

AFAPL-TR-68-143

AD723653

**THEORETICAL DETERMINATION OF
CONVECTION HEAT-TRANSFER COEFFICIENTS
AROUND A TURBINE AIRFOIL
(WITH COMPUTER PROGRAM)**

**LUCIEN L. DEBRUGE
WALKER H. MITCHELL**

TECHNICAL REPORT AFAPL-TR-68-143

APRIL 1969



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DOCUMENT CONTROL DATA - R & D

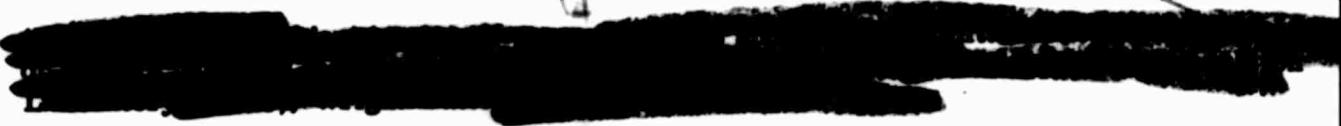
(Security classification of title, body of abstract and indexing annotation must be entered when the overall report is classified)

1. ORIGINATING ACTIVITY (Corporate author) Air Force Aero Propulsion Laboratory Wright-Patterson Air Force Base, Ohio 45433		2a. REPORT SECURITY CLASSIFICATION UNCLASSIFIED
2b. GROUP		
3. REPORT TITLE THEORETICAL DETERMINATION OF CONVECTION HEAT-TRANSFER COEFFICIENTS AROUND A TURBINE AIRFOIL (WITH COMPUTER PROGRAM)		
4. DESCRIPTIVE NOTES (Type of report and inclusive dates)		
5. AUTHOR(S) (First name, middle initial, last name) Lucien L. Debruge Walker H. Mitchell		
6. REPORT DATE April 1969	7a. TOTAL NO. OF PAGES 66	7b. NO. OF REFS 5
8a. CONTRACT OR GRANT NO.	9a. ORIGINATOR'S REPORT NUMBER(S) AFAPL-TR-68-143	
b. PROJECT NO. 3066	9b. OTHER REPORT NO(S) (Any other numbers that may be assigned this report)	
c. Task 306606		
11. SUPPLEMENTARY NOTES		
12. SPONSORING MILITARY ACTIVITY Air Force Aero Propulsion Laboratory Wright-Patterson Air Force Base, Ohio 45433		

13. ABSTRACT

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This report describes a theoretical prediction of the convection heat-transfer coefficient distribution on a test blade and the computer program for making the necessary calculations. The program is written in Fortran IV ready for an IBM 7094. The input and output are described. The program starts with the blade surface pressure distribution obtained experimentally and yields the heat-transfer coefficients on the blade contour.



DD FORM NOV 1968 1473

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Security Classification

UNCLASSIFIED

Security Classification

14. KEY WORDS	LINK A		LINK B		LINK C	
	ROLE	WT	ROLE	WT	ROLE	WT
Boundary Layer Convection Heat Transfer						

UNCLASSIFIED

Security Classification

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FOREWORD

The work on which this report is based was accomplished under Project 3066, "Gas Turbine Technology," Task 306606, "Turbine Research Exploratory Development," using the computer facilities of the Turbine Engine Division, Air Force Aero Propulsion Laboratory, Wright-Patterson Air Force Base, Ohio. This work was administered under the direction of Mr. Charles E. Bentz, Project Engineer.

This report describes work conducted between 1 July 1968 and 1 October 1968. Mr. Walker Mitchell was responsible for the development of the computer program and Mr. Lucien Debruge for the theoretical development and discussion. This report was submitted by the authors October 1968.

This technical report has been reviewed and is approved.



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SYMBOLS

A	channel cross-sectional area
A*	channel cross-sectional area at which Mach number is unity
C_f	turbulent coefficient of skin friction
C_p	specific heat at constant pressure
h	convection heat-transfer coefficient
H	velocity shape factor (turbulent boundary layer)
n	distance along velocity potential line
N_x	local Nusselt number
P	pressure
P_r	Prandtl number
r	radius
R	gas constant
T	temperature
V or U	velocity
V_{my}	mid channel reference velocity at a distance my from centerline of cascade
x	surface distance from stagnation point
y	distance along radial potential line
ρ	density
γ	ratio of specific heats
ν	kinematic viscosity
μ	viscosity
δ	boundary layer thickness
δ*	displacement thickness
δ**	boundary layer energy thickness
λ	velocity shape factor (laminar boundary layer)
θ	momentum thickness
τ	shearing stress

SUBSCRIPTS

m	refers to mid-channel conditions
CR	refers to critical condition
o	stage entrance conditions (cold flow)
l	stage entrance conditions (hot flow)
n	distance along velocity potential line
no	distance along potential line (cold flow)
nl	distance along potential line (hot flow)
S	static conditions
ad	adiabatic conditions

**SECTION I
INTRODUCTION**

Currently, the Air Force Aero Propulsion Laboratory is installing an in-house High-Temperature Test Facility which will be used initially to analyze various cooling techniques, as applied to turbine engine blades, over an extended gas temperature range. The objective is to evaluate these cooling schemes with respect to gas temperature and pressure levels. Experimental data will be correlated with the various theoretical predictions of blade cooling effectiveness, thus providing a basis for future high-temperature turbine blade designs.

The experimental data used is that obtained from the recording of surface metal temperatures by infrared thermometry. In the theoretical prediction of turbine blade temperatures, cooled or uncooled, the major steps are the calculation of the convection heat-transfer coefficients on the blade surface and the calculation of the driving or adiabatic wall temperatures. These calculations depend primarily on the accuracy with which the behavior of the boundary layer is predicted. It is generally assumed that the introduction of a cooling fluid in the boundary layer has a negligible effect on the convection heat-transfer coefficients, but it affects considerably the adiabatic or driving wall temperature.

This report presents a theoretical approach to the problem of determining the adiabatic wall temperatures and the convection heat-transfer coefficients .

This program is written in Fortran IV ready for use on an IBM 7094 for an uncooled blade and the computer program to which it led. The results obtained from the program developed here are compared with those from the computer program developed by the Allison Division of General Motors on Contract AF 33(615)-2985.

SECTION II

THEORY AND DISCUSSION

The velocity of a perfect, frictionless, compressible gas flowing through a channel, at any point across a potential line, is given by the equation

$$v = v_{my} \exp \left[-\frac{n}{2\Delta c} (c^2 - c_m^2) \right] \quad (1)$$

where, for a nonrotating channel,

$$v_{my} = v_{yo} \exp \left[\int_{yo}^y -\frac{1}{\Delta c} \sin^2 \phi dy \right] \quad (2)$$

is the mid channel velocity at a distance y from a reference point y_0 along a radial potential line and v_{yo} is the velocity at the reference point (Figure 1). It is seen from Equations 1 and 2 that V is strictly a function of channel geometry and v_{yo} .

In the computer program currently in use at AFAPL (Reference 1), v_{yo} is arbitrarily chosen; then, the fluid velocity and density are evaluated at specified locations along a velocity potential line, the latter being obtained from the equation

$$\rho_n = \rho_i \left\{ \left(1 - \left(\frac{\gamma-1}{\gamma+1} \right) \left(\frac{v_n}{v_{CR}} \right)^2 \right) \right\}^{\frac{1}{\gamma-1}} \quad (3)$$

Integration of the product $v_n \rho_n$ over a given channel cross section yields the total mass flow which is compared with the required flow (usually the maximum or choked flow). v_{yo} is improved until $\int_A \rho_n v_n dA$ (required flow) \leq tolerance. Use of this computer program

requires an accurate description of the channel configuration at each of the cross sections where the channel wall velocity must be obtained. Eleven cross sections are presently used to provide enough data for interpolation of the velocity profile along the channel walls between the stage entrance and the throat, beyond which extrapolation is depended upon to obtain the velocity profile. As inputs to the program, curvatures, length of velocity potential lines, and the angle between the gas stream direction upstream of stage entrance and the mid channel stream-line must be measured or calculated. A table of V/V_{cr} versus axial chord

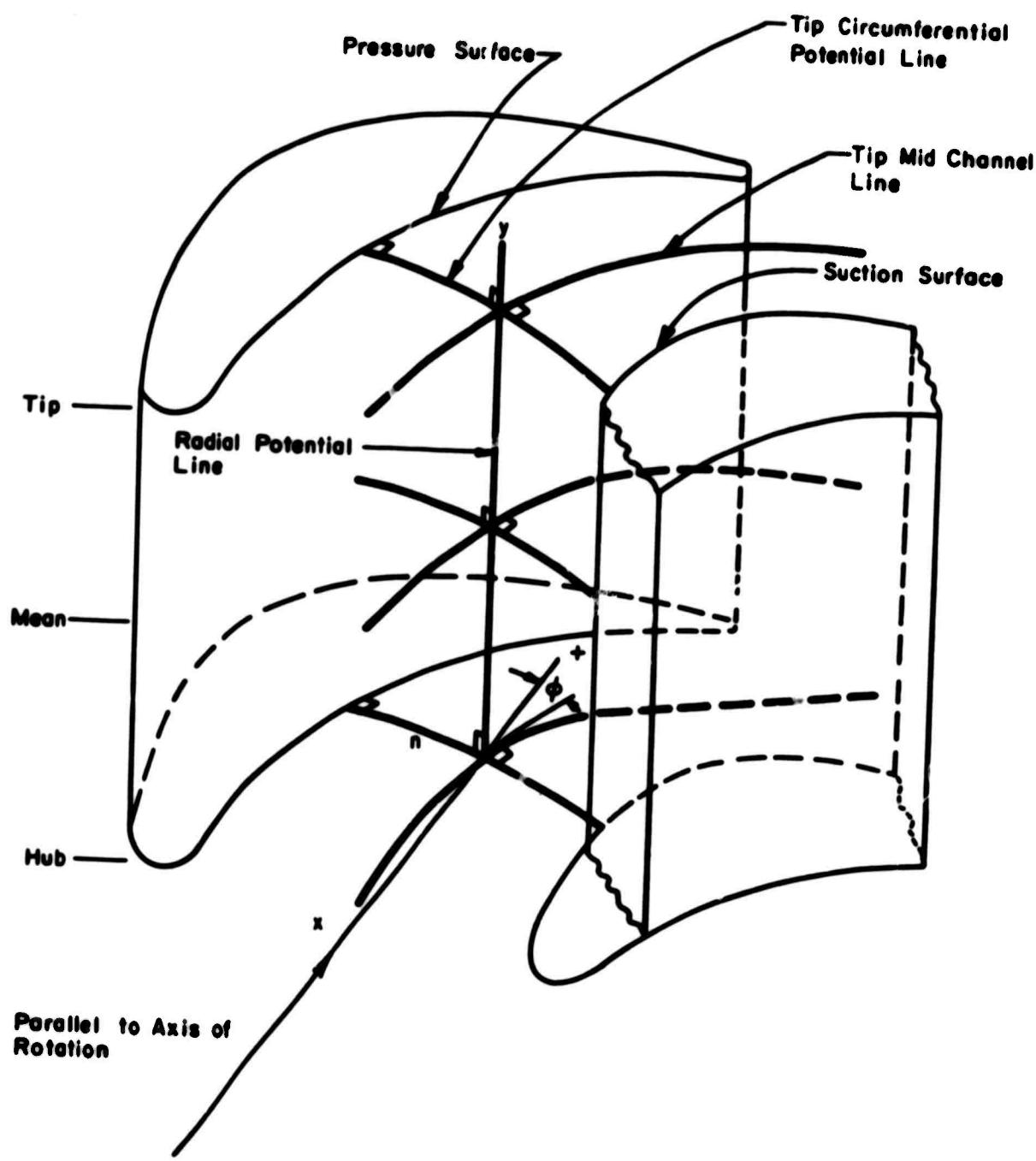


Figure 1. Channel Configuration (From Reference 1)

distance must be prepared from a curve drawn through the extrapolated and interpolated points as an input to a second program (described later) which in turn translates V/V_{CR} versus axial chord distance into V/V_{CR} versus surface distance from the blade stagnation point and ultimately yields the convection heat-transfer coefficients along the blade profile.

It follows that, even when only changes in the gas flow parameters (P_0 , T_0 , R_0 , γ_0 , V_0) are involved, preparation of a new table from the output of the first computer program requires several hours. When a different blade profile must be tested, a tedious, time-consuming determination of the channel parameters listed above must also be conducted.

A method is herein described which uses solely as inputs the static pressure distribution on the blade surface, obtained directly from the cold flow test described in Reference 2, and the gas flow parameters at the stage entrance for both the cold flow and hot flow tests. This method proceeds as follows:

Maximum flow per unit area (cold flow):

$$\frac{w_0}{A^*} = P_0 \left[\frac{g \gamma_0}{R_0 T_0} \right]^{\frac{1}{2}} \left[\frac{2}{\gamma_0 + 1} \right]^{\frac{(\gamma_0 + 1)}{2(\gamma_0 - 1)}} \quad (4)$$

Maximum flow per unit area (hot flow):

$$\frac{w_1}{A^*} = P_1 \left[\frac{g \gamma_1}{R_1 T_1} \right]^{\frac{1}{2}} \left[\frac{2}{\gamma_1 + 1} \right]^{\frac{(\gamma_1 + 1)}{2(\gamma_1 - 1)}}$$

Fractional change in flow rate:

$$FR = \frac{w_1 - w_0}{A^*} \quad (5)$$

Densities (inlet conditions):

$$\rho_0 = P_0 / R_0 T_0 ; \quad \rho_1 = P_1 / R_1 T_1$$

Critical velocities:

$$v_{CRO} = \left[2 R_0 g (\gamma_0 / \gamma_0 + 1) T_0 \right]^{\frac{1}{2}} \quad (6)$$

$$v_{CRI} = \left[2 R_1 g (\gamma_1 / \gamma_1 + 1) T_1 \right]^{\frac{1}{2}}$$

Local channel cold flow densities:

$$\rho_n = \rho_0 \left[1 - \left(\frac{\gamma_0 - 1}{\gamma_0 + 1} \right) \left(\frac{v_{no}}{v_{CRO}} \right)^2 \right]^{\frac{1}{\gamma_0 - 1}} \quad (7)$$

Desired local channel, hot-gas mass flow:

$$\rho_{no} v_{no} + (\rho_{no} v_{no}) (FR) = GO \quad (8)$$

Local channel hot flow density:

$$\rho_{hi} = \rho_i \left[1 - \left(\frac{\gamma_i - 1}{\gamma_i + 1} \right) \left(\frac{v_{no} + \Delta v_{no}}{v_{CR_i}} \right)^2 \right]^{\frac{1}{\gamma_i - 1}} \quad (9)$$

Δv_{no} is changed until

$$GO - \rho_{hi} (v_{no} + \Delta v_{no}) \leq \text{tolerance}$$

Figures 2 and 3 show the velocity versus axial chord distance plots obtained from the former computer program and the present method for identical input gas stream conditions.

The computer program presently in use at AFAPL calculates convection heat-transfer coefficients and adiabatic wall temperatures along the blade profile. Static temperature and pressure are calculated outside the boundary layer from channel flow theory, using the following equations:

$$\begin{aligned} T_S &= T_0 \left[1 - \left(\frac{\gamma - 1}{\gamma + 1} \right) \left(\frac{U(x)}{U_{CR}} \right)^2 \right] \\ P_S &= P_0 \left(\frac{T_S}{T_0} \right)^{\frac{\gamma}{\gamma - 1}} \end{aligned}$$

C_p , μ , P_R , and ρ , characteristic of the fluid, are entered as tables for the appropriate range of temperatures and pressures.

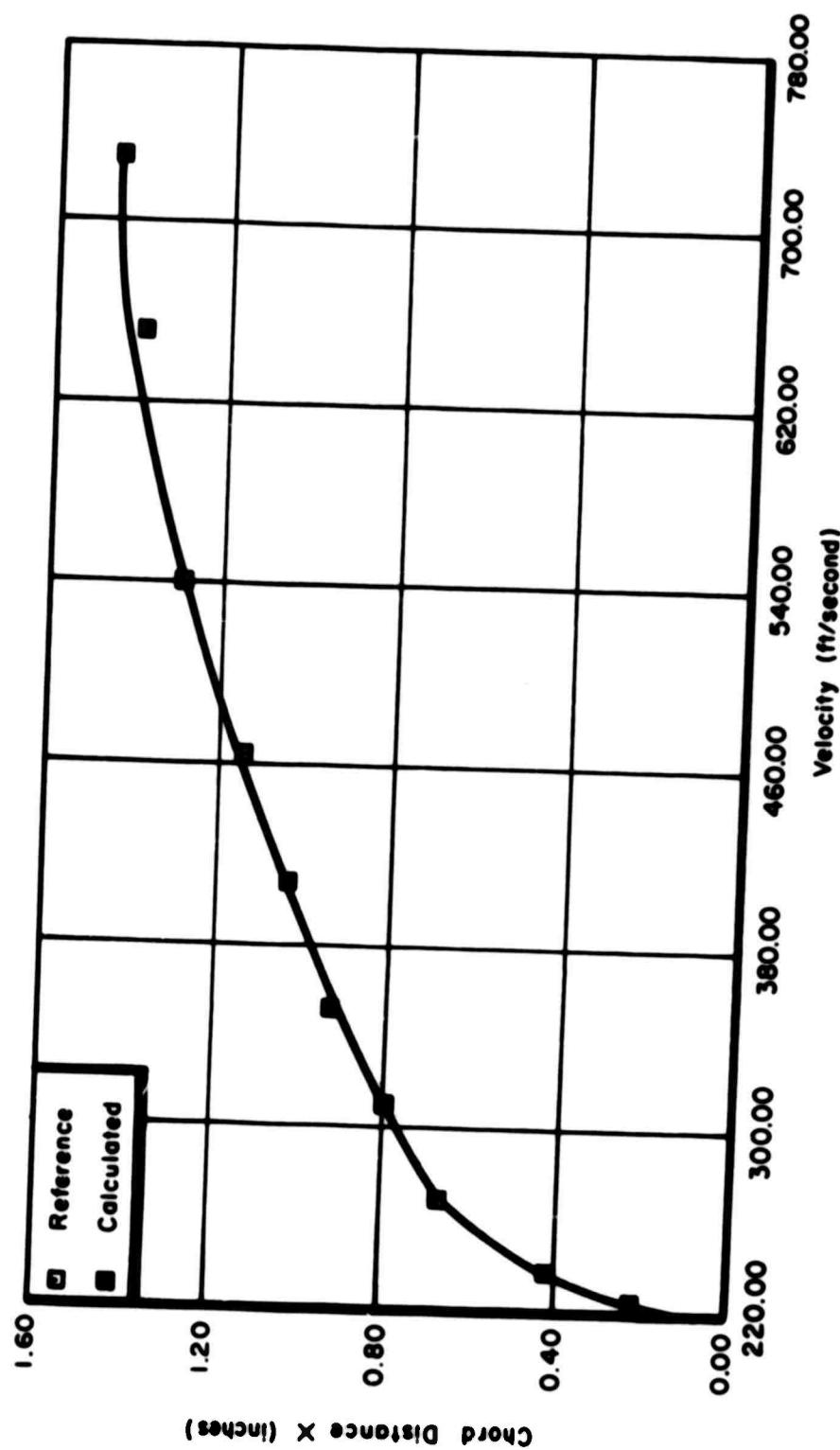


Figure 2. Suction Surface Velocity

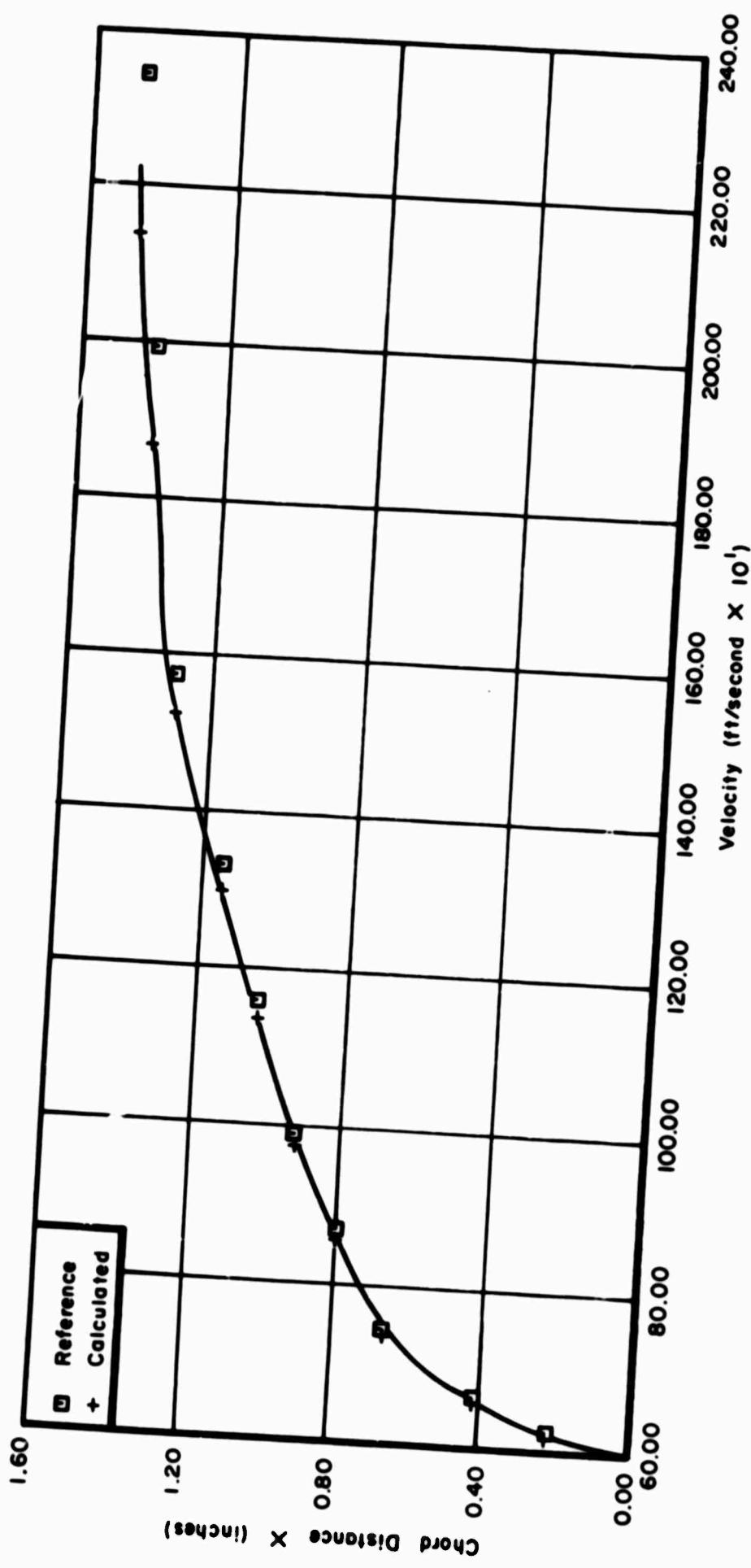


Figure 3. Pressure Surface Velocity

The calculation of convection heat-transfer coefficients and adiabatic wall temperatures is then carried out on the following assumptions:

1. On the suction side, the boundary layer is laminar from the stagnation point to the point of minimum pressure. From this latter point on, the flow is turbulent.
2. On the pressure side, the boundary layer is turbulent from the neighborhood of the stagnation point to the trailing edge.

The adiabatic wall temperatures are obtained from the following equations:

$$(laminar) \quad T_{ad} = T_s + (T_\infty - T_s) P_R^{\frac{1}{2}}$$

$$(turbulent) \quad T_{ad} = T_s + (T_\infty - T_s) P_R^{\frac{1}{3}}$$

On the leading edge and in the laminar part of the boundary layer, Squire's method (Reference 3) for the calculation of heat transfer on a cylinder and on a flat plate is used. In the turbulent part of the boundary layer, an approximation of the von Karman formula for heat transfer in turbulent flows is used.

$$N_x = \frac{1}{2} C_f P_R^{\frac{1}{3}} R_x$$

assuming the local coefficient of skin friction for a flat plate to be

$$\frac{1}{2} C_f = \frac{\tau_0}{\rho U^2} = 0.0128 \left(\frac{U \theta}{v} \right)^{-\frac{1}{4}} \quad (II)$$

where

$$\theta(x) = 0.036 \times \left(\frac{U_x}{v} \right)^{-\frac{1}{5}} \quad (III)$$

The fact that the Reynolds numbers anticipated in the testing of the blades will be low, $\approx 10^5$, and that, for the pressure profiles obtained (Figure 4), $\frac{dp}{dx}$ is small in an extended neighborhood of the minimum pressure point makes questionable the assumption that the latter coincides with the transition point. Also, Equation 11 suggests that $\theta(x)$ is rather insensitive to fluctuations in U , the latter being overshadowed by those in x . A comparison of Figures 4 through 6 shows that the drastic changes in the velocity profiles, particularly on the pressure side, are not reflected in $\theta(x)$ and that, for instance, the momentum thickness of the turbulent boundary layer is approximately the same on both pressure and suction surfaces beyond a surface distance of 1.3 inch, corresponding approximately to the transition point on the suction side. Obviously, this behavior of θ will

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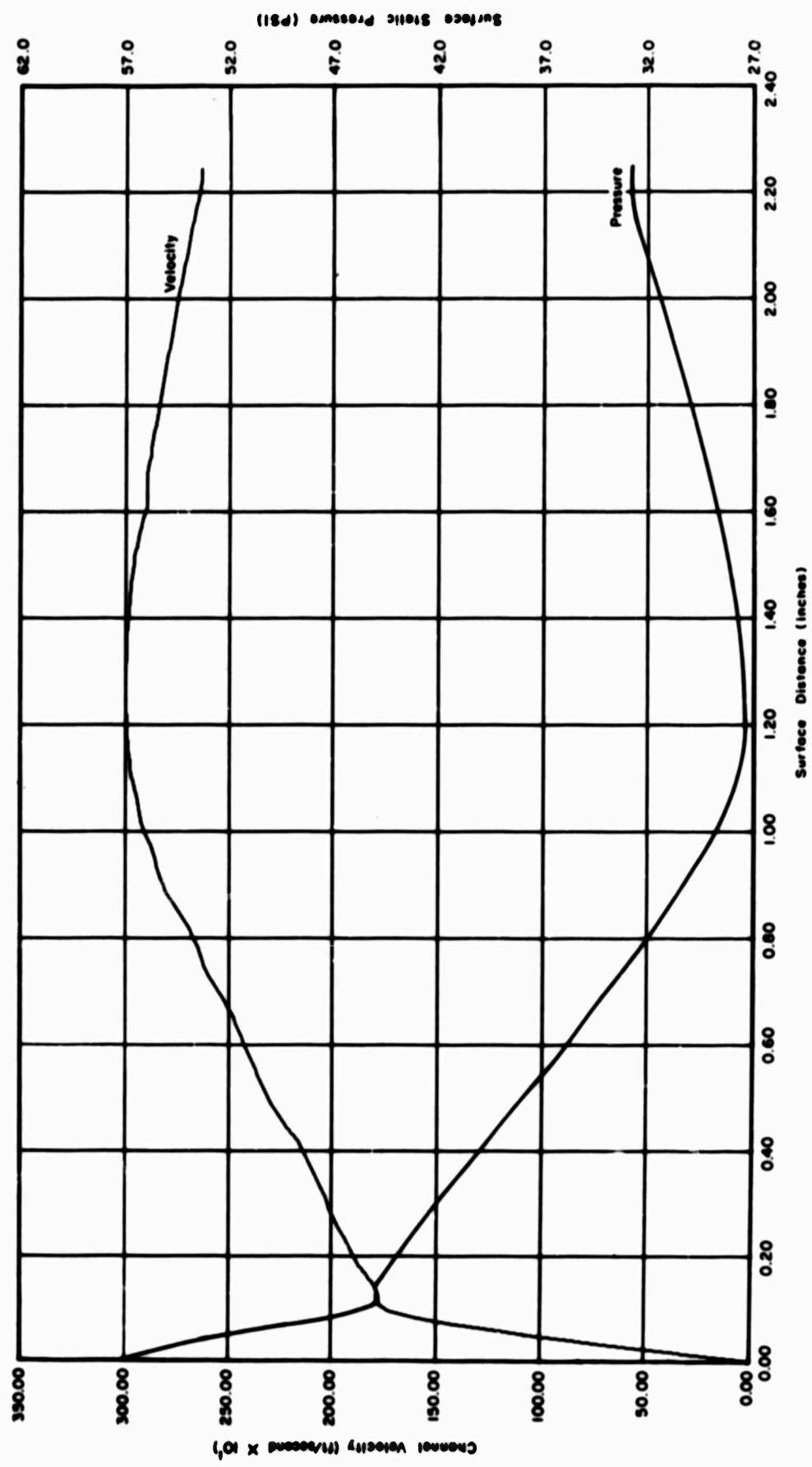


Figure 4. Suction Surface Velocity and Pressure

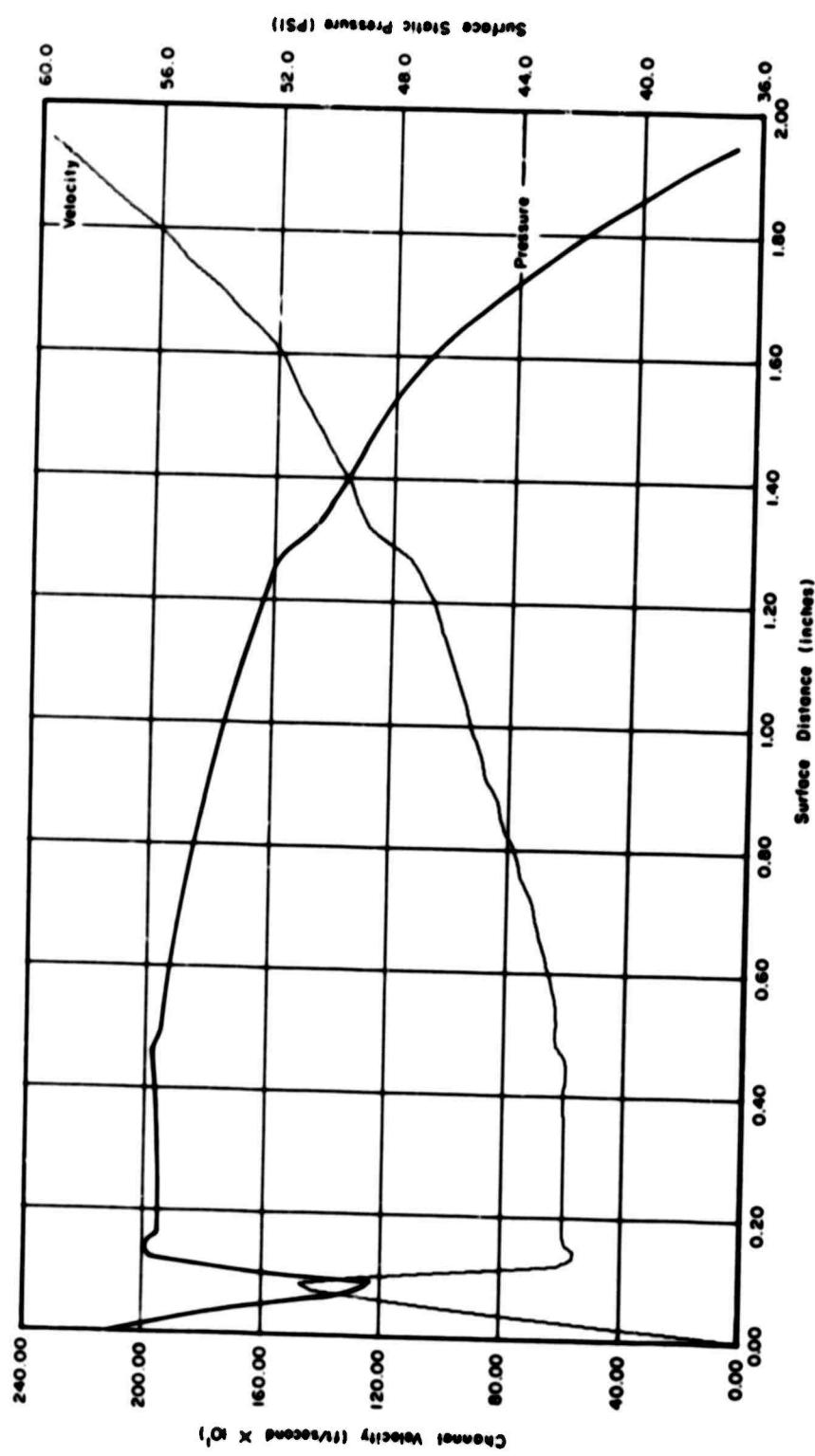


Figure 5. Pressure Surface Velocity and Pressure

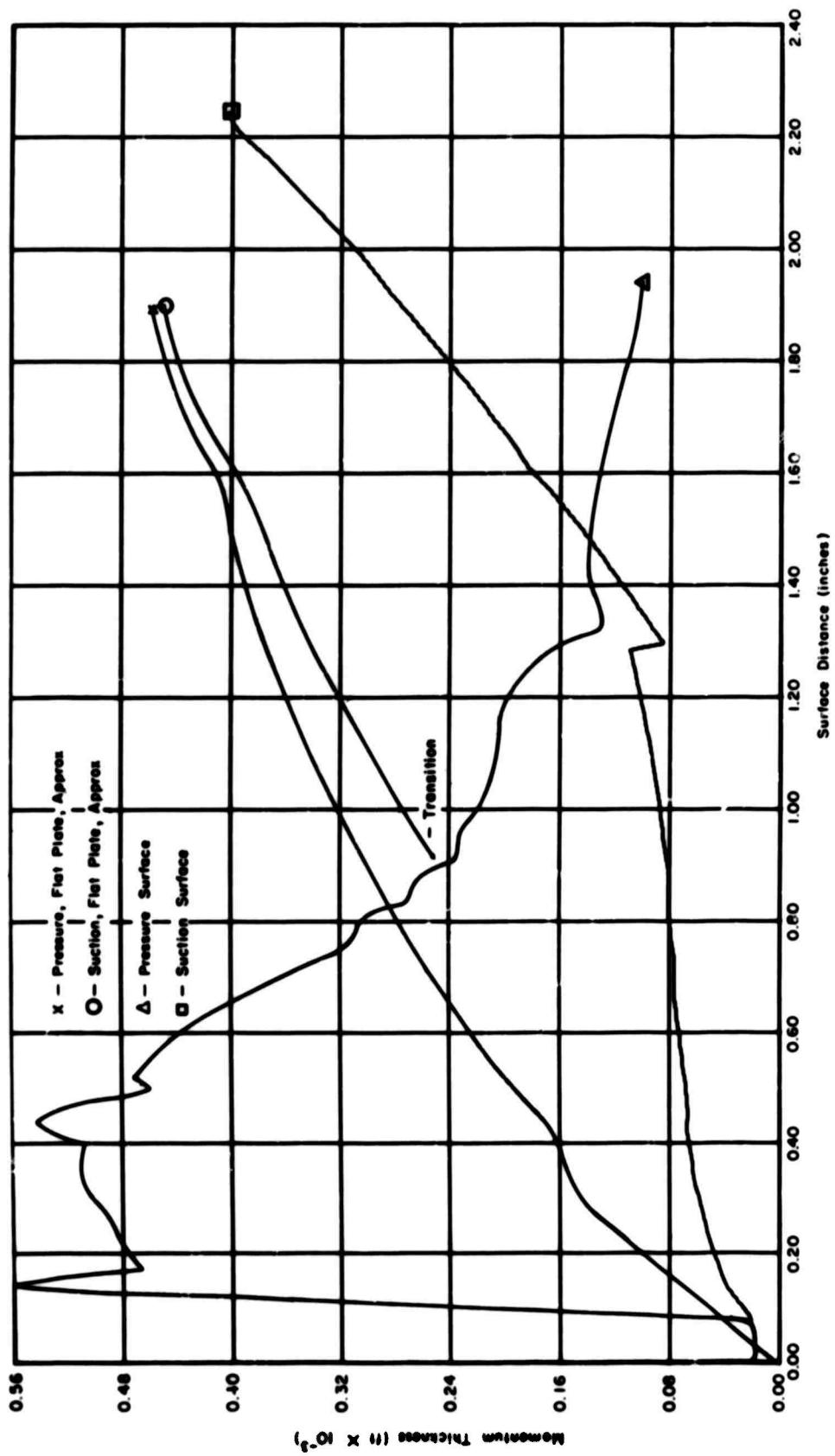


Figure 6. Momentum Thickness

be reflected in N_x , since

$$N_x \text{ varies with } \theta^{-\frac{1}{4}}, \text{ and, therefore, } h(x)$$

In an attempt to evaluate the discrepancies that might result from the preceding observations, we have adopted the theories of H. Schlichting and E. Truckenbrodt (References 4 and 5, respectively) relative to the determination of the transition point and to the computation of a two-dimensional turbulent boundary layer momentum thickness, to the specific requirements of AFAPL turbine blade hot testing investigation and incorporated them in a computer program described in this report. These theories will be described briefly.

In the new program, the laminar boundary layer is calculated using Squire's method which uses a simple quadrature to obtain θ , where

$$\theta^2 = \frac{0.47v}{U^6} \int_{x=0}^x U^5 dx \quad (12)$$

The displacement thickness δ^* and boundary layer thickness δ are obtained from the assumptions

$$\frac{\delta}{\theta} = \frac{315}{37} ; \frac{\delta^*}{\delta} = \frac{3}{10}$$

The shape factor of the boundary layer velocity profiles is defined as

$$\lambda = \frac{\delta^2}{v} \frac{dU}{dx}$$

The pressure decreases for $\lambda > 0$ and increases for $\lambda < 0$, hence the point of minimum pressure occurs for $\lambda = 0$

Original form:

$$\frac{\delta^*}{\delta} = \frac{3}{10} - \frac{1}{120} \lambda ; \frac{\theta}{\delta} = \left(\frac{37}{315} - \frac{1}{945} \lambda - \frac{1}{9072} \lambda^2 \right)$$

A family of neutral stability curves defined by the shape factor λ and representing the variation of δ^* with the Reynolds number $\frac{v\delta^*}{\nu}$ has been obtained by H. Schlichting and A. Ulrich (Reference 4). The point on these curves at which the Reynolds number R_{δ^*} has its smallest value is defined as the limit of stability for the laminar flow of interest. This R_{δ^*} is called the critical Reynolds number, $R_{\delta^* CR}$.

It follows that $R_{\delta CR}^*$ can be plotted as a function of λ , hence, of the surface distance x . The intercept of this curve with that representing the variation of the local Reynolds number $\frac{U\delta}{v}$ with x will yield the separation point.

As may be seen from Figures 7 and 8 for small x 's, $R_{\delta CR}^*$ is small and λ is large. As x becomes larger, this relationship is inverted and consequently $R_{\delta CR}^*$ decreases while R_{δ}^* increases.

The tormented profile of the variation of R_{δ}^* with x is to be attributed to the dependence of λ on $\frac{du}{dx}$ which undergoes abrupt changes along the blade surface.

The calculation of θ from E. Truckenbrodt's method (Reference 5) is based on the energy integral equation

$$\frac{1}{U^3} \frac{d}{dx} (U^3 \delta^{**}) = \frac{1.12 \times 10^{-2}}{\left(\frac{U\theta}{v}\right)^{\frac{1}{6}}} \quad (13)$$

where the energy thickness δ^{**} is a measure of the kinetic energy loss resulting from friction and is defined as

$$U^3 \delta^{**} = \int_0^{\infty} U(y) [U^2(x) - U^2(y)] dy$$

and

$$\frac{1.12 \times 10^{-2}}{\left(\frac{U\theta}{v}\right)^{\frac{1}{6}}}$$

represents a good approximation of the friction work performed in the boundary layer by the shearing stresses τ (H. Schlichting).

Integration of Equation 13 was performed by E. Truckenbrodt (Reference 5) and yields

$$\theta \left(\frac{U\theta}{v}\right)^{\frac{1}{6}} = C_1 + A \int_{x=x_1}^x \frac{U^3 + 2n}{U^3 + \frac{n}{6}} dx$$

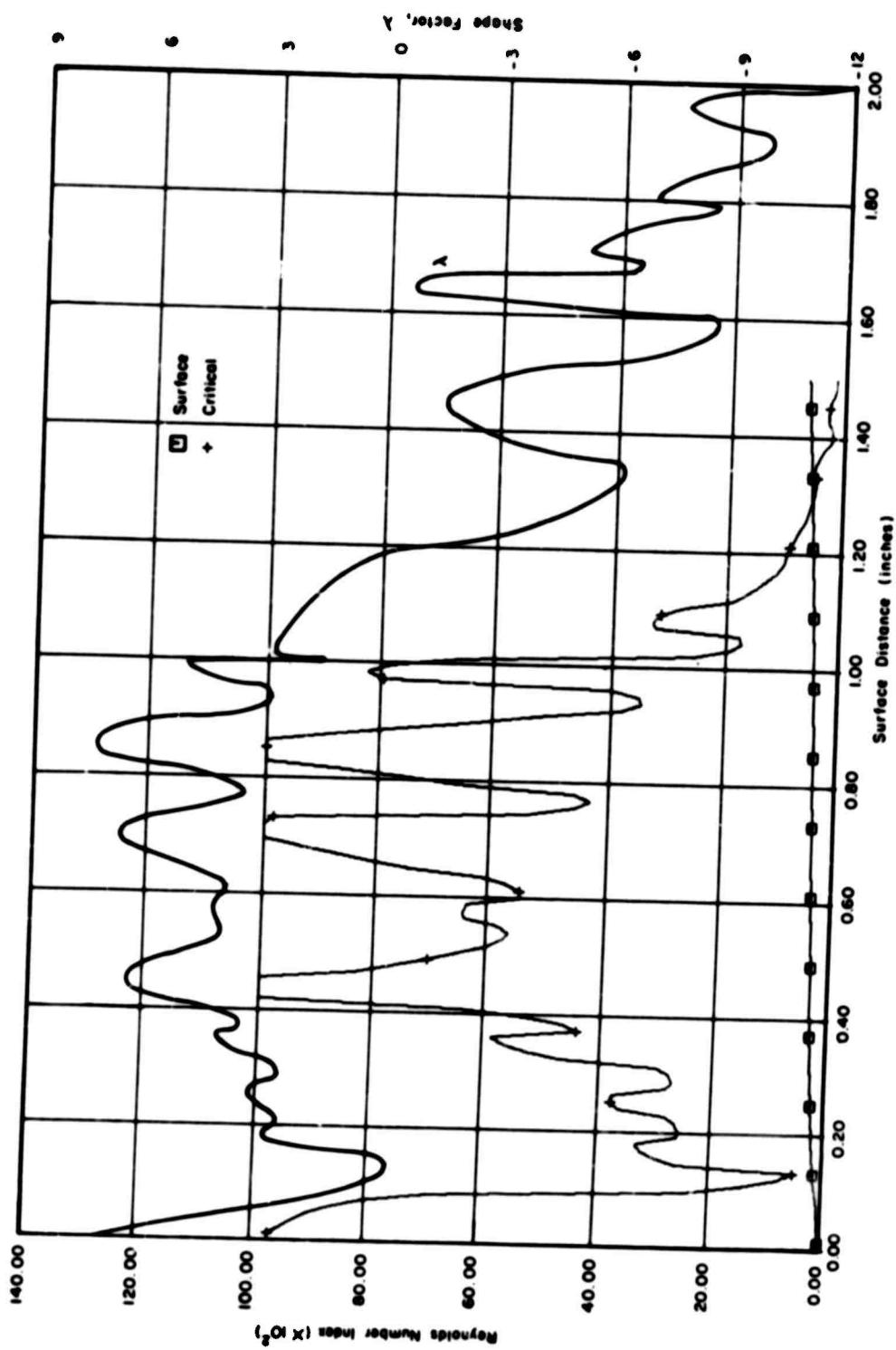


Figure 7. Section Surface Reynolds Number

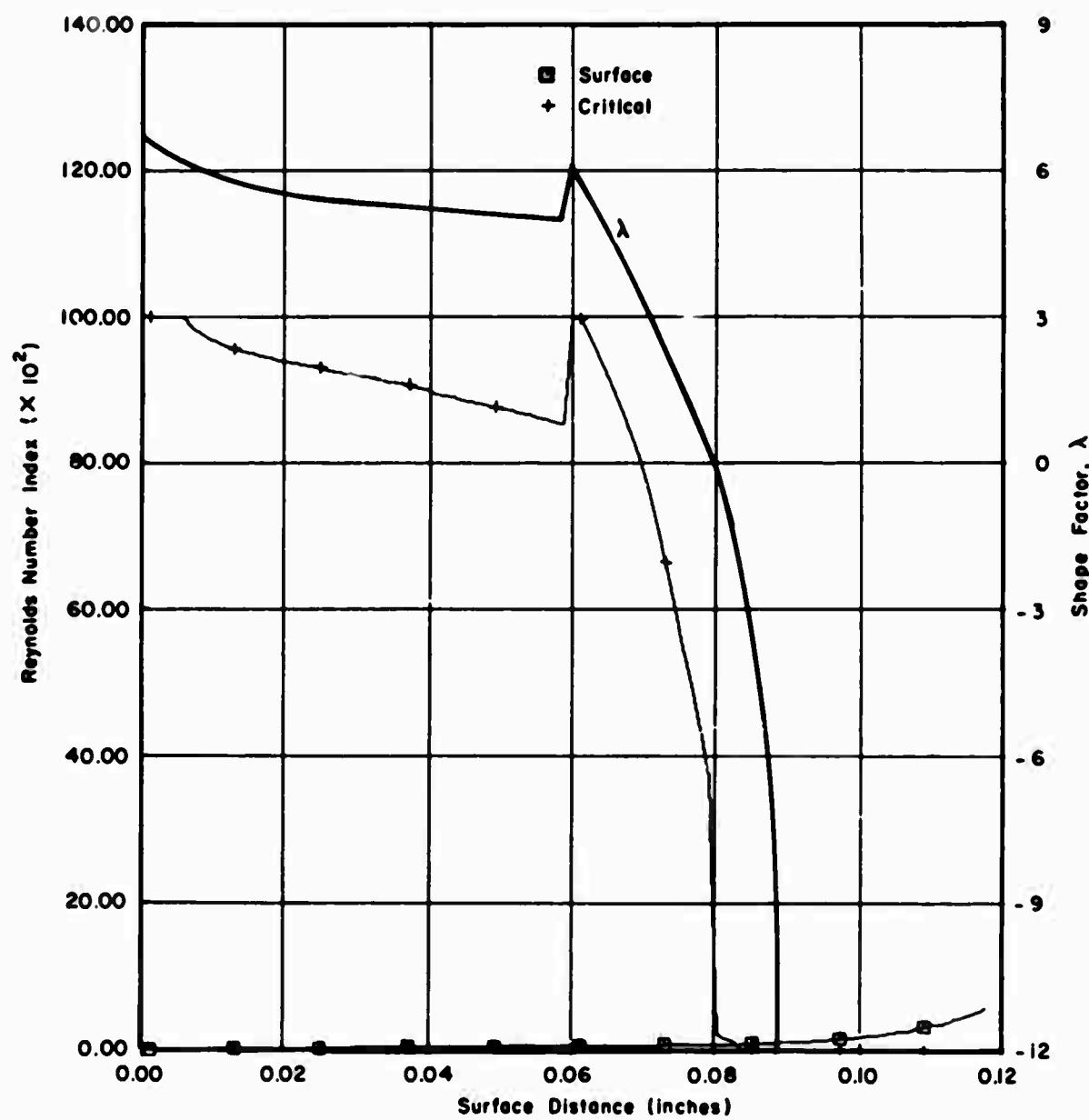


Figure 8. Pressure Surface Reynolds Number

which may be rewritten using the turbulent coefficient of skin friction for a flat plate as

$$\frac{\theta(x)}{l} = \left(\frac{U}{U_\infty}\right)^{-3} \left\{ C_1^* + \left(\frac{C_f}{2}\right)^{\frac{n+1}{n}} \int_{\frac{xL}{l}}^{\frac{x}{l}} \left(\frac{U}{U_\infty}\right)^{3+\frac{2}{n}} d\left(\frac{x}{l}\right) \right\}^{-\frac{n}{T+n}} \quad (14)$$

where

$$C_1^* = \left[\frac{1}{2} C_f l \left(\int_0^{\frac{xL}{l}} \left(\frac{U}{U_\infty}\right)^3 d\left(\frac{x}{l}\right) \right) \right]^{\frac{1}{2}} \left[\frac{(n+1)}{n} \right]$$

represents the laminar portion of the boundary layer.

It may be seen from Equation 14 that θ is highly sensitive to the variations in the velocity U . Figures 4 through 6 afford a comparison of the variations of θ and U with respect to x for the suction and pressure sides.

A very good value of the local coefficient of skin friction could have been obtained through the relationship

$$\frac{\tau_0}{\rho U^2} = .123 \times 10^{-0.678 H} \left(\frac{U\theta}{v}\right)^{-0.268}$$

but unfortunately E. Truckenbrodt's method for the variation of the shape factor H in the range of transition could not be used because $\frac{U\theta}{v}$ in this range was too small. Instead, $\frac{1}{2}C_f'$ was obtained from

$$\frac{\tau_0}{\rho U^2} = .0128 / \left(\frac{U\theta}{v}\right)^{.25}$$

and this value introduced into the von Karman formula

$$N_x = \frac{1}{2} C_f' R_x P_R$$

$$1 + 5 \sqrt{\frac{1}{2} C_f'} \left\{ \left(\frac{P}{P_f} - 1 \right) + \ln \left(1 + \frac{5}{6} \left(\frac{P}{P_f} - 1 \right) \right) \right\}$$

which takes into account the variation of the Prandtl number.

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The convection heat-transfer coefficient for the laminar part of the boundary layer is calculated from Squire's method, using the universal function

$$H\left(\frac{\delta T}{\delta}\right) = H(\Delta) = \frac{3}{10} - \frac{3}{10} \frac{1}{\Delta} + \frac{2}{15} \frac{1}{\Delta^2} - \frac{3}{140} \frac{1}{\Delta^4} + \frac{1}{180} \frac{1}{\Delta^5}$$

obtained from integration of the energy equation with $P_r < 1$. Squire's paper (Reference 3) is referred to for the details of the procedure. The new computer program, instead of using a table of H versus Δ , computes $H(\Delta)$ at every point where h is calculated.

SECTION III

RESULTS AND CONCLUSIONS

On the suction side, the transition point as determined in the new program is shifted by 0.37 inch downstream. At this point h_T is 35% higher than the h obtained from the former program at the same location (Figure 9). On the pressure side, Figure 10 shows that the new convection heat-transfer coefficient assumes lower values immediately downstream of the transition point with a maximum change of 40% with respect to the former h at the same location and increases at a faster rate to assume a value at the trailing edge representing an increase of 36% over the former h .

The average value of h over the blade remains essentially unchanged when Truckenbrodt's method is used, so that the total amount of coolant required for the blade will not be changed significantly.

The large discrepancies in local heat-transfer coefficients would necessitate a redistribution of the coolant flow formerly determined from the Allison program.

Confirmation of the validity of the improvements suggested in this report will necessitate experimental data which will become available when the AFAPL in-house testing program is initiated.

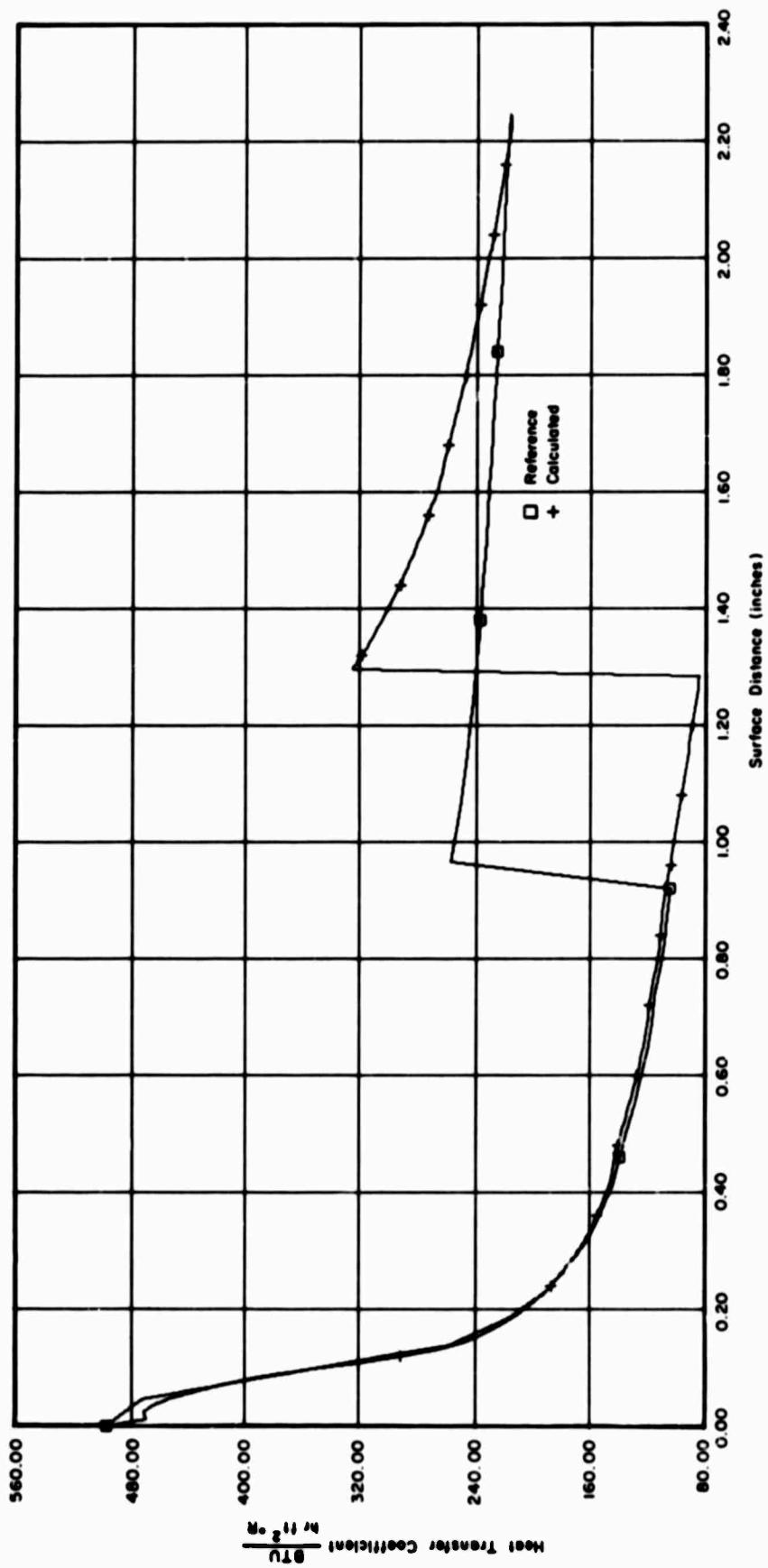


Figure 9. Suction Surface Heat-Transfer Coefficient

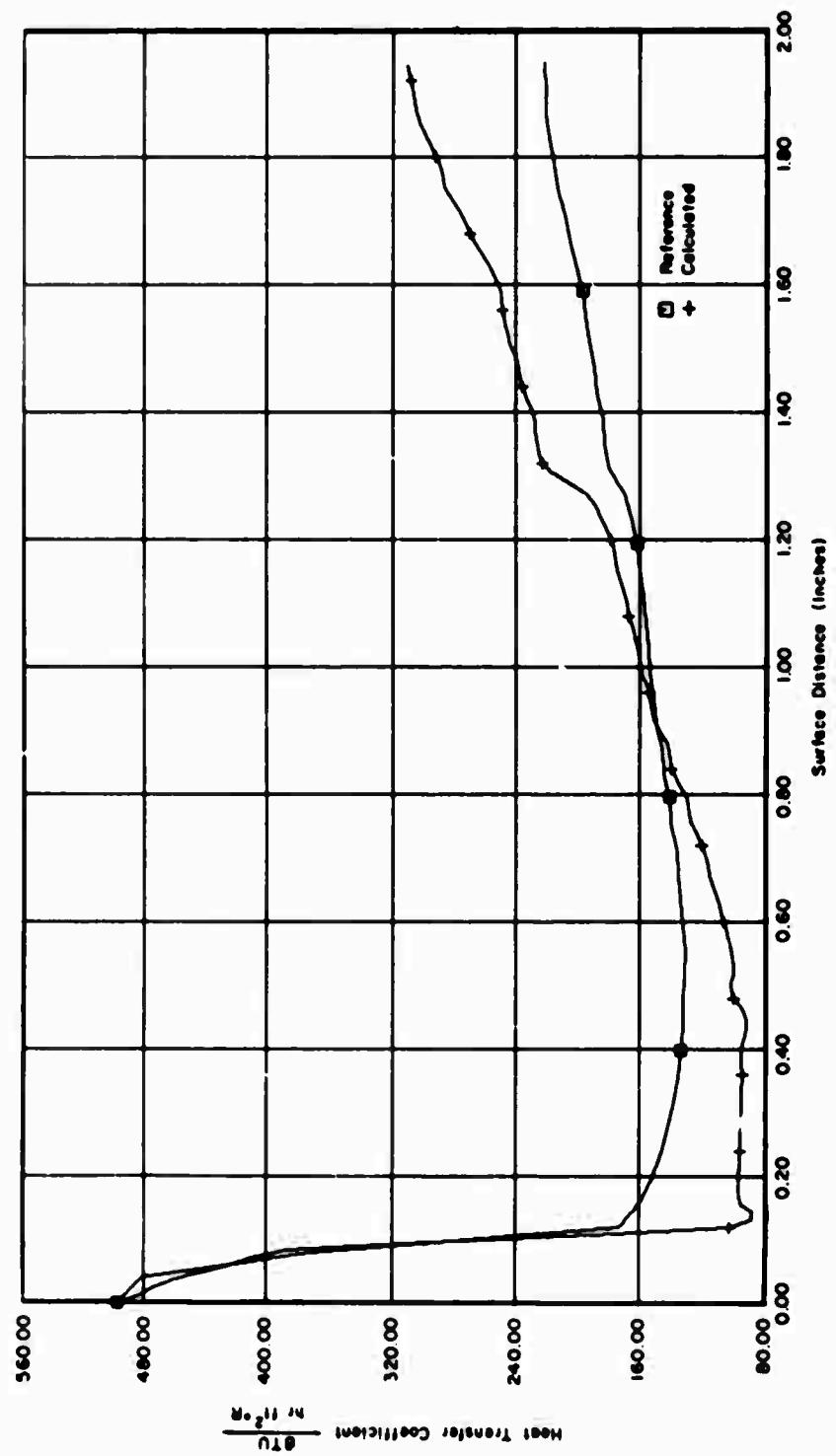


Figure 10. Pressure Surface Heat-Transfer Coefficient

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APPENDIX

COMPUTER PROGRAM

PROGRAM FUNCTIONS

LUMIT

This is the main program. It is divided into two basic parts: laminar boundary layer and turbulent boundary layer. Initially the program reads in the input data, calculates the initial conditions of the laminar boundary layer, iterates through the laminar calculations until transition is reached, then proceeds into the turbulent section and iterates until the end of the blade is reached. All integrations are performed in the program and are basically trapezoidal.

VLOCT (alternate entry CURVE)

This routine reads in the velocity profile versus surface distance. It uses the alternate entry to find the velocity and the first and second derivatives for a given surface distance. It should be noted that the first and second derivatives are somewhat inaccurate since they are based upon a finite length rather than a point.

Uses subroutine TLOCK

DTFRMX

This routine solves the universal function of Δ for Δ greater than 1. It iteratively solves for the unknown Δ given $H(\Delta)$.

Uses subroutine AFQUIR.

See Chapter XII of Reference 3.

PRANX

This routine looks up in a table the constant used in the heat-transfer equation near the stagnation point as a function of the Prandtl number.

Uses subroutine SRCHX

PROPEX

This routine calculates the viscosity, density, Prandtl number, and specific heat of air as a function of temperature and pressure.

Uses subroutine PROCOM and TLOOK.

TLOOKX

The function subprogram TLOOK is a general purpose routine to perform a table look-up in a two-dimensional table (dependent variable versus independent variable). It first locates the input independent variable in its table, then takes the nearest 'N' pairs of points and calls subroutine LAGRNG. This program uses an interpolating polynomial of degree 'N-1', in the Lagrangian form, to evaluate the dependent variable. TLOOK also has the capability of remembering where it found the independent variable in the table. Thus, search time is saved when the next time it is called the independent variable has changed only slightly.

Use subroutine LAGRNG.

LAGRNG

See description of TLOOKX.

SRCHXX

This subprogram is a table lookup routine using linear interpolation.

PROCOM

This routine calculates the thermodynamic properties of air or air-JP4 mixtures. Given temperature and fuel-air ratio, it calculates speed of sound, ratio of specific heats, specific heat of constant pressure, gas constant, and nonpressure biased entropy and enthalpy.

AFQUR

This program is a quadratic convergence routine. It is a routine having general application and is used to converge practically any function.

CRITXX

This routine takes an input shape factor (ALAM) and looks up on a curve the critical Reynolds number.

Uses subroutine SRCHX.

See Chapter XVII of Reference 3.

INPUT VARIABLES

NUMB - number of points in velocity profile curve

XS - surface distance

VS - surface velocity

ALENTH - characteristic blade length

TTZERO - total temperature of free stream

PTZERO - total pressure of free stream

UCRIT - sonic velocity of free stream

AF - average specific heat ratio

UIA - free stream velocity

DIA - leading edge diameter

DX - integration interval

PRINT - print interval

OUTPUT VARIABLES

Laminar

X - surface distance

UX - surface velocity

T - static temperature of surface

P - static pressure of surface

VISM - kinematic viscosity

DEL - laminar boundary layer thickness

THETA - momentum loss thickness

DELSTR - boundary layer displacement thickness

UNDVFS - characteristic surface Reynolds number

TRMCRT - critical surface Reynolds number

ALAM - velocity profile shape factor

H - universal function

DELT - thermal boundary layer thickness

HL - convection heat-transfer coefficient

TND - adiabatic wall temperature

Turbulent

X - surface distance

UX - surface velocity

T - static temperature of surface

P - static pressure of surface

VISN - kinematic viscosity

TAP - adiabatic wall temperature

CF2 - surface friction coefficient

AFAPL-TR-68-143

THETA - momentum loss thickness

PN - Prandtl number

RHO - density

TUQV - Reynolds number associated with momentum loss thickness

HX - turbulent heat-transfer coefficient

INPUT FORMAT

First Cards

Curve title card (12A6)

Used to identify the particular velocity profile

Second Cards

NUMB (I3)

Number of points in velocity versus surface distance curve

Next NUMB cards

XS VS (2F10.0)

Surface distance and velocity cards

Next Card

Case title card (12A6)

Used to identify the particular case

Next Card(s)

NAME LIST/INPUT/

Case input; see input variables for definition.

```

S18FTC LUMIT M94,XR7
DIMENSION ATITLE(12)
NAMELIST/INPUT/ALENTH,TTZERO,PTZERO,UCRIT,AK,UIN,OIA,
AOX,PRINT
CALL READIN(XMAX)
READ(5,510)(ATITLE(I),I=1,12)
WRITE(6,511)(ATITLE(I),I=1,12)
510 FORMAT(12A6)
511 FORMAT(1H1,12A6)
READ(5,INPUT)
R=OIA/2.
AINT=0.0
BINT=0.0
VISKI=0.0
URAT11=0.0
URAT12=0.0
X=0.0
UX5=0.0
I=0
IBIN=1
ALAM=7.053
C***** START OF LAMINAR *****
C***** X=0.0 CALCULATIONS
C
CXB=DX
ALAH=7.0529
X=U.0
CALL CURVE(X,OXB,UX,UPX,UPPX)
T=TTZERO
P=PTZERO
CALL PROPER(T,P,AMU,RHO,PN,CP)
VISKO=AMU/RHO
VISKO=VISK
CFL=1.328/SQRT(UIN*ALENTH/VISKO)
DEL=SQRT(ALAM*VISK/UPX)
THETA=0.11746*DEL
DELSTR=2.554*THETA
CALL PRAN(PN,CONST1)
ANO=2.*CONST1*SQRT(UIN*DIA/VISK)
DELT=2.*DIA/ANO
RAT=DEL/DELT
H=0.3-0.3*RAT+0.13333*(RAT**2.)-0.0214286*(RAT**4.)
A=0.005555*(RAT**5.)
HL=2.*CP*AMU/(PN*DELT)+4.6275
TAD=T
HO=H
OEL0=DEL
C
C END OF X=ZERO CALCULATIONS
C
IPS=PRINT/DX+OX
UX5=UX**5.
WRITE(6,100)X,UX,T
WRITE(6,101)P,VISK,THETA
WRITE(6,102)DEL,DELSTR,UDQVIS
WRITE(6,103)TRMCRT,ALAM,PN
WRITE(6,104)DELT,HL

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      WRITE(6,105)TAD
100  FORMAT(8H0      X=E15.7,5X,7H    UX=E15.7,5X,7H    T=E15.7)
101  FORMAT(8H      P=E15.7,5X,7H    VISK=E15.7,5X,7H  THETA=E15.7)
102  FORMAT(8H      DEL=E15.7,5X,7H  DELSTR=E15.7,5X,7H  UDQVIS=E15.7)
103  FORMAT(8H  TRMCRT=E15.7,5X,7H  ALAM=E15.7,5X,7H    PN=E15.7)
104  FORMAT(8H  DELTA=E15.7,5X,7H  DELT=E15.7,5X,7H    HL=E15.7)
105  FORMAT(8H      TAD=E15.7)

      IP=0
      UX5=UX**5.
11     I=I+1
      AI=I
      X=A1*OX
      IP=IP+1
14     CALL CURVE(X,DX,UX,UPX,UPPX)
      IF(UX .LT. 6.0) GO TO 11
      UX5=UX**5.
      T=TTZERO*(1.-(AK-1.)/(AK+1.))*(UX/UCRIT)**2.
      P=PTZERO*((T/TTZERO)**(AK/(AK-1.)))
      CALL PROPER(T,P,AMU,RHO,PN,CP)
      VISK=AMU/RHO
      CALL PRAN(PN,CONST1)
      ANO=2.*CONST1*SORT(UIN*OIA/VISK)
      DELTO=2.*OIA/ANO
      IH=1
      DEL02=ALAM0*VISK/UPX
      TERM1=DEL02*UX**6./(34.*VISK)
      UEINT1=0.0
      OTUM2=0.0
      DELAS=DEL0
      DEL2AS=DELAS*DELAS
      GO TO 2
1     I=I+1
      AI=I
      X=A1*OX
      IP=IP+1
2     CONTINUE
      UX5S=UX5
      UX5=UX
      CALL CURVE(X,OX,UX,UPX,UPPX)
      UX5=UX**5.
      T=TTZERO*(1.-(AK-1.)/(AK+1.))*(UX/UCRIT)**2.
      P=PTZERO*((T/TTZERO)**(AK/(AK-1.)))
      CALL PROPER(T,P,AMU,RHO,PN,CP)
      VISK=AMU/RHO
      VISKI=VISK*DX
      TERM1=TERM1+((UX5+UX5S)/2.)*OX
      C=34.*VISK/((UX5+UX+UX5S+UX51)/2.)
      DFL2A=DEL2AS+C*((UX5+UX5S)/2.)*DX
      OELA=SORT(DFL2A)
      OEL2E=C*TERM1
      OEE=SORT(OEL2E)
      OEL=OEE
      OEL2=OEL2E
      THETA=0.11746*OEL
      DELSTR=2.554*THETA
      UDQVIS=UX*DELSTR/VISK
      ALAM=DEL2*UPX/VISK
      CALL CRITCL(ALAM,TRMCRT)
      IF(UDQVIS .GE. TRMCRT) GO TO 190
      GO TO (150,99),IH

C   USEO FIRST TIME ONLY

```

```

C
50   IH=2
      X1=X
      CALL CURVE(X1,OX,UX1,UPX1,UPPX1)
      Z1=PN*(OEL0*UX1*H0)**2./(4.*VISK)
      Z2=Z1+(H0*(UX1+UX))/2.*OX
      ZZ1=OEL0**2.*UX1**6./134.*VISK)
      ZZ2=ZZ1+((UX1**5.+UX**5.)/2.)*OX
      HD2=0.11765*UX**4.*Z2/(PN*ZZ2)
      CALL OTFRM(HD2,OELTA2)
      HG=H02/(OELTA2**2.)
      A08=H02/((0.11765/PN)*UX**4.)
      C00=(H02/((0.11765/PN)*UX**4.))+HG
      TERMC=UX*HG*OX
      TERMO=C/C00
      TERM8=TERMO
      TERMA=8/A08
      GO TO 108

C
C USEO ALL BUT FIRST TIME
99   CONTINUE
      TERMA=TERMA+((UX+UXS)/2.)*OX
      TERM8=TERM8+((UX**5.+UXS**5.)/2.)*DX
      O2HG=(0.11765/PN)*UX**4.*TERMA/TERM8
      CALL OTFRM(O2HG,OELTA1)
      HG=O2HG/(OELTA1**2.)
      TERMC=TERMC+((UX+UXS)/2.)*(HG+HS)/2.)*OX
      TERMO=TERM8
      D2HG1=(0.11765/PN)*UX**4.*TERMC/(TERMO*HG)
      CALL OTFRM(D2HG1,OELTA2)
108  H=HG
      OELTA=OELTA2
      OELT=OELTA*OEL
      HL=2.*CP*AMU/(PN*OELT)+4.62725
      TAO=T+(TTZERO-T)*SQR(T/PN)
      OXL=DX/ALENT
      AINT=AINT+(((UX/UIN)**5.+UXS/UIN)**5.)/2.)*DXL
      C1STR=((CFL/2.)*SURT(AINT))**1.25
      UX$=UX
      HS=H
      IF(IP .NE. IPS) GO TO 1
      IP=0
      WRITE(6,100)X,UX,T
      WRITE(6,101)P,VISK,THETA
      WRITE(6,102)DEL,DELSTR,UDQVIS
      WRITE(6,103)TRMCRT,ALAM,PN
      WRITE(6,104)DELTA,DELT,HL
      WRITE(6,105)TAD
      GO TO 1
C***** END OF LAMINAR *****
C***** 190  WRITE(6,211)X
211  FORMAT(1H2,16HTRANSITION AT X=,E15.7)
      WRITE(6,100)X,UX,T
      WRITE(6,101)P,VISK,THETA
      WRITE(6,102)DEL,DELSTR,UDQVIS
      WRITE(6,103)TRMCRT,ALAM,PN
      WRITE(6,104)DELTA,OELT,HL
      WRITE(6,105)TAO

```

```

XT=X
VISK1=VISK1/XT
C1STRS=C1STR
C***** START OF TURBULENT *****
C***** END OF TURBULENT *****
IF(IP .EQ. IPS) IP=0
800 I=I+1
AI=I
UXS=UX
X=AI*OX
IP=IP+1
CALL CURVE(IX,DX,UX,UPX,UPPX)
T=TTZERO*(1.-(AK-1.)/(AK+1.))*(UX/UCRIT)**2.)
P=PTZERO*(T/TTZERO)**(AK/(AK-1.))
CALL PROPER(T,P,AMU,RHO,PN,CP)
VISK=AMU/RHO
TAO=T+(TTZERO-T)*(PN**(1./3.))
BINT=BINT+((UX/UIN)**3.5*(UXS/UIN)**3.5)/2.*DXL
CF2=0.016/((UIN*ALENTH/VISK)**0.25)
THQL=(UX/UIN)**(-3.)*(C1STRS+CF2*BINT)**0.8
THETA=THQL*ALENTH
TUQV=THETA*UX/VISK
TAUQDU=0.0128/TUQV**0.25
HX=TAUQDU*RHO*G*UX*(3600./778.)
A(1.+5.*SQRT(TAUQDU ))*(PN-1.)*ALOG(1.+(5./6.)*(PN-1.)))
IF(IP .EQ. IPS) GO TO 900
825 IF(IX .LT. XMAX) GO TO 800
1111 STOP
900 IP=0
WRITE(6,100)X,UX,T
WRITE(6,101)P,VISK,THETA
WRITE(6,901)CF2,RHO,TUQV
WRITE(6,902)PN,TAD,HX
901 FORMAT(8H CF2=E15.7,5X,7H RHO=E15.7,5X,7H TUQV=E15.7)
902 FORMAT(8H PN=E15.7,5X,7H TAD=E15.7,5X,7H HX=E15.7)
GO TO 825
C***** END OF TURBULENT *****
C***** END *****
END

```

```
SIBFTC VLOCT M94,XR7,DECK
SUBROUTINE READIN(XMAX)
DIMENSION XS(200),VS(200)
DIMENSION ATITLE(12)
READ(5,510)(ATITLE(I),I=1,12)
WRITE(6,511)(ATITLE(I),I=1,12)
510 FORMAT(12A6)
511 FORMAT(1H1,12A6)
READ(5,100)NUMB
READ(5,101)(XS(I),VS(I),I=1,NUMB)
100 FORMAT(I3)
101 FORMAT(2F10.0)
DO 1 I=1,NUMB
1=I
1 XS(I)=XS(I)/12.
XMAX=XS(1)
RETURN
ENTRY CURVE(X,DX,UE,UEP,UEPP)
X1=X+DX
X2=X1+DX
K=0
NPT=4
UE=TLOOK(X,XS,VS,NUMB,NPT,K,ILAST)
UE1=TLOOK(X1,XS,VS,NUMB,NPT,K,ILAST)
UE2=TLOOK(X2,XS,VS,NUMB,NPT,K,ILAST)
UEP=((UE)-UE)/(X1-X))
UEPX=((UE2-UE1)/(X2-X1))
UEPP=((UEPX-UEP)/(X1-X))
RETURN
END
```

```
SIBFTC DTFRMX M94,XR7,DECK
SUBROUTINE DTFRM(ANS,DEL)
DIMENSION Q(9)
Q(2)=0.0
Q(3)=0.0
AJ=50.
TOL=0.0001
DIR=1.01
TRY=1.5
1 TRY2=TRY*TRY
TERM=0.3*TRY2-0.3*TRY+0.13333-(0.0214286/TRY2)*
A0.005555/(TRY2*TRY)
CALL AFQUIR(Q,TRY,TERM,ANS,AJ,TOL,DIR,ANEW,ICON)
IF(ICON .EQ. 3) GO TO 5
IF(ICON .EQ. 2) GO TO 10
TRY=ANEW
GO TO 1
5 WRITE(6,100)ANS
100 FORMAT(1HO,19HERROR IN DELTA,ANS=,E15.7)
10 DEL=TRY
RETURN
END
```

```
SIBFTC PRAMX M94,XR7,DECK
SUBROUTINE PRAM(P,C)
DIMENSION PX(9),CX(9)
DATA (PX(I),I=1,9)/0.6,0.7,0.8,0.9,1.0,1.1,1.7,.10.,.15./
DATA (CX(I),I=1,9)/0.466,0.495,0.521,0.546,0.570,
A0.592,1.18,1.34,1.54/
CALL SRCHX(P,PX(1),9,0,IL,ATERM)
C=CX(IL)+ATERM*(CX(IL+1)-CX(IL))
RETURN
END
```

```

SIBFTC PROPEX M94,XR7,DECK
  SUBROUTINE PROPERIT,P,AMU,RHO,PN,CP)
  DIMENSION HT5(31),HT6(31)

C 5 TEMPERATURE (INDEPENDENT VARIABLE TABLE)
C  NUMBER OF POINTS 31
  DATA (HT5(K),K=1,31)/450.,540.,630.,720.,810.,900.,990.,1080.,1170
  A.,1260.,1350.,1440.,1530.,1620.,1710.,1800.,1980.,2160.,2340.,2520
  8.,2700.,2880.,3060.,3240.,3420.,3600.,3780.,3960.,4140.,4320.,4620
  C./

C 6 PRANDTL NUMBER VERSUS TEMPERATURE
C           (R)
C  INDEPENDENT VECTOR AT (5)
C  LENGTH 31
C  NPR FOR DRY AIR
  DATA (HT6(K),K=1,31)/.722,.708,.697,.689,.683,.68,.68,.682,.68
  A4,.686,.689,.692,.696,.699,.702,.706,.714,.722,.726,.734,.741,.749
  8,.759,.767,.783,.803,.831,.863,.916,.972/
  NP=4
  NT=31
  KL=0

C T=DEGREES RANKIN
C P=POUNDS/SQ. IN.
C AMU=POUNDS*SEC./SQ. FT.
C RHO=POUNDS*SEC. SQ./FT.***4
C CP=FT.SQ./(SEC. SQ. DEGREE RANKIN)
C TK=BTU/(HR FT DEGREE RANKIN)
C PN=UNITLESS
C VIS=POUNDS/MR FT
C T3=DEGREES KELVIN
C RX=BTU/(POUND DEGREE RANKIN)
C CPX=BTU/(POUND DEGREE RANKIN)
  CALL PRDCOM(D,0,T,X1,X2,CPX,RX,X3,X4)
  T3=0.555556*T
  VIS=0.00353*T3**1.5/(T3+110.6)
  TK=0.6325*SORT(T3)*0.00248/(1.+245.4*10.**(-12./T3)/T3)
  PN=TLOOK(T,HT5,HT6,NT,np,KL,ILAST)
  CP=CPX*32.174049*778.26
  AMU=VIS/(3600.*32.174049)
  RHO=(P*144./(RX*778.26*T))/32.174049
  RETURN
  ENO

```

```

SIBFTC TLOOKX M94/2,XR7,DECK
FUNCTION TLOOK(P,PT,QT,NT,NP,K,ILAST)

C PT IS TABLE OF INDEPENDENT VARIABLES
C QT IS TABLE OF DEPENDENT VARIABLES
C NT = SIZE OF ABOVE TABLES
C NP = NUMBER OF POINTS FOR INTERPOLATION
C K = 0, LIMIT OUTPUT TO BOUNDARY OF TABLE
C K = 1, EXTRAPOLATE FOR VALUES OUTSIDE TABLE
C DIMENSION PT(1), QT(1), XT(10), YT(10)
C IF(ILAST .LE. 0) ILAST = 1
C I = ILAST+1
C IF(PT(I) = PT(NT)) 4,15,15
C TABLE PT IS IN ASCENDING ORDER
4 IF(PT(I) .GE. P .AND. PT(ILAST) .LE. P) GO TO 8
DO 5 I=1,NT
IF(P .LE. PT(I)) GO TO 8
5 CONTINUE
ILAST = NT-1
IF(K .GE. 1) GO TO 7
TLOOK = QT(NT)
RETURN
7 IL = NT-NP+1
GO TO 20
8 IF(I .GT. 1) GO TO 10
ILAST = 1
IF(K .GE. 1) GO TO 9
TLOOK = QT(1)
RETURN
9 IL = 1
GO TO 20
10 ILAST = I-1
IL = I-NP/2
GO TO 20
C TABLE PT IS IN DESCENDING ORDER
15 IF(PT(I) .LE. P .AND. PT(ILAST) .GE. P) GO TO 8
DO 16 I=1,NT
IF(P .GE. PT(I)) GO TO 8
16 CONTINUE
GO TO 6
20 IF(IL .LT. 1) IL = 1
IF(IL .GT. NT-NP+1) IL = NT-NP+1
DO 21 J = 1,NP
L = IL+J-1
XT(J) = PT(L)
YT(J) = QT(L)
CALL LAGRNG(P,Y,XT,YT,NP)
TLOOK = Y
RETURN
END

```

```
SIBFTC LAGRNG M94/2,XR7,OECK
SUBROUTINE LAGRNG(X,Y,XT,YT,N)
C
C THIS ROUTINE USES A LAGRANGIAN POLYNOMIAL BASED ON N TABULAR
C POINTS TO INTERPOLATE Y AS A FUNCTION OF X IN A TWO DIMENSIONAL
C TABLE.
C
DIMENSION XT(1), YT(1)
DO 1 I=1,N
IF(X .EQ. XT(I)) GO TO 5
1 CONTINUE
L1 = 1
L2 = N-1
S = (XT(N)-XT(1))/ABS(XT(N)-XT(1))
DO 6 I=L1,L2
IF(ABS(XT(I)-XT(I+1)) .GT. .001*ABS(XT(1))) GO TO 7
IF((X-XT(I))*S .LE. 0.) GO TO 8
L1 = I+1
GO TO 6
8 L2 = I
GO TO 9
7 CONTINUE
L2 = N
Y = 0.
9 DO 3 I=L1,L2
Z = 1.
DO 2 J=L1,L2
IF(J .EQ. I) GO TO 2
Z = Z*(X-XT(J))/(XT(I)-XT(J))
2 CONTINUE
3 Y = Y+Z*YT(I)
RETURN
5 Y = YT(I)
RETURN
ENO
```

```
SIBFTC SRCHXX M94/2,XR7,DECK
      SUBROUTINE SRCHX(V,VT,N,KEX,IL,C)
C
C      THIS ROUTINE LOCATES V IN TABLE VT
C      IF KEX = 0, LIMIT OUTPUT TO TABLE BOUNDARY
C      IF KEX = 1, EXTRAPOLATE IF V IS OUTSIDE TABLE
      DIMENSION VT(N)
      IF(VT(2) .LT. VT(1)) GO TO 6
C      TABLE VT IS IN ASCENDING ORDER
      DO 1 I=1,N
      IF(V-VT(I)) 2,2,1
1    CONTINUE
15   IL = N-1
      IF(KEX .EQ. 1) GO TO 3
      C = 1.
      RETURN
2    IL = I-1
      IF(I .EQ. 1) GO TO 4
3    C = (V-VT(IL))/(VT(IL+1)-VT(IL))
      RETURN
4    IL = 1
      IF(KEX .EQ. 1) GO TO 3
      C = 0.
      RETURN
C      TABLE VT IS IN DESCENDING ORDER
5    DO 7 I=1,N
      IF(V-VT(I)) 7,2,2
7    CONTINUE
      GO TO 15
END
```

```

SIBFTC PROCOM M94,XR7,OECK
SUBROUTINE PROCOM(FARX,TEX,CSEX,AKEX,CPEX,REX,SEX,MEX)
IF(TEX<300.)12,3,3
12 WRITE(6,102)
102 FORMAT(1H0,35HPROCOM INPUT TEMPERATURE BELOW 300.)
RETURN
3 IF(TEX>4500.)15,5,4
4 WRITE(6,103)
103 FORMAT(1H0,36HPROCOM INPUT TEMPERATURE ABOVE 4500.)
RETURN
5 IF(FARX)<6.7,7
6 WRITE(6,104)
104 FORMAT(1H0,38HPROCOM INPUT FUEL-AIR RATIO BELOW ZERO)
FARX=0.0
C AIR PATH
7 CPA = (((((1.0115540E-25*TEX-1.4526770E-21)*TEX
1+7.6215767E-18)*TEX-1.5128259E-14)*TEX-6.7178376E-12)
2*TEX+6.5519486E-08)*TEX-5.1536879E-05)*TEX+2.5020051E-01
MEA=(((((1.2644425E-26*TEX-2.0752522E-22)*TEX
1+1.2702630E-18)*TEX-3.0256518E-15)*TEX-1.6794594E-12)*TEX
2+2.1839826E-08)*TEX-2.5768440E-05)*TEX+2.5020051E-01)*TEX
3-1.7558886E+00
SEA=+2.5020051E-01 ALOG(TEX)+((((1.4450767E-26*TEX
1-2.4211288E-22)*TEX+1.5243153E-18)*TEX-3.7820648E-15)*TEX
2-2.2392790E-12)*TEX+3.2759743E-08)*TEX-5.1576879E-05)*TEX
3+4.5432300E-02
IF(FARX)>200,200,8
C FUEL/AIR PATH
8 IF(FARX-.067623)>10,10,9
9 WRITE(6,101)
101 FORMAT(1H0,63HINPUT FUEL-AIR RATIO ABOVE LIMITS, IT HAS BEEN RESET
2TO 0.067623)
FARX=0.067623
10 CPF = (((((7.2678710E-25*TEX-1.3335668E-20)*TEX
1+1.0212913E-16)*TEX-4.2051104E-13)*TEX+9.9686793E-10)*TEX
2-1.3771901E-06)*TEX+1.2258630E-03)*TEX+7.3816638E-02
HEF=(((((9.0848388E-26*TEX-1.9050949E-21)*TEX
1+1.7021523E-17)*TEX-8.4102208E-14)*TEX+2.4921698E-10)*TEX
2-4.5906332E-07)*TEX+6.1293150E-04)*TEX+7.3816638E-02)
3*TEX+3.0581530E+01
SEF=+7.3816638E-02 ALOG(TEX)+((((1.0382670E-25*TEX
1-2.2226118E-21)*TEX+2.0425826E-17)*TEX-1.0512776E-13)*TEX
2+3.3228928E-10)*TEX-6.8859505E-07)*TEX+1.2258630E-03)*TEX
3+6.483398E-01
200 CPEX=(CPA+FARX*CPF)/(1.+FARX)
MEX=(MEA+FARX*HEF)/(1.+FARX)
SEX=(SEA+FARX*SEF)/(1.+FARX)
AMW=28.97-.946186*FARX
REX=1.986375/AMW
AKEX=CPEX/(CPEX-REX)
CSEX=SQRT(AKEX*REX*TEX*25031.37)
RETURN
ENO

```

```

S1BFTC AFQUIR M94,XR7,DECK
  SUBROUTINE AFQUIR(X,AIND,DEPEND,ANS,AJ,TDL,DIR,ANEW,ICON)
  DIMENSION X(9)

C X(1)=NAME OF ARRAY TO USE
C AIND=INDEPENDANT VARIABLE
C DEPEND= DEFENDANT VARIABLE
C ANS=ANSWER UPON WHICH TO CONVERGE
C AJ=MAX NUMBER OF TRYS
C TOL=PERCENT TOLEKANCE FOR CONVERGENCE
C DIR=DIRECTION AND PERCENTAGE FOR FIRST GUESS
C ANEW=CALCULATED VALUE OF NEXT TRY AT INDEPENDANT VARIABLE
C ICON=CONTROL   =1 GO THRU LOOP AGAIN
C           =2 YOU HAVE REACHED THE ANSWER
C           =3 COUNTER HAS HIT LIMITS
C X(2)=COUNTER STORAGE
C X(3)=CHOSES METHOD OF CONVERGENCE
C X(4)=THIRD DEPEND VAR
C X(5)=THIRD IND VAR
C X(6)=SECOND DEPEND VAR
C X(7)=SECOND IND VAR
C X(8)=FIRST DEPEND VAR
C X(9)=FIRST IND VAR
C X(3) MUST BE ZERD UPDN FIRST ENTRY TO ROUTINE

Y=0.
IF(ANS)1,2,1
1  DEP=DEPEND-ANS
TDLANS=TDL*ANS
GO TO 3
2  DEP=DEPEND
TOLANS=TDL
3  IF(ABS(DEP)-TOLANS)5,5,4
4  IF(X(2)-AJ)8,8,7
5  ANEW=AIND
X(2)=0.
ICON=2
RETURN
6  ANEW=Y
X(2)=X(2)+1.
ICON=1
RETURN
7  ANEW=Y
X(2)=0.
ICON=3
RETURN
8  IF(X(3))9,9,12
C *** FIRST GUESS USING DIR
9  X(3)=1.
X(8)=DEP
X(9)=AIND
IF(AIND)10,11,10
10 Y=DIR*AIND
GO TO 6
11 Y=DIR
GO TO 6
12 IF(X(3)-1.)13,13,16
C *** LINEAR GUESS
13 X(3)=2.
X(6)=DEP
X(7)=AIND
IF(X(8)-X(6))14,9,14
14 IF(X(9)-X(7))15,9,15

```

```

15    A=(X(9)-X(7))/(X(8)-X(6))
      Y=X(9)-A*X(8)
      IF(ABS(10.*X(9))-ABS(Y))19,9,6
C *** QUADRATIC GUESS
16    X(4)=OEP
      X(5)=AINO
      IF(X(7)-X(5))18,17,18
17    IF(X(6)-X(4))13,9,13
18    IF(X(6)-X(4))19,13,19
19    IF(X(9)-X(5))23,20,23
20    IF(X(8)-X(4))21,22,21
21    X(9)=X(7)
      X(8)=X(6)
      GO TO 13
22    X(9)=X(7)
      X(8)=X(6)
      X(3)=1.
      IF(X(9))10,11,10
23    IF(X(8)-X(4))24,21,24
24    F=(X(6)-X(4))/(X(7)-X(5))
      A=(X(8)-X(4)-F*(X(9)-X(5)))/((X(9)-X(7))*(X(9)-X(5)))
      B=F-A*(X(5)+X(7))
      C=X(4)+X(5)*(A+X(7)-F)
      IF(A)242,240,242
240   IF(B)241,7,241
241   Y=-C/B
      GO TO 37
242   IF(B)247,243,247
243   IF(C)245,244,245
244   Y=0.
      GO TO 37
245   G=-C/A
      IF(G)7,7,246
246   Y=SQRT(G)
      YY=-SQRT(G)
      GO TO 270
247   IF(C)249,248,249
248   Y=-B/A
      YY=0.
      GO TO 270
249   D=4.*A*C/B**2
      IF(1.-D)13,25,26
25    Y=-B/(2.*A)
      GO TO 37
26    E=SQRT(1.-D)
27    Y=(-B/(2.*A))*(1.+E)
      YY=(-B/(2.*A))*(1.-E)
270   J=4
      DEPMIN=ABS(X(4))
      DO 29 I=6,8,2
      IF(DEPMIN-ABS(X(I)))29,29,28
28    J=I
      DEPMIN=ABS(X(I))
      CONTINUE
      K=J+1
      IF((X(K)-Y)*(X(K)-YY))32,32,30
30    IF(ABS(X(K)-Y)-ABS(X(K)-YY))37,37,31
31    Y=YY
      GO TO 37
32    IF(J=6)33,34,34
33    JJ=J+2
      KK=K+2

```

```
      GO TO 35
34    JJ=J-2
      KK=K-2
35    SLOPE=(X(KK)-X(K))/(X(JJ)-X(J))
      IF(SLOPE*X(J)*(X(K)-Y))36,36,37
36    Y=YY
37    X(9)=X(7)
      X(8)=X(6)
      X(7)=X(5)
      X(6)=X(4)
      GO TO 6
      END
```

```
SIBFTC CRITXX M94,XR7,OECK
SUBROUTINE CRITCL(ALAM,TERM)
DIMENSION ALMTAB(13),TRMTAB(13)
DATA(ALMTAB()),I=1,13)/-6.,-5.,-4.,-3.,-2.,-1.,0.,
A1.,2.,3.,4.,5.,6./
DATA(TRMTAB()),I=1,13)/0.,120.,138.,175.,250.,375.,
A645.,1125.,2000.,3500.,5500.,8000.,10000./
CALL SRCHX(ALAM,ALMTAB(),13,0,IL,C)
TERM=TRMTAB(IL)+C*(TRMTAB(IL+1)-TRMTAB(IL))
RETURN
END
```

DATA
FOR
SAMPLE PROBLEM
ONE
SUCTION SURFACE

050	
0.0	0.0
0.0460	979.01
0.0920	1708.05
0.1380	1783.37
0.1840	1872.09
0.2300	1932.82
0.2760	1995.84
0.3220	2040.62
0.3680	2101.52
0.4141	2156.37
0.4601	2244.38
0.5061	2311.80
0.5521	2366.87
0.5981	2422.29
0.6441	2472.06
0.6901	2533.90
0.7361	2611.21
0.7821	2653.90
0.8281	2708.52
0.8741	2789.65
0.9201	2841.08
0.9661	2875.03
1.0121	2926.40
1.0581	2946.46
1.1041	2972.77
1.1501	2987.53
1.1962	2995.23
1.2422	2999.11
1.2882	2998.92
1.3342	2995.76
1.3802	2992.24
1.4262	2980.23
1.4722	2971.30
1.5182	2955.19
1.5642	2932.29
1.6102	2901.40
1.6562	2901.40
1.7022	2882.99
1.7482	2865.65
1.7942	2841.45
1.8402	2822.82
1.8862	2802.41
1.9322	2779.79
1.9783	2762.91
2.0243	2739.22
2.0703	2715.27
2.1163	2692.51
2.1623	2669.67
2.2083	2642.64
2.2543	2646.15

SAMPLE PROBLEM NUMBER ONE

SINPUT ALENGTH=0.15945,TTZERO=3510.,PTZERO=57.2,UCRIT=2714.,
AK=1.26,UIN=900.,DIA=0.013333,PRINT=1.E-2,DX=1.E-58

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SUCTION SURFACE

SAMPLE PROBLEM NUMBER ONE

X= 0.	UX= 0.	T= 0.3510000E 04
P= 0.5720000E 02	VISK= 0.9318774E-03	THETA= 0.1893401E-04
OEL= 0.1611954E-03	OELSTR= 0.4835746E-04	UOOVIS= -0.0000000E-19
TRMCRT= -0.0000000E-19	ALAM= 0.7052900E 01	PN= 0.7742500E 00
OELTA= -0.0000000E-19	OELT= 0.2284553E-03	ML= 0.4968198E 03
TAO= 0.3510000E 04		
X= 0.9990000E-02	UX= 0.1789103E 04	T= 0.3334522E 04
P= 0.4461234E 02	VISK= 0.1103231E-02	THETA= 0.3177282E-04
OEL= 0.2704991E-03	OELSTR= 0.8114778E-04	UOOVIS= 0.1315968E 03
TRMCRT= 0.7859695E 03	ALAM= 0.2936866E-00	PN= 0.7628164E 00
OELTA= 0.1415952E 01	OELT= 0.3830136E-03	ML= 0.2908361E 03
TAO= 0.3487783E 04		
X= 0.1998000E-01	UX= 0.1946693E 04	T= 0.3302247E 04
P= 0.4255835E 02	VISK= 0.1139101E-02	THETA= 0.5320450E-04
OEL= 0.4529584E-03	OELSTR= 0.1358843E-03	UOOVIS= 0.2322226E 03
TRMCRT= 0.3637746E 04	ALAM= 0.3068873E 01	PN= 0.7614853E 00
OELTA= 0.1304691E 01	OELT= 0.5909708E-03	ML= 0.1876126E 03
TAO= 0.3483539E 04		
X= 0.2997000E-01	UX= 0.2090257E 04	T= 0.3270475E 04
P= 0.4061036E 02	VISK= 0.1175906E-02	THETA= 0.6427801E-04
OEL= 0.5472332E-03	OELSTR= 0.1641660E-03	UOOVIS= 0.2918169E 03
TRMCRT= 0.5844446E 04	ALAM= 0.4137778E 01	PN= 0.7602210E 00
OELTA= 0.1305334E 01	OELT= 0.7143219E-03	ML= 0.1544796E 03
TAO= 0.3479318E 04		
X= 0.3996000E-01	UX= 0.2274878E 04	T= 0.3226294E 04
P= 0.3801994E 02	VISK= 0.1229694E-02	THETA= 0.6808716E-04
OEL= 0.5796625E-03	OELSTR= 0.1738946E-03	UOOVIS= 0.3216970E 03
TRMCRT= 0.7683456E 04	ALAM= 0.4873382E 01	PN= 0.7582584E 00
OELTA= 0.1349648E 01	OELT= 0.7823404E-03	ML= 0.1401398E 03
TAO= 0.3473340E 04		
X= 0.4995000E-01	UX= 0.2423690E 04	T= 0.3187962E 04
P= 0.3588031E 02	VISK= 0.1278979E-02	THETA= 0.7368910E-04
OEL= 0.6273549E-03	OELSTR= 0.1882020E-03	UOOVIS= 0.3566465E 03
TRMCRT= 0.5445121E 04	ALAM= 0.3972560E 01	PN= 0.7561379E 00
OELTA= 0.1367097E 01	OELT= 0.8576547E-03	ML= 0.1271730E 03
TAO= 0.3467799E 04		
X= 0.5994000E-01	UX= 0.2584312E 04	T= 0.3143864E 04
P= 0.3353821E 02	VISK= 0.1338901E-02	THETA= 0.7690438E-04
OEL= 0.6547282E-03	OELSTR= 0.1964138E-03	UOOVIS= 0.3791129E 03
TRMCRT= 0.1000000E 05	ALAM= 0.6485039F 01	PN= 0.7536534E 00
OELTA= 0.1396174E 01	OELT= 0.9141145E-03	ML= 0.1185997E 03
TAO= 0.3461718E 04		
X= 0.6993000E-01	UX= 0.2727728E 04	T= 0.3102099E 04
P= 0.3143352E 02	VISK= 0.1399058E-02	THETA= 0.8105530E-04
OEL= 0.6900672E-03	OELSTR= 0.2070152E-03	UOOVIS= 0.4036154E 03
TRMCRT= 0.1000000E 05	ALAM= 0.7281691E 01	PN= 0.7513070E 00
OELTA= 0.1412590E 01	OELT= 0.9747819E-03	ML= 0.1105676E 03
TAO= 0.3455659E 04		
X= 0.7992000E-01	UX= 0.2869559E 04	T= 0.3058578E 04
P= 0.2935326E 02	VISK= 0.1465535E-02	THETA= 0.8512876E-04
OEL= 0.7247468E-03	OELSTR= 0.2174188E-03	UOOVIS= 0.4257123E 03
TRMCRT= 0.3966627E 04	ALAM= 0.3233314E 01	PN= 0.7489302E 00

OELTA= 0.1426261E 01 TAD= 0.3449242E 04	DELT= 0.1033678E-02	HL= 0.1036072E 03
X= 0.8991000E-01 P= 0.2805268E D2 DEL= 0.7836371E-03 TRMCRT= 0.3313718E D4 OELTA= 0.1415977E 01 TAO= 0.3445030E D4	UX= 0.2958661E D4 VISK= 0.1511253E-02 DELSTR= 0.2350855E-03 ALAM= 0.2875812E 01 DELT= 0.1109612E-02	T= 0.30301D9E 04 THETA= 0.9204601E-04 UDQVIS= 0.4602395E D3 PN= 0.7475599E 00 HL= 0.9608484E 02
X= 0.999D000E-01 P= 0.2751652E D2 DEL= 0.8645095E-03 TRMCRT= 0.9882192E 03 OELTA= 0.1388053E 01 TAD= 0.3443239E 04	UX= 0.2995553E D4 VISK= 0.1531149E-02 DELSTR= 0.2593467E-03 ALAM= 0.7150400E 00 DELT= 0.1199985E-02	T= 0.3018067E 04 THETA= 0.1015453E-03 UDQVIS= 0.5073881E 03 PN= 0.7469943E 00 HL= 0.8867655E 02

TRANSITION AT X= 0.1076700E-00

X= 0.1076700E-00 P= 0.2747037E D2 DEL= 0.9372568E-03 TRMCRT= 0.5496133E 03 OELTA= 0.1361217E 01 TAD= 0.3443083E D4	UX= 0.2998734E 04 VISK= 0.1532892E-02 DELSTR= 0.2811703E-03 ALAM= -0.3532841E-00 DELT= 0.1275678E-02	T= 0.3017021E 04 THETA= 0.11009D2E-03 UDQVIS= 0.550D421E D3 PN= 0.7469456E 00 HL= 0.83400D75E 02
X= 0.1098900E-00 P= 0.2749557E D2 CF2= 0.9145630E-03 PN= 0.7469722E 00	UX= 0.2996996E 04 VISK= 0.1531939E-02 RMD= 0.7642255E-03 TAO= 0.3464371E D4	T= 0.3017592E 04 THETA= 0.9122335E-04 TUQV= 0.1784640E D3 HX= 0.3184159E D3
X= 0.1198800E-00 P= 0.27772D9E D2 CF2= 0.9130137E-03 PN= 0.7472640E 00	UX= 0.2977954E 04 VISK= 0.1521585E-02 RMD= 0.77D3190E-03 TAD= 0.3465007E D4	T= 0.302383DE 04 THETA= 0.1268618E-03 TUQV= 0.2482862E D3 HX= 0.2916595E D3
X= 0.1298700E-00 P= 0.2838903E D2 CF2= 0.9096209E-03 PN= 0.7479144E 00	UX= 0.2935570E 04 VISK= 0.1499094E-02 RHO= 0.7838692E-03 TAD= 0.3466403E D4	T= 0.303757DE 04 THETA= 0.1642179E-03 TUQV= 0.3215763E D3 HX= 0.2728721E D3
X= 0.1398600E-00 P= 0.29001D3E D2 CF2= 0.9063392E-03 PN= 0.7485592E 00	UX= 0.2893645E 04 VISK= 0.1477577E-02 RHO= 0.7972509E-03 TAD= 0.3467759E 04	T= 0.3050968E 04 THETA= 0.2009674E-03 TUQV= 0.3935687E D3 HX= 0.2591173E D3
X= 0.1498500E-00 P= 0.2979026E D2	UX= 0.2839714E 04 VISK= 0.145D926E-02	T= 0.3067919E 04 THETA= 0.241D173E-03

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CF2= 0.9022244E-03	RHO= 0.8144224E-03	TUQV= 0.4717127E 03
PN= 0.7494271E 00	TAD= 0.3469474E 04	HX= 0.2474587E 03
X= 0.1598400E-00	UX= 0.2786490E 04	T= 0.3084336E 04
P= 0.3057077E 02	VISK= 0.1425708E-02	THETA= 0.2821632E-03
CF2= 0.8982782E-03	RHO= 0.8313121E-03	TUQV= 0.5514767E 03
PN= 0.7503235E 00	TAD= 0.3471133E 04	HX= 0.2377090E 03
X= 0.1698300E-00	UX= 0.2732069E 04	T= 0.3100800E 04
P= 0.3136976E 02	VISK= 0.1400985E-02	THETA= 0.3253351E-03
CF2= 0.8943584E-03	RHO= 0.8485095E-03	TUQV= 0.6344379E 03
PN= 0.7512347E 00	TAD= 0.3472787E 04	HX= 0.2291490E 03
X= 0.1798200E-00	UX= 0.2672002E 04	T= 0.3118595E 04
P= 0.3225190E 02	VISK= 0.1374886E-02	THETA= 0.3726592E-03
CF2= 0.8901637E-03	RHO= 0.8673923E-03	TUQV= 0.7242392E 03
PN= 0.7522297E 00	TAD= 0.3474562E 04	HX= 0.2211537E 03

DATA
FOR
SAMPLE PROBLEM
TWO
PRESSURE SURFACE

052
0.0 0.0
0.020 450.
0.0398 858.41
0.060 1220.
0.0795 1509.01
0.1193 619.57
0.1591 597.11
0.1988 597.11
0.2386 594.67
0.2784 597.11
0.3182 597.11
0.3579 597.11
0.3977 602.20
0.4675 608.53
0.4772 624.25
0.5170 627.84
0.5568 638.86
0.5965 657.37
0.6363 680.57
0.6761 703.61
0.7158 722.00
0.7556 758.18
0.7954 776.07
0.8352 818.28
0.8749 836.17
0.9147 876.76
0.9545 896.55
0.9942 926.74
1.0340 944.86
1.0738 972.54
1.1135 997.11
1.1533 1027.38
1.1931 1050.58
1.2328 1094.16
1.2726 1146.04
1.3124 1269.38
1.3522 1319.13
1.3919 1348.27
1.4317 1400.73
1.4715 1442.27
1.5112 1492.66
1.5510 1539.72
1.5908 1577.51
1.6305 1645.02
1.6703 1731.88
1.7101 1809.32
1.7498 1911.27
1.7896 1981.68
1.8294 2089.07
1.8692 2189.85
1.9089 2280.51
1.9487 2382.70

SAMPLE PROBLEM NUMBER TWO

\$INPUT ALENTH=0.15945,TTZERO=3510.,PTZERO=57.2,UCRIT=2714.,
AK=1.26,UIN=900.,DIA=0.013333,PRINT=1.E-2,DX=1.E-5\$

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PRESSURE SURFACE

SAMPLE PROBLEM NUMBER TWO

X= 0.	UX= 0.	T= 0.3510000E 04
P= 0.5720000E 02	VISK= 0.9318774E-03	THETA= 0.1806377E-04
DEL= 0.1537866E-03	DELSTR= 0.4613487E-04	U00V1S= -0.0000000E-19
TRMCRT= -0.0000000E-19	ALAM= 0.7052900E 01	PN= 0.7742500E 00
DELT= -0.0000000E-19	DELT= 0.2284553E-03	HL= 0.4968198E 03
TAD= 0.3510000E 04		

TRANSITION AT X= 0.6940000E-02

X= 0.6940000E-02	UX= 0.1481076E 04	T= 0.3389744E 04
P= 0.4830857E 02	VISK= 0.1045191E-02	THETA= 0.2497281E-04
DEL= 0.2126069E-03	DELSTR= 0.6378055E-04	UDQVIS= 0.9037951E 02
TRMCRT= 0.7968158E 02	ALAM= -0.5335987E 01	PN= 0.7653682E 00
DELT= 0.1497112E 01	DELT= 0.3167091E-03	HL= 0.3543541E 03
TAD= 0.3494925E 04		
X= 0.9990000E-02	UX= 0.6150699E 03	T= 0.3489260E 04
P= 0.5558060E 02	VISK= 0.9502386E-03	THETA= 0.4114564E-03
CF2= 0.8116362E-03	RHO= 0.1336008E-02	TUQV= 0.2663273E 03
PN= 0.7724281E 00	TAO= 0.3508290E 04	HX= 0.1023814E 03
X= 0.1998000E-01	UX= 0.5947076E 03	T= 0.3490611E 04
P= 0.5568493E 02	VISK= 0.9490288E-03	THETA= 0.4848506E-03
CF2= 0.8113777E-03	RHO= 0.1337998E-02	TUQV= 0.3038310E 03
PN= 0.7725442E 00	TAD= 0.3508402E 04	HX= 0.9570405E 02
X= 0.2997000E-01	UX= 0.5972618E 03	T= 0.3490444E 04
P= 0.5567203E 02	VISK= 0.9491782E-03	THETA= 0.5090107E-03
CF2= 0.8114096E-03	RHO= 0.1337752E-02	TUQV= 0.3202904E 03
PN= 0.7725298E 00	TAO= 0.3508388E 04	HX= 0.9475287E 02
X= 0.3996000E-01	UX= 0.6267583E 03	T= 0.3488465E 04
P= 0.5551920E 02	VISK= 0.9509524E-03	THETA= 0.4668246E-03
CF2= 0.8117885E-03	RHO= 0.1334837E-02	TUQV= 0.3076770E 03
PN= 0.7723598E 00	TAO= 0.3508223E 04	HX= 0.1002918E 03
X= 0.4995000E-01	UX= 0.6589614E 03	T= 0.3486195E 04
P= 0.5534436E 02	VISK= 0.9529923E-03	THETA= 0.4294948E-03

CF2= 0.8122236E-03 PN= 0.7721659E 00 X= 0.5994000E-01 P= 0.5496C10E 02 CF2= 0.8131852E-03 PN= 0.7717417E 00 X= 0.6993000E-01 P= 0.5434445E 02 CF2= 0.8147424E-03 PN= 0.7710679E 00 X= 0.7992000E-01 P= 0.5377816E 02 CF2= 0.8161931E-03 PN= 0.7704551E 00 X= 0.8991000E-01 P= 0.5319458E 02 CF2= 0.8171068E-03 PN= 0.7698310E 00 X= 0.9990000E-01 P= 0.5253218E 02 CF2= 0.8194486E-03 PN= 0.7691326E 00 X= 0.1098900E-00 P= 0.5043962E 02 CF2= 0.8251241E-03 PN= 0.7670051E 00 X= 0.1198800E-00 P= 0.4911196E 02 CF2= 0.8288693E-03 PN= 0.7659678E 00 X= 0.1298700E-00 P= 0.4756542E 02 CF2= 0.8333838E-03 PN= 0.7648301E 00 X= 0.1398600E-00 P= 0.4514220E 02 CF2= 0.8408131E-03 PN= 0.7631662E 00 X= 0.1498500E-00 P= 0.4179890E 02 CF2= 0.8518649E-03 PN= 0.7609956E 00 X= 0.1598400E-00 P= 0.3762851E 02 CF2= 0.8671912E-03 PN= 0.7578822E 00	RHO= 0.1331499E-02 TAD= 0.3508034E 04 UX= 0.7249753E 03 VISK= 0.9575137E-03 RHO= 0.1324157E-02 TAO= 0.3507616E 04 UX= 0.8203803E 03 VISK= 0.9648691E-03 RHO= 0.1312371E-02 TAO= 0.3506937E 04 UX= 0.8998981E 03 VISK= 0.9717594E-03 RHO= 0.1301506E-02 TAO= 0.3506304E 04 UX= 0.9756962E 03 VISK= 0.9879083E-03 RHO= 0.1290285E-02 TAO= 0.3505642E 04 UX= 0.1055869E 04 VISK= 0.9873564E-03 RHO= 0.1277516E-02 TAO= 0.3504880E 04 UX= 0.1280759E 04 VISK= 0.1014995E-02 RHO= 0.1236960E-02 TAO= 0.3502390E 04 UX= 0.1408113E 04 VISK= 0.1033550E-02 RHO= 0.1211049E-02 TAO= 0.3500756E 04 UX= 0.1546309F 04 VISK= 0.1056252E-02 RHO= 0.1180682E-02 TAO= 0.3498794E 04 UX= 0.1747139E 04 VISK= 0.1094422E-02 RHO= 0.1132690E-02 TAO= 0.3495583E 04 UX= 0.2003249E 04 VISK= 0.1153108E-02 RHO= 0.1065585E-02 TAO= 0.3490855E 04 UX= 0.2302305F 04 VISK= 0.1238359E-02 RHO= 0.9803017E-03 TAO= 0.3484350E 04	TUQV= 0.2969809E 03 HX= 0.1061871E 03 T= 0.3481186E 04 THETA= 0.3500712E-03 TUQV= 0.2650542E 03 HX= 0.1197856E 03 T= 0.3473104E 04 THETA= 0.2687294E-03 TUQV= 0.2284873E 03 HX= 0.1398232E 03 T= 0.3465604E 04 THETA= 0.2327934E-03 TUQV= 0.2155784E 03 HX= 0.1545282E 03 T= 0.3457811E 04 THETA= 0.2126662E-03 TUQV= 0.2119511E 03 HX= 0.1668912E 03 T= 0.3448882E 04 THETA= 0.1979046E-03 TUQV= 0.2116372E 03 HX= 0.1789277E 03 T= 0.3420074E 04 THETA= 0.1360377E-03 TUQV= 0.1716574E 03 HX= 0.2224568E 03 T= 0.3401300E 04 THETA= 0.1331502E-03 TUQV= 0.1814045E 03 HX= 0.2359600E 03 T= 0.3378917E 04 THETA= 0.1311976E-03 TUQV= 0.1920679E 03 HX= 0.2487954E 03 T= 0.3342657E 04 THETA= 0.1196315E-03 TUQV= 0.1909801E 03 HX= 0.2701050E 03 T= 0.3290000E 04 THETA= 0.1087852E-03 TUQV= 0.1889882E 03 HX= 0.2921286E 03 T= 0.3219412E 04 THETA= 0.1014762E-03 TUQV= 0.1886604E 03 HX= 0.3089611E 03
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REFERENCES

1. J. R. Arvin. Quasi Three Dimensional Blade Surface Velocity Calculations. Technical Data Report AX .0010-007. Allison Division of General Motors Corp. 21 June 1965.
2. David H. Quick, Robert E. Henderson, and Wayne A. Tall. Experimental Cold Flow Investigation of Chordwise Static Pressure Distribution Around a Turbine Foil. Technical Report AFAPL-TR-67-147. Air Force Aero Propulsion Laboratory, Wright-Patterson AFB, Ohio. March 1968.
3. H. B. Squire. Heat Transfer Calculation for Aerofoils. Report No. 1986. Ministry of Aircraft Production. November 1942.
4. H. Schlichting. Boundary Layer Theory. Translated by Dr. J. Kestin. 4th Edition. McGraw-Hill Book Company, Inc., New York.
5. E. Truckenbrodt. A Method of Quadrature for the Calculation of the Laminar and Turbulent Boundary Layer in Case of Plane and Rotationally Symmetrical Flow. Technical Memorandum 1379. National Advisory Committee for Aeronautics. 1952.