

**AD-786 616**

**CONCEPT FOR ATTENUATION OF THE BACK  
BLAST REGION OF A 105 mm RECOILLESS RIFLE**

**Hugo J. Nielsen**

**IIT Research Institute**

**Prepared for:**

**Watervliet Arsenal**

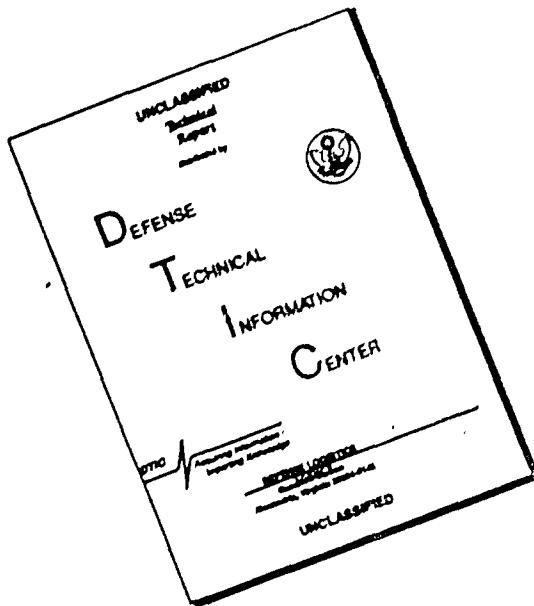
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20. ABSTRACT (Continue on reverse side if necessary and identify by block number)  <p>A concept for attenuating the back blast field of a recoilless rifle by the ejection of liquid or solid particles was investigated with respect to feasibility. The concept involves attaching a cylinder partially filled with liquid or solid particles to the nozzle. In this way the propellant gas is forced to expend some of its energy in driving the particles out of the cylinder and the duration of the flow of propellant gas into the blast field is altered.</p> <p style="text-align: center;">SEE REVERSE SIDE</p>														

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ABSTRACT (Continued)

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The feasibility of the concept was investigated computationally. Computer programs were prepared to solve the gas dynamics of the blast field which included traveling particles. Computational procedures were used that are analogous to current single phase gas dynamics methods, but which are also based on the conservation relations for mass, momentum and energy in multiphase systems. The velocity and temperature of the gas and particles are allowed to be different in this computational procedure.

The results of the investigation, are that attenuation of the blast field is possible if the attached cylinder is long and the total weight of the expelled particles approaches the weight of the projectile. For shorter cylinders and smaller weights of particles, the blast field is not attenuated. Thus, the blast attenuation concept studied is feasible only in a rifle which is encumbered with an attachment which is so heavy the rifle is no longer a practical weapon.

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CONCEPT FOR ATTENUATION OF THE BACK BLAST  
REGION OF A 105 MM RECOILLESS RIFLE

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## FOREWORD

This is the final report on Contract DAAF07-73-C-0155 for Watervliet Arsenal, IIT Research Institute Project J6293. Charles C. Andrade was project monitor. A significant contribution to the effort described in this report was made by Arnold Wiedermann in the area of mechanisms that would influence the blast field and assistance in the programming effort.

Respectfully submitted,  
IIT Research Institute



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## TABLE OF CONTENTS

	<u>Page</u>
1. INTRODUCTION	1
2. BLAST ATTENUATION	2
a. Basic Mechanism	2
b. Approaches for Implementing the Blast Attenuating Mechanism	4
(1) Davis Gas	5
(2) Short Cylinder Concept	6
3. MATHEMATICAL MODELING	6
a. Conservation Relations	
(1) Mass Conservation	7
(2) Momentum Conservation	9
(3) Energy Conservation	11
b. Subsidiary Relations	12
c. Computational Procedure	15
4. RESULTS	20
5. SUMMARY OF RESULTS AND CONCLUSIONS	34
REFERENCES	35
APPENDIX A - ONE-DIMENSIONAL GAS PARTICLE FLOW	A-1
APPENDIX B - TWO-DIMENSIONAL GAS PARTICLE FLOW	B-1

## LIST OF FIGURES

<u>Figure</u>		<u>Page</u>
1a	Distance of Wave Propagation	3
1b	Pressure Profile at Various Distances from Nozzle	3
2	Elemental Cell	8
3	Element Spatial Distribution with Interleaving of Velocity Points Between Points at Which Density, Energy, Pressure and Composition are Calculated	18
4	Recoilless Rifle and Distribution of Nodes in Finite Difference Grid	19
5	Chamber Pressure; No Water	21
6	Chamber Pressure; 5 lb Water, 5 mm Drop Size	22
7	Chamber Pressure; 5 lb Water, 1 mm Drop Size	23
8	Projectile Velocity and Travel Distance, No Water	24
9	Projectile Velocity and Travel Distance, 5 lb Water, 5 mm Drop Size	25
10	Projectile Velocity and Travel Distance, 5 lb Water, 1 mm Drop Size	26
11	Pressure Profile Contours, 3.5 Msec After Ignition, 5 lb Water, 1 mm Drop Size	28
12	Pressure Profile Contours, 5.7 Msec After Ignition, 5 lb water, 1 mm Drop Size	29
13	Location of Points in Blast Field for which Pressure is Plotted as a Function of Time	30
14	Pressure (Static Plus Dynamic) vs Time with No Water in the Cylinder	31
15	Pressure (Static Plus Dynamic) vs Time with 5 lb of Water in the Cylinder Assumed Drop Size, 5 mm	32
16	Pressure (Static Plus Dynamic) vs Time with 5 lb of Water in the Cylinder, Drop Size, 1 mm	33

## 1. INTRODUCTION

The army is currently investigating methods for arming helicopters with weapons of greater firepower. A major difficulty stems from the relatively weak helicopter structure which cannot sustain the recoil of most large caliber weapons. Although recoilless rifles obviate one problem, the blast field created by propellant gases discharged through the rifle nozzle creates other problems. Damaging peak overpressures of several pounds per square inch would be produced on some parts of the helicopter fuselage.

Constraints which arise from considerations of loading, firing, etc., prevent mounting the rifle so that the blast field does not affect the helicopter's structure. Moreover, severe weight penalties are involved in shielding the fuselage or employing ducts to carry away the nozzle blast gases. The net effect of these constraints is to make the feasibility of arming helicopters with recoilless rifles depend on finding a means for attenuating the intensity of the blast field.

A particular concept for attenuating the blast field was investigated. The concept involves attaching a short cylinder filled with water or solid particles to the rifle nozzle to delay the emergence of propellant gas. The flowing propellant gas would be slowed by driving the particles\* out of the cylinder, thereby reducing the blast pressure, if the expelled liquid or solid does not give up its acquired momentum to the atmosphere too rapidly after it emerges from the cylinder.

The approach taken in this investigation is to develop a computational method and program for describing the blast field produced by the particles expelled from the cylinder. This is accomplished by extending the numerical methods presently used for solving unsteady compressible single component flows to a multiphase flow where the velocity and temperature of the particles can be different from that of the gas in which they are suspended.

\*The word "particles" as used herein refers to solid or liquid particles.

## 2. BLAST ATTENUATION

### a. Basic Mechanism

The blast field behind a recoilless rifle depends mainly upon two factors, the total energy of the propellant gas flowing through the nozzle and the duration of the flow. Since the comparative importance of these factors varies with the distance from the nozzle, it is desirable to have an assessment of the distances in which one or the other has a predominant influence.

The distribution of pressure, density, energy or velocity in the blast field can be regarded as a system of traveling waves in which the local wave speed is the speed of sound. As the propellant gas flows into the blast field and raises the temperature by the effect of compression or by the convection of gases of higher temperature, the wave speed increases. A consequence of this is that a profile of pressure versus time that formerly rose gradually to the peak pressure in the vicinity of the nozzle, changes so that it rises more rapidly at greater distances. As one considers increasing distances from the nozzle the pressure profile eventually steepens to form a shock wave. The process takes place as illustrated in Figs. 1a and 1b. For distances large enough for the profile to steepen up to a shock wave the pressure is independent of the duration of the nozzle flow and only depends on the total energy of the gas and the distance from the nozzle. If the shock pressure were still strong compared to the ambient pressure at these distances it would approach the Taylor's result for a point source explosion (Ref. 1),

$$p \propto E_t / R^3 \quad (1)$$

---

1. Taylor, G., "The Formation of a Blast Wave by a Very Intense Explosion," Vol. 201.

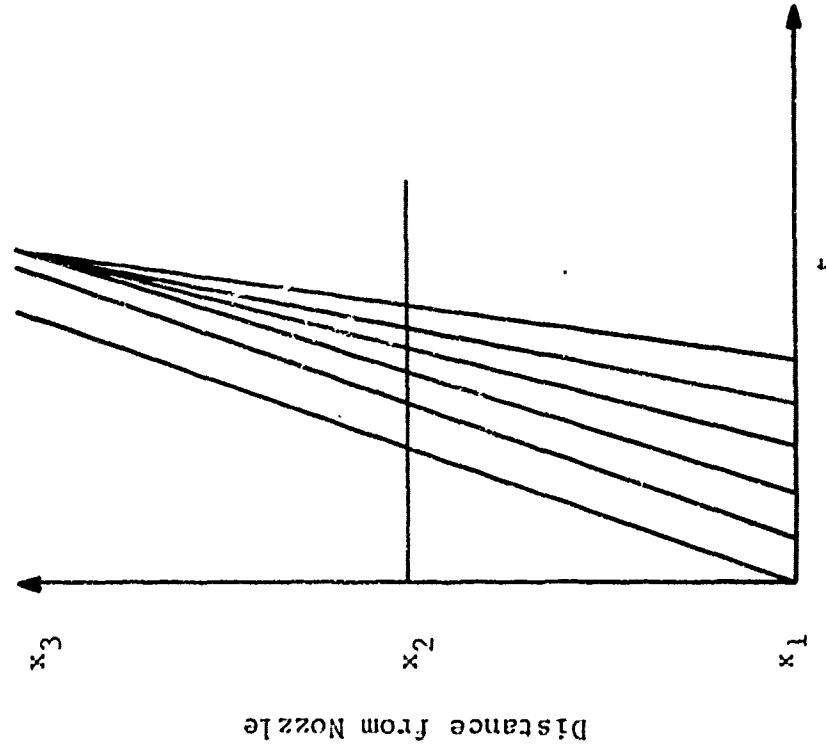


Figure 1a. DISTANCE OF WAVE PROPAGATION

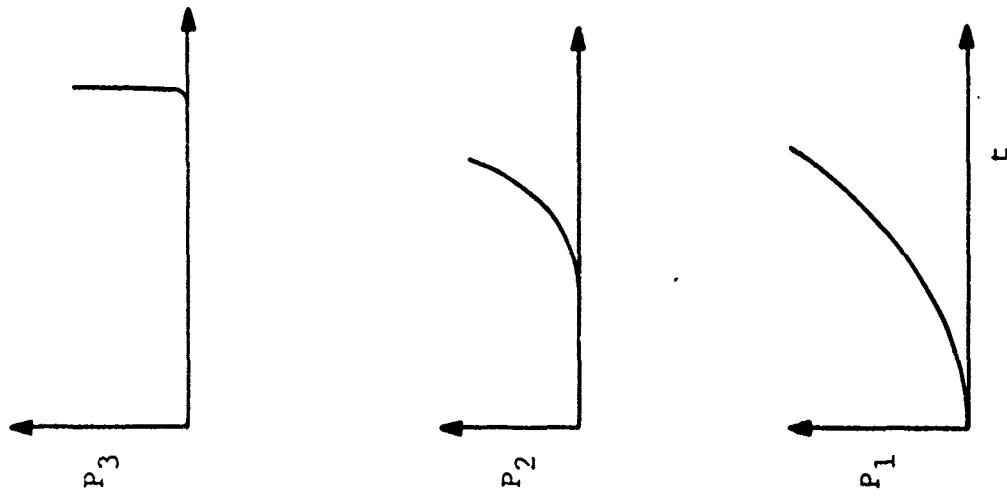


Figure 1b. PRESSURE PROFILE AT VARIOUS DISTANCES FROM NOZZLE

where

$E_t$  = total energy released by explosion  
or in propellant gases

$p$  = pressure

$R$  = realistic distance from source

Although Taylor's result may not be useful for a quantitative estimate of the blast pressure in the problem of concern, the indicated linear dependence of the pressure on the total gas energy is probably a good guide.

These preliminary considerations of the propagation of the blast wave show that for positions in the blast field beyond the distance where a shock wave forms, the only means for attenuating blast intensity is to reduce the total energy in the propellant gas. At lesser distances, nozzle flow duration is a factor and prolonging it would result in reduced peak pressure. An approximation of the distance required for the formation of the shock wave can be made as follows. The temperature of the propellant gas increases the speed of sound two to three times over that which exists in ambient air. The peak chamber pressure is reached about 6 msec after ignition. Equating the travel distances for waves emitted at the initial and peak pressure conditions and assuming that the waves at the peak condition travel at a speed three times greater than the others, yields a distance of 10 ft.

The area of interest on the helicopter extends from about 3 to 10 ft from the fuselage. For much of this area it is apparent that both of the factors discussed will influence the blast pressure, but at the extremity the peak pressure is determined by the total energy in the propellant gases.

b. Approaches for Implementing the Blast Attenuating Mechanism

Two recoilless rifle configurations were considered in which particles are expelled. Each epitomizes a different blast attenuation mechanism: (1) reduction of total energy, and (2) prolongation of flow duration.

(1) Davis Gas

A rifle based on this principle would consist of a straight tube in which particles are expelled from one end and the projectile from the other. Since the momentum of the particles must equal that of the projectile to fulfill the requirements for cancellation of recoil, the tube length required is large unless the weight of the particles is much larger than that of the projectile. For particles of weight equal to the projectile, the tube length would be twice that of a conventional rifle and, therefore, impractical. The blast pressure is reduced because the gas does not escape from the rifle freely until the particles are expelled from the tube. An estimate of the energy removed from the propellant gas by accelerating the projectile and particles may be obtained by assuming that the expansion is isentropic,

$$\frac{e_2}{e_1} = (\text{volume ratio})^{\nu-1} = 0.66 \quad (2)$$

where

$e_1$  = initial internal energy

$e_2$  = internal energy when propellant gas emerges

$\nu$  = ratio of specific heat, 1.21 for propellant  
gas volume ratio = 1/7, chamber-to-chamber  
plus barrel volume

About one-third of the energy in the propellant gas is removed and the approximate effect on the blast field is proportional to the value given for the ratio of the emergent to the initial internal energy.

This concept provides a means for reducing the blast intensity and shows that it is feasible to attenuate the blast pressure by expelling particles. The question remaining is, do the expelled particles release their acquired momentum to the air after exiting? If the particles remain as a coherent mass, they would not; if they expand rapidly, the drag forces acting on the particles would cause

them to transmit their momentum to the air again and produce a blast field. This problem is dealt with by means of the two-dimensional blast field code discussed in the following section. A listing of one- and two-dimensional codes is provided in Appendices A and B.

#### (2) Short Cylinder Concept

This concept was developed in an attempt to achieve blast attenuation without the excessive length of the Davis gun. The cylinder from which particles are expelled is shorter and a nozzle is used between the cylinder and rifle chamber to permit the chamber pressure to build up properly. With the shorter cylinder, the amount of energy that can be removed from the propellant gas is less than with the Davis Gas concept. To have a significant reduction in the intensity of the blast field, the effect of flow duration has to be exploited. In this study, the particles are not compacted and the propellant gas is permitted to leak through void spaces, thus prolonging the flow period. Since the particles are not attached to the cylinder and do not transmit an axial load to it, the recoilless properties of the rifle are not affected significantly by the cylinder.

#### 3. MATHEMATICAL MODELING

The physical problem to be modeled involves the motion of liquid droplets or solid particles through a gas in which strong compressible effects take place that include the formation of shock waves. Because the temperature and velocity of the particles are not usually the same as of the gas at the same location, various interactions take place between the gas and the suspended

particles. The effects of drag and heat transfer cause momentum and energy to be transferred between the gas and the particles. The motion and temperature of the gas therefore, are different than in an analogous flow case without particles.

A numerical method is developed for the solution of this problem that is patterned after the same techniques used for the numerical solution of single component flows. Conservation relations for the mass, momentum and energy are developed for the gas and particle phases and these relations are then expressed in finite difference form for solution by numerical methods. Approaches to the development of the conservation relations and some solution for particular flow cases are summarized by Soo (Ref. 2) and Marble (Ref. 3).

#### a. Conservation Relations

The conservation relations are developed for an elemental cell as indicated in Fig. 2. Particle sizes and mean separation distances are assumed to be small relative to the size of the cell. This limits the applicability of the method to problems in which the mean particle separation distance is small relative to the system size and the scale of the phenomena of interest.

##### (1) Mass Conservation

Equating the accumulation of gas or particles to the net flux of gas or particles into the cell and the contributions due to evaporation and other effects, gives the following expressions for the gaseous and particle phases:

- 
2. Soo, S. L., Fluid Dynamics of Multiphase System, Blaudell Publishing Co., (1967).
  3. Marble, F. E., "Dynamics of Dusty Gases," Annual Rev. Fluid Mech., Vol. 2, (1970).

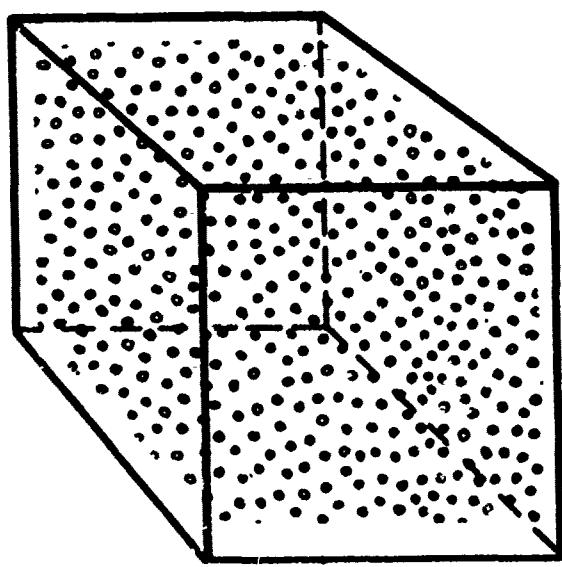


Figure 2 ELEMENTAL CELL.

$$\frac{\partial c_g}{\partial t} = - \nabla \cdot \vec{u}_g c_g + N w_e + w_{pb} \quad (3)$$

$$\frac{\partial c_d}{\partial t} = - \nabla \cdot \vec{u}_d c_d - N w_e \quad (4)$$

$$\frac{\partial N}{\partial t} = - \nabla \cdot \vec{u}_d N \quad (5)$$

where

$c_g$  = concentration of gas

$c_d$  = concentration of matter present as particles

$N$  = number of particles per unit volume

$t$  = time

$\vec{u}_d$  = velocity of particles

$\vec{u}_g$  = velocity of gas

$w_e$  = mass loss of a single particle by vaporization

$w_{pb}$  = mass addition by propellant burning

## (2) Momentum Conservation

When one considers the motion of a single particle the governing equation is obtained by equating the Lagrangian acceleration to the drag force and the pressure difference across the particle.

$$m \frac{D\vec{u}_d}{Dt} = - \vec{D} - V \nabla p \quad (6)$$

where

$\vec{D}$  = drag force vector

$m$  = mass of the particle

$p$  = pressure

$V$  = volume of the particle

For the purpose of the computational method to be developed, a Eulerian expression (i.e., at a fixed point for the derivative), is required and can be obtained if the number of particles within the cell indicated in Fig. 2 is large enough so that the mean velocity is reasonably well defined and can be assumed to be continuous.

$$m \frac{\partial \vec{u}_d}{\partial t} = - m \vec{u}_d \cdot \nabla \vec{u}_d - \vec{D} - V V_p \quad (7)$$

Multiplying through by the number of particles and using Eq. (4) gives the following for the momentum of the particle phase.

$$\frac{\partial c_d \vec{u}_d}{\partial t} = - \nabla \cdot c_d \vec{u}_d; \vec{u}_d - ND - \frac{c_d}{\rho_d} \nabla p \quad (8)$$

where  $\rho_d$  is the density of the material of which the particles are composed.

Although the dyadic notation used ( $V \cdot cu$ ;  $u$ ) is inconvenient, it permits the development of a conservative computational scheme, i.e., one in which the accumulation of momentum in the computational grid is exactly consistent with the fluxes of momentum over the grid boundaries. The alternative and more common expression for acceleration ( $u \cdot \nabla u$ ), does not permit this.

The momentum equation for the gas phase may be obtained by subtracting the equation for the particle momentum derived here from the equations for total momentum of both the gas and the particles. However, the experience obtained with various different computation procedures with this problem, showed that a more stable program is obtained if the computational procedure is based on the equations for the total momentum of both the gas and particles and the momentum of the particles alone rather than on the equations for the momentum of the gas and particle phases.

Equating the accumulation of the momentum to the fluxes across the cell boundaries and the effects of pressure, gives the following expression for the total momentum of both phases,

$$\frac{\partial}{\partial t} (c_g \vec{u}_g + c_d \vec{u}_d) = - \nabla \cdot (c_g \vec{u}_g; \vec{u}_g + c_d \vec{u}_d; \vec{u}_d) - \nabla p \quad (9)$$

Terms relating to particle drag do not appear in this equation since they control only the transfer of momentum between the gas and particle phases and thus do not add to or subtract from the momentum sum.

### (3) Energy Conservation

Considering again a single particle, the following equation is obtained for the temperature by equating the rate of change of stored sensible heat to the losses by convection and evaporative cooling.

$$m c_{pd} \frac{dT_d}{dt} = - (Q_c + Q_e) \quad (10)$$

where

$c_{pd}$  = specific heat of the particle

$Q_c$  = cooling rate of particle by convection

$Q_e$  = cooling rate of particle by evaporation

An Eulerian representation for the rate of temperature change can be obtained when the number of particles within the cell is large enough to permit a reasonable definition of a mean particle temperature.

$$c_{pd} \frac{\partial c_d T_d}{\partial t} + \nabla \cdot c_d \vec{u}_d T_d = - N(Q_c + Q_e) \quad (11)$$

An expression for the total energy in both phases is obtained by equating the rate of accumulation of energy to the fluxes and the work done by pressure effects at the cell boundaries.

$$\begin{aligned}
 & \frac{\partial}{\partial t} c_g (e_g + \frac{1}{2} \vec{u}_g \cdot \vec{u}_g) + c_d (c_{pd} T_d + \frac{1}{2} \vec{u}_d \cdot \vec{u}_d) \\
 & = - \nabla \cdot \vec{u}_g c_g (e_g + \frac{1}{2} \vec{u}_g \cdot \vec{u}_g) + V F p \\
 & - V \cdot \vec{u}_d c_d (c T_d + \frac{1}{2} \vec{u}_d \cdot \vec{u}_d) + (1 - V F) p
 \end{aligned} \tag{12}$$

where

$e_g$  = internal energy of the gas phase

$V F$  = void fraction

As in the case of the momentum equation, the computation scheme is more stable if the computations are based on the total energy and the energy in the particle stream. The gas phase energy is then obtained by calculating the difference in these quantities rather than by calculating the gas energy from an equation for the energy of the gas phase.

### b. Subsidiary Relations

To obtain solutions for the above set of equations, it is necessary to connect the concentration, pressure and density with an equation of state, to evaluate the drag forces and particle heat transfer rates that transfer momentum and energy between the gas and particle phases. A propellant burning law is also required to predict the rate at which mass and energy is added to the propellant gases.

#### Equation of State

Tabulated values for the thermodynamic properties of the propellant gas from 23 different military propellants are given in Ref. 4. For computational purposes a polynomial representation was used to fit the equation of state data. The following nine term polynomial was fitted by least squares to the data for M8 propellant with a maximum discrepancy of only 0.3 of 1 percent:

---

4. Baer, P. G. and Bryson, K. R., Tables of Computed Thermodynamics Properties of Military Gun Propellants, BNL Memo. Rept. No. 1338 (Mar. 1961).

$$p_R = \sum_{i=1}^3 \sum_{j=0}^2 A_{ij} \rho_g^i e_g^j \quad (13)$$

where

$\rho_g$  = density

$e_g$  = internal energy, including energy of formation as defined for  $e$  in Ref. 4

Numerical values for the coefficients  $A_{ij}$  are given in Appendix A in the subroutine entitled EQSTAT of the one-dimensional code.

The gas density to be used in this equation of state is determined from the amount of gas existing in a unit volume and the void fraction.

$$VF = 1 - \frac{c_d}{pd} \quad (14)$$

$$\rho_g = c_g / V \quad (15)$$

### • Drag Forces

Drag forces acting on the drops are calculated from the drag coefficient and the dynamic pressure as follows:

$$D = C_d \frac{\pi}{4} a^2 \rho_g \left| \vec{u}_d - \vec{u}_g \right| \frac{(\vec{u}_d - \vec{u}_g)}{2} \quad (16)$$

where

$a$  = particle diameter

$C_d$  = drag coefficient

$\rho_g$  = gas density

Absolute values of the velocity difference are used in the manner shown to preserve the proper sign and direction of the drag force irrespective of the sign of the velocity difference.

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4. Baer, P. G. and Bryson, K. R., Tables of Computed Thermodynamics Properties of Military Gun Propellants, BRL Memo. Rept. No. 1338 (Mar. 1961).

Coefficients of drag  $C_d$  are obtained from the particle Reynolds number  $Re$  as shown, Ref. 5

$$C_d = \frac{24}{Re} \quad Re < 2.05 \quad (17)$$

$$C_d = \frac{18}{Re} 0.6 \quad 2.05 < Re < 486 \quad (18)$$

$$C_d = 0.44 \quad 486 < Re \quad (19)$$

where

$$Re = \frac{\rho_g a |u_d - u_g|}{\mu_g}$$

$\mu_g$  = gas viscosity

#### • Heat Exchange

The rate at which heat is transferred from the gas to the particulate phase is obtained from correlations for the heat transfer coefficient on a single particle (Ref. 6),

$$\frac{ha}{k_g} = 2 + 0.34 Re^{0.6} Pr^{1/3} \quad (20)$$

where

$h$  = heat transfer coefficient

$k_g$  = thermal conductivity of the gas

$Pr$  = Prandtl number of the gas

The heat transfer rate,  $Q$ , is given by

$$Q = \pi a^2 h (T_g - T_d) \quad (21)$$

5. Perry, J. H., Chemical Engineering Handbook, McGraw-Hill Publishing Co. (1950).

6. McAdams, Heat Transmission, McGraw-Hill Publishing Co. (1954).

where

$T_g$  = the gas temperature.

• Propellant Burning Law

The rate at which gas and energy is added to the propellant gas will be computed from surface regression rate of the burning propellant. Watervliet Arsenal provided the following correlation for the propellant to be considered.

$$R = 0.00186 p^{0.83} \quad (22)$$

where  $p$  is the pressure in pounds per square inch and  $R$  is the regression rate of the propellant surface in inches per second.

c. Computational Procedure

For the purpose of presenting the numerical method by which solutions to the preceding equation may be obtained, it is useful to use a more compact notation. Each of the differential Eqs. (3), (4), (5), (8), (9), (11) and (12) can be expressed in the following form.

$$\frac{\partial r_n}{\partial t} + \frac{\partial r(u_n + v_n)}{\partial r} + r \frac{\partial v_n}{\partial r} + \frac{\partial r(w_n + z_n)}{\partial z} = r \xi_n \quad (23)$$

where  $r$  is the radial distance from the axis and  $z$  is the distance along the axis. Each of the variables  $\alpha$  to  $\xi$  are defined in Table I. The velocity components,  $u$  and  $w$ , are of the phase considered.

The numerical procedure is based on a finite difference form for each of the equations represented by Eq. 23. Conceptually, the field of interest is divided into discrete cells and the finite difference equations describe the rate of accumulation of mass, number of particles, momentum, energy, etc. in terms of the fluxes of these quantities across the cell boundaries and the other quantities appearing in Eq. 23. In the particular grid system used in this study, velocity is defined at the cell boundaries

Table I DEFINITION OF TERMS IN EQUATION

Conservation of	$\alpha$	$\beta$	$\gamma$	$\nu$	$\delta$	$\xi$
Gas	$c_g$	0	0	0	$NW_e + W_p g$	
Particle Mass	$c_d$	0	0	0	$-NW_e$	
Number of Particles	$N$	0	0	0	0	
Radial Momentum of Particles	$c_d u_d$	0	0	0	$-ND_r - \frac{c_d}{\rho_d} \frac{\partial p}{\partial r}$	
Radial Momentum of Gas and Particles	$c_g u_g + c_d u_d$	0	0	0	0	
Axial Momentum of Particles	$c_d w_d$	0	0	0	$-ND_z - \frac{c_d}{\rho_d} \frac{\partial p}{\partial z}$	
Axial Momentum of Gas and Particles	$c_g w_g + c_d w_d$	0	0	0	0	
Energy of Particles	$c_{pd} c_d T_d$	0	0	0	$-N(Q_c + Q_e)$	
Energy of Gas and Particles	$c_g (e_g + \frac{1}{2} u_g \cdot u_g)$ $+ c_d (c_{pd} T_d + \frac{1}{2} u_d \cdot u_d)$	$VF \cdot p \cdot u_g$ $+(1-VF) \cdot p \cdot u_d$	0	$VF \cdot p \cdot w_g$ $+(1-VF) \cdot p \cdot w_d$	0	

and particle number, concentration, pressure energy and temperature are defined at the cell centers as indicated in Fig. 3. The fluxes across the cell boundaries are computed in accordance with the donor cell concept described by Gentry and Martin (Ref. 7). That is, the flux of particles for example, is calculated from the particle density in the cell which donates the particles.

Because velocity, in the computational procedure used here, is defined at the cell boundaries, computations for the momentum of the gas and of the particles are based on special cells displaced one half the distance between the grid lines so that it is centered over the points where the velocity is defined. The momentum,  $p_u$ , is thus based on the velocity at the special cell centers and an interpolated value for the density at that point. Similarly, the kinetic energy at the center of the cells where internal energy is defined is based on interpolated values for the kinetic energy.

Our experience with this computational procedure is that spurious negative values for the internal energy and pressure are obtained less frequently than with the more usual procedure in which the velocity is calculated for the same positions as the density and energy.

For the study of the blast field behind the weapon, the method would be implemented in a two-dimensional grid as shown in Fig. 4. The grid spacing increases with distance from the nozzle to accommodate a large region without an excessive number of grid points. Two computer programs were prepared for solving the blast field problem: (1) a one-dimensional program which describes the interior ballistics of the rifle and the flow from the cylinder; (2) a two-dimensional program which uses the flow from the cylinder as input and calculates the blast field.

- 
7. Gentry, R. A.; Martin, R. E.; and Daly, B. J., "An Eulerian Differencing Method for Unsteady Compressible Flow Problems," Computational Phys., Vol. 1, pp 87-118 (1966).

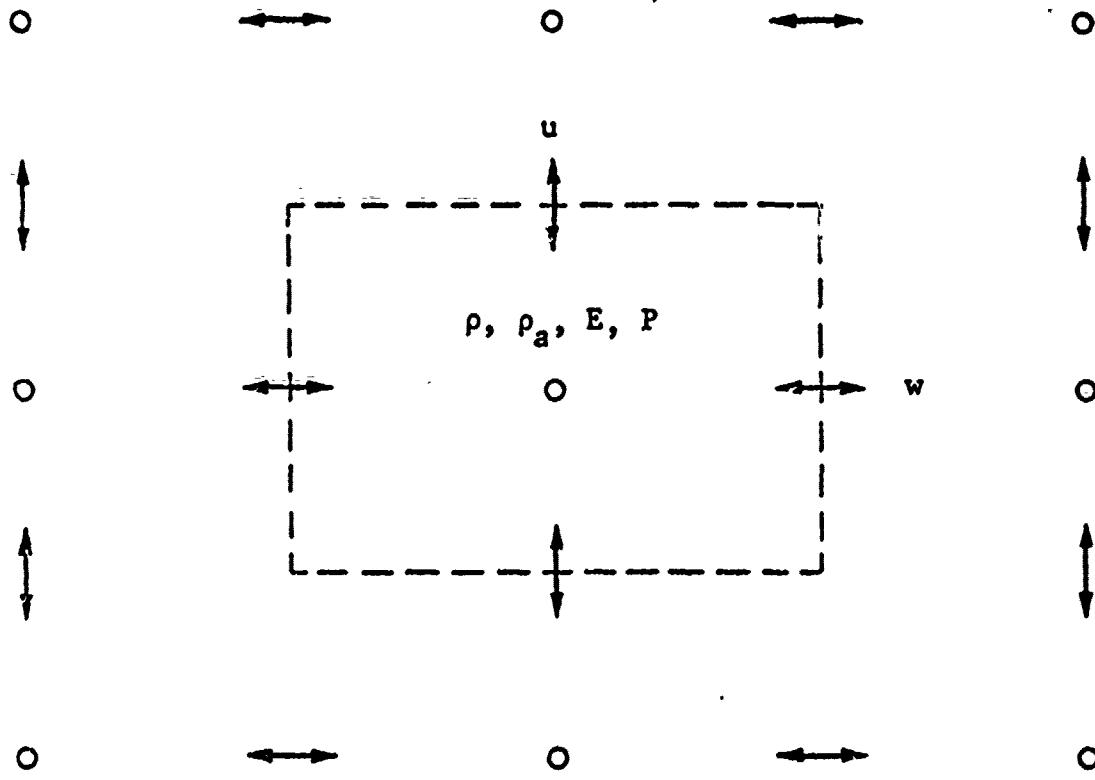


Figure 3

ELEMENT SPATIAL DISTRIBUTION WITH INTERLEAVING  
OF VELOCITY POINTS BETWEEN POINTS AT WHICH  
DENSITY, ENERGY, PRESSURE AND COMPOSITION ARE  
CALCULATED

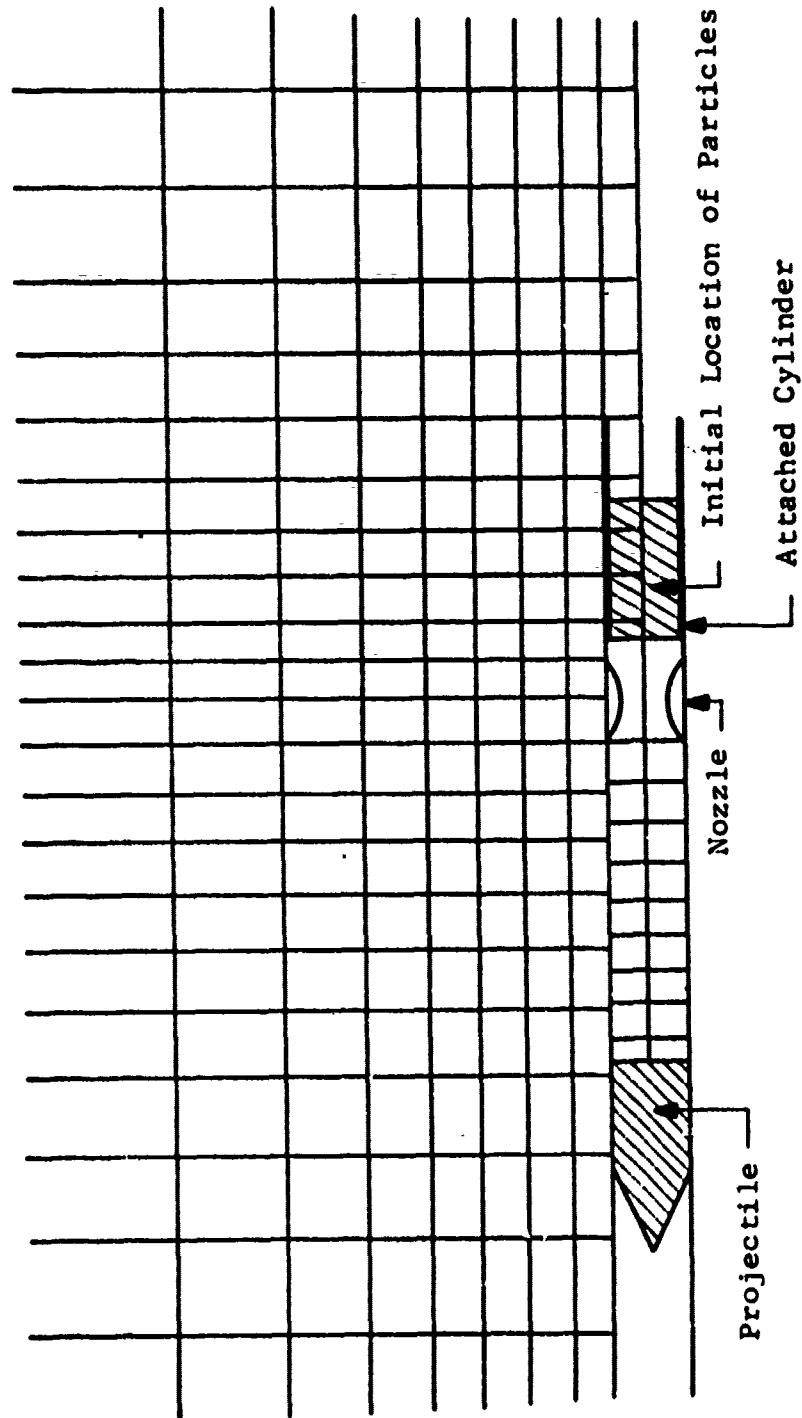


Figure 4 RECOILLESS RIFLE AND DISTRIBUTION OF NODES IN FINITE DIFFERENCE GRID

#### 4. RESULTS

The interior ballistics and nozzle blast field were calculated for the conditions defined by the following values:

charge	8.1 lb
web	0.061 in.
bore	105 mm
barrel length	140 in.
chamber volume	200 in.
cylinder diameter	7.4 in.
cylinder length	24 in.
throat diameter (effective)	3.26 in.

Results for three different conditions in the attached cylinder are presented:

- no water in the cylinder
- 5 lb of water with a drop size of 5 mm
- 5 lb of water with a drop size of 1 mm

Results obtained with the one-dimensional model which furnished the inputs for the two-dimensional model are given in the following figures. Chamber pressures are given in Figs. 5-7.

These were obtained by calculating the average value of the pressures at nodes in the chamber region of the gun. A value of approximately 8000 lb was obtained for the peak chamber pressure in each case. The peak pressure is shown to increase slightly when water is used in the cylinder and when the drop size is diminished. This is due to the resistance to the flow or propellant gas developed by the water drops which diminish the leak rate of the rifle. The abrupt drop in chamber pressure that occurs at about 15 msec, coincides with the burnout of propellant. Values obtained for the projectile travel and velocity while in the barrel are shown in Figs. 8-10.

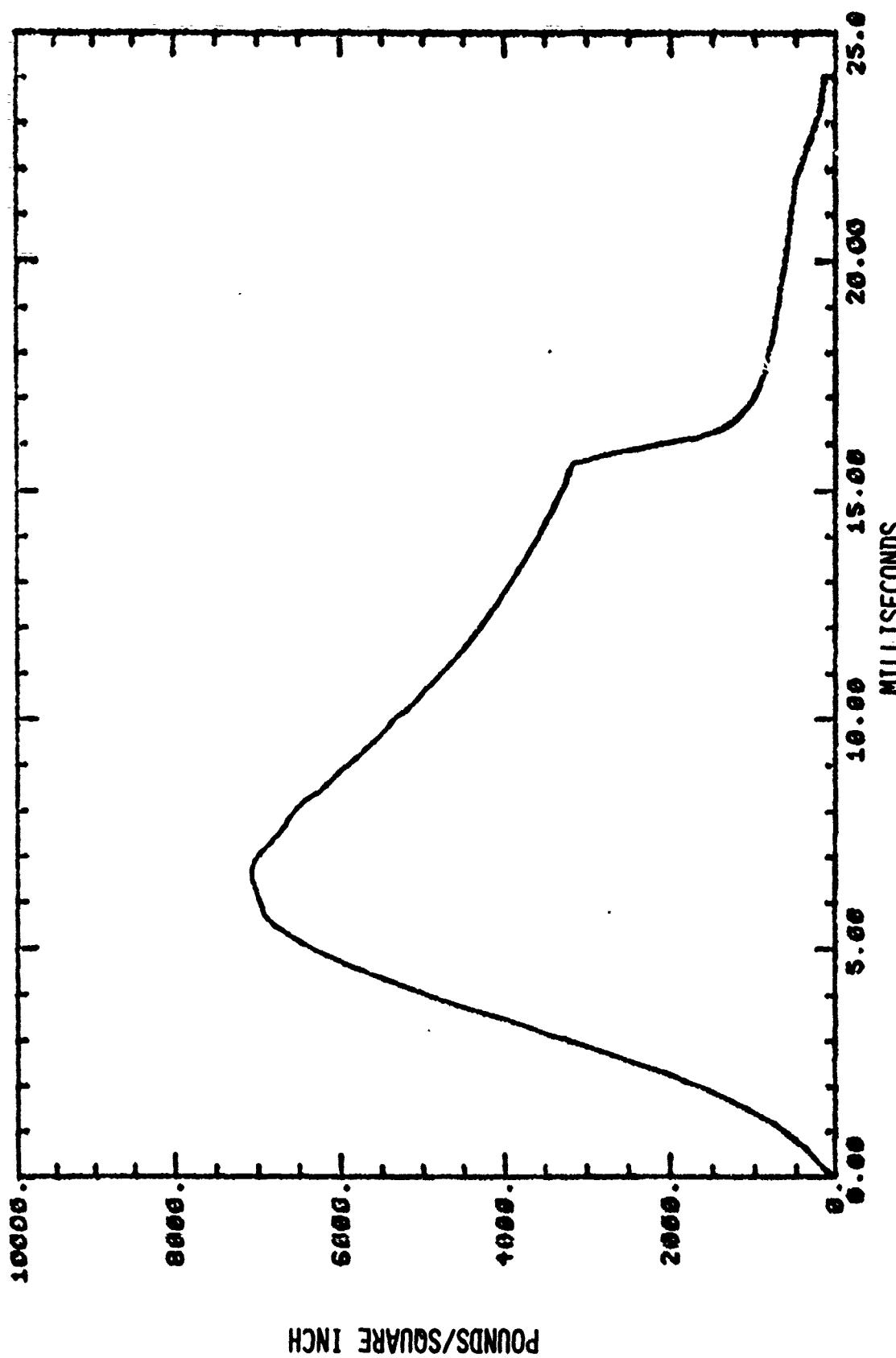


Figure 5 CHAMBER PRESSURE; NO WATER

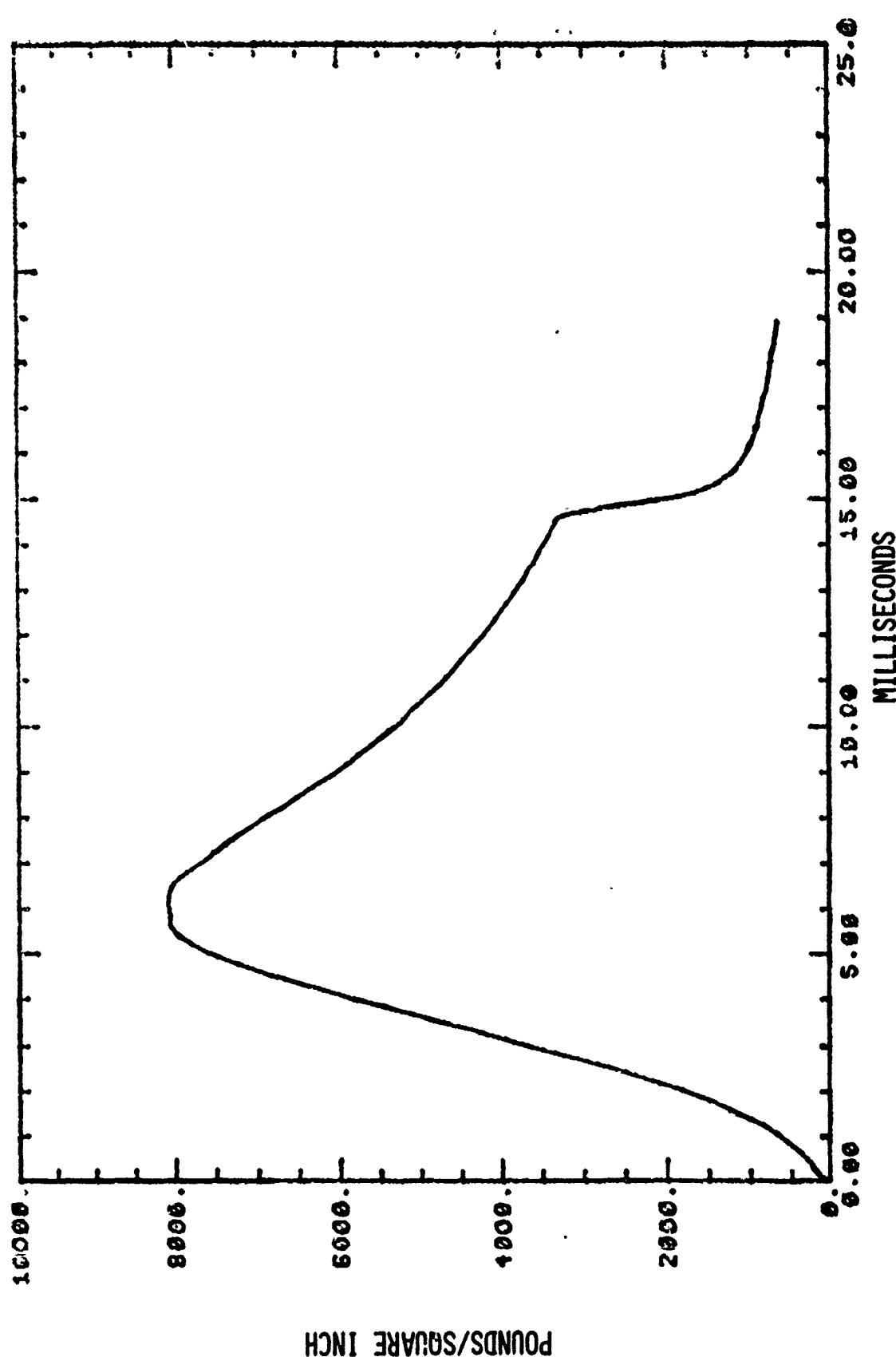


Figure 6 CHAMBER PRESSURE; 5 LB WATER, 5 MM DROP SIZE

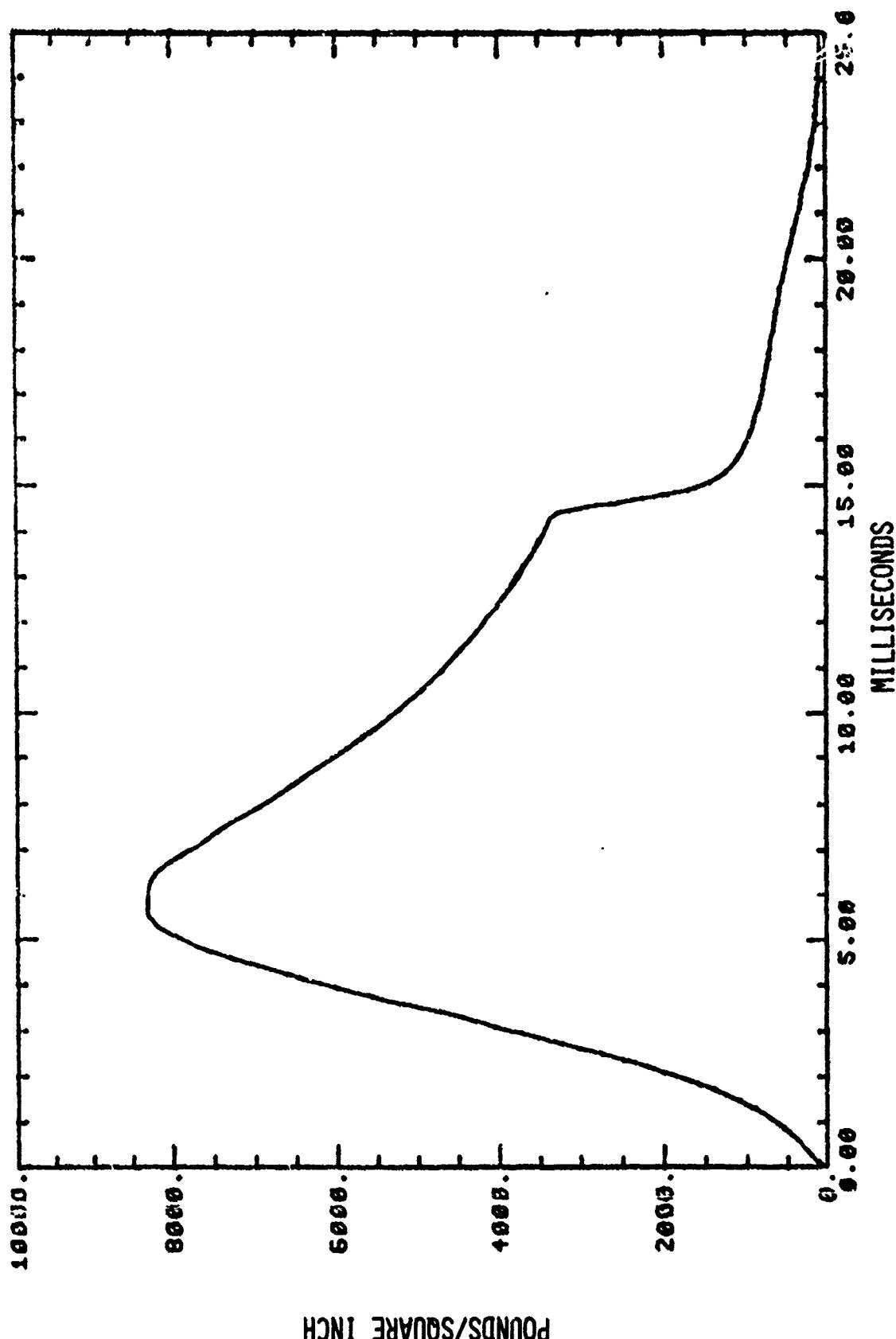


Figure 7 CHAMBER PRESSURE, 5 LB WATER, 1 MM DROP SIZE

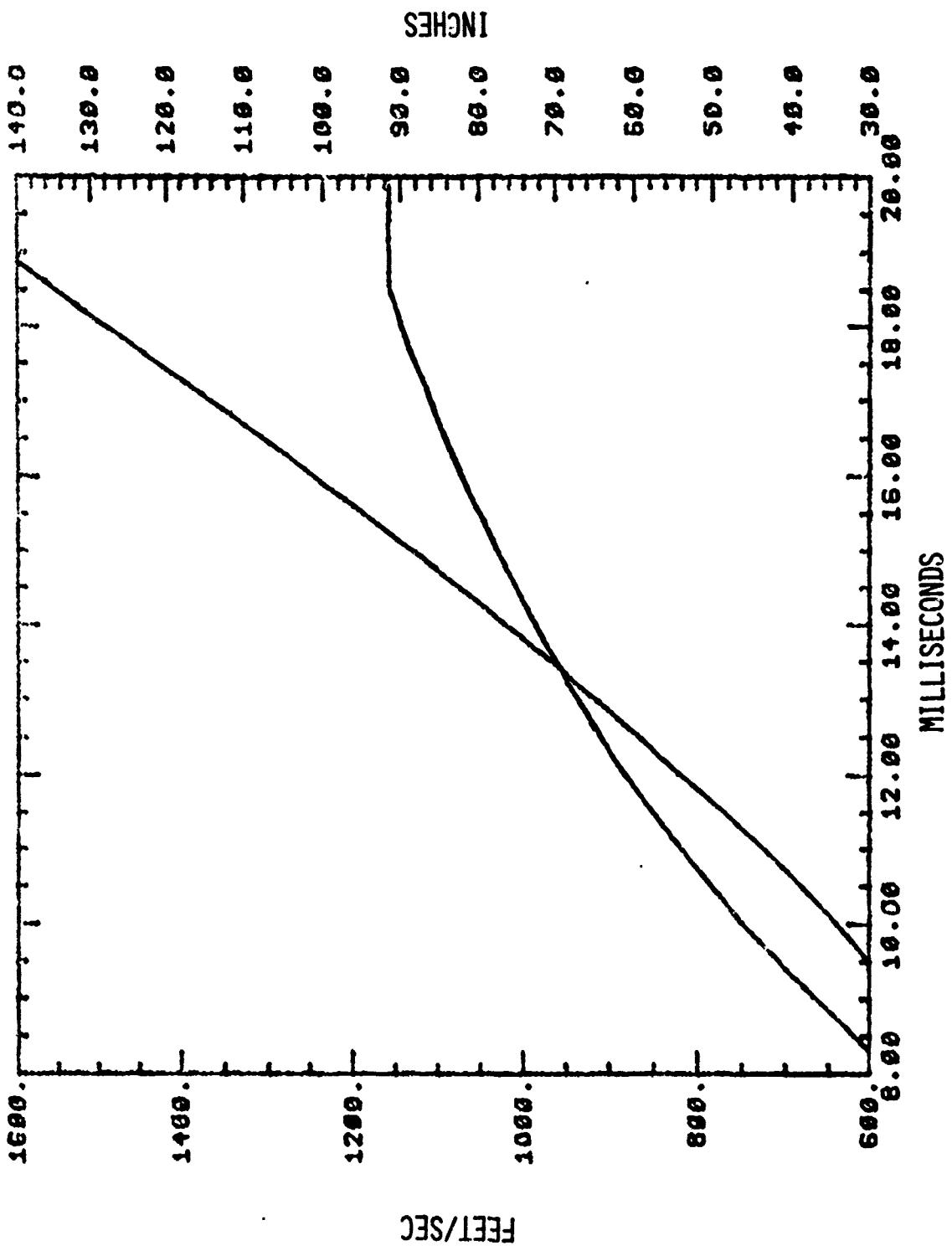


Figure 8 PROJECTILE VELOCITY AND TRAVEL DISTANCE, NO WATER

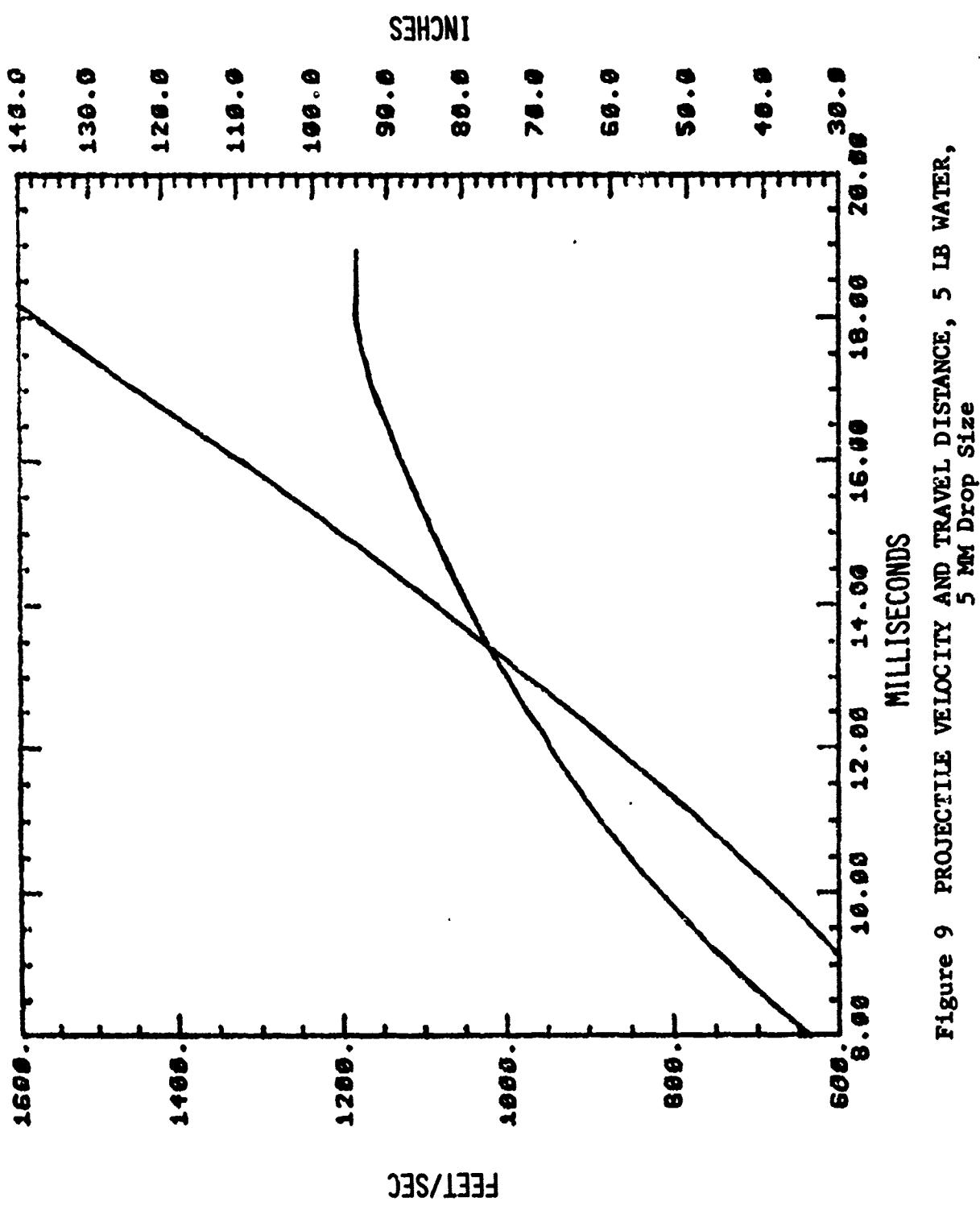


Figure 9 PROJECTILE VELOCITY AND TRAVEL DISTANCE, 5 LB WATER,  
5 MM DROP SIZE

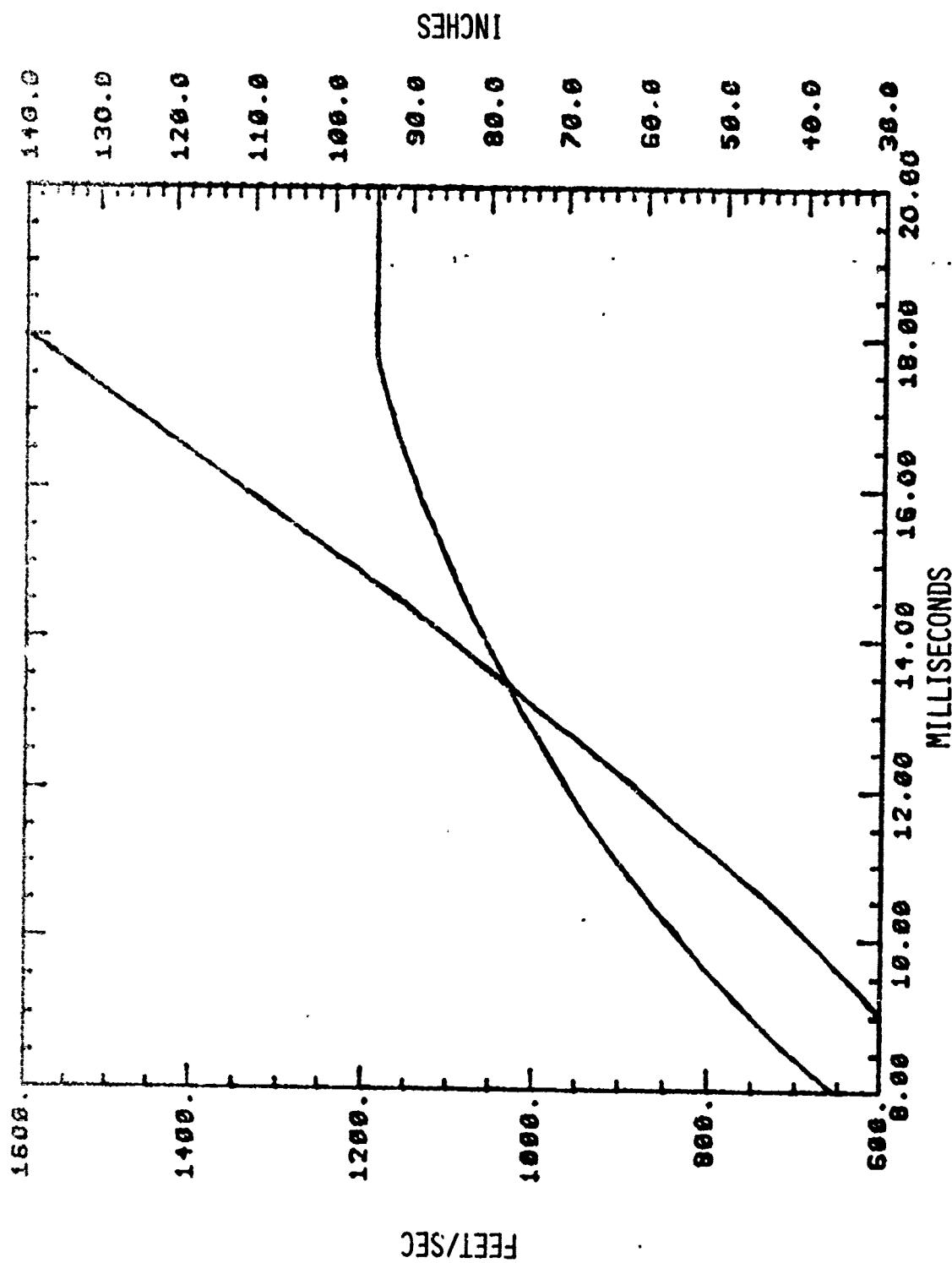


Figure 10 PROJECTILE VELOCITY AND TRAVEL DISTANCE, 5 LB WATER,  
1 MM DROP SIZE

The output of the one-dimensional program was used as an input condition for the two-dimensional program. Early time examples of the spatial pressure distribution are shown in Figs. 11-12. The flow out of the attached cylinder is directed to the right and the cylinder exit is located on the horizontal axis in the center of the smallest contour. As one would expect, the pressure profile is elongated in the direction of flow. For the purpose of evaluating the effect on the blast pressure of water in the cylinder attached to the rifle, the pressure was listed for selected points for each case. The location of these points A-F is indicated in Fig. 13, and the pressure pulse profiles in Figs. 14-16. These pressure pulse profiles show that the peak pressure increases as water is added to the cylinder and the drop size is diminished.

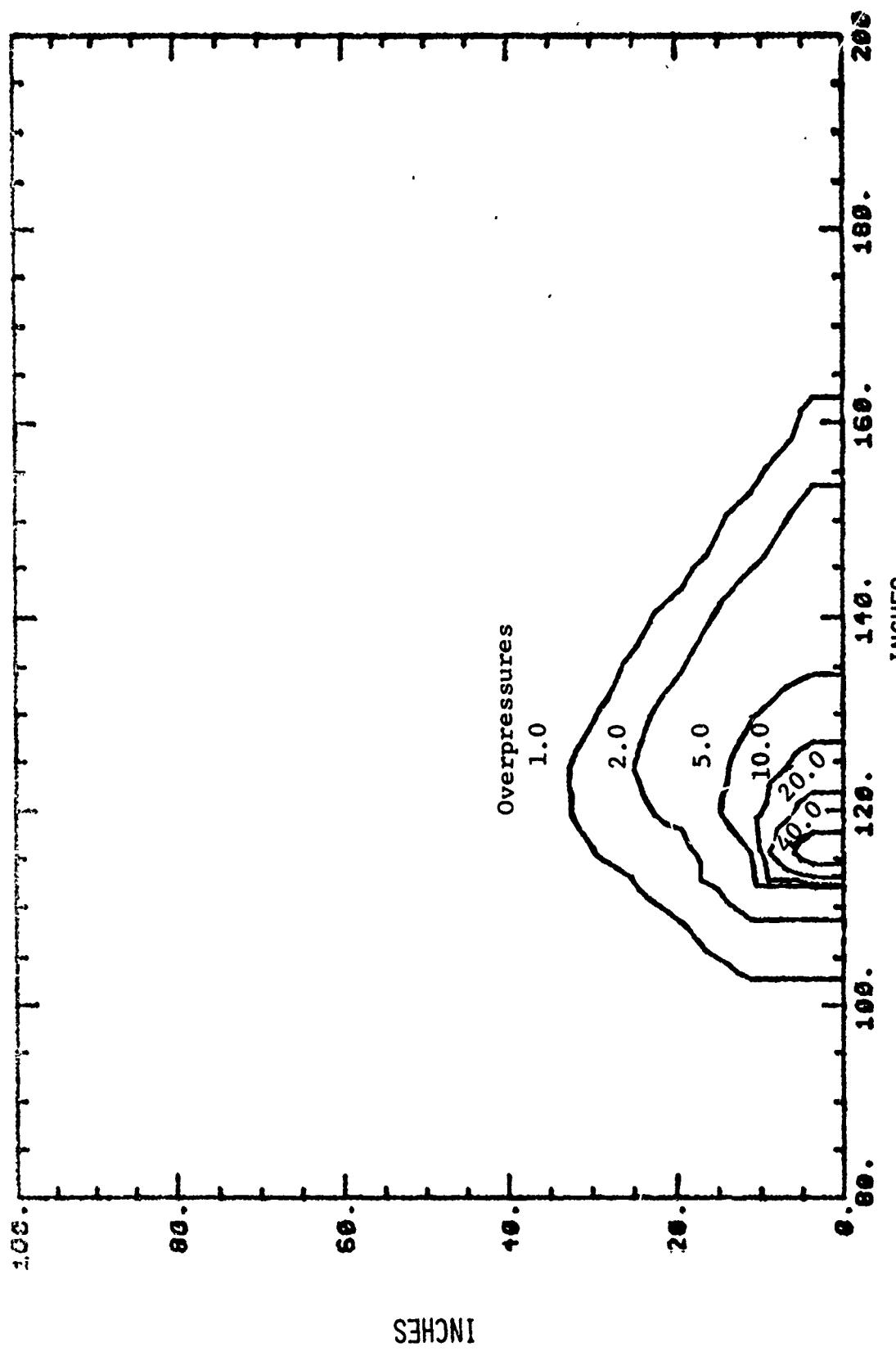


Figure 11 PRESSURE PROFILE CONTOURS, 3.5MSEC AFTER IGNITION, 5 LB WATER  
1 MM DROP SIZE

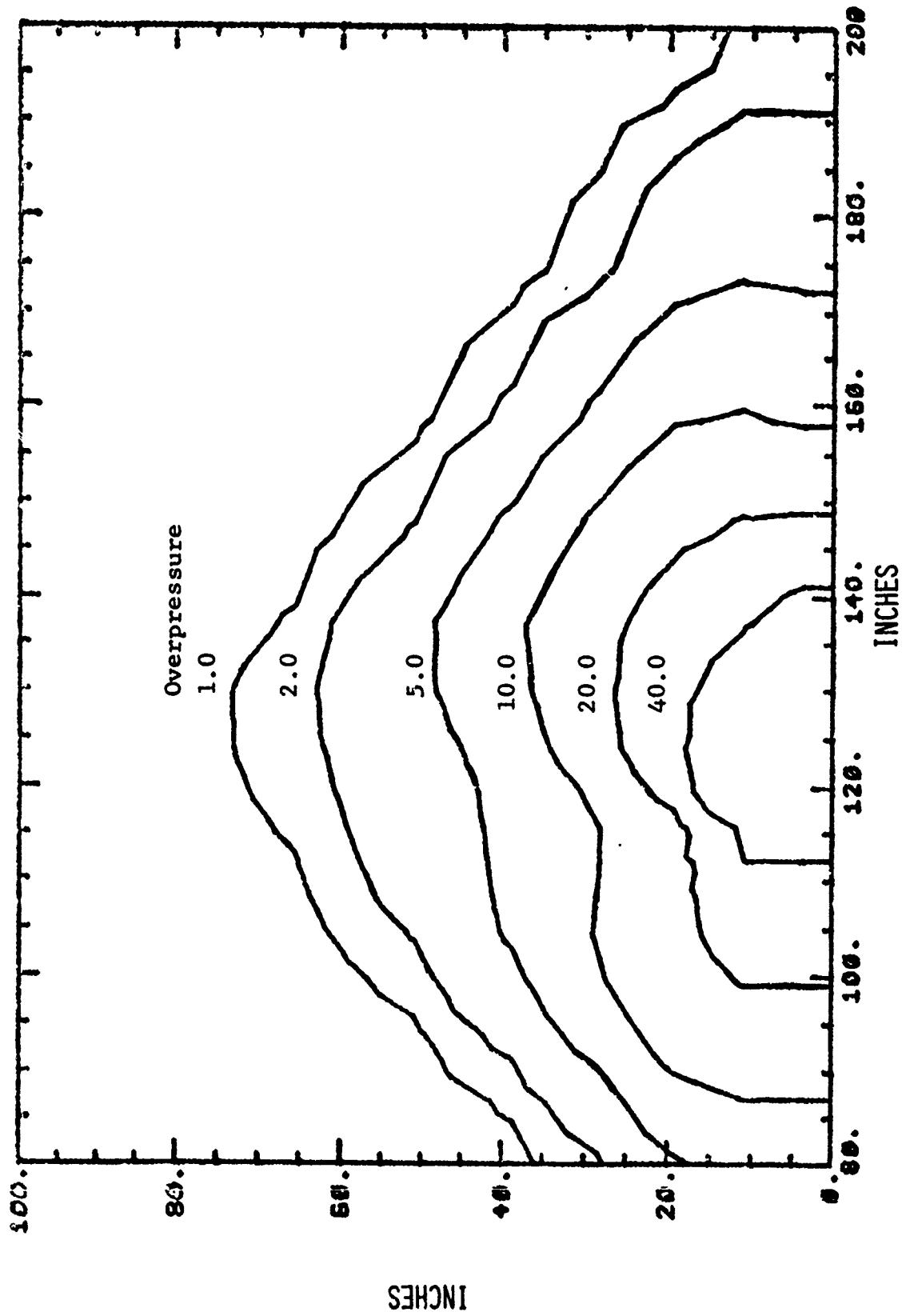


Figure 12 PRESSURE PROFILE CONTOURS, 5.7 MSECS AFTER IGNITION, 5 LB WATER,  
1 MM DROP SIZE



Figure 13 LOCATION OF POINTS IN BLAST FIELD FOR WHICH PRESSURE IS PLOTTED AS A FUNCTION OF TIME

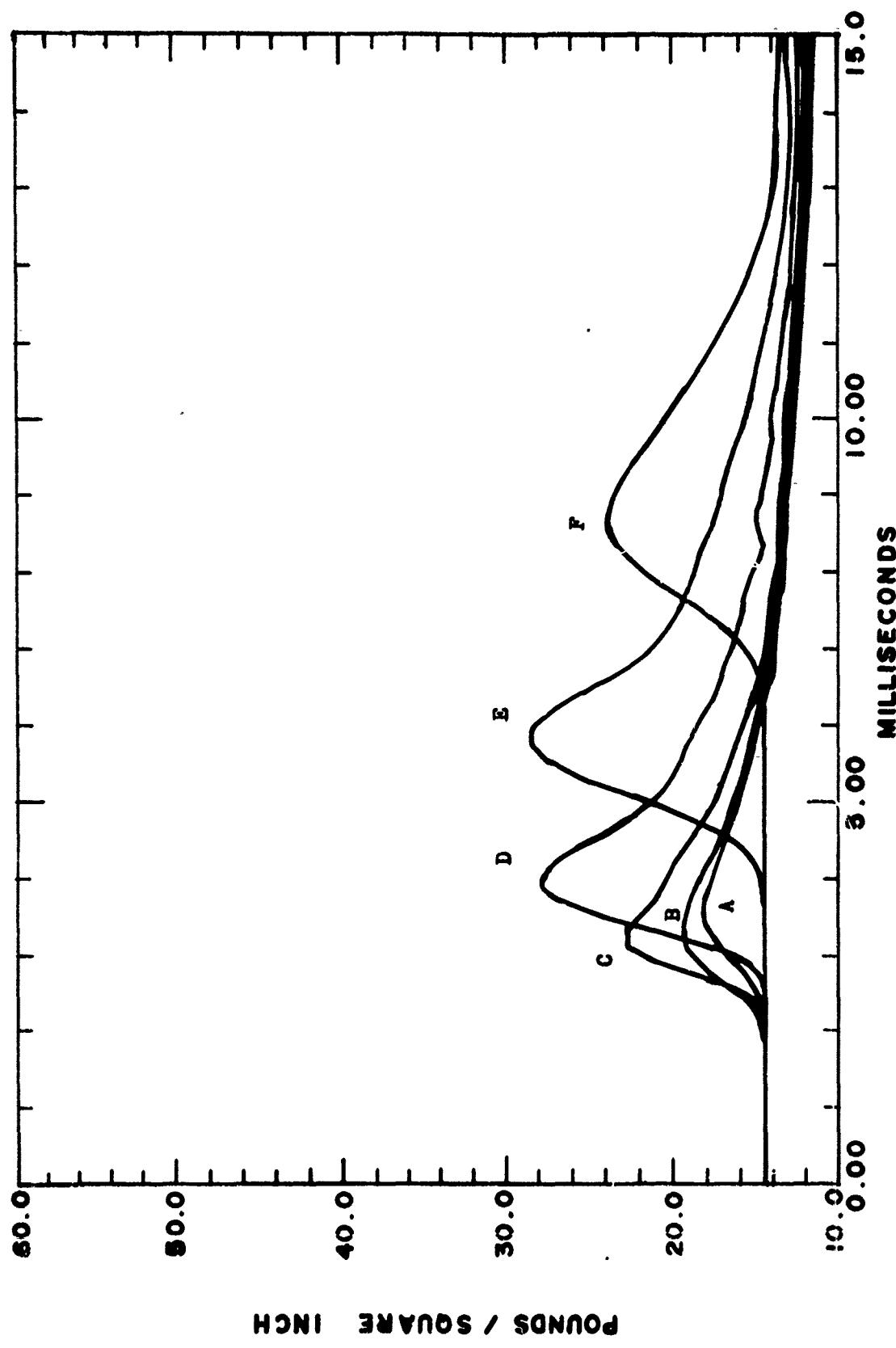


Figure 14. Pressure (static plus dynamic) vs time with no water in the cylinder

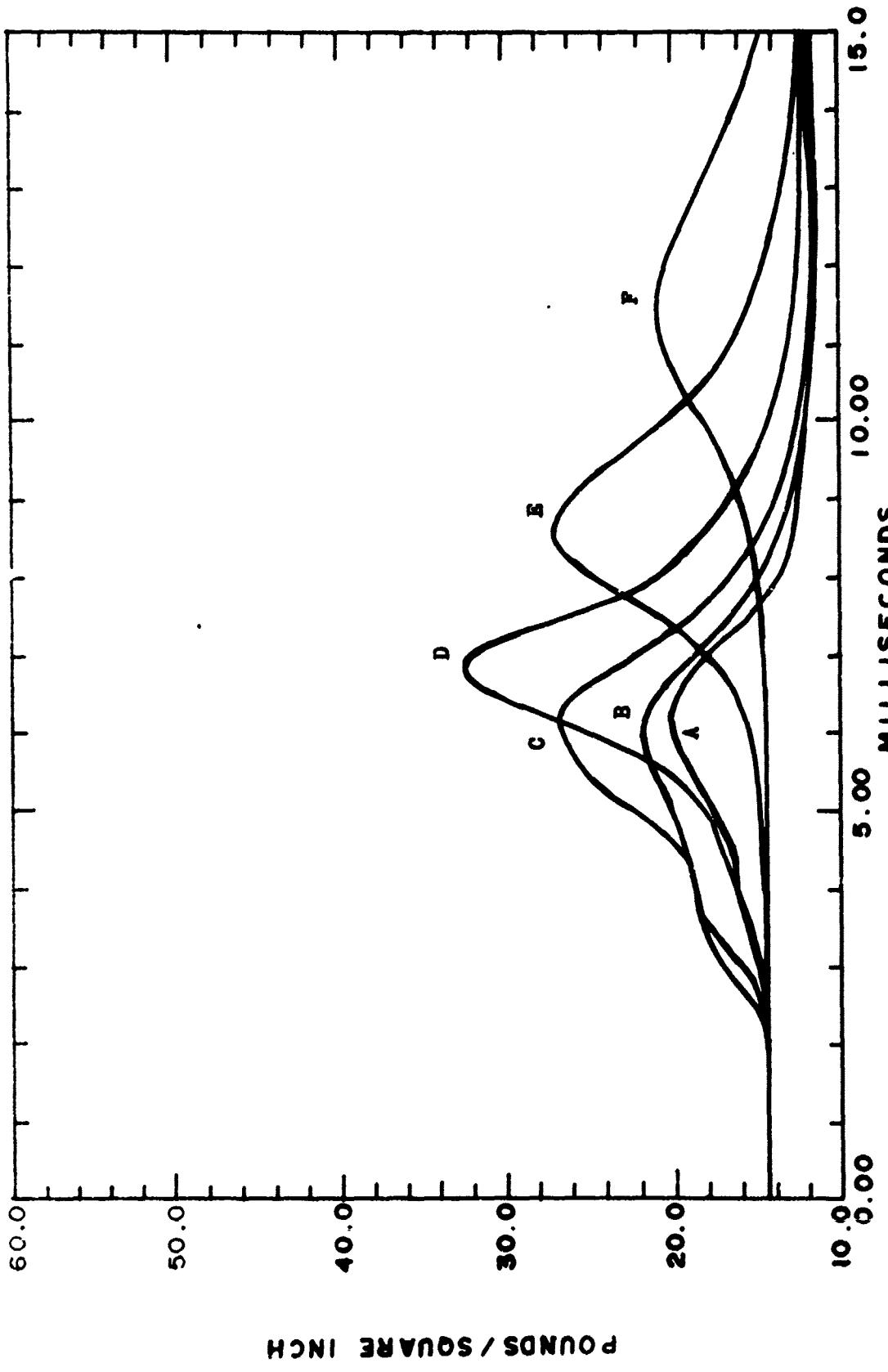
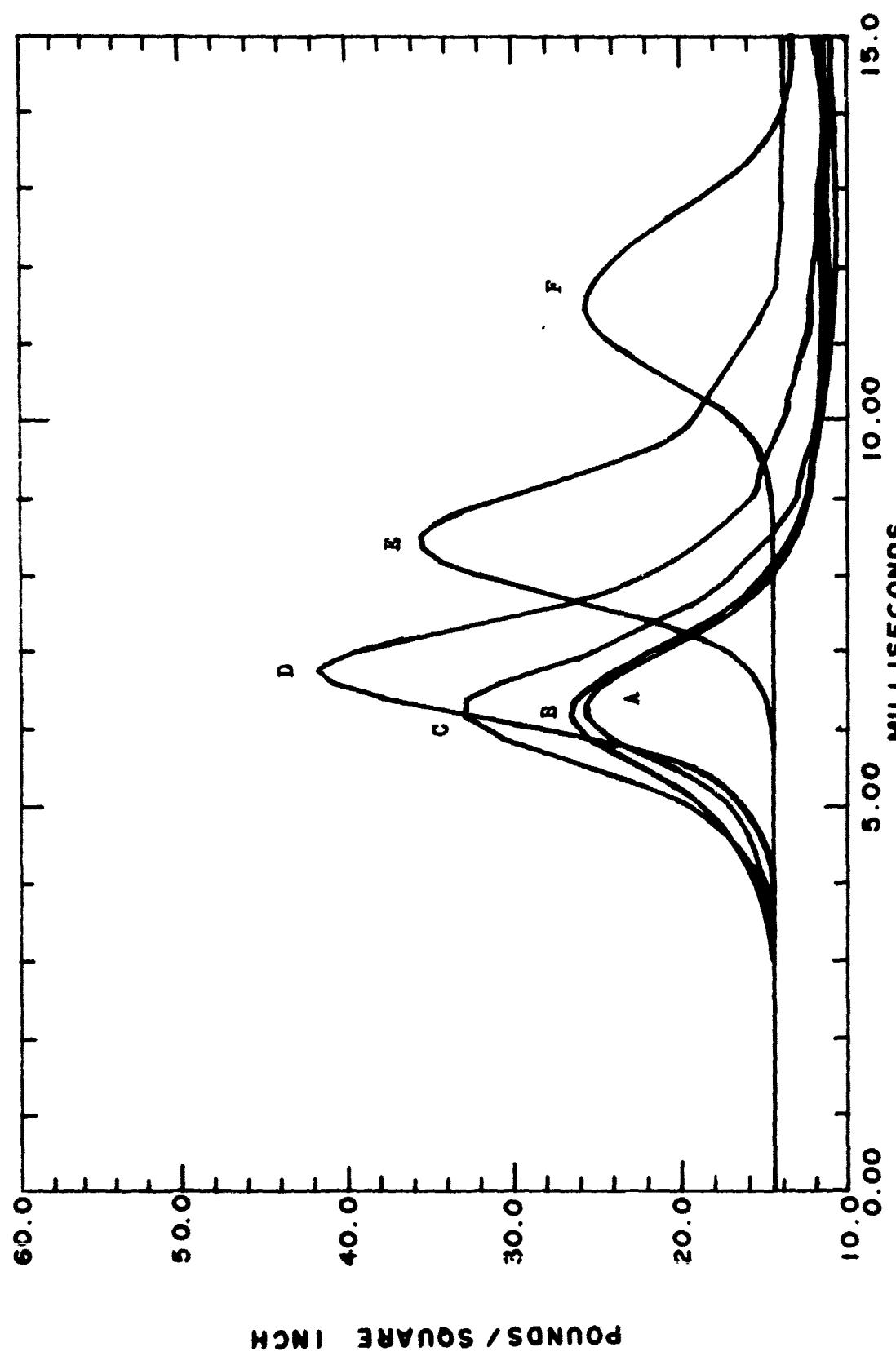


Figure 15 PRESSURE (STATIC PLUS DYNAMIC) VS TIME WITH 5 LB OF WATER IN THE ASSUMED DROP SIZE - 5 MM CYLINDER.

Figure 16 PRESSURE (STATIC PLUS DYNAMIC) VS TIME WITH 5 LB OF WATER IN THE  
CUPHOLDER, TOP SIZE, 1 IN.



POUNDS / SQUARE INCH

## 5. SUMMARY OF RESULTS AND CONCLUSIONS

Contrary to the reasons advanced for expecting blast attenuation, the results obtained show that the peak pressure is increased rather than reduced by expelling water. The duration of the pulse is shorter, however, so that the total blast load represented in the pulse may be somewhat reduced. The most probable explanation involves the effect of flow duration and perhaps also the ability of the particles to transfer momentum to the blast field after expulsion from the cylinder.

In the study of the short cylinder concept it was thought that an optimum particle size might exist that would prolong flow duration, thereby reducing the peak blast pressure. It appears, however, that particles of suitable size, on the order of 1 mm, also have a drag-to-weight ratio so large that the momentum absorbed from the propellant gas in the cylinder is given back to the air when the particles emerge. The remaining hope for reducing the blast pressure with a concept involving particle expulsion is to use considerably more water so as to absorb more energy from the propellant gas, or to exploit other phenomena not investigated in this study, such as quenching the gas by the cooling effect of droplet vaporization.

## REFERENCES

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5. Perry, J. H., Chemical Engineering Handbook, McGraw-Hill Publishing Co. (1950).
6. McAdams, Heat Transmission, McGraw-Hill Publishing Co. (1954).
7. Gentry, R. A.; Martin, R. E.; and Daly, B. J., "An Eulerian Differencing Method for Unsteady Compressible Flow Problems," Computational Phys., Vol. 1, pp 87-118 (1966).

**APPENDIX A**  
**ONE-DIMENSIONAL GAS PARTICLE FLOW**

ONE DIMENSIONAL GAS PARTICLE FLOW

MAIN010  
MAIN020  
MAIN030  
MAIN040  
MAIN050  
MAIN060  
MAIN070  
MAIN080  
MAIN090  
MAIN100  
MAIN110  
MAIN120  
MAIN130  
MAIN140  
MAIN150  
MAIN160  
MAIN170  
MAIN180  
MAIN190  
MAIN200  
MAIN210  
MAIN220  
MAIN230  
MAIN240  
MAIN250  
MAIN260  
MAIN270  
MAIN280  
MAIN290  
MAIN300  
MAIN310  
MAIN320  
MAIN330  
MAIN340  
MAIN350  
MAIN360  
MAIN370  
MAIN380  
MAIN390

IA = MAXIMUM AXIAL NOSE  
KU = OUTPUT FREQUENCY  
KP = PLOT FREQUENCY  
KN = NUMBER OF RUNGE KUTTA STEPS TO BE EXECUTED ON THIS RUN  
KST = 1 START WITH CONDITIONS AT INSTANT OF IGNITION  
KST = 2 CONTINUE INTEGRATION WITH CONDITIONS ON A FILE PRODUCED  
DURING A PREVIOUS RUN  
KKST = RUNGE KUTTA STEP ON FILE USED FOR STARTING CONDITIONS  
KS1S = 1 PARTICLE SLIP ACCOUNTED FOR  
KS1S = 2 NO SLIP IS ASSUMED  
KS1H = 1 TEMPERATURE DIFFERENCE BETWEEN GAS AND PARTICLES IS  
ASSUMED TO EXIST AND HEAT TRANSFER IS CALCULATED.  
KS4H = 2 GAS AND PARTICLES HAVE THE SAME TEMPERATURE.  
KS1K = 1 PARTICLES EVAPORATE  
KS1K = 2 PARTICLES DO NOT EVAPORATE.  
FL = ARTIFICIAL VISCOSITY COEFFICIENT  
EE = ALLOWABLE ERROR LIMIT IN RUNGE KUTTA INTEGRATION  
RHOP = DENSITY OF PARTICULATE PHASE  
VISCG = VISCOSITY OF GAS  
VFMIN = VALUE OF MINIMUM VOID FRACTION WHICH IF EXCEEDED  
ACTUATES ARTIFICIAL PRESSURE IN PARTICULATE PHASE  
PDF = FACTOR FOR ARTIFICIAL PRESSURE IN DISPERSED PHASE  
FJ = MECHANICAL EQUIVALENT OF HEAT  
CMAX = MAXIMUM ALLOWABLE VALUE FOR TIME STEP LIMITING COEFFICIENTS  
PD(1) = ARTIFICIAL PRESSURE IN MOMENTUM EQUATION FOR  
PARTICULATE PHASE  
Q(1) = ARTIFICIAL VISCOSITY  
Y(1) = UNBURNED PROPELLANT POUNDS  
Y(2) = PROJECTILE VELOCITY FT/SEC  
Y(3) = TRAVEL INCHES  
Y(4) = IMPULSE POUND X SEC  
Y(5) = IMPULSE X TIME POUND X SEC XX 2  
FILES  
8 FYST  
9 RESTART  
11 FEXI  
12 FY52  
PARAMETER VDC=200  
PARAMETER NFK=1330

```

DIMENSION Y(1000),X(1000),AC(NRKD),AE(NRKD),EEF(7)
COMMON /WRC/ NZ
COMMON /ALR/ IN,K,KP,KM,IPL1,IP2,XST,KKST,IMW,KSW,KK0,
2 VFS,VFE,VPS,VPE,VAD,VIO,X83,ZMAX,Z,I2,VHL(NDC),VHR(NDC),
3 FL,RHCB,VISCC,VFIN,P05,FJCMAX,V1,PV2,PV3,CHARG,PROJ,CHAML,
4 WIDH,CPP,BL,FORCE,DSCP5,5C,3C,A,CCPCIN,AC,VPROJ,ZPRO,PB,
5 FCNDC,7),CG(NDC),EG(NDC),FN(NDC),TP(NDC),FM(NDC),UG(NDC),
6 UPNDC,(4CN5),(4NC5),AE(NDC),V(NDC),V3(NDC),XC(9),RHG(NDC),PG(NDC),
7 PRNDC),DPNDC,(5)NDC,DF(NDC,7),G(NDC,7),Q(NDC),Z(NDC),ZB(NDC)
4 ,GAC(NDC),GCA(NDC),GEA(NDC),VFA1(NDC),FWV(NDC)
CCINON, / MU / KSW,S,KSWH,K5,M
COMMON /NC/ NZ,Z,(7),ZWC(7),IZC(7),ZW(7),IEX
CONTINUE
4 READ(5,101) IM,KK,KP,KM,KST,KKST,KSJS,KSJH,KSHH
101 FORMAT(8I10/I10)
      WRITE(6,102) IM,KK,KP,KM,KST,KSJS,KSJH,KSHH,K5,M
102 FORMAT(14I4X,2D14.6,14I4,14I4)
      2   3X,2HK4

```

A-3

ONE CYCLES/NATIONAL 645 PARTICLE FLOW

```

3      5X,2-KP   1E-12,160
4      5X,2-KV   1E-12,160
5      5X,3-KST   1E-12,160
6      5X,4-KST   1E-12,160
7      5X,4-KSW   1E-12,160
8      5X,4-KSWH  1E-12,160
9      5X,4-KSWH  1E-12,160
IF (14) 13,4,15
4 STOP
1 CO:NTINUE
READ (5,110) IR,Z23,ZMAX,ZPL1,ZPL2
110 FORMAT (1I3,4F10.5)
READ (5,153) DPO,FL,ER,RHO,CPP,VISCG,VISCS,VFMIN,PDF,FJ,CMAX,PV1,PV2,
2 DV3
121 FORMAT (6,104) DPO,FL,ER,RHO,CPP,VISCG,VFMIN,PDF,FJ,CMAX,PV1,PV2,
2 PV3
WRITE (6,105) SF10.5 / SF10.5
124 FORMAT (1H3,9X,3HDP0
9X,2HFL
9X,2HER
9X,4HRHOP
9X,3HCPD
9X,5HVISCG
9X,5HVFIN
9X,3-HDF
9X,2HFJ
9X,4-HC MAX
9X,3HPV1
9X,3HPV2
9X,3HPV3
D READ (5,105) CMAX,PCQJW,WH2C,WICHT,BL,BORE,VCHAMB,CNA1,CNA2,
2 R.,DTH,DEXC,ENL,GWT
1C5 FORMAT (AF10.5 / 6F10.5)
WRITE (6,106) CHARG,PROJW,WICHT,BL,BORE,VCHAMB,CNA1,CNA2,
2 R.,DTH,DEXC,ENL,GWT
1C4 FORMAT (1H3,9X,6HCARGE
1H3,1PE14.6, 7H POUNDS
1C3,2-PROJW
1C2,1CX,2-H20
1C1,1CX,5-H13TH
1C0,1CX,5-H13TH
MAIN0580
MAIN0590
MAIN0600
MAIN0610
MAIN0620
MAIN0630
MAIN0640
MAIN0650
MAIN0660
MAIN0670
MAIN0680
MAIN0690
MAIN0700
MAIN0710
MAIN0720
MAIN0730
MAIN0740
MAIN0750
MAIN0760
MAIN0770
MAIN0780
MAIN0790
MAIN0800
MAIN0810
MAIN0820
MAIN0830
MAIN0840
MAIN0850
MAIN0860
MAIN0870
MAIN0880
MAIN0890
MAIN0900
MAIN0910
MAIN0920
MAIN0930
MAIN0940
MAIN0950
MAIN0960

```

```

5   ,13X,2-3L    ,1H-5,   E14,6, 74 INCHES
6   ,13X,4-3D2E   ,1H-5,   E14,6, 3H MY
7   ,13X,5-VCH4 13E   ,1H-5,   E14,5,134 CUBIC INCHES
8   ,13X,4-CNA1   ,1H-5,   E14,5, 8H DEGREES
9   ,13X,4-CNA2   ,1H-5,   E14,5, 8H DEGREES
A   ,13X,2-PRV   ,1H-5,   E14,5, 7H INCHES
B   ,13X,3-DTH   ,1H-5,   E14,5, 7H INCHES
C   ,13X,4-CEXC   ,1H-5,   E14,6, 7H INCHES
D   ,13X,3-4EVL   ,1H-5,   E14,5, 7H INCHES
E   ,13X,4-5VLT   ,1H-5,   E14,5, 7H POUNDS
F   KK:= -1
G   KK:= 1
H   KK:= 7*14+5
I   CALL CALXC (CVAL,C\A2,RN,DTH,DEXC,SL,BORE,VCHAM8,ENL,XC,XBS)
J   WRITE (6,108) (I,XC(I),I=1,9)
K   FC=NAT (1H / (1H +10X,2H18,12,3X,6HX5(I)=,1PE14.6))
L   CALL ZSPACE
M   CALL I0FZB(ZPL1=2,54,IPL1)

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

CALL ICFZB(ZP,2*2,54,IPL2)
IPL=IPL1-1
CALL IOFZ(-ENL*2,54,1EX)
IEX=IEX+1
      WRITE(6,111) 13,Z,2,ZMAX,ZPL1,ZPL2,IPL2,IPL1,IEX
111 FORMAT(1H0,5X,3.1R*,16.5X,3H2*,1PE12.5,5X,5HZWAX,E12.5,5X,
      2.5HZPL1*,E12.5,5X,5HZPL2*,E12.5, / 1H .5X,5HPL1*.16.5X,
      3.5HPL2*.16.5X,4.1EX*.16)
      WRITE(6,137) (I/2(I),2B(I),A(I),V(I),V8(I),I=1,1H)
137 FCRTAT(1+1,5X,1.4,10X,1H2,16X,2-25) 17X,1H4,18X,2HAB,17X,1H,
1.1AX,2-NYD /(1A,1.6,1PE19.6,5E19.6)
      READ(5,112) VZW,Z(1),I=1,7)
112 FORMAT(13,7F10.5)
      DC 5 I=1,2,
      Z2=2.54*(XC(3)-Z(1))
      ZNC(I)=Z2
      CALL IOFZ(22,11)
      I2A(I)=11
      WRITE(6,133) (1.12W(I),2W(I),1.2W(I),I=1,N2W)
133 FORMAT(1H0,14X,1.1W,7X,3H12W,8X,2H2A,12X,3HZWC /
      2.61H,10X,210,1DE14.5,E14.5)
      DSCPSS=455.59*980.,516/(2,54**2)
      CCPC1N=2.54**3
      AP=2,3*CH4*2G*453,53/(1.6**10TH*(2,54**3))
      AC=0,25*3.141593*((80RE/25,4)**2)
      Z2=0.5*(XC(3)+XC(4))/2.54
      CALL ICFZB(22,NFS)
      CALL IOFZB(2.54*XC(7),NFE)
      NPS=NFE
      NFE=NFE+1
      CHANL=VCHA*4E*(2.54**3)/(0.25*3.141593*(0,1*B0RE)**2)
      Z2=Z(NPS)+CHANL+2.54*4.0
      CALL IOFZ(22,NPE)
      WRITE(6,139) NFS,Z(NPS),NPE,Z(NPE)
139 FORMAT(1H0, 9X,4HNF,3,16.5X,1PE14.6,
      2 10X,4HNPS*,16.5X, E14.6,
      3 10X,4HNPE*,16.5X, E14.6,
      4 1CX,4RNOP*(1CP0/1G)*3)
      F1:=3.141593/6,C*RNOP*(1CP0/1G)*3)
      MAIN150
      MAIN149
      MAIN148
      MAIN147
      MAIN146
      MAIN145
      MAIN144
      MAIN143
      MAIN142
      MAIN141
      MAIN140
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      MAIN138
      MAIN137
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      MAIN15
      MAIN14
      MAIN13
      MAIN12
      MAIN11
      MAIN10
      MAIN9
      MAIN8
      MAIN7
      MAIN6
      MAIN5
      MAIN4
      MAIN3
      MAIN2
      MAIN1
      MAIN0
      )

```

```

CL=RHO*(1.0-VFN1)
FLLEN=MH20*453.59/(CL*0.25*3.141593*(DEXC*2.54)**2)
ZL=2.54*XC(4)-FLLEN
CALL I0FZ(2.54*XC(4),12)
CALL I0FZ(ZL,11)
I1=11-1
I2=12-1
VOLP=(29*(I2)-25*(I1-1))*0.25*3.141593*(DEXC*2.54)**2
CL=MH20*453.59/VOLP
CLEARMAX(CL,1.0E-13)
F,F1=CL/F,Y1
VE=1.0-CL/RHOP
CGG=VE*G/3910.94
IF (KST-1) 7,2,7
Y(1)=CHAE6
2 DO 3 I=2,5
3 Y(I)=3.0
FNPN1=ENPN1*1.36-3

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

FNPV1=MAX1(FNPV1,1.0E-15/FMN)
ZP=CHAML+2.54*(4.0+XC(7))
CALL IOUFZ(ZP,IPRJ)
VV=ABC(IPRJ)*(ZP-Z3(IPRJ-1))
IMX=IPRJ
IPO=1
KS=1
DO 11 I=1,15
  IF (I-IPRJ) 15,14,15
  14 VVV=VV
  15 VVV=V(I)
  20 CONTINUE
  F(I,1)=0.001094*VV
  F(I,3)=FNPV1*VV
  F(I,5)=FMN*FNPV1*VV
  F(I,4)=293.0*F(I,5)
  F(I,2)=F(I,1)*(-1.145E3)+F(I,4)
  F(I,6)=0.0
  F(I,7)=0.0
  11 DC 12 I=11,12
  F(I,1)=CGG*V(I)
  F(I,3)=FNPV1*V(I)
  F(I,5)=FNPV1*V(I)
  F(I,4)=F(I,5)*296.0
  12 F(I,2)=F(I,1)*(-1.145E3)+F(I,4)
  DT=0.00001
  EZ=ER*0.01
  7 CONTINUE
  DO 9 I=1,5
    9 RE(I)=ER
    AE(1)=EZ*CHARG
    AE(2)=EZ*2000.0
    AE(3)=EZ*140.0
    AE(4)=EZ*2003.0
    AE(5)=AE(4)
    AEF(1)=EZ*0.1
    AEF(2)=AEF(1)*1000.0
    AEF(3)=EZ*FNPV1

```

AEF(5)=EZ\*FM\*\*FNP  
AEF(4)=AEF(5)\*5CJ.0  
AEF(5)=AEF(1)\*40000.0  
AEF(7)=AEF(5)\*40000.0  
L=5  
DO 6 I=1,1  
CC 6 K=1,7  
L=L+1  
RF(L)=ER  
AE(L)=AEF(K)\*V(L)  
V(L)=F(I,K)  
RE=1.0 6  
RE=1.0 9  
REALD 1C  
REWIND 11  
IF (KST-2) 17,16,17  
16 CC,T1UE  
OC 13 LL=1,1000

MAIN2110  
MAIN2120  
MAIN2130  
MAIN2140  
MAIN2150  
MAIN2160  
MAIN2170  
MAIN2180  
MAIN2190  
MAIN2200  
MAIN2210  
MAIN2220  
MAIN2230  
MAIN2240  
MAIN2250  
MAIN2260  
MAIN2270  
MAIN2280

ONE DIMENSIONAL GAS PARTICLE FLOW

```
MAIN220
MAIN230
MAIN2310
MAIN2320
MAIN2330
MAIN2340
MAIN2350
MAIN2360
MAIN2370
MAIN2380
MAIN2390
MAIN2400
MAIN2410
MAIN2420
MAIN2430
MAIN2440
MAIN2450
MAIN2460
MAIN2470
MAIN2480
MAIN2490
MAIN2500

READ (5) KK,T,DT,IPRJ,IMW,KSW,(Y(I)),I=1,IRK)
READ (1C) K9
IF (KK-KKST) 18,19,19
19 CONTINUE
12 CC,TINE
      DD 2 LL=1,10000
      READ (8) KK1
      READ (11) KK3
      IF (KK1-KK3) 6,13,13
      6 CONTINUE
      13 CONTINUE
      KK=KK-1
      IPR=IPRJ
17 CONTINUE
      EXTERNAL DEFIV,CNTL
      CALL RK2 (DEFIV,CNTL,Y,DY,AE,AE,T,DT,IRK,2,0E6)
      RE*TND 8
      RE*TND 9
      RE*TND 10
      RE*TND 11
      CC*TQ 1
      END
```

ONE-DIMENSIONAL GAS PARTICLE FLOW

A-11

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11 FORCE=FORCE+PG(1)\*(AB(1-1)-AB(1))  
11 FORCE=FORCE/(780.616\*453.59)  
DY(4)=FORCE  
DY(5)=EV(4)  
RETURN  
END

DER10400  
DER10410  
DER10420  
DER10430  
DER10440  
DER10450

## **Preceding page blank**

```

CG(1)=F(1,1)/V(1)
FN(1)=2*X1(FXN,F(1,3))/V(1)
FXV(1)=2*AX1(FMN,F(1,5))/V(1)
FN(1)=FMV(1)/FN(1)
? CONTINUE
  GO TO 1,32,KSW
 4: CG(IPRJ)=F(IPRJ,1)/VV
FN(IPRJ)=AN(YT(FN),F(IPRJ,3))/VV
FXV(IPRJ)=AN(X1(FN),F(IPRJ,5))/VV
3: CONTINUE
DC 3 I=2,1w
CG=(VN((1)*CG(I+1)*VN((I+1))*C5(I+1))/VN(I))
FN5=(VN((1)*F(VN((I+1)*VN((I+1))*FXV(I+1))/VN(I))
GT0(42,33),KSPS
42 CONTINUE
UP(I)=F(I,7)/(FN3*VB(I))
UG(I)=(F(I,6)-F(I,7))/(CGB*VB(I))
GO TO 3

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

33 CONTINUE
      UP(1)=F(1,6)/(CC5+FM6)*VB(1))
      UC(1)=UP(1)
      CONTINUE
      UC(1)=(2.0*UC(2)+45*(2-UH(3))*5*(3))/48(1)
      UP(1)=(2.0*UP(2)+45*(2-UH(3))*48(1))/48(1)
      GO TO 4,X5,
      UC(IPRJ)=32.45*VB(0)
      UP(IPRJ)=32.45*VB(0)
      UC(IV+1)=UC(IV)
      UB(IV+1)=UB(IV)
      EXSCV(IV)=EXSCV(IV)
      EXAC(IV)=EXAC(IV)
      EXPAC(1)=EXP(1)
      GCTD(35,34),KS=-
      CONTINUE
      EC(1)=(F(1,2)-F(1,1)*EC0+F(1,5)*EECP)/FJ
      TPC(1)=F(1,4)/F(1,5)*CP
      CALL TDETA( ECD(1),RHG(1),TG(1))
      GOTO 7
      CONTINUE
      SF(1,2)-(F(1,1)*EC0+F(1,5)*EECP)/FJ
      VFB(1,5)=MF(1,5)/RHG(1)
      RCB(5)=VFB
      F1=3.655322*740*(2.15013-ABD(1,34853-24124))
      F2=1.337984E+24*CH(1,34853-24124)
      F3=-3.15*CP+F(1,1)*CP+F(1,2)
      K2=SF2*F(1,1,5)*CP-S
      IF (F(1,5)-1.0-E-4*F(1,1))23124,24,2
      23 CONTINUE
      ET=ET-(X1+ET)*(W2+E1*W1-W2*E1)
      ET=ET-(X1+ET)*(W2+E1*W1-W2*E1)
      EG(1)=ET

```

GO TO 902

C FLAG EG(1)=(SCRT(W2-W4,0-W1-W3)-W2)/(2,0-W3)

24 WTST=W2-W4,WTST=3,WTST=4,WTST=5

WTST1=A4MAX1(WTST,3,0)

EG(1)=(SCRT(WTST1),WTST1-2)/(2,0-W3)

IE=(WTST) 901,902,902

901 WRITE(6,901),S,A40,WTST,W1,W2,W3,F1,F2,F3

901 FORMAT(1H,5X,12DG,E21) WARNING,5X,241=,15,5X,2HS,1PE12,5,5X,

2412,5,5X,3H,3=E12,5,5X,3H,1=E12,5,5X,3H,2=,

312,5,5X,3H,3=E12,5,5X,3H,1=E12,5,5X,3H,2=,

434F3=,E12,5,5X,3H,3=E12,5,5X,3H,1=E12,5,5X,

902 CALL TINKEAR(EG(1),THC,TP(1))

TGA(1)=TP(1)

CONTINUE

7 EG(1)=2,0-EG(2)-EG(3)

TP(1)=2,0-TP(2)-TP(3)



```

2 -(PG(I+1)-PG(I)*(I-4)*AB(I)*(I-5)*FMVB/R40)
DF(I,7)=DF(I,7)+F(I,7)*DC(I)*V5(I)
GC TO 13
DER11540
DER11550
DER11560
DER11570
DER11580
DER11590
DER11600
DER11610
DER11620
DER11630
DER11640
DER11650
DER11660
DER11670
VER11680
VER11690
DER11700
DER11710

21 CO,TINUE
DF(I,7)=C,C
13 CO,TINUE
DC 14 I=1,IMAX1
IM1=1-I
IM1=MAX0(IM1,1)
UB=0.5*(UP(I)+UP(I+1))
CALL LOGFI (UB,L)
CALL LOGFI (UB,L)
C(I,7)=A(I)*F(I,V(I)*UP(I+1))
G(I,6)=G(I,7)
UB=0.5*(UG(I)+UG(I+1))
CALL LOGFU (UB,L)
G(I,6)=G(I,6)
CALL LOGFU (UP(I),L)
IL=I+1

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

DER11720
DER11730
DER11740
DER11750
DER11760
DER11770
DER11780
DER11790
DER11800
DER11810
DER11820
DER11830
DER11840
DER11850
DER11860
DER11870
DER11880
DER11890
DER11900
DER11910
DER11920
DER11930
DER11940
DER11950
DER11960
DER11970
DER11980
DER11990
DER12000
DER12010
DER12020
DER12030
DER12040
DER12050
DER12060
DER12070
DER12080
DER12090
CER12100

IL=M1*V1*(1-MP1,IL)
ILM1=IL-1
ILW1=MAX(0,ILM1,1)
G1,3)=A3(1)*JP(1)*FNC(IL)
G1,5)=A5(1)*JP(1)*FMV(IL)
G1,4)=A4(1)*JP(1)*FMV(IL)*CPB*T(IL)
G1,2)=G1,4*
2+4*(1-MP1)*FWV(IL)*(EXP((1-LR)+2*(1-LR)+(PC((1-LR)+2*(1-LR))/RHOP)/FJ
C4761)DOEJ ((1G1,1),LR)
IL=I+1
ILM1=A2*(ILM1,1)
ILW1=A2*(ILW1,1)
ILD=MP1*(1-MP1,IL)
PR=0.0
DO 51 I=NPS,NEC
51. P=SDP+SD(I)
      PZP1/ELCAT(NPE-NPS+1)
      PZP2/DSCP,I
      PC=AMAX1(20.0,P1,P2)
      SR=0.00186*(P1,P2)
      DYQT=-6.0*SR*2.6*CPCL/A/453.59
      EE=YAV/E/CHARG
      CON7=1.0E-05
      DMDT=-MDT*453.59/(A(NPE)*(ZB(NPE)-ZB(NPS-1)))
      DO 18 I=2,1MW
      GO TO 40 (48,44),K6N
      GO T0 (185(EE)-0.01) 203,204,202
      201 DVCT=0.0
      202 IF (ABS(EE)-0.01) 203,204,202
      203 DVDT=DYQT*EE/5.01
      204 CON7=1.0E-05
      205 VVV=VV
      43 VVV=VV
      45 GO T0 45
      46 VVV=VV

```

```

45 CONTINUE
  DF(I,1)=-{G(I,1)-G(I-1,1)}
  IF(I-NPS)17,15,15
15  IF(I-NPE)16,16,17
16  DF(I,1)=DF(I,1)+N4DT*VVV
17  DF(I,2)=-(G(I,2)-G(I-1,2))
18  DF(I,3)=-(G(I,3)-G(I-1,3))
19  DF(I,4)=-(G(I,4)-G(I-1,4))
20  DF(I,5)=-(G(I,5)-G(I-1,5))
21  DF(I,6)=DF(I,6)-{(G(I+1,6)-G(I,6))
22  DF(I,7)=DF(I,7)-(G(I+1,7)-G(I,7))
23  GO TO (37,46),KSW+
24  CONTINUE
25  DU=0,5*(UP(I)-UG(I)+UP(I-1)-UG(I-1))
26  RE=DP(I)*RHOG(I)*ABS(DU)/VISCG
27  REP6=ROOT(IRE,S)
REP6=REP6*REP6*REP6
FNU=2.0+C.34+C.89*REP6

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

H=FN0=0.25*VISCC/(0.7*DP(1))
TG=TGA(1)
TP=TP(1)
QC=(TP-TG)*(DP(1)**2)*3.141593
GO TO (3a,39),KSMX
3a CONTINUE
GK=FN0*VISCC/(PG(1)*DP(1)*0.7)
PV1=PV1-PV2/(TP(1)-273.0+PV3)
PVL=AMIN1(PVL,30.0)
PV=EXP(PVL*2.302585)
C FLAG
C PV=AMIN1(PV,760.0)
PV=14.7*(PV/760.0)*0.058751
DMDDT=3.141593*GK*(DP(1)**2)*(24*0.19*PG(1))
DMDDT=MAX1(DMDDT,0.0)
GO TO 40
40 DMDDT=0.0
CONTINUE
41 DF(1,1)=DF(1,1)+DMDDT*F(1,3)
GE=DMDDT*560.0-(2*MDDT*TP(1)*C9P+QC+C8E)*F(1,3)
DF(1,4)=DF(1,4)-(2*MDDT*TP(1)*C9P+QC+C8E)*F(1,3)
DF(1,5)=DF(1,5)-DMDDT*F(1,3)
GO TO 47
47 DF(1,4)=0.0
48 QC=0.0
GE=0.0
DF(1,4)=0.0
CONTINUE
49 CC\TINUE
50 CCA(1)=QC
QEA(1)=QE
QEA(1)=QEA(1-1)
51 CONTINUE
52 CEA(1)=0.0
CEA(1,MUP1)=QEA(1-1)
DO 22 I=2,1M
DO 22 I=2,1M
53 GO TO (26,27),KSMX
26 DF(1,7)=DF(1,7)-(CEA(1)*FNC(1)*VH(1)+CEA(1+1)*FNC(1+1)*VH(1+1))
DF(1,7)=DF(1,7)/560.0
GO TO 22
27 DF(1,7)=0.0
22 CC\TINUE

```

```
DER12660  
DER12690  
VER12700  
DER12710  
VER12720  
DER12730  
VER12740  
DER12750  
DER12760  
  
DO 21 K=1,7  
21 DF(1,K)=0,0  
    GO TO (19,20),KSM  
19 I=IPRJ  
    DF(I,6)=0,0  
    DF(I,7)=0,0  
    CONTINUE  
20 RETURN  
END
```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE CNTRL (Y,DY,DT,T,NT,RY)
PARAMETER NDC=20C
PARAMETER NRKD=18C0
DIMENSION Y(NRKD),DY(NRKD)
COMMON /ALL/ IX,K,KP,KM,IP1,IPL1,IPL2,KST,KKST,IMW,KSW,KKO,
NFS,NFE,NPE,IPRJ,IP0,XBB,ZMAX,ZR,IR,YH,(NDC),VHR,(NDC),
FL,RHCP,YISCG,VF1IN,BUFFFJ,CHMX,PV1,PV2,PV3,CHARG,PROJ,CHML,
WIDTH,CPP,BL,FORCE,DSCP51,BR,DXJT,A3,CCPCIN,AC,VPROJ,ZPROJ,PB,
FC(NDC,7),CG(NDC),EG(NDC),FN(NDC),TP(NDC),FM(NDC),UG(NDC),
UP(NDC),A(NDC),AB(NDC),V(NDC),V3(NDC),XC(9),RHOG(NDC),
PC(NDC),DP(NDC),GC(NDC),DF(NDC,7),G(NDC,7),Q(NDC),
TG(NDC),QCA(NDC),DEA(NDC),VFA(NDC),FMV(NDC),
COMMON /NRKC/ NRK
COMMON /MC/ NZ4,Z,(7),ZWC(7),IZW(7),PW(7),IEX
IF (ZPROJ+4.0-BL) 1,1,5
1 KSX=1
2 ZP=CHAML+2.54*(ZPROJ+4.0+XC(7))
CALL IGFZ (ZP,IPRJ)
3 NM=IPRJ
NRK=5+7*IPRJ
IF ((IPRJ-19)18,6,2
CONTINUE
4 DDC=ZP-Z3(IPRJ-2)
VR=(ZP-ZB(IPRJ-1))/RC
VRc=V(IP0)/(DD0+A3(IPC))
DC 3 K=1,5
F(IPRJ,K)=VRc*F(IP0,K)
5 F(IP0,K)=V90*F(IP0,K)
UG(IP0)=UC(IP0-1)+(VPROJ*30,40-U5(IP0-1))*(ZB(IP0)-ZB(IP0-1))/2
(ZP-ZB(IP0-1))
6 UF(IP0)=UP(IP0-1)+(VPROJ*30,40-U5(IP0-1))*(ZB(IP0)-ZB(IP0-1))/2
(ZP-Z5(IP0-1))
7 F(IP0,7)=UP(IP0)*F(IP0,5)
F(IP0,6)=F(IP0,7)+UG(IP0)*F(IP0,1)
L=5
DO 4 I=1,1,MN
DO 4 K=1,7
L=L+1
4 Y(L)=F(I,K)

```

CNTR0400  
CNTR0410  
CNTR0420  
CNTR0430  
CNTR0440  
CNTR0450  
CNTR0460  
CNTR0470  
CNTR0480  
CNTR0490  
CNTR0500  
CNTR0510  
CNTR0520  
CNTR0530  
CNTR0540  
CNTR0550  
CNTR0560  
CNTR0570

- 17 C0TINYE (Y,DX,T)
- 18 C0ALD DEERIV (Y,DX,T)
- 19 C0D1PR3  
C0D1PR6
- 20 C0S1W4  
C0S1W6
- 21 F1M2H1  
N2K2H3
- 22 F1M2H1  
I1M2H1
- 23 C0NT1WUE  
I1M2H1-P0
- 24 C0,11,W3  
6 A0=A2+1
- 25 I1F1M2H1-P0  
7 NTRY=2  
GO TO 9
- 26 F1M2H1-P0  
F1M2H1-P0,5  
F1M2H1-P0,7  
JUG(IPO)  
GO TO 13

ONE DIMENSIONAL GAS PARTICLE FLOW

```

6 NY=Y=1
7 WRITE (6,100) KK,T,DT,IMW,ZP,Z (1:N)
8 FORMAT (1H,5X,34KK=,10,5X,2H T=,;PE12,5,5X,3HDT=,E12,5,5X,
9 10 2 4HIMW,10,5X,3HZPS;E12,5,5X,7+Z(IW)=,E12,5,
11 DC 16 I=1,N2X
12 I=1,I1
13 I=1,I2
14 I=1,I3
15 I=1,I4
16 I=1,I5
17 I=1,I6
18 I=1,I7
19 I=1,I8
20 I=1,I9
21 I=1,I10
22 I=1,I11
23 I=1,I12
24 I=1,I13
25 I=1,I14
26 I=1,I15
27 I=1,I16
28 I=1,I17
29 I=1,I18
30 I=1,I19
31 I=1,I20
32 I=1,I21
33 I=1,I22
34 I=1,I23
35 I=1,I24
36 I=1,I25
37 I=1,I26
38 I=1,I27
39 I=1,I28
40 I=1,I29
41 I=1,I30
42 I=1,I31
43 I=1,I32
44 I=1,I33
45 I=1,I34
46 I=1,I35
47 I=1,I36
48 I=1,I37
49 I=1,I38
50 I=1,I39
51 I=1,I40
52 I=1,I41
53 I=1,I42
54 I=1,I43
55 I=1,I44
56 I=1,I45
57 I=1,I46
58 I=1,I47
59 I=1,I48
60 I=1,I49
61 I=1,I50
62 I=1,I51
63 I=1,I52
64 I=1,I53
65 I=1,I54
66 I=1,I55
67 I=1,I56
68 I=1,I57
69 I=1,I58
70 I=1,I59
71 I=1,I60
72 I=1,I61
73 I=1,I62
74 I=1,I63
75 I=1,I64
76 I=1,I65
77 I=1,I66
78 I=1,I67
79 I=1,I68
80 I=1,I69
81 I=1,I70
82 I=1,I71
83 I=1,I72
84 I=1,I73
85 I=1,I74
86 I=1,I75
87 I=1,I76
88 I=1,I77
89 I=1,I78
90 I=1,I79
91 I=1,I80
92 I=1,I81
93 I=1,I82
94 I=1,I83
95 I=1,I84
96 I=1,I85
97 I=1,I86
98 I=1,I87
99 I=1,I88
100 I=1,I89
101 I=1,I90
102 I=1,I91
103 I=1,I92
104 I=1,I93
105 I=1,I94
106 I=1,I95
107 I=1,I96
108 I=1,I97
109 I=1,I98
110 I=1,I99
111 I=1,I100
112 I=1,I101
113 I=1,I102
114 I=1,I103
115 I=1,I104
116 I=1,I105
117 I=1,I106
118 I=1,I107
119 I=1,I108
120 I=1,I109
121 I=1,I110
122 I=1,I111
123 I=1,I112
124 I=1,I113
125 I=1,I114
126 I=1,I115
127 I=1,I116
128 I=1,I117
129 I=1,I118
130 I=1,I119
131 I=1,I120
132 I=1,I121
133 I=1,I122
134 I=1,I123
135 I=1,I124
136 I=1,I125
137 I=1,I126
138 I=1,I127
139 I=1,I128
140 I=1,I129
141 I=1,I130
142 I=1,I131
143 I=1,I132
144 I=1,I133
145 I=1,I134
146 I=1,I135
147 I=1,I136
148 I=1,I137
149 I=1,I138
150 I=1,I139
151 I=1,I140
152 I=1,I141
153 I=1,I142
154 I=1,I143
155 I=1,I144
156 I=1,I145
157 I=1,I146
158 I=1,I147
159 I=1,I148
160 I=1,I149
161 I=1,I150
162 I=1,I151
163 I=1,I152
164 I=1,I153
165 I=1,I154
166 I=1,I155
167 I=1,I156
168 I=1,I157
169 I=1,I158
170 I=1,I159
171 I=1,I160
172 I=1,I161
173 I=1,I162
174 I=1,I163
175 I=1,I164
176 I=1,I165
177 I=1,I166
178 I=1,I167
179 I=1,I168
180 I=1,I169
181 I=1,I170
182 I=1,I171
183 I=1,I172
184 I=1,I173
185 I=1,I174
186 I=1,I175
187 I=1,I176
188 I=1,I177
189 I=1,I178
190 I=1,I179
191 I=1,I180
192 I=1,I181
193 I=1,I182
194 I=1,I183
195 I=1,I184
196 I=1,I185
197 I=1,I186
198 I=1,I187
199 I=1,I188
200 I=1,I189
201 I=1,I190
202 I=1,I191
203 I=1,I192
204 I=1,I193
205 I=1,I194
206 I=1,I195
207 I=1,I196
208 I=1,I197
209 I=1,I198
210 I=1,I199
211 I=1,I200
212 I=1,I201
213 I=1,I202
214 I=1,I203
215 I=1,I204
216 I=1,I205
217 I=1,I206
218 I=1,I207
219 I=1,I208
220 I=1,I209
221 I=1,I210
222 I=1,I211
223 I=1,I212
224 I=1,I213
225 I=1,I214
226 I=1,I215
227 I=1,I216
228 I=1,I217
229 I=1,I218
230 I=1,I219
231 I=1,I220
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557 I=1,I996
558 I=1,I997
559 I=1,I998
560 I=1,I999
561 I=1,I1000
562 I=1,I1001
563 I=1,I1002
564 I=1,I1003
565 I=1,I1004

```

```

104 FORMAT(1H0,7X,1H!,4X,2HEC,12X,3HCA,11X,2HTP,12X,2HFN,12X,2HDP,
105   2HDC,12X,3HSCA,11X,3HGE4 / 1H,18,1PE14,6,7E14,6)
106 WRITE(6,105) (1,FM(1),FMV(1),I=1,IMNP1)
107 CALL PLOTS (1H0,7X,1H!,4X,2HFM,12X,3+FMV / 1H,18,1PE14,6,E14,6)
108 IPL3=MVAL1,N,1PL2)
109 CALL PLOTS (2,PG,30,PG,1,IPL1,IP-3,2D0,1H0,1H*,1HG,1H*,0,0,0,0,
110   20,0)
111 CALL PLOTS (2,FN,SV,PG,1,IPL1,1H*,1HG,1H*,0,0,0,0,0,
112   2,0,0)
113 CALL PLOTS (2,HUP,PG,25,2,1PL1,1E3,200,1HG,1H*,0,0,0,0,0,0,
114   20,0)
115 WRITE (6,126)
116 FORMAT (1H1-1;X,1)
117 CONTINUE
118 END

```

### ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE DRAGC(CE,CORE,FMACH)
DATA N / 1 /
CC7C (1,2),1
RE12=(24.5/14.5)*0.5
RE23=(16.5/14.5)*0.6
N2
CC7C 7
CORE=0.44*CE
IF (CE-2E23)>5.6
5 CORE=18.5*RCOT(RE23*E,5)
IF (FMACH<0.81) 8,9,9
8 CORE=RE
9 RETURN
END

```

### ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE EGSTAT (E,RHO,P)
F1 = 1.6663384E 05+RHO*( 2.3860914E 05+RHO* 1.8121513E 05)
F2 = 8.804000 E 01+RHO*( 2.039948 E 02+RHO*-1.7081190E 01)
F3 =-3.9915C83E -02+RHO*(-6.3478293E -03+RHO*-1.0366801E -01)
P=RHO*(F1+E*(F2+E*F3))
RETURN
END

```

### ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE TOEAR (E,RHO,T)
F1 =3.607725E 3+RHO*(1.041906E 3-2RH0*1.501111E 3)
F2 =1.655822+R.H0*(2.115313-2RH0*1.548174)
F3 =-C :07984E -2+RHO*(-0.686307E -3+RHO*0.422347E -2)
T=F1+E*(F2+E*F3)
RETURN
END

```

### ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE LOFU (U,L)
IF (U) 2,1,1
1 LSC
2 RETURN
2 L21
2 RETURN
END

```

## ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE RK2 (DERIV,CNTRL,Y,DY,A,R,T,DT,N,DTM)
C
C   SECOND ORDER RUNGE KUTTA
C   NTRY IS ASSIGNED ONE OF THE VALUES LISTED BELOW IN CNTRL
C
C   NTRY = 1  CONTINUE INTEGRATION
C   NTRY = 2  RETURN FROM RUNGE KUTTA
C   NTRY = 3  REPEAT STEP WITH NEW DT GIVEN IN CNTRL
C   NTRY = 4  CONTINUE INTEGRATION WITH FIXED STEP
C
PARAMETER NRKD=1800
CIVE,XISION Y(NRKD),DY(NRKD),A(NRKD),R(NRKD),YST(NRKD),
COWN/NRKD/NRK
EXTERNAL DERIV,CNTRL
TWA10=10,*(1.0/3.0)
GA=3.5
BETA=0.5/GAM
ALPHA=1.0-BETA
CALL DERIV (Y,DY,T)
CALL CNTRL(Y,DY,DT,T,NTHY)
TST=T
4  N=NRK
DO 5 I=1,N
YST(I)=Y(I)
5  DYST(I)=DY(I)
6  IF (DT) 8,7,8
7  WRITE (6,121)
121  FORMAT (1H0,20X,17HSTEP SIZE = ZERO, )
8  T=TST+GAM*DT
9  QC 9 131,N
9  Y(I)=YST(I)+GAM*DT*DYST(I)
CALL DERIV (Y,DY,T)
T=TST+DT
DO 10 I=1,N
10  Y(I)=YST(I)+DT*(ALPHA*DYST(I)+BETA*DY(I))
CALL DERIV (Y,DY,T)
EOCM=J,0
DC 13 131,N
E=Y(I)-(YST(I)+0.5*DT*(DYST(I)+DY(I)))
CZ(I)+R(I)*A3S(Y(I))
IF (C) 12,11,12

```

```

11 WRITE (6,132)
12 FORMAT (1H0, 20X, 27HA(1)+R(1)*ABS(Y(1))=0 AT 12 , 16)
13 RETURN
14 EOC=ABS(E/C)
C   EOCY=4*14X1(EOC,EOCY)
15 IF (EOC-EOCY) 13,13,201
201 EOCY=EOC
LS21
16 CONTINUE
17 IS=(LS+1)/7
KS=LS-5-7*(IS-1)
IF (EOC4-L,0; 17,17,14
18 CONTINUE
19 WRITE (6,321) EOC,LS,KS,IS
321 FORMAT (1H ,10X,S-EOCY,1PE12.5,5X,34LS,16,5X,34KS,16,5X,
2 3=IS,16)
C   CALL DUMPE
T=TST

```

RK2 0400  
RK2 0410  
RK2 0420  
RK2 0430  
RK2 0440  
RK2 0450  
RK2 0460  
RK2 0470  
RK2 0480  
RK2 0490  
RK2 0500  
RK2 0510  
RK2 0520  
RK2 0530  
RK2 0540  
RK2 0550  
RK2 0560  
RK2 0570

ONE DIMENSIONAL GAS PARTICLE FLOW

```

DO 15 I=1,N
Y(I)=YST(I)
15 DY(I)=YST(I)
ECCM=EOCM/10.3
DT=DT/THR10
IF (EOCM-1.0) 6,6,16
16 CONTINUE
GO TO 6
17 CALL CNTRL(Y,DY,DT,T,NTRY)
GO TO (21,18,19,4),NTRY
18 RETURN
19 T=TST
20 DC 20 I=1,N
Y(I)=YST(I)
21 DY(I)=YST(I)
22 DT=DT/THR10
WRITE (6,301) EOCH,LS,KS,IS
GO TO 6
23 IF (EOCM-C,3) 23,23,22
24 DT=DT/THR10
IF(ABS(DT)-ABS(DTM)) 4,4,24
DT=ABS(DTM)*DT/ARS(DT)
GO TO 4
25 IF (ECCM-C,3) 25,4,4
RK2 0560
RK2 0590
RK2 0600
RK2 0610
RK2 0620
RK2 0630
RK2 0640
RK2 0650
RK2 0660
RK2 0670
RK2 0680
RK2 0690
RK2 0700
RK2 0710
RK2 0720
RK2 0730
RK2 0740
RK2 0750
RK2 0760
RK2 0770
RK2 0780
RK2 0790
RK2 0800
RK2 0810
RK2 0820
RK2 0830
RK2 0840
END

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE CALX(CNA1, CNA2, RN, DT, DEXC, BL, O, VCHAMB, ENL, XC, XBB)
DIMENSION XC(9)
XC(1)=1.0E+37
XC(3)=-ENL
XC(4)=3.0
TC(4)=STA*(3.141593*SIN(ANG/180.0))
SC(4)=TCNA1/SCRT(1.0+C+TCNA1*O*2)
CCNA1=SCOS(3.141593*CNA1/180.0)
IF (ENL-1.0E-10) 16,16,17
16 ANG=CNA1
      GC TO 18
17 ANG=3.0
      SANG=SIN(3.141593*ANG/180.0)
18 RC=2.0
      RCC=RCC*(SCRT(2.0)-1.0)/(SCRT(2.0)-SANG-SCRT(1.0-SANG*0.2))
      XC(2)=-(ENL+RCC)*(SCRT(1.0-SANG*0.2)-1.0/SCRT(2.0))
      RXC2=5.0*DEXC+RCC*(SCRT(1.0-SANG*0.2)-1.0/SCRT(2.0))
      O1=0.25,4
      XC15=5.0*(DEXC-DTH)/TCNA1
      XC(6)=XC(5)+12.0
      XBB=0.5*(XC(6)+5.0*CI-BTH)/TCNA1
      CHL=4.0*VCHANB/(3.141593*O1*O1)
      XC(8)=XC(7)+CHL+EL
      XC(9)=1.0E37
      XC(1)=XC(1)
      X2=XC(2)
      X2=1
      X2=0.0
      RETURN
ENTRY RADIUS(XCN,2)
X=XCN/2.54
IF (X-X2) 4,3,3
3 IF (X-X2) 7,7,4
4 DO 5 I=1,9
      J=1
      IF (XC(I)-X) 5,5,6
      5 CO,TINUE
      6 K=j-1

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

CC TO 15
R=2.501+SQRT ((X-XC(8))**2+A*A)-1
CONTINUE
R=2.054
RETURN
END

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE ZSPACE
PARAMETER NCC=203
DIMENSION ZS(202)
COMMON /ALL/ IM,KP,KM,IL1,IPL2,KST,KKST,IMW,KW,KKO,
2 NFS,NPE,NPS,NPE,IP0,X3B,ZMAX,Z3,IR,VHL(NDC),VHR(NDC),
3 FL,RHOP,VISCG,VFM1N,PDF,FJ,CMAX,PV1,PV2,PV3,CHARG,PROJW,CHAML,
4 W!DTK,CPP,BL,FORCE,OSCPSI,GR,CYCT,A,CCPCIN,AC,VPROJ,ZPROJ,PB,
5 F(INCC,7),CG(NDC),EC(NDC),EN(NDC),TPI(NDC),FM(NDC),UG(NDC),
6 UF(NDC),A(NDC),AB(NDC),V(NDC),V3(NDC),XC(9),RHOG(NDC),
7 PC(NDC),DP(NDC),DG(NDC),DF(NDC),G(NDC,7),G(NDC,7),Q(NDC),
8 TGAC(NDC),GCA(NDC),GEA(NDC),VFA(NDC),FMV(NDC),
9 IM3=IM+1,Z4XC=ZMAX*2.54,ZRC=ZR*2.54
CALL UNESR ((143), 14C,IR,ZRC,ZS)
J=143
DO 8 L=1,1000
J=J-1
1 IF ((J) 2,1,2
1 J=-2
2 JA=1ABS(J)
2 ZST=ZS(JA)
1 IF ((J) 4,5,3
3 ZL=X39*2.54-ZST
GC T3 5
4 ZL=X39*2.54+ZST
5 IF (((L/2)*2-L) 6,7,6
6 I=I+1
6 ZL=ZL
GO TO 8
7 ZL=ZL
IF ((1-IM) 8,10,12
CONTINUE
CONTINUE
R2C=0.0
DO 9 I=1,IM
CALL RADIUS ((Z((1),R))
CALL RADIUS ((ZB((1),R2))
ZSPACC10
ZSPACC20
ZSPACC30
ZSPACC40
ZSPA050
ZSPA060
ZSPA070
ZSPA080
ZSPA090
ZSPA100
ZSPA110
ZSPA120
ZSPA130
ZSPA140
ZSPA150
ZSPA160
ZSPA170
ZSPA180
ZSPA190
ZSPA200
ZSPA210
ZSPA220
ZSPA230
ZSPA240
ZSPA250
ZSPA260
ZSPA270
ZSPA280
ZSPA290
ZSPA300
ZSPA310
ZSPA320
ZSPA330
ZSPA340
ZSPA350
ZSPA360
ZSPA370
ZSPA380
ZSPA390

```

```

A(1)=3.141593*R*2
AB(1)=3.141593*R2*92
I41=M4XG(1)-1
V4R(1)=3.141593*(2*(1)-2*(1)*(32*R2+32*R*R)/3.0
Y4L(1)=3.141593*(2*(1)-2*(1)*(32*R2+32*R*R20)/3.0
K22=R2
* CONTINUE
V4L(1)=V4R(1)
V4R(1)=V4L(1)
DO 11 I=1,1
V(1)=V4L(1)+V4R(1)
11 V(1)=V4R(1)+V4L(1)
      RETURN
      END
      ZSPA0400
      ZSPA0410
      ZSPA0420
      ZSPA0430
      ZSPA0440
      ZSPA0450
      ZSPA0460
      ZSPA0470
      ZSPA0480
      ZSPA0490
      ZSPA0500
      ZSPA0510
      ZSPA0520
      ZSPA0530
      ZSPA0540

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE IOFZ(ZZ,II)
PARAMETER NDC=200
COMMON /ALL/ IN,K,XP,KM,IPL1,IPL2,KST,IMW,KSD,KXD,
2 NFS,NPE,NPS,NEP,IPRJ,IP0,XSS,ZMAX,ZR,IR,YHL(NDC),VHR(NDC),
3 FL,ZNCP,VISCG,VF11Y,PDF,FJ,CMAX,PV1,PV2,PV3,CHARG,PROJX,CHAML,
4 WIDTH,CPP,BL,FORCE,DSCHPSI,SR,CYDT,A3,CCPCIN,AC,VPROJ,ZPROJ,PB,
5 FNDC,71,CG(NDC),EG(NDC),FN(NDC),TP(NDC),UG(NDC),
6 UG(NDC),AB(NDC),V(NDC),V3(NDC),XC(9),RHOG(NDC),PG(NDC),
7 PR(NDC),DP(NDC),DG(NDC),DF(NDC),G(NDC),Z(NDC),ZS(NDC),
8 TGA(NDC),GC(NDC),GEA(NDC),VFA(NDC),VFMV(NDC),
DATA LLL / 1 /
GO TO (1,2),LLL
1 Z1=Z(1)
2 Z2=Z(2)
10=1
10
LLL=2
2 IF (ZZ-Z1) 5,3,3
3 IF (ZZ-Z2) 4,6,6
4 I=10
5 RETURN
5 IS=1
6 GO TO 7
6 IS=10
7 DC 8 I=IS,14
8 J=1
1 IF (ZZ-Z1) 10,9,3
9 CD,TINUE
9 II=J
10 GO TO 11
10 II=J-1
11 GO TO 11
11 II=1
12 Z2=Z(I+1)
12 Z2=Z(I+1)
RETURN
END

```

	END RETURN	
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ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE UNEQR(14,RM,IR,RR,Q)
DIMENSION R(12,2)
FIR=FLOAT(IR)
F14=FLOAT(IN)
B=1,C
DC 1 K=1,5
EX=EXP(-3*(F14+F14-2,C))+((1.0-EX)*(-2.0*B*(FIR-1.0)))*RM/RR
B=ALOG(EX)/(F14-F14)
WRITE (6,101) K,3,14,IR,RY,35
101 FORMAT (1-3,X,2H4<,15,3X,2H5<,19E14.6,3X,3HIM<,15,3X,
2,3,IR=15,3X,34RM=,E14.6,3X,3H32=,E14.6),
1 CCONTINUE
1 DC 2 K=6,25
F1=QM*31YNH(E*(F12-1.0))
F2=RR*31YNH(B*(F14-1.0))
DC=F1-F2
C1=RM*(F12-1.0)*C3SH(B*(F13-1.0))-RR*(F1M-1.0)*COSH(B*(F1M-1.0))
C2=F1*(F14-1.0)**2-F2*(F1M-1.0)**2
DB=5*GL(CLOG(1.0C-CALE(DC))*DBL(D2)/DBL(D1)**2)*DBL(D1)/
2 DBL(D2)
B=B+DB
WRITE (6,152) K,32,3
152 FORMAT (14G.3X,2H4<,15,3X,3HIM<,1PE14.6,3X,2H8<,E14.6)
IF (ABS(DB)-1.CE-7)>3.2
2 CCONTINUE
3 A=RR/SINH(3*(FIR-1,C))
DC 4 I=1,14
4 R(I)=A*SINH(B*FLOAT(I-1))
4 RETURN
END

```

ONE FINE VISUAL GAS PARTICLE FLOW

SUBROUTINE PLOTS (X,Y1,Y2,Y3,N1,N2,N3,XMIN,XMAX,  
 XMIN,YMAX)  
 PURPOSE - TO PLOT A GRAPH WITH ONE INDEPENDENT VARIABLE AND UP  
 TO 9 DEPENDENT VARIABLES. THE INDEPENDENT VARIABLE PLOTTED ON A  
 HORIZONTAL AXIS, THE DEPENDENT ONES ON A VERTICAL AXIS, WHICH  
 IS 102 PRINT POSITIONS, HEIGHT IS 50.  
 PARAMETER USAGE.  
 NUMBER OF OBSERVATIONS  
 NUMBER OF VARIABLES (INDEPENDENT + DEPENDENT)  
 XMAX,XMIN,YMAX,YMIN, MAXIMUM AND MINIMUM VALUES OF THE ! INDEPENDENT  
 AND DEPENDENT VARIABLES TO BE USED IN THE PLOT.  
 IF XMAX = XMIN, THE PROGRAM CALCULATES ITS OWN MAXIMUM AND MINIMUM  
 FOR THE INDEPENDENT VARIABLE, SIMILARLY FOR YMAX = YMIN  
 KPS PLOTTING SYMBOL FOR LTH VARIABLE. AAC(I,L) SYMBOL FOR LTH VARIABLE,  
 REQUIRED SUBROUTINES SCAL  
 DIMENSION OF A MUST BE THE PRODUCT OF THE DIMENSIONS OF AA,  
 DIMENSION X(N1),Y1(N2),Y2(N3),Y3(N4),A(800),KPS(4)  
 DATA K3/H2/  
 N1=12-11+1  
 N2=4+1  
 KPS(1)=KD  
 KPS(2)=KL  
 KPS(3)=SK2  
 KPS(4)=SK3  
 DC=1,1=1,  
 J=1+11-1  
 L2=1+  
 L3=1+2+N  
 L4=1+3+N  
 A(I)=X(J)  
 A(L2)=Y1(J)  
 A(L3)=Y2(J)  
 A(L4)=Y3(J)  
 XLAX=XMAX  
 XLIN=XMIN  
 YLAX=YMAX  
 YLIN=YMIN  
 EXTERNAL BLANK  
 FUNC(3)

A-38

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```
CALL PLOT (C,A,N,V,YFUNC,XLAX,XLIN,YLAX,YLIN,KPS)
RETURN
END
```

```
PLOT0400
PLOT0410
PLOT0420
```

### ONE DIMENSIONAL GAS PARTICLE FLOW

```
SUBROUTINE BLANK (X,Y)
Y=5.0
RETURN
END
```

```
BLANO0010
BLANO0020
BLANO0030
BLANO0040
```

## ONE DIMENSIONAL GAS PARTICLE FLOW

SUBROUTINE PLOT (TC, N, NFLG, FUNC, XLAX, XLIN, YLIN, KFS)  
 PURPOSE - TO PLOT A GRAPH WITH ONE INDEPENDENT VARIABLE AND UP  
 TO 9 DEPENDENT VARIABLES, WITH THE ADDITIONAL ABILITY TO PLOT A  
 CALCULATED CURVE. THE INDEPENDENT VARIABLE IS PLOTTED ON A  
 HORIZONTAL AXIS, THE DEPENDENT VALUES ON A VERTICAL AXIS. WIDTH  
 IS 120 POINT POSITIONS, HEIGHT IS 50, EVERY POINT OF EACH  
 DEPENDENT VARIABLE IS INDICATED BY A NUMBER (1-9). WHILE THE  
 CALCULATED POINTS ARE INDICATED BY ASTERISKS.  
 PARAMETER USAGE:  
 TC = FIXED POINT NUMBER, UP TO 3 DIGITS, PRINTED AS THE  
 CHART NUMBER  
 N = NUMBER OF POSITION CONTAIN THE INDEPENDENT  
 VARIABLE, AND WHOSE NEXT N SETS OF N POSITIONS CONTAIN  
 THE DEPENDENT VARIABLES  
 NFLG = NUMBER OF OBSERVATIONS  
 FUNC = NUMBER OF VARIABLES (INDEPENDENT + DEPENDENT)  
 XLAX = X IS GIVEN TO SUBROUTINE MAXIMUM AND MINIMUM VALUES OF THE  
 CALCULATED FUNCTION GOES.

PRINTED  
 A VECTOR WHOSE FIRST N POSITIONS CONTAIN THE INDEPENDENT  
 VARIABLE, AND WHOSE NEXT N SETS OF N POSITIONS CONTAIN  
 THE DEPENDENT VARIABLES  
 WHERE X IS GIVEN TO SUBROUTINE MAXIMUM AND MINIMUM VALUES OF THE  
 CALCULATED FUNCTION GOES.  
 CALCULATED POINTS ARE INDICATED BY ASTERISKS.

FUNCTION GENERATOR THAN ZERO IF A CALCULATED CURVE IS TO BE  
 PRINTED

PRINTED  
 A VECTOR WHOSE FIRST N POSITIONS CONTAIN THE INDEPENDENT  
 VARIABLE, AND WHOSE NEXT N SETS OF N POSITIONS CONTAIN  
 THE DEPENDENT VARIABLES  
 WHERE X IS GIVEN TO SUBROUTINE MAXIMUM AND MINIMUM VALUES OF THE  
 CALCULATED FUNCTION GOES.  
 WHERE X IS GIVEN TO SUBROUTINE MAXIMUM AND MINIMUM VALUES OF THE  
 CALCULATED FUNCTION GOES.

REQUERED SUBROUTINES, FUNC (IF USED), AND SCAL.  
 KFS(1) = PLOTTING SWAG FOR DATA IN FIRST ARRAY,  
 KFS(2) = PLOTTING SWAG FOR DATA IN SECOND ARRAY,  
 CALC IS 1 LASER THAT MAX X AND MIN X AND MAX Y AND MIN Y FOR THE INDEPENDENT VARIABLE,  
 CALC IS 2 PLACEMENT AND DEPENDENT VALUES TO BE USED IN THE  
 INDEPENDENT AND DEPENDENT VALUES TO BE USED IN THE  
 CALC IS WHERE CALCULATED FUNCTION GOES.  
 DATA K/1/H  
 EQUIVALENT (OUT11, AP11))

```
113 FORMAT(1D-16.0DN,74 CHART 13)
114 FORMAT(1D-12X+2-, 1D16.1H-)
```

PLOT0010  
 PLOT0020  
 PLOT0030  
 PLOT0040  
 PLOT0050  
 PLOT0060  
 PLOT0070  
 PLOT0080  
 PLOT0090  
 PLOT0100  
 PLOT0110  
 PLOT0120  
 PLOT0130  
 PLOT0140  
 PLOT0150  
 PLOT0160  
 PLOT0170  
 PLOT0180  
 PLOT0190  
 PLOT0200  
 PLOT0210  
 PLOT0220  
 PLOT0230  
 PLOT0240  
 PLOT0250  
 PLOT0260  
 PLOT0270  
 PLOT0280  
 PLOT0290  
 PLOT0300  
 PLOT0310  
 PLOT0320  
 PLOT0330  
 PLOT0340  
 PLOT0350  
 PLOT0360  
 PLOT0370  
 PLOT0380  
 PLOT0390

```

2 FORMAT(1X,1PE12.3,2H+,1D1A.1H+,E12.3)
2 FIND EXTREES OF X GIVEN, FIND THEM
3 PRINT CHART N
3 WRITE(6,1) N
4 READ(LINE,5,*,END=10)
5 IF (LINE.EQ.'') GO TO 10
6 READ(LINE,7,*,END=10)
7 IF (LINE.EQ.'') GO TO 10
8 FCBMTR(LINE,5,1PE12.3,1D1A.1H+,E12.3)
9 CALL CFCB(LINE,5,1PE12.3,1D1A.1H+,E12.3)
10 IF (XMAX.EQ.XMIN) GO TO 15
11 XMAX = A(1)
12 IF ((A(1))-XMAX).LT.0.0001 GO TO 15
13 J = 1
14 DO 15 I=1,N-1
15 XMAX = MAX(XMAX,XMIN)
16 XMIN = MIN(XMAX,XMIN)
17 IF (XMAX-XMIN).GT.0.0001 GO TO 18
18 IF (XMAX-XMIN).LT.0.0001 GO TO 19
19 IF ((A(J))-XMAX).LT.0.0001 GO TO 20
20 IF ((A(J))-XMAX).GT.0.0001 GO TO 21
21 IF ((A(J))-XMAX).LT.0.0001 GO TO 22
22 IF ((A(J))-XMAX).GT.0.0001 GO TO 23
23 IF ((A(J))-XMAX).LT.0.0001 GO TO 24
24 IF ((A(J))-XMAX).GT.0.0001 GO TO 25
25 IF ((A(J))-XMAX).LT.0.0001 GO TO 26
26 IF ((A(J))-XMAX).GT.0.0001 GO TO 27
27 IF ((A(J))-XMAX).LT.0.0001 GO TO 28
28 IF ((A(J))-XMAX).GT.0.0001 GO TO 29
29 IF ((A(J))-XMAX).LT.0.0001 GO TO 30
30 IF ((A(J))-XMAX).GT.0.0001 GO TO 31
31 IF ((A(J))-XMAX).LT.0.0001 GO TO 32
32 IF ((A(J))-XMAX).GT.0.0001 GO TO 33
33 IF ((A(J))-XMAX).LT.0.0001 GO TO 34
34 IF ((A(J))-XMAX).GT.0.0001 GO TO 35
35 IF ((A(J))-XMAX).LT.0.0001 GO TO 36
36 IF ((A(J))-XMAX).GT.0.0001 GO TO 37
37 IF ((A(J))-XMAX).LT.0.0001 GO TO 38
38 IF ((A(J))-XMAX).GT.0.0001 GO TO 39
39 IF ((A(J))-XMAX).LT.0.0001 GO TO 40
40 IF ((A(J))-XMAX).GT.0.0001 GO TO 41
41 IF ((A(J))-XMAX).LT.0.0001 GO TO 42
42 IF ((A(J))-XMAX).GT.0.0001 GO TO 43
43 IF ((A(J))-XMAX).LT.0.0001 GO TO 44
44 IF ((A(J))-XMAX).GT.0.0001 GO TO 45
45 IF ((A(J))-XMAX).LT.0.0001 GO TO 46
46 IF ((A(J))-XMAX).GT.0.0001 GO TO 47
47 IF ((A(J))-XMAX).LT.0.0001 GO TO 48
48 IF ((A(J))-XMAX).GT.0.0001 GO TO 49
49 IF ((A(J))-XMAX).LT.0.0001 GO TO 50
50 IF ((A(J))-XMAX).GT.0.0001 GO TO 51
51 IF ((A(J))-XMAX).LT.0.0001 GO TO 52
52 IF ((A(J))-XMAX).GT.0.0001 GO TO 53
53 IF ((A(J))-XMAX).LT.0.0001 GO TO 54
54 IF ((A(J))-XMAX).GT.0.0001 GO TO 55
55 IF ((A(J))-XMAX).LT.0.0001 GO TO 56
56 IF ((A(J))-XMAX).GT.0.0001 GO TO 57
57 IF ((A(J))-XMAX).LT.0.0001 GO TO 58
58 IF ((A(J))-XMAX).GT.0.0001 GO TO 59
59 IF ((A(J))-XMAX).LT.0.0001 GO TO 60
60 IF ((A(J))-XMAX).GT.0.0001 GO TO 61
61 IF ((A(J))-XMAX).LT.0.0001 GO TO 62
62 IF ((A(J))-XMAX).GT.0.0001 GO TO 63
63 IF ((A(J))-XMAX).LT.0.0001 GO TO 64
64 IF ((A(J))-XMAX).GT.0.0001 GO TO 65
65 CGT;NUE

```

ONE-DIMENSIONAL GAS PARTICLE FLOW

```

: IF CALCULATED CURVE WANTED GET VALUES BETWEEN XMIN AND XMAX
: IF (NEURC) 213.0215.0211
211 F = XMIN
212 JZ = 1
213 CALL, EFUNC(F,C-LC(JP))
214 IF (JZ = 794) 212,212,213
215 F = F + 5E-04
216 GO TO 213
217 CONTINUE
218 SPINT POINT AT MAXIMUM Y
219 YPR = YMAX
220 CLEAR PRINT LINE
221 GO 55 JP = 1.01
222 IF (YPR < 0) 223
223 IF (SPINT CURVE WANTED) SET UP POINTS
224 IF (NEURC) 214.02.4.0.215
225 F = XMAX
226 PLOT970
PLOT980
PLOT990
PLOT1000
PLOT1010
PLOT1020
PLOT1030
PLOT1040
PLOT1050
PLOT1060
PLOT1070
PLOT1080
PLOT1090
PLOT1100
PLOT1110
PLOT1120
PLOT1130
PLOT1140

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

C SCAN ALL VALUES OF Y FOR X BETWEEN XMIN AND XMAX
C
C JP = POINT WITHIN HALF A SCALE OF PRINT POSITION
C 223 IF (ASSLYPRA-LALC(JP)) - .5 * YSCAL) 216,217,218
C IF EXACTLY BETWEEN PRINT POSITIONS ONLY PRINT IT ONCE
C 217 IF (YFR - CALC (JP)) 218,219,216
C BELIEVE IT OR NOT THIS IS AN ASTERISK (NUMBER TOO LARGE TO WRITE
C AS ONE NUMBER)
C 215 IOUT(JP) =EXP5(1)
C 214 IF (F - XMAX) 219,214,214
C 215 JP = JP + 1
C F = F + XSCAL
C GO TO 220
C END. COIN EACH SET OF DEPENDENT VARIABLES
C
C 214 IF (N) 70,70,300
C 353 G0 222; J = 214
C 222 L = 1;
C CALCULATE SUBSCRIPT FOR A
C LL = (J - 1) * N + L
C IS IT WITHIN HALF A SCALE OF PRINT POSITION
C 223 IF (ASSLYPRA - A(LL)) - .5 * YSCAL) 223,224,225
C IF EXACTLY HALF WAY BETWEEN, PRINT ONLY ONCE
C 324 IF (V22 - V11) 225,223,223
C 223 FJF = (V11 - V22) / XSCAL + 1.5
C
C IF OFF Graph, FORSET IT
C 226 IF (JP - 1) 225,226,226
C THIS GIVES 1,2,3 ETC. FOR J=2,3,4 ETC
C 227 IOUT(JP) =EXP5(J);
C
C 225 CONTINUE
C 222 CONTINUE
C 221 CONTINUE
C 220 COUNT = COUNT +1
C PRINT VALUE ON VERTICAL AXIS EVERY FIVE POSITIONS
C IF (COUNT - 5) 120,119,120
C 121 WRITE (6,112) (IOUT(JP), JP=1,101)

```

### ONE DIMENSIONAL GAS PARTICLE FLOW

```

GO TO 80
C MAKE ZERO PRINT AS ZERO, NOT SMALL NUMBER
119 IF (ABS(XA(1))-5 * XSCAL) 232,232,233
120 XA(1)=0.0
PLOT1540 PLOT1550 PLOT1560 PLOT1570 PLOT1580 PLOT1590 PLOT1600 PLOT1610 PLOT1620 PLOT1630 PLOT1640 PLOT1650 PLOT1660 PLOT1670 PLOT1680 PLOT1690 PLOT1700 PLOT1710 PLOT1720 PLOT1730 PLOT1740 PLOT1750 PLOT1760 PLOT1770
PLOT1540 PLOT1550 PLOT1560 PLOT1570 PLOT1580 PLOT1590 PLOT1600 PLOT1610 PLOT1620 PLOT1630 PLOT1640 PLOT1650 PLOT1660 PLOT1670 PLOT1680 PLOT1690 PLOT1700 PLOT1710 PLOT1720 PLOT1730 PLOT1740 PLOT1750 PLOT1760 PLOT1770
END
232 F=0.
233 F=YD2
234 Y=ITEN(6,2) F, (ICOUNT(JP),JPS2,I01),F
C ICOUNT = C
C ELSE DECREMENT Y
C IF REACHED YMIN, STOP
C 63 IF (YPR - YM1) <=6.86,86,45
C PRINT BOTTOM SCALE
C XPR(JP+1)=XPR(JP)+XSCAL*10.
C XPR(1)=XMIN
C 90 XPR(JP+1)=0.
C 91 XPR(JP+1)=0.
C 92 CON1,1,E
235 WRITE(6,7)
C 93 IF (XPR(JP+1) = 0.
C 94 RETURN
IF (X55(XHAR(JP+1)) = -5*XSCAL) 231,231,90
236 CON1,1,E
WRITE(6,8) (XPR(JP),JPS2,I01)
RETURN
END

```

ONE-DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE SCAL (XSCAL,XMAX,XMIN)
PURPOSE. GIVEN XIA SCALE AND END POINTS, GET ROUNDED VALUES,
F=LOG10(XSCAL*1.00001)
IF (F) 1,2,2
1 IF NEGATIVE, STOP FORTRAN FROM ROUNDING UP
2 IF JP=-INT(-(F-1.0))
   GO TO 25
3 FIND VALUE JUST LARGER THAN 1.E4 YSCA-, OF FORM 1,2,2,5,2,OR 10
4 TIMES 10 TO AN INTEGRAL POWER -
27 F=10.*JP
4 IF (F-XSCAL) 3,4,4
3 F=F+F
4 IF (F-XSCAL) 5,4,4
5 F=1.25*F
6 IF (F-XSCAL) 7,4,4
7 F=F+F
8 IF (F-XSCAL) 30,4,4
37 F=F+F
25 GO TO 6
C   SET EQUAL TO SCALE
4 XSCALE=F
4 IF (ABS(XMAX/XSCAL)-1.0E9) 8,11,11
8 IF (XMIN/XSCAL) 14,15,15
C   14 IF END POINTS INTEGRAL MULTIPLES OF SCALE
17 F=XSCALE*FLCAT(JP)
18 IF (F-XMAX) 10,11,11
19 JP=JP+1
20 GO TO 12
C   11 IF (435(XMIN/XSCAL)-1.0E9) 9,14,14
21 JP=INT(XMIN/XSCAL)
22 F=XSCALE*FLCAT(JP)
23 IF (F-XMAX) 14,15,15
24 RETURN
END

```

ONE-DIMENSIONAL GAS PARTICLE FLOW

GO TO 15  
10 X2=X\*X  
10 X4=X2\*X2  
X8=X4\*X4  
XP=X3\*X2  
15 GO TO (16,17),KS  
16 PCW=1.0/XP  
16 RETURN,  
17 POW=XP  
17 RETURN,  
END

POW 0400  
POW 0410  
POW 0420  
POW 0430  
POW 0440  
POW 0450  
POW 0460  
POW 0470  
POW 0480  
POW 0490  
POW 0500

ONE DIMENSIONAL GAS PARTICLE FLOW

```

FUNCTION ROOT (X,<)
ROOT=KTH ROOT CF X
K MUST SATISFY GE..0 . AN
CFATL / 1 , F / 0..9 /
DIVISION A(1),C(12,12)
C(1,1)=1,0
C(1,2)=1,5*** (12,0,7/12)
A(1,2)=FLCAT(1)
FX=FLCAT(1)
FC(J+1,M)=2.0**((FJ/F))
FC(J,M)=2.0**((FJ/F))
CONTINUE
IF (X) 6,7,0
6 ROOT=0.0
7 RETURN
8 IF (X-1) 11,11,12
9 RETURN
10 IF (X) 13,13,12
11 RETURN
12 WRITE(KH,N=1-129)
N=(J+100*X)/K+100
Y=S*(X-K)+S=J+128
FL(C,9,S)=J+128
NR=N-KH
END

```

```

15 ROOT=0,0
15 RETYR;
14 Y5=Y
14 DC 33 LB=1,13
6C T3 {21,22,23,24,25,26,27,28,29,30},<
24 P=X
6C TC 31
22 F=(Y+X)/(2.0*Y)
6C TC 31
23 Y2=Y*Y
23 P=(2.0*Y2+Y)/(3.0*Y2)
6C TC 31
24 Y2=Y*Y
24 Y4=Y2*Y2
F=(3.0*Y4+X)/(4.0*Y2*Y)
6C TC 31
25 Y2=Y*Y
25 Y4=Y2*Y2

```

C)

# ONE DIMENSIONAL GAS PARTICLE FLOW

```

P=(4.0*Y4+X)/(5.0*Y4)
GO TO 31
26 Y2=Y*Y
    Y4=Y2*Y2
    P=(5.0*Y4+Y2+X)/(6.0*Y4+Y)
    GO TO 31
27 Y2=Y*Y
    Y4=Y2*Y2
    Y6=Y4*Y2
    P=(6.0*Y6+Y+X)/(7.0*Y6+X)
    GO TO 31
28 Y2=Y*Y
    Y4=Y2*Y2
    P=(7.0*Y4+Y4+X)/(5.0*Y4+Y2+Y)
    GO TO 31
29 Y2=Y*Y
    Y4=Y2*Y2
    Y8=Y4*Y4
    P=(8.0*Y6+Y+X)/(9.0*Y6+X)
    GO TO 31
30 Y2=Y*Y
    Y4=Y2*Y2
    Y8=Y4*Y4
    P=(9.0*Y8+Y2+X)/(10.0*Y8+Y)
    IF (ABS(1.0-Y/P)-1.0E-5)34,34,32
32 Y=P
33 CC:TIME
34 FACT=P
      RETURN
END

```

**APPENDIX B**  
**TWO-DIMENSIONAL GAS PARTICLE FLOW**

TWO DIMENSIONAL GIS PARTICLE FLOW

```
READ (11) K1, T1(LL), PINC(LL), CIND(LL), WINDG(LL), WINDP(LL);
MAIN0100
2 FMV(LL)
1F (K1-G412) 37,38,38
37 CONTINUE
38 CONTINUE
39 CONTINUE
REWIND 14
DO 39 LLL=2,LS
  WINDG(LL)=WINDS(LL)
  WINDP(LL)=WINDS(LL)
  NIND(LL)=PINCP(LL)
  T1(1)=0.
  PINC(LL)=0.
  CIND(LL)=0.
  WINDG(1)=0.
  WINDP(1)=0.
  NIND(1)=0.
  READ (5,1020) N1,N2,(N11,N21,A1),(J1,J2,J3,J4)
1020 FORMAT (115/8110,11/8110)
```

TWO-DIMENSIONAL GAS PARTICLE FLOW



THE THREE-DIMENSIONAL GAS PARTICLE FLUX

```

/MAIN1150
/MAIN1160
/MAIN1170
/MAIN1180
/MAIN1190
/MAIN1200
/MAIN1220
/MAIN1230
/MAIN1240
/MAIN1250
/MAIN1260
/MAIN1270
/MAIN1280
/NMAIN1290
/HAIN1300
/HAIN1310
/HAIN1320
/HAIN1330
/HAIN1340
/HAIN1350
/HAIN1360
/HAIN1370
/HAIN1380
/HAIN1390
/HAIN1400
/HAIN1410
/HAIN1420
/HAIN1430
/HAIN1440
/HAIN1450
/HAIN1460
/HAIN1470
/HAIN1480
/HAIN1490
/HAIN1500
/HAIN1510
/HAIN1520
/HAIN1530

620X30H PARTICLE DIAMETER,DIAP   ,E10.4;2X12H(CM)
720X30H MAX ALLOWABLE YFL,YFLMAX  ,E10.4;
820X30H PARTICLE PRESSURE FACTOR,PAV  ,E10.4;2X12H(DY/SQ-CM)
920X30H ARTIFICIAL VISC. FACTOR,FL  ,E10.4;
A 20X.30H EER LIMIT, ER      ,E10.4; //1X)

        WRITE(6,2306)
2306 FORMAT(1H,3X10-4, TYPE,M,4X)B,RELATIVE ERROR FACTOR,REF(M),10X2MAIN1200
1AHABSOLUTE ERROR FACTOR,AEF(M)/3X)
00 2303 4217
000A WRITE(6,2313) M,REF(M),AEF(M)
2010 FORMAT(1B,F22.2,E43.2)
2010 WRITE(6,2313)(1.0W(1),JW(1),I,10X,1W(1))
2030 FORMAT(1H,19X,1W,8X,2H1W,16X,2HJW,1W(1),10X,3120)
2030 WRITE(6,2312)
2012 FORMAT(1H,1,27X25,RADIAL POSITION DATA,(CM)//3X32HNODE NUMBER,0,J
10DE R421US,2(J),6X5H2R(J),SX,HDELRL(J),SX,HDELRR(J),SX,1X),
00 2014 J21JN
2014 WRITE(6,2316) J,RR(J),RR(J),ZELR(J),ZELR(J),AZ(J),AZD(J),
2016 FORMAT(110,18,1,F17,2,F11,2,F13,2,2F13,6)
2016 WRITE(6,2315)
2018 FORMAT(1H,1,27X24,X14L POSITION DATA,(CM)//3X32HNODE NUMBER,11
1DE POSITION,Z(1),5X5W,2Z(1),5X5W,2Z(1),SX,HDELZ(1),SX,HDELZ(1),
00 2020 J22JW
2020 WRITE(6,2322) 1,2,(1,22(1),2ELZ(1),CELZZ(1))
2022 FORMAT(11,F18,1,F12,2,F11,2,F13,2)
2024 WRITE(6,2324)
2024 F084T(1,1,30X17,WNOZ2L(FM),NPJT,DATA//5X14W;8X5Y71(M);13X7WP1ND(M),WIND(M),11X7WP1ND(M),13X,8WINDP(M),10X,WINDP(M),11X)
00 2026 J21LS
2026 WRITE(6,2326) H,T(M),PINQ(M),CIND(M),WINDG(M),WINDP(M),NIND(M)
2028 FORMAT(1H,1,512P16.5,5E18.5)
C INITIALIZE PHYSICAL VARIABLES AND F(1:,j,M) = COMPUTE ERROR LIMITS FOR MAIN1460
00 50 1=2,IA
00 50 J=2,JA
IF (J,E0,2,IAND,0,1,LT,1S) GO TO 50
N(1,J)=0,
IP(1,J)=J,
WP(1,J)=0,
CP(1,J)=DATA

```

B-7

```

C = 50, CONTINUE = 1
L = 0
DO 60 J = 2, 14
DO 60 I = 2, 14
IF (E(I,J) .GT. 2.5 * PATK / FJ) THEN
  UG(I,J) = 0
  MG(I,J) = 0
  EG(I,J) = 2.5 * PATK / FJ
  FG(I,J) = N(I,J)
  F(I,J,1) = UP(I,J)
  F(I,J,2) = UP(I,J)
  F(I,J,3) = UP(I,J)
  F(I,J,4) = C(I,J)
  F(I,J,5) = C(I,J)
  F(I,J,6) = D(I,J)
  F(I,J,7) = E(I,J)
  END IF
CONTINUE = 1
END
      
```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

RE(L) = REF(M)
AE(L) = RE(M)*AEF(M)
62 Y(L) = F(I,J,N)
60 CONTINUE
1RK 1E
T = 0.
DT = .0001
EXTERNAL DERIVICNTL
REWIND 8
REWIND 9
REWIND 10
IF (KST=2) 34,30,34
30 DO 31 K=1,10000
READ (K,T,D,T,Y(I),Y(I),RK)
READ (10) K1
IF (KK=KKS) 31,32,32
31 CONTINUE
32 CONTINUE
DO 41 LL=1,10000
READ (8) K<1
IF (KK=KK) 41,42,42
41 CONTINUE
42 CONTINUE
KK=KK-1
34 CONTINUE (DERIVICNTL,Y,D,Y,AE,RE,T,D,T,RK,.0E6)
CALL RK2
REWIND 8
REWIND 9
REWIND 10
STOP
END

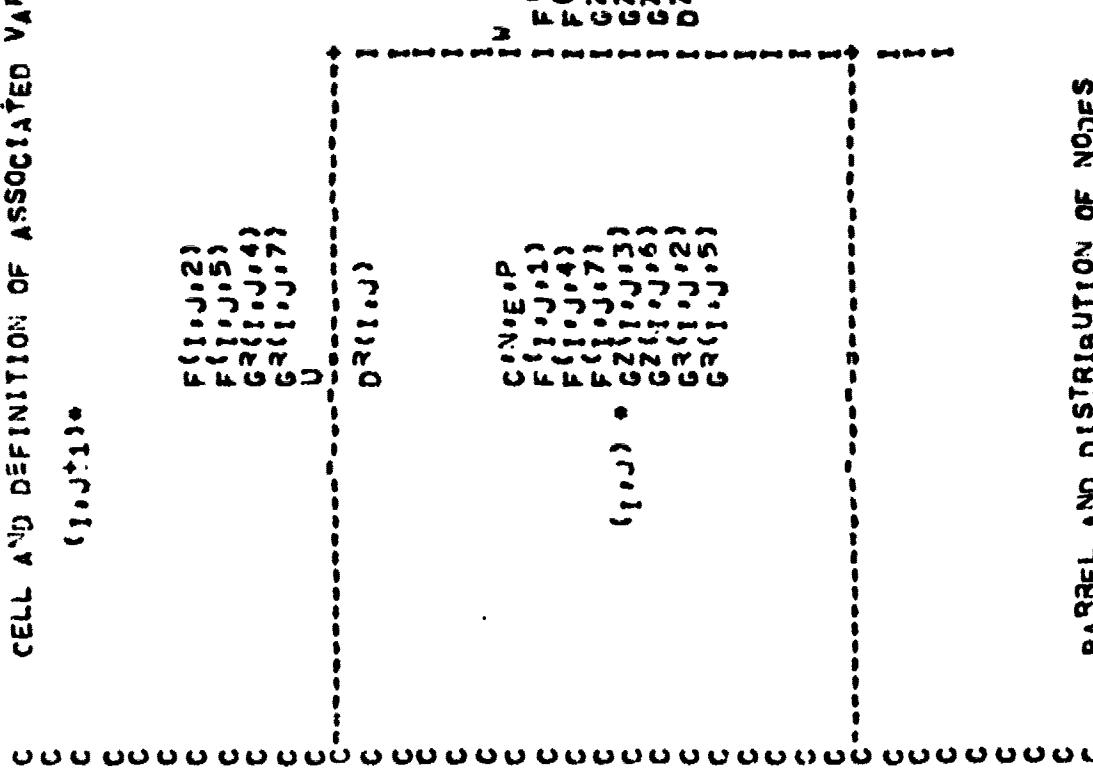
```

TWO DIMENSIONAL GAS PARTICLE FLOW

SUBROUTINE DERIV(Y,OY,T)  
CELL AND DEFINITION OF ASSOCIATED VARIABLES

(I,J+1)\*

DERI0010  
 DERI0020  
 DERI0030  
 DERI0040  
 DERI0050  
 DERI0060  
 DERI0070  
 DERI0080  
 DERI0090  
 DERI0100  
 DERI0110  
 DERI0120  
 DERI0130  
 DERI0140  
 DERI0150  
 DERI0160  
 DERI0170  
 DERI0180  
 DERI0190  
 DERI0200  
 DERI0210  
 DERI0220  
 DERI0230  
 DERI0240  
 DERI0250  
 DERI0260  
 DERI0270  
 DERI0280  
 DERI0290  
 DERI0300  
 DERI0310  
 DERI0320  
 DERI0330  
 DERI0340  
 DERI0350  
 DERI0360  
 DERI0370  
 DERI0380  
 DERI0390



BARREL AND DISTRIBUTION OF NODES

B-10

TWO-DIMENSIONAL GAS PARTICLE FLOW

```

DER10970
DER10980
DER10990
DER11000
DER11010
DER11020
DER11030
DER11040
DER11050
DER11060
DER11070
DER11080
DER11090
DER11100
DER11110
DER11120
DER11130
DER11140

L=0
DO 1 I=2,1A
C0 1 J=2,J4
IF(J.EQ.2.AND.I.LT.JS) GO TO 1
DO 3 M=1,7
L=L+1
3 F(I,J,M)=Y(L)
1 CONTINUE
C CONVERT PHYSICAL VARIABLES FROM F(I,J,M) : EXCEPT CRUG AND CZWG
C
DO 10 I=2,1A
DO 10 J=2,JA
IF(J.EQ.2.AND.I.LT.JS) GO TO 15
N(I,J)=F(I,J,1)
N(I,J)=F(I,J,2)
UP(I,J)=F(I,J,2)
WP(I,J)=F(I,J,3)
C(I,J)=F(I,J,4)
E(I,J)=F(I,J,7)

```

TWO DIMENSIONAL GAS PARTICLE FLOW

**IC CONTINUE  
C BOUNDARY VALUES FOR C(1,J)**

N(1,JB)=N(1,JA)  
UP(1,JB)=U<sup>2</sup>(1,JA)  
UG(1,JB)=U<sup>3</sup>(1,JA)  
XP(1,JB)=U<sup>4</sup>(1,JA)  
WG(1,JB)=U<sup>5</sup>(1,JA)  
DO(36,1)=2011  
E(1,2)=E(1,3)  
N(1,2)=N(1,3)  
KP(1,2)=KP(1,3)  
KG(1,2)=KG(1,3)  
UP(1,2)=0  
UG(1,2)=0  
DO(36,1)=15118  
E(1,1)=E(1,2)  
N(1,1)=N(1,2)  
KP(1,1)=KP(1,2)  
KG(1,1)=KG(1,2)  
IG(1,1)=0

34

DERI1540  
DERI1550  
DERI1560  
DERI1570  
DERI1580  
DERI1590  
DERI1600  
DERI1610  
DERI1620  
DERI1630  
DERI1640  
DERI1650  
DERI1660  
DERI1670  
DERI1680  
DERI1690  
DERI1700  
DERI1710

36

TWO-DIMENSIONAL GAS PARTICLE FLOW

DEMI 1210 = .50(MG(15,2)+MING)  
HGM(15,2) = .50(MG(15,2)+MING)  
HGD(15,2) = .50(MG(15,2)+MING)  
ACCA = C(15,2)/(15,2)  
ACCV = C(15,2)/(15,2)  
DUO = MG(15,2)/(15,2)  
DOD = MG(15,2)/(15,2)  
DFP = APPAGEN/APP  
VFSQD = CONC/CNC  
ANG = ATAN(DGn/Dg)  
DENI 2190 = DPP<sup>\*</sup>ESI(NAG)  
DENI 2190 = DPP<sup>\*</sup>COS(NAG)  
DENI 2190 = DR(15,2)  
DENI 2190 = DR(15,2)  
DENI 2190 = K(15,2)  
DENI 2190 = L(15,2)  
DENI 2190 = M(15,2)  
DENI 2190 = N(15,2)  
DENI 2190 = O(15,2)  
DENI 2190 = P(15,2)  
DENI 2190 = Q(15,2)  
DENI 2190 = R(15,2)  
DENI 2190 = S(15,2)  
DENI 2190 = T(15,2)  
DENI 2190 = U(15,2)  
DENI 2190 = V(15,2)  
DENI 2190 = W(15,2)  
DENI 2190 = X(15,2)  
DENI 2190 = Y(15,2)  
DENI 2190 = Z(15,2)  
DERI 1220 = IF(MG(15,2)=0)  
DERI 1220 = K(15,2)=0  
DERI 1220 = L(15,2)=0  
DERI 1220 = M(15,2)=0  
DERI 1220 = N(15,2)=0  
DERI 1220 = O(15,2)=0  
DERI 1220 = P(15,2)=0  
DERI 1220 = Q(15,2)=0  
DERI 1220 = R(15,2)=0  
DERI 1220 = S(15,2)=0  
DERI 1220 = T(15,2)=0  
DERI 1220 = U(15,2)=0  
DERI 1220 = V(15,2)=0  
DERI 1220 = W(15,2)=0  
DERI 1220 = X(15,2)=0  
DERI 1220 = Y(15,2)=0  
DERI 1220 = Z(15,2)=0

TWO DIMENSIONAL GAS PARTICLE FLOW

C INTERIOR REGION CALCULATIONS FOR COMPUTED VARIABLES

DO 40 I=2,4

DO 40 J=2,4

IF(I-J.EQ.2) AND(I-J.EQ.1) GO TO 45

E1(1,J)=E1(1,J)/C(1,J)+C(1,J)\*2+UG(1,J)\*2+UG(1,J-1)\*2+UG(1,J-2)/F1

VFL=LN(1.0-VFL)\*VFL

VFL=MAX(VFL,0.999)

PD(I,J)=C(1,J)\*VFL

IF(VFL.GE. VFLMAX) PD(I,J)=PD(VFLMAX)

P1(I,J)=C(1,J)\*VFL

RHOG=C(1,J)\*VFL

DELX=C(1,J)\*C(1,J)

DELY=C(1,J)\*C(1,J)

DELZ=C(1,J)\*C(1,J)

DELU=C(1,J)\*C(1,J)

DELV=C(1,J)\*C(1,J)

DELW=C(1,J)\*C(1,J)

DELUP=C(1,J)\*C(1,J)

DELVZ=C(1,J)\*C(1,J)

DELWZ=C(1,J)\*C(1,J)

DELUR=C(1,J)\*C(1,J)

DELVR=C(1,J)\*C(1,J)

DELWR=C(1,J)\*C(1,J)

DELURZ=C(1,J)\*C(1,J)

DELVRZ=C(1,J)\*C(1,J)

DELWRZ=C(1,J)\*C(1,J)

DELUPZ=C(1,J)\*C(1,J)

DELVZ=C(1,J)\*C(1,J)

DELWZ=C(1,J)\*C(1,J)

DELURZ=C(1,J)\*C(1,J)

DELVRZ=C(1,J)\*C(1,J)

DELWRZ=C(1,J)\*C(1,J)

DELUPZ=C(1,J)\*C(1,J)

DELVZ=C(1,J)\*C(1,J)

DELWZ=C(1,J)\*C(1,J)

DELURZ=C(1,J)\*C(1,J)

DELVRZ=C(1,J)\*C(1,J)

DELWRZ=C(1,J)\*C(1,J)

DERI2300  
DERI2310  
DERI2320  
DERI2330  
DERI2340  
DERI2350  
DERI2360  
DERI2370  
DERI2380  
DERI2390  
DERI2400  
DERI2410  
DERI2420  
DERI2430  
DERI2440  
DERI2450  
DERI2460  
DERI2470  
DERI2480  
DERI2490  
DERI2500  
DERI2510  
DERI2520  
DERI2530  
DERI2540  
DERI2550  
DERI2560  
DERI2570  
DERI2580  
DERI2590  
DERI2600  
DERI2610  
DERI2620  
DERI2630  
DERI2640  
DERI2650  
DERI2660  
DERI2670

```

DFP = "APPENDEN.VFS
ANGATAN(DJD/DWD)
DZ(J,J) = COS(ANG)
DR(J,J) = SIN(ANG)
LUP(J,J) = 1
KUP(J,J) = 1
KUG(J,J) = 1
IF (JPI(J,J) > 0) LWP(J,J) = 0
IF (JUP(J,J) > 0) KUP(J,J) = 0
IF (JUG(J,J) > 0) KUG(J,J) = 0
IF (JUC(J,J) > 0) KUC(J,J) = 0
DO 50 J=3, J1
P(1,J) = P(2,J)
C(1,J) = CD(2,J)
C(2,J) = 32(2,J)
50

```

**C SET BOUNDARY VALUES FOR COMPUTED VARIABLES**

```

DER12690
DER12690
DER12700
DER12710
DER12720
DER12730
DER12740
DER12750
DER12760
DER12770
DER12780
DER12790
DER12800
DER12810
DER12820
DER12830
DER12840
DER12850

```

TWO DIMENSIONAL GAS PARTICLE FLOW

B-19

```

IM1=MAX0(I-1,1)
WGB=0.5*(W3(IM1,J)+WG(1,J))
CALL LOFU (4GB,I)
IM1PL=MIN0(I-1,L!IM)
IM2PL=MIAZO(I-MPL,I)
GZW(I,J)=A2(J)*C(I,J)*(WG(IM1PL,J)**2)
IP1=MIN0(I+1,LX)
UCB=0.5*(UJ(I,J)+UG(IP1,J))
CALL LOFU (JCB,K)
JPK=MIN0(J-K,J)
JP1=MIN0(J+1,J)
CA=C(I,J)+C(IP1,J)+C(I,JP1)+C(IP1,JPK)
GRW(I,J)=A3(I,J)*CA*UGB*WG(I,JPK)
JY1=34AX0(J-1,1)
UCB=0.5*(UJ(I,JM1)+UG(I,J))
CALL LOFU (JGB,K)
JM1PK=MIAZO(J-1,L)
JM2PK=MIAZO(JM1PK,1)

```

O O

TWO DIMENSIONAL GAS PARTICLE FLOW

```

CRU(I,J)=A2*NC(I,J)*C(I,J)*(UG(I,J)*PK)+0.2)
VG3=0.5*(AG(I,J)+UG(I,J))
CALL LOFU(45B,L)
VPLSMI*UG(I,J)
300 GZJ(I,J)=AZJ(I,J)*GB*WGB*UG(IPL,J)
C COMPUTE DF((IS,2,M) AT NOZZLE CELL
C LP = LNP((IS,2)
K0 = KUP((IS,2)
C NF((IS,2,1) = (AZ(2)*(WINP*VN*UP((IS,2)*VN*(S+LP,2))
1 *AH((IS,2)*UP((IS,2)*VN((IS,2+KP)))/VN((IS,2)
C TERM1 = -U^2((IS,2)/DELZ((IS)
IF (UPR((IS,2),LT,0.) TERM1 = (UP((IS,2)-UP((IS,2))/DELZ((IS)
C DF((IS,2,2) = WPR((IS,2)*TERM1+UP((IS,2)*(UP((IS,2+KP)-UP((IS,1+KP))/-
DF((IS,2,2)*DP((IS,2)/48)*(PD((IS,3)-P((IS,2)/(NR((IS,2)*WN*DELR(3))
2*DELZR(2+KP)*DP((IS,3)*GPR((IS,2))/WN*NR((IS,2)*DELR(3))
2*GPR((IS,3)*GPR((IS,2))/WN*NR((IS,2)*DELR(3))
C TERM1 = (WINP-WP((IS,2))/DELZ((IS)
IF (WP((IS,2),LT,0.) TERM1 = (WP((IS,2)-WP((IS,2))/DELZ((IS)
IF (UPZ((IS,2),LT,0.) TERM2 = (WP((IS,3)-WP((IS,2))/DELZ((IS)
C DF((IS,2,3) = WP((IS,2)*TERM1-UPZ((IS,2)*TERM2-DZ((IS,2)/WN
1-(PD((IS,2)*P((IS,2)/48*(Z((IS,2)*WN*DELZ((IS))
2*(GPZ((IS,2)*GUPZ((IS,2)/48*(Z((IS,2)*WN*DELZ((IS))
C LP = LNC((IS,2)
KP = KUG((IS,2)
C CF((IS,2,4) = (AZ(2)*(WINP*VN*UG((IS,2)*C((S+LP,2))-_
AR((IS,2)*UG((IS,2)*C((IS,2+KP))/VN((IS,2)
C DF((IS,2,5) = (-GZU((IS,2)*GRU((IS,2)*GRU((IS,3)
2*AR((IS,2)*(P((IS,3)+GR((IS,3)*P((IS,2)*GR((IS,2))/VN((IS,2)
3*VR((IS,2)*C2((IS,2)
C

```

```

WB=0.5*(WN3+WG(1S,2))
IF (WB) 302,301,301
301 WBB*WN3
      GO TO 303
302 WBB*WG(1S,2)
303 GZM1=AZ(2)*P(1S,2)*(WBB**2)
      DF(1S,2,6)=GZM1=GZW(1S+1,2)*GW(1S,2)
      2-AZ(2)*P(1T,2)*GZ(1T,2)-P(1S,2)*GZ(1S,2)))/N2(1S,2)
      3+NZ(1S,2)*DZ(1S,2)
C      DF(1S,2,7) = ((AZ(2)*(1NG*(EIN*FJ+PLN)-WG(1S,2)*(E(1S+LP,2)*FJ+
      IN(1S+LP,2)*GZ(1S+LP,2))-A(1S,2)*UG(1S,2)*E(1S,2+KP)*FJ+
      2P(1S,2+KP)+3R(1S,2+KP))/N(1S,2)+.5*N(1S,2)*DZ(1S,2)*WF(1S,2)+
      3QR(1S,2)*U(1S,2))/FJ
C      CALCULATE DF VALUES AT INTERIOR NODES
C      00 200 1*2,1A

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

C
DF(I,J,J) = ((AZ(J)*WG(I,J))*E(I-J+LN,J)*FJ*P(I-LN,J)*
1GZ(I-J)*G(I,J)*E(I,J)*FJ*P(I+LP,J)*GZ(I+LP,J))*
2R(I,J)*UG(I,J)*E(I,J+KP)*FJ*P(I,J+KP)*GR(I,J+KP)*
3UG(I,J-1)*E(I,J-1+KN)*FJ*P(I,J-1+KN)*GR(I,J-1+KN)*
4.G+N(I,J)*GZ(I,J)*WP(I,J)+D2(I,J)*WP(I,J)*GR(I,J)*UP(I,J)*
5DR(I,J-1)*JP(I,J-1))/FJ
DERI4390
DERI4400
DERI4420
DERI4430
DERI4440
DERI4450
DERI4460
DERI4470
DERI4480
DERI4490
DERI4500
DERI4510
DERI4520
DERI4530
DERI4540
DERI4550
DERI4560
DERI4570

200 CONTINUE DYL FROM DF(I,J,M)
L=0
DO 2 I=2,12
DO 2 J=2,12
IF (J.EQ.2,AND,I.EQ.1) GO TO 2
DO 4 H=1,7
L=L+1
4 DYL(L)=DF(I,J,H)
2 CONTINUE
RETURN
END

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE CNTRL(Y,DY,DT,T,NTRY)
PARAMETER IC=25,JD=15,LD=400,NAKD=2625
DIMENSION Y(NRKD),G(NRKD)
COMMON /DC/ C1,C2,C3,C4,WNP,NV,
            GRU(ID,JD),GRW(ID,JD),GZM(ID,JD),
            COMMON /AL-/ F(ID,JD,7),DF(ID,7),11,IS,IA,IB,IM,JA,JB,JM,FT,
            1F,J,VOLP,NM,APF,V=LMAX,PAV=FLRS,KWKKKK,PIN,IRK,RHOP,
            2,TT(LD),PING(LD),CIND(LD),NIND(LD),
            3Z(ID),Z2(Z(ID),DELZ(ID),RJD),RR(JD),DELR(JD),DELR(JD),
            4A2(JD),AZC(JD),ARZ(ID,JD),ARZ(ID,JD),ARZ(ID,JD),ARZ(ID,JD),
            SVR(ID,JD),C(ID,JD),CR(ID,JD),CD(ID,JD),CD(ID,JD),
            6xGN(ID,JD),4GQ(ID,JD),UGN(ID,JD),UGN(ID,JD),
            7xPR(ID,JD),UP(ID,JD),UPZ(ID,JD),NZ(ID,JD),
            8E(ID,JD),E1(ID,JD),P(ID,JD),3R(ID,JD),PD(ID,JD),
            9GZ(ID,JD),WP(ID,JD),K1P(ID,JD),LGWG(ID,JD),
            A,WINDP(LD),
            COMMON/MC/V1JW,IV1JW(6),PW(6),
            REAL N,N1,N2,N3,N4,N5,N6,N7,N8,N9,N10,N11,N12,N13,N14,N15,N16,N17,N18,N19,N20,
            DATA PG/0,0,0/AVPROJ/0,0,0/,ZPROJ/0,0,0/
            KK=KK+1
            IF (KK>KM) I=2,I2
            KK=KK+1
            IF (KK>KM) I=1,I2
            I=NTRY+1
            GO TO 3
            2 NTRY = 2
            3 CONTINUE
            WRITE(6,1J9) KK,KK0,DT,T,PI*V
            1J8 FORMAT(1H,10X,3WKK=16,10X,4WKK0=16,10X,3WDT=1PE14.6,
            2 5X,24T=1E14,6,5X,4PIN=E14,6)
            DO 6 I=1,NIJW
            IJW=IWI(I)
            JIW=IJW(I)
            PL=PI*W(I,JW)+0.5*(WW,JWW)*(WG(N1WW,JWW)*2+UGN(NWW,JWW)*2)
            2+0.5*4*EN(1WW,JWW)*(WPL(JWW,JWW)*2+UP(JWW,JWW)*2)
            6 PW(1)=PL*2.54/2.54/(980.616*453.59)
            WRITE(6,3J3)(1,IPX(I),I=1,NIW)
            100 FORMAT(1H,6(3X,3,HPW(1,1,2)=,1PE11.4))
            IF ((KK/5)-5-KK) 8,7,8

```

```

7 CONTINUE
    WRITE(8) KK,T,(PW(I),I=1,NIJW),PB,VPROJ,ZPROJ,Y(4),Y(5)
8 CONTINUE
    IF((KKK(KW))<=K<) 5,4,5
4 CONTINUE
    WRITE(9) KK,T,DT,(Y(I),I=1,IRK)
    DO 9 I=1,1
    DO 9 J=1,1
    9 CP(I,J)=N((I,J))**WY
    WRITE(10) KK,(CP(I,J),J=1,IM),(2(I),I=1,IM),
2 (CP(I,J),I=1,IM),(CP(I,J),I=1,IM),I=1,IM)
    WRITE(6,320) PW,CIN,XING,MNP,N
320 FORK(1,4,2X,4)PIN=1PE11.5,2X,4HCIN=E11.5,2X,5HWING"
2 E11.5,2X,2HWINGP=E11.5,2X,4HNIN=E11.5
    CALL OUTPT(IHUP,IJD,IM,JM,10,1DHP FIELD
    CALL OUTPT(IH,O,AG,IJD,IM,JM,10,1DHWG FIELD
    CALL OUTPT(IH,O,JC,IJD,IM,JM,10,1DHWG FIELD
    CALL OUTPT(IH,O,XP,IJD,IM,JM,10,1DHP FIELD

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```
CALL OUTPT (1H0, UP ,1D,JD,1M,1M,10,10HUP FIELD )
CALL OUTPT (1H0,C .1D,JD,1M,1M,10,10HC FIELD )
CALL OUTPT (1H0,N .1D,JD,1M,1M,10,10HN FIELD )
CALL OUTPT (1H0,E1 .1D,JD,1M,1M,10,10HE1 FIELD )
5 CONTINUE
RETURN
END
```

TWO DIMENSIONAL GAS PARTICLE FLOW

```
SUBROUTINE LCFLU (U,L)
IF (U) 2·1·1
1 L=0
2 RETURN
2 L=1
3 RETURN
END
```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE UNEQRCIM(RM,IR,RR,R,TD)
DIMENSION R(10)
FIRSFLOAT(IR)
FINSFLOAT(IR)
R=1.0
DO 1 K=1,5
EX=EXP(-R*(FIR+IR-2.0))+(1.0-EXP((-2.0*B*(FIR+0.0))))*RM/RR
A=ANALOG(EX)/(FIR-IR)
WRITE(6,101) K,3,IR,RR
101 FORMAT(1Z3,3X,24K2,15,3X,2H8,1PE14.6,3X,3H1H,15,3X,
2,3H1A,15,3X,3H4H,1E14.6,3X,2H3A,1E14.6)
1 CONTINUE
DO 2 K=6,25
F1=SINH((B*(F13-1.0))
F2=RR*SINH((B*(F14-1.0))
D1=F1*F2*(FIR-1.0)*COSH(B*(FIR-1.0))-RR*(FIR-1.0)*COSH(B*(FIR-1.0))
D2=F1*(FIR-1.0)**2*F2*(FIR-1.0)**2
D3=SNGL(D1*D2)/DBLE(D2)/DBLE(D1)**2*DBLE(D1)/
2 DBLE(D2)
R=R+78*(6,1J2)*JCB'B3,5,3X,3H9B,1PE14,6,3X,2H8,1E14,6)
102 FORMAT(1H,3X,24K2,15,3X,3H9B,1PE14,6,3X,2H8,1E14,6)
IF (ABS(D3)-1.0E-7)>3.02
2 CONTINUE
3 ASR/SINH((3*B*(FIR-1.0)))
4 R1=1.0*SINH((B*FLOAT(I-1)))
RETURN
END

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE NZLIND (T1,PIND,CIND,WINDG,WINDP,NIND,T,PIN,CIN,WING,
2 WINDP,NIN,L0)
2 REAL(WINDC,WIN)
DIMENSION T(LD),PIND(LD),CIND(LD),WINDG(LD),WINDP(LD),NIND(LD),
DATA LLL/1/
GO TO (1,2),LLL
1 T1=T1(1)
2 T2=T1(2)
3 I=1
4 LLL=2
5 IF (T-T1) 7,3,3
6 IF (T-T2) 10,10,11
7 KS=I+1
8 DO 9 K=KS,D
9 SK (T1(K)-T) 4,5,6
10 CONTINUE
11 CONTINUE
12 J=J
13 T1=T1(1)
14 T2=T1(1+1)
15 G0 T0 10
16 S-J-1
17 T1=T1(1)
18 T2=T1(1+1)
19 G0 T0 10
20 ME=-I-1
21 DO 8 N=1,N5
22 N=1*N
23 IF (T1(N)+T) 9,9,8
24 CONTINUE
25 T2=T1(N+1)
26 T2=T1(1+1)
27 P1N =TF*2*PIN (1)+TF*PIN (1+1)
28 C1N =TF*2*CIND (1)+TF*CIND (1+1)
29 WING=TF*2*WINDG (1)+TF*WINDG (1+1)
30 NZL100010
31 NZL100020
32 NZL100030
33 NZL100040
34 NZL100050
35 NZL100060
36 NZL100070
37 NZL100080
38 NZL100090
39 NZL10100
40 NZL10101
41 NZL10120
42 NZL10130
43 NZL10140
44 NZL10150
45 NZL10160
46 NZL10170
47 NZL10180
48 NZL10190
49 NZL10200
50 NZL10210
51 NZL10220
52 NZL10230
53 NZL10240
54 NZL10250
55 NZL10260
56 NZL10270
57 NZL10280
58 NZL10290
59 NZL10300
60 NZL10310
61 NZL10320
62 NZL10330
63 NZL10340
64 NZL10350
65 NZL10360
66 NZL10370
67 NZL10380
68 NZL10390

```

UINP\*TF2\*WINCP(1)+TF\*WINDP(1+1)  
NIN\*TF2\*WINC(1)+TF\*NIND(1+1)  
RETJRI  
END

NZL10400  
NZL10450  
NZL10420  
NZL10430

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE RK2 (CPIV,CNTRL,Y,DY,A,R,T,DT,N,DTM)
SECOND ORDER RUNGE KUTTA
NTRY IS A DESIGNATED ONE OF THE VALUES LISTED BELOW IN CNTRL
CNTRL CONTINUES INTEGRATION
NTRY = 1 RETURN FROM RUNGE KUTTA
NTRY = 2 RETURN FROM RUNGE KUTTA
NTRY = 3 REPEAT STEP WITH NEW DT GIVEN IN CNTRL
NTRY = 4 CONTINUE INTEGRATION WITH FIXED STEP
PARAMETER NRKD=25
DIMENSION Y(NRKD),DY(NRKD),A(NRKD),R(NRKD),YST(NRKD)
EXTERNAL DERIV,CY,V
THR10=1.0E-03,THR2=0.5
CAM=0.5
BETA=C/5/CAH
ALPHA=1.0-BETA
CALL DERIV (Y,DY,T)
CALL CNTRL (Y,DY,C,T,NTRY)
TST=T
DO 5 I=2,N
YST(I)=Y(I)
5 CYST(I)=DY(I)
6 IF (DT) 8,7,8
7 WRITE (6,10)
101 FORMAT (1H,20X,17HSTEP SIZE = ZERC.)
RETURN
8 T=TST+5*DT
9 Q(1)=YST(1)+CY*DY(1)+BETA*D(Y(1))
CALL DERIV (Y,DY,T)
T=TST+DT
DO 10 I=2,N
10 Y(I)=YST(I)+DT*(ALPHA*D(Y(I))+BETA*D(Y(I)))
CALL DERIV (Y,DY,T)
SOCM=C/0
DO 13 I=1,N
E(Y(I))=(YST(I)+0.5*DT*D(Y(I))+DY(I))
C=A(I)+R(I)*ABS(Y(I))
IF (C) 12,11,12
11 WRITE (6,13)
132 FORMAT (1H,20X,27HA(1)+R(1)*ABS(Y(1)))=0 AT I = + 16)

```

RETURN  
12 EOC=ABS(E/C)  
C EOC=NMAX1(EOC'EOCM)  
IF (EOC>EOCM) 13:13.901  
901 EOC>EOC  
LSN=1  
13 CONTINUE  
1F (EOC<1.0) 17,17,14  
14 T=TST  
DO 15 I=1,N  
Y(I)=YST(I)  
15 D(Y(I))=YST(I)  
CALL IJM (L8V 'EOCM')  
DO 16 J=1,40  
EOCM=EOCM/10.0  
DT=QT/THR10  
IF (EOCM>0.31 6,5,16  
16 CONTINUE

RK2 0400  
.RK2 0410  
RK2 0420  
RK2 0430  
RK2 0440  
RK2 0450  
RK2 0460  
RK2 0470  
RK2 0480  
RK2 0490  
RK2 0500  
RK2 0510  
RK2 0520  
RK2 0530  
RK2 0540  
RK2 0550  
RK2 0560  
RK2 0570

TWO DIMENSIONAL GAS PARTICLE FLOW

```

GO TO 6
17 CALL CNTRL(Y,UY,DT,T,NTRY)
    GO TO (21,18,19,4),NTRY
18 RETURN
19 TSTST
    DO 20 I=1,4
        Y(I)=YST(I)
20 CYC(1)*CYST(I)
    GO TO 6
21 IF (EOCH=3,3) 25,25,22
22 DT=DT/THR13
    CALL IJ1 (-SY, EOCM)
    GO TO 4
23 IF (EOCM-C,03) 1, 26,4,4
25 DT=DT/THR13
    IF (ABS(DT)-ABS(DTK)) 4,4,24
24 DT=ABS(DT)*DT/ABS(DT)
    GO TO 4
END

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE LJM (LSV,EQCM)
PARAMETER IJ=25,JD=15,LD=400,NRKD=2625
COMMON /ALL/ F(1,1),C(1,1),DF(10,JD),S(10,JD),IB(10,JD),JA(10,JD),
  VOLP,WY(APF,VFLNAX,PAY,FL,RC,KK,KK,PIN,IRK,RHOP,
  2T1(LD),PI(Y(LD),WIND(LD),NIND(LD),
  3Z(LD),DELZ(LD),DELZ(LD),RR(JD),DELR(JD),DELR(JD),
  4A2(JD),ARD(ID,JD),ARD(ID,JD),V(ID,JD),V(ID,JD),
  SVR(ID,JD),C2(ID,JD),C1(ID,JD),CD(ID,JD),
  EWGN(ID,JD),UGN(ID,JD),UGN(ID,JD),UGN(ID,JD),
  7WPR(ID,JD),UPF(ID,JD),UPF(ID,JD),UPF(ID,JD),
  BE(ID,JD),BE(ID,JD),BE(ID,JD),BE(ID,JD),
  9G2(JD),KUP(ID,JD),KUP(ID,JD),KUP(ID,JD),
  A(WINDP(LD),
L=U
DO 2 I=2,14
 1SV=1
  DO 2 J=2,JA
    1SV=2
    IF (J.EQ.2 .AND. I.EQ.6) TC 2
    IF (J.EQ.17) 1,0,7
    1SV=3
    LEL+1
    IF (L.EQ.1) 1,3,01
    1 CONTINUE
    2 CONTINUE
    3 CONTINUE
    WRITE (6,101) E0CH,LSV,LSV,LSV,LSV,MSV
101 FORMAT (1H,10X,5HEOCM=,1PE12.5,10X,2HL=,16,10X,2HL=,16,10X,
  2 24J=,16,1,X,2HN=,4,6)
  RETURN
END

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE OUTPT (IPC,F,JD,IM,JM,NL,LABEL)
DIMENSION = (ID,JD),LABEL(22),LAB2(20)
DATA LBW/64/
GO TO 200
ENTRY OUTPT7 (IPC,G,K3,JD,IM,JM,NL,LABEL)
DIMENSION G (ID,JD,7)
DO 201 I=1,14
DO 201 J=1,14
201 F(I,J)=G(I,J,K3)
203 CONTINUE
JMM=MING(JM,12)
NW=I+(NL-N+1)/6
NST=10-(N+1)/2
DO 1 I=N+2,J
1 LAB2(I,J)=5
502 I=N
503 NST+1-I
2 LAB2(K)=LAB2(I)
WRITE (6,101) IPC,LAB2(1),LAB2(2),(J,I,JMM)
101 FORMAT (A120,/,1H ,2X,1H ,2X,2H J,I2,1110)
102 WRITE (6,102) I,(F(I,J),J=1,JMM)
102 FORMAT (1H ,13,1PE10.3,1E10.3)
103 RETURN
END

```