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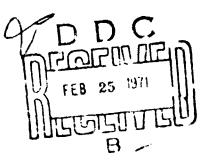
AIR-AUGMENTED COMBUSTION OF BORON AND BORON-METAL COMPOUNDS

Henry T.-S. Hsia United Technology Center

SEMIANNUAL REPORT AFRPL-TR-71-10
Junuary 1971
CONTRACT NO. FO4611-70-C-0065

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United States Air Force
Air Force Systems Command
Air Force Rocket Propulsion Laboratory
Edwards, California 93523



UTC 2385-SAR

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FOREWORD

This report covers research performed during the period 15 May 1970 through 15 November 1970 and is submitted by the author 15 January 1971. This report contains no classified information extracted from other classified documents.

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LABORATORY HAVING

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This technical report has been reviewed and is approved.

Alan W. McPeak, Captain, USAF Project Engineer, Liquid Rocket Division Air Force Rocket Propulsion Laboratory

ABSTRACT

Under Contract No. AF04(611)-70-C-0065, United Technology Center has completed the first 6 months of a 12-month program to investigate the ignition delay times, burn times or rates and combustion efficiencies of doped and undoped boron and compounds of boron with aluminum, magnesium, and lithium. A literature survey has been conducted for information on the properties and combustion of aluminum, magnesium and lithium borides. An optical burner apparatus built under a previous Air Force contract, AF04 (611)-11544, has been modified and calibrated for the present investigation. Eight borides, which have been obtained or prepared for this program, were analyzed for purity on the basis of chemical, spectrographic, or X-ray data, and are ready for test.

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SECTION I

INTRODUCTION AND SUMMARY

With the current development of air-augmented rocket and Scramjet systems much interest has arisen in the use of solid fuel particles as high-energy additives to the liquid or solid primary propellants. Boron has outstanding potential as an additive to propellants because of its high volumetric heat of combustion However, this potential can only be realized if with oxygen. efficient combustion of the boron with oxygen in air is attained in the ramburner over the desired wide range of flight altitudes and Mach numbers. Work to date has shown a direct relationship between ramburner pressure and boron combustion efficiency: ramburner pressure leads to poor performance. Previous work sponsored by the Air Force has suggested that the use of catalytic dopants, for example, a coating of LiF deposited on the boron particle surface may facilitate combustion by lowering the particle ignition temperature even at low pressures. Another approach is to replace elemental boron with a boron compound or alloy such as AlB_X , MgB_X or LiB_X . The objective of this program is to evaluate the merits of using such compounds of boron and doparts. The program involves three closely related phases:

- A. Phase I: A literature survey for available information from both U.S. and foreign cources on compounds or alloys of boron will be conducted. Selected physical properties and compositions of each compound, alloy or mixture are determined as needed.
- B. Phase II: Combustion testing of the compounds and discrete mixtures selected in Phase I is to be accomplished in this phase. The combustion testing is conducted in the optical burner apparatus constructed at UTC under Contract AF04(611)-11544. Photography and chemical analysis of the residues are the primary data gathering methods.
- C. Phase III: This phase consists of the data reduction, presentation and recommendations derived as a result of the work accomplished under Phases I and II.

This report summarizes the work accomplished in Phase I and a portion of Phase II. In Phase I, the available literature on aluminum, magnesian, and lithium borides, which is mostly of foreign origin, was reviewed; synopses of the pertinent information are given herein. Eight borides which have been obtained or prepared for the program were analyzed for purity on the basis of chemical, spectrographic,

or X-ray data. In Phase II, the burner apparatus has been modified and calibrated for operation with a CO-O₂-air system at 5, 10, 15, 25, and 40 psia and at 1700° and 2000°K. Particles of boron, MgB₂, and LiB₂ were added in some demonstration test runs. Traces of burning particles showed fairly straight trajectories which allow the ignition and burning times to be determined. The parametric testing of various sizes of elemental boron and of all the borides obtained is about to be carried out under various pressure and temperature conditions.

SECTION II

TECHNICAL DISCUSSION

It is well known that several of the low atomic weight metals are excellent rocket fuels. Heats of combustion data (table I) indicate that when heat evolved per unit weight of metal oxide is taken as a measure of metal fuel value, boron, aluminum, lithium, and magnesium are better fuels than carbon and hydrogen. volume-limited vehicle system, boron appears most attractive because of its high heat of combustion per unit volume. However, in practice boron in powder form has been found to be more difficult to burn than other metal powders. This can be attributed $^{(1)}$ * to the fact that the boiling point of boron oxide lies below that of boron itself. Thus, combustion must take place on the surface of the metal particle. On the other hand, the boiling points of the oxides of aluminum, lithium, and magnesium lie above that of each respective metal, so that the metal burns in the vapor phase. Thus it has been shown both theoretically and experimentally that boron differs considerably from other light metals in its combustion properties.

1. BACKGROUND

Ignition of metal fuel particles can take place only when they have been heated to their ignition temperature. Initially, heat is supplied primarily by convection, and the heating time is proportional to the square of the particle diameter. As the particle temperature increases, heating by surface reactions becomes important; the heating rate accelerates and becomes proportional to the particle diameter. Most of the total time to ignition is spent in the slow convective heating regime, and this ignition delay time is usually roughly proportional to the particle diameter squared.

The particle temperature history is given by the solution of the followi.g equation (2)

$$\frac{d T_p}{dt} = \frac{6}{\rho_p C_p d} \left[\frac{k_g Nu}{d} \left(T_g - T_p \right) - \sigma \epsilon T_p^4 \right]$$
 (1)

where ${\bf k_g}$ denotes the thermal conductivity of the gas, Nu the Nusselt number, ρ_p the density, ${\bf C_p}$ the heat capacity, ${\bf T_p}$ the

^{*}Parenthetical numbers cript numbers denote references appearing on page 35.

TABLE I

PROPERTIES OF FUELS

Fuel	Density g/cm ³	Molecular	Density Molecular Weight	Heat of Combusticn Unit Weight of Oxide kcal/g	Heat of Combustion Unit Weight of Fiel kcal/g	Heat of Combustion Unit Volume of Fuel kcal/cm ³
Boron	2.37	10.82	0.231	3.02	14.0	33.2
Aluminum	2.70	26.97	0.100	3.93	7.4	20.0
Magnesium	1.74	24.32	0.0716	3.56	2.900	10.30
Lithium	0.53	6.94	0.0763	4.43	9.540	5.05
Carbon	2.25	12.01	0.1875	2.14	7.830	17.63
Hydrogen	0.063	2.02	0.0312	3.21	28.900	1.82

particle temperature, $T_{\bf g}$ the gas temperature, d the diameter, σ the Stefan-Boltzmann constant, and ε the emissivity of the particle.

The equation shows that a high value of Nu and a low value of $^{\rho}_{\rm p}C_{\rm p}$ lead to rapid heating of the particle; this is true for lithium, magnesium, and aluminum. Aluminum has an ignition temperature similar to that of boron, and those of magnesium and lithium are considerably lower. Thus, the ignition delay of these three metals will be shorter than that of boron. Compounds or alloys of these metals with boron will also have a different heatup profile and lower ignition delay time than pure boron.

Previous studies have indicated that three different controlling mechanisms are involved in determining the combustion time of metal particles. Boron apparently burns by the diffusion of the oxidizing species to the particle surface, followed by surface reaction and diffusion of the gaseous combustion products away from the surface. (3,4) This sequence occurs because the vapor pressure of boron oxide exceeds that of boron at the combustion temperature. The combustion rate in this case is limited by the rate of diffusion of the oxidizer through the combustion products. A theory developed by Spalding (5) indicates that the burning time is proportional to the square of the initial particle diameter, is independent of pressure, and depends only slightly on temperature.

Belyaev⁽⁶⁾ has recently made a successful correlation of aluminum particle burning rates in fuel-rich gases, assuming that water and carbon dioxide are equally effective oxidants. If there is more than one oxidizing species, j, in the gas, Macek and Semple⁽²⁾ suggested a generalized expression to calculate the burning time, t, of a metal particle with original diameter, d, as

$$\frac{1}{t} = \sum_{j} \frac{1}{t_{j}} = \frac{8\delta}{(\rho_{p}/M)} \frac{\sum_{j} \frac{\beta_{j} P_{j}}{\gamma_{j}}}{\sum_{j} \frac{\beta_{j} P_{j}}{\gamma_{j}}}$$
(2)

where $^{\rho}p/M$ denotes the molar density of the metal particle given in Table I, and δ the ratio of flame to particle diameter ($\delta > 1$ for vapor phase combustion, e.g., 2.7 for aluminum; $\delta = 1$ for surface burning, e.g., boron). $\beta = D/RT_g$ where D is the diffusion coefficient, R the gas constant, and T_g the gas temperature. $\frac{P_s = P \ln \frac{1}{1-X}}{1-X}$ where X is the mole fraction, P the static pressure, and 7 the stoichiometric fuel-oxidant coefficient (e.g., 3/4 for the reaction of boron or aluminum with oxygen).

When the diffusion contribution of carbon dioxide is included, the calculated burning times in dry gases agree with the experiment to within 10% to 20%. Typical burning times for boron were

found to be 12 to 15 msec and 20 to 25 msec for 35 μ and 44 μ particles, respectively. The burning times decreased slightly with increasing gas temperature.

A shock tube study was conducted by $Uda^{(7)}$ to determine the ignition limit of clouds of boron particles in air. The boron samples, consisting of 30μ to 50μ agglomerates (1μ to 2μ primary particles) and 0.015μ particles, were ignited in the high-temperature region behind the reflected shock wave. The 30μ to 50μ agglomerated particles ignited at a reflected shock temperature of about 1.900° K at 1-atm pressure. The ignition temperature decreased steadily with increasing pressure, to about 1.400° K at 20 atm. Ignition of the 0.015μ particles appeared to be insensitive to pressure, and the ignition temperature stayed constant at 1.150° K. For a constant reflected shock pressure, the ignition temperature decreased with decreasing particle size. The ignition delay time of the 0.015μ particles decreased as the reflected shock temperature increased. It was less than 1 msec at 1.140° K and decreased to less than 0.1 msec above 1.400° K.

The studies of boron combustion thus indicate that ignition and burning are sensitive to pressure and temperature conditions, particle size, type of oxidizing environment, and particle concentration. As indicated by equations 1 and 2, the properties of other metals such as lithium, magnesium, and aluminum, if used in conjunction with boron, will contribute to shorter ignition delay and burning times. The shorter burning time is due mainly to the fact that these metal particles burn by a vapor phase mechanism. It seems to be logical to consider compounds or mixtures of boron and these other metals as candidate fuels.

In evaluating boron-rich solid propellants for air-augmented systems, Sims, Lee, and Gonzales (8) replaced boron with boron compounds, including ZrB2, B4C, TiB2, AlB12, and MgB2. Some promising data were obtained, but the exploratory investigation was too limited to provide systematic results.

In another approach, some experimental results indicate that the ignition temperature of powdered boron in oxygen can be remarkedly decreased by the addition of doping impurities (9) to the metal. LiF is one of the promising dopants, which probably increases the diffusion of boron ions through the oxide surface layer or increases the oxygen diffusion through the oxide film. The ignition temperature of the 1% LiF doped boron was reduced by 160°C.

In a recent air-augmentation combustion study, Rosenberg, et al. (10) deposited LiF on the surface of boron particles and found that the combustion rate of these products was increased.

2. METAL BORIDES

As discussed in the preceding sub-section, the physical and thermochemical properties of the candidate borides or alloys of boron with other metals will control their heat-up, ignition and burning characteristics when they are used as particulate fuel additives in a secondary combustion system, and thus will determine how their performance will compare with that of boron alone. For instance, they may provide an increase of overall fuel density with little loss in energy released. In general, all the metal borides have very high melting points and are known as refractory materials. (11) Since metal borides have not been considered previously as fuel additives, their thermochemical properties are not readily available. The following subsections summarize accessible data, mostly taken from foreign publications.

a. Aluminum Borides

There are five reported and authenticated phases in the aluminum boron system $^{(12)}\colon$ AlB2, AlB10, $\alpha\text{-AlB}_{12},$ $\beta\text{-AlB}_{12},$ Y-AlB12. No information has been found on AlB6. The three forms of AlB12 and AlB10 are hard materials with structures similar to boron or boron carbide, whereas AlB2 is a soft graphite-like material of hexagonal structure. Some of the physical properties of aluminum borides are shown in Table II.

TABLE II

PHYSICAL PROPERTIES OF ALUMINUM BORIDES

Boride	Crystal Structure	Theoretical Density g/cm ³	Melting Point °F
AlB ₂	Hexagonal	3.16	3,010 <u>+</u> 90
AlB ₁₀	Orthorhombic	2.54	4,390+90
lpha-AlB ₁₂	Tetragonal	2.58	3,925±90
β -AlB ₁₂	Orthorhombic	2.60	4,015±90
Y-A1B ₁₂	Orthorhombic	2.56	-

Serebryanskii and Epel'baum $^{(13)}$ reported that the boron-containing specimens were prepared from pure elemental aluminum and boron in a tubular furnace. They give the phase composition in relation to specimen composition and synthesis temperature as shown in table III.

Formation and decomposition processes of aluminum borides were investigated by Atoda et al $^{(14)}$ using Differential Thermal Analysis, X-ray and chemical analysis techniques on samples prepared in an electric furnace. AlB₂ begins to form at 600° C and decomposes into the α -AlB₁₂ phase above 920°C. The latter is stable up to at least 1900°C; it decomposes above 1900°C, separating elemental Al.

The energies of combustion of AlB2 and α -AlB12 were measured by Domalski and Armstrong (15) in a bomb calorimeter using flourine as the oxidant. From the data obtained in these experiments the heats of formation of AlB2 and α -AlB12 were calculated as -16 +3 and -48 +10 kcal/mol, respectively. The lack of precision in these values is due to uncertainties in the impurity corrections and in the heats of formation of the combustion products.

b. Magnesium Borides

The magnesium-boron system displays a wide range of mutual solubility: MgB_2 will dissolve in magnesium; on the other hand, if MgB_2 is heated above 300°C, it will lose magnesium progressively to form MgB_4 , MgB_6 and MgB_{12} . (11) The magnesium borides (16) react with free oxygen, MgB_2 at 580°C and and MgB_4 at 400°C, but the reactions are not complete at 1100°C. MgB_2 reacts with water and with HCl at 15°C to produce 97% hydrogen and 3% boranes; MgB_4 reacts only with boiling HCl while the other borides do not react at all.

The heat of formation of MgB $_{12}$ was estimated as -34.4 kcal/mol $_{17}^{(17)}$ Information on the heats of formation of other magnesium borides has not yet been found.

c. Lithium Borides

Information on lithium borides is scarce. Markovskii and Kondrashev $^{(18)}$ reported that as a result of the electrolysis of lithium borate, a product was obtained containing 82.9% B and 9.4% Li, probably a mixture of elemental boron and LiB6. No other lithium borides are mentioned in the open literature.

TABLE III

PHASE COMPOSITION OF ALUMINUM BORIDES

Origina	Original composition			S	nthesi	Synthesis temperature, °C	ature,	၁့			
ж Д	8 A1	650°	700°	800°	006	950°	1000°	1100°	1000° 1100° 1200° 1300°	1300°	1400°
	71.1		AlB	AlB ₂ , Al		AlB2					
	55. T					WT.		ช	α -AlB, +Al		
61.9	38.1								7 7		
	29.1										
	23.5	AlB,+Al	+A1	AlB2		\a-AlB12					
	19.7					1					
	17.5							a	$^{\alpha}$ -AlB ₁₂		

d. Estimated Heat Release of Borides

In the absence of information on the heats of formation of most of the borides considered in this program, the heat release from the reaction of the borides with oxygen was calculated on the basis of heat release data on each of the two component elements. The results are compared to pure boron in Table IV.

From the viewpoint of volumetric heat release, the lithium borides appear to be the best fuel additives among the metal borides, followed by the aluminum and the magnesium borides.

e. Analysis of Test Samples

All the nine (9) compounds specified in the program, i.e. AlB2, AlB6, AlB12, MgB2, MgB6, MgB12, LiB2, LiB6 and LiB12, were obtained in the form of chemical compounds except AlB6. No information could be found in the literature on AlB6 and it probably does not exist as a compound. The other compounds are either available commercially or were specially synthesized for this program. The purity of each boride was determined from chemical, spectrographic or X-ray diffraction analyses as summarized in table V.

The MgB6 obtained shows a medium pattern of MgB2 and a weak pattern of MgB12; and the LiB6 shows a strong pattern of LiB12 and a weak pattern of LiB2. It is likely that MgB6 and LiB6 are unstable and temperature dependent; although formed in the synthesis process at high temperature, they may be transformed into other borides during the cooling period.

Scanning electron beam micrographs were taken of all the borides at 300, 1000 and 3000 magnification. Micrographs of an elemental boron were also taken for reference. In the following micrographs the borides appear as agglomerates of amorphous particles of various sizes (Figure 1, 2 and 3).

3. EXPERIMENTS

The major components of the test facility are the optical burner apparatus, a gas supply system, an optical system for high speed photography, a device for exhaust residue sampling, a control console and sequencer for remote control of ignition, flow valves, camera and particle sampling, plus electronic recording equipment monitoring pressures and temperatures. The general arrangement of the test setup is shown in Figures 4 and 5.

TABLE IV

ESTIMATED HEAT RELEASE OF BORIDES RELATIVE TO BORON

	B	A1B2	AlB6	AlB ₁₂	MgB2	MgB6	MgB ₁₂	LiB2	LiB6	LiB ₁₂
Heat release per unit weight of fuel relative to boron	1.0	.798	. 895	. 942	. 598	.780	.871	.730	.730 .895 .944	.944
Volumetric heat release relative to boron	1.0	.740	.860	.860 .918	769.	.840	.911	.918	968	.982

TABLE V

Borides	Wet	Chemical	Analysis	ANALYSIS OF BORIDES Spectrographic Analysis(b)	X-Ray Analysis
AlB ₂ Al (55.2/44.4) ^(a) C N		55.2% 0.18% 0.18%	B 43.9% H 0.002% O 0.61%		AlB ₂ Medium weak pattern AlB ₁₂ Trace Al ₂ 03 Trace Al Medium pattern
AlB12 (17.1/82.9)	Al Fe C Zr	18-208 0.058 0.8% 0.18	B 78-81% Si 0.2% Mg 0.5%		AlB ₁₂ α-phase good pattern Al ₂ 0 ₃ 5 weak lines of -phase
MgB ₂ (52.9/47.1)	₩.	52.68		Si 0.01-0.1% Mn 0.03-0.3% Cu 0.003-0.3% Fe 0.03-0.3% Pb 0.003-0.03% Al 0.01-0.01%	MgB ₂ Strong pattern MgB ₄ Trace MgO Trace
MgB ₆ (27.3/72.7)	Мg	26.97%		Si 0.01-0.1% Mn 0.03-0.3% Cu 0.003-0.3% Fe 0.03-0.3% Pb 0.003-0.03% Al 0.01-0.01%	MgB ₂ Medium pattern(c) MgB ₁₂ Weak pattern MgO Trace
MgB12 (15.8/84.2)	М _Ф	15.25%	i	Si 0.01-0.1% Mn 0.03-0.3% Cu 0.003-0.3% Fe 0.03-0.3% Pb 0.003-0.03% Al 0.01-0.01%	MgB ₁₂ Strong pattern MgB ₂ Trace
LiB ₂ (24.3/75.7)	ŗ.	24.18		Si 0.01-0.1% Mn 0.03-0.3% Cu 0.003-0.3% Fe 0.03-0.3% Pb 0.003-0.03% Al 0.01-0.01%	Perfect pattern
LiB ₆ (9.8/90.2)	Ľį	9.79%		3i 0.01-0.1% Mn 0.03-0.3% Cu 0.003-0.3% Fe 0.03-0.3% Pb 0.003-0.03% Al 0.01-0.01%	LiB ₁₂ Strong pattern(d) LiB ₂ Weak pattern
LiB ₁₂ (5.1/94.9)	Li	5.28		Si 0.01-0.1% Mn 0.03-0.3% Cu 0.003-0.3% Fe 0.03-0.3% Pb 0.003-0.03% Al 0.01-0.01%	Perfect pattern

Number in parenthesis is the weight ratios, metal to boron All the same as same source of ray materials were used No MgB₆ detected although chemistry was perfect No AlB₆ detected although chemistry was perfect g (c) (b) (c) Note:

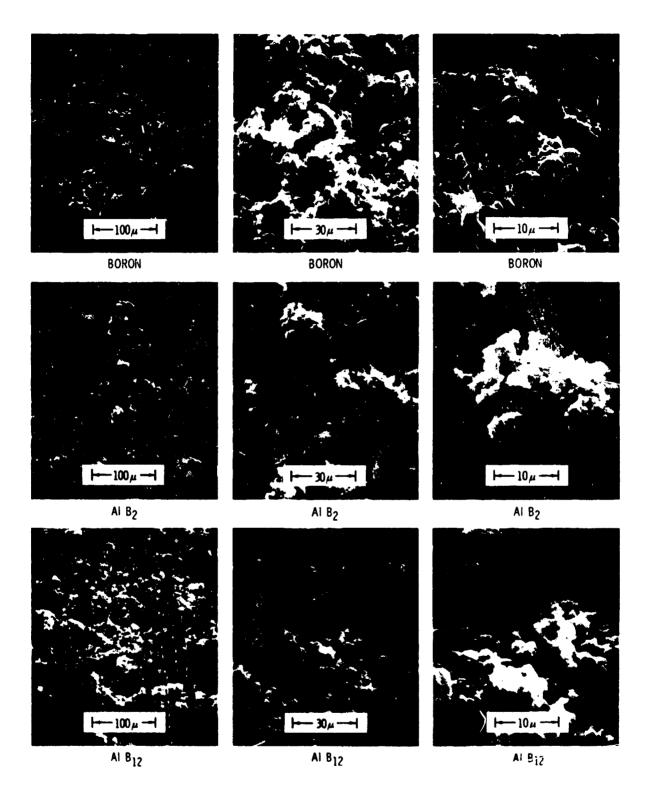


Figure 1. Scanning Electron Micrographs of Boron (325 mesh) and Aluminum Boride (AlB2-200 mesh, AlB12-325 mesh) Powders 01496

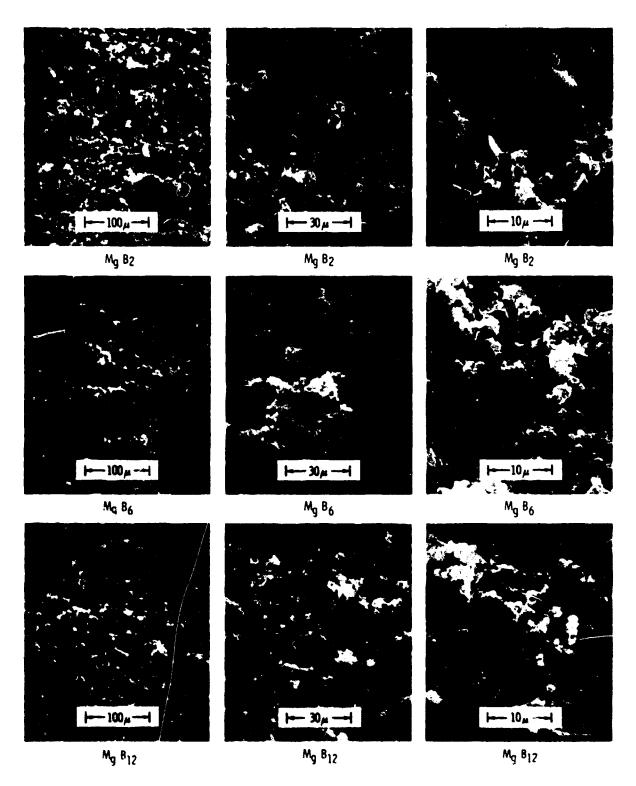


Figure 2. Scanning Electron Micrographs of Magnesium Boride Powders (MgB $_2$ -200 mesh, MgB $_6$ and MgB $_{12}$ -325 mesh)

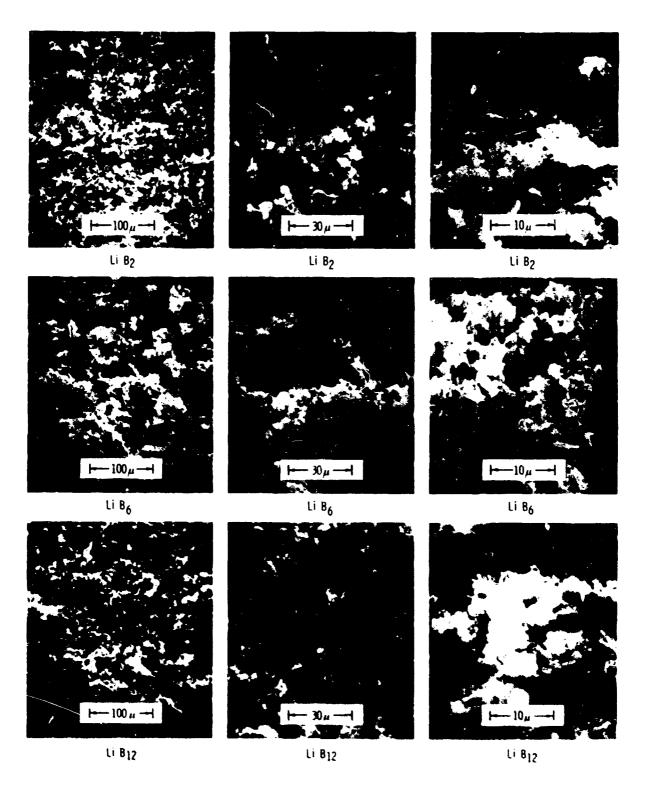
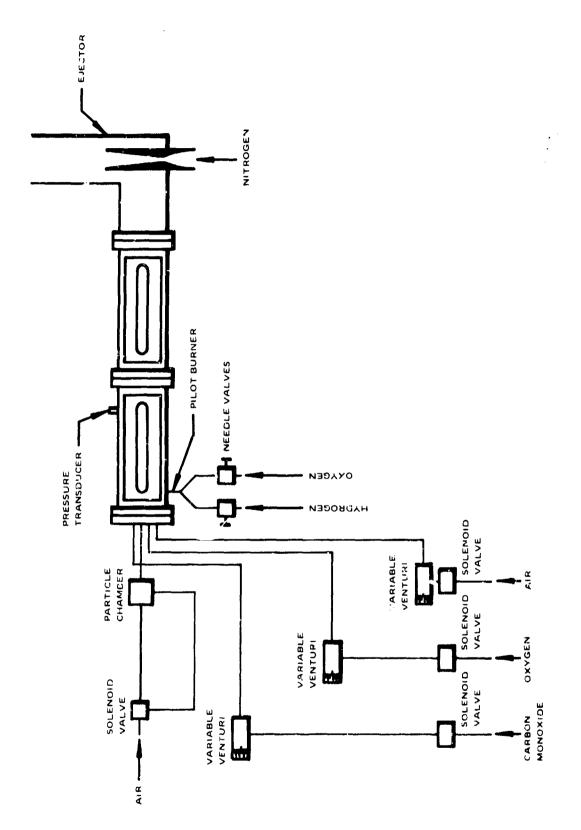
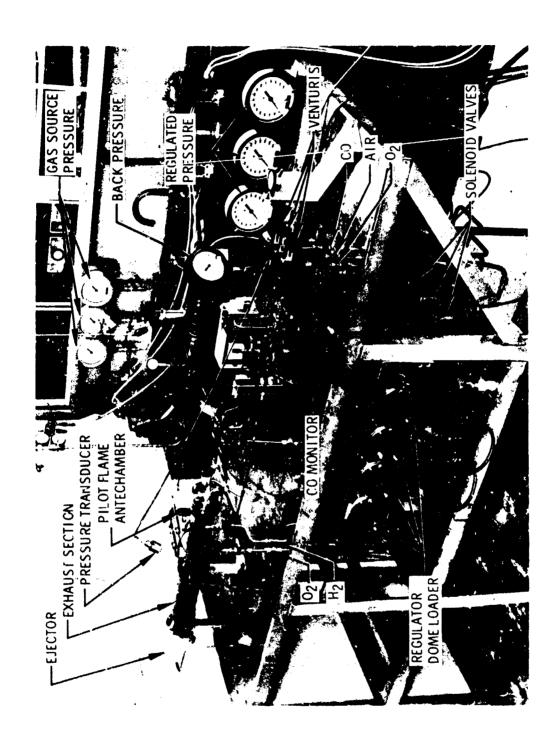


Figure 3. Scanning Electron Micrographs of Lithium Boride Powders (325 mesh)





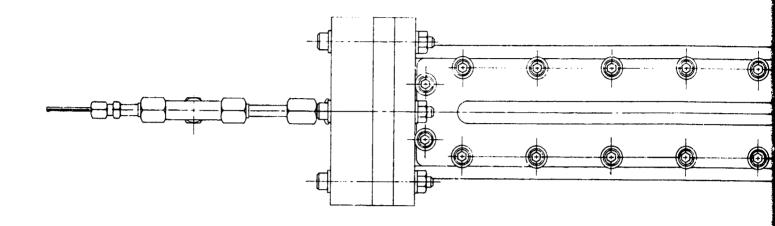
a. Test Apparatus

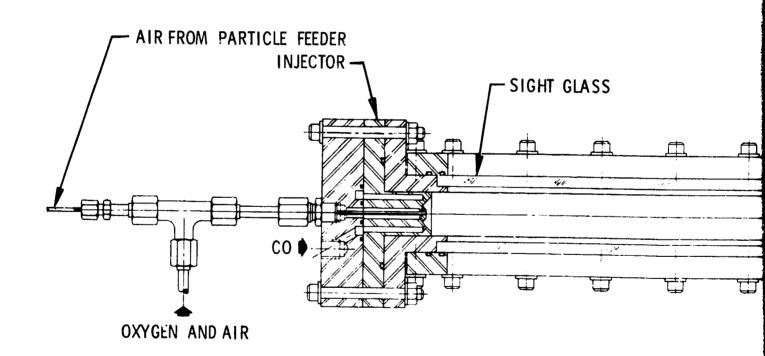
The major piece test equipment used in this program was constructed at UTC under contract AF04(611)-11544. (19) Several modifications were made to meet the requirements of the current contract; the major ones were (1) use of a CO/O_2 flame instead of a H_2/O_2 flame, to eliminate the effect of the presence of water vapor on the combustion; (2) installation of an ejector system attached to the burner exhaust duct for maintaining low chamber pressure conditions, (3) installation of a thermocouple to monitor the flame temperature and (4) extending the running period to facilitate collection of large amounts of exhaust residue. A large part of the experimental effort in the first six months of the program was devoted to carrying out these modifications and to calibration of the burner.

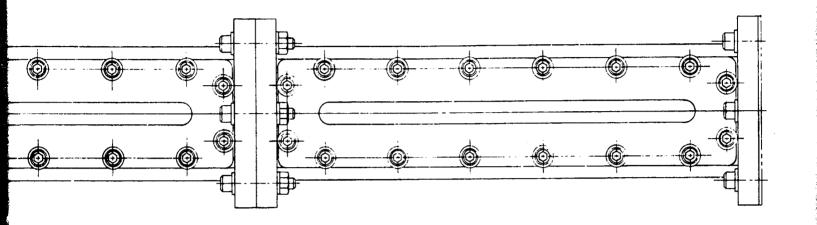
(1) Optical Burner

The optical burner, shown in Figure 6, consists of a combustion chamber of l in. I.D. fitted with a transparent Vycor window operating with carbon monoxide and oxygen. The fuel/oxygen injector consists of a central port, through which the oxygen is admitted, surrounded by six manifolded fuel jets. fuel inlets end in a series of jets canted 45° to These jets impinge on the the axis of the burner. oxygen jets which are canted outward at 45°. A 1/16-in. O.D., 0.020 in. I.D. stainless steel capillary tube is fitted coaxially inside the oxygen inlet port and serves for the injection of solid fuel. Air is used as the carrier for the solid particles and at the same time serves as a diluent to lower the temperature of the burnt gases. Four combustion chambers, with lengths of 3, 6, 9 and 12 in., are Taps for monitoring pressures and temavailable. perature are installed near the exhaust end of the chamber.

An exhaust duct is mounted downstream of a replaceable nozzle section. This duct can be fitted with two windows or a sampling probe. Five different sizes of graphite inserts were fabricated for use in the replaceable nozzle section to yield 5, 10, 15, 25 and 40 psia burner pressure at a specific flow rate setting. Difficulty was experienced in maintaining the desired temperature level, or sometimes even sustaining combustion, when large throat inserts were used. Using a 12-in. long chamber instead







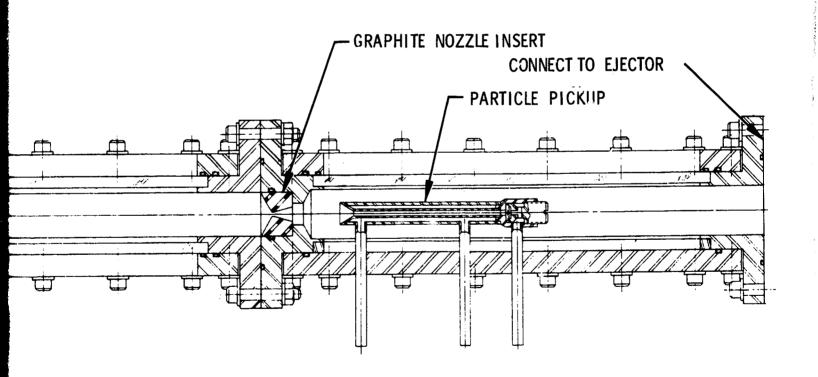


Figure 6. Optical Burner 01501

19/20

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of the 6-in. chamber, thus increasing the L* by a factor two and facilitating combustion, did not fully resolve the problem. However, a trial-and-error adjustment of CO, O₂ and air flow rates made it possible to obtain the desired pressure and temperature level for each specific size of nozzle throat insert.

(2) Ignition System

Ignition is initiated by a pilot flame in an antechamber attached to the main burner which is itself ignited by a spark plug. Originally the pilot flame operated on small amounts of CO and O2 regulated by needle valves. Problems were encountered in obtaining a stable pilot CO flame since ignition was very sensitive to the gas flow rates and the flame often went out when the spark was turned off. High gas flow rates or long spark durations resulted in rough starts, burnout of the spark plug, and window breakage. On the other hand, low pilot flow rates or short spark durations failed to give good combustion and caused carbon to deposit on the window in the main burner. The problem was resolved by switching to a H2/O2 pilot flame and by installing fixed orifices in lieu of the needle valves to insure a stoichiometric flow rate ratio in the pilot gas supply. Satisfactory ignition of the main burner gas was achieved with a pilot flame turned on for the first second only, in total run times up to 10 seconds. Any effect of the presence of water vapor on the combustion of the materials under investigation should be negligible under these circumstances.

(3) Particle Feed System

The parcicle feed system is shown in Figure 7. The diluent air supply to the main burner also provides the air supply to the particle injector. The latter is taken off through a tee placed downstream of the main air venturi so that no correction to the chamber condition is necessary for the air injected through the particle feeder. A check valve in the main air line downstream of the tee provides a small pressure drop which is independent of the absolute pressure of the system. This pressure drop assures a positive flow of air through the particle feeder throughout a firing.

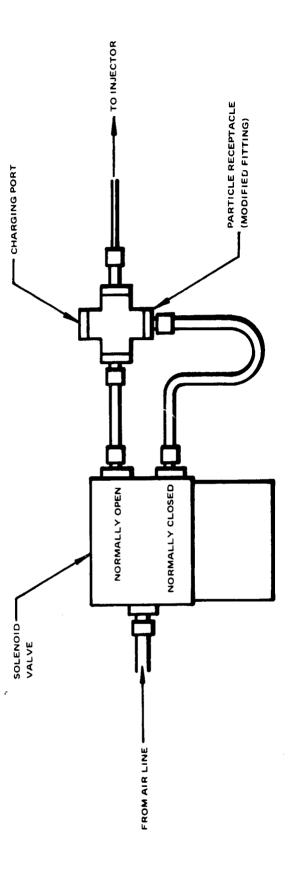


Figure 7. Particle Feed Mechanism

In operation, air begins to flow through the particle injector as soon as the main combustion gas valves open. The solenoid valve on the injector is not activated, and the air flows through the normally open port without disturbing the particle container. After 1 second of firing, when flow rates and pressures have stabilized, the injector solenoid valve is activated; the air flow is diverted through the sintered filter which supports the particle charge and the latter is fed into the combustion chamber.

(4) Sampling Probe

The sampling probe available for use from the previous program is a miniature water-cooled condenser designed for insertion into the exhaust gases immediately downstream of the nozzle (Figure 6). probe is mounted on a plate dimensionally identical to that retaining the windows in the exhaust section. The entire assembly replaces one of the windows when the exhaust residue is to be sampled. In operation the probe is fitted with a 10-mm diameter sintered glass filter disc through which a vacuum is drawn. The particles in the gas sample are thus drawn into the condenser section, quenched and deposited on the removable filter disc for analysis. In the previous program, some difficulties were experienced in obtaining samples. The sampling probe burned out twice, once because of inadequate cooling water and once because of the cracking of a faulty weld. the current program, a commercial water-cooled gas sampling probe (United Sensor and Control Corporation GC-24-24-050) has been acquired as a back-up. This probe has been endurance tested up to 4,000°F.

In the previous program the sampling problem was also in part due to an insufficient quantity of particles. This should no longer be a difficulty since the running time has been successfully extended to 10 seconds without causing any damage to the test hardware.

Another sampling technique under consideration is the use of a microscope slide which would be dropped, appropriately guided, through the exhaust gas stream to collect burned and unburned particles which are quenched and deposited on the face of the glass. This technique has proven fruitful in another investigation. (20)

(5) Ejector System

An ejector system was designed, fabricated and installed to provide the exhaust vacuum required for the low pressure runs. The ejector system replaces closed vacuum tank originally installed, which presented a potential hazard due to the possibility of the formation of an explosive mixture in the tank. As shown in Figure 8, the ejector uses nitrogen supplied by a high pressure reservoir to drive the exhaust gas through the concentric channel. The back pressure reached the desired 2 psia as required to permit running the combustion chamber at 5 psia.

b. Gas Supply System

All CO, O_2 and air used are supplied by commercial bottled gases (CO and O_2 by Liquid Carbonic Corp., CO commercial grade, by Matheson Company). Three sets of regulators, valves and control venturis are provided for control of the flow of CO, O_2 and air. A fourth system, originally designed to be compatible with fluorine serves as a spare. Remotely operated regulators reduce the supply pressure to the desired working pressure. The gases are metered through variable venturis which were calibrated against standard orifices using nitrogen as a test gas.

c. Control Console and Sequencer

A schematic diagram of the control console containing the sequencer for operating the optical burner system is shown in figure 9. This sequencer provides for programmed operation of the burner control components. Six individual channels are available; one channel is hard-wired in, the other five may be programmed by utilizing a patchboard to set up the desired sequence. Five of the outputs provide 28-vdc power, the sixth supplies a contact closure for remote starting of recorders. A manual switch for purging the burner with inert gas is also provided.

To provide the most versatility, the sequencer makes use of a relay-controlled switch, switch driver, and patch panel. This allows the operator to set up a sequence where power may switch any function on and off repeatedly and to vary the time for each condition.

The stepper switch is relay-operated and consists of 10 banks of contacts; each bank contains 10 active positions and a home position. One bank of contacts is used to supply timing resistors for the driver, and one bank is used for supplying power to a series of lights which

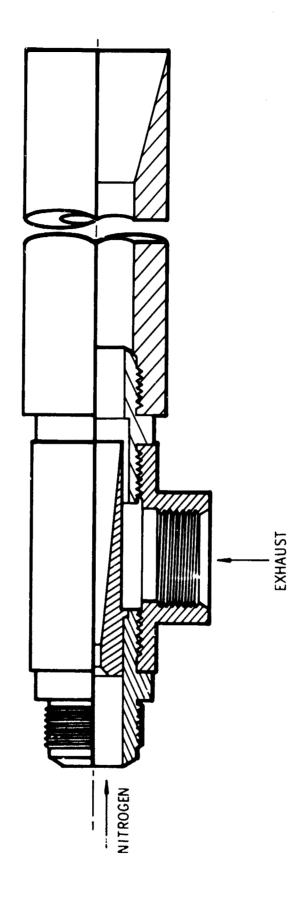


Figure 8. Ejector

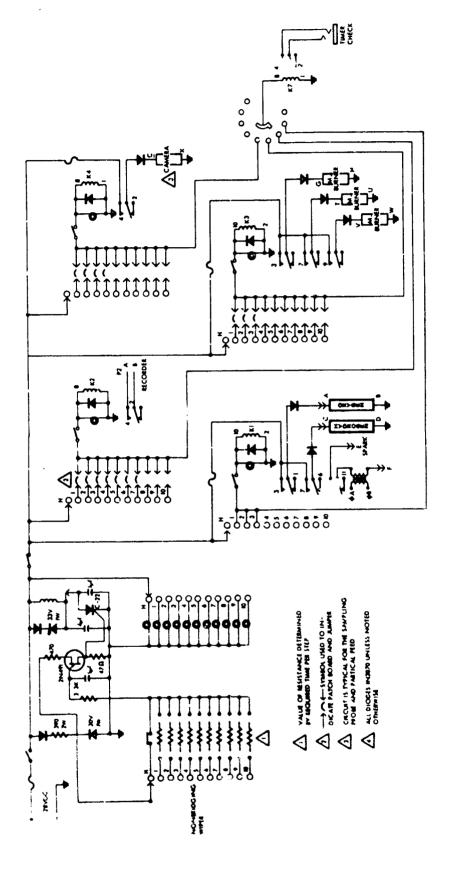


Figure 9. Schematic Diagram of Sequencer

indicate the position of the switch. Five banks are wired to the patch panel for programming, one bank is hard-wired in for the ignition function, and the remaining two banks are spares.

The stepper switch driver is a solid-state device that is used to switch power on and off the stepper switch solenoid. The time that the switch is in any one position may be varied by connecting an external resistor across the test jacks supplied for this purpose. One pair of jacks is supplied for each step position of the switch. The time for each step may be varied from approximately 70 msec to 5 sec.

Provisions have been included in the sequence to enable the operator to check the time duration of any step of the switch or the time duration of the entire sequence. A phone jack has been provided on the side of the console; by plugging a standard timer into this jack and selecting the desired channel on the timer check rotary switch, the time for that particular event may be checked.

The patch panel consists of 10 rows of 10 contacts. Two rows of contacts are utilized for each control function. One row of contacts is wired together and is connected to the otuput function control switch. The other row is connected to the contacts of the stepper switch. The wiper of the stepper is wired to +28 vdc; as the stepper is advanced the contacts pick up the 28 v and apply it to the patch board. If a patch wire is plugged into the board, this voltage is jumped onto the common bus and is applied to the load. This is typical for each channel.

The function control switches are supplied power from the patch board. If a particular channel is patched in and the control switch is turned on, an indicator light next to the switch will light when that channel is activated, indicating that power is present and that a relay is energized. The contacts of the stepper switch have a low-power switching capacity; therefore, an additional relay was used to supply power to the load. Loads requiring up to 5 amp at 28 vdc may be powered from this sequencer. The recorder channel is an exception to the above; instead of switching 28 vdc to the output, it supplies a contact closure which is used to turn a recorder on and off remotely.

The emergency shutdown switch is the main power shut-off switch. In order to have power available to the output, this switch must be in the "on" position. If for any reason it becomes necessary to cut off power to the load during the sequence, the red switch guard is pushed down which

cuts off all output power. The sequencer will continue to step through the remaining steps until it hits the home position where it will stop; however, no power will be supplied to the load during this time.

d. Optical System

Two cameras are being used in connection with this study. High-speed photographs were taken with a Hycam* K-1001 camera and particle tracks were photographed using an Automax† pulse camera. The high speed camera was used to limit the motion of the particles on the film and thereby permit a direct velocity measurement.

The first photographs were taken of boron, MgB_2 and LiB_2 in the $CO-O_2$ -air flame with the pulse camera at 1/60 sec and f/8 lens opening, and show fairly straight particle trajectories. As can be seen from a typical photograph, figure 10, the ignition delay is evidenced by the location of which particle ignition occurs. Because of the long burning time of these particles, their combustion was not completed when they left the 6-in. chamber used. The 12-in. chamber will be used later and may provide sufficient length for complete particle combustion.

e. Data Recording

A platinum-platinum/10% rhodium thermocouple (Tempton, Inc.) was used to measure the flame temperature just upstream of the exhaust nozzle during calibration. The burner pressure is monitored by a CEC (Consolidated Engineering Corporation) pressure transducer, model 4-327-001, connected to a pressure tap located at 90° to the thermocouple connection. Both temperature and pressure measurement are recorded by a CEC recorder, Type 5-124.

4. CALIBRATION OF BURNER FOR THE TEST CONDITIONS

The test conditions are set at 5, 10, 15, 25 and 40 psia and at 2000° and 1700° K. 2000° K was closen because it represents the threshold of boron ignition at low pressure and the upper limit of the platinum thermocouple used, and 1700° K is the limit at which the CO₂ flame is stable. As mentioned in the previous sections, the calibration was carried out by trial-and-error adjustment of CO, O₂ and air flow rates. Over three hundred test runs were conducted. The CO/O₂ ratio was held at the approximate stoichiometric ratio for CO₂ and air was added as diluent. All the settings were obtained with a 0.336-in. diameter throat nozzle,

^{*} Red Lake Laboratories, Santa Clara, California † Traid Corp., Los Angeles, California



Figure 10. Typical Particle Tracks - MgB2 in CO2 Flame

except the 5 psia - 2000°K condition. Stable flame could not be sustained at a pressure lower than 6 psia and a temperature higher than 1900°K. A slight modification of the burner nozzle throat size to 0.375 in. still failed to obtain precisely this desired pressure and temperature. Instead, two conditions at a pressure slightly higher than 5 psia and a temperature lower than 2000°K were obtained. The measured pressures and temperatures are listed in the following table VI, along with the flow rates of CO, O₂ and air.

Calculations, using an available UTC computer program, were carried out to evaluate the theoretical equilibrium conditions for the CO-O₂-air system, assuming complete mixing and combustion, at pressures corresponding to a given set of mass flow rates and throat areas. The results are also listed in table VI.

The characteristic velocity c* was computed from the relationship between pressure, flow rate and throat area. Comparing the experimental values with the theoretical ideal characteristic velocity, c* efficiencies were derived which are also listed in table VI.

The thermal properties of the gas system and the composition of the combustion products were also printed out in this computer program study. These data are attached as Appendix I.

TABLE VI

COMBUSTION EFFICIENCY FOR VARIOUS TEST CONDITIONS

						Th	Theoretia	a	Σ	Measured	
	Flow	Flow Rates, 1b/sec	/sec	D.	Α.	Ęi	ర	P	Ţ	Д.	
	02	00	Air	in.	in.	, X	fps	psia	ပ်မှူ	psia	C*Eff
	.00479	.00846	.0265	.336	.08866	2096	3661	51.02	1700	39.7	.778
60-	.00334	.00588	.01398	.336	.08866	2152	3877	31.53	1700	25	.793
-10	.0022	.00393	.00652	.336	.08866	2547	4071	18.05	1700	15	.830
	.00161	.00287	.0034	.336	99880.	2641	4155	11.48	1700	10	.871
-12	.001257	.002205	.000859	.336	99880.	2782	4252	6.44	1700	Ŋ	.777
-13	.00715	.0125	.01493	.336	99880.	2742	4201	50.93	2000	39.5	.776
-14	.00534	86600.	60200.	.336	99880.	2834	4269	32.64	2000	26	.796
-15	.00428	.00753	.00255	.336	.08866	2913	4319	21.74	2000	16	.735
-16	.00251	.0048	.001307	.336	,08866	2934	4336	13.10	2000	10	.764
-19	.00181	.00327	.00671	.375	.11045	2837	4285	6.93	1900	9	.865
-20	.001925	.00345	.000747	.375	.11045	2840	4286	7.38	1960	9.9	.893

SECTION III

FUTURE WORK

The modification and calibration of the burner apparatus for the current program requirements have been completed. The boron and boron-metal compounds obtained will be separated by sifting into lots of different particle sizes; these will then be ready for combustion testing under the already calibrated pressure and temperature conditions. The ignition delay times, burn times or rates and combustion efficiencies will be determined from these tests. At least two samples of the test materials will be coated with LiF as dopant. These will be burned for determination of dopant effectiveness in reducing ignition temperature, increasing burn rate and improving combustion efficiency. X-ray diffraction analysis will be carried out on the combustion residue for quantitative interpretation of the completeness of combustion. chemical analysis will be performed on two selected samples of residue and compared with the result obtained by the X-ray diffraction technique. The effects of particle size and chamber pressure will be analyzed and discussed.

Sources of supply and preparation methods for the borides will be further investigated and discussed. The discussion will deal with the best preparation methods found in the literature and with the availability from commercial suppliers, including cost.

An extension of the current program to a parametric study of secondary combustion using the most promising borides selected under the current contract and employing the UTC connected pipe test facility (21) will be formulated and discussed, and potential applications of the results of the program to the design of future air-augmented propulsion systems will be investigated.

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APPENDIX I

THEORETICAL EQUILIBRIUM CALCULATION FOR CO-O₂-AIR COMBUSTION

INGREDIENTS	WT.	PCT. LLEMENTS	GH ATUMS
0498 CARHON MONOXIDE		1.28 n	2.477956809+00
0189 DXYGEN, GAS		2.05 C	7.59701546P-01
9999 AIR		6.67 N	3,597931870+00
Carlot T. Ten and M. Marine, and a second		AR	2.073072140-02
PROPELLANT DENSITY, G	1.00000		21013012144-01
		The state of the same of the same of the state of the same of the	n en all Management de la Marie (1986) (1986
	40.4.440.124	THRUAT	EXHAUST[1]
AREA RATIO		1.00000000+00	6.472247450+00
OPTIMUM ISP, SEC		7.839713550+01	1.744731500+02
VACUUM ISP, SEC		1.418251590+02	1.887886807+02
C+, FT/SEC		3.660651240+03	and the same as a second secon
CO) 11/3EC		3.000031240403	
VFLOCITY, FT/SEC		2.522349440+03	5.613499129+03
DENSITY, GM/CC		4.134524156-04	2.870397300-05
		70 11 m 10 10 10 10 10 10 10 10 10 10 10 10 10	
and the second s	CHAMBER	THROAT	EXHAUSTE 11
PRESSURE, PSTA	5.144000000#+01	2.867667810+01	1.000000000+00
PRESSURE, ATM	3,500272180+00	1.951325400+00	6.804572678-02
TEMPERATURE, DEG K	2,096791828+03	1.850183080+03	9.445215560+02
HEAT CAP. , CAL/DEG K/		3.054571860-01	2.817542689-01
ENTHALPY, KCAL/G	-2.006903578-01	-2.71291081P-01	-5.50366470 P -01
ENTROPY, CALINEG KIG	1,96424799#+00	1.964248000+00	1.964247999+00
HOLS OF GAS / 100 G	3.06052959#+00	3.059076610+00	3.058674759+00
COMBUSTION PRODUCTS			
	CHAMBER	THROAT	EXHAUSTE 13
	MOLS/100 G	MULS/100 G	MOLS/100 G
C	1.00000000-10	1.000000000-10	1.000000000-10
CN G	1,000000000-10	1.00000000-10	1.000000000-10
Cn G	2,902252448-03	6,20254630#-04	1.00000000-10
Ch2 G	7,567995868-01	7,590616379-01	7.597024084-01
C> G	1.000000000-10	1.00000000-10	1.000000000-10
C2N2 G	1,000000000-10	1.000000000-10	1.00000000-10
C 3 G	1.000000000-10	1.00000000-10	1.0000000000-10
C305 2	1,00000000=10	1.00000000=10	1.000000000-10
CA G	1.00000000-10	1.00000000-10	1.00000000
CS G	1,00000000-10	1.00000000-10	1.000000000-10
N G	4,187736268-09	2.228711339-10	1.000000000-10
Nn G	2,348795778-02	1.301387510-02	4.241220170-05
Nu5 G	5,16551816#=05	3.13654606P-05	7.630434669-07
Nn3 G	1,203033798+10	1,000000000-10	1.000000000-10
N2 G	1,787194230+00	1.792442530+00	1,79894439#+00
NOU G	1,90/679748-06	8.015928460-07	6.899792719-10
N203 G	1.000000000-10	1.0000000000-10	1.0000000000000000000000000000000000000
N204 G	1,0000000000-10	1.000000000=10	1.0000000000000000000000000000000000000
n G	8.603201819-04	2.149593540-04	1.009322707-10

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	0 2 A4	G G	CHAMBER MOLS/100 G 4.685009528-01 2.073072148-02	THRUAT MULS/100 G 4.729404669=01 2.073072140=02	EXHAUST[1] MOLS/100 G 4.792540598-01 2.073072148-02
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9997 4:			60,26	N N	3.252006020+00
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Obtivity	150. cfr		8.1563	357130+01	1.77346973#+02
VACUUM I				75120+02	1.95437114#+02
VACOUM I	37) 310			,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	10,243,1144,05
C+, FT/S	FC		3.8769	92411#+03	•
VELOCITY	• FI/SEC		2,624	226349+03	5.70596150#+03
DENSITY,			2.306	542470-04	2.234664528-05
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		CHAMBER	THROA		EXHAUST(1]
PRESSURE	PSTA	3,162000000+0	1.782	65143#+01	1.000000000#+00
PRESSURE	, ATM	2,15160588#+00		018126+00	6.804572678-02
	URE. DEG K	2,342454700+0		559450+03	1.243906678+03
HEAT CAP	CAL/DEG K/	6 3.14440401F-0		25784#-01	2.92390314P-01
ENTHALPY	. KCAL/G	-2.38979965#-0	1 -3.1539	989448-01	-6.00270282 P- 01
ENTROPY,	CAL/DEG K/G	2.01101901#+00	2.0110	019010+00	2.01101900#+00
HOLS OF	GAS / 100 G	2.997507798+00	2.988	50558 P +00	2.983232190+00
COMBUSTI	ON PRODUCTS				
		CHAMBER	THRUA	T	EXHAUST[1]
		MOL5/100 G		S/100 G	MOLS/100 G
С	G	1.00000000=1		000000-10	1.000000000=10
ČN	Ğ	1.000000000-1		2000-10	1.000000000-10
Cn	G	2.37620621 -0	2 8.6 4	31-120-03	4.245190498-07
Cus	G	8.80882379#-0	8.95	U69P-01	9.046447538-01
C?	G	1.000000000-1		000000-10	1.0000000000-10
C2N2	G	1.000000000-1		00000P-10	1.000000000-10
Ca	G	1.000000000-1	0 1.000	000000-10	1.0000000000-10
C302	G	1.00000000-1		000000-10	1.00000000000000
CA	G	1.00000000-1		000008-10	1.000000000-10
CS	G	1.00000000-1	0 1.000	000000-10	1.000000000-10
N	G	9.099147648-0		629/38-08	1.000000000-10
Nn	G	3.659190818-0		983830-02	6.136013257-04
Nn2	Ğ	4.298910518-0		29583#-05	1.77901950#-06
Nn3	G	9.64828/079-1		000000-10	1.000000000-10
N?	G	1.607654309+0		039150+00	1.625696340+00
N2U	G	2.22122802#-0		48905 8- 06	7.891406879-09
NoU3	G	1.00000000-1		000000-10	1.0000000000-10
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02 G AD G	CHAMBER MULS/100 G 3.87205861#+01 1.60261194#+02	THROAT MULS/100 G 3.751556419=01 1.602611940=02	EXHAUST[1] MULS/100 G 3.59446813P=01 1.60261194P=02
C S	0.000000000+00	0.000000000+00	0.000000000+00
			and the second s
	44		

					PAGE	1
INGRED	IFNTS		•PCT•	ELEMENTS	GM ATUMS	
	CARBON MONOXIDE		36.42	0	3.201727818	+00
	UXYGEN, GAS		20.43	Ċ	1.300203498	
	AIR		43.15	Ň	2.32864497F	
				AR	1.34172886	
PROPELI	LANT DENSITY, G	/CC 1.00000	000#-03	***		
		•	THROAT		EXHAUST[1]	l
AREA RA	ATIO		1.000000	00+400	2.66574008	+00
Dettuu	M 150. ela		8.384819	HOMAN4	1.69063834	1102
	M ISP, SEC ISP, SFC		1.589022	the state of the s	1.99207800	
VACOUR	1011 010		14307422	100102	10992010000	. 402
C+, FT,	/SEC		4.154834	644+03	•	
VELOCI'	TY, FT/SEC		2,697731	95@+03	5.439459818	+03
DENSIT	Y. GM/CC		7.561391	859-05	1.406/8253	1-05
		CHAMBER	THRUAT		EXHAUST[1]	<u> </u>
PRESSU	RE, PSIA	1.14200000#+01	6.637303	440+00	1.000000000	
	RE, ATM	7,770821998-01	4.516401	360-01	6.804572678	1-02
TEMPER	ATURE, DEG K	2.640850720+03	2,522284	130+03	2.103342768	+03
HEAT C	AP. CAL/DEG K/	G 3,204673188-01	3.197817	450-01	3.15667128	
ENTHALF	PY, KCAL/G	-3.43474756P-01	-4,242347	430-01	-6.71804473P	-01
	Y, CALIDEG KIG	2,097778494+00	2.097778		2.09777849	
MILS OF	F GAS / 100 G	2.917210420+00	2.885912	140+00	2.80253000	+00
COMBUS	TION PRODUCTS					
		CHAMBER	THROAT		EXHAUSTE 13	ł
		MULS/100 G	MULS/1	00 G	MOLS/100	
C	G	1.000000000-10	1.000000	and the second second second second	1.000000000	
CH	G	1.000000000=10	1.000000		1.00000000	
Ch	G	2.440254798-01	1.901917	770-01	4.27981482	
Cu5	G	1.05617820#+00	1,110011	910+00	1.257405618	+00
C2	G	1.00000000-10	1.000000	000-10	1.00000000	-10
C>N2	.	1.000000000=10	1.000000	009-10	1.000000000	-10
6.3	Ğ	1.00000000-10	1.000000	000-10	1.000000000	-10
C 305	G	1,000000008-10	1.000000	000-10	1.00000000	-10
CA	G	1.000000000-10	1.000000	008-10	1.00000000	-10
CS	G	1.0000000000-10	1.000000		1.00000000	-10
N	G	2,053443220=06	9.571621		2.536471920	
NŪ	<u> </u>	4.92702048#-02	3,974338		1.56814065	
Nn2	G	2,398331238-05	1.636123		4.05358311	
Nn3	G	1.000000000-10	1,000000		1.00000000	
NO	G	1,13967263#+00	1.144441		1.156479610	
N20	<u> </u>	1,539021598-06	9,513558	Control of the Contro	1,49736820	- '
Nous	G	1,000000000-10	1.000000		1.00000000	
N204	<u> </u>	1.000000000-10	1.000000		1.00000000	
0	G	3,321142647-02	2.444145	206-05	5.05860167	-05

VIC151	5			UTC151511- PAGE 2
D? AR C	G S	CHAMBER MOLS/100 G 3.814074158-01 1.341728668-02 0.00000000P+00	THROAT MULS/100 G 3.63646864#-01 1.34172866#-02 0.00000000#+00	EXHAUST[1] MOLS/100 G 3.11685108P=01 1.34172886P=02 0.00000000P+00
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<u> </u>			PAGE 1
		E I MMPN 90	CM ATIME
INGREDIENTS	WT.PCT.	ELEMENTS	GM ATUMS
0498 CARBON MONUXIDE GAS	51,03		3.927696750+0U 1.821784300+00
0189 UXYGEN, GAS	29,09	C N	1.072849649+00
9999 AIR	19,88	AR	6.181592049-03
PRUPELLANT DENSITY. G/CC.	1.0000000000-03	A.V.	0.101372042-03
PAUPELLAND VENSION WALL	1,000,000,00		MATERIAL CONTROL MATERIAL CONTROL CONT
	THROA	I	EXHAUST[1]
1-51 B150	4 000	000000400	1 844043338400
AREA RATIO	1.000	000000+00	1.846943329+00
OPTIHUM ISP, SEC	8,509	257830+01	1.538141470+02
VACUUM ISP, SEC		55849#+02	1.917771220+02
C	A 242	28830#+03	
C., FT/SEC	4,232	C 0 0 3 0 P T U 3	
VFLOCITY, FT/SEC	2.737	768618+03	4.94881638F+03
DENSITY, GM/CC		016920-05	1.22778280#-05
· · · · · · · · · · · · · · · · · · ·		_	
CHAMP			EXHAUST[1]
		948858+00	1.0000000000+00
	· · · · · · · · · · · · · · · · · · ·	504068-01	6.804572678-02
		884478+03	2.457475970+03 3.225322870-01
HEAT CAP. CAL/DEG K/G 3.235	2607588=01 =5.644	21199#-01 35628#-01	-7.53030641 8 -01
	· -	198910+00	2.144198910+00
		527250+00	2.748377350+00
COMBUSTION PRODUCTS			
CHAME	BER THROA		EXHAUST[1]
	_	\$/100 G	MOL 5/100 G
	T	000000-10	1.000000000
		60940P=11	1.0000000000-10
		223640-01	4.414218288-01
		16211#+00	1.380362678+00
		00000#-10	1.00000000-10
		00000#=10	1.000000000-10
		000000-10	1.00000000-10
		000000-10	1.000000000
	000000#-10 1.000	00000#-10	1.000000000-10
		000000-10	1.00000000000-10
		360194-06	8.897080518-07
		845070-02	2.289499368-02
		784540-06	3.837767740-06
		000000-10	1.000000000000
. · · · · · · · · · · · · · · · · · · ·		436280-01	5.249748248-01
		614400-07	1.475301699-07
	-	00000#=10	1.000000000-10
		000009-10	1.00000000P=10 4.24263295P=02
n G 8,190	6831468-02 6.852	933538-02	4.646036778-08

02 G A2 G C 5	CHAMRER MULS/100 G 4.062291920=6 5.191592040=6 0.000000000000	03 6.181592040-03	6.181592040-0
			English of April 1980
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1.67060288#=02

1.12708945#-04

2.360866739-02

G

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UIC15	515.			UTC151513= PAGE 2
779	9 9 3	CHAMBER MOLS/100 + 3.69415940#+01 1.34/35U/5#+02 5.76767674	THRUAT MULS/100 G 3.53/333920-01 1.342350/50-02 0.303030300-00	EXHAUST[1] MOLS/100 G 3.11681253P=01 1.34235075P=02 0.000000000P+00
			odarka siginan menenjada dan perioda da kaman dalam da kaman da kaman da kaman da kaman da kaman da kaman da k	
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VIC151	<u> </u>					
					PAGE 1	
[++GRED]	ICNTC		IT.PCT.	ELEMENTS	GM ATOMS	
	CARBON MONOXIDE		43.01	0	3.536090447+00	
	TXYGEN, GAS	ung.	24.48	č	1.535468219+00	
	AIR		32.51	N	1.754443/50+00	
• , • •	T			AR	1.01088308#-02	
PAUPELI	LANT DEHSITY, G	/CC 1.0000	00000#-03			
			*	_	# W	
			THRUA	ĭ	EXHAUST[1]	
AREA R	ATIU		1.000	000000+00	5.944308278+00	_
0671411	M ISP, SEC		A.594	496806+01	2,03052608#+02	
	ISP. SFC		•	996210+02	2.271796630+02	
C+, FT.	/5FC		4.268	968698+03		
VFLOCE	TY. FT/SEC		2.765	193400+03	6.533014608+03	
	A» GH/CĈ		2.055	20250#-04	1.463407178-05	
		CHAMBER	THROA	1	EXHAUST[1]	
PRESSUI	RE, PSIA	3,269000000+01		363140+01	1.000000000+00	
	RE, ATH	2.22441481F+00		157280+00	6.804572679-02	
	ATURE, DEG K	2,833946327+03		314878+03	2.109415280+03	-
		3.237321178-01		055289-01	3.184926888-01	
	PY, KCAL/G	-4.056246379-01		742120-01	-8.792401340-01	
	Y, CAL/DEG K/G	2.04619238#+00	2.046	192380+00	2.046192388+00	
MOLS DI	F GAS / 100 G	2,863324340+00	2.829	39769#+00	2.65633344P+00	
COMBUS	TION PRODUCTS		- 			٠.
				_		
		CHAMBER	THROA		EXHAUST[1]	
_	_	MULS/100 G		S/100 G	MOLS/100 G	
C	G	1.000000000-10		000000-10	1.0000000000-10	
CN	<u>G</u>	2,30954256#-10		817290-11	1.000000000-10	
(n) -	G	3.7347 (6717-01		63570 9- 01 70481 9 +00	5.726727348-02	
Cn2	G G	1.161996700+00		000000-10	1.47820120P+90 1.00000000P=10	
C2N2		1.000000000-10		0000000-10	1.00000000000000	
CZ	G G	1.000000000=10		0000000-10	1.0000000000000000000000000000000000000	
C302	G	1.00000000		000000-10	1.00000000#=10	
C.) (E	G	1.00000000=10	and the second s	000000-10	1.00000000000000	
CS	G	1.000000000-10		000000-10	1.00000000000000	
N	Ğ	4,431342538-06		776420-06	2.33250313#-08	
NO	G	5,542844458-02		232310-02	1.243659628-02	
NO2	Ğ	3.804059170-05		075150-05	2.928651770-06	
NO3	Ğ	1,414513820-10		937189-11	1.000000000-10	
N2	G	A.49481758P-01	many to the many the many to the property of the contract of t	598469-01	8.710019620-01	
NOU	Ğ	2,567765439-06		105000-06	1.048883379-07	
N203	G	1.000000000-10		000000-10	1.000000000-10	
N204	G	1.000000000-10		000000-10	1.000000000-10	
n	G	4.246107928-02		51302#=02	4.65068625#-03	

	VIC151	5			UTC151514- PAGE 2
	02 AP	G G	CHAMRER MULS/100 G 3.70328612 8- 01 1.01088308 8- 02	THROAT MOL5/100 G 3.50433049#=01 1.01088308#=02	EXMAUST[1] MOLS/100 G 2.526637350-01 1.010883680-02
•	C	S	0.000000000+00	0.000000000000	0.0000000000000000000000000000000000000
× •	many to a responsable to the second				
CHAMMER THROAT MULS/100 G 3,7012/0612P-01 3,50433049P=C S 0,000000000P+00 0.000000000P+C					
		· -			
					The second secon

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INGREDIENTS 0/95 CARBON NUNDXIDE		PCT. 2.44	ELEMENTS O	GM ATUMS 3.991719518+00
0189 OXYGEN, GAS	2	9.50	C	1.8721214/#+00
9999 AIR	1	7,76	Ν ,	9.584411288-01
			AR	5.522388068-03
PROPELLANT DENSITY, G/	cc 1.00000	008-03	.,	
		THROAT		EXHAUSTE 13
AREA RATIO		1.00000	000+00	4.451710710+00
DPTIMUM ISP. SEC			7000+01	1.955732849+02
VACUUM ISP, SFC		1,64999	7098+02	2.231272899+02
C++ FT/SEC		4,31936	9880+03	
VFLOCITY, FT/SEC			4130+03	6.29237485R+03
DENSITY, GM/CC		1.33703	9030-04	1.330404818-05
and the second s	CHAMBER	THROAT		EXHAUSTE 11
PRESSURE, PSIA	2,169000000+01		0030+01	1.0000000000+00
PRESSURE, ATM	1,475911818+00		1820-01	6.804572678-02
TEMPERATURE, DEG K	2,913361918+03		2510+03	2.35582412#+03
HEAT CAP. , CAL/DEG K/G		-	730=-0;	3.234272300-01
			(() / 1000() 1	-9.339257708-01
ENTHALPY, KCAL/G	-4.945583818-01	-5.80769		
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G	2.07555641#+00	2.07555	641P+00	2.075556490+00
ENTHALPY, KCAL/G		2.07555		2.075556490+00
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G	2.07555641#+00	2.07555	641P+00	2.075556490+00
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G	2.07555641#+00 2.83929678#+60	2.07555 2.80166	641P+00	2.075556490+00 2.645821350+00
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G	2.07555641#+00 2.83929678#+60 CHAMBER	2.07555 2.80166 THROAT	641P+00 915P+00	2.07555649P+00 2.64582135P+00 EXHAUST[1]
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS	2.83929678P+60 2.83929678P+60 CHAMBER MDLS/100 G	2.07555 2.80166 THRUAT	641P+00 915P+00	2.07555649P+00 2.64582135P+00 EXHAUST[1] MOLS/100 G
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P=10	2.07555 2.80166 THRUAT MOLS/ 1.00000	641P+00 915P+00 7100 G	2.07555649P+00 2.64582135P+00 EXHAUST[1] MOLS/100 G 1.00000000P=10
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000#=10 5.66228713#=10	2.07555 2.80166 THRUAT MOLS/ 1.00000 2.03130	641P+00 915P+00	2.07555649P+00 2.64582135P+00 EXHAUST[1] MOLS/100 G 1.0000000P-10
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P=10	2.07555 2.80166 THRUAT MOLS/ 1.00000 2.03130 5.62662	7100 G 90000-10	2.07555649P+00 2.64582135P+00 EXHAUST[1] MULS/100 G 1.0000000P=10 1.0000000P=10 3.06944491P=01
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G CO G CO G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000#=10 5.66228713#=10 6.45923971#=01	2.07555 2.80166 THRUAT MOLS/ 1.00000 2.03130 5.02682 1.28943	7100 G 90000-10 94610-01	2.07555649P+00 2.64582135P+00 2.64582135P+00 EXHAUST[1] MOLS/100 G 1.00000000P=10 1.00000000P=10 3.08944491P=01 1.56317739P+00
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G Cn G Cn G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P=10 5.66228713#=10 6.45923971#=01 1.22619784#+00	7HRUAT MOLS/ 1.00000 2.03130 5.02682 1.28943	7100 G 90000-10 94610-10 96450-01	2.07555649#+00 2.64582135#+00 2.64582135#+00 EXHAUST[1] MOLS/100 G 1.00000000P=10 1.00000000P=10 3.08944491#=01 1.56317739#+00 1.000000000P=10
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G CN G Cn G Cn2 G C> G C> G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P=10 5.66228713#=10 6.45923971#=01 1.22619784#+00 1.000000000#=10	7HRUAT MOLS/ 1.00000 2.03130 5.02682 1.28943 1.00000	7100 G 00000=10 04610=10 04610=10	Z.07555649P+00 Z.64582135P+00 EXHAUST[1] MOLS/100 G 1.00000000P=10 3.08944491P=01 1.56317739P+00 1.00000000P=10 1.00000000P=10
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G Cn G Cn G Cn G Cn G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000#=10 5.66228713#=10 6.45923971#=01 1.22619784#+00 1.00000000#=10	7HRUAT MOLS/ 1.00000 2.03130 5.02682 1.28943 1.00000 1.00000	7100 G 9150+00 7100 G 90000-10 94610-10 94610-10 90000-10	Z.07555649P+00 Z.6458Z135P+00 EXHAUST[1] MOLS/100 G 1.00000000P=10 3.06944491P=01 1.56317739P+00 1.00000000P=10 1.00000000P=10
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P=10 5.66228713#=10 6.45923971#=01 1.22619784#+00 1.00000000P=10 1.00000000P=10 1.00000000P=10 1.00000000P=10	2.07555 2.80166 THRUAT MOLS/ 1.00000 2.03130 5.62662 1.28943 1.00000 1.00000 1.00000	7100 G 9150+00 9150+00 90000-10 94610-10 94650-01 99180+00 90000-10 90000-10	Z.07555649P+00 Z.64582135P+00 2.64582135P+00 1.00000000P=10 1.00000000P=10 1.56317739P+00 1.00000000P=10 1.00000000P=10 1.00000000P=10 1.00000000P=10
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P-10 5.66228713#-10 6.45923971#-01 1.22619784#+00 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10	7HRUAT MOLS/ 1.00000 2.03130 5.02662 1.28943 1.00000 1.00000 1.00000	7100 G 9150+00 7100 G 90000-10 94610-10 96480-01 97180+00 90000-10 90000-10 90000-10	Z.07555649P+00 Z.6458Z135P+00 Z.6458Z135P+00 MULS/100 G 1.0000000P-10 3.08944491P-01 1.56317739P+00 1.0000000P-10 1.0000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G CN G CO	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P=10 5.66228713#=10 6.45923971#=01 1.27619784#+00 1.00000000P=10 1.00000000P=10 1.00000000P=10 1.00000000P=10 7.24863546#=06	2.07555 2.80166 THRUAT MOLS/ 1.00000 2.03130 5.02682 1.28943 1.00000 1.00000 1.00000 1.00000 4.31728	7100 G 9150+00 7100 G 90000-10 94610-10 94640-01 99180+00 90000-10 90000-10 90000-10 90000-10 90000-10	Z.07555649P+00 Z.64582135P+00 2.64582135P+00 1.00000000P=10 1.00000000P=10 3.08944491P=01 1.56317739P+00 1.00000000P=10 1.00000000P=10 1.00000000P=10 1.00000000P=10 2.99395564P=00
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P-10 5.66228713#-10 6.45923971#-01 1.27619784#+00 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 7.24863546#-06 4.61260496#-02	2.07555 2.80166 THRUAT MBLS/ 1.00000 2.03130 5.02682 1.28943 1.00000 1.00000 1.00000 1.00000 4.31728 3.88550	7100 G 9150+00 7100 G 90000=10 94610=10 946450=01 97180+00 90000=10 90000=10 90000=10 90000=10 90000=10 9420=06 96870=02	Z.07555649P+00 Z.64582135P+00 Z.64582135P+00 MULS/100 G 1.00000000P-10 3.08944491P-01 1.56317739P+00 1.00000000P-10 1.00000000P-10 1.00000000P-10 2.99395564P-07 1.58943262P-02
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000#=10 5.66228713#=10 6.45923971#=01 1.27619784#+00 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 2.4863546#=06 4.61260496#=02 2.48101501#=05	7HRUAT MOLS/ 1.00000 2.03130 5.02682 1.28943 1.00000 1.00000 1.00000 1.00000 4.31728 3.88550 1.7129	7100 G 9150+00 7100 G 90000-10 94610-10 94610-10 90000-10 90000-10 90000-10 90000-10 9420-06 9420-05	Z.07555649P+00 Z.64582135P+00 Z.64582135P+00 MULS/100 G 1.00000000P-10 3.06944491P-01 1.56317739P+00 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 2.99395564P-07 1.58943262P-02 2.71647055P-06
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000#=10 5.66228713#=10 6.45923971#=01 1.27619784#+00 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 1.00000000#=10 6.81881836#=11	7HRUAT MOLS/ 1.00000 2.03130 5.02682 1.28943 1.00000 1.00000 1.00000 1.00000 4.31728 3.88550 1.71295 1.00000	(100 G (100 G	Z.07555649P+00 Z.64582135P+00 Z.64582135P+00 MULS/100 G 1.00000000P-10 3.06944491P-01 1.56317739P+00 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 2.9939564P-07 1.58943262P-02 2.71647055P-06 1.00000000P-10
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P=10 5.66228713#=10 6.45923971#=01 1.22619784#+00 1.00000000P=10 1.00000000P=10 1.00000000P=10 1.00000000P=10 1.00000000P=10 1.00000000P=10 1.00000000P=10 1.00000000P=10 4.61260496#=05 6.81881636#=11 4.56140232#=01	7HRUAT MOLS/ 1.00000 2.03130 5.62662 1.28943 1.00000	7100 G 9150+00 7100 G 90000-10 94610-10 94610-10 90000-10 90000-10 90000-10 90000-10 9420-06 9420-05 9970-05 9420-01	Z.07555649P+00 Z.64582135P+00 1.00000000P-10 1.00000000P-10 3.08944491P-01 1.56317739P+00 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 2.99395564P-07 2.71647055P-06 1.00000000P-10 4.71271807P-07
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P-10 5.66228713#-10 6.45923971#-01 1.22619784#+00 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 7.24863546#-06 4.61260496#-02 2.48101501#-05 6.81881636#-11 4.56140232#-01 1.28473749#-06	7HRUAT MOLS/ 1.00000 2.03130 5.02682 1.28943 1.000000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.000000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.0000 1.000000 1.000000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.00000 1.0	7100 G 9150+00 7100 G 90000-10 94610-10 94610-10 90000-10	Z.07555649P+00 Z.6458Z135P+00 1.00000000P-10 1.00000000P-10 3.08944491P-01 1.56317739P+00 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 2.9939564P-07 1.58943Z6ZP-02 2.71647055P-06 1.00000000P-10 4.71Z71807P-01 9.8874Z047P-06
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS C G CN G	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P-10 5.66228713#-10 6.45923971#-01 1.22619784#+00 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 7.24863546#-06 4.61260496#-02 2.48101501#-05 6.81881836#-11 4.56140232#-01 1.28473749#-06 1.00000000P-10	2.07555 2.80166 THRUAT MOLS/ 1.00000 2.03130 5.02682 1.28943 1.00000 1.00000 1.00000 1.00000 4.31728 3.88550 1.71295 1.00000 4.59781 8.32245 1.00000	100 G 100 G 1000P=10 1461P=10 1461P=10 1464P=01 1918P+00 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10 1000P=10	Z.07555649P+00 Z.64582135P+00 MULS/100 G 1.00000000P=10 1.00000000P=10 3.08944491P=01 1.56317739P+00 1.00000000P=10 1.00000000P=10 1.00000000P=10 1.00000000P=10 2.99395564P=07 1.58943262P=02 2.71647055P=06 1.00000000P=10 4.71271807P=01 9.88742047P=06 1.00000000P=10
ENTHALPY, KCAL/G ENTROPY, CAL/DEG K/G MOLS OF GAS / 100 G COMBUSTION PRODUCTS	2.07555641#+00 2.83929678#+60 CHAMBER MOLS/100 G 1.00000000P-10 5.66228713#-10 6.45923971#-01 1.22619784#+00 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 1.00000000P-10 7.24863546#-06 4.61260496#-02 2.48101501#-05 6.81881636#-11 4.56140232#-01 1.28473749#-06	2.07555 2.80166 THRUAT MOLS/ 1.00000 2.03130 5.02682 1.28943 1.00000 1.00000 1.00000 1.00000 4.31728 3.88550 1.71295 1.00000 4.59781 6.32245 1.00000	7100 G 9150+00 7100 G 90000-10 94610-10 94610-10 90000-10	2.07555649P+00 2.64582135P+00 EXHAUST[1]

() n A :> C	G G S	CHANNE - MULS/100 - ANDES/100	14R0A1 MULS/190 G 3.654922/1#=01 5.52238896#=03 0.000000000#+00	EXHAUST[1] MOLS/100 G 2.595125944=01 5.522388764=03 0.0000000004+00
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The REPORT	NTS		ET.PCT.	ELFMENTS	GM ATUMS
	ARHON TONOXIDE		55.70	n	4.028/339/#+0U
	LYGEN, GAS	• • • • • • • • • • • • • • • • • • • •	29.13	C	1.988504528+00
9749 A1			15,17	Ň	8.186684630-01
, , , , , ,	•		. , , , ,	AR	4.717039508-03
PROPERTA	ANT DEHSITY, G/	cc 1.000	00000==03		
		,,	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		
			THROA	T	EXHAUST[1]
AREA PAT	10		1.000	U00U0#+0U	4.459666378+00
OPTIMIE	15P, 5FC		8.694	618180+01	1.963809418+02
VACUUM 1				29995#+02	2.240905168+02
C++ FT/S	SEC		4.336	028298+03	
VERNOTTY	FT/SEC		2.797	406459+03	6.318360388+03
DENSITY				089010-04	1.717494658-05
			7000		
		CHAMBER	THROAT	Ţ	EXHAUST[1]
POESSURE	. PS14	2.1690000000+0	1 1.266.	36204#+01	1.0000000000+00
PPESSURF	. ATM	1.475911818+0	0 8.6170	052849=01	6.80457267#=02
	MAE > JEG K	7.93447414P+0		26848#¥03	2.382058109+03
HEAT CAP	. CAL /DEG K/G			56603# - 01	3.24442767#-01
		-5.25301238#=0		412340-01	-9.68307019#-01
	CALINES KIG	2.0781+1079+0		16107P+00	2.07816198#+00
MALS OF	GAS / 100 G	2.840044390+0	0 2.8010	612390+00	2.642323420+00
CAMBUSTI	IN PRODUCTS		The the desirable of the same		
		CHAMBET	THRUA	1	EXHAUST[1]
		MULS/100 G	MOL	5/100 G	MOL5/100 G
С	G	1.00000000#-1	0 1.000	000000-10	1.000000000=10
C **	G	7,63355265#-1	0 2.907	412710-10	1.000000000#=10
(~	G	7,50631460#=0	1 6.862.	346320-01	4.054728 -19-01
Cu5	ℓ_b^*	1.23787020#+0		2/004#+00	1.583031837+00
c ~	S	1.000000000-1	0 1.0000	00000#-10	1.0000000000-10
6245	G	1,000000000-1		00000P-10	1.00000000000000
CI	G	1.00000000#-1		000000-10	1.000000000-10
CIUS	G	1.000000000-1		000000-10	1.000000000-10
CA	6	1.00000000#-1		000000-10	1.00000000#-10
C <	G	1.00000000		00000#=10	1.000000000
N.	G	7,720923038-0		620630-06	3.62337511#*07
Nn	6	4.119674144-0		051370-02	1.39152699#=02
NU5	G	2,052257849+0		75608p=05	2.075373030=06
Nn3	<u>G</u>	4.378949330-1		000008-10	1.0000000009-10
トラリ	G	3.88/206868=0		139458-01	4.023753100-01
₩⊅() ₩⊅ U3	G G	1,06007254#=0		75715e-07	8.00357892==00 1.00000000P=10
h2114	is G	1.0000000000-1		00000 0- 10	1.0000000000000000000000000000000000000
6	G	7.26/14804#=0		370820-02	2.23392126#=02
•	•	. * 5 A. 1400 d 0		J. 00 E - VE	* * * * * * * * * * * * * * * * * * *

Ω 2 Δ 2 C	(g - (g - 3)	 CHAMBE MULS/100 0 3.44224275#=01 4.71/03480#=03 0.00000000#+00	THROAT MULS/100 G 3.213/3125#=01 4.71/03900#=03 0.00000000#+00	EXHAUSTE 11 MOLS/100 G 2.10469348@=01 4.71703980@=03 0.000000000#+00
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I amenients	A	T.PCT.	ELEMENTS	GM ATUMS
0498 CARBON MUNDAIDE		56.46	0	4.165/29/28+00
0189 HXYGEN, GAS		31.47	Ċ	2.029916820+00
9099 AIR		11.67	Ň	6,297864848=01
		1100	AR	3.628/31348=03
PROPELLANT DENSITY, GA	rr 1.0000	00009=03	AIN	34024173134~~173
and Carrier of the Live and		0000		
		THROAT		EXHAUST[1]
AREA RATTO		1.0000	0000#+00	1.944591060+00
DPTIMUM ISP, SEC		8.57(16)	10130+01	1,578485750+02
VACUUM ISP, SEC			12470+02	1.952218168+02
C+, FT/SEC		4.2851	96/19+03	
VELOCITY, FT/SEC	•• • •	2.75750	08108+03	5.078620068+03
DENSITY, GM/CC			065H-05	1.215280328=05
	CHAMBER	THRUAT		EXHAUST[1]
PRESSURE, PSIA	6,9300000000+00		7199 2 +00	1.000000000#+00
PALSSURF, ATM	4,715568868-01		1/624-01	6.804572678-02
TEMPERATURE, DEG K	2.836563608+03		5763P+03	2.50329204#+03
HEAT CAP. , CAL/DEG K/G	3.240035500-01		18926-01	3.239630508-01
	-5,36243126 2 -01		7120-01	-8.22456613F-01
ENTROPY, CALINEG KIG	2,140665860+00		55868+00	2.140665928+00
MOLS OF GAS / 100 G	2.86044703P+00	2,82117	50A56+00	2.725831612+00
COMBUSTION PRODUCTS				
	AUAUUT:	740047		F WALLETT A 1
	CHAMBE	THRUAT	44.00.0	EXHAUST[1]
C G	MUL\$/100 i		/100 G 000 00-1 0	MDLS/100 G
Ç 4	3.024313438-10		3438-10	1.0000000000000000000000000000000000000
· · · Čn· · · · · · · · · · · · · · · ·	A.215990618-01		4546-01	5.96883864P=01
Cn2 G	1.208317918+00		6530+00	1.433033148+00
Co G	1.000000000-10		00000-10	1.000000000-10
C2N2 G	1.000000000-10		00000-10	1.000000000-10
C a G	1.000000000-10		00000-10	1.0000000000-16
CAU2 G	1.000000000=10	1.00000	00000-10	1.000000000=10
Ca	1,000000000-10	1.0000	0000-10	1.0000000009-10
Cs G	1,000000000-10	1.00000	0000-10	1.0000000000-10
N G	6.06624063#-06	3.75748	3718 P- 06	1.040503598-06
Nn G	3,41587983#-02		409#-02	1.853396718-02
Kn2 G	1,117570898-05		4016-09	2.90048187#+06
4n3 G	1.00000000-10		0000-10	1.000000000-10
R2 G	2,97804799#-01		6920-01	3.056242098-01
N20 G	4.316470448-07		5884-07	9.154376668-08
N203 G	1,000000000-10		00000-10	1.000000000-10
112U4 G	1.00000000-10		00000-10	1.0000000000-10
0 6	9,6567;2208-02	9.5005	24898-05	5.200787608-02

		CHAMHER	THRUAT	F.XHAUSTE 11
		MULS/100 G	MULS/100 G	MOUS/100 6
() a	G	3,98372931 0= 01	3.76169428@=01	J.16115785@=01
AR	G	3,6287 31 348 - 03	3.628731340-03	3,62873134#=03
C	S	0.00000004+00	0.0000000000000000000000000000000000000	0.0000000000+00

T PROTENTS CHOS CARBON MONOXIDE CHOS CXYGEN, GAS 9099 ATS		7.PCT. 56.36 31.44 12.20	ELEMENTS O C N AR	GM ATUM5 4.15367669#+00 2.01206669#+00 6.58388612#=01 3.79353234#=03
PHOPFILLANT DESSITY, GA	/cc 1.0000	0000 = =03	47	31/43332346-03
		THRUAT		EXHAUST[1]
AREA RATTO		1.0000	00006+00	2.029313740+00
OPTIMUM ISP. SEC		8.5/37	7417#+01	1.60211040@+02
VACUUM ISP, SEC		1.6363	2329#+02	1.96840731#+02
C++ FT/SEC		4.2859	3397@+03	
VELOCITY, FT/SEC	Market	2.7585	7610#+03	5.15463000@+03
DENSITY, GM/CC		4.6325	69/70-05	1.22166568#=05
Dat SELLON DE	СНАМВЕЧ	THRUAT	0.15.00.00	EXHAUST[1]
PRESSURE, PSIA PRESSURE, ATM	7.3800000000+00 5.02177463#-01		21520+00 59930 - 01	1.00000000000+00 6.8045726/9-02
TEMPERATURE, DEG K	2.83977036P+03		55370+03	2.49475642#+03
HEAT CAP. CAL/DEG K/C			4950#=01	3.239152498-01
ENTHALPY, KCAL/G	-5,315276578-01	-6.1596	8555 P- 01	-0.263/25719-01
ENTROPY, CAL/DEG K/G	2,13694855P+00	2.1369	4856M+00	2.136948569+00
MNLS OF GAS / 100 G	2,85904057#+00	2.8178	3834#+00	2.72086292*+00
COMBUSTION PRODUCTS		• • • • • •	r a man men	
	CHAMBER	THRUAT		EXHAUST[1]
	MOLS/100 G		/100 G	MULS/100 G
C G	1,000000000-10	·	00000-10	1.000000000-10
CH G	3.09/640220-10		2810#-10	1.00000000000000
CuS G	A.03437224F-01		8518#=01	5.72219034#-01
Control of the contro	1,204629628+00		5433 0 +00	1.439847958+00
			00000-10	1.0000000000000000000000000000000000000
6 6 6	1.000000000-10		0000 0-1 0 0000 0-1 0	1.000000000000000
CallS	1.00000000000000	= =	0000F-10	1.000000000=10
Ca	1,0000000000-10		00000-10	1.00000000000-10
C5 G	1,000000000-10		000000-10	1.000000000000000
8 6	6.148611128-06		86308-06	9.825487638-07
Rn G	3.52180/58#-02		5012 8 =02	1.869542618-02
Nn2 G	1,190594634-05		729#=06	2.95831205#-06
Nr3 G	1,0000000000		00000-10	1.00000000#=16
	3.115757A0A-01	3.14237	1760-01	3.198445404-01
N2O G	4.69926275#-07	3.0748	150#-07	9.45414833F-Or
5203 G	1.000000009-10		00/0#-10	1.0000000000-10
N204 6	1.00000000-10		0000#-10	1.000000000-10
3 6	9.503772768-02	8.06203	5113 8- 02	4.985643348-02

07 A4 C	6 6 5	CHA 1 d E ₹ MOLS / 100 G 4.01357086#=01 3.79353234#=03 0.00000000#+00	THRUAT MOLS/100 G 3.792062938=01 3.793532348=03 0.000000008+00	EXHAUSTI 11 MOLS/100 G 3.166020654-01 3.793532344-03 0.000000000#+00
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13. ABSTRACT

11. SUPPLEMENTARY NOTES

Under Contract No. AF04(611)-70-C-0065, United Technology Center has completed the first 6 months of a 12-month program to investigate the ignition delay times, burn times or rates and combustion efficiencies of doped and undoped boron and compound of boron with aluminum, magnesium, and lithium.

12 SPONSORING MILITARY ACTIVITY
United States Air Force
Air Force Systems Command

Air Force Rocket Propulsion Laboratory

A literature survey has been conducted for information on the properties and combustion of aluminum, magnesium and lithium borides.

An optical burner apparatus built under a previous Air Force contract, AF04(611)-11544, has been modified and calibrated for the present investigation. Eight borides have been obtained or prepared for this program, were analyzed for purity on the basis of chemical, spectrographic, or X-ray data, and are ready for test.

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Security Classification

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