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CALCULATION OF THE THREE DIMENSIONAL PARTICLE TRAJECTORIES IN A ONE AND ONE-HALF STAGE OF A COMPRESSOR

M. Fathy Hussein, et al

Cincinnati University

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Army Research Office-Durham

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The equations of motion, in three dimensions, for solid particles moving in a compressible gas flow in a rotating cascade are solved for the case of the particles moving through a compressor guide vane followed by a compressor stage. The solution considers the particle impact and rebound with both the blade walls and the compressor The three dimensional absolute paths of the particles, their trajectories relative to the compressor rotor, their velocity histories, and the combined particle velocity diagrams in the compressor cascades are given. The effects of flow parameters on the dynamic behavior of the solid particles throughout the compressor one and one-half stage are investigated. / Parameters considered included particle mean diameter and material density, initial particle and gas velocities at the guide vane inlet, and compressor rotor rotational speed. Observations concerning the erosion damage to the blades of the compressor cascades are also discussed.

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CALCULATION OF THE THREE DIMENSIONAL PARTICLE TRAJECTORIES IN A ONE AND ONE-HALF STAGE OF A COMPRESSOR

M. Fathy Hussein and W. Tabakoff

February 1973



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### NOMENCLATURE

В	frame fixed in blades (Figure 1)
Во	origin of the frame B (Figure 3)
ß	angle between particle relative velocity and tangent to surface
c <sub>g</sub>	absolute gas velocity
c <sub>p</sub>	absolute particle velocity
c'g ·	gas absolute velocity component in the x,0 plane
C'p	particles absolute velocity component in the x,0 plane
C <sub>p</sub> g	specific heat of gas at constant pressure
- g Y	modified stream function (Equation (13))
d <sub>p</sub>	particle mean diameter
Δχ	spacing between adjacent points in the meridional direction Figure 8
Δθ	spacing between adjacent points in the tangential direction Figure 8
Δt	increment of time
E	frame fixed in the engine (Figure 1)
Eo	origin of E (Figure 1)
G	coefficient inversely proportional with the particle characteristics time (Equation (4))
g(Re)	Reynolds number dependent function (Equation (5))
h	normal stream channel thickness (blade height) (Figure 2)
λ	angle between meridional streamline and engine axis
μď	gas viscosity
$\bar{n}_1, \bar{n}_2, \bar{n}_3$	unit vectors in the direction of the coordinate curves $\mathbf{x}$ , $\boldsymbol{\theta}$ , $\mathbf{z}$
$\bar{\mathbf{N}}_1, \bar{\mathbf{N}}_2, \bar{\mathbf{N}}_3$	unit vectors in the direction of the axes X, Y, Z
p .	pressure at a point
R	blade mean radius (Figures 1 and 2)

Re	Reynolds number (Equation (10))
r	radius from axis of rotation (Equation (12))
<sup>o</sup> g	gas density
$\bar{\rho}_{\mathbf{p}}$	particle material density
T <sub>g</sub>	gas temperature
U	blade speed at the mean radius (Figure 7)
u g	gas relative velocity component in the x-direction
v <sub>g</sub>	gas relative relocity
v <sub>p</sub>	particle relative velocity
v'g	gas relative velocity component in the x,0 plane
V'p	particle relative velocity component in the x,0 plane
v <sub>g</sub>	gas relative velocity component in the tangential direction
W	weight flow rate of mixture per channel
<b>w</b> p	particle relative velocity component in the radial direction
ω	blade angular velocity
x,θ,z	coordinate axis in the meridional, tangential and radial direction, fixed in B (Figures 1 and 2)
X,Y,Z	axes fixed in engine (Figures 1 and 2)
x,0,z	particle velocity components measured in B
 x,θ,z	particle acceleration components measured in B
<b>ż,</b> ż,ż	absolute velocity measured in E
x,Ÿ,Ż	absolute acceleration measured in E
У	distance measured along the tangential direction
Subscripts	
a	absolute trajectory
g	gas
i -	initial conditions at particles entrance

conditions at the boundary AH (Figure 14)

in

	n	normal to surface
•	0	total conditions
	out	after cascade
i	p	particle
	t	tangent to surface
	1	before collision
•	2	after collision

#### INTRODUCTION

In modern gas turbine engines, solid particles entrained by the gas flow passing through the channels of the compressor impinge with the compressor blades and cause their erosion. The study of the dynamic behavior of the solid particles is important to further understand the blade erosion The fundamental equations, in three dimensions, that govern the motion of the solid particles suspended by the gas flow in a cascade of a turbomachine are given by the authors in References 1 and 2 for the cases of stationary and rotating cascades, respectively. These fundamental equations are solved for the case of particle motion in turbines in Reference 2. Due to the difference in geometry and the function of turbines and compressors, the dynamic behavior of the solid particles in compressor cascades are expected to be different from that for a turbine. In this investigation the solid particles equations of motion of Reference 2 are solved to determine the dynamic behavior of the solid particles in a one and one-half stage of a compressor. The particles are taken to enter the compressor guide vanes uniformly. The compressor cascade pitch, mean radius and speed of rotation of the rotor are taken the same as those for the turbine example of Reference 2, in order to show the fundamental difference in the dynamic characteristics of the solid particles in compressors and turbines. The particles are assumed to be spheres of constant average mean diameter, uniform material density, and small in size. The forces acting on the solid particles causing their motion in the gas flow are assumed to be mainly the drag forces that the gas exerts on them. It is further assumed that the presence of the solid particles in the flow does not alter the gas properties from that for the nonparticulate gas flow passing through the same cascade. This assumption is valid for small particle concentrations and high particle material densities.

The computer program given by the authors in Reference 3 is used to compute and plot the particle dynamic behavior, namely, the particle absolute and relative three dimensional paths, their velocity distributions, and overall velocity diagrams. The results of the investigation of the impact and rebound pheromenon of the solid particles with the blades given in Reference 1 gives the restitution and rebound to incidence angle ratios of the particles. These ratios define the particle condition after impact and are used in solving the equations of motion of the solid particles in the compressor. Particle collision and rebound from both compressor blades and casing are considered. The gas properties anywhere in the cascade channel are calculated by solving the fundamental equations of motion for a gas in a cascade.

The equations of motion of the particles are formulated with respect to axes fixed in the blades at the entrance of the cascade row. With the impact and rebound phenomenon well described, and the drag coefficient and gas properties known, the equations of motion of the particles may be solved. One row of blades is considered at a time. The particles enter the row with known initial conditions, hit the walls and rebound (perhaps several times), until they leave the nozzle. The particles outlet conditions constitute the initial condition for the successive row. The equations of motion of the particles with respect to a new frame of axes using the known initial conditions are then solved using the corresponding gas properties in the new cascade row and so on. The particles positions

may be referred to the initial axes by a simple transformation. Repeated solution of equations of motion of the particles for all successive cascade rows gives the particles dynamic behavior through the compressor stages. This study showed the effects of the flow main parameters such as the particles mean diameter, solid particles material density, particle and gas initial velocities, and compressor rotor rotational speed on the dynamic behavior of the solid particles.

Examination of the particles trajectories showed the areas on the blades of the compressor guide vanes, both rotor and stator, which are subjected to more particle impacts. This made it possible to predict the blades portions that are likely to erode and predict solutions to minimize blade erosion.

# Equations of Motion of Solid Particles Suspended By the Gas Flow in a Rotating Cascade

Referring to Figure 1 and Figure 2, the frame B, is fixed in an arbitrary blade of the rotating cascade with  $n_1$ ,  $n_2$ , and  $n_3$  a set of nonparallel, noncoplaner, right-handed unit vectors in the direction of the coordinate curves x,  $\theta$  and z, respectively. The point  $B_0$  is the origin of the frame B, which is taken at the intersection of the plane tangent to the blade row at the entrance and the blade axial chord in the mid-stream surface of revolution of radius R that passes through the middle of the blade height. The coordinate curves, x,  $\theta$  and z are in the axial or meridional direction, the tangential, and the radial directions, respectively. Further, it is assumed that the frame B, fixed in the blade row, moves with a constant angular velocity  $\omega$ , equal to the angular speed of the rotor in a reference frame E fixed in the engine. In the reference frame E,  $\bar{N}_1$ ,  $\bar{N}_2$  and  $\bar{N}_3$  are unit vectors in the direction of the mutually perpendicular set of axes X, Y and Z, and are fixed in the engine at a point  $E_{\rm O}$ . Point  $E_{\rm O}$  is the intersection of the engine axis with the plane tangent to the blade row at the entrance. The coordinate axis X is in the axial direction, while Y and Z are axes normal to the X axis in the plane tangent to the blade row at the entrance, as shown in Figures 1 and 2.

Referring to Figure 3, the coordinate curves x,  $\theta$  and z, that rotate with an angular velocity  $\omega$ , after a time t, are at an angle equal to  $\omega t$  from the Z axis. The particle p is at any arbitrary position x,  $\theta$  and z measured from  $B_O$ . According to Newton's laws of motion using a proper transformation between the relative and fixed frames, it is shown (Reference 2) that the three dimensional equations of motion of the solid particles entrained by the gas flow in a rutating cascade are

$$\ddot{\mathbf{x}} = \mathbf{G}(\mathbf{u}_{\mathbf{G}} - \dot{\mathbf{x}}) \tag{1}$$

$$\ddot{\theta} = \frac{G}{(R+z)} \left[ v_{g} - (R+z) \dot{\theta} \right] - \frac{2\dot{z}}{(R+z)} \left( \dot{\theta} + \omega \right) \tag{2}$$

$$\dot{z} = -G\dot{z} + (R + z)(\dot{\theta} + \omega)^2 \tag{3}$$

where  $u_g$  and  $v_g$  are the gas relative velocity components in the axial and tangential directions. Also, x,  $\theta$ , z and  $\dot{x}$ ,  $\dot{\theta}$ ,  $\dot{z}$  and x,  $\dot{\theta}$ , z are the particles coordinate curves, velocity and acceleration components in the axial, tangential and radial directions, respectively, measured in the relative frame B. It may be noted that the second term in the right hand side of Equation (2) represents the Coriolis acceleration, while the second term in the right hand side of Equation (3) represents the centrifugal accelerations of a particle moving in curved path in the rotating frame B.

The coefficient G in Equations (1), (2) and (3), which is inversely proportional to particle characteristic time, is given by

$$G = \frac{18 \mu_g}{d^2 p \rho_p} g(Re)$$
 (4)

In Equation (4), the Reynolds number dependent function g(Re) is a correction factor to the drag force formula given by Stokes for spherical particles moving at a very small Reynolds number in a gas flow (Reference 1). This function is given by:

$$g(Re) = C_D \frac{Re}{24} = \frac{C_D}{C_{D_O}}$$
 (5)

where  $C_{D_O}$  is the Stokes drag coefficient, and

C<sub>D</sub> is the drag coefficient for spherical particle at any Reynolds number.

From Reference 1, this drag coefficient is given by

$$C_{D} = \frac{24}{Re} \qquad \qquad C < Re < 1 \qquad (6)$$

$$C_D = \frac{24}{Re} (1 + \frac{3}{16} Re)$$
  $1 \le Re \le 4$  (7)

$$C_D = 21.9416 \text{ Re}^{-0.718} + 0.3240 \qquad 4 \le \text{Re} \le 2000$$
 (8)

The Reynolds number given in Equations (6), (7), (8), and (9) is defined as:

$$Re = \frac{d_{p} \rho_{q}}{\mu_{q}} \sqrt{(u_{q} - \dot{x})^{2} + [v_{q} - \dot{\theta}(R + z)]^{2} + \dot{z}^{2}}$$
 (10)

The distance y that a particle travels in the  $\theta$  direction on the surface of revolution with radius (R + z) is given as a function of the particle relative position vector components z and  $\theta$  and the cascade mean radius R as

$$y = (R + z) \theta \tag{11}$$

The gas relative velocity components ug and vg in Equations (1), (2), and (3) can be computed at every mesh point of a square grid constructed in the cascade channel by solving the gas equations of motion give in Reference 2. The gas equations of motion are:

Combined Momentum and Continuity Equations

$$\frac{\partial^{2}\Psi}{\partial x^{2}} + \frac{1}{r^{2}} \frac{\partial^{2}\Psi}{\partial \theta^{2}} + \left[\frac{\sin \lambda}{r} - \frac{1}{h \rho_{g}} \frac{\partial (h \rho_{g})}{\partial x}\right] \frac{\partial \Psi}{\partial x} - \frac{1}{r^{2} \rho_{g}} \frac{\partial \rho_{g}}{\partial \theta} \frac{\partial \Psi}{\partial \theta} = \frac{2h \rho_{g}}{W} \omega \sin \lambda \tag{12}$$

where Y is a form of the stream function give by

$$u_g = \frac{W}{rh \rho_g} \frac{\partial \Psi}{\partial \theta}$$

$$v_{g} = -\frac{W}{h} \frac{\partial \Psi}{\partial x}$$
 (13)

the combined energy and state equation is

$$\frac{\rho_{g}}{\rho_{g_{in}}} = \left[1 - \left(\frac{|\vec{c}_{g}|^{2}}{2 c_{p_{g}} T_{g_{in}}}\right)\right]$$
 (14)

Discussion of the numerical solution of Equations (12), (13) and (14) is reported in Reference 3.

The particle velocity and direction after impact are determined experimentally (Reference 4) for corn cups particles and steel blades. The restitution ratio is shown in Figure 4 while the rebound to incidence angle ratio is given in Figure 5. The restitution ratio data is

represented by the dotted line in Figure 4 and give by the expression:

$$\frac{v_{p_2}}{v_{p_1}} = \frac{v_{p_{n2}}}{v_{p_{n1}}} \cdot \sqrt{\frac{1 + \cot^2 \beta_2}{1 + \cot^2 \beta_1}}$$
 (15)

also the dotted line in Figure 5 represents the rebound to incidence angle ratio as,

$$\frac{\beta_2}{\beta_1} = \frac{1}{\beta_1} \cot^{-1} \left[ \left( \frac{v_{p_{t2}}}{v_{p_{t1}}} \cdot \frac{v_{p_{n1}}}{v_{p_{n2}}} \right) \cdot \cot \beta_1 \right]$$
 (16)

In Equations (15) and (16) the ratio between the particle relative velocity components tangent and normal to the blade surface after and before collision [1] are given, respectively, by the equations:

$$v_{p_{t2}}/v_{p_{t1}} = 0.95 + 0.00055 \beta_1$$
 (17)

$$v_{p_{n2}}/v_{p_{n1}} = 1.6 - 0.02108 \beta_1 + 0.0001417 \beta_1^2$$
 (18)

Equations (1), (2), and (3) may be solved numerically for every particle entering the cascade in increments of time if the initial conditions are known. The time increment may have a constant value as long as it does not take the particle beyond the walls, thus, at the regular increment nearest the wall the time increment has to be iterated to the exact value that is necessary for the particle to just hit the wall. Solution of the general system of equations of the type of Equations (1), (2), and (3) and a discussion of errors are given in Reference 3. The solution of the particle equations of motion utilizes Equations (6) through (9) to compute the coefficient G of Equation (4), the solution of Equations (12), (13), and (14) to yield the gas properties, and Equations (15) through (18) to give the particle conditions after rebound that can be used as the new initial conditions at the points of discontinuity.

The solution of the equations of motion of the particles, Equations (1), (2), and (3) gives the relative and absolute locations as well as the velocity components of a particle in the rotating cascade row. Successive solution of these equations for every cascade row will give the particles paths throughout the compressor. The computer program of Reference 3 uses the IBM 1130 and the Calcomp plotter to draw the particle trajectories and velocities in the compressor.

# PARTICLES DYNAMIC BEHAVIOR IN ONE AND ONE-HALF STAGE OF A COMPRESSOR

The dimensions of the compressor guide vanes, the rotor, and the stator that constitute the one and one-half stage of a compressor are given in Figure 6. The cascade pitch equals 1.295 inch, the cascade mean radius R = 7.05 inches and the cascade height equals 1.5 inch. The diameter of the compressor is taken relatively small so that the centrifugal effects on the particles are pronounced and also in order to give a more general particle path. Reference 5 gives the airfoil data. The rotor blades are assumed to be at the position shown in Figure 6 when the particle is at the guide vane exit. The combined gas velocity diagram for a compressor stage of 43.8% degree of reaction is given in Figure 7. The mesh distribution is shown in Figure 8. gas conditions at the compressor guide vanes inlet are: gas initial, velocity  $C_{g_i} = 142.64$  ft/sec, initial gas density  $\rho_{g_{in}} = 0.076$  lb/ft<sup>3</sup>, initial gas total temperature  $T_{g_{in}} = 60$ °F, and the total mass flow rate per channel W = 0.123 lb/sec. The particles enter at the stream surface of revolution of radius 7.05 inches. The cascade design angular speed at the mid-radius R is taken to be  $\omega_d = 603.5$  radians per second, which is equivalent to a mid-radius blade velocity of 352.5 ft/sec. pressor cascade pitch, the design speed of rotation, the radius of the mean surface of revolution, the total flow rate per channel as well as the gas initial condition at inler to the guide vanes, are taken equal to those of the turbine stage example of Reference 2 in order to notice the fundamental differences between the particle dynamic behavior in turbines and compressors.

A general idea about the dynamic behavior of the solid particles in the given one and one-half compressor stage may be obtained from the figures that give the absolute and relative trajectories, the radial displacement and nondimensional absolute velocity distribution throughout the compressor blades, Figures 9 through 24. These results are given in groups of four figures, each giving the dynamic behavior of twelve particles entering the compressor guide vanes with a uniform speed equal to 30 percent of the gas inlet velocity at a distance upstream of the compressor guide vanes leading edge. These four groups of figures are for particles with mean diameters equal to 1000, 200, 40 and 8 microns, respectively. They all have material density of 68.7 lb/ft3 and  $C_{p_i}/C_{q_i} = 0.3$ . In order to show the effect of the particle collision with the guide vanes leading edge, the distance between particles number 1 and 2 and 11 and 12 is taken smaller, due to the smaller leading edge radius of compressor blades as compared to those for turbine blades [2]. The particles are categorized in four different patterns, such as particles number 2, 5, 8 and 11, according to their trajectories in the guide vanes. Figures 9, 13, 17 and 21 show the projection of the particle absolute trajectories ya versus x in the x-0 surface. Figures 10, 14, 18 and 22 give particle trajectories relative to the rotor. The particles with smaller  $d_{\mathbf{p}}$  tend to follow more closely the gas streamlines in the guide vanes, move close together and become less scattered in the rotor and stator. Larger diameter particles, however, do not enter the opposite blade channel but scatter in the successive rotor channels (Figures 10 and 22). Unlike the turbine stage example [2], the particles with large diameters of 1000 and 200 microns, do not return to the guide vanes after hitting the compressor rotor. This is a result of the difference in the stage geometry and blade leading edge radius. Since the radial displacement of the particles increase with increased mean diameter (Figures 11, 15, 19, and 23), larger particles tend to reach the casing of the compressor before leaving the one and one-half stage. The particles absolute velocities, nondimensionalized with respect to gas velocity at the inlet to the guide vanes, are given in Figures 12, 16, 20, and 24. Less abrupt changes in the value of the velocity are observed for particles with smaller dp, but they are more influenced by the changes in gas velocity, especially near the blade surface (Figures 12 and 24). Smaller particles move with higher initial accelerations in the guide vanes. The particle velocity approximately reaches a constant value in the rotor. higher particle velocities in the rotor indicate that the rotor blades can suffer from severe erosion.

Observations concerning blade erosion may be summarized from Figures 9 through 24. In general, compressor guide vanes and rotor blades may suffer leading edge erosion due to the impingement of all size particles. The pressure side of the guide vanes blade, however, will primarily suffer erosion by particles with higher dp, since they follow trajectories further from the gas streamlines. As for the compressor rotor, particles of higher dp tend to hit the lower part of the leading edge, and as dp decreases the particles are shown to hit at the first half of the rotor pressure side. Less collisions are observed with the rotor blades for particles with  $d_p = 8$  microns. This indicates that the first half of the pressure side of the compressor rotor will be eroded severely. The trajectories also show that the pressure side of the compressor stator will be subjected to erosion damage due to the impingement of particles of all sizes. Only particles with higher  $d_{\mathbf{p}}$  will cause stator blade leading edge erosion. suction sides will suffer no erosion damage in any cascade row since no particle collisions are observed there. The radial displacement of the particles will cause them to travel toward the blade tip, and after a few stages the blade tips will be eroded by the impingements of all the particles that enter the nozzle at all radii. Erosion of sections closer to the hub is less severe (Reference 6).

#### Effect of Particles Mean Diameter on Their Dynamic Behavior

The effect of d<sub>p</sub> on the dynamic behavior of the four typical particles, namely, particles number 2, 5, 8 and 11 is shown in four groups of five figures each, Figures 25 through 44. Each group of figures consists of the absolute and relative projected particle paths in the stream surface of revolution, its radial displacement, and its nondimensional particle absolute velocity distributions in the one and one-half stage of the compressor. The figures also include particle combined velocity diagrams compared to the gas velocity diagram at the design point. The particles mean diameter takes the values 1000, 200,

40 and 8 microns with constant  $\rho_p = 68.7 \text{ lb/ft}^3$  and  $C_{p_i}/C_{g_i} = 0.3$ . Figures 29, 34, 39 and 44 show the deviation of the particle velocity diagram from that of the gas decreases as  $d_p$  decreases. The diagrams give the overall particle velocity at the inlet and the exit of the compressor's first two rows. Similar observations to those given in the preceding paragraph concerning the effects of varying the particle mean diameter on the particles dynamic behavior may be noticed from Figures 25 through 44.

#### Effect of Particles Material Density on Their Dynamic Behavior

Figures 45 through 60, illustrate the effect on the particle dynamic behavior for the four typical particles to the changes in  $\rho_{\rm p}$ . The particle material density,  $\rho_{\rm p}$ , takes the values of 34.29 7 and 151 lb/ft<sup>3</sup>, d<sub>p</sub> and C<sub>p<sub>i</sub></sub>/C<sub>g<sub>i</sub></sub> have constant values of 40 microns and 0.3, respectively. A decrease in  $\rho_{\rm p}$  causes less deviation of particle motion from gas streamlines, earlier impingements with the rotor pressure side, and lower velocities in the stator.

## Effect of Particles and Gas Initial Velocities on Particles Dynamic Behavior

The effect of changing  $C_{p_i}/C_{g_i}$  on the particle dynamic behavior is shown in Figures 61 through 76. Small effects are observed on the particle trajectories, especially the radial displacement component, due to changing  $C_{p_i}/C_{g_i}$ . The four typical particles show that the particle velocities tend to reach the same value at the exit from the guide vanes for different  $C_{p_i}/C_{g_i}$ . In Figures 61 through 76,  $C_{p_i}/C_{g_i}$  take the values 0.15, 0.3 and 0.6, while  $d_p$  and  $\rho_p$  have the constant values; 40 microns and 68.7 lb/ft<sup>3</sup>, respectively.

The effects on the particle dynamic behavior of increasing the gas speed at the inlet to the guide vanes for a certain particle inlet velocity is similar to the effects of decreasing  $C_{p_i}/C_{g_i}$ . The particle diameter has the greatest effect on the particle dynamic behavior, while  $\overline{\rho}_p$  has a greater effect than  $C_{p_i}/C_{g_i}$ .

# Effect of Compressor Rotor Rotational Speed on the Dynamic Behavior of the Solid Particles (Compressor Off-Design Conditions)

The combined velocity diagrams for the compressor guide vanes and rotor for different blade rotational speeds are shown in Figure 77. The particular case of the rotor angular velocity equal to 0.8

times its design value is termed the negative off-design condition. Likewise, the positive design condition is the case for which  $\omega/\omega_d=1.2$ . Table 1 gives the conditions of gas and particle inlet velocity for the design, negative, and positive off-design conditions. In Table 1,  $\omega/\omega_d$  is the ratio between blade rotational speed at any off-design flow condition and that at design condition, and  $C_{g_i}$  is the gas velocity at the guide vane inlet.

The effect of  $\omega/\omega_d$  on the dynamic behavior of the solid particles having 1000 microns mean diameter for the four typical particles is shown in groups of four figures each, in Figures 78 through 93. Similar groups of figures for  $d_p=200$ , 40 and 8 microns are given in Figures 94 to 109, 110 to 125, and 126 to 141, respectively.

From the above mentioned figures the following observations may be made. The paths of the large particles do not change in the guide vanes with changing  $\omega/\omega_d$  (Figure 78). As the particle mean diameter decreases, slight deviation in the trajectories of particles in the guide vanes is observed (Figure 126). In general, a particle with  $d_D = 1000$  microns would enter a different rotor nozzle if  $\omega/\omega_d$ , is changed, Figure 79. As do decreases the particles tend to enter the same rotor nozzle irrespective of the value of  $\omega/\omega_d$  (Figure 127). radial displacement does not change with  $\omega/\omega_{\tilde{G}}$  in the guide vanes. the rotor, the radial displacement depends to a great extent on particle displacement in the tangential direction, which determines the initial place of collision with the rotor blade (Figures 100 and 104). For particles of all mean diameters, the particle velocity increases more for higher  $\omega/\omega_d$  (Figures 81 and 129). It may be concluded that the change in  $\omega/\omega_d$  causes slight changes in the places of collisions, but the general pattern of the trajectories are maintained. The areas of the blades suffering from erosion damage will remain the same as in the design conditions.

#### CONCLUSION

The three dimensional dynamic behavior of solid particles entrained by the compressible gas flow in a one and one-half stage of a compressor is determined. The drag forces on the particles are calculated using drag formulas that fit the drag curve of a spherical particle over the practical range of application of the Reynolds numbers. The compressible gas flow properties are computed by solving numerically the gas equations of motion in a blade to blade surface of revolution of a rotating cascade. Experimental investigation is made to study the impact and rebound phenomenon of the particles from the walls, to determine formulas for the restitution ratio, and rebound to incidence angle ratio. These formulas define the particle conditions after collision which are then used to continue the solution of the equations of motion for the particles. These formulas have to be determined experimentally for every particle-target material combination once the turbomachine operating condition is known.

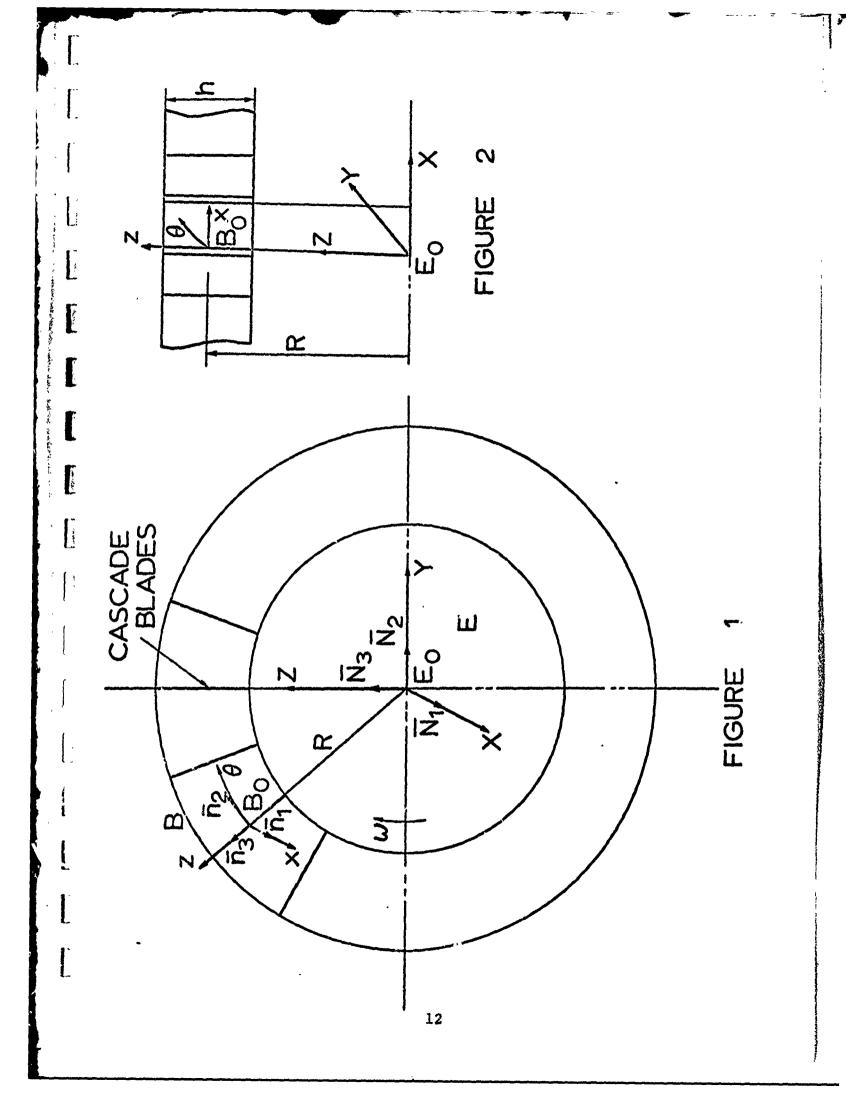
The study showed that in general, solid particle paths are deviated from gas streamlines. This deviation increases with increased particle mean diameter, material density, particle initial velocity or decreased initial gas velocity. The particle mean diameter has the greatest effect on the dynamic behavior of the particles, while the particle material density has a lesser effect and the particle initial velocity has the least effect. Changing rotational speed of the cascade does not effect either the patterns of the trajectories of the particles or the cascade eroded parts.

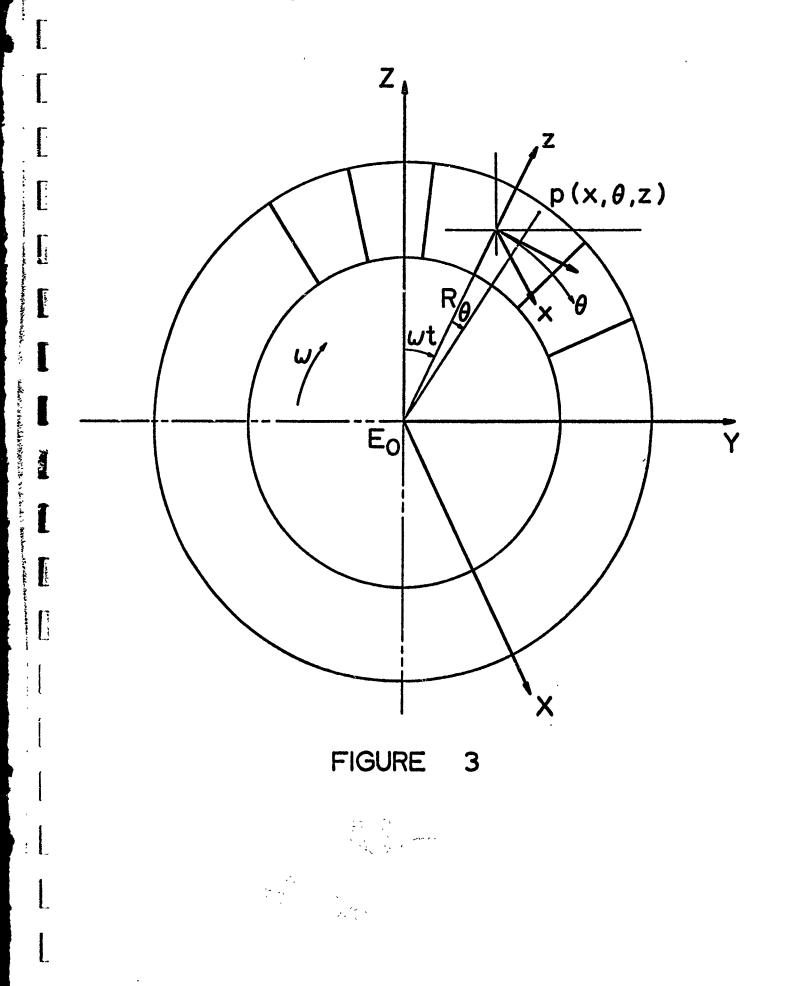
The compressor stator and rotor will be eroded from the leading edges and pressure sides, especially due to impacts of bigger particles. The study shows that particles tend to displace radially, especially in the rotors, as they move through the compressor. After a few stages the particles will be moving at the tip stream surface of revolution causing severe damage to blade tips and less erosion to blade sections further from the tips.

Turbomachines may be designed to both minimize erosion as well as optimizing aerodynamic characteristics using the results of this investigation. Means may be introduced to collect or deviate some of the particles, especially those that contribute most to erosion, away from the blades, and hence, reduce their erosion damage.

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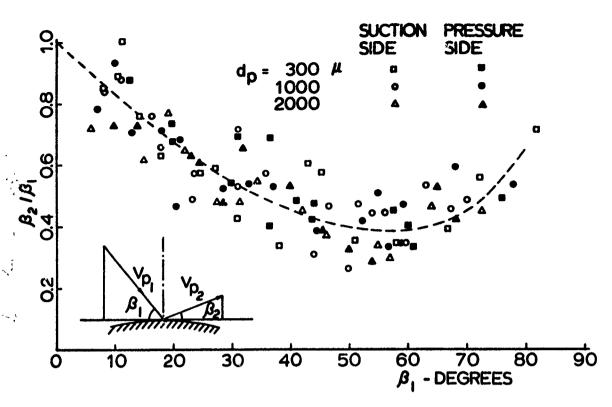


FIG. 4 NONDIMENSIONAL ANGLE OF REBOUND

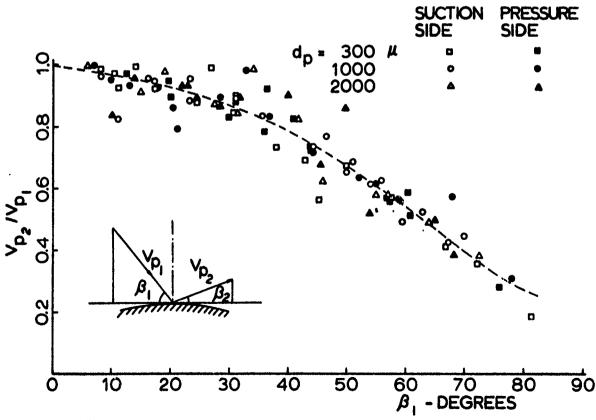


FIG. 5 DROP IN PARTICLE RELATIVE VELOCITY DUE TO COLLISION (RESTITUTION RATIO)

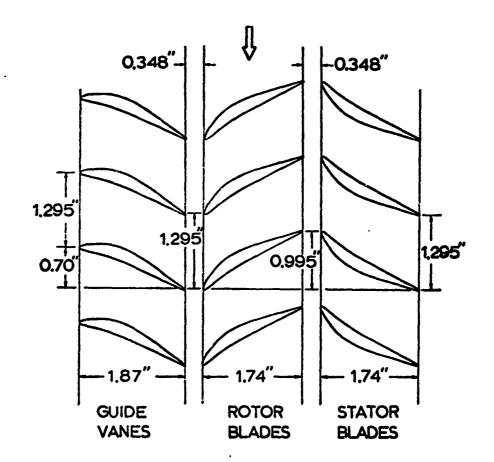


FIGURE 6 COMPRESSOR STAGE DIMENSIONS

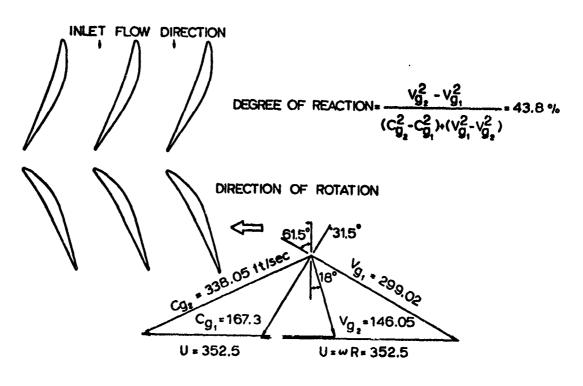
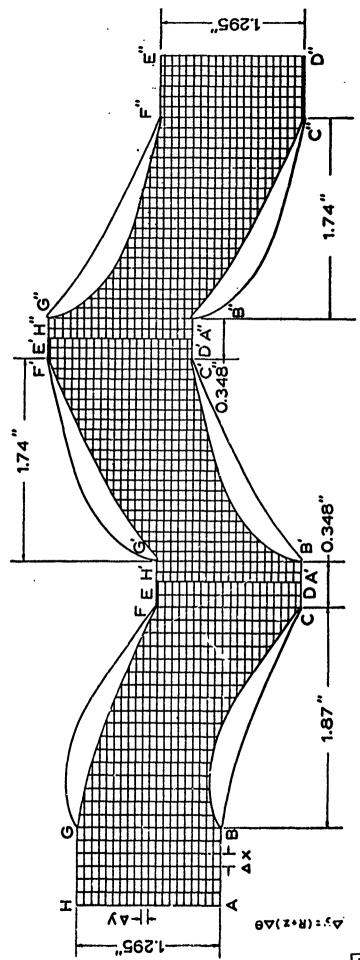
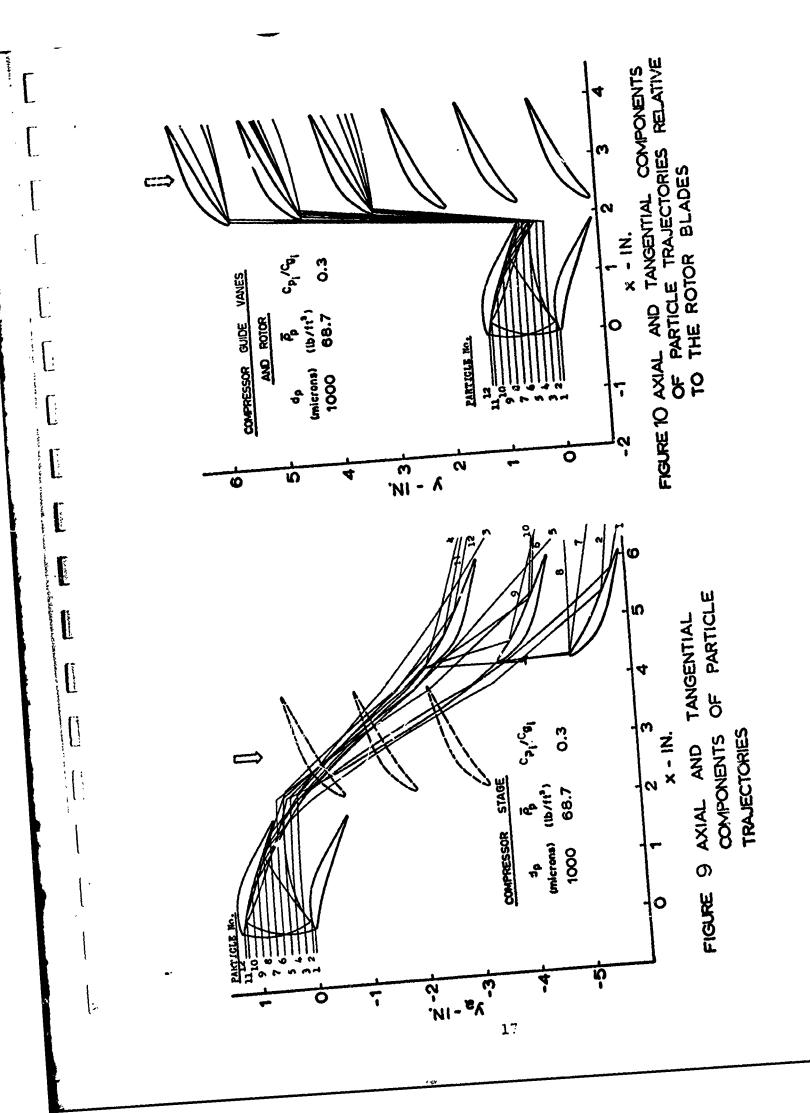


FIGURE 7 COMBINED GAS VELOCITY DIAGRAM (COMPRESSOR STAGE)





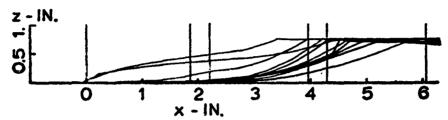


FIGURE 11 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

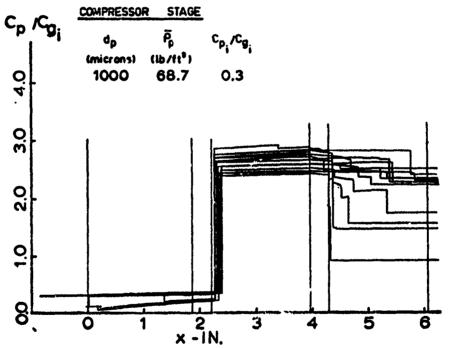
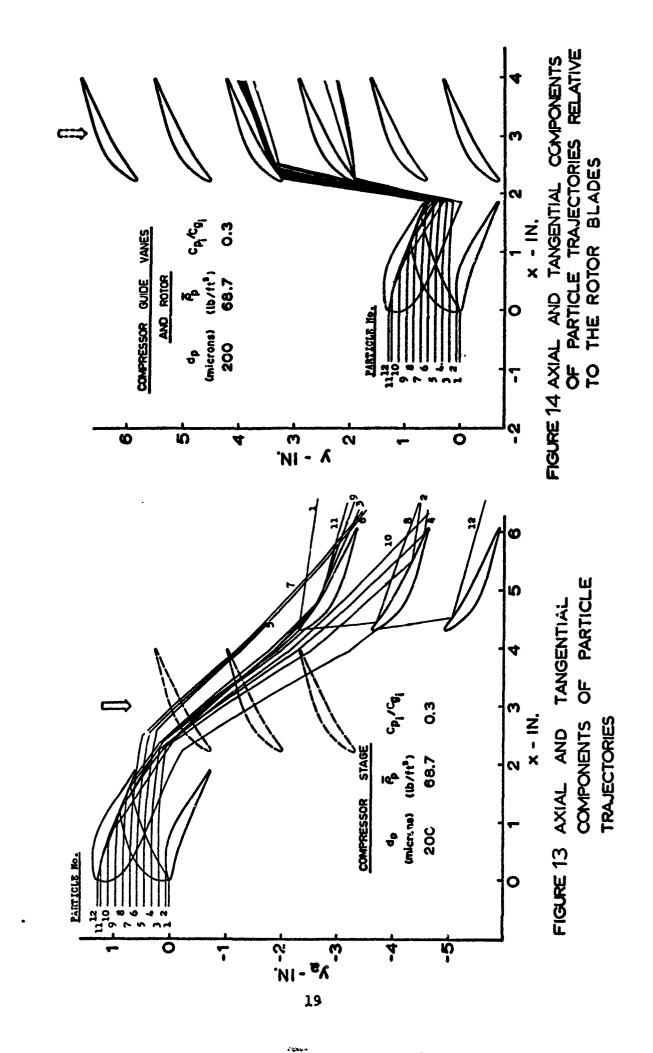


FIGURE 12 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES



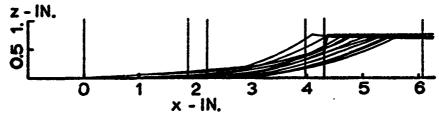


FIGURE 15 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

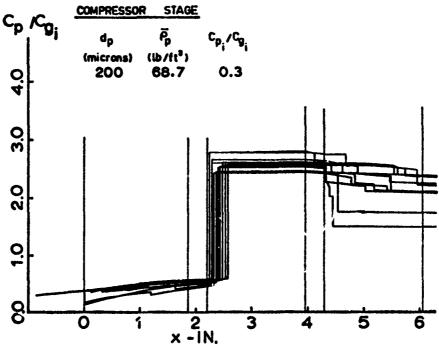


FIGURE 16 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES

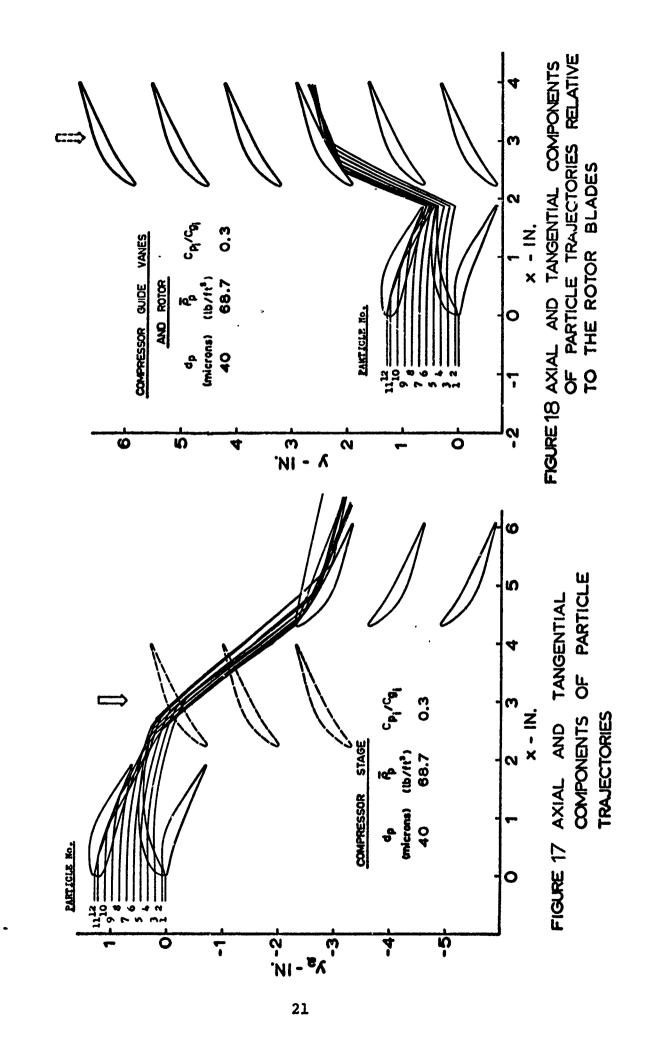


FIGURE 19 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

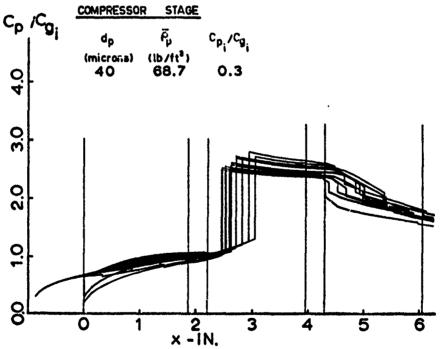
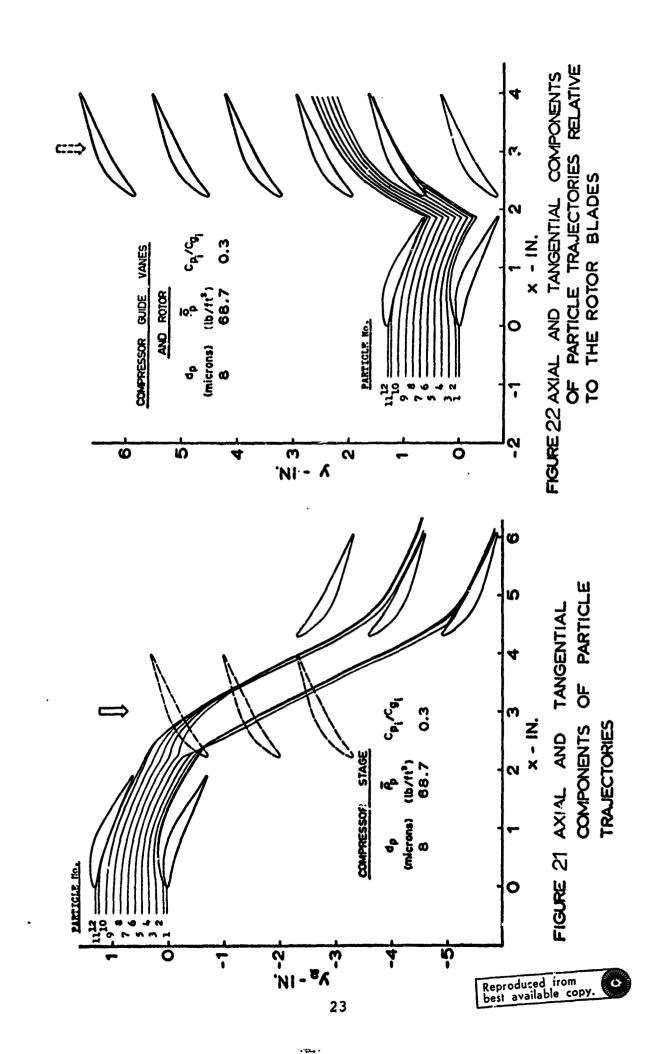


FIGURE 20 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES



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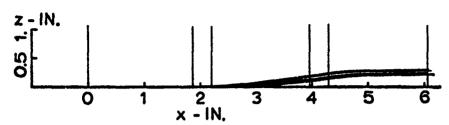


FIGURE 23 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

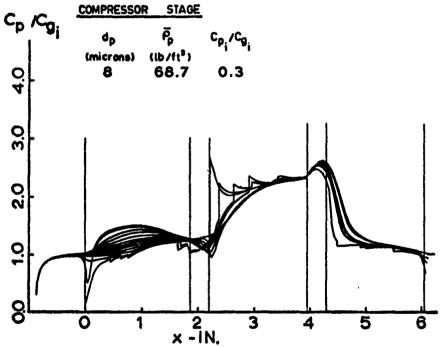
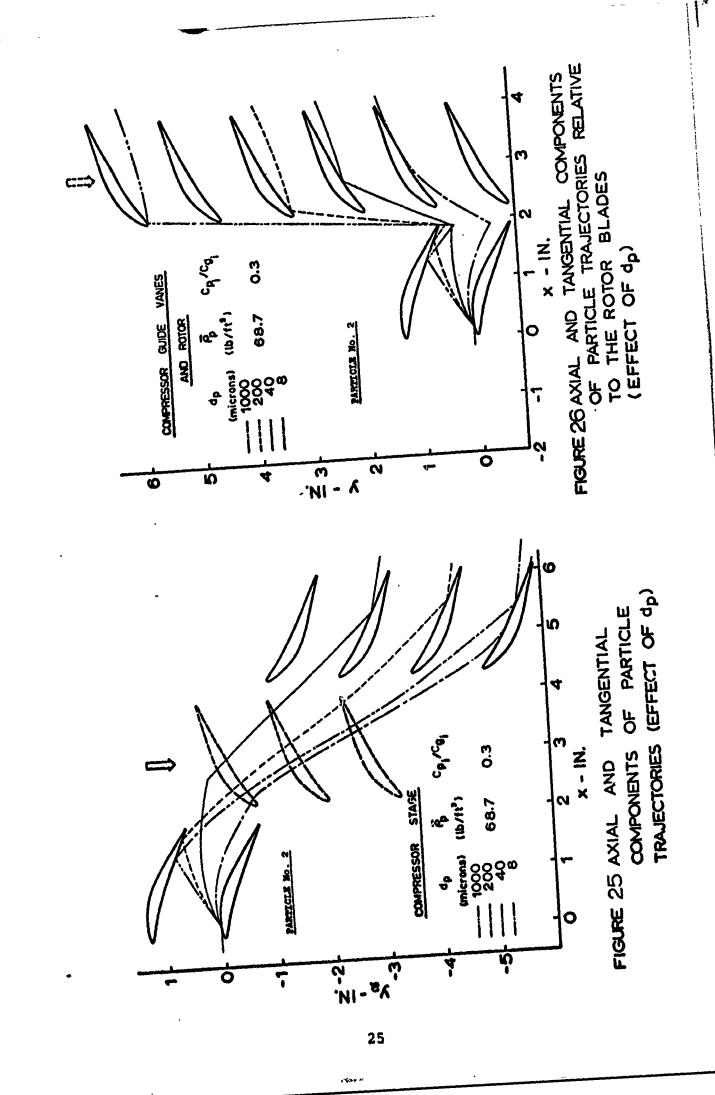
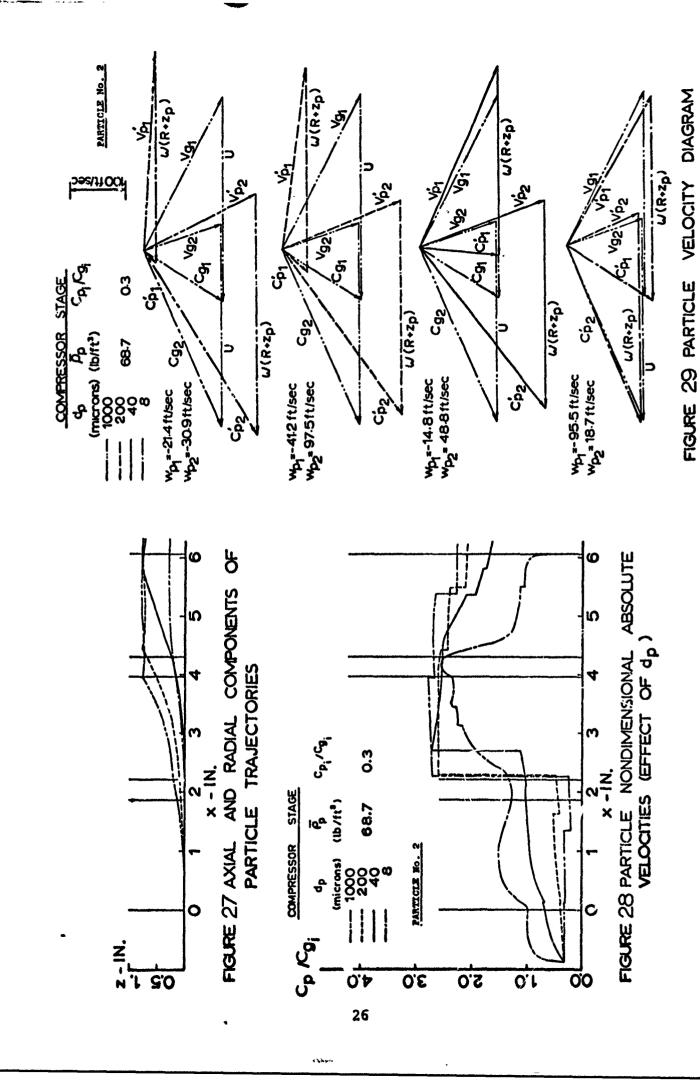
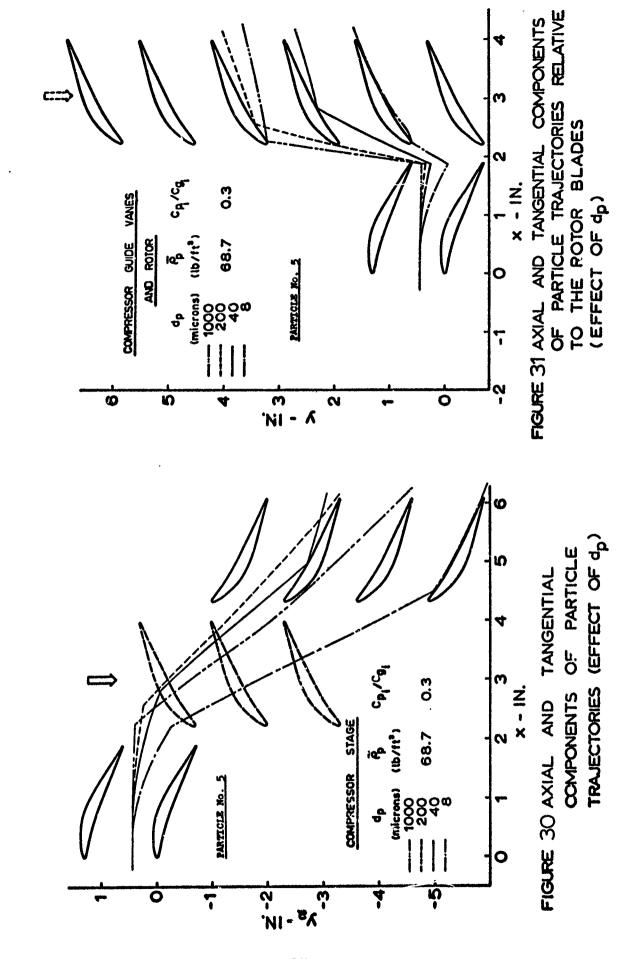


FIGURE 24 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES





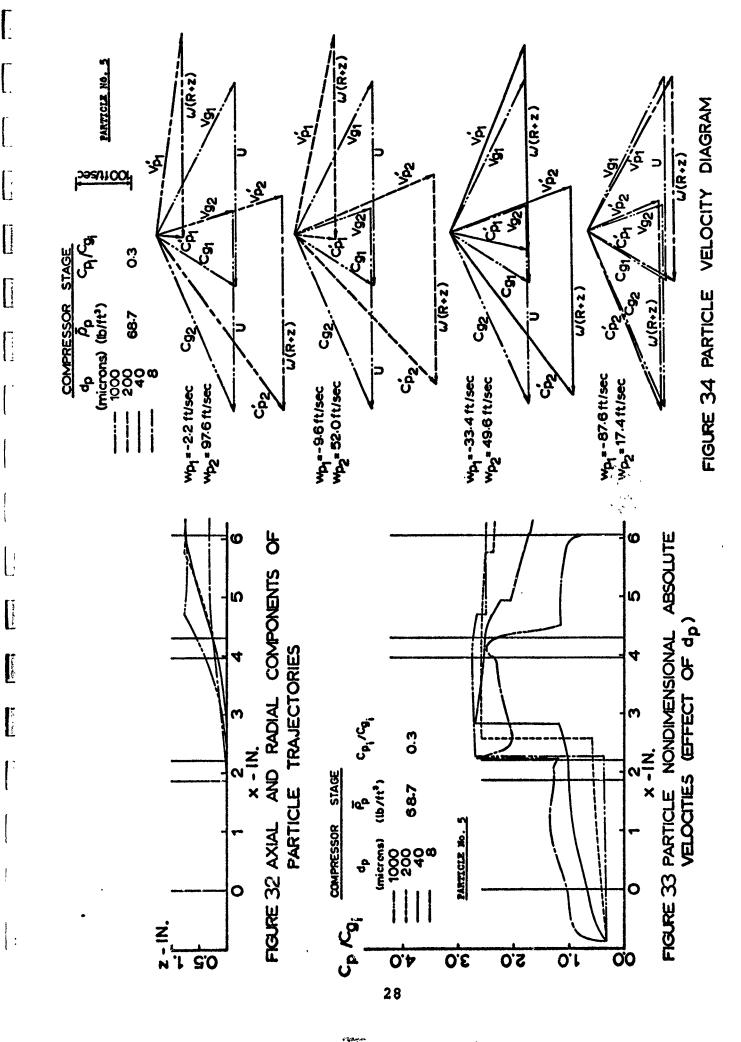
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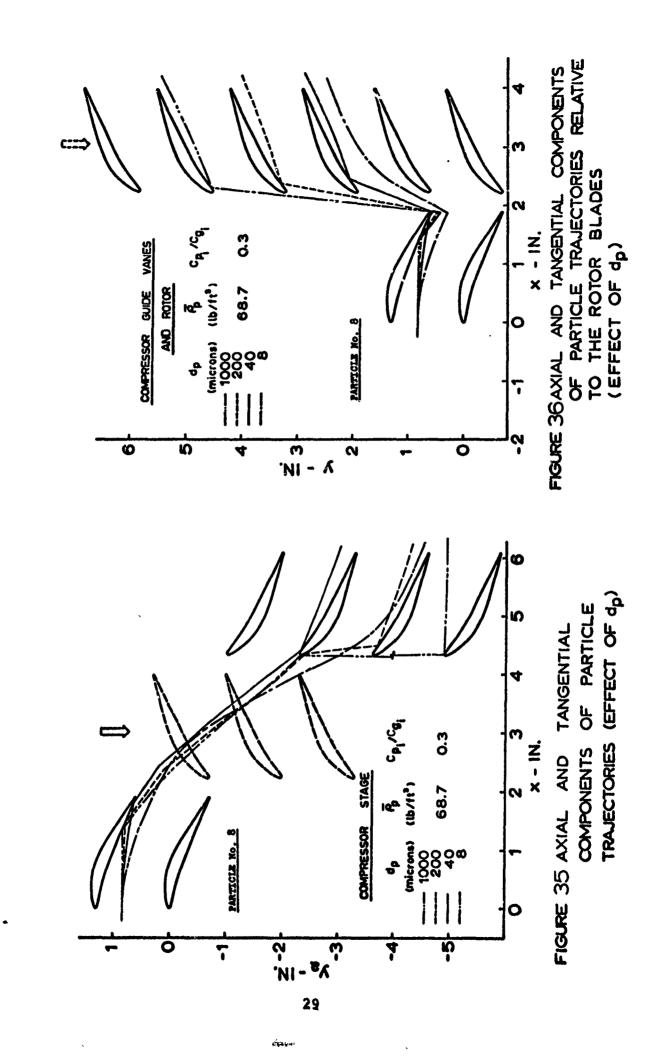


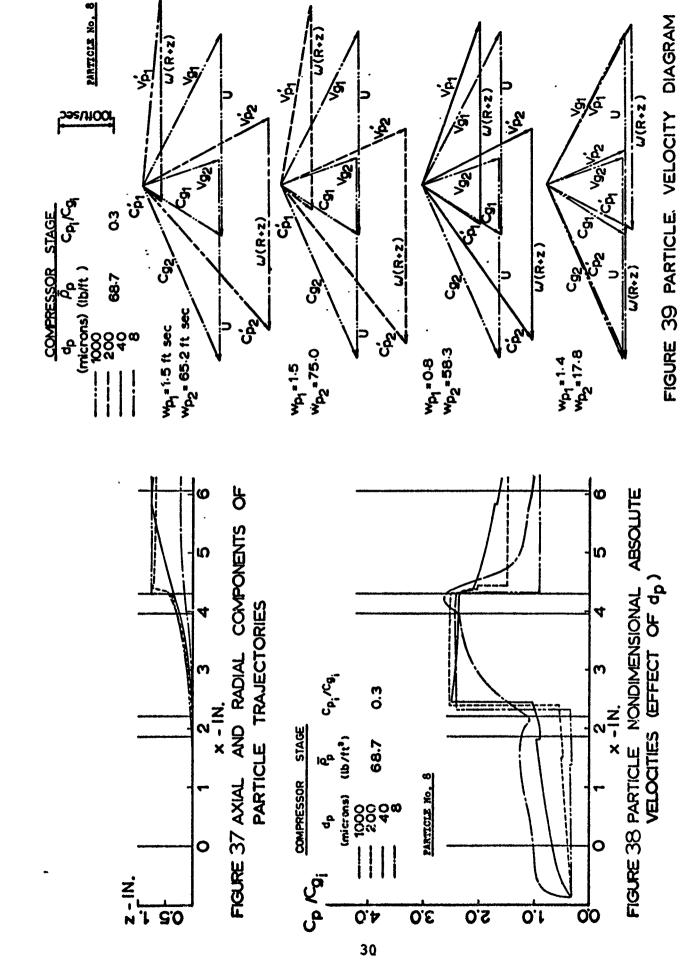
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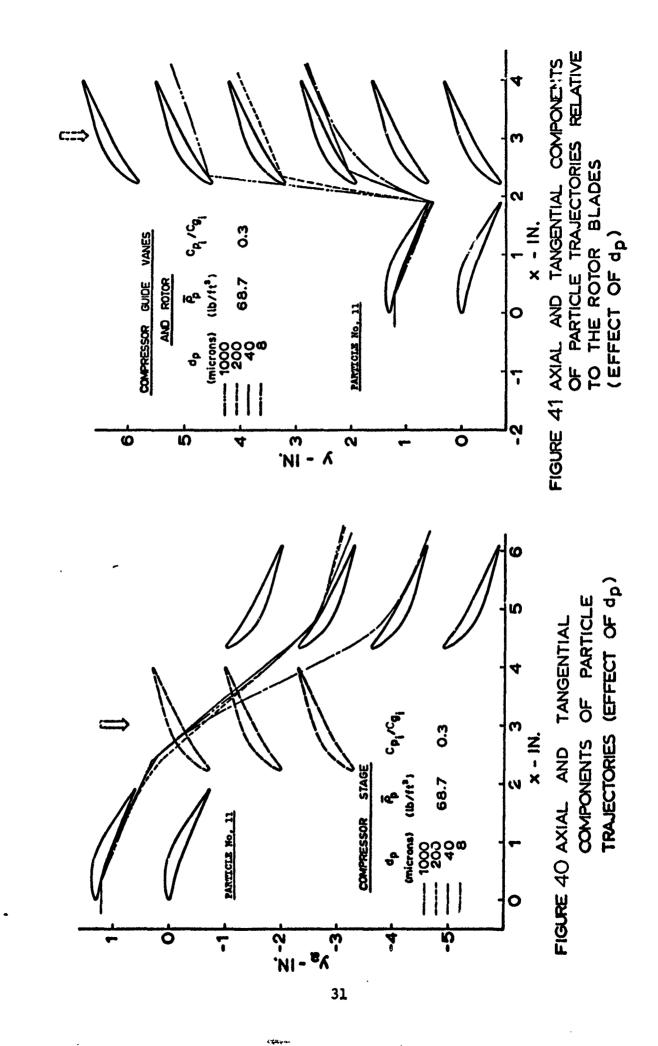
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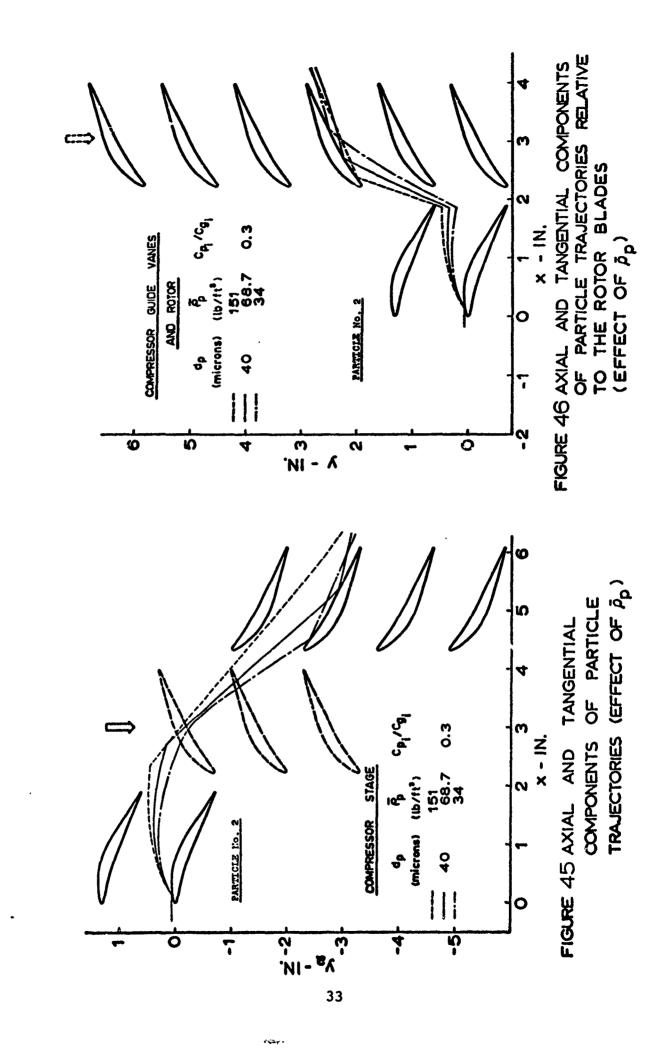


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FIGURE 44 PARTICLE VELOCITY DIAGRAM

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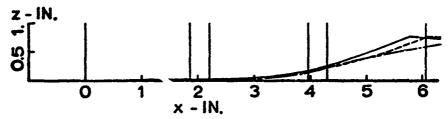


FIGURE 47 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

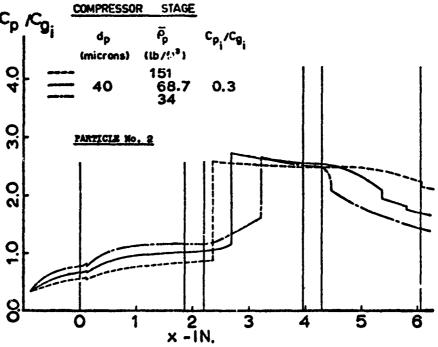
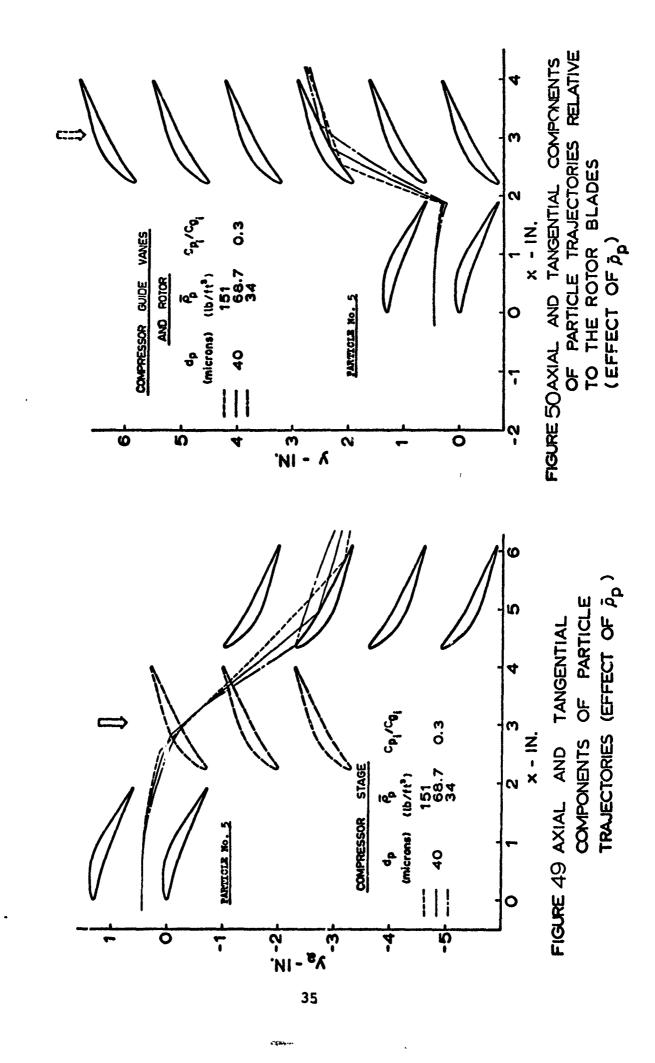


FIGURE 48 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\bar{\rho}_{\mathrm{D}}$ )

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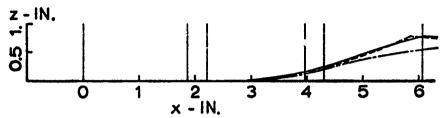


FIGURE 51 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

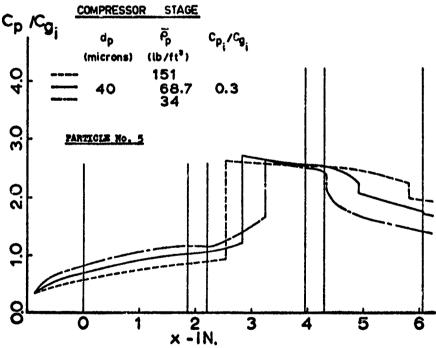


FIGURE 52 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF \$\bar{\rho}\_{\bar{\rho}}\$)

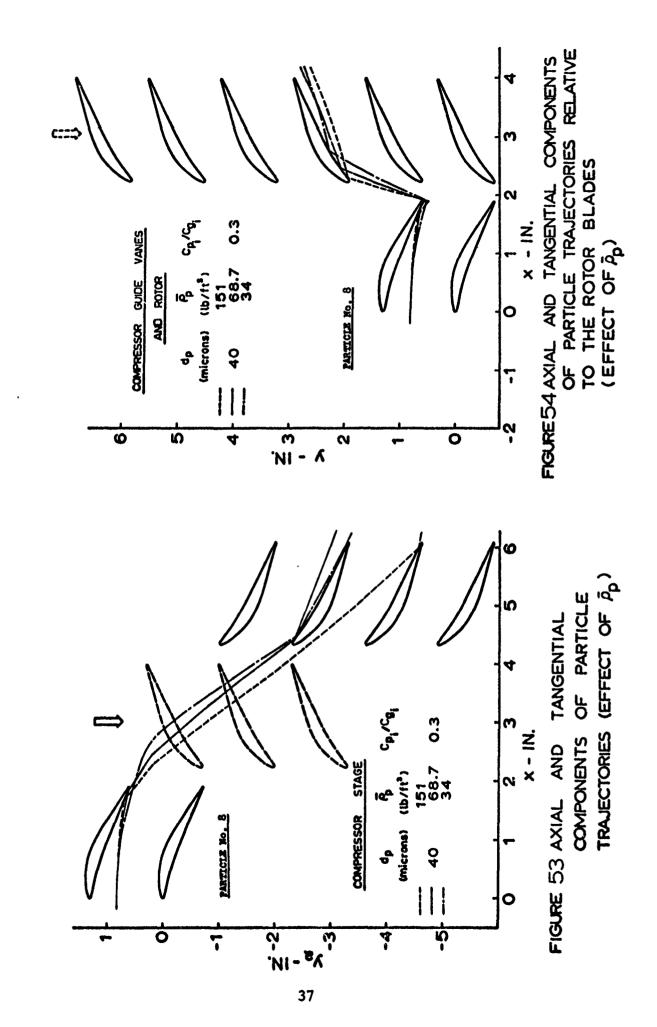




FIGURE 55 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

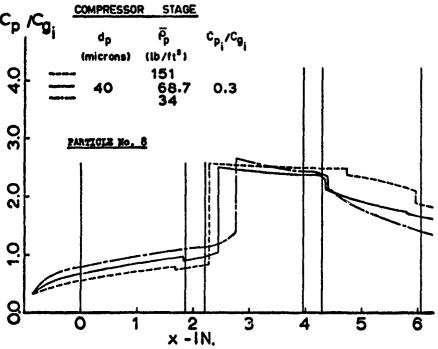


FIGURE 56 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\vec{\rho}_{p}$ )

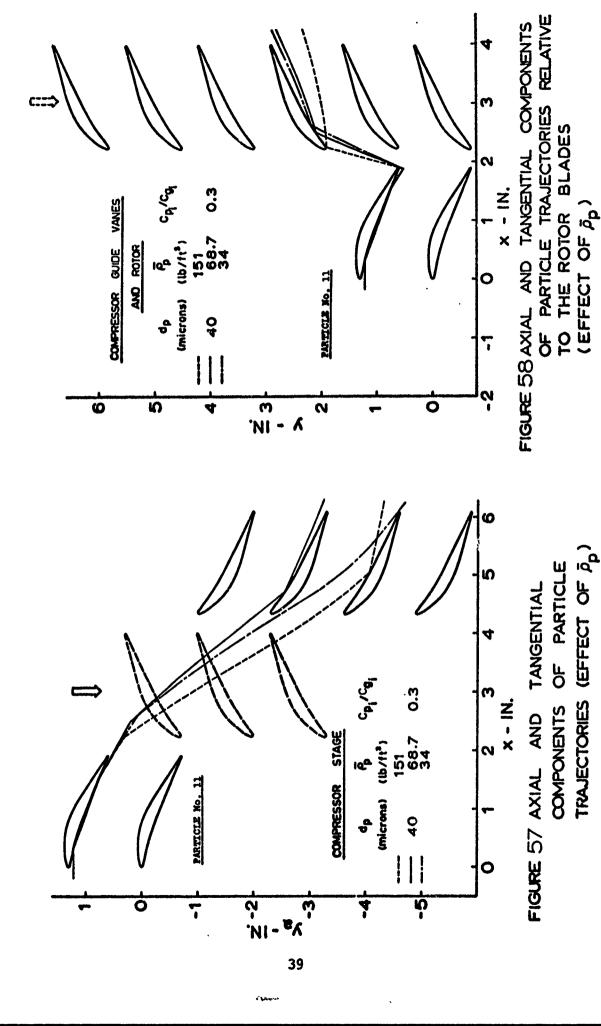




FIGURE 59 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

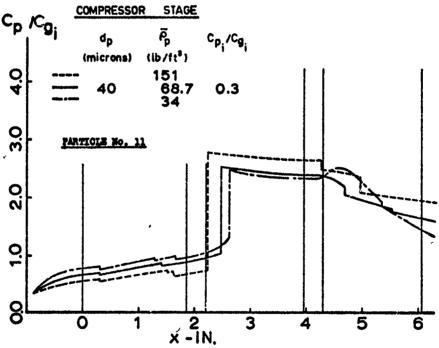
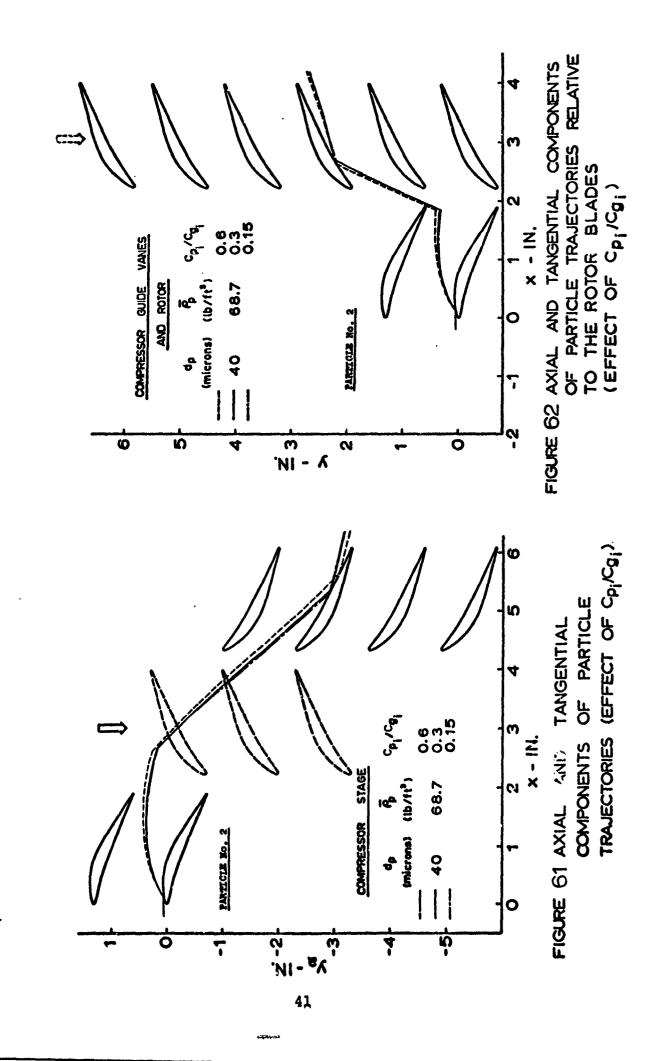


FIGURE 60 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\overline{\rho}_{p}$ )



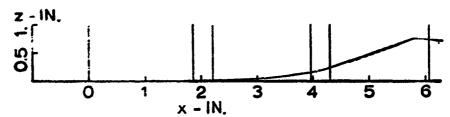


FIGURE 63 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

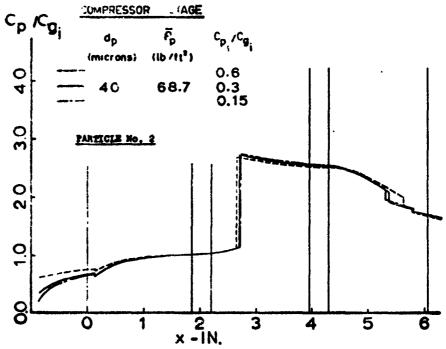
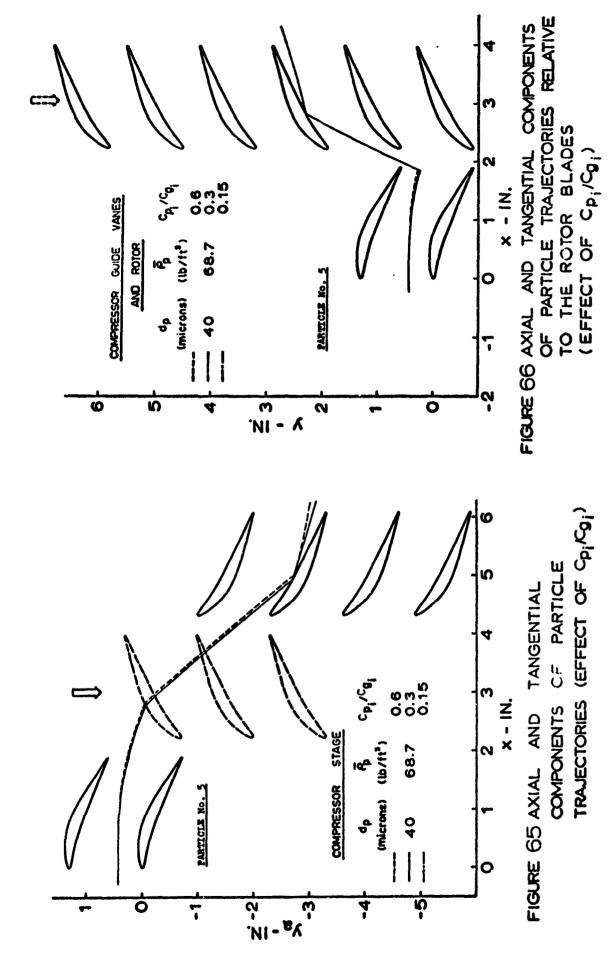


FIGURE 64 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF Cp;/Cg;)



and the

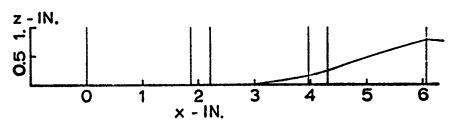


FIGURE 67 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

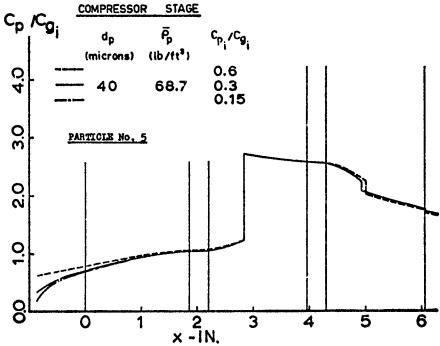
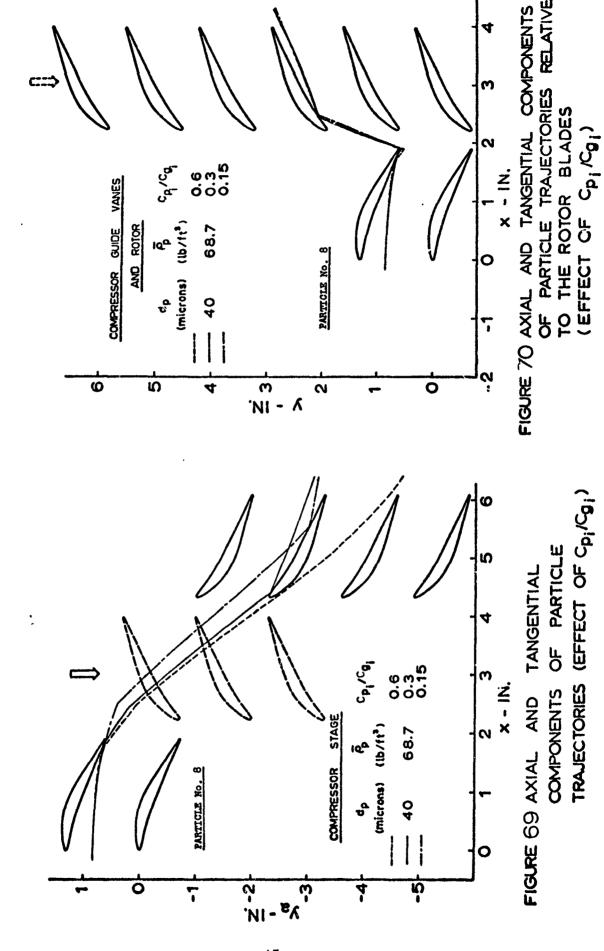


FIGURE 68 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF Cp, Cg,)



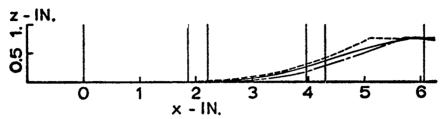


FIGURE 71 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

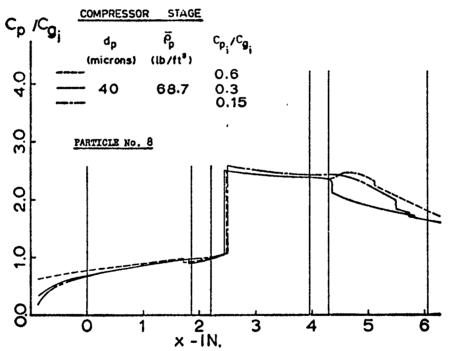
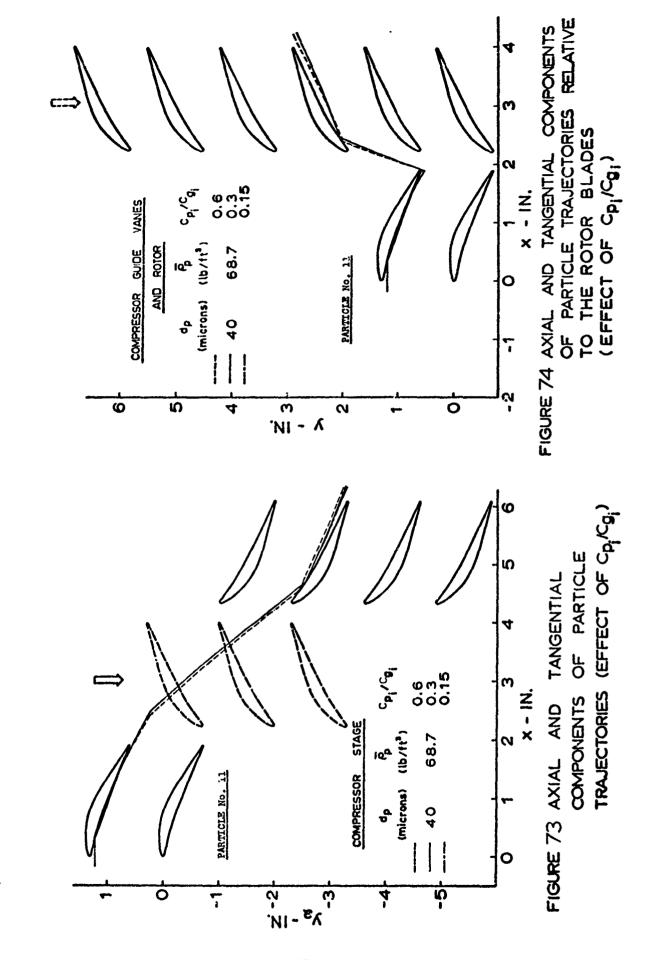


FIGURE 72 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $C_{p_i}/C_{g_i}$ )



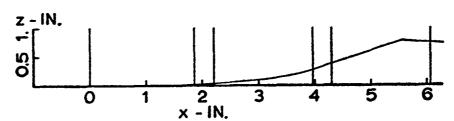


FIGURE 75 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

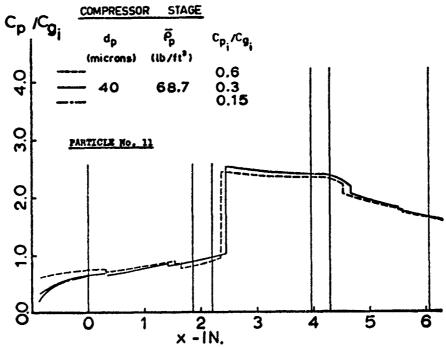


FIGURE 76 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF Cp;/Cg;)

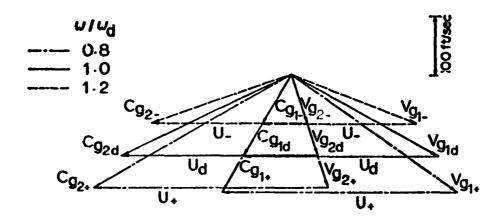
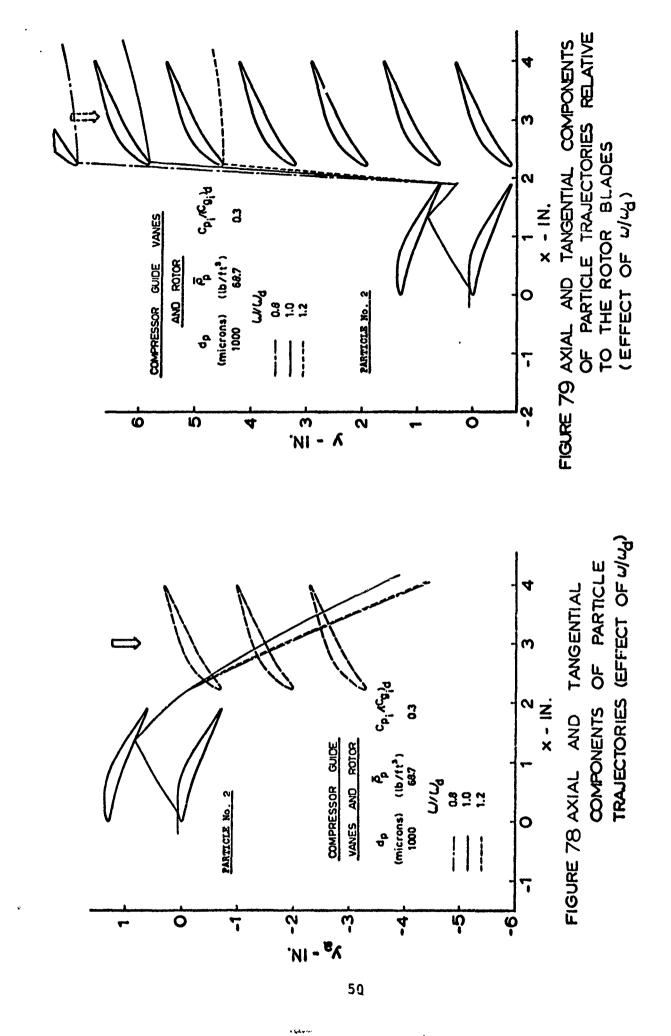


FIGURE 77 COMBINED GAS VELOCITY DIAGRAM FOR DESIGN AND OFF DESIGN BLADE ANGULAR VELOCITY (COMPRESSOR STAGE)

	NEGATIVE OFF- DESIGN CONDITION	DESIGN CONDITION	POSITIVE OFF - DESIGN CONDITION
ω (radiance/sec)	482.8	603.5	724.2
ωιω <sub>d</sub>	0.8	1.0	1.2
Cg <sub>i</sub> (ft/sec)	114.11	142-64	171 - 17
ρ <sub>gi</sub> (lb/ft <sup>3</sup> )	0.076	0.076	0.076
W; (lb/sec/channel)	0.074	0.123	0-172
c <sub>pi</sub> /c <sub>gi</sub>	0.3	0.3	0.3
Cp <sub>i</sub> (1t/sec)	34.2	42.8	51.4

TABLE 1



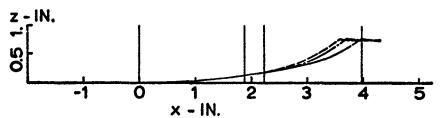


FIGURE 80 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

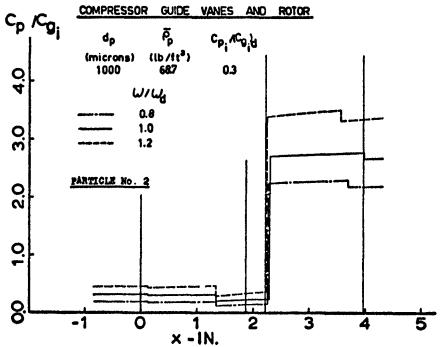
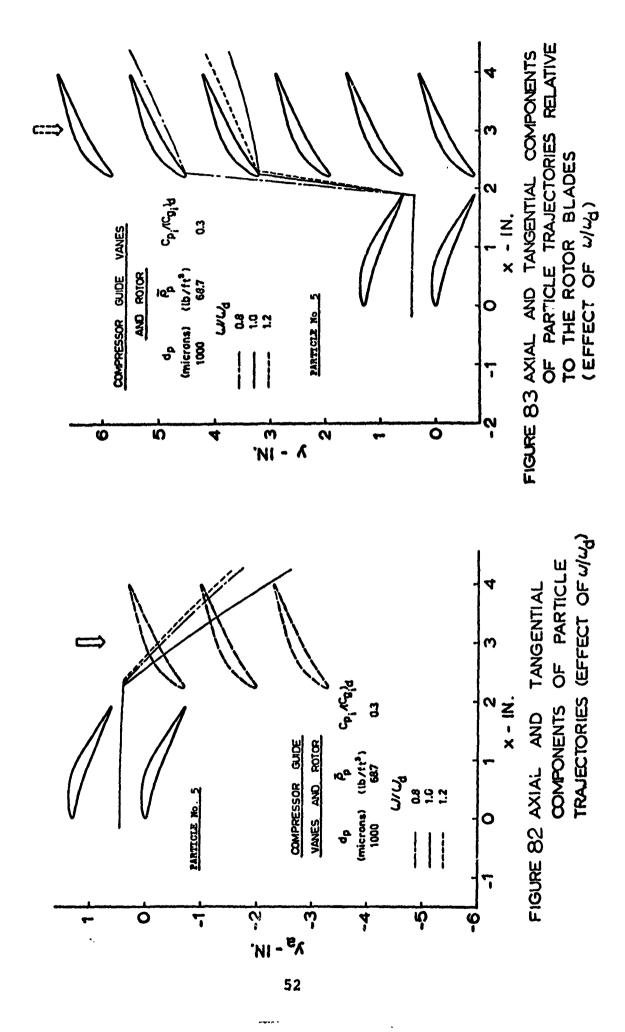


FIGURE 81 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF \(\omega/\omega\_{\text{d}}\))



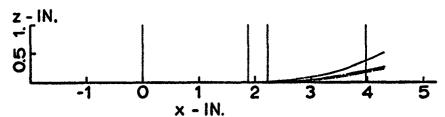


FIGURE 84 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

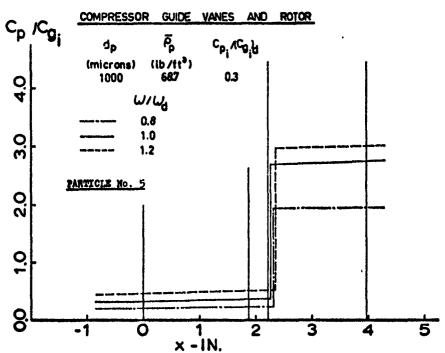
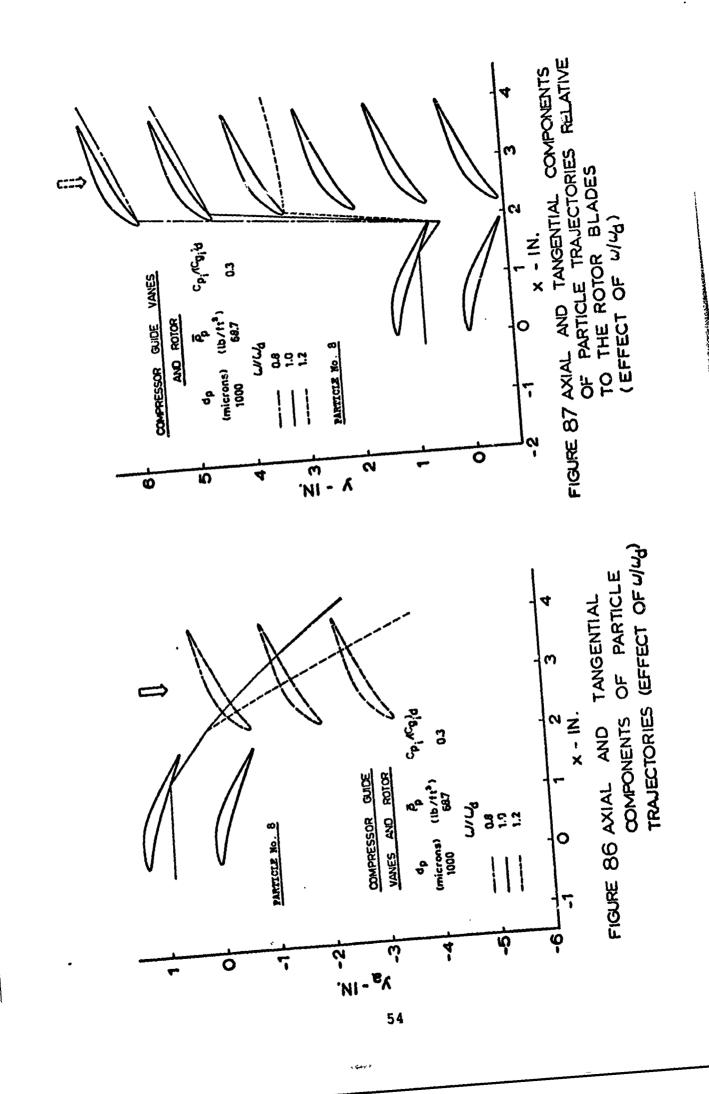


FIGURE 85 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_{\rm d}$ )



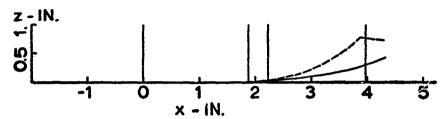


FIGURE 88 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

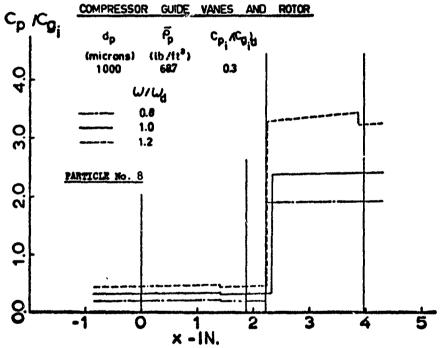
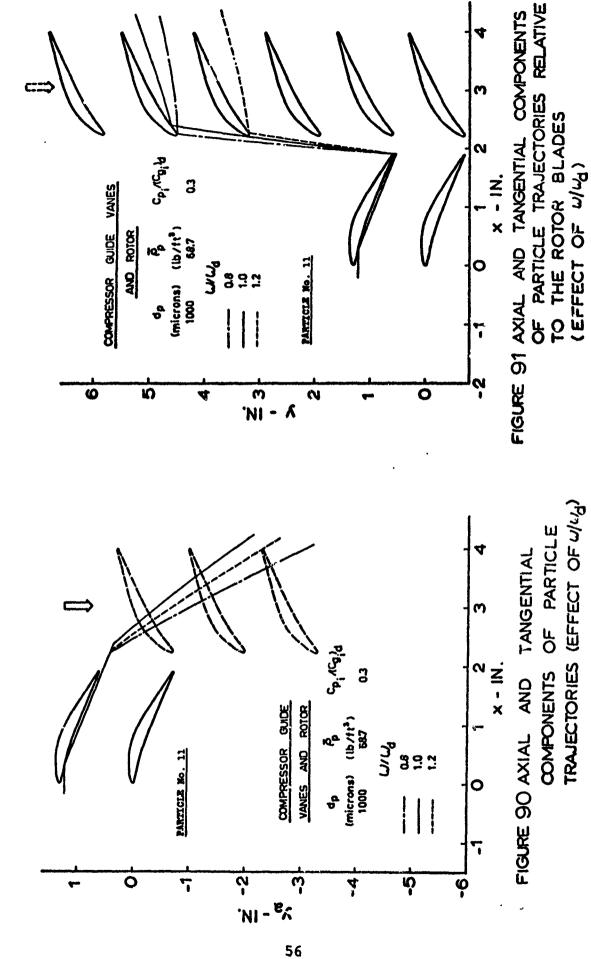


FIGURE 89 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_{\rm d}$ )



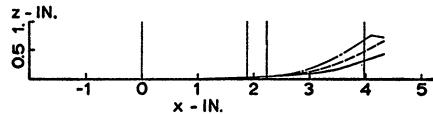


FIGURE 92 AXIAL. AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

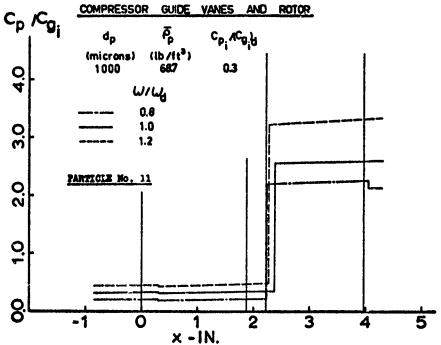
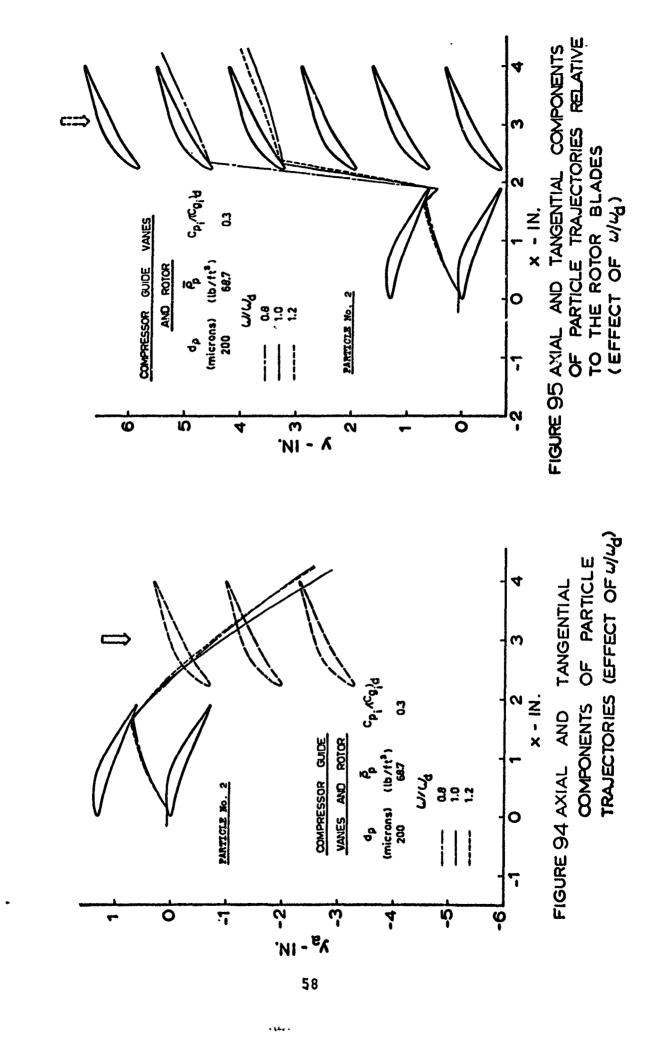


FIGURE 93 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_{\rm d}$ )



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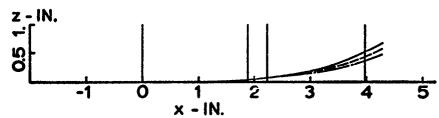


FIGURE 96 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

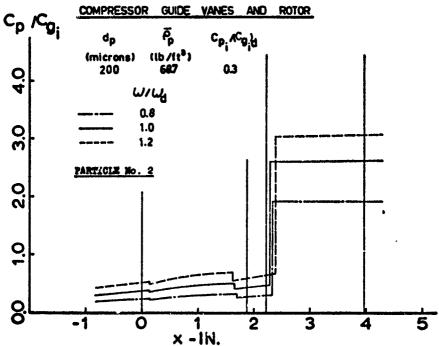
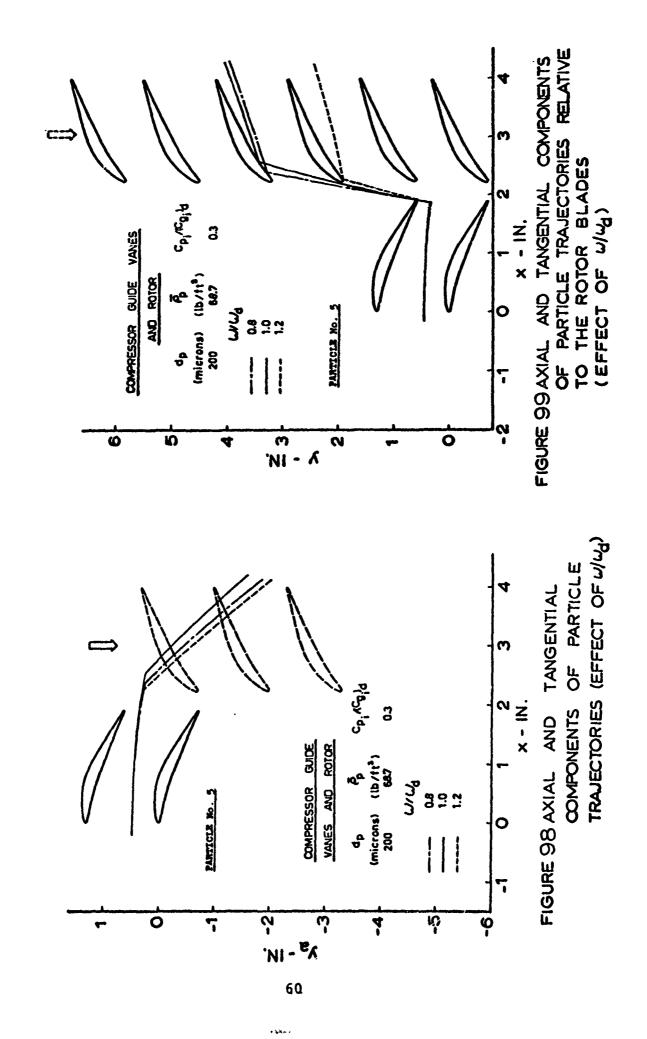


FIGURE 97 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $^{\prime\prime\prime}\omega_{\rm d}$ )



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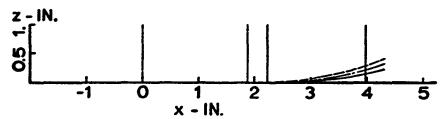


FIGURE 100 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

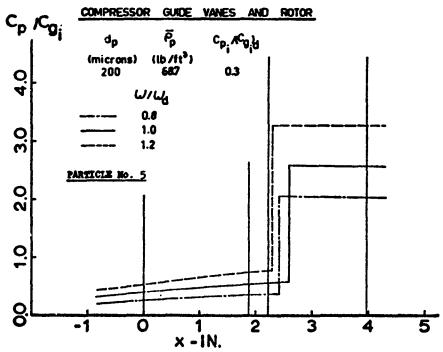
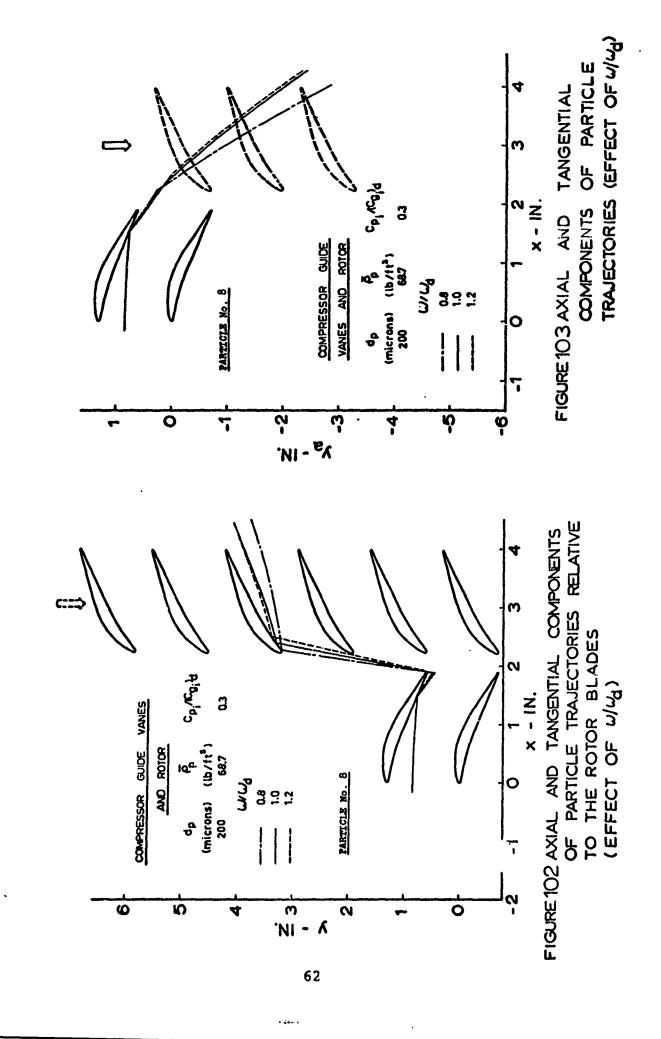


FIGURE 101 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_{\rm d}$ )



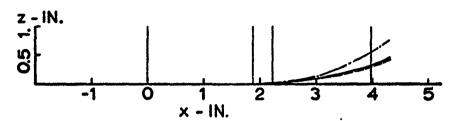


FIGURE 104AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

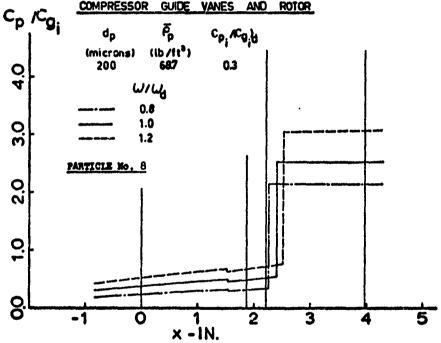
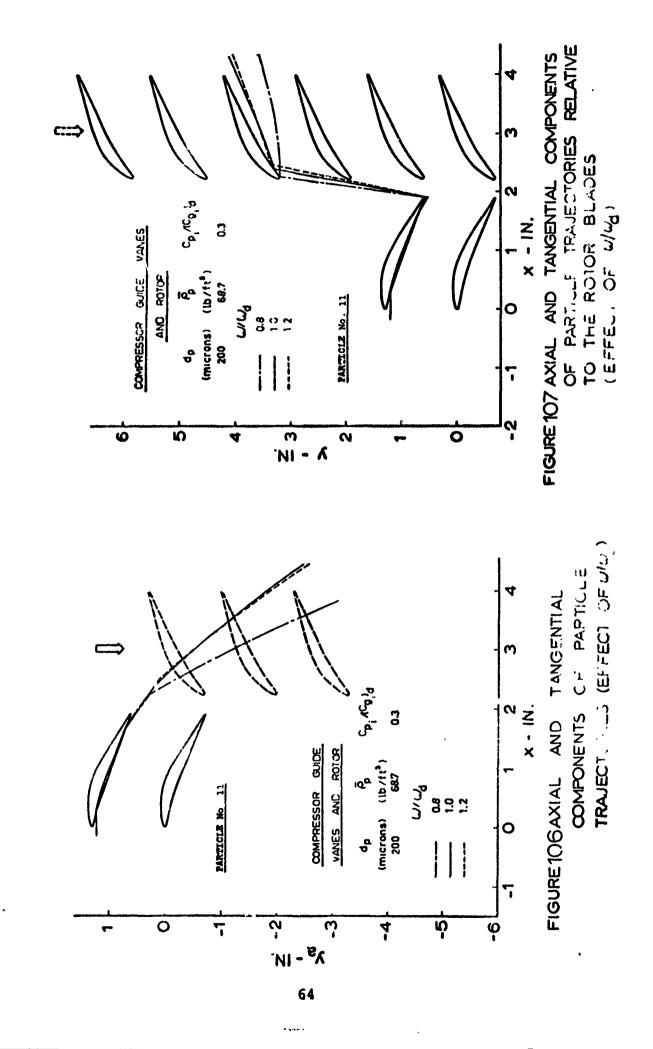


FIGURE 105 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $w/w_{\rm d}$ )



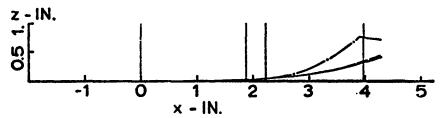


FIGURE 108AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

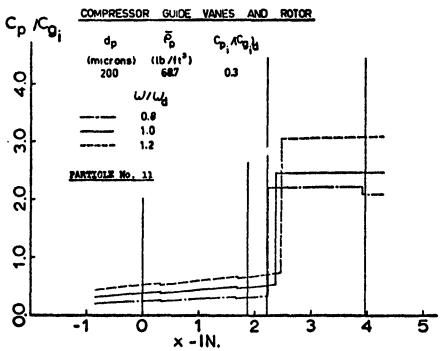
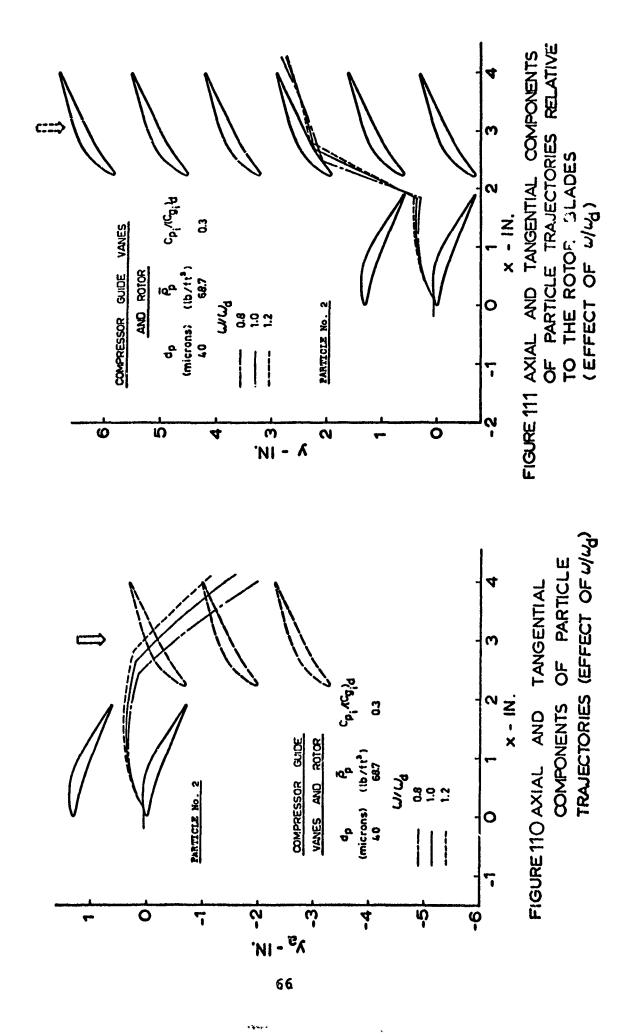


FIGURE 109 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_{\rm d}$ )



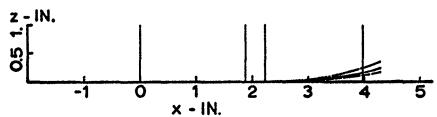


FIGURE 112 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

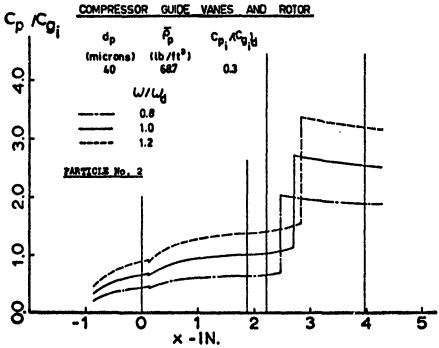


FIGURE 113 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_{\rm d}$ )

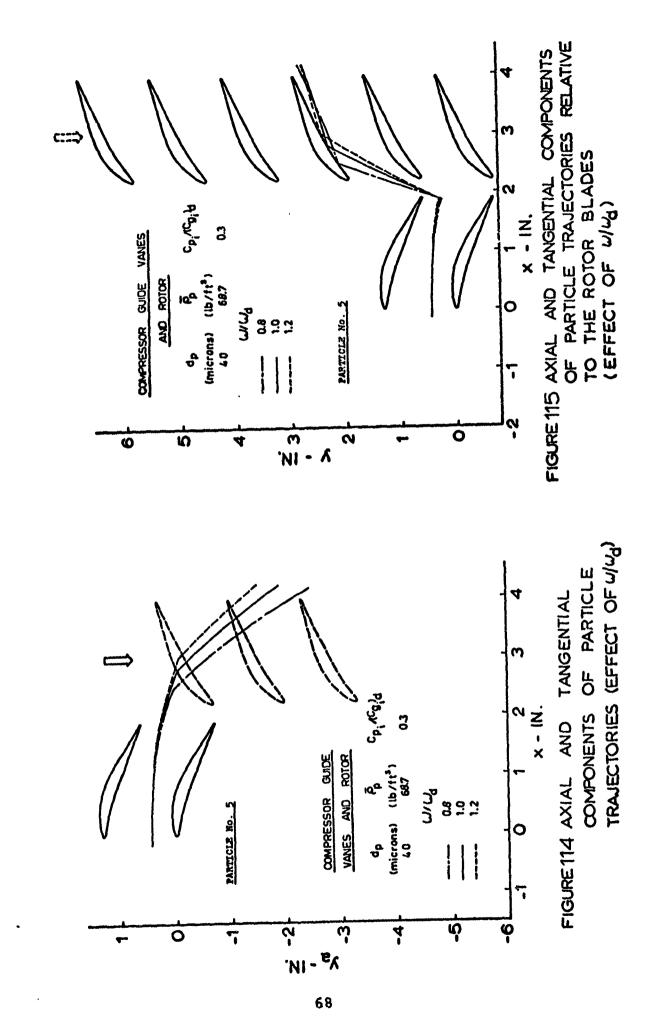




FIGURE 116 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

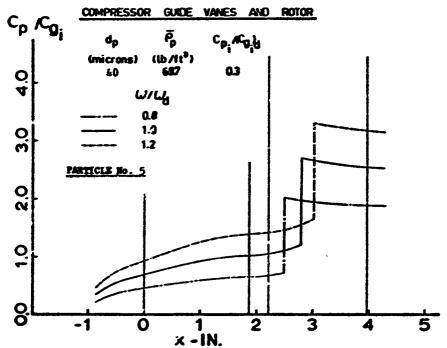
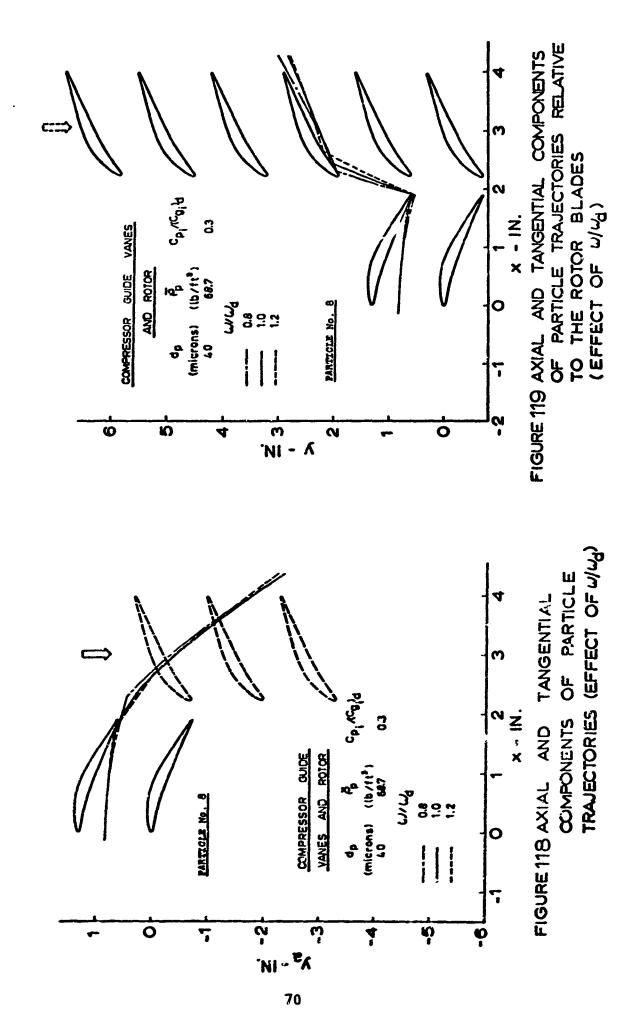


FIGURE 117 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (FFFECT OF  $\omega/\omega_{\rm d}$ )



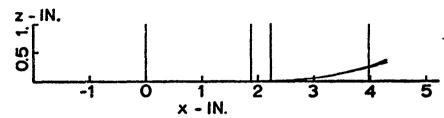


FIGURE 120 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

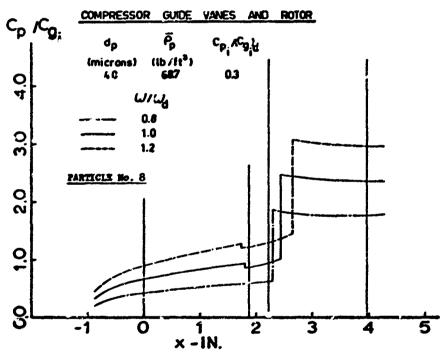
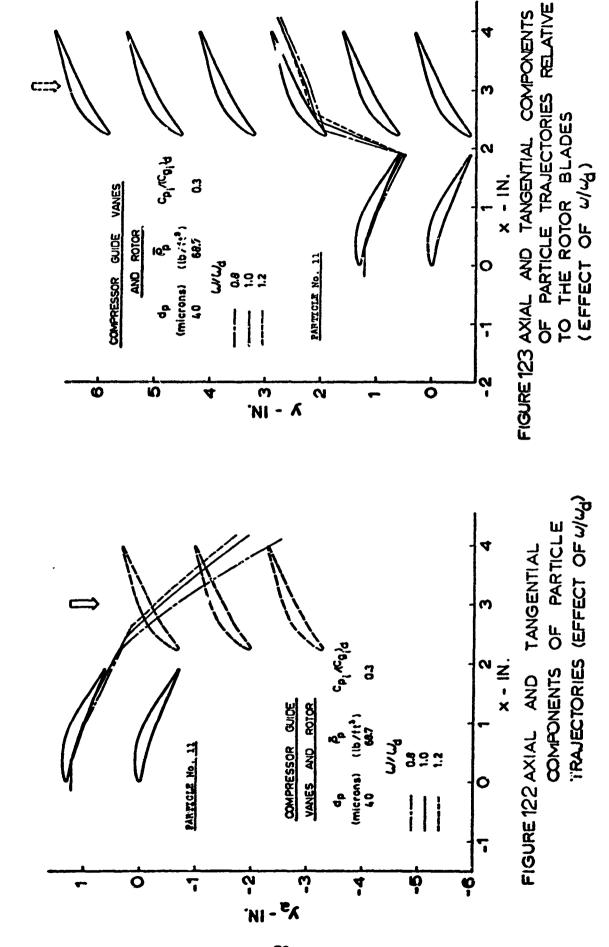


FIGURE 121 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_{\rm d}$ )



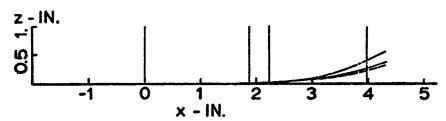


FIGURE 124 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

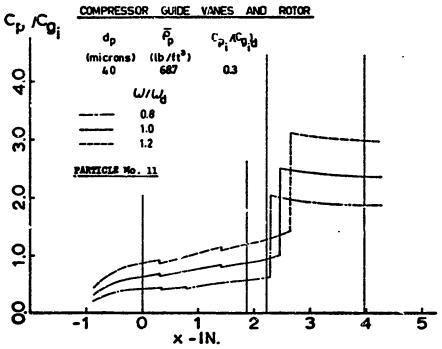
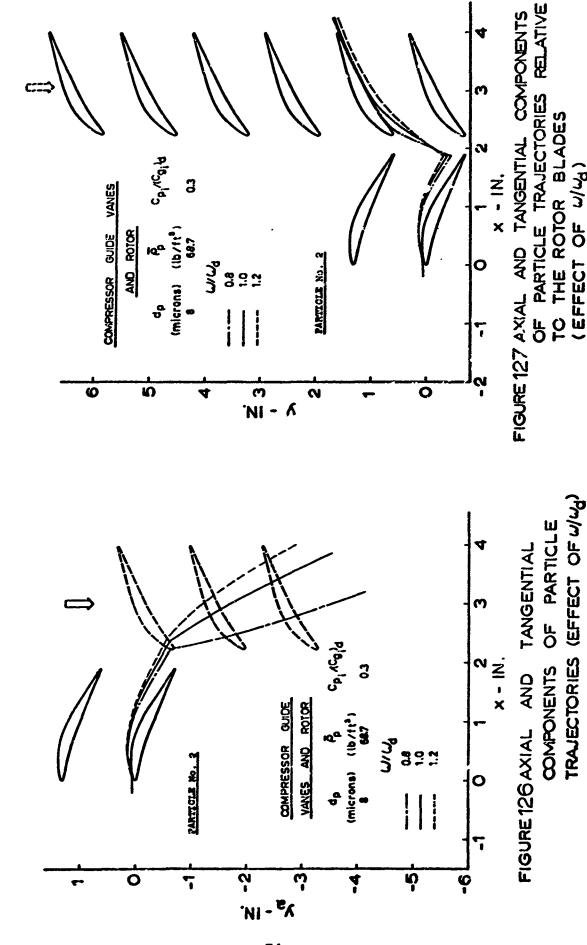


FIGURE 125 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_{\rm d}$ )



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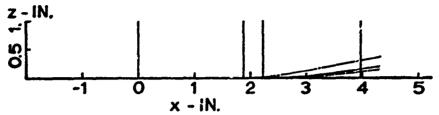


FIGURE 128 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

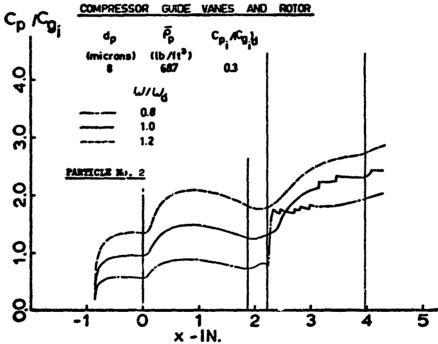
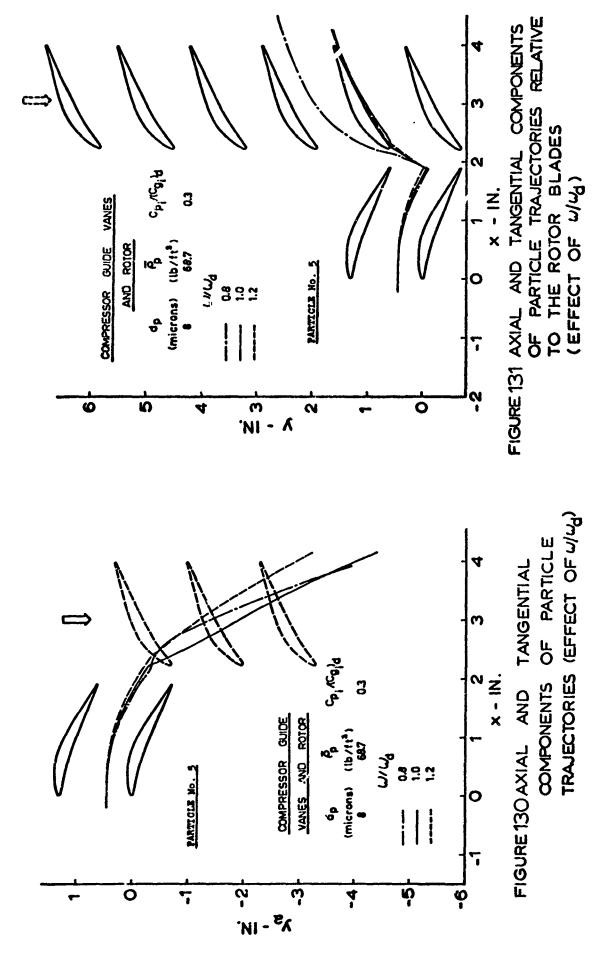


FIGURE 129 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF U/Ud)



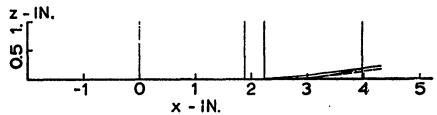


FIGURE 132 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

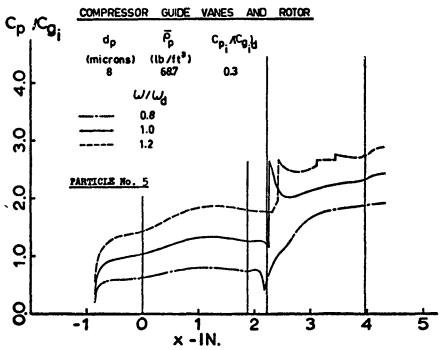
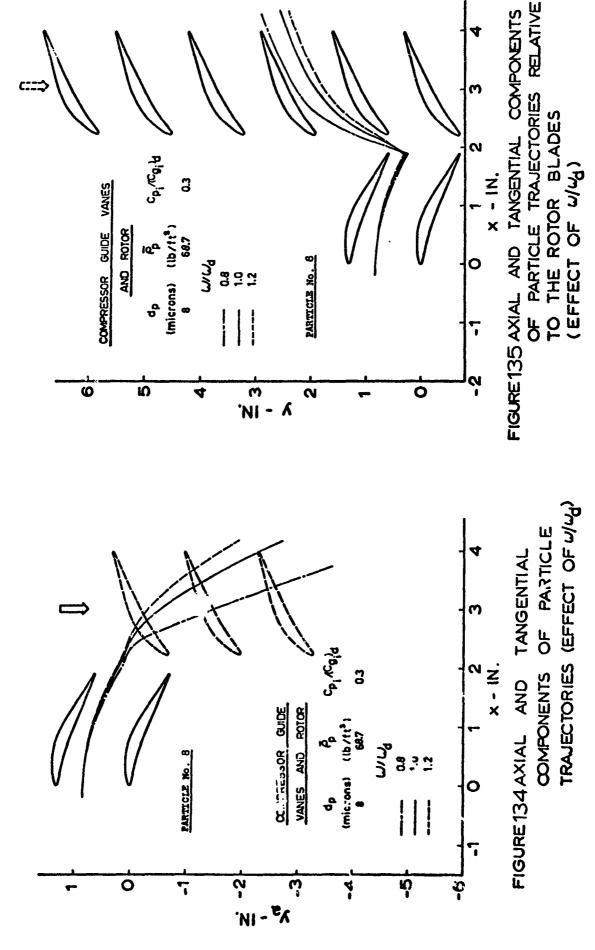


FIGURE 133 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_{\rm d}$ )



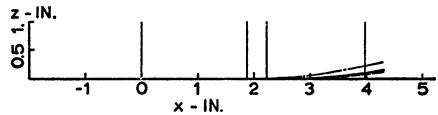


FIGURE 136 AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

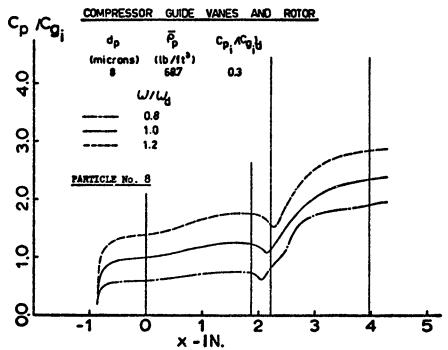
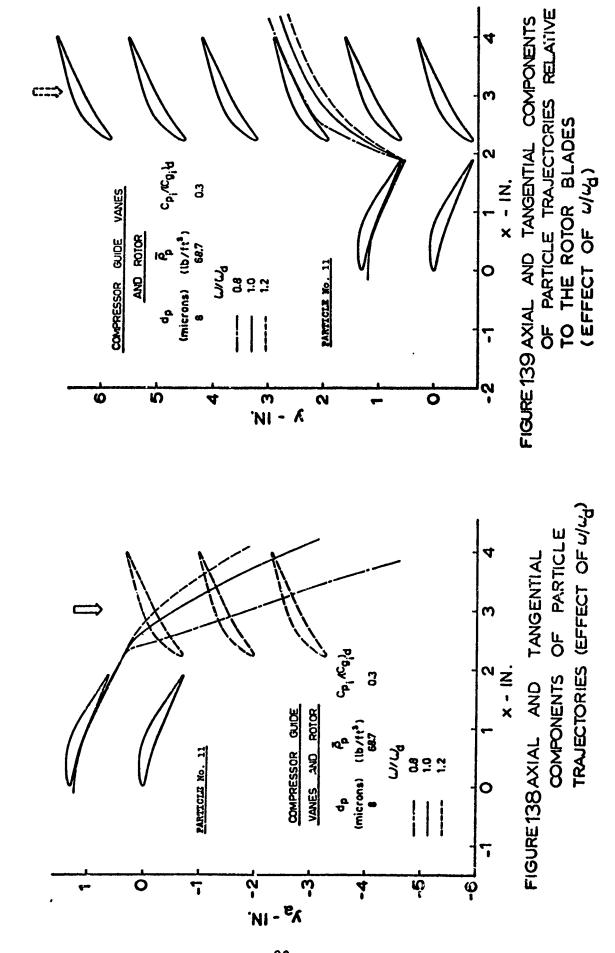


FIGURE 137 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_d$ )



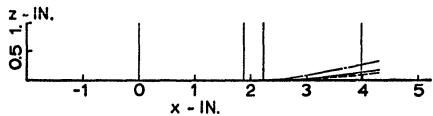


FIGURE 140.AXIAL AND RADIAL COMPONENTS OF PARTICLE TRAJECTORIES

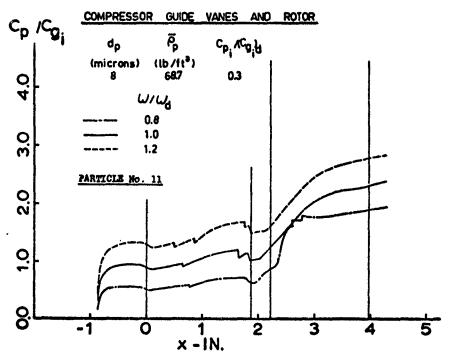


FIGURE 141 PARTICLE NONDIMENSIONAL ABSOLUTE VELOCITIES (EFFECT OF  $\omega/\omega_{\rm d}$ )