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DEVELOPMENT OF AN IMPROVED JAN 6299

FINAL REPORT

1 May 1961 through 30 June 1964

- OBJECTIVE: (1) To obtain better performance and greater reliability from the JAN 6299 by evaluating and adapting the latest tube technological advancements.
 - (2) To build 1000 tubes capable of passing Signal Corps Technical Requirements SCS-90 dated 1 July 1960.

CONTRACT NO. DA-36-039-SC-85953

SIGNAL CORPS TECHNICAL REQUIREMENTS SCS-90, 1 July 1960

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Report Prepared By:

D. L. Cook

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ABSTRACT

The period covered by this report is from 1 May 1961 through 30 June 1964. No work was performed from 30 April 1962 to 17 September 1962 when manufacturing facilities were being transferred from Scranton, Pennsylvania to Owensboro, Kentucky.

The pilot run has been completed; test data is shown in Project VIII.

Results from improved alignment and concentricity, optimization of cathode coating and improved exhaust fixturing are now being applied to regular production tubes.

Best results during humidity test have been obtained by improving plating techniques and controls to minimize metal shell corrosion.

The improved tubes have given superior life test results with the anode seal temperature at 225° C.

The inverted cathode support ring results in cathode subassemblies with better uniformity and increased ruggedness.

The temperature controller has been shown to decrease operator skill necessary to perform uniform exhaust cycles.

The extended life test has completed 1795 hours. The complete data and failure analysis will be presented in an addendum to the Final Report.

-1-

PURPOSE

The purpose of this contract is to evaluate certain areas of advanced tube manufacturing techniques and apply them where feasible to JAN 6299 to result in a more reliable and better performing tube. The objective requirements for the improved tube are Signal Corps Technical Requirement SCS-90 (Improved JAN 6299) and operation at a tube temperature rating of 225° C. The areas investigated were:

- 1. Improved alignment, concentricity and ceramic strength.
- 2. Improved anode to ceramic seal.
- 3. Temperature control at exhaust.
- 4. Improved application of cathode coating.
- 5. Improved cathode mounting.
- 6. Improved processing for higher temperature operation.
- 7. Improvement in humidity testing.
- 8. Improved exhaust fixturing.
- 9. Extended life test and tube failure analysis.

NARRATIVE

Project I IMPROVED ALIG'MENT, CONCENTRICITY, AND CERAMIC STRENGTH

All eccentricity dimensions presently listed for JAN 6299 are measured with respect to the centerline of the tube using a go, no-go type of gauge as outlined in the existing MIL-E-1/484B specification. Since actual eccentricity measurements would be required for a proper evaluation of improved tube alignment as a result of using tighter dimensioned parts, it was decided to build a gauge capable of providing this type of information. For reasons of simplicity in gauge construction, the grid terminal of the tube was used as a reference and the eccentricity of the anode, cathode, getter, and heater pin terminals were measured from this point. An illustration is shown in Figure 1.

In an effort to improve the alignment and concentricity of the tube, the ceramics and metal parts have been made to tighter tolerences. The ceramic composition has been changed from forsterite to 96% alumina in the heater, getter, and anode ceramics for greater strength. The cathode ceramic, when changed to 96% alumina, produced a median Cgk of 4.81 pf. This is an increase of 31.8% over the bogy value of 3.65 pf. Redesign of the cathode ceramic to compensate for a change of this magnitude, it is felt would be a major design change.

The improvements made in this project enable improved exhaust fixturing (Project IX) to further improve alignment and concentricity of the tube.

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Project II IMPROVED ANODE SEAL

The general configeration of the present design and the hard solder designs is shown in Figure 2.

The getter ceramic was redesigned to provide a better sealing surface for the hard solder seals. The material was changed from forsterite to 96% alumina for improved strength. The two metal shells were changed from copper clad steel to #142 nickel-iron alloy to obtain a closer expansion match. A new getter assembly was obtained to fit the new configeration. The butt seals were obtained utilizing silver-copper eutectic.

The anode seal is a butt seal using silver-copper eutectic. Care must be taken when metalizing this seal to prevent grid-plate capacitance from being too high.

It was found during the course of the contract that the metalizing was not giving consistently strong seals. A much better seal was obtained by using a metalizing mix of finer particle size to give better adhesion to the ceramic at the butt seals.

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CONFIGURATION OF PRESEAL AND ANODE SEALS Figure 2

Project III TEMPERATURE CONTROL AT EXHAUST

One of the major factors contributing to the variation experienced in tubes is the lack of temperature control at exhaust. A molybdenum oven encloses the tubes in a fixture and RF energy is used to heat the oven, outgassing and sealing the tubes.

The temperature controller shown in Figure 3 was used to regulate the RF energy input during exhaust processing. Several trial neating schedules were examined, with the best results obtained using a schedule approximating the schedule being used in production.

The temperature controller was used to control processing on two exhaust sets during the day shift and the method of observation of Isobutyl Methacrylate and titanium hydride pressure breakdowns was used to indicate the manual settings on the night shift as in the last quarter.

An evaluation was undertaken of the difference in exhaust losses by the two methods. There were 2320 tube mounts exhausted by the manual method and 1580 tube mounts exhausted in conjunction with the temperature controller. The temperature controller method had 2.3% less exhaust shrinkage than the manual method. This would indicate the temperature controller gives more consistent processing at exhaust resulting in better uniformity of seals.

Test data was tabulated for 1293 of the tubes processed at exhaust by the temperature controller and 1500 tubes which were processed at exhaust by the manual control method. The tubes with exhaust processing regulated by the temperature controller had a 5.67 improvement in yield. This also indicates improved processing which is resulting in more consistent tube quality.

-7-

The temperature controller does decrease the operator skill required to perform a uniform exhaust cycle and therby insures a more consistently uniform product.



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Project IV OPTIMIZE CATHODE COATING

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In order to reduce variations in cathode coating density, an evaluation of cathode spray guns, spray fixtures and cathode density was undertaken. A Paasche A - Automatic spray gun was composed with the DeVilbiss spray gun in use and found to give more uniform results. An improvement was made in fixturing used to hold the cathode during the spraying operation to prevent over spray. Production controls were established to maintain the proper spray density.

The Paasche A - Automatic spray gun along with the improved spray fixtures continue to give uniform results in production. An illustration of the spray booth is shown in Figure 4. The life rack used for evaluation of this project is shown in Figure 5. The spray density life tests indicated for favorable life test results, the density should be greater than 1.0 mg/mm³. Cathode spray density has been adjusted from $0.9 - 1.05 \text{ mg/mm}^3$ to $1.25 - 1.35 \text{ mg/mm}^3$ on production tubes. The $1.25 - 1.35 \text{ mg/mm}^3$ density gave good life test results and is easier to activate than the higher density groups. The spraying of the higher cathode densities are also more difficult to control in production with the present cathode spray equipment. In view of data derived in this test, coupled with manufacturing experience, it is felt that the $1.25 - 1.35 \text{ mg/mm}^3$ density group will greatly improve the quality of the tube.

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Life Rack

Figure 5

Project V IMPROVED CATHODE MOUNTING

Two methods of improving cathode mounting were investigated, a brazed cathode support ring assembly and a welded cathode support ring assembly. These two constructions were built with various cathode foil thicknesses and cathode temperature was measured for each construction. These were then compared with the present construction 6299. The most promising construction of each type was then sealed into tubes. The construction where the cathode is welded to the cathode support ring could not be made with satisfactory yields although cathode temperature appeared to be correct. The cathode assembly with the cathode support ring brazed to the cathode gave satisfactory results. This construction utilized .00045" cathode foil material. A more rugged assembly with better contact to the cathode shell is realized by use of this method. The variations due to tilting and canting of the individual clips of the old method of assembly are eliminated.

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Project VI HIGH TEMPERATURE OPERATION

An evaluation was performed on tubes to obtain satisfactory operation with the anode seal at 225° C. A major problem encountered was deterioration of the plating. Luring high temperature life, the copper plating diffuses through the gold plating of the JAN 6299. This causes a very poor contact surface which results in degradation in high frequency performance. The solution to the diffusion of plating was to plate nickel over the copper, then gold over the nickel. This nickel barrier prevents the deterioration of the plating and good high frequency results are obtained.

Most failures due to air leakers of the regular construction 6299 during the evaluation were found to be at the anode seal. To eliminate this weakness, the hard solder seals at the anode and preseals were utilized. This increases reliability of the tube under high temperature life conditions.

A. C. aging will be used to process tubes for high temperature life. Results have been good using this type aging. The cathode structure is rather cool for this tube to operate adequately as an k.F. oscillator from field results where it was used in this application. R.F. aging is more expensive initially and maintenance is of a higher cost.

Life test results have shown the construction with three of the seals of hard solder construction is superior to the regular construction on life when the anode seal is run at 225° C.

An illustration of the high temperature life rack is shown in Figure 6.

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Project VII HUMIDITY TESTING

It has been demonstrated by gas cooling curves and mass spectrometric gas content analysis that the failure mechanism of the JAN 6299 when subjected to a temperature of 100° centigrade and 100% humidity is due to a build up of hydrogen gas pressure in the tube. The increased mobility of the hydrogen gas as compared to air causes a marked increase in heater current over that found in a tube which is an air leaker.

The conclusion reached after work on this problem is the failure mechanism is due to hydrogen permeation of the JAN 6299's metal shell. The shell material is .010" thick 10-80-10 copper clad AISI 1010 steel alloy. After processing of the tube is complete, a copper-gold electroplating is performed. If there is the slightest pinhole in the protective coating, the base metal of the netal shell will corrode when subjected to the conditions of the humidity test chamber. The hydrogen generated by the corrosion reaction diffuses through the steel wall and recombines as H2 inside the tube if no barrier exists. Tubes that show obvious corrosion but no indication of hydrogen, probably have long diffusion paths as a result of the location of the corrosion and/or the presence of a continuous copper layer on the inside surfaces which acts as a fairly effective barrier at the temperature in question.

The hydrogen must be formed at the base metal in order to permeate into the tube. Examination of lend-metal and lead-ceramic boundaries of tubes before and after humidity test have not shown any change in condition. Since lead's susceptibleness to hydrogen permeation is very slight

-16-

or nil at these temperatures, it is felt that seal corrosion does not contribute to hydrogen permeation. Also tests in which the seal areas were covered with a protectant, showed no significant improvement over other tests. In fact, several groups where there is doubt of the curing of a silic(ne which was use², an apparent severe attack upon the plating over the tube in general was observed (confinement of the silicone to the seal area only being difficult - a considerable amount came in contact with the metal shell¹. Failure rates were very high. In general, when lower corrosion rates were observed on the metal shell there were lower failure rates due to hydrogen permeation.

Several lots of tubes which showed good results on humidity test had different processing dates up to the plating operation. With a common plating operation, good results were obtained.

A noted improvement was obtained in humidity test results when the gold plating bath was corrected to give a better plating. The gold content had been allowed to drop to a low level by an inarcurate method of measuring gold content. When this was corrected, corrosion of tube subjected to humidity test was reduced.

During the plating operation, hydrogen also permeater into a percentage of tubes. The hydrogen forms at the base metal due to the plating reaction and if a suitable diffusion path exists, the tube will become filled with hydrogen.

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In order to reduce this plating hydrogen permeation and also to give more copper barrier for the resistance of hydrogan penetration during the humidity test conditions an improved method of removing excess lead from the metal parts has been developed. The existing method was to chuck the tube to a motor and while rotating at a high speed, remove the lead with a file. This was highly dependent on operator technique and in most cases much of the outer copper clading was removed, allowing the base metal to become exposed. The improved method utilizes a rotating wire brush. The lead is removed by this brush and very little copper clading is removed.

Shown in Figure 7 are some illustrations of corrosion and possibile flaws in the platings and copper clading. The grid flange shown where virtually all clading has been removed was cleaned by the old method of using a file on the tube.

In summary, the failure of the 6299 during humility test has been found to be due to hydrogen permeation of the base metal of the tube's shell. Best minimization of this problem has been obtained by improved cleaning methods and improved plating techniques which give protection to the base metal of the tube's shell.

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Surface Conditions and Corrosion Of The 6299 During Humidity Test

-19-

Figure 7 A

50X 4X 6299 tube - Cu clad 1010 with ExIINI clentroplate + immersion Ay. 39 days at 100°C., 100% humidity. Localized bose metal corrosion hos progressed nearly through thickness of flonge. -20-Figure 7 B

Cu lad 1010 ban (4 + N, cketroplate + electroplated A4. - A4 -Ni The discontinuity - Electroplated in the Cu cladding Cú is typical of several areas in - Clad Cy one cross sectional - Steel base Metal playe. Etchant. NHYOH+ H.D. 500 X. Same as above, but different area. - Au - Ni Note absence of -Electroplated Cu cladding. Base metal has oxidized uyder the electroplate. Steel base Metal Note base metal grain distortion at surface. Etchant: NHYOH + H.O. Nital 500X. Cy clad 430 stainless steel base metal (ut Nj e legtroplate + elegtroplate Au. Note absence of -Au Lu cladding. $-N_i$ Penetration of Flectroplated monsture and air (U through a dete-t 430 stn. stl in the plating base metal has caused orraion of how metal Note: None of the tubes with Etchant: NH, SH + H2 2 alumina ceramics showed any 500 X. Cu riating - N' plated directly





200X

Cu clad 1010 base. Cut Ni electroplate + immersion Hy. Note variation in cladding and electroplation, over a relatively small area. Etchant: Alty M+ Hale; Nital.

Figure 7 1

Project VIII ENGINEERING SAMPLES ANI FILOT RUN

Engineering samples were submitted in April, 1962. After transfer of facilities from Scranton to Owensboro, another group of engineering samples were submitted in February, 1963 showing work done to that point.

Preproduction samples were constructed incorporating the improvements made under the various projects.

Alumina heater, getter, and anode ceramics were used with hard solder seal construction being utilized for the preseal assembly and anode seals. Parts were used with the tightened tolerances. The improved cathode construction was used and the cathode spray techniques developed were used in coating the cathode. The tubes were exhausted in the improved exhaust fixturing in conjunction with the temperature controller. The wire brush method of cleaning was used to remove excess lead after exhaust. The tubes were d-c and a-c aged and copper-nickel- gold plated.

A mutually acceptable working specification was established for preproduction and pilot run testing. This specification is shown in the appendix. The preproduction run conformed to the test specification.

The pilot run was started on 24 January and was terminated on 17 February due to poor yields. The tubes had very poor emission and this was caused by the cathode temperature being approximately 50° C. too cool. This problem was caused by increased copper flow while brazing the cathode assembly. The length of the legs of the cathode su port ring was shortened and cathode temperature has been adjusted to the proper value. Considerable delay and excessive subassembly and tube losses were experienced due to inconsistent metalizing of the high alumina ceramics used in the hard solder seals. Stronger and much more consistent hard solder seals have beer obtained by using finer particle size in the metalizing mix.

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The 2000 tubes produced in the pilot run were scrapped as well as in-process cathode, ancde and preseal subassemblies.

A new pilot run was begun with the cathode temperature corrected to the normal value and with the three hard solder seals utilizing the finer particle size metalizing mix.



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Table I

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ELECTRICAL CHARACTERISTICS 6299 PEM Pilot Run

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## Table II

## HUMIDITY TEST DATA

# 6299 PEM Pilot Run

Days	0	5	6	9	10
Tube No.					
1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20	305 309 308 310 307 309 304 310 314 315 319 310 309 300 311 301 311 301 310 307	305 310 305 318 310 305 320 320 320 318 322 310 310 300 310 300 310 300 305 305	308 310 305 315 308 309 305 312 315 313 320 310 308 302 310 300 310 305 306	310 310 305 310 308 307 310 312 313 312 320 310 307 302 310 400 310 303 308	310 308 305 310 305 308 312 313 313 313 313 313 310 308 303 311 720 310 305 308
	ייכ	305	312	310	310

≸ Rejects (10 Days) = 1/20 = 5%

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#### Table III

### HIGH TEMPERATURE LIFE TEST D'TA

6299 PEM Pilot Run ELECTRONIC TUBE LIFE TEST DATA

Eb-200 VDC Ambient Temp.=75° C. Life Test Conditions: Ef=6.3V RK/Ib=10Ma

Accum. Hrs. 0 500

Test Characteristic/Tube No. 1

If RGK RGP Eg Gm Mu Ik Eb N G Cin	307 5+ 50+ .40 14.9 129 7.3 149 7.5 18.8 3.49 1.68	307 5+ 50+ .30 13.7 131 6.2 157 7.6 17.2 3.50
Cgp	1.68	1.69

Test Characteristic/Tube No. 2

If	303	306
RGK	5+	5+
RGP	50*	50+
Eg	•59	.65
Gm	14.3	13.2
Mu	113	115
Ik	4.1	4.4
Eb	124	121
N	7.9	8.6
G	17.1	17.0
Cin	3.93	3.62
Cgp	2.00	2.13

HIGH TEMPERATURE LIFE TEST DATA

6299 PEM Pilot Run ELECTRONIC TUBE LIFE TEST DATA

Eb-200 VDC Ambient Temp.=75° C Life Test Conditions: Ef=6.3V RK/Ib=1CMa

Accum. Hrs. 0 500

Test Characteristic/Tube No. 3

lf RCK RCP Eg Gm Mu Ik Er N G Cin	301 5+ 50+ .45 14.9 118 4.4 144 8.4 17.6 3.43	303 5+ 50+ •39 12.8 118 3.3 150 8.3 17.6 3.20
Can	3.43	-
-0r	L I C L	1.72

est Characteristic/Tube No. 4

If RGX RGP Eg Gm Mu Ik Eb N G Cin Cgp	314 5+ 50+ .26 13.9 126 5.5 144 7.7 18.1 3.42 1.68	307 5+ 50+ .70 15.9 124 7.2 111 7.5 18.0 3.33
Cgp	1.68	1.68

## Table IV

# 6299 FEM Filot Run

# 1000 Hour Life Test Data

Life Te	est Conditi	Nb - ons: Ef =	200 VDC 6.3 V R	k/Ib = 10 Ma	
Accum.	Hrs.0	140	558	1009	
Test Ch	Test Characteristic/Tube No. 1				
If RGK RGP Eg Gm Mu Ik Eb Noise Gain Cin Cgp	307 5+ 50+ .50 16.2 120 8.6 133 7.6 19.1 3.54 1.75	5+ 50+ 15.9	5+ 50+ •30 15•5 £•0	311 5+ 50+ .17 14.3 123 6.0 159 7.6 18.0 3.44 1.78	
Test Ch	aracteristi	.c/Tube No.	2		
If RGK RGP Eg Gm Mu Ik Eb Noise Gain Cin Cgp	309 5+ 50+ .45 15.9 127 5.5 143 7.3 19.1 3.56 1.68	5+ 50- 16.0	5+ 50+ •35 15•9 7•6	311 5+ 50+ .24 15.5 127 4.6 150 7.4 18.8 3.51 1.68	

## 6299 PEM Pilot Run

## 1000 Hour Life Test Data

Life Tes	t Conditio	Eb - ns: Ef =	200 VDC 6.3 V 1	RK/Ib = 10 Ma
Accum. Hi	rs.0	140	558	1009
Test Char	racteristi	c/Tube No.	3	
lf RGK ROP Eg Gm Mu Ik Eb Noise Gain Cin Cgp	306 5+ 50+ 13.7 112 6.5 143 7.9 17.7 3.41 1.69	5+ 50+ 13.6 7.6	5+ 50+ •39 13•3 7•9	310 5+ 50+ .26 12.4 112 5.0 150 7.6 17.8 3.40 1.69

#### Project IX IMPROVED EXHAUST FIXTURING

The purpose of this project is to further improve alignment and concentricity of the tube beyond that attained in Project I. Improvements made in Project I were attained by reductions in tolerences of tube parts. The basic limitation in making this improvement is the fixtures used to hold the tube's parts during the exhaust and sealing cycle. Materials and design of fixtures were such that warping of the fixture took place during exhaust.

The improved exhaust fixture shown in ligure ô was selected from six designs as giving best results. The center shaft immediately below the fixture top was turned down to allow increased pressure on the tubes during the exhaust cycle.

Cathode, getter, and heater pin eccentricity data were taken on 102 regular production tubes solected at random. After a familierization and debugging run. 110 tubes were exhausted in the improved exhaust fixtures and eccentricity data was taken. Eccentricity data was taken with the eccentricity gauge (P69087-2390591 Rev 0) as presented in the Second Quarterly Report. Probability plots of that data are shown in Figures 9, 10, and 11.

The data shows the greatest improvement in heater pin eccentricity. This is the area where the most deterioration was caused by the old exhaust fixtures. The getter eccentricity appears to have improved by having less tubes with very large eccentricities. Anode eccentricity should not be effected by the improved exhaust fixturing.

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There appears to be little difference in cathode eccentricities. A successful reduction of cathode eccentricity should also further improve getter and heater pin eccentricity.

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GENERAL ELECTRIC COMPANY, SCHENECTADY, N. Y., U. S. A.

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PROBABILITY PAPER



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PROEABILINY PAPER

#### Project X EXTENDED LIFE TESTING

This contract and the present MIL specification on the JAN 6299 specify 1000 hour life test. It is well recognized that much longer life than 1000 hours of operation is desired in many Signal Corps equipments. The purpose of this project is to determine the life results of the improved tube to 5000 hours and to determine the nature of any resulting failures so that information can be made available for possible tube or manufacturing improvements.

Control tubes were constructed for extended life testing. These tubes are standard JAN 6299's; however, they do include some of the benefits of the improved cathode spray project. Cathodes were sprayed with the Paasche A-automatic spray gun and the improved masking fixtures were used. The cathodes were sprayed to the density being used prior to optimization of cathode spray.

Tubes were constructed utilizing the improvements developed during the contract. These tubes and the control tubes were placed on life test.

Life test has now completed 1795 hours. Tube No. 8 of the test group failed as an air leaker at 566 hours. These tubes were constructed before the improvements in metalizing techniques were achieved. The hard solder seals are now stronger as a result of the change to finer particle size of the metalizing mix.

All remaining tubes still meet the 1000 hour life test end point. The improved tubes show 7% less median transconductance degradation than the control tubes. The grid voltage degradation is about 20% more in the improved tube. Noise figure, capacitances, and amplification factor are generally stable for both groups of tubes. Life test data is shown in Table V.

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The complete 5000 hour life test data and the analysis of mode of failure will be presented in an addendum to the Final Report.

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## Table V

# EXTENDED LIFE TEST

# 6299 Control Tubes

Life Te	st Condi+i		• 200 VDC • 6.3 V RI	K/Ib = 10 M	la
Accum.	Hrs.0	108	245	406	566
Test Cha	aracterist	ic/Tube No	<u> </u>		
lı Eg	308	r sa			
Mu	.75 110	.65 107	.60	.59	.45
Sm	16.1	16.0	108 15.9	110	112
Ik	7.0	40.00	±J • 7	15.8	15.4
Eb	115				
Cain	18.4				
Noise	7.4	7.6	7,6	7.8	7.6
Cin Cgp	3.83	3.89	3.91	3.91	3.92
Cbk	1.72 .016	1.72 .016	1.72	1.71	1.73
- For		•010	.016	.015	.017
Test Cha	racteristi	.c/Tube No.	. 2		
If	305				
Eg	•39	•39	•39	•38	•30
Mu	108	108	108	109	109
Sm 70-	12.5	12.6	12.4	12.4	12.0
Ik Eb	6.8				•••
Gain	152 17.6				
Noise	8.0	8.3	7,8	0 0	<b>6</b> •
Cin	3.61	3.61	3.61	8.3 3.61	8.1
Cgp	1.79	1.79	1.78	1.78	3.62 1.79
Cpk	.012	.003	.012	.011	.013

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6299	Control	Tubes
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Life Tes	st Conditi		= 200 VDC = 6.3 V RK	:/Љ = 10 M	a	
Accum. H	Irs.726	866	1004	1286	1780	1795
Test Cha	racterist	ic/Tube No	<u>. 1</u>			
If Eg Mu Sm Ik Eb Gein	.59 112 15.4	.50 113 15.3	306 •59 115 15•6 7•9 128	.59 114 14.7	.38 115 14.4	•36 113 13•0
Noise Cin Cgp Cpk	7.8 3.92 1.73 .916	7.6 3.91 1.72 .016	18.3 7.5 3.90 1.72 .016	7.7 3.87 1.72 .017	7.3 3.86 1.72 .016	7.2 3.87 1.72 .015
	racterist	ic/Tube No	<u>    2</u>			
If Eg Mu Sm Ik Eb	•39 109 11.8	•39 110 11•8	300 .30 110 11.6 7.0 15.3	.39 111 11.4	•30 111 11•0	.11 109 10.0
Gain Noise Cin Cgp Cpk	8.2 3.61 1.79 .012	8.0 3.61 1.79 .014	17.4 8.0 3.60 1.79 .011	8.3 3.60 1.78 .013	7.7 3.59 1.78 .011	7.9 3.59 1.78 .014

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### 6299 Control Tubes

Life Tes	t Condition		200 VDC 5.3 V RK/1	lb = 10 Ma	
Accum. Hi	rs.0	108	245	406	566
Test Char	racteristic	/Tube No.	3		
If Eg Mu Sm Ik Eb Gain	305 .70 106 15.9 7.6 121 18.8	.65 105 16.3	.65 106 15.8	.65 107 15.6	.65 105 15.8
Noise Cin Cgp ?pk Test Char	6.8 3.90 1.77 .016	6.9 3.89 1.77 .016	6.8 3.89 1.78 .016	7.3 3.87 1.77 .01	7.2 3.90 1.79 .017
lf Eg Mu Sm Ik Eb Gain	308 .45 119 14.5 4.0 142 18.2	•39 119 14.4	•30 118 13•5	.30 120 14.0	.15 121 11.7
Noise Cin Cgp Cpk	7.5 3.88 1.71 .014	7.3 3.87 1.70 .014	7.3 3.56 1.70 .014	7.5 3.87 1.70 .014	7.4 3.87 1.72 .016

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## 6299 Control Tubes

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/Ib = 10 Ma									
Accum. H	<b>rs.</b> 726	866	1004	1286	1490	1795			
Test Cha	racterist	ic/Tube No	<u>· 3</u>						
If Eg Mu Sm Ik Eb Gain	.65 107 1.5.7	.59 106 15.4	301 .65 106 15.2 7.2 124 18.8	.60 108 15.0	.59 107 14.5	.52 105 14.2			
Noise Cin Cgp Cpk	7.0 3.90 1.79 .016 racterist:	7.0 3.90 1.78 .017 ic/Tube No	7.0 3.90 1.78 .016	7.1 3.89 1.78 .016	7.0 3.88 1.78 .015	6.9 3.88 1.78 .016			
If Eg Mu Sm Ik Eb Gain	.30 120 13.8	.30 120 14.0	303 .39 120 14.0 4.7 54 18.4	.39 120 13.9	.25 121 13.4	.26 119 13.8			
Noise Cin Cgp Cpk	7.5 3.86 1.71 .015	7.4 3.86 1.71 .010	7.2 3.85 1.71 .016	7.4 3.84 1.71 .015	7.1 3.84 1.71 .015	7.3 3.84 1.71 .015			

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## 6299 Control Tubes

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/Tb = 10 Ma								
Accum. Hi	rs.0	108	245	406	566			
Test Char	racteristic	/Tube No.	5					
lf Eg Mu Sm Ik Eb Gain	308 .45 127 14.0 5.7 149 18.2	.39 125 13.9	.39 124 13.9	.28 127 13.8	.30 125 13.5			
Noise Cin Cgp Cpk	7.6 3.60 1.70 .012	7.3 3.61 1.71 .013	7.2 3.60 1.71 .013 6	7.5 3.60 1.70 .012	7.7 3.62 1.71 .013			
If Eg Mu Sm Ik Eb	309 •39 114 13•3 7•6 146	.39 114 13.0	.30 110 12.8	13.1 115 13.1	.12 114 10.8			
Gain Noise Cin Cgp Cok	18.0 7.6 3.53 1.75 .012	7.7 3.53 1.75 .013	7.6 3.53 1.75 .012	7.8 3.52 1.75 .012	7.9 3.54 1.76 .013			

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# 6299 Control Tubes

Eb = 200 VDC Life Test Conditions: Ef = 5.3 7 RK/Ib = 10 Ma								
Accum. Hr	s.726	866	1004	1286	1490	1795		
Test Char	acteristic	/Tube No.	5					
If Eg Mu Sm Ik Eb Gain	.19 127 13.3	.25 127 13.1	301 •25 127 13.0 6.6 163 17.5	.30 128 13.0	.25 128 12.4	.10 125 12.0		
Nois <del>e</del> Cin Cgp Cpk	7.5 3.59 1.72 .012	7.6 3.59 1.71 .013 /Tube No.	7.5 3.58 1.71 .012	7.8 3.58 1.71 .014	7.3 3.56 1.72 .013	7.8 3.56 1.71 .013		
If Eg Mu Sm Ik Eb	.30 115 12.6	.20 116 12.4	 307 .30 115 12.1 7.6 162	.30 116 12.1	.19 115 10.9	.13 111 11.6		
Gain Noise Cin Cgp Cpk	7.9 3.52 1.76 .013	7.7 3.52 1.75 .008	17.2 8.1 3.51 1.75 .012	8.1 3.50 1.75 .014	7.5 3.50 1.76 .010	7.6 3.49 1.75 .012		

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## 6299 Control Tubes

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/Ib = 10a									
Accum. Hr	s.0	108	245	406	566				
Test Char	acteristic,	Tube No.	<u>7</u>						
If Eg !/tu Sm Ik Eb	304 •55 113 16•2 7•5 128	.65 111 16.7	.59 109 16.3	.55 113 16.5	•30 113 16•2				
Gain Noise Cin Cgp Opk Test Char	18.8 6.8 3.84 1.72 .015 acteristic,	7.2 3.86 1.72 .015	7.0 3.86 1.72 .015	7.1 3.87 1.72 .014	7.0 3.89 1.73 .015				
If	313	1000 NO.	<u> </u>						
Eg Mu Sm Ik Eb	•99 87.0 14.0 7.2 106	.60 88.9 16.3	.90 86.4 13.2	.90 37.0 13.7	.79 88.7 12.6				
Gain Noise Cin Cgp Opk	18.2 7.3 3.64 1.88 .018	7.3 3.66 1.89 .018	7.2 3.65 1.89 .018	7.7 3.65 1.88 .018	7.9 3.65 1. 70 .019				

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# 6299 Control Tubes

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/Tb·= 10 Ma								
Accum. H	Irs.726	866	1004	1286	1490	1795		
Test Cha	aracterist	ic/Tube No	• 7					
lf Eg Mu Sm Ik Eb Gain	.50 114 15.9	.50 114 15.3	300 .59 113 15.9 8.5 132 17.9	.59 114 15.8	.50 114 15.3	.40 113 15.2		
Noise Cin Cgp Cpk	7.1 3.89 1.73 .012	7.0 3.89 1.72 .015	7.0 3.88 1.72 .014	7.3 3.88 1.72 .016	7.0 3.86 1.72 .015	7.0 3.86 1.72 .015		
	racterist	ic/Tube No						
<u>If</u> Eg Mu Sm Ik Eb Gain	.35 67.8 13.0	.85 98.0 13.0	309 .85 86 12.7 6.3 114 16.4	• • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • • •	.80 89.0 12.2	.71 88.0 12.0		
Noise Cin Cgp Cpk	7.7 3.64 1.90 .018	·7.2 3.63 1.90 .018	7.3 3.61 1.90 .017	7.7 3.60 1.90 .012	7.2 3.58 1.90 .019	7.5 3.58 1.90 .018		

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## 6299 Control Tubes

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/Tb = 10 Ma							
Accum. Hr	s.0	108	245	<b>4</b> 06	566		
Test Char	acteristic	/Tube No.	9				
Mu Sm Ik Eb	98.3 13.6 6.0 127	.70 97.2 14.1		.65 98.2 14.0	.65 98.7 13.4		
Noise	18.1 7.2 3.69 1.78 .016	7.3 3.69 1.78 .016	7.4 3.69 1.78 .016	7.4 3.69 1.77 .015	7.3 3.70 1.79 .010		
Test Char	acteristic	/Tube No.	10				
Mu Sm Ik Eb	118 12.7 5.3 110	•59 116 13•9	•50 115 13•2	.45 116 13.8	.15 116 11.6		
Gain Noise Cin Cgp Cpk	17.8 7.8 3.86 1.74 .014	8.4 3.80 1.75 .014	8.2 3.80 1.75 .014	7.9 3.80 1.75 .013	7.8 3.81 1.75 .014		

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#### 6299 Control Tubes

#### Eb = 200 VDC Life Test Condition: Ef = 6.3 V RK/Tb = 10 Ma

Life Test Conditions: Ef = $6.3$ V RK/Ib = 10 Ma							
Accum. Hr	s.726	866	1004	1286	1490	1795	
Test Char	acterístic	/Tube No.	<u>9</u>				
If Eg Mu Sm Ik Eb Gain	.65 100 13.3	.59 99.4 12.9	301 •59 100 12.7 6.4 131 18.3	.60 100 12.5	.45 100 11.4	.37 100 11.5	
Noise Cin Cgp Cpk	7.3 3.70 1.79 .016	7.3 3.69 1.78 .017	8.1 3.69 1.79 .016	7.3 3.68 1.79 .016	7.3 3.67 1.79 .016	7.6 3.67 1.78 .016	
Test Char	acteristic	/Tube No.	10				
If Eg Mu Sm Ik Eb	.30 116 13.0	.115 116 13.7	305 .49 116 13.8 8.0 141	.45 116 13.5	.45 115 12.9	.31 115 12.6	
Gain Noise Cin Cgp Cpk	7.7 3.80 1.76 .015	7.7 3.77 1.75 .015	18.6 7.5 3.79 1.75 .014	7.7 3.78 1.75 .013	7.3 3.76 1.75 .010	7.6 3.76 1.75 .014	

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### 6299 Control Tubes

Eb = 200 VDC Life Test Conditions: Ef = $6.3$ V RK/Ib = 10 Ma								
Accum. Hr	's.0	108	245	406	564			
Test Char	acteristic	/Tube No.	11					
If Eg Mu Sm Ik Eb	310 •50 129 16.5 6.1 125 18	.50 127 16.8	•55 124 17•0	.48 127 16.6	.45 125 16.5			
Gain Noise Cin Cgp Cpk	18.4 7.3 3.92 1.72 .013	7.3 3.93 1.72 .014	7.4 3.93 1.72 .013	7.5 3.95 1.72 .013	7.4 3.96 1.73 .014			
Test Char	acteristic	Tube No.	12					
If Eg Mu Sm Ik Eb	309 .45 112 13.2 6.8 149	.39 112 13.1	•39 112 13•0	•39 113 13•0	.19 113 11,0			
Gain Noise Cin Cgp Cpk	17.7 7.14 3.65 1.71 .014	7.4 3.64 1.71 .014	7.7 3.63 1.71 .014	7.8 3.64 1.70 .014	7.6 3.64 1.71 .014			

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# 6299 Control Tubes

Life Tes	st Conditic	Eb = ns: Ef =	200 VDC 6.3 V RK/	'Ic = 10 Ma	L	
Accum. H	lrs.726	866	1004	1286	1490	1795
Test Cha	racteristi	c/Tube No.	11			
lf Eg Mu Sm Ik Eb Gain	•50 125 16.6	•50 125 16•2	288 •59 124 16•7 7•5 179	•50 127 16•0	.45 126 15.9	.32 124 15.5
Noise Cin Cgp Cpk	7.3 3.95 1.73 .014	7.3 3.96 1.73 .013	19.6 7.3 3.95 1.72 .012	7.6 3.95 1.72 .014	7.1 3.95 1.73 .014	7.3 3.94 1.72 .011
Test Char	racteristic	Tube No.	12			
If Eg Mu Sm Ik Eb Gain	.25 114 11.9	•30 113 12•6	303 .25 114 12.1 6.1 166	•30 115 12•0	.19 115 10.9	.14 112 11.0
Noise Cin Cgp Cpk	7.6 3.65 1.71 .014	7.5 3.62 1.71 .010	18.2 7.3 3.62 1.71 .013	7.7 3.62 1.71 .014	7.3 3.61 1.71 .011	7.1 3.61 1.71 .014

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# 6299 Control Tubes

Eb = 200  VDC Life Test Conditions: Ef = 6.3 V RK/Ib = 10 Ma						
Accum. H	lrs.0	108	245	406	566	
Test Cha	Test Characteristic/Tube No. 13					
If Eg Mu Sm Ik Eb Gain	309 .65 104 14.1 5.8 125	.60 104 14.0	.40 102 14.0	.59 105 13.8	.50 103 13.8	
Noise Cin Cgp Cpk	18.1 7.5 3.90 1.76 .015	7.7 3.89 1.76 .015	7.6 3.89 1.76 .015	7.7 3.89 1.76 .015	7.6 3.91 1.78 .016	
	racteristi	c/Tube No.	14			
If Eg Mu Sm Ik Eb	309 .50 117 14.8 6.6 135	.50 116 14.8	.45 114 14.7	.39 118 14.6	•35 117 14•2	
Gain Noise Cin Cgp Cpk	18.1 7.3 3.46 1.74 .014	7.1 3.45 1.74 .014	6.9 3.45 1.74 .014	7.4 3.45 1.73 .014	7.3 3.46 1.77 .015	

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# 6299 Control Tubes

Life T	est Condit:	Eb ions: Ef	= 200 VDC = 6.3 V R	K/Ib = 10 1	Ma	
Accum.	Hrs.726	866	1004	1286	1490	1795
Test C	haracterist	tic/Tube N	0.13			
If Eg Mu Sm Ik Eb G <b>a</b> in	.59 106 13.7	•59 105 13•6	306 .50 104 13.4 6.9 137	.60 104 13.5	•45 105 13•1	.40 105 13.0
Noise Cin Cgp Cpk	7.4 3.90 1.77 .015	7.5 3.89 1.73 .015	17.5 7.2 3.68 1.77 .016	7.7 3.88 1.78 .014	7.5 3.88 1.77 .015	7.3 3.88 1.78 .014
Test Ch	aracterist	ic/Tube No	. 14			
If Eg Mu Sm Ik Eb Gain	.39 118 13.5	•39 118 13•6	309 .45 118 13.9 5.9 145	.45 119 13.8	•25 119 12.6	.21 119 12.8
Noise Cin Cgp Cpk	7.7 3.44 1.76 .014	7.1 3.44 1.74 .015	18.3 7.1 3.43 1.74 .015	7.1 3.14 1.74 .014	7.0 3.43 1.74 .015	6.9 3.42 1.74 .014

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### 6299 Control Tubes

Eb = 200 VDC Life Test Conditions: $Ef = 6.3 V RK/Ib = 10 Ma$						
Accum. Hr	<b>s</b> .0	108	245	406	566	
Test Char	acteristic	/Tube No.	15			
If Eg Mu Sm Ik ED Gain	308 .50 111 13.2 7.1 137 17.5	.50 110 13.2	.45 109 13.2	.39 110 12.9	.29 110 12.1	
Noise Cin Cgp Cpk	7.5 3.57 1.76 .014	7.6 3.57 1.76 .014	7.7 3.59 1.76 .014	7.8 3.58 1.76 .013	7.6 3.62 1.78 .013	

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## 6299 Control Tubes

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/Ib = 10 Ma							
Accum. Hi	<b>s</b> ,726	866	1004	1286	1490	1795	
Test Char	acteristic	/Tube No.	15				
l <b>f</b> Eg Mu Sm Ik Eb G <b>a</b> in	•35 111 12•5	.30 111 12.0	301 •30 112 11.7 7.4 160 18.6	•39 112 11•8	.19 113 10.3	.15 109 .10.8	
Noise Cin Cgp Cpk	7.7 3.59 1.78 .014	7.7 3.60 1.76 .013	7.7 3.59 1.77 .014	7.8 3.58 1.77 .013	7.6 3.57 1.77 .014	7.9 3.57 1.77 .014	

## Table V

## EXTENDED LIFE TEST

## Improved 6299

Life Test	t Condition		200 VDC 5.3 V RK/1	[b = 10 Ma	
Accum. Hi	<b>.</b> 0	108	245	406	566
Test Char	acteristic	s/Tube No.	1		
If Eg Mu Sm Ik Eb	301 .50 108 14.0 5.9 136	•55 109 14•2	.45 108 13.0	.45 110 13.6	.30 110 12.9
Gain Noise Cin Cgp Cpk	18.2 7.3 3.50 1.80 .015	7.3 3.45 1.80 .015	7.6 3.47 1.78 .015	7.4 3.46 1.78 .015	7.4 3.48 1.81 .016
Test Char	racteristic	s/Tube No.	2		
If. Eg Mu Sm Ik Eb	303 •30 124 13•2 4•2 163	.19 124 13.4	.25 122 13.1	.20 125 13.7	.19 124 13.3
Gain Noise Cin Cgp Cpk	17.6 7.7 3.42 1.70 .014	7.2 3.41 1.69 .013	7.4 3.41 1.69 .013	7.6 3.41 1.69 .014	7.7 3.43 1.70 .015

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			Improved	6299			Li
life Tee	t Conditio		200 VDC	/Ib = 10 M	•		Ac
DILE 169	C CONVECTO			/10 - 10 M	a		Te
Accum. H	<b>rs</b> .726	866	1004	1286	1490	1795	ľ
Test Cha	racterist:	ics/Tube N	<u>0.1</u>				Eg Mu
If Eg Mu Sm Ik Eb Gain	.19 110 10.9	•39 110 12.8	301 •45 110 13 •3 3 •8 147 18 •2	.48 110 13.4	.30 110 12.6	•30 108 12•9	Sm Ik Eb Ga: No: Cii Cgi
Noise Cin Cgp Cpk	7.3 3.47 1.81 .015	7•3 3•48 1•81 •016	7.0 3.46 1.81 .016	7.9 3.46 1.81 .016	7.6 3.46 1.81 .016	7.3 3.46 1.81 .016	Cpi Te: If
Test Cha	racteristi	ics/Tube N	<b>b.</b> 2				Eg
If Eg Mu Sm Ik Eb	.17 125 13.0	.20 124 13.0	301 •25 125 13.2 3.4 169	•25 125 13•3	.19 125 13.0	.09 124 13.0	Mu Sm Ik Eb Gai Noi Cin
Gain Noise Cin Cgp Cpk	7.8 3.43 1.70 .015	7.8 3.42 2.70 .015	17.7 7.5 3.43 1.69 .014	7.8 3.43 1.69 .014	7.7 3.42 1.69 .015	7.8 3.41 1.70 .015	Cgp Cpk

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# Improved 6299

Life T	est Condit	E ions: E	t = 200 VD f = 6.3 V	C RK/ID = 10 1	Ma
Accum.	Hrs.0	108	245	406	566
Test C	naracterist	tics/Tube	e No. 3		
lf Eg Mu Sm Ik Eb	302 •45 127 15•5 8•5 139	•29 127 15•6	•25 125 15•0	•20 129 15•2	.15 129 14.3
Gain Noise Cin Cgp Cpk	17,6 7.8 3.34 1.71 .013	7.9 3.35 1.71 .012	8.3 3.32 1.71 .013	7.9 3.36 1.71 .012	7.8 3.38 1.72 .014
Test Ch	aracterist	ics/Tube	No. 4		
If Eg Mu Sm Ik Eb	303 •59 105 13.0 6.8 135	.45 105 13.2	.45 105 13.3	•39 106 13.0	•30 106 12•6
Gain Noise Cin Cgp Cpk	17.4 7.6 3.31 1.82 .014	7.8 3.30 1.82 .014	8.1 3.32 1.82 .014	7.8 3.30 1.82 .014	7.8 3.32 1.83 .015

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## Improved 6299

Life Tes	st Conditi	Eb = ons: Ef =	200 VDC 6.3 V RK,	/Ib = 10 M	8		Life	
Accum, H	irs.726	866	1004	1286	1490	1795	Accu	
Test Cha	aracterist	ics/Tube N	0.3				Test	
lf Eg Mu Sm Ik Eb Gain Noise Cin Cgp	.19 128 14.3 8.1 3.37 1.73 .014	.25 128 14.3 8.0 3.37 1.72	289 .25 129 14.4 8.1 180 17.4 7.8 3.36 1.72 .014	•25 129 14•2 7•9 3•36 1•72	.19 129 13.3 7.9 3.35 1.72	.05 127 13.2 7.9 3.33 1.72	If Eg Mu Sm Ik Eb Gain Nois Cin Cgp Cpk	
Cpk Test Cha		.013 dics/Tube N		.014	.015	•013	Test	
If Eg Mu Sm Ik Eb Gain Noise Cin Cgp Cpk	•38 106 12•3 7•7 3•32 1•84 •015	.39 106 12.3 7.7 3.33 1.83 .015	301 .39 106 12.2 6.4 153 17.0 7.9 3.32 1.83 .014	•39 106 12.1 8.1 3.32 1.84 •014	.25 107 11.4 7.7 3.31 1.84 .015	•19 105 11•5 7•7 3•31 1•85 •014	If Eg Mu Sm Ik Eb Gain Nois Cin Cgp Cpk	

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## Improved 6299

Life Tes	t Conditio		200 VDC 6.3 V RK	/Ib = 10 Ma	a
Accum. H	lrs.0	108	245	106	566
Test Cha	racteristi	.cs/Tube N	<u>. 5</u>		
lf Eg Mu Sm Ik Eb	302 •55 113 16•0 6•7 132	.45 113 15.8	.40 113 15.8	.40 114 15.9	.33 114 15.3
Gain Noise Cin Cgp Cpk	18.2 7.3 3.43 1.69 .015	8.2 3.46 1.69 .015	7.9 3.45 1.70 .J15	8.1 3.44 1.68 .015	8.2 3.45 1.70 .015
Test Cha	racterist	.cs/Tube N	0. 6		
If Eg Mu Sm Ik Eb	308 •59 113 16•5 5•6 123	•50 111 16•4	•59 110 16•1	•50 112 16•3	.45 112 16.2
Gain Noise Cin Cgp Cpk	18.5 7.2 3.56 1.73 .017	7.5 3.55 1.73 .016	7.6 3.57 1.76 .016	7.7 3.55 1.73 .016	7•3 3•56 1•75 •017

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# Improved 6299

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/Ib = 10 Ma						
Accum.	Hrs.726	866	1004	1286	1490	1795
Test C	haracturis	tics/Tube	No. 5			-177
lf Eg Mu Sm Ik Eb Gain	•39 114 15•3	•39 114 15•0	300 •45 115 15•2 5•9 148	.45 114 15.1	•39 115 114•6	•20 115 14•5
Noise Cin Cgp Cpk	7.6 3.45 1.70 .016	7.7 3.45 1.70 .016	17.8 7.6 3.43 1.70 .016	7.6 3.44 1.70 .016	7.4 3.14 1.70 .016	7.4 3.43 1.70 .015
Test Ch	aracterist	ics, Tube N	0.6			
lf Eg Mu Sm Ik Eb Gain	•50 113 15•6	.50 113 15.8	305 •49 114 15•3 5•2 136	•59 112 15•3	.40 114 14.9	•41 111 14•8
Gain Noise Cin Cgp Cpk	7.4 3.56 1.76 .016	7.6 3.59 1.75 .017	19.0 7.4 3.56 1.75 .016	7•4 3•54 1•75 •017	7.1 3.53 1.75 .016	7•3 3•54 1•76 •018

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	Improved 6299						
Life T	est Condit		= 200 VDC = 6.3 V F	K/Ib = 10 1	Ma		
Accum.	Hrs.O	108	245	406	566		
Test C	haracteris	tics/Tube 1	10.7				
If Eg Mu Sm Ik Eb Gain	309 .49 114 13.9 5.8 139	•49 114 13•9	.30 114 13.2	•30 115 13•9	•25 115 13•3		
Noise Cin Cgp Cpk	17.6 7.2 3.27 1.72 .014	7.1 3.26 1.72 .014	7.6 3.27 1.73 .014	7.7 3.27 1.72 .01h	7.7 3.26 1.74 .015		
Test Ch	aracterist	ics/Tube No	<u>. 8</u>				
If Eg Mu, Sm Ik Eb	305 .50 113 13.2 4.6 146	.49 113 13.4	.25 112 12.8	.10 114 13.9	.10 86 0		
Gain Noise Cin Cgp Cpk	17.9 7.5 3.25 1.68 .014	7.1 3.23 1.68 .014	8.1 3.24 1.68 .014	7.6 3.27 1.68 .014	3.26 1.69 .015		

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# Improved 6299

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/Ib = 10 Ma								
Accum.	Hrs.726	866	100b	1286	1490	1 200		
Test Ci	Test Characteristics/Tube No. 7							
If Eg Mu Sm Ik Eb Gain	•25 115 13•4	.30 115 13.2	307 •30 116 13•4 4•6 158	•59 113 11•5	•30 115 13•4	•19 114 13•0		
Noise Cin Cgp Cpk	7.5 3.27 1.74 .015	7.3 3.29 1.74 .015	18.4 7.3 3.27 1.73 .014	7.7 3.26 1.73 .015	7.3 3.27 1.73 .015	7.3 3.27 1.74 .015		
	aracteristi	cs/Tube No	. 8					
If Eg Mu Sm Ik Eb Gain Noise Cin Cgp Cpk		SLOW AIR	LEAKER					

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## Improved 6299

Eb = 200 VDC Life Test Conditions: Ef = $6.3$ V RK/Tb = 10 Ma								
Accum Hrs	••0	108	245	406	566			
Test Char	racteristic	s/Tube No.	9					
If Eg Mu Sm Ik Eb Gain	305 .85 100 15.1 3.9 110 18.3	.75 100 15.1	.70 100 1)4.6	.70 100 15.0	.65 100 15.0			
Noise Cin Cgp Cpk	7.4 3.93 1.70 .020	7.2 3.90 1.71 .020	7.9 3.90 1.71 .020	7.4 3.89 1.70 .020	7.2 3.90 1.72 .021			
		s/Tube No.	10					
If Eg Mu Sm Ik Eb	303 .40 114 14.2 6.7 148	.45 114 13.9	•39 113 13•9	•39 115 14•0	•39 115 14•0			
Gain Noise Cin Cgp Cpk	18.1 7.6 3.09 1.69 .01L	7.4 3.06 1.69 .014	7.7 3.06 1.70 .014	7.6 3.05 1.69 .013	7.6 3.06 1.70 .014			

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# Improved 6299

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/Ib = 10 Ma							
Accum.	Hrs.726	866	1004	1286	1490	7 700	
Test C	haracteris	tics/Tube	No. 9		-4/0	1755	
If Eg Mu Sm Ik Eb Gain	.70 100 14.7	.70 100 14.7	303 .70 100 14.7 3.8 121	.70 100 14.5	.59 100 14.6	.56 100 14.5	
Noise Cin Cgp Cpk	7.6 3.91 1.73 .021	7.2 3.90 1.72 .021	18.2 7.0 3.88 1.71 .020	7.4 3.88 1.78 .021	7.0 3.88 1.72 .021	6.9 3.87 1.72 .021	
	aractorist	ics/Tube N	0.10				
If Eg Mu Sm Ik Eb	•39 115 13.6	.19 120 11.5	299 •38 115 13•0 6•7 171	.30 115 12.9	•39 115 13•1	•24 114 13.0	
Gain Noise Cin Cgp Cpk	7.4 3.08 1.71 .014	7.2 3.08 1.71 .014	17.6 7.3 3.05 1.70 .014	7.6 3.05 1.70 .014	7.6 3.04 1.70 .010	7.8 3.02 1.70 .014	

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## Improved 6299

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/Ib = 10 Ma								
Accum.	Hrs.O	108	245	1406	566			
Test Characteristics/Tube No. 11								
If Eg Mu Sm Ik Eb Gain Noise Cin Cgp Cpk	309 .39 119 15.0 3.8 148 18.9 7.6 3.51 1.62 .015	.30 119 15.1 7.1 3.51 1.61 .015	.30 118 14.2 7.7 3.56 1.62 .015	•39 120 15•0 7•3 3•49 1•61 •017	.25 120 14.3 7.2 3.51 1.62 .016			
Test Characteristics/Tube No. 12								
If Eg Mu Sm Ik Eb	305 .50 105 14.2 5.4 139	.50 105 14.2	.45 104 14.1	.40 105 14.0	.45 105 14.0			
Gain Noise Cin Cgp Cpk	18.0 8.4 3.50 1.72 .017	7.4 3.50 1.73 .017	8.1 3.50 1.73 .016	7.8 3.40 1.72 .018	7.6 3.50 1.74 .017			

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## Improved 6299

Eb = 200 VDC Life Test Conditions: Ef = 6.3 V RK/To = 10 Ma								
Accum. Hr	<b>s.</b> 726	866	1004	1286	1490	1795		
Test Characteristics/Tube No. 11								
If Eg Mu Sm Ik Eb Gain	.30 120 14.4	•39 120 15•1	307 •39 120 14•5 4.0 156 18•3	•39 120 14•6	.30 120 14.2	.24 119 14.2		
Noise Cin Cgp Cpk	7.1 3.53 1.63 .017	7.1 3.53 1.62 .015	7.1 3.52 1.62 .016	7.1 3.51 1.62 .017	7.3 3.52 1.62 .017	6.9 3.51 1.62 .016		
Test Characteristics/Tube No. 12								
If Eg Mu Sm Ik Eb Gain	.15 105 13.9	.49 105 13.5	303 •45 105 13.9 5.5 147 17.7	.45 105 13.4	.40 105 13.3	.34 105 13.2		
Noise Cin Cgp Cpk	7.7 3.49 1.75 .017	7.3 3.49 1.74 .017	17.1 7.4 3.50 1.74 .014	7.7 3.49 1.74 .016	7.3 3.40 1.74 .018	7.5 3.50 1.74 .018		

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## Improved 6299

Life Tes	t Conditio		200 VDC 5.3 V RK/	IB = 10 Ma			
Accum. H	rs.0	108	21,5	106	566		
Test Characteristics/Tube No. 13							
If Eg Mu Sm Ik Eb	308 •39 119 12•5 5•6 152	.25 118 12.5	.20 11.7 12.0	.19 120 12.6	.19 119 11.3		
Gain Noise Cin .Cgp Cyk	17.0 8.4 3.14 1.74 .012	8.1 3.14 1.75 .012	8.1 3.15 1.76 .012	8.2 3.15 1.74 .004	8.2 3.15 1.76 .013		
Test Characteristics, Tube No. 14							
If Eg Mu Sm Ik Eb	301 .45 123 14.7 6.2 142	.45 122 15.3	•30 121 15•0	•39 123 15•2	•29 122 14•6		
Gain Noise Cin Cgp Cpk	18.4 7.3 3.17 1.73 .014	7.2 3.20 1.73 .013	7.7 3.19 1.73 .014	7.3 3.18 1.73 .015	7.3 3.20 1.75 .015		

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4
# EXTENDED LIFE TEST

# Improved 6299

Life 7	est Condit:		= 200 VDC = 6.3 V R	K/Ib = 10 M	<b>f</b> a	
Accum.	Hrs.726	866	1004	1286	1490	1 <b>7</b> 95
Test C	haracterist	ics/Tube	No. 13			
If			310			
Eg	.19	.19	.15	.19	.19	oř
Mu	119	119	11.9	110	119	.06 119
Sm	12.0	11.7	11.2	11.1	11.8	11,6
Ik			5.5			
so Gain	-		178			
Noise	8.0	7 0	17.3			
Cin	3.19	7.8	7.7	8.1	7.7	7.8
Cgp	1.76	3 <b>.1</b> 9 1.76	3.17	3.15	3.15	3.14
Cpk	.012	.013	1.70 .013	1.75 .014	1.75 .014	1.76
Test Cl	aracterist:	2		•0.TH	•014	.014
If			300			
Eg	•39	.19	•39	•45	•39	•29
Mu Sm	122	123	124	123	124	123
Ik	15.1	11.0	14.4	14.7	14.6	14.7
Eb			6.6			
Gain			148			
Noise	7.2	7.2	18.4 7.3	7 2	~ <b>1</b>	
Cin	3.20	3.20	3.18	7.3 3.19	7.1	7.2
Cgp	1.76	1.75	1.75	1.75	3.19 1.76	3.20
Cpk	.012	.014	.015	.014	.014	1.76 .014

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## EXTENDED LIFE TEST

# Improved 6299

Life Test	Condition		00 VDC •3 V RK/I	b = 10 Ma	
Accum. Hr	s, 0	108	245	406	566
Test Char	acteristic	s/Tube No.	15		
If Eg Mu Sm Ik Eb Gain	300 .45 110 14.1 8.1 151 17.6	.45 109 15.1	•39 103 14•0	•39 110 15•0	•30 109 14•9
Noise Cin Cgp Cpk	7.5 3.111 1.88 .015	7.5 3.44 1.90 .015	8.2 3.43 1.91 .015	7.8 3.43 1.92 .015	7.5 3.45 1.95 .015

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			EXTENDED	LIFE TEST			
			Improve	d 6299			to I
	est Condit	Eb ions: Ef	= 200 VDC = 6.3 V R	K/Ib = 10	Ma		proc
	Hrs.726 haracterist	866 tics/Tube	1004 No. 15	1286	1490	1795	give
lf Eg Mu Sm Ik Eb Gain	•39 110 14•4	.19 112 14.2	305 •39 110 14•1 8•3 150	.45 110 14.2	•39 110 13•4	•30 108 13•7	crea nick with
Noise Cin Cgp Cpk	7.8 3.13 1.95 .015	7•5 3•44 1•95 •016	17.1 7.5 3.42 1.95 .016	7.7 3.42 1.96 .016	7.8 3.42 1.96 .015	8.0 3.41 1.97 .015	to t due best good
							cathc regul humid
							obtai coat

#### CONCLUSIONS

The temperature controller does decrease the operator skill required to perform an uniform exhaust cycle and thereby insures a more uniform product.

The inverted cathode support ring with .00045" cathode foil will give proper cathode temperature and result in better uniformity, increased ruggedness and a better cathoce-co-cathode shell connections.

Tubes with three seals of the hard solder construction with coppernickel-gold plating and a-c aging have shown good results or life test with the anode seal at 225° C. Tubes of this construction are superior to the regular 6299 on high temperature operation.

Failure of the 6299 during humidity testing has been found to be due to hydrogen penetration of the base metal of the tube's shell. The best results in minimizing hydrogen penetration has been obtained by a good plating of the tube.

Results from improved alignment and concentricity, optimization of cathode coating, and improved exhaust fixturing are now being applied to regular production tubes. Improved cleaning and plating resulting from humidity testing is also now standard practice.

Increased strength and uniformity in hard solder seals has been obtained by using a finer particle size in the metalizing mix used to coat the high alumina ceramics.

The pilot run has been completed and conforms to the test specification.

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The extended life test has completed 1795 hours. The complete 5000 hour life test data and the analysis of mode of failure will be presented in an addendum to the Final Report.

### PUBLICATIONS, LECTURES

### REPORTS AND CONFERENCES

- PUBLICATIONS None
- LECTURES None
- REPORTS Monthly Narrative Reports Nos. 1 8 <u>Development Of An Improved JAN 6299</u> by F. A. Marra for the period from 1 May 1961 through 31 December 1961.

Monthly Narrative Reports Nos. 9 - 12 Development Of An Improved JAN 6299 by F. S. Sawicki for the period from 1 January 1962 through 30 April 1962.

Monthly Narrative Reports Nos. 13 - 34 Development Of An Improved JAN 6299 by D. L. Cook for the period from 15 September 1962 through 30 June 1964.

Quarterly Progress Reports Nos. 1 - 3 Development Of An Improved JAN 6299 by F. A. Marra for the period from 1 May 1961 through 31 January 1962.

Quarterly Progress Report No. 1: Development Of An Improved JAN 6299 by F. S. Sawicki for the period from 1 February 1962 through 30 April 1962

Quarterly Progress Reports Nos. 5 - 10 Development Of An Improved JAN 6299 by D. L. Cook for the period from 17 September 1962 through 31 March 1964

### CONFERENCES - 1. Organization and personnel present:

USASSA H. P. Blodgett General Electric Company A. T. Tomko, J. D. Secord, F. A. Marra

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CONFERENCES - 1. Place and date:
```

General Electric Company Receiving Tube Department Scranton, Pennsylvania

September 11, 1961

Subject:

Review status of the contract.

- 2. Organization and personnel present:
  - USASSA L. Coblentz

General Electric Company J. E. Campbell, J. T. Duncan, F. S. Sawicki J. D. Secord, H. L. Thorson, A. T. Tomko

Place and date:

General Electric Company Receiving Tube Department Scranton, Pennsylvania

February 15, 1962

Subject:

Discuss what effect the transfer of Production Engineering measures Contract No. DA-36-039-SC-85953 (Type 6299) to Owensboro, Kentucky, would have on performance.

3. Organization and personnel present:

USASSA S. Vitali, L. Coblentz General Electric Company

D. L. Cook, L. K. LaDue, F. S. Sawicki, J. D. Secord, A. T. Tomko

Place and date:

General Electric Company Receiving Tube Department Scranton, Pennsylvania

April 10, 1962

CONFERENCES - 3. Subject:

evice status of contract and iscuss what effect cur transfer of iroduction Engineering measures Contract No. DA-36-039-SC-85953 (Type 6299) to Owensboro, Kentucky will have on performance. 4. Organization and personnel present: USASSA L "oblentz General Electric Company L. Cook, E. L. lavis, J. T. Duncan, A. T. Tomko Place and date: General Electric Company Receiving Tube Lepartment Owensboro, Kentucky September 12, 1962 Subject: Leview status of the contract and discuss the effects of the transfer of Production Engineering measures Contract No. DA-36-039-30-85953 (Type 6299) to Owensboro, Kentucky. 5. Organization and personnel present: USASSA L. Coblentz General Electric Company D. L. Cook, E. L. Davis, J. N. McClanahan, A. T. Tomko Place and date: General Electric Company 316 East Ninth Street Owensboro, Kentucky January 15, 1963 Subject: Feview status of the contract.

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CONFERENCES - 6. Organization and personnel present:

USASSA Leonard Coblentz

General Electric Company D. L. Cook, E. L. Davis, A. T. Tomko

Place and date:

General Electric Company Receiving Tube Department Owensboro, Kentucky

April 24, 1963

Subject:

Review status of the contract

7. Organization and personnel present:

USAERDL Helmith Kaunzinger

General Electric Company D. L. Cook, E. L. Davis, A. T. Tomkc

Place and date:

General Electric Company Receiving Tube Department Owensboro, Kentucky

June 26, 1963

Subject:

Review status of the contract

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8. Organization and personnel present

USASSA Leonard Coblentz

General Electric Company D. L. Cook, E. L. Davis, D. L. Dyke, A. T. Tomko CONFERENCES - 8. Place and date: General Electric Company Tube Department Owensboro, Kentucky October 16, 1963 Subject: Review status of the contract 9. Organization and personnel present **USAEMSA** Simon Zucker General Electric Company D. L. Cook, L. L. Davis, A. T. Tomko Place and date: General Electric Company Tube Department Ovensboro, Kentucky November 14, 1963 Subject: Discuss specification for testing of preproduction samples. Organization and personnel present 10. USASSA Stan Sockalov General Electric Company D. L. Cook, F. L. Lavis, M. R. Speray, A. T. Tomko Elace and date: General Electric Company Tube _epartment Owensboro, Kentucky January 24, 1964 Subject: Review status of the contract and view pilot run facilities.

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IDENTIFICATION OF	F TECHNICIANS	in F
A. MAN POWER EFFORT		in l
TECHNICAL		time
Barrass, Martha	17	
Childs, C. G.	19	three
Cook, D. L. Crawford, S. C.	1637	
Dyke, D. L.	23 62	
Grady, B. I.	28	of t
Haberkern, R. J.	45	01 01
Jeffery, L. F.	2	compl
Kirby, P.	19	
LaDue, L. K.	250	
Marra, F. A.	744	7 - D
McClanahan, J. N. McDowell, J. K.	127	LaDue
Moore, G. E.	8 10	
Moredock, D.	2	
Morris, M. E.	;. <b>ت</b>	from
Owsley, M. F.	364	
Ringland, R. S.	10	Elect
Sawicki, F. S.	320	
Speray, M. R.	18	the m
Stephens, P. Tomko, A. T.	18	
Winkler, R. H.	471	1
······································	20	Corps
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### BIOGRAPHICAL INFORMATION - TECHNICAL

### Cook, D. L.

A native of Potosi, Missouri, Mr. Cook received a Bachelor's Degree in Electrical Engineering from Missouri School of Mines and Metallurgy in 1960. ١

He has been associated with the General Electric Company since that time starting as an Engineering and Science Program trainee.

Since 1961, he has worked in Planar tube manufacturing except for a three month assignment in Planar Product Design Engineering.

Mr. Cook had responsibility for technical cognizance and guidance of the contract for the period from 15 September 1962 through the completion of the contract.

### LaDue, L. K.

Mr. LaDue is a native of New York State where he graduated in 1955 from St. Lawrence University. He joined the General Electric Company, Electronic Division Physics Training Program oriefly prior to entering the military service.

From 1956 through 1960 he served as a lieutenant in the U.S. Army Corps of Engineers.

Upon leaving the service in early 1961 he joined the Receiving Tube Department's Planar Design Section. He was with the Receiving Tube Department's Scranton planar production facility for approximately one year assigned to small ceramic lighthouse transmitting tubes. In 1962 he was transferred to the Owensboro location as Planar Design Engineer.

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Marra, F. A.	Morri
A native of Jessup, Pennsylvania, Mr. Marra earned his Bachelor's	as a f
Degree in Electrical Engineering from the Pennsylvania State University	1
in 1956.	
He has been associated with the General Electric Company since that	a B.S.
time starting as a Manufacturing Training Program trainee.	Owsley
From 1957 to 1961, his assignments have been that of a Factory	M
Engineer responsible for the manufacture of Thyratrons and Ceramic	tube m
Lighthouse tubes.	Planar
Mr. Marra had responsibility for technical cognizance and guidance	H
of the contract for the period from 1 May 1961 through 31 December 1961.	chemic
McClanahan, J. N.	in 193
Mr. McClanahan, a native of Kansas, received his Bachelor's Degree	process
in Electrical Engineering from the University of Kansas in June, 1962.	engine
Upon graduation, he joined the Planar and Thyratron Section as a	in 1938
Process Control Engineer, working primarily on the Miniature Ceramic	Ве
Lighthouse tubes for one year.	setting
nightingse tubes for one year.	the sal
Morris, M.L.	He
Mr. Morris is a native of Lancaster, Kentucky. He served as an	chemist
Airborne Radio and Radar Repairman in the U.S.A.F. from 1954 to 1958.	His ass
He spent two and one half years at Valparaiso Technical Institute	prepara.
where he received an associate degree in Electronic Engineering.	producti
Upon leaving school in June, 1960, he joined the General Electric	plating
Company in Owensboro, Kentucky, serving as an engineering aide in the	

Miniature Ceramic Section.

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### Morris, M. E. (Cont'd)

In December 1963, he joined the Ceramic Lighthouse Section, serving as a Tube Engineering Technician.

During his tenure at General Electric, he has continued work toward a B.S. by way of night school.

## Owsley, N. F.

Mr. Owsley has over 25 years experience as a chemist in electron tube manufacturing operations. To is presently chemist for General Electric Planar-Thyratron manufacturing operations, located at Owensboro, Kentucky.

He was employed by the Engineering section - chemical laboratory and chemical preparations Ken-Rad Tube and Lamp Corporation, Owensboro, Kentucky, in 1933. His assignments were: analytical chemist, chemical preparations, process development and control.* In 1936 he was transferred to factory engineering as Process Control Engineer. He left the Ken-Rad organization in 1938.

Between 1938 and 1942 he was employed in crude oil production, initially setting up and operating a field laboratory for checking and controlling the salt content of crude oil purchased for shipment to refineries.

He returned to the Ken-Rad organization, February, 1942, as chief chemist for Ken-Rad Transmitting Tube Corporation of Owensboro, Kentucky. His assignments were to set up and supervise the operation of a chemical preparations section, to develop and control processes related to the production of transmitting and cathode-ray tubes, included were electroplating operations.

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## inclu Mr. Owsley became associated with the General Electric Company Ceran through its purchase of the Ken-Rad installations in 1945. He continued with General Electric as a chemist supervising the operation Assis of the chemical laboratory and chemical preparation section serving all of the Owensboro manufacturing operations. He was assigned special for a projects related to process development and control and in new materials 1 evaluation in the production of metal and glass receiving tubes. guida In mid 1951 he was transferred to the General Electric Anniston 30 Api Tube Plant organization as chief chemist, later becoming Supervisor of process control. The balance of 1951, he spent in the planning Tomko, and procurement of laboratory and chemical preparation facilities for M establishment in the new plant. He transferred to the Anniston, Alabama Degree Jocation March 31, 1952. F Mr. Owsley was transferred to the Owensboro Planar-Thyratron Operation Force February 1963. His present position title: Engineer, Chemical Process Base,

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## Control.

* As related to the manufacturing of metal and glass receiving tubes.

## Sawicki, F. S.

Owsley, W. F. (Cont'd)

A native of Scranton, Pennsylvania, Mr. Sawicki attended the product University of Scranton, where he received his bachelor's degree in Electronics in 1958.

He has been associated with General Electric Company since 1954. In From 1959 through 1962 as Factory Engineer, he was responsible for Lighthouse tubes. This interval assigne

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### Sawicki, F. S. (Cont'd)

included a six months period as Process Control Engineer assigned to Ceramic Lighthouse tubes.

During 1957 through 1959 his assignments included engineering Assistant assigned to Magnetrons and Gap tubes.

From 1953 through 1956 Mr. Sawicki served as Electronic Technician for a two and one half year period.

Mr. Sawicki had the responsibility for technical cognizance and guidance of the contract from the period from 1 January 1962 through 30 April 1962.

### Tomko, A. T.

Mr. Tomko attended Villancva University and received his Bachelor's Degree in Electrical Engineering in 1950.

Following graduation he was recalled to active duty with the Air Force assigned to the Armed Forces Special Weapons Project at Sandia Base, New Mexico and the Los Alamos Scientific Laboratories at Los Alamos, New Mexico.

Upon completion of his tour of active duty he joined the Power Tube Department in 1952 as Line Engineer on Hydrogen Thyratrons. During the next three years this responsibility was extended to include the production engineering of Inert Gas and Mercury Industrial Control Thyratrons. In 1955 he was appointed Engineer-General Foreman of the Ceramic Lighthouse Manufacturing.

In 1957 he was appointed Manager, Manufacturing of the Ceramic Lighthouse Sub-section. From January 1961 through May 1964 he was Issigned as Manager, Manufacturing Engineering, Planar-Thyratron Operation.

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# APPENDIX A

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Proposed by General Electric Company Owenaboro Kentucky 2 December 1963

MIL-E-1/___(EL)

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### MILL ARY SPECIFICATION SHEET

### ELECTRON TUBE. UHE PLANAR TRIODE

### 6299

## This specification sheet forms a part of the latest issue of Military Specification MIL-E-1.

### DESCRIPTION: Low Noise class A amplifier

F1 = 3,000 megacycles

### ABSOLUTE-MAXIMUM RATINGS

I.

Paremeter:	Eí	Eb	Ec	ГЬ	Рр	tk	Cooling	T (seal)	Alt	
Unit:	v	Vdc	Vdc	mAdc	w	Sec		•C	ft	
Maximum ¹	6.6	200	0	12	20		Conduction	225	Unlimited	
Minimum:	6.0		- 10			•				
	(see note	1)	(see note	2)		(5	iee notes 3 and 4	(See note 4)	(See notes 3 a	in4 5)
TEST CONDITION	ONS: 6.3	175	Adjust	10	 (8	180 es note	Conduction 6)			

PAR. NO.	TEST	CONDITIONS	AQL (PERCENT IN DEFECTIVE)	SPECTION	SYM. BOL	- LIM Min.	ITS Max.	UNIT
	General							
3.1	Qualification	Required for JAN marking			•••	•••	•••	•••
3.6	Performance	(See note 7)						
4.5	Holding period	t = 7 days min					•••	
4. 9, 2	Dimensions	(See fig 1)		• ••			<b>.</b>	
	Qualification inspection (see note 8)							
4. 9. 20. 5	Shock test	No voitages, hamme angle = 20°(see note			•••			• • •
	Arcoplance inspection peril (production)		.,					
4.8	Insulation of erectrodes	Ebb = -500 Vdc, Thk = +45 Vdc, grid grounded (see note 11)			Rgk Rgp	0.25 5.0		Meg Meg
4. 10. 1. 1	Emission	Eb = 0, $Ef = 5.5 V$ (max), $eb = 390 v$ poak-to-peak 60 cycles, $Ec =$ -18.0 Vdc, $eg = 46 v$ peak-to-peak 60 cycles, $Rg =$ 470 ohm, $Rk = 10$ ohms (see note 12)	(See v note 10}	(See note 10)	I.	35		mAdc
4.10.5.3	Plate voltage	Eb/1b = 10 mA, Ec = 0 (see note 13)			ЕЪ	75	175	Vdc

PAR. NO	. TEST	CONDITIONS	NOU (PPRCENT Dur ECLIVE)	INSPICTI LEVEL	OH BO		LIMITS		r
	Acceptance inspection part 1 (production) - (Contd)					Mir	n Ma	x	
4.10.8	Heater current								
4.10.9	Transconductance				11	28		20 mA	
	Power gain (1)	Eb/1b = 10 0 mAdc, Ec = 0, F = 1,200±5 Mc, bandwidth = 10 Mc min (see notes 33 and 14)	(See nots 10)	(See pate 10)	galı	11,50 n 13.(		µmho db	•
•••	Noise figure (1)	Eb/1b = 10 mA, Ec = 0 F = 1,200±5 Mc (ree notes 13 and 14)			NF	•••	. 8	5 46	
	Acceptance inspection part 2 (design)								
4.9.	Low-frequency vibration	Eb/1b = 10 0 mAdc, Ec = 0 Rp = 10,000 ohms (see note 15)	6. 5	L6	Ep	••••	10	)0 mV	
4. 10. 11. 1	Amplification factor		6. <b>5</b>	L6	Mu	** n			
4, 10, 14	Diract interelectrode capacitance	No voltages (see note 16)	6.5 6.5 6.5	L6 L6 L6	Mu Cgk Cgp Cpk	\$5.0 3.0 1.5	9. i 2. i	0 0 µµ£ 0 µµž 5 µµ£	
	Power gain (2)	Power gain (1), F = 3, 00° 25 Mc (see notes 13 and 17)	6.5	L6		10. C		5 հուլ	1
	Noise figure (2)	Noise figure (1), F = 3, 000±5 Mc (see notes 13 and 17)	6.5	L6	NF	•••	13.5	i db	1
-	Acceptance inspection part 3 (life)								12
ill and	Humidity Text	(See note 20)	10.0		۵If	•••	10	<i></i>	
6. 11. 3. 4 <u>1</u>	Life test (1)	Eb = 200 Vdc, Rk/Ib = 10 mA, group &	••••	••••	t	1000		hr	13
.114 L	lfe-test(1) end points	Transconductance			4Sm	•••	25 0	≪de + + rease	14
•••••		Noise ligare (1)	•••	••••	۵NF	••••	JU	db m- Vrease	15
. 11 and . 11. 3. 5 Li	ife test (2)	Eb - 200 Vdc. Rk/1b = 10 mA. Group C. TE = 225°C(mi	in)		t	500	•••	hr	16
11.4 Li	ife test(2) end points	Transconductance			≙Sm	•••	25.0	% de- Crease	17
		Noise figure (1)		'n	۵NF	•••	1.0	db in- Crease	18
9-18 Co	ontainer drop	Roquirod							19.
									20.
Pr	reparation for	(See nots 18)							20.

#### NOTES:

- 1. Heater may be operated at 5.3 solve +36 percent. This life and noise figure may be affected by this wider variation. The tube is estimated for series bester string operation.
- 2. Grid shall not draw current. Excelling grid-cathode wattige may cause damage due to extremely small spacing.
- 3. a. Tube cannot be cooled by free radiation and convection, means for conducting and dissipating heat must be provided in order to prevent excessive real temperatures.
  - **b.** Applications at high adjutudes shall be examined carefully to assure that sufficient provision for discipation of heat has been made
- 4. Sufficient conduction or convection cooling, or by n, must be provided for heater, cathode, grid, and anode seals to limit the maximum evelope temperatures to the specified maximum of 225°C under all operating conditions. Where compliants is placed on long and reliable life, lower tube envelope temperatures is if the used.
- 5. Altitude is unlimited as the maximum rating of 200 volts is insufficient to cause voltage breakdown at any altitude
- 6. The heater preheating miy be 6 6 volts maximum, unless otherwise specified.
- 7. In addition to the paragraphs specified hereon, only the following test and requirements listed in 3.6 shall apply 3.3, 3.3, 1, 3.7, 3.7, 7, 3.8, 4.1, 4.3, 4.4, 4.6, 4.8, 4.9, 1, 4.9, 21.
- 8. All tests listed hereon shall be performed during qualification, however, this shock test is normally performed during qualification inspection only.
- 9. Apply the force perpendicular to the plane of the grid from the cathode end. Use fixture as shown on Drawing 274-JAN, or equivalent. Electrical tests after shock shall include transconductance and electrode insulation.
- 10. The AQL of the combined defectives for attributes in acceptance in pection, part 1 (production), excluding inoperatives and mechanical, shall be 1 percent. A the paying one or more defects shall be counted as one defective. Standard MIL-STD-105, inspection level II, shall apply.
- 11. Anode and cathode voltages shall not be applied simultaneously. Allowable circuit resistance is 1,000 ohms per volt of supply voltage.
- 12. Preheat 1 minute minimum at Ef = 5.5 V Voltages eb and eg must be in phase. Read average cathode current. If the current exceeds the minimum limit and is increasing, the tube is a If the current exceeds the minimum limit and is decreasing, the reading shall be allowed to re, and the tube is acceptable if the stable reading exceeds the minimum limit. Provision must be inade in the test equipment so that switching transients of plate voltage apply no more voltage than the amount specified.
- 13. Preheat 1 minute minimum at 6.3 voits.
- 14. Test in cavity as shown on Drawing 271-JAN, or equivalent. An approved noise source, or equivalent, shall be used for noise figure measurements. Power input level shall be about -75 dbm
- 15. Test in fixture as shown on Drawing 273-JAN, or equivalent. Vibrate in plane perpendicular to the plane of the grid.
- 16. Test in fixture as shown on Drawing 270-, or equivalent
- 17. Test in cavity as shown on Drawin, 272-JAN, or equivalent. An approved noise source or equivalent shall be used for noise figure measurements. Power input level shall be about -75 dbm.
- 18. Tubes shall be prepared for comestic or correcus it client as specified in the contract or order. in accordance with Specification MIL-L-7² 1 k and (continuer drop) test (a) and container size D shall apply
- 19. Referenced documents shall be of the policy in officer on the detect invitation for the
- 20. Test tubes first production interaction of the state to prove the state device the state of the state of



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- All dimensions in inches, Preship test all tubes for TIR. ۶,

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- Test these dimensions on 10 tubes 6, per month when in continuous production. Failure of more than one tube to most the tolorance for my of those dimensions shall cause that dimension to become a 6.5 AQL, L6 Design Test for all lots in
- process. Eccontricity of contact surfaces shall be ٩. saged from center line of reference, and shall be as follows. Note b shall apply.

Contact Surface	TIR, maximum	Reformeo
Anode	0.015	Grid
Cathode	0.020	Grid
Cettor Heator	0.030	Orid
MELTOT	0.045	Orid

DIM	AQL (PERCENT	INSPECTION	1	-IMETS
	DEFECTIVE;	LEVEL	Min	MAE
	ACCEPTANCE	INSPI.CTION,	PART 2 (DES	IKJINI
			0. 6410	11,040
····		1.6	0 410	0. :410
<u> </u>	'	1.0	0.410	0 1/0
		1./1	•••	0.:12
+	0.5	1.11		0 415
_	0.0	10	1 0	0.103
ACCEPT	ANCE INSPECT	Ote, PART 3 (	PLRIODKILE	SEA ST PLE AL
	•-•	•••	. 03?	
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			3 ' (N	R
			0.08	
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Figure 1. Quilling drawing.

## A P P E N D I X B

Limited Production Equipment

### LIMITED PRODUCTION EQUIPMENT

The following is a description of the limited production equipment listed under Sub-Item 1-2 of the contract.

```
1. A-C aging rack (2)
     Dimensions:
       33" wide
       76" high
       24" deep
     Approximate weight: 325 pounds
Voltage input: 115V A-C
     Purpose: Specialized equipment for a-c aging of electron
                tube type 6299.
     Prints: 13700K T6-27-41 (4 sheets)
2. High temperature life rack with recorder (1)
     Dimensions:
      33" wide
      76" high
      24" deep
     Approximate weight: 350 pounds
     Voltage input: 115V A-C
     Purpose: Specialized equipment for the life testing at
               225 C. anode seal temperature of electron tube
               type 6299.
     Prints: 13700K T5-23-41
3. 50 position life rack (1)
     Dimensions:
      33" wide
      76" high
      24" deep
      Approximate weight: 310 pounds
Voltage input: 115V A-C
      Purpose: Specialized equipment to perform d-c life
                testing of electron tube type 6299.
      Prints: 13700K T5-23-42
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## LIMITED PROLUCTION EQUIPMENT (CONT'D)

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Note 1: Equipment should be calibrated every three (3) months when in use.

Note 2: Faulty positions should be reported for maintenance.



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Frinch E/COR NEW & HOLES ADDON , DIA TUDNED				- 4. 134 57:2 2 15 134 1 4 4 4 4 5 1 2 13 13 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	



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# APPENII. C

Processing Specification

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## PROCESSING SPECIFICATION

The processes developed or proven for use on the 6299 in the performance of this contract are as follows:

I. Hard Solder Anode Seal Assembly

Α.	C	omponent Pa	rt	Processes
1.	S-K-K586	Pt. 1	Solder Washer	Cl-1B, 06-30
2.	KR3703		Anode Ceramic	Cl-3E, F3-1P, Jl-1A, F2-4G 1330C. 45 min. RIE/SCR-1, 20 amp. 30 min. F2-1 950C 15 min.
3.	KR60102		Anode	Normal processing

B.1. Anode ceramic is placed in brazing fixture. Solder washer is placed on anode ceramic. Anode is inserted in anode ceramic and brazing weight is placed on anode. Fixtures are taken to furnace area.

2. Anode assemblies are brazed F2-1 in a belt furnace with a belt speed of 0.4 feet per minute at 850C.

3. Anode assemblies are removed from brazing fixtures.

L. Anode assemblies are inspected 100% on helium leak detector to check quality of hard solder seals.

٩.		Co	mponent Part	Processes		
	1.	SK-K-586	Pt. 2	Brazing Washer	Cl-1B, C6-3C	
	2.	SK-K-586	Pt. 3	Brazing Washer	Cl-1B, C6-3C	
	3.	SK-∴-584		Getter Shell	Cl-1B, C4-1A Cl-2L, F2-4A 1000C 30 min C4-1A, C5-1A/SCR1 R1E/SCR1, 25 amp 60 min. (1200 parts with metal pins) F2-1 850C 30 min.	
	4.	KR70384		Cathode Shell	Cl-lE, CL-l: Cl-2L, F2-LA 1000C 30 min. CL-LA, C5-LA/SCRL RLE/SCRL 25amp 60 min. (800 parts with 3mm plastic balls) F2-L 850C 30 min	
	5.	к-582		Getter Insulator	Cl-2E, F3-1P J11A, F2-4G 1330C R1E/SCR1 20amp. 10 min. F2-1 850C 15 min.	

B. 1. Cathe de shell is placed on brazing fixture followed by #3 brazing washer, getter ceramic, #2 brazing washer, and getter shell. Brazing weight is placed on stock taking care to keep alignment. Fixture is taken to furnace area.

2. Preseal assemblies are brazed F2-1 in belt furnace at 850C with a belt speed of J.L feet per minute.

3. Preseal assemblies are removed from brazing fixture.

4. Preseal assemblies are inspected 100% on helium leak detector to check quality of hard solder seals.

III. Improved Cathode And Insulator Assemblies

Α.		Component Par	t	Processes		
	1.	KR3735	Cathode Ceramic	Cl-3E, F3-1P Dip Coat moly manganese F2-2D/S1		
	2.	KR70473	Cathode Support Ring	C1-1B, CL-1A C5-2E/SCR1, C6-3D R1A/SOR3		
	3.	AC606DA	Cathode Assembly	Normal Processing		

B. 1. Cathode ceramic is placed on brazing fixture. Cathode assembly is inserted in cathode ceramic. Cathode support ring is inserted with legs between cathode assembly and cathode ceramic. Brazing fixture is placed in the cathode boat. When boat is loaded, the boat is transferred to the furnace area.

2. Cathode and insulator assemblies are brazed F2-1 1110C four minutes in box furnace.

3. Cathode and insulator assemblies are removed from brazing fixture and examined under a 10x microscope for brazing quality.

4. Clean Cl-2C

5. Spray Л-1Р

IV. Heater Ceramic

Cl-3E, F3-1P Coat with titanium hydride

-3-

### V. Final Assembly N11606"

Plating Processing

//SCR-1 (with metal pins - 4 x 3 / min, AF 30 min.) '5-3D RIE/3 (metal pins 200 tubes Lo amp. 60 min. RIM/S1 (metal pins 200 tubes 10 amp. 120 min.) C6-3D 1 min. RIP/1 metal pins 100 tubes 20 amp 1 min 10 amp 10 min RIP metal pins 100 tubes 6 amp 20 sec. 4 amp 1 min. 2 amp 18 min.

Barrel Burnish (metal pins & AP2X

VI. A-C Aging Schedule (6299)

### EQUIPMENT

100 position a-c aging rack

1. Place tubes in fixtures. Make certain a positive connection is made on all elements.

2. Turn on low pressure air for moderate cooling.

3. Adjust filament voltage to 7.0 volts a-c. Allow one minute warmup time.

4. Press plate voltage start button and adjust to 310 a-c.

5. Adjust grid current to 8 ma and plate current to 10 ma on each tube.

6. If a tube fails to draw current, check its position in the fixture and/or check its characteristics in the static test set. Reject those tubes which are inoperative.

7. Repeat Step 5 at 1 hour and 6 hours.

8. After 24 hours adjust filament voltage to 6.3 volts a-c.

-4-

9. Adjust grid current to 6.0 ma and maintain plate current at 10 ma on each tube.

10. Tubes are to be removed after 24 hours.

11. Report faulty positions so they may be repaired.

Aging Conditions

Step 1  $E_f$  7.0 vac  $I_c = 8.0 \text{ ma/tube}$   $E_{bb} = 310 \text{ vac}$   $I_b = 10.0 \text{ ma/tube}$ Time = 24 hours  $E_f = 6.3 \text{ vac}$   $I_g = 6.0 \text{ ma/tube}$   $E_{bb} = 310 \text{ vac}$   $I_b = 10.0 \text{ ma/tube}$ Time = 24 hours

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# Cl-lB

DEGREASING WITH CHLORINATED HYDROCARBON SOLVENTS

Vapor	Degreasing (	cool solven	t immersion		PURP

#### PURPOSE

This method is used to remove non-oxidized oils, greases, fats and such lubricants as are used during forming or other manufacturing operations, or are placed on the work to protect it from corrosion during storage.

#### MATERIALS

Acetone

# EQUIPMENT

1. Two Dip Immersion Degreaser

2. Baskets

# PROCEDURE

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1. Give the parts a cursery examination for paints or tapes used for color coding. If these materials are present, remove them by washing in acetone before proceeding.

2. Parts are thoroughly dried.

3. Parts are placed in the basket so they drain easily and liquid solvent is not trapped in the parts.

4. Basket of parts is placed in the vapor chamber until the vapor no longer condenses to a liquid on the parts.

5. Parts are slowly transferred to the rinse chamber and immersed for at least 30 seconds.

6. Parts are again placed in the vapor chamber until the vapor no longer condenses to a liquid on the parts.

7. If necessary parts are tilted or retated while still in the vapor chamber to encourage solvent drainage.

8. Parts are removed from the degreaser.

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C1-2C/SCR1

# CLEANING WITH WATER, ACETONE AND/OR ALCOHOL

#### PURPOSE

This method is used to remove dust and particles.

# MATERIALS

Denatured ethyl alcohol Dry Acetone

# EQUIPMENT

- 1. Ultra-Sonic cleaning unit
- 2. Suitable holder
- 3. Container for solvent
- 4. Culture dish
- 5. Tweezers

# PROCEDURE

Alcohol or Acetone is poured into container to a height of 2".
 Parts are assembled onto the holder, so that the open end of

the eyelet is pointing towards the center.

3. Holder is placed into the container with the denatured

ethyl alcohol so that the parts are just under the surface of the liquid.

b. The generator is allowed to operate for three minutes.
5. The holder is removed and parts are removed with tweezers.
6. Parts are blown dry with low pressure filtered air.

- 7. Parts are stored in a covered culture dish.

# Cl-2L

# CLEANING WITH WATER, ACETONE AND/OR ALCOHOL

# Ultra-Sonic Cleaning With Acetone

MATERIALS	
Acetone	PURPOS
EQUIPMENT	T. S
1. Suitable holder or container	p.
2. Ultra-sonic generator (GE Cat. #8665966 G-3)	a
3. Container for solvent	f
4. Watch glass cover for holder	T
	W.
PROCEDURE	
1. Acetone is poured into container to a height of 2".	MATERL
2. Parts are assembled onto the holder or container.	N
3. Holder is placed into the container with the acetone so that	
the parts are just below the surface of the liquid. A watch glass	Bath Com
cover is used to keep cleaning solvent from evaporating.	
4. The generator is operated at 150 ma. for 3 minutes.	ACE
5. Holder is removed and parts are spread on lint-free paper	
to dry.	B. Dei
PRECAUTIONS	C. Ige
1. Cleaner should be kept covered when not in use.	det
2. Use fresh cleaning agent for each cleaning.	equ
3. Use only clean containers for cleaning agent.	င်မှင

D. Nit

EQUIPME A.

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# C1-3E

# CLEANING WITH WATER, ACETONE OR ALCOHOL

(Ultrasonic-Acetone, Deionized Water-Nitric Acid - Ceramics)

# PURPOSE

The purpose of this process is to clean dense ceramic insulators in such a manner that all conceivable contaminants are anticipated to be present on the parts before cleaning and are effectively removed, and that the resulting ceramic parts are clean to the degree required for use in the making of high quality, reliable electronic tubes. This process uses ultrasonic cleaning of dense ceramic insulators with acetone and deionized water coupled with acid cleaning in HNO₃.

# MATERIALS

NOTE: Deionized Water Used Throughout

ith	Composition	Composition Patio	Them cal irade	no. Baths .cquirea
A.	cetone	Acetone alone, rm. temp.		(2 Ultrasonic
В.	Deionized H ₂ O	Mater alone, rm. temp.	1,000,000 ohm min.	) (1 Ultrasonic)
C.	Igepal (850) detergent or equivalent	Added to first deionized water bath	Andora Chemicals General Analine & Film Company 135 Hudson Street New York 14, N.Y.	5-10 cc/gal.

Vo Dethe

D. Nitric Acid 30% HNO3 - rm. temp.

# EQUIPMENT

A. Suitable tanks, beakers or other containers for the required baths.
B. Suitable basket or other perforated container for holding parts.
Should be preferably non-metallic, such as nylon, diallyl phthalate or polyvinyl chloride, or a metallic basket lined with clean ceramic chips so that ceramic parts do not contact the metal.
C. Ultrasonic generator; transducer, either built into tank or suitable for immersion into bath. Capacity - 50 watt/gal. liquid, minimum.
D. Nitric acid resistant perforated basket lined with clean ceramic chips, if metallic.

## BASIC PROCESS

Because at the present state of the art it is not possible to accurately and exactly specify and measure the desired end result of this process, it is necessary to specify the process itself in detail. The described process is a compilation of the best thinking of those dealing with the cleaning of ceramic insulators within the department and is supported by actual and successful application of the process, in detail, within the department. In order to guarantee the attainment of success theretofore obtained with the process, it is necessary that it be carried out as specified and departures from the process not be made without being sure of the necessity for any modifications.

#### PROCEDURE

Note: Ceramic parts should never be handled with bare hands, with woven gloves, with paper over fingers or with metallic tools. It is important to use handling tools or equipment provided with approved non-metallic contact surfaces.

A. Thoroughly rinse in acetone. Ultrasonorate in acetone. Remove parts from bath with ultrasonic power on.
B. Ultrasonorate in delonized water to which a quantity of Igepal 850 detergent, or equivalent, about 5-10 cc/gal. has been added. Remove parts from bath with ultrasonic power on.
C. Rinse in three-step deionized water bath for at least 15 seconds in each step.
D. Transfer parts to nitric acid resistant perforated basket, if not already so contained, lined with clean ceramic chips if metallic, and soak in 30% nitric acid for 5 minutes.
E. Thoroughly rinse parts in the three step deionized water bath for at least 15 seconds in each step.
F. Ultrasonic clean in deionized water for 5 minutes.
G. Parts are rinsed in two separate acetore baths for at least five seconds in each bath.

H. Infra-red dry.

# PRECAUTIONS AND CONTROLS

A. Successful processing of parts according to this instruction will depend in large measure upon proper control of the solvents, solutions and equipments called for. Necessary control procedures should be incorporated in corresponding specific standing instructions. B. In order to make the cleaning action most effective in the ultrasonic baths, the ultrasonic generator should be adjusted for each case and each batch of parts to produce optimum cavitation within the bath.

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# PRECAUTIONS AND CONTROLS (CONT'L)

D. In order to preserve the processed parts in their cleaned condition, it is advisable that they be placed in clean, covered containers after this processing and be so stored or transported to the next operation.

MEASURABILITY OF END RESULT Parts which have been properly cleaned per this basic process will look thoroughly clean to the naked eye and under a magnifying lens, with no evidence of any stain, soil or "water marks".

# C4-1A

# ALKALINE CLEANING

# Clepo #6h

# PURPOSE

This method is used to remove heavy metal soaps as well as exidized organic compounds which are not removed by vapor degreasing.

# MATERIALS

Control Bath Composition Limits Solution #1		Engineering Data Chemical Grade Conc. in Container
Clepo #64 5-10 oz./g Deionized water	al 8 oz. 1 gal.	Gum Chemical Co. 100% powdér 500,000 ohms or greater
Solution	is used at boiling	•
Solution #2		
Hydrochloric acid Deionized water	l part 3 parts	37% HCl 500,000 ohms or greater
Solutio	n is used at room te	mperature.
Solution #3 Ammonium hydroxide	l part	28% NH3
Deionized water	3 parts	500,000 ohms or greater
Solutio	n is used at room te	•
Solution :		
Hydrochloric acid	acid only	37% HC1
	ank plastic crocks o enware crocks.	n stainless steel tanks, r earthenware crocks and ould be used.
agitation is selecte if the work is compl	d. A much greater l etely withdrawn from	movement of parts for thorough evel of agitation is provided the cleaning and rinsing baths y swishing the work about.

# PROCEDURE (CONT'D)

Parts are immersed in solution #1 for a minimum of 10 minutes. Clepo solution must be 90-100C in order to clean parts thoroughly. 3. Parts are agitated in hot water for at least 15 seconds with inlet faucet wide open. Hot rinse water must be 90-1000 to dissolve all of the lepo solution. u. Parts are agitated in cold water for at least 15 seconds with inlet faucet wide open. 5. Parts to receive further aqueous cleaning, omit Steps 5 to 11. 6. Parts with visible heavy rust are soaked in Solution #4 until clean. Other parts are agitated in Solution #2 until clean. 7. Parts are agitated in cold water for at least 15 seconds with inlet faucet wide open. 8. Parts are agitated in Solution #3 for at least 15 seconds. 9. Parts are agitated in cold water for at least 15 seconds with inlet fauc t wide open. 10. Parts are agitated in hot water for at least 15 seconds with inlet faucet wide open. Parts are shaken to remove excess water. 11. Parts are rinsed in acetone for at least 15 seconds. 12. Parts are dried with compressed air.

# TROUBLE SHOOTING

Dirty parts - parts remaining dirty during the process could be caused by:

1. Operating temperature of solution #1 is not at temperature specified.

- 2. Hot water rinse is not hot enough.
- 3. Solutions #1, #2, or #3 are contaminated.

4. Degreasing prior to caustic cleaning often sets up the drawing compound making it difficult to remove.

5. Caustic cleaning will not remove a carbon smut.

# C5/1A/SCR1

# CLEANING WITH ACID COMBINATIONS

Nitric, Sulfuric (Bright Dip)

# PURPOSE

This method is used to remove stains from molybdenum, copper, nickel or monel. Parts should be bright when cleaned by this method. Fernico or iron are not left bright. Oxides are not removed by this process, or they are removed so slowly that pitting results.

## MATERIALS

Note: Deionized water used throughout

Bath Composition Solution #1	Composition Ratio	Chemical Grade	Engineering Data Conc. In Container
-			
Nitric Acid	l Part		70% HNO3
Sulfuric Acid	l Part		98% H2SÓL
Deionized Water	l Part	1, 000,000 ohms o	r
		greater	

Solution is used at room temperature.

Suitable containers for deionized water.

#### EQUIPMENT

1. Tanks - Pla-Tank plastic crocks or earthenware crocks can be used for tanks.

2. Baskets - Stainless steel basket should be used.

# PROCEDURE

1 A basket large enough to allow free movement of parts for thorough agitation is selected. Cylinders may be handled with a hooked rod or strung on a wire to prevent contact between them.

2. Basket of parts is agitated in solution #1 for 2-5 seconds.

- 3. Parts are agitated in cold deionized water for at least 15 seconds.
- 4. Parts are agitated in hot deionized water for at least 15 seconds.
- 5. Parts are agitated in cold deionized water for at least 15 seconds.
- 6. Parts are rinsed in a 3 step deionized water bath for at least 15 seconds in each step.

Note: If next step in processing is plating then omit operations 7 and 8 and go directly to plating bath,

7. Parts are agitated in 2 separated acetome rinses for at least 5 seconds in each rinse.

PROCEDURE (CONT'D) 8. Parts are infra-red dried.

Parts should not be redipped if metal thickness is held to a close tolerance, since continual dipping reduces the thickness. Not more than 24 hours shall elapse between cleaning and assembly of parts.

# 15-2 / .r.-1

# CLEANING WITH HYDROCHLORIC ACID

(Immediately Before Plating)

# PURPOSE

Removal of oxide films and tarnish films - This instruction describes a preferred method for removing oxides and films from steel and fernico parts.

Appearance of part after cleaning - After cleaning the part with hydrochloric acid, the part should have a clean surface free from oil or discoloring stain. The clean metal may be etched or shiny.

# MATERIALS

		Engineering Data		
	Composition		Conc. in	
Bath Composition	ratio	Chemical Grace	Container	
Solution #1				
Acetone				
Hydrochloric acid	l Part		37% HCl	
Igepal 630	<b>l</b> cc/l	Jeneral Aniline & Fili	m	
Deionized water	l part	500,000 onms		
Solution is used a	at room tempera	ature.		
Sclution "2				
Sodium Cyanide	60 g/l	90% DuPont Special Qua	ality	
Igepal 630	1 cc/l	General Aniline & Fili	m	
Deionized water		500,000 ohms		
Solution is used a	it room tempera	ature.		
Solution #3				
Ammonium hydroxide	e 1 part		30% NH3	
Deionized water	3 parts	500,000 ohms	-	
Solution is used a	at room tempera	ature.		
EQUIPMENT				
1. Tanks - Pla-Ta	ank plastic cr	ocks and earthenware cro	cks can be	
used for hydrochlo solutions.	oric acid, sod	ium cyanide and ammonium	hydroxide	

2. Baskets - Baskets are stainless steel, nickel, monel, or polyvinyl chloride coated mesh baskets.

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#### PROCEDURE

1. A basket large enough to allow free movement of parts for thorough agitation is selected.

2. Parts are cleaned in Solution #1 according to the instruction number on the process cards which describes the operation following cleaning.

Operation Following	Immersion	Agitation	Steps Following
Cleaning	Time	Time	Step (2)
RIJ	10-30 min.	2 min	(3)(4)(6)(7)
RLE	10 <b>-30</b> min.	2 min	(3) (4)(6)(7)
RIM	10-30 min.	2 min	(3)(4)(5)
PlF	2-10 min.	2 min	(3)(4)(5)
A, dB, RIL	2-10 min.	2 min	(3)(4)(6)(7)
All other parts	10-30 min.	10 <b>-3</b> 0 sec	(3)(4)
(Assembly parts)			(3A)(4A)(5A)(6A)

Parts which are to be plated:

3. Parts are rinsed in cold water for at least one minute. Parts must be kept in motion during rinsing. Inlet faucet must be wide open. 4. Parts are rinsed in hot water for one minute with the inlet faucet wide open.

5. Parts to receive nickel plating operation can now be placed in the plating tank.

6. Parts to receive copper, silver or cadmium plating operation are placed in Solution #2 for one to ten minutes. Crocks used for sodium cyanide (Solution #2) will be labeled:

"Solution #2, C5-2E for RlJ only"

# and

"Solution #2, C5-2E" Parts which do not receive operation RlJ should not be placed in the procks designated "For RlJ only".

7. Parts to receive copper, silver or cadmium plating operations are placed in their respective plating tanks.

All other parts:

3A. Parts designated as "all other parts" (assembly parts in the table) are rinsed in Solution "3 for 15 seconds.
bA. Parts are rinsed in cold water for 15 seconds with inlet faucet wide open. Parts are shaken to remove excess water.
5A. Parts are rinsed twice in acetone. Discard the acetone when the specific gravity increases to 0.82. Specifice gravity should be measured with a lab hydrometer in the range desired.
óA. Parts are dried with compressed air.

# C6-3C

# CLEANING WITH SALTS

# (Sodium Cyanide)

PURPOSE

PURPOSE This method is used for	or removing sulfides from s	ilver and silver solder.	PURPC
acid. If acids come in acid, is formed. 2. Do not discard cya	nat containers of cyanide a n contact with cyanide, a d anide down the drain, pour se which will be sent to th	eadly g.s, hydrocyanic	SAFET
MATERIALS Bath Composition Solution #1 Sodium cyanide Deionized water Soluti	<u>Composition Ratio</u> l part l6 parts ion is used at room tempera	Chemical Grade 96% DuPont Co. 500,000 ohms or greater ture	MATER I Sol I
Solution #2 Acetic acid, glacial 99,5% Deionized water Deionized water	l part 19 parts	Reagent Grade 500,000 ohms or better 500,000 ohms or better	EQUIPM 1
Acetone <u>EQUIPMENT</u> 1. Tanks - Pla-Tank y PVC lined steel tanks	plastic crocks or eartherwa ss steel, monel or nichrome	re crocks can be used.	PROCEL 1 a 2 3
agitation is selected. 2. Parts are agitated 3. Parts are agitated faucet wide open. 4. Parts are agitated	bugh to allow free movement i in Solution #1 for at lea i in cold water for at leas i in solution #2 for 15 sec in cold water for 15 second	st 30 seconds. t 15 seconds with inlet onds.	i s <u>1</u> t: o:

5. Parts are rinsed with agitation in hot deionized water for 15 seconds with inlet faucet open.

7. Parts are rinsed in acetone for 15 seconds.

E. Parts are dried with compressed air.

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C6-3D

# CLEANING WITH SALTS

Sodium Cyanide

# PURPOSE

This method is used to neutralize parts prior to plating.

#### SAFETY

I. It is important that containers of cyanide are not located near any acid. If acids come in contact with cyanide, a deadly gas, hydrocyanic acid is formed.

2. Do not discard cyanide down the drain. Pour into steel barrel marked for that purpose.

#### MATERIALS

Bath Composition	Composition Ratio	Chemical Grade
Solution #1		
Sodium cyanide	l part	96% DuFont Co.
Deionized water	lé parts	500,000 ohms or
		greater
Igepol 630	1/1000 part	General Aniline and Film

Solution is used at room temperature

#### EQUIPMENT

1. Tanks - Pla-Tank plastic crocks or earthenware crocks can be used.

2. Baskets - Stainless steel, monel or nichrome baskets can be used.

# PROCEDURE

1. A basket large enough to allow free movement of parts for thorough agitation is selected.

2. Parts are immersed in Solution #1 for 1-40 minutes.

3. The parts can be transferred directly to a cyanide plate solution if there is no possibility of dripping onto the floor or into other solution. Otherwise, the parts must be rinsed in cold tap water. 4. When this operation is followed by a plating operation, parts are transported in a container of Solution #1 and must be allowed to dry or partially dry before being placed in the plating solution.



# DRY HYDROGEN FIRING

F2-1

# EQUIPMENT

1. Suitable hydrogen furnace

- 2. Thermocouple and meter
- 3. Optical pyrometer or equivalent
- 4. Sutiable firing boats

5. Rod to push boats through furnace and hooked rod to remove boats from cooler.

6. Clean white gloves to wear when handling fired parts.

7. Source of dry hydrogen - Dew Point - 60F to - 90F. Line hydrogen may be purified and dried by running it through a copper chip furnace (maintained at 650C) and an alumina dryer (maintained at 35F) or Catalytic Oxidizer, "Deoxo" purchasable from Baker Chemical Co., Philipsburg, New Jersey, or equivalent.

# PROCEDURE

Parts are loaded in the firing boats then pushed into the hot zone where they are fired at the specified temperature for the specified time.

# LIMITATION

The specified times and temperatures appear on the appropriate Standardizing Notice and in all cases indicate the period of time for which the parts are to be held in the heat zone. When cemperature only is specified parts are to be brought up to that temperature then pushed into the cooling section. A tolerance of  $\pm$  25C is allowed on all specified temperatures. All stated times are in minutes unless otherwise specified.

Parts are pushed into the cooler and then removed when cooled.

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# F2-2D/S1

# SPECIAL HYDROGEN FIRING

(Coated Ceramic Cylinders)

# PURPOSE

To issue instructions for firing coated ceramic cylinders used in metal-ceramic seals.

# EQUIPMENT

Hydrogen furnace, opening 6" high x 8" wide with dry hydrogen cooling chamber. Source of wet hydrogen Source of dry hydrogen with dew point of -60 to -90F. Molybdenum firing boats with covers  $12" \ge 6" \ge 5 \frac{1}{2"}$  high Molybdenum spacer sheets  $11 \frac{1}{2"} \ge 5 \frac{1}{2"} \ge .020" - .030"$  thick Fire brick, Babcock & Wilson #28

Note: Alundum chips (All) may be used in the bottom of the firing boat in place of the fire brick.

# PROCEDURE

1. Bottom of boat is lined with  $3/4^{\alpha}$  layer of fire brick and covered with a specer sheet. Cylinders are placed on sheet with the axis vertical, isolated from each other and from side of boat. (More layers may be built with spacer sheets between if cylinder lengths permit.) The boat is covered.

Note: For ceramic cylinders having wall thickness greater than 1/8" or for ceramics having large mass, all sides of boats should be lagged.

2. The filled boat is preheated for 15 minutes on the fore-hearth just inside the furnace door.

3. The boat is then heated for 45 minutes at 1300C in the hot zone. 4. The boat is pushed into the cooler and left to cool for 30 minutes. (H₂O temperature 120F.)

5. Cooling chamber door (between firing zone and cooling chamber) should be closed when firing or cooling because wet hydrogen is run in the box portion of the furnace while dry hydrogen is run into the cooling chamber.

# F2-LA

# FIRING IN WET HYDROGEN

# EQUIPMENT

1. Suitable furnace.

2. Wet hydrogen supply, having a dew point of 460 to 495F.

Wet hydrogen may be obtained by bubbling hydrogen through water just before it enters the furnace.

# PROCEDURE

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1. Parts are fired in wet hydrogen for specified time at specified temperature.

2. Parts are pushed into cooling chamber to cool to approximately 80C.

# F2-4G

# HYDRUGEN FIRING LETALIZED CLRAMICS

# PURPOSE

Hydrogen firing metalized ceramics serves six purposes:

- A. Creates positive bond between metalizing and ceramic
- B. Sinters metalizing to permit strong leak-tight seals.
- C. Removes metalizing binder by converting it to gaseous products.
- D. Causes oxidation in metalizing to insure maximum bond
- E. Degasses both ceramic and metalizing.
- F. Cleans up minor contamination on both ceramic and metalizing.

# MATERIALS

Ceramic insulators as specified on the drawing.

#### EQUIPMENT

A. Hydrogen furnace 6" x 8" wide opening, hydrogen atmosphere cooling chamber, or retort type furnace for larger pieces or high production runs. B. Source of wet nydrogen (preferably from passing dry line hydrogen through water bubbler).

C. City gas pilot line for pilot flame and flame curtains (hydrogen dew point -60 to -90F.).

D. Thermocouple and controller-recorder.

E. Seals Flo-Scope gauges for measuring hydrogen entering muffle

- and and cooler end of furnace.
- F. Molybdenum firing boats, 12" x 6" x 5 1/2" high
- G. Alundum chips, minus 20 mesh, Norton Co.
- H. Timer, electric or windup.

I. Rod to push boats through furnace with brackets to store rod in and keep it off the floor.

J. Asbestos gloves.

K. Hooked hol ow rod connected nitrogen line for flusning boats before bringing through flame cirtain.

# PROCEDUPE

Caution: At no time are ceramic parts to be handled or exposed to the building atmosphere. The audit check during metalizing, proper location of parts in boat after metalizing, careful transport of boat to and from furnace area, and the inspection which follows will result in entirely satisfactory audit of metalizing and firing.

A. All toats will be loaded and unloaded in the metalizing area by metalizing personnel. These boats will be of molybdenum with the bottoms lined with at least 1/2 inch of alundum chips. Each layer of parts to be fired will be supported above the previous layer with spacers. When the boat is properly loaded, the correct processing card should be added to it and then it should be hand carried to the furnace area for firing. PROCEDURE (CONT'D)

Note: Extreme care should be exercised in handling loaded boats since the metalized insulators tend to slide rather easily. This will cause sticking and subsequent rejection of parts.

B. Check that the furnace is at temperature as called for on the processing card.

C. See that the water level is to red line as marked on bubbler, and H2 is bubbling through it. If below line, add water. If above line, call foreman.

D. Preheat boat on fore-hearth just inside furnace door for time as specified on process card.

E. Move boat to hot zone of furnace for time specified on planning and processing ticket counting from time boat is first pushed into the hot zone.

F. Push boat into cooling chamber and leave there for time as specified. G. Purge hydrogen from boat with nitrogen and then pull boat through flame curtain.

H. Check off operation completed and initial process card.

DISPOSITION

After firing operation is completed, boats will be picked up by Metalizing personnel, carried to metallizing area, unloaded and reloaded with more parts.

# INSPECTION

Metalized ceramic parts are sorted as called for in Standing Instruction N3-23.

PROCESS CONTROL

A. See that all 'drogen entering hot zone is passed through bubbler and furnace flushed 20 min. with wet H2 before each firing shift begins. B. Hydrogen flow according to Selas Floscopes should be 75 cubic feet per hour to the hot zone and 50 cubic feet per hour to the cooler whenever parts are being fired. Lower flow rates will not maintain sufficient atmospheric control in furnace.

C. Use furnace, firing boats, and spacer plates for firing metalized ceramics exclusively. If used for other purposes, do not use them for firng ceramics again. This furnace must be free from iron and other metal contaminants before it will give good ceramic parts.

Boats are provided to be used exclusively for firing metalized ceramic insulators. These boats should not be used to sinter the copper or nickel plated insulators as boat contamination may result.

D. When new boats or spacer plates are to be put into use for firing ceramics, fire them at the regular ceramic firing cycle before using them with ceramic parts.

## PROCESS CONTROL (CONT'D)

E. Mark the position of the rod used for pushing boat into hot zone and come to this position each time a boat is moved to the hot zone. This will increase firing reproducibility. F. When converting from line hydrogen (-60 to-30F dew point) to wet hydrogen (through water bubbler) or vice versa, be sure furnace is purged for 20 minutes with 75 cubic feet per hour going to the bot

zone and 50 cubic feet per hour going to the cooler.

# TROUBLE SHOOTING

A. Air may enter the furnace in the following ways:

 While a boat is being removed from the cooler. Flame curtain at end of tube tends to minimize this.
 A leak in the furnace.
 Insufficient flushing or preheating of closed or covered

boats.

B. This air may make parts unusable as follows:

Free oxygen will cause scale on metal parts or bands.
 Air from a leak or admittance through cooling chamber

will cause a spectrum color on fired parts.

3. Internal explosion and part distortion or rupture if diffusion is restricted too much.

C. Remove covered boats from the cooling chamber with care as a combustibal mixture of hydrogen and air may form inside. This will be minimal if the boat is properly flushed with nitrogen.

D. Dust on boats fixtures or parts usually means sluff accumulations on the hearth. Cool furnace and clean hearth.

E. All parts must be covered with molybdenum trays. City gas used in the flame curtains has a tendency to leave soot and, or sulpher deposits. If parts are contaminated, it may be necessary to substitute hydrogen for city gas in the pilot flame lines.

F. Cooling chamber temperatures are important. Keep it high enough to avoid condensate accumulation along the floor of the cooler. Under a hot boat this condensate converts to steam which oxidizes work being cooled. Avoid this condition at all times.

G. If lack of reproducibility in seal strength is a problem, it may be the result of not using wet hydrogen for this firing or not purging enough before firing shift is started.

# MAINTENANCE

A, Cleaning - During normal operation, furnaces are bound to get crudded up one way or another. Scot and sulpher deposits will build up at both ends of the furnace due to the constant burning of city gas. Rust accumulates in the cooler sections tecause of the unavoidable sweating problem which crops up every once in a while. Boat lagging

23.

MAINTENANCE

A. Cleaning (Cont'd)

material covers the bottom of the furnace because boats have gaps or holes in them. If the furnaces are not cleaned on a periodic basis a serious degradation in parts' quality will result. Furnaces should be cleaned at least twice a year. The following procedure is recommended:

1. Shut furnace down as outlined in procedure under "starting and stopping".

2. Wire brush entire cooling chamber to remove all rust, scale, and dust.

3. Check all furnace doors for cracks and/or missing pieces. Rebuild or replace if necessary.

4. Check cooling chamber for water leaks. Patch and/or replace if necessary.

5. Check elements and all brick work. If brick work is badly cracked, and has the "ready to cave in" look, a major rebricking job is suggested.

6. Vacuum clean the entire interior of the furnace.

B. Calibrating - Furnace controls must be calibrated periodically to insure the validity of their readings. All work of this type must be handled by the electrical service group. An accurate millivolt source is hooked to the input terminals of the recorder and a set procedure is followed to insure reproducibility of results. There is no need to check thermocouples or thermopiles since they are accurate until they short out. At that time, the indicator will climb past the limit point and the furnace will be shut off automatically. The recorders will be calibrated every second menth with the calibrated millivelt source. The person doing this will then label the furnace with date calibration was completed and his initials. Also, every sixth month a traveling thermocouple will be run through the furnace with resulting readings being checked against the furnace controls. This should be done after shut down periods and before parts are started through the furnace again.

Note: The electrical service group is responsible for the accuracy of the furnaces. It is important that they be notified whenever a furnace controller seems to be acting up. No controls should be tampered with by anyone except people from this electrical service group.

- C. Starting and stopping
  - 1. Ignition of eight inch hydrogen box furnaces.

# C. Starting and stopping (Cont'd)

a. Close end doors of furnace and open cooler door. b. Purge furnace for two hours with nitrogen. Use a flow of 100 cfh. on each hydrogen flow scope. c. Turn power switch from off to instrument. d. After two hours of nitrogen purging, light pilot lights. Check flame curtains. Open water valve to cooler and close off the water bypass. e. Increase nitrogen flow for five minutes to a reading of 200 cfh. on each hydrogen flow scope. f. Simultaneously, introduce hydrogen and shut off nitrogen to the furnace. Regulate to 75 cfh. of hydrogen in the hot box and to 50 cfh. of hydrogen in the cooler. g. Purge with hydrogen for one hour. h. After one hour close the cooler door. i. Turn power switch from instrument to heat. Reactrol unit should be reading approximately 80. j. Bring furnace to desired temperature in intermediate steps. That is, hold heat constant at various stages to allow brickwork to reach thermal equilibrium.

2. Idling of eight inch hydrogen box furnaces.

- a. Open cooler door.
- b. Decrease flow of hydrogen to 35 cfh. in the cooler section.
- c. Turn off all hydrogen Leading into the hot box. Maintain
- 35 cfh. in cooler section.
- d. Bring temperature down to 900C or 1000C.

3. To prepare for operation

- a. Increase flow of hydrogen to 50 cfh. in the cooler.
- b. Flow 75 cfh. of hydrogen in the hot box.
- c. Close the cooler door.
- d. Adjust to desired temperature.

4. Shutting down of eight inch hydrogen box furnaces.

- a. Turn power switch from heat to instrument.
- b. Open cooler water bypass. Regulate water flow until it
- is coming out warm.
- c. Open cooler door.
- d. Allow temperature to drop below LOOC.
- e. Simultaneously, open up nitrogen and turn off the hydrogen.
- Regulate nitrogen flow to 200 cfh. on each hydrogen flowscope.
- f. When hydrogen is no longer burning off at either end of

the furnace, shut off nitrogen and allow the furnace to go to air.

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# 4. Shutting down of eight inch hydrogen box furnaces (Cont'd)

- 28 -

- g. Turn off pilot lights.h. Open both end doors.

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#### F3-1P

# AIR FIRING CERAMICS

#### PURPOSE

The purpose of air firing ceramics is threefold:

A. To oxidize all organic and carbonaceous materials and convert them to gaseous products which go off into the furnace atmosphere.

B. To drive undesirable volatiles out of the body of the ceramic and replace them with air gases which can be removed relatively easily at exhaust without altering crystal phases.C. To oxidize any iron deposits and show them as stains or color variations in the piece.

This instruction, therefore, is written to provide a means of accomplishing these purposes on ceramic materials.

#### MATERIALS

Ceramic parts as specified on the drawing.

#### EQUIPMENT

Suitable summel kil capable of reaching 11000 Silicon carbide saggers Portable indicator with thermocouple leads.

#### PROCEDURE

A. Parts come to furnace loaded in carbide saggers covered with mullite lids.

B. Parts are fired in a tunnel kil with air forced through furnace against the movement of the ceramics. The parts are 7 hours up to maximum temperature and 7 hours of cooling down from maximum temperature. Maximum temperature is 1100C.

# DISPOSITION

Send boats to next station on processing ticket, still covered (usually inspection).

# INSPECTION

After the boat has cooled to room temperature, lift the cover vertically without tilting or moving it away from covering area over the parts. Give the parts a cursory visual examination for obvious spots, cracks, chips, areas of discoloration or contamination without touching or removing the fired parts. If no defects are observed, replace the cover and send the boat to the next planned station. If defects are noted, call foreman. PROCESS CONTROL

A. The furnace used for firing ceramics shall not be used for firing any other materials at any time.

B. Use boats for firing ceramics only. Firing other parts in them only leads to contamination of several batches of ceramics.

TROUBLE SHOOTING

A. If parts show spots, it indicates:

1. The boats are contaminated with something that is being transferred to the parts during firing.

2. Parts were not clean when placed in boats after acetone wash.

3. The oven is contaminated with something which is dropping or being splashed on parts during firing.

4. Something near the surface of the ceramic body is being converted to a colored product by air firing (such as iron deposits from the die used in making the part).

B. Larger discolorations on the parts indicates:

- 1. Contaminated furnace.
- 2. Contaminated parts.
- 3. Non-uniform milling lot at vendors plant.
- 4. Diffused iron deposits left on parts by vendor's processing.

C. Parts coming from the furnace cracked, chipped or broken show:

- 1. Incipient cracks in the part as received from the vendor.
- 2. Incipient cracks from rough handling in our plant.
- 3. Thermal shock oven temperature too high when parts placed
- in oven or removed from oven.

D. Air firing was first started to oxidize the iron left by vendor and show it up as discoloration areas in the part. Since the problem has been largely corrected, the firing has been continued to insure against falling into the same trouble again. Occasionally one or two are found in a lot of 100 or more pieces.

E. Conical recrystallization is a condition which vendors have not yet found means of controlling. It is, however, strictly their problem.

#### MAINTENANCE

A. Check the furnace temperature at the beginning of each shift as the first job is run in the furnace.

# Procedure

1. Set furnace at 1000C (corrected to latest controller calibration factor' and record setting in log book.

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MAINTENANCE (CONT'D)

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# Procedure

2. When the furnace has reached equilibrium temperature, insert the thermocouple leads from a portable indicator.

3. When this has reached equilibrium, record in a log book the extremes of the temperature cycle against the furnace number, setting and the date.

4. If extreme readings are between 9850 and 10150 continue firing.

5. If extreme readings are not within 985C to 1015C, stop firing and notify foreman.

B. Calibrate both portable indicator and controller-indicators according to the controller-indicator calibration schedule and tabulate the calibration correction factory and dete of calibration on a tag attached to the instrument and in a book kept in the furnace area.

C. Whenever a firing of some lot of ceramics in these furnaces causes large volumes of volatiles to pour out of the over (high boiling solvent, body contaminants, etc.) remove it from service until the furnace can be thoroughly cleaned by firing empty furnace at 1100C for 1/2 hr. before it is used again at 1000C for ceramics. Bo this once in 3 months as regular practice to insure no buildup of contamination.

# SILK SCREEN COATING (Silk Screen Metalizing Machine)

# PURPOSE

To butt or end coat ceramic insulators with a uniform, smooth, controllable layer of metalizing mix.

# MATERIALS AND EQUIPMENT

- 1. Jig or fixture to hold insulators stationary at some fixed height.
- 2. Jig or fixture to hold screen taunt and in a fixed position.
- 3. Stainless steel mesh screen of proper mesh size and wire diameter.
- L. Teflon tipped squeegee to spread paint evenly on the screen and also to force the paint through the screen and to the insulators.
- 5. Properly adjusted moly-manganese mix.

6. Small oven to dry coating after being applied to the insulator.

- 7. Holybdenum trays to load parts on for drying and firing.
- 8. Two 100 ml beakers, one for the mix and the other for acetone or other cleaning solvent.

9. Cotton swabs for touch up cleaning on ceramic insulators.

- 10. Pliers for setting the moly trays into the drying oven and also for pulling them out.
- 11. Two sided tape for holding insulators down and in a fixed position.

#### PROCEDURE - SETUP

1. Place a clean piece of two sided tape down on the parts holding fixture.

2. Lay five (5) parts to be coated on the tape in the following pattern.

3. Lay the .040" shim stock across three of the insulators. 4. Lay a flat surfaced object on the shim stock and across two of the micro-adjustment nuts.

une micro-aujusument nuts.

Adjust each nut until it just barely touches the flat surface.
 Lay the flat surfaced object across the other two adjustment nuts

and on the shim stock.

7. Repeat Step 5.

8. Set the stainless steel screen supported by the screen fixture into proper position. The two pins in the parts fixture should come through the screen fixture and the bottom of the screen fixture should rest on top of all four micro-adjustment muts.

9. Check the screen fixture for wobble and make necessary adjustments.
10. Place proper number of ceramic insulators to be coated on the sticky tape. The only criteria for loading is that no part should touch any other part.

#### PROCTOURE - SETUP CONTID

11. Pour erough mix on the screen to allow coverage of the entire area.

12. With the teflon tipped squeegee wipe the paint into the screen using firm but not hard pressure. Continually turn the screen over so that all the screen holes are filled with mix. The last wipe should be made on the bottom side of the screen.

13. Place the screen fixture on the parts jig and make one pass with the squeegee.

14. Remove screen, examine parts, and made adjustments where necessary.

## PROCEDURE - PRODUCTION

1. Flace proper number of ceramic insulators on the parts fixture. 2. Put the screen fixture in place and draw the squeegee across the screen.

3. Remove the screen fixture, add paint to the screen if necessary, and work the paint into the screen until all meshes are filled with mix.

4. Take the coated insulators from the fixture with tweezers and load them on the molybdenum trays.

5. Place loaded tray in the drying oven for approximately 15 minutes.

# PROCESS CONTROL

1. Use nothing but properly adjusted screen mix.

2. Do not place excess coating on the screen. It will tend to run on the fixture and eventually on the operator and the insulators. 3. Do not leave the mix lying on the screen for long periods of time. The vehicles and binders will separate from the metallic particles and an inhomogeneous mix will result. The screen should be clean of all mix at lunch break and again at the end of a shift. 4. The teflon on the end of the squeeree will tend to wear over a period of time. Then the insulators on the outermost rows are not coating the teflon should be squared off.

#### TROUBLESHOOTING

- 1. Mix not adhering to the ceramic insulator
  - e. Finder has not been added to the mix.

b The oven is too hot and the bunder is coung curnul off

- 2. mitty particles in the mix.
  - a. We colling time who had sufficient to tale all
     b.e. functe M5 into collition.
     b.e. call allow cycle was not correct clarticles
  - of metal have not been reduced in size.
- Mix is not working properly into the screen.
   a. The mix is too thick. Theck viscosity and add Butyl Carbitel Acetate if necessary.



TROUPLESHOOTING CONTID

- li. Mix running on the sides of the parts.
  a. Temperature of the room is too high.
  b. Viscosity of the mix is too low. Discard
  - and start using from a new bottle.

# Jl-lP

# SPRAYING CATHODES (Emission Coating)

# PURPOSE

To provide instructions for applying a uniform coating to the entire cathode surface of cathode and insulator assemblies.

# MATERIALS

1. Cathode assemblies per drawing list.

- 2. Triple carbonate suspension specified on drawing list.
- 3. Acetone

# EQUIPMENT

1. Vented spray booth with spraying disc, motor and other fixtures mounted.

- 2. Paasche spray gun.
- 3. Binocular microscope with light.
- 4. Spraving fixtures.
- 5. Post grinder with carboloy cutter,
- 6. Dial gauge.
- 7. Tweezers
- 8. Cathode dummies
- 9. Precison scales

# PROCEDURE

1. The assemblies are ready for use as received from the previous ultrasonic cleaning operation.

2. The assemblies are placed in the spraying fixtures face down and carefully centered so the cathode is in the hole in the face of the fixture. The back is then screwed on.

3. The magnetic fixtures are arranged around the circumference of the spraying disc. Two cathode dummies are included with each load to check spray density.

4. Cathedes are sprayed until .0025" to .0035" of coating has been deposited. If uncertain of spray gun setting, a run containing only dummies should be performed and coating density and height checked. 5. Cathode dummies are removed and checked for spray coating thickness. These must be within specified limits.

6. Cathode assemblies are removed from spraying fixtures and placed in trays.

7. Cathode assembly is grasped by back of ceramic with tweezers and run through track of post grinder, applying light pressure against the cutter. The coating thickness is gauged. If within the drawing tolerance the part is placed in a tray, coating side up for future inspection. If coating is too thick, the part is run through the cutter and regauged, if too thin either the cutter is not properly PROCEDURE (CONT'D)

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adjusted or one of the braze joints on the cathode assembly has come loose. Each assembly must be gauged.

C. The cathode assembly is inspected under microscope for proper coverage of coating, chipped edges, gauges, tilts, etc.

coverage of coating, chipped edges, gauges, tilts, etc. 9. After spraying is completed, the jar of coating is removed and a beaker is filled with acetone and the gun is thoroughly flushed out.

# RIA/SCR3

# COPPER STILL PLATING

(Pasket)

# PUE.PUTE

To provide an adherent copper flash on small nickel tubing and wire leads (less than 1/16" diameter x 1" long) for brazing purposes.

# MATERIALS

Material New Bath Content Control Limits 5-6 oz/gal Copper Cyanide 902 oz Sodium cvanide 1320 02 1.5-2.0 oz/gal (Free) 2.0-610 oz/gal 328 02 Sodium carbonate pH 12-13 Sodium hydroxide 246 oz 4-10% (volume) "Rocheltex" Deionized water to make up to 164 gallons 500,000 ohms or greater Operating temperature 140-160 F Anode to cathode area = 1:1 Adjust as required to maintain copper cyanide content) Current density - See Plating Process Cards EQUIPMENT 1. Plating Tank - Plastisol or Koroseal lined steel 24" x 24" x 72" working volume 164 gallons equipped with steam heating coil and indicating automatic temperature control, 2. ectifiers - separate unit for each of four positions 50 amp. 10 v. 3. Stainless steel anodes - size and number as required. 4. Pinse Tarks - stainless steel 5. Paskets - stanless, approximately (" x (" dia. 6. Filter - immersion type with impeller pump. 7. "abor Exhaust Venting System.

# MAINTENANCE

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1. Maintain solution at working volume - at determined point approximately  $3 \frac{1}{2}$  inches below top of tank by addition of deionized water as required.

2. Anode Maintenance - Proper copper ion content of plating bath will be maintained by use of one copper anode and two stainless anodes on each of two anode bars. Adjustment in anodes will be required as copper anodes errode and are reduced in area. Adjust to maintain approximately the initial balance between area of copper and stainless anodes.

3. Anode Area - Maintain 4 on each of 2 bars. Copper 1" x 4" x 15".

# PROCEDURE

1.	Parts are placed in nickel mesh basket.
2.	Parts are cleaned thoroughly before plating.
3.	Parts are copper flashed at about 3v for 2 to 3 minutes with
agi	tation of parts to prevent sticking together. (Negative
con	tact is made directly to the basket by means of a wire-clip
com	bination.)
4.	Parts are rinsed thoroughly in cold running water, 10 sec.
5.	Parts are rinsed in hot running water, 10 sec.
6.	Parts are rinsed in acetone for 10 sec. and drained.

7. Parts are blown dry with carefully directed compressed air.

# INSPECTION

All parts should be covered with copper plating.

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# R1.:/S1

# NICKEL PLATING

(Barrel)

# PURPOSE

To provide an adherent nickel plate to tube parts. Stainless steel, tungsten and molybdenum is struck with nickel from nickel strike, bath to provide a surface for further plating because other plates do not adhere to these metals.
 Plating is to be uniform, unstained, unblistered and of the

specified thickness.

# MATERIALS

# 1. Strike Bath

Bath Composition	Chemical Grade	New Bath Content Tith Solution Level <u>3" Below Top Of Tank</u>	Control Limits
Nickel Chloride Hydrochloric Acid Deionized Water to make up volume	Udylite Corp.	26,100 g 13,750 cc	220-260 g/l 100-150 cc/l 500,000 ohms or greater

Temperature - Room

2. Plate Bath

Bath Composition	Chemical Grade	New Bath Content With Solution Le <u>3" Below Top Of</u>	evel Control	
Nickel Sulfate (22.1) Ammonium Chloride Boric Acid Deionized Water to make up volume pH	₹ Ni) Udylite Corp	13,200 g 2,800 g 3,300 g	135-155 g/l 20-30 g/l 25-35 g/l 500,000 ohms or greater 5.4-6.0	5

Temperature - Room

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# EQUIPMENT

l. Tank

Construction Material	Capacity At Solution Level 3" Below Top Of Tank	Overall Dimension (inches)	
Koroseal Lined Steel	llO liter	22 x 24 x 16 deep	
Koroseal Lined Steel	llO liter	22 x 24 x 16 deep	

2. Barrels

Belke-Porto Plater with 3/4 inch diameter slug contact for nickel plating = 2 quarts.

# MAINTENANCE

1. Sclution Level - Maintain level at  $\pm 1/2$  inches below the top of the tank. A marker is located on each tank to indicate the 3 inch level.

2. Filtering Plating Solution - To determine the cleanliness of a solution, fill a bottle with the solution and observe the solution by holding it up to the light.

3. Anode Area - Maintain anode areas as follows:

Type Of Plate	Size Of Anode (inches)	Anode Metal	Chemical Grade	No. Of Anodes
Nickel Strike	1/4 x 5 x 8	Nickel	99+% Chemical Co.	4 on each of 2 bars
Nickel Strike	1/2 x 5 x 8	Nickel	Rolled Depolarized or cast in carbon	4 on each of 2 bars

4. Parrel Maintenance -

a. Deplate cathode chain contacts used in the Belke-Porte Platers once a day.

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b. Use Belke-Porto Platers for all nickel deplating.

# PROCEDUPE

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1. The number of parts to be plated in barrel are weighed out. 2. Parts are cleaned thoroughly before plating. Only parts which are uniformly clean looking should be plated. Send back any parts having dirt stains or nonuniform appearance because dirty parts are likely to blister when heated later.

# PROCEDURE (CONT'D)

3. Parts are poured gently from cleaning basket to the barrel. 4. Parts to be struck as specified in striking table, are immersed in barrel in striking tank. For all the other parts, omit Steps 4, 5, and 6. 5. Strike parts according to time and current specified in table. Make sure the barrel is rotating and the filter pump is operating during striking. 6. Barrel is lifted out of strike solution while still rotating and allowed to rotate with one end resting on the drain board for four revolutions to drain strike solution out of the parts. 7. Barrel is transferred to plating tank. 8. Plate according to the number of parts per barrel, current and time specified in the table. Make sure the barrel is rotating and the filter is operating during plating. 9. Barrel is lifted out of plating solution while still rotating and allowed to rotate with one end resting on drain board for four revolutions to drain plating solution out of parts. 10. Barrel with parts still rotating, is placed into cold water rinse and barrel is allowed to rotate for one minute. Barrel is lifted out of cold water rinse while still rotating and allowed to rotate with one end resting on drain board for four revolutions to drain cold water out of parts. (See note.) 11. Barrel, with parts still rotating is placed into hot water rinse and barrel is allowed to rotate for one minute. Barrel is lifted out of hot water rinse while rotating and allowed to rotate with one end resting on drain board for four revolutions to drain hot water out of parts, Electric plug is pulled out to stop barrel rotating. 12. Barrel is carried to hot water rinse next to Kreider dryer. Barrel of parts is dumped through funnel cover into drying basket submerged in running hot water. 13. Drying basket, with parts is lifted out of hot water and into

Kreider spin dryer. Parts are spun until dry which usually takes about two minutes with steam heated hot air.

Rinsing and drying must be done carefully and equipment kept in top condition or stains will appear on plated parts causing rejection of tubes composed of stained parts.

Note: if subsequent operation is *(6-3D, it must start immediately after this rinse. Parts must not be permitted to dry or partially dry between trese operations.

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#### RLE/SCR-1

#### COPPER BARREL PLATING

#### PURPOSE

1. To provide an adherent copper plating to assemblies and type parts.

2. Plate is to be uniform unstained, unblistered, and of specified thickness.

#### SAFETY

Plating Bath - observe safe handling procedures required in working with hot strongly alkaline cyanide solutions. Do not mix with acid or expose to acid fumes. Venting - Vent bath vapors into vapor exhaust system. Acetone - Observe safe handling procedure required for volatile and flammable solvent.

#### EQUIPMENT

 Plating Tank - Plastisol or Koroseal lined steel 24" x 24" x 72" working volume 164 gallons equipped with steam heating coil and indicating automatic temperature control.
 Plating Barrels - Daniels' 8H Plastic.
 Barrel Rotating Drive - Motor/reduction gear driving common shaft providing rotating drive for four barrel positions.
 Rectfiers - separate unit for each of four positions 50 amp., 10V.
 Stainless steel anodes - size and number as required.
 Contact medium - metal pins or copper-clad plastic balls.
 Baskets - stainless, approximately 8" x 8" dia.
 Filter - immersion type with impeller pump.

10. Vapor Exhaust Venting System.

MATERIALS

Copper cyanide, 70 - 715 copper	Kr02075
Sodium cyanide, 96%	KR0107
Sodium carbonate	K:01429
Sodium hydroxide	KEOIL32
"Rocheltex" (brightener)	KRO1414
Copper anodes, CFHC	KTQ3372
Acetone	KE04358

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#### BATH COMPOSITION

Control Limits "ew Bath Content Material Copper cyanide 902 oz. 5-6 02/2al 1.5-2. oz/gal (Free) Socium cyanide 1320 cz. Sodium cerbonate 328 oz. 2.0-6.0 oz/gal Sodium nydrox/de 246 oz. pH 12-13 6-10% (volume) "Rocheltex" Deionized water to make up to 164 gallons 500,000 ohms or greater

Operating temperature 140-160 F.

Anode to cathode area = 1:1(adjust az required to maintain copper cyanide content)

Current density - see Plating Process Cards

#### MAINTFNANCE

1. Solution level - maintain level 2 - 2 1/2 inches below top of plating tank by addition of deionized water as required. 2. Bath composition control - The maintenance of proper balance between area of copper and stainless anodes will assist in holding copper cyanide bath content within limits.

#### PROCEDURE

1. The specified number of precleaned parts are placed into the plating barrel, containing the specified type and quanity of contact medium.

2. The loaded plating barrel is inserted into one of the four plating positions provided at the plating tank - insert with barrel rotating drive running.

3. Immediately turn switch of rectifier serving the position being loaded to "ON". Adjust rectifier control to specified plating current. u. Plate as specified - time and current.

5. Turn rectifier switch to "CFF".6. Immediately raise plating barrel to position above solution level. Drain excess solution from parts.

. Transfer loaded barrel to cold running r_nse water tank. Immerse barrel until water covers plated parts. Tumble rinse by rotating barrel 10 - 15 seconds.

8. Drain to remove excess rinse water. Transfer plated parts to stainless steel basket. Rinse in cold running water with agitation 10 - 15 seconds.

#### PROCEDURE (CONT'D)

9. Rinse in cold flowing deionized water 10 - 15 seconds.

10. Rinse in hot flowing deionized water 10 - 15 seconds.

11. Rinse in hot flowing deionized water 10 - 15 seconds. (Repeat Step 10 but in second tank or tank section).

12. Rinse in cold flowing deionized water 10 - 15 seconds.

13. Parts that are to receive further plating application are carried into the next plating procedure or pretreatment without drying.
14. Parts not to be immediately transferred to another plating operation are rinsed in acetone 10 - 15 seconds, dried, and placed in storage or transport containers, omitting cold deionized rinse of Step #12.

#### PROCESS SCHEDULES AND INSTRUCTIONS

1. See Parts Process Cards for specified precleaning and preprocessing schedule.

2. See Plating Process Cards for specified number of parts per barrel load, type and quantity of plating contact medium, plating current, plating time, and plating thickness.

3. See Tumbling Process Card for specified tumbling procedure where tumbling is called for by Parts Process Card.

#### S-RIE/3

#### COPPER, BARREL PLATING

#### PURPOSE

1. To provide an adherent copper plating to tube assemblies.

2. Plating is to be semibright, unstained, free of blisters and

of specified thickness.

#### SAFETY

Plating Bath - Observe safe handling procedures required in working with hot strongly alkaline cyanide solutions. Do not mix with acid or expose to acid fumes,

Venting - Vent bath vapors into Vapor Exhaust System

#### EQUIPMENT

1. Plating Tank - Plastisol or Koroseal lined steel, 24" x 24" x 16", working volume 36 gallons, equipped with steam herting coil and automatic temperature control.

- 2. Plating Barrel Daniels SH Plastic
- 3. Rectifier 50 amp. 12V
- L. Baskets stainless, approximately 8" x 8" dia.
- 5. Finse Tanks stainless
- 6. Filter immersion type with impeller pump.
- 7. Contact Medium metal pins.
- 8. Stainless steel Anodes 1/8" x 2" x 11 1/2"
- 9. Vapor Exhaust Venting System

#### MATERIALS

Copper Cyanide, 70 - 71% copper	KR02075
Potassium cyanide, 98%	KR0479
Potassium carbonate, Reagent, Anhydrous	KR0478
Potassium hydroxide, Reagent	KR0480
"Rocheltex" (brightener)	KR01414
Copper Anodes, OFHC, 1 1/2" x 5" x 9"	KR03372

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#### BATH COMPOSITION

Material	New Bath Content	Control Limits
Copper cyanide Potassium cyanide Potassium carbonate Potassium hydroxide "Rocheltex" Deionized water to m	286 oz. 464 oz. 72 oz. 200 oz. ake up to 34 gal.	7.2-8.8 oz/gal 0.8-1.2 oz/gal (Free) 6 oz/gal max. Ph 13 or greater 8-10% (volume) 500,000 ohms or greater
Operating Temperatur	e 1∞-170 F.	or Precedi

Anode to cathode area = 2:1

Current density - See Plating Process Card

#### MAINTENANCE

1. Maintain solution at working volume - at determined point approximately  $2 - 2 \frac{1}{2}$  inches below top of tank by addition of deionized water as required.

2. Anode Maintenance - proper copper ion content of plating bath will be maintained by use of one copper anode and two stainless anodes on each of two anode bars. Adjustment in anodes will be required as copper anodes errode and are reduced in area. Adjust to maintain approximately the initial balance between area of copper and stainless anodes.

#### PROCEDURE

1. The specified number of precleaned tube assemblies or parts are transferred into the plating barrel.

2. Plating barrel is inserted into plating tank with barrel rotating drive on and the bath at operating temperature.

3. Rectifier is immediately turned on and set to specified plating current. After initial adjustment duplicate carrel loads may be inserted with the current on followed by slight current adjustment as required. Hold immersion time with current off to a minimum.

4. Flate as specified - current and time.

5. Raise plating barrel to position above solution level. Drain excess solution from parts.

6. Transfer barrel to cold running water rinse tank. Immerse barrel until rinse water covers plated parts. Tumble rinse by rotating barrel 10 - 15 sec.

7. Drain to remove excess rinse water. Transfer parts to stainless basket, Rinse in cold running water with agitation.

#### PROCEDURE (CONTID)

- 8. Rinse parts in cold flowing deionized water 10-15 sec. with agitation.
- 9. Rinse in hot flowing deionized water 10 sec.
- 10. Repeat Step 9 in a second hot rinse tank section.
- 11. Rinse in cold flowing deionized water 10 sec.
- 12. Tubes to be nickel plated are transferred to that operation without drying.
- 13. Parts not to be immediately transferred to another plating operation are dried and placed in storage or transport containers, omitting the cold deionized rinse of Step #11.

#### PROCESS SCHEDULES AND INSTRUCTIONS

1. See Parts Process Cards for specified precleaning and preprocessing schedule.

2. See Plating Process Cards for specified number of parts per barrel load, plating current, plating time and plating thickness.

3. See Tumbling Process Cards for specified tumbling procedure where tumbling is called for by Parts Processing Card.

#### LIMITATION

The time of rinsing in hot water in Steps 9 and 10 is reduced to 10 seconds to prevent oxidization of copper plating prior to nickel plating.

#### GOLD, BARREL PLATING

#### PURPOSE

To provide an adherent gold plate to tube assemblies and parts.
 Plating is to be yellow in color, unblistered and of specified thickness.

#### SAFETY

Plating Bath - Observe safe handling procedure required in working with hot alkaline cyanide solutions. Do not mix with acid or expose to acid fumes. Keep ammonium hydroxide and ammonium salts away from gold drag-out rinses, gold plating and deplating solutions to insure against the formation of EXPLOSIVE gold fulminate. Acetone - Observe safe handling procedure required for volatile and flammable solvent. Venting - vent bath vapor into Vapor Exhaust System.

### EQUIPMENT

1. Plating Tank, stainless steel - type 304, 40 gallon capacity, 24" x 18" x 24" deep set in water bath tank 31" x 24" x 30" equipped with an 8 pass 3/4" steam coil - bottom mounted, automatic indicating thermostatic temperature control. 2. Power Supply: Rectifier - stepless voltage control, 50 amp. 9V. capacity, equipped with an amperehour meter of 100 amp. capacity. 1/4 scale with totalizing dial. 3. Plating Barrel - Daniels' 8H Plastic - entire bottom fitted with 2 nickel plate as cathode. 4. Drag-out Tank - Plastisol or Koroseal lined steel. 5. Rinse tanks - stainless steel 6. Rinse baskets - stainless steel 7. Anodes - stainless, 18 - 8 grade. 8. Filter - immersion type with impeller pump. 9. Warm Air Drying Unit - Open rectangular tank, approximately 24" x 48" x 24" deep, air input into end supplied with steam heat coil, air filter and fan for clean flowing warm air drying.

#### MATERIALS

Gold Potassium Cyanide Solution	
Technic Trushade, 24 kt. (50ml = 1 dwt)	KROLLO
Potassium Cyanide, 98%	KR0479

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#### MATERIALS (CONT 'P)

Potassium phosphate, dibasic, Reagent	
(Dipotassium phosphate)	KR01181
Potassium carbonate, Reagent	KR0478
Acetone	KR04358

#### BATH COMPOSITION

Material	New Bath Content	Control Limits
Gold cyanide solution Potassium cyanide Potassium piosphate	17,000 ::1 160 - 7	8-9 dwt/cal 3- oc/gai cree)
(Dibasic)	160 oz	3
Potassium carbonate	16) oz	4-15 oz/gal
Deionized water to mak	e up to hO gallons	500,000 ohms or greater

Operating temperature 145-155 F.

Anode to cathode area = 1:1

#### MAINTENANCE

1. Solution level - maintain working of the plating bath 3 1/2 inches below top of plating tank by transferring solution from the drag-out rinse tank as required. Use deionized water for make up of drag-out rinse volume. Maintain fluid level in water bath plating tank jacket as required.

2. Maintain plating bath gold content by additions of Trushade gold concentrate solution based on ampere hours indicated on meter, confirming gold content by gravimetric analysis performed at intervals of one week. At the lower current densities with cathode efficiency at 70%, the replenishment would be 17 dwt. (850 ml Trushade gold concentrate solution) for each 5 ampere hours (20 meter untis) of plating. Five ampere hours of lating will reduce the gold content of a LO gallon bath from .5 dwt/gal. (midpoint of operating range) to  $\delta.07 \, dwt/gal$ .

#### PROCEDUPE

 Place specified number of precleaned parts into plating barrel barrel will have been preloaded where gold strike procedure SI 13700 RLP/1 is specified to precede this plating operation.
 Turn rectifier switch to "on" position and set voltage control to approximate first step position. Turn barrel rotating drive on.
 Insert loaded plating barrel into plating tank, contacting (with current on) the cathode contact in a minimum time. **PROCEDURE** (CONT'E)

4. Immediately adjust voltage control for specified plating current.

5. Plate as specified - time and current schedule.

6. Turn rectifier switch to "off" position.

7. Raise plating barrel to drain position and drain of excess solution.

8. Transfer loaded plating barrel to drag-out rinse tank and tumble rinse for 10 - 15 sec. Drain excess solution into drag-out rinse tank.

9. Transfer parts to stainless steel basket.

10. Rinse in cold deionized water for 15 - 30 sec.

11. Rinse in hot deionized water for 15 - 30 sec.

12. Rinse in hot deionized water for 15 - 30 sec.

13. Rinse in acetone for 10 - 15 sec.

14. Drain thoroughly and dry in warm air.

15. Remove from basket to storage and transport containers or to next process.

#### PROCESS SCHEDULES AND INSTRUCTIONS

See Parts Process Cards for precleaning and preprocessing schedules for additional processing.

See Plating Process Cards for specified number of parts per barrel load, plating current, plating time, and plating thickness.

See Tumbling Process Cards where tumbling procedures are called for in Parts Processing Cards.

#### LIMITATIONS

This gold plating bath is not designed to produce a bright plate deposit. Burnishing may follow plating where a bright finish is required as an external final finish on completed tube assemblies.

All rinsing is in flowing deionized water with agitation, except for drag-out and final acetone rinse.

#### R1P/1

#### GOLD STRIKE BARREL PLATING

#### PURPOSE

To provide an adherent gold strike plate on a nickel plated substrate upon which a heavier deposit of gold may be plated in a convential gold plating bath.

#### SAFETY

Plating Bath - observe safe handling procedures required in working with hot strongly alkaline cyanide solutions. Do not mix with acid or expose to acid fumes.

Vent vapors into vapor exhaust system. Large volumes of hydrogen are liberated at the cathode during plating with this bath; therefore, the vapor and spray produced must be vented into an exhaust system.

#### EQUIPMENT

1. Plating tank - Plastisol or Koroseal lined steel  $2\mu$ " x  $2\mu$ " x 16" having a working volume of 36 gallons, equipped with a stainless steel heating coil and automatic temperature control.

2. Plating barrel - Daniels' 8H Plastic equipped with a solid nickel plate covering entire bottom as cathode.

3. Anodes - stainless steel, size and number as required to provide an anode equal to the cathode area. Equal anode area provided for each of 2 anode bars.

- 4. Rinse tanks stainless steel
- 5. Rectifier 50 amp., 12v
- 6. Filter immersion type with impeller pump.
- 7. Vapor Exhaust Venting System.

#### MATERIALS

1.	Gold concentrate solution, technic	
	24 kt. industrial (20 ml = 1 dwt)	KR01177
2.	Potassium cyanide, 98%	KR0479
3.	Potassium phosphate dibasic, Heagent	
	(Dipotassium phosphate	KR01181

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#### BATH COMPOSITION

Material	New Bath Content	Control Ligits
Gold Concentrate Solution	720 ml	85-1.15 dwt/gal.
Potassium cyanide	234 oz.	4.3-6.5 oz/gal. (Free)
Potassium Phosphate		-
(Dibasic)	112 oz.	2.1-3.1 oz/gal
Potassium Carbonate	None	15oz/gal. max.
Deionized water to make up to	5 36 gal.	500,000 onms resistance
•		or greater
Operating Temperature 112-11	18 F.	-
Anode to Cathode area = 1:1		

Current density - See Plating Process Card

#### MAINTENANCE

1. Maintain solution at working volume - at determined point approximately  $2-2 \frac{1}{2}$  below top of tank by addition of deionized water as required.

#### PROCEDURE

The specified number of parts to be plated are placed into the plastic plating barrel. Parts shall have been pretreated to insure that they are clean and free of any acid residues.
 The loaded plating barrel is inserted into the plating tank with the barrel rotating drive running and the bath at operating temperature.
 The rectifier is immediately turned on and set to the specified plating current.
 Plate as specified - current and time.
 At the end of the plating cycle lift the plating barrel to the drain position and drain excess solution from parts.
 Immediately transfer loaded plating barrel to cyanide gold plating bath (RIP) without intermediate rinse.

#### PROCESS SCHEDULES AND INSTRUCTIONS

 See Parts Process Card for specified precleaning, plating and rinsing schedules.
 See Plating Process Card for specified number of parts per barrel

load, current density and time schedule.

#### LEGITATION

This hold: trike bath JP/1 composition is compatible with the bath composition of Syanice Gold Taking ath MP; therefore, the small amount of chemicals carried over, as drag-out, into Gold Taking math MP will do no narr. Mowever, this strike bath shall not be used, without inter enaber mission, in continuing the strike bath shall not be

The plating bath control limit of 15 oz/gal, maximum set for potassium carbonate is an estimated value. The actual concentration limit must be determine through additional operating experience.

RGA/SCR-1

#### BARREL FINISHING

#### PURPOSE

This method is used for depurring, cleaning, descaling and for surface refinement of most metals.

#### EQUIPMENT

Closed polygonal (vertical) barrels lined with neopreme, or its equivalent Bins for storing tumbling media. Stainless steel graduated scoop (4 cup). Glass bottle, graduated in cunces (4 oz.) Suitable loading and unloading equipment. Stainless steel mesh screens and vibrating equipment.

Cutting Life Of

#### MATERIALS

Alumina chips, (Lord Chemical Company), sizes #1, 3, 4, 8, 12 and special sizes. (#1 is the largest)

Compound	Use	Compound (Hrs.)
γx	Fine abrasive for light burrs and low micro-inch finishing	2-4
3A	Fast cutting during life, then a gradual breakdown to polishing action.	3-6
6A	Same as 3A, but a coarser abrasive	3-6 3-6
HS <b>-</b> 9	Same coarseness as 6A but used especially for hard metals. Will breakdown to fine	
24-48	polishing action in 20-24 hours. Alumina - used for cleaning caramics	6-10
	(Norton Company)	
a.	compounds (Lord Chemcial Company). GW (neutral)	
Finishin	MC-3 (alkaline) g and burnishing compound (Lord Chemical Compa Cap (for copper and lead)	any)
b.	Hi-Brite (other metals - except nickel) DL (for nickel)	
d.	AP2X (Copper and lead)	
	g compound (Lord Chemical Company) (for oxide removal)	
Steel bu	rnishing pins (Hartford Steel Ball Company) 6" diameter x 1/4" long tapered on ends.	

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	MATERIALS (CONTID
ace	<pre>Steel burnishing cones (Hartford Steel Ball Company)</pre>
	PROCEDUPE
ivalent.	<ol> <li>Alumina chip-media are washed by tumbling with hot water and l to 4 oz. GW for 5 minutes. (if necessary)</li> <li>Media is rinsed well with warm water.</li> <li>Parts to be tumbled are added so that the total load cf parts and media will settle to 50-60% of the barrel volume during tumbling.</li> </ol>
) .)	<ul> <li>Note: a. Fragile parts must be handled with care to prevent distortion during loading and unloading - may require alternate loading of parts and chips in layers.</li> <li>b. Geometry of the parts will determine the initial height of load.</li> <li>c. Fo prevent damage to heavy parts during tumbling, select or add a larger size of chips.</li> </ul>
	<ul> <li>h. The amount and type of abrasive compound to be used is added based on experience.</li> <li>5. Tap water is added to desired level - usually 1 to 6 inches below load level. Abrasive action increases as water decreases.</li> <li>6. Barrel is closed and rotated at desired rpm. Decrease the speed of rotation as mass and/or fragility of individual parts increases. Time and rpm. must be based on experience - normally 8-25 rpm. for 1 cu. ft. barrel.</li> <li>7. Barrel contents are rinsed well with water.</li> <li>8. For copper and lead: CAP is added for cleaning and finishing.</li> <li>a. Tap water is added to load level.</li> <li>b. Barrel is closed and rotated at desired rpm. for 1 hour.</li> <li>c. Barrel contents ere rinsed well with water, the load is dumped with care, and parts spearated from chips by screening or vibrating equipment.</li> <li>d. Parts are rinsed in acetone and blown dry.</li> </ul>
	9. For all other metals: Add MC-3 for cleaning.
	<ul> <li>a. Hot tap water is added to load level.</li> <li>b. Parrel is clused and rotated at desired rpm. for 10-30 min.</li> <li>c. Barrel contents are rinsed well with water.</li> </ul>

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#### PROCEDURE (CONTID)

10. Operation 9 is followed with a brightening cr burnishing process: Add Hi-Brite compound.

- a. Tap water is added to cover the load with 1 to 2" of water.
- b. Barrel is closed and rotated at desired rpm. for about 1 hour.
- c. Barrel conterts are rinsed well with water, the load is dumped with care and parts separated from chips by screening or vibrating equipment (except steel and nickel).
- d. Parts are dried in Kreider Dryer.
- 11. For steep parts:
  - a. Operations 10, 10a, 10b are performed.
  - b. Barrel contents are rinsed well with water.
  - c. Water is added to load level.
  - d. Watershed is added.
  - e. Barrel is closed and rotated at desired rpm. for 10 min.
  - f. Water is drained from barrel.
  - g. The load is dumped with care and parts separated from chips by screening or vibrating equipment.
  - h. Parts are dried thoroughly in Kreider Dryer.
  - i. Parts are dipped with agitation, in rust preventing mineral oil and drained,
- 12. For nickel parts:
  - a. Operations 10, 10a, 10b are performed.
  - b. Barrel contents are rinsed well with water.
  - c. Water is added to cover load.
  - d. DL is add.
  - e. Barrel is closed and rotated at desired rpm. for 1/2 to 2 hours.
  - f. Barrel contents are rinsed well with water,
  - g. The load is covered with clean water, the barrel is closed and tumble rinsed for 5 minutes.
  - h. Step 12f is repeated, then load is dumped with care and parts separated from chips by screening or vibrating equipment.
  - i. Parts are rinsed well with clean acetone and blown dry.

#### BBC CEDENT (IXVILID)

Lord hen, To pound	Bbl. #1 3/4 ft.3 Amount-'rups	2b1. 3 5 1/2 ft.3 Amount-(cups)	Hbl. 3 · 7 1/2 ft. ³ Amount-(cups)
άX	,	15	1(
36 68	1	11 1/2 11	0 5
HS - 9	1	5	7
∴-3 Hi-Brite	1/4 1/2	1 1/2 3 1/?	د -
CAP	1/2	J 1/2	2
AP2X G ^r (liq.)	3 oz 1 oz	22 oz ل oz	3. oz 6 oz
L (liq.)	5 oz	24 oz	32 cz
Watershed (lic Heatbath (crp.	1 1/2 or	' <b>0Z</b>	3.2. 5

#### PHOCESS CONTROL

Barrels and chip-media should be kept clean and sharp  $r_{i}^{-1}$  perion  $c > m_{i}n_{i}$  runs with hot water and SU. Intervals will vary with the application. Chips should be screened to insure proper size, especially if wedges of chips are likely to occur.

Mixing of compounds in a water slurry may be necessary with tubing or shells up to 3/8" inside diameter, to prevent packing of compound in the inside diameters.

Use hot water with 10-3 and GV.

Do not use W as a final rinse on steels, since it is a wetting agent Never leave a DL charge in the barrel when the barrel and parts are stopped; it may spot soft steels when not in motion.

#### SAFETY

Locsen door clamps slowly with care to "bleed" pressure which has built up during tumbling. LL solution is phosphoric acid, essentially; handle with care and avoid contact between it and cyanide. )

### APPENDI: J

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#### MANUAL OF INSPECTION AND QUALITY CONTROL PROCEDURES COVERING ELECTRON TUBE TYPE 6299

Order Number 6008-PP-61-81-81

Contract Number DA-36-039-SC-85953

General Electric Company Electronic Components Division Tube Department Owensboro, Kentucky

E.L. Davis

E. L. Davis, Superintendent- Planar & Thyratron Production

J.J.L. Finney, Supervisor-Test & Quality Control

J. E. Martin, Supervisor-Process Engineering - Planar & Thyratron Production

# GENERAL ELECTRIC

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August 7,	1964	New	ii	
DISTR	IBUTI	ON:		
	Initia	l distribution of	this manual is shown below:	
	CONT			
	GENI	ERAL ELECTRI		
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		<b>4</b> . 5.	J. L. Finney	
		6.	J. F. Madole	
		7.	J. E. Martin	
		8.	H. L. Thorson	
		9.	R. L. Watson	
	US	ARMY ELECTR	CONICS MATERIEL AGENCY:	
	0.0.			
		<u>Serial No.</u>	Holder	
		10.	George C. Munger, Contracting Officer	
		11.	George C. Munger, Contracting Officer	
		12. 13.	George C. Munger, Contracting Officer Stanley A. Sokolove, Project Engineer	
		13.	Stanley A. Sokolove, Project Engineer Stanley A. Sokolove, Project Engineer	
	CONT	TROL:		
		This manual i	s unclassified with respect to military security,	
			e Company and Army confidential in accordance	
	with S	SIG 434 SIP 3016	o (SPL), Exhibit II, Paragraph 2b.	
		Obsolete or m	evised material should be destroyed by the holder.	
			the match at should be destroyed by the holder.	
		For additional	l copies of this manual, contact: Manager,	
	Engin		tration and Application Engineering, General	
	Elect	ric Company, T	ube Department, Owensboro, Kentucky.	

TUBE DEPARTMENT GENERAL DELECTRIC

Owensbere, Kentucky

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#### INTRODUCTION

The electron tube type 6299 is a high-mu metal and ceramic triode intended for operation as a grounded-grid class A radio-frequency amplifier at frequencies as high as 3,000 megacycles. Features of the tube include small size, planar electrode construction with close spacing, inherent rigidity, and an envelope structure convenient for coaxial circuit applications.

The purpose of the contract was to evaluate certain areas of advanced tube manufacturing techniques and to apply them where feasible to JAN 6299, resulting in a more reliable and better performing tube. The objective requirements for the improved tube are Signal Corps Technical Requirement SCS-90 (Improved JAN 6299) and operation at a tube temperature rating of  $225^{\circ}$ C. The areas investigated were:

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1. Improved alignment, concentricity and ceramic strength.

- 2. Improved anode to ceramic seal.
- 3. Temperature control at exhaust.
- 4. Improved application of cathode coating.
- 5. Improved cathode mounting.
- 6. Improved processing for higher temperature operation.
  - 7. Improvement in humidity testing.
  - 8. Improved exhaust fixturing.
  - 9. Extended life test and tube failure analysis.



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		QUALI	GE	INERAL NOTES		
		QUALI				
		QUALI				
			TY CONTROL D	ATA FEEDBACK AND ANALYSI	S	
		<ul> <li>A. Fest records from the Engineering Test Laboratory and Test and</li> <li>Quality Control are fed back to process engineering and manage-</li> </ul>				
		me	ent for product o	control.		
]	II.	TEST E	EQUIPMENT			
		A. Each section is responsible for the maintenance and calibration				
		of	its test equipme	ent.		
IJ	[] <i>.</i>	TOOLS	AND GAGES			
		A. Each section is responsible for the maintenance and calibration				
		of	the tools and ga	ges used within the section.		
I	v.	ENGIN	ATION CHANGES			
		A. Alteration Notices (AN's) and Temperary Alteration Notices (TAN's)				
		on	construction an	d test specifications are issued,	and controlled by	
		a p	ed system as covered in Departn	nent Instruction		
		#7.	. 1-8 (Classifica	tion Engineering).		
	V.	TUBES	REQUIRING M	ILITARY QUALIFICATION INSPI	ECTION	
		A. When it is necessary to have samples available for "In-plant"				
		qua	alification testir	ng the Engineering Administration	n Section is	
		re	sponsible for:			
		1.	-	necessary data;		
		2.	U	in the Engineering Test Laborate	ory and Finished	
		~	Product Quali	•		
		3.	Writing desig	n – and – construction informatio	∙n;	
## Wenter to the transformed to the

ate leque	d Sup	ercedes	Section	Page
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	5. Ind wh 6. Ma in au 7. Pr B. The Pr	forming the G nen "In-plant aking arrang Charge to w thorized by p reparing the coject Engine	truction photographs; Quality Assurance Representative qualification testing is requeste ements with the Quality Assuranc itness "In-plant" tests when such proper authority; qualification test report. eer is responsible for supplying E h photographic samples and up to	d; e Representative tests have been ingineering
VI.	tion de INDUSTRIA	tails. L SECURIT	Y	
	-	·	Officer is responsible for mainter and, where required, military se	
VII.	MILITARY	COGNIZANO	CE	
	ment D		cognizance: (U.S. Army), Cincin 5. Army, 550 Main Street, Federa ti 2, Ohio.	
			e: (U.S. Navy), Inspector of Nav. vd., Building 101, St. Louis 20,	
	Procur	ement Distr	ognizance: (U.S. Air Force), Cir ict, 3rd Floor. Swift Building, 9t Cincinnati 2, Ohio.	
VIII.	RESPONSIE	ILITIES OF	ENGINEER - PROCESS CONTRO	DL
	objecti	•	cost and quality information and e consistent with the broad functi on.	

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	2. Fo	ormulate shori ar	nd long range plans for improvemer	nts in pro-
	du	ct performance a	and quality and manufacturing proce	8888.
	3. Re	evise plans and g	oals in a timely fashion as indicate	d by changes
	in	engineering requ	lirements so as to meet objectives.	
	4. Or	rganize own work	and time in the most efficient and	effective
2 T	m	anner.		
	5. Or	rganize the availa	able resources of equipment, perso	nnel, and
<b>.</b>	ot	her factors at his	s disposal to efficiently obtain his o	bjectives.
	6. Di	rect efforts towa	rd the manufacture of products .nat	t meet
•	en	jineering specifi	cations and which are competitive :	in quality
_	an	d costs.		
	7. Pi	rovide manufacta	ring with timely, accurate and effe	ctive instruc-
1	tic	ons for reducing	costs and improving product quality	<i>.</i>
] L	8. Pi	irsue a program	of self-development and contribute	to the
)	te	chnical education	of others within the department.	
	9. Pr	rovide engineerin	ng leadership within the plant by cor	ntributing
	ne	w and/or origina	l ideas for solving problems assoc	iated with
4	m	anufacturing.		
I	10. In	nplement plans fo	or and continuously maintain an agg	ressive
J	sh	rinkage and over	-all manufacturing loss reduction p	program and
<b>.</b>	in	stitute corrective	e measures as deemed necessary.	
i	11. Re	esponsible for wo	orking with Design Engineering rega	arding process,
	sŗ	pecification and p	roduction problems. Recommend r	nanufacturing
	pr	ocesses and cont	tribute whenever possible to the des	sign of new
	tu	bes.		
	12. Se	et up techniques f	or following product quality and ini	tiate corrective
	m	easures as deem	ed necessary.	

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	13.	production and evalu	andards for incoming parts and : ate sample parts from vendors; necessity for and the extent of pr	and is responsible
		and inspections.		
	14.		nd interpret the measured result readjust work of measuring as r	
	15.		d reports to indicate the effectiv	-
	16.	-	or - Manufacturing Engineering ce in his area of responsibility o	0
			ionships with others.	<b>1</b> 41
	17.	regarding related pr	ngineers, and Specialists in his a roblems.	subsection
	18.	Consult with other su duties and responsib	ubsection personnel as required ilities.	to fulfill his
	19.	Consult with other en needed regarding pro	ngineering and manufacturing co oblems in his area.	mponents as
IX.	IDE	NTIFICATION OF RE	JECTED MATERIAL	
	A.	Rejected material, i analyzed and scrapp	n Shop Operations, Ceramic Tul ed.	pes, is tagged,
x.	STA	NDARDS CALIBRAT	ION PROCEDURE AND SCHEDU	LE
	Α.	-	are in general checked once a ye to the Bureau of Standards.	ar ty a
ŧ	в.		rd for measuring voltages and cu calibrated as per "A" above.	irrents is a

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	C. The	e secondary sta	andards are meters calibrated by u	sing the				
	sta	ndard cell. Th	his is done approximately every 3 m	nonths.				
	D. Me	ters are calib:	rated periodically against the second	lary standards.				
	Me	Meters are tagged with their date of calibration. All removable						
	me	tere gre calibr	rated monthly. The permanently loo	cated meters				
	are	calibrated eve	ery 90 days with an additional calib:	ration at				
	sea	sonal changes,	, such as summer to winter, and in	the event of				
	any	question on re	esults.					
VI	NEDEC							
XI.	INSPECTION NOTES The first phase of this contract specifies a production rate of 1000							
		-						
	-		process inspection is accomplished					
	-	operators in a bench inspection set-up under the Foreman-Glass Light-						
			sembly and Exhaust, under the surv	reillance of the				
	process	ongineer.						
	The	e following add	itional information is presented:					
	I.	Reference Do	ocuments are:					
		A. Standard	lized construction drawings for type	6299.				
		B. Standard	lized process specifications for type	6299.				
	п.	Changes in p	arts, tolerances, limits, processin	g instructions.				
			n procedures are authorized by Eng	-				
		*	-	, ,				

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		INSPI	ECTION STATIONS	
1.	RECE	VING MATERIAL	S INSPECTION	
	A. P	rocess: Collect,	inspect, and distribute incoming parts	and raw
	m	aterials.		
	(1)	Inspection Proc	edure: Incoming stock is identified a	ccording to
		purchase order	or contract. Material is sampled in	accordance
		with internal in	spection specification, (see index). N	isual and
		mechanical insp	pection is performed in accordance wi	th this
		specification.	Material is either accepted to stock o	r returned
		to supplier.		
	(2)	AQL's and sam	ple sizes: Inspection specification, (	see index).
	(3)	Classification o	of defects: Inspection specification, (s	see index).
	(4)	Calibration of t	est equipment Calibration is conduct	ed in
		accordance with	h TM-100.	
	(5)	Reference docu	ment: Inspection specification index,	and TM-100.
	<b>(</b> 6)	Changes in part	ts, tolerances, limits, etc., are auth	orized by:
		Alteration Notic	ces or Temporary Alteration Notices	originated
		by the Process	Control Engineer.	
	(7)	Changes in insp	pection procedures are authorized by:	Process
		Control Engine	6 <b>7</b>	

## GENERAL TELECTRIC

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2.	CA	THOD	E ASSEMBLY		
	А.	Cath	ode Assembly Pr	COCESS	
	в.	Insp	ection Procedure		
		(1)	After cathode as:	sembly, cathodes are inspected under a	10X
			microscope.		
		(2)	AQL's and sampl	le sizes: 100% inspection.	
		(3)	Classification of	defects: Burrs, torn, malformed foil.	
		(4)	Inspection instru	ments: 10X microscope.	
		(5)	Forms used: Mi	niature Ceramic Shrinkage Report, Ex	nibit #10;
			Ro	ute Process card, Exhibit #11 is a <u>sam</u>	ple of
				this type of card.	
[					

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ate Issue	d	Supercedes	Section	Page
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. <u>3</u> .	ĆOATF	D CATHODE AN	D INSULATOR ASSEMBLY	
	A. Ca	thode Spray Proc	ê 8 8	
	B. Ins	pection Procedur	e	
	(1)	a. Cathode de	nsity is checked each run;	
		b. Cathode he	ight is checked after milling cathode:	
		c. Each catho	de is inspected under a microscope for vi	sual
		defects.		
	(2)		n) a sizas	
	(-/		•	
			l cathodes are checked for density;	
		b. 100% inspe		
		c. 100% inspe	ction.	
	(3)	Classification o	f defects:	
		a. Density, hi	gh or low,	
		b. Cathode he	ight, high or low;	
		c. Tilted cath	ode; chipped or insufficient coating.	
	(4)	Inspection instr	uments: 10X microscope, dial gauge, ba	lance
			dummies (control cathodes).	]
	(5)			1
	(5)		xhibit #10; Exhibit #11; Cathode Assemb	ly j
		Shrinkage Repo	rt. Exhibit #12.	4
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4.	HE	ATE	R AND CATHODE	CASSEMBLY	
	А.	Ass	embly Process		
	B.	Ins	pection Procedure	e	
	•	(1)	-	welded into coated cathode and insulator	
2		(-)		X microscope is used to inspect heater c	osting
ſ			weld and cathode		varing,
L •		( )			
			-	ble sizes: 100% inspection.	e .
•		(3)		f defects: Open or weak welds, chipped	heater
			coating, cathode	e coating chipped or dirty.	
;		(4)	Inspection instru	uments: 10X microscope.	
, )		(5)	Forms used: Ex	xhibits #10 and #11.	
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, 5.	GR	ID M	AKING		
	А.	Gri	d Manufacturing	Process	
	в.		pection Procedu		
		(1)		grids are placed under a 10X microscope	2,
			inspected and t		
		(2)		ple sizes: 100% inspection.	
		(3)		of defects: Windows, copper balls, poor	spacing,
			overlapped wir		
		(4)	-	ruments: 10X Binocular microscope.	
		(5)	Forme used: E	Exhibits #10 and #11.	

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6. GRID ASSEMBLY

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- A. Assembly Process
- B. Inspection Procedure
  - All grids are inspected with a 10X microscope for visual defects.
     Grids are then checked for vibration.

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- (2) AQL's and sample size: Visual inspection 100% inspection.
   For vibration, lots sizes to 300 are sampled using MIL-STD-105, Level II, 2.5% AQL; for lot sizes over 300, 1.0% AQL.
- (3) Classification of defects: Windiws, copper balls, poor brazing, poor spacing, overlapped wires, lint and dirt, poor tension on wires.
- (4) Inspection instruments: 10X microscope, vibration equipment.
- (5) Forms used: Exhibits #10 and #11.

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. 7.	PRE	SEAL ASSEMBLY		
	<b>A</b> . 1	Preseal Assembly Pro	ocedure	
	B. J	Inspection Procedure		
	(	(1) a. Assemblies a	are inspected under a 10X microscope.	
		b. After preseal	l assembly and braze, assemblies are	
,		tested for lea	akers with helium leak detector.	
I	(	(2) AQL's and sample	e sizes:	
		a. 100% inspecti	ion.	
		b. 100% inspecti	ion.	
	(	(3) Classification of 1	Defects	
; )		a. Improper ass	sembly, poor solder flow.	
		b. Leakers.		
	(	(4) Inspection instrum	ments: Helium leak detector, 10X mic	roscope.
		-	hibits #10 and #11.	-
	•			
1	с. (	Getter welding proces	15	
I				
•	n	After the getter has h	een welded, the operator makes a chec	to to the
		~	een werdeu, the operator makes a chec	
	1	proper weld.		

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. 8.	AN	ODE	ASSEMBLY		
	A.	Ano	de Assembly Pr		
	в.	T	ection Procedu		
	، در				
		(1)		e assembly and braze, assemblies are t	ested for
			leakers wi	th helium leak detector.	
			b. Assemblie	s are inspected under a 10X microscope	for visual
			defects.		
		(2)	AQL's and sam	ple sizes	
			a. 100% inspe	ction.	
			b. 100% inspe	ction.	
		(3)	Classification of	of defects:	
			a. Leakers.		
			b. Anode not	seated; burred, defaced anode.	
		(4)		ruments: Helium leak detector, 10X mic	TOSCODE.
		(5)		Cxhibits #10 and #11.	
		(-)	- orms nood, r	Antoro HIV CHU TII.	

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<u> </u>					
. 9.	EXHA	UST AND SEALIN	٩G		
	A. E	xhaust and Sealin	g Process		
	B. In	spection Procedu	re		
	(1	) After exhaust	and sealing, the tubes are checked for i	noperatives.	
	(2		nple sizes: 100% inspection.	-	Q U
	(3	) Classification	of defects: Open and shorted heaters,	air-leakers,	A
		grid-anode sho	-		L
	(4	-	ruments: Heater voltage power supply.		I T
			Exhibit #10; Manufacturing Record, Ex		Ŷ
	()	j i dinib useu.	Exhibit #10, Manufacturing Necord, Ex	IIDIC ##J.	
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<ol> <li>AGING         <ul> <li>Aging Process</li> <li>Daily Quality Control Check                 <ol></ol></li></ul></li></ol>	<ol> <li>AGING         <ul> <li>Aging Process</li> <li>Daily Quality Control Check                 <ol></ol></li></ul></li></ol>	
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			Tube Acceptance Test		••
	_	1) Inspection proc	•		
			ory iests, tubes shall be submitted to	Test and	
		Quality Co	ntrol for complete electrical and me	chanical	a a
		tests in ac	cordance with the applicable MIL-E-	l test	บิ
		specificati	on, MIL-STI)-105, and other referen	nced docu-	A L
		ments.			I
	(	2) AQL's and sam	nple sizes: AQL's and sample sizes	shall be in	T Y
		accordance wit	h the applicable test specification.		-
	(	3) Classification	of defects: Defects are defined by lin	mits on the	С
		applicable test	specification sheet.		0
	(	4) Inspection equi	pment used: The conventional equip	ment used	N T
		for testing tube	e type 6299 has received approval and	d is listed	R O
		in the List of M	Miniature Ceramic List of Production	n Test	L
		Facilities date	d 18 June 1962. The equipment used	for the	
		improved vers	ion of the 6299 has received approval	l and is	м
		listed in the In	nproved Miniature Ceramic List of T	est Facilities	A N
		dated 15 Octob	er 1963.		U
	(	5) Forms used:			A L
		a. Product A	cceptance Sampling Record, Exhibit	#15.	
		b. Median Co	ntrol Data, Exhibit #16.		
			Tube Location Card, Exhibit #17.		
			Data, Exhibit #18.		
			Status Report, Exhibit #19.		
		f. Masier Sh	rinkage Symbol List, Exhibit #20.		

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### GENERAL 💓 ELECTRIC

Owonakare, Kentucky

<ol> <li>COMMERCIAL SERVICE AND WAREHOUSE</li> <li>Commercial Service</li> <li>Order Service: Orders requiring government inspection are received from customers or via other sales offices and edited by Commercial Service Clerks.</li> <li>Order Service clerks release material for inspection and shipment as required by purchase orders. Copies of this release authorize inspection of material, as indicated, and packaging/ packing and shipment of material.</li> <li>Instructions for tube branding are furnished the Branding Department and Warehouse by Commercial Service.</li> <li>Instructions for packaging and unit packaging Department and Warehouse by Commercial Service.</li> <li>Container marking labels are prepared by Commercial Service.</li> <li>Packing lists, invoices, shipping Department.</li> <li>Packing lists, invoices, shipping documents, etc., are prepared for each shipment by commercial Service.</li> <li>Reference document*. Commercial Service and Warehouse Procedures 2.7, 2.12-1, 2.15, 2.15-1, 2.13-1, 3.1-1, ST 13700K.</li> </ol>	August 7,	-	Supercedes Secti New	on 11 - QUALITY CONTROLS	<b>Page</b> II - 14	Date I Augu
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#### B. Warehouse

- Tubes that require completion of life test prior to shipment, are transferred to Warehouse after all other tests have been completed. These lots are placed in "life-held" status until a notice of satisfactory completion of life test is received.
- (2) Prior to branding, tubes are inspected 100% by branding operator for type. Each set-up is checked for accuracy and legibility by the set-up operator. After branding, spot checks are made for proper brand. Marking permanency tests are

### GENERAL GO ELECTRIC

Owensberg, Kentucky

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made on tubes branded for government use, in accordance with method 1105, MIL-E-1.

- (3) Tubes are either bulk packaged or unit packaged as required by purchase order.
- (4) Shipping Department places labels on shipping containers, places invoices, packing lists, etc., inside the containers, seals containers and releases material to carriers for shipment.
- (5) Reference documents: Commercial Service and Warehouse Procedures (see paragraph 12. A. 3).
- C. Exhibits: Section III, Exhibits 21 through 23.

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2. 2. Spray J1-1P (30 asm/load) & check	
3. <u>2/30 for coating thickness</u>	
4. 3. Mill coating to size & check coat	Ing
5. thickness on dial indicator	
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