $\pm 5$ NTU or $\pm 10 \%$ (whichever is greater)

# Form FD 9000-24 <br> GROUNDWATER SAMPLING LOG 

| SITE | NAS Jox | SITE | JOCATION: | Jacksomille, FL |
| :--- | :--- | :--- | :--- | :--- |
| NAME: | NELLNO: | EKMW-11 | SAMPLEID: | EKMW-11 |

## PURGING DATA



SAMPLING DATA


NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212. SECTION 3)
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2{ }^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTU; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)
 Calibrate specific conductance using at least two standards that bracket the range of expected sample readings (unless readings $<0.1 \mathrm{~ms} / \mathrm{cm}$ then one standard of $0.1 \mathrm{mS} / \mathrm{cm}$ is acceptable)


 1. See Table FS 2200-2 on the back of this form


| $\begin{aligned} & \text { !ey do } \\ & \text { ssed } \end{aligned}$ | (^u) <br> Su!peay | әұе ${ }^{-d \times \exists}$ p.epuels | \# 707 p.epueis | 0. duəュ <br> (0) 1 w - PIS | эแ! | 2¢P] | V/N dOS | d8O |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |



|  |  |
| :---: | :---: |
|  |  |






## GROUNDWATER SAMPLING LOG

$\square$ SYSTEM ON $\square$ SYSTEM OFF $\square$ NOT APPLICABLE (NO SYSTEM)


## PURGING DATA



SAMPLING DATA


NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUIVE READINGS (SEE FS 2212, SECTION 3)
pH: $\pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saltation (see Table FS 2200-2); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)




GROUNDWATER SAMPLING LOG

为

PURGING DATA


SAMPLING DATA


NOTES: 1. The above do not constitute all of the information required by Chapter $62-160$, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3 )
pH: $\pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTU; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)
well needs repair $\qquad$ needs well tag $\qquad$ E locking cap: $\qquad$ O other comment:
$\because$ DI Water Lot \# $\qquad$ MS / MS $\qquad$ Equip blk $\qquad$ ¿ Ambient blk $\qquad$ Trip blk $\qquad$ (B)

1 PE 2SOML Nome
1 $\square$
20121102
Bromide
500 mL Mom $\left.\begin{aligned} & \text { Bromide } \\ & \text { Iodide } \\ & \text { merobal }\end{aligned} \right\rvert\,$

1-2 Nome microbial

## GROUNDWATER SAMPLING LOG

I SYSTEM ON $\triangle$ SYSTEM OFF $二$ NOT APPLICABLE (NO SYSTEM)


## PURGING DATA



SAMPLING DATA


[^0] Turbidity: all readings $\leq 20$ Nf; optionally $\pm 5$ NTU or $\pm 10 \%$ (whichever is greater)

- well needs repair $\qquad$ needs well tag locking cap: $\qquad$ I other comment: $\qquad$
= DI Water Lot \# $\qquad$ ZMS/MSD $\qquad$ Equip blk $\qquad$ ᄃ Ambient blk $\qquad$ - Trip blk $\qquad$


# GROUNDWATER SAMPLING LOG 

$\square$ SYSTEM ON םSYSTEM OFF ■NOT APPLICABLE (NO SYSTEM)


## PURGING DATA

| $\begin{aligned} & \text { DIAM } \\ & \hline \end{aligned}$ | ER (inche | 2 | TUBING DIAMETER (inches): $1 / 4$ |  | WELL SCREEN INTERVAL DEPTH: 19 feet to $\mathbf{Z} \boldsymbol{3}$ feet |  |  | STATIC DEPTH TO WATER (feet): $\varphi, 71$ |  | $\begin{aligned} & \text { PURGE PUMP TYPE } \\ & \text { OR BAILER: } \end{aligned}$ |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL VOLUME PURGE: 1 WELL VOLUME = (TOTAL WELL DEPTH - STATIC DEPTH TO WATER) x WELL CAPACITY <br> (only fill out if applicable) |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| INITIAL PUMP OR TUBING DEPTH IN WELL (feet): $\qquad$ |  |  | FINAL PUMP OR TUBING DEPTH IN WELL (feet): |  |  |  | PURGING <br> INITIATED AT: $/ 250$ |  | $\begin{aligned} & \text { PURGING } \\ & \text { ENDED AT: } 1425 \end{aligned}$ |  | $\begin{aligned} & \text { TOTAL VOLUME } \\ & \text { PURGED (galions): } 4,5 \% \end{aligned}$ |  |  |
| Tim | Purged (gallons) | Cum. <br> Volume Purged (gallons) | $\begin{aligned} & \text { Rate } \\ & \text { (gpm) } \end{aligned}$ | Depth to <br> Water <br> (ft BTOC) | $\begin{gathered} \mathrm{pH} \\ \text { (SU) } \end{gathered}$ |  | $\begin{gathered} \text { Cond. } \\ (\mathrm{mS} / \mathrm{cm}) \end{gathered}$ | en | Salinity (\%) | $\begin{aligned} & \text { (mP } \\ & (\mathrm{mV}) \end{aligned}$ |  | Odor cribe) | Turbidity (NTUs) |
|  | 0. |  | ci, 06 |  | 5.17 |  |  | 0.13 | 1.61 | 1 |  | d |  |
|  |  |  | 0.055 | 186 |  |  | 3.11 | 0.10 | 162 | 102.3 |  | $\cdots$ |  |
| 1320 | 0.55 | 70 | 0,055 | 9.01 | 5,14 | 25,8 | 3.1 | 0.08 | 1064 | 91.6 | \% | 2 | 1 |
| 1330 | 0.45 | 2,1 | 0.045 | 8.90 | 5.29 | 26.3 | 3.22 | $0 \cdot 07$ | 1.68 | 58.9 | n | 4 | , 1.6 |
| 134 | 0.45 | 2.40 | 0,045 | 8.90 | 5.41 | 26.6 | 3,21 | 0.07 | 1,67 | 35.0 | a | 4 | 5.98 |
| 1350 | 0.45 | 3.05 | 0.045 | 9,70 | 5,48 | 26.4 | 3.13 | . 08 | 1.203 | 9,6 |  | - | 5.47 |
| 1355 | 0.48 | 3,46 | 0.045 | 9.31 | 5.50 | 26.4 | 3.10 | 0,08 | 12 | 7 |  | 14 | 4.15 |
| 12 | 0,25 | 3,47 | 0.045 | 9.40 | 5.53 | 20.5 | 3.08 | 0.09 | 1.60 | 8,3 | ' | 11 | 3.15 |
|  | 0,22 | 3.64 | 0.0 | 9.42 | $5.5 C$ | 26.7 | 3.04 | 0.09 |  | -0, |  | a | 3.20 |
| 1410 | 0.22 | 3.81 | 0.045 | 9.43 | 5,56 | 26.7 | 3.01 | 0.09 | 1.50 | $-3,4$ | 9 |  | 3.21 |
| 1415 | 0.72 |  | 0.045 | 4,44 |  | 26.5 |  | 0.09 | 1.55 | $-4.2$ | ' | $\cdots$ |  |
| WELL CAPACITY (gal/ft): $0.75^{\prime \prime}=0.02 ; \quad 1^{\prime \prime}=0.04 ;$TUBING INSIDE DIA. CAPACITY ( $\mathrm{gal/ft}$ ): $1 / 8^{\prime \prime}=0.0006 ;$ |  |  |  |  | $\begin{aligned} 1.25^{\prime \prime}=0.06^{\prime} & 2^{\prime \prime}=0.16 ; \\ 3 / 16^{\prime \prime}=0.0014 ; & 1 / 4^{\prime \prime}=0.0026 ; \end{aligned}$ |  |  | $\begin{aligned} & 7 ; 4^{\prime \prime}=0.65 ; \\ & 5 / 16^{\prime \prime}=0.004 ; 5^{\prime \prime}=1.02 ; \quad 6^{\prime \prime}=1.47 ; \quad 12^{\prime \prime}=0.006 ; \quad 1 / 2^{\prime \prime}=0.010 ; \quad 5 / 8^{\prime \prime}=0.016 \\ & \hline \end{aligned}$ |  |  |  |  |  |
| PURGING EQUIPMENT CODES: |  |  | : B = Bailer; BP |  | = Bladder Pump; |  | ESP = Electric Submersible Pump; P |  |  | $\mathrm{P}=$ = Peristaltic Pump; |  | $0=$ Other (Specify) |  |

## SAMPLING DATA



NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OFLAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS 2200-2); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)
$\square$ well needs repair
. $n$ needs well tag $\qquad$ ᄃ locking cap: $\qquad$ ᄃ other comment:

- Equip blk Ambient blk $\qquad$ Thrip blk


## GROUNDWATER SAMPLING LOG




## SAMPLING DATA



NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CEATERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTU; optionally $\pm 5$ NTU or $\pm 10 \%$ (whichever is greater)


E needs well tag $\qquad$ $\square$ locking cap: $\qquad$ © other comment: $\qquad$
Equip blk $\qquad$ Ambient blk $\qquad$ $\sqsupset$ Trip blk $\qquad$
www.trinityadc.com

## GROUNDWATER SAMPLING LOG

$\square$ SYSTEM ON ESYSTEM OFF $\square$ NOT APPLICABLE (NO SYSTEM)


## PURGING DATA

|  | WELL <br> DIAMETER (inches): 2 |  |  | TUBING $0.25 \times 0.17$ DIAMETER (inches): |  | WELL SCREEN INTERVAL <br> DEPTH: 19 feet to 23 feet |  |  | STATIC DEPTH <br> TO WATER (feet): 4.82 |  | PURGE PUMP TYPE <br> OR BAILER: DERSAALTIC DOMA |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  | EQUIPMENT VOLUME PURGE: 1 EQUIPMENT VOL. $=$ PUMP VOLUME + (TUBING CAPACITY $\mathrm{x} \quad$ TUBING LENGTH) + FLOW CELL VOLUME(only fill out if applicable) |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  | INITIAL PUMP OR TUBING DEPTH IN WELL (feet): $2 l^{\circ}$ |  |  | FINAL PUMP OR TUBING DEPTH IN WELL (feet): |  |  |  | PURGING 1305 <br> INITIATED AT: $=020$ |  |  | PURGING <br> ENDED AT: 1425 | TOTAL VOLUME PURGED (gallons): 4.00 |  |  |
| 1520 | Time <br> Ave | $\begin{gathered} \text { GALS } \\ \text { Volume } \\ \text { Purged } \\ \text { (gatlons) } \\ \text { of } \end{gathered}$ | Cum. <br> Volume <br> Purged (gallons) Anmex |  | Depth to Water (ft BTOC) | $\underset{(\mathrm{SU})}{\mathrm{pH}}$ | Temp. ( ${ }^{\circ} \mathrm{C}$ ) | Spec. <br> Cond. <br> (mis/cm) <br> $\mu$ | Dissolved Oxygen (mg/L) | Salinity (\%) pr | ORP (mV) |  | lor/ Odor describe) | Turbidity (NTUs) |
|  | 1520 | 0.75 | c. 75 | 120 | 4.95 | 6.35 | 26.2 | 902 | 0.91 | 0.44 | 89.1 | Cumal | ne cour | Ze, c |
| 1330 | 1530 | 0.50 | 1.25 | 200 | 8.75 | 6.12 | 26.6 | 1640 | 1.23 | 0.83 | -9.7 | CIGAC-N | ne ctorr | 9.67 |
| $1340$ | +545 | 10.50 | 1.75 | 205 | 9.20 | 5.96 | 2 d .8 | 1831 | 1.99 | 6.42 | 7.2 | Clex | NO ODCR | 5.78 |
| 1350 | iss | c. 50 | 1.25 | 200 | 9.28 | 5.89 | 26.9 | 1949 | 2.68 | 0.19 | 12.6 | clatal | NO oDOR | 4.65 |
| 1460 | decs | 0.50 | 2.75 | 2 co | 9.33 | 5.89 | 27.1 | 1928 | 3.07 | 1.01 | $-16.9$ | Clame | NE CDOR | 3.90 |
| 1416 | 11619 | 0.50 | 3.25 | 205 | 9,35 | 5.86 | 27.1 | $2 \times 23$ | 3.35 | 1.02 | -19.6 | CLEAR | no comer | 3.70 |
| 140 | 16.5 | 0.25 | 3.50 | 200 | 9.35 | 5.87 | 67.0 | 2037 | 3.42 | 1.03 | $-19.7$ | clate | NAC CDER | 2.04 |
| 1420 | 1620 | 0.25 | 3.75 | 200 | 9.35 | 5.80 | 27.2 | $2 c 49$ | 3.50 | 1.44 | $-20.8$ | cleor | I ne cjera | 1.66 |
|  | 1425 | c.25 | 4.00 | 200 | 9.35 | 5.85 | 27.3 | 2048 | 3.52 | 1.04 | -20.1 | cictir | ne edor | 1.23 |
|  | 12s | $0 \cdot 25$ |  |  |  | sios |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  | WELL TUBIN | CAPACITY <br> G INSIDE | (gal/ft): 0. <br> A. CAPAC | $\begin{aligned} & 75^{\prime \prime}=0.02 ; \\ & \text { ITY (gal/ft): } \end{aligned}$ | $\begin{aligned} & 1^{\prime \prime}=0.04 ; \\ & 18^{\prime \prime}=0.0006 ; \end{aligned}$ | $\begin{array}{r} 1.25^{\prime \prime}=0 \\ 3 / 16^{\prime \prime} \\ \hline \end{array}$ | $\begin{aligned} & 56 ; \mathbf{2 "}^{\prime \prime}= \\ & 0.0014 ; \end{aligned}$ | $\begin{aligned} & 16 ; \quad 3^{\prime \prime \prime}= \\ & 14^{\prime \prime}=0.002 \end{aligned}$ | $\begin{array}{r} 4^{\prime \prime}= \\ 5 / 16^{\prime \prime}= \end{array}$ | $\begin{array}{r} 5 "= \\ 3 / 8 \\ \hline \end{array}$ | $\begin{aligned} & 2 ; \quad 6^{\prime \prime}= \\ & 0.006 ; \end{aligned}$ | $\begin{array}{lr} \hline 47 ; & 12 \prime \prime \\ 2^{\prime \prime}= & 0.010 \\ \hline \end{array}$ | $\begin{aligned} & 2 "=5.88 \\ & 10 ; \quad 5 / 8^{\prime \prime}= \end{aligned}$ | $\stackrel{16}{ }$ |
|  | PURG | ING EQUIP | EENT COD | ES: $\quad B=B$ | Bailer; BP | = Bladde | Pump; | SP = Electri | ubmersible | mp; | = Peristaltic | Pump; | $0=0$ ther | Specify) |

SAMPLING DATA


[^1]$\square$ well needs repair $\qquad$ $\square$ needs well tag $\square$ locking cap: $\qquad$ - other comment:
$\square$ DI Water Lot \# $\qquad$ $\square$ MS / MSD $\qquad$ - Equip blk $\qquad$ $\square$ Ambient blk $\qquad$ \&Trip blk T8-1

| (IONTANEESS | MAREMA CIDE pe | volume 250 mL | prestrivative | ANALYSES Bromingt | SAmping ca. code App | Plows RATG zoc |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | pe | 500 mL | - | loand |  |  |
| 2 | c6 | 40 ml | - | $v$ va |  |  |
| 1 | pe | IL | - | muncoing |  | 1 |

## GROUNDWATER SAMPLING LOG

## $\square$ SYSTEM ON ®SYSTEM OFF םNOT APPLICABLE (NO SYSTEM)



## PURGING DATA

| WELL DIAMETER (inches): $2^{2}$ |  |  | TUBING 0.25"×0.17" DIAMETER (inches): |  | WELL SCREEN INTERVAL DEPTH: 19.5 feet to 24.5 feet |  |  | $\begin{aligned} & \text { STATIC DEPTH } \\ & \text { TO WATER (feet): } 4.63 \end{aligned}$ |  |  | PURGE PUMP TYPE ORBAILER: PCRSTALTIC pUMP |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| EQUIPMENT VOLUME PURGE: 1 EQUIPMENT VOL. = PUMP VOLUME + (TUBING CAPACITY x TUBING LENGTH) + FLOW CELL VOLUME <br> (only fill out if applicable) |  |  |  |  |  |  |  |  |  |  |  |  |  |
| INITIAL PUMP OR TUBING DEPTH IN WELL (feet): $22^{\prime}$ |  |  | FINAL PUMP OR TUBING DEPTH IN WELL (feet): $\quad 22^{\prime} \mathrm{BC} \mathrm{B}^{3}$ |  |  |  | PURGING InITIATED AT: 1510 |  | PURGING ENDED AT: 1420 |  | TOTAL VOLUME PURGED (gallons): 4.0. |  |  |
| Time | Volume <br> Purged (gallons) | Cum. <br> Volume <br> Purged (gallons) | Purge Rate (gpm) | Depth to Water (ft BTOC) | ${\underset{\text { (SU) }}{ } \mathrm{pH}}^{\text {(S) }}$ | Temp. $\left({ }^{\circ} \mathrm{C}\right)$ | Spec. Cond. ( $\mathrm{mS} / \mathrm{cm}$ ) | Dissolved Oxygen ( $\mathrm{mg} / \mathrm{L}$ ) | $\underset{(\%)}{\substack{\text { Salinity } \\(\%)}}$ | $\underset{(m V)}{(\mathrm{RF})}$ |  | $\begin{aligned} & \text { or/ Odor } \\ & \text { escribe) } \end{aligned}$ | Turbidity (NTUs) |
| 1525 | 0.90 | 0.90 | 230 | 5.79 | 5.79 | 26.9 | 5368 | 0.53 | 2.89 | $-25.9$ | clear | se EDAR | 17.0 |
| 1535 | 0.60 | 1.50 | 230 | 5.81 | 10.06 | 27.5 | 5847 | 2.30 | 3.18 | 91.7 | ciant | vo ciose | 4.38 |
| 045 | 0.60 | 2.10 | 230 | 5.82 | 6.13 | 26.9 | 5382 | 3.30 | 289 | -105. 1 | clate | No ator | 2.90 |
| 1155 | 0.60 | 2.70 | $23 x$ | 5.82 | 6.14 | 26.9 | 5175 | 3.75 | 2.77 | - 4.4 | clear | ni odor | 2.11 |
| 1605 | Q. 60 | 3.10 | 230 | 5.82 | 6.16 | 27.0 | 3226 | 3.93 | 2.67 | -14. 4 | cleamel | no adet | 2.08 |
| 4.15 | 0.60 | 3.70 | 230 | 5.82 | 6.16 | 26.9 | 4905 | 3.99 | 2.61 | -117.1 | cidath ${ }^{\text {a }}$ | conor | 1.63 |
| 1620 | 0.65 | 4.00 | 230 | 5.82 | 6.16 | 27.1 | 4815 | 4,00 | 2.57 | $-118.4$ | capuel | jo cpar | Z.ci |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| PURGING EQUIPMENT CODES: |  |  | $\mathrm{B}=$ Bailer; $\quad \mathrm{BP}$ |  | = Bladder Pump; |  | ESP = Electric Submersible Pump; |  |  | Peristaltic | Pump; | $\mathrm{O}=$ Other | Specify) |

## SAMPLING DATA



NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABIIIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3 )
pH: $\pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); 0 ptionally, $\pm 0.2 \mathrm{mgh}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NT}$ ū; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)
$\square$ well needs repair $\qquad$ $\square$ needs well tag $\qquad$ $\square$ locking cap: $\qquad$ $\square$ other comment:
$\qquad$ CMS / MSD Elume 05 . - Equip blk $\qquad$ $\square$ Ambient blk $\qquad$ ©Trip blk T -MS |-MSD

# GROUNDWATER SAMPLING LOG 

$\square$ SYSTEM ON - SYSTEM OFF $\square$ NOT APPLICABLE (NO SYSTEM)


## PURGING DATA

| WELL DIAME | ER (inches) |  | TUBING 0.2 DIAMETER ( | $25{ }^{\circ} \times 0.4$ nches): | $\begin{aligned} & \text { WELL } \\ & \text { DEPT } \end{aligned}$ | $\begin{aligned} & \text { REEN IN } \\ & \text { feet } \end{aligned}$ | $\begin{aligned} & \text { RVAL } \\ & 23 \text { fee } \end{aligned}$ | STATIC D TO WATE | $\begin{aligned} & \text { PTH } \\ & \text { (feet): } 4 . \\ & \hline \end{aligned}$ | PUR | E PUMP T | YPE isiatic |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL (only fil | OLUME P out if appli | $\begin{aligned} & \text { RGE: } 1 \text { W } \\ & \text { able) } \end{aligned}$ | ELL VOLUME | $\begin{aligned} E & =(\text { TOTA } \\ & =1 \end{aligned}$ | $\begin{aligned} & \text { WELL } \\ & 3.25 \end{aligned}$ | $\begin{aligned} & \text { TH - } \\ & \text { feet - } \end{aligned}$ | ATIC DEP <br> 10 | O WATER) <br> feet) |  | PACITY | foot | $291$ | gallons |
| EQUIP (only fil | $\begin{aligned} & \text { UENT VO } \\ & \text { out if app } \end{aligned}$ | $\begin{aligned} & \text { TE PURC } \\ & \text { ble) } \end{aligned}$ | 1 EQUIPM | ENT VOL. | PUMP | $\begin{aligned} & \text { LUME + } \\ & \text { allons + } \end{aligned}$ | BING CA | ns/foot $x$ | TUBING L | $\begin{aligned} & \text { GTH) + FL( } \\ & \text { feet }+ \end{aligned}$ | ICELL VOL | LUME <br> allons = |  |
| $\begin{aligned} & \hline \text { INITIA } \\ & \text { DEPT } \end{aligned}$ | PUMP OR IN WELL | TUBING <br> et): ${ }^{2}$ | FINAL PUM DEPTH IN | MP OR TUB WELL (fee) | $21^{\circ}$ |  | PURGING INITIATED | $1015$ |  | GING <br> ED AT:1130 | TOTAL PURG | AL VOLUME GED (gallons) | $4.5$ |
| Time | Volume Purged Anetor Angor | Cum. <br> Volume <br> Purged (gallons) | Purge Rate (gpmil | $\begin{aligned} & \text { Depth } \\ & \text { to } \\ & \text { Water } \\ & \text { (ft BTTC) } \end{aligned}$ | $\begin{gathered} \mathrm{pH} \\ (\mathrm{SU}) \end{gathered}$ | Temp. ( ${ }^{\circ} \mathrm{C}$ ) | $\begin{aligned} & \text { Spec. } \\ & \text { Cond. } \\ & \text { (ffism) } / \mathrm{cm}) \\ & N \end{aligned}$ | Dissolved Oxygen (mg/L) | Salinity (\%\%) ppi | $\begin{aligned} & \text { (mV) } \end{aligned}$ |  | or/ Odor escribe) | Turbidity (NTUs) |
| 1025 | 0.50 | 050 | 200 | 6.86 | 6.62 | 24.1 | 10126 | 1.13 | 3.48 | $-42.5$ | 32 | Siski | 321 |
| 163 | 0.50 | 1.00 | 200 | 1.39 | 6.71 | 24.2 | 7836 | 0.46 | 4.35 | . 92.8 | $4.64{ }^{\text {sin }}$ | Lind asocios2 | 43.5 |
| 1645 | c. 45 | 1.45 | 20 | 7.60 | 6.60 | 24.3 | 8 Cl 9 | 0.21 | 4.43 | -45.1 | Subiter su | maindooxe | 49.0 |
| 1055 | 055 | 2.00 | 205 | 1.70 | 6.48 | 24.5 | 7104 | 0.32 | 3.89 | 91.0 | Macsial | ne cout | 23.0 |
| 105 | 0.50 | 2.50 | 200 | 7.76 | 6.30 | 24.6 | 6149 | 1.19 | 3.34 | -98.1 | plais | \|nce edol | 64.5 |
| Efri | c. | 3.00 | 200 | 7.81 | 6. 23 | 24.8 | 5090 | 2.50 | 2.73 | -107.3 | Brewns | No ador | 54.2 |
| 1120 | 0.250 | 3250 | 205 | 1.81 | 6.22 | 24.9 | 4714 | 2.74 | 2.51 | -110.7 | beamal | No adie | 50.9 |
| 125 | Q 255 | 2 4 4 | 200 | 781 | 6.21 | 24.9 | 4582 | 2.85 | 2.44 | -112.4 | messiy | no esper | 45.5 |
| 1130 | 0.20 | 40 | 200 | 1.81 | 6.19 | 255.1 | 448 | 3.12 | 2.23 | -114.2 |  | no codar | 33.1 |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| WELL CAPACITY (gal/ft): 0.75" $=0.02$; TUBING INSIDE DIA. CAPACITY (gal/ft): |  |  |  | $\begin{aligned} 1^{\prime \prime} & =0.04 ; \\ 1 / 8^{\prime \prime} & =0.0006 \end{aligned}$ | $\begin{aligned} & 1.25^{\prime \prime}=0.06 ;{ }^{2 \prime \prime} \\ & ; \quad 3 / 16^{\prime \prime}=0.0014 ; \end{aligned}$ |  | $\begin{aligned} & 3^{3 \prime 1} \\ & 1 / 4^{\prime \prime}=0.00 \\ & \hline \end{aligned}$ | $\begin{array}{rr} 4^{\prime \prime \prime}=0.65 ; & 5^{\prime \prime}= \\ 5 / 16^{\prime \prime}=0.004 ; & 3 / 8^{\prime \prime} \end{array}$ | $\begin{array}{ll} 5^{\prime \prime}=1.02 ; \quad 6^{\prime \prime}=1.47 ; \quad 12^{\prime \prime}=5.88 \\ 3 / 8^{\prime \prime}=0.006 ; \quad 1 / 2^{\prime \prime}=0.010 ; \quad 5 / 8^{\prime \prime}=0.016 \end{array}$ |  |  |  |  |
| PURGING EQUIPMENT CODES |  |  | B = Bailer; |  | P = Bladder Pump; |  | ESP = Electric Submersible Pump; |  |  | $\mathrm{PP}=$ Peristaltic Pump; |  | $\mathrm{O}=$ Other (Specify) |  |

## SAMPLING DATA



## REMARKS: <br>  MATERIAL CODES: $\quad \mathbf{A G}=$ Amber Glass; $\quad \mathrm{CG}=$ Clear Glass; $\quad \mathrm{PE}=$ Polyethylene; $\quad \mathrm{PP}=$ Polypropylene; $\quad \mathbf{S}=$ Silicone; $\quad \mathrm{T}=$ Teflon; $\quad \mathrm{O}=$ Other (Specify) SAMPLING EQUIPMENT CODES: APP = After Peristaltic Pump; $\quad \mathrm{B}=$ Bailer; $\quad \mathrm{BP}=$ Bladder Pump; $\quad$ ESP $=$ Electric Submersible Pump; RFPP = Reverse Flow Peristaltic Pump; $\quad$ SM = Straw Method (Tubing Gravity Drain); $\quad 0=0$ ther (Specify)

[^2]$\square$ well needs repair $\qquad$ $\square$ needs well tag
$\square$ locking cap $\qquad$ $\square$ other comment:

- DI Water Lot \# $\qquad$ $\square$ MS / MSD $\qquad$ $\square$ Equip blk
- Ambient blk $\qquad$ - Trip bik TB.)
 www.trinityade.com


## GROUNDWATER SAMPLING LOG

$\square$ SYSTEM ON $\square$ SYSTEM OFF $\square$ NOT APPLICABLE (NO SYSTEM)


## PURGING DATA



## SAMPLING DATA



NOTES: 1. The above do not constitute all of the information required by Chapter $62-160$, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTÜ; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)
$\square$ well needs repair $\qquad$ $\square$ needs well tag $\qquad$ $\square$ locking cap: $\qquad$ $\square$ other comment:

- DI Water Lot \# $\square$ MS /MED
2012_1102 1 250 mL Mane Prom, dr PE 500 mz Hone Iodide

GROUNDWATER SAMPLING LOG
$\square$ SYSTEM ON $\square$ SYSTEM OFF $\square$ NOT APPLICABLE (NO SYSTEM)


PURGING DATA


PURGING EQUIPMENT CODES: $\quad \mathrm{B}=$ Bailer; $\quad \mathrm{BP}=$ Bladder Pump; $\quad$ ESP = Electric Submersible Pump; $\quad$ PP = Peristaltic Pump; $\quad \mathrm{O}=\mathrm{Other}$ (Specify)
SAMPLING DATA


NOTES: 1. The above do not constitute all of the information required by Chapter $62-160$, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3 )
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$\qquad$ $\square$ needs well tag $\qquad$ $\square$ locking cap: $\qquad$ $\square$ other comment: $\qquad$ -DI Water Lot \# $\qquad$ $\square$ MS / MS $\qquad$ - Equip blk $\qquad$ $\square$ Ambient blk $\qquad$ べTrip blk $\qquad$ $1 B-2$
 $\qquad$ ( 1 $\backslash$
$\square$ SYSTEM ON $\square$ SYSTEM OFF $\square$ NOT APPLICABLE (NO SYSTEM)


WELL VOLUME PURGE: 1 WELL VOLUME $=($ (TOTAL WELL DER TH
(only fill out if applicable)


## SAMPLING DATA



NOTES: 1. The above do not constitute all of the information required by Chapter $62-160$, F.A.C
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
$\mathrm{pH}: \pm 0.2$ units /temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS 2200-2); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: al pleadings $\leq 20$ NTÜ; optionally $\pm 5$ NTU or $\pm 10 \%$ (whichever is greater)
$\square$ well needs repair $\square$ needs well tag - locking cap: $\qquad$ - other comment:

- DI Water Lot \# $\qquad$ $\square$ MS / MS $\qquad$ $\square$ Equip blk -Ambient blk $\qquad$ - Trip blk
$\qquad$


## GROUNDWATER SAMPLING LOG

$\square$ SYSTEM ON 『SYSTEM OFF םNOT APPLICABLE (NO SYSTEM)


## SAMPLING DATA



## NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.

2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3 )
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTU
$\square$ well needs repair $\square$ needs well tag $\square$ locking cap: $\qquad$ - other comment:
$\qquad$ $\square M S / M S D$ $\qquad$ $\square$ Equip blk $\qquad$ $\square$ Ambient blk $\qquad$ -Trip MiBi2

SAIIRUNGGa. CODE RON LATE 1

2 Ap 20
materider CODS
vacume
PRES $(-2 \cdot A T V E$
Antuysis
pe

66

## 250 ml Berande

 10DIDE VFA500inl

40 mL -

## GROUNDWATER SAMPLING LOG

## $\square$ SYSTEM ON ■SYSTEM OFF ם NOT APPLICABLE (NO SYSTEM)



PURGING DATA


## SAMPLING DATA



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2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3 )
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ © ©fseolved' xyg en: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) -Funtidify:-altreadings $<20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater) $O \Omega \perp \geq 10 \%$
$\square$ well needs repair_ $\boldsymbol{N} \quad \square$ needs well tag $\boldsymbol{N}$ _ locking cap:
$Y$


 $\square$ other comment:

## GROUNDWATER SAMPLING LOG

| SITE NAME: Sidtll |  | SITE LOCATION: NAS MOVMNWAdd | $\text { DATE: } 23 \mathrm{MDNOH}$ |
| :---: | :---: | :---: | :---: |
| $\text { WELL NO: } \mathrm{F} / \mathrm{MMM}-\mathrm{D} 2$ |  |  | FIELD DUPLICATE: $\quad$ Y (N) DUPLICATEID: |

## PURGING DATA

| WELLDIAMETER (inches): |  |  | $\begin{array}{\|l\|l\|} \hline \text { TUBING } \\ \text { DIAMETER (inches) } \end{array}$ |  | WELL SCREEN INTERVAL DEPTH: feet to |  |  | STATIC DEPTH <br> TO WATER (feet): 5.34 |  |  | PURGE EUMP TYYEOR BALLER: |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL VOLUME PURGE: 1 WELL VOLUME $=$ (TOTAL WELL DEPTH - STATIC DEPTH TO WATER) $x$ WELL CAPACITY <br> (only fill out if applicable) $=$ feet _ feet) $x$ gallons |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  (oniy fill out if applicable) |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| INITAL PUMP OR TUBING DEPTH IN WELL (feet): 2 |  |  | FINAL PUMP OR TUB:ING DEPTH IN WELL (feet): |  |  |  | $\begin{aligned} & \text { PURGING } \\ & \text { NNTIATED AT: } \\ & \hline 1200 \end{aligned}$ |  | $\left.\begin{aligned} & \text { URGING } \\ & \text { NoED AT: } \end{aligned} 10 \right\rvert\, \begin{aligned} & \text { Ti } \\ & \hline \end{aligned}$ |  |  | TOTAL VOLUME <br> PURGED (gallons): 4.20 |  |
| Time |  | Cum. Poume Purged (gallons) | Purge Rate $\underset{\substack{\text { Rate } \\ \text { (gmom) }}}{ }$ | Wator <br> (f BTOC) | PH ${ }_{\text {P }}^{\text {SU) }}$ |  | Spoc. Sond. (mslem) | Dissolved Oxygen ( $\mathrm{mg} / \mathrm{L}$ ) | $\underset{\substack{\text { Salinity } \\\left(\%_{0}\right)}}{\text { Soy }}$ | (mp) | $\underset{\text { (describer }}{\text { Color }}$ | $\underset{\substack{\text { Odor } \\ \text { (dascribe) }}}{ }$ | urbidity NTUU) |
|  | , |  | 0.00 | 39 | 5 |  | 3,34 | 0.34 | 8 | 0.9 |  | NA | 9.7 |
| 1220 | 0.60 | 0.20 | D 0.06 | 8.18 |  | -3.3 | 3.38 | 0. 2 |  | 24.2 |  |  | 1,6 |
| 1230 | 0.60 | 1.80 | 0.06 | 8.44 | +.79 | 23.45 | 3.28 | 0.7 | 1.72 | 26.0 |  |  |  |
| 240 | 0.60 | 2.40 | 0.06 | 8.51 | 4.87 | 23.6 | 3.19 | 0.27 | . 67 | -37.6 |  |  |  |
| 1250 | 0.60 | 3.00 | 0.06 | Q.56 | +, ${ }^{1} 1$ | 23.70 | 3.00 | 0.26 | 1.56 | 48.6 |  |  |  |
| 1300 | 0.60 | 3.60 | 0.80 | 8.61 | 4.98 | 24.08 | 2.93 | 0.24 | 1.52 | -55.3 |  |  | 6.6 |
| 1305 | 0.30 | 3.90 | 0.60 | 8.58 | 1.93 | 24.17 | 2.90 | 0.24 | 1.51 | -56.2 |  |  |  |
| 1310 | 0.30 | 4.20 | 0.60 | 8,56 | 5.05 | 24.35 | 2.28 | 0.24 | 1.46 | 58.2 |  |  | 7.59 |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |

## SAMPLING DATA



# GROUNDWATER SAMPLING LOG 

- SYSTEM ON ם SYSTEM OFF DNOT APPLICABLE (NO SYSTEM)



## PURGING DATA



## SAMPLING DATA

| SAMPELED BY/RRINT)/AFFLLAATION: Juh Bowner Ininity |  |  |  | SAMPLER(S) कIGNATURE(S): |  |  |  | $\begin{array}{r} \text { SAMPLE TIME: } \\ 1304 \end{array}$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\begin{array}{ll} \text { PUMP R TUUNG } \\ \text { OEPTH NWEL (feet): } 21 \end{array}$ |  |  |  |  |  |  |  |  |  |
| FIELD DECONTAMINATION: PUMP Y |  |  |  | tueing y ${ }^{\text {cid }}$ (eplaced) |  |  | FIELD EQUIPMENT IDENTIFICATION |  |  |
|  |  |  |  | INTENDED ANALYSIS MEFHOD C | SAMPLINGEQUIPMENT CODE | SAMPLE PUMP <br> FLOW RATE <br> (mL per minute) | H20 QUALITY PARAMETER |  |  |
| CONTANERS | MATERIAL CODE | VOLUME | PRESERVATIVE USED |  |  |  | Model $Y$ Y frot |  | 64 |
| 3 | EG | 40 | Hul | CSIA | APP | 220 |  | TURBIDIME |  |
|  | $C 6$ | 40 | - | VFA |  |  | ModelMLVOTPL | 1 Snf: | 201 |
| 3 |  | 40 | HCL | VOC |  |  |  | ОтНеR |  |
| 3 | 6 | 40 | Hel | Wk\& |  |  |  |  |  |
| 2 | $A G$ | 40 | Hel | 10C |  |  |  |  |  |
| Remarks: fage in |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| MATERIAL CODES: $\quad$ AG = Amber Glass; $C$ c |  |  |  | ear Glass; PE = Polyethylene; |  | PP = Polypropylene; | $\mathbf{S}=$ Silicone; $\quad \mathbf{T}=$ | Teflon; | $\mathrm{O}=\mathrm{Ot}$ |
| SAMPLING EQUIPMENT CODES: |  |  | APP = After Peristaltic Pump; $\quad \mathrm{B}=$ Bailer; $\quad \mathrm{BP}=$ Bladder Pump; $\quad \mathrm{ESP}=$ Electric Submersible Pump; RFPP = Reverse Flow Peristaltic Pump; $\quad$ SM $=$ Straw Method (Tubing Gravity Drain); $\quad 0=0$ Other (Specify) |  |  |  |  |  |  |

## NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C

2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3) $\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Speciflc Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS 2200-2); optionally, $\pm 0.2 \mathrm{mg} /$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)
$\square$ well needs repair___ $\quad$ needs well tag _______

- DI Water Lot \# $\qquad$ $\square$ MS / MSD $\qquad$ - - Equip blk $\qquad$ cap:-Ces $\qquad$ - other comment: $\qquad$
$\square$ Ambient blk $\qquad$ $\square$ Trip blk $\qquad$


PURGING DATA


SAMPLING DATA


## NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.

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$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table $\mathrm{FS} 2200-2$ ); optionally $\pm 0.2 \mathrm{mgh}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTU; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)
[ well needs repair $\qquad$ $\square$ needs well tag $\qquad$ $\square$ locking cap: $\qquad$ - other comment:

ᄃ DI Water Lot \# $\qquad$ - MS / MSD $\qquad$ - Equip blk $\qquad$ $\sqsupset$ Ambient blk $\qquad$ - Trip blk
$\qquad$
$\qquad$

## GROUNDWATER SAMPLING LOG

■ SYSTEM ON םSYSTEM OFF R NOT APPLICABLE (NO SYSTEM)


## PURGING DATA



## SAMPLING DATA

| SAMPEED BY (PRNVT)/AFFILIATION: 1 nowity |  |  |  |  |  |  |  | SAMPLE TIME: $110^{2}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\begin{aligned} & \text { PUMPORTL } \\ & \text { DEPTH INW } \end{aligned}$ | ING $L$ (feet): | 21 |  | TUBING MATERIAL CO | $P G$ |  | $\begin{gathered} Y \\ \text { ht Type: } \end{gathered}$ | ILTER SIZE: ___ $\mu \mathrm{m}$ |
| FIELD DECONTAMINATION: PUMP Y |  |  |  | TUBING Y èreplaced) |  |  | FIELD EQUIPMENT IDENTIFICATION |  |
| SAMPLE CONTAINER SPECIFICATION |  |  |  |  | SAMPLING EQUIPMENT CODE | SAMPLE PUMP FLOW RATE (mL per minute) | H20 Quality parameter |  |
| $\begin{gathered} \# \\ \text { CONTANERS } \\ \hline \end{gathered}$ | $\begin{gathered} \text { MATERIAL } \\ \text { CODE } \\ \hline \end{gathered}$ | VOLUME (mL) | PRESERVATIVE USED |  |  |  |  | SN: $16 A 102711$ |
| 2 | $C 6$ | 40 | $\cdots$ | VFA | $A P$ | 220 |  | URBIDIMETER |
| 2 |  | 40 | HU1 | VOC | 1 |  | Modelminstas | SN\# 20112930 |
| 3 | 61 | $2 / 0$ | HL1 | Vhlch |  |  |  | OTHER |
| 2 | 46 | 40 | HCN | T0C |  | 1 |  |  |
|  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |
| $\text { REMARKS: } 1 \text { P步 } 12$ |  |  |  |  |  |  |  |  |
| MATERIAL CODES: |  | AG = Amber Glass; $\quad \mathbf{C G}=$ |  | ar Glass; PE = Polyethylene; |  | PP = Polypropylene | $\mathbf{S}=$ Silicone; $\quad \mathbf{T}=$ Teflon; | eflon; $\quad 0=$ Other (Specify) |
| SAMPLING EQUIPMENT CODES: |  |  | APP $=$ Atter Peristaltic Pump; $\quad \mathrm{B}=$ Bailer;RFP $=$ Reverse Flow Peristaltic Pump; $\quad$ SM $=$ S |  |  | BP $=$ Bladder Pump; $\quad \mathbf{E S P}=$ Electric Submersible Pump; <br> $=$ Straw Method (Tubing Gravity Drain); $\quad \mathbf{O = O t h e r}$ (Specify) |  |  |

NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
pH: $\pm 0.2$ units Temperature: $\pm 0 .{ }^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS 2200-2); optionally, $\pm 0.2 \mathrm{mgh}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)
$\sqsubset$ well needs repair $\qquad$ $\square$ needs well tag __mmorm
$\square$ DI Water Lot \# ___ $\quad$ MS / MSD ___ E___ Equip blk $\qquad$ man ambient blk
$\qquad$ - other comment: $\qquad$

## PURGING DATA

| WELLDIAMETER (inches) |  |  | $\begin{array}{\|c\|c\|} \hline \text { TUBIN } \\ \text { DIAME } \end{array}$ | $3 / 10$ | DEPTH | feet to | to feet |  |  |  |  | P |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL VOLUME PURGE: 1 W <br> (only fill out if applicable) |  |  | 1 WELL VOLUME = (TOTAL WELL DEPTH - STATIC DEPTH |  |  |  |  | TO WATER) $\times$ WELL CAPACITY <br> feet) $x$ <br> gallons/foot |  |  |  |  | gallons |
|  |  |  | EQUIPMENT VOLUME PURGE: 1 EQUIPMENT VOL. (only Fill out if applicable) |  |  |  |  |  |  |  |  |  | feet- $\frac{\text { VOLUME + (TUBIITERAA PAC }}{}$ |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  | gallo |
| INITIAL PUMP OR TUBING,DEPTH IN WELL (feet): |  |  | FINAL PUMP OR TUBING DEPTH IN WELL (feet): |  |  |  | PURGING |  |  |  |  | $\begin{aligned} & \text { TOTAL VOLUME } \\ & \text { PURGED (gallons): } \end{aligned} 4.20$ |  |
| Time | $\begin{aligned} & \text { Pury } \\ & \text { (gall } \end{aligned}$ | Purged (gallons) | d <br> s)Purge <br> Rate <br> (gmm) | Water <br> (ft BTOC) | (SH) |  | $\begin{aligned} & \text { Cond. } \\ & (\mathrm{ms} / \mathrm{cm}) \end{aligned}$ | $\begin{gathered} \text { Oxygen } \\ (\mathrm{mg} / L) \end{gathered}$ | $\underset{\substack{\text { Salinity } \\\left(\%_{0}\right)}}{ }$ | $\begin{aligned} & \text { ORP } \\ & \text { (mv) } \end{aligned}$ | $\underset{\substack{\text { Color } \\ \text { (describe) }}}{\text { chen }}$ | $\underset{\text { (describe) }}{\text { (dor })}$ |  |
|  | 0.60 |  | 01000 | 5.7 | 88 | 3.0 | 5.62 | 0.85 | 3.05 | 2.4 | cluar | NA | 20.8 |
|  | .60 | 20 | 00.06 | 5.83 | 4.74 | 23.08 | 5.25 | 0.55 | 2.82 | 0.4 | clear | NA | 15.9 |
| 0830 | 060 | 80 | 0.010 | 592 | 80 | 2408 | 4.15 | 0.40 | 2.19 | 4.6 |  |  | 9.74 |
|  | 0.60 | 2.40 | D 0.06 | 5.99 | . 87 | 24.04 | 3.29 | 0.34 | 1.71 | 1.5 |  |  | 5.58 |
| 0850 | 0.60 | 3.00 | 0.06 | 0.06 | 4.76 | 24.40 | 2.54 | 0.31 | 1.31 | 4.76 |  |  | 4.74 |
| 0900 | 0.60 | 3.60 | 0.06 | 6.17 | 4.80 | 24.73 | 2.24 | 0.31 | 1.35 | 1.20 |  |  | 4.47 |
| 0905 | 0.30 | 3.90 | 00.06 | 6.1 | 4.81 | 24.8 .3 | 2.13 | 0.29 | 1.09 | 4.40 |  |  |  |
| 910 | 0.30 | H. 20 | 0.06 | 6.18 | 480 | 24.90 | 2.08 | 0.27 | 1.06 | 4.90 |  |  | 3.30 |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| PURGING EQUIPMENT CODES: $\quad \mathbf{B}=$ Bailer; $\quad \mathrm{BP}=$ Bladder Pump; |  |  |  |  |  |  | ESP $=$ Electric Submersible Pump; |  |  |  |  |  |  |

SAMPLING DATA


NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212. SECTION 3 )
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Speclic Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)


## GROUNDWATER SAMPLING LOG

$\square$ SYSTEM ON םSYSTEM OFF RNOT APPLICABLE(NO SYSTEM)

| SITE NAME: Site 11 |  | site location: AYS IAAX |  | DATE: 312311 |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| WELL NO: 2 LVWW-7 | SAMPLEID: \& KWWW-07 $\quad$FREEPRODUCT: Y <br> DEPTH TO PRODUCT (ft BTOC): |  |  | FIELD DUPLICATE: $Y$ DUPLICATEID: | ( |

## PURGING DATA

| WELLDIAMETER (inches): |  |  | NG <br> ETER | $\begin{aligned} & 3 \\ & \mathrm{es}): \\ & \hline 1 / \end{aligned}$ |  | fee | $23 \text { feet }$ |  |  |  |  | PE |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL VOLUME PURGE: (only flll out if applicable) |  |  | 1 WELL VOLUME $=$ (TOTAL WELL DEPTH - STATICDEPTH TO WATER) $\times$ WELL CAPACITY |  |  |  |  |  |  |  |  |  |  |
| EQUIPMENT VOLUME PURGE: 1 EQUIPMENT VOL. <br> (only fill out if applicable) |  |  |  |  | VOLUME + (TUBING CAPACITY $x$gallons + ( gallons/foot $x$ |  |  |  | TUBING LENGTH) + FLOW CELL VOLUME <br> feet) + gallons |  |  |  | gall |
| INITIAL PUMP OR TUBIMGDEPTH IN WELL (feet): |  |  | FINAL PUMP OR TUBING DEPTH IN WELL (feet): |  |  |  | PURGING <br> INITIATED AT: |  | $\begin{aligned} & \text { PURGING } O^{a} \backslash 13 \\ & \text { ENDED AT: } \end{aligned}$ |  |  | $\begin{aligned} & \text { TOTAL VOLUME } 438 \\ & \text { PURGED (gallons): } \end{aligned}$ |  |
| Time | Volume Purged (gallons) | Volume Purged (gallons) | $\begin{gathered} \text { Rate } \\ (\mathrm{gpm}) \end{gathered}$ | $\begin{gathered} \text { Depth } \\ \text { to } \\ \text { Water } \\ (\mathrm{t} \text { BTOC) } \end{gathered}$ | $\begin{gathered} \mathrm{pH} \\ (\mathrm{SU}) \end{gathered}$ | $\begin{aligned} & \text { Temp. } \\ & \text { ( }{ }^{\circ} \mathrm{C} . \end{aligned}$ | Cond. <br> ( $\mathrm{mS} / \mathrm{cm}$ ) | $\begin{aligned} & \text { Oxygen } \\ & (\mathrm{mg} / \mathrm{L} \end{aligned}$ | Salinity $\left(\%_{0}\right)$ | $\begin{aligned} & \text { ORP } \\ & (\mathrm{mV}) \end{aligned}$ | $\begin{gathered} \text { Color } \\ \text { (describe) } \end{gathered}$ | $\underset{\text { (describe) }}{\text { Odor }}$ | Turbidity (NTUs) |
| OUN | 0 | 0.6 | O.Ole |  | . 4 |  | 3.68 | 0 | 1.9 | 15 |  | No |  |
| 0820 | 0.6 | 1,2 | 0.06 |  | 5.52 | 25.2 | 3.68 | 0.22 | . 94 |  |  | n |  |
| 0830 | O. 10 | 1.8 | 0.01 |  |  | 25.4 | 3.76 | 0.16 | 98 | 45 | , | WOL |  |
|  | 0.6 | 2.4 | 0.06 | 9.92 |  | 25.6 | 3.75 | 0.14 |  |  |  | Nore |  |
|  | O.le | 3.0 | 0.06 | 0.14 | 5.78 | 25.7 | 26.4 | 0.12 | 1.911 | 5 |  | nowe |  |
| 000 | 0.6 | 3.6 | 0.06 | 0.31 | 5.84 | 25.7 | 3.47 | 0.11 | 1.82 | , |  | lone | 34.62 |
| 0905 | 0.3 | 3.9 | 0.06 | 10.4 | 5.85 | 25.8 | 3.38 | 0.11 | 1.77 | $-70.9$ |  | none | 28.43 |
| 0910 | 0.3 | 4.2 | 0.06 | 10.49 | . .95 | 25.8 | 3.33 | 0.11 | 1.74 | $-72.2$ | Gatio | nome | 25.56 |
| 0913 | 0.18 | 4.38 | 0.06 | 0.49 | 5.87 | 25.7 | 3.26 | 0.10 | 1.70 | -74 | 0 | nove | 23.88 |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| URGING EQUIPMENT CODES: |  |  |  |  | : $\mathrm{B}=$ Bailer; $\quad \mathrm{BP}=$ Bladder Pump; |  | ESP = Electric Submersible Pump; |  |  | PP $=$ Per | Pump; |  | Specify) |

## SAMPLING DATA

| SAMPGED BY (PRANT)/AFFILIATION |  |  |  |  |  |  |  |  | ETME: |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\begin{aligned} & \text { PUMFOR TU } \\ & \text { DEPTH IN WE } \end{aligned}$ | $\begin{aligned} & 3 \operatorname{SNG} \\ & L L \text { (feet): } \end{aligned}$ | $2$ |  |  |  | $\begin{aligned} & \text { FIELD-FILTERED: Y Y } \\ & \text { Filtration Equipment Type: } \end{aligned}$ |  | LTER | IZE:___mm |
| FIELD DECONTAMINATION: PUMP Y $\quad$ Y |  |  |  | tubing y (0)replaced) |  |  | FIELD EQUIPMENT IDENTIFIGATION |  |  |
| SAMPLE CONTAINER SPECIFICATION |  |  |  | INTENEDANALYISANDORMETHOD | SAMPLINGEQUPMENT CODE | SAMPLE PUMP FLOW RATE (mL per minute) | H20 QUALITY PARAMETER |  |  |
| $\begin{gathered} \# \\ \text { CONTANERS } \\ \hline \end{gathered}$ | $\begin{array}{\|c} \hline \text { MATERIAL } \\ \text { CODE } \\ \hline \end{array}$ | $\begin{gathered} \hline \text { VOLUME } \\ \text { (mL) } \\ \hline \end{gathered}$ | $\begin{gathered} \text { PRESERVATIVE } \\ \text { USED } \\ \hline \end{gathered}$ |  |  |  | Model VIP Pot |  | 64102 |
| 2 \% 20001000 |  |  | $\longrightarrow$ | NGS | App | 220 | TURBIDIMETER |  |  |
| 2 | $00^{60} 46$ | 40 | - | VFA |  |  | Model Marstins |  | 016090 |
| 3 | Ca | 40 | HCl | VOL |  |  |  | OTHE |  |
| 3 | $C, C$ | 40 | HCl | Wı\& |  |  |  |  |  |
| 2 | $A 12$ | 110 | du | Toc | 1 |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |
| REMARKS: |  |  |  |  |  |  |  |  |  |
| MATERIAL C | DES: | AG = Amber Glass; $\quad \mathbf{C G}=$ Clear Glass; |  |  | PE = Polyethylene; | PP = Polypropylene: | $\mathbf{S}=$ Silicone; $\quad \mathbf{T}=$ Teflon; |  | 0 = Other (Spe |
| SAMPLING EQUIPMENT CODES: |  |  | APP = After Peristaltic Pump; $\quad \mathrm{B}=$ Bailer; $\quad \mathbf{B P}=$ Bladder Pump; $\quad \mathbf{E S P}=$ Electric Submersible Pump; RFPP = Reverse Flow Peristaltic Pump; $\quad$ SM $=$ Straw Method (Tubing Gravity Drain); $\quad 0=0$ ther (Specify) |  |  |  |  |  |  |

NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F,A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE, READINGS (SEE FS 2212, SECTION 3)
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissoived Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mgh}$ or $\pm 10 \%$ (whichever is greater) Turidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)
$\square$ well needs repair $\qquad$ $\square$ MS / MSD $\square$ needs well tag $\qquad$ $\square$ locking cap: $\qquad$ 10 $\square$ oth
$\square$ Di Water Lot\# $\qquad$ -Equip blk $\neg$ Ambient blk - $\quad$ oth comment: $\qquad$

## GROUNDWATER SAMPLING LOG

$\square$ SYSTEM ON ᄃ SYSTEM OFF $\square$ NOT APPLICABLE (NO SYSTEM)

| SITE NAME: $\quad(\dot{T}\|l\|$ | SITE LOCATIO | $\text { SITE LOCATION: NAS } 10 Q \mathrm{NO} H \mathrm{Lel}$ | DATE: 23 NAMOH 7 |
| :---: | :---: | :---: | :---: |
| WELL NO: Evnn-0 | SAMPLEIDEKMN-OQ | $\begin{aligned} & \text { FREE PRDDUCT: Y } \\ & \text { DEPTH TO PRODUCT (ft BTOC): } \end{aligned}$ | FIELD DUPLICATE: Y N DUPLICATE ID: |

## PURGING DATA

| WELLDIAMETER (inchas): 2 |  |  | $\underset{\text { DUAMETER (incheses: }}{3} / 16$ |  | WELL SCREEN INTERVAL <br> DEPTH: feet to |  |  | $\begin{aligned} & \text { TAATIC DEPTH } \\ & \text { TO WATER (feet): } 53.53 \text { OURGE PUMP TYPF } \\ & \text { ORPALER: } \end{aligned}$ |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL VOLUME PURGE: 1 WELL VOLUME ( (TOTAL WELL DEPTH - STATIC DEPTH TO WATER) $\times$ WELL CAPACITY |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| INITIAL PUMP OR TUBING DEPTH IN WELL (feet): 21 |  |  | FINAL PUMP OR TUBING DEPTH IN WELL (feet): |  |  |  | $\begin{aligned} & \text { PURGING } \\ & \text { INTIATED AT: } \\ & 0.945 \end{aligned}$ |  |  | $\begin{aligned} & \text { PURGING } \\ & \text { ENDED AT: } 1055 \end{aligned} \begin{aligned} & \text { TOTAL VOLUME } \\ & \text { PURGED (gallons): } \end{aligned} \mathbf{4} .20$ |  |  |  |
| Time | Volume Purged (gallons) | Purged (anlons | (gpm) | $\begin{gathered} \text { to } \\ \text { Water } \\ \text { (f BTOC) } \end{gathered}$ | (SH) | $\begin{aligned} & \text { Temp. } \\ & \text { Poc } \end{aligned}$ | $\left.\begin{array}{c} \text { Cond. } \\ (\mathrm{ms}(\mathrm{~m}) \end{array}\right)$ | $\begin{gathered} \text { Oxygen } \\ \text { (mgL) } \end{gathered}$ | $\underset{\substack{\text { Salinity } \\(\text { \%oo }}}{ }$ | $\begin{aligned} & \text { ORP } \\ & \text { (mv) } \end{aligned}$ | $\begin{gathered} \text { Color } \\ \text { (describe) } \end{gathered}$ | $\begin{gathered} \text { Odor } \\ \text { (describe) } \end{gathered}$ | Tictidity |
|  | , | 0.00 | 0.06 | 9.02 | 4.03 |  | 3.55 | 2.86 | . 84 | 84.3 | Clear | NA | , |
| 1005 | 0.60 | 1.20 | 0.06 | 10.38 | . 11 | 24.93 | 3.86 | 2.51 | 2.04 | 70.4 |  |  | 26.4 |
| 1015 | 0,60 | 1.80 | 0.06 | 1.46 | 3.92 | 25.04 | 4.66 | 2.12 | 2.49 | 09.2 |  |  | 9.1 |
| 1025 | 0.60 | 2.40 | 0.00 | 2.21 | 3.90 | 25.17 | 5.02 | 1.86 | 2.69 | 68.9 |  |  | 22.4 |
| 1035 | 0.60 | 3.00 | 0.06 | 12.74 | 378 | 25.09 | 5.68 | 1.54 | 3.07 | 70.5 |  |  | 25.2 |
| 1045 | 0.60 | 3.60 | 0.06 | 3.42 | 3.83 | 25.64 | 5.49 | 1.66 | 2,06 | 07.1 |  |  | 60. |
| 1050 | 0.30 | 3.90 | 0.06 | 3.95 | 3.85 | 25.08 | 5.55 | 1.53 | 3.00 | 63.6 |  |  |  |
| 1055 | 0.30 | 4.20 | 0.06 | 14.19 | 3.83 | 25.67 | 5.65 | 1.46 | 3.05 | 62.3 |  |  | 61.9 |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| T CODES: $\quad \mathrm{B}=$ Bailer; $\quad \mathrm{BP}=$ Bladder Pump; $\quad$ ESP $=$ Electric Submersile Pump; $\quad \mathrm{PP}=$ Peristaltic Pump; $\quad 0=0$ |  |  |  |  |  |  |  |  |  |  |  |  |  |

## SAMPLING DATA



## GROUNDWATER SAMPLING LOG

■SYSTEM ON $\beth$ SYSTEM OFF $\square$ NOT APPLICABLE (NO SYSTEM)


PURGING DATA

| WELL DIAMETER (inches): |  |  | $\begin{aligned} & \text { TUBING } 3 / 16 \\ & \text { DIAMETER (inches): } \end{aligned}$ |  | WELL SCREEN INTERVAL DEPTH: 19 feet to 23 feat |  |  | STATIC DEPTHTO WATER (feet): 5,30 |  |  | $\begin{aligned} & \text { PURGE PUMP TYPE } \\ & \text { OR BAILER: } p \text { ump } \end{aligned}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL VOLUME PURGE: (only fill out if applicable) |  |  | feet |  |  |  |  | WATER) <br> feet) | $x$ WELL C | CAPACITY <br> gallo | ns/foot = |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| INITIAL PUMP OR TUBING DEPTH IN WELL (feet): |  |  | FINAL PUMP OR TUBING $\partial l$DEPTH IN WELL (feet): |  |  |  | $\begin{aligned} & \text { PURGING } \\ & \text { INITIATED AT: } \end{aligned} 0815$ |  | $\begin{aligned} & \text { PURGING } \\ & \text { ENDED AT: } O 930 \\ & \hline \end{aligned}$ |  |  | TOTAL VOLUMEPURGED (gallons): |  |
| Time | Volume Purged (gallons) | Cum. <br> Volume Purged (gallons) (gallons) | $\begin{aligned} & \text { Purge } \\ & \text { Rate } \\ & \text { (gpm) } \end{aligned}$ | Depth Water (ft BTOC) | $\begin{gathered} \mathrm{pH} \\ (\mathrm{SU}) \end{gathered}$ | Temp. ( ${ }^{\circ} \mathrm{C}$ ) | Spec. Cond. ( $\mathrm{ms} / \mathrm{cm}$ ) | Dissolved Oxygen (mgh) | Salinity (\%os) | $\begin{aligned} & \text { ORP } \\ & (\mathrm{mV}) \end{aligned}$ | $\begin{gathered} \text { Color } \\ \text { (describe) } \end{gathered}$ | Odor (describe) | Turbidity |
| 0825 | 0. | 0.6 | 0.00 | 1.80 | 6. | 24 | 3.10 | 0. | 1.61 | 15.4 | c104 | rane | \%. |
| 0835 | 0.6 | 1.2 | 0.06 | 9.22 | 5.86 | 25.0 | 2.01 | 0.55 | 1.57 | 1 |  |  | 37.6 |
| 0845 | 0.6 | 1.8 | 0.06 | 10.64 | 5,57 | 25.1 | 2.89 | 0.50 | 1.50 | 20.5 |  |  | 10.5 |
| 0855 | 0.6 | 2.4 | 0.06 | 11.47 | 5.46 | 25.1 | 2,80 | 0.50 | 1.4 | 25,6 |  |  | 18.9 |
| 0905 | 0.6 | 3.0 | 0.06 | 12.50 | 5,38 | 25,2 | 2.70 | 0.51 | 1. 39 | 28.3 | Clear |  | 19.2 |
| 0915 | 0.6 | 3.6 | 0.06 | 3,08 | 5,34 | 25,3 | 2.59 | 0.29 | 1.33 | 28.3 |  |  | 9.85 |
| 09720 | 0.3 | 3.9 | 0.06 | 13.22 | 5,34 | 25.2 | 2.59 | 0.27 | 1.33 | 29.5 |  |  | 12.7 |
| 0975 | 0.3 | 4.2 | 0.06 | 13.22 | 5.32 | 25,1 | 2.55 | 0.24 | 1.31 | 30.1 |  |  | 10.5 |
| 0930 | 0.3 | 4.5 | 0.06 | 13,22 | 5.30 | 25,2 | 2.53 | 0.24 | 1.20 | 29.8 |  |  | 10.4 |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| PURGING EQUIPMENT CODES: $\quad \mathrm{B}=$ Bailer; |  |  |  |  | SP = Bladder Pump; |  | ESP = Electric Submersible Pump; |  |  | PP = Peristaltic Pump; |  | $0=$ Other (Specify) |  |

## SAMPLING DATA



## NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.

2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 22.12, SECTION 3)
pH: $\pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ ©issolved-xxygens: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turtidify all readings $\leq 40 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater) ofR $\pm 10 \%$
$\qquad$ $\square M S / M S D$ NA
$\qquad$ $\square$ locking cap: $\qquad$ 4 $\square$ other comment: $\checkmark$ DI Water Lot \# NA aEquipblk $N$ A $\square$ Ambient blk $\qquad$ $1 \times$ $\square$ Trip blk NA

## GROUNDWATER SAMPLING LOG

■SYSTEMON $\square S Y S T E M$ OFF $\exists$ NOT APPLICABLE (NO SYSTEM)


PURGING DATA


## SAMPLING DATA



## NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.

2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS 2200-2); optionally, $\pm 0.2 \mathrm{mg} /$ L or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater) $\exists$ well needs repair_ $\quad \sim$ needs well tag $N$ $\sqsupset \mathrm{D} \mid$ Water Lot \# NA $\lrcorner \mathrm{MS} / \mathrm{MSD} \mathrm{N} / \mathrm{A} \quad$ Equip blk $\square$ Ambient blk
$\qquad$ ㅁ other comment:
$\partial \mid$ pe $(\partial 50)$ woof $\mid$ subaqua $\square$ 240

## GROUNDWATER SAMPLING LOG

| SITE NAME: Sell |  |  |  |  | SITE LOCATOMA chechemuilla |  |  |  |  | DATE: $6 / 13 / 17$ |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELLQLINW-O1 |  |  | S\&MPLELiD: |  |  |  | FREE PRODUCT: Y DEPTH TO PRODUCT (ft BTOC): |  |  | FIELD DUPLICATE: Y 交 DUPLICATEID: |  |  |  |
|  |  |  | PURGING DATA |  |  |  |  |  |  |  |  |  |  |
| WELLDIAMETER (inctios): |  |  | TUBING 2 IAMETER (inches) 4 |  | WELL SCREEN INTERYA DEPTH: $\qquad$ feet to feet |  |  | STATIC DEPTH 4.0 (feet):TO WATER |  |  | PURGE PUMP TYPE OR BAILER: |  |  |
| WELL VOLUME PURGE: 1 WELL YOLUME _(TOTAL WELL DEPTH - STATIC DEPTH TO WATER) $\times$ WELL CAPACITY (only fill out if appicable) |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| EQUIPMENT VOLUME PURGE: 1 EQUIPMENT VOL. = PUMP VOLUME + (TUBING CAPAC̈ITY x TUBING LENGTH) + FLOW CELL VOLUME |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  | gallons + ( |  | gallons/foot $x$ |  |  | feet) + | gallons $=$ |  |  |
| INITIAL PUMP OR TUBHANDEPTH IN WELL (feet): |  |  | FINAL PUMP OR TUBING DEPTH IN WELL (feet): |  |  |  | PURGING INITIATED AF? |  |  | PURGING 0924 TOTAL VOLUME <br> PURGED (gallons):, 2,2 |  |  |  |
| Time | Volume <br> Purged <br> (gallons) | Cum. <br> Volume <br> Purged <br> (gallons) | Purge Rate (gpm) | $\begin{aligned} & \text { Depth } \\ & \text { to } \\ & \text { Water } \\ & \text { (ft BTOC) } \end{aligned}$ | $\underset{(\mathrm{SU})}{\mathrm{pH}}$ | Temp. ( $\left.{ }^{\circ} \mathrm{C}\right)$ | Spec. Cond. ( $\mathrm{mS} / \mathrm{cm}$ ) | Dissolved Oxygen (mg/L) | Salinity (\%) | ORP (mV) | Color (describe) | Odor (describe) | Turbidity (NTUs) |
| 002 | 0.6 | 0.6 | . 06 | 5.12 | 6. 2 | $26.1$ | $3.41$ |  | 1.7 | 136 | $x^{M}$ |  | 4.6 |
| 08 | 0.6 | n | $0.06 \%$ | 5.103 | 54. | 24.1 | 0.31 | 0.74 | 3.44 | $-155$ | clear | none | 9.3 |
| 00 | 0.6 | 1.8 | 0.09 | $\sum_{6} 69$ | 2 | 779 | 0.30 | $0 \frac{1}{1}$ | 3.41 | $-161$ | Cloar | vone | (8,5 |
| 0854 | 0.6 | 72.4 | 0.06 | T 7 | 5. | 28.0 | C. 13 | 1.12 | 3.32 | $-161$ | clear | none |  |
| 090 | 0.6 | 3.0 | ${ }^{\circ} 0.00$ | 79 | 5 | 10 | 6.05 | 1.14 | 3.27 | -161 | clear | none | 12.8 |
| ball | 0.6 | 3.6 | 0.01 | 96 | 2. | 28.1 | 5.91 | 1.16 | 3.19 | -162 | cleser | nowe | 9.8 |
| 6910 | 0.5 | 39 | 0.06 | 96 | $5 \cdot 7$ | 28,3 | $5 \cdot 86$ | till | 3.16 | $-164$ | clear | Lone | 4.6 |
| 0924 | 0.3 | 46 | 0.06 | - 96 | 5 | 28.3 | 5.81 | 1.16 | 3.12 | -161 | Clew | none | 11.1 |
| WELL CAPACITY (gal/ft): $0.75^{\prime \prime}=0.02 ;$ $1^{\prime \prime}=0.04 ;$ $1.25^{\prime \prime}=0.06 ;$ $2^{\prime \prime}=0.16 ;$ $3^{\prime \prime}=0.37 ;$ $4^{\prime \prime}=0.65 ;$ $5^{\prime \prime}=1.02 ;$ $6^{\prime \prime}=1.47 ;$ $12^{\prime \prime}=5.88$ <br> TUBING INSIDE DIA. CAPACITY (gal/f): $1 / 8^{\prime \prime}=0.0006 ;$ $3 / 16^{\prime \prime}=0.0014 ;$ $1 / 4^{\prime \prime}=0.0026 ;$ $5 / 16^{\prime \prime}=0.004 ;$ $3 / 8^{\prime \prime}=0.006 ;$ $1 / 2^{\prime \prime}=0.010 ;$ $5 / 8^{\prime \prime}=0.016$   |  |  |  |  |  |  |  |  |  |  |  |  |  |
| PURGING EQUIPMENT CODES: |  |  | : $\quad \mathrm{B}=$ Bailer; $\quad \mathrm{B}$ |  | BP = Bladder Pump; |  | ESP = Electric Submersible Pump; |  |  | PP = Peristaltic Pump; |  | $0=0$ ther (Specify) |  |

## SAMPLING DATA



## NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.

2. STABILZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTU; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whicheveris greater)


## GROUNDWATER SAMPLING LOG




SAMPLING DATA




 SAMPLING EQUIPMENT CODES: $\quad A P P=$ After Peristaltic Pump; $\quad B=$ Bailer; $\quad B P=$ Bladder Pump; $\quad$ ESP $=$ Electric Submersible Pump; RFPP = Reverse Flow Peristaltic Pump; $\quad \mathbf{S M}=$ Straw Method (Tubing Gravity Drain); $0=$ Other (Specify)
NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3) $\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20 \mathrm{NTU}$; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)
〕 well needs repair_


GROUNDWATER SAMPLING LOG
$\square$ SYSTEM ON $\square$ SYSTEM OFF SOT APPLICABLE (NO SYSTEM)



PURGING EQUIPMENT CODES: $\quad \mathrm{B}=$ Bailer; $\quad \mathrm{BP}=$ Bladder Pump; $\quad$ ESP $=$ Electric Submersible Pump; $\quad$ PP $=$ Peristaltic Pump; $\quad 0=$ Other (Specify)


NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3 )
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E well needs repair $\qquad$ - needs well tag $\qquad$ - locking cap: $\qquad$ ᄃ: other comment:
Li DI Water Lot \# $\qquad$ $\square$ MS / MS $\qquad$ Equip blk $\qquad$ ! - Ambient blk $\qquad$ $\square$ Trip blk $\qquad$ 1 is loos now Dux Ohbiver., Ais y40

## GROUNDWATER SAMPLING LOG




PURGING DATA


## SAMPLING DATA



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$\square$ well needs repair___ $\square$ needs well tag locking cap:___ $\_$other comment:



GROUNDWATER SAMPLING LOG


## PURGING DATA



## SAMPLING DATA



NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3) pH: $\pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{h}$ or $\pm 10 \%$ (whichever is greater) Tubidity: all readings $\leq 20$ NTU; optionally $\pm 5 \mathrm{NTU}$ or $\pm 10 \%$ (whichever is greater)


| 2 | AG | 40 | HCl | TOC |
| :---: | :---: | :---: | :---: | :---: |
| 3 | $C Q$ | 40 | HCl | MEE |
| $2013_{102}$ | $C G$ | 40 | HCl | $V O C$ |

GROUNDWATER SAMPLING LOG
$\square$ SYSTEM ON ■ SYSTEM OFF GNOT APPLICABLE (NO SYSTEM)


PURGING DATA


PURGING EQUIPMENT CODES: $\quad \mathrm{B}=$ Bailer; $\quad \mathrm{BP}=$ Bladder Pump; $\quad \mathrm{ESP}=$ Electric Submersible Pump; $\quad \mathrm{PP}=$ Peristaltic Pump; $\quad \mathrm{O}=\mathrm{Other}$ (Specify)


NOTES: 1. The above do not constitute all of the information required by Chapter $62-160$, F.A.C.
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[] well needs repair $\qquad$ $[\square$ needs well tag $\qquad$ $\square$ locking cap: $\qquad$ $1]$ other comment: $\qquad$

- DI Water Lot \# $\qquad$ [MS / MSS $\qquad$ $+$ $\square$ Equip blk $\qquad$ [ Ambient blk $\qquad$ -- Trip blk $\qquad$ 1 Ph 1000 hove Alithovill All $>400$


## GROUNDWATER SAMPLING LOG



| WELL <br> DIAMETER (inches): |  |  | TUBINGDIAMETER (inches)? |  | WELL SCREEN INTERYA <br> DEPTH: 10 feet to 23 feet |  |  | STATIC DEPTH <br> TO WATER (feet): 4.5 |  |  | PURGE PUMP TYRE OR BAILER: |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL VOLUME PURGE: 1 WELL VOLUME = (TOTAL WELL DEPTH - STATIC DEPTH TO WATER) $\times$ WELL CAPACITY(only fill outfapplieabla) |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| INITIAL PUMP OR TUBING DEPTH IN WELL (feet): 21 |  |  | FINAL PUMP OR TUBING DEPTH IN WELL (feet): $\qquad$ |  |  |  | $\begin{aligned} & \text { PURGING } \\ & \text { INITIATED AT: } \\ & \text { I } \end{aligned}$ |  |  | $\begin{array}{l\|l\|l\|} \hline \text { PURGING } \\ \text { ENDED AT: } \end{array}+0 \text { TOTAL VOLUME } \quad \text { PURGED (gallons): } 4.20$ |  |  |  |
| Time | Volume Purged (gallons) | Cum, <br> Volume Purged (gallons) (gallons) | Purge Rate (gpm) | Depth <br> to Water (ft BTOC) | (SU) | Temp. ( ${ }^{\circ} \mathrm{C}$ ) | Spec. Cond. ( $\mathrm{mS} / \mathrm{cm}$ ) | Dissolved Oxygen ( $\mathrm{mg} / \mathrm{L}$ ) | Salinity (\%) | $\begin{aligned} & \text { orp } \\ & \text { (mV) } \end{aligned}$ | $\begin{gathered} \text { Color } \\ \text { (describe) } \end{gathered}$ | $\begin{gathered} \text { Odor } \\ \text { (describes) } \end{gathered}$ | Turbidity |
| ,ou | 0.0 | 0.0 | 0.0 | 0.4 |  | 27.4 | 5.82 | 0.90 | 3.13 | 2.0 | lear | NA |  |
| 3 Sl | 0.100 | .2 | 0.06 |  | I | 27.4 | 4.85 | 1.06 | 1.1 | 25.6 |  |  |  |
|  | 0.00 | 1.80 | 0.06 |  | HO | 27.3 | H. 25 | 1.08 | 2.24 | $\frac{24.0}{42}$ |  |  | $\frac{2.8}{40.5}$ |
| 33 | 0.60 | 2.40 |  |  | ). | 21.3 | 3.95 | 1.11 | 2.07 | 50.6 |  |  | 70.5 |
|  | 0.60 | 3.00 | 0.06 |  | 5.42 | 27.4 | 3,78 | 1.15 | 2.98 | $-56.4$ |  |  | 72.4 |
| 3 | 0.60 | 3.100 | 0.06 | 9. 2 | 6.4 | 27.1 | 3.108 | 1.17 | 1.98 | -54.8 |  |  | 21.3 |
| 1404 | 0.80 | 3.90 | 0.06 | C,f | $i . \mathrm{H}$ | 27. | 3.08 | 1.19 | 1.8.0 |  |  |  | 21.3 |
| H01 | 0.70 | 4.20 | V. $1 \times$ | 9.55 | 5.3 | 7. | $\bigcirc$ | i. 19 | 1.88 | - |  |  | 8:4 |
| WELL CAPACITY (gal/ft): $\quad 0.75^{\prime \prime}=0.02 ; \quad \mathbf{1 "}^{\prime \prime}=0.04 ; \quad 1.25^{\prime \prime}=0.06 ; \quad 2^{\prime \prime}=0.16 ; \quad 3^{\prime \prime}=0.37 ; \quad 4^{\prime \prime}=0.65 ; \quad \mathbf{5}^{\prime \prime}=1.02 ; \quad 6^{\prime \prime}=1.47 ; \quad 12^{\prime \prime}=5.88$ TUBING INSIDE DIA. CAPACITY (gal/ft): $\quad 1 / 8^{\prime \prime}=0.0006 ; \quad 3 / 16^{\prime \prime}=0.0014 ; \quad 1 / 4^{\prime \prime}=0.0026 ; \quad 5 / 16^{\prime \prime}=0.004 ; \quad 3 / 88^{\prime \prime}=0.006 ; \quad 1 / 2^{\prime \prime}=0.010 ; \quad 5 / 8^{\prime \prime}=0.016$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |

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## GROUNDWATER SAMPLING LOG

## $\square$ SYSTEM ON ■SYSTEM OFF םNOT APPLICABLE (NO SYSTEM)



## PURGING DATA

| WELL <br> DIAMETER (inches): |  |  | TUBING $\quad 3 / 16$ |  | WELL SCREEN INTERVAL DEPTH: feet to |  |  | STATIC DEPTHTO WATER (feet): 322 |  |  | PURGE PUMP TYPCOR BAILER: |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL VOLUME PURGE: 1 WELL VOLUME $=$ (TOTAL WELL DEPTH - STATIC DEPTH TO WATER) $\times$ WELL CAPACITY(onlyffilterutif_applicable) |  |  |  |  |  |  |  |  |  |  |  |  |  |
| EQUIPMENT VOLUME PURGE:M-EQUIRMENT VOL. $=$ PUMP VOLUME + (TUBING CAPACIJY <br> (only fill out if applicable) |  |  |  |  |  |  |  |  |  |  |  |  |  |
| INITIAL PUMP OR TUBING DEPTH IN WELL (feet): $\mathcal{Q}$ |  |  | FINAL PUMP OR TUBING DEPTH IN WELL (feet): $\qquad$ |  |  |  | PURGING PINTATED AT: O82 25 |  |  | $\begin{aligned} & \text { PARGGAG } \\ & \text { ENDEDAT: } 4+5 \end{aligned}$ |  | $\underset{\text { TOTAL VOLUME }}{\text { TURER_(gallons): }} 4.8$ |  |
| Time | Volume Purged (gallons) | Cum. <br> Volume Purged (gallons) <br> (gallons) | Purge Rate (gpm) | Depth <br> to Water (ft BTOC) | $\begin{aligned} & \mathrm{pH} \\ & (\mathrm{SU}) \end{aligned}$ | Temp. ( ${ }^{\circ} \mathrm{C}$ ) | Spec. Cond. ( $\mathrm{mS} / \mathrm{cm}$ ) | Dissolved Oxygen (mg/L) | Salinity (\%os) | $\begin{aligned} & \text { ORP } \\ & (\mathrm{mV}) \end{aligned}$ | $\underset{\text { (describe) }}{\text { Color }}$ | $\begin{gathered} \text { Odor } \\ \text { (describe) } \end{gathered}$ | Turbidity (NTUs) |
| 0935 | Oilo | 0.6 | 0.06 | 9.45 | 5.63 | 27.8 | 3.05 | 0.13 | 1.57 | 62.2 | clan | menc | 176 |
| 0845 | 0.6 | 02 | 0.66 | 10.38 | 5.53 | 27.8 | 3.18 | 0.13 | 1.82 | 75.0 |  |  | 158 |
| O8s | 2. | 1.6 | 0.06 | 11.07 | 5.26 | 279 | 4.76 | 0.51 | 2.54 | 93.4 |  |  | $12-1$ |
| 0905 | $0 . \%$ | 2.4 | 0.06 | 11.77 | 5.24 | 278 | 4.76 | 0.50 | 2.53 | 102.2 |  |  | 15.2 |
| 0915 | 0.6 | 3.0 | 0.0 .6 | 12,31 | 5.21 | 27.8 | 4.88 | 0.55 | 2.56 | 103.3 |  |  | 16.6 |
| 09.25 | 0.6 | 3.6 | 0.06 | 12.94 | 5,08 | 277 | 5.39 | 0.40 | 2.91 | 114.4 |  | ) | 14.9 |
| 0985 | 0.6 | 42 | 0.06 | 13.43 | 5.19 | 277 | 4.33 | 0.54 | 2.29 | 108.3 |  |  | 17.7 |
| 0440 | 0.3 | 45 | 0.06 | 13.69 | 5.13 | 27.7 | 450 | 0.52 | 2.28 | 110.4 |  |  | 15.4 |
| 0945 | 0.3 | 4.8 | 0.06 | 13,90 | 5.16 | 77.7 | 4.44 | 0.54 | 2.31 | 109.6 |  |  | 13.9 |
| WELL CAPACITY (gal/ft): $0.75^{"}=0.02 ;$TUBING INSIDE DIA. CAPACITY (gal/ft): |  |  |  | $\begin{aligned} 1^{\prime \prime} & =0.04 ; \\ 1 / 8^{\prime \prime} & =0.0006 ; \end{aligned}$ | $\begin{array}{r} 1.25^{\prime \prime}=0.06 \\ 3 / 16^{\prime \prime}=0 \end{array}$ | $\begin{aligned} & 16 ; 2^{\prime \prime}= \\ & 0.0014 ; \end{aligned}$ | $\begin{aligned} & 3^{\prime \prime}=0 \\ & 1 / 4^{\prime \prime}=0.0026 ; \end{aligned}$ | $\begin{array}{r} 374^{\prime \prime}=0 . \\ 5 / 16^{\prime \prime}=0 . \end{array}$ | $\begin{array}{lrl} \hline .65 ; & 5^{\prime \prime}=1 \\ 004 ; & 3 / 8^{\prime \prime} \end{array}$ | $\begin{aligned} & 1.02 ; 6 "=1 \\ & "=0.006 ; \end{aligned}$ | $1.47 ;$ <br> $1 / 2^{\prime \prime}=0.010$ <br>  <br> 12 | $\begin{gathered} =5.88 \\ 5 / 8^{\prime \prime} \end{gathered}$ |  |
| PURGING EQUIPMENT CODES: |  |  | : $\quad \mathrm{B}=$ Bailer; $\quad \mathrm{BP}$ |  | P = Bladder Pump; |  | ESP = Electric Submersible Pump; |  |  | PP = Peristaltic Pump; |  | $0=0$ | Specify) |

## SAMPLING DATA



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ᄃ well needs repair__ $\quad$ _ needs well tag ___ $\qquad$ _ - other comment: $\qquad$ ก. DI Water Lot \# $\qquad$ $\square \mathrm{MS} / \mathrm{MSD}$ ——
$\qquad$ ᄃ Equip blk $\qquad$ -- Ambient blk $\qquad$ ᄃ. Trip blk $\qquad$

## GROUNDWATER SAMPLING LOG

$\square$ SYSTEM ON ᄃ SYSTEM OFF $\square$ NOT APPLICABLE (NO SYSTEM)


## PURGING DATA



## SAMPLING DATA



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$\square$ well needs repair $\qquad$ $\square$ needs well tag $\qquad$
$\qquad$ $\square$ other comment: $\qquad$

- DI Water Lot \# $\qquad$ $\sqsubset \mathrm{MS} / \mathrm{MSD}$ $\qquad$ コ Equip bilk $\qquad$ $\square$ Ambient blk -Trip blk
 VAS OK, CleAn Probe + Alow the cell stake sech e 1110


## GROUNDWATER SAMPLING LOG

$\square$ SYSTEM ON םSYSTEM OFF $\supseteq$ NOT APPLICABLE (NO SYSTEM)

| SITE NAME: SITE \\| |  | SITE SOCATION: <br> AS SACKSOMLNG | DATE: $6 / 12 / 17$ |
| :---: | :---: | :---: | :---: |
| $\begin{aligned} & \text { WELLNO: } \\ & \text { EKMW-11 } \end{aligned}$ | SAMPLE ID: Ckmunㅔ | $\begin{aligned} & \text { FREE PRODUCT: Y } \\ & \text { DEPTH TO PRODUCT (ft BTOC): } \end{aligned}$ | FIEL_D DUPLICATE: Y DUPLICATEID: |

## PURGING DATA

| $\begin{aligned} & \text { WELL } \\ & \text { DIAMETER (inches): } 2 \end{aligned}$ |  |  | TUBING $3 / 16$DAMETER (inches): |  | WELL SCREEN INTERVAL DEPTH: 19 feet to 23 feet |  |  | $\begin{aligned} & \text { STATIC DEPTH } \\ & \text { TO WATER (feet): } \end{aligned} 4.38$ |  |  | PURGE PUMP TYPEOR BAILER: |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| WELL VOLUME PURGE: 1 WELL VOLUME = (TOTAL WELL DEPTH - STATIC DEPTH TO WATER) $\times$ WELL CAPACITY(only filloutifi-applicabla) |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  | lonsfoot |  | feet) |  | ons |  |
| INITIAL PUMP OR TUBIN DEPTH IN WELL (feet): |  |  | FINAL PUMP OR TUBING DEPTH IN WELL (feet): |  |  |  | $\begin{aligned} & \text { PURGING } \\ & \text { INITATED AT: } / 430 \\ & \hline \end{aligned}$ |  |  |  |  |  |  |
| Time |  | Volum Purged (gallons) |  | Water (ft BTOC) | $\begin{aligned} & \text { P" } \\ & \text { (SU) } \end{aligned}$ | $\underset{\substack{\text { Temp. } \\\left(0^{\circ}\right)}}{ }$ | Spec. Cond. ( $\mathrm{ms} / \mathrm{cm}$ ) |  | Saliit | $\begin{aligned} & \text { ORP } \\ & \text { (mv) } \end{aligned}$ | Color | $\underset{\text { (descrif }}{\text { Oddo }}$ | (tarbidity |
| 1410 | 0. | 6 | ,06 | . 6.6 | , |  | S.3 | 0.08 |  | 17.4 |  | NO.ve | 25.7 |
| 1450 | 0.6 |  | . 06 | 9.47 | 5,55 | 26.4 | 5,31 | 0.08 | 2.85 | 15.6 |  |  |  |
| 1500 | 0.6 | 1.8 | 0.06 | 11.26 | 5.54 | 26.1 | 5.28 | 0.08 |  | 15.3 |  |  |  |
| 1510 | 0.6 | 2.4 | 0.06 | 11.43 | \% 54 | 259 | 5.27 | $0.0{ }^{\circ}$ | 283 | 148 |  |  |  |
| 150 | 0.6 | 3.0 | 0.06 | 11.81 | 5.55 | 26.1 | 5.33 | 0.07 | 2.87 | 15. |  |  |  |
| 1530 | 0.6 | 3.6 | 0.06 | 2.31 | 5 | 26.1 | 5.66 | 0.10 | 3,01 | 16.6 |  |  | 6.4 |
| 1540 | 0.6 | 42 | 0.06 | 12.52 | 5,55 | 26.3 | 5.66 | 0.09 | 3.16 | 11.8 |  |  | 8.58 |
| 154S | 0.3 | 4.5 | 0.06 | 12.69 | 5.56 | 26.3 | 5.69 | 0.09 | 3.20 | 10.9 |  |  | 5.56 |
| 15s0 | 0.3 | $4 \cdot 8$ | 0.06 | 12.80 | 5.58 | 26.4 | 5:70 | 0.09 | 3.21 | 10.7 |  | 1 | 7.76 |
|  PURGING EQUIPMENT CODES: |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |

## SAMPLING DATA



NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
2. STABLLIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
$\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTU; optionally $\pm 5$ NTU or $\pm 10 \%$ (whichever is greater)
J well needs repair $\qquad$ $\square$ needs well tag _ locking cap: $\qquad$ - $\square$ other comment: $\qquad$
$\checkmark$ DI Water Lot
$-\longrightarrow$ MS / MSD $\qquad$ Equip blk $\qquad$ ——Ambient blk $\qquad$ Trip blk $\qquad$

## GROUNDWATER SAMPLING LOG

$\square$ SYSTEM ON 〔 SYSTEM OFF $\square$ NOT APPLICABLE (NO SYSTEM)

| SITE NAME: $C_{3} 1, \in 1$ |  | SITE LOCATION: $\operatorname{MAS} A C L O W H M$ | DATE: < / / $1 / 10$ |  |
| :---: | :---: | :---: | :---: | :---: |
| WELL NO: 6 Man 13 | $\begin{gathered} \text { SAMPLEID: } \\ E K M C O \end{gathered}$ | FREE PRODUCT: $\quad$ Y DEPTH TO PRODUCT (ft BTOC): | FIELD DUPLICATE: $Y$ DUPLICATE ID: | N |

## PURGING DATA



## SAMPLING DATA



|  | $\square$ well needs repair |  | $\ulcorner$ needs well tag | - | $J$ locking cap: | - | $\square$ other comment: | - |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |

[^3]
## APPENDIX E LABORATORY ANALYSES CHAIN OF CUSTODY FORMS

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## Accutest Laboratories Southeast

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FA32283: Chain of Custody
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FA32320: Chain of Custody
Page 1 of 2









FA42355: Chain of Custody
Page 1 of 2


APPENDIX F GROUNDWATER MONITORING DATA SUMMARY

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Baseline Event - October 2014


First Comprehensive Event (March 2016) - 8 months of full system operaiton; 5 months since bioaugmentation


Re-Baseline Event (September 2016) - 6 months since shutdown after Stage 1 operation; before system re-start for Stage 2


## March 2017 - End of 5-month Stage 2 operation

|  |  | EKMW-01 | EKMW-02 | EKMW-03 | EKMW-04 | EKMW-05 | EKMW-07 | EKMW-09 | EKMW-10 | EKMW-11 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| pH | unit | 5.5 | 5.0 | 5.8 | 5.5 | 4.8 | 5.9 | 3.8 | 5.3 | 5.2 |
| ORP | mV | -79 | -58 | -43 | 4.5 | 4.9 | . 75 | 62 | 30 | 114 |
| Dissolved oxygen | mg/l | 0.1 | 0.2 | 0.1 | 0.1 | 0.3 | 0.1 | 1.4 | 0.2 | 0.1 |
| Analyte | Units |  |  |  |  |  |  |  |  |  |
| BROMIDE | $\mathrm{mg} / \mathrm{L}$ |  |  |  |  |  |  |  |  |  |
| TOTAL ORGANIC CARBON | $\mathrm{mg} / \mathrm{L}$ | 6.3 | 3.2 | 3.5 | 2.1 | 2.0 | 53.0 | 1.1 |  | 3.3 |
| Chloride | $\mathrm{mg} / \mathrm{L}$ |  |  |  |  |  |  | 1790 |  | 2430 |
| SULFATE | $\mathrm{mg} / \mathrm{L}$ |  |  |  |  |  |  | 22.8 |  | 36.5 |
| CALCIUM | $\mathrm{mg} / \mathrm{L}$ |  |  |  |  |  |  | 295 |  | 386 |
| IRON | $\mathrm{mg} / \mathrm{L}$ |  |  |  |  |  |  | 79.2 |  | 95.5 |
| MAGNESIUM | $\mathrm{mg} / \mathrm{L}$ |  |  |  |  |  |  | 85.3 |  | 86.3 |
| POTASSIUM | $\mathrm{mg} / \mathrm{L}$ |  |  |  |  |  |  | 6.3 | 12.4 | 8.1 |
| TDS (FILTERABLE) | $\mathrm{mg} / \mathrm{L}$ |  |  |  |  |  |  | 2950 | 1230 | 3770 |
| 1,1-DICHLOROETHENE | ug/L | 19.9 | 1.2 | 1.6 | 1.6 | 2.0 | 4.0 | 32 U | 1.6 U | 11 |
| cis-1,2-DICHLOROETHENE | ug/L | 1140 | 164 | 384 | 237 | 444 | 755 | 310 | 318 | 6890 |
| TETRACHLOROETHENE | ug/L | 400 | 144 | 32 | 70 | 603 | 55 | 9690 | 104 | 4660 |
| trans-1,2-DICHLOROETHENE | ug/L | 104 | 2 | 3 | 3 | 36 | 19 | 44 | 10 | 45 |
| TRICHLOROETHYLENE | ug/L | 168 | 8 | 23 | 37 | 159 | 53 | 533 | 129 | 1210 |
| VINYL CHLORIDE | ug/L | 3640 | 68 | 51 | 12 | 57 | 191 | 31 | 86 | 55 |
| METHANE | ug/L | 164 | 7890 | 5480 | 4100 | 339 | 7120 |  |  |  |
| ETHENE | ug/L | 294 | 123 | 54 | 12 | 23 | 106 |  |  |  |
| ETHANE | ug/L | 0.3 U | 0.3 U | 0.3 U | 0.3 | 0.3 U | 0.3 U |  |  |  |
| Total VFA | $\mathrm{mg} / \mathrm{L}$ | 14.1 | $<1$ | 7.5 | 1.1 | 0.1 | 204.7 |  |  |  |

## June 2017-3 Months post Stage 2 operation

|  |  | EKMW-01 |  | EKMW-02 |  | EKMW-03 |  | EKMW-04 |  | EKMW-05 |  | EKMW-07 |  | EKMW-08 |  | EKMW-09 |  | EKMW-10 |  | EKMW-11 |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| pH | unit | 5.7 |  | 6.4 |  | 6.3 |  | 6.9 |  | 5.7 |  | 6.2 |  | 5.4 |  | 5.2 |  | 6.3 |  | 5.6 |  |
| ORP | mV | -161 |  | -70 |  | -79 |  | $\begin{array}{r}-173 \\ \hline 1.5\end{array}$ |  | -390.4 |  | -880.9 |  | -57 |  | 109 |  | 1010.1 |  | 11 |  |
| Dissolved oxygen | mg/ | 1.1 |  | 0.7 |  | 1.4 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| Analyte | Units | Result | Qual | Result | Qual | Result | Qual | Result | Qual | Result | Qual | Result | Qual | Result | Qual | Result | Qual | Result | Qual | Result | Qual |
| BROMIDE | mg/L | 4.5 | 1 | 2.6 | 1 | 1.2 | U | 0.6 | U | 3.0 | U | 3.0 | U | 1.2 | U | 3.0 | U | 1.2 | U | 6.0 | U |
| TOTAL ORGANIC CARBON | mg/L | 20.1 |  | 3.9 |  | 3.0 |  | 2.6 |  | 2.1 |  | 57 |  | 2.1 |  | 1.9 |  | 10.1 |  | 3.3 |  |
| CHLORIDE | mg/L | 1950 |  | 756 |  | 717 |  | 465 |  | 1570 |  | 1670 |  | 1300 |  | 1630 |  | 793 |  | 2220 |  |
| Sulfate | mg/L | 15 | u | 6 | u | 7.7 |  | 17 |  | 27.3 | 1 | 15 | u | 15.5 |  | 23.4 | 1 | 22.9 |  | ${ }^{41.8}$ | 1 |
| CALCIUM | mg/L | 229 |  | 202 |  | 174 |  | 115 |  | 229 |  | 419 |  | 258 |  | 296 |  | 166 |  | 345 |  |
| IRON | mg/L | 93.4 |  | 103 |  | 99 |  | 56.3 |  | 92.4 |  | 85.1 |  | 80.9 |  | 78.1 |  | 49.5 |  | 104 |  |
| MAGNESIUM | mg/L | 57.7 |  | 54.4 |  | 53 |  | 31.3 |  | 55.8 |  | 56.9 |  | 72 |  | 77.8 |  | 47.7 |  | 73.7 |  |
| POTASSIUM | mg/L | 5.9 | 1 | 4.94 | 1 | 5.86 | 1 | 3.6 | 1 | 6.2 | 1 | 16.3 |  |  |  | 5.9 | 1 | 21.4 |  |  |  |
| TDS (FILTERABLE) | mg/L |  |  |  |  |  |  |  |  |  |  |  |  |  |  | 3890 |  | 2040 |  |  |  |
| 1,1-DICHLOROETHENE | ug/L | ${ }^{21}$ |  | 0.7 | 1 | 1.6 | U | 0.8 | U | 6 | 1 | 8 | 1 | 3 | U | 32 | U | 1.6 | U | 32 | U |
| cis-1,2-DICHLOROETHENE | ug/L | 783 |  | 167.0 |  | 376 |  | 277 |  | 2,160 |  | 2,250 |  | 813 |  | 204 |  | 312 |  | 5,920 |  |
| Tetrachloroethene | ug/L | 406 |  | 44.9 |  | 13.8 |  | 41.1 |  | 3,540 |  | 92.4 |  | 593 |  | 8,930 |  | 55.3 |  | 5,850 |  |
| trans-1,2-DICHLOROETHENE | ug/L | 94.1 |  | 2.0 |  | 2.1 | 1 | 2.7 |  | 170 |  | 34.8 |  | 28.4 |  | 37.9 |  | 11.3 |  | 22 | u |
| TRICHLOROETHYLENE | ug/L | 311 |  | 7.9 |  | 15 |  | 27.4 |  | 699 |  | 75.2 |  | 64.3 |  | 499 |  | 93.1 |  | 1,430 |  |
| VINYL CHLORIDE | ug/L | 4780 |  | 36.2 |  | 36 |  | 12 |  | 379 |  | 724 |  | 32.3 |  | 41 | $\cup$ | 157 |  | 62.1 |  |
| METHANE | ug/L | 399 |  | 8740 |  | 7930 |  | 5010 |  | 987 |  | 8200 |  |  |  |  |  |  |  |  |  |
| ETHENE | ug/L | 1280 |  | 119 |  | 69 |  | 7.6 |  | 192 |  | 260 |  |  |  |  |  |  |  |  |  |
| EthANE | ug/L | 0.3 | U | 0.3 | $\cup$ | 0.3 | $u$ | 0.3 | $\cup$ | 0.3 | $\cup$ | 0.3 | $\cup$ |  |  |  |  |  |  |  |  |
| Dhc | cell/L | $1.96 \mathrm{E}+09$ |  | $2.98 \mathrm{E}+06$ |  | 3.70E+06 |  | 2.60E+06 |  | 2.44E+07 |  | $1.52 \mathrm{E}+08$ |  |  |  | <5000 |  | 1.60E+03 |  |  |  |
| tce | cell /L | $2.66 \mathrm{E}+08$ |  | 7.33E+04 |  | 2.23E+05 |  | $5.03 \mathrm{E}+05$ |  | 3.76E+06 |  | $1.11 \mathrm{E}+07$ |  |  |  | <5000 |  | $2.00 \mathrm{E}+03$ | J |  |  |
| bvc | cell /L | $2.08 \mathrm{E}+08$ |  | 9.13E+04 |  | 6.12E+04 |  | 2.30E+05 |  | $8.01 \mathrm{E}+05$ |  | $7.22 \mathrm{E}+06$ |  |  |  | <5000 |  | <5000 |  |  |  |
|  | cell / | 5.23E+08 |  | 8.37E+05 |  | 1.69E+06 |  | $8.59 \mathrm{E}+05$ |  | 4.80E+06 |  | 1.11E+06 |  |  |  | <5000 |  | <5000 |  |  |  |
| Dhb | cell /L | $6.60 \mathrm{E}+07$ |  | 4.39E+05 |  | $1.72 \mathrm{E}+06$ |  | 2.33E+04 |  | $2.36 \mathrm{E}+06$ |  | $<5000$ |  |  |  | <4000 |  | <5000 |  |  |  |
| Total VFA | mg L | 57.6 |  | $<1$ |  | $<1$ |  | 3.1 |  | $<1$ |  | 195.9 |  |  |  |  |  |  |  |  |  |

Grab Groundwater From Soil Core Locations (June 2017)

|  |  | C1 |  | C2 |  | C3 |  | C6 |  | C7 |  | C9 |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Analyte | Units | Result | Qual | Result | Qual | Result | Qual | Result | Qual | Result | Qual | Result | Qual |
| TOTAL ORGANIC CARBON | mg/L | 6.1 |  | 950 |  | 160 |  | 3.4 |  | 820 |  | 790 |  |
| 1,1-DICHLOROETHENE cis-1,2-DICHLOROETHENE TETRACHLOROETHENE trans-1,2-DICHLOROETHENE TRICHLOROETHYLENE VINYL CHLORIDE | ug/L <br> ug/L <br> ug/L <br> ug/L <br> ug/L <br> ug/L | $\begin{gathered} \hline \hline 6 \\ 4300 \\ 3500 \\ 630 \\ 1300 \\ 290 \end{gathered}$ |  | $\begin{gathered} \hline 0.2 \\ 86 \\ 11 \\ 31 \\ 5 \\ 1200 \end{gathered}$ | U | $\begin{gathered} \hline 5 \\ 3700 \\ 160 \\ 470 \\ 430 \\ 570 \\ \hline \end{gathered}$ |  | $\begin{gathered} \hline 3 \\ 2600 \\ 1400 \\ 410 \\ 660 \\ 380 \\ \hline \end{gathered}$ |  | $\begin{gathered} \hline 0.4 \\ 220 \\ 28 \\ 35 \\ 29 \\ 330 \end{gathered}$ | U | $\begin{gathered} \hline \hline 4 \\ 1900 \\ 250 \\ 140 \\ 67 \\ 5000 \end{gathered}$ |  |
| METHANE <br> ETHENE <br> ETHANE | ug/L ug/L ug/L | $\begin{gathered} 458 \\ 65 \\ 2 \\ \hline \end{gathered}$ |  | $\begin{gathered} \hline 2490 \\ 1710 \\ 18 \\ \hline \end{gathered}$ |  | $\begin{gathered} \hline 3840 \\ 474 \\ 12 \\ \hline \end{gathered}$ |  | $\begin{gathered} 634 \\ 100 \\ 5 \\ \hline \end{gathered}$ | 1 | $\begin{gathered} \hline 4090 \\ 1880 \\ 6 \\ \hline \end{gathered}$ |  | $\begin{gathered} \hline 259 \\ 402 \\ 3 \\ \hline \end{gathered}$ |  |
| Dhc tce bvc vcr Dhb | cell / L <br> cell / L <br> cell / L <br> cell / L <br> cell / L | $\begin{gathered} \hline \hline<3 \mathrm{E}+04 \\ \text { NA } \\ \text { NA } \\ \text { NA } \\ <3 \mathrm{E}+04 \\ \hline \end{gathered}$ |  | $\begin{aligned} & \hline \hline 5.00 \mathrm{E}+06 \\ & 1.00 \mathrm{E}+06 \\ & 5.00 \mathrm{E}+05 \\ & 4.00 \mathrm{E}+06 \\ & 1.00 \mathrm{E}+04 \end{aligned}$ |  | $\begin{gathered} \hline \hline 2.00 \mathrm{E}+05 \\ 5.00 \mathrm{E}+04 \\ 4.00 \mathrm{E}+03 \\ 1.00 \mathrm{E}+05 \\ <4 \mathrm{E}+03 \\ \hline \end{gathered}$ |  | $\begin{aligned} & \text { 2.00E+03 } \\ & <3 \mathrm{E}+04 \\ & <3 \mathrm{E}+04 \\ & <3 \mathrm{E}+04 \\ & <3 \mathrm{E}+04 \\ & \hline \end{aligned}$ | J | $\begin{aligned} & \hline \hline 2.00 \mathrm{E}+07 \\ & 4.00 \mathrm{E}+06 \\ & 1.00 \mathrm{E}+06 \\ & 1.00 \mathrm{E}+07 \\ & 3.00 \mathrm{E}+05 \end{aligned}$ |  | $\begin{gathered} \hline \hline<4 \mathrm{E}+04 \\ \text { NA } \\ \text { NA } \\ \text { NA } \\ <4 \mathrm{E}+04 \end{gathered}$ |  |


[^0]:    NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
    2. STABILIZATION CRITERIA FOK RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3 )
    $\mathrm{pH}: \pm 0.2$ units Temperature: $\neq 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater)

[^1]:    NOTES: 1. The above do not constitute all of the information required by Chapter $62-160$, F.A.C.
    2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
    $\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTU; optionally $\pm 5$ NTU or $\pm 10 \%$ (whichever is greater)

[^2]:    NOTES: 1. The above do not constitute all of the information required by Chapter 62-160, F.A.C.
    2. STABILIZATION CRITERIA FOR RANGE OF VARIATION OF LAST THREE CONSECUTIVE READINGS (SEE FS 2212, SECTION 3)
    $\mathrm{pH}: \pm 0.2$ units Temperature: $\pm 0.2^{\circ} \mathrm{C}$ Specific Conductance: $\pm 5 \%$ Dissolved Oxygen: all readings $\leq 20 \%$ saturation (see Table FS $2200-2$ ); optionally, $\pm 0.2 \mathrm{mg} / \mathrm{L}$ or $\pm 10 \%$ (whichever is greater) Turbidity: all readings $\leq 20$ NTÜ; optionally $\pm 5$ NTU or $\pm 10 \%$ (whichever is greater)

[^3]:    - DI Water Lot \# $\qquad$
    $\qquad$ $\square$ Ambient bik $\qquad$ $\square$ Trip blk $\qquad$

