Kinetic and Rheological Studies of a Model In-Situ Molecular Composite System (PAA/DNI-3A)

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COPIES OF THIS REPORT SHOULD NOT BE RETURNED UNLESS RETURN IS REQUIRED BY SECURITY CONSIDERATIONS, CONTRACTUAL OBLIGATIONS, OR NOTICE ON A SPECIFIC DOCUMENT.
A model compound of In-Situ Molecular Composite system, poly(amic dialkylamide) was prepared and characterized in an attempt to better understand the rod conversion for designing a processing scheme for these materials. The conversion kinetics and the chemorheology of the system were studied by using FTIR and TICA. The activation energy was found to be higher than the values reported for poly(amic esters). The rod conversion kinetics was controlled by rheology. Two different kinetic rates were observed before and after the vitrification point. A Fixed-Time-Interval method for using FTIR data to analyze kinetic rate was developed. The effect of pressurization on the thermal behavior of the model system was analyzed. This study clearly indicated that the rod conversion chemistry is rheologically controlled.
FOREWORD

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This report covers research conducted from April 1989 to June 1990.
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SECTION 1
INTRODUCTION

The concept of In-Situ Molecular Composites (ISMС) was introduced previously [1,2]. These ISMC systems will undergo an intramolecular thermal elimination (ring closure) to form the rigid-rod polyimide, and the evolved pendants can crosslink to form an in-situ network. The feasibility of the conversion (ring-closure only) has been proven spectroscopically [3]. However, to yield useful properties, the ISMC materials will have to consolidate, to attain complete conversion to generate high aspect ratio rods, and to remain molecularly dispersed. These factors are very much controlled by the rheology of the systems during processing. Sufficiently low viscosity is required for consolidation and rod conversion, but too low a viscosity will cause the aggregation of the rod molecules. The successful conversion of the aforementioned poly(amic dialkylamides) into molecular composites will necessitate a careful definition of the processing window.

In an attempt to understand better the process of rod conversion so as to design a processing scheme for these materials, the kinetics of rod conversion and its relationship with the rheology of a prototype system, poly(amic amide/DNI-3A) (PAA/DNI-3A) where DNI-3A is an alkyl dinadiimide derived from 3,3'-iminobispropylamine and nadic anhydride, was studied. The structure and imidization of PAA/DNI-3A is shown in Fig.1. FTIR was used to follow the degree of imide conversion. Analysis of the kinetic algorithm showed that systematic errors could be introduced if the final concentration of reactant was not accurately known. A modified fixed-time-interval approach was developed and was used to analyze the kinetic data. Chemorheology of the system was studied by using TICA
Fig. 1. Chemistry of PAA/DNI-3A for in-situ rod reinforced molecular composite
DNI-3A matrix network

Fig. 1. (continued)
in isothermal and temperature scan modes. The DSC of the model system polymer and the model leaving group under ambient and pressurized condition was analyzed.
SECTION 2
EXPERIMENTAL

The poly(amic amide) samples (PAA/DNI-3A) (sample #A90501) used in this study was prepared by Tan [1,2]. The synthesis of this compound is based on a previously published synthesis route for poly(amic dialkyl amide) [4]. The details of the synthesis of this compound will be published separately [1,2]. The syntheses reaction is summarized in Fig. 2. PMDA (pyromellitic dianhydride) and TMB (tetramethyl benzidine) as the starting monomers were reacted to yield a poly(amic amide), which was sequentially converted to polyisoimide, and finally to poly(amic dialkyl amide). The leaving group of this compound is an alkyl group terminated with norbornene.

Film samples of PAA/DNI-3A were solvent casted from 0.4% concentration DMAc solutions. About 10 ml of this solution was placed on a 3.5" petri dish. Vacuum was applied for 24 hours to remove the solvent. The film was then immersed in acetone overnight to remove residual DMAc. The film was subsequently rinsed with acetone several times and dried in air. Small pieces of the films were sandwiched between KCl plates for FTIR studies. The plates were mounted inside a temperature controlled fixture for kinetic studies.

After placing the fixture inside the IR chamber, the film was heated at the rate of about 40°C/min to the desired temperature. When the system reached a predetermined temperature, the timer was started and an initial IR scan was recorded. Subsequent spectra were recorded at appropriate time intervals. The spectra were stored in an on-line computer for later use. After the last spectrum was recorded the heater was turned off and the film was allowed to cool. The final IR scan for the cooled sample was also recorded.
Fig. 2. Synthesis route for PAA/DNI-3A and polyimide
The details of TICA specimens preparation and experimentation were described elsewhere [5]. A piece of glass cloth of 3"x4" was prepared by pulling two strands of fibers every half inch in the width direction. The cloth was immersed in a 4% DMAc solution of the polymer and placed in a desiccator for vacuuming and drying. Then the cloth was immersed in acetone overnight to remove residual DMAc. Before being dried in air the cloth was rinsed with acetone several times. The dried cloth was then cut in halves and folded into strips of 1.2 cm wide, 6.4 cm long and 0.2 cm thick, with the cut edges folded inside the strips. The specimen was made by stacking two strips with the ends sandwiched by two metal plates held together by a screw at the center. The TICA specimen was mounted on the RDS instrument with the end metal plates as fixtures. The instrument was set at "torsion" mode and the control mode was set at "cure".
SECTION 3
BACKGROUND

3.1 Possible Chemistry Description

The PAA/DNI-3A chemistry is similar to PMR-15 [6]. The monomers used in PMR-15 include a dialkyl ester of aromatic tetracarboxylic acid such as BTDE, an aromatic diamine like MDA, and a monoalkyl ester of norbornene 2,3-dicarboxylic acid (NE). They are dissolved in a low boiling alkyl alcohol. After heating to 150-220°C temperature range, the the solvent was removed and the monomers undergo in-situ condensation and cyclodehydration to yield norbornenyl end-capped low molecular weight imide prepolymer. Under pressurized condition, the end-capped prepolymer undergoes addition polymerization (crosslinking) at 260-315°C without evolution of volatiles.

The same types of reactions occur in the current PAA/DNI-3A system. The high molecular weight poly(amic amide) will undergo ring closure imidization probably at a higher reaction temperature. A leaving group with a reactive end-cap will be released from the reaction. This leaving amine group, NH(nadic-3A)2, may undergo crosslinking reaction and degrade due to the instability of the alphilic bonds in its structure.

3.2 Temperature Range of the Reactions and the FTIR Measurement

The polyimide formation reactions from different prepolymers such as poly(amic acid), poly(amic ester) or poly(amic amide) are similar. Most of the data in literature were from poly(amic acid) system and in solution state. The activation energy and mechanism for the imide formation in the solution state can be different from that in the solid state. It has been shown that the solvent-polymer interaction caused difficulty in the removal of solvent in the
final stage [7,8] and affected the imidization rate [9]. The condensation reaction product, water, also induced hydrolysis of the polymer and cause rapid degradation [10].

The kinetics of the formation of imide showed that it was a first order reaction and is linearly proportional to the concentration of amic acid. Recently, a second order reaction mechanism of maleimide formation was reported [11]. It was argued that the imidization rate is proportional to the product of the amic acid concentration and the catalyst acetic anhydride concentration. Nevertheless, most reports agreed that the imide formation reaction being a first order reaction. Most of the research on imide formation kinetics were based on FTIR technique. The temperature range for the imide formation and the associated kinetic data including pre-exponent constant and the activation energy constant are listed in Table 1.

For PMR type polyimide, the crosslinking reaction of the nadic group, occurs at a higher temperature. The reaction mechanism still remains controversial. Some possible reaction routes found in the literature are shown in Fig.3 [20,21]. The crosslinking reaction of the nadic group involves a retro-Diels Alder reaction in which the nadic group cracks down to form maleimide and cyclopentadiene. The cyclopentadiene has boiling temperature about 41°C which is much lower than the crosslinking temperature. In order to incorporate the cyclopentadiene compound in the crosslinking reaction, a high pressure environment has to be maintained to suppress the evolution of pentadiene.

Experiments also showed this crosslinking reaction for the PMR system to be a first order reaction. The kinetic data of this reaction was determined by DSC thermoanalysis. Only one set of kinetic data was found in the literature [15], and the values are:

\[ A=2.5 \times 10^5 \text{ min}^{-1}, \ E=44\pm2 \text{ Kcal/mole}, \ T=275-325^\circ \text{C with pressure.} \]
Table 1. The kinetic parameters of imidization in the literature

<table>
<thead>
<tr>
<th>$k_0$(min$^{-1}$)</th>
<th>E (Kcal/mole)</th>
<th>Reaction Temp (°C)</th>
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<tr>
<td></td>
<td>28.2</td>
<td>150-200</td>
<td>[9]*a</td>
</tr>
<tr>
<td></td>
<td>23±7 (slow)</td>
<td>161-188</td>
<td>[12]*b</td>
</tr>
<tr>
<td></td>
<td>26±3 (fast)</td>
<td></td>
<td></td>
</tr>
<tr>
<td>4.6 E 10</td>
<td>26 ± 4</td>
<td></td>
<td>[13]*c</td>
</tr>
<tr>
<td></td>
<td>19.5</td>
<td></td>
<td>[14]*d</td>
</tr>
<tr>
<td>8.4 E 8</td>
<td>24 ± 6</td>
<td>120-204</td>
<td>[15]*e</td>
</tr>
<tr>
<td></td>
<td>10 ± 1</td>
<td>100-170</td>
<td>[16]*f</td>
</tr>
<tr>
<td></td>
<td>14-65</td>
<td>150-250</td>
<td>[17]*g</td>
</tr>
<tr>
<td>6.8 E 10</td>
<td>26</td>
<td>140-170</td>
<td>[18]*h</td>
</tr>
<tr>
<td></td>
<td>8.6 ± 2.3</td>
<td>140-200</td>
<td>[19]*i</td>
</tr>
<tr>
<td>12 (2nd order rxn)</td>
<td>27-80</td>
<td></td>
<td>[11]*j</td>
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*a*  BTDA + DABP in diglyme solvent, by FFIR, 720 and 1780 cm$^{-1}$

*b*  4,4'-diaminodiphenyl ethe: + PMDA in DMAc solvent, by FTIR, 725 cm$^{-1}$

*c*, *d*, dianhydride + diamine (not specified), 720 & 1380 cm$^{-1}$ (recommended)

*e*  NE + MDA + BTDE in methanol (PMR system), by FTIR, 1370cm$^{-1}$

*f*  PMR-15 by RDS method

*g*  PMDA/ODA, E=28, BTDA/ODA, E=22, BPDA/ODA, E=16, BPDA/ODA, E=14, Toray photoneece, E=26, PMDA/ODA ethyl ester, E=65, all by FTIR, 1780cm$^{-1}$

*h*  BTDA + DDS + siloxane oligomer in NMP/CHP cosolvent for solution imidization, by FTIR, 725cm$^{-1}$

*i*  PMDA + ODA in NMP solvent, by Fluorescence Spectroscopy

*j*  Maleamic acid --> maleimide, 2nd order reaction, by 1H-NMR
(Scola, 1985 [21])

\[
\begin{align*}
\text{endo or exo nadimide isomer} \\
\text{crosslinked polyimide}
\end{align*}
\]

Fig. 3. Possible reaction routes for nadic group
Fig. 3. (continued)
Myers [16] used PMR-15 prepreg by RDS instrument to obtain the activation energy of the
crosslinking reaction to be 14±2 Kcal/mole, a value much smaller than Lauver's data.

3.3 First Order Reaction Kinetics Based on Normalized Concentration

From FTIR data, the first order reaction kinetic parameters can be obtained by two
methods. One is based on the reactant or product normalized concentration, and the other
is based on fixed-time-interval data. These two techniques will be analyzed in detail in this
and the next sections. But first let's examine the first order reaction kinetics.

The first order chemical reaction

\[ \text{C} \rightarrow \text{P} \]

is represented by the following differential equation:

\[
\frac{dp}{dt} = -k[c] = k[c] \quad \text{(la)}
\]

The initial conditions are defined as:

\[ \text{i.c. @ } t=0, [c] = [c]_0, [p] = [p]_0 \quad \text{(1b)} \]

The following equation holds for the first order reaction:

\[
[p]_0 + [c]_0 = [p]_t + [c]_t = [p]_\infty + [c]_\infty = \text{constant.} \quad \text{(1c)}
\]

Please note that in this report the notation \([c]_\infty\) represents the reactant concentration at
infinite reaction time and is therefore zero. With the conditions (1b) and (1c), the
differential equation (1a) can be solved by direct integration method to obtain the solution of \([c]_t\) and \([p]_t\),

\[
[c]_t = [c]_0 e^{-kt}
\]

\[
[p]_t - [p]_0 = [c]_0 (1 - e^{-kt})
\]

(2)

For accurate determination of the first order kinetics parameters, either the initial product concentration \([p]_0\) or the final reactant concentration has to be accurately determined. In infrared spectroscopy the concentration can be extracted from the absorbance according to Beer's Law, which is,

**Beer's Law:**

\[
A = ab[c] = - \log_{10} T
\]

where \(A\) is the absorbance,

- \(a\) is the absorptivity, \([\text{cm}^2/\text{mole}]\),
- \(b\) is the path length, \([\text{cm}]\),
- \([c]\) is the concentration of the absorbing species, \([\text{mole/cm}^3]\)
- \(T\) is the transmittance,

If the systems contains some inert species (an absorption peak that does not change in intensity in the course of the reaction being studied) which absorb at the same frequency, then

\[
A(v_C, t) = A_C(t) + A_i = a_C b[c]_t + a_i b[I]
\]

\[
A(v_P, t) = A_P(t) + A_{i'} = a_P b[p]_t + a_{i'} b[I']
\]

(4)

where \(A(v_C, t)\) and \(A(v_P, t)\) are the apparent absorbance at peak frequency for C and P moieties respectively, \(A_C(t)\) and \(A_P(t)\) are the true absorbance of C and P at time \(t\), \(A_i\) and \(A_{i'}\) are the absorbance of inert species I and I' respectively.
In equation (4), $A_c(t)$ and $A_{pr}(t)$ are the desired quantities for the kinetic study, but $A(v_o,t)$ and $A(v_p,t)$ are the experimentally measured data. The background absorbance can be removed by subtracting different spectra:

$$A(v_o,t_1) - A(v_o,t_2) = A_c(t_1) - A_c(t_2) = a_b ([c]_{t_1} - [c]_{t_2}) \tag{5}$$

$$A(v_p,t_1) - A(v_p,t_2) = A_p(t_1) - A_p(t_2) = a_b ([p]_{t_1} - [p]_{t_2})$$

This subtraction result is the change in absorbance as a result of the reaction. Normalizing the subtraction data with the total change between $t=0$ at the beginning of the experiment and $t=\tau$ at the end of the experiment, will yield

$$\frac{A(v_o,0) - A(v_o,t)}{A(v_o,0) - A(v_o,\tau)} = \frac{[c]_0 - [c]_{\tau}}{[c]_0 - [c]_{\tau}} \tag{6a}$$

$$\frac{A(v_p,t) - A(v_p,0)}{A(v_p,\tau) - A(v_p,0)} = \frac{[p]_{\tau} - [p]_0}{[p]_{\tau} - [p]_0} \tag{6b}$$

with

$$\frac{[c]_0 - [c]_{\tau}}{[c]_0 - [c]_{\tau}} = \frac{[p]_{\tau} - [p]_0}{[p]_{\tau} - [p]_0} \tag{6c}$$

The ratio terms shown in equation (6c) represent the normalized degree of reaction conversion. If $[c]_{\tau}$ is sufficiently close to zero ($[c]_\tau \sim [c]_\infty = 0$) then the data obtained according to equation (6a) and (6b) can be analyzed by replacing $\tau$ by $\infty$ and using the kinetic equation (2). Thus the logarithm of $[c]_t/[c]_0$ (or $[A(t)-A(\infty)/A(0)-A(\infty)]$) versus time $t$ plot will yield a straight line with the slope being the desired reaction constant $k$. But if $[c]_\tau$ is not zero, equation (6) will not be equivalent to equation (2), but instead be
\[ 1 - \frac{A(t) - A(0)}{A(\tau) - A(0)} = \frac{A(t) - A(\tau)}{A(0) - A(\tau)} = \frac{[p]_h - [p]_r}{[p]_0 - [p]_r} = \frac{[c]_h - [c]_r}{[c]_0 - [c]_r} \neq e^{-kt} \quad (7) \]

The logarithm of \( ([c]_r - [c]_r)/([c]_0 - [c]_r) \) versus time \( t \) plot in this case will not give the correct quantity \( k \). The analysis in the following section then has to be taken.

### 3.4 First Order Reaction Kinetics Based on Fixed-Time-Interval Data

From equation (2) one can immediately obtain the following equation,

\[
[c]_h_i - [c]_h_2 = [c]_0 (e^{-kt_i} - e^{-kt_2}) \\
[p]_h_i - [p]_h_2 = - [c]_0 (e^{-kt_i} - e^{-kt_2}) \quad (8)
\]

Equation (5) can be rewritten in the following general form,

\[
\Delta A(t_1, t_2) = k' (e^{-kt_1} - e^{-kt_2}) \quad (9)
\]

where \( \Delta A(t_1, t_2) \) represents either \( A(c, t_1) - A(c, t_2) \) or \( A(p, t_1) - A(p, t_2) \) and \( k' = a_c b[c]_0 \) or \( -a_p b[c]_0 \). Taking the logarithm of equation (9) yields

\[
\ln \Delta A(t_1, t_2) = \ln k' - \ln (1 - e^{-k(t_1 - t_2)}) \\
\quad = \ln k' - kt_1 + \ln (1 - e^{-k(t_1 - t_2)}) \quad (10)
\]

Now if \( (t_1 - t_2) \) is set to be constant (equally spaced time data), equation (10) can be rewritten as

\[
\ln \Delta A(t_1, t_2) = \ln k' - kt_1 + \ln (1 - e^{-k(t_1 - t_2)}) = k'' - kt_1 \quad (11)
\]
with $k''$ being a constant as well.

From equation (11) with equally spaced data, the plot of $[\ln \Delta A(t_1, t_2)]$ verse $t_1$ will generate the slope $(-k)$, which is the desired reaction rate constant at that particular temperature. The example for using these two different approaches to calculate the kinetic data are shown in Appendix A for comparison.
SECTION 4
RESULTS AND DISCUSSION

4.1 Chemistry Correlated with DSC and TGA/MS Results

To further characterize the chemistry of PAA/DNI-3A system (sample #A90501) at elevated temperature, the system was analyzed by TGA/MS spectra. The report from SRL is shown in Appendix B. The result, shown in Fig.4a, illustrated that cyclopentadiene (C₅H₆) started to evolve ~150°C as the product of the reverse Diels Alder reaction. No other product were released in this temperature range. The next volatile product started above 300°C with m/e being 138 and was assigned as C₃H₆NC₃H₅NCO. This is part of the secondary amine from DNI group. Fig.4b showed the TGA/MS result of the model compound, DNI-3A (also see Appendix B for the SRL report). It suggested that the sample be consumed by degradation. The expected product cyclopentadiene was observed at 220°C, which was 10°C below the corresponding data from poly(amic amide)/DNI-3A.

The DSC experiments were run for DNI-3A and PAA/DNI-3A under both ambient and high pressure (750 psi) environments. The DSC result for PAA/DNI-3A systems under ambient pressure condition is shown in Fig.5a. The region between 200°C to 350°C can be interpreted as a composite of an endotherm superposed on an exotherm. The endotherm started at about 200°C. The exotherm started at a higher temperature and showed a peak at about 280°C. At even higher temperature, the exothermic reaction overshadowed the endothermic reaction. The peak at 343°C was the tail section of the exotherm. This interpretation can be substantiated by studying the pressured DSC result shown in Fig.5b. The exotherm is due to the ring closure imidization reaction and the crosslinking reaction of the nadic end groups. The endotherm is from the evolution of cyclopentadiene. Under the pressurized condition, the evolution of cyclopentadiene was suppressed and the DSC...
Fig. 4. TGA/MS spectra for (a) PAA/DNI-3A, and (b) DNI-3A
Fig. 4. (continued)

Sample LST-70357-14A
G. S. 15/89
Fig. 5. DSC thermogram for PAA/DNI-3A under (a) ambient, and (b) 750psi pressure, and for DNI-3A under (c) ambient, and (d) 750psi pressure.
Sample: LST 70359-44A
Size: 3.8 mg
Run No.: #3990 (23)
Date: JUL/12/89 12:29

OMNITHERM DATA SYSTEM

DSC (HP)

Operator: EJS
Disk ID: EJS-HP DATA-2
File No.: D11.DAT V2.1
Plotted: JUL/12/89 14:15

750 psi p(amic amide)

$\Delta H = 153.50$ kcal/mg

293.0 °C

243.4 °C

112.1 °C 140.4 °C

Fig. 5. (continued)
showed only the exothermic component. The exotherm showed a well-behaved profile and peaked at \(-290^\circ C\). The high temperature tail section of the exotherm corresponded nicely with the high temperature peak (343°C) shown in Fig. 5a.

The DSC result of the model leaving group, DNI-3A, is shown in Figs. 5c and 5d. The unpressurized DSC result in Fig. 5c shows a melting endotherm at about 92°C. Another endotherm starts at about 200°C. This endotherm is due to the evaporation of the cyclopentadiene which is released from the decomposition of the nadic end group. The decomposed end groups can not crosslink at higher temperature. Thus no appreciable exotherm is shown in Fig. 5c. The pressurized DSC in Fig. 5d shows a similar melting endotherm at about 90°C. Evolution of cyclopentadiene is suppressed by the pressure. Two exotherms can be detected peaking at 272°C and 322°C respectively. Crosslinking reactions will occur at higher temperature if the cyclopentadiene evolution can be suppressed by external pressure.

4.2 FTIR Spectra and Subtraction Results

FTIR was used to study the imidization kinetics. In this study three different temperatures were chosen for the PAA/DNI-3A film reaction, namely, 240, 260 and 280°C. The typical FTIR results were shown in Figs. 6a to 6c. The detail spectra for the polymers during the imidization were shown in Appendix C. The spectra changes were enhanced by subtracting the spectrum at t=0 from the spectrum collected at different times. The base line was offset by an arbitrary unit to display the negative side of the subtraction. The typical subtraction results were shown in Figs. 6d and 6e. The details of the resultant charts from subtraction are shown in Appendix D.
Fig. 5. (continued)
Fig. 5. (continued)
BECKMAN

WAVELENGTH IN MICROMETERS

1725 cm\(^{-1}\) for C=O vibration in imide group

1690 cm\(^{-1}\) for C=O vibration in amide group

1015 cm\(^{-1}\)

840 cm\(^{-1}\)

Fig. 6. FTIR absorbance for PAA/DNI-3A at (a) 240°C, t=20 min, (b) 260°C, t=10 min, and (c) 280°C, t=10 min, respectively, and the subtraction results for (d) [A(t=5min)-A(0)], and (e) [A(t=180min)-A(0)] at 280°C
Fig. 6. (continued)
Fig. 6. (continued)
In comparing the FTIR spectra from different samples, one should notice the thickness effect since different thickness cause different amount of peak intensity. From the literature the internal reference is chosen at 840 cm⁻¹ (C-H out-of-plane bending from p-substituted benzene) [22] or 1015 cm⁻¹ (C-H in-plane bending from p-substituted benzene) peak [23,24]. In this report the 1015 cm⁻¹ was chosen. (Indeed, both bands do not change much). With this reference peak the relative thickness was calibrated and the correct peak intensity was obtained.

4.3 FTIR Absorption Bands for PAA/DNI-3A and Polyimide

The characteristic bands of amide or imide is from its carbonyl vibration. The band at 1690 cm⁻¹ was assigned as the stretching vibration of the secondary amide. The 1640 cm⁻¹ peak is assigned to the tertiary amide. For imide, the peaks assigned are 1775 (1780), 1725, 1350 (1370), and 735 (720) cm⁻¹ [9,12,13,17,18,22-29] (see Table 2.) The increasing or decreasing of the aforementioned peaks during imidization was observed. But not every peaks can be quantitatively characterized due to the noise in the data. The most significant changes of the peaks are those of 1690 and 1725 cm⁻¹. The former one is an amide peak along the unreacted backbone while the latter one is associated with the resultant imide [30]

The comparison of the normalized data from increasing intensity of 1725 cm⁻¹ peak with that from the decreasing intensity of 1690 cm⁻¹ peak at 280°C is shown in Fig.7a. The good agreement between the increase of 1725 cm⁻¹ peak and the decrease of 1690 cm⁻¹ peak at 280°C suggested that there is no intermediate formed during the amide-imide conversion. Similar plots for 260°C and 240°C experiments are shown in Figs. 7b and 7c. The agreement between these two peaks were not that good at 240°C due to the noise effect on the relative small value of the denominator ΔA(0,τ). But they are still in the same range
Table 2. The assigned imide peaks in the literature

<table>
<thead>
<tr>
<th>Ref. No.</th>
<th>Absorption Peaks (cm(^{-1}))</th>
</tr>
</thead>
<tbody>
<tr>
<td>9.</td>
<td>720*, 1725, 1780 (* used for kinetics, ref. 995 for Aromatic ring vibration)</td>
</tr>
<tr>
<td>12.</td>
<td>725</td>
</tr>
<tr>
<td>13.</td>
<td>1380*, 1780 (recommended)</td>
</tr>
<tr>
<td>17.</td>
<td>1780</td>
</tr>
<tr>
<td>18.</td>
<td>725 (ref 1480 for aromatic structure)</td>
</tr>
<tr>
<td>22.</td>
<td>720, 1370, 1720, 1780 (ref. 820 for C-H)</td>
</tr>
<tr>
<td>23.</td>
<td>1720, 1780 (ref. 1012)</td>
</tr>
<tr>
<td>24.</td>
<td>725, 1380 (ref 1015 for aromatic ring vibr.)</td>
</tr>
<tr>
<td>25.</td>
<td>1380, 1780</td>
</tr>
<tr>
<td>26.</td>
<td>1380, 1720, 1780</td>
</tr>
<tr>
<td>27.</td>
<td>730, 1370*, 1780 (* recommended)</td>
</tr>
<tr>
<td>28.</td>
<td>700, 1776</td>
</tr>
<tr>
<td>29.</td>
<td>725, 1778 (ref 1480 for aromatic structure)</td>
</tr>
</tbody>
</table>
Fig. 7. Normalized absorption at increasing peak 1725 cm\(^{-1}\) and decreasing peak 1690 cm\(^{-1}\) for PAA/DNI-3A during imidization at (a) 280°C, (b) 260°C, and (c) 240°C
Fig. 7. (continued)

260°C normalized FTIR data

\[ \frac{\Delta A(0, \tau)}{\Delta A(0, \tau)} \]

Time (min)

\( \times \) 1725 cm\(^{-1}\)

\( \circ \) 1690 cm\(^{-1}\)

(b)
240°C normalized FTIR data

![Graph showing normalized FTIR data at 240°C. The x-axis represents time (min) ranging from 0 to 100, and the y-axis represents the change in absorbance, ΔA(0,t)/ΔA(0,τ). The graph includes data points for 1725 cm⁻¹ indicated by 'x' and 1690 cm⁻¹ indicated by 'o'.](image)

Fig. 7. (continued)
after the error from noise (±20%) is taken into account. It is worth noting that the imidization at these two temperatures for 4 hours is not complete.

4.4. \( \frac{[C]_t-[C]_\infty}{[C]_0-[C]_\infty} \) Concentration Ratio Analysis and Kinetic Parameters

As explained in Section 3.3, the kinetic data can be characterized by equations (6) or (7). At 280°C let \( \tau = 180 \) minutes. It was noticed that the imidization is very close to completion at 280°C for 180 minutes (this point will be verified in Section 4.5), i.e., \( A(180 \text{ min}) - A(\infty) \) at 280°C. From Beer's Law, the path-independent characteristic absorbance of any moiety for different specimen at any temperature \( T \) can be represented by the following equation:

\[
\Delta A(0,\infty)_{280^\circ C}/b_{280^\circ C} = \Delta A(0,\infty)_{T}/b_T
\]

or

\[
\Delta A(0,\infty)_T = \Delta A(0,\infty)_{280^\circ C} \times b_T/b_{280^\circ C}
\] (12)

where \( \Delta A(0,\infty)_{280^\circ C} \) is \( A(0) - A(\infty) \) at 280°C. The path (or thickness) ratio, \( b_T/b_{280^\circ C} \), can be calibrated by the absorbance of the internal reference peak at 1015 cm\(^{-1}\). [Note: This peak was not very obvious in the absorption spectrum, but can be readily detected in the computer "pick-peak" option.] In equation (12) the notation \( \infty \) can be interchanged with time \( \tau \) without losing any generality. This equation provides an easy way to calculate the corresponding value of \( \Delta A(0,\infty)_T \) for different specimen at temperature \( T \). The function \( \ln\left\{ \frac{([C]_t-[C]_\infty)/([C]_0-[C]_\infty)}{\Delta A(0,\infty)_{T}} \right\} \) (or \( \ln\left\{ \frac{[A(t)-A(\tau)]}{\Delta A(0,\infty)_{T}} \right\} \) with the understanding that \( \Delta A(0,\infty)_T \) comes from equation (12)) were plotted versus time. The results were shown in Figs.8a-8c for 1725 cm\(^{-1}\) and Figs.8d-8f for 1690 cm\(^{-1}\) at different temperatures. From the plots it is observed that there are two first order stages during the whole reaction process. The slopes of the curves, which were the (\( -k \)) values at that temperature, were calculated by the least square method. These \( k \) values are listed in Table 3.
Fig. 8. In \(\frac{([C]_t-[C]_o)}{([C]_o-[C]_t)}\) versus time for PAA/DNI-3A at 1725 cm\(^{-1}\) at (a) 240°C, (b) 260°C, and (c) 280°C, and at 1690 cm\(^{-1}\) at (d) 240°C, (e) 260°C, and (f) 280°C.

\[
\begin{align*}
\ln \left(\frac{([C]_t-[C]_o)}{([C]_o-[C]_t)}\right) &= k_1 \text{ min}^{-1} \\
k_1 &= 5.20 \times 10^{-3} \text{ min}^{-1} \\
k_2 &= 9.63 \times 10^{-4} \text{ min}^{-1}
\end{align*}
\]
260°C, 1725cm⁻¹, PAA/DNI-3A (iv=1.0)

Fig. 8. (continued)

\[
\ln \left( \frac{\left[ C^\prime \right]}{[C]} \right) = \ln \left( \frac{\left[ C_0 \right] - [C]}{[C]} \right)
\]

\[
k_1 = 2.27 \times 10^{-2} \text{ min}^{-1}
\]

\[
k_2 = 7.36 \times 10^{-3} \text{ min}^{-1}
\]
280°C, 1725 cm⁻¹, PAA/DNI-3A (iv=1.0)

$$k_1 = 4.648 \times 10^{-2} \text{ min}^{-1}$$

$$k_2 = 2.388 \times 10^{-2} \text{ min}^{-1}$$

Fig. 8. (continued)
240°C, 1690 cm$^{-1}$, PAA/DNI-3A ($\nu v=1.0$)

![Graph]

$k_1=3.52E^{-3}$ min$^{-1}$

$k_2=8.1E^{-4}$ min$^{-1}$

Fig. 8. (continued)
260°C, 1690 cm⁻¹, PAA/DNI-3A (iv=1.0)

\[ \ln \left( \frac{[C_i]_0 - [C_i]}{[C_0] - [C_p]} \right) \]

- Time (min)
- \[ k_1 = 2.162 \times 10^{-2} \text{ min}^{-1} \]
- \[ k_2 = 4.509 \times 10^{-3} \text{ min}^{-1} \]

Fig. 8. (continued)
280°C, 1690 cm⁻¹, PAA/DNI-3A (iv=1.0)

\[ \ln \left( \frac{[\text{Cl}]}{[\text{Cl}]} \right) \]

\[ k_1 = 4.826 \times 10^{-2} \text{ min}^{-1} \]
\[ k_2 = 2.566 \times 10^{-2} \text{ min}^{-1} \]

Fig. 8. (continued)
Table 3. The kinetic parameters of imidization from ([Cl]_t-[Cl]_f)/([Cl]_0-[Cl]_f) data

(a) at 1725 cm\(^{-1}\)

<table>
<thead>
<tr>
<th></th>
<th>(k_1) (min(^{-1}))</th>
<th></th>
<th>(k_2) (min(^{-1}))</th>
</tr>
</thead>
<tbody>
<tr>
<td>280°C</td>
<td>4.684E-2</td>
<td>280°C</td>
<td>2.388E-2</td>
</tr>
<tr>
<td>260°C</td>
<td>2.27E-2</td>
<td>260°C</td>
<td>7.36E-3</td>
</tr>
<tr>
<td>240°C</td>
<td>5.20E-3</td>
<td>240°C</td>
<td>9.63E-4</td>
</tr>
</tbody>
</table>

(b) at 1690 cm\(^{-1}\)

<table>
<thead>
<tr>
<th></th>
<th>(k_1) (min(^{-1}))</th>
<th></th>
<th>(k_2) (min(^{-1}))</th>
</tr>
</thead>
<tbody>
<tr>
<td>280°C</td>
<td>4.826E-2</td>
<td>280°C</td>
<td>2.566E-2</td>
</tr>
<tr>
<td>260°C</td>
<td>2.162E-2</td>
<td>260°C</td>
<td>4.51E-3</td>
</tr>
<tr>
<td>240°C</td>
<td>3.52E-3</td>
<td>240°C</td>
<td>8.11E-4</td>
</tr>
</tbody>
</table>
4.5 ΔA Absorbance Difference Analysis and Kinetic Parameters

The above analysis based on concentration ratio data, ([C]t-[C]r)/([C]0-[C]r), is subject to error in calculating the kinetic data k values because of the possible non-zero value of [C]r as mentioned in Section 3.3. The data were following the absorbance difference, ΔA, analysis mentioned in Section 3.4. Since the initial data set was not in equally spaced time basis, the interpolation of the data is required. There are two ways to interpolate the data, direct and indirect. The direct interpolation simply was done from the original data set while the indirect way would be done after some massage of the original data. It is noted that the raw data shown in Figs.8a-f are not smoothly distributed. When the equally spaced time data were directly interpolated from these scattered data, the logarithm of the difference, ln[ΔA(t1,t2)], for each pair of data will become very scattering. Significant error will be generated by this way of data treatment. It is this sensitivity that the indirect way, the least-square-fitted curves in Figs.8a-f, were used to interpolate the equally spaced time data for the ΔA/[A(τ)-A(0)] readings. The ΔA data were then obtained by multiplying [A(τ)-A(0)] with the interpolation values. After this conversion the ΔA values really represent the true difference between any two different times no matter how the ([C]t-[C]r)/([C]0-[C]r) data were distorted from the true first-order one by the non-zero [C]t value since the ([C]0-[C]r) values do not play any role in the ΔA terms. In principle, this is just the interpolation of [C]t or A(c,t) value, nothing to do with [C]r value. Recall that, from Section 3.4,

\[
\ln \Delta A(t_1, t_2) = \ln k' - k t_1 + \ln \left\{ 1 - e^{-k(t_1 - t_2)} \right\} = k'' - k t_1
\]  

(11)

The Δt=t1-t2=5 minute in the fast reaction period and Δt=t1-t2=10 minutes in the slow reaction period were then taken for ΔA readings. The results of [ln ΔA] verse t1, based on
equation (11), were plotted and shown in Figs. 9a-9c for 1725 cm\(^{-1}\) and Figs. 9d-9f for 1690 cm\(^{-1}\) band. From each curves the slopes, i.e., the (-k) values, was computed by the least square method. The resultant k values are listed in Table 4.

From this Table it is clear that the corresponding k values derived from the concentration ratio, \((\lbrack C \rbrack_t - \lbrack C \rbrack_0)/ (\lbrack C \rbrack_0 - \lbrack C \rbrack_t)\), method and from fixed-time-interval data, \(\Delta A\), method are very close (within 2%). This implies that the \(\tau (=180 \text{ min}) \sim \infty\) assumption is reasonable and that \(\lbrack C \rbrack_t\) is indeed close to zero. Besides, by using the k values obtained from 280°C to back calculate the degree of conversion, \([\lbrack C \rbrack_{t=180 \text{ min}}\) is only 1% of \([\lbrack C \rbrack_0\). (Please note that this value is calculated from the 1725 cm\(^{-1}\) data. If the calculation is based on the 1690 cm\(^{-1}\) data, \([\lbrack C \rbrack_{t=180 \text{ min}}\) is about 0.8% of \([\lbrack C \rbrack_0\). In doing such calculation, the transition from \(k_1\) to \(k_2\) is set at time equal to 12 minutes as shown in Figs. 8 and 13.) Using the 1725 cm\(^{-1}\) data and the same calculation techniques, the corresponding time for the residue concentration, \([\lbrack C \rbrack_t\), to reach 1% of \([\lbrack C \rbrack_0\) is about 20 hours at 260°C and 80 hours at 240°C, respectively.

From the k values at different temperatures the Arrhenius plot can be employed to compute the activation energy and pre-exponent constant. Figs. 10a and 10b and Table 4 show the results. It is noticed from the results that the activation energy is about 34±3 Kcal/mole for the fast reaction and 48±2 Kcal/mole for the slow reaction. Compared to the data from literature, the two values of activation energy are much higher, and the overall reaction constant, k, at the same temperature are quite different. However, the literature data are mostly the ring closure of amic ester while the reaction being studied in this report was amic amide.

A comparison of the k values for slow reactions between the current PAA/DNI-3A system and the PMR-15 system is given in Fig. 11. Although the fast reaction constants were not
Fig. 9. In ΔA versus time for PAA/DNI-3A at 1725 cm\(^{-1}\) at (a) 240°C, (b) 260°C, and (c) 280°C, and at 1690 cm\(^{-1}\) at (d) 240°C, (e) 260°C, and (f) 280°C.
260°C, 1725cm⁻¹

\[ k_1 = 2.106 \times 10^{-2} \text{ min}^{-1} \]
\[ k_2 = 7.362 \times 10^{-3} \text{ min}^{-1} \]

![Graph showing reaction kinetics](image)

Fig. 9. (continued)
Fig. 9. (continued)

\[
280, 1725 \text{ cm}^{-1}
\]

\[
\ln \Delta A(t_{1},t_{2})
\]

\[
\begin{align*}
k_1 &= 4.624 \times 10^{-2} \text{ min}^{-1} \\
k_2 &= 2.411 \times 10^{-2} \text{ min}^{-1}
\end{align*}
\]

\[
\begin{array}{c}
0 & 20 & 40 & 60 & 80 \\
\hline
-5 & -4 & -3 & -2
\end{array}
\]

\[
\text{Time (} t_1 \text{) (min)}
\]
Fig. 9. (continued)

240°C, 1690 cm−1

\[ \ln \Delta A(t_1|t_2) \]

\[ k_1 = 3.58 \times 10^{-3} \text{ min}^{-1} \]
\[ k_2 = 8.00 \times 10^{-4} \text{ min}^{-1} \]
260°C, 1690 cm⁻¹

\[ k_1 = 2.17 \times 10^{-2} \text{ min}^{-1} \]
\[ k_2 = 4.53 \times 10^{-3} \text{ min}^{-1} \]

Fig. 9. (continued)
Fig. 9. (continued)

280,1690 cm\(^{-1}\)

\[
k_1 = 4.744 \times 10^{-2} \text{ min}^{-1}
\]

\[
k_2 = 2.563 \times 10^{-2} \text{ min}^{-1}
\]
Table 4. The kinetic parameters of imidization from ΔA data

(a) at 1725 cm⁻¹

<table>
<thead>
<tr>
<th></th>
<th>k₁ (min⁻¹)</th>
<th>k₂ (min⁻¹)</th>
</tr>
</thead>
<tbody>
<tr>
<td>280°C</td>
<td>4.624E-2</td>
<td>2.411E-2</td>
</tr>
<tr>
<td>260°C</td>
<td>2.106E-2</td>
<td>7.362E-3</td>
</tr>
<tr>
<td>240°C</td>
<td>5.34E-3</td>
<td>9.50E-4</td>
</tr>
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</table>

K₀ = 5.75 E10, E₁ = 31 Kcal/mole

(b) at 1690 cm⁻¹

<table>
<thead>
<tr>
<th></th>
<th>k₁ (min⁻¹)</th>
<th>k₂ (min⁻¹)</th>
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<td>280°C</td>
<td>4.744E-2</td>
<td>2.563E-2</td>
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<td>260°C</td>
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<td>4.53E-3</td>
</tr>
<tr>
<td>240°C</td>
<td>3.58E-3</td>
<td>8.00E-4</td>
</tr>
</tbody>
</table>

K₀ = 1.57 E13, E₁ = 37 Kcal/mole

K₀ = 4.72 E10, E₂ = 49 Kcal/mole
Fig. 10. Arrhenius plot for imidization of PAA/DNI-3A at (a) 1725 cm$^{-1}$ and (b) 1690 cm$^{-1}$.
Comparison of PAA/DNI-3A and PMR-15

Fig. 11. Comparison of Arrhenius plot for imidization of PAA/DNI-3A and PMR-15
shown in the same report, the author [15] did point out that the fast reaction constants should be one to three orders of magnitude larger than the rate constants of the slower reaction. This large difference of rate constants did not happen in the PAA/DNI-3A systems since the reaction kinetics was controlled by the system viscosity and the viscosity change during the solid state processing for PAA/DNI-3A is not very significant compared to the PMR systems. Furthermore, from Fig.11, it shows that for the PAA/DNI-3A system the k curves have steeper slopes and are located in the higher temperature range for similar k values than for the PMR systems. This means that the PAA/DNI-3A systems have much smaller processing window and also only in a shorter higher temperature range can the reaction occur in a reasonable rate.

4.6 The TICA Results and Correlation with the Two Kinetic Rates

The TICA experiments were conducted with RDS in both cure mode and isothermal scans. The results are shown in Figs.12a-12c. The cure scan illustrated that the material began to soften at about 200°C and the softening rate is very slow. At 250°C the viscosity reached the minimum and increased again due to additional reaction. The softening window was very narrow.

The isothermal scans were conducted at 280 and 240°C respectively. The moduli curves from both temperature scans showed the typical softening at the beginning, followed by the vitrification process. The FTIR kinetic results showed that there were two reaction rates associated with the ring closure reaction, a fast reaction (k₁) at the beginning followed by a slower rate (k₂). Clearly, this change in rate was related to the rheology of the material. When the material was in the softening stage, the reaction proceeded according to rate k₁. After the system vitrified, the glassy state rheology slowed down the conversion rate, and the remaining conversion proceeded according to rate k₂.
Fig. 12. TGA spectra of PAAADNI-3A for (a) temperature scan, and (b) isothermal scan at 240 °C, and (c) isothermal scan at 280 °C.
To illustrate the relationship between the softening and the reaction rates, the TICA and FTIR data were replotted in Fig. 13. It is very clear that the fast reaction is associated with the softening region. After the material vitrified at time $t=12$ minutes, the reaction rate assumed the $k_2$ value.
Processing Consideration of In-Situ Rod Formation

(a) TICA rheology

(b) kinetics from IR

TICA, 280°C Isothermal Scan

\[ G' \text{ (arbitrary unit)} \]

Time (min)

280°C, 1690 cm⁻¹, PAA/DNI-3A (lβ=1.0)

\[ \ln \left( \frac{[c]_0 - [c]}{[c]_0} \right) \]

Time (min)

k₁ = 4.626E-2 min⁻¹
k₂ = 2.566E-2 min⁻¹

Fig. 13. Relationship between softening and reaction rate for PAA/DNI-3A
SECTION 5

SUMMARY

The rod conversion kinetics of the PPA/DNI-3A system was studied using the FTIR. Analysis of the isothermal 280°C FTIR data showed a nice correlation between the disappearance of amic amide and the formation of imide, indicating a direct conversion without intermediate. The activation energy obtained for the poly(amic amide) was substantially higher than the literature value of amic esters. The isothermal results showed that the conversion proceeded initially according to a fast reaction rate $k_1$ and slowed to a different reaction rate $k_2$ later. The crossover point between $k_1$ and $k_2$ corresponds nicely with the vitrification time of the rheology measurement. This proves that the conversion rate and possibly the degree of conversion, is rheologically controlled.

This study defined the kinetic parameters of the rod conversion reaction at the beginning of the reaction. The effect of the crosslinking chemistry was not studied. The cracking of the nadic end group into cyclopentadiene presented a complication in the study of the crosslinking effect. The cyclopentadiene evolution temperature range overlapped with the rod conversion reaction range. Another crosslinking chemistry will be more suitable to study the crosslinking effect on rod conversion.
REFERENCES


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APPENDIX A

Illustrated examples for kinetic data calculation from Sections 3(c) and 3(d)
Example 1. For a first order reaction, \( [c]_t = [c]_0 \exp(-t/100) \) then \( k=0.01 \), the \([c]\) values at different time \( t \) are listed in the following table.

<table>
<thead>
<tr>
<th>time (min)</th>
<th>([c]_t/[c]_0)</th>
</tr>
</thead>
<tbody>
<tr>
<td>0</td>
<td>1.00</td>
</tr>
<tr>
<td>5</td>
<td>0.95123</td>
</tr>
<tr>
<td>10</td>
<td>0.90484</td>
</tr>
<tr>
<td>15</td>
<td>0.86071</td>
</tr>
<tr>
<td>...</td>
<td></td>
</tr>
<tr>
<td>120</td>
<td>0.30119</td>
</tr>
<tr>
<td>180</td>
<td>0.16530</td>
</tr>
</tbody>
</table>

If the data were analyzed by assuming \( [c]_t \) at \( t=120 \) min to be zero (\([c]_{120}=0\)) and apply equation (10) to get the \( k \) value the error is about 70% (\( k=0.017 \)), if \([c]_{180}\) is assumed to be zero the error is reduced to 50% (\( k=0.015 \)). Because of other complication in solid state reaction like diffusion controlled quenching of the reaction, it is difficult to determine if \([c]_t\) is indeed zero. That is the motive to develop the approach for evaluating the \( k \) values, in which whether \( t \) is equal to infinity or not is not involved at all.

The same example is used to demonstrate the application of this approach as follows.
Example 2.

For the same first order reaction \[ [c]_t = [c]_0 \exp(-t/100) \], assume \( a_c b = 1 \). Then

\[ A_c(t) = a_c b [c]_t = [c]_t \]

and

\[ \Delta A(t_1, t_2) = \Delta A_c(t_1, t_2) = [c]_{t_1} - [c]_{t_2} = \Delta[c] \]

The concentration, concentration difference and its logarithm values are listed in the following table.

<table>
<thead>
<tr>
<th>time (min)</th>
<th>([c]_0 / [c]_0)</th>
<th>(\Delta[c] / [c]_0)</th>
<th>(\ln \Delta[c] / [c]_0)</th>
</tr>
</thead>
<tbody>
<tr>
<td>0</td>
<td>1.00</td>
<td>0.049</td>
<td>-3.021</td>
</tr>
<tr>
<td>5</td>
<td>0.95123</td>
<td>0.046</td>
<td>-3.071</td>
</tr>
<tr>
<td>10</td>
<td>0.90484</td>
<td>0.044</td>
<td>-3.121</td>
</tr>
<tr>
<td>15</td>
<td>0.86071</td>
<td></td>
<td></td>
</tr>
<tr>
<td>...</td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>120</td>
<td>0.30119</td>
<td></td>
<td></td>
</tr>
<tr>
<td>180</td>
<td>0.16530</td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

After plotting \((\ln \Delta[c] / [c]_0)\) or \((\ln \Delta A(t_1, t_2))\) verse time \(t_1\), the slope was found to be exactly equal to the true \(k\) value, 0.01.

Two things have to be emphasize. Firstly, it is ploted of \((\ln \Delta[c] / [c]_0)\) or \((\ln \Delta A(t_1, t_2))\) verse \(t_1\), not verse other \(t\). Secondly, it has to be equally spaced data used. Non equally spaced data do not fit equation (12). This technique is very useful for analyzing FTIR spectra. No infrared absorbance due to the unidentified background or the initial product is involved here. With the data treatment shown in this approach the correct kinetic data \(k\) can then be obtained.
APPENDIX B

The Report of TGA/MS Results of PAA/DNI-3A and DNI-3A Systems from SRL.
8 August 1989

In Reply Reference: 5556

Wright Research and Development Center
Materials Laboratory
WRDC/MLBP (Attn: Lisa R. Denny)
Wright-Patterson Air Force Base, OH 45433-6533

SUBJECT: Analysis of Sample LST-70359-44A

1. Initial Weight 4.3 mg
   Weight Loss (950°C) 2.8 mg (65%)

2. The temperature dependence of the total-ionization current is shown in Fig. 93. The behavior of dW/dT provides no information due to noise in the data. This is the fifth sample in this series where dW/dT data are poor (c.f., LST-70357-19A, LST-70359-5A, -13A, -13B). One possible explanation is swinging of the sample which is induced by the rapid loss of C₅H₆. The overall weight loss in this sample falls in the range (51 - 68%) established from the previous three samples.

   Two major maxima in the total-ionization profile occur at 230 and 370 °C; these are essentially as observed for Sample LST-70357-19A.

3. At temperatures below 230°C, only traces of products are observed. Three profiles can be discerned; however, the low abundance of these products precludes assignment. The peak in the total-ionization current at 230°C arises from the release of C₅H₆ as the product of the retro-Diels Alder reaction. No other products are released in this temperature region.
4. The next volatile product arises from the imidization process. The rate of its production maximizes at 370°C and accounts for the second peak in the total-ionization spectrum. Although it is not possible to make positive identification of the structure, it can be said that it is a complex secondary amine. The highest mass ion observed is at m/e 189; the largest major ion is at m/e 138 and is tentatively assigned as

$$C_3H_6NC_3H_5N=C=0$$

Since no other volatiles of any magnitude are seen following the retro-Diels Alder reaction prior to the imidization, it is possible that the amine cyclizes prior to undergoing the imidization. No molecular ion is observed corresponding to the nominal mass of the diamine expected from the retro-Diels Alder reaction. Since all ions in this region have the same temperature dependence, it is concluded that a single secondary amine is being observed which is not degraded thermally but by electron impact during detection.

5. Other identified products (thermal degradation) include CO, CH₄, H₂, HCN, and tetramethyl-substituted biphenyl.

6. The temperature dependence of the identified products is shown in Figs. 94 and 95.

Very truly yours,

SYSTEMS RESEARCH LABORATORIES, INC.
A Division of Arvin/Calspan

E. Grant Jones, Ph.D.
Senior Chemist
Research Applications Division

EGJ:mw
Fig 94
Sample LST 70359-444A
G. Jones
Aug 8/89
15 August 1989

In Reply Reference: 5556

Wright Research and Development Center
Materials Laboratory
WRDC/MLBP (Attn: Lisa R. Denny)
Wright-Patterson Air Force Base, OH 45433-6533

SUBJECT: Analysis of Sample LST-70357-14A

1. Initial Weight 5.8 mg  Weight Loss 5.7 mg  (98%)

2. The temperature dependence of dW/dT and total-ionization current is shown in Fig. 101. The extent of weight loss and the profiles in Fig. 101 indicate that the entire sample is consumed either by degrading to produce volatiles or by sublimation of the original sample prior to thermal degradation.

3. The expected major low-temperature product, C₅H₆ from the retro-Diels Alder reaction, is several times smaller than was observed in Sample LST-70359-44A. When it is realized that the current sample has the potential to release much more C₅H₆, it becomes apparent that sublimation of the original sample is competing with C₅H₆ production and, in fact, dominates. The temperature dependence of C₅H₆, shown in Fig. 102, displays a maximum at 220°C which is about 10 deg. below the corresponding maximum from Sample LST-70359-44A. This illustrates the truncation of the retro-Diels Alder reaction due to sample loss. This process appears as a high-temperature satellite maximum in the total-ionization profile (c.f., Fig. 101).
4. The major volatile products observed from this sample are unrelated to the sample per se. The largest product is unreacted reagent $C_9H_8O_3$, accounting for the large peak in the total-ionization profile. The low-temperature region around 90 and 140°C is dominated by the solvent chloroform $CHCl_3$. This observation is surprising since the solvent reported for the original preparation was $CH_3Cl$.

5. At 230°C approximately 90% of the original sample weight has been lost. Analysis of volatiles at higher temperature is questionable. The profile of m/e 138 is shown in Fig. 103; this was previously ascribed (Sample No. LST-70359-44A) to the $S$-amine released during cyclization.

6. Over the same temperature region, a broad release occurs, accounting for the maximum in the total-ionization and dW/dT temperature profiles around 420°C. Possibly significant is the fact that this unidentified product was also observed in the companion sample (unidentified) over a narrower range.

7. It should be pointed out that for small non-polymeric systems where sublimation commonly occurs, it is important that reagents and other contaminants be removed because of their increased significance compared to the products released in reduced abundance due to competition with sublimation, i.e., a cleaner sample may improve the chances of identifying the cured products.

Very truly yours,

SYSTEMS RESEARCH LABORATORIES, INC.
A Division of Arvin/Calspan

E. Grant Jones, Ph.D.
Senior Chemist
Research Applications Division

EGJ:mw
Fig 101

Sample LST-70357-14A
G. Jomo
Aug 15/89

TOTAL ION INTENSITY

DW/DT

TEMPERATURE (°C)
Figure 102
Sample LS7-70357-14A
G. Swa
A-2 15/89
APPENDIX C

Absorption Spectra from FTIR for PAA/DNI-3A
t=0 min. @240°C
t = 10 min. @ 240°C
t=60 min. @280°C
APPENDIX D

Subtraction Spectra from FTIR for PAA/DNI-3A
BECKMAN

WAVELENGTH IN MICROMETERS

4,000  3,600  3,200  2,800  2,400

2.5  2.6  2.7  2.8  2.9  3.0  3.1  3.2  3.3  3.4  3.5

3.5  6.25  8.33  12.5  25

t = 90 - 0 min. @ 240°C
t = 15 - 0 min. @ 260°C
t = 20 - 0 min. @ 260°C
t=30 -0 min. @260°C
t=60 - 0 min. @260°C
t=15 - 0 min. @280°C
BECKMAN

WAVELENGTH IN MICROMETERS

WAVENUMBER CM⁻¹

2.0  2.2  2.4  2.6  2.8  3.0  3.2  3.4  3.6  3.8  4.0
4000 3600 3200 2800 2400 2000 1600 1200 800 400

2.0  2.2  2.4  2.6  2.8  3.0  3.2  3.4  3.6  3.8  4.0
4.0  3.8  3.6  3.4  3.2  3.0  2.8  2.6  2.4  2.2  2.0

t=30 - 0 min. @280°C
BECKMAN

WAVELENGTH IN MICROMETERS

4.0  3.8  3.6  3.4  3.2  3.0  2.8  2.6  2.4  2.2  2.0

2.73  2.77  3.57  5  6.25  8.33  12.5  25

ABSORPTION UNITS

WAVENUMBER CM⁻¹

t = 40 - 0 min. @280°C
BECKMAN

WAVELENGTH IN MICROMETERS

4.0  2.778  3.571  5  6.25  8.333  12.5  25
2.273

RESIDENCE UNITS

4.0  3.8  3.6  3.4  3.2  3.0  2.8  2.6  2.4  2.2  2.0
4400 3600 2800 2000 1600 1200 800 400

WAVENUMBER CM\(^{-1}\)

t = 90 - 0 min. @280°C
t = 180 - 0 min. @ 280°C