

AD 741570

# THE CONTROL OF OXIDES AND NITROGEN EMISSIONS FROM AIRCRAFT GAS TURBINE ENGINES

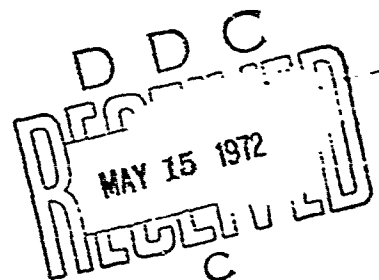
Volume 3: The Flow Model

Ronald S. Fletcher    Richard D. Siegel  
Northern Research and Engineering Corporation  
219 Vassar Street  
Cambridge, Massachusetts 02139



U.S. International Transportation Exposition  
Dulles International Airport  
Washington, D.C.  
May 27-June 4, 1972

DECEMBER 1971  
FINAL REPORT



Availability is unlimited. Document may be released to the National Technical Information Service, Springfield, Virginia 22151, for sale to the public.

Prepared for  
Reproduced by  
NATIONAL TECHNICAL  
INFORMATION SERVICE  
Springfield, Va. 22151

DEPARTMENT OF TRANSPORTATION  
FEDERAL AVIATION ADMINISTRATION  
Systems Research & Development Service  
Washington, D.C. 20591

ENVIRONMENTAL PROTECTION AGENCY  
Office of Air Programs  
ANN ARBOR, MICH. 48105

SEE AD 741506

The contents of this report reflect the views of the Northern Research and Engineering Corporation which is responsible for the facts and the accuracy of the data presented herein. The contents do not necessarily reflect the official views or policy of the Department of Transportation or the Environmental Protection Agency. This report does not constitute a standard, specification or regulation.

ACCESSION NO.	
WEST	WHITE SECTION <input checked="" type="checkbox"/>
DOC	DIFF SECTION <input type="checkbox"/>
ILLUSTRATIONS	
JUSTIFICATION	
BY	
DISTRIBUTION/AVAILABILITY CODES	
SIST.	AVAIL. and/or SPECIAL
A	

1. Report No. FAA-RD-71-111-3	2. Government Accession No.	3. Recipient's Catalog No.	
4. Title and Subtitle THE CONTROL OF OXIDES OF NITROGEN EMISSIONS FROM AIRCRAFT GAS TURBINE ENGINES VOLUME 3: THE FLOW MODEL		5. Report Date December, 1971	
		6. Performing Organization Code	
7. Author(s) Ronald S. Fletcher Richard D. Siegel		8. Performing Organization Report No. 1162-3	
9. Performing Organization Name and Address Northern Research and Engineering Corporation 219 Vassar Street Cambridge, Massachusetts 02139		10. Work Unit No.	
		11. Contract or Grant No. DOT FA70WA-2428	
12. Sponsoring Agency Name and Address Department of Transportation Environmental Protection Federal Aviation Administration Agency Washington, D. C. 20590 Office of Air Programs Ann Arbor, Michigan 48105		13. Type of Report and Period Covered Final Report: June, 1970-December, 1971	
		14. Sponsoring Agency Code	
15. Supplementary Notes			
16. Abstract <p>The objective of this study was to develop criteria for use in the design of aircraft gas turbine combustion chambers to minimize nitrogen oxide emissions. The approach adopted involved the development of a mathematical model of NO<sub>x</sub> emission from aircraft engine combustors; a parametric analysis, using the model, to determine the sensitivity of NO<sub>x</sub> emissions to variations of model parameters and engine design variables; evaluation of critical model parameters by means of experimental measurements; and the incorporation of the model into combustor design methods to provide guidelines for minimizing NO<sub>x</sub> emission while maintaining other performance and emission characteristics. The results of the study and the NO<sub>x</sub> emission control criteria are described in Volume 1 (FAA-RD-71-111-1). Volume 2 (FAA-RD-71-111-2) describes the nitric oxide formation process and a computer program (NOXRAT) for calculating thermodynamic data. The program is based upon a six-reaction model of NO formation. Volume 3 (FAA-RD-71-111-3) describes combustion and flow processes in gas turbine combustors and a computer program (GASNOX) for calculating gas properties and NO concentrations throughout a combustor. This program is based upon a three-zone, heterogeneous model of gas turbine combustor operation. Program GASNOX is used with input data from Program NOXRAT to calculate NO emission rates.</p>			
17. Key Words Air Pollution      Gas Turbine Nitrogen Oxides    Theoretical Model Nitric Oxide       Experimental Measurement Aircraft            Design Criteria		18. Distribution Statement Availability is unlimited. Document may be released to the National Technical Information Service, Springfield, Virginia 22151, for sale to the public.	
19. Security Classif. (of this report) UNCLASSIFIED	20. Security Classif. (of this page) UNCLASSIFIED	21. No. of Pages 173	22. Price \$3.00 PJ .95 MF

The study reported here was carried out under the technical direction of Dr. D. M. Dix with Dr. Ronald S. Fletcher assuming project responsibilities. Other participants in the program were Dr. R. D. Siegel, Dr. E. K. Bastress, and Mr. R. J. Murad; Professors J. B. Heywood, A. H. Lefebvre, and Mr. E. R. Norster served in a consulting capacity during the course of the study.

This study was sponsored in part by the Federal Aviation Administration and the Environmental Protection Agency under Contract No. DOT FA70WA-2428. Technical monitoring of the program was conducted by Mr. William T. Westfield (FAA) and Mr. George D. Kittredge (EPA).

## CONTENTS

	Page
1. INTRODUCTION . . . . .	1
2. THE FLOW MODEL . . . . .	2
2.1 The Generalized Conservation Equations . . . . .	2
2.2 The Distribution Function . . . . .	4
2.3 Application to the Primary Zone . . . . .	5
2.4 Application to the Intermediate Zone . . . . .	6
2.5 Application to the Dilution Zone . . . . .	10
2.6 Computational Procedure . . . . .	11
2.6.1 Required Input . . . . .	11
2.6.2 Preliminary Calculations . . . . .	12
2.6.3 Prediction Procedure . . . . .	13
3. PROGRAM GASNOX . . . . .	16
3.1 Introduction . . . . .	16
3.1.1 Program Function and Capabilities . . . . .	16
3.1.2 Report Arrangement . . . . .	17
3.2 Input Data . . . . .	17
3.2.1 General Description . . . . .	17
3.2.2 Detailed Description of Input Data . . . . .	19
3.2.3 Discussion of Input Data . . . . .	23
3.2.4 Description of Sample Case Input . . . . .	23
3.3 Output Data . . . . .	23
3.3.1 Normal Output . . . . .	24
3.3.2 Error Messages and Additional Output . . . . .	29
3.3.3 Description of Sample Case Output . . . . .	32
3.4 Miscellaneous Operational Information . . . . .	32
3.5 Data input Sheet . . . . .	33
3.6 Sample Case Output . . . . .	35
4. REFERENCES . . . . .	43
5. FIGURES . . . . .	44
6. NOMENCLATURE . . . . .	49
7. APPENDICES . . . . .	51
Appendix I - Over-All Program Logic . . . . .	52
Appendix II - Common Fortran Nomenclature . . . . .	54
Appendix III - Main Routine GASNOX . . . . .	62
Appendix IV - Subroutine PRIMRY . . . . .	70
Appendix V - Subroutine ZINTER . . . . .	78
Appendix VI - Subroutine DILUTE . . . . .	99
Appendix VII - Subroutine PRCALC . . . . .	112
Appendix VIII - Subroutine PRRAT . . . . .	123
Appendix IX - Subroutine MINT . . . . .	126
Appendix X - Subroutine CALCBC . . . . .	131
Appendix XI - Subroutine CHECKK . . . . .	134

## CONTENTS (CONTINUED)

	Page
Appendix XII - Subroutine KUNKUT . . . . .	137
Appendix XIII - Subroutine DERIV . . . . .	141
Appendix XIV - Subroutine ZMASS . . . . .	146
Appendix XV - Subroutine PRINTS . . . . .	160
Appendix XVI - Method of Calculation of Air Distribution Characteristics . . . . .	165

# LIST OF FIGURES

	Page
1 ASSUMED FLOW AND DISTRIBUTION PATTERNS THROUGHOUT COMBUSTOR LINER . . . . .	45
2 PRIMARY ZONE COMBUSTION EFFICIENCY CORRELATION . . . . .	46
3 SCHEMATIC REPRESENTATION OF INPUT STRUCTURE . . . . .	47
4 MODULAR TREE DIAGRAM . . . . .	48

## 1. INTRODUCTION

Volume 1 of this report carries a full description of the complete program but omits mathematical details of the model developed to predict the nitric oxide (NO<sub>x</sub>) emissions from aircraft gas turbine combustors and also the details of two computer programs developed as part of the study for obtaining predictions from the model. It is the purpose of Volumes 2 and 3 of the report to present full descriptions of both the model and the computer programs.

It is convenient to consider the model in two parts, one part being concerned with the NO<sub>x</sub> formation process and the other with modeling the flow behavior within gas turbine combustors. The convenience arises not only due to the basic difference in the studies of these two parts, but also due to the fact that a separate computer program has been developed for each part. This approach has been adopted in the interests of economy of computation as calculation of the necessary data for the determination of the NO<sub>x</sub> formation process requires appreciable computer time but the data once collected can, of course, be applied to any combustion calculation with the same reference conditions (in this case, combustor inlet conditions) of pressure and temperature. The computer program developed for this task has the name NOXRAT, and its function is to compute the rate terms of the NO<sub>x</sub> formation process and all relevant thermodynamic data for a series of fuel-to-air ratios with a common reference state.

Volume 2 of this report is solely concerned with the nitric oxide formation process. It presents a mathematical description of the program NOXRAT and also includes a section which is essentially a user's manual for the program. Volume 3 produces the same details for the flow model developed to describe the flow conditions in a gas turbine combustor. The corresponding computer program is named GASNOX and it is so arranged that the rate terms and all relevant thermodynamic data computed in NOXRAT are punched onto a deck of computer cards which serves as input data to the main program GASNOX.

The objective of this volume of the report, therefore, is to present the theory behind the flow model and details of the computer program developed for its application.

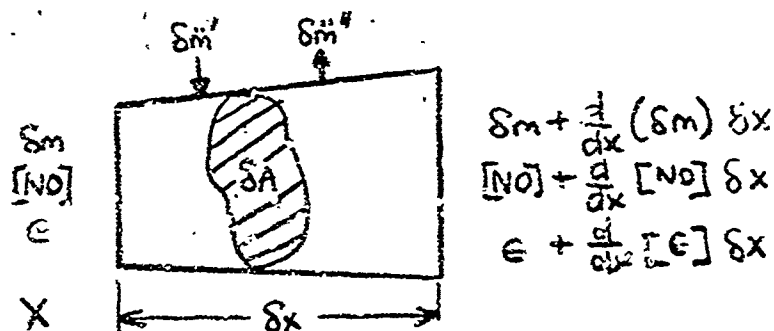
## 2. THE FLOW MODEL

Calculations based upon the reaction scheme described in Volume 2 clearly show that for significant concentrations of nitric oxide to be formed during the short time it takes the gases to pass through an aircraft gas turbine engine, the temperature must exceed 2000 deg K. Such high temperatures only exist within the combustor, and only then for a limited time, so clearly, nitric oxide concentrations in the exhausts of aircraft engines are solely dependent upon the flow behavior and the chemical processes occurring within the combustion chamber and it is these features that must be adequately represented in the model.

The first task, therefore, is to select a method of modeling the flow processes in the gas turbine combustor. Such combustors are conventionally divided into three zones as shown in Figure 1a. The distinction between these zones is discussed qualitatively in Volume 1, Section 3, but in the next section these distinctions are quantified. Firstly, the basic conservation equations are derived for the generalized case of an inhomogeneous, reacting gas mixture of the type that occurs in a gas turbine combustor. These equations are then reduced to conditions applicable to the three combustor zones, the primary, intermediate and dilution zones, which are of interest to this study, and finally, they are used to demonstrate how the nitric oxide levels may be calculated for each zone.

### 2.1 THE GENERALIZED CONSERVATION EQUATIONS

A control volume will be considered to contain products of constant fuel-to-total mass ratio,  $F$ , which will be termed the mixture ratio. (The constancy of  $F$  is taken as it has particular utility in this study insofar as that it minimizes the number of calculations for the equilibrium conditions necessary to determine local nitric oxide reaction rates.) The volume is as shown below:



where,  $\delta m$  = mass flow in interval  $\delta F$  about  $F$   
 $[NO]$  = mass fraction of nitric oxide  
 $\epsilon$  =  $m_{fu}/m$ , fractional mass flow of unburned fuel  
 $\delta m'$  = mass flow per unit length of fuel ratio  $F'$ , with mass fraction of NO =  $[NO]'$  which enters the volume due to mixing  
 $\delta m''$  = mass flow per unit length, with mass fraction of NO =  $[NO]''$  which leaves the volume due to mixing  
 $\delta A$  = cross sectional area of element  
 $\dot{r}$  = rate of formation of NO per unit volume by chemical reaction

The conservation equations become,

$$\text{for NO,} \quad \frac{d}{dx} (\delta m [NO]) = \dot{r} \delta A + \delta m' [NO]' - \delta m'' [NO]'' \quad A-1$$

$$\text{mass,} \quad \frac{d}{dx} (\delta m) = \delta m' - \delta m'' - \frac{d}{dx} (\epsilon \delta m) \quad A-2$$

$$\text{burned fuel,} \quad F \frac{d}{dx} (\delta m) = \delta m' F' - \delta m'' F'' - \frac{d}{dx} (\epsilon \delta m) \quad A-3$$

$$\text{unburned fuel,} \quad \frac{d}{dx} (\epsilon \delta m) = \dot{R} \quad \text{- specified} \quad A-4$$

In the limit as  $\delta x$  tends to zero, these equations take the form,

$$\frac{d}{dx} \left( [NO] \frac{dm}{dF} \right) = \dot{r} \frac{dA}{dF} + [NO]' \frac{dm'}{dF} - [NO]'' \frac{dm''}{dF} \quad A-1a$$

$$\frac{d}{dx} \left( \frac{dm}{dF} \right) = \frac{dm'}{dF} - \frac{dm''}{dF} - \frac{d}{dx} \left( \epsilon \frac{dm}{dF} \right) \quad A-2a$$

$$F \frac{d}{dx} \left( \epsilon \frac{dm}{dF} \right) = F' \frac{d\dot{m}'}{dF} - F'' \frac{d\dot{m}''}{dF} - \frac{d}{dx} \left( \epsilon \frac{dm}{dF} \right) \quad A-3a$$

$$\frac{d}{dx} \left( \epsilon \frac{dm}{dF} \right) = \dot{R} \quad A-4a$$

## 2.2 THE DISTRIBUTION FUNCTION

The control volume considered above is only concerned with an element of mass  $\delta m$  with a mixture ratio  $\delta F$  about  $F$ . It was proposed to represent the distribution of mass about mixture ratio by a normal distribution function of the form,

$$\frac{\delta m}{\delta F} = C \exp \left\{ -\frac{1}{2} \left( \frac{F - \bar{F}}{\sigma} \right)^2 \right\} \quad A-5$$

The parameter  $\sigma$ , in statistical terms, is called the standard deviation and represents the degree of distribution of  $F$  about the mean value  $\bar{F}$ .

$C$  is termed the normalizing factor and for the purpose of this study is defined by the expression that,

$$\int_0^{2\bar{F}} \frac{\delta m}{\delta F} dF = \dot{m}(1 - \epsilon) \quad A-6$$

The value of  $\bar{F}$  is the ratio of the total fuel burned to the total mass flow. Clearly both  $C$  and  $\bar{F}$  will be a function of the axial position in the combustor as they are computed from Equations A-2 and A-3.

A normal distribution has been selected as it is known to fit the spray characteristics of the type of fuel injectors used in gas turbine combustors and it provides a convenient way of describing the mixing process, by specification of the relationship  $\sigma = \sigma(x)$ . The value of  $\delta m_i$ , the mass flow in interval  $\delta F$  about  $F_i$  can also be evaluated functionally by the equation

$$\delta m_i = \int_{F_i - \delta F/2}^{F_i + \delta F/2} \frac{\delta m}{\delta F} dF \quad A-7$$

and so the whole flow field can be readily represented by a series of discrete elements of constant, but different, mixture ratios.\*

### 2.3 APPLICATION TO THE PRIMARY ZONE

The model of the flow behavior described previously assumes that no mixing takes place in the primary zone after the specified distribution of mass mixtures ratios is attained. Thus, referring to the control volume above,

$$\delta \dot{m}' = \delta \dot{m}'' = 0$$

and further, it is also assumed that only a certain fraction  $\beta$  of the total fuel entering the zone is burned and that this fraction burns instantaneously.

$$\frac{d}{dx} (\epsilon \delta m) = 0$$

so equation (A-1) reduces to,

$$\frac{d}{dx} (\delta m [NO]) = \dot{r} \delta A \quad A-8$$

or,

$$[NO]_x = \int_0^x \frac{\dot{r} \delta A}{\delta m} dx \quad A-9$$

or alternatively,

$$[NO]_t = \frac{1}{\rho} \int_0^t \dot{r} dt \quad A-10$$

where  $\rho$  is the density of the element and  $t$  is the time it takes to pass through the primary zone. It is taken that  $\rho = \bar{\rho}$ , the mean density in the primary zone where,

$$\bar{\rho} = \frac{1}{\dot{m}} \int_0^{2\bar{F}} \rho \cdot \frac{\delta m}{\delta F} dF \quad A-11$$

\* The nature of the normal distribution function is that  $f(F)dF$  only tends to zero as  $F$  tends to  $\pm\infty$ . Negative  $F$ 's have no physical significance so a constraint is imposed upon the function that  $0 < F < 2\bar{F}$  thus preserving the useful feature of symmetry about  $\bar{F}$ . In fact, if  $\sigma$  is less than  $\bar{F}/3$ , this constraint modifies the function to only a very small extent as it can be shown that the integral is greater than 99.7 per cent of that over the range  $\pm\infty$ . Practically, a range of  $\sigma$  from 0 to  $\bar{F}/3$  will represent a wide range in distribution characteristics. It should also be noted that  $C$  and  $m$  are simply related by the equation  $C = \sqrt{2\pi} \sigma m$ , if the limits are expressed from  $\pm\infty$ .

but the value of  $t$  cannot be so simply expressed for the case of a completely-stirred reactor. Theoretical considerations dictate (see Ref 1) that various fractions of the mass flow  $\delta m$  have different residence times according to the function,

$$F(t) = \frac{1}{\bar{\tau}} \exp(-t/\bar{\tau}) \quad \text{A-12}$$

where  $\bar{\tau}$  is the mean residence time and is equal to the ratio of  $(V_p \bar{\rho} / \dot{m})$  and where  $V_p$  is the volume of the primary zone. The relationship,

$$f(t) = F(t) dt = \frac{1}{\bar{\tau}} \int_{t-\frac{1}{2}dt}^{t+\frac{1}{2}dt} \exp(-t/\bar{\tau}) dt \quad \text{A-13}$$

then defines a fraction  $f_t$  of  $\delta m$  which has a residence time within the range  $dt$  about  $t$ . It is therefore necessary to solve Equations A-10 and A-13 to compute a series of  $f_t$  values corresponding to the  $[\bar{NO}]_t$  concentrations over the range of  $t$  from zero to infinity. The mean nitric oxide concentration at the exit of the zone for an element of mixture ratio  $F$ ,  $[\bar{NO}]_F$ , is then calculated from,

$$[\bar{NO}]_F = \sum_{t=0}^{\infty} f_t \times [\bar{NO}]_t \quad \text{A-14}$$

and the process repeated for all elements over the mixture range of interest.

Finally, an over-all mass mean average nitric oxide concentration for all products leaving the primary zone can then be computed by summing all products  $[\bar{NO}]_F \times \delta m$  and dividing by the total mass flow rate through the primary zone.

## 2.4 APPLICATION TO THE INTERMEDIATE ZONE

In the intermediate zone, mixing is assumed to occur over the length of the zone  $L$ , such that at the exit it is uniformly mixed. We postulate that mixing is characterized by the expression,

$$\epsilon = \epsilon_0 \left\{ 1 - (X_I/L)^{A_1} \right\} \quad A-15$$

where  $\epsilon_0$  is the prescribed deviation for the primary zone,  $A_1$  is a model constant and  $X_I$  is the axial distance from the primary zone exit. The distribution of the mixture ratio  $F$  is therefore known at every point, i.e.,  $\delta m = f(F, X) \delta X$  is prescribed by Equations A-5, A-6, and A-15. The problem therefore reduces to determining  $\delta \ddot{m}'$ ,  $\delta \ddot{m}''$ , and  $F'$  from Equations A-2 and A-4 and to making certain assumptions about the mixing process, as  $[NO]'$  and  $[NO]''$  must be determined in order that Equation A-1 can be solved for  $[NO]$  as a function of  $F$  and  $X$ .

We will postulate that all mixing occurs at conditions corresponding to entry conditions into the control volume so,

$$\begin{aligned} [NO]' &= [NO] \\ [F]'' &= F \end{aligned}$$

and also that,

$$\delta \ddot{m}'' = K \delta m \quad A-16$$

which is to say that the flow out of the elemental control volume, due to mixing, is proportional to the amount flowing into the control volume. Clearly  $K$  must have units of 1/length and the physical interpretation of  $K$  can best be thought of in terms of the ratio,  $C_N$ , of the mass flow rate leaving the element over the length of the intermediate zone to the mass flow rate within the element. If this latter mass flow rate is constant, then clearly

$$\delta \ddot{m}'' = C_N \delta m$$

or,

$$K = C_N / X_L$$

It will be assumed that the value of  $K$  is known. Equation A-2 then yields,

$$\delta \ddot{m}' = \frac{d}{dx} (\delta m) + \dot{R} + K \delta m \quad A-17$$

where it is to be noted that the restrictions,

$$K > 0$$

$$K > \left\{ -\frac{1}{\delta m} \left( \frac{d}{dx}(\delta m) + \dot{R} \right) \right\}_{\max}$$

A-18

must be satisfied for the model to be valid.

The gases flowing into the control volume as a result of mixing,  $\delta \ddot{m}'$ , will originate from two sources: firstly, from the mixing of gases already within the combustor liner, which we will denote as  $\delta \ddot{m}_m$  and secondly by the mixing action of the diluent air with previously mixed gases, which we will call  $\delta \ddot{m}_a$ . Clearly,

$$\delta \ddot{m}' = \delta \ddot{m}_m + \delta \ddot{m}_a \quad \text{A-19}$$

and we will postulate that,

$$\delta \ddot{m}_a = \frac{\delta m}{m} \ddot{m}_a \quad \text{A-20}$$

that is, that the amount of diluent air entering the control volume is in proportion to the total mass flow rate in the volume. The problem is then defined in terms of  $\delta \ddot{m}'$ ,  $\delta \ddot{m}''$ , and  $F'$  as,

$$\delta \ddot{m}_m = \frac{d}{dx}(\delta m) + K \delta m - \frac{\delta m}{m} \ddot{m}_a + \dot{R} \quad \text{A-21}$$

from Equations A-17, A-19, and A-20, and also as a consequence of Equation A-3.

$$F' = \frac{F}{\delta \ddot{m}'} \left( \delta \ddot{m}'' + \frac{d}{dx}(\delta m) \right) + \frac{\dot{R}}{\delta \ddot{m}'} \quad \text{A-22}$$

The value of  $[NO]$  must now be calculated. Clearly, the total nitric oxide mass which leaves all the elements by mixing must also return via the mixing process to preserve conservation of the specie. The following relationship is assumed to apply, therefore, that

$$[NO'] \sum_0^{2\bar{F}} \delta \ddot{m}' = \sum_0^{2\bar{F}} (\delta \ddot{m}'' \times [NO'']) \quad \text{A-23}$$

The value of  $\dot{R}$ , the rate of burning of the unburned fuel which leaves the primary zone (see Equation A-4), is now all that is necessary to calculate NO concentrations throughout the intermediate zone.

It is postulated that this rate of burning is controlled by the mixing process, so in keeping with the Equation A-15, the following is assumed,

$$\varepsilon = \varepsilon_0 \left(1 - A_3 (x_I/L)^{A_2}\right) \quad A-24$$

where  $A_2$  and  $A_3$  are model constants,  $\varepsilon_0$  is the fractional mass of unburned fuel entering the intermediate zone and is given by\*,

$$\varepsilon_0 = (1 - \beta) m_f / m \quad A-25$$

$\dot{R}$  may therefore be computed, as by definition (see Equation A-4), it is equal to  $\frac{d}{dx} (\varepsilon \dot{S}_m)$ . Thus the problem is defined as,

$\dot{S}_m'$  is known from Equations A-19 and A-21

$\dot{S}_m''$  is known from Equation A-16

$[NO]'$  is known from Equation A-23

$[NO]''$  is equal to  $[NO]_x$

and  $\dot{S}_m = F(F, x) \delta F$ , is given by the specified distribution function.

If these values are substituted into the conservation equation for nitric oxide (Equation A-2) then it can be shown that,

$$\begin{aligned} [NO]_{x+dx} - [NO]_x &= \int_x^{x+dx} \frac{\rho}{\rho V} dx + \int_x^{x+dx} [\Delta NO] K dx \\ &+ \int_{\dot{S}_m}^{\dot{S}_m + d\dot{S}_m} ([\Delta NO] + \varepsilon [NO']) \frac{d\dot{S}_m}{\dot{S}_m} + \int_{\varepsilon}^{\varepsilon + d\varepsilon} [NO'] d\varepsilon \end{aligned} \quad A-26$$

where  $V$  is the velocity and,

$$[\Delta NO] = ([NO]' - [NO]_x) \quad A-27$$

This equation has to be evaluated in a stepwise manner in order to calculate the relationship  $[NO] = F(F, x) \delta X$  in the intermediate zone. It is then a simple matter to compute an over-all mass average nitric oxide concentration at each axial station from,

\* Another way to express these relationships is as:

$$m_{fu_0} = (1 - \beta) m_f$$

$$m_{fu} = m_{fu_0} \left(1 - A_3 (x_I/L)^{A_2}\right)$$

$$[NO]_x = \frac{1}{\dot{m}} \sum_{F=0}^{F=2\bar{F}} [NO]_{F,x} \delta \dot{m}$$

A-28

and so complete the computation.

## 2.5 APPLICATION TO THE DILUTION ZONE

In the dilution zone all gases are assumed to perfectly mix to a mean mixture ratio. All fuel is assumed to have been burned previously in the combustor and only diluent air enters the zone. For this case therefore, one cannot consider a control volume of constant mixture ratio  $F$ , as was done at the introduction to this section, as  $F$  must change with axial distance due to the added air flow. For the special case of the assumptions made above, this change may be accounted for by modifying only Equation A-3 of the conservation equations so that this dependency of  $F$  with  $x$  is properly accounted for.

The conservation Equations A-1 through A-4, can be shown to be given by,

$$\frac{d}{dx}(\delta \dot{m} [NO]) = \dot{r} \delta A$$

$$\frac{d}{dx}(\delta \dot{m}) = \delta \ddot{m}_a$$

$$\frac{d}{dx}(\delta \dot{m} F) = 0$$

$$\frac{d}{dx}(\varepsilon \delta \dot{m}) = 0$$

as the above assumptions imply that,

$$\delta \ddot{m}'' = \delta \ddot{m}_a$$

and,

$$[NO]' = F' = \dot{R} = \delta \dot{m}'' = 0$$

The conservation equation for nitric oxide can be reduced to the form,

$$[NO]_{x+dx} - [NO]_x = \int_x^{x+dx} \frac{\dot{r}}{\rho v} dx + \int_F^{F+dF} \frac{[NO]}{F} dF \quad A-29$$

which predicts directly, the mean average nitric oxide concentration at the new axial position. This process can be repeated in a step-wise manner to the end of the combustion chamber and hence the nitric oxide concentration at the exit plane may be predicted.

## 2.6 COMPUTATIONAL PROCEDURE

A summary is presented below of the computational procedure necessary to combine the flow model and the chemical reaction scheme presented in Volume 2 in order to predict nitric oxide emissions from aircraft turbine engines.

### 2.6.1 Required Input

The following input is required in order for the computation to proceed:

#### a. Chemical Reaction Scheme

1. A means of evaluating the adiabatic flame temperature, density and composition of the equilibrium products for the combustion of hydrocarbons in air. Program NOXRAT described in Volume 2 serves the purpose.
2. Values of the rate constants  $k_f$  to  $k_r$ .
3. Fuel properties in terms of C:H ratio.

#### b. Combustor Dimensions

These should be expressed in such a way as to allow calculation of,

1. Volume of the primary zone.
2. Area of the intermediate and dilution zones as a function of distance  $x$ .

#### c. Combustor Operating Conditions

The following should be expressed as a function of aircraft operating mode,

1. Combustor inlet temperature and pressure.
2. Total fuel flow rate.
3. Air-flow conditions in terms of the fraction entering the primary zone and the rate of addition at the walls as it varies with axial position along the combustor.

#### d. Other Inputs to be Specified

1. The functions,

$$\sigma = \sigma(x) \quad (\text{see Equation A-15})$$

$$\text{and, } \epsilon = \epsilon(x) \quad (\text{see Equation A-24})$$

2. The value of  $K$ , or  $C_N$ , which defines the fraction of gases that leave an element of constant mixture ratio  $F$  due to mixing (see Equation A-16)

### 2.6.2 Preliminary Calculations

Two preliminary calculations must be performed before the computation of NO concentration levels can be undertaken.

These involve,

- a. The determination of a value for  $\beta$ , the fraction of total fuel entering the primary zone that is burned in the zone.
- b. A consideration of the mixing characteristics of the cooling air that enters the combustor liner from the walls of the intermediate and dilution zones. The bulk of such flow normally enters perpendicular to the direction of the mainstream product flow and has then to be deflected and entrained before it can enter the fully developed mixing processes. This action must require a finite time (i.e., distance) to occur, and its effect upon the nitric oxide formation process has to be considered.

### Combustion Efficiency

A correlation does exist to relate primary zone combustor efficiency to the fuel loading parameter  $\dot{m}_f / V_p^2$ . The correlation is given in Reference 2 and is reproduced in Figure 2. There is significant scatter in the data points used to obtain the correlation and the values of the primary zone efficiency determined using the correlation can be expected to have error limits of approximately  $\pm 20$  per cent of the indicated value.

### Air Distribution Characteristics

In the calculation of the rate of diluent air addition to the intermediate and dilution zones, some provision must be made for the time (hence distance) necessary for the dilution gases to mix into the mainstream flow. This mixing lag could conceivably affect NO

emissions significantly under certain circumstances as it controls the rate of temperature change at positions downstream of the primary zone exit. A simple method was developed to take some account of this effect and is described fully in Appendix XVI. The method is consistent with the mixing assumptions used to develop the model for the intermediate zone of the combustor and at the same time, it determines the fraction of the air that enters the primary zone.

### 2.6.3 Prediction Procedure

In the interests of economy of use of Program NOXRAT which determines the flame temperatures and concentrations of the C-H-O-N species at equilibrium conditions, hence the NO formation rates, the distribution function of mixture ratio  $F$ , versus mass fraction  $S_F$  (Equation A-5), is considered as a series of elements of differing  $S_F$ . The first task in each step is to calculate the mass fraction in each element from the equation,

$$dm = \int_{F - \Delta F/2}^{F + \Delta F/2} \frac{dm}{S_F} dF$$

for the prescribed conditions and thus relate  $S_m$  to  $F$ .

The  $S_F$  increments are selected, then the adiabatic flame temperatures  $T$ , the density  $\rho$  and the corresponding equilibrium concentrations of the species  $N$ ,  $N_2O$ ,  $NO$ ,  $C_2$ ,  $O$ ,  $OH$ , and  $NO$  are determined from Program NOXRAT for each  $F$ . These specie concentrations are then used to determine the values of  $R_1$ ,  $R_6$ ,  $K_1$ , and  $K_2$  (for each  $F$ ) which are needed to compute the rate of nitric oxide formed by chemical reaction and the calculation then proceeds as follows.

#### Primary Zone

- a. The specified value of  $\beta$ , the fraction of fuel burned in the primary zone, is used to compute  $\bar{F}_p$ .  $S_m$  can then be determined for all  $F$  values over the range of interest ( $0 < F < 2\bar{F}_p$ ).

- b. The value of the mean residence time  $\bar{\tau}$  is determined from Equation A-12.
- c. Nitric oxide concentrations at the primary zone exit can then be computed for each  $F$  and for the prescribed residence time distribution by solving in an iterative manner the relationship,

$$[\text{NO}]_F = \sum_{t=0}^{\infty} [\text{NO}]_t \times f_t$$

- d. Finally the mass average nitric oxide concentration is computed for all gases leaving the primary zone from the relationship,

$$[\text{NO}]_p = \sum_{F=0}^{F=2\bar{F}} [\text{NO}]_F \times \delta \dot{m}$$

#### Intermediate Zone

The calculation procedure for this zone, for each incremental step in the axial direction, is essentially identical to that for the primary, except for the necessity to compute a change in NO concentration due to the mixing process. The procedure is as follows:

- a. For  $X = X + dX$ , new values of  $\delta \dot{m}$  are computed at each  $F$  from Equation A-5.
- b. The value of  $[\text{NO}]'$ , the concentration of nitric oxide in the gases entering the control volume by mixing over the step is computed according to Equation A-23.
- c. The nitric oxide concentration at position  $X + dX$  is then computed for each mixture ratio  $F$  by integration of Equation A-26.
- d. Finally the new mass average nitric oxide concentration is computed as for Step d above.

These steps are repeated to the end of the intermediate zone.

#### Dilution Zone

The results of the intermediate zone calculation serve as input to the dilution zone. At this stage all elements in the combustor are

of equal composition and temperature, and dilution proceeds by the addition of pure air and so one can use the relationship (see Equation A-29) that,

$$[NO]_{x+dx} - [NO]_x = \int_x^{x+dx} \frac{\dot{r}}{pV} dx + \int_F^{F+dF} \frac{[NO]}{F} dF$$

This can be integrated in a stepwise manner with respect to  $X$  by interpolation of the nitric oxide rate data at each step to determine the nitric oxide concentration conditions at the corresponding  $F$  value.

The nitric oxide formation rate quickly reduces in this zone as the temperature decreases rapidly.

### 3. PROGRAM GASNOX

#### 3.1 INTRODUCTION

##### 3.1.1 Program Function and Capabilities

Program GASNOX is a digital computer program written in Fortran IV language for use with the CDC 6600 computing system. The program has been developed for the purpose of predicting the nitric oxide emission level from an aircraft gas turbine combustor. Based on a given set of combustor dimensions, operating conditions, kinetic rate constants, thermodynamic properties, equilibrium compositions, and a primary zone mixing parameter, the program will compute nitric oxide concentrations as a function of axial position in annular and canannular combustors.

The analytical procedures on which the computer program is based have been discussed in Section 2 of this volume and in Reference 3. Briefly the model considers a combustor to consist of three zones: primary, intermediate, and dilution. The primary zone is modeled as a partially stirred reactor with the variation of gas composition, temperature, and residence time occurring within the zone taken into account statistically. The program predicts only the gross features of the flow at the zone exit. The intermediate zone represents a transition between the primary and dilution zones. Here mixing occurs between the heterogeneous products from the primary zone and the entering cooling air. The program predicts the gross features of the flow as a function of axial position in this zone. In the dilution zone, the flow is uni-dimensional with the gases uniformly mixed across each cross section. Only the mean mixture ratio is considered, and this only changes as the remaining compressor air is mixed into the combustor. The procedures incorporated into the program have been found to be quite acceptable in terms of accuracy and calculation efficiency.

### 3.1.2 Report Arrangement

The main body of the report begins with a section in which the input data necessary for the solution of any case are described in detail; this includes instructions for preparing and supplying these data to the program and a sample case in the appropriate format. The next section contains a discussion of the various types of output data obtained from the program and also of the output data from the sample case. A description of the error messages printed by the program is also included. Following that is a section containing miscellaneous information regarding the operation of the program with the CDC 6600 computing system.

The first appendix consists of a general discussion of the over-all logic structure of the program. The next appendix gives the Fortran nomenclature for the variables in the COMMON blocks of the program. The remaining appendices except the last provide detailed descriptions of the various components (main routine and subroutines) which make up the over-all program, one appendix for each component. The appendix for each new subroutine contains a presentation of the input and output variables, an internal Fortran nomenclature, a description of the step-by-step calculation procedure, and a Fortran listing of the subroutine. The last appendix contains a discussion of the method of calculation of the air distribution characteristics.

## 3.2 INPUT DATA

### 3.2.1 General Description

Program GASNOX requires the following input data in order to determine the nitric oxide emission level from an aircraft gas turbine engine.

#### a. Combustor Dimensions

1.  $V_p$  - Volume of the primary zone
2.  $X_L$  - Length of the intermediate zone (from the exit of the primary)

3.  $X_{END}$  - Distance from the primary zone exit to the exit from the combustor liner
4.  $R_X$  - Radius of liner at position  $X$  for canannular configuration
5.  $R_{X_i}, R_{X_o}$  - Inner and outer radii of liner at position  $X$  for annular configuration:

b. Combustor Operating Conditions

1.  $T$  - Inlet temperature
2.  $P$  - Operating pressure
3.  $\phi_p$  - Mass mean equivalence ratio in the primary zone (before fuel burns)
4.  $\beta$  - Fraction of fuel entering the primary zone which burns in the zone
5.  $E_{rat}$  - Variable for altering  $\phi_p$  parametrically yet maintaining constant the over-all air-to-fuel ratio in the combustor
6.  $(M_{aX} \%)$  - Total mass per cent of air mixed with the product stream at position  $X$  in the liner
7.  $M_A$  - Total mass of air fed into the combustor liner
8.  $\bar{\tau}_p$  - Mean primary zone residence time (applies only if  $V_p$  is set equal to zero)

c. Mixing Parameter for the Primary Zone

1.  $S_o$  - Degree of mixedness in the primary zone (where  $\phi_o$  in the distribution function is given by  $\phi_o = S_o \bar{\phi}_p$ )

d. Kinetic Constants for each Mixture Ratio Element

1.  $R_1$  - Forward reaction rate constant for the first reaction (see Section 2, Volume 2 or Ref 3)
2.  $R_6$  - Forward reaction rate constant for the sixth reaction (see Section 2, Volume 2 or Ref 3)

3.  $K_1$  - Ratio of forward reaction rate constants  
(see Section 2, Volume 2 or Ref 3)
4.  $K_2$  - Ratio of forward reaction rate constants  
(see Section 2, Volume 2 or Ref 3)
- e. Thermodynamic Properties for each Mixture Ratio Element
  1.  $\rho$  - Density of the combustion products
  2.  $T_f$  - Adiabatic flame temperature of the combustion products.
- f. Equilibrium Compositions for each Mixture Ratio Element
  1.  $(NO)_e$  - Nitric oxide equilibrium mole fraction
  2.  $(CO)_e$  - Carbon monoxide equilibrium mole fraction
  3.  $(C_{(s)})_e$  - Solid carbon equilibrium mole fraction
  4.  $(CH_2)_e$  - Unburned hydrocarbons (exclusive of CO and  $C_{(s)}$ ) equilibrium mole fraction.

The input data is read in three categories: 1) the kinetic, thermodynamic, and equilibrium data and the combustor inlet temperature and pressure; 2) the combustor airflow distribution and radius versus axial position; and 3) the remaining combustor dimensions, operating conditions, and the primary zone mixing parameter. With this structure there may be several sets of data in a given computer run. Figure 3 is a schematic representation of the data input structure.

### 3.2.2 Detailed Description of Input Data

The information required to prepare the input data for a case is furnished in the table given below. This information contains a description of each input item as well as a description of the form in which these items are written on input data sheets. The descriptions of the input items refer frequently to several points, relevant to the selection of input values, which are discussed in the following subsection. The discussions of these points provide additional detailed information useful in preparing the input data for any case.

The first input item read by Program GASNOX is the integer variable IDATA which identifies the number of sets of data in category 1. This input is then followed by the first set of category 1 data (see point a).

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number</u>	<u>Fortran Symbol</u>	<u>Description</u>
1	1-6		Int	IDATA	Number of sets of data in category 1
2	1-72		A	SET(1)	Descriptive data identifying atomic composition of fuel and the turbine inlet temperature
3	1-14		A	SET(1)	Descriptive data of units of combustor inlet pressure
3	15-29	P	FP	PPP	Combustor inlet pressure (atm)
3	30-51		A	SET(1)	Descriptive data of set of kinetic constants used in calculation (see Volume 1, Table 2; descriptive data of $k_s$ )
3	52-66	$k_s$	FP	EKS	Fuel-to-air mass ratio at stoichiometric conditions
4	1-12	$F_i$	FP	FF(1)	Mixture ratio of an element
4	13-24	$\phi_i$	FP	PHI(1)	Equivalence ratio of an element
4	25-36	$\rho_i$	FP	RHO(1)	Density of combustion products for an element ( $\text{gm}/\text{cm}^3$ )
4	37-48	$T_i$	FP	ATT(1)	Adiabatic flame temperature for an element (deg K)
4	49-60	$(\text{NO}_i)_e$	FP	BCON6(1)	Equilibrium mole fraction of NO for an element
4	61-72	$(\text{CO}_i)_e$	FP	BCON2(1)	Equilibrium mole fraction of CO for an element
5	1-12	$(C_{(s)i})_e$	FP	BCON1(1)	Equilibrium mole fraction of $C_{(s)}$ for an element
5	13-24	$(\text{CH}_2)_i$ $e$	FP	CH2(1)	Equilibrium mole fraction of unburned hydrocarbons exclusive of $C_{(s)}$ and CO for an element
5	25-36	$(R_1)_i$	FP	R1(1)	Forward reaction rate for the first kinetic reaction (see Section 2, Volume 2 or Ref 3) ( $\text{gm-mole}/\text{cm}^3\text{-sec}$ ) for an element

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number</u>	<u>Fortran Symbol</u>	<u>Description</u>
5	37-48	$(R_6)_i$	FP	R6(I)	Forward reaction rate for the sixth kinetic reaction (see Section 2, Volume 2 or Ref 3) ( $\text{gm-mole/cm}^3\text{-sec}$ ) for an element
5	49-60	$(K_1)_i$	FP	EK1(I)	Ratio of forward reaction rate constants (see Section 2, Volume 2 or Ref 3) for an element
5	61-72	$(K_2)_i$	FP	EK2(I)	Ratio of forward reaction rate constants (see Section 2, Volume 2 or Ref 3) for an element

Lines 4-5 are repeated for each of the 35 discrete mixture ratio elements specified in the distribution function. At the conclusion of this data, the integer variable KASE is read. KASE identifies the number of sets of data in category 2 that follow for the given set of data in category 1.

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number</u>	<u>Fortran Symbol</u>	<u>Description</u>
74	1-6		Int	KASE	Number of sets of data in category 2
75	1-12	X	FP	AXX(J)	Axial position in the combustor (in)
75	13-24	$(M_{ax})\%$	FP	APR(J)	Per cent of total mass of air-flow in combustor liner at position X (cumulative)
75	25-36	$R_X$	FP	ARR(J)	Radius of liner at position X; applies only for canannular configuration (in) (see point b)
75	37-48	$R_{X1}$	FP	ANR(J)	Inner radius of liner at position X; applies only for annular configuration (in) (see point b)
75	49-60	$R_{X0}$	FP	ANNR(J)	Outer radius of liner at position X; applies only for annular configuration (in) (see point b)

Line 75 is repeated for each of 11 axial positions in the combustor. The first axial position must be taken as  $X = 0$ ; that is, at the exit of the combustor primary zone.

There may be as many sets of data in category 3 for each set of data in category 2 as the user desires. The number of these data sets is read as the variable IN, on line 86.

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number</u>	<u>Fortran Symbol</u>	<u>Description</u>
86	1-6		Int	IN	Number of sets of data in category 3

Following the data on line 86 is the data of category 3.

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number</u>	<u>Fortran Symbol</u>	<u>Description</u>
87	1-12	$V_p$	FP	VP	Volume of primary zone ( $\text{in}^3$ ) (see point c)
87	13-24	$X_L$	FP	XL	Length of intermediate zone (in)
87	25-36	$X_{END}$	FP	XEND	Length of intermediate zone and dilution zone (combined) (in)
87	37-48	$\phi_p$	FP	EQUIV	Mass mean equivalence ratio in the primary zone (before fuel burns)
87	49-60	$\rho$	FP	BETA	Combustion efficiency in the primary zone
87	61-72	$M_A$	FP	TOTALR	Total mass of air fed into the combustor liner (lb/sec)
88	1-12	$S_o$	FP	S	Degree of mixedness in the primary zone
88	13-24	$E_{rat}$	FP	ERAT	Variable for varying $\phi_p$ parametrically yet maintaining constant air-to-fuel ratio in the combustor
88	25-36	$\bar{\tau}_p$	FP	TAUBAR	Mean primary zone residence time (applies only if $V_p$ is set equal to zero) (see point c)

Lines 87-88 are repeated for each set of data in category 3 that the user wishes to specify.

### 3.2.3 Discussion of Input Data

Some important aspects to be considered in appropriately specifying the input data are discussed below. Reference to these discussions has been made in the preceding subsection in which the input format was described. The points referred to are as follows:

- a. Data in category 1 (lines 2-73) are generated by Program NOXRAT described in Volume 2.
- b. If a canannular configuration is tested, the variables  $R_{X1}$  and  $R_{X0}$  are set equal to zero. If an annular configuration is tested, the variable  $R_X$  is set equal to zero.
- c. If the user chooses to specify the volume of the primary zone,  $V_p$ , then the mean primary zone residence time ( $\bar{\tau}_p$ ) is set equal to zero in the input.  $\bar{\tau}_p$  is then calculated by the program. If, on the other hand, the user chooses to specify  $\bar{\tau}_p$ , he must set  $V_p$  equal to zero in the input.

### 3.2.4 Description of Sample Case Input

Completed input data sheets are shown on pages 32 and 33. In this table lines 1-73 comprise the data and controls for category 1 (note: lines 6-73 are omitted for brevity); lines 74-85 comprise the data and controls for category 2; and lines 86-88 comprise the data and controls for category 3.

In this case, the fictitious combustor examined has an inlet temperature of 700 deg K and an operating pressure of 5.78 atm. The combustor is 10 inches in length from the exit of the primary zone, has a primary zone volume of 55 in<sup>3</sup>, and is being operated with a mean primary zone equivalence ratio (before the fuel burns) of 0.9. The over-all air-to-fuel ratio is 92.

## 3.3 OUTPUT DATA

The output of Program GASNOX consists entirely of printed data. The printed data falls into two main categories: normal output, and

error messages with additional output. The normal output which is illustrated by the sample case included in the report, will be described first.

### 3.3.1 Normal Output

The information included in the normal output can be divided into the following categories:

1. General input data and miscellaneous calculated input data.
2. Elemental primary zone exit conditions from the converged solution.
3. Over-all primary zone exit conditions from the converged solution.
4. Over-all intermediate zone conditions at various axial positions in the zone from the converged solution.
5. Over-all dilution zone conditions at various axial positions in the zone from the converged solution.

A description of the items in each category is given below.

The normal output of a typical case begins with the items in category 1-- general input data and miscellaneous calculated input data. This data consists of:

- a. Axial position in the combustor (where the origin is taken as the primary zone exit) (in).
- b. Total mass per cent of air mixed with the product stream at position X.
- c. Radius of liner at position X for canannular configuration or inner and outer radii of liner at position X for annular configuration (in).
- d. The case number; this number corresponds to the set of combustor dimensions, operating conditions, and the primary zone mixing parameter for the given combustor airflow characteristics.
- e. The cumulative normal distribution data.
- f. The atomic formula of the fuel.
- g. The combustor air inlet temperature (deg K).
- h. The combustor operating pressure (atm).

- i. A code number identifying the set of kinetic constants employed in the reaction scheme.
- j. The value of the fuel-to-air mass ratio at stoichiometric conditions.
- k. For each element in the distribution function: the mixture ratio (mass fuel to mass fuel and air); the equivalence ratio; the density of the combustion products in  $\text{gm/cm}^3$ ; the adiabatic flame temperature of the combustion products in deg K; the equilibrium mole fraction of  $\text{NO}$ ,  $\text{CO}$ ,  $\text{C}_{(s)}$ , and  $\text{CH}_2$  (unburned hydrocarbons); and the kinetic parameters  $R_1$ ,  $R_6$  (in  $\text{gm-moles/cm}^3\text{-sec}$ ),  $K_1$  and  $K_2$  (dimensionless) defined in Section 2 of Volume 2.
- l. The volume of the primary zone ( $\text{in}^3$ ).
- m. The length of the intermediate zone (in).
- n. The length of the intermediate and dilution zone (combined) (in).
- o'. The mean primary zone equivalence ratio (before the fuel burns).
- p. The combustion efficiency in the primary zone.
- q. The total mass of air fed into the combustor liner (lb/sec).
- r. The degree of mixedness in the primary zone.
- s.. The variable used for altering the mean primary zone equivalence ratio parametrically without changing the over-all air-to-fuel ratio in the combustor.
- t.. The total mass of fuel fed into the combustor (lb/hr).
- u.. The over-all air-to-fuel ratio in the combustor.

The normal output of a typical case continues with the items in category 2-- elemental primary zone conditions for the converged solution. These items, which begin after a statement describing them, consist of:

- a. The mass fraction in the element.
- b. The  $\text{NO}$  concentration in the element (ppm) (vol).
- c. The cumulative sum of the  $\text{NO}$  formed up to and including the element (lb/sec).
- d. The element number.

Only those elements with a finite rate of formation of NO are included in this output table.

The normal output of a typical case continues, after a statement describing the data, with the items in category 3-- over-all primary zone exit conditions from the converged solution. This data consists of:

- a. The axial position in the combustor (in).
- b. The mass mean primary zone equivalence ratio, accounting for the inefficiency of the primary zone combustion.
- c. The mass mean exit temperature of the primary zone (deg F).
- d. The mass mean density of the primary zone combustion products (lb/ft<sup>3</sup>).
- e. The mass mean primary zone residence time (msec).
- f. The mass mean concentration of NO in the primary zone (ppm) (vol).
- g. The mass mean concentration of NO in the primary zone, expressed as NC<sub>2</sub> (lb/1000 lb fuel burned).
- h. The mass mean equilibrium concentration of C<sub>(s)</sub> in the primary zone (ppm) (vol).
- i. The mass mean equilibrium concentration of C<sub>(s)</sub> in the primary zone (lb/1000 lb fuel burned).
- j. The mass mean equilibrium concentration of CO in the primary zone (ppm) (vol).
- k. The mass mean equilibrium concentration of CO in the primary zone (lb/1000 lb fuel burned).
- l. The mass mean equilibrium concentration of unburned hydrocarbons (exclusive of CO and C<sub>(s)</sub>) in the primary zone (ppm) (vol).
- m. The mass mean equilibrium concentration of unburned hydrocarbons (exclusive of CO and C<sub>(s)</sub>) in the primary zone (lb/1000 lb fuel burned).
- n. The fuel loading (lb/sec-ft<sup>3</sup>-atm<sup>2</sup>).

The normal output of a typical case continues, after a statement describing the data, with the items in category 4-- over-all intermediate zone conditions at axial positions in the zone corresponding to the converged solution. This data consists of:

- a. The axial position in the combustor (in).
- b. The mass mean equivalence ratio, at the given axial station in the intermediate zone, accounting for the inefficiency of the primary zone combustion.
- c. The mass mean exit temperature at the given axial station in the intermediate zone, (deg F).
- d. The mass mean density of the combustion products at the given axial station in the intermediate zone ( $\text{lb/ft}^3$ ).
- e. The mass mean residence time of the combustion products from the combustor entrance to the given axial station in the intermediate zone (msec).
- f. The mass mean concentration of NO at the given axial station in the intermediate zone (ppm) (vol).
- g. The mass mean concentration of NO, expressed as  $\text{NO}_2$ , at the given axial station in the intermediate zone ( $\text{lb/1000 lb fuel burned}$ ).
- h. The mass mean equilibrium concentration of  $\text{C}_{(s)}$  at the given axial station in the intermediate zone (ppm) (vol).
- i. The mass mean equilibrium concentration of  $\text{C}_{(s)}$  at the given axial station in the intermediate zone ( $\text{lb/1000 lb fuel burned}$ ).
- j. The mass mean equilibrium concentration of CO at the given axial station in the intermediate zone (ppm) (vol).
- k. The mass mean equilibrium concentration of CO at the given axial station in the intermediate zone ( $\text{lb/1000 lb fuel burned}$ ).
- l. The mass mean equilibrium concentration of unburned hydrocarbons (exclusive of CO and  $\text{C}_{(s)}$ ) at the given axial station in the intermediate zone (ppm) (vol).
- m. The mass mean equilibrium concentration of unburned hydrocarbons (exclusive of CO and  $\text{C}_{(s)}$ ) at the given axial station in the intermediate zone ( $\text{lb/1000 lb fuel burned}$ ).

If the chemical rate of production of NO is frozen at any axial station in the intermediate zone, the program prints a message to that effect and proceeds with the dilution zone calculations and output.

The normal output of a typical case concludes, after a statement describing the data, with the items in category 5-- over-all dilution

zone conditions at axial positions in the zone corresponding to the converged solution. If the chemical rate of formation of NO was frozen at any axial station in the intermediate zone, only the dilution zone exit conditions are printed. The data in this category consists of:

- a. The axial position in the combustor (in).
- b. The mass mean equivalence ratio, at the given axial station in the dilution zone, accounting for the inefficiency of the primary zone combustion.
- c. The mass mean exit temperature at the given axial station in the dilution zone (deg F).
- d. The mass mean density of the combustion products at the given axial station in the dilution zone ( $\text{lb/ft}^3$ ).
- e. The mass mean residence time of the combustion products from the combustor entrance to the given axial station in the dilution zone (msec).
- f. The mass mean concentration of NO at the given axial station in the dilution zone (ppm) (vol).
- g. The mass mean concentration of NO, expressed as  $\text{NO}_2$  at the given axial station in the dilution zone ( $\text{lb/1000 lb fuel burned}$ ).
- h. The mass mean equilibrium concentration of  $\text{C}_{(s)}$  at the given axial station in the dilution zone (ppm) (vol).
- i. The mass mean equilibrium concentration of  $\text{C}_{(s)}$  at the given axial station in the dilution zone ( $\text{lb/1000 lb fuel burned}$ ).
- j. The mass mean equilibrium concentration of  $\text{C}_{(s)}$  at the given axial station in the dilution zone (ppm) (vol).
- k. The mass mean equilibrium concentration of CO at the given axial station in the dilution zone ( $\text{lb/1000 lb fuel burned}$ ).
- l. The mass mean equilibrium concentration of unburned hydrocarbons (exclusive of CO and  $\text{C}_{(s)}$ ) at the given axial station in the dilution zone (ppm) (vol).
- m. The mass mean equilibrium concentration of unburned hydrocarbons (exclusive of CO and  $\text{C}_{(s)}$ ) at the given axial station in the dilution zone ( $\text{lb/1000 lb fuel burned}$ ).

If the chemical rate of prediction of NO is frozen at any axial station in the dilution zone, the program prints a message to that

effect after completing the dilution zone calculations and printing the output at the axial position that corresponds to the combustor exit.

### 3.3.2 Error Messages and Additional Output

In addition to the normal output, various messages may appear in the output of a case. These messages either indicate that difficulty has been encountered during execution of the case or that the user has specified the printing of intermediate output to examine progress in the iterations. The messages are considered below in the order of their appearance in the program.

- a. If intermediate output is requested by the user, the program will print the value of the total mass contained in each mixture ratio element and the value of the parameters that define the range of the mass distribution function. These values are printed in Subroutine ZMASS; they are printed for each converged axial position in the combustor.
- b. If, in calculating the values of  $(\alpha_r)_j$ , the number of iterations on a given element equal ten, the program prints the number of iterations and the last value of  $(\alpha_r)_j$ . This is a nonfatal error as the program assumes the value of  $(\alpha_r)_j$  to be the last value calculated. The error message is printed in Subroutine PRCALC. This error is caused by limiting the number of iterations to ten; it can be relieved by increasing the limit.
- c. POTENTIAL ERROR DUE TO LACK OF CONVERGENCE, SUMTNO(1) =  $\pm X.XXXXXXXXE\pm XX$  PRIOR VALUE OF SUMTNO(1) =  $\pm X.XXXXXXXXE\pm XX$  I = XXX

This message is printed in Subroutine PRCALC for a primary zone element that fails to satisfy convergence criteria after five iterations. This is a nonfatal error as the program assumes that the value of SUMTNO(1) is the last value calculated. The error is caused by limiting the number of iterations to five; it can be remedied by increasing the limit.

- d. If intermediate output is requested by the user, the program will print the value of the nitric oxide content of each mixture ratio element for each converged axial position in the combustor. These values are printed in Subroutine PRINTS.
- e. If the number of iterations attempting to satisfy the mixing criteria equal 40 for any mixture ratio element at any axial station in the intermediate zone, Subroutine ZINTER will print the most recent value of  $E_i$ , and the number of iterations. This is a fatal condition to the program causing immediate termination of the calculations. This procedure is a safety control to keep the program from continuing into an indefinite loop; it is likely caused by some trouble in the calculation of element masses and can only be remedied by detailed examination of the flow rates into and out of each mass element.

f.  $X(CM) = +X.XXXXXE+XX$   $J = XX$   
 AVE.  $RHO(GM/CC) = +X.XXXXXE+XX$   
 AVE.  $NO(GM/GM) = +X.XXXXXE+XX$

This message is printed from Subroutine ZINTER at the end of each iteration loop in the intermediate zone if intermediate output is requested by the user. The meaning of the message is quite clear; both the density and nitric oxide concentrations are mass averages. J is the number of iterations.

g. RUNGE-KUTTA ITERATION FAILED TO CONVERGE TO SPECIFIED LIMIT,  
 $DIFNO = +X.XXXXXE+XX$   $N = XXXX$   $X = CMS$

This nonfatal message is printed by Subroutine ZINTER at each axial position in the intermediate zone where convergence criteria on the NO iterations are not satisfied. N here is the number of steps each major step is divided into for the last iteration; DIFNO identifies the difference in the calculated nitric oxide levels at the end of the major step down the combustor to position X. There are two possible reasons for the appearance of the message:

1. The number of steps allowed in the Runge-Kutta integration are inadequate.

2. The convergence limit is too narrow.

Relaxation of either of these control criteria will eliminate the iteration difficulty.

h.  $X(CM) = +X.XXXXXE+XX$        $J = XX$        $AVE.RHO$   
 $GM/CC) = +X.XXXXXE+XX$        $AVE.NO = +X.XXXXXE+XX$   
 $+X.XXXXXE+XX$        $+X.XXXXXE+XX$

This message is printed from Subroutine DILUTE at the end of each iteration in the dilution zone if intermediate output is requested by the user. The meaning of the message is quite clear except for the last two variables printed; these variables are rate of change of nitric oxide mass fraction with position due to chemical reaction and, dilution, respectively. Both the density and nitric oxide concentrations are mass averages. J is the number of iterations.

i. If intermediate output is requested by the user, Subroutine DILUTE prints the difference between the calculated nitric oxide levels for the last two iterations at the end of each major step down the combustor. In addition, DILUTE also prints the number of integration steps each major step is divided into for the last iteration.

j. RUNGE-KUTTA ITERATION FAILED TO CONVERGE TO SPECIFIED LIMIT.

$DIFNO = +X.XXXXXE+XX$        $N = XXXX$        $X = +X.XXXXXE+XX$

This nonfatal message is printed by Subroutine DILUTE at each axial position in the dilution zone where convergence criteria on the NO iterations are not satisfied. N here is the number of steps each major step is divided into for the last iteration; DIFNO identifies the difference in the calculated nitric oxide levels at the end of the major step down the combustor to position X. There are two possible reasons for the appearance of the message:

1. The number of steps allowed in the Runge-Kutta integration are inadequate.

2. The convergence limit is too narrow.

Relaxation of either of these control criteria will eliminate the iteration difficulty.

### 3.3.3 Description of Sample Case Output

The output from the fictitious sample case described on pages 33 and 34 is presented on pages 35-42. The data on pages 35-38 represents the input data for this fictitious case while calculated results are shown on pages 39-42. From the data it is seen that the mean primary zone residence time for the combustor is 2 msec; and, in that time, a mass average concentration of 300 ppm (vol) of nitric oxide has been formed. Within a distance of 1.5 inches down the combustor intermediate zone, the chemical rate of formation of nitric oxide is negligible in comparison with the amount of nitric oxide previously formed. Consequently, only the dilution of the total nitric oxide formed to that point is important to the final emission figure of 73 ppm (vol).

### 3.4 MISCELLANEOUS OPERATIONAL INFORMATION

Program GASNOX occupies approximately 20,000 core locations during loading and approximately 12,000 core locations during execution on the CDC 6600 computer. Actual program length is approximately 7100 core locations. Hence, the total storage requirement for this program is comfortably within the CDC 6600 core capacity of 131,000 locations.

The execution time for Program GASNOX depends upon the characteristics of the particular combustor being analyzed. It has been found, however, that a typical case will require approximately 10 to 15 seconds of central processor time on the CDC 6600 with another 1 to 2 systems seconds necessary to satisfy input/output requirements. Approximately 12 systems seconds are required to load and compile the program.

There are no known sources of convergence difficulty in the program save the limits imposed on the number and accuracy of the Runge-Kutta integrations. These requirements are adequate for most applications of the program; they are neither too restrictive to cause convergence difficulties nor too loose to permit an abundance of iterations and excessive computer costs.

## 33

ENGINEER: RDS PROJECT: NOx from Gas Turbine Combustors PROJECT NO: 1162  
TITLE: Sample to Illustrate the Use of Program GASNOX SHEET: 1 OF 2

[illegible]

## 34

ENGINEER: RDS PROJECT: NOx from Gas Turbine Combustors PROJECT NO: 1162  
TITLE: Sample to Illustrate the Use of Program GASNOX SHEET: 2 OF 2

[illegible]

## 35

[illegible]

0.	2.00000E+01	3.00000E+00	-0.	-0.
1.00000E+00	3.00000E+01	3.00000E+00	-0.	-0.
2.00000E+00	3.50000E+01	3.00000E+00	-0.	-0.
3.00000E+00	4.00000E+01	3.00000E+00	-0.	-0.
4.00000E+00	4.50000E+01	3.00000E+00	-0.	-0.
5.00000E+00	5.00000E+01	3.00000E+00	-0.	-0.
6.00000E+00	6.00000E+01	3.00000E+00	-0.	-0.
7.00000E+00	7.00000E+01	3.00000E+00	-0.	-0.
8.00000E+00	8.00000E+01	3.00000E+00	-0.	-0.
9.00000E+00	9.00000E+01	3.00000E+00	-0.	-0.
1.00000E+01	1.00000E+02	3.00000E+00	-0.	-0.

**CASE NO. ■** . . . . .

### CUMULATIVE NORMAL DISTRIBUTION DATA

ZP	CUMDIS	ZP	CUMDIS	ZP	CUMDIS	ZP	CUMDIS	ZP	CUMDIS	ZP	CUMDIS	ZP	CUMDIS
0.00	.5000	.50	.6915	1.00	.8413	1.50	.9132	2.00	.9772	2.50	.9938	3.00	.9987
.05	.5159	.55	.7088	1.05	.8531	1.55	.9194	2.05	.9798	2.55	.9946	3.05	.9990
.10	.5398	.60	.7257	1.10	.8643	1.60	.9452	2.10	.9821	2.60	.9953	3.10	.9990
.15	.5596	.65	.7422	1.15	.8749	1.65	.9505	2.15	.9842	2.65	.9960	3.15	.9992
.20	.5753	.70	.7580	1.20	.8849	1.70	.9554	2.20	.9861	2.70	.9965	3.20	.9993
.25	.5987	.75	.7734	1.25	.8944	1.75	.9599	2.25	.9878	2.75	.9970	3.25	.9994
.30	.6179	.80	.7881	1.30	.9032	1.80	.9641	2.30	.9893	2.80	.9974	3.30	.9995
.35	.6368	.85	.8023	1.35	.9115	1.85	.9678	2.35	.9906	2.85	.9978	3.35	.9996
.40	.6554	.90	.8159	1.40	.9192	1.90	.9713	2.40	.9918	2.90	.9981	3.40	.9997
.45	.6736	.95	.8289	1.45	.9265	1.95	.9744	2.45	.9929	2.95	.9984	3.45	.9997



22	0.0022AF-02	1.30000F+00	0.1001F-04	2.75500F+03	1.00000F+04	1.00000F+04	9.41000F-02
23	0.0022AF-02	1.30000F-04	1.10000F-04	2.75500F-04	1.00000F-04	1.00000F-04	1.00000F-04
24	0.0022AF-02	1.30000F+00	1.10000F+00	2.75500F+00	1.00000F+00	1.00000F+00	1.00000F+00
25	0.0022AF-02	1.30000F-04	1.10000F-04	2.75500F-04	1.00000F-04	1.00000F-04	1.00000F-04
26	0.0022AF-02	1.30000F+00	1.10000F+00	2.75500F+00	1.00000F+00	1.00000F+00	1.00000F+00
27	0.0022AF-01	1.30000F-04	1.10000F-04	2.75500F-04	1.00000F-04	1.00000F-04	1.00000F-04
28	0.0022AF-01	1.30000F+00	1.10000F+00	2.75500F+00	1.00000F+00	1.00000F+00	1.00000F+00
29	0.0022AF-01	1.30000F-04	1.10000F-04	2.75500F-04	1.00000F-04	1.00000F-04	1.00000F-04
30	0.0022AF-01	1.30000F+00	1.10000F+00	2.75500F+00	1.00000F+00	1.00000F+00	1.00000F+00
31	0.0022AF-01	1.30000F-04	1.10000F-04	2.75500F-04	1.00000F-04	1.00000F-04	1.00000F-04
32	0.0022AF-01	1.30000F+00	1.10000F+00	2.75500F+00	1.00000F+00	1.00000F+00	1.00000F+00
33	0.0022AF-01	1.30000F-04	1.10000F-04	2.75500F-04	1.00000F-04	1.00000F-04	1.00000F-04
34	0.0022AF-01	1.30000F+00	1.10000F+00	2.75500F+00	1.00000F+00	1.00000F+00	1.00000F+00
35	0.0022AF-01	1.30000F-04	1.10000F-04	2.75500F-04	1.00000F-04	1.00000F-04	1.00000F-04

THE REST OF THE INPUT VARIABLES

THE VOLUME OF THE PRIMARY ZONE IS 5.50000E+01 CU.IN.

THE LENGTH OF THE INTERFACIAL ZONE IS 7.00000E+00 IN.

THE LENGTH OF THE INTERFACIAL ZONE AND DILUTION ZONE (COMBIAFD) IS 1.00000E+01 IN.

THE MEAN PRIMARY ZONE EQUIVALENCE RATIO IS 8.00000E+01

THE COMBUSTION EFFICIENCY IN THE PRIMARY ZONE IS 9.00000E+01

THE TOTAL MASS OF AIR FED INTO THE COMBUSTOR IS 5.00000E+00 LB./SEC.

THE DEGREE OF MIXEDNESS IS 5.00000E+01

ERAT = 1.00000E+00

THE MEAN PRIMARY ZONE RESIDENCE TIME (ONLY APPLIES IF THE VOLUME OF THE PRIMARY ZONE IS ZERO IN INPUT) IS 0. SEC.

THE COMPUTED TOTAL MASS OF FUEL FED INTO THE COMBUSTOR IS 1.95703E+02 LB./HR.

THE COMPUTED OVERALL AIR/FUEL RATIO IS 9.19763E+01

## PRIMARY ZONE EXIT COMPOSITIONS

MASS FRACTION	NO	TOTAL NO	ELEMENT NO.
PPM(VOL)	IR/SEC		
1.00484F-02 0.	0.		1
3.54556F-02 0.	0.		2
7.77667F-02 7.04282E-07	6.44284E-14		3
9.63209F-02 1.38332E-03	1.34357E-10		4
7.03778E-02 3.65236E-02	2.74581E-09		5
5.00434E-02 1.33805E-01	9.71715E-09		6
5.33612E-02 4.09180E-01	3.10081E-08		7
5.69147E-02 1.06374E+00	9.17577E-08		8
5.52783F-02 2.39828E+00	2.124921E-07		9
5.68466F-02 4.64425E+00	4.87494E-07		10
5.35626E-02 3.79710E+02	2.15028E-05		11
5.13500E-02 6.81470E+02	5.74047E-05		12
4.81185F-02 1.03452E+01	1.07530E-04		13
4.68685F-02 1.24321E+03	1.67436E-04		14
4.09380F-02 1.30218F+03	2.37949E-04		15
3.67762F-02 1.07783E+03	2.62517E-04		16
3.25742F-02 7.27704E+02	2.84784E-04		17
2.81198F-02 4.12037E+02	2.90782E-04		18
2.44663F-02 2.04478E+02	3.07825E-04		19
2.05742F-02 9.32173F+01	3.04787E-04		20
1.72139F-02 4.02463F+01	3.04494E-04		21
1.41327F-02 1.68514E+01	3.04740E-04		22
1.15454F-02 6.81227E+00	3.04820E-04		23
9.22063F-02 2.74841F+00	3.04884E-04		24
5.22083F-02 0.	3.04844E-04		25

THIS IS THE MAIN PRINTOUT FOR THE PRIMARY ZONE

X(IN.)	PHI	Y	AVE. DEG F	RHC	TAU	NO	NO <sub>2</sub>	C(S)	C(S)	CO	CO	CH <sub>2</sub>	CH <sub>2</sub>
				AVE.	AVE.	PPM	LBS PER	LBS PER	LBS PER	LBS PER	LBS PER	PPM	LBS PER
				(IN/CLFT)	(IN/CLFT)	(VOL)	1000 LR	1000 LR	1000 LR	1000 LR	1000 LR	(VOL)	1000 LR
							FUEL BURNED	FUEL BURNED	FUEL BURNED	FUEL BURNED	FUEL BURNED		FUEL BURNED
0.00	.72	.3235	.0658	2.00	3.000F+02	9.617F+00	0.	0.	1.453F+04	2.836E+02	1.820F+02	1.776E+00	

-- THE FUEL LOADING IS 5.11234E-02 LB./SEC.-CU.FT.-ATMO.-ATMO.

THIS IS THE MAIN PRINTOUT FOR THE INTERMEDIATE ZONE

X(IN.)	PHI	T	THC	TAU	NO	PPM	NO <sub>2</sub>	C(S)	C(S)	LBS PER 1000 LA	FUEL BURNED	CO	LBS PER 1000 LA	FUEL BURNED	CH <sub>2</sub>	LBS PER 1000 LA	FUEL BURNED
AVE.	DEG F		AVE.	MSEC	(VOL)			PPM	(VOL)			PPM	(VOL)				
.30	.64	3124	.0677	2.27	2.886E+02	1.036E+01	0.	0.	0.	0.	0.	6.433E+03	1.404E+02	1.642E+02	1.795E+00		
.60	.57	2962	.0712	2.53	2.717E+02	1.085E+01	0.	0.	0.	0.	0.	2.845E+03	6.516E+01	1.479E+02	1.797E+00		
.90	.52	2806	.0746	2.78	2.502E+02	1.103E+01	0.	0.	0.	0.	0.	1.221E+03	3.275E+01	1.343E+02	1.801E+00		
1.20	.49	2716	.0764	3.01	2.370E+02	1.112E+01	0.	0.	0.	0.	0.	6.672E+02	1.905E+01	1.268E+02	1.809E+00		
1.50	.47	2656	.0775	3.24	2.264E+02	1.111E+01	0.	0.	0.	0.	0.	4.071E+02	1.214E+01	1.218E+02	1.819E+00		

NITRIC OXIDE REACTION FROZEN AT THIS POINT

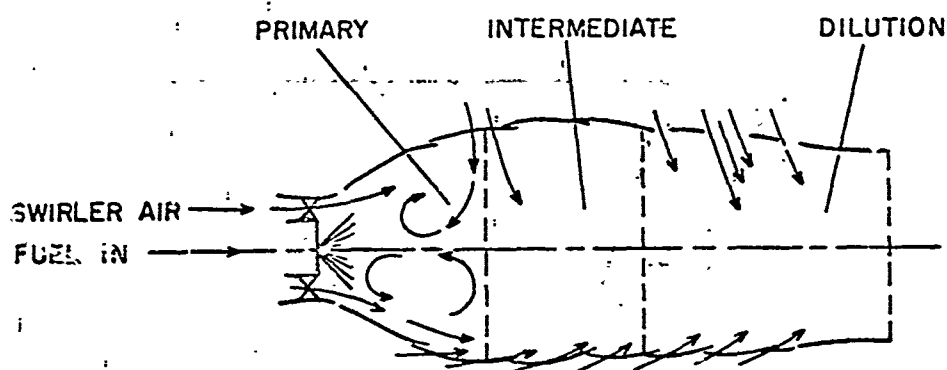
THIS IS THE MAIN PRINTOUT FOR THE CILUTION ZONE

X (IN.)	PHI AVE.	T DEG F	RHC AVE.	TAU AVE.	NO PPM (VOL)	NO <sub>2</sub> LAS PER 1000 LA FUEL BURNED	C (S) PPM (VOL)	C (S) LAS PER 1000 LA FUEL BURNED	CO PPM (VOL)	CO LAS PER 1000 LA FUEL BURNED	CH <sub>2</sub> LAS PER 1000 LA FUEL BURNED
10.00	.16	1513	.0976	7.27	7.288E+01	1.051E+01	0.	0.	4.260E+01	1.870E+00	

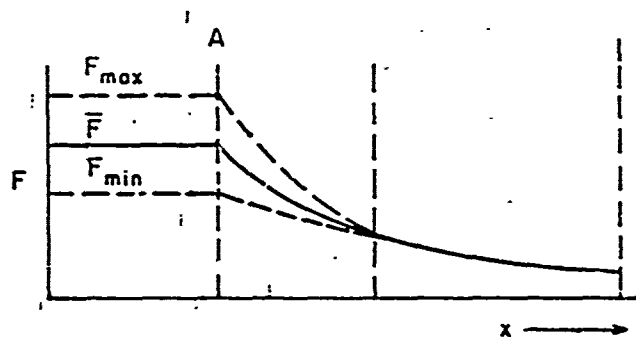
## 4. REFERENCES

1. Danckwerts, P. V., "Continuous Flow Systems, Distribution of Residence Times", Chemical Engineering Science, vol. 1, 1953, pp. 1-13.
2. Jackson, S. R. and Odgers, J., "Factors Influencing Heat Release in Combustion Chambers and Consideration of the Related Materials and Structures", Combustion in Advanced Gas Turbine Systems, Proceedings of an International Propulsion Symposium held at the College of Aeronautics, Cranfield, England, April, 1967.
3. Fletcher, R. S. and Heywood, J. B., A Model for Nitric Oxide Emissions from Aircraft Gas Turbine Engines (AIAA Paper No. 71-123), American Institute of Aeronautics and Astronautics, Presented at the AIAA 9th Aerospace Sciences Meeting, New York, N.Y., January 25-27, 1971.

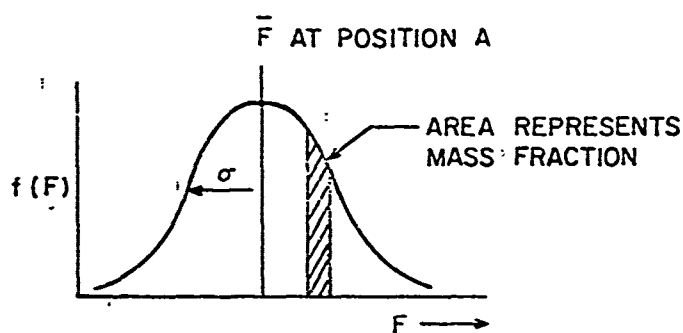
## 5. FIGURES



(a) CROSS SECTION of COMBUSTOR LINER  
SHOWING MEAN FLOW PATTERN

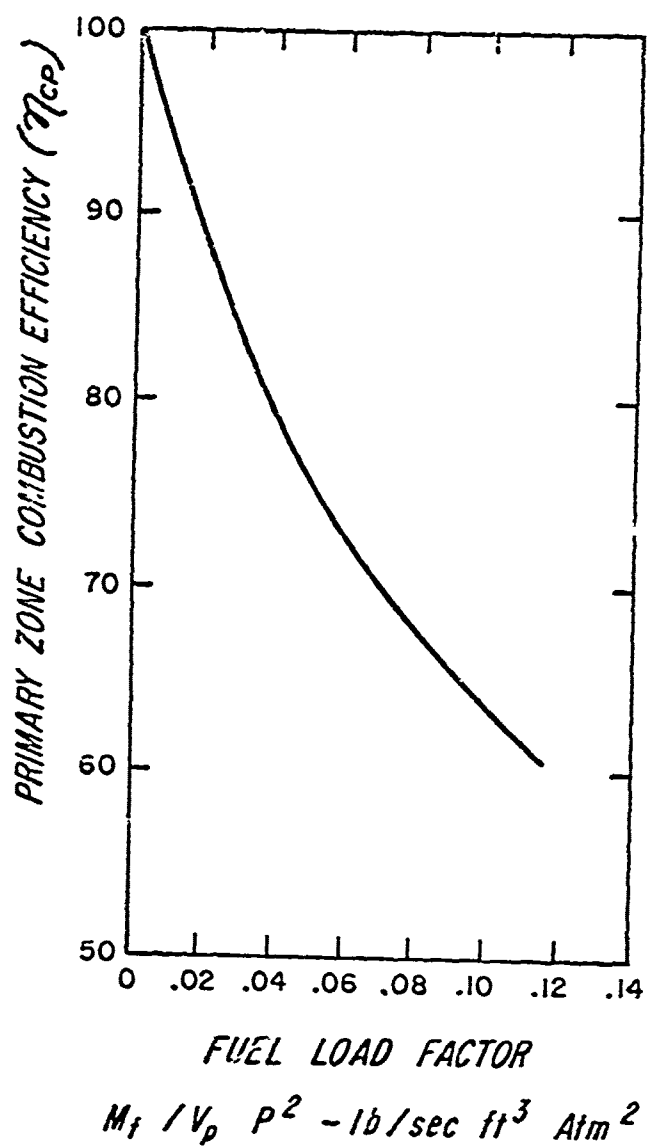


(b) DISTRIBUTION of MIXTURE RATIO  $F$ ,  
ALONG LINER LENGTH



(c) DISTRIBUTION of MASS AS A FUNCTION  
of MIXTURE RATIO and POSITION

Figure 1 ASSUMED FLOW AND DISTRIBUTION PATTERNS  
THROUGHOUT COMBUSTOR LINER



REPRODUCED FROM REFERENCE 2

Figure 2 PRIMARY ZONE  
COMBUSTION EFFICIENCY CORRELATION

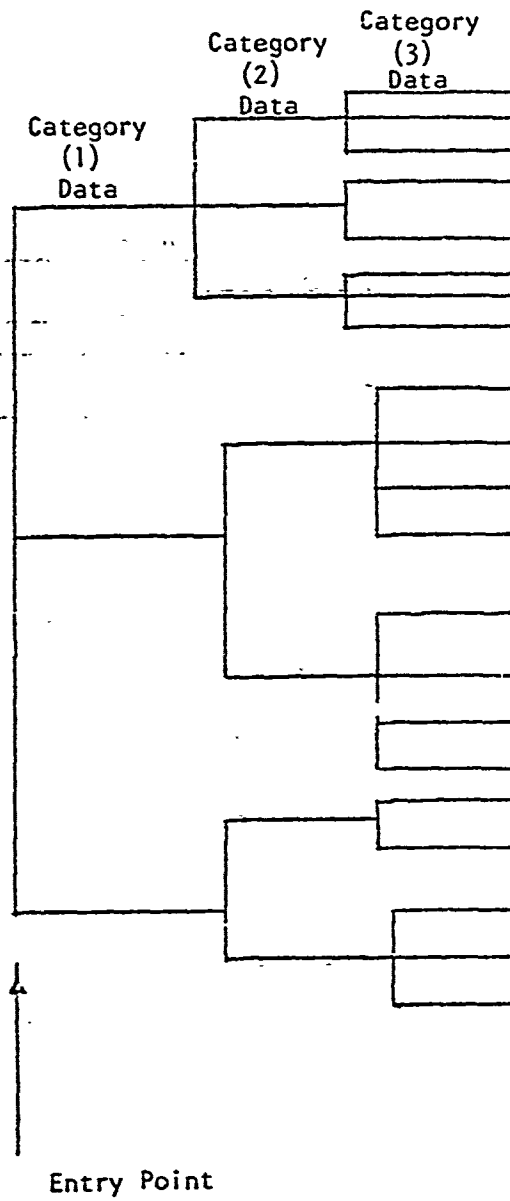


FIGURE 3 - SCHEMATIC REPRESENTATION OF INPUT STRUCTURE

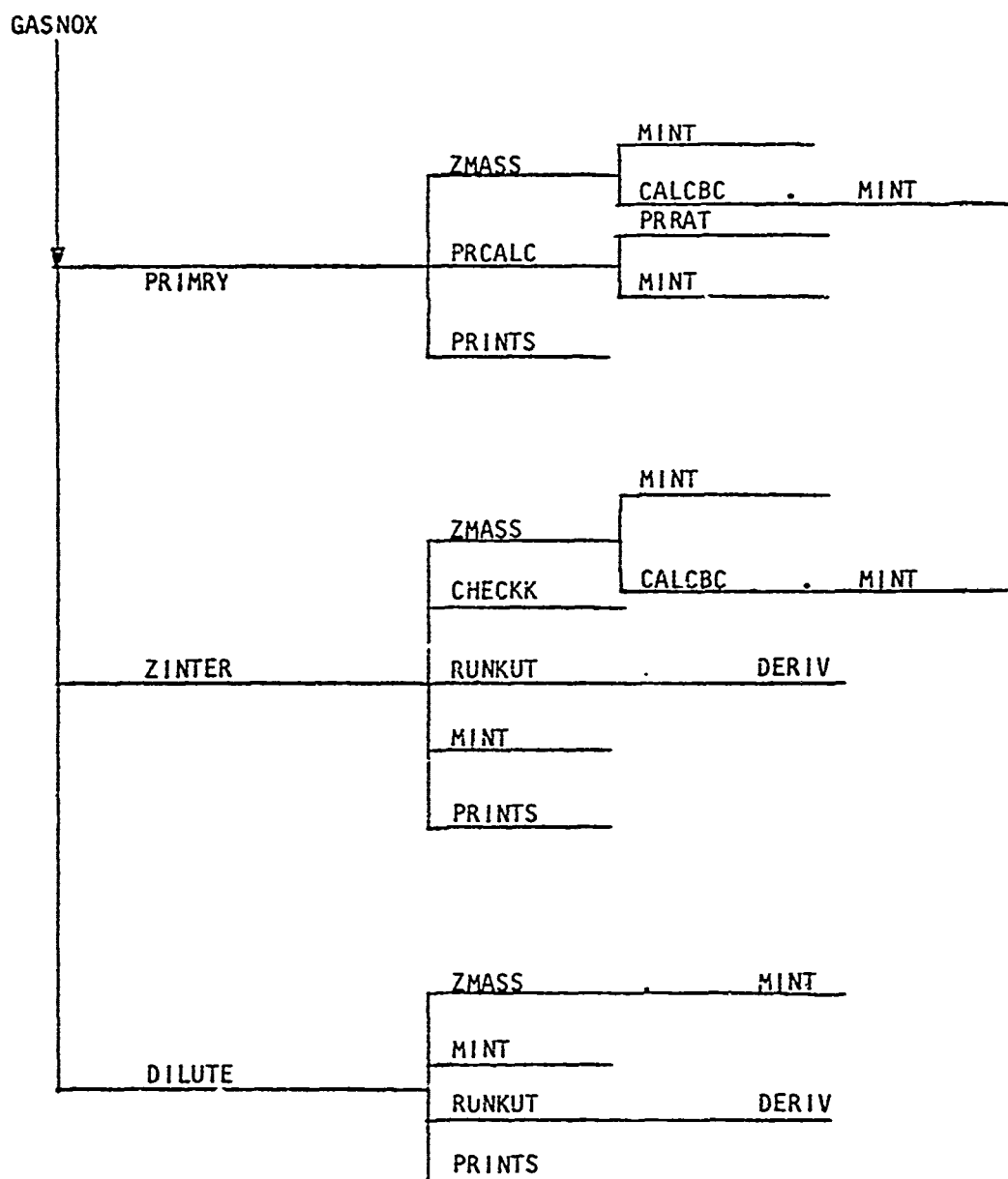


FIGURE 4 - MODULAR TREE DIAGRAM

## 6. NOMENCLATURE

<u>Symbols</u>	<u>Description</u>
$A'$	Preexponential factor in Arrhenius equation
$A$	Total cross-sectional area of combustor liner
$A_1$	Model constant in equation A-15
$A_2$	Model constant in equation A-24
$A_3$	Model constant in equation A-24
$b$	Coefficient in combustor efficiency parameter
$C$	Normalizing factor in distribution function
$E$	Activation energy
$f$	Fraction of mass $\delta m$
$F$	Mixture ratio, (fuel mass/total mass)
$k$	Reaction rate constant
$K$	Fraction of mass $\delta m$ leaving control value over $\delta x$
$L$	Length of intermediate zone
$\dot{m}$	Total mass flow rate in combustor liner
$\dot{m}_a$	Mass flow rate of diluent air per unit length
$M_{NO}$	Molecular weight of nitric oxide
$[NO]$	Mass fraction of nitric oxide, (Mass NO/total mass)
$[\Delta NO]$	$\{[NO]' - [NO]_x\}$
$P$	Pressure
$\dot{\omega}$	Rate of formation of nitric oxide per unit volume
$R$	Gas constant
$R_n$	Equilibrium rate of reaction
$\dot{R}$	$d/dx$ ( $\in \delta m$ )
$t$	Time
$T$	Temperature
$V$	Velocity
$V^*$	Characteristic combustor velocity
$V_p$	Volume of primary zone
$x$	Axial distance
$\delta A$	Cross-sectional area of element with mixture ratio $F$
$\delta m$	Mass rate of element with mixture ratio $F$
$\delta F$	Range of $F$ about $F$ in element with mass
$\alpha$	Nitric oxide concentration as fraction of equilibrium

<u>Symbols</u>	<u>Description</u>
$\epsilon$	Fractional mass flow of unburned fuel, $m_{fu}/m$
$\beta$	Fraction of fuel burned in primary zone
$\sigma$	Standard deviation
$\rho$	Density
$\tau$	Residence time
$\theta$	Combustion efficiency parameter

<u>Subscripts</u>	<u>Description</u>
$a$	Dilution air
$f$	Total fuel
$fu$	Unburned fuel
$F$	With characteristic mixture ratio $F$
$i$	$i$ element in series
$L$	State below that indicated by *
$P$	Condition in primary zone
$t$	With characteristic residence time $t$
$u$	State above that indicated by *
$o$	Condition at entrance to intermediate zone

<u>Superscripts</u>	<u>Description</u>
$( )'$	Condition at entry to control volume
$( )''$	Condition at exit from control volume
$( )^*$	Condition of combustor products entrained into control volume
$( - )$	Mass average value

## 7. APPENDICES

## APPENDIX I - OVER-ALL PROGRAM LOGIC

Program GASNOX consists of a main routine and twelve subroutines. The subroutines are PRIMRY, ZINTER, DILUTE, PRCALC, PRRAT, CHECKK, CALCBC, RUNKUT, DERIV, MINT, ZMASS, and PRINTS. Information is transmitted within the computer program through blocks of COMMON and as arguments of certain subroutines. The over-all control of the programmed calculation procedure is maintained by the main routine.

The logic flow begins at the start of the main routine where the input data is read and then printed. Subroutine PRIMRY, which controls the combustor primary zone calculations, is then called.

The primary zone is modeled as a partially stirred reactor, with the variations in gas composition, temperature, and residence time taken into account statistically. Thus, PRIMRY first calls Subroutine ZMASS to calculate element masses. ZMASS, in turn, calls Subroutines MINT and CALCBC. MINT provides interpolated values of tabulated functions of one variable assuming a linear relationship between the adjacent tabular entries. CALCBC calculates values of the mass flow coefficient at each axial station of the combustor primary and intermediate zones. CALCBC also calls Subroutine MINT. After calling ZMASS, Subroutine PRIMRY calls Subroutines PRCALC and PRINTS. PRCALC controls and calculates the average nitric oxide level in the primary zone for each specified mixture ratio element in the mass distribution function. PRCALC calls Subroutines PRRAT and MINT to conduct its calculations; PRRAT solves the analytical expression relating the elemental nitric oxide concentration to the elapsed time in the primary zone. PRINTS provides the written output of the calculated results of the program.

Having completed the primary zone calculations, GASNOX calls Subroutine ZINTER to perform and control the intermediate zone analysis if the primary zone mixing parameter is other than zero. If the mixing parameter is set at zero, GASNOX skips over the intermediate zone calculations and proceeds with dilution zone calculations via Subroutine DILUTE.

The intermediate zone of the combustor is divided into a series of finite length axial elements in which the heterogeneous products from the primary zone mix with one another and with the entering cooling air. By the end of the zone the distribution is collapsed to a uni-dimensional profile. To accomplish this mixing process ZINTER calls on Subroutines ZMASS, CHECKK, RUNKUT, MINT, and PRINTS. The function of Subroutines ZMASS and MINT are as before; PRINTS writes the calculated mass mean conditions at the end of each finite length axial combustor segment. Subroutine CHECKK calculates the proportionality constant between the mass flow rate out of an element due to mixing and the total mass flowing into it at a given axial position in the combustor. RUNKUT is employed to obtain the solution to the first order ordinary differential equation between nitric oxide concentration and axial position in the combustors by the Gill variation of the Runge-Kutta numerical integration scheme. In doing so, RUNKUT calls Subroutine DERIV which calculates the rate of nitric oxide formation with respect to axial distance in the combustor intermediate or dilution zone.

In the dilution zone, the flow is uni-dimensional with the gases uniformly mixed across each cross section. To perform and control these calculations GASNOX calls on Subroutine DILUTE. DILUTE in turn calls on Subroutines ZMASS, MINT, RUNKUT, and PRINTS for calculations and printout at specified axial stations in the zone. The only deviation of these subroutines from their previously described functions occurs in ZMASS: since the mixture ratio distribution is collapsed to a flat profile, it omits reference to Subroutine CALCBC.

This concludes the description of the over-all logic structure of Program GASNOX. A modular diagram of GASNOX is provided as Figure 4.

## APPENDIX II - COMMON FORTRAN NOMENCLATURE

The following tables contain the COMMON Fortran nomenclature for Program GASNOX. COMMON consists of seven labeled blocks; the nomenclature is arranged in alphabetic order for each block. Singly subscripted arrays are indicated by their respective indices.

I - Element index

J - Incremental station index for the X direction

K - Distribution index

Nomenclature for COMMON/DATA1/

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AIR(J)	$M_A _X$	Combustor airflow at axial station X	gm/sec
ATT(I)	$T_i$	Adiabatic flame temperature for an element i	deg K
A1	$A_1$	Exponent in relationship governing collapse of mixture ratio distribution function	
A2	$A_2$	Factor in relationship defining the rate at which unburned fuel is burned in the intermediate zone	
A3	$A_3$	Exponent in relationship defining the rate at which unburned fuel is burned in the intermediate zone	
BCON1(I)	$(C_{(s)_i})_e$	Equilibrium mole fraction of carbon for an element i	
BCON2(I)	$(CO_i)_e$	Equilibrium mole fraction of carbon monoxide for an element i	
BCON6(I)	$(NO_i)_e$	Equilibrium mole fraction of nitric oxide for an element i	
BETA		Combustion efficiency in the primary zone	
CH2(I)	$(CH_{2,i})_e$	Equilibrium mole fraction of unburned hydrocarbons exclusive of $C_{(s)}$ and CO for an element i	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
CN	$C_N$	Mixing characteristic	
CUMDIS(K)		Value of cumulative normal distribution	
EN <sub>S</sub>	$k_s$	Fuel-to-air mass ratio at stoichiometric conditions	
EK1(I)	$(K_1)_i$	Ratio of forward reaction rate constants (see Volume 2, Section 2 or Ref 3)	
EK2(I)	$(K_2)_i$	Ratio of forward reaction rate constants (see Volume 2, Section 2 or Ref 3)	
FF(I)	$F_i$	Mixture ratio	
FNOXP	$(NO_0)$	NO formed in the flame front	ppm
PHIP	$\bar{\phi}_p$	Mean primary zone equivalence ratio accounting for the inefficiency of the primary zone combustion	
PPP	P	Operating pressure	atm
RHO	$\rho_i$	Density of combustion products for an element	gm/cm <sup>3</sup>
RR(J)	$R_x$	Radius of combustor liner if canannular configuration; equivalent radius of combustor liner if annular configuration	in; cm
R1(I)	$(R_1)_i$	Forward reaction rate for the first kinetic reaction (see Volume 2, Section 2 or Ref 3)	gm-mole/cm <sup>3</sup> -sec
R6(I)	$(R_6)_i$	Forward reaction rate for the sixth kinetic reaction (see Volume 2, Section 2 or Ref 3)	gm-mole/cm <sup>3</sup> -sec
S	$S_0$	Degree of mixedness in the primary zone	
VP	$V_p$	Volume of the primary zone	in <sup>3</sup> ; cm <sup>3</sup>
XEND	XEND	Length of intermediate zone and dilute zone (combined)	in; cm
XL	$X_L$	Length of intermediate zone	in; cm
XX(J)	X	Axial position in the combustor	in; cm

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
ZP(K)	$Z_p$	Limit of integration of cumulative normal distribution	

Nomenclature for COMMON/OUT1/

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AVCH2D	$[\overline{CH_2}]_e$	Average equilibrium concentration of unburned hydrocarbons exclusive of $C_{(s)}$ and CO at a given axial station in the combustor	gm/cc
AVCH2F	$\{CH_2\}_e$	Average equilibrium concentration of unburned hydrocarbons exclusive of $C_{(s)}$ and CO at a given axial station in the combustor	gm/1000 gm fuel burned
AVCH2G	$[CH_2]_e$	Average equilibrium concentration of unburned hydrocarbons exclusive of $C_{(s)}$ and CO at a given axial station in the combustor	
AVCH2P	$\{CH_2\}_e$	Average equilibrium concentration of unburned hydrocarbons exclusive of $C_{(s)}$ and CO at a given axial station in the combustor	ppm(vol)
AVECOD	$[\overline{CO}]_e$	Average equilibrium concentration of CO at a given axial station in the combustor	gm/cc
AVECOF	$\{CO\}_e$	Average equilibrium concentration of CO at a given axial station in the combustor	gm/1000 gm fuel burned
AVECOG	$[CO]_e$	Average equilibrium concentration of CO at a given axial station in the combustor	
AVECOP	$\{CO\}_e$	Average equilibrium concentration of CO at a given axial station in the combustor	ppm(vol)
AVECSD	$[\overline{C_s}]_e$	Average equilibrium concentration of $C_{(s)}$ at a given axial station in the combustor	gm/cc
AVECSF	$\{C_s\}_e$	Average equilibrium concentration of $C_{(s)}$ at a given axial station in the combustor	gm/1000 gm fuel burned
AVECSG	$[C_s]_e$	Average equilibrium concentration of $C_{(s)}$ at a given axial station in the combustor	

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AVECSP	$\{\bar{C}_s\}_e$	Average equilibrium concentration of $C_{(s)}$ at a given axial station in the combustor	ppm(vol)

Nomenclature for COMMON/OUT2/

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AVENFU	$[\bar{NO}]_{up}$	Average nitric oxide concentration at prior axial station in the combustor	gm/1000 gm fuel burned
AVENOD	$[\bar{NO}]^*$	Average nitric oxide concentration at a given axial station in the combustor	gm/cc
AVENOF	$[\bar{NO}]$	Average nitric oxide concentration at a given axial station in the combustor	gm/1000 gm fuel burned
AVENOG	$[\bar{NO}]$	Average nitric oxide concentration at a given axial station in the combustor	
AVENOP	$\{\bar{NO}\}$	Average nitric oxide concentration at a given axial station in the combustor	ppm(vol)
ILAST		Indicator ILAST = 0 if the nitric oxide chemical reaction is not frozen at a given axial position in the combustor ILAST = 1 if the nitric oxide chemical reaction is frozen at a given axial position in the combustor	
RRO	$(\bar{P})_{rr}$	Mean density of combustion products at a given axial station in the combustor	gm/cc

Nomenclature for COMMON/OUT3/

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AVET	$\bar{T}$	Average temperature of combustion products at a given axial station in the combustor	deg K
FBARD	$\bar{F}$	Mean mixture ratio at a given axial station in the combustor	
IMAX	$i_{MAX}$	Subscript of mass element with highest equivalence ratio	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
INDIC		Indicator INDIC = 1 for primary zone INDIC = 2 for intermediate zone type calculation INDIC = 3 for dilution zone type calculation	
LEN		Indicator LEN = 0 if intermediate zone calculations end at $X_i$ LEN = 1 if intermediate zone calculations end at $X_{END}$	
NO(I)	$[NO_i]$	Nitric oxide concentration for an element i of the distribution function	
PHIBAR	$\bar{\Phi}$	Mean equivalence ratio at a given axial station in the combustor	
RHCBAR	$\bar{\rho}$	Mean density of combustion products at a given axial station in the combustor	gm/cc
TAUBAR	$\bar{\tau}$	Mean residence time in the combustor at a given axial station	sec
TAUDIL	$\bar{\tau}_{DIL}$	Mean residence time in the combustor dilution zone	sec
TAUINT	$\bar{\tau}_{INT}$	Mean residence time in the combustor intermediate zone	sec
VELOC	V	Velocity of combustion products at a given axial station in the combustor	cm/sec
XD	$X_D$	Axial position (downstream) in the combustor	cm
XU	$X_U$	Axial position (upstream) in the combustor	cm

Nomenclature for COMMON/OUT4/

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AIRD	$M_A _{X_D}$	Airflow at a given axial station in the combustor	gm/sec

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
ANO	$[\overline{NO}]_{AN}$	Average nitric oxide concentration at a given axial station in the combustor	
AQQ	Q	Measure of the round-off error in the Runge-Kutta integration routine at a given axial station in the combustor	
AREAD	$A _{x_D}$	Cross-sectional area of combustor at a given axial station in the combustor	cm <sup>2</sup>
ASLOPE	$(\frac{\partial \dot{M}_A}{\partial X})_{x_D}$	Rate of change of airflow rate in the combustor liner with axial position at a given axial station in the combustor	gm/sec-cm
AVEMW	$\overline{MW}$	Average molecular weight of reaction products at a given axial station in the combustor	gm/gm-mole
CONGNO(I)	$[NO^*]_{i_e}$	Nitric oxide equilibrium concentration for an element i of the distribution function	
DDM(I)	$(\delta \dot{M}_i)_D$	Elemental mass flow rate at the downstream limit of integration	gm/sec
DELMD(I)	$(\Delta \dot{M}_i)_D$	Elemental mass flow rate at the downstream limit of integration	gm/sec
DIFNO(I)		Difference in NO concentrations for successive iterations for an element i of the distribution function	
DMDDA(I)	$(\dot{m}_A)''_i$	Elemental mass flow of gases into control volume due to mixing of the dilution air with previously mixed gases	gm/sec-cm
DMDDM(I)	$(\dot{m}_M)''_i$	Elemental mass flow of gases into control volume due to mixing action of gases already within the combustion liner	gm/sec-cm
DMDDP(I)	$(\dot{m}')_i$	Total elemental mass flow of gases into control volume due to mixing	gm/sec-cm
DMDDPP(I)	$(\dot{m}'')_i$	Total elemental mass flow of gases out of control volume due to mixing	gm/sec-cm
DMFFED	$(\dot{M}_f)_{fed}$	Total mass flow of fuel fed to the combustor	gm/sec

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
DMFT	$(\dot{M}_f)_{x_D}$	Total mass flow of combusted fuel at a given axial station in the combustor	gm/sec
DMFUD	$(\dot{M}_{fu})_{x_D}$	Total mass flow of unburned fuel at a given axial station in the combustor	gm/sec
DMFUO	$(\dot{M}_f)_o$	Total mass flow of unburned fuel at the primary zone exit	gm/sec
E(I)	$E_i$	Proportionality factor between mass flow rate out of an element i due to mixing and the total mass flowing into it	$\text{cm}^{-1}$
EKKD	$K_D$	Proportionality factor between mass flow rate out of an element due to mixing and the total mass flowing into it	$\text{cm}^{-1}$
FB(I)	$(F_B)_i$	Boundaries between which each mixture ratio value applies	
FPRIME(I)	$(F')_i$	Mixture ratio at entrance to elemental control volume i	
NOEQXD	$[\overline{\text{NO}}]_{e, x_D}$	Mass average nitric oxide equilibrium concentration at a given axial station in the combustor	
NOP(I)	$[\text{NO}]_i$	Nitric oxide concentration of the mass flowing into an elemental control volume due to mixing at a given axial station in the combustor	
NOZERO(I)		Indicator NOZERO = 0 if chemical rate of production of NO in an element i is finite NOZERO = 1 if chemical rate of product of NO in an element is zero	
RDOT(I)	$\dot{R}_i$	Elemental rate of change of unburned fuel with axial station in the combustor	gm/sec-cm
RSUBX	$R_{x_D}$	Combustor radius at a given axial station in the combustor	cm
SIG	$\sigma$	Standard deviation of the distribution function at a given axial station in the combustor	
SIGZER	$\sigma_o$	Standard deviation of the distribution function in the primary zone of the combustor	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
SLOPE(I)	$\left[ \frac{\partial (\dot{S} \dot{M}_i)}{\partial x} \right]_{x_D}$	Rate of change of elemental mass flow rate with axial position at a given axial station in the combustor	gm/sec-cm
SUEA(I)		Difference in NO concentrations for successive iterations for an element i of the distribution function	
TSLOPE	$\left[ \frac{\partial \dot{m}^*}{\partial x} \right]_{x_D}$	Rate of change of total mass flow rate with axial position at a given axial station in the combustor	gm/sec-cm
UDM(I)	$(\dot{S} \dot{M}_i)_u$	Elemental mass flow rate at the upstream limit of integration	gm/sec

Nomenclature for COMMON /OUT5/

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
MSTARD	$\dot{M}_D^*$	Total mass flow at downstream limit of integration	gm/sec
MSTARU	$\dot{M}_U^*$	Total mass flow at upstream limit of integration	gm/sec
DILL	$(\dot{r})_{DIL}$	Rate of change of NO concentration with axial position in the combustor dilution zone due to air dilution	cm <sup>-1</sup>
REAT	$(\dot{r})_{react}$	Rate of change of elemental NO concentration with axial position in the combustor due to chemical reaction	cm <sup>-1</sup>

## APPENDIX III - MAIN ROUTINE GASNOX

The principal function of the main routine is to control the logic of the calculation procedure for the prediction of the nitric oxide emissions from gas turbine combustors. In addition, the main routine reads and writes the input data, sets certain values, and performs many related minor calculations.

The main routine calls Subroutines PRIMARY, ZINTER, and DILUTE. The external input required by the main routine consists of:

ANNR	ANR	APR	ARR	ATT
AXX	BCON1	BCON2	BCON6	BETA
CH2	EKS	EK1	EK2	EQUIV
ERAT	FF	IDATA	IN	KASE
PH1	PHIP	PPP	RHO	R1
R6	S	SET	TAUBAR	TOTAIR
VP	XEND	XL		

The external output provided by the main routine consists of:

ANNR	ANR	APR	ARR	ATT
AXX	BCON1	BCON2	BCON6	BETA
CH2	CUMDIS	EKS	EK1	EK2
EQUIV	ERAT	FF	NOZERO	PH1
PHIP	PPP	RHO	R1	R6
S	SET	TAUBAR	TOTAIR	XEND
XL	VP	ZP		

Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols in the main routine which are not part of COMMON. Singly and doubly subscripted arrays are indicated by their respective indices:

- I - General index of descriptive data
- IJ - Incremental axial station index for combustor air
- J - Element index

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AAR(IJ)	$\dot{M}_{A,X}$	Total mass of airflow into combustor liner at position X (cumulative)	lb/sec
ANNR(IJ)	$R_{X_0}$	Outer radius of liner at position X; applies only for annular configuration	in
AWR(IJ)	$R_{X_1}$	Inner radius of liner at position X; applies only for annular configuration	in
APR(IJ)	$(\dot{M}_{A,X})\%$	Per cent of total mass of airflow into combustor liner at position X (cumulative)	
ARR(IJ)	$R_X$	Radius of liner at position X; applies only for canannular configuration	in
AXX	X	Axial position in the combustor	in
DELAIR	$\Delta M_{AIR}$	Combustor air scaling factor	lb/sec
DEX	$\Delta X$	Combustor length	in
EQUIV	$\phi_p$	Mass mean equivalence ratio in the primary zone (before fuel burns)	
ERAT	$E_{rat}$	Variable for varying $\phi_p$ parametrically yet maintaining constant air-to-fuel ratio in the combustor	
IDATA		Number of sets of kinetic, thermodynamic, and equilibrium data and combustor inlet conditions	
IN		Number of sets of combustor dimensions, operating conditions, and primary zone mixedness parameter	
KASE		Number of sets of airflow distribution data	
PHI(J)	$\phi_j$	Equivalence ratio of an element j	
SET(1)		Combustor descriptive data	
TOTALR	$\dot{M}_A$	Total mass of air fed into the combustor liner	lb/sec

### Analysis Procedure

The step-by-step procedure of the main routine is given below. The Fortran listing of the routine is presented at the conclusion of the step-by-step procedure.

1. Read the input kinetic, thermodynamic, and equilibrium data and the combustor inlet conditions for the case.
2. Set the values of certain parameters.
3. Read the input airflow distribution data.
- Step 4 is performed only if the combustor is an annular configuration.
4. Calculate the equivalent can radii as:  

$$R_X = \left[ (R_{X_0})^2 - (R_{X_1})^2 \right]^{\frac{1}{2}}$$
5. Read the input combustor dimensions, operating conditions, and primary zone mixing parameter.
6. Convert the percentage airflow data to mass flow for each specified axial station by the relationship:  

$$(M_A)_X = (M_{A_X})_{\%} * M_A / 100.0$$
7. Calculate  $\bar{\phi}_p$  as  

$$\bar{\phi}_p = \phi_p * S$$
8. Calculate  $\bar{\phi}_p$  as:  

$$\bar{\phi}_p = \bar{\phi}_p * E_{rat}$$
9. Set the values of certain parameters and constants.
10. Write the heading for the airflow distribution data for the case.
11. Calculate the total mass of airflow into the combustor liner for each specified axial station correcting for the effect of  $E_{rat}$ .
12. Convert the units of the airflow distribution data to the metric system.
13. Write the input data.
14. Convert the units of the combustor dimensions to the metric system.
15. Using Subroutine PRIMARY, calculate the primary zone exit conditions.

16. Set certain indicators.

Step 17 is performed only if  $X_{\text{END}} = 0$ .

17. Go to step 24.

Step 18 is performed only if  $S_o = 0$ .

18. Go to step 23.

19. If  $X_{\text{END}} < X_L$ , reset certain indicators.

20. Using Subroutine ZINTER, perform the intermediate zone calculations.

Step 21 is performed only if the chemical rate of formation of nitric oxide is frozen in the intermediate zone.

21. Go to step 23.

Step 22 is performed only if  $X_{\text{END}} < X_L$ .

22. Go to step 24.

23. Using Subroutine DILUTE, perform the dilution zone calculations.

24. If this is the last set of combustor dimensions, operating conditions, and primary zone mixing parameter for the given airflow distribution, continue to step 25. If not, return to step 5.

25. If this is the last set of combustor airflow distribution data for the given kinetic, thermodynamic, and equilibrium data and combustor inlet conditions, continue to step 26. If not, return to step 3.

26. If this is the last set of kinetic, thermodynamic, and equilibrium data and combustor inlet conditions, continue to step 27. If not, return to step 1.

27. Stop.

```

PROGRAM GASNOX(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT)
DIMENSION SET(25),PHI(50),AAR(50),AXX(50),APR(50),ARR(50),ANR(50),
1ANNR(50)
COMMON/DATA1/AIR(50),RR(50),XX(50),FF(50),BCON1(50),BCON2(50),CH2
150),ZP(70),CUMDIS(70),VP,RHO(50),BCON6(50),ATT(50),POP,FNOXP,R1(50)
2),R6(50),EK1(50),EK2(50),A2,A3,XL,CN,BETA,S,PHIP,EKS,XEND,A1
COMMON/OUT1/AVECSG,AVECOG,AVCH2G,AVECSP,AVECOP,AVCH2P,AVECSD,AVECOGAS
1D,AVCH2D,AVECSF,AVECOF,AVCH2F
COMMON/OUT2/AVENOG,AVENOD,AVENOP,AVENOF,AVENFU,RR0,ILAST
COMMON/OUT3/INDIC,NO(50),AVET,TAUBAR,RHOBAR,PHIBAR,IMAX,XD,
1FBARU,XU,LEN,TAI'INT,TAUDIL,VELOC
COMMON/OUT4/CONC(NO(50),DELM(50),AREAD,ASLOPE,DMFUD,SLOPE(50),TSLOGAS
1PE,NUP(50),EKKD,DMFT,UDM(50),DDM(50),FP(50),DMFUD,AIRD,DMFFEDGAS
2,RSUBX,SIG,SIGZER,AVEMW,DMDDA(50),DMDDM(50),DMDDP(50),DMDDPP(50),F
3PRIME(50),NOEQXD,ANO,AQQ,DIFNO(50),NOZERO(50),ROOT(50),E(50)
COMMON/OUT5/MSTARU,MSTARU
DATA(ZP(L),L=1,70)/0.0,0.05,0.10,0.15,0.20,0.25,0.30,0.35,0.40,0.45,
15,0.50,0.55,0.60,0.65,0.70,0.75,0.80,0.85,0.90,0.95,1.0,1.05,1.10,
21.15,1.20,1.25,1.30,1.35,1.40,1.45,1.50,1.55,1.60,1.65,1.70,1.75,1.8
3.80,1.85,1.90,1.95,2.00,2.05,2.10,2.15,2.20,2.25,2.30,2.35,2.40,2.45,
445,2.50,2.55,2.60,2.65,2.70,2.75,2.80,2.85,2.90,2.95,3.00,3.05,3.1
50,3.15,3.20,3.25,3.30,3.35,3.40,3.45,
DATA(CUMDIS(L),L=1,70)/0.5000,0.5199,0.5398,0.5596,0.5793,0.5987,0.6179,
1.6179,0.6368,0.6554,0.6736,0.6915,0.7088,0.7257,0.7422,0.7580,0.77
234,0.7881,0.8023,0.8159,0.8289,0.8413,0.8531,0.8643,0.8749,0.8849,
30.8944,0.9032,0.9115,0.9192,0.9265,0.9332,0.9394,0.9452,0.9505,0.95
4554,0.9599,0.9641,0.9678,0.9713,0.9744,0.9772,0.9798,0.9821,0.9842,
5.9861,0.9878,0.9893,0.9906,0.9918,0.9929,0.9939,0.9946,0.9953,0.99
660,0.9965,0.9970,0.9974,0.9978,0.9981,0.9984,0.9987,0.9989,0.9990,
70.9992,0.9993,0.9994,0.9995,0.9996,0.9997,0.9997/
C****
C**** READ IN AND WRITE OUT THE REQUIRED DATA
C****
READ(5,50) IDATA
DO 925 I1K =1,IDATA
READ(5,400) (SET(I),I=1,15),PPP,SET(16),SET(17),SET(18),SET(19),EKSGAS
400 FORMAT(12A6/2A6,A2,E15.8,3A6,A4,E15.8)
DO 600 J = 1,35
READ(5,450) FF(J),PHI(J),RHO(J),ATT(J),BCON6(J),BCON2(J),BCON1(J),CS
1H2(J),R1(J),R6(J),EK1(J),EK2(J)
NOZERO(J)=0
IF(RH(J).EQ.0.0.AND.R1(J).EQ.0.0) NOZERO(J)=1
600 CONTINUE
450 FORMAT(6E12.5)
READ(5,50) KASE
50 FORMAT(I6)
DO 900 IJ = 1,KASE
DO 300 IJ =1,11
READ(5,250) AXX(IJ),APR(IJ),ARR(IJ),ANR(IJ),ANNR(IJ)
XX(IJ) = AXX(IJ)
RR(IJ) = ARR(IJ)
IF(RR(IJ).EQ.0.0) RR(IJ) = SQRT(ANNR(IJ)**2.0-ANR(IJ)**2.0)
300 CONTINUE
250 FORMAT(5E12.5)
READ(5,200) IN
200 FORMAT(I6)
DO 325 K =1,IN
READ(5,410) VP,XL,XEND,EQUIV,BETA,TOTAIR,S,ERAT,TAUBAR
DO 425 IJ=1,11
AAR(IJ) = APR(IJ)*TOTAIR/100.0

```

```

425 CONTINUE
    PHIP = EGUIV*BETA
    PHIP=PHIP*ERAT
    FNOXP = 0.0
    CN = 5.0
    A1 = 0.5
    A2 = 0.5
    A3 = 1.0
410 FORMAT(6E12.5/6E12.5)
    DELAIR=AAR(1)*(1.0-1.0/ERAT)
    DEX=XX(11)-XX(1)
    WRITE(6,100)
    WRITE(6,775)
775 FORMAT(///49X,34HCOMBUSTOR AIR FLOW CHARACTERISTICS///)
    WRITE(6,780)
780 FORMAT(64X,3HCAN,21X,7HANNULAR)
    WRITE(6,785)
785 FORMAT(28X,8HDISTANCE,8X,10HPERCENTAGE,9X,6HRADIUS,8X,12HINNER RAD
    IUS,5X,12HOUTER RADIUS)
786 FORMAT(45X,8HAIR FLOW)
    WRITE(6,786)
    WRITE(6,790)
790 FORMAT(29X,6HINCHES,28X,6HINCHES,11X,6HINCHES,11X,6HINCHES///)
    DO 350 IJ=1,11
    AIR(IJ)=AAR(IJ)-DELAIR*(XX(11)-XX(IJ))/DEX
    WRITE(6,825) AXX(IJ),APR(IJ),ARR(IJ),ANR(IJ),AVNR(IJ)
825 FORMAT(26X,5(E12.5,5X))
    AIR(IJ) = AIR(IJ)*454.
    IF(K.GT.1) GO TO 350
    XX(IJ) = XX(IJ)*2.54
    RR(IJ) = RR(IJ)*2.54
350 CONTINUE
    WRITE(6,500) K
500 FORMAT(///58X,11HCASE NO. = ,I6///)
    WRITE(6,550)
550 FORMAT(///48X,35HCUMULATIVE NORMAL DISTRIBUTION DATA///)
    WRITE(6,115)
115 FORMAT(14X,2HZP,3X,6HCUMDIS,5X,2HZP,3X,6HCUMDIS,5X,2HZP,3X,6HCUMDIS,5X,2
    1S,5X,2HZP,3X,6HCUMDIS,5X,2HZP,3X,6HCUMDIS,5X,2HZP,3X,6HCUMDIS,5X,2
    2HZP,3X,6HCUMDIS///)
    DO 120 L=1,10
    WRITE(6,110) ZP(L),CUMDIS(L),ZP(L+10),CUMDIS(L+10),ZP(L+20),CUMDIS(L+20),
    1(L+20),ZP(L+30),CUMDIS(L+30),ZP(L+40),CUMDIS(L+40),ZP(L+50),CUMDIS(L+50),
    2(L+50),ZP(L+60),CUMDIS(L+60)
110 FORMAT(12X,7(F4.2,3X,F6.4,3X))
120 CONTINUE
    WRITE(6,100)
    WRITE(6,650)
650 FORMAT(///58X,16HEQUILIBRIUM DATA///)
    WRITE(6,675) (SET(I),I=1,15),PPP,SET(16),SET(17),SET(18),SET(19),EK
    1S
675 FORMAT(1X,14A6,A2,E15.8/33X,3A6,A4,E15.8///)
    WRITE(6,680)
680 FORMAT(1X,123HTHE FOLLOWING DATA TABLE CONTAINS THE THERMODYNAMIC
    1PROPERTIES,KINETIC RATE CONSTANTS,AND EQUILIBRIUM COMPOSITIONS FOR
    2 EACH/1X,124HPRESCRIBED EQUIVALENCE RATIO. FOR EACH ELEMENT THESE
    3 PROPERTIES ARE,IN ORDER OF PRINTING...MIXTURE RATIO,EQUIVALENCE RA
    4TIO,/1X,119HDENSITY,ADIABATIC FLAME TEMPERATURE,NO,C0,C(S),AND CHGAS
    52(UNBURNED HYDROCARBONS) EQUILIBRIUM MOLE FRACTION,AND THE KINETIC
    6/1X,27HPARAMETERS R1,R0,K1,AND K2.//)

```

```

WRITE(6,690)
690 FORMAT(24X,7HELEMENT/)
DO 750 J =1,35
WRITE(6,700) J,FF(J),PHI(J),RHO(J),ATT(J),BCON6(J),BCON2(J),BCON1(
1J),CH2(J),R1(1),R6(J),EK1(J),EK2(J)
700 FORMAT(26X,I2,3X,6E12.5/31X,6E12.5)
750 CONTINUE
WRITE(6,100)
WRITE(6,850)
850 FORMAT(///51X,31HTHE REST OF THE INPUT VARIABLES///)
WRITE(6,851) VP
851 FORMAT(10X,34HTHE VOLUME OF THE PRIMARY ZONE IS ,E12.5,7H CU.IN.//
1)
WRITE(6,852) XL
852 FORMAT(10X,39HTHE LENGTH OF THE INTERMEDIATE ZONE IS ,E12.5,4H IN.
1//)
WRITE(6,853) XEND
853 FORMAT(10X,67HTHE LENGTH OF THE INTERMEDIATE ZONE AND DILUTION ZONE
1E(COMBINED) IS ,E12.5,4H IN.//)
WRITE(6,854) EQUIV
854 FORMAT(10X,43HTHE MEAN PRIMARY ZONE EQUIVALENCE RATIO IS ,E12.5//)
WRITE(6,855) BETA
855 FORMAT(10X,49HTHE COMBUSTION EFFICIENCY IN THE PRIMARY ZONE IS ,E1
12.5//)
WRITE(6,856) TTAIR
856 FORMAT(10X,48HTHE TOTAL MASS OF AIR FED INTO THE COMBUSTOR IS ,E12
1.5,9H LB./SEC.//)
WRITE(6,857) S
857 FORMAT(10X,27HTHE DEGREE OF MIXEDNESS IS ,E12.5//)
WRITE(6,858) ERAT
858 FORMAT(10X,7HERAT = ,E12.5//)
WRITE(6,859) TAUBAR
859 FORMAT(10X,105HTHE MEAN PRIMARY ZONE RESIDENCE TIME(ONLY APPLIES I
1F THE VOLUME OF THE PRIMARY ZONE IS ZERO IN INPUT) IS ,E12.5,5H SE
2C.)
VP = VP*2.54*2.54*2.54
XL = XL*2.54
XEND = XEND*2.54
100 FORMAT(1H1)
C****
C**** PERFORM PRIMARY ZONE CALCULATIONS
C****
CALL PRIMRY
C****
C**** PERFORM INTERMEDIATE ZONE CALCULATIONS
C****
LEN = 0
IF(XEND.EQ.0.0) GO TO 1000
IF(S.EQ.0.0) GO TO 950
IF(XEND.LT.XL) LEN = 1
CALL ZINTER
C****
C**** PERFORM DILUTION ZONE CALCULATIONS
C****
IF(ILAST.EQ.1) GO TO 950
IF(LEN.EQ.1) GO TO 1000
950 CALL DILUTE
1000 CONTINUE
325 CONTINUE
900 CONTINUE

```

GAS\*1200  
 GAS\*1210  
 GAS\*1220  
 GAS\*1230  
 GAS\*1240  
 GAS\*1250  
 GAS\*1260  
 GAS\*1270  
 GAS\*1280  
 GAS\*1290  
 GAS\*1300  
 GAS\*1310  
 GAS\*1320  
 GAS\*1330  
 GAS\*1340  
 GAS\*1350  
 GAS\*1360  
 GAS\*1370  
 GAS\*1380  
 GAS\*1390  
 GAS\*1400  
 GAS\*1410  
 GAS\*1420  
 GAS\*1430  
 GAS\*1440  
 GAS\*1450  
 GAS\*1450  
 GAS\*1470  
 GAS\*1480  
 GAS\*1490  
 GAS\*1500  
 GAS\*1510  
 GAS\*1520  
 GAS\*1530  
 GAS\*1540  
 GAS\*1550  
 GAS\*1560  
 GAS\*1570  
 GAS\*1580  
 GAS\*1590  
 GAS\*1600  
 GAS\*1610  
 GAS\*1620  
 GAS\*1630  
 GAS\*1640  
 GAS\*1650  
 GAS\*1660  
 GAS\*1670  
 GAS\*1680  
 GAS\*1690  
 GAS\*1700  
 GAS\*1710  
 GAS\*1720  
 GAS\*1730  
 GAS\*1740  
 GAS\*1750  
 GAS\*1760  
 GAS\*1770  
 GAS\*1780  
 GAS\*1790

925 CONTINUE  
STOP  
END

GAS\*1800  
GAS\*1810  
GAS\*1820

## APPENDIX IV - SUBROUTINE PRIMRY

The function of Subroutine PRIMRY is to calculate the nitric oxide emissions at the primary zone exit of a gas turbine combustor.

Subroutine PRIMRY is called by the main routine (GASNOX); it, in turn, calls Subroutines PRCALC, ZMASS, and PRINTS. The subroutine does not require external input but does provide external output. Internal input and output are transmitted through COMMON. The internal input consists of:

ATT	BCON1	BCON2	BCON6	CH2
FNOXP	PHIP	PPP	RHO	S
TAUBAR	VP			

The internal output consists of:

ANO	AVCH2D	AVCH2F	AVCH2G	AVCH2P
AVECOD	AVECOF	AVECOG	AVECOP	AVECSD
AVECSF	AVECSG	AVECSP	AVEMW	AVENOD
AVENOF	AVENOG	AVENOP	AVET	CONGNO
FNOXG	INDIC	PHIBAR	RHOBAR	TAUBAR
VELOC	XD	XU		

The external output consists of:

FELD	I	QQNO	QSUMNO
------	---	------	--------

Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols used in Subroutine PRIMRY which are not included in COMMON.

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
CH2AV	$(\overline{\text{CH}_2})_e$	Average equilibrium mole fraction of unburned hydrocarbons exclusive of $\text{C}_{(s)}$ and CO in the primary zone	
COAV	$(\overline{\text{CO}})_e$	Average equilibrium mole fraction of CO in the primary zone	
CSAV	$(\overline{\text{C}_{(s)}})_e$	Average equilibrium mole fraction of $\text{C}_{(s)}$ in the primary zone	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
DELX	$\Delta X$	Increment of the combustor length across which the solution is generated	cm
FELD(I)	$(M_{frac})_i$	Element i mass fraction	
FNOXG	$[NO]_o$	NO formed in the flame front (mass fraction)	
I	i	Index of the element	
NPRINT		Indicator NPRINT = 0 if intermediate output is not requested by the user NPRINT = 1 if intermediate output is requested by the user	
QQNO(I)	$[NO]_i$	Nitric oxide concentration in the element i	ppm(vol)
QSUMNO(I)	$\sum NO-m$	The cumulative sum of the NO formed up to and including the element i	lb/sec
SUMCHI	$\sum CH-m$	Sum of the elemental mass flow rates times their respective unburned hydrocarbon (exclusive of CO and $C_{(s)}$ ) equilibrium mole fractions	gm/sec
SUMCOI	$\sum CO-m$	Sum of the elemental mass flow rates times their respective CO equilibrium mole fractions	gm/sec
SUMCSI	$\sum C_{(s)}-m$	Sum of the elemental mass flow rates times their respective $C_{(s)}$ equilibrium mole fractions	gm/sec
SUMNOI	$\sum NO-m$	Sum of the elemental mass flow rates times their respective NO mass fractions	gm/sec
SUMTI	$\sum T-m$	Sum of the elemental mass flow rates times their respective adiabatic flame temperatures	gm-deg K/sec

#### Analysis Procedure

The step-by-step procedure of Subroutine PRIMARY is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. Convert  $(NO)_o$  to  $[NO]$  by  

$$[NO] = (NO)_o \times 10^{-6} \times \frac{30.0}{28.0}$$
2. Set the values of  $X_U$ ,  $X_D$ , and  $\Delta X$  as:  

$$X_U = 0.0$$
  

$$X_D = 0.0$$
  

$$\Delta X = 0.0$$
3. Using Subroutine ZMASS, calculate the mass in each element, the mean mixture ratio, the airflow, and the total mass flow.

4. Calculate  $\bar{p}$  as:  

$$\bar{p} = \frac{\sum_{i=1}^{L_{MAX}} \rho_i (A \bar{u}_i)_D / \bar{m}_D^*}{S_D \neq 0}$$
  

$$\bar{p} = \rho_{i_{MAX}} \quad S_D = 0$$

Step 5 is performed if  $V_p \neq 0.0$

5. Go to step 8.
6. Calculate  $V_p$  as:

$$V_p = \frac{\bar{T} \cdot \bar{m}_D^*}{\bar{p}}$$

7. Go to step 9.
8. Calculate  $\bar{T}$  as:

$$\bar{T} = \frac{V_p \cdot \bar{p}}{\bar{m}_D^*}$$

9. Calculate  $[NO]_e$  as:

$$[NO]_e = \frac{\sum_{i=1}^{L_{MAX}} (NO)_e \cdot 30.0}{\rho_i \cdot T_i \cdot 82.057/P} \quad S_D \neq 0$$

$$[NO]_e = \frac{(NO)_{i_{MAX}} \cdot 30.0}{\rho_{i_{MAX}} \cdot T_{i_{MAX}} \cdot 82.057/P} \quad S_D = 0$$

10. Using Subroutine PRCALC, calculate the NO concentration in each element in the distribution.

Step 11 is performed only if intermediate output is requested by the user.

11. Write the heading identifying the primary zone elemental exit conditions.

12. For each element in which  $m_i$  is non-zero, calculate  $\sum NO-m$ ,  $\sum C_{(s)}-m$ ,  $\sum CO-m$ ,  $\sum CH-m$ ,

$$\sum T-m, \quad \text{and} \quad (M_{\text{frac}})_i \quad \text{as:}$$

$$\sum NO-m = \sum_{i=1}^{I_{\text{MAX}}} [NO]_i (\Delta M_i)_D$$

$$\sum C_{(s)}-m = \sum_{i=1}^{I_{\text{MAX}}} (C_{(s)})_i (\Delta M_i)_D$$

$$\sum CO-m = \sum_{i=1}^{I_{\text{MAX}}} (CO)_i (\Delta M_i)_D$$

$$\sum CH-m = \sum_{i=1}^{I_{\text{MAX}}} (CH_2)_i (\Delta M_i)_D$$

$$\sum T-m = \sum_{i=1}^{I_{\text{MAX}}} T_i (\Delta M_i)_D$$

$$(M_{\text{frac}})_i = (\Delta M_i)_D / M_D^*$$

Steps 13-14 are performed only if intermediate output is requested by the user.

13. Convert the units of  $\sum NO-m$  from gm/sec to lb/sec.

14. Convert the units of  $[NO]_i$  from mass fraction to ppm(vol) -  $\frac{\text{gm-mole}}{\text{gm}}$

15. Calculate  $[NO]$ ,  $\bar{T}$ , and  $\bar{MW}$  as:

$$[NO] = \sum NO-m / M_D^*$$

$$\bar{T} = \sum T-m / M_D^*$$

$$\bar{MW} = \bar{P} + \bar{T} * 82.057 / P$$

Steps 16-17 are performed only if intermediate output is requested by the user.

16. Convert the units of  $[NO]_i$  from ppm(vol) -  $\frac{\text{gm-mole}}{\text{gm}}$  to ppm(vol).

17. For each element in the distribution, write the element mass fraction, the nitric oxide concentration (ppm-vol),

the cumulative sum of the NO formed up to and including the element, and the element number.

18. Calculate  $\bar{\phi}$  as

$$\bar{\phi} = \bar{\phi}_p$$

19. Calculate V as

$$V = M_D^* / \bar{e} * A |_{x_D}$$

20. Calculate  $\{\bar{NO}\}$ ,  $[\bar{NO}]$ ,  $[\bar{NO}]$  as:

$$\{\bar{NO}\} = [\bar{NO}] * 10^6 * \bar{MW} / 30.0$$

$$[\bar{NO}] = [\bar{NO}] * \bar{e}$$

$$[\bar{NO}] = [\bar{NO}] * M_D^* * 1000 / (\dot{M}_f)_{x_D}$$

21. Calculate  $(\bar{C}_{(s)})_e$ ,  $(\bar{CO})_e$ , and  $(\bar{CH}_2)_e$  as:

$$(\bar{C}_{(s)})_e = \sum C_{(s)-m} / M_D^*$$

$$(\bar{CO})_e = \sum CO-m / M_D^*$$

$$(\bar{CH}_2)_e = \sum CH_2-m / M_D^*$$

22. Calculate  $[\bar{C}_{(s)}]_e$ ,  $[\bar{CO}]_e$ , and  $[\bar{CH}_2]_e$  as:

$$[\bar{C}_{(s)}]_e = (\bar{C}_{(s)})_e * 12 / \bar{MW}$$

$$[\bar{CO}]_e = (\bar{CO})_e * 28 / \bar{MW}$$

$$[\bar{CH}_2]_e = (\bar{CH}_2)_e * 14 / \bar{MW}$$

23. Calculate  $\{\bar{C}_{(s)}\}_e$ ,  $\{\bar{CO}\}_e$ , and  $\{\bar{CH}_2\}_e$  as:

$$\{\bar{C}_{(s)}\}_e = [\bar{C}_{(s)}]_e * 10^6 * \bar{MW} / 12$$

$$\{\bar{CO}\}_e = [\bar{CO}]_e * 10^6 * \bar{MW} / 28$$

$$\{\bar{CH}_2\}_e = [\bar{CH}_2]_e * 10^6 * \bar{MW} / 14$$

24. Calculate  $[\bar{C}_{(s)}^*]_e$ ,  $[\bar{CO}^*]_e$ , and  $[\bar{CH}_2^*]_e$  as:

$$[\bar{C}_{(s)}^*]_e = [\bar{C}_{(s)}]_e * \bar{P}$$

$$[\bar{CO}^*]_e = [\bar{CO}]_e * \bar{P}$$

$$[\bar{CH}_2^*]_e = [\bar{CH}_2]_e * \bar{P}$$

25. Calculate  $[\bar{C}_{(s)}]_e$ ,  $[\bar{CO}]_e$ , and  $[\bar{CH}_2]_e$  as:

$$[\bar{C}_{(s)}]_e = [\bar{C}_{(s)}^*]_e * \dot{M}_D^* * 1000 / (\dot{M}_F)_{X_D}$$

$$[\bar{CO}]_e = [\bar{CO}^*]_e * \dot{M}_D^* * 1000 / (\dot{M}_F)_{X_D}$$

$$[\bar{CH}_2]_e = [\bar{CH}_2^*]_e * \dot{M}_D^* * 1000 / (\dot{M}_F)_{X_D}$$

26. Using Subroutine PRINTS, write the output for the primary zone.
27. Return.

```

SUBROUTINE PRIMARY
REAL NO
REAL MSTARD,MSTARU
DIMENSION QQNO(50),QSUMNO(50),FELD(50)
COMMON/DATA1/AIR(50),RR(50),XX(50),FF(50),BCON1(50),BCON2(50),CH2(
150),ZP(70),CUMCIS(70),VP,RHO(50),BCON6(50),ATT(50),PPP,FNOXP,R1(50
2),R6(50),EK1(50),EK2(50),A2,A3,XL,CN,BETA,S,PHIP,EKS,XEND,A1
COMMON/OUT1/AVECSG,AVECOG,AVCH2G,AVECSP,AVECOP,AVCH2P,AVECSD,AVECOP
1D,AVCH2D,AVECSF,AVECOF,AVCH2F
COMMON/OUT2/AVENOG,AVENOD,AVENOP,AVENOF,AVENFU,RRO,ILAST
COMMON/OUT3/INDIC,NO(50),AVET,TAUBAR,RHOBAR,PHIBAR,IMAX,XD,
1FBARD,XU,LEN,TAUINT,TAUDIL,VELOC
COMMON/OUT4/CONGNO(50),DELMD(50),AREAD,ASLOPE,DMFUO,SLOPE(50),TSLOP
1PE,NOP(50),EKKD,DMFT,UDM(50),DDM(50),FB(50),DMFUD,AIRD,DMFFED
2,RSUBX,SIG,SIGZER,AVEMW,DMDDA(50),DMDDM(50),DMDDP(50),DMDDPP(50),F
3PRIME(50),NOEQXD,ANO,AQQ,DIFNO(50),NOZERO(50),RDOT(50),E(50)
COMMON/OUT5/MSTARD,MSTARU
NPRINT=1
INDIC = 1
C****
C**** CONVERT FLAME NO UNITS (NOTE...MEAN MW TAKEN AS 28.0)
C****
FNOXG=FNOXP*1.0E-06*(30.0/28.0)
C****
C**** CALCULATE MASS IN EACH ELEMENT
C****
XU = 0.0
XD = 0.0
DELX = 0.0
CALL ZMASS(DELX)
WRITE(6,100)
C****
C**** CALCULATE AVERAGE RHO AND TAU
C****
RHOBAR = 0.0
DO 1000 I = 1,IMAX
IF(S.EQ.0.0.AND.I.LT.IMAX) GO TO 1000
RHOBAR = RHOBAR+RHO(I)*DELMD(I)/MSTARD
1000 CONTINUE
IF(VP.NE.0.0) GO TO 1025
VP=TAUBAR*MSTARD/RHOBAR
GO TO 1050
1025 TAUBAR=(VP*RHOBAR/MSTARD)
1050 CONTINUE
C****
C**** DO NO CALCULATIONS
C****
SUMNOI = 0.0
SUMTI = 0.0
SUMCSI = 0.0
SUMCOI = 0.0
SUMCHI = 0.0
DO 2000 I = 1,IMAX
IF(S.EQ.0.0.AND.I.LT.IMAX) GO TO 2000
CONGNO(I) = BCON6(I)*30.0/(RHO(I)*ATT(I)*82.057/PPP)
2000 CONTINUE
CALL PRCALC(FNOXG)
IF(NPRINT.EQ.0) GO TO 2500
WRITE(6,9987)
9987 FORMAT(///,52X,28HPRIMARY ZONE EXIT CONDITIONS)

```

PRI\*0000  
 PRI\*0010  
 PRI\*0020  
 PRI\*0030  
 PRI\*0040  
 PRI\*0050  
 PRI\*0060  
 PRI\*0070  
 PRI\*0080  
 PRI\*0090  
 PRI\*0100  
 PRI\*0110  
 PRI\*0120  
 PRI\*0130  
 PRI\*0140  
 PRI\*0150  
 PRI\*0160  
 PRI\*0170  
 PRI\*0180  
 PRI\*0190  
 PRI\*0200  
 PRI\*0210  
 PRI\*0220  
 PRI\*0230  
 PRI\*0240  
 PRI\*0250  
 PRI\*0260  
 PRI\*0270  
 PRI\*0280  
 PRI\*0290  
 PRI\*0300  
 PRI\*0310  
 PRI\*0320  
 PRI\*0330  
 PRI\*0340  
 PRI\*0350  
 PRI\*0360  
 PRI\*0370  
 PRI\*0380  
 PRI\*0390  
 PRI\*0400  
 PRI\*0410  
 PRI\*0420  
 PRI\*0430  
 PRI\*0440  
 PRI\*0450  
 PRI\*0460  
 PRI\*0470  
 PRI\*0480  
 PRI\*0490  
 PRI\*0500  
 PRI\*0510  
 PRI\*0520  
 PRI\*0530  
 PRI\*0540  
 PRI\*0550  
 PRI\*0560  
 PRI\*0570  
 PRI\*0580  
 PRI\*0590

```

WRITE(6,9988)
9988 FORMAT(///,46X,4HMASS,9X,2HNO,8X,8HTOTAL NO,7X,7HELEMENT)
WRITE(6,9989)
9989 FORMAT(44X,8HFRACTION,5X,8HPPM(VOL),5X,6HLB/SEC,10X,3HNO.,/)
2500 CONTINUE
DO 3000 I =1,IMAX
  IF(DELMD(I).EQ.0.0) GO TO 3000
  SUMNOI = SUMNOI+NO(I)*DELMD(I)
  SUMCSI = SUMCSI+BCON1(I)*DELMD(I)
  SUMCOI = SUMCOI + BCON2(I)*DELMD(I)
  SUMCHI = SUMCHI+CH2(I)*DELMD(I)
  SUMTI = SUMTI+ATT(I)*DELMD(I)
  FELDI = DELMD(I)/MSTARD
  IF(NPRINT.EQ.0) GO TO 3000
  QSUMNO(I) = SUMNOI/454.0
  QQNO(I) = NO(I)*1.0E+06/30.0
3000 CONTINUE
  AVENOG = SUMNOI/MSTARD
  ANO = AVENOG
  AVET = SUMTI/MSTARD
  AVEMW = RHOBAR*AVET*82.057/PPP
  IF(NPRINT.EQ.0) GO TO 3200
  DO 3100 I =1,IMAX
    QQNO(I) = QQNO(I)*AVEMW
  WRITE(6,9990) FELDI,QQNO(I),QSUMNO(I),I
9990 FORMAT(42X,3E12.5,7X,I3)
3100 CONTINUE
3200 CONTINUE
C****
C**** CALCULATE VELOCITY AND PHIBAR
C****
  PHIBAR = PHIP
  VELOC = MSTARD/(RHOBAR*AREAD)
  AVENOP=AVENOG*1.0E+06*AVEMW/30.0
  AVENOD = AVENOG*RHOBAR
  AVENOF = AVENOG*MSTARD*1000./DMFT
  CSAV = SUMCSI/MSTARD
  COAV = SUMCOI/MSTARD
  CH2AV = SUMCHI/MSTARD
  AVECSG = CSAV*12.0/AVEMW
  AVECOG = COAV*28.0/AVEMW
  AVCH2G = CH2AV*14.0/AVEMW
  AVECSF=AVECSG*1.0E+06*AVEMW/12.0
  AVECOF=AVECOG*1.0E+06*AVEMW/28.0
  AVCH2F=AVCH2G*1.0E+06*AVEMW/14.0
  AVECSU = AVECSG*RHOBAR
  AVECOU = AVECOG*RHOBAR
  AVCH2U = AVCH2G*RHOBAR
  AVECSF=AVECSG*MSTARD*1000.0/DMFT
  AVECOF = AVECOG*MSTARD*1000./DMFT
  AVCH2F = AVCH2G*MSTARD*1000./DMFT
  CALL PRINTS
100 FORMAT(1H1)
  RETURN
  END

```

PRI\*0600  
 PRI\*0610  
 PRI\*0620  
 PRI\*0630  
 PRI\*0640  
 PRI\*0650  
 PRI\*0660  
 PRI\*0670  
 PRI\*0680  
 PRI\*0690  
 PRI\*0700  
 PRI\*0710  
 PRI\*0720  
 PRI\*0730  
 PRI\*0740  
 PRI\*0750  
 PRI\*0760  
 PRI\*0770  
 PRI\*0780  
 PRI\*0790  
 PRI\*0800  
 PRI\*0810  
 PRI\*0820  
 PRI\*0830  
 PRI\*0840  
 PRI\*0850  
 PRI\*0860  
 PRI\*0870  
 PRI\*0880  
 PRI\*0890  
 PRI\*0900  
 PRI\*0910  
 PRI\*0920  
 PRI\*0930  
 PRI\*0940  
 PRI\*0950  
 PRI\*0960  
 PRI\*0970  
 PRI\*0980  
 PRI\*0990  
 PRI\*1000  
 PRI\*1010  
 PRI\*1020  
 PRI\*1030  
 PRI\*1040  
 PRI\*1050  
 PRI\*1060  
 PRI\*1070  
 PRI\*1080  
 PRI\*1090  
 PRI\*1100  
 PRI\*1110  
 PRI\*1120  
 PRI\*1130  
 PRI\*1140

## APPENDIX V - SUBROUTINE ZINTER

The function of Subroutine ZINTER is to calculate the concentration of nitric oxide at specified axial stations, and at the exit, of the intermediate zone of a gas turbine combustor.

Subroutine ZINTER is called by the main routine (GASNGX); it, in turn, calls Subroutines MINT, CHECKK, RUNKUT, ZMASS, and PRINTS. The subroutine does not require external input but does provide external output. Internal input and output are transmitted through COMMON.

The internal input consists of:

ATT	BCON1	BCON2	BCON6	CH2
CN	CONGNO	EKS	EK1	EK2
FF	LEN	NO	NOZERO	PPP
RHO	RSUBX	R1	R6	TAUBAR
XD	XEND	XL		

The internal output consists of:

ANO	AQQ	AVCH2D	AVCH2F	AVCH2G
AVCH2P	AVECOD	AVECOF	AVECOG	AVECOP
AVECSD	AVECSF	AVECSG	AVECSP	AVEMW
AVENFU	AVENOD	AVENOF	AVENOG	AVENOP
AVET	CONGNO	DMDDA	DMDDM	DMDDP
DMDDPP	EKKD	ILAST	INDIC	LEN
NO	NOP	PHIBAR	RHOBAR	RRO
TAUBAR	TAUINT	VELOC	XD	XU

The external output consists of:

AVNO	AVRHO	DDFNO	E	IEE
J	N	XD		

Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols used in Subroutine ZINTER which are not included in COMMON:

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AVNO(J)	NO <sub>j</sub>	Mass average nitric oxide concentration for a given iteration j at the end of each major step in the combustor	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AVRHO(J)	$\bar{\rho}_j$	Mass average density of the combustion products for a given iteration j at the end of each major step in the combustor	gm/cc
AVVNO	rat <sub>1</sub>	Ratio of total nitric oxide mixing out of the elements to the total mass mixing into the elements	
AVVNOG	$\bar{NO}$	Mass average nitric oxide concentration for a given iteration at a given axial step in the combustor	
CH2AV	$(\bar{CH}_2)_e$	Mass average equilibrium mole fraction of unburned hydrocarbons (exclusive of $C_{(s)}$ and CO) at a given axial station in the combustor	
CNOLST	$[\bar{NO}]_{IK}$	Nitric oxide equilibrium concentration for the last incremental step in the intermediate zone	
COAV	$(\bar{CO})_e$	Mass average equilibrium mole fraction of carbon monoxide at a given axial station in the combustor	
CSAV	$(\bar{C}_s)_e$	Mass average equilibrium mole fraction of $C_{(s)}$ at a given axial station in the combustor	
DDFNO	$[\Delta NO]$	Measure of difference in the calculated NO levels after successive iterations at a given axial station in the combustor	
DELTA X	$\Delta X$	Integration step size (major) in the intermediate zone	cm
DELX	$\delta X$	Increment of the combustor length across which the solution is generated	cm
DIFNO	$[\Delta NO]$	Measure of difference in the calculated NO levels after successive iterations at a given axial station in the combustor	
DUMMY	$[\bar{NO}]_{DUM}$	Dummy variable	
EK*	$k_e$	Constant - equal to 0.05	
EK1LST	$(K_1)_{LST}$	Ratio of forward reaction rate constants for the last step in the intermediate zone at the mean mixture ratio (see Volume 2, Section 2 or Ref 3)	

\*Variable initialized but not used in subroutine

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
EK2LST	$(K_2)_{LST}$	Ratio of forward reaction rate constants for the last step in the intermediate zone at the mean mixture ratio (see Volume 2, Section 2 or Ref 3)	
EN	N	Proportionality constant between $\Delta X$ and $\xi X$	
FFF	F	Mean mixture ratio for the last step in the intermediate zone	
FURAT	$[\Delta \overline{NO}]_{\Delta x}$	Measure of change in NO concentration for successive steps in the combustor	
GNOMI	$[NO]_{gm}$	Nitric oxide content of an element i at a given axial station in the combustor	gm
IENDZ		Indicator IENDZ = 0 for all except the last major integration step in the intermediate zone IENDZ = 1 for the last major integration step in the intermediate zone	
II	II	Integration increment index	
IIE	$I_{ie}$	Counter of number of iterations attempting to satisfy $E_i$ criteria	
J	J	Number of iterations for each major axial step in the combustor	
K	K	Number of iterations for each major axial step in the combustor	
KON(I) *		Index KON(I) = 0 if integration for the element has not converged KON(I) = 1 if integration for the element has converged	
LSGN		Indicator LSGN = 1 if intermediate zone and not the last step in the zone LSGN = 2 if intermediate zone and the last step in the zone LSGN = 3 if dilution zone	

\*Variable initialized but not used in subroutine

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
N	N	Proportionality constant between $\Delta X$ and $\delta X$	
NOAVGS**	$[NO]_{spec}$	Nitric oxide concentration of the last element in the array	
NONO(I)	$[NO_i]_{NO}$	Dummy variable	
NOSTAR**	$[NO^*]$	Nitric oxide concentration of the combustion products before air addition at a given axial station in the combustor	
NPRINT		Indicator NPRINT = 0 if intermediate output is not requested by the user NPRINT = 1 if intermediate output is requested by the user	
OUTNO	$[NO]_{0-1}$	Total nitric oxide mixing out of the elements at a given axial station in the combustor intermediate zone	gm/sec-cm
OUTNO2	$[NO]_{0-2}$	Total nitric oxide at a given upstream axial station in the combustor intermediate zone	gm/sec
PINO	$M_{in}$	Total mass mixing into the elements at a given axial station in the combustor	gm/sec-cm
Q(I)	$q_i$	Measure of the round-off error for the element i at a given axial station in the combustor	
QQ(I)	$qq_i$	Measure of the round-off error for the element i at a given axial station in the combustor	
RHOLST	$\rho_{LST}$	Density of combustion products for the last step in the intermediate zone at the mean mixture ratio	gm/cm <sup>3</sup>
RHOMI	$D_p$	Dummy variable	gm <sup>2</sup> /cm <sup>3</sup>
RILST	$(R_1)_{LST}$	Forward reaction rate for the first kinetic reaction for the last step in the intermediate zone at the mean mixture ratio (see Volume 2, Section 2 or Ref 3)	gm-mole/cm <sup>3</sup> -sec

\*\*variable set real but not used in subroutine.

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
R6LST	$(R_6)_{LST}$	Forward reaction rate for the sixth kinetic reaction for the last step in the intermediate zone at the mean mixture ratio (see Volume 2, Section 2 or Ref 3)	gm-mole/cm <sup>3</sup> -sec
STEPS	$n_{step}$	Number of remaining integration steps before end of intermediate zone	
STORE1		Dummy variable	gm-mole/cm <sup>3</sup> -sec
STORE2		Dummy variable	gm-mole/cm <sup>3</sup> -sec
STORE3		Dummy variable	
STORE4		Dummy variable	
STORE5		Dummy variable	
STORE6		Dummy variable	deg K
STORE7		Dummy variable	gm/cm <sup>3</sup>
SUMNO1	$\sum NO/i$	Summation of the total nitric oxide present at a given axial location in the intermediate zone	gm
SUM1(J)	$(\sum_1)_j$	Dummy variable	gm <sup>2</sup> /cm <sup>3</sup>
SUM2(J)	$(\sum_2)_j$	Summation of the total nitric oxide present at a given axial location in the intermediate zone at the jth iteration at that point	gm
TAU	$\bar{T}_{inc}$	Incremental residence time	sec
TTLAST	$T_{LST}$	Adiabatic flame temperature for the last step in the intermediate zone at the mean mixture ratio	deg K
XI	$X_1$	Integrated length of intermediate zone	cm
XXX	$X_{XX}$	Axial position in the combustor	cm
XXXX	$X_{XXX}$	Distance between upstream end of integration interval and end of intermediate zone	cm
YNOLST	$(NO_e)_{LST}$	Equilibrium mole fraction of NO for the last step in the intermediate zone at the mean mixture ratio	

### Analysis Procedure

The step-by-step procedure of Subroutine ZINTER is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. Initialize indicators.
2. Initialize  $\left\{ \bar{N} \right\}_{UP}$  as:  

$$\left\{ \bar{N} \right\}_{UP} = 0$$

3. Set  $k_e$  as:

$$k_e = 0.05$$

4. Calculate  $X_U$  as

$$X_U = X_D$$

5. Initialize  $\bar{T}_{INT}$  as:

$$\bar{T}_{INT} = 0$$

Step 6 is performed for each potential array element satisfying the criteria  $1 \leq i \leq 50$ .

6. initialize  $q_i$  as:

$$q_i = 1.0 \times 10^{-15}$$

7. Calculate  $\Delta X$  as:

$$\Delta X = 0.1 * R_{X_D}$$

8. Calculate  $X_I$  as:

$$X_I = X_L - X_U \text{ if intermediate zone calculations end at } X_L$$

$$X_I = X_{END} - X_U \text{ if intermediate zone calculations end at } X_{END}$$

Step 9 is performed only if  $\Delta X \leq X_I$

9. Go to step 12.

10. Recalculate  $\Delta X$  as:

$$\Delta X = X_I$$

11. Reset the indicator to indicate that this is the last major integration step in the intermediate zone.

Steps 12 and 13 are performed for each potential array element satisfying the criteria:  $1 \leq i \leq 50$

12. Calculate  $[NO]_{NO}$  and  $q_{q_i}$  as

$$[NO]_{NO} = [NO]$$

$$q_{q_i} = q_i$$

13. Initialize convergence indicators.

Step 14 is performed for each potential integration iteration satisfying the criteria  $1 \leq J \leq 6$

14. Initialize  $(\xi_1)_j$  and  $(\xi_2)_j$  as:

$$(\xi_1)_j = 0$$

$$(\xi_2)_j = 0$$

15. Set  $X_{XX}$  equal to  $X_D$ .

16. Set J and N as:

$$J = 1$$

$$N = 5$$

Step 17 is performed only if  $J = 1$ .

17. Go to step 21.

18. Calculate  $X_U$  and  $X_D$  as:

$$X_U = X_{XX}$$

$$X_D = X_U$$

19. Using Subroutine ZMASS, calculate the elemental and over-all mass flow rates, the mean mixture ratio, and the airflow rate at  $X_D$ .

Step 20 is performed for each element in the array satisfying the criteria  $1 \leq i \leq i_{MAX}$

20. Calculate  $[NO]_i$  and  $q_i$  as:

$$[NO]_i = [NO]_{NO}$$

$$q_i = q_{q_i}$$

21. Calculate  $\delta X$  as:

$$\delta X = \Delta X / N$$

22. Calculate  $K_D$  and  $\overline{NO}$  as:

$$K_D = C_N / X_L$$

$$\overline{NO} = [NO]$$

23. Set  $II = 1$ .

24. initialize  $[NO]_{0-1}$ ,  $[NO]_{0-2}$  and  $[NO]_{P-1N}$  as:

$$[NO]_{0-1} = 0$$

$$[NO]_{0-2} = 0$$

$$[NO]_{P-1N} = 0$$

25. Calculate  $X_D$  as:

$$X_D = X_U + \delta X$$

Step 26 is performed only if  $11 = N$  and if this is the last major integration step in the intermediate zone.

26. Go to step 100.

27. Using Subroutine ZMASS, calculate the elemental and over-all mass flow rates, the mean mixture ratio, and the airflow rate at  $X_D$ .

28. Using Subroutine CHECKK, calculate the proportionality constant between the mass flow rate out of an element due to mixing and the total mass flowing into it.

29. Set  $i = 1$ .

30. initialize  $l_{ie}$  as:

$$l_{ie} = 0$$

Step 31 is performed only if  $\left[ \frac{\partial (\delta \dot{m}_i)}{\partial X} \right]_{X_D} < 0$

and if  $(\delta \dot{m}_i)_D = 0$ .

31. Calculate  $[NO]_{0-2}$  as:

$$[NO]_{0-2} = [NO]_{0-2} + (\delta \dot{m}_i)_U * [NO]$$

Step 32 is performed only if  $(\delta \dot{m}_i)_D = 0$ .

32. Go to step 44.

33. Calculate  $(\delta \ddot{m}_A)_i$  as:

$$(\delta \ddot{m}_A)_i = (\delta \dot{m}_i)_U * \left( \frac{\partial \dot{m}_A}{\partial X} \right)_{X_D} / \dot{m}_U$$

34. Calculate  $(\delta \ddot{m}')_i$ ,  $(\delta \ddot{m}_m)_i$  and  $(\delta \ddot{m}'')_i$  as:

$$(\delta \ddot{m}')_i = \left[ \frac{\partial (\delta \dot{m}_i)}{\partial X} \right]_{X_D} + E_i * (\delta \dot{m}_i)_U - \dot{R}_i$$

$$(\delta \ddot{m}_m)_i = (\delta \ddot{m}')_i - (\delta \ddot{m}_A)_i$$

$$(\delta \ddot{m}'')_i = E_i * (\delta \dot{m}_i)_U$$

Step 35 is performed only if  $(S_{m,m}^{\prime\prime})_i > 0$

35. Go to step 43.

36. Calculate  $E_i$  as:

$$E_i = 2E_j$$

Step 37 is performed only if  $E_i = 0.$

37. Calculate  $E_i$  as:

$$E_i = 0.02$$

38. Calculate  $l_{ie}$  as:

$$l_{ie} = l_{ie} + 1$$

Step 39 is performed only if  $l_{ie} < 40$ .

39. Go to step 34.

40. Write  $l_{ie}$  and  $E_i$ .

41. Reset the appropriate indicator to indicate that intermediate zone calculations end at  $X_{END}$ .

42. Go to step 125.

43. Calculate  $[NO]_{0-1}$  and  $M_{IN}$  as:

$$[NO]_{0-1} = [NO]_{0-1} + (S_{m,m}^{\prime\prime})_i + [NO]_i$$

$$M_{IN} = M_{IN} + (S_{m,m}^{\prime\prime})_i + R_i$$

44. If this is not the last element in the array satisfying the criteria  $1 \leq i \leq i_{MAX}$  increment  $i$  as  $i = i + 1$  and go to step 30. If this is the last element, go to step 45.

45. Calculate  $[NO]_{0-1}$  as:

$$[NO]_{0-1} = [NO]_{0-1} + [NO]_{0-2} / \delta X$$

46. Calculate  $rat_1$  as:

$$rat_1 = [NO]_{0-1} / M_{IN}$$

47. Initialize  $\sum_{m,c} w_c / i$  as:

$$\sum_{m,c} w_c / i = 0$$

48. Set  $i = 1$ .

Step 49 is performed only if  $(S_{m,c})_0 = 0$  or if the chemical rate of production of NO in the element is zero.

49. Go to step 55.

50. Calculate  $[NO']$  as:

$$[NO'] = rat_1$$

51. Using Subroutine RUNKUT, calculate the values of  $[NO']$  and  $q_i$  at  $X_D$ .

Step 52 is performed only if  $[NO'] < 0$

52. Calculate  $[NO]$  as:

$$[NO] = rat_1$$

53. Calculate  $\sum NO/i$  as:

$$\sum NO/i = \sum NO/i + [NO'] * (\Delta m_i)_D$$

54. Recalculate  $X_U$  as:

$$X_U = X_D - \delta X$$

55. If this is not the last element in the array satisfying the criteria  $1 \leq i \leq i_{MAX}$  increment  $i$  as  $i = i + 1$  and go to step 49. If this is the last element, go to step 56.

56. Calculate  $\bar{NO}$  as

$$\bar{NO} = \sum NO/i / m_D^*$$

57. Set  $X_U$  equal to  $X_D$ .

58. If  $II < N$ , increment  $II$  as  $II = II + 1$  and go to step 24 to continue the integration. If not, go to step 59.

59. Set  $i = 1$ .

60. Calculate  $D_p$  and  $[NO]_{gm}$  as:

$$D_p = p_i * (\Delta m_i)_D$$

$$[NO]_{gm} = [NO'] * (\Delta m_i)_D$$

61. Calculate  $(z_1)_j$  and  $(z_2)_j$  as:

$$(z_1)_j = (z_1)_j + D_p$$

$$(z_2)_j = (z_2)_j + [NO]_{gm}$$

62. If this is not the last element in the array satisfying the criteria  $1 \leq i \leq i_{MAX}$  increment  $i$  as  $i = i + 1$  and go to step 60. If this is the last element, go to step 63.

63. Calculate the mass average density,  $\bar{\rho}_j$ , and the mass average nitric oxide concentration  $\bar{NO}_j$  for the  $j$ th iteration as:

$$\bar{\rho}_j = (\sum_1)_j / M_D^*$$

$$\bar{NO}_j = (\sum_2)_j / M_D^*$$

Step 64 is performed only if intermediate output is requested by the user.

64. Write  $X_D$ ,  $J$ ,  $\bar{\rho}_j$  and  $\bar{NO}_j$ .

Steps 65-66 are performed only if  $J = 1$ .

65. Calculate  $[NO]_{DOM}$  as:

$$[NO]_{DOM} = \bar{NO}$$

66. Go to step 69.

Steps 67-71 are performed only if  $1 < J < 5$ .

67. Calculate  $[\Delta NO]$  as:

$$[\Delta NO] = \frac{\bar{NO} - [NO]_{DOM}}{\bar{NO}}$$

Step 68 is performed only if  $[\Delta NO] < 0.01$

68. Go to step 74.

69. Reset  $J$  and  $N$  as:

$$J = J + 1$$

$$N = 2N$$

70. Set  $[NO]_{DOM} = \bar{NO}$ .

71. Go to step 17.

Steps 72-73 are performed only if  $5 \leq J \leq 6$ .

72. Calculate  $[\Delta NO]$  as:

$$[\Delta NO] = \left| \frac{\bar{NO} - [NO]_{DOM}}{\bar{NO}} \right|$$

73. Write  $[\Delta NO]$ ,  $N$ , and  $X_D$  with the error message indicating that the Runge-Kutta iteration failed to converge to the specified limit.

Step 74 is performed only if  $!! = N$  and this is the last major integration step in the intermediate zone.

74. Go to step 119.

75. Calculate  $[\bar{NO}]$ ,  $\bar{p}$ ,  $\bar{T}$ ,  $(\bar{C}_{(s)})_e$ ,  $(\bar{CO})_e$  and  $(\bar{CH}_2)_e$  as:

$$[\bar{NO}] = \sum_{i=1}^{i_{MAX}} [NO_i] * (\Delta m_i)_D / M_D^*$$

$$\bar{p} = \sum_{i=1}^{i_{MAX}} p_i * (\Delta m_i)_D / M_D^*$$

$$\bar{T} = \sum_{i=1}^{i_{MAX}} T_i * (\Delta m_i)_D / M_D^*$$

$$(\bar{C}_{(s)})_e = \sum_{i=1}^{i_{MAX}} (C_{(s)i})_e * (\Delta m_i)_D / M_D^*$$

$$(\bar{CO})_e = \sum_{i=1}^{i_{MAX}} (CO_i)_e * (\Delta m_i)_D / M_D^*$$

$$(\bar{CH}_2)_e = \sum_{i=1}^{i_{MAX}} (CH_{2i})_e * (\Delta m_i)_D / M_D^*$$

76. Calculate  $\bar{MW}$  as:

$$\bar{MW} = \bar{p} * \bar{T} * 82.057 / P$$

77. Calculate  $[\bar{C}_{(s)}]_e$ ,  $[\bar{CO}]_e$ , and  $[\bar{CH}_2]_e$  as:

$$[\bar{C}_{(s)}]_e = (\bar{C}_{(s)})_e * 12 / \bar{MW}$$

$$[\bar{CO}]_e = (\bar{CO})_e * 28 / \bar{MW}$$

$$[\bar{CH}_2]_e = (\bar{CH}_2)_e * 14 / \bar{MW}$$

78. Calculate  $\{\bar{NO}\}$ ,  $[\bar{NO}^*]$ , and  $[\bar{NO}]$  as:

$$\{\bar{NO}\} = [\bar{NO}] * 10^6 * \bar{MW} / 30.0$$

$$[\bar{NO}^*] = [\bar{NO}] * \bar{p}$$

$$[\bar{NO}] = [\bar{NO}] * M_D^* * 1000 / (M_F)_{x_D}$$

79. Calculate  $\{\bar{C}_{(s)}\}_e$ ,  $\{\bar{CO}\}_e$ , and  $\{\bar{CH}_2\}_e$  as:

$$\{\bar{C}_{(s)}\}_e = [\bar{C}_{(s)}]_e * 10^6 * \bar{MW} / 12$$

$$\{\bar{CO}\}_e = [\bar{CO}]_e * 10^6 * \bar{MW} / 28$$

$$\{\bar{CH}_2\}_e = [\bar{CH}_2]_e * 10^6 * \bar{MW} / 14$$

80. Calculate  $[\bar{C}_{(s)}^*]_e$ ,  $[\bar{CO}^*]_e$ , and  $[\bar{CH}_2^*]_e$  as:

$$[\bar{C}_{(s)}^*]_e = [\bar{C}_{(s)}]_e * \bar{P}$$

$$[\bar{CO}^*]_e = [\bar{CO}]_e * \bar{P}$$

$$[\bar{CH}_2^*]_e = [\bar{CH}_2]_e * \bar{P}$$

81. Calculate  $[\bar{C}_{(s)}]_e$ ,  $[\bar{CO}]_e$  and  $[\bar{CH}_2]_e$  as:

$$[\bar{C}_{(s)}]_e = [\bar{C}_{(s)}]_e * M_D^* * 1000 / (\dot{M}_F)_{x_D}$$

$$[\bar{CO}]_e = [\bar{CO}]_e * M_D^* * 1000 / (\dot{M}_F)_{x_D}$$

$$[\bar{CH}_2]_e = [\bar{CH}_2]_e * M_D^* * 1000 / (\dot{M}_F)_{x_D}$$

82. Calculate  $[\Delta \bar{NO}]_{\Delta x}$  as:

$$[\Delta \bar{NO}]_{\Delta x} = \frac{[\bar{NO}] - [\bar{NO}]_{op}}{[\bar{NO}]}$$

83. Calculate  $n_{step}$  as:

$$n_{step} = (X_{END} - X_U) / \Delta x$$

Step 84 is performed only if  $([\Delta \bar{NO}]_{\Delta x} * n_{step}) < 0.05$

84. Set the appropriate indicator to indicate that the nitric oxide reaction is frozen at this point in the combustor.

85. Calculate  $\bar{\gamma}_{inc}$  as:

$$\bar{\gamma}_{inc} = \Delta X \cdot \bar{\rho} \cdot A|_{x_D} / \dot{m}_D^*$$

86. Calculate  $\bar{\gamma}_{int}$  and  $\bar{\gamma}$  as:

$$\bar{\gamma}_{int} = \bar{\gamma}_{inc} + \bar{\gamma}_{inc}$$

$$\bar{\gamma} = \bar{\gamma} + \bar{\gamma}_{inc}$$

87. Calculate  $V$  as:

$$V = \dot{m}_D^* / \bar{\rho} \cdot A|_{x_D}$$

88. Calculate  $\bar{\phi}$  as:

$$\bar{\phi} = \bar{F} / (K_S \cdot (1 - \bar{F}))$$

89. Using Subroutine PRINTS, write the output for this axial station in the intermediate zone.

Step 90 is performed only if the nitric oxide reaction is frozen at this point in the combustor.

90. Write a message indicating frozen conditions exist in the combustor.

Step 91 is performed only if the appropriate indicator has been previously set to indicate that the nitric oxide reaction is frozen.

91. Go to step 124.

92. Set  $\left[ \bar{NO} \right]_{UP}$  as:

$$\left[ \bar{NO} \right]_{UP} = \left[ \bar{NO} \right]$$

93. Calculate  $(\bar{\rho})_{rr}$  as:

$$(\bar{\rho})_{rr} = \bar{\rho}$$

Step 94 is performed only for the last major integration step in the intermediate zone.

94. Go to step 125.

95. Calculate  $X_{XXX}$  as:

$$X_{XXX} = X_L - X_U \quad \text{if intermediate zone calculations end at } X_L.$$

$$X_{XXX} = X_{END} - X_U \quad \text{if intermediate zone calculations end at } X_{END}.$$

Step 96 is performed only if  $\Delta X < X_{XXX}$

96. Go to step 12.

97. Calculate  $\Delta X$  as:

$$\Delta X = X_{XXX}$$

98. Set the appropriate indicator to indicate that this is the last major integration step in the intermediate zone.

99. Go to step 12.

100. Set the appropriate indicator to indicate a dilution zone type calculation is to be applied to the last element in the intermediate zone.

101. Using Subroutine ZMASS, calculate the over-all mass flow rate, the mean mixture ratio, and the airflow rate at  $X_D$ .

102. Using Subroutine CHECKK, calculate the mass flow rate out of an element due to mixing and the total mass flowing into it.

103. Reset the appropriate indicator to indicate intermediate zone calculations.

104. Calculate  $Q$  and  $[NO]_{AN}$  as:

$$Q = \sum_{i=1}^{I_{MAX}} \dot{Q}_i \times (\Delta m_i)_D / M_D^*$$

$$[NO]_{AN} = \sum_{i=1}^{I_{MAX}} [NO]_i \times (\Delta m_i)_D / M_D^*$$

105. Using Subroutine MINT, calculate  $(R)_LST$

106. Using Subroutine MINT, calculate  $(R_O)_LST$

107. Using Subroutine MINT, calculate  $(T_1)_LST$

108. Using Subroutine MINT, calculate  $(T_2)_LST$

109. Using Subroutine MINT, calculate  $(NO_e)_LST$

110. Using Subroutine MINT, calculate  $P_{L-T}$

111. Using Subroutine MINT, calculate  $T_{L-T}$

112. Calculate  $[NO]_{IK}$  as:

$$[NO]_{IK} = (NO_e)_{LST} \times 30.0 / P_{LST} \times T_{LST} \times 82.057 / P$$

113. Set the appropriate indicator to indicate that this is the last step of the intermediate zone calculations.
114. Using Subroutine RUNKUT, compute the values of  $[\bar{C}]_{AN}$  and  $Q$  at  $X_D$ .
115. Recalculate  $X_U$  as:  

$$X_U = X_D - \delta X$$
116. Reset the appropriate indicator to signify intermediate zone calculations.
117. Calculate  $\bar{P}_j$  and  $\bar{NO}_j$  as:  

$$\bar{P}_j = P_{LST}$$

$$\bar{NO}_j = [\bar{NO}]_{AN}$$
118. Go to step 65.
119. Compute  $\bar{T}$ ,  $\bar{P}$  and  $[\bar{NO}]$  as:  

$$\bar{T} = T_{LST}$$

$$\bar{P} = P_{LST}$$

$$[\bar{NO}] = [\bar{NO}]_{AN}$$
120. Using Subroutine MINT, compute  $(\bar{C}_{(s)})_e$ .
121. Using Subroutine MINT, compute  $(\bar{CO})_e$ .
122. Using Subroutine MINT, compute  $(\bar{CH}_2)_e$ .
123. Go to step 76.
124. Calculate  $[\bar{NO}]_{AN}$  as:  

$$[\bar{NO}]_{AN} = [\bar{NO}]$$
125. Return.

```

SUBROUTINE ZINTER
REAL NONO(50),MSTARU,MSTARD,NO,NOAVGS,NOP,NOSTAR
DIMENSION AVRHO(10),AVNO(10),KON(10),Q(50),QQ(50),SUM1(10),SUM2(10)
1) COMMON/DATA1/AIR(50),RR(50),XX(50),FF(50),BCON1(50),BCON2(50),CH2(
150),ZP(70),CUMDIS(70),VP,RHO(50),BCON6(50),ATT(50),PPP,FNOXP,R1(50)
2),R6(50),EK1(50),EK2(50),A2,A3,XL,CN,BETA,S,PHIP,EKS,XEND,A1
COMMON/OUT1/AVECSG,AVECOG,AVCH2G,AVECSP,AVECOP,AVCH2P,AVECSD,AVECO
1D,AVCH2D,AVECSF,AVECOF,AVCH2F
COMMON/OUT2/AVENOG,AVENOD,AVENOP,AVENOF,AVENFU,RRO,ILAST
COMMON/OUT3/INDIC,NO(50),AVET,TAUBAR,RHOBAR,PHIBAR,IMAX,XD,
1FBARD,XU,LEN,TAUINT,TAUDIL,VELOC
COMMON/OUT4/CONGNO(50),DELMO(50),AREAD,ASLOPE,DMFUO,SLOPE(50),TSLO
1PE,NOP(50),EKKO,DMFT,UDM(50),DDM(50),FB(50),DMFUD,AIRD,DMFFED
2,RSUBX,SIG,SIGZER,AVEMW,DMDDA(50),DMDDM(50),DMDDP(50),DMDDPP(50),F
3PRIME(50),NOEQXD,ANO,AQQ,SUEA(50),NOZERO(50),RDOT(50),E(50)
COMMON/OUT5/MSTARD,MSTARU
COMMON/OUT6/REAT,DILL
C****
C**** SET INITIAL INDICATORS,CALCULATE DELTAX,CHECK X
C****
  NPRINT=0
  ILAST=0
  LSGN = 1
  INDIC = 2
  IENDZ=0
  AVENFU=0.0
  EK=0.05
  XU = XD
  TAUINT = 0.0
  DO 100 I = 1,50
    Q(I) = 1.0E-15
100 CONTINUE
  DELTAX = 0.1*RSUBX
  IF(LEN.EQ.0) XI=XL-XU
  IF(LEN.EQ.1) XI = XEND-XU
  IF(DELTAX.LE.XI) GO TO 200
  DELTAX = XI
  IENDZ = 1
200 CONTINUE
C****
C**** STORE INITIAL VALUES FOR BEGINNING OF EACH MAJOR STEP
C****
  250 CONTINUE
    DO 300 I = 1,50
      NONO(I) = NO(I)
      QQ(I) = Q(I)
      KON(I) = 0
300 CONTINUE
    DO 350 K = 1,6
      SUM1(K) = 0.0
      SUM2(K) = 0.0
350 CONTINUE
    XXX = XD
    J = 1
    N=5
C****
C**** SET INITIAL VALUES EQUAL TO STORED VALUES EACH TIME N CHANGES
C****
  360 CONTINUE

```

```

IF(J.EQ.1) GO TO 500
XU = XXX
C****
C**** SUBST UDM(I) FOR CALCULATION OF SLOPE
C****
XD=XU
CALL ZMASS(DELX)
DO 400 I = 1,IMAX
NO(I) = NONO(I)
Q(I) = QO(I)
400 CONTINUE
500 EN = N
DELX = DELTAX/EN
EYKD=C/XL
AVVNDG=AVVENDG
C****
C**** START THE MAJOR STEPS DOWN THE COMBUSTOR
C****
DO 3000 II=1,N
OUTNO=0.0
OUTNO2=0.0
PINO=0.0
XD = XU+DELX
IF(II.EQ.N.AND.IENDZ.EQ.1) GO TO 8000
CALL ZMASS(DELX)
CALL CHECKK(DELX)
C****
C**** TEST EACH ELEMENT FOR CONVERGENCE
C****
C****
C**** IF NOZERO=1 BYPASS THE NO CALC
C****
DO 2000 I=1,IMAX
IIE=0
IF(SLOPE(I).LT.0.0.AND.DDM(I).EQ.0.0) OUTNO2=OUTNO2+UDM(I)*NO(I)
IF(DDM(I).EQ.0.0) GO TO 2000
DMDDA(I) = UDM(I)*ASLOPE/MSTARU
600 DMDDP(I)=SLOPE(I)+E(I)*UDM(I) -RDOT(I)
DMDDM(I)=DMDDP(I)-DMDDA(I)
DMDDPP(I) = E(I)*UDM(I)
IF(DMDDM(I).GT.0.0) GO TO 700
E(I)=2.0*E(I)
C****
C**** CN,HENCE E(I),CANNOT EQUAL ZERO
C****
IF(E(I).EQ.0.0) E(I)=0.02
IIE=IIE+1
IF(IIE.LT.40) GO TO 600
WRITE(6,9999) IIE,E(I)
LEN=1
GO TO 9000
700 CONTINUE
OUTNO=OUTNO+DMDDP(I)*NO(I)
PINO=PINO+DMDDP(I)*ROOT(I)
2000 CONTINUE
OUTNO=OUTNO+OUTNO2/DELX
AVVNO=OUTNO/PINO
SUMNOI=0.0
DO 4000 IJ=1,IMAX
IF(DDM(IJ).EQ.0.0) GO TO 4000

```

```

ZIN*0600
ZIN*0610
ZIN*0620
ZIN*0630
ZIN*0640
ZIN*0650
ZIN*0660
ZIN*0670
ZIN*0680
ZIN*0690
ZIN*0700
ZIN*0710
ZIN*0720
ZIN*0730
ZIN*0740
ZIN*0750
ZIN*0760
ZIN*0770
ZIN*0780
ZIN*0790
ZIN*0800
ZIN*0810
ZIN*0820
ZIN*0830
ZIN*0840
ZIN*0850
ZIN*0860
ZIN*0870
ZIN*0880
ZIN*0890
ZIN*0900
ZIN*0910
ZIN*0920
ZIN*0930
ZIN*0940
ZIN*0950
ZIN*0960
ZIN*0970
ZIN*0980
ZIN*0990
ZIN*1000
ZIN*1010
ZIN*1020
ZIN*1030
ZIN*1040
ZIN*1050
ZIN*1060
ZIN*1070
ZIN*1080
ZIN*1090
ZIN*1100
ZIN*1110
ZIN*1120
ZIN*1130
ZIN*1140
ZIN*1150
ZIN*1160
ZIN*1170
ZIN*1180
ZIN*1190

```

```

IF(N0ZER0(IJ).EQ.1) GO TO 4000
NOP(IJ)=AVVNO
CALL MUNKUT(XU,DELX,NO(IJ),3(IJ),LSGN,IJ)
IF(N0(IJ).LT.0.0) NO(IJ)=AVVNO
SUMNOI = SUMNOI+NO(IJ)*DELMO(IJ)
XU=XU-DELX
4000 CONTINUE
AVVNOG=SUMNOI/MSTARD
XU=XU
3000 CONTINUE
DO 3500 I =1,IMAX
  RHOMI = RHO(I)*DELMO(I)
  GNOMI = NO(I)*DELMO(I)
  SUM1(J) = SUM1(J)+RHOMI
  SUM2(J) = SUM2(J)+GNOMI
3500 CONTINUE
AVRHO(J) = SUM1(J)/MSTARD
AVNO(J) = SUM2(J)/MSTARD
C****
C**** WRITE CONTROL
C****
IF(NPRINT.EQ.0) GO TO 3550
WRITE(6,3600) XC,J,AVRHO(J),AVNO(J)
3600 FORMAT(9H X(CM) = ,E12.5,4HJ = ,I2.18HAVE. RHO(GM/CC) = ,E12.5,17H
1AVE. NO(GM/GM) = ,E12.5)
3550 CONTINUE
C****
C**** LOGIC CONTROL ON J
C****
GO TO (4100,4300,4300,4300,4600,4600),J
4100 DUMMY=AVVNOG
GO TO 4500
4300 DIFNO=ABS((AVVNOG-DUMMY)/AVVNOG)
IF(DIFNO.LT.0.01) GO TO 5000
4500 J=J+1
N = 2*N
DUMMY=AVVNOG
GO TO 360
4600 DDFNO=ABS((AVVNOG-DUMMY)/AVVNOG)
WRITE(6,4700) DDFNO,N,XD
4700 FORMAT(///,69H RUNGE-KUTTA ITERATION FAILED TO CONVERGE TO SPECIFIED
1ED LIMIT.DIFNO = ,E12.5,5H N = ,I4,5H X = ,E12.5,5H CHS.//)
4800 CONTINUE
5000 CONTINUE
IF(I1.EQ.N.AND.IENDZ.EQ.1) GO TO 8500
C****
C**** WRITE THE APPROPRIATE OUTPUT FOR THIS AXIAL STATION
C****
AVENOG = 0.0
RHOBAR = 0.0
AVET = 0.0
CSAV = 0.0
COAV = 0.0
CHZAV = 0.0
DO 6000 I =1,IMAX
  AVENOG = AVENOG+NO(I)*DELMO(I)
  RHOBAR = RHOBAR+RHO(I)*DELMO(I)
  AVET = AVET+ATT(I)*DELMO(I)
  CSAV = CSAV+BCON1(I)*DELMO(I)
  COAV = COAV+BCON2(I)*DELMO(I)

```

ZIN\*1200  
 ZIN\*1210  
 ZIN\*1220  
 ZIN\*1230  
 ZIN\*1240  
 ZIN\*1250  
 ZIN\*1250  
 ZIN\*1270  
 ZIN\*1280  
 ZIN\*1290  
 ZIN\*1300  
 ZIN\*1310  
 ZIN\*1320  
 ZIN\*1330  
 ZIN\*1340  
 ZIN\*1350  
 ZIN\*1360  
 ZIN\*1370  
 ZIN\*1380  
 ZIN\*1390  
 ZIN\*1400  
 ZIN\*1410  
 ZIN\*1420  
 ZIN\*1430  
 ZIN\*1440  
 ZIN\*1450  
 ZIN\*1460  
 ZIN\*1470  
 ZIN\*1480  
 ZIN\*1490  
 ZIN\*1500  
 ZIN\*1510  
 ZIN\*1520  
 ZIN\*1530  
 ZIN\*1540  
 ZIN\*1550  
 ZIN\*1560  
 ZIN\*1570  
 ZIN\*1580  
 ZIN\*1590  
 ZIN\*1600  
 ZIN\*1610  
 ZIN\*1620  
 ZIN\*1630  
 ZIN\*1640  
 ZIN\*1650  
 ZIN\*1660  
 ZIN\*1670  
 ZIN\*1680  
 ZIN\*1690  
 ZIN\*1700  
 ZIN\*1710  
 ZIN\*1720  
 ZIN\*1730  
 ZIN\*1740  
 ZIN\*1750  
 ZIN\*1760  
 ZIN\*1770  
 ZIN\*1780  
 ZIN\*1790

```

CH2AV = CH2AV*CH2(I)*DELMO(I)
6000 CONTINUE
AVENOG = AVENOG/MSTARD
RHOBAR = RHOBAR/MSTARD
AVET = AVET/MSTARD
CSAV = CSAV/MSTARD
COAV = COAV/MSTARD
CH2AV = CH2AV/MSTARD
6500 AVEMM = RHOBAR*AVET*02.057/PPP
AVECSG = CSAV*12.0/AVEMM
AVECOG = COAV*28.0/AVEMM
AVCH2G = CH2AV*14.0/AVEMM
AVENOP=AVENOG*1.0E+06*AVEMM/30.0
AVENOF = AVENOG*RHOBAR
AVENOF = AVENOG*MSTARD*1000./DMFT
AVECSP=AVECSG*1.0E+06*AVEMM/12.0
AVECOP=AVECOG*1.0E+06*AVEMM/28.0
AVCH2P=AVCH2G*1.0E+06*AVEMM/14.0
AVECSO = AVECSG*RHOBAR
AVECOO = AVECOG*RHOBAR
AVCH2O = AVCH2G*RHOBAR
AVECSF = AVECSG*MSTARD*1000./DMFT
AVECOF = AVECOG*MSTARD*1000./DMFT
AVCH2F = AVCH2G*MSTARD*1000./DMFT
FURAT=(AVENOF-AVENFU)/AVENOF
STEPS=(XEND-XU)/DELTAX
IF (FURAT*STEPS.LT.0.05) ILAST=1
C****
C**** CALCULATE RESIDENCE TIME,ETC.
C****
TAU = DELTAX*RHOBAR*AREAD/MSTARD
TAUINI = TAUINI*TAU
TAUBAR = TAUBAR*TAU
VELOC = MSTARD/(RHOBAR*AREAD)
PHIBAR = FBARD/(EKS*(1.0-FBARD))
CALL PRINTS
IF (ILAST.EQ.1) WRITE(6,9500)
9500 FORMAT(/////,10X,42HNITRIC OXIDE REACTION FROZEN AT THIS POINT,///)
1) IF (ILAST.EQ.1) GO TO 8600
C****
C**** CONTROL OVERALL STEPS
C****
AVENFU=AVENOF
RRO=RHOBAR
IF (IENDZ.EQ.1) GO TO 9000
IF (LEN.EQ.0) XXXX = XL-XU
IF (LEN.EQ.1) XXXX = XEND-XU
IF (DELTAX.LT.XXXX) GO TO 250
DELTAX = XXXX
IENDZ = 1
GO TO 250
C****
C**** COMPUTATION FOR LAST ELEMENT
C****
9000 INDIC = 3
CALL ZMASS(DELTAX)
CALL CHECKK(DELTAX)
INDIC = 2
AQO = 0.0

```

4NO = 0.0	ZIN*2400
DO 8100 I = 1, IMAX	ZIN*2410
AGQ = AGQ + 0(I) * DELMD(I)	ZIN*2420
ANO = ANO + NO(I) * DELMD(I)	ZIN*2430
8100 FFF = F9ARD	ZIN*2440
AGQ = AGQ / MSTARD	ZIN*2450
ANO = ANO / MSTARD	ZIN*2460
CALL MINT(1, FFF, 35, FF, R1, R1LAST)	ZIN*2470
CALL MINT(1, FFF, 35, FF, R6, R6LAST)	ZIN*2480
CALL MINT(1, FFF, 35, FF, EK1, EK1LST)	ZIN*2490
CALL MINT(1, FFF, 35, FF, EK2, EK2LST)	ZIN*2500
CALL MINT(1, FFF, 35, FF, BCON6, YNOLST)	ZIN*2510
CALL MINT(1, FFF, 35, FF, RHO, RHOLST)	ZIN*2520
CALL MINT(1, FFF, 35, FF, ATT, TTLAST)	ZIN*2530
CNOLST = YNOLST * 30.0 / (RHOLST * TTLAST * 82.057 / PPP)	ZIN*2540
STORE1 = R1(1)	ZIN*2550
STORE2 = R6(1)	ZIN*2560
STORE3 = EK1(1)	ZIN*2570
STORE4 = EK2(1)	ZIN*2580
STORE5 = CONGNO(1)	ZIN*2590
STORE6 = ATT(1)	ZIN*2600
STORE7 = RHO(1)	ZIN*2610
R1(1) = R1LAST	ZIN*2620
R6(1) = R6LAST	ZIN*2630
EK1(1) = EK1LST	ZIN*2640
EK2(1) = EK2LST	ZIN*2650
RHO(1) = RHOLST	ZIN*2660
ATT(1) = TTLAST	ZIN*2670
CONGNO(1) = CNOLST	ZIN*2680
LSGN = 2	ZIN*2690
CALL RUNKUT(XU, DELX, ANO, AGQ, LSGN, 1)	ZIN*2700
XU = XU - DELX	ZIN*2710
R1(1) = STORE1	ZIN*2720
R6(1) = STORE2	ZIN*2730
EK1(1) = STORE3	ZIN*2740
EK2(1) = STORE4	ZIN*2750
CONGNO(1) = STORE5	ZIN*2760
ATT(1) = STORE6	ZIN*2770
RHO(1) = STORE7	ZIN*2780
AVRHO(J) = RHOLST	ZIN*2790
AVNO(J) = ANO	ZIN*2800
LSGN = 1	ZIN*2810
GO TO 3550	ZIN*2820
C****	ZIN*2830
C**** COMPUTE APPROPRIATE AVERAGES	ZIN*2840
C****	ZIN*2850
6500 AVET = TTLAST	ZIN*2860
RHOBAR = RHOLST	ZIN*2870
AVENOG = ANO	ZIN*2880
CALL MINT(1, FFF, 35, FF, BCON1, CSAV)	ZIN*2890
CALL MINT(1, FFF, 35, FF, BCON2, COAV)	ZIN*2900
CALL MINT(1, FFF, 35, FF, CH2, CH2AV)	ZIN*2910
GO TO 6500	ZIN*2920
9999 FORMAT(10X, I6, RE12.5)	ZIN*2930
8600 ANO = AVENOG	ZIN*2940
9000 RETURN	ZIN*2950
END	ZIN*2960

## APPENDIX VI - SUBROUTINE DILUTE

The function of Subroutine DILUTE is to calculate the concentration of nitric oxide at specified axial stations, and at the exit of the dilution zone of a gas turbine combustor.

Subroutine DILUTE is called by the main routine (GASNOX); it, in turn, calls Subroutines ZMASS, MINT, RUNKUT, and PRINTS. The subroutine does not require external input but does provide external output. Internal input and output are transmitted through COMMON. The internal input consists of:

AIRD	ANO	AQQ	ATT	BCON1
BCON2	BCON6	CH2	EKS	EK1
EK2	FF	ILAST	PPP	RHO
RSUBX	R1	R6	S	XEND
XD				

The internal output consists of:

ANO	AVCH2D	AVCH2F	AVCH2G	AVCH2P
AVECOD	AVECOF	AVECOG	AVECOP	AVECSD
AVECSF	AVECSG	AVECSP	AVEMW	AVENFU
AVENOD	AVENOF	AVENOG	AVENOP	AVET
INDIC	NOEQXD	PHIBAR	RRO	TAUBAR
TAUDIL	VELOC	XD	XU	

The external output consists of:

DDIFNO	DILL	DNO	J	N
REAT	RHOBAR	XD		

Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols used in Subroutine DILUTE which are not included in COMMON.

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AIRXX	$M_{A,X}$	Combustor airflow at axial station $X_D$	gm/sec
DDIFNO	[ANO]	Difference in NO concentrations for successive iterations at the end of each major step in the combustor	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
DELTAX	$\Delta X$	Integration step size (major) in the dilution zone	cm
DELX	$\delta X$	Increment of the combustor length across which the solution is generated	cm
DNO	$[\overline{NO}]_{DN}$	Average NO at given axial station (downstream) in the combustor	
DUMMY	$[NO]_{DUM}$	Dummy variable	
EK1LST	$(K_1)_{LST}$	Ratio of forward reaction rate constants at a given axial station in the dilution zone at the mean mixture ratio (see Volume 2, Section 2 or Ref 3)	
EK2LST	$(K_2)_{LST}$	Ratio of forward reaction rate constants at a given axial position in the dilution zone at the mean mixture ratio (see Volume 2, Section 2 or Ref 3)	
EN	N	Proportionality constant between $\Delta X$ and $\delta X$	
FURAT	$[\Delta NO]_{\Delta X}$	Measure of change in NO concentration for successive steps in the combustor	
IENDD		Indicator IENDD = 0 for all except the last major integration step in the dilution zone IENDD = 1 for the last major integration step in the dilution zone	
II	II	Integration increment index	
J	J	Number of iterations for each major axial step in the combustor	
LSGN		Indicator LSGN = 1 if intermediate zone and not the last step in the zone LSGN = 2 if intermediate zone and the last step in the zone LSGN = 3 if dilution zone	
N	N	Proportionality constant between $\Delta X$ and $\delta X$	
NONO	$[\overline{NO}]_{NO}$	Dummy variable	

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
NPRINT		Indicator NPRINT = 0 if intermediate output is not requested by the user NPRINT = 1 if intermediate output is requested by the user	
Q	q	Measure of the round-off error in the Runge-Kutta integration routine at a given axial station in the combustor	
QQ	qq	Measure of the round-off error in the Runge-Kutta integration routine at a given axial station	
R1LST	$(R_1)_{LST}$	Forward reaction rate for the first kinetic reaction at a given axial position in the dilution zone at the mean mixture ratio (see Volume 2, Section 2 or Ref 3)	gm-mole/cm <sup>3</sup> -sec
R6LST	$(R_6)_{LST}$	Forward reaction rate for the sixth kinetic reaction at a given axial position in the dilution zone at the mean mixture ratio (see Volume 2, Section 2 or Ref 3)	gm-mole/cm <sup>3</sup> -sec
STEPS	$n_{step}$	Number of remaining integration steps before combustor exit	
STORE1		Dummy variable	gm-mole/cm <sup>3</sup> -sec
STORE2		Dummy variable	gm-mole/cm <sup>3</sup> -sec
STORE3		Dummy variable	
STORE4		Dummy variable	
TAU	$\bar{\tau}_{inc}$	Incremental residence time	sec
YDZ	$X_{DZ}$	Distance between upstream end of integration interval to combustor exit	cm
XXX	$X_{XX}$	Axial position in the combustor	cm
XXXX	$X_{XXX}$	Distance between upstream end of integration interval and combustor exit	cm
YCH2XD	$(CH_2)_{exD}$	Equilibrium mole fraction of unburned hydrocarbon (exclusive of $C_2H_2$ and CO) at a given axial station in the dilution zone at the mean mixture ratio	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
YCOXD	$(CO)_{exD}$	Equilibrium mole fraction of CO at a given axial station in the dilution zone at the mean mixture ratio	
YCSXD	$(C_{(s)})_{exD}$	Equilibrium mole fraction of $C_{(s)}$ at a given axial station in the dilution zone at the mean mixture ratio	
YNOXD	$(NO)_{exD}$	Equilibrium mole fraction of NO at a given axial station in the dilution zone at the mean mixture ratio	

### Analysis Procedure

The step-by-step procedure of Subroutine DILUTE is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. Initialize indicators.

2. Set  $[\overline{NO}]_{DN} = [\overline{NO}]_{AN}$

Step 3 is performed only if the nitric oxide reaction is frozen at the point in the combustor.

3. Go to step 16

4. Calculate  $X_U$ ,  $\overline{\tau}_{DIL}$ , and  $q$  as:

$$X_U = X_D$$

$$\overline{\tau}_{DIL} = 0$$

$$q = Q$$

5. Calculate  $\Delta X$  and  $X_{DZ}$  as:

$$\Delta X = 0.1 * R_{X_D}$$

$$X_{DZ} = X_{END} - X_U$$

Step 6 is performed if  $\Delta X \leq X_{DZ}$

6. Go to step 8.

7. Set the indicator to indicate that this is the last step in the combustor and calculate  $\Delta X$  as:

$$\Delta X = X_{DZ}$$

8. Initialize dummy variables  $M_A|_{XX}$  and  $[\overline{NO}]_{NO}$  as:

$$M_A|_{XX} = M_A|_{X_D}$$

$$[\overline{NO}]_{NO} = [\overline{NO}]_{DN}$$

9. Initialize  $qq$  and  $X_{XX}$  as:

$$qq = q$$

$$X_{XX} = X_D$$

10. Initialize  $J$  and  $N$  as:

$$J = 1$$

$$N = 20$$

11. Initialize  $II$  as:

$$II = 1$$

Step 12 is performed only if  $J = 1$ .

12. Go to step 14.

13. Calculate  $M_A|_{X_D}$ ,  $X_U$ ,  $q$ , and  $[NO]_{DN}$  as:

$$M_A|_{X_D} = M_A|_{XX}$$

$$X_U = X_{XX}$$

$$q = q_D$$

$$[NO]_{DN} = [NO]_{NO}$$

14. Calculate  $\delta X$  as:

$$\delta X = \Delta X / N$$

15. Go to step 19.

16. Set  $N$ ,  $II$ , and  $J$  as:

$$N = 10$$

$$II = N$$

$$J = 6$$

17. Calculate  $\delta X$ ,  $\Delta X$  and  $X_U$  as:

$$\delta X = X_{END} - X_U$$

$$\Delta X = \delta X$$

$$X_U = X_D$$

18. Calculate  $[NO]_{AN}$  as:

$$[NO]_{AN} = [NO]_{DN}$$

19. Calculate  $X_D$  as:

$$X_D = X_U + \delta X$$

20. Using Subroutine ZMASS, calculate the over-all mass flow rate, mean mixture ratio, and airflow rate at  $X_D$

21. Using Subroutine MINT, calculate  $(R_1)_{LST}$

22. Using Subroutine MINT, calculate  $(R_0)_{LST}$

23. Using Subroutine MINT, calculate  $(K_1)_{LST}$

24. Using Subroutine MINT, calculate  $(K_2)_{LST}$

25. Using Subroutine MINT, calculate  $(NO)_{exp}$   
 26. Using Subroutine MINT, calculate  $\bar{p}$   
 27. Using Subroutine MINT, calculate  $\bar{T}$   
 28. Using Subroutine MINT, calculate  $(C_{(s)})_{exp}$   
 29. Using Subroutine MINT, calculate  $(CO)_{exp}$   
 30. Using Subroutine MINT, calculate  $(CH_2)_{exp}$
- Steps 31 and 32 are performed only if the nitric oxide reaction is frozen at this point in the combustor.

31. Calculate  $[NO]_{DN}$  as:

$$[NO]_{DN} = [NO]_{AN} * [M_O^*/M_P^*]$$

32. Go to step 38.

33. Calculate  $[NO_e]_{X_D}$  as:

$$[NO_e]_{X_D} = (NO)_{exp} *$$

34. Using Subroutine RUNKUT, calculate the value of  $[NO]_{DN}$  and q

Steps 35 and 36 are performed only if  $11 < N$

35. Calculate  $11 = 11 + 1$

36. Return to step 20.

Step 37 is performed only if intermediate output is requested by the user.

37. Write  $X_D, T, \bar{p}, [NO]_{DN}, (\dot{r})_{react}, (\dot{r})_{DIL}, [\Delta NO],$   
and  $N.$

Steps 38 and 39 are performed only if  $J = 1$

38. Calculate  $[NO]_{DUM}$

$$[NO]_{DUM} = [NO]_{DN}$$

39. Go to step 43.

Steps 40-42 are performed only if  $1 < J < 5.$

40. Calculate  $[\Delta NO]$  as:

$$[\Delta NO] = \left| \frac{([NO]_{DN} - [NO]_{DUM})}{[NO]_{DN}} \right|$$

Step 41 is performed only if  $[\Delta NO] < 0.005.$

41. Go to step 48.

42. Reset  $[NO]_{DUA}$  as:

$$[NO]_{DUA} = [NO]_{DN}$$

43 Calculate J and N as

$$J = J + 1$$

$$N = 2N$$

44. Go to step 11.

Steps 45 and 46 are performed only if  $J = 5$ .

45. Write the error message stating that the Runge-Kutta iteration failed to converge. Write also the value of  $[ANO]$ , N, and  $X_D$ .

46. Go to step 48.

Step 47 is performed only if  $J = 6$ .

47. Set the appropriate indicator to indicate that this is the last major step in the combustor.

48. Calculate  $[NO]$  as

$$[NO] = [NO]_{DN}$$

49. Calculate  $\bar{M}$  as

$$\bar{M} = \bar{p} + \bar{T} * 82.0571 / P$$

50. Calculate  $[\bar{C}_{15}]_e$ ,  $[\bar{CO}]_e$ , and  $[\bar{CH}_2]_e$  as:

$$[\bar{C}_{15}]_e = (\bar{C}_{15})_{ex_D} * 12 / \bar{M}$$

$$[\bar{CO}]_e = (\bar{CO})_{ex_D} * 28 / \bar{M}$$

$$[\bar{CH}_2]_e = (\bar{CH}_2)_{ex_D} * 14 / \bar{M}$$

51. Calculate  $\{NO\}$ ,  $[NO^*]$ , and  $[NO]$  as:

$$\{NO\} = [NO] * 10^6 * \bar{M} / 30.0$$

$$[NO^*] = [NO] * \bar{p}$$

$$[NO] = [NO] * M_D^* * 1000 / (\dot{M}_F)_{x_D}$$

52. Calculate  $\{\bar{C}_{15}\}_e$ ,  $\{\bar{CO}\}_e$ , and  $\{\bar{CH}_2\}_e$  as:

$$\{\bar{C}_{15}\}_e = [\bar{C}_{15}]_e * 10^6 * \bar{M} / 12$$

$$\{\bar{CO}\}_e = [\bar{CO}]_e * 10^6 * \bar{M} / 28$$

$$\{\bar{CH}_2\}_e = [\bar{CH}_2]_e * 10^6 * \bar{M} / 14$$

53. Calculate  $[\bar{C}_{(s)}^*]_e$ ,  $[\bar{CO}^*]_e$ , and  $[\bar{CH}_2^*]_e$  as:

$$[\bar{C}_{(s)}^*]_e = [\bar{C}_{(s)}]_e * \bar{p}$$

$$[\bar{CO}^*]_e = [\bar{CO}]_e * \bar{p}$$

$$[\bar{CH}_2^*]_e = [\bar{CH}_2]_e * \bar{p}$$

54. Calculate  $[\bar{C}_{(s)}]_e$ ,  $[\bar{CO}]_e$ , and  $[\bar{CH}_2]_e$  as:

$$[\bar{C}_{(s)}]_e = [\bar{C}_{(s)}^*]_e * M_D^* + 1000 / (\dot{M}_F)_{x_D}$$

$$[\bar{CO}]_e = [\bar{CO}^*]_e * M_D^* + 1000 / (\dot{M}_F)_{x_D}$$

$$[\bar{CH}_2]_e = [\bar{CH}_2^*]_e * M_D^* + 1000 / (\dot{M}_F)_{x_D}$$

Steps 55 and 56 are performed only if the nitric oxide reaction is frozen at this point in the combustor.

55. Calculate  $M_D^*$  as:

$$M_D^* = \frac{1}{2} (M_D^* + M_U^*)$$

56. Calculate  $\bar{p}$  as:

$$\bar{p} = \frac{1}{2} (\bar{p} + (\bar{p})_{rr})$$

57. Calculate  $\bar{\gamma}_{inc}$  as:

$$\bar{\gamma}_{inc} = \Delta X * \bar{p} * A|_{x_D} / M_D^*$$

58. Calculate  $\bar{\gamma}_{DIL}$  and  $\bar{\gamma}$  as:

$$\bar{\gamma}_{DIL} = \bar{\gamma}_{DIL} + \bar{\gamma}_{inc}$$

$$\bar{\gamma} = \bar{\gamma} + \bar{\gamma}_{inc}$$

59. Calculate  $V$  as:

$$V = M_D^* / \bar{p} * A|_{x_D}$$

60. Calculate  $\bar{\phi}$  as:

$$\bar{\phi} = \bar{F} / (k_s (1 - \bar{F}))$$

61. Calculate  $[\Delta \bar{NO}]_{\Delta x}$  as:

$$[\Delta \bar{NO}]_{\Delta x} = \frac{[\bar{NO}] - [\bar{NO}]_{UP}}{[\bar{NO}]}$$

62. Calculate  $n_{step}$  as:

$$n_{step} = (X_{END} - X_U) / \Delta X$$

Step 63 is performed only if  $([\Delta \bar{NO}]_{\Delta x} * n_{step}) < 0.05$

63. Set the appropriate indicator to indicate that the nitric oxide reaction is frozen at this point in the combustor.

64. Using Subroutine PRINTS, write the output for this axial station in the dilution zone.

65. Reset  $[\bar{NO}]_{UP}$  as:

$$[\bar{NO}]_{UP} = [\bar{NO}]$$

66. Reset  $(\bar{p})_{rr}$  as:

$$(\bar{p})_{rr} = \bar{p}$$

Step 67 is performed only if the appropriate indicator indicates that this is the last step in the dilution zone.

67. Go to step 75.

Step 68 is performed only if the nitric oxide reaction is frozen at this point in the combustor.

68. Write a message indicating frozen conditions exist in the combustor.

Step 69 is performed only if the appropriate indicator has been previously set to indicate that the nitric oxide reaction is frozen.

69. Go to step 16.

70. Calculate  $X_{XXX}$  as:

$$X_{XXX} = X_{END} - X_D$$

Step 71 is performed only if  $\Delta X < X_{XXX}$

71. Go to step 8.

72. Calculate  $\Delta X$  as:

$$\Delta X = X_{XXX}$$

73. Set the appropriate indicator to indicate that this is the last step in the dilution zone.

74. Go to step 8.

75. Return.

```

SUBROUTINE DILUTE
REAL MSTARD,NO,NOEQXD,NONO,MSTARU
COMMON/DATA1/AIR(50),RR(50),XX(50),FF(50),BCON1(50),BCON2(50),CH2(
150),ZP(70),CUMDIS(70),VP,RHO(50),BCON6(50),ATT(50),PPP,FNOXP,R1(50)
2),R6(50),EK1(50),EK2(50),A2,A3,XL,CN,BETA,S,PHIP,EKS,XEND,A1
COMMON/OUT1/AVECSG,AVECOG,AVCH2G,AVECSP,AVECOP,AVCH2P,AVECSO,AVECODIL
1D,AVCH2D,AVECSF,AVECOF,AVCH2F
COMMON/OUT2/AVENUG,AVENOD,AVENOP,AVENOF,AVENFU,RRO,ILAST
COMMON/OUT3/INDIC,NO(50),AVET,TAUBAR,RHOBAR,PHIBAR,IMAX,XD,
1FBARD,XU,LEN,TAUINT,TAUDIL,VELOC
COMMON/OUT4/CONGNO(50),DEL4D(50),AREAD,ASLOPE,DMFUO,SLOPE(50),TSLODIL
1PE,NOP(50),EKKD,DMFT,UDM(50),DDM(50),F8(50),DMFUD,AIRD,DMFFEDDIL
2,RSUBX,SIG,SIGZER,AVEMM,DMDDA(50),DMDDM(50),DMDDP(50),DMDDPP(50),FDIL
3PRIME(50),NOEQXD,ANO,AQQ,DIFNO(50),NOZERO(50),ROOT(50),E(50)
COMMON/OUT5/MSTARD,MSTARU
COMMON/OUT6/REAT,DILL
C****
C**** SET INITIAL INDICATORS, CALCULATE DELTAX, CHECK X
C****
  NPRINT=0
  LSGN=3
  INDIC=3
  IEND=0
  IF(S.EQ.0.0) ILAST=0
  DNO = ANO
  IF(ILAST.EQ.1) GO TO 2000
  XU=XD
  TAUDIL=0.0
  Q=AQQ
  DELTAX=0.1*RSUBX
  XDZ = XEND-XU
  IF(DELTAX.LE.XDZ) GO TO 200
  DELTAX = XDZ
  IEND=1
200 CONTINUE
C****
C**** STORE INITIAL VALUES FOR BEGINNING OF EACH MAJOR STEP
C****
  250 CONTINUE
  AIRXX = AIRD
  NONO = DNO
  QQ=Q
  XXX = XD
  J=1
  V=20
  DDIFNO = 0.0
C****
C**** SET INITIAL VALUES EQUAL TO STORED VALUES EACH TIME N CHANGES
C****
  300 II=1
  IF(J.EQ.1) GO TO 400
  AIRD = AIRXX
  XU=XXX
  Q=QQ
  DNO = NONO
  400 EN=N
  DELX=DELTAX/EN
C****
C**** START THE MAJOR STEPS DOWN THE COMBUSTOR
C****

```

```

GO TO 2500
2000 N=10
    II=N
    J=6
    DELX=XEND-XD
    DELTAX=DELX
    XU=XD
    ANO=DNO
2500 DO 3000 II=1,N
    XD=XU*DELX
    CALL ZMASS(DELX)
C****
C**** CALCULATE NO AT XD
C****
    CALL MINT(1,FBARD,35,FF,R1,R1LST)
    CALL MINT(1,FBARD,35,FF,R6,R6LST)
    CALL MINT(1,FBARD,35,FF,EK1,EK1LST)
    CALL MINT(1,FBARD,35,FF,EK2,EK2LST)
    CALL MINT(1,FBARD,35,FF,BCON6,YNOXD)
    CALL MINT(1,FBARD,35,FF,RHO,RHOBAR)
    CALL MINT(1,FBARD,35,FF,ATT,AVET)
    CALL MINT(1,FBARD,35,FF,BCON1,YCSXD)
    CALL MINT(1,FBARD,35,FF,BCON2,YCOXD)
    CALL MINT(1,FBARD,35,FF,CH2,YCH2XD)
    IF(IILAST.EQ.1) DNO=ANO*MSTARU/MSTARD
    IF(IILAST.EQ.1) GO TO 4000
    STORE1 = R1(1)
    STORE2 = R6(1)
    STORE3 = EK1(1)
    STORE4 = EK2(1)
    R1(1) = R1LST
    R6(1) = R6LST
    EK1(1) = EK1LST
    EK2(1) = EK2LST
    NOEQXD=YNOXD*30.0/(RHOBAR*AVET*82.057/PPP)
    CALL RUNKUT(XU,DELX,DNO,Q,LSGN,1)
    R1(1) = STORE1
    R6(1) = STORE2
    EK1(1) = STORE3
    EK2(1) = STORE4
3000 CONTINUE
C****
C**** WRITE CONTROL
C****
    IF(NPRINT.EQ.0) GO TO 4000
    WRITE(6,3500) XD,J,RHOBAR,DNO,REAT,DILT
    WRITE(6,9997) DDIFNO,N
3500 FORM44(9H X(CM) = ,E12.5,4HJ = ,I6,18H AVE. RHO(GM/CC) = ,E12.5,17H
1AVE. NO(GM/CM) = ,E12.5,5X,2E12.5)
C****
C**** LOGIC CONTROL ON J
C****
4000 CONTINUE
    GO TO (4100,4300,4300,4300,4600,4800), J
4100 DUMMY = DNO
    GO TO 4500
4300 DDIFNO = ABS((DNO-DUMMY)/DNO)
    IF(DDIFNO.LT.0.005) GO TO 5000
    DUMMY = DNO
4500 J=J+1

```

DIL\*0600  
 DIL\*0610  
 DIL\*0620  
 DIL\*0630  
 DIL\*0640  
 DIL\*0650  
 DIL\*0660  
 DIL\*0670  
 DIL\*0680  
 DIL\*0690  
 DIL\*0700  
 DIL\*0710  
 DIL\*0720  
 DIL\*0730  
 DIL\*0740  
 DIL\*0750  
 DIL\*0760  
 DIL\*0770  
 DIL\*0780  
 DIL\*0790  
 DIL\*0800  
 DIL\*0810  
 DIL\*0820  
 DIL\*0830  
 DIL\*0840  
 DIL\*0850  
 DIL\*0860  
 DIL\*0870  
 DIL\*0880  
 DIL\*0890  
 DIL\*0900  
 DIL\*0910  
 DIL\*0920  
 DIL\*0930  
 DIL\*0940  
 DIL\*0950  
 DIL\*0960  
 DIL\*0970  
 DIL\*0980  
 DIL\*0990  
 DIL\*1000  
 DIL\*1010  
 DIL\*1020  
 DIL\*1030  
 DIL\*1040  
 DIL\*1050  
 DIL\*1060  
 DIL\*1070  
 DIL\*1080  
 DIL\*1090  
 DIL\*1100  
 DIL\*1110  
 DIL\*1120  
 DIL\*1130  
 DIL\*1140  
 DIL\*1150  
 DIL\*1160  
 DIL\*1170  
 DIL\*1180  
 DIL\*1190

```

      N=2*N
      GO TO 300
4600 WRITE(6,4700) DDIFNO,N,XD
4700 FORMAT(///,59H RUNGE-KUTTA ITERATION FAILED TO CONVERGE TO SPECIFIED LIMIT.DIFNO = ,E12.5,5H N = ,I4,5H X = ,E12.5,5H CMS.//)
      GO TO 5000
4800 IENDU = 1
5000 CONTINUE
C****
C**** WRITE THE APPROPRIATE OUTPUT FOR THIS AXIAL STATION
C****
      AVENOG = DNO
      AVE MW = RHOBAR*AVET*82.057/PPP
      AVE CSG = YCSXD*12.0/AVEMW
      AVE CUG = YCOXD*28.0/AVEMW
      AVCH2G = YCH2XD*14.0/AVEMW
      AVENOP = AVENOG*1.0E+06*AVEMW/30.0
      AVENOU = AVENOG*RHOBAR
      AVENOF = AVENOG*MSTARD*1000.0/DMFT
      AVE CSP = AVE CSG*1.0E+06*AVEMW/12.0
      AVE CUP = AVE CUG*1.0E+06*AVEMW/28.0
      AVCH2P = AVCH2G*1.0E+06*AVEMW/14.0
      AVE CSU = AVE CSG*RHOBAR
      AVE COU = AVE CUG*RHOBAR
      AVCH2U = AVCH2G*RHOBAR
      AVE CSF = AVE CSG*MSTARD*1000.0/DMFT
      AVE COF = AVE CUG*MSTARD*1000.0/DMFT
      AVCH2F = AVCH2G*MSTARD*1000.0/DMFT
C****
C**** CALCULATE RESIDENCE TIMES, ETC
C****
      IF(I-LAST.EQ.1) MSTARD = 0.5*(MSTARDU+MSTARD)
      IF(I-LAST.EQ.1) RHOBAR = 0.5*(RHOBARU+RRO)
      TAU = DELTAX*RHOBAR*AREAD/MSTARD
      TAU DIL = TAU DIL + TAU
      TAU BAR = TAU BAR + TAU
      VELOC = MSTARD/(RHOBAR*ARLAD)
      PHIBAR = FBARD/(EKS*(1.0-FBARD))
      FURAT = (AVENOF-AVENFU)/AVENOF
      STEPS = (XEND-XU)/DELTAX
      IF(FURAT*STEPS.LT.0.05) I-LAST = 1
      CALL PRINTS
C****
C**** CONTROL OVERALL STEPS
C****
      AVENFU = AVENOF
      RRO = RHOBAR
      IF(I-END.EQ.1) GO TO 9000
      IF(I-LAST.EQ.1) WRITE(6,9500)
9500 FORMAT(////,10X,42HNITRIC OXIDE REACTION FROZEN AT THIS POINT,///)
      1)
      IF(I-LAST.EQ.1) GO TO 2000
      XXXX = XEND-XU
      IF(DELTAX.LT.XXXX) GO TO 250
      DELTAX = XXXX
      IENDU = 1
      GO TO 250
9000 RETURN
9997 FORMAT(20X,E10.3,15)
      END

```

```

DIL*1203
DIL*1210
DIL*1220
DIL*1230
DIL*1240
DIL*1250
DIL*1260
DIL*1270
DIL*1280
DIL*1290
DIL*1300
DIL*1310
DIL*1320
DIL*1330
DIL*1340
DIL*1350
DIL*1360
DIL*1370
DIL*1380
DIL*1390
DIL*1400
DIL*1410
DIL*1420
DIL*1430
DIL*1440
DIL*1450
DIL*1460
DIL*1470
DIL*1480
DIL*1490
DIL*1500
DIL*1510
DIL*1520
DIL*1530
DIL*1540
DIL*1550
DIL*1560
DIL*1570
DIL*1580
DIL*1590
DIL*1600
DIL*1610
DIL*1620
DIL*1630
DIL*1640
DIL*1650
DIL*1660
DIL*1670
DIL*1680
DIL*1690
DIL*1700
DIL*1710
DIL*1720
DIL*1730
DIL*1740
DIL*1750
DIL*1760
DIL*1770
DIL*1780
DIL*1790

```

## APPENDIX VII - SUBROUTINE PRCALC

The function of Subroutine PRCALC is to calculate the average nitric oxide level at the exit of the primary zone for each mixture ratio element.

Subroutine PRCALC is called by Subroutine PRIMRY; it, in turn, calls Subroutine MINY. Subroutine PRCALC does not require external input and does not provide external output except for an error message and diagnostic data table. External output is written directly onto the output-tape unit. Internal input and output are transmitted through COMMON and as arguments of the subroutine. The internal input consists of:

ATT	BCON1	BCON2	BCON6	CH2
CONGNO	DELMD	EK1	EK2	FBARD
FF	FNOXG	IMAX	NOZERO	PPP
RHO	R1	R6	S	

The internal output consists of:

AQQ	AVET	NO	NOEQXD	RHOBAR
TAUBAR				

The external output consists of:

ALPHA2	DUMMY	LIMIT	SUMTNO
--------	-------	-------	--------

Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols in Subroutine PRCALC which are not included in COMMON.

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AAA(i)	$\alpha_2$	Ratio of NO concentration to NO concentration at equilibrium for a mixture element i at the end of the integration interval	
ALPHA2(i)	$(\alpha_D)_i$	Ratio of NO concentration to NO concentration at equilibrium for a mixture element i at the end of the integration interval	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
ALPHAT(I)	$(\alpha_T)_i$	Ratio of NO concentration to NO concentration at equilibrium for a mixture element i at the mean primary zone residence time	
ALPHAU(I)	$(\alpha_U)_i$	Ratio of NO concentration to NO concentration at equilibrium for a mixture element i at the start of the integration interval	
ALPHA1	$\alpha_1$	Ratio of NO concentration to NO concentration at equilibrium for a mixture element i at the start of the integration interval	
ALPHA2	$\alpha_2$	Ratio of NO concentration to NO concentration at equilibrium for a mixture element i at the end of the integration interval	
ALPHD	$(\alpha_D)_i$	Ratio of NO concentration to NO concentration of equilibrium for a mixture element i at the end of integration interval	
ALPHU	$(\alpha_U)_i$	Ratio of NO concentration to NO concentration at equilibrium for a mixture element i at the start of the integration interval	
DALP	$(\Delta\alpha)_i$	Integration interval	
DALPHA	$(\Delta\alpha)_i$	Integration interval	
DUMMY(I)		Dummy variable	
EK1LST	$(K_1)_{LST}$	Ratio of forward reaction rate constants at mean primary zone mixture ratio (See Volume 2, Section 2 or Ref 3)	
EK2LST	$(K_2)_{LST}$	Ratio of forward reaction rate constants at mean primary zone mixture ratio (See Volume 2, Section 2 or Ref 3)	
EN	$\tau$	Integration step size control	
ERR	$\epsilon_{err}$	Convergence limit	
FNOXG	$[NO_x]$	NO formed in the flame front (mass fraction)	
FT	$f_t$	Fractional mass in an element that has a residence time $dt$ about $t$	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
FTD	$(f_{T_e})_D$	Accumulated mass fraction leaving element before $t_D$	
FTU	$(f_{T_e})_U$	Accumulated mass fraction leaving element before $t_U$	
INDEX		Indicator: INDEX = 0 at start of iteration INDEX = 1 if convergence criteria not satisfied	
J		Counter: J < 6 if convergence occurs on $\sum_{t=ND}$ J = 6 if convergence limit is not satisfied on $\sum_{t=ND}$	
JJ		Counter: JJ ≤ 20 if convergence test on $(f_{T_e})_{rem}$ applied JJ > 20 if convergence test on $(f_{T_e})_{rem}$ not applied	
K		Indicator: K = 1 if first integration step K ≠ 1 if other than first integration step	
LIMIT		Indicator: LIMIT < 10 if convergence occurs LIMIT ≥ 10 if convergence criteria not satisfied	
N	N	Integration step size control	
REMAIN (I)	$(f_{T_e})_{rem}$	Fraction of mass remaining in element i after convergence criteria satisfied	
R1LST	$(R_1)_{LST}$	Forward reaction rate for the first kinetic reaction for an element at mean primary zone mixture ratio (See Volume 2, Section 2 or Ref 3)	gm-mole/cm <sup>3</sup> -sec
R6LST	$(R_6)_{LST}$	Forward reaction rate for the sixth kinetic reaction for an element at mean primary zone mixture ratio (See Volume 2, Section 2 or Ref 3)	gm-mole/cm <sup>3</sup> -sec
STORE1		Dummy variable	gm-mole/cm <sup>3</sup> -sec

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
STORE2		Dummy variable	gm-mo.e/ cm <sup>3</sup> -sec
STORE3		Dummy variable	
STORE4		Dummy variable	
SUMT (i)	$\sum t$	Sum to time t of the mass fractions in an element i	
SUMTNO (i)	$\sum t_{NO}$	Sum to time t of the products of the mass fraction and NO concentrations in an element i	
TD	$t_D$	Time at end of integration interval	sec
TIMEN	$t_n$	Characteristic time used to calculate $(F_t)_D$	sec
TT	$tt$	Dummy variable	sec
TTS	$tt_s$	Time at end of integration interval	sec
TTU	$tt_u$	Time at start of integration interval	sec
TU	$t_u$	Time at start of integration interval	sec
YCH2XD	$[CH_2]_{e,x_D}$	Equilibrium mole fraction of unburned hydrocarbons exclusive of $C_{(s)}$ and CO for an element at the mean primary zone mixture ratio	
YCOXD	$[CO]_{e,x_D}$	Equilibrium mole fraction of CO for an element at the mean primary zone mixture ratio	
YCSXD	$[C_{(s)}]_{e,x_D}$	Equilibrium mole fraction of $C_{(s)}$ for an element at the mean primary zone mixture ratio	
YNOXD	$[NO]_{e,x_D}$	Equilibrium mole fraction of NO for an element at the mean primary zone mixture ratio	

#### Analysis Procedure

The step-by-step procedure of Subroutine PRCALC is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. Estimate  $(\alpha_2)_i$  as:

$$(\alpha_2)_i = 0.5$$

2. Calculate  $(\alpha_0)_i$  as:

$$(\alpha_0)_i = 0 \quad \text{if} \quad [\text{NO}_i] = 0$$

$$(\alpha_0)_i = \frac{[\text{NO}_i]}{[\text{NO}_i]_e} \quad \text{if} \quad [\text{NO}_i] \neq 0$$

Step 3 is performed only if the chemical reaction rate is not significant.

3. Go to step 10.
4. Using Subroutine PRRAT, calculate a value of time which corresponds to the estimate of  $(\alpha_2)_i$
5. Calculate  $t_{err}$  as:

$$t_{err} = 1 - \frac{t}{\bar{t}}$$

Steps 6 and 7 are performed only if  $|t_{err}| \gg 0.05$ .

6. Reestimate  $(\alpha_2)_i$

Step 7 is performed only if the number of iterations on  $(\alpha_2)_i$  are less than 10.

7. Go to step 4.
8. Calculate  $(\alpha_1)_i$  as:

$$(\alpha_1)_i = (\alpha_2)_i$$

Step 9 is performed only if the number of iterations on  $(\alpha_1)_i$  equal 10.

9. Write the value of  $\alpha_2$
10. If this is not the last element in the array, go to step 1.
11. Initialize  $n$  as:

$$n = 10$$

Step 12 is performed only if  $(\alpha_1)_3 = 0$ .

12. Go to step 50.

Step 13 is performed only if the chemical reaction rate is not significant.

13. Go to step 50.

14. Calculate  $(\Delta x)_i$  and  $t_u$  as:

$$(\Delta x)_i = (x_u)_i / n$$

$$t_u = 0$$

15. Calculate  $(\alpha_D)_i$  as:

$$(\alpha_D)_i = (x_u)_i + (\Delta x)_i$$

Step 16 is performed only if  $(\alpha_D)_i > 1.0$ .

16. Recalculate  $(\alpha_D)_i$  as:

$$(\alpha_D)_i = 1.0$$

Steps 17 through 27 are performed only if  $S_0 = 0$

17. Using Subroutine MINT, calculate  $(R_1)_{LST}$   
 18. Using Subroutine MINT, calculate  $(R_2)_{LST}$   
 19. Using Subroutine MINT, calculate  $(k_1)_{LST}$   
 20. Using Subroutine MINT, calculate  $(k_2)_{LST}$   
 21. Using Subroutine MINT, calculate  $[NO]_{e,x_D}$   
 22. Using Subroutine MINT, calculate  $\bar{P}$   
 23. Using Subroutine MINT, calculate  $\bar{T}$   
 24. Using Subroutine MINT, calculate  $[CO]_{e,x_D}$   
 25. Using Subroutine MINT, calculate  $[O]_{e,x_D}$   
 26. Using Subroutine MINT, calculate  $[H_2]_{e,x_D}$   
 27. Calculate  $[NO]_{e,x_D}$  as:

$$[NO]_{e,x_D} = \frac{[NO]_{e,x_D} \times 30.0 \times \bar{P}}{\bar{P} \times \bar{T} \times 82.057}$$

28. Using Subroutine PRRAT, calculate  $(\alpha_D)_i$ .

Step 29 is performed only if  $S_0 = 0$

29. Calculate  $Q$  as:

$$Q = 0$$

Steps 30 through 32 are performed only for the first integration step.

30. Calculate  $(F_t)_0$  as:

$$(F_t)_0 = 0$$

31. Reset  $(x_u)_i$  and  $t_u$  as:

$$(x_u)_i = (x_u)_i$$

$$t_u = t_t$$

32. Go to step 15.

33. Calculate  $t_D$  as:

$$t_D = tt$$

34. Calculate  $t_n$  as:

$$t_n = \frac{1}{2} (t_U + t_D)$$

35. Calculate  $(F_t)_D$  as:

$$(F_t)_D = 1 - \exp(-t_n/\sigma_T)$$

36. Calculate  $F_t, (F_t)_U, \Sigma_t$  and  $\Sigma_{t-NO}$

37. Reset  $(x_U)_i$  and  $t_U$  as:

$$(x_U)_i = (x_D)_i$$

$$t_U = t_D$$

Step 38 is performed if the convergence criteria on  $(F_t)_{rem}$  are not satisfied but those on  $\Sigma_{t-NO}$  are.

38. Go to step 45.

Step 39 is performed if  $tt < 5\sigma_T$

39. Go to step 15.

Steps 40 through 42 are performed if the convergence criteria on  $\Sigma_{t-NO}$  are not satisfied.

40. If the number of iterations on  $\Sigma_{t-NO}$  equal 6 go to step 43.

41. Reset  $n$  as:

$$n = 2n$$

42. Go to step 14.

43. If the number of iterations on  $\Sigma_{t-NO}$  are equal to 6, write a diagnostic statement identifying element and the last two values of  $\Sigma_{t-NO}$

44. Calculate  $(\Delta x)_i$  as:

$$(\Delta x)_i = 5(\Delta x)_i$$

45. Calculate  $(F_t)_{rem}$  as:

$$(F_t)_{rem} = 1 - \Sigma_t$$

Step 46 is performed if  $\sum_{t=NO} < 10^{-5}$

46. Go to step 48.

Step 47 is performed only if the number of iterations on  $(f_t)_{rem}$  are less than or equal to 20.

47. If convergence criteria on  $(f_t)_{rem}$  are not satisfied, reset  $(\alpha_i)_i$  as:

$$(\alpha_i)_i = (\alpha_i)_i$$

and go to step 15.

48. Calculate  $\sum_{t=NO}$  and  $[NO]$

49. Reset  $n$  as:

$$n = n/8$$

50. If this is not the last element in the array, go to step 12.

51. Return.

```

SUBROUTINE PRCALC(FNOXG)
REAL NO
DIMENSION SUMTNC(50),DUMMY(50),SUNT(50),REMAIN(50),ALPHAT(50),ALPHA
1AU(50),ALPHAD(50)
COMMON/DATA1/AIR(50),RR(50),XX(50),FF(50),BCON1(50),BCON2(50),CH2(
150),ZP(70),CUMDIS(70),VP,RHO(50),BCON6(30),ATT(50),PPP,FNOXP,R1(50
2),R6(50),EK1(50),EK2(50),A2,A3,XL,CN,BETA,S,PHIP,EKS,XEND,A1
COMMON/OUT3/INDIC,NO(50),AVET,TAUBAR,RHOBAR,PHIBAR,IMAX,XD,
1FBAHD,XU,LEN,TAUINT,TAUDIL,VELOC
COMMON/OUT4/CONGNO(50),DELM(50),AREAD,ASLOPE,DMFUD,SLOPE(50),TSLO
1PE,NOP(50),EKKD,DMFT,UDM(50),DDM(50),F8(50),DMFUD,AIRD,DMFFED
2,RSUBX,SIG,SIGZER,AVEMW,DMDDA(50),DMDDM(50),DMDDP(50),DMDCPP(50),F
3PRIME(50),NOEGXD,ANO,AQQ,DIFNO(50),NOZERO(50),RDOT(50),E(50)
C****
C**** SET INDICES,INITIAL VALUES,ETC.
C****
TTU = 0.0
TTS=0.0
DO 50 I = 1,50
NO(I) = 0.0
50 CONTINUE
DO 1000 I =1,IMAX
ALPHA2=0.5
LIMIT = 0
IF(CONGNO(I).EQ.0.0) ALPHAU(I) = 0.0
IF(CONGNO(I).NE.0.0) ALPHAU(I) = FNOXG/CONGNO(I)
IF(NOZERO(I).EQ.1) GO TO 1000
ALPHA1 = ALPHAU(I)
DALP=ALPHA1
C****
C**** CALCULATE THE VALUE OF ALPHA-TAU
C****
100 TT = TTU
LIMIT=LIMIT+1
CALL PRRAT(ALPHA1,ALPHA2,TT,I)
AAA=ALPHA2
ERR=(1.0-(TT/TAUBAR))
IF(ABS(ERR)-0.05) 300,200,200
200 ALPHA2=AAA+(AAA-DALP)*(TAUBAR-TT)/(TT-TTS)
IF(ALPHA2.LE.0.0) ALPHA2 = AAA/2.
IF(ALPHA2.GT.1.0) ALPHA2=1.2*AAA
IF(ALPHA2.GT.1.0) ALPHA2=0.998
DALP=AAA
TTS=TT
IF(LIMIT.LT.10) GO TO 100
300 ALPHAT(I)=ALPHA2
IF(LIMIT.EQ.10) WRITE(6,9997) ALPHA2,LIMIT
1000 CONTINUE
C****
C**** BEGIN NO CALCULATIONS FOR THE ITH ELEMENT
C****
N = 10
EN = N
DO 5000 I =1,IMAX
NO(I) = ALPHAU(I)
IF(DELM(I).EQ.0.0) GO TO 4000
IF(NOZERO(I).EQ.1) GO TO 4000
C****
C**** SET ADDITIONAL INDICES,INITIAL VALUES,ETC.
C****

```

INDEX = 0	PRC*0600
J = 1	PRC*0610
JJ=1	PRC*0620
DUMMY(I) = 0.0	PRC*0630
1150 DALPHA=ALPHAT(I)/EN	PRC*0640
SUMTNO(I) = 0.0	PRC*0650
SUMT(I) = 0.0	PRC*0660
K = 0	PRC*0670
ALPHU=ALPHAU(I)	PRC*0680
TU=0.0	PRC*0690
1200 ALPHD=ALPHU+DALPHA	PRC*0700
C****	PRC*0710
C**** PRRAI OVERWRITTEN IF ALPHD.GT.0.99	PRC*0720
C****	PRC*0730
IF(ALPHD.GT.1.0) ALPHD = 1.	PRC*0740
TT=TU	PRC*0750
C****	PRC*0760
C**** SPECIAL CASE S=0.0 IN PRIMARY ZONE	PRC*0770
C****	PRC*0780
IF(S.NE.0.0) GO TO 1210	PRC*0790
CALL MINT(1,FBARD,35,FF,R1,R1LST)	PRC*0800
CALL MINT(1,FBARD,35,FF,R6,R6LST)	PRC*0810
CALL MINT(1,FBARD,35,FF,EK1,EK1LST)	PRC*0820
CALL MINT(1,FBARD,35,FF,EK2,EK2LST)	PRC*0830
CALL MINT(1,FBARD,35,FF,BCON6,YNOXD)	PRC*0840
CALL MINT(1,FBARD,35,FF,RHO,RHOBAR)	PRC*0850
CALL MINT(1,FBARD,35,FF,ATT,AVET)	PRC*0860
CALL MINT(1,FBARD,35,FF,BCON1,YCSXD)	PRC*0870
CALL MINT(1,FBARD,35,FF,BCON2,YCOXD)	PRC*0880
CALL MINT(1,FBARD,35,FF,CH2,YCH2XD)	PRC*0890
STORE1 = R1(I)	PRC*0900
STORE2 = R6(I)	PRC*0910
STORE3 = EK1(I)	PRC*0920
STORE4 = EK2(I)	PRC*0930
R1(I) = R1LST	PRC*0940
R6(I) = R6LST	PRC*0950
EK1(I) = EK1LST	PRC*0960
EK2(I) = EK2LST	PRC*0970
NOEQXD=YNOXD*30.0/(RHOBAR*AVET*82.057/PPP)	PRC*0980
1210 CALL PRRAT(ALPHU,ALPHD,TT,I)	PRC*0990
IF(S.NE.0.0) GO TO 1220	PRC*1000
R1(I) = STORE1	PRC*1010
R6(I) = STORE2	PRC*1020
EK1(I) = STORE3	PRC*1030
EK2(I) = STORE4	PRC*1040
AQQ=0.0	PRC*1050
1220 CONTINUE	PRC*1060
K = K+1	PRC*1070
IF(K.NE.1) GO TO 1251	PRC*1080
FTU=0.0	PRC*1090
ALPHU=ALPHD	PRC*1100
TU=TT	PRC*1110
GO TO 1200	PRC*1120
1251 TD=TT	PRC*1130
TIMEN=0.5*(TU+TD)	PRC*1140
FTD=1.0-EXP(-TIMEN/TAUBAR)	PRC*1150
FT=FTD-FTU	PRC*1160
FTU=FTD	PRC*1170
TU=TD	PRC*1180
ALPHU=ALPHD	PRC*1190

SUMT(I) = SUMT(I)+FT	PRC*1200
SUMTNC(I)=SUMTNO(I)+ALPHU*CONGNO(I)*FT	PRC*1210
IF(INDEX.EQ.1) GO TO 1400	PRC*1220
IF(TT.LT.5.0*TAUBAR) GO TO 1200	PRC*1230
IF(ABS((SUMTNO(I)-DUMMY(I))/SUMTNO(I)).LE.0.01 ) GO TO 1300	PRC*1240
IF(J.EQ.6) GO TO 1300	PRC*1250
EN = 2.0*EN	PRC*1260
DUMMY(I) = SUMTNO(I)	PRC*1270
J = J+1	PRC*1280
GO TO 1150	PRC*1290
1300 IF(J.NE.6) GO TO 1350	PRC*1300
WRITE(6,9000) SUMTNO(I),DUMMY(I),I	PRC*1310
9000 FORMAT(55H POTENTIAL ERROR DUE TO LACK OF CONVERGENCE,SUMTNO(I)= ,	PRC*1320
1E15.8,2X,26HPRIOR VALUE OF SUMTNO(I)= ,E15.8,2X,3HI= ,I2///)	PRC*1330
1350 DALPHA=5.0*DALPHA	PRC*1340
1400 REMAIN(I) = 1.-SUMT(I)	PRC*1350
IF(REMAIN(I)*CONGNO(I) .GT.0.001*SUMTNO(I)) INDEX = 1	PRC*1360
IF(SUMTNO(I).LT.1.0E-05) GO TO 1500	PRC*1370
JJ=JJ+1	PRC*1380
IF(JJ.GT.20) GO TO 1500	PRC*1390
IF(REMAIN(I)*CONGNO(I) .GT.0.001*SUMTNO(I)) DALPHA=ALPHA(I)	PRC*1400
IF(REMAIN(I)*CONGNO(I) .GT.0.001*SUMTNO(I)) GO TO 1200	PRC*1410
1500 SUMTNO(I)=SUMTNO(I)+(CONGNO(I)*ALPHU*REMAIN(I))	PRC*1420
NO(I) = SUMTNO(I)	PRC*1430
EN=EN/8.	PRC*1440
4000 CONTINUE	PRC*1450
5000 CONTINUE	PRC*1460
9997 FORMAT(35X,E12.5,I6)	PRC*1470
RETURN	PRC*1480
END	PRC*1490

## APPENDIX VIII - SUBROUTINE PRRAT

The function of Subroutine PRRAT is to solve the analytical expression relating nitric oxide concentration to time.

Subroutine PRRAT is called by Subroutine PRCALC; it does not call any other subroutines. Subroutine PRRAT does not require external input and does not provide external output. Internal input and output are transmitted through COMMON and as arguments of the subroutine. The internal input consists of:

CONGNO	EK1	EK2	FINIS	I
INIT	R1	R6	RHO	TIME

The internal output consists of:

TIME

### Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols in Subroutine PRRAT which are not included in COMMON:

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
A	A	Constant	cm <sup>3</sup> /gm-mole
B	B	Constant	gm-mole/cm <sup>3</sup> - sec
D	D	Constant	gm-mole/cm <sup>3</sup> - sec
DUMMY	C <sub>1</sub>	Dummy variable	cm <sup>3</sup> -sec/gm- mole
DUMMYA	C <sub>2</sub>	Dummy variable	cm <sup>3</sup> -sec/gm-mole
DUMMYB	C <sub>3</sub>	Dummy variable	
E	E	Constant	gm-mole/cm <sup>3</sup> - sec
FINIS	( $\alpha_{fin}$ ) <sub>i</sub>	Ratio of NO concentration to NO concentration at equilibrium for an element of mixture ratio F and pressure P at the end of the integration interval	

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
I	i	Index of the element in question	
INIT	$(\alpha_{init})_i$	Ratio of NO concentration to NO concentration at equilibrium for an element of mixture ratio F and pressure P at the start of the integration interval	
TIME	$t_0$ and $t_f$	Value of time at start of integration interval ( $t_0$ ) and at end of integration interval ( $t_f$ )	sec

### Analysis Procedure

The step-by-step procedure of Subroutine PRRAT is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. If  $(\alpha_{fin})_i$  is greater than 0.99, then  $t_f = 10t_0$ . Go to step 10.

2. Calculate  $A = \frac{\sum M_{NO}}{P_i [NO]_e}$

3. Calculate  $B = \frac{(R_0)_i}{1 + (K_2)_i}$

4. Calculate  $D = (R_1)_i + B$

5. Calculate  $E = B(K_1)_i$

6. Calculate  $C_1 = \frac{E(K_1)_i - D}{E^2 - D^2}$

7. Calculate  $C_2 = \frac{E - (K_1)_i + D}{E^2 - D^2}$

8. Calculate  $C_3 = \frac{[1 + (\alpha_{fin})_i][1 - (\alpha_{init})_i]}{[1 + (\alpha_{init})_i][1 - (\alpha_{fin})_i]}$

9. Calculate  $t_f = t_0 + \frac{1}{A} \left\{ \left[ \frac{1}{2} C_1 \ln C_3 \right] + \left[ C_2 \ln \left[ \frac{(D + E(\alpha_{fin})_i)(1 - (\alpha_{init})_i)^{1/2}}{(D + E(\alpha_{init})_i)(1 - (\alpha_{fin})_i)^{1/2}} \right] \right] \right\}$

10. Return.

```

SUBROUTINE PRRAT(INIT,FINIS,TIME,I)
REAL INIT
COMMON/DATA1/ATR(50),RR(50),XX(50),FF(50),BCON1(50),BCON2(50),CH2(
150),ZP(70),CUMDIS(70),VP,RHO(50),BCON6(50),AIT(50),PPP,FNOXP,R1(50)
2),R6(50),EK1(50),EK2(50),A2,A3,XL,CN,BETA,S,PHIP,EKS,XEND,A1
COMMON/OUT4/CONGNO(50),DELM(50),AREAD,ASLOPE,DMFUO,SLOPE(50),TSLOP
1PE,NOP(50),EKKD,DMFT,UDM(50),DDH(50),FB(50),DMFUD,AIRD,DMFFED
2,RSUBX,SIG,SIGZER,AVEM,DMDDA(50),DMDDM(50),DMDDP(50),DMDDPP(50),F
3PRIME(50),NOEXN,ANO,AQG,NIFNO(50),NOZERO(50),RDOT(50),SUEA(50)
C****
C**** CALCULATE CONSTANTS
C****
IF(FINIS.GT.0.99) GO TO 2000
A = (2.0*30.6)/(RHO(I)*CONGNO(I))
B = R6(I)/(1.+EK2(I))
D = R1(I)*B
E = B*EK1(I)
DUMMY = (E*EK1(I)-D)/(E*E-D*D)
DUMMYA = (E-EK1(I)*D)/(E*E-D*D)
C****
C**** CALCULATE TIME
C****
DUMMYB = ((1.+FINIS)*(1.-INIT))/((1.-FINIS)*(1.+INIT))
TIME = (1./A)*((0.5*DUMMY*ALOG(DUMMYB))+(DUMMYA*ALOG((D+E*FINIS)*
1SQRT(1.-INIT*INIT))/(D+E*INIT)*SQRT(1.-FINIS*FINIS))))+TIME
GO TO 1000
2000 TIME = 10.0*TIME
1000 RETURN
END

```

PRR\*0000  
 PRR\*0010  
 PRR\*0020  
 PRR\*0030  
 PRR\*0040  
 PRR\*0050  
 PRR\*0060  
 PRR\*0070  
 PRR\*0080  
 PRR\*0090  
 PRR\*0100  
 PRR\*0110  
 PRR\*0120  
 PRR\*0130  
 PRR\*0140  
 PRR\*0150  
 PRR\*0160  
 PRR\*0170  
 PRR\*0180  
 PRR\*0190  
 PRR\*0200  
 PRR\*0210  
 PRR\*0220  
 PRR\*0230  
 PRR\*0240  
 PRR\*0250  
 PRR\*0260  
 PRR\*0270  
 PRR\*0280

## APPENDIX IX - SUBROUTINE MINT

The function of Subroutine MINT is to provide an interpolated value of a tabulated function of one variable assuming a linear, logarithmic, or exponential relationship.

Subroutine MINT is called by Subroutines PRCALC, ZINTER, DILUTE, CALCBC, and ZMASS; it does not call any other subroutines. Subroutine MINT does not require external input and does not provide external output. Internal input and output are transmitted as arguments of the subroutine. The internal input consists of:

ILN                      NTAB                      X                      XTAB                      YTAB

The internal output consists of:

Y

Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols used in Subroutine MINT. Since the subroutine may be used with any consistent set of units, the units of the symbols are not specified.

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
A	a	Coefficient in the expression for Y as a function of X	
B	b	Coefficient in the expression for Y as a function of X	
ILN		Indicator: ILN=1 if linear interpolation is required ILN=2 if logarithmic interpolation is required ILN=3 if exponential interpolation is required	
N	n	Index of the tabular entry	
NTAB	N	Number of tabular entries	
N1	n <sub>1</sub>	Index of the tabular entry preceding X	
N2	n <sub>2</sub>	Index of the tabular entry following X	

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
X	$X$	Value of the independent variable at which interpolation is required	
XTAB(N)	$\hat{X}_n$	Tabular entries of the independent variable	
X1	$X_{n_1}$	Value of the independent variable at $n_1$	
X2	$X_{n_2}$	Value of the independent variable at $n_2$	
Y	$Y$	The value of the dependent variable to be interpolated	
YTAB(N)	$\hat{Y}_n$	Tabular entries of the dependent variable	
Y1	$Y_{n_1}$	Value of the dependent variable at $n_1$	
Y2	$Y_{n_2}$	Value of the dependent variable at $n_2$	

#### Analysis Procedure

The step-by-step procedure of subroutine MINT is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. If there is only one tabular entry, set  $Y = Y_1$  and return.
2. If linear or logarithmic interpolation is specified, exclude extrapolation; that is,  
     set  $Y = Y_1$  if  $X < X_1$   
     set  $Y = Y_n$  if  $X > X_n$   
     and return.
3. Determine the tabular entries  $n_1$  and  $n_2$  between which  $X$  lies.
4. Exclude those cases for which the interpolation formulas will degenerate, that is  
     set  $Y = \frac{1}{2}(Y_{n_1} + Y_{n_2})$  if  $X_{n_1} = X_{n_2}$   
     or, set  $Y = Y_{n_1}$  if  $Y_{n_1} = Y_{n_2}$
5. If linear interpolation is specified, set  
      $Y = a + bX$

where  $a = Y_{n_1} - bX_{n_1}$

and  $b = (Y_{n_2} - Y_{n_1}) / (X_{n_2} - X_{n_1})$

and return .

6. If logarithmic interpolation is specified, set

$$Y = e^{a+b/X}$$

where

$$a = \ln(Y_{n_1}) - b/X_{n_1}$$

and

$$b = \ln(Y_{n_2}/Y_{n_1}) / (1/X_{n_2} - 1/X_{n_1})$$

and return .

7. If exponential interpolation is specified; set

$$Y = a/X^b$$

where

$$a = Y_{n_1} (X_{n_1})^b$$

and

$$b = \ln(Y_{n_1}/Y_{n_2}) / \ln(X_{n_2}/X_{n_1})$$

and return .

```

SUBROUTINE MINT(ILN,X,NTAB,XTAB,YTAB,Y)
C      INTERPOLATION OF A FUNCTION OF ONE VARIABLE USING A MULTIPLICITY
C      OF METHODS
      DIMENSION XTAB(1),YTAB(1)
C      CHECK IF THERE IS ONLY ONE TABULAR ENTRY
      IF (NTAB.NE.1) GO TO 10
      Y=YTAB(1)
      RETURN
C      CHECK FOR EXTRAPOLATION IF  $Y=A+B*X$  OR  $LN(Y)=A+B/X$  IS BEING USED
10  IF (ILN.EQ.3) GO TO 50
      IF (X.GT.XTAB(1)) GO TO 20
      Y=YTAB(1)
      RETURN
20  IF (X.LT.XTAB(NTAB)) GO TO 50
      Y=YTAB(NTAB)
      RETURN
C      FIND THE TABULAR ENTRIES BETWEEN WHICH X LIES
50  DO 100 N=2,NTAB
      IF (X.GT.XTAB(N)) GO TO 100
      N2=N
      GO TO 200
100  CONTINUE
      N2=NTAB
200  N1=N2-1
      X1=XTAB(N1)
      X2=XTAB(N2)
      Y1=YTAB(N1)
      Y2=YTAB(N2)
C      CHECK FOR SPECIAL CASES
      IF (X1.NE.X2) GO TO 300
      Y=0.5*(Y1+Y2)
      RETURN
300  IF (Y1.NE.Y2) GO TO 400
      Y=Y1
      RETURN
400  GO TO (500,600,700),ILN
C      INTERPOLATE FOR Y USING  $Y=A+B*X$ 
500  B=(Y2-Y1)/(X2-X1)
      A=Y1-B*X1
      Y=A+B*X
      RETURN
C      INTERPOLATE FOR Y USING  $LN(Y)=A+B/X$ 
600  B=ALOG(Y2/Y1)/(1.0/X2-1.0/X1)
      A=ALOG(Y1)-B/X1
      Y=EXP(A+B/X)
      RETURN

```

C INTERPOLATE FOR Y USING  $Y=A/X^{**B}$

700 B=ALOG(Y1/Y2)/ALOG(X2/X1)

A=Y1\*X1\*\*B

Y=A/X\*\*B

RETURN

END

130

MIN\*0600

MIN\*0610

MIN\*0620

MIN\*0630

MIN\*0640

MIN\*0650

MIN\*0660

MIN\*0670

## APPENDIX X - SUBROUTINE CALCBC

The function of Subroutine CALCBC is to calculate the value of the mass flow coefficient at each axial station in the combustor primary and intermediate zones.

Subroutine CALCBC is called by Subroutine ZMASS; it, in turn, calls Subroutine MINT. Subroutine CALCBC does not require external input and does not provide external output. Internal input and output are transmitted as arguments of the subroutine and through COMMON. The internal input consists of:

CUMDIS                      MSTARD                      ZP                      ZPD

The internal output consists of:

C

Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols in Subroutine CALCBC which are not included in COMMON.

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
C	$C_{XD}$	Mass flow coefficient	gm/sec
P1	$P_1$	Value of the cumulative normal distribution at $Z_p$	
P2	$P_2$	Value of the cumulative normal distribution at $-Z_p$	
ZPD	$Z_p$	Limit of integration of the cumulative normal distribution	

Analysis Procedure

The step-by-step procedure of Subroutine CALCBC is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. Using Subroutine MINT, calculate  $P_1$
2. Calculate  $P_2$  as :  
$$P_2 = 1 - P_1$$

3. Calculate  $C_{XD}$  as:

$$C_{XD} = m_D^* / (P_1 - P_2)$$

4. Return:

```
SUBROUTINE CALCBC(ZPD,C)
REAL MSTARD,MSTARU
COMMON/DATA1/AIR(50),RR(50),XX(50),FF(50),BCON1(50),BCON2(50),CH2(
150),ZP(70),CUMDIS(70),VP,RHO(50),BCON6(50),ATT(50),PPP,FNOXP,R1(50
2),R6(50),EK1(50),EK2(50),A2,A3,XL,CN,BETA,S,PHIP,EKS,XEID,A1
COMMON/OUT5/MSTARD,MSTARU
CALL MINT(1,ZPD,70,ZP,CUMDIS,P1)
P2 = 1.0-P1
C = MSTARD/(P1-P2)
RETURN
END
```

```
CAL*0000
CAL*0010
CAL*0020
CAL*0030
CAL*0040
CAL*0050
CAL*0060
CAL*0070
CAL*0080
CAL*0090
CAL*0100
```

## APPENDIX XI - SUBROUTINE CHECKK

The function of Subroutine CHECKK is to calculate the proportionality constant between the mass flow rate out of an element due to mixing and the total mass flowing into it. Subroutine CHECKK is called by Subroutine ZINTER; it does not call any other subroutines. Subroutine CHECKK does not require external input and does not provide external output. Internal input and output are transmitted as arguments of the subroutine and through COMMON. The internal input consists of:

A2	A3	CN	DELX	DMFUO
IMAX	MSTARU	SLOPE	UDM	XD
XL	XU			

The internal output consists of:

E	EKKD	RDOT
---	------	------

Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols in Subroutine CHECKK which are not included in COMMON.

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
DELX	$\delta x$	Integration interval	cm
DUMMYA	$\psi_i$	Dummy variable	cm <sup>-1</sup>
RDOTT	$\dot{R}_T$	Total rate of change of unburned fuel with axial position in the combustor	gm/sec-cm

Analysis Procedure

The step-by-step procedure of Subroutine CHECKK is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. Calculate  $K_D$  as:

$$K_D = C_N / X_L$$

2. Calculate  $\dot{R}_T$  as:

$$\dot{R}_T = (\dot{m}_{F_{U_0}})(A_3) \left[ \left( \frac{X_D}{X_L} \right)^{A_2} - \left( \frac{X_U}{X_L} \right)^{A_2} \right] / \delta x$$

3. For the element in question, calculate  $E_i$  and  $\dot{R}_i$  as:

$$E_i = K_D$$

$$\dot{R}_i = \dot{R}_T (S m_i)_0 / m_0^*$$

Step 4 is performed only if  $(S m_i)_0 = 0$

4. Go to step 7.

5. Calculate  $\psi_i$  as:

$$\psi_i = - \left[ \frac{\partial (S m_i)_0}{\partial x} - \dot{R}_i \right] / (S m_i)_0$$

Step 6 is performed only if  $\psi_i \geq K_D$

6. Calculate  $E_i$  as:

$$E_i = 1.1 Q_i$$

7. If this is the last element to be considered go to step 8.  
If not, return to step 3.
8. Return.

```

SUBROUTINE CHECKK(DELX)
REAL MSTARU
DIMENSION DUMMYA(50)
COMMON/DATA1/AIR(50),RR(50),XX(50),FF(50),BCON1(50),BCON2(50),CH2(
150),ZP(70),CUMDIS(70),VP,RHO(50),BCON6(50),ATT(50),PPP,FNOXP,R1(50)
2),R6(50),EK1(50),EK2(50),A2,A3,XL,CN,BETA,S,PHIP,EKS,XEND,A1
COMMON/OUT3/INDIC,NO(50),AVET,TAUBAR,RHOBAR,PHIBAR,IMAX,XD,
1FBARD,XU,LEN,TAUINT,TAUDIL,VELOC
COMMON/OUT4/CONGNO(50),DELM(50),AREAD,ASLOPE,DMFUO,SLOPE(50),TSLOCHK
1PE,NOP(50),EKKD,DMFT,UDM(50),DDM(50),F8(50),DMFUD,AIRD,DMFFEDCHK
2,RSUBX,SIG,SIGZER,AVEMW,DMDDA(50),DMDDM(50),DMDDP(50),DMDDPP(50),
3PRIME(50),NOEQXD,ANO,AQQ,DIFNO(50),NOZERO(50),RDOT(50),E(50)
COMMON/OUT5/MSTARD,MSTARU

C****
C**** CALCULATE K
C****
C**** EKKD=CN/XL
C****
C**** CHECK K VALUE
C****
      RDOTT = DMFUO*A3*(((XD/XL)**A2)-((XU/XL)**A2))/DELX
      DO 1000 I=1,IMAX
      E(I)=EKKD
      RDOT(I) = RDOTT*UDM(I)/MSTARU
      IF(UDM(I).EQ.0.0) GO TO 1000
      DUMMYA(I) = -(SLOPE(I)-RDOT(I))/UDM(I)
      IF(DUMMYA(I).GE.EKKD) E(I)=1.1*DUMMYA(I)
1000 CONTINUE
      RETURN
      END

```

```

CHK*0000
CHK*0010
CHK*0020
CHK*0030
CHK*0040
CHK*0050
CHK*0060
CHK*0070
CHK*0080
CHK*0090
CHK*0100
CHK*0110
CHK*0120
CHK*0130
CHK*0140
CHK*0150
CHK*0160
CHK*0170
CHK*0180
CHK*0190
CHK*0200
CHK*0210
CHK*0220
CHK*0230
CHK*0240
CHK*0250
CHK*0260
CHK*0270
CHK*0280
CHK*0290

```

## APPENDIX XII - SUBROUTINE RUNKUT

The function of Subroutine RUNKUT is to obtain the solution of a first-order ordinary differential equation by the Gill variation of the Runge-Kutta method.

Subroutine RUNKUT is called by Subroutine ZINTER and DILUTE; it, in turn, calls Subroutine DERIV. The subroutine does not require external input and does not provide external output. Internal input and output are transmitted as arguments of the subroutine. The internal input consists of:

DELX                    I                    LSGN                    Q                    XD  
Y

The internal output consists of:

Q                    XU                    Y

Fortran Nomenclature for Subroutine RUNKUT

The following table gives the Fortran nomenclature for those symbols used in Subroutine RUNKUT. Since the subroutine may be used with any consistent set of units, the units of the symbols are not specified. The subscript K, where it appears, is the index of the step in the Runge-Kutta solution.

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
A(K)	$a_i$	A set of constants used to determine DIFF	
B(K)	$b_i$	A set of constants used to determine DIFF	
C(K)	$c_i$	A set of constants used to determine Q	
D(K)	$d_i$	A set of constants used to determine X	
DELX	h	Increment in the independent variable across which the differential equation is to be solved	

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
DELY	$k_i$	Product of YPRIME and DELX at each stage of the solution	
DIFF	$\Delta Y$	The change in the value of the dependent variable at each stage of the solution	
I		Index of element	
K	i	Index of the stage of the solution	
LSGN		Indicator: LSGN=1 if intermediate zone and not the last step in the zone LSGN=2 if intermediate zone and the last step in the zone LSGN=3 if dilution zone or dilution zone type calculation	
Q	$q_i$	Quantity used to calculate DIFF at each stage of the solution; the value of Q in the final stage of the solution is a measure of the round-off error in Y	
X	$X_i$	Value of the independent variable at each stage of the solution	
Y	$Y_i$	Value of the dependent variable at each stage of the solution	
YPRIME	$f(X_i, X_i)$	Value of $dY/dX$ at each stage of the solution	

#### Analysis Procedure

The step-by-step procedure of Subroutine RUNKUT is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. Calculate the value of the independent variable at the given stage  $i$  of the solution as

$$X_i = X_{i-1} + (\Delta i)(h)$$

2. Using Subroutine DERIV, calculate the value of  $f(X_i, Y_i)$  at the given stage of the solution.

3. Calculate  $k_i$  at the given stage of the solution as:

$$k_i = [f(x_i, y_i)] [h]$$

4. Calculate the change in the dependent variable at the given stage of the solution as:

$$\Delta Y = a_i + (k_i - b_i)(g_i)$$

5. Calculate the value of the dependent variable at the given stage of the solution as:

$$Y_i = Y_{i-1} + \Delta Y$$

Step 6 is performed only if  $Y_i < 0$ . If  $Y_i \geq 0$  go to step 7.

6. Set  $Y_i = 0$ .

7. Calculate  $g_i$  as:

$$g_i = g_{i-1} + 3(\Delta Y) - (c_i)(k_i)$$

8. If this is the last stage of the solution, go to step 9.

If not, return to step 1.

9. Return .

		140	RUN*0000
SUBROUTINE RUNKUT(X,DELX,Y,Q,LSGN,I)			RUN*0010
DIMENSION A(4),B(4),C(4),D(4)			RUN*0020
DATA (A(I),I=1,4)/0.5,0.2928932,1.7071068,0.1666667/, (B(I),I=1,4)			RUN*0030
1/2,0,1,0,1,0,2,0/, (C(I),I=1,4)/0.5,0.2928932,1.7071068,0.5/,			RUN*0040
2(D(I),I=1,4)/0.0,0.5,0.0,0.5/			RUN*0050
C****			RUN*0060
C**** RUNKUT - SOLUTION OF A FIRST ORDER ORDINARY DIFFERENTIAL EQUATION			RUN*0070
C**** BY THE GILL VARIATION OF THE RUNGE-KUTTA METHOD			RUN*0080
C****			RUN*0090
DO 100 K=1,4			RUN*0100
X = X+D(K)*DELX			RUN*0110
CALL DERIV(X,Y,YPRIME,LSGN,I)			RUN*0120
DELY = YPRIME*DELX			RUN*0130
DIFF = A(K)*(DELY-B(K)*Q)			RUN*0140
Y = Y+DIFF			RUN*0150
IF(Y.LT.0.0) Y=0.0			RUN*0160
100 Q = Q+3.0*DIFF-C(K)*DELY			RUN*0170
RETURN			RUN*0180
END			

## APPENDIX XIII - SUBROUTINE DERIV

The function of Subroutine DERIV is to calculate the rate of formation of nitric oxide with respect to axial distance in the combustor intermediate or dilution zone.

Subroutine DERIV is called by Subroutine RUNKUT; it does not call any other subroutines. Subroutine DERIV does not require external input and does not provide external output. Internal input and output are transmitted as arguments of the subroutine and through COMMON. The internal input consists of:

AREAD	ASLOPE	CONGNO	DDM
DMDDP	E	EK1	EK2
FNOXP	I	LSGN	MSTARD
NO	NOEQXD	NOP	NOZERO
RDOT	R1	R6	SLOPE
UDM	XD	Y	

The internal output consists of:

DILL	REAT	YPRIME
------	------	--------

Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols in Subroutine DERIV which are not included in COMMON.

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
DFLAME	$(\dot{r})_{\text{Flame}}$	Rate of change of elemental NO concentration with axial position in the combustor intermediate zone due to formation of "prompt NO"	$\text{cm}^{-1}$
DMIXT	$(\dot{r}_{\text{mix}})_{\text{TOT}}$	Total rate of change of elemental NO concentration with axial position in the combustor intermediate zone due to mixing	$\text{cm}^{-1}$

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
DMIX1	$(\dot{r}_{mix})_1$	Rate of change of elemental NO concentration with axial position in the combustor intermediate zone due to mixing into the element	$\text{cm}^{-1}$
DMIX2	$(\dot{r}_{mix})_2$	Rate of change of elemental NO concentration with axial position in the combustor intermediate zone due to mass change mixing term	$\text{cm}^{-1}$
DMIX3	$(\dot{r}_{mix})_3$	Rate of change of elemental NO concentration with axial position in the combustor intermediate zone due to mixing out of the element	$\text{cm}^{-1}$
FNOXG	$[NO_0]$	NO formed in the flame front (mass fraction)	
I	i	Index of element	
LSGN		Indicator: LSGN=1 if intermediate zone and not the last step in the zone LSGN=2 if intermediate zone and the last step in the zone LSGN=3 if dilution zone or dilution zone type calculation	
RAT	$\left\{ \begin{array}{l} (x_D)_i \\ (x_D) \end{array} \right.$	Ratio of NO concentration to NO concentration at equilibrium for an element of mixture ratio F and pressure P at axial position $x_D$ ; ratio of NO concentration to NO concentration at equilibrium at axial position $x_D$	
X	$x_D$	Axial position (downstream) in the combustor	cm
Y	$\left\{ \begin{array}{l} [NO]_{x_D} \\ [NO]_{x_D} \end{array} \right.$	Nitric oxide concentration for an element of mixture ratio F and pressure P (mass fraction) at $x_D$ ; nitric oxide concentration at $x_D$	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
YPRIME	$\left\{ \begin{array}{l} \left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D} \\ \left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D} \end{array} \right.$	Rate of change of elemental NO concentration with axial position in the combustor intermediate zone; rate of change of NO concentration with axial position in the combustor dilution zone	$\text{cm}^{-1}$

### Analysis Procedure

The step-by-step procedure of Subroutine DERIV is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. Calculate  $[\text{NO}_e]$

Steps 2 through 5 are performed only in the dilution zone or for a dilution zone type calculation.

2. If  $[\text{NO}_e]_{x_D} = 0$ , then calculate  $\left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D}$  as:

$$\left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D} = 0$$

3. If  $[\text{NO}_e]_{x_D} = 0$ , go to step 18.

4. Calculate  $(\alpha_D)$  as:

$$(\alpha_D) = \frac{[\text{NO}]_{x_D}}{[\text{NO}_e]_{x_D}}$$

5. Go to step 9.

6. Calculate  $\left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D}$  as:

$$\left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D} = 0$$

Step 7 is performed only if  $[\text{NO}_e^*] = 0$  or if the chemical reaction rate is not significant.

7. Go to step 18.

8. Calculate  $(\alpha_D)_i$  as:

$$(\alpha_D)_i = \frac{[\text{NO}_i]}{[\text{NO}_e^*]_e}$$

9. Calculate  $(\dot{r})_{\text{react}}$ .

Steps 10 through 13 are performed in the intermediate zone except for the last step in the zone.

10. Calculate  $(\dot{r}_{\text{mix}})_1$ ,  $(\dot{r}_{\text{mix}})_2$ ,  $(\dot{r}_{\text{mix}})_3$  and  $(\dot{r})_{\text{flame}}$ .

11. Calculate  $(\dot{r}_{\text{mix}})_{\text{TOT}}$  as:

$$(\dot{r}_{\text{mix}})_{\text{TOT}} = (\dot{r}_{\text{mix}})_1 - (\dot{r}_{\text{mix}})_2 - (\dot{r}_{\text{mix}})_3 + (\dot{r})_{\text{flame}}$$

12. Calculate  $\left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D}$  as:

$$\left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D} = (\dot{r}_{\text{mix}})_{\text{TOT}} + (\dot{r})_{\text{react}}$$

13. Go to step 18.

Steps 14 and 15 are performed only for the last step in the intermediate zone.

14. Calculate  $\left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D}$  as:

$$\left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D} = (\dot{r})_{\text{react}}$$

15. Go to step 18.

Steps 16 and 17 are performed in the dilution zone or for a dilution zone type calculation.

16. Calculate  $(\dot{r})_{\text{DIL}}$

17. Calculate  $\left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D}$  as:

$$\left[ \frac{\partial [\text{NO}]}{\partial x} \right]_{x_D} = (\dot{r})_{\text{react}} + (\dot{r})_{\text{DIL}}$$

18. Return.

```

SUBROUTINE DERIV(X,Y,YPRIME,LSGN,I)
REAL MSTARD,MSTARU,NOP,NOEQXD,NO
COMMON/DATA1/AIR(50),RR(50),XX(50),FF(50),BCON1(50),BCON2(50),CH2(50),ZP(70),CUMDIS(70),VP,RHO(50),BCON6(50),ATT(50),FOP,FNOXP,R1(50),R6(50),EK1(50),EK2(50),A2,A3,XL,CN,BETA,S,PHIP,EKS,XEND,A1
COMMON/OUT3/INDIC,NO(50),AVET,TAUBAR,RHOBAR,PHIBAR,IMAX,XD,
1FBARD,XU,LEN,TAUINT,TAUDIL,VELOC
COMMON/OUT4/CONGNO(50),DELM(50),AREAD,ASLOPE,DMFUO,SLOPE(50),TSLODER
1PE,NOP(50),EKKD,DMFT,UDM(50),DDM(50),FB(50),DMFJD,AIRD,DMFFEDDER
2,RSUBX,SIG,SIGZER,AVEMW,DMDDA(50),DMDDM(50),DMDDP(50),DMDDPP(50),FDER
3PRIME(50),NOEQXD,ANO,AQQ,DIFNO(50),NOZERO(50),RDOT(50),E(50)
COMMON,OUT5/MSTARD,MSTARU
COMMON/OUT6/REAT,DILL
FNOXG = FNOXP*1.0E-06*(30.0/28.0)
IF(LSGN.NE.3) GO TO 500
IF(NOEQXD.EQ.0.0) YPRIME = 0.0
IF(NOEQXD.EQ.0.0) GO TO 4000
RAT = Y/NOEQXD
GO TO 750
500 CONTINUE
YPRIME=0.0
IF(CONGNO(I).EQ.0.0.OR.NOZERO(I).EQ.1) GO TO 4000
RAT = Y/CONGNO(I)
750 CONTINUE
YPRIME=((2.0*30.0)/(MSTARD/AREAD))*(1.0-RAT**RAT)*((R1(I)/(1.0+(RADER
1T*EK1(I))))+(R6(I)/(1.0+EK2(I))))
REAT = YPRIME
GO TO (1000,2000,3000),LSGN
1000 DMIX1=(DMDDP(I)+RDOT(I))*NOP(I)
DMIX2=E(I)*UDM(I)*NO(I)
DMIX3=SLOPE(I)*NO(I)
DFLAME = FNOXG*RDOT(I)
DMIXT = DMIX1-DMIX2-DMIX3+DFLAME
DMIXT=DMIXT/DDM(I)
YPRIME = DMIXT*REAT
GO TO 4000
2000 YPRIME = REAT
GO TO 4000
3000 DILL = -(Y/MSTARD)*ASLOPE
YPRIME=YPRIME+DILL
4000 RETURN
END

```

DER\*0000  
 DER\*0010  
 DER\*0020  
 DER\*0030  
 DER\*0040  
 DER\*0050  
 DER\*0060  
 DER\*0070  
 DER\*0080  
 DER\*0090  
 DER\*0100  
 DER\*0110  
 DER\*0120  
 DER\*0130  
 DER\*0140  
 DER\*0150  
 DER\*0160  
 DER\*0170  
 DER\*0180  
 DER\*0190  
 DER\*0200  
 DER\*0210  
 DER\*0220  
 DER\*0230  
 DER\*0240  
 DER\*0250  
 DER\*0260  
 DER\*0270  
 DER\*0280  
 DER\*0290  
 DER\*0300  
 DER\*0310  
 DER\*0320  
 DER\*0330  
 DER\*0340  
 DER\*0350  
 DER\*0360  
 DER\*0370  
 DER\*0380  
 DER\*0390  
 DER\*0400  
 DER\*0410

## APPENDIX XIV - SUBROUTINE ZMASS

The function of Subroutine ZMASS is to determine the mass flow in each element of the distribution function at a prescribed axial station in a gas turbine combustor. In addition, ZMASS calculates the mean mixture ratio, total mass flow, and the airflow rate at each of these axial stations.

Subroutine ZMASS is called by Subroutines PRIMARY, ZINTER, and DILUTE; it, in turn, calls Subroutines CALCBC and MINT. The subroutine does not require external input but does provide external output. Internal input and output are transmitted as arguments of the subroutine and through COMMON. The internal input consists of:

AIR	A1	A2	A3	BETA
CUMDIS	DDM	DELX	EKS	FF
INDIC	MSTARD	PHIP	PPP	RR
S	VP	XD	XL	XU
XX	ZP			

The internal output consists of:

AIRD	AREAD	ASLOPE	DDM	DELMD
DMFFED	DMFT	DMFUD	DMFUO	FB
FBARD	IMAX	MSTARD	MSTARU	NOZERO
SIG	SIGZER	SLOPE	TSLOPE	UDM

The external output consists of:

AFR	DDM	FEDF	FULOAD	IHIGHD
ILOWD				

#### Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols used in Subroutine ZMASS which are not included in COMMON.

<u>Fortran Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
A	A	Lower integration limit for the evaluation of the cumulative normal distribution integral	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
ADDM	$(\dot{G}_m)_A$	Dummy variable	gm/sec
AFR	A/F	Over-all air-to-fuel ratio	
AIRI	$(\dot{M}_A)_I$	Airflow rate at the primary zone exit	gm/sec
AIRU	$(\dot{M}_A)_{X_U}$	Airflow rate at the upstream axial integration limit of the combustor	gm/sec
S	B	Upper integration limit for the evaluation of the cumulative normal distribution integral	
C	$C_{X_D}$	Mass flow coefficient	gm/sec
DELX	$\Delta X$	Increment of the combustor length across which the solution is generated	cm
DUMMY	$(FB)_{DUM}$	Dummy variable	
FEDF	$(\dot{M}_f)_f$	Total mass of fuel fed into the combustor	lb/hr; lb/sec
FJLOAD	$\psi$	Fuel loading	lb/sec-ft <sup>3</sup> -atm <sup>2</sup>
I	i	Index of the element	
IHIGHD	$(I_{HIGH})_D$	Subscript of the mass element with the highest equivalence ratio (downstream end of integration interval)	
IHIGHU	$(I_{HIGH})_U$	Subscript of the mass element with the highest equivalence ratio (upstream end of integration interval)	
ILOWD	$(I_{LOW})_D$	Subscript of the mass element with the lowest equivalence ratio (downstream end of integration interval)	
ILOWU	$(I_{LOW})_U$	Subscript of the mass element with the lowest equivalence ratio (downstream end of integration interval)	
IN		Counter; indicates first mass element with zero mass at upper end of equivalence ratio distribu- tion function	
KKOUNT	$K_{KOUNT}$	Indicator KKOUNT = 0 if $FB(I) \leq 2\bar{F}$ for the element i KKOUNT = 1 if $FB(I) > 2\bar{F}$ for the element i	

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
KOUNT	$K_{COUNT}$	Indicator KOUNT = 0 if the element i has no mass KOUNT = 1 if the element i contains mass	
NN	$N_n$	Number of elements in the array	
NNN	$N_{nn}$	Number of last mixture ratio boundary	
NPRINT		Indicator NPRINT = 0 if intermediate output is not requested by the user NPRINT = 1 if intermediate output is requested by the user	
PI	$\pi$	Constant - equal to 3.14159265	
P1	$P_1$	Value of the normal distribution integral from $-\infty$ to A	
P2	$P_2$	Value of the cumulate normal distribution integral from $-\infty$ to B	
SDDM	$\sum \dot{M}_i$	Sum of the element mass flows	gm/sec
ZPD	$Z_{PXD}$	Limit of integration of the cumulative normal distribution	

#### Analysis Procedure

The step-by-step procedure of Subroutine ZMASS is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

Step 1 is performed only for the primary zone.

1. Calculate  $(I_{LOW})_D$  and  $(I_{HIGH})_D$  as:

$$(I_{LOW})_D = 0$$

$$(I_{HIGH})_D = 50$$

2. Calculate  $(I_{LOW})_U$  and  $(I_{HIGH})_U$  as:

$$(I_{LOW})_U = (I_{LOW})_D$$

$$(I_{HIGH})_U = (I_{HIGH})_D$$

3. Initialize  $N_n$

4. Calculate  $N_{nn}$  as:

$$N_{nn} = N_n + 1$$

5. Initialize  $\sum \dot{m}_i$  as:

$$\sum \dot{m}_i = 0$$

6. Using Subroutine MINT, calculate  $(\dot{m}_A)_I$   
 7. Using Subroutine MINT, calculate  $(\dot{m}_A)_{x_D}$   
 8. Using Subroutine MINT, calculate  $M_A|_{x_D}$   
 9. Using Subroutine MINT, calculate  $R_{x_D}$   
 10. Calculate  $A|_{x_D}$  as:

$$A|_{x_D} = \pi R_{x_D}^2$$

11. Calculate  $(\dot{m}_f)_{red}$  as:

$$(\dot{m}_f)_{red} = k_s * \bar{Q}_f * (\dot{m}_A)_I / \beta$$

Step 12 is only performed in the intermediate and dilution zones.

12. Calculate the fuel loading,  $\psi$  as:

$$\psi = (\dot{m}_f)_{red} * 12^3 * 2.54^3 / (454 * V_P * P^2)$$

Step 13 is performed only in the intermediate zone and if  $M_u^* = 0$ .

13. Write the fuel loading,  $\psi$ .

14. Calculate  $(\dot{m}_f)_o$  and  $(\dot{m}_f)_f$  as

$$(\dot{m}_f)_o = (\dot{m}_f)_f * (1 - R)$$

$$(\dot{m}_f)_f = (\dot{m}_f)_{red} * 454$$

15. Calculate the over-all air-to-fuel ratio  $A/F$  as:

$$A/F = M_A|_{x_{END}} / (\dot{m}_f)_{red}$$

16. Readjust the units on  $(\dot{m}_f)_f$  from lb/sec to lb/hr.

Step 17 is only performed for the primary zone.

17. Write  $(\dot{m}_f)_f$  and  $A/F$ .

Step 18 is performed only in the dilution zone.

18. Calculate  $(\dot{m}_{fu})_{x_D}$  as:

$$(\dot{m}_{fu})_{x_D} = 0$$

Step 19 is performed only in the primary and intermediate zones.

19. Calculate  $(\dot{m}_{fu})_{x_D}$  as:

$$(\dot{m}_{fu})_{x_D} = (\dot{m}_f)_o \left[ 1 - A_3 \left( \frac{x_D}{x_L} \right)^{A_2} \right]$$

20. Calculate  $(\dot{M}_f)_{x_D}$  as:

$$(\dot{M}_f)_{x_D} = (\dot{M}_f)_{\text{fed}} - (\dot{M}_{fU})_{x_D}$$

21. Calculate  $M_U^*$  as:

$$M_U^* = 0 \text{ in the primary zone}$$

$$M_U^* = M_D^* \text{ in the intermediate and dilution zones}$$

22. Calculate  $M_D^*$  as:

$$M_D^* = (\dot{M}_f)_{x_D} + M_A|_{x_D}$$

23. Calculate  $\bar{F}$  as:

$$\bar{F} = \frac{(\dot{M}_f)_{x_D}}{M_D^*}$$

Step 24 is only performed in the primary zone.

24. Calculate  $S_o$  as:

$$S_o = S_o^* \bar{F}$$

25. Calculate  $G$  as:

$$G = S_o \left[ 1 - \left( \frac{x_D}{x_L} \right)^{A_1} \right]$$

Steps 26 and 27 are performed only in the dilution zone:

26. Recalculate  $G$  as:

$$G = 0$$

27. Go to step 91.

Step 28 is performed only if  $S_o = 0$ .

28. Go to step 31.

29. Calculate  $Z_{P_{x_D}}$  as:

$$Z_{P_{x_D}} = \bar{F} / G$$

30. Using Subroutine CALCBC, calculate  $C_{x_D}$ .

Step 31 is performed only in the intermediate and dilution zones.

31. Go to step 36.

32. Calculate  $(F_B)_1$  as:

$$(F_B)_1 = 0.$$

Step 33 is performed for each boundary  $i$  satisfying the criteria

$$Z \leq i \leq N_n$$

33. Calculate  $(F_B)_i$  as:

$$(F_B)_i = \frac{1}{2} (F_i + F_{i-1})$$

34. Calculate  $(F_B)_{N_{nn}}$  as:

$$(F_B)_{N_{nn}} = 2 + \bar{F}_{N_n} - (F_B)_{N_{nn}}$$

35. Go to step 41.

Steps 36 and 37 are performed for each element  $i$  satisfying the criteria  $1 \leq i \leq i_{MAX}$ .

36. Calculate  $(S m_i)_U$  as:

$$(S m_i)_U = 0$$

in the primary zone

$$(S m_i)_U = (S m_i)_D$$

in the intermediate and dilution zones

37. Calculate  $(\Delta m_i)_D$  as:

$$(\Delta m_i)_D = 0$$

Step 38 is performed only if  $i_{MAX} = N_n$

38. Go to step 41.

Steps 39 and 40 are performed for each element  $i$  in the array satisfying the criteria  $(i_{MAX} + 1) \leq i \leq N_n$ .

39. Calculate  $(\Delta m_i)_D$  as:

$$(\Delta m_i)_D = 0$$

40. Calculate  $(S m_i)_U$  as:

$$(S m_i)_U = 0$$

41. Calculate  $i_{MAX}$  as:

$$i_{MAX} = 50$$

Step 42 is performed only for the special case that  $S_D = 0$  in the primary zone.

42. Go to step 44.

43. Go to step 49.

Steps 44 through 48 are performed for each element  $i$  in the array satisfying the criteria  $1 \leq i \leq i_{MAX}$ .

44. Calculate  $(S m_i)_D$  and  $(\Delta m_i)_D$  for the next element as:

$$(S m_i)_D = 0$$

$$(\Delta m_i)_D = 0$$

Step 45 is performed only if  $(F_B)_i < \bar{F}$ .

45. Go to step 44.

46. Recalculate  $i_{MAX}$  as:

$$i_{MAX} = i - 1$$

47. Calculate  $(S m_i)_D$  and  $(G m_i)_D$  as:

$$(S m_i)_D = M_D^*$$

$$(G m_i)_D = M_D^*$$

48. Go to step 92.

49. Initialize the indicators KCOUNT and KOUNT as

$$K_{COUNT} = 0$$

$$K_{KOUNT} = 0$$

Steps 50-85 are performed for each element  $i$  in the array satisfying the criteria  $2 \leq i \leq N_{nn}$ .

Steps 50 and 51 are performed only if the element  $i$  is equal to  $N_{nn}$ .

50. Calculate  $i_{MAX}$  as:

$$i_{MAX} = N_{nn} - 1$$

51. Go to step 75.

Step 52 is performed only if  $(F_B)_i \leq 2\bar{F}$

52. Go to step 54.

53. Calculate  $(F_B)_{DUM}$ ,  $(F_B)_i$ ,  $i_{MAX}$ , and  $K_{KOUNT}$  as:

$$(F_B)_{DUM} = (F_B)_i$$

$$(F_B)_i = 2\bar{F}$$

$$i_{MAX} = i - 1$$

$$K_{KOUNT} = 1$$

54. Calculate the distribution integration limits as:

$$A = [(F_B)_i - \bar{F}] / \sigma$$

$$B = [(F_B)_{i-1} - \bar{F}] / \sigma$$

Steps 55 and 56 are performed only if  $A \geq 0$ .

55. Using Subroutine MINT, calculate  $P_1$ , the value of the normal distribution integral from  $-\infty$  to  $A$ .

56. Go to step 60.

57. Calculate A as:

$$A = -A$$

58. Using Subroutine MINT, calculate the value of the normal distribution integral from  $-\infty$  to A.

59. Recalculate  $P_1$  as

$$P_1 = 1 - P_1$$

Steps 60 and 61 are performed only if  $B \neq 0$ .

60. Using Subroutine MINT, calculate  $P_2$ , the value of the normal distribution integral from  $-\infty$  to B.

61. Go to step 65.

62. Calculate B as:

$$B = 1 - B$$

63. Using Subroutine MINT, calculate  $P_2$ , the value of the normal distribution integral from  $-\infty$  to B.

64. Recalculate  $P_2$  as:

$$P_2 = 1 - P_2$$

65. Calculate  $(Sm_i)_D$  as:

$$(Sm_i)_D = C_{XD} * (P_1 - P_2)$$

Step 66 is performed only if  $(Sm_i)_D > 0$ .

66. Set  $(I_{LOW})_D$  equal to 1.

Step 67 is performed only if  $(I_{LOW})_D > 0$ .

67. Go to step 69.

Step 68 is performed only if  $(Sm_{i-2})_D = 0$  and  $(Sm_{i-1})_D > 0$ .

68. Set  $(I_{LOW})_D$  equal to  $i-1$ .

Step 69 is performed only if  $(Sm_{i-1})_D > 0$ .

69. Reset  $K_{COUNT}$  as:

$$K_{COUNT} = 1$$

Step 70 is performed only if  $(Sm_{i-1})_D = 0$  and if

$$K_{COUNT} = 1.$$

70. Go to step 77.

Step 71 is performed only if  $(i-1) = i_{MAX}$ .

71. Go to step 74.

72. Calculate  $\sum \delta m_L$  as:

$$\sum \delta m_L = \sum \delta m_L + (\delta m_{L-1})_D$$

73. Go to step 83.

74. Calculate  $(\delta m)_A$  as:

$$(\delta m)_A = (\delta m_{L-1})_D$$

75. Calculate  $(\delta m_{L-1})_D$ ,  $(\Delta m_{L-1})_D$ , and  $(I_{HIGH})_D$  as:

$$(\delta m_{L-1})_D = M_D^* - \sum \delta m_L$$

$$(\Delta m_{L-1})_D = (\delta m_{L-1})_D$$

$$(I_{HIGH})_D = L-1$$

76. Go to step 81.

77. Calculate  $(\delta m_{L-2})_D$ ,  $(\Delta m_{L-2})_D$  and  $(\Delta m_{L-1})_D$  as:

$$(\delta m_{L-2})_D = M_D^* - \sum \delta m_L + (\delta m_{L-2})_D$$

$$(\Delta m_{L-2})_D = (\delta m_{L-2})_D$$

$$(\Delta m_{L-1})_D = 0$$

78. Calculate  $(I_{HIGH})_D$  and  $L_{MAX}$  as:

$$(I_{HIGH})_D = L-2$$

$$L_{MAX} = L-2$$

Step 79 is performed only if  $K_{KOUNT} = 1$ .

79. Calculate  $(F_B)_{IMAX+2}$  as:

$$(F_B)_{IMAX+2} = (F_B)_{DOM}$$

80. Reset  $K_{KOUNT} = 0$ .

Step 81 is performed only if  $L_{MAX} > N_{nn}$ .

81. Go to step 85.

82. Go to step 86.

83. Calculate  $(\Delta m_{i-1})_D$  as:

$$(\Delta m_{i-1})_D = (S m_{i-1})_D$$

Step 84 is performed only if  $i_{MAX} < 50$ .

84. Go to step 86.

85. If this is the last element in the array, continue to step

86. If not, return to step 50 with  $i = i + 1$ .

Steps 86-87 are performed only if intermediate output is requested by the user.

Step 86 is performed for each element in the array satisfying the criteria  $1 \leq i \leq i_{MAX}$ .

86. Write  $(S m_i)_D$

87. Write  $(I_{LOW})_D$  and  $(I_{HIGH})_D$ .

Step 88 is performed if  $K_{COUNT} = 1$ .

88. Calculate  $(F_0)_{i_{MAX}+1}$  as:

$$(F_0)_{i_{MAX}+1} = (F_0)_{DUM}$$

Step 89 is performed only in the primary zone.

89. Go to step 92.

Step 90 is performed for each element in the array satisfying

the criteria  $1 \leq i \leq i_{MAX}$ .

90. Calculate  $\left[ \frac{\partial (S m_i)}{\partial x} \right]_{x_D}$  as:

$$\left[ \frac{\partial (S m_i)}{\partial x} \right]_{x_D} = \frac{(S m_i)_D - (S m_i)_U}{\Delta x}$$

91. Calculate  $\left[ \frac{\partial M_A}{\partial x} \right]_{x_D}$  and  $\left[ \frac{\partial M^*}{\partial x} \right]_{x_D}$  as:

$$\left[ \frac{\partial M_A}{\partial x} \right]_{x_D} = \frac{M_A|_{x_D} - (M_A)_{x_U}}{\Delta x}$$

$$\left[ \frac{\partial M^*}{\partial x} \right]_{x_D} = \frac{M_D^* - M_U^*}{\Delta x}$$

92. Return.

```

SUBROUTINE ZMASS(DELX)
REAL MSTARU,MSTARU
COMMON/DATA1/AIR(50),RR(50),XX(50),FF(50),BCON1(50),BCON2(50),CH2(
150),ZP(70),CUMDIS(70),VP,RHO(50),BCON6(50),ATT(50),PPP,FNOXP,R1(50
2),R6(50),EK1(50),EK2(50),A2,A3,XL,CN,BETA,S,PHIP,EKS,XEND,A1
COMMON/OUT3/INDIC,NO(50),AVET,TAUBAR,RHGBAR,PHIBAR,IMAX,XD,
1)FBARD,XU,LEN,TAUINT,TAUDIL,VELOC
COMMON/OUT4/CONGNO(50),DELM(50),AREAD,ASLOPE,DMFUO,SLOPE(50),TSLOZMA*0000
1)FE,NOP(50),EKKD,DMFT,UDM(50),DDM(50),FB(50),DMFUD,AIRD,DMFFEDZMA*0010
2,RSUBX,SIG,SIGZER,AVEM,DMDDA(50),DMDDM(50),DMDDP(50),DMDDPP(50),FZMA*0020
3PRIME(50),NOEQXD,ANO,AQQ,DIFNO(50),NOZERO(50),RDOT(50),E(50)ZMA*0030
COMMON/OUT5/MSTARU,MSTARU
DATA PI/3.14159265/ZMA*0040
C****ZMA*0050
C****ZMA*0060
C****ZMA*0070
C****ZMA*0080
C****ZMA*0090
C****ZMA*0100
C****ZMA*0110
C****ZMA*0120
C****ZMA*0130
C****ZMA*0140
C****ZMA*0150
C****ZMA*0160
C****ZMA*0170
C****ZMA*0180
C****ZMA*0190
C****ZMA*0200
C****ZMA*0210
C****ZMA*0220
C****ZMA*0230
C****ZMA*0240
C****ZMA*0250
C****ZMA*0260
C****ZMA*0270
C****ZMA*0280
C****ZMA*0290
C****ZMA*0300
C****ZMA*0310
C****ZMA*0320
C****ZMA*0330
C****ZMA*0340
C****ZMA*0350
C****ZMA*0360
C****ZMA*0370
C****ZMA*0380
C****ZMA*0390
C****ZMA*0400
C****ZMA*0410
C****ZMA*0420
C****ZMA*0430
C****ZMA*0440
C****ZMA*0450
C****ZMA*0460
C****ZMA*0470
C****ZMA*0480
C****ZMA*0490
C****ZMA*0500
C****ZMA*0510
C****ZMA*0520
C****ZMA*0530
C****ZMA*0540
C****ZMA*0550
C****ZMA*0560
C****ZMA*0570
C****ZMA*0580
C****ZMA*0590

```

```

      ZPD = FBARD/SIG
      CALL CALCBC(ZPD,C)
C****
C**** CALCULATE BOUNDARIES AT WHICH EACH F VALUE APPLIES
C****
      500 CONTINUE
          IF(INDIC.NE.1) GO TO 1500
          FB(1) = 0.0
          DO 1000 I=2,NN
      1000 FB(I) = 0.5*(FF(I)+FF(I-1))
          FB(NN)=2.0*FF(NN)-FB(NN)
          GO TO 3000
C****
C**** STORE MASS FLOWS AT PREVIOUS STATION
C****
      1500 CONTINUE
          DO 2000 I =1,IMAX
          IF(INDIC.EQ.1) UDM(I) = 0.0
          IF(INDIC.NE.1) UDM(I) = DDM(I)
          DELMD(I)=0.0
      2000 CONTINUE
          IF(IMAX.EQ.NN) GO TO 2200
          IN=IMAX+1
          DO 2100 I=IN,NN
          DELMD(I)=0.0
      2100 UDM(I) = 0.0
      2200 CONTINUE
C****
C**** CALCULATE IMAX
C****
      3000 CONTINUE
          IMAX=50
C****
C**** SPECIAL CASE S=0.0 IN PRIMARY ZONE
C****
          IF(S.EQ.0.0.AND.INDIC.EQ.1) GO TO 2300
          GO TO 2500
      2300 DO 2400 I=1,IMAX
          DDM(I)=0.0
          DELMD(I)=0.0
          NOZERO(I)=1
          IF(FB(I).LT.FBARD) GO TO 2400
          IMAX=I-1
          DDM(I-1)=MSTARD
          DELMD(I-1)=MSTARD
          NOZERO(I-1)=0
          GO TO 9000
      2400 CONTINUE
      2500 CONTINUE
          KOUNT=0
          KKOUNT=0
          DO 5000 I =2,NNN
          IF(I.EQ.NNN) IMAX=NNN-1
          IF(I.EQ.NNN) GO TO 4880
          IF(FB(I).LT.(2.0*FBARD)) GO TO 4000
          DUMMY = FB(I)
          FB(I) = 2.0*FBARD
          IMAX = I-1
          KKOUNT=1
      4000 CONTINUE

```

```

ZMA*0600
ZMA*0610
ZMA*0620
ZMA*0630
ZMA*0640
ZMA*0650
ZMA*0660
ZMA*0670
ZMA*0680
ZMA*0690
ZMA*0700
ZMA*0710
ZMA*0720
ZMA*0730
ZMA*0740
ZMA*0750
ZMA*0760
ZMA*0770
ZMA*0780
ZMA*0790
ZMA*0800
ZMA*0810
ZMA*0820
ZMA*0830
ZMA*0840
ZMA*0850
ZMA*0860
ZMA*0870
ZMA*0880
ZMA*0890
ZMA*0900
ZMA*0910
ZMA*0920
ZMA*0930
ZMA*0940
ZMA*0950
ZMA*0960
ZMA*0970
ZMA*0980
ZMA*0990
ZMA*1000
ZMA*1010
ZMA*1020
ZMA*1030
ZMA*1040
ZMA*1050
ZMA*1060
ZMA*1070
ZMA*1080
ZMA*1090
ZMA*1100
ZMA*1110
ZMA*1120
ZMA*1130
ZMA*1140
ZMA*1150
ZMA*1160
ZMA*1170
ZMA*1180
ZMA*1190

```

```

C****
C**** CALCULATE THE ELEMENT MASSES
C****
      A = (FB(I)-FBARD)/SIG
      B = (FB(I-1)-FBARD)/SIG
      IF(A.GE.0.0) CALL MINT(1,A,70,ZP,CUMDIS,P1)
      IF(A.GE.0.0) GO TO 4500
      A = -A
      CALL MINT(1,A,70,ZP,CUMDIS,P1)
      P1 = 1.0-P1
4500  IF(B.GE.0.0) CALL MINT(1,B,70,ZP,CUMDIS,P2)
      IF(B.GE.0.0) GO TO 4800
      B = -B
      CALL MINT(1,B,70,ZP,CUMDIS,P2)
      P2 = 1.0-P2
4800  DDM(I-1) = C*(P1-P2)
      IF(DDM(I).GT.0.0) ILOWD=1
      IF(ILOWD.GT.0) GO TO 4850
      IF(DDM(I-2).EQ.0.0.AND.DDM(I-1).GT.0.0) ILOWD=I-1
4850  IF(DDM(I-1).GT.0.0) KOUNT=1
      IF(DDM(I-1).EQ.0.0.AND.KOUNT.EQ.1) GO TO 4900
      IF((I-1).EQ.IMAX) GO TO 4875
      SDDM=SDDM+DDM(I-1)
      GO TO 4950
4875  ADDM=DDM(I-1)
4880  DDM(I-1)=MSTARD-SDDM
      DELMD(I-1)=DDM(I-1)
      IHIGHD=I-1
      GO TO 4925
4900  DDM(I-2)=MSTARD-SDDM+DDM(I-2)
      DELMD(I-2) = DDM(I-2)
      DELMD(I-1)=0.0
      IHIGHD=I-2
      IMAX=I-2
      IF(KKOUNT.EQ.1) FB(IMAX+2)=DUMMY
      KKOUNT=0
4925  CONTINUE
      IF(IMAX.GT.NNN) GO TO 5000
      GO TO 6000
4950  DELMD(I-1)=DDM(I-1)
      IF(IMAX.LT.50) GO TO 6000
5000  CONTINUE
6000  CONTINUE
      IF(NPRINT.EQ.1) WRITE(6,9999) (DDM(I),I=1,IMAX)
      IF(NPRINT.EQ.1) WRITE(6,9998) ILOWD,IHIGHD
      IF(KKOUNT.EQ.1) FB(IMAX+1)=DUMMY

C****
C**** CALCULATE SLOPES
C****
      IF(INDIC.EQ.1) GO TO 9000
      DO 7000 I =1,IMAX
      SLOPE(I) = (DDM(I)-UDM(I))/DELX
7000  CONTINUE
8000  CONTINUE
      ASLOPE = (AIRD-AIRU)/DELX
      TSLOPE = (MSTARD-MSTARU)/DELX
9100  FORMAT(//////,10X,58HTHE COMPUTED TOTAL MASS OF FUEL FED INTO THE C
10MBUSI
OR IS ,E12.5,8H LB./HR.//)
9150  FORMAT(10X,42HTHE COMPUTED OVERALL AIR-TO-FUEL RATIO IS ,E12.5,///
1)

```

```

ZMA*1200
ZMA*1210
ZMA*1220
ZMA*1230
ZMA*1240
ZMA*1250
ZMA*1260
ZMA*1270
ZMA*1280
ZMA*1290
ZMA*1300
ZMA*1310
ZMA*1320
ZMA*1330
ZMA*1340
ZMA*1350
ZMA*1360
ZMA*1370
ZMA*1380
ZMA*1390
ZMA*1400
ZMA*1410
ZMA*1420
ZMA*1430
ZMA*1440
ZMA*1450
ZMA*1460
ZMA*1470
ZMA*1480
ZMA*1490
ZMA*1500
ZMA*1510
ZMA*1520
ZMA*1530
ZMA*1540
ZMA*1550
ZMA*1560
ZMA*1570
ZMA*1580
ZMA*1590
ZMA*1600
ZMA*1610
ZMA*1620
ZMA*1630
ZMA*1640
ZMA*1650
ZMA*1660
ZMA*1670
ZMA*1680
ZMA*1690
ZMA*1700
ZMA*1710
ZMA*1720
ZMA*1730
ZMA*1740
ZMA*1750
ZMA*1760
ZMA*1770
ZMA*1780
ZMA*1790

```

159

9998 FORMAT(5X,20I5//)  
9999 FORMAT(10X,10E10.3/ )  
9000 RETURN  
END

ZMA\*1800  
ZMA\*1810  
ZMA\*1820  
ZMA\*1830

## APPENDIX XV - SUBROUTINE PRINTS

The function of Subroutine PRINTS is to provide the written output of the calculated results of the program.

Subroutine PRINTS is called by Subroutines PRIMARY, ZINTER, and DILUTE; it does not call any other subroutine. Subroutine PRINTS does not require external input and does provide external output. Internal input is transmitted through COMMON. There is no internal output. The internal input consists of:

AVCH2D	AVCH2F	AVCH2P	AVECOD	AVECOF
AVECOP	AVECSD	AVECSF	AVECSP	AVENOD
AVENOF	AVENOP	AVET	INDIC	PHIBAR
RHOBAR	TAUBAR	XD		

Additional Fortran Nomenclature

The following table gives the Fortran nomenclature for those symbols in Subroutine PRINTS which are not included in COMMON.

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AVCH2	$[\overline{\text{CH}_2}^*]$	Equilibrium concentration of unburned hydrocarbons exclusive of $\text{C}_{(s)}$ and CO at $X_D$ .	lb/ft <sup>3</sup>
AVECO	$[\overline{\text{CO}}^*]$	Equilibrium concentration of CO at $X_D$	lb/ft <sup>3</sup>
AVECS	$[\overline{\text{C}_s}^*]$	Equilibrium concentration of $\text{C}_{(s)}$ at $X_D$	lb/ft <sup>3</sup>
AVENO	$[\overline{\text{NO}}^*]$	Concentration of NO at $X_D$	lb/ft <sup>3</sup>
AVENO <sub>2</sub>	$[\overline{\text{NO}_2}]$	Equivalent concentration of NO <sub>2</sub> at $X_D$	lb/1000 lb fuel burned
AVETF	T	Temperature at $X_D$	deg F
DENOM		Constant	$\frac{\text{ft}^3 - \text{gm}}{\text{cm}^3 - \text{lb}}$
IPRINT		Indicator IPRINT = 0 if intermediate zone heading is to printed IPRINT = 1	-

<u>Fortran</u> <u>Symbol</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
		if intermediate zone heading is not to be printed IPRINT = 2 if dilution zone heading is not to be printed	
RHOBA	$\bar{\rho}$	Mean density of combustion products at $X_D$	lb/ft <sup>3</sup>
TTUBAR	$\bar{\tau}$	Mean residence time at $X_D$	msecs
XOUT	$X_D$	Axial position downstream in the combustor	in

### Analysis Procedure

The step-by-step procedure of Subroutine PRINTS is given below. The Fortran listing of the subroutine is presented at the conclusion of the step-by-step procedure.

1. Convert  $X_D$  from cm to in.
2. Convert  $\bar{\tau}$  from secs to msecs.
3. Convert NO, CO,  $C(s)$ , and CH<sub>2</sub> concentrations from gm/cc to lb/ft<sup>3</sup>.
4. Convert NO concentration at  $X_D$  to the equivalent NO<sub>2</sub> concentration.
5. Convert  $\bar{\rho}$  from gm/cc to lb/ft<sup>3</sup>.
6. Convert  $T$  from deg K to deg F.
7. If this is the primary zone, write the primary zone heading and output. Go to step 12. If it is not the primary zone, go to step 8.
8. If this is the intermediate zone and the first written output for the zone, write the heading for the intermediate zone. If not, go to step 9.
9. If this is the intermediate zone, write the output at  $X_D$ . Go to step 12. If it is not the intermediate zone, go to step 10.
10. If this is the dilution zone and the first written output in the zone, write the heading for the dilution zone. If not, go to step 11.

11. If this is the dilution zone, write the output for the dilution zone at  $X_D$ . Go to step 12.
12. Return.

```

SUBROUTINE PRINTS
REAL NO
COMMON/OUT1/AVECSG,AVECOG,AVCH2G,AVECSP,AVECOP,AVCH2P,AVECSD,AVECOPRT*0000
10,AVCH2D,AVECSF,AVECOF,AVCH2F PRT*0010
COMMON/OUT2/AVENOG,AVENOD,AVENOP,AVENOF,AVENFU,RRO,ILAST PRT*0020
COMMON/OUT3/INDIC,NO(50),AVET,TAUBAR,RHOBAR,PHIBAR,IMAX,XD, PRT*0030
1FBARD,XU,LEN,TAUINT,TAJDIL,VELOC PRT*0040
COMMON/OUT4/CONGNO(50),DELM(50),AREAD,ASLOPE,DMFUO,SLOPE(50),TSLOPRT*0050
1PE,NOP(50),EKKD,DMFT,UDM(50),DDM(50),FB(50),DMFUD,AIRD,DMFFEDPRT*0060
2,RSUBX,SIG,SIGZER,AVEMW,DMDDA(50),DMDDM(50),DMDDP(50),DMDDPP(50),FPRT*0070
3PRIME(50),NOEQXD,ANO,AQQ,DIFNO(50),NOZERO(50),RDOT(50),E(50) PRT*0080
NPRINT=0 PRT*0090
IF(INDIC.EQ.1) IPRINT=0 PRT*0100
XOUT=XD/2.54 PRT*0110
TTUBAR = TAUBAR*1000. PRT*0120
DENOM=454.0*3.532E-05 PRT*0130
AVEN0=AVENOD/DENOM PRT*0140
AVEC0=AVECOD/DENOM PRT*0150
AVECS=AVECSD/LENOM PRT*0160
AVCH2=AVCH2D/DENOM PRT*0170
AVEN02 = AVENOF*46.0/30.0 PRT*0180
RH0BA=RHOBAR/DENOM PRT*0190
AVETF=((AVET-273.16)*1.8)+32.0 PRT*0200
GO TO (1000,2000,3000),INDIC PRT*0210
1000 CONTINUE PRT*0220
WRITE(6,1010) PRT*0230
1010 FORMAT(1H1) PRT*0240
WRITE(6,1020) PRT*0250
1020 FORMAT(48H THIS IS THE MAIN PRINTOUT FOR THE PRIMARY ZONE //) PRT*0260
GO TO 4000 PRT*0270
2000 IF(IPRINT.EQ.1) GO TO 5500 PRT*0280
WRITE(6,1010) PRT*0290
WRITE(6,2020) PRT*0300
2020 FORMAT(53H THIS IS THE MAIN PRINTOUT FOR THE INTERMEDIATE ZONE PRT*0310
1//) PRT*0320
IPRINT=1 PRT*0330
GO TO 4000 PRT*0340
3000 IF(IPRINT.EQ.2) GO TO 5500 PRT*0350
WRITE(6,1010) PRT*0360
WRITE(6,3020) PRT*0370
3020 FORMAT(49H THIS IS THE MAIN PRINTOUT FOR THE DILUTION ZONE //) PRT*0380
IPRINT=2 PRT*0390
4000 WRITE(6,5000) PRT*0400
5000 FORMAT(1X,6HX(IN.),1X,3HPhi,3X,1HT,6X,3HRHO,3X,3HTAU,6X,2HNO,9X,3HPRT*0410
1ND2,9X,4HC(S),6X,4HC(S),8X,2HCO,9X,2HCO,8X,3HCH2,8X,3HCH2) PRT*0420
WRITE(6,5100) PRT*0430
5100 FORMAT(8X,4HAVE.,1X,5HDEG F,3X,4HAVE.,2X,4HAVE.,5X,3HPPM,6X,7HLBS PRT*0440
1PER,7X,3HPPM,5X,7HLBS PER,7X,3HPPM,5X,7HLBS PER,6X,3HPPM,7X,7HLBS PRT*0450
2 PER) PRT*0460
WRITE(6,5200) PRT*0470
5200 FORMAT(19X,7HLB/CUFT,1X,4H4SEC,4X,5H(VOL),5X,7H1000 LB,6X,5H(VOL), PRT*0480
14X,7H1000 LB,6X,5H(VOL),4X,7H1000 LB,5X,5H(VOL),4X,7H1000 LB) PRT*0490
WRITE(6,5300) PRT*0500
5300 FORMAT(43X,11HFUEL BURNED,11X,11HFUEL BURNED,11X,11HFUEL BURNED,11 PRT*0510
1X,11HFUEL BURNED) PRT*0520
5500 WRITE(6,6000)XOUT,PHIBAR,AVETF,RH0BA,TTUBAR,AVENOP,AVEN02,AVECSP, PRT*0530
1AVECSF,AVECOP,AVECOF,AVCH2P,AVCH2F PRT*0540
6000 FORMAT(1X,F5.2,1X,F4.2,1X,F5.0,1X,F6.4,1X,F6.2,1X,8(E10.3,1X)//) PRT*0550
IF(NPRINT.EQ.1) WRITE(6,9999)(NO(I),I=1,IMAX) PRT*0560
9999 FORMAT(10X,4H **,8E12.4) PRT*0570

```

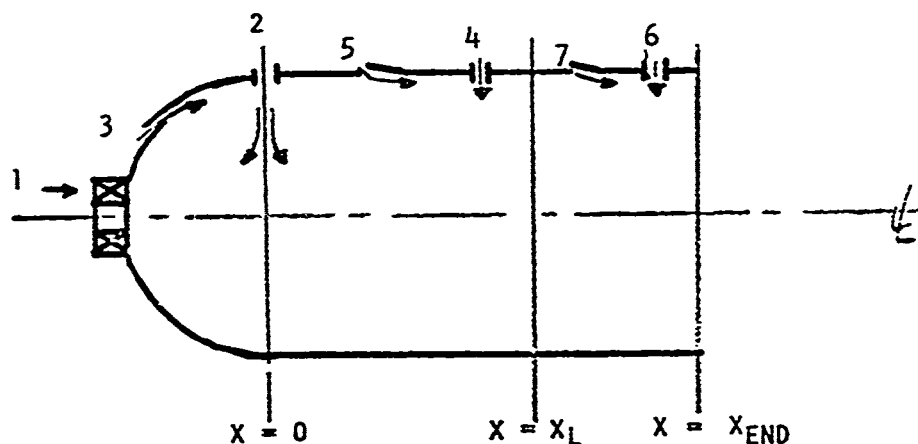
164

PRT\*0600  
PRT\*0610

RETURN  
END

## APPENDIX XVI - METHOD OF CALCULATION OF AIR DISTRIBUTION CHARACTERISTICS

Air enters the combustor liner at discrete positions over the whole length of the liner. The bulk of such flow normally enters perpendicular to the direction of the mainstream product flow and has then to be deflected and entrained before it can mix with the combustion products. This action requires a finite time (i.e., distance) to occur, and its effect upon the nitric oxide formation process has to be considered. A method has been developed, therefore, to take account of this effect. The method is consistent with the mixing assumptions made in the flow model described in this report; it has been applied to all combustors considered in this report and is described below.



The flow behavior at each port shown in the figure above is assumed to behave as follows:

- Port 1 All air entering at this position is assumed to mix with the products in the primary zone.
- Port 2 Some fraction of the air,  $f$ , mixes with the primary zone and the remainder is entrained according to the law described for port 4.

Port 3 Cooling air mixes according to the relationship

$$M_X = M_3 \left( \frac{\text{Distance from port 3 to } X}{\text{Distance from port 3 to } X_L} \right)^{0.5}$$

and that part which mixes before the primary zone exit ( $X = 0$ ), is assumed to burn in the primary zone.

Port 4

and 5 Both cooling and combustion air mix according to the relationship shown above,

$$\text{i.e., } M_X = M_4 \left( \frac{(X - X_L)}{(X_L - X_4)} \right)^{0.5}$$

Port 6

and 7 This air enters the dilution zone so it is assumed that instantaneous mixing occurs (see Section 2.5).

All these independent mass flows are then summed at a particular position along the combustor to give the total airflow contained with the combustion products at that point. For example:

air burning in the primary zone  $M_{pz}$  is given by,

$$M_{pz} = M_0 = M_1 + f M_2 + M_{3x=0}$$

air at position  $X$  ( $0 < X < X_L$ )

$$M_X = (1-f) M_2 + M_{3x} + M_{4x} + M_{5x} + M_{pz}$$

air at position  $X$ , ( $X_7 < X < X_6$ )

$$M_X = \sum_i M_i + M_7$$

This method was applied to combustors A and B studied in this report and in each case the value of  $f$ , the fraction of air entering the primary zone from the first row of air ports, was assumed to equal one third. For Combustor A this value corresponded to the value recommended by the designers, but in the case of Combustor B, the value was estimated based on the design features. Errors in the predictions of nitric oxide emission levels from this latter estimate can be expected to be negligible as the total airflow through port 2 represents less than two per cent of the total airflow.