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POLLUTANT PRODUCTION IN A SIMULATED TURBOJET AFTERBURNER

Part II. COMPUTER PROGRAM FOR CALCULATION OF POLLUTANT HISTORY IN AFTERBURNING TURBOJET ENGINES

L. W. Crawford, A. A. Mason, J. M. Lents, et al.
The University of Tennessee Space Institute

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PART II: COMPUTER PROGRAM FOR CALCULATION OF
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FOREWORD

This research program was initiated 1 November 1970 under USAF Contract F33615-71-C-1125. The work was performed between 1 November 1970 and 31 July 1971 by The University of Tennessee Space Institute, Tullahoma, Tennessee, and administered by the Air Force Aero Propulsion Laboratory, Wright-Patterson Air Force Base, Ohio, Mr. Kenneth N. Hopkins (AFAPL/TBC), Project Engineer. The contract was initiated under Project 3056, "Gas Turbine Technology," Task 306605 "Combustion Systems Performance and Stability."

Scientific and engineering personnel of the Space Institute, identified as "et al." on the cover, who engaged in the experimental work and preparation of this report, are:

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The authors wish to express sincere appreciation to Mr. R. Kamm, Special Assistant to Dr. Goethert, for his active cooperation in the project; to Mr. R. Nygaard, Engineer, and to Mr. J. Goodman, Mr. J. Boazman, and Mr. J. Rothert, Technicians, for their cooperation and assistance in the Combustion Laboratory; to the personnel at ESF and CCO of ARO, Inc., especially Mr. J. McCabe and Mr. W. Armstrong, for their cooperation.

This report was submitted by the authors in August, 1971.

This report is bound in two parts. Part I contains technical details of the report. Part II consists of a User's Manual for the computer program developed for calculating pollutant production in a turbojet afterburner.

The program has been operated on the IBM 370/155 using FORTRAN IV G Level 18. To keep within B partition it was necessary to overlay INIT with INTEG, SETUP, SETYP, SETHP, GAUSS. All pages of this manual are effective 31 July 1971.

Publication of this report does not constitute Air Force approval of the report's findings or conclusions. It is published only for the exchange and stimulation of ideas.


ERNEST C. SIMPSON
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ABSTRACT

An experimental and theoretical study has been made of the history of the pollutants carbon monoxide (CO), unburned hydrocarbons (HC) and nitrogen oxides (NO_x) in a turbojet afterburner. Experimental traverses at several axial stations were performed in a simulated afterburner in which exhaust from a J-47 combustor can, operated at medium power, was mixed with fuel spray. Experiments were carried out both in a non-bypass and in a bypass configuration (secondary air was mixed with primary exhaust). The non-bypass tests were carried out at high combustor efficiency, and yielded the following: CO = 300 ppm, HC less than 10 ppm, NO_x = 100 ppm. In the bypass tests, fuel distribution was nonuniform and combustor efficiency was low. The concentrations obtained were CO = 10,000 ppm, HC = 1000 ppm, NO_x = 100 ppm. The theoretical analysis consisted of a computer program for reacting flow with turbulent mixing. The computer program was very slow and therefore of limited usefulness in terms of cost and questionable results, since it could not be checked against experiment. Infrared measurements of NO in the combustion tunnel were attempted. Indications were obtained of NO at the 5.3 micron band, but quantitative measurements were not obtained.

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GLOSSARY

R	Radial position - inches
T	Temperature - °K
S	Temperature - °R
U	Velocity - ft/sec
Y	Species mass fractions
ROU	Mass flux - lb/(sec sq. ft.)
PSI	Stream function $\sqrt{(\text{lb}/\text{sec})}$
UPR	Velocity at previous location - ft/sec
YPR	Species mass fraction at previous location
HST	Static enthalpy Btu/lb
HT	Total enthalpy Btu/lb
TPR	Temperature at previous location °R
HTPR	Total enthalpy at previous location Btu/lb
CM	Molecular weight (average)
X	Mole fraction
H	Species chemical enthalpy Btu/lb mole
W	Species production rate lb/lb
E	Species production per lb/lb ft
YO	Initial fuel mass fraction
TO	Time since start of burning
TAU	Burning time
ISP	Number of species
IRE	Number of reactions
IMU	IMU.5 = Number of 3 body reactions
UM	Turbulent viscosity lb/ft sec

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SECTION I

INTRODUCTION

This users manual was prepared under contract number F33615-71-C-1125, and represents Item Number 0001 Sequence Number A002 under requirements of that contract. The purpose of writing the computer program was to provide the Air Force with a means of estimating air pollution concentrations in the exhaust gases from afterburning turbojet engines.

SECTION II

COMPUTER PROGRAM SYSTEM CAPABILITIES

2.1 PURPOSE

The purpose of this computer program is to solve the partial differential equations of change for momentum, species, and enthalpy, to obtain radial and axial profiles of velocity, temperature, and species concentrations in a turbulent reacting fluid. A finite difference approximation to the equations is made.

The chemical species considered and chemical reactions involved are those pertinent to burning of a liquid hydrocarbon fuel in a hot exhaust gas from a primary combustor. By controlling the input a calculation of the mixing and combustion in a bypass type engine may also be made. While the primary purpose of the research has been to estimate levels of the pollutants NO, CO, and unburned hydrocarbons, in exhaust gases, the levels of several other species must be taken into account in order to calculate pollutant levels.

2.2 GENERAL DESCRIPTION OF THE SYSTEM

A FORTRAN program has been written to achieve the purpose described above. The differential equations, transformed from (length, radius), to (length, stream function) coordinates, have been approximated by finite difference equations.

Initially, certain thermodynamic data for the chemical species are read, followed by data necessary to calculate chemical reaction rates. Then, initial data of temperature, velocity, and species concentrations as a function of radial position in an axisymmetric flow are read in. The program does not read any more data.

From the initial profiles as a function of radius, a conversion to the stream function variable is made, with appropriate interpolation.

An iteration scheme is used to solve for dependent variables (velocity, enthalpy, species concentration) as a function of axial distance. The program proceeds stepwise from the initial condition, until a maximum axial distance is reached. The outer boundary condition is an inviscid reacting flow. When the flow variables at the stream function location adjacent to the inviscid flow deviate from the inviscid flow by 1 part in 10^4 , the viscous flow region is expanded by one step in stream function. The number of stream function

steps is allowed to increase to 50, if necessary. If more expansion is needed, the stream function step size is doubled, and number of steps is halved. This process repeats itself as necessary.

2.3 FUNCTIONS PERFORMED

There are 13 subdivisions of the program.

1. MAIN Program
2. Subroutine SPECIE (KK1, KK2, NU)
3. Subroutine THERMO (KRIS, JA, IT)
4. Subroutine INIT
5. Subroutine TRANSP (NLOW, NHIGH)
6. Subroutine INTEG (NLOW, NHIGH, IN)
7. Subroutine SETUP (RUP)
8. Subroutine SETYP (RUP)
9. Subroutine SETHP (RUP)
10. Subroutine GAUSS
11. Subroutine CHANGE (RUP)
12. Subroutine PRINT (KUSK, KUN)
13. Subroutine CHEMIE (KRYS, KRAS, IJ)

The MAIN program controls the flow of information, causing THERMO, CHEMIE, and INIT to read in initial data. It then proceeds with the computation and prints out results at every 50th axial station, until stopped by either reaching the maximum desired axial distance (ZMAX feet) or exceeding the time limitation.

2.4 FUNCTION DESCRIPTIONS

2.4.1 Main Program

Summary of Operations performed by MAIN

The main program first sets certain parameters, namely ISP = 14, IRE = 17, IMU = 11, which are in labelled common ZZZ. There are, respectively, the number of species, the number of reactions, and the number of the last reaction which involves three bodies (see₃ CHEMIE). In addition, the variable TAU is set equal to $.4 \times 10^{-3}$, which is the hydrocarbon burning time in seconds. TAU is in labeled common XXX. Certain other parameters are also set, so as to cause THERMO to read thermodynamic data, and CHEMIE to read chemical reaction rate data. The main program then calls upon INIT to read in velocity, temperature, and species concentrations as a function of radius. The first item actually read is NNN, which defines the number of radial locations considered. INIT converts the indepen-

dent variable from radius to stream function, and interpolates to obtain initial dependent variables, velocity, temperature, and species concentrations, at equal intervals of stream function. The stream function interval is denoted by DPSI. DELX is the interval in feet, and is defined to be .00001. $RUP = DELX/DPSI^{**2}$ is defined. XMAX = 0.7 (feet) is defined as the maximum axial distance to be considered.

The main program calls upon SPECIE to calculate mole fractions, molecular weights, and mass fluxes at all radial locations, and calls upon THERMO to calculate static enthalpies of the species. Total enthalpies are calculated. The TRANSP subprogram is called upon to calculate a turbulent viscosity, and INTEG to calculate radius as a function of stream function, and also to calculate certain coefficients (AP, APR) needed for subsequent finite difference calculations.

The main program writes the data on initial profiles as a function of stream function. It then proceeds in a stepwise fashion to calculate the flow variables as a function of axial location.

After the writing of the initial data, there is very little necessity or possibility for operator or programmer intervention in the main program. The number of radial locations, NNN, is a major variable which is controlled initially and internally. The variables IK and IA define the locations of the inner and outer bounds of the viscous flow region. In the present application, the inner bound is taken to be the center-line. The outer bound is always $IA = NNN - 1$. Species calculations run from 1 to ISP, which is defined previously.

A variable KUSK defines the number of iterations which have been performed at an axial location. The iterations stop after $KUSK = 3$. Prior to the start of calculations, the axial position, Z, is incremented. IA is checked to see if the maximum number of streamlines permitted has been reached. If $IA = NILS - 1$, a doubling of stream function step size is incurred, together with a reduction of the number of steps considered. This is done through the subroutine CHANGE. In the present program, $NILS = 51$ is defined as data. NILS must be odd. The resulting profiles are written after CHANGE.

Whether or not a change occurs, the boundary values at NNN are calculated at the incremented axial position. The boundary value for velocity, $UEO = U(NNN)$ never changes since the inviscid flow is considered to occur at constant pressure. The velocities at the other radial locations are calculated through SETUP and GAUSS. If $|(U(IA) - UEO)/UEO| > TOL$, an indicator, IAP is set up to tell the program to increase the viscous region (this is not done until after all iterations are complete). The species concentrations are calculated at NNN, and then in the viscous region through SETUP and GAUSS. If the relative difference in molecular weights at IA and NNN exceeds TOL, the indicator IAP is set. The total enthalpy at NNN, $HT(NNN) = HEO$ is constant in the inviscid flow. In the viscous region, new

total enthalpies, HT(I) are calculated through SETUP and GAUSS. If the relative difference in total enthalpies at IA and NNN exceeds TOL, the indicator IAP is set.

In the first iteration, species production terms at the previous location are used. In the second and third iterations the species production terms at the midpoint of the interval are approximated by a Taylors series expansion. The same process of calculating boundary values, then viscous flow values, of the flow variables is followed. In between iterations, TRANSP and INTEG are called upon to obtain improved values of turbulent viscosity and the terms AP, APR used in SETUP, SETYP, SETHP.

After the third iteration, IAP is checked to see if the flow field should be expanded. If it should be it is expanded. If it should not, previous values of the flow variables are identified, and the program returns to increment another axial step. The results are printed every 50 steps, as defined by the variable KYS. KYS is set to 50 near the start of the main program. If this causes too much printing, KYS could be set to a larger value.

Inputs to MAIN

There are no inputs read into MAIN by tape, cards, etc.

Expected Outputs

After INIT, the MAIN program writes initial profiles of selected flow variables as a function of stream function.

After CHANGE, the MAIN program writes resultant profiles of selected flow variables.

Other writing is done by other subroutines.

2.4.2 SPECIE (KK1, KK2, NU)

Purpose and Uses of SPECIE

SPECIE is capable of calculating CM(I) (average molecular weight), X(J,I) (mole fractions of ISP species) and ROU(I) (mass flux), from axial location KK1 to KK2

If NU = 0, CM(I) and X(J,I) are transmitted

If NU < 0, ROU(I) is also transmitted

If NU = 0, only ROU(I) is transmitted

Inputs

There are no system inputs on cards or tape to SPECIE

Expected output

There are no system outputs on cards or tape from SPECIE

2.4.3 THERMO (KRIS, JA, IT)

Summary of Operations Performed by THERMO

In the initial phases of the program, JA is set to be greater than zero, which causes THERMO to read in coefficients for calculating species enthalpies. When JA is less than or equal to zero, and KRIS equals 100, species enthalpies are calculated at T(IT) (temperature allocation IT); if KRIS is different from 100, temperature is determined at a static enthalpy HST(IT), by means of a Newton-Raphson process.

System Inputs

A total of ISP sets of coefficients A, followed by ISP coefficients B. These are, respectively, the 300-1000°K and 1000-5000°K coefficients $a_1 - a_0$ from Table V of NASA SP-3001, for the appropriate compounds. For fuel, a value of -23900R calories per gram mole of $C_{10}H_{22}$ has been estimated to be the enthalpy of fuel at 477°F (estimated boiling point) from the elements at 298°K. The program also reads SENS, heats of formation at 298°K. These are not used in the present program.

System Outputs

The coefficients B are printed after being read in.

2.4.4 INIT

Summary of Operations Performed by INIT

INIT is called only once. It reads in NNN, the number of streamlines considered, then NNN cards containing UE(I) (velocity) SE(I) (temperature) and R(I) (radius) with R(I) starting at zero and increasing monotonically. Initial profiles of species mass fractions (YE(J,I)) are then read in at R(I). Stream functions are calculated for the initial profile, and the data are interpolated to equal intervals of stream function with the interval $DPSI = PSI/(NNN-1)$, where $PSI(I)$ is the value of stream function at location I.

System Inputs

NNN is an integer less than or equal to NELS (main program). UE(I) is in feet per second, SE(I) in degrees, Rankine, R(I) in inches. Species mass fractions are introduced per card up to ISP, for each R(I)

System Outputs

Nothing is written on card or tape from INIT.

2.4.5 TRANSP (NLOW, NHIGH)

Summary of Operations Performed by TRANSP

TRANSP calculates a turbulent viscosity, UM , according to Schetz's displacement thickness model, as described in the report. A DATA statement defines RJ , an inner jet radius, in feet.

System Inputs and Outputs

Nothing is read or written by TRANSP.

2.4.6 INTEG (NLOW, NHIGH, IN)

Summary of Operations Performed by INTEG

INTEG calculates radial values (R1I) as a function of stream function. It also calculates AP(I) and APR(I) at locations NLOW to NHIGH.

If $IN = 0$, $AP = APR = SP$

If IN is not zero, $AP = .5 (SP + APR)$

where $SP = UM * R(I) **2 * ROU(I)/PSI(I)$

is a term which arises in the transformation of equations to stream function coordinates.

System Inputs and Outputs.

No information is read to or written from INTEG.

2.4.7 SETUP (RUP)

Summary of Operations Performed by SETUP

SETUP calculates coefficients for solution of the finite difference equations for velocity. These are transmitted to labelled COMMON UPSET and used by GAUSS. The indicator KOR is set equal to -10.

System Inputs and Outputs

There are no INPUT/OUTPUT Statements in SETUP.

2.4.8 SETYP (RUP)

Summary of Operations Performed by SETYP

SETYP calculates coefficients for solution of the finite difference equations for species mass fractions, to be used by GAUSS. The indicator KOR is set to 0. A DATA statement defines CN which is the inverse of the turbulent Prandtl number. CN is taken to be 1 in the present study.

System Inputs and Outputs

There are no INPUT/OUTPUT Statements in SETYP.

2.4.9 SETHP (RUP)

Summary of Operations Performed by SETHP

SETHP calculates coefficients for solution of the finite difference equations for total enthalpy, to be used by GAUSS. The indicator KCR is set to + 10. A DATA statement sets CN = 1 as in SETYP, in the present program.

System Inputs and Outputs

There are no INPUT/OUTPUT statements in SETHP.

2.4.10 GAUSS

Summary of Operations Performed by GAUSS

Depending on whether KOR (see previous three subroutines) is negative, zero, or positive, GAUSS solves for velocity (U), species mass fractions (Y(J,I)) or total enthalpy (HT) through the viscous flow field. When KOR = 0, the mole fractions (X(J,I)) and average molecular weights (CM) are also determined. When KOR is positive, static enthalpy (HST) is also determined. In addition, GAUSS determines the outermost location at which the flow variables U, CM, HT deviate significantly from the inviscid external flow. This is defined to be IAP, as discussed in MAIN.

The highest location at which significant deviation occurs in each branch is defined to be NO(I), I = 1, 2, 3. Quantities NE(I), defining the innermost location at which the flow variables deviate significantly from an inviscid center flow, are also defined but are not used in the present program. An inner, reacting, inviscid flow could not be included in the program without some modification (essentially everything done in the stepwise calculations at NNN would have to be done at the inner boundary). An inner equilibrium flow could be included with slight modification.

The "significant deviation" mentioned above is defined in DATA as TOL, and is taken to be $1. \times 10^{-4}$ in the present program.

System Inputs and Outputs

There are no INPUT/OUTPUT statements in GAUSS.

2.4.11 CHANGE (RUP)

Summary of Operations Performed by CHANGE

CHANGE is called upon when the viscous flow field has expanded to its maximum size. The value of DPSI (stream function step size) is doubled, and the number of intervals is halved. In the present program, NNN is reduced from 51 to 26. Values of the flow variables are also transferred so that the flow variables correspond to the proper stream function values.

System Inputs and Outputs

There are no INPUT Statements in CHANGE. A printed output indicates that the number of points has been halved, and gives values of certain variables which are the distance downstream from the start in inches, and the distance interval in inches. The values are duplicated because at one time, DELX was changed when DPSI was changed. This is no longer done.

2.4.12 PRINT (KUSK, KUN)

Summary of Operations Performed by PRINT

PRINT lists pertinent variables when called upon by the MAIN program.

System Output

The first data listed are

Z(feet), ZX(inches), DELX(feet), DPSI, NEL, NEU, IA,
KUSK, KUN

Then at each of NNN locations, I(radial location), PSI, R, S(Temperature in °R) AP, APR, HT in one line, followed by Y(I,J) (2 lines) W(I,J) (2 lines) E(I,J) (2 lines) and a final line with YTOT, CM, ROU. This output represents the fundamental output for the program.

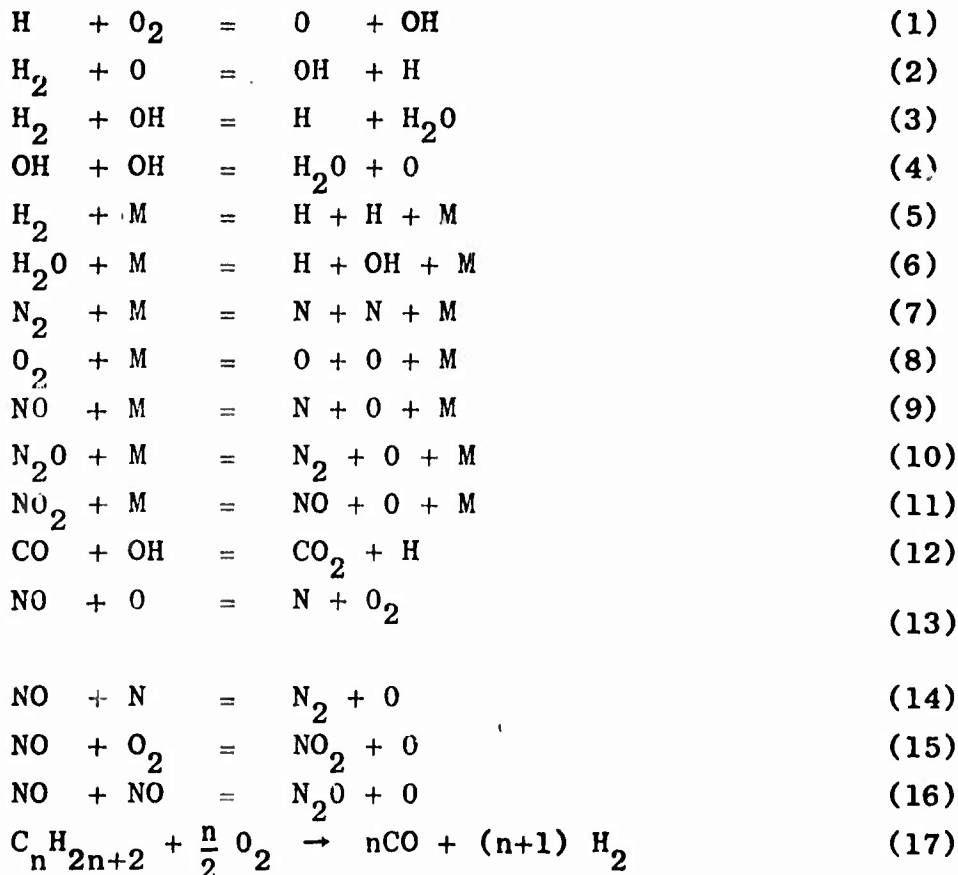
2.4.13 CHEMIE (KRY, KRAS, IT)

Purpose and Uses of CHEMIE

This subroutine calculates quantities necessary to calculate the species production terms for inclusion in the species conservation equations. It also reads in the parameters for calculating reaction rates. If (KRY + KRAS) is not less than zero, the parameters for the reactions rates are read in and listed. If (KRY + KRAS) is less than zero, the reaction rates, species production, and linearization terms are calculated. If KRAS is greater than zero, species production terms (W) are calculated.

If KRAS is equal to zero, linearized terms are calculated.

The reactions considered are:



System Inputs and Outputs

When called upon near the start of the program, CHEMIE reads data for calculating chemical reaction rates. These are, in order,

CW (molecular weights)
AU (collision terms in forward rate constants)
CU (collision terms in backward reaction rate constants)
E (forward rate activation energy/R)
D (backward rate activation energy/R)
GNUF(I,J) (stoichiometric coefficients for species I in forward reaction J)
GNUB(I,J) (stoichiometric coefficients for species I in backward reaction J)
AF, BF, AB, (respectively; temperature coefficient
BB density coefficient for forward reaction, similarly for reverse)
EN (number of carbon atoms in fuel $C_n H_{2n+2}$)

Certain of the above are listed after being read in, namely, CW, AU, CU, E, D, GNUF, GNUB.

2.5 Usage Instructions

2.5.1 Preparation of Inputs

Titles and Description of Inputs

The basic inputs to the program, initial profiles, are read by the subroutine INIT. The titles of the inputs, read in INIT, are

NNN - Number of inputs, number of streamlines considered initially.

UE, SE, R - One set per card.

UE is specified initial velocity, (ft/sec); specified initial temperature (degrees Rankin); at R, radial position in inches.

YE(J,I) A total of ISP species mass fractions, arranged in the order, H, O, H₂O, OH, O₂, H₂, N₂, N, NO, N₂O, NO₂, CO, CO₂, fuel at R. This requires two cards for the present value of ISP = 14.

The data are read on cards.

The cards must be read in the sequency:

NNN Card

UE, SE, R - Total of NNN cards

YE - One set of cards for each R (2 NNN cards in the present program).

Limitations

The first R is taken to be zero. R must increase from card to card. Negative values for any variable would have no physical meaning.

Formats

READ(5,100) NNN

READ(5,101)(UE(L),SE(L),R(L),L=1,NNN)

READ(5,102)((YE(J,I),J=1,ISP),I=1,NNN)

100 FORMAT(I5)

101 FORMAT(3F10.0)

102 FORMAT(7D10.0)

Relationship of Inputs to Outputs

These are the fundamental starting values for the differential equations. All output profiles are related to these.

In particular, selected flow variables are printed in MAIN directly after INIT. These are dependent on PSI, rather than R, as are all subsequent outputs of flow variables. Only values at the end points should be the same.

2.5.2 Results of Operation

Description of Results

The major results are profiles of velocity, temperature, and species mass fraction at specified axial locations. The output comes on the printer.

Format and Content

The output instruction and format are as follows

```
Z=ZX/12.  
WRITE (6,30) Z,ZX,DELX,DPSI,NEL,NEU,IKS,KUSK,KUN  
DO 20 I=IK,IA  
YTOT=0.0  
DO 10 J=1,ISP  
10  YTOT=YTOT+Y(J,I)  
   WRITE (6,40) I,PSI(I),R(I),S(I),U(I),AP(I),APR(I),HT(I)  
   WRITE (6,50) I,(Y(J,I),J=1,ISP)  
   WRITE (6,50) I,(W(J,I),J=1,ISP)  
   WRITE (6,50) I,(E(J,I),J=1,ISP)  
   WRITE (6,60) I,YTOT,CM(I),ROU(I)  
20  CONTINUE  
   WRITE(6,60) KQ,UM  
   RETURN  
C  
30  FORMAT ('1',////,4(2X,F15.10),5(3X,I5),7H OUTPUT,///)  
40  FORMAT (/,2X,I4,7(2X,E14.7))  
50  FORMAT (2X,I4,7(2X,E14.7)/,6X,7(2X,F14.7))  
60  FORMAT (2X,I4,3(2X,E14.7))
```

Use of Outputs

The outputs contain information on the pollutant concentrations, and other concentrations. Hence the use of output, at the end of the afterburner, will be to predict pollutant concentrations. Intermediate results indicate the evolution of the pollutants.

A Sample input is presented in this and the following page

21		
286.	2145.	0.
286.	2145.	.184
286.	2145.	.368
285.	2140.	.552
282.	2136.	.736
278.	2130.	.92
270.	2120.	1.104
262.	2110.	1.288
258.	2100.	1.472
254.	2088.	1.656
250.	2076.	1.84
246.	2062.	2.024
242.	2050.	2.208
238.	2038.	2.392
234.	2022.	2.576
232.	2004.	2.76
230.	1980.	2.944
228.	1950.	3.128
226.	1910.	3.312
224.	1872.	3.496
223.	1840.	3.68
223.	1830.	3.864
223.	1830.	4.048
223.	1830.	4.232
223.	1830.	4.416
223.	1830.	4.6
223.	1830.	4.784

2.6 Operating Instructions

2.6.1 Operating Procedures

Initiation of Program

The program is on cards, together with data. For a particular computer, proper control cards must be introduced. Input is on cards, output on printer.

Maintaining Computer Program Operation

The program will continue to operate, as long as too large a step size is not used. If too large a step size is used, the procedure is unstable, and is characterized by logs of negative numbers, due to temperature going negative. The program must be started with a smaller step size (DELX).

Termination and Restart

Termination is achieved when $Z > ZMAX$. If interruption of the program is necessary, some subroutine would have to be written to identify the necessity for interruption at statement 40, MAIN, store program and all data, and restart at the same point.

2.6.2 Operator Inputs

Initial inputs, other than the basic initial profile mentioned previously, include the thermodynamic and chemical data initially read in THERMO and CHEMIE.

The input statements and formats, and data used in the present version, are shown below.

In THERMO

```
180 READ (5,260) ((A(K,J),K=1,6),J=1,ISP)
    DO 190 J=1,ISP
      READ (5,260) (B(K,J),K=1,6)
      WRITE (6,280) (B(K,J),K=1,6)
190 CONTINUE
    READ (5,270) (SENS(J),J=1,ISP)
    GO TO 170
200 WRITE (6,210) M,R(M),PSI(M),HST(M),HTS,FA,FB,TP,T(M)
    GO TO 90
C
210 FORMAT (///,2X,14,8(2X,E13.5),1X,4HTHER,///)
220 FORMAT (/,2(2X,15),6(2X,E15.8))
230 FORMAT (2X,15,4(2X,E15.8))
240 FORMAT (2X,15,7(2X,E15.8))
250 FORMAT (2X,15,7(2X,E15.8),/)
260 FORMAT (4D15.8,/2D15.8)
270 FORMAT (7D10.0)
280 FORMAT (////////,1X,6E20.8,////////)
```

The Data used in the present version are as follows:

0.25000000E 01

0.25470497E 05

0.30218894E 01-0.21737249E-02 0.37542203E-05-0.29947200E-08

0.90777547E-12 0.29137190E 05

0.41565016E 01-0.17244334E-02 0.56982316E-05-0.45930044E-08

0.14233654E-11-0.30288770E 05

0.38234708E 01-0.11187229E-02 0.12466819E-05-0.21035896E-09

-0.52546551E-13 0.35852787E 04

0.37189946E 01-0.25167288E-02 0.85837353E-05-0.82998716E-08

0.27082180E-11-0.10576706E 04

0.28460849E 01 0.41932116E-02-0.96119332E-05 0.95122662E-08

-0.33093421E-11-0.96725372E 03

0.36916148E 01-0.13332552E-02 0.26503100E-05-0.97688341E-09

-0.99772234E-13-0.10628336E 04

.2514793700E 01-.112437910E-03.2964750600E-06-.324640490E-09

.1259546500E-12.5612776700E 05

.4146947600E 01-.411972370E-02.9692246700E-05-.786336390E-08

.2277951200E-11.9744789400E 04

.2382117100E 01.1035055600E-01-.111676340E-04.6958316500E-08

-.187801920E-11.8722996400E 04

.3434456300E 01.2223429700E-02.6714897500E-05-.974277190E-08

.3721252300E-11.2864768500E 04

.3787133200E 01-.217095260E-02.5075733700E-05-.347377280E-08

.7721684100E-12-.143635080E 05

.2170100000E 01.1037811500E-01-.107339380E-04.6345917500E-08

-.162807010E-11-.483526020E 05

Blank Card

-.239000000E 05

0.25000000E 01

0.25470497E 05

0.25372567E 01-0.18422190E-04-0.88017921E-08 0.59643621E-11

-0.55743608E-15 0.29230007E 05

0.26707532E 01 0.30317115E-02-0.85351570E-06 0.11790853E-09

-0.61973568E-14-0.29888994E 05

0.28895544E 01 0.99835061E-03-0.21879904E-06 0.19802785E-10

-0.38452940E-15 0.38811792E 04

0.35976129E 01 0.78145603E-03-0.22386670E-06 0.42490159E-10

-0.33460204E-14-0.11927918E 04

0.30436897E 01 0.61187110E-03-0.73993551E-08-0.20331907E-10

0.24593791E-14-0.85491002E 03

0.28545761E 01 0.15976316E-02-0.62566254E-06 0.11315849E-09

-0.76897070E-14-0.89017445E 03

.2442226100E 01.1227618700E-03-.849927190E-07.2140083000E-10

-.125110580E-14.5614083100E 05

.3152936000E 01.1405995500E-02-.570784620E-06.1062820900E-09

-.737207830E-14.9852204800E 04

.4626547900E 01.3021680700E-02-.121560140E-05.2285595200E-09

-.158497010E-13.8535664500E 04

.4613921900E 01.2638663900E-02-.109485410E-05.2081842500E-09

-.146543910E-13 .234037800E 04

.2951151900E 01.1552556700E-02-.619114110E-06.1135033600E-09

-.778827320E-14-.142318270E 05

.4412926600E 01.3192289600E-02-.129782300E-05.2414744600E-09

-.167429860E-13-.489440430E 05

Blank Card

-.239000000E 05

52097.7 59556.6 -57797.9 9312.5

113024.6 21600. 19490. 8007.5 -26415.7 -94051.8 -59670

In CHEMIE, the INPUT/OUTPUT STATEMENTS are

```

READ(5,600)(CW(J),J=1,ISP)
WRITE(6,700)(CW(J),J=1,ISP)
READ(5,601)(AU(K),K=1,IRE)
WRITE(6,701)(AU(K),K=1,IRE)
READ(5,601)(CU(K),K=1,IRE)
WRITE(6,701)(CU(K),K=1,IRE)
READ(5,602)(E(K) ,K=1,IRE)
WRITE(6,702)(E(K) ,K=1,IRE)
READ(5,602)(D(K) ,K=1,IRE)
WRITE(6,702)(D(K) ,K=1,IRE)
WRITE(6,703)
READ(5,605) ((GNUF(J,K),J=1,ISP),K=1,IRE)
WRITE(6,705) GNUF
READ(5,605) ((GNUB(J,K),J=1,ISP),K=1,IRE)
WRITE(6,705) GNUB
605 FORMAT(7F10.0)
705 FORMAT(2X,7F12.5)
DO 5 K=1,IRE
5 READ(5,606) AF(K),BF(K),AB(K),BB(K)
606 FORMAT(4F10.0)

```

J

```

READ(5,606) EN

```

Data are

1.008	16.	18.016	17.008	32.	2.016	28.016	CW
14.008	30.008	44.016	46.008	28.011	44.011	142.286	CW
.72000E	15.33000E	13.62000E	14.77000E	13.31000E	16		A
.54000E	18.47500E	17.35600E	19.39900E	21.10000E	16		A
.54000E	22.71000E	13.32000E	10.15500E	14.18000E	11		A
.26000E	13.20000E	09					A
.55000E	14.14000E	13.32000E	15.83000E	14.70000E	18		C
.15000E	17.61000E	15.10000E	15.90000E	15.18200E	14		C
.20000E	17.47000E	15.13300E	11.70000E	14.58000E	11		C
.14200E	15.10000E	10					C
8504.	4026.	3019.	503.	55353.	62196.	113171. 59378. 75841.	E
30696.	37237.	3875.	19675.	0.	23651.	32105. 6914.	E
503.	3019.	10618.	9108.	0.	0.	0. 0. 0.	D
10769.	0.	13712.	3563.	37992.	0.	14090. 0.	D

The GNUF are

1.

1.

1.

1.

1.

1.

2.

1.

1.

1.

1.

1.

1.

1.

1.

1.

1.

1.

1.

1.

1.

1.

2.

5.

1.

The AF, BF, AB, BB are

	1.		1.
	1.		1.
	1.		1.
	1.0		1.0
	1.	-1.	2.
	1.		2.
-.5	1.		2.
-1.	1.		2.
-1.5	1.		2.
	1.		2.
-1.	1.		2.
	1.		1.
1.	1.	1.	1.
	1.		1.
.5	1.	.5	1.
	1.		1.

This card all zeros

EN is _____

10.

SECTION III

LISTING OF PROGRAM

A listing of the program and data input are presented in this section

```

C MAIN PROGRAM RRR00034
C
C READ IN INITIAL PROFILES (VELOCITY, TEMPERATURE AND CONCENTRATIONS)
IMPLICIT REAL*(A-H,O-Z)
DIMENSION DID(14),DES(14)
COMMON R(51),S(51),U(51),Y(14,51),ROU(51),T(51),PSI(51)
COMMON UPR(51),YPR(14,51),HST(51),HT(51),TPR(51),HTPR(51)
COMMON CM(51),X(14,51),AP(51),APR(51),UEO,UEI,RHUE,RHJD,TEI,TEO
COMMON HEI,HEO,CMEI,CMO,DPSI,MNN,NEL,NEU
COMMON /TFT/ YOEI,YOEO
COMMON /TOSK/ H(14)
COMMON /SAX/ ZX,UM
COMMON /UPSET/ A(51),B(51),C(51),D(14,51),V(14,51),ALP(51),BAK,A
ISKA,BUK,PISK,IKS,IK,IA,KO,KOR
COMMON /SU/ DELX
COMMON /SIG/ PA(14,14),PT(14),W(14,51)
COMMON /SYLT/ E(14,51)
COMMON /YVY/ IZE
COMMON /CEN/ KRISE
COMMON /SA/ AREX
COMMON /SSS/ IAP
COMMON /VVV/ YO(51)
COMMON /ZZZ/ ISP,IRE,IMU
COMMON /YP/ YEI(14),YEO(14)
COMMON / RRR/ TO(51)
COMMON /XXX/ TAU
COMMON /UUU/ ZZ(51)
KQ +VE INDICATES REGIME 2 HAS BEEN REACHED
DATA NILS/517,KRIS,JA,IT/-10,10,17,KRYS,KRAS/-10,20/
DATA Z/O,07,KZ/5007,KRN/507,KRI/107,KILLE/107,KUN/07
DATA KTELL/37,CN/1.0007
TSP=14
IRE=17
IMU=11
TAU=.40-3
IZE=0
KAN=-10
KUM=0
KYS=50
KRISE=-10
KQ=-10
ZX=0.0
CALL ITHRMO (KRIS,JA,IT)

```

B 3
B 4
A 5
B 10
B 12
B 15
B 18
B 19
A 20
A 21
A 2
B 23
B 25
B 26
A 27
A 28

31

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```

1 J=1
KRAS=20
KRY5=-11
CALL CHEMIE (KRY5,KRAS,[J])
WRITE (6,390)
CALL INIT
NINA=NNN
DELX=.00001
RUP=DELX/(DPSI**2)
ZMAX=.7
AREX=DELX
KK1=1
KK2=NNN
NU=-10
CALL SPECIE (KK1,KK2,NU)
JA=-10
KRIS=100
DO 20 I=1,NNN
UPR(I)=U(I)
IT=1
CALL THERMO (KRIS,JA,IT)
HSI=0.0
DO 10 J=1,ITSP
VPR(J,I)=V(J,I)
HST(I)=HST+X(J,I)*H(J)
HST(I)=HST*IR00./CH(I)
HT(I)=(U(I)**2)/(2.*32.17*778.16)+HST(I)
YPR(I)=S(I)
HPR(I)=HT(I)
HEJ=HT(I)
HEO=HT(NNN)
NLOW=1
NHIGH=NNN-1
CALL TRANSP(NLOW,NHIGH)
TN=0
CALL INTEG (NLOW,NHIGH,TN)
WRITE (6,370) NNN
WRITE (6,380) (I,R(I),PSI(I),U(I),T(I),S(I),CH(I),Y(6,I),I=1,NNN)
WRITE (6,380) (I,R(I),PSI(I),HT(I),HST(I),HPR(I),X(6,I),X(3,I),I=
11,NNN)
30 CONTINUE
DUPX=AREX
DELX=AREX

```

A 29
B 30
B 31
A 32
B 33
A 34

B 37
B 38
B 39
A 40
A 41
A 42
A 43
A 44
A 45
A 46
A 47
A 48
A 49

A 51
B 52
A 53
A 54
A 55
A 56
A 57
A 58
P 60

B 62
B 63
B 64
B 65
A 66
A 67
A 68
A 69
B 70

```

40 Z=Z+DELX B 71
IF (Z.GT.ZMAX) GO TO 310 B 72
ZX=Z*12. B 73
KUN=KUN+1 B 74
KUSK=0 B 75
NEVU=NEU B 76
NEVL=NEL B 77
IA=NNN-1
NEU=IA-4
NEVU=NEU
IK=NEL-4 B 79
IF (IK.LE.1) IK=1 B 80
IKS=(IA-IK)+1 B 81
IKU=IKS-1 B 82
RUP=DELX/(DPSI**2) B 83
IF (IA.GE.(NILS-1)) GO TO 50
GO TO 60 B 85
50 CONTINUE
KUN=0
KUM=0
CALL CHANGE(RUP)
Z=ZX/12.
IK=1
IA=NNN-1
NEU=IA-4
IF (IK.LE.1) IK=1
IKS=(IA-IK)+1
NINA=NNN
WRITE (6,370) NNN B 91
WRITE (6,380) (I,K(I),PSI(I),U(I),T(I),S(I),CM(I),Y(6,I),I=1,NNN) B 92
60 KUSK=KUSK+1 A 93
UEO=U(NNN)
CALL SETUP (RUP) B 94
CALL GAUSS B 95
KRY5=-1 B 96
KRAS=5 B 97
IJ=NNN
CALL CHEMIE(KRYS,KRAS,IJ)
DO 400 J=1,IJSP
400 E(J,NNN)=W(J,NNN)/U(NNN)
DO 401 J=1,IJSP
401 Y(J,NNN)=DELX*E(J,NNN)+YPR(J,NNN)
KK1=NNN

```

```

KK2=NNN
NI=10
CALL SPECIE(KK1, KK2, NU)
DO 402 J=1, ISP
402 YFN(J)=Y(J, NNN)
CMO=CM(NNN)
JA=-10
KRIS=10
IT=NNN
HST(NNN)=HT(NNN)-(U(NNN)**2)/(2.*32.17*78.76)
CALL THERMO(KRIS, JA, IT)
TEO=S(NNN)
NI=0
CALL SPECIE(KK1, KK2, NU)
RHUO=ROU(NNN)
DO 110 I=IK, IA
IF (KQ.GT.0) GO TO 70
IF (I.LT.IK) GO TO 90
70 IF (I.GT.IA) GO TO 90
IJ=I
3 CALL CHEMIE (KRY, KRAS, IJ)
4 DO 80 J=1, ISP
80 E(J, I)=.5*(U(I)*UPR(I))+W(J, I)/(U(I)*UPR(I))
GO TO 110
90 DO 100 J=1, ISP
E(J, I)=0.0
100 W(J, I)=0.0
110 CONTINUE
CALL SETYP (RUP)
CALL GAUSS
IF (KRIS.GT.0) GO TO 320
CALL SETHP (RUP)
CALL GAUSS
KK1=IK
KK2=IA
JA=-10
KRIS=10
DO 120 I=IK, IA
IT=I
CALL THERMO (KRIS, JA, IT)
120 CONTINUE
NI=0
CALL SPECIE (KK1, KK2, NU)

```

B 99

B 100

B 103

B 104

B 1

B 107

B 109

B 110

B 111

B 112

B 113

B 114

B 115

B 116

B 117

B 118

B 119

B 120

B 121

B 122

B 123

B 124

B 125

B 126

130 NLOW=IK
NHIGH=IA
IN=10

CALL TRANSP(NLOW,NHIGH)
CALL INTEG (NLOW,NHIGH,IN)
IF(KUN.EQ.50) KAN=10
IF(KAN.LT.0) GO TO 623
CALL PRINT (KUSK,KUN)
KAN=-10

623 CONTINUE
UEO=U(NNN)
CALL SETUP (RUP)
CALL GAUSS
KRAS=0
KUSK=KUSK+1
DAD=(S(NNN)-TPR(NNN))/1.8
T(NNN)=.5*(T(NNN)+TPR(NNN))/1.8
DO 403 J=1,ISP

01D(J)=Y(J,NNN)-YPR(J,NNN)
403 Y(J,NNN)=.5*(Y(J,NNN)+YPR(J,NNN))
IJ=NNN

CALL CHEMIE(KRYS, KRAS, IJ)
DO 404 KI=1,ISP
SUM=0.

DO 405 J=1,ISP
DES(J)=01D(J)*PA(J,KI)

405 SUM=SUM+DES(J)
RA=W(KI,NNN)/U(NNN)*2.
BE=(DAD*PT(KI)+SUM)/U(NNN)
E(KI,NNN)=.5*(RA+BE)

404 CONTINUE
DO 406 J=1,ISP
406 Y(J,NNN)=DELX*E(J,NNN)+YPR(J,NNN)

KK1=NNN
KK2=NNN
NU=10

CALL SPECIF(KK1, KK2, NU)
DO 407 J=1,ISP

407 YEO(J)=Y(J,NNN)
CMO=C:H(NNN)
JA=-10
KRIS=10
IT=NNN

8 127
8 128
8 129
8 130
8 131
8 132
8 133
8 134
8 135

HST(NNN)=HT(NNN)-(U(NNN)**2)/(2.*32.17*778.76)

CALL THERMO(KRIS,JA,IT)

TEO=S(NNN)

NU=0

CALL SPECIE(KK1, KK2, NU)

RMU=ROU(NNN)

DO 220 I=IK,IA

IF (KO.GT.0) GO TO 140

IF (I.LT.IK) GO TO 200

140 IF(I.GT.IA) GO TO 200

DAD=(S(I))-TPR(I)/I.8

T(I)=.5*(T(I)+TPR(I)/I.8)

DO 150 J=1,ISP

DIO(J)=Y(J,I)-YPR(J,I)

150 Y(J,I)=.5*(Y(J,I)+YPR(J,I))

IJ=I

CALL CHEMIE (KRY5,KRAS,IJ)

DO 190 KI=1,ISP

SUM=0.0

DO 170 J=1,ISP

IF (DAMS(PA(J,KI)).GT.0.ID=30) GO TO 160

DES(J)=0.0

GO TO 170

160 DES(J)=DIO(J)*PA(J,KI)

170 SUM=SUM+DES(J)

BA=(U(I)+UPR(I))*W(KI,I)/(U(I)*UPR(I))

BE=(DAD*PT(KI))+SUM/U(I)

180 E(KI,I)=.5*(BA+BE)

190 CONTINUE

GO TO 220

200 DO 210 J=1,ISP

210 E(J,I)=0.0

220 CONTINUE

CALL SETYP (RUP)

CALL GAUSS

IF (KRIS.GT.0) GO TO 320

CALL SETHF (RUP)

CALL GAUSS

DO 230 I=IK,IA

IT=I

CALL THERMO (KRIS,JA,IT)

230 CONTINUE

NU=0

8 136

8 137

8 141

8 143

8 144

8 145

8 146

8 148

8 150

8 151

8 152

8 153

8 154

8 155

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8 164

8 165

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8 168

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8 170

8 171

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8 173

8 174

8 175

8 176

8 177

8 178

KK1=IK
KK2=IA
CALL SPECIE (KK1, KK2, NU)
IF (KUSK.EQ.3) GO TO 240
GO TO 130
240 CONTINUE
IN=0
IF(IAP.LY.IA) GO TO 280
NEU=IA-3
IA=NNN
NNN=NNN+1
IF(NNN.GT.NILS) GO TO 50
PSI(NNN)=PSI(NNN-1)+DPST
U(NNN)=U(NNN-1)
UPR(NNN)=UPR(NNN-1)
S(NNN)=S(NNN-1)
T(NNN)=S(NNN)/I.B
YPR(NNN)=YPR(NNN-1)
DO 408 J=1,ISP
Y(J,NNN)=Y(J,NNN-1)
X(J,NNN)=X(J,NNN-1)
408 YPR(J,NNN)=YPR(J,NNN-1)
YO(NNN)=YO(NNN-1)
YO(NNN)=YO(NNN-1)
HT(NNN)=HT(NNN-1)
HST(NNN)=HST(NNN-1)
ZZ(NNN)=ZZ(NNN-1)
ROU(NNN)=ROU(NNN-1)
NLOW=IK
NHIGH=NNN-1
CALL TRANSP(NLOW, NHIGH)
CALL INTEG(NLOW, NHIGH, ITO)
270 CONTINUE
280 CONTINUE
IK=NEL-4
IF (IK.LE.1) IK=1
IKS=(IA-IK)+1
NLOW=IK
NHIGH=IA
CALL TRANSP(NLOW, NHIGH)
CALL INTEG (NLOW, NHIGH, IN)
DO 300 I=IK, NNN
UPR(I)=U(I)

B 179
BCH180
B 181
B 182
B 184

B 198
B 199
B 200
B 201
B 202
B 203
B 204
B 206

```

TPR(I)=S(I)
HTPR(I)=HT(I)
DO 290 J=1,ISP
  290 YPR(J,I)=Y(J,I)
  300 CONTINUE
  KUM=KUM+1
  IF(KUM.NE.KYS) GO TO 624
  KUM=0
  IF(KUM.LT.100) GO TO 624
  CALL PRINT (KUSK,KUM)
  624 CONTINUE
  IF(KUM.EQ.2) GO TO 71
  IF(KUM.EQ.4) GO TO 72
  IF(KUM.LT.100) GO TO 73
  IF(KUM.GE.100) GO TO 74
  GO TO 30
310 STOP
  71 CONTINUE
  DELX=.00001
  GO TO 75
  72 CONTINUE
  DELX=.00001
  GO TO 75
  73 CONTINUE
  DELX=.00001
  GO TO 75
  74 CONTINUE
  DELX=.00001
  GO TO 75
  75 CONTINUE
  RUP=DELX/(DPSI**2)
  AREX=DELX
  GO TO 30
320 KRISE=-10
  Z=Z-DELX
  DELX=DELX/2.
  KUM=KUM-1
  NELE=NEV1
  NEU=NEV0
  GO TO 40
  C
330 FORMAT (2X,4(2X,15),14H SJERK FOR NEU,7)
340 FORMAT (2X,2(2X,14),6(2X,014,7))
350 FORMAT (2X,7(2X,014,7))

```

6 207
8 208

8 210
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8 213
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8 215
8 216

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8 220

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8 224
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8 226
8 227

```

360  FORMAT (/,2X,13HSTEP DECREASE,3(2X,D20.10),//)      B 228
380  FORMAT (2X,14,7D18.7)                                A 230
370  FORMAT ('1',2X,6HNNN=,14,////)
390  FORMAT ('1')
END
SUBROUTINE SPECIE (<K1,<K2,NU)
IMPLICIT REAL*(A-H,O-Z)
DIMENSION G(14),CW(14)
COMMON R(51),S(51),U(51),Y(14,51),ROU(51),T(51),PSI(51)
COMMON UPR(51),YPR(14,51),HST(51),HI(51),TPR(51),HPR(51)
COMMON CM(51),X(14,51),AP(51),APR(51),UEO,UEI,RHUE,RMUO,TEI,TEO
COMMON HEI,HEO,CMEI,CMO,DPSI,NNN,NEL,NEI
COMMON /ZZZ/ISP,IRE,IMU
DATA P/1.0007
DATA CW/1.008,16.0,18.016,17.008,32.0,2.016,28.016,14.008,30.008,
1 44.016,46.008,28.011,44.011,142.286/
DO 40 I=KK1,KK2
IF (NU.EQ.0) GO TO 30
CM(I)=0.0
GM=0.0
DO 10 J=1,ISP
G(J)=Y(J,I)/CW(J)
10  GM=GM+G(J)
DO 20 J=1,ISP
X(J,I)=G(J)/GM
20  CM(I)=CM(I)+X(J,I)*CW(J)
IF (NU.EQ.10) GO TO 40
CONTINUE
RM=1545.3/CM(I)
ROP=*2116.27/(RM*(I)*1.8)
ROU(I)=RO*(I)
40  CONTINUE
RETURN
END
SUBROUTINE THERMO (KRIS,JA,IT)
THERMODYNAMIC SUBROUTINE, BASED ON NASA SP-3001
C  REFERENCE TEMPERATURE 298.15 DEG. K
C  SPECIFSH,O,H2O,OH,O2,H2,N2
C  FRY5 -VE : IMPLIES FROZEN FLOW,HENCE SENS(J)NOT ZERO
C  JA  +VE : READ IN CONSTANTS
C  JA  -VE : CALCULATE ENTHALPIES
IMPLICIT REAL*(A-H,O-Z)
DIMENSION A(6,14),B(6,14),SENS(14)

```

```

COMMON R(51),S(51),U(51),V(14,51),ROU(51),Y(51),PSI(51)
COMMON UPR(51),YPR(14,51),HST(51),HT(51),T(51),T(51),MTPR(51)
COMMON CM(51),X(14,51),AP(51),APR(51),UEO,UEI,RHUF,RHUD,TEI,TEO
COMMON HEI,HEO,CMEI,CMO,DPSI,NNN,NEL,NEU
COMMON /ZZZ/ISP,IRE,IRU
COMMON /TNSK/ H(14)
M=I
IF (JA) 10,10,180
CONTINUE
10 IF (KRIS.EQ.+100) GO TO 100
NR=0
TP=S(M)
T(M)=TP/1.8
TO=TP
CONTINUE
HAS=0.0
GO TO 100
30 CONTINUE
DO 40 J=1,ISP
HAS=HAS+X(J,M)*H(J)
HTS=HAS*100./CM(M)
NR=NR+1
IF (NR.GE.20) GO TO 90
CHH=HST(M)-HTS
CHK=0ABS(CHH/HST(M))
IF (CHK.LE.0.001) GO TO 90
IF (NR.GE.2) GO TO 80
TA=TP
PA=CHH
IF (CHH) A0,90,50
TP=TP+1.
GO TO 70
60 TP=TP-1.
70 T(M)=TP/1.8
GO TO 20
80 TR=TP
FB=CHH
IF ((FB=FA).EQ.0.0) GO TO 200
TP=TA-FA*((1B-TA)/(FB-FA))
T(M)=TP/1.8
FA=FB
TA=TR
GO TO 20

```

D 14
D 15
D 16
D 17
D 18
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D 21
D 22
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D 41
D 42
D 43
D 44
D 45
D 46
D 47
D 48
D 49
D 50

```

90 CONTINUE D 51
S(M)=T(M)*1.8 D 52
GO TO 170 D 57
100 CONTINUE D 58
G=1.98726 D 59
DO 160 J=1,ISP
IF (T(M)-1000.) 110,110,120 D 61
110 HA=A(I,J)+(A(2,J)/2.+(A(3,J)/3.+(A(4,J)/4.+(A(5,J)/5.)*T(M))*T(M)) D 62
1*(T(M))*T(M)+A(6,J)/T(M) D 63
GO TO 130 D 64
120 HA=B(I,J)+(B(2,J)/2.+(B(3,J)/3.+(B(4,J)/4.+(B(5,J)/5.)*T(M))*T(M)) D 65
1*(T(M))*T(M)+B(6,J)/T(M) D 66
130 IF (KRIS) 140,140,150 D 67
140 CONTINUE D 68
H(J)=(HA*G*T(M)-SENS(J))/1000. D 69
GO TO 160 D 70
150 H(J)=HA*G*T(M)/1000. D 71
160 CONTINUE D 72
IF (KRIS.EQ.+100) GO TO 170 D 73
GO TO 30 D 74
170 CONTINUE D 75
RETURN D 76
180 READ (5,260) ((A(K,J),K=1,6),J=1,ISP)
DO 190 J=1,ISP
READ (5,260) (B(K,J),K=1,6)
WRITE (6,280) (B(K,J),K=1,6)
190 CONTINUE
READ (5,270) (SENS(J),J=1,ISP)
GO TO 170
200 WRITE (6,210) M,R(M),PSI(M),HST(M),HTS,FA,FB,TP,T(M)
GO TO 90
C
210 FORMAT (///,2X,14,8(2X,E13.5),1X,4#THFR,///)
220 FORMAT (/,2(2X,15),6(2X,E15.8))
230 FORMAT (2X,15,4(2X,E15.8))
240 FORMAT (2X,15,7(2X,E15.8))
250 FORMAT (2X,15,7(2X,E15.8),/)
260 FORMAT (4D15.8,2D15.8)
270 FORMAT (7D10.0)
280 FORMAT (///,1X,6E20.8,///)
END
SUBROUTINE INIT
IMPLICIT REAL*(A-H,O-Z)

```

```

DIMENSION UE(51),SE(51),YE(I4,51),PS(51)
COMMON R(51),S(51),U(51),Y(I4,51),R00(51),T(51),PSI(51)
COMMON UPR(51),YPR(I4,51),HST(51),HT(51),TPR(51),H1PR(51)
COMMON CM(51),X(I4,51),AP(51),APR(51),UFD,UEI,RAUE,RAUO,TEI,TEO
COMMON HEI,HEO,CHEI,CMO,DPST,NN,NEL,NEU
COMMON /TTTT/ YOEI,YOEO
COMMON /ZZZ/ TSP,IRE,IMU
COMMON / RRR/ TO(51)
COMMON /YYP/ YE(I4),YEO(I4)
COMMON /UUU/ ZZ(51)
COMMON /VVV/ YU(51)
READ(5,100) NNN
READ(5,101)(UE(L),SE(L),R(L),L=1,NNN)
READ(5,102)((YE(J),J=1,TSP),T=1,NNN)
DO 40 L=1,NNN
S(L)=SE(L)
T(L)=S(L)/1.8
U(L)=UE(L)
DO 30 J=1,TSP
40 30 Y(J,L)=YE(J,L)
40 40 CONTINUE
KK1=1
KK2=NNN
NU=10
CALL SPECIE (KK1,KK2,NU)
PSI)=0.
FR0=0.
DSI=0.
DO 50 L=1,NNN
IF((L-2).LT.0) GO TO 50
DELR=(R(L)-R(L-1))/12.
FRI=ROU(L)*R(L)/12.
DP=DELR*(FR0+FRI)
FR0=FRI
DSI=DSI+DP
PS(L)=DSORT(DST,
50 CONTINUE
UEI=U(I)
UEO=U(NNN)
TEI=S(I)
TEO=S(NNN)
CHEI=CM(I)
CMO=CM(NNN)

```

```

DO 60 J=1,ISP
VEI(J)=Y(J,I)
60 VEI(J)=Y(J,NNN)
DPST=PS(NNN)/(NNN-1)
RHUE=RQU(I)
RHUD=RQU(NNN)
PSI(I)=0.
DO 2 J=2,NNN
2 PSI(J)=PSI(J-1)+DPST
NMI=NNN-1
DO 3 J=2,NMI
DO 4 K=1,NNN
DIF=PSI(J)-PS(K)
IF(DIF) 5,6,4
6 U(J)=UE(K)
S(J)=SE(K)
I(J)=SI(J)/I.8
DO 8 L=1,ISP
8 Y(L,J)=YE(L,K)
GO TO 3
43
5 RAT=(PSI(J)-PS(K-I))/(PS(K)-PS(K-I))
U(J)=UE(K-I)+RAT*(UE(K)-UE(K-I))
S(J)=SE(K-I)+RAT*(SE(K)-SE(K-I))
I(J)=SI(J)/I.8
DO 9 L=1,ISP
9 Y(L,J)=YE(L,K-I)+RAT*(YE(L,K)-YE(L,K-I))
GO TO 3
4 CONTINUE
3 CONTINUE
PSI(NNN)=PS(NNN)
NEL=1
NEU=22
DO 11 J=1,NNN
11 YU(J)=Y(ISP,J)
DO 12 J=MEL,NNN
12 ZU(J)=0.
DO 14 J=1,NNN
14 T(U,J)=0.
YUE=Y(ISP,I)
YUEO=Y(ISP,NNN)
RETURN
100 FORMAT(I5)
101 FORMAT(3F10.0)

```

102 FORMAT(7D10.0)

END

SUBROUTINE TRANSP(NLOW,NHIGH)

IMPLICIT REAL*8(A-H,O-Z)

COMMON R(51),S(51),U(51),V(1,51),R0U(51),T(51),PSI(51)

COMMON UPR(51),YPR(14,51),HST(51),HT(51),TPR(51),HTPR(51)

COMMON CM(51),X(14,51),AP(51),APR(51),UEO,UEI,RHUE,RHUU,TEI,TEO

COMMON HEI,HEO,CMEI,CMO,DPSI,NNN,NEL,NEU

COMMON /SAX/ ZX,UM

DATA RJ /,2/

COEFF=.036/RJ

L=NLOW

LL=NHIGH+1

SUM=0.

DO I K=L,LL

ARG=DABS(TROJ(LL)-ROU(K))/ROU(K))*PSI(K)

I SUM=SUM+ARG

SUM=SUM*DPSI

UM=SUM*COEFF

RETURN

END

SUBROUTINE INTEG (NLOW,NHIGH,IN)

IMPLICIT REAL*8(A-H,O-Z)

COMMON R(51),S(51),U(51),V(14,51),R0U(51),T(51),PSI(51)

COMMON UPR(51),YPR(14,51),HST(51),HT(51),TPR(51),HTPR(51)

COMMON CM(51),X(14,51),AP(51),APR(51),UEO,UEI,RHUE,RHUU,TEI,TEO

COMMON HEI,HEO,CMEI,CMO,DPSI,NNN,NEL,NEU

COMMON /SAX/ ZX,UM

C INTEGRATION ROUTINE BACK TO PHYSICAL PLANE

C IF IN GT. THAN 0.0 A IS AVERAGED

C IF IN EQ. TO 0.0 A IS BASED ON PAST TIME ROW.

INIT=1

L=NLOW

LL=NHIGH+1

DO 60 K=L,LL

IF (LIMIT=2) 10,30,30

OM=PSI(K)

IF (OM.EQ.0.0) GO TO 20

IK=K

F1=PSI(K)/ROU(K)

OM=F1*OM

R(K)=IDSORT(8)*12.

RR=(R(K)/12.)*2

10

G 1
G 3
G 6
G 7
G 8
G 9
G 10
G 11
G 13
G 14
G 15
G 16
G 17
G 18
G 19
G 20
G 21


```

SP=UM*RU(K)*RR/PSI(K)
FO=FI
INIT=10
GO TO 40
20 R(K)=0.0
B=0.0
FO=0.0
SP=0.0
GO TO 40
30 IK=K
FI=PSI(K)/ROU(K)
BR=(FO+FI)*NPSI
B=B+BR
R(K)=(DSORT(B))*I2.
RR=(R(K)/I2.)*Z
IF (PSI(K).EQ.0.0) GO TO 70
SP=UM*RR(K)*RR/PSI(K)
FO=FI
40 IF (IN.EQ.0) GO TO 50
AP(K)=.5*(SP+APR(K))
GO TO 60
50 APR(K)=SP
AP(K)=SP
60 CONTINUE
RETURN
70 WRITE (6,RO) K,LL,ZX,OU(K)
STOP
C
80 FORMAT (//,I14)INTEG. STOP,3X,3(2X,I4),2(3X,F15.8)
END
SUBROUTINE SETUP (RUP)
IMPLICIT REAL*8(A-H,O-Z)
COMMON R(51),S(51),U(51),V(14,51),ROU(51),I(51),PSI(51)
COMMON UPR(51),YPR(14,51),HST(51),HT(51),T(51),T(51),HTPR(51)
COMMON CM(51),X(14,51),AP(51),APR(51),U(51),U(51),RMUE,RMUD,TEI,TEU
COMMON MEI,HEO,CMEI,CMD,DPSI,NNN,NEL,NEU
COMMON ZUPSET/ AT(51),BT(51),CT(51),DT(14,51),VT(14,51),ALP(51),RAK,A
ISKA,RIK,PIK,IKS,IK,IA,KO,KOR
COMMON /SAX/ ZX,UM
Q=RP
I=K-1
DO 50 K=1,IKS

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G 23
G 24
G 25
G 26
G 27
G 28
G 29
G 30
G 31
G 32
G 33
G 34
G 35
G 36
G 37
G 38
G 40
G 41
G 42
G 43
G 44
G 45
G 46
G 47
G 48
G 49
G 50
G 51
G 52-
H 1
H 5
H 8
H 9
H 10
H 11

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```

I=I+1
IF (K.EQ.1) GO TO 10
IF (K.EQ.1K5) GO TO 40
A(I)=0*(AP(I)-.25*AP(I+1)+.25*AP(I-1))
B(I)=2.*(PSI(I)+AP(I)*Q)
C(I)=Q*(AP(I)+.25*AP(I+1)-.25*AP(I-1))
BAK=2.*(PSI(I)-AP(I)*Q)
D(I,I)=A(I)*UPR(I-1)+BAK*UPR(I)+C(I)*UPR(I+1)
ALP(I)=B(I)-A(I)*C(I-1)/ALP(I-1)
V(I,I)=D(I,I)+A(I)*V(I,I-1)/ALP(I-1)
GO TO 50
10 A(I)=0.0
IF (K.EQ.1) GO TO 20
B(I)=2.*(PSI(I)+AP(I)*Q)
C(I)=Q*(AP(I)+.25*AP(I+1)-.25*AP(I-1))
ASKA=Q*(AP(I)-.25*AP(I+1)+.25*AP(I-1))
BAK=2.*(PSI(I)-AP(I)*Q)
D(I,I)=2.*ASKA*UEI+BAK*UPR(I)+C(I)*UPR(I+1)
GO TO 30
20 B(I)=1.+2.*UM*Q
C(I)=2.*UM*Q
D(I,I)=1.-2.*UM*Q)*UPR(I)+C(I)*UPR(I+1)
ALP(I)=B(I)
V(I,I)=D(I,I)
GO TO 50
40 C(I)=0.0
A(I)=Q*(AP(I)-.25*AP(I+1)+.25*AP(I-1))
B(I)=2.*(PSI(I)+AP(I)*Q)
BOK=2.*(PSI(I)-AP(I)*Q)
PISK=Q*(AP(I)+.25*AP(I+1)-.25*AP(I-1))
D(I,I)=A(I)*UPR(I-1)+BOK*UPR(I)+2.*PISK*UEO
ALP(I)=B(I)+A(I)*C(I-1)/ALP(I-1)
V(I,I)=D(I,I)+A(I)*V(I,I-1)/ALP(I-1)
50 CONTINUE
DO 60 I=K,IA
60 CONTINUE
KOR=10
RETURN
C
END
SUBROUTINE SETYP (RUP)
IMPLICIT REAL*8(A-H,O-Z)
COMMON R(SI),S(SI),U(SI),V(I+1),R(U(SI)),I(SI),PSI(SI)

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H 12
H 13
H 14
H 15
H 16
H 17
H 18
H 19
H 20
H 21
H 22
H 23
H 24
H 25
H 26
H 27
H 28
H 29
H 30
H 31
H 32
H 33
H 34
H 35
H 36
H 37
H 38
H 39
H 40
H 41
H 42
H 43
H 44
H 45
H 46
H 47
H 48
H 49
H 50
H 51
I 1

1
6
30
40
50
60
C

```

COMMON UPR(51),YPR(14,51),HST(51),HT(51),YPR(51),HTPR(51)
COMMON CRT(51),X(14,51),AP(51),APR(51),UEO,DEF,RRDE,RRDD,TEI,TEO
COMMON HEI,HEO,CMEI,CMO,DPSI,NNN,NEL,NEU
COMMON ZUPSET/ A(51),B(51),C(51),D(14,51),*(14,51),ALP(51),BAK,QA
ISKA,BUK,PISK,IKS,IK,IA,KQ,KOR
COMMON /SYLT/ E(14,51)
COMMON /ZZZ/ISP,IRE,IMU
COMMON /SU/ DELX
COMMON /YP/ YET(14),YEO(14)
COMMON /SAX/ ZX,UM
DATA CN/I,ODD/
Q=RP
I=IK-1
DO 100 K=1,IKS
I=I+1
IF (K.EQ.1) GO TO 20
IF (K.EQ.IKS) GO TO 80
A(I)=CN*A(I)
R(I)=2.*(PST(I)+AP(I))*Q*CN)
C(I)=CN*C(I)
BAK=2.*(PST(I)-AP(I))*Q*CN)
ALP(I)=B(I)-A(I)*C(I-1)/ALP(I-1)
DAX=2.*(PST(I)*DELX
ON 10 J=1,ISP
D(J,I)=A(I)*YPR(J,I-1)+BAK*YPR(J,I)+C(I)*YPR(J,I+1)+F(J,I)*DAX
GO TO 100
A(I)=0.0
IF (K.EQ.1) GO TO 40
R(I)=2.*(PST(I)+AP(I))*Q*CN)
C(I)=CN*C(I)
ASKA=CN*ASKA
BAK=2.*(PST(I)-AP(I))*Q*CN)
DAX=2.*(PST(I)*DELX
DAX=2.*(PST(I)*DELX
ON 30 J=1,ISP
D(J,I)=2.*ASKA*YET(I)+BAK*YPR(J,I)+C(I)*YPR(J,I+1)+F(J,I)*DAX
GO TO 60
R(I)=1.+2.*UM*CN*Q
C(I)=2.*UM*CN*Q
DO 50 J=1,ISP
D(J,I)=(I.-2.*UM*CN*Q)*YPR(J,I)+C(I)*YPR(J,I+1)+E(J,I)*DELX
ALP(I)=R(I)

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70 DO 70 J=1,ISP
   V(J,I)=D(J,I)
   GO TO 100
80 C(I)=0.0
   A(I)=CN*A(I)
   B(I)=2.*(PSI(I)+AP(I)*Q*CN)
   BUK=2.*(PSI(I)-AP(I)*Q*CN)
   PISK=CN*PISK
   ALP(I)=B(I)-A(I)*C(I-1)/ALP(I-1)
   DAX=2.*PSI(I)*DELX
   DO 90 J=1,ISP
     D(J,I)=A(I)*YPR(J,I-1)+BUK*YPR(J,I)+ PISK*YEN(J)+E(J,I)*DAX
     I+PISK*YPR(J,I)
90 V(J,I)=D(J,I)+A(I)*V(J,I-1)/ALP(I-1)
100 CONTINUE
   DO 110 I=IK,IA
110 CONTINUE
   KDR=0
   RETURN
C
4 8 END
SUBROUTINE SETHP (RUP)
IMPLICIT REAL*8(A-H,O-Z)
COMMON R(51),S(51),U(51),Y(14,51),R0U(51),T(51),PST(51)
COMMON UPR(51),YPR(14,51),HST(51),HT(51),TPR(51),HTPR(51)
COMMON CMT(51),X(14,51),API(51),APR(51),UEO,UEI,RHNE,RHDO,TEI,TEO
COMMON HEI,HEO,CMEI,CMO,DPST,NNN,NEL,NEU
COMMON /UPSET/ A(51),B(51),C(51),D(14,51),V(14,51),ALP(51),BAK,A
ISKA,BUK,PISK,IKS,IK,IA,KO,SKR
COMMON /SAX/ ZX,UM
DATA CN/1.0D0/
Q=RP
I=IK-1
DO 50 K=1,IKS
  I=I+1
  IF (K.EQ.1) GO TO 10
  IF (K.EQ.IKS) GO TO 40
  BAK=2.*(PSI(I)-AP(I)*Q*CN)
  D(I,I)=A(I)*HTPR(I-1)+BAK*HTPR(I)+C(I)*HTPR(I+1)
  V(I,I)=D(I,I)+A(I)*V(I,I-1)/ALP(I-1)
  GO TO 57
10 IF (K.EQ.1) GO TO 20
  BAK=2.*(PSI(I)-AP(I)*Q*CN)

```

I 45
 I 46
 I 47
 I 48
 I 49
 I 50
 I 51
 I 52
 I 53
 I 55
 I 56
 I 57
 I 58
 I 59
 I 60
 I 61
 I 62
 I 63=
 J 1
 J 5
 J 8
 J 9
 J 10
 J 11
 J 12
 J 13
 J 14
 J 15
 J 16
 J 17
 J 18
 J 19
 J 20

```

ASKA=0*(AP(I))-0.25*AP(I+1)+.25*AP(I-1))*CN
D(I,I)=2.*ASKA*HEI+HAK*HTPR(I)+C(I)*HTPR(I+I)
GO TO 30
20 D(I,I)=(I.-2.*UM*Q*CN)*HTPR(I)+C(I)*HTPR(I+I)
30 V(I,I)=D(I,I)
40 BUK=2.*(PSI(I)-AP(I))*Q*CN)
PTSK=Q*(AP(I)+.25*AP(I+1)-.25*AP(I-1))*CN
D(I,I)=A(I)*HTPR(I-1)+BUK*HTPR(I)+2.*PTSK*HEO
V(I,I)=D(I,I)+A(I)*V(I,I-1)/ALP(I-1)
50 CONTINUE
DO 60 I=K,IA
60 CONTINUE
KOR=+IO
RETURN
C
END
SUBROUTINE GAUSS
IMPLICIT REAL*8(A-H,O-Z)
DIMENSION G(14),CW(14)
DIMENSION NE(3), NO(3)
COMMON R(51),S(51),U(51),V(14,51),ROU(51),T(51),PSI(51)
COMMON UPRT(51),YPR(14,51),HST(51),HT(51),TPR(51),HTPR(51)
COMMON CM(51),X(14,51),AP(51),APR(51),UED,UEI,RHUE,RHOO,TEI,TEO
COMMON HEI,HEO,CHEI,CMO,DPSI,NNN,NEL,NEU
COMMON ZOPSET/ AT(51),BT(51),CT(51),DT(14,51),VT(14,51),ALP(51),YAK,A
ISKA,BUK,PTSK,IKS,IK,IA,KO,KOR
COMMON /SSS/ TAP
COMMON /NOO/ ZZ(51)
COMMON /ZZZ/ TSP,IRE,IMU
COMMON /GEN/ KRISE
DATA TOL/1.00E-04/
DATA CW/1.008,16.0,18.016,17.008,32.0,2.016,28.016,14.008,30.008,
1 44.016,46.004,28.011,44.011,142.286/
IF(NOT(3).LT.1A) GO TO 1
WRITE(6,310) NO(1),NO(2),NO(3)
NO(3)=0
1 I=IA+1
KAS=-IO
KOS=-IO
IF (KOR) IO,70,170
DO 60 M=1,IKS
IR=IR-1

```

J 21

J 22

J 23

J 24

J 25

J 26

J 27

J 28

J 29

J 30

J 31

J 32

J 33

J 34

J 35

J 36

J 37

K 1

K 3

K 7

K 10

K 11

K 14

K 15

K 16

K 17

K 18

```

IF (M.EQ.1) GO TO 20
U(I,B)=V(I,I,B)+C(I,B)*U(I,B+1))/ALP(I,B)
GO TO 30
20 U(I,B)=V(I,I,B)/ALP(I,B)
30 CONTINUE
IF (KOS.GT.0) GO TO 40
IF (DABS(U(I,B)-UE0)/UE0.GT.TOL) GO TO 50
40 CONTINUE
IF (KAS.GT.0) GO TO 60
IF (DABS(U(I,B)-UE1)/UE1).GT.TOL) GO TO 60
KAS=10
NF(I)=IR
GO TO 80
50 NF(I)=IR
KOS=10
60 CONTINUE
IF (KAS.LT.0) NF(I)=IK
GO TO 300
70 DO 160 M=1,IKS
IR=IR-1
IF (M.EQ.1) GO TO 90
DO 80 J=1,I,ISP
Y(J,IR)=V(J,I,B)+C(I,B)*Y(J,IR+1))/ALP(I,B)
80 CONTINUE
GO TO 110
90 DO 100 J=1,I,ISP
Y(J,IR)=V(J,I,B)/ALP(I,B)
100 CONTINUE
110 CONTINUE
CM(I,B)=0.0
GM=0.0
DO 120 J=1,I,ISP
G(J)=Y(J,I,B)/CW(J)
120 GM=(M+G(J))
DO 130 J=1,I,ISP
X(J,IR)=G(J)/GM
130 CM(I,IR)=CM(I,IR)+X(J,IR)*CW(J)
IF (M.PQ.1) GO TO 160
IF (KOS.GT.0) GO TO 140
IF (DABS(CM(I,B)-CMD)/CMD.GT.TOL) GO TO 150
140 CONTINUE
IF (KAS.GT.0) GO TO 160
IF (DABS(CM(I,B)-CME1)/CME1.GT.TOL) GO TO 160

```

K 19
K 20
K 21
K 22
K 24
K 25
K 26
K 27
K 28
K 29
K 30
K 31
K 32
K 33
K 34
K 35
K 36
K 38
K 39
K 40
K 41

K 43
K 44
K 45

K 47
K 48
K 49
K 50
K 51

K 53
K 54

K 56
K 57

K 58
K 59

K 60
K 61
K 62

```

NE(2)=IR
KAS=+10
GO TO 160
150 ND(2)=IR
KOS=+10
CONTINUE
IF (KAS.LT.0) NE(2)=K
GO TO 300
170 DO 220 M=1,IKS
IA=IS-1
IF (M.EQ.1) GO TO 180
HT(18)=(V(1,18)+C(18)*HT(19+1))/ALP(18)
HST(18)=HT(18)-(U(18)**2)/(2.*32.17*778.16)
GO TO 190
180 HT(18)=V(1,18)/ALP(18)
HST(18)=HT(18)-(U(18)**2)/(2.*32.17*778.16)
GO TO 220
190 CONTINUE
IF (KOS.GT.0) GO TO 200
IF (DABS(HT(19)-HEI)/HEI).GT.10L) GO TO 210
CONTINUE
IF (KAS.GT.0) GO TO 220
IF (DABS(HT(19)-HEI)/HEI).GT.10L) GO TO 220
KAS=+10
NF(3)=IR
GO TO 220
210 ND(3)=IR
KOS=+10
CONTINUE
IF (KAS.LT.0) NE(3)=K
IF (NF(1).EQ.1.OR.NE(2).EQ.1.OR.NE(3).EQ.1) KQ=+10
IF (NE(1).LT.NE(2)) GO TO 230
NU=NE(2)
GO TO 240
230 NU=NE(1)
240 IF (NU.LT.NE(3)) GO TO 250
NFL=1
GO TO 260
250 NFL=1
260 IF (ND(1).GT.ND(2)) GO TO 270
ND=ND(2)
GO TO 280
270 ND=ND(1)

```

K 63

K 64

K 65

K 66

K 67

K 68

K 69

K 71

K 72

K 73

K 74

K 75

K 76

K 77

K 78

K 79

K 80

K 81

K 82

K 84

K 85

K 86

K 87

K 88

K 89

K 90

K 91

K 92

K 95

K 96

K 97

K 98

K 99

K 100

K 101

K 103

K 105

K 106

K 107

K 108

```

280 IF (MU.GT.NN(3)) GO TO 290          K 109
IAP=NN(3)
GO TO 300          K 111
290 IAP=MU          K 113
IF (NEL.EQ.1) KO=+10
MN=NEU+3-1A
IF (1A.GT.0) GO TO 300
72=1A-4
MNPI=MN+1
ON 600 KK=I,MNPI
600 ZZ(I0+MN)=ZX/12.
300 RETURN
C
310 FORMAT (2X,5HGAUSS,2X,3I10)          K 114
320 FORMAT (2X,14,4F22.10)          K 115
END          K 116
SUBROUTINE CHANGE(IMP)          K 117
IMPLICIT REAL*8(A-H,O-Z)
COMMON R(51),S(51),D(51),Y(14,51),ROU(51),T(51),PSI(51)
COMMON UPR(51),YPR(14,51),HST(51),HT(51),TPRT(51),HTPR(51)
COMMON CM(51),X(14,51),AP(51),APR(51),UEI,UEI,RHUE,RHUE,TEI,TEI
COMMON HFI,HEO,CMEI,CMO,DPSI,NNN,NEL,NEI
COMMON/SAX/ ZX,UM          L 5
COMMON / RRR/ TO(51)
COMMON /UUU/ ZZ(51)
COMMON/ZZZ/ISP,IRE,IMU
COMMON /SU/ DELX          L 6
COMMON /VVV/ VO(51)
COMMON /SA/ AREX          L 7
PSA=PSI(NNN)
NNN=(NNN-1)/2+1
DPSI=PSA/(NNN-1)
DAX=DELX*12.
ZX=ZX
UX=(ZX/12.)*DELX          L 11
ARFX=DELX          L 13
RUP=DELX/(DPSI**2)          L 15
OIX=DELX*12.
OX=OX*DELX
ZIX=OX*12.
ZX=ZIX
ON 40 MI=1,NNN
14 ((MI-2).LT.0) GO TO 30          L 19
          L 20

```



```

MA=MA+2
10  PST(MI)=PSI(MA)
    AP(MI)=AP(MA)
    APR(MI)=APR(MA)
    R(MI)=R(MA)
    U(MI)=U(MA)
    UPR(MI)=UPR(MA)
    HT(MI)=HT(MA)
    HTPR(MI)=HTPR(MA)
    VO(MI)=VO(MA)
    TU(MI)=TU(MA)
    ZZ(MI)=ZZ(MA)
    S(MI)=S(MA)
    T(MI)=T(MA)
    TPR(MI)=TPR(MA)
    DO 20 J=1,ISP
    Y(J,MI)=Y(J,MA)
    YPR(J,MI)=YPR(J,MA)
    GO TO 40
30  MA=1
    GO TO 10
40  CONTINUE
    NIL=NEL/2+1
    NIU=NEU/2+1
    NEL=NIL
    NEU=NIU
    WRITE (6,50)
    WRITE (6,60) NEL,NEU
    WRITE (6,70) ZAX,DAX,ZIX,DIK
    RETURN
C
50  FORMAT (77,2X,20HR, OF POINTS HALVED)
60  FORMAT (2X,5HNEU=,I5,5HNEU=,I5)
70  FORMAT (2X,4HZAX=,F14,10,2X,4HDAX=,F14,10,2X,4HZIX=,F14,10,2X,4HDI
    IX=,F14,10,777)
    END
SUBROUTINE PRINT (KUSK,KUN)
IMPLICIT REAL*8(A-H,O-Z)
COMMON R(51),S(51),U(51),Y(14,51),RDU(51),T(51),PSI(51)
COMMON UPR(51),YPR(14,51),HST(51),HT(51),TPR(51),HTPR(51)
COMMON CM(51),X(14,51),AF(51),APR(51),UEU,DEI,RHOU,TEI,TEU
COMMON HEI,HEU,CMEI,CMU,DPST,NNN,NFL,NEU
COMMON /SAX/ ZX,UM
M 1
M 5
M 6

```

L 21
L 22
L 23
L 24
L 25
L 26
L 27
L 28
L 29

L 30
L 31
L 32

L 34
L 35
L 36
L 37
L 38
L 39
L 40
L 41
L 42
L 43
L 44
L 45
L 46
L 47
L 48
L 49
L 50
L 51
L 52
L 53-
M 1

M 5
M 6

```

COMMON /UPSET/ A(51),B(51),C(51),D(14,51),V(14,51),ALP(51),9AK,A
ISKA,BUK,PISK,IKS,IA,IA,KO,KOR
COMMON/ZZZ/ISP,IRE,IMU
COMMON /SU/ DELX
COMMON /SIG/ PATI,I4),PT(I4),WT(I4,51)
COMMON /SYLT/ E(14,51)
Z=ZX/12.

```

```

WRITE (6,30) Z,ZX,DELX,DPST,NEL,NEU,IKS,KUSK,KUN
DO 20 I=1K,1A
YTOT=0.0
DO 10 J=1,I,ISP

```

```

10 YTOT=YTOT+Y(J,I)
WRITE (6,40) I,PSI(I),R(I),S(I),U(I),AP(I),APR(I),HT(I)
WRITE (6,50) I,(Y(J,I),J=1,ISP)
WRITE (6,50) I,(W(J,I),J=1,ISP)
WRITE (6,50) I,(E(J,I),J=1,ISP)
WRITE (6,60) I,(YTOT,GM(I),ROU(I)

```

```

20 CONTINUE
WRITE(6,60) KQ,UM
RETURN

```

54

```

C 30 FORMAT ('1',777,4(2X,F15.10),5(3X,F5),7H OUTPUT,777)
C 40 FORMAT (7,2X,I4,7(2X,E14.7))
C 50 FORMAT (2X,I4,7(2X,E14.7),6X,7(2X,E14.7))
C 60 FORMAT (2X,I4,3(2X,E14.7))
END

```

```

SUBROUTINE CHEMTE (KRY5,KRAS,IJ)
SPECIE PRODUCTION SUBROUTINE -W/(RHO)*U - I./FEET
C INPUT REQD. PRESSURE(ATOM),AXIAL STEP SIZE(FT),NR. OF RADIAL MESH
C POINTS(NNN),TEMP(DEG.K) AND SPECIE MASS FRACTIONS
C REACTIONS CONSIDERED: H + O2 = OH + O (1)
C O + H2 = OH + H (2)
C H2 + OH = H + H2O (3)
C 2OH = O + H2O (4)
C H2 + M = 2H + M (5)
C H2O + M = OH + H + M (6)
C OH + M = O + H + M (7)
C O2 + M = 2O + M (8)
C H2 + O2 = OH + OH (9)

```

```

C FRY5 = -VEY FROZEN FLOW
C FRY5 = +VEY FINITE RATE CHEMISTRY
IMPLICIT REAL*(A-H,O-Z)
DIMENSION CW(18), AU(22), E(22), D(22), A(22)

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```

DIMENSION C(22), G(18)
DIMENSION AF(22), BF(22), AB(22), BB(22)
DIMENSION Z(18), F(22), R(22), RW(22), FW(22), BW(22), CR(22)
DIMENSION PRT(22), PK(18,22)
DIMENSION GNUP(14,17), GNUR(14,17)
COMMON R(51), S(51), U(51), V(14,51), Y(14,51), ROU(51), T(51), PSI(51)
COMMON UPR(51), YPR(14,51), HST(51), HT(51), TPR(51), HTPR(51)
COMMON CH(51), X(14,51), AP(51), APR(51), UEO, UEI, RHUE, RHUO, TEI, YEO
COMMON WEI, HEO, CMET, CMU, DPSI, NNN, NEL, NEU
COMMON /SIG/ PA(14,14), PT(14), W(14,51)
COMMON /UUD/ ZZ(51)
COMMON /ZZZ/ ISP, IRE, IMU
COMMON /VYV/ IZE
COMMON /SU/ DELX
COMMON /SAX/ ZX, UM
COMMON /RRR/ TO(51)
COMMON /XXX/ TAU
COMMON /VVV/ YO(51)
KF=KRY$+KRAS
P=1.00
IF (KF.LT.0) GO TO 50
CNV=453.5924/(30.4801**3)
CNV2=CNV**2
READ(5,600) (CH(J), J=1,ISP)
WRITE(6,700) (CH(J), J=1,ISP)
READ(5,601) (AU(K), K=1,IRE)
WRITE(6,701) (AU(K), K=1,IRE)
READ(5,601) (CU(K), K=1,IRE)
WRITE(6,701) (CU(K), K=1,IRE)
READ(5,602) (E(K), K=1,IRE)
WRITE(6,702) (E(K), K=1,IRE)
READ(5,602) (U(K), K=1,IRE)
WRITE(6,702) (U(K), K=1,IRE)
WRITE(6,703)
READ(5,605) ((GNUP(J,K), J=1,ISP), K=1,IRE)
WRITE(6,705) GNUP
READ(5,605) ((GNUR(J,K), J=1,ISP), K=1,IRE)
WRITE(6,705) GNUR
605 FORMAT(1F10.0)
705 FORMAT(2X,7F12.5)
      DN 5 K=1,IRE
      5 READ(5,606) AF(K), BF(K), AB(K), BB(K)
      606 FORMAT(4F10.0)

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```

READ(5,606) EN
IMP=IMP+1
DO 1 I=1,IRE
A(I)=DLOG(AU(I)*CNV)
IF(I.GT.4.AND.I.LT.IMP) GO TO 2
C(I)=DLOG(CU(I)*CNV)
GO TO 1
2 C(I)=DLOG(CU(I)*CNV2)
1 CONTINUE
A(IRE)=DLOG(AU(IRE))
C(IRE)=DLOG(CU(IRE))
GO TO 20
50 I=J
IF (KRAS.EQ.0) GO TO 401
TO(I)=TO(I)+.5*DELX*(I./U(I)+1./UPR(I))
401 CONTINUE
P=1.
GM=0.0
DO 10 J=1,ISP
G(J)=Y(J,I)/CW(J)
5 10 GM=GM+G(J)
SM=0.0
DO 11 J=1,ISP
Z(J)=G(J)/GM
11 SM=SM+Z(J)*CW(J)
RM=1545.3/SM
RMP=2116.2/(RMP+I)*I*.8)
DO 13 LK=1,IRE
F(LK)=DEXP(A(LK))-E(LK)/I(I)
B(LK)=DEXP(C(LK))-D(LK)/I(I)
13 CONTINUE
B(5)=B(5)/I(I)
F(7)=F(7)/I(I)*0.5)
F(8)=F(8)/I(I)
F(9)=F(9)/I(I)*I*.5)
F(11)=F(11)/I(I)
F(13)=F(13)*I(I)
B(13)=B(13)*I(I)
F(15)=F(15)*I(I)*0.5)
B(15)=B(15)*I(I)*0.5)
F(17)=F(17)*(P**0.3)*I(I)/I(I)*0-0.5)
FW(I)=F(I)*R0*G(I)*G(5)
BW(I)=B(I)*R0*G(4)*G(2)

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FW(2)=F(2)*R0*G(6)*G(2)
RW(2)=B(2)*R0*G(4)*G(1)
FW(3)=F(3)*R0*G(6)*G(4)
RW(3)=B(3)*R0*G(1)*G(3)
FW(4)=F(4)*R0*G(4)*G(4)
RW(4)=B(4)*R0*G(3)*G(2)
FW(5)=F(5)*R0*G(6)*GM
RW(5)=B(5)*R0*R0*G(1)*G(1)*GM
FW(6)=F(6)*R0*G(3)*GM
RW(6)=B(6)*R0*R0*G(4)*G(1)*GM
FW(7)=F(7)*R0*G(7)*GM
RW(7)=B(7)*R0*R0*G(9)*G(8)*GM
FW(8)=F(8)*R0*G(5)*GM
RW(8)=B(8)*R0*R0*G(2)*G(2)*GM
FW(9)=R0*G(9)*GM*F(9)
RW(9)=B(9)*R0*R0*G(8)*G(2)*GM
FW(10)=F(10)*R0*G(10)*GM
RW(10)=B(10)*R0*R0*G(7)*G(2)*GM
FW(11)=F(11)*R0*G(11)*GM
RW(11)=B(11)*R0*R0*G(9)*G(2)*GM
FW(12)=F(12)*R0*G(12)*G(4)
RW(12)=B(12)*R0*G(13)*G(1)
FW(13)=F(13)*R0*G(9)*G(2)
RW(13)=B(13)*R0*G(5)*G(8)
FW(14)=F(14)*R0*G(9)*G(8)
RW(14)=B(14)*R0*G(7)*G(2)
FW(15)=F(15)*R0*G(9)*G(5)
RW(15)=B(15)*R0*G(11)*G(2)
FW(16)=F(16)*R0*G(9)*G(9)
RW(16)=B(16)*R0*G(10)*G(2)
FW(17)=F(17)*R0*G(14)*G(5)
IF(4*PR(I).GE.5.02) GO TO R0
ZZ(I)=ZX/I2.
TO(I)=0.
IF(T(I).LT.6.02) GO TO I7
R0 CONTINUE
IF(TO(I).GE.TAU) GO TO I7
FW(I7)=VO(I)*1.57*TAU*(DSORT(I)-TO(I)/TAU)/CH(I4)
GO TO I8
I7 FW(I7)=0.
I8 RW(I7)=0.02
IF(IZE.GT.0) FW(I7)=0.
DO 15 M=1,IAE

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```

CR(M)=FW(M)-BW(M)
PR(M)=(FW(M)*(AF(M)-BF(M))*T(I)+E(M))-BW(M)*(AR(M)-BR(M))*T(I)+
ID(M))/T(I)**2)
15 CONTINUE
PRT(I)=FW(IRE)*I.0/T(I)-555.5)+E(I)/T(I)**2)
PRT(I)=0.
IF(IZE.GT.0) PRT(I)=0.
I=(KRAS.GT.0) GO TO 3
IREM=IRE-1
DO 71 II=1,IISP
DO 71 J=1,IREM
PK(II,J)=FW(J)*(GNUM(II,J)/G(II)-BF(J)*SM)-BW(J)*(GNUM(II,J)/G(II
I))-BR(J)*SM)
IF(J.GE.5.AND.J.LE.10) GO TO 72
GO TO 71
72 PK(II,J)=PK(II,J)+(FW(J)-BW(J))/GM
71 PK(II,J)=PK(II,J)/G(II)
DO 73 II=1,IISP
PK(II,IRE)=0.0
5 73 CONTINUE
88 IF(IZE.GT.0) GO TO 3
3 CONTINUE
IF(KRAS.EQ.0) GO TO 4
W(1,1)=CW(1)*(-CR(1)+CR(2)+CR(3)+2.0*CR(5)+CR(6)+CR(12))
W(2,1)=CW(2)*(CR(1)-CR(2)+CR(4)+2.0*CR(8)+CR(9)+CR(10)+CR(11)-CR(1
13)+CR(14)+CR(15)+CR(16))
W(3,1)=CW(3)*(CR(3)+CR(4)-CR(6))
W(4,1)=CW(4)*(CR(1)+CR(2)-CR(3)-2.0*CR(4)+CR(6)-CR(12))
W(5,1)=CW(5)*(-CR(1)-CR(8)+CR(13)-CR(15)-EN/2.0*CR(17))
W(6,1)=CW(6)*(-CR(2)-CR(3)-CR(5)+(EN+1.0)*CR(17))
W(7,1)=CW(7)*(-CR(7)+CR(10)+CR(14))
W(8,1)=CW(8)*(2.0*CR(7)+CR(9)+CR(13)-CR(14))
W(9,1)=CW(9)*(-CR(9)+CR(11)-CR(13)-CR(14)-CR(15)-2.0*CR(15))
W(10,1)=CW(10)*(-CR(10)+CR(16))
W(11,1)=CW(11)*(-CR(11)+CR(15))
W(12,1)=CW(12)*(-CR(12)+EN*CR(17))
W(13,1)=CW(13)*CR(12)
W(14,1)=CW(14)*(-EN*CR(17))
IF(KRAS.GT.0) GO TO 20
4 CONTINUE
PT(1)=CW(1)*(-PRT(1)+PRT(2)+PRT(3)+2.0*PRT(5)+PRT(6)+PRT(12))
PT(2)=CW(2)*(PRT(1)-PRT(2)+PRT(4)+2.0*PRT(8)+PRT(9)+PRT(10)+PRT(11
1)-PRT(13)+PRT(14)+PRT(15)+PRT(16))

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```

PY(3)=CW(3)*PRT(3)+PRT(4)-PRT(6))
PY(4)=CW(4)*PRT(1)+PRT(2)-PRT(3)-2.0*PRT(4)+PRT(6)-PRT(12))
PT(5)=CW(5)*(-PRT(1)-PRT(8)+PRT(13)-PRT(15)-EN/2.0*PRT(17))
PT(6)=CW(6)*(-PRT(2)-PRT(3)-PRT(5)+EN+1.0)*PRT(17))
PT(7)=CW(7)*(-PRT(7)+PRT(10)+PRT(14))
PT(8)=CW(8)*2.0*PRT(7)+PRT(9)+PRT(13)-PRT(14))
PT(9)=CW(9)*(-PRT(9)+PRT(11)-PRT(13)-PRT(14)-PRT(15)-2.0*PRT(16))
PT(10)=CW(10)*(-PRT(10)+PRT(16))
PY(11)=CW(11)*(-PRT(11)+PRT(15))
PY(12)=CW(12)*(-PRT(12)+EN*PRT(17))
PY(13)=CW(13)*PRT(12))
PY(14)=CW(14)*(-PRT(17))
DO 21 L=1,15
PA(L,1)=CW(1)*(-PK(L,1)+PK(L,2)+PK(L,3)+2.0*PK(L,5)+PK(L,6)+PK(L,12))
PA(L,2)=CW(2)*(PK(L,1)-PK(L,2)+PK(L,4)+2.0*PK(L,8)+PK(L,9)+PK(L,10))
PA(L,3)=CW(3)*(PK(L,3)+PK(L,4)-PK(L,6))
PA(L,4)=CW(4)*(PK(L,1)+PK(L,2)-PK(L,3)-2.0*PK(L,4)+PK(L,6)-PK(L,12))
PA(L,5)=CW(5)*(-PK(L,1)-PK(L,8)+PK(L,13)-PK(L,15)-EN/2.0*PK(L,17))
PA(L,6)=CW(6)*(-PK(L,2)-PK(L,3)-PK(L,5)+EN+1.00)*PK(L,17))
PA(L,7)=CW(7)*(-PK(L,7)+PK(L,10)+PK(L,14))
PA(L,8)=CW(8)*2.0*PK(L,7)+PK(L,9)+PK(L,13)+PK(L,14))
PA(L,9)=CW(9)*(-PK(L,9)+PK(L,11)-PK(L,13)-PK(L,14)-PK(L,15)-2.0*PK(L,16))
PA(L,10)=CW(10)*(-PK(L,10)+PK(L,16))
PA(L,11)=CW(11)*(-PK(L,11)+PK(L,15))
PA(L,12)=CW(12)*(-PK(L,12)+EN*PK(L,17))
PA(L,13)=CW(13)*PK(L,12))
PA(L,14)=CW(14)*(-PK(L,17))
21 CONTINUE
IF(KRYS.NE.-10) GO TO 20
20 CONTINUE
RETURN
600 FORMAT(7F10.0)
601 FORMAT(5E10.4)
602 FORMAT(9F8.0)
700 FORMAT(2X,7F14.4)
701 FORMAT(2X,9E14.4)
702 FORMAT(2X,9F14.2)
703 FORMAT(1V)

```

END

0.25000000E 01

0.25470497E 05

0.30218894E 01-0.21731249E-02 0.37542203E-05-0.29947200E-08

0.90777547E-12 0.29137190E 05

0.41565016E 01-0.17244334E-02 0.56982316E-05-0.45930044E-08

0.14233654E-11-0.30288770E 05

0.38234708E 01-0.11187229E-02 0.12466819E-05-0.21035896E-09

-0.52546551E-13 0.35852787E 04

0.37189946E 01-0.25167288E-02 0.85837353E-05-0.82998716E-08

0.27082180E-11-0.10576706E 04

0.28460849E 01 0.41932116E-02-0.96119332E-05 0.95122662E-08

-0.33093421E-11-0.96725572E 03

0.36916148E 01-0.1332552E-02 0.26503100E-05-0.97688341E-09

-0.99772234E-13-0.10628336E 04

.2514793700E 01-.112457910E-03.2964750600E-06-.324640490E-09

.1239546500E-12.5612776700E 05

.4146947600E 01-.411972370E-02.9692246700E-05-.786336390E-08

.2230951200E-11.9744789400E 04

.2382117100E 01.1039055600E-01-.111676340E-04.6958316500E-08

-0.187801920E-11.8722996400E 04

.3434456300E 01.2223429700E-02.6714897500E-05-.974277190E-08

.3721252300E-11.2864789500E 04

.3787133200E 01-.217095280E-02.5075733700E-05-.347377280E-08

.7721684100E-12-.143635080E 05

.2170100000E 01.1037811500E-01-.107339380E-04.6345917500E-08

-0.162807010E-11-.483524020E 05

.7159908600E 02

-0.213479840E 05

0.25000000E 01

0.25470497E 05

0.25372567E 01-0.18422190E-04-0.88017921E-08 0.59643621E-11

-0.59743608E-15 0.29230007E 05

0.26707532E 01 0.30317115E-02-0.85351570E-06 0.11790853E-09

-0.61973968E-14-0.29888994E 05

0.28895544E 01 0.99839081E-03-0.21879904E-06 0.19802785E-10

-0.34452940E-15 0.38811792E 04

0.35976129E 01 0.78145803E-03-0.22386670E-06 0.42490159E-10

-0.33460204E-14-0.11927914E 04

0.30436897E 01 0.61187110E-03-0.73993551E-08-0.20331907E-10

0.24593791E-14-0.83491002E 03

0.28545761E 01 0.15978310E-02-0.62566234E-06 0.11315849E-09

-0.76897070E-14-0.89017449E 03

.2442226100E 01.1227618700E-03-.849927190E-07.2140083000E-10
 -.125110580E-14.5614882100E 05
 .3152936000E 01.1405995500E-02-.570784620E-06.1062820900E-09
 -.737207830E-14.9852204800E 04
 .4626547900E 01.3021680700E-02-.121560140E-05.2285595200E-09
 -.158497010E-13.8535664500E 04
 .4613921900E 01.2638663900E-02-.109485410E-05.201842500E-09
 -.146543910E-13 .234037800E 04
 .2951151900E 01.1552556700E-02-.619114110E-06.1135033600E-09
 -.77827320E-14-.142318270E 05
 .4412926600E 01.3192289600E-02-.129782300E-05.241474600E-09
 -.167429860E-13-.489440430E 05
 .7159908600E 02

-.213479840E 05

52097.7 59556.6 -57797.9 9312.5

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 258. 2100. 1.472
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13. ABSTRACT <p>An experimental and theoretical study has been made of the history of the pollutants carbon monoxide (CO), unburned hydrocarbons (HC) and nitrogen oxides (NO_x) in a turbojet afterburner. Experimental traverses at several axial stations were performed in a simulated afterburner in which exhaust from a J-47 combustor can, operated at medium power, was mixed with fuel spray. Experiments were carried out both in a non-bypass and in a bypass configuration (secondary air was mixed with primary exhaust). The non-bypass tests were carried out at high combustor efficiency, and yielded the following: CO = 300 ppm, HC < 10 ppm, NO_x = 100 ppm. In the bypass tests, fuel distribution was non-uniform and combustor efficiency was low. The concentrations obtained were CO = 10000 ppm, HC = 1000 ppm, NO_x = 100 ppm. The theoretical analysis consisted of a computer program for reacting flow with turbulent mixing. The computer program was very slow and therefore of limited usefulness in terms of cost and questionable results, since it could not be checked against experiment. Infrared measurements of NO in the combustion tunnel were attempted. Indications were obtained of NO at the 5.3 micron band, but quantitative measurements were not obtained.</p>			

14. KEY WORDS	LINK A		LINK B		LINK C	
	ROLE	WT	ROLE	WT	ROLE	WT
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