MASS TRANSFER AND FIRST-ORDER BOUNDARY-LAYER EFFECTS ON SHARP CONE DRAG

Clark H. Lewis, Ernest O. Marchand, and Herbert R. Little
ARO, Inc.

March 1966

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ON SHARP CONE DRAG

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FOREWORD

The work reported herein was done at the request of Headquarters, Arnold Engineering Development Center (AEDC), Air Force Systems Command (AFSC), under Program Element 62405334, Project 8953, Task 895303.

The results presented were obtained by ARO, Inc. (a subsidiary of Sverdrup and Parcel, Inc.), contract operator of the AEDC, AFSC, Arnold Air Force Station, Tennessee, under Contract AF40(600)-1200. The research was conducted under ARO Project No. VW3507, and the manuscript was submitted for publication on January 27, 1966.

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This technical report has been reviewed and is approved.

Larry R. Walter
1st Lieutenant, USAF
Gas Dynamics Division
DCS/Research

Donald R. Eastman, Jr.
DCS/Research
ABSTRACT

A theoretical model is developed based on an iterated perfect gas inviscid-viscous flow field which includes first-order displacement (viscous interaction), transverse curvature, wall slip, and temperature jump in addition to mass transfer effects. The effects of inviscid (tangent cone) and viscous (nonsimilar laminar boundary layer) flow field matching conditions are also considered. Numerical results are compared with experimental and analytical results of King and Talbot (AIAA J., 1964) for a 5-deg half-angle cone at $M_\infty = 3.93$ and 5.64. The predicted viscous-induced pressure without mass transfer and the zero-lift drag with and without injection were in agreement with the experimental data within experimental uncertainty. The theoretical model was also used to predict zero-lift drag of a 9-deg half-angle cone at $M_\infty = 9.37$ and 10 and $Re_\infty/in. = 400$ to 45,000 for a range of wall-to-stagnation temperature ratios. Again, in general, without mass transfer the predictions were within experimental uncertainty. The inability of the theoretical model to adequately treat nonuniform mass transfer distributions is discussed. At the lowest Reynolds number the effects of slip were most significant. At all conditions the effects of inviscid-viscous flow field matching were significant. Experimental zero injection equilibrium wall temperature distributions and cool-wall pressure data are given at $M_\infty = 10$ and $Re_\infty/in. = 400$ to 2600.
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NOMENCLATURE

\begin{align*}
A_B & \quad \text{Base area} \\
A_w & \quad \text{Surface area} \\
C_{D_f} & \quad \text{Skin-friction drag coefficient referenced to base area} \\
C_{D_p} & \quad \text{Pressure drag coefficient} \\
C_f & \quad \text{Local skin-friction coefficient, } 2r_w/\rho u^2 \\
C_m & \quad \text{Constant of proportionality in linear viscosity law,} \\
& \quad (T_\infty/T_w)(\mu_w/\mu_\infty) \\
f' & \quad \text{Velocity ratio, } u/u_e \\
g & \quad \text{Stagnation enthalpy ratio, } H/H_e \\
H & \quad \text{Stagnation enthalpy} \\
h & \quad \text{Static enthalpy} \\
h_{\text{ref}} & \quad \text{Reference enthalpy (}2.119 \times 10^8 \text{ ft}^2/\text{sec}^3) \\
L & \quad \text{Slant cone length} \\
\ell & \quad \text{Axial length} \\
M & \quad \text{Mach number} \\
\dot{m} & \quad \text{Mass transfer rate} \\
Pr & \quad \text{Prandtl number} \\
p & \quad \text{Static pressure} \\
p'_n & \quad \text{Normal shock stagnation (pitot) pressure} \\
q & \quad \text{Heat-transfer rate} \\
R & \quad \text{Gas constant} \\
\end{align*}
Reynolds number
Radius normal to axis of symmetry
Base radius
Effective wall radius, \( r_e(x) + \cos \theta_c \delta^* (n-1) \)
Stanton number, \( q/\rho u (H_0 - H_w) \)
Temperature, °K
Wall thickness
Tangential velocity component
Normal velocity component
Hypersonic viscous parameter, \( M_\infty \left( C_\infty / Re_\infty \right)^{1/2} \)
Surface distance measured from cone tip
Origin of continuum boundary layer plus slip and temperature jump
Distance normal to the surface
Axial distance measured from cone tip
Ratio of specific heats
Boundary-layer thickness (where \( u/u_e = 0.995 \))
Boundary-layer displacement thickness
Transformed coordinate normal to the wall, \( \left( u_e L/\rho_* \mu_* x \right)^{1/2} \int \rho \ dy \)
Cone half-angle
Mean free path
Viscosity
Mass density
Shear stress

**SUBSCRIPTS**

c: Corrected pressure
e: Local inviscid conditions at the "edge" of the boundary layer
i: Initial location of continuum boundary layer with slip
inv: Inviscid conditions without wall boundary layer
m  Measured pressure

0  Free-stream stagnation conditions

w  Wall conditions

∞  Free-stream conditions

*  Reference conditions at inviscid sharp cone conditions

SUPERSSCRIPTS

(n)  Iteration index corresponding to the pressure distribution over the "effective" body \( r_{ef}^{(n)} = r_w + \cos \theta_c \delta^{*(n-1)} \). Zero denotes the inviscid sharp cone edge conditions. Iteration with slip is denoted \((ns + js)\) where \(n\) is no-slip and \(j\) is slip iteration number.

Differentiation with respect to the transformed variable \( \eta \)
SECTION I
INTRODUCTION

For several years viscous effects on sharp and blunt slender cones have been studied in the Arnold Engineering Development Center, von Kármán Gas Dynamics Facility (Refs. 1-3). The large viscous-induced drag increment at zero-lift observed in these studies encouraged Whitfield and Griffith (Ref. 2) to consider the effects of mass transfer to reduce the drag. They experimentally investigated the effects of tangential injection of gases on zero-lift drag at $M_a = 10$ and 21. The experimental investigations have recently been extended by Little and Griffith (Ref. 4) to include the effects of normal injection on zero-lift drag at $M_a = 10$. The present report presents an analysis of some of the latter experimental results after developing a theoretical model and making comparisons with some experimental and theoretical data at supersonic conditions.

King and Talbot (Refs. 5 and 6) studied the effects of normal gas injection on the pressure distributions and zero-lift drag of a sharp 5-deg half-angle cone in the Berkeley Low Density Wind Tunnel. Experimental data were taken at near adiabatic wall conditions ($T_w/T_0 = 0.96$) and $Re_{\infty}/\text{in.} = 1765$ and 6286 at $M_a = 3.93$ and 5.64, respectively. They gave an analysis based on approximate methods which is described in more detail below. The experimental and theoretical data of King and Talbot are compared with the results from methods developed in the present report.

King and Talbot (Ref. 6) and Little and Griffith (Ref. 4) obtained experimental data for binary boundary layers with injected gases other than the test gases (air and nitrogen) used in the wind tunnel experiments. For example, the latter investigators also used helium, argon, and carbon dioxide as injected gases. In the present report, however, only the cases of injection of air into air or nitrogen into air or nitrogen will be considered.

The experimental drag data of Little and Griffith were taken with a partially porous 9-deg half-angle cone at $M_a = 9.37$ and 10 and for a span of Reynolds numbers $Re_{\infty}/\text{in.} = 388$ to 42,640. The estimated range of wall-to-stagnation temperature ratios was from 0.2 to 0.75. Quite recently some experimental data were obtained on the equilibrium wall temperature variation over a hollow cone in the AEDC-VKF low density tunnel (Gas Dynamic Wind Tunnel, Hypersonic (L)), and the pressure was measured on a sharp, water-cooled cone at $Re_{\infty}/\text{in.} = 388$, 1602, and 2606 in the same wind tunnel. These recent experimental data are also included in this report.
Under certain experimental conditions the effects of slip and temperature jump were significant, and the present analysis presents an approximate treatment of those effects on pressure and heat-transfer distributions and zero-lift drag. The effects of slip were considered significant upon comparison of the experimental results with the numerical results of the present investigation when slip and temperature jump effects were neglected.

Before further considering the theoretical model used in the present report, the experimental conditions which were studied will be presented.

SECTION II
EXPERIMENTAL CONDITIONS STUDIED

2.1 WIND TUNNELS

The experimental data used in the present study were obtained at Berkeley by King and Talbot (Refs. 5 and 6) and at the AEDC-VKF by Little and Griffith (Ref. 4). Some details concerning their experimental investigations are given in this section for the convenience of the reader.

Three wind tunnels were used in the experimental studies: viz. the low density wind tunnel at Berkeley and two AEDC-VKF Mach 10 tunnels (Gas Dynamic Wind Tunnels, Hypersonic (C) and (L)). The Berkeley tunnel is an unheated air, continuous flow, free jet facility using axisymmetric contoured nozzles to produce Mach numbers of 3.93 and 5.64. Tunnel C is a continuous flow, hypersonic wind tunnel. Air, heated to a temperature sufficient to avoid liquefaction, expands through a contoured, axisymmetric nozzle to the 50-in.-diameter test section. The free-stream Reynolds number was varied by changing the free-stream stagnation (reservoir) pressure. Tunnel L is an arc-heated, continuous flow facility using interchangeable axisymmetric contoured nozzles to produce nominal Mach 10 flow. Nitrogen was used as the test gas.

The flow conditions from the experimental investigations which are considered in the present report are given in Table I. The experimental conditions are given in the first row, and the data used in the numerical calculations are given in the second row. For most cases the perfect gas data for the numerical calculations were based on the measured free-stream pitot pressure and (equilibrium) free-stream stagnation temperature. The equilibrium stagnation enthalpy was then determined, and the ideal gas ($\gamma = 1.4$) stagnation temperature was computed. Ideal gas, normal shock, and one-dimensional, isentropic flow
relations were then used to obtain the free-stream and reservoir conditions. This procedure gave an ideal gas stagnation temperature somewhat higher than the corresponding equilibrium value, and this also produced other differences as shown in Table I.

2.2 MODELS

The force models used for the experimental studies were sharp cones with partially porous surfaces. King's models were 5-deg half-angle cones with small solid base and tip regions (Fig. 1a). The porous material was sintered, powdered, Monel® metal particles. An experimentally determined mass flux distribution is shown in Fig. 2. King states that the distribution of mass flux represents a circumferential average and should be regarded as qualitative rather than quantitative. Surface pressure data were taken with mass injection, but since the porous surface near the taps was distorted the pressure data were affected. Therefore, the only experimental pressure data of King and Talbot used in the present report were taken on solid (no injection) cone models.

The AEDC-VKF force model was a sharp, 9-deg half-angle cone with a base diameter of 0.75-in. (Fig. 1b). The solid nose was followed by a porous afterbody machined from General Electric 50-percent dense nickel Foametal®. The impervious nose extended over 0.57 of the (slant) length of the cone. Over the remainder of the cone, however, the constant density and thickness of the wall gave a mass flux distribution constant within ±15 percent as obtained from a hot-wire anemometer survey. Figure 2 also shows a typical mass flux distribution for the AEDC-VKF model.

The zero injection drag data were taken after the model had been in the flow a sufficient time to reach approximately 90 percent of the equilibrium wall temperature (as indicated from changes in measured drag data). Although no experimental wall temperature data exist for the force model, the values quoted below for a hollow stainless steel model are believed representative for the zero-injection drag data as well.

The pressure was measured at two locations on a water-cooled copper model (Fig. 1c) in Tunnel L. The thin copper wall was cooled to the water temperature (~ 295°K), and the temperature was assumed to remain constant over the entire surface.

The wall temperature was measured with a thin-wall (t ≤ 0.010 in.) stainless steel model as shown in Fig. 1d. The output of thermocouples
welded to the inside surface of the model was recorded as a function of time. Wall temperatures reached 90 percent of the equilibrium value within one to three minutes, and equilibrium was reached within about ten minutes.

2.3 EXPERIMENTAL DATA AND PRECISION

The primary test measurements were axial force and surface pressures in the Berkeley experiments and axial force with and without mass transfer, and surface pressures and wall temperatures without mass transfer in the AEDC-VKF experiments. The estimated precision of these data is shown in the table below:

<table>
<thead>
<tr>
<th>Source</th>
<th>Force, percent</th>
<th>Pressure, percent</th>
<th>Pressure, percent</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td></td>
<td>( \dot{m} = 0 )</td>
<td>( \dot{m} &gt; 0 )</td>
</tr>
<tr>
<td>Berkeley</td>
<td>±5</td>
<td>±2</td>
<td>±5</td>
</tr>
<tr>
<td>Tunnel C</td>
<td>±7</td>
<td>--</td>
<td>--</td>
</tr>
<tr>
<td>Tunnel L</td>
<td>±7</td>
<td>--</td>
<td>--</td>
</tr>
</tbody>
</table>

The experimental value of \( CD \) for each value of injected mass flow used in the numerical calculations is shown in Table II, the experimental pressure data are shown in Table III, and wall temperature data are shown in Table IV. It should be noted that the drag data presented do not necessarily correspond to actual data points but rather were taken from fairings of the data.

Wall-to-stagnation temperatures are also tabulated. For the Berkeley tests the data were from readings of thermocouples located at the base of the model. The ratios for the AEDC-VKF zero injection data in Tunnel L are shown in Fig. 3, and the data from Tunnel C are from the previous data of Whitfield and Griffith. The accuracy of the thermocouple output is about ±2 percent; however no attempt has been made to assess effects of conduction losses through the wall. With injection the assumption is made that the cooled wall was maintained at the injection gas temperature (300°K).

No precision is quoted here for the pressure data in Tunnel L. However, the repeatability of the measured pressures was ±2 percent. (Also, the free-stream pitot pressure for the conditions \( M_\infty = 9.37 \) and \( Re_\infty/in. = 1602 \) was repeated and found to agree with previous tunnel calibrations within 1 percent.) Relatively large corrections to the measured pressure data are required to account for orifice size and heat-transfer effects,
and these effects will be discussed below. Because of the necessary corrections, a precision for the pressure data was more difficult to determine.

\section*{SECTION III
SOME THEORETICAL CONSIDERATIONS}

\subsection*{3.1 KING AND TALBOT'S ANALYSIS}

The Berkeley experimental data were analyzed by King and Talbot using (1) the similar boundary-layer solutions of Low (Ref. 7), (2) the effects of transverse curvature reported by Yasuhara (Ref. 8), (3) the inviscid flow field from the approximate tangent cone theory, and (4) the matching of the inviscid-viscous flow fields based on $d\delta*/dx$. The "second-order" boundary-layer effects were assumed to be uncoupled, and a linear combination of these effects was added to the effects of mass transfer from Low's solutions.* Also, the effects of the impermeable nose were neglected in their calculations.

At the time the analysis was made by King and Talbot (1962), the above-mentioned theories and procedures were perhaps the best in existence. However, since that time certain theoretical developments have occurred which make a re-examination of their experimental data and comparisons with their analytical results of interest. This seems especially significant since their experimental data were taken at supersonic Mach numbers and moderate Reynolds number where other second-order boundary-layer effects (viz., external vorticity, slip, and temperature jump) should be small. Therefore, both their experimental data and analysis provide interesting data to test new theoretical models designed for application at hypersonic, cold-wall, low Reynolds number conditions.

\subsection*{3.2 PRESENT ANALYSIS}

The basic theoretical model used in the numerical calculations was an iterated perfect gas ($\gamma = 1.4$) inviscid-viscous flow field. The viscous flow field was computed with the nonsimilar, laminar boundary-layer theory of Clutter and Smith (Ref. 9) which includes approximate transverse curvature terms. In addition, all boundary-layer calculations

\*Low's flat-plate similarity solutions were transformed with the Mangler factor $(3)^{1/2}$. 

5
were based on Sutherland's viscosity law and Prandtl number \( \text{Pr} = 0.71 = \) constant. The inviscid flow field was computed from the approximate tangent-cone theory. The matching of the inviscid and viscous flow fields was treated in two ways: (1) using the usual matching condition 
\[
\theta_{	ext{eff}} = \theta_c + \tan^{-1}(d\delta^*/dx)
\]
and (2) 
\[
\theta_{	ext{eff}} = \theta_c + \tan^{-1}\left(\frac{v_e}{u_e}\right),
\]
where \( v_e/u_e \) was computed from the formula proposed by Li and Gross (Ref. 10).* Some comments on the matching conditions are given in Appendix I.

The inviscid-viscous flow field was iterated until there was negligible change in \( \delta^*(x) \) or \( p_e(x) \). At high Reynolds numbers only two iterations or three boundary-layer calculations were required. At low Reynolds numbers and especially at high injection rates, five iterations or six boundary-layer calculations were required. Moreover, significant effect of matching conditions was noted on the number of iterations required (the number being less with \( v_e/u_e \) since with this matching condition the inviscid outer flow was displaced less from the geometric wall \( \theta_c(x) = \) constant). The method used for iterating the flow fields is discussed in Appendix II.

It should be noted that King and Talbot used a graphical method for matching the inviscid outer flow (tangent cone) with the viscous, boundary-layer edge conditions (Low's similar solutions). The matching was done simultaneously step by step along the body rather than obtaining successive approximations to the entire "effective" body as was done in the present investigation.

Because of the difficulties associated with iterating the inviscid-viscous flow field, most calculations presented in this report were based on a uniform injection (constant blowing) rate rather than constant \( f_w \sim 1/x^{1/2} \) as required for similarity (see, e.g., Low, Ref. 7). Uniform injection more nearly represented the actual mass flux distributions over the porous region of the model in the \( M_{\infty} = 10 \) experiments and appears to be a reasonable approximation for the experimental distributions of King and Talbot. The effects of the impermeable nose region were investigated for the King and Talbot conditions and for one set of conditions at \( M_{\infty} = 10 \).

The experimental data of King and Talbot indicated a near-constant, wall-to-stagnation temperature ratio \( T_w/T_0 = 0.96 \). Most of the numerical calculations for the present report at \( M_{\infty} = 10 \) were completed before the experimental wall temperature data were available. The wall-to-stagnation temperature ratios assumed in the calculations are indicated

---

*Hereafter the matching conditions will be denoted as \( d\delta^*/dx \) or \( v_e/u_e \).
in the figures where comparisons with experimental data are given. In all calculations the wall temperature was assumed to be constant, and the effects of wall temperature distributions such as shown in Fig. 3 have not been investigated.

The effects of slip and temperature jump were investigated at all conditions. The boundary-layer theory of Clutter and Smith (Ref. 9) was modified to include these effects. For more direct comparison with others, the mean free path was evaluated at the wall temperature, \( T_w \), rather than at the slip condition \( T(\eta = 0) \); however, this is not a necessary condition for the numerical procedure. Details of the procedure used in the present investigation are given in Appendix III.

It should be noted that the so-called second-order boundary-layer effects have all been treated as first-order effects. The first-order momentum and energy equations included (approximate)* transverse curvature terms, and the boundary conditions were modified to include slip and temperature jump. Moreover, the displacement effect is considered a first-order effect since the inviscid and viscous flow fields were iterated to "convergence". This is not, however, internally consistent since the outer flow was treated as inviscid (see Van Dyke, Ref. 1), and low density effects on the shock wave (e.g., finite thickness, curvature, and slip) were neglected (see Pan and Probstein, Ref. 12). These deficiencies can, in principle, be eliminated by a proper treatment of the "outer" flow.

SECTION IV
RESULTS AND DISCUSSION

The theoretical model used in the present report was tested against King and Talbot's experimental data and analytical results at \( M_e = 3.93 \) and 5.64. The theoretical model was then used to analyze the AEDC-VKF experimental data of Little and Griffith at \( M_e = 9.37 \) and 10. A large volume of interesting results were generated; however, the data presented herein will be confined to some of the more significant results.

4.1 BERKELEY CONDITIONS

The inviscid-viscous flow field was iterated as described above and in Appendix II. For convenience of comparison with the analytical results

*See the revised version of Clutter and Smith (Ref. 9).
of King and Talbot at $M_w = 5.64$ and $Re_{\infty}/in. = 6200$, the ratio $\delta^*/r_w$ was computed without mass transfer and is shown in Fig. 4. Excellent agreement was found with King and Talbot's results using the $d\delta^*/dx$ matching condition and the similar solutions of Low. The matching condition $v_{e}/u_{e}$ predicted a slightly larger $\delta^*$ since the inviscid outer flow was displaced less by the boundary layer, and thus the viscous-induced pressure was less which in turn produced larger boundary-layer and displacement thicknesses. Under these conditions, transverse curvature had a negligible effect on $\delta^*(x)$.

The viscous-induced pressure increment $(p - p_{inv})/P_{inv}$ at $M_w = 3.93$ and 5.64 is shown in Fig. 5. The effects of matching condition and transverse curvature (TVC) were also considered. Using the matching condition $v_{e}/u_{e}$ gave results which were in better agreement with the experimental pressure data of King and Talbot, especially at $M_w = 5.64$. The effects of slip and temperature jump are also shown. As suggested by King (Ref. 5), the effects of slip and temperature jump on the pressure distribution were indeed small. However, we will see later that the effects on the zero-lift drag are somewhat larger.

The effects of uniform mass transfer on the viscous-induced pressure increment at $M_w = 5.64$ are shown in Fig. 6. At the highest injection rate considered (0.09375 lbm/hr), the effects of matching conditions are also shown. At high injection rates the effects of matching conditions on the viscous-induced pressure increment became more important especially over the forward portion of the cone as shown in Fig. 6.

The ratio of local skin-friction coefficients $C_f/C_f^{(o)}$ at $M_w = 5.64$ is shown in Fig. 7, where $C_f^{(o)}$ is the value without viscous interaction, transverse curvature, or mass transfer. The separate and combined effects of viscous interaction and transverse curvature at zero injection are in contrast with the King and Talbot results. As noted by King (Ref. 5), $C_f^{(a)}/C_f^{(o)}$ should be greater than unity; however, his analysis predicted $C_f^{(a)}/C_f^{(o)} < 1$, a result which he attributed to his neglecting the viscous-induced axial pressure gradient by using the flat-plate results of Low (Ref. 7). The effect of transverse curvature on $C_f$ based on the approximate theory of Clutter and Smith was in substantial agreement with King and Talbot's prediction using the theory of Yasuhara.

The coupled and uncoupled effects of viscous interaction and transverse curvature on $C_f$ could be seen by comparing the results denoted $VI^{(o)} + TVC^{(o)}$ with $(VI + TVC)^{(a)}$. The comparison (not shown in Fig. 7) indicated excellent agreement. This tends to support the usual assumption of linear independence of these second-order effects. The results denoted $(VI + TVC)^{(o)}$, however, have treated both as coupled first-order effects.
Three injection laws, viz., (1) $\rho_w v_w = \text{constant}$, (2) $I_w = \text{constant}$, and (3) $\rho_w v_w = \phi(x)$ from the experimentally measured distribution of King and Talbot at $M_w = 5.64$, and their effects on friction drag are shown in Fig. 8. The effects of viscous interaction and transverse curvature coupled with the effects of injection laws on $C_D$ are also shown. One significant result for the conditions considered was that the effects of the impervious nose and various injection laws on the friction drag were negligible. It is also significant that the prediction including viscous interaction and transverse curvature was in good agreement with the faired experimental data of King and Talbot. The latter data were obtained by subtracting the integrated experimental pressure drag from the experimentally measured total drag with a correction for mass injection (cf., King, Ref. 5).

Figure 9 shows the drag components and total drag coefficient $C_D = C_D f + C_D p$ from the present investigation compared with the experimental data and analytical results of King and Talbot at $M_w = 3.93$ and $5.64$. The effects of viscous interaction, transverse curvature, and matching conditions with mass transfer are shown in the figure. The present results are in substantially better agreement with the experimental data than were the predictions of King and Talbot. In fact, the present results iterated to convergence and based on $v_e/u_e$ matching conditions and with or without injection predicted total drag in agreement with the experimental data at $M_w = 5.64$ within the experimental uncertainty. This encouraging result should be tempered with the observation that the present analysis cannot be extended to much higher injection rates. Without viscous interaction, "blow-off" occurred far forward on the body at $\dot{m} = 0.12 \text{ lbm/hr}$, whereas King's experimental data extended to $\dot{m} = 0.32 \text{ lbm/hr}$ before injection caused the total drag to reach a minimum.

The effects of slip and temperature jump on the zero injection drag at $M_w = 3.93$ and $5.64$ are shown in Fig. 9 (the procedure used is discussed in more detail below for $M_w = 10$ conditions). At both Mach numbers, the effects of slip and temperature jump were about 5 percent, and this should be contrasted with the almost negligible effect on the viscous-induced pressure increment (see Fig. 5). If the present theoretical model is appropriate with respect to slip and temperature jump, it appears once again that experimental and theoretical zero-lift drag studies might be a useful tool for investigating another second-order boundary-layer effect. Of course, much work remains to solve the leading edge problem as well as the kinetic theory problems, such as reflection and accommodation coefficients. Although the predicted effects of slip at the Berkeley conditions were approximately equal to experimental uncertainty, the effects may be large enough to permit experimental verification at similar conditions.
4.2 AEDC-VKF CONDITIONS

The theoretical model was applied to the experimental data of Little and Griffith at $M_\infty = 10$. The effects of iteration on the displacement thickness and corresponding viscous-induced pressure increment with mass transfer at $Re_\infty/in. = 396$ are shown in Fig. 10. With injection the displacement thickness was substantially increased, and this in turn produced a large variation in the viscous-induced pressure increment with iteration. It should be noted that the solution had not converged with five iterations; however, the converged solution was bounded by the fourth and fifth iterations.

Figure 11 shows the effects of different injection laws on the zeroth iteration values of $\delta$ and $\delta^*$. The difficulty of iterating the inviscid-viscous flow field near the beginning of the injection region ($x = 0.57$ to $0.75$) prevented us from considering further the experimental distribution. Substantial differences in $\delta$ and $\delta^*$ caused by the two distributions (experimental and constant mass transfer) are evident in the figure.

Figure 12 shows the effects of mass transfer on the displacement and total boundary-layer thicknesses at $Re_\infty/in. = 396$. The thicknesses were, of course, increased; however, the character of the thicknesses was not substantially changed at this moderately high injection rate.

4.3 EFFECTS OF SLIP AND TEMPERATURE JUMP

Before presenting the comparisons of the numerical results with the experimental data for the effects of mass transfer on the drag coefficient at $M_\infty = 9.37$ and 10, the effects of slip and temperature jump on the numerical results are considered.

Figure 13 shows the ratio of the wall slip velocity to free-stream velocity and temperature jump at $M_\infty = 10$ and the lowest Reynolds number for which experimental data were available. The effects of matching conditions are shown, and the effects of viscous interaction are implicit since the calculations with slip and temperature jump were started from the converged no-slip solutions (see Appendix III). The temperature jump at the wall especially deserves a few comments. Near $x = 0$ where the slip velocity is largest, the temperature jump is smallest - a surprising result. However, the temperature jump is dominated by the quantity $(\partial h/\partial \eta)_{\eta=\eta_w}$ (see Appendix III). From the energy equation, $\partial h/\partial \eta = h_{\eta=\eta_w}' - u_e^2 f'$, where prime denotes differentiation with respect to $\eta$. Thus with slip there exist values of $f'$, $g'$ and $f''$ such that $\partial h/\partial \eta = 0$ or $h(\eta = 0) = h_{\eta_w}$. Also, the solution based on $d\delta^*/dx$
matching conditions reached a maximum temperature jump near \( x = 0.7 \) and began to decrease. Of course, the asymptotic limit \( T(\eta = 0) = T_w \) must be reached as \( x \to \infty \); however, for this low Reynolds number condition there were large slip and temperature jump effects over the entire cone.

The effects of slip* and temperature jump on \( \delta^* \) and \( \delta \) are shown in Fig. 14. Also, the effects of mass transfer and slip on the pressure distribution are shown in Fig. 15. At zero injection, the effects of slip on the pressure distribution became negligibly small as \( x \to 1 \).

The skin-friction coefficient, \( C_{f*} \), and Stanton number, \( S_{t*} \), are shown in Figs. 16a and b, respectively. The results with mass transfer and slip are shown, and the effects of viscous interaction and transverse curvature were included in the calculations. In accord with the previously discussed results with slip, the effects of \( C_{f*} \) and \( S_{t*} \) were substantially reduced as \( x \) increased; however, it is interesting to note that the effects of slip were somewhat greater on \( S_{t*} \) than on \( C_{f*} \), whereas the effects of mass transfer on the two coefficients were nearly equal.

Comparisons of experimental pressure data and theoretical predictions are shown in Fig. 17. The uncorrected experimental data are indicated with flagged symbols. The data were corrected for orifice size after Potter, Kinslow, and Boylan (Ref. 13), and those results are also shown. The predictions from the present investigations are shown, and for comparison the inviscid sharp cone values and the free-molecule values after Hayes and Probstein (Ref. 14) are also shown. The present iterated flow field and free-molecule flow predictions both overestimate the measured surface pressure. As noted earlier, the orifice correction is large and the experimental uncertainty is currently unknown. The trends of both the uncorrected and corrected surface pressure data are as expected, i.e., the pressure tends toward the free-molecule value as \( x \to 0 \). The agreement between experimental data and numerical results is encouraging; however, further work is required to better define the experimental uncertainty and correction factors (orifice size and thermal transpiration) as well as the applicability of the theoretical model at these low Reynolds number conditions.

It is also worth noting that the difference between the inviscid sharp cone value and the free-molecule value is primarily due to the large wall-to-free-stream temperature ratio. The wall temperature effect increases with increasing \( T_w/T_\infty \) (see Hayes and Probstein, Ref. 14).

---

*Hereafter slip will be used to denote both slip and temperature jump effects.
Comparisons of the experimental drag data at $M_a = 10$ with the predictions from the present investigation are shown in Fig. 18. The effects of mass transfer, viscous interaction, transverse curvature, matching conditions, slip, and temperature jump are indicated. Only the final converged solutions are shown except at the lowest Reynolds number. The results of each iteration and the combined effects of mass transfer and slip at the lowest Reynolds number are shown in Fig. 19 to indicate the large changes in the total drag between iterations. The effect of the term $\rho_w v_{wr} / \rho_e u_{re}$ on the matching condition with and without slip is also shown in the figure. The effect of the term on the total drag was about 5 percent and in a direction away from the experimental results.

It is interesting to note that for the same total mass flow rate, $\dot{m}$, the effects of injection on the drag increase with decreasing Reynolds number. This is also in agreement with the experimental results of Whitfield and Griffith (Ref. 2) for the case of tangential injection. It thus appears that the effects of mass transfer (either normal or tangential) are more important on inviscid-viscous flow fields under low Reynolds number conditions.

In considering the comparison of numerical results and experimental data with mass transfer, the basic deficiency in the theoretical model should be remembered. Uniform mass transfer was assumed over the entire cone, whereas in the AEDC-VKF experiments the forward 32.5 percent of the cone surface area was impervious to mass transfer. Moreover a theoretical model with impervious nose and porous afterbody would probably predict an increase in total drag because of (1) an increase in pressure and friction drag over the impervious nose and (2) an increase in pressure drag over the porous afterbody. It is not clear whether the friction drag would be increased or decreased over the porous region since the increased mass flux would tend to reduce the skin friction; however, the thicker boundary layer would tend to increase the viscous and transverse-curvature-induced friction drag. Therefore considering the deficiency in the theoretical model with regard to nonuniform mass transfer distributions, the results of the present predictions are considered to be satisfactory.

A comparison of numerical results and experimental data for all the zero-lift drag data without mass transfer is shown in Fig. 20. For comparison, the previously published experimental data of Whitfield and Griffith are also shown. The drag data are shown against the
hypersonic interaction parameter \( \bar{v}_\infty = M_\infty (C_\infty /Re_\infty)^{1/2} \) proposed by Whitfield and Griffith.\(^*\) In general, the numerical results based on the matching condition \( v_e/u_e \) and including slip agree with the experimental data within experimental uncertainty.

SECTION V
CONCLUDING REMARKS

When the theoretical model developed in the present report was used to predict the viscous-induced pressure increment and zero-lift drag of a sharp, 5-deg half-angle cone at the Berkeley conditions (\( M_\infty = 3.93 \) and 5.64), the results were in better agreement with the experimental data than were the previous analytical results of King and Talbot (Refs. 5 and 6). This was especially true for the effects of mass transfer on the total drag at moderately high injection rates.

The same theoretical model was used to predict viscous effects on a 9-deg half-angle cone at \( M_\infty = 9.37 \) and 10 over a range of Reynolds numbers and wall-to-stagnation temperature ratios. At zero injection, in general the predictions of zero-lift drag agreed with the experimental data within experimental uncertainty. However with injection, the basic deficiency of the theoretical model, viz., neglecting the effects of a large impermeable nose, was more important. The effects of inviscid-viscous flow field matching conditions, slip, and temperature jump as applied in the present report were found to have a significant effect on viscous-induced pressure and friction drag increments.

The comparison of experimental and predicted surface pressures showed substantial disagreement, and the need for further investigation is indicated. Without mass transfer the theoretical model of this report is applicable to arbitrary, pointed, two-dimensional, and axisymmetric bodies as long as boundary-layer theory is applicable and an inviscid outer flow exists which can be approximated by tangent wedge or cone theory. Under the rarefied flow conditions at \( M_\infty = 10 \) considered in this report, the above-noted requirements might not have been met. However, the comparisons shown are encouraging, and further experiments and numerical studies are required to better define the effects of wall-to-stagnation temperature ratio and wall temperature distributions and the nature of the outer flow field and shock wave.

\(^*\)Some additional comments and a derivation of the parameter \( \bar{v}_\infty \) are given by Lewis and Whitfield (Ref. 3).
REFERENCES


APPENDIX I

INVISCID-VISCOUS FLOW FIELD MATCHING CONDITIONS

The effects of mass transfer on inviscid-viscous flow field matching conditions have been considered by Mann (Ref. 15) and Thyson and Schurmann (Ref. 16). More recently, Li and Gross (Ref. 10) considered the combined effects of mass transfer and transverse curvature by integrating the continuity equation from \( y = 0 \) to \( y = \delta(x) \). In so doing they obtained the following matching conditions for a sharp cone in hypersonic flow:

\[
\frac{v_e}{u_e} = \frac{\rho_w v_w r_w}{\rho_e u_e r_e} + \frac{d\delta}{dx} \left( 1 \right) + \frac{r_w}{r_e} \left[ \frac{d\delta^*}{dx} - \frac{\delta - \delta^*}{\rho_e u_e r_e} \frac{d\delta}{dx} \left( \rho_e u_e r_w \right) \right] - \cos \theta_c \left[ \frac{\delta^3 - \delta^{*3}}{2 \rho_e u_e r_e} \frac{d\left( \rho_e u_e \right)}{dx} - \frac{1}{r_e} \left( \delta \frac{d\delta}{dx} - \delta^* \frac{d\delta^*}{dx} \right) \right] \tag{I-1}
\]

Li and Gross then state "... In hypersonic boundary layers, \( \delta^* \rightarrow \delta \); then Eq. (I-1) becomes

\[
\frac{v_e}{u_e} = \frac{\rho_w v_w r_w}{\rho_e u_e r_e} + \frac{d\delta^*}{dx} \tag{I-2}
\]

(which) provides the necessary condition ..."

For two of the conditions studied in the present report, the following data were obtained from the zeroth iteration without mass transfer at \( x = 0.90 \):

<table>
<thead>
<tr>
<th>( M_\infty )</th>
<th>( Re_\infty/\text{in} )</th>
<th>( \theta_c, \text{deg} )</th>
<th>( T_w/T_\infty )</th>
<th>( \delta^* / \delta )</th>
<th>( \tan^{-1} (d\delta^*/dx), \text{deg} )</th>
<th>( \tan^{-1} (v_e/u_e), \text{deg} )</th>
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</thead>
<tbody>
<tr>
<td>5.64</td>
<td>6200</td>
<td>5</td>
<td>0.96</td>
<td>0.73</td>
<td>1.68</td>
<td>1.01</td>
</tr>
<tr>
<td>10.0</td>
<td>396</td>
<td>9</td>
<td>0.20</td>
<td>0.71</td>
<td>4.12</td>
<td>1.97</td>
</tr>
</tbody>
</table>

The effect of the terms neglected by Li and Gross under the hypersonic approximation caused a 40- and 50-percent change in \( \tan^{-1} (d\delta^*/dx) \) at \( M_\infty = 5.64 \) and 10, respectively. This corresponds to a reduction of the viscous-induced pressure term \( \rho / p_{\text{in}} - 1 \) of 39 and 56 percent at \( M_\infty = 5.64 \) and 10, respectively. It therefore appears significant and desirable to evaluate the complete Eq. (I-1) rather than using the hypersonic approximation and the resulting Eq. (I-2).

The effect of the term \( \rho_w v_w r_w / \rho_e u_e r_e \) in Eq. (I-2) was investigated at \( M_\infty = 10 \) and \( Re_\infty/\text{in.} = 396 \) where the effect on \( v_e/u_e \) was a maximum.
Under those conditions, the effect on total drag was about 5 percent. Therefore for more direct comparison with King and Talbot,

\[ \frac{v_e}{u_e} = \frac{d\delta^*}{dx} \quad (I-3) \]

was used in most of the calculations. The inviscid flow field was computed from the approximate tangent cone theory. The pressure on the effective cone of half-angle \( \theta_{\text{eff}} = \theta_c + \tan^{-1}(v_e/u_e) \) was determined according to either Eq. (I-1) or (I-3), and matching is denoted \( v_e/u_e \) or \( d\delta^*/dx \), respectively.
In order to consider the coupled effects of the various second-order terms including viscous interaction, it was necessary to iterate successive boundary-layer solutions until a converged solution was obtained. Regardless of whether the matching condition was based on $\delta^*/dx$ or $v_e/u_e$, it was difficult to obtain sufficiently smooth pressure and velocity distributions. Three-point numerical differentiation of $\delta(x)$ and $\delta^*(x)$ was satisfactory at the lower Mach numbers, $M_\infty = 3.93$ and 5.64, but was unsatisfactory at $M_\infty = 9.37$ and 10 since small variations in the smoothness of the $\theta_{eff}$ profile, inherent in the numerical differentiation scheme, caused appreciable oscillations in succeeding boundary-layer solutions. Several schemes for fitting $\delta(x)$ and $\delta^*(x)$ with polynomials were tried, and although good fits of the profiles were obtained the corresponding analytical derivatives were poorly behaved.

The $\delta$ and $\delta^*$ calculated data were fitted with a power law and exponential equation of the form

$$\delta = ax^b - \exp (cx - d)$$

This equation fitted the data well (average error about ±0.2 percent) for the majority of the cases considered. Also, the resulting derivative

$$\frac{d\delta}{dx} = abx^{b-1} - c \exp (cx - d)$$

was well behaved. However, this form of equation characteristically gave a poor solution near $x = 0$, and to account for this, $\theta_{eff}$ was graphically extrapolated over the region $0 \leq x \leq 0.1$. This gave reasonable values of pressure and velocity for starting the solution and had a negligible effect on the total zero-lift drag since only 1 percent of the cone surface area was within the extrapolated region.

For the cases with mass transfer at the wall, the problem was further complicated. Solutions based on the experimental injection laws (at $M_\infty \sim 10$ injection started at $x = 0.57$) proved impossible to iterate by the method of successive approximations since the rapid changes in $d\delta^*/dx$ encountered near the start of the injection region induced serious oscillations into the solution. In the cases which were iterated, the mass flux was computed from $\rho_w v_w = \dot{m}/A_w$, where $\dot{m}$ is the total (experimental) mass transfer rate and $A_w$ is the total surface area of the cone. The resulting average mass flux was assumed constant over the entire surface of the cone. This eliminated the oscillations and permitted inviscid-viscous flow field iterations to be made. When the mass flux reached a sufficiently large value, boundary-layer "blow-off" ($f^*_w \rightarrow 0$)
occurred on the cone. It was possible, however, to obtain iterated flow field solutions at moderately high injection rates if the rapid increase in \( \delta(x) \) and \( \delta^*(x) \) as \( x \to 1 \) was ignored. This is justified on the basis that the corresponding viscous-induced pressure acts to reduce a rapid increase in \( \delta^*(x) \). It is also noted that each calculation is to be considered as an iterate or approximate solution to the final converged solution, and thus an exact fit of \( \delta^*(x) \) was not necessarily the most desirable for each successive approximation at moderately high blowing rates.

With the "effective" body obtained as described above, the "effective" cone angle \( \theta_{\text{eff}} \) and matching condition \( d\delta^*/dx \) or \( v_e/u_e \) were used with the ideal gas (\( \gamma = 1.4 \)) tangent cone solutions to determine \( p_e(x) \) and \( u_e(x) \). The boundary-layer calculations then proceeded in the usual manner.
APPENDIX III
SLIP AND TEMPERATURE JUMP CONDITIONS

The effects of slip and temperature jump at the surface of blunt-nosed bodies have been studied by several investigators in recent years (see, e.g., Refs. 11 and 17). Recently Pan and Probstein (Ref. 12) and Li and Street (Ref. 18) have considered an impermeable, semi-infinite flat plate under rarefied flow conditions. The results of the latter investigations varied greatly on the prediction of the beginning of the region of continuum, strong interaction plus wall slip and temperature jump. Moreover, most authors have evaluated the mean free path at the wall conditions, say \( T_w \) and \( p_w \), rather than at the slip conditions \( T(\eta = 0) \) and \( p_w \). This usual procedure was also used in the present report but is not a necessary condition for the numerical calculations.

The wall slip velocity and temperature jump were computed according to the formulas given by Street (Ref. 19) and Van Dyke (Ref. 11):

\[
\begin{align*}
  u(0) &= (\mu R/p) \left( \frac{\pi T/2R}{2} \right)^{1/2} \frac{\partial u}{\partial y} + \frac{3}{4} \frac{\partial T}{\partial x} \\
  T(0) &= T_w - \frac{\mu R/p}{15/8} \left( \frac{\pi T/2R}{2} \right)^{1/2} \frac{\partial T}{\partial y}
\end{align*}
\]

where the right-hand sides of both equations were evaluated at the wall conditions, the hard sphere model was used to evaluate constants in both formulas, and the reflection and thermal accommodation coefficients were assumed to be unity.

Under the transformations used by Clutter and Smith (Ref. 9),

\[
x = x \text{ and } \eta = \left( \frac{u_e L}{\rho_w u_s^*} x \right)^{1/2} \int_0^\eta \rho \, dy
\]

Eqs. (III-1) and (III-2) become, respectively,

\[
\begin{align*}
  f(\eta = 0) &= \frac{\mu_w}{p_w} \frac{1}{L} \left[ \left( \frac{\pi}{2} \frac{\gamma - 1}{\gamma} h_w \frac{u_e}{u_s} \frac{1}{x} \right)^{1/2} \frac{\rho_w}{\rho_s} f_w \\
  &\quad + \frac{3}{4} \frac{1}{\gamma - 1} \frac{u_e}{u_s} \frac{h_{ref}}{u_s} \frac{\partial}{\partial x} \left( \frac{h_{ref}}{h_w} \right) \right] \\
  h(\eta = 0) &= h_w + \frac{15}{8} \frac{\mu_w}{p_w} \left( \frac{\pi}{2} \frac{\gamma - 1}{\gamma} h_w \frac{u_e}{u_s} \frac{1}{x} \right)^{1/2} \frac{\rho_w}{\rho_s} \frac{1}{L} \left( \frac{\partial h}{\partial \eta} \right)_w
\end{align*}
\]

The local skin-friction coefficient

\[
C_{f*} = 2 \frac{\eta}{\rho_w u_s^*} = 2 \left( \frac{u_e}{u_s} \right)^{1/2} \left( \frac{1}{x} \right) \left( \frac{\rho_w \mu_w}{\rho_s \mu_s} \right) f_w
\]
is not altered because of slip and temperature jump; however, the heat-transfer rate to the surface becomes

\[
q_w = \left( \frac{\mu}{Pr} \right) \frac{\partial h}{\partial y} + \mu u (\partial u/\partial y) \right)_w
\]

and with the Stanton number defined

\[
St = \frac{q_w}{\rho v w (H_e - h_w)}
\]

the ratio \(St/C_f\) becomes

\[
\frac{St}{C_f} = \frac{1}{2 (1 - e_w)} \frac{\frac{u_x}{v_x}}{\left[ \frac{1}{Pr} \frac{\frac{e_w}{\gamma - 1}}{H_e} + \frac{\frac{e_w}{\gamma - 1}}{H_w} \right] \left( 1 - \frac{1}{Pr} \right)}
\]

The Clutter-Smith theory (Ref. 9) was modified to include Eqs. (III-4), (III-5), and (III-6). However, before sharp-nosed body calculations could be made it was necessary to consider the effects of the singularity at \(x = 0\). The order of the singularity for a pointed body is such as to preclude internally consistent calculations at that point. However, the boundary-layer equations are not applicable at \(x = 0\) and a small region near \(x = 0\) was in near free-molecule flow. The extent of the noncontinuum region for a sharp cone in rarefied flow has not been investigated. However, Pan and Probstein have considered the problem for a sharp flat plate, and their estimates for the conditions of the present investigation are of interest.

Pan and Probstein gave the criterion \(Re_{\infty, x_1} / M_{\infty} = 8\) for the beginning of the "boundary layer plus normal pressure gradient" region. This region lies downstream of the near free-molecule and transition regions and upstream of the hypersonic strong interaction region (see Ref. 12). The region was treated by Pan and Probstein as continuum flow with wall slip and temperature jump, and they investigated the effects of slip, curvature, and thickness of the shock wave in addition to the effects of the normal pressure gradient. (In the present report all transport effects on the shock wave and the normal pressure gradient effects were ignored.)

Using the Pan and Probstein criterion,

\[
\frac{x_1}{\lambda_{\infty}} = \frac{Re_{\infty, x_1}}{M_{\infty}} \frac{1}{C_{\infty} M_{\infty}} \frac{2}{\gamma - 1} \left( \frac{T_w}{T_{\infty}} \frac{\gamma + 1}{\gamma} \frac{1}{\pi} \right)^{\frac{1}{2}}
\]

with \(Re_{\infty, x_1} / M_{\infty} = 8\), for the Tunnel L conditions the initial location \(x_1\) was computed as follows:
One thus sees that except at the lowest Reynolds number, the non-continuum region was very small in extent. Pan and Probstein also predicted that the region of strong viscous interaction plus slip should begin at $\text{Re}_{\infty, x}/M_{\infty} = 40$ to 45. Thus at the lowest Reynolds number approximately one-half of the cone was within the (flat-plate) noncontinuum and boundary-layer plus normal pressure gradient regions. For the other conditions no more than 0.125 of the length or 0.0156 of the area of the cone was upstream of the (flat-plate) strong interaction region. Also without slip the strong interaction region of a cone is much less than for a flat plate.

Therefore in the present study the noncontinuum and boundary layer plus normal pressure gradient regions were neglected. The boundary-layer solutions with slip and temperature jump were begun as near $x = 0$ as practical (usually at $x \sim 0.025$) using the modified Clutter-Smith theory and the tangent cone theory. The calculations were started from the converged no-slip solutions. At $x_i$ the nonsimilar terms (e.g., $\partial f/\partial x$, $\partial g/\partial x$) in the momentum and energy equations were set to zero. However, the transverse curvature term, which in the original Clutter-Smith machine program was also set to zero at the initial station, was retained in the modified theory. The boundary layer with slip and temperature jump was also iterated as the no-slip solutions were, and the method of iteration is discussed in Appendix II.
a. Berkeley Low Density Tunnel Force Model

\[ \theta_c = 5 \text{ deg} \]

\[ L = 3.00 \]

\[ \ell = 3.50 \]

All Dimensions in Inches

b. AEDC-VKF Force Model

\[ \theta_c = 9 \text{ deg} \]

\[ 0.75 \]

\[ 1.05 \]

\[ \ell = 2.37 \]

All Dimensions in Inches

Fig. 1 Force, Pressure, and Wall Temperature Models
c. AEDC-VKF Pressure Models

All Dimensions in Inches

d. AEDC-VKF Wall Temperature Model

Fig. 1 Concluded
Fig. 2 Comparison of Gas Injection Laws

$M_\infty = 3.93$, 0.0625 lbm/hr $f_w = \text{Constant (No Interaction)}$

$M_\infty = 10$, 0.072 lbm/hr AEDC-VKF, Experiment

$p_{wv} = \text{Constant}$
Experimental Data
AEDC-VKF Tunnel L

<table>
<thead>
<tr>
<th>Sym</th>
<th>$M_\infty$</th>
<th>$Re_\infty$/in.</th>
<th>$T_o$, °K</th>
</tr>
</thead>
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<td>●</td>
<td>9.38</td>
<td>2606</td>
<td>1033</td>
</tr>
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<td>1602</td>
<td>1662</td>
</tr>
<tr>
<td>■</td>
<td>10.15</td>
<td>388</td>
<td>3020</td>
</tr>
</tbody>
</table>

Zero Injection

Fig. 3 Equilibrium Wall Temperature Distributions over a Hallow 9-deg Half-Angle Cone
Fig. 4 Boundary-Layer Displacement Thickness over a 5-deg Half-Angle Cone
\( M_{\infty} = 3.93 \)
\( Re_{\infty}/in. = 1765 \)
\( M_{\infty}/\sqrt{Re_{\infty}/\lambda} = 0.05 \)
\( T_w/T_0 = 0.96 \) (No Slip)
\( \lambda_{\infty} = 0.0032 \) In.

Zero Injection

Numerical Results

<table>
<thead>
<tr>
<th>Sym.</th>
<th>Matching Condition</th>
<th>Iteration</th>
<th>Source</th>
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<td>2</td>
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</tr>
<tr>
<td>( \frac{d\delta^*/dx}{dx} )</td>
<td>-</td>
<td>-</td>
<td>King and Talbot</td>
</tr>
<tr>
<td>( \frac{v_E/u_E}{u_E} )</td>
<td>2</td>
<td>2</td>
<td>Present Results</td>
</tr>
<tr>
<td>( \frac{v_E/u_E}{u_E} )</td>
<td>2s + 1s</td>
<td>2s + 1s</td>
<td>Present Results</td>
</tr>
</tbody>
</table>

Experimental Data

Berkeley Low Density Tunnel

\( M_{\infty} = 3.93 \)

Fig. 5  Effects of Viscous Interaction and Transverse Curvature on Sharp Cone Pressure Distribution
$M_{\infty} = 5.64$
$Re_{\infty}/In. = 6286$
$M_{\infty}/Re_{\infty} = 0.038$
$T_w/T_0 = 0.96$ (No Slip)
$\lambda_{\infty} = 0.0012$

Zero Injection

Numerical Results

<table>
<thead>
<tr>
<th>Sym</th>
<th>Matching Condition</th>
<th>Iteration</th>
<th>Source</th>
</tr>
</thead>
<tbody>
<tr>
<td>TVC</td>
<td>$\frac{d\delta^*}{dx}$</td>
<td>2</td>
<td>Present Results</td>
</tr>
<tr>
<td>No</td>
<td>$\frac{d\delta}{dx}$</td>
<td>-</td>
<td>King and Talbot</td>
</tr>
<tr>
<td>Yes</td>
<td>$\frac{v_e}{u_e}$</td>
<td>2</td>
<td>Present Results</td>
</tr>
<tr>
<td></td>
<td>$2s + 1s$</td>
<td></td>
<td>Present Results</td>
</tr>
</tbody>
</table>

Experimental Data

Berkeley Low Density Tunnel

Fig. 5 Concluded
Fig. 6 Effects of Mass Transfer and Viscous Interaction on a 5-deg Half-Angle Cone at $M_\infty = 5.64$
Fig. 7 Effects of Viscous Interaction and Transverse Curvature on Skin-Friction Coefficient
\[ M_\infty = 5.64 \]
\[ Re_\infty /\text{in.} = 6200 \]

### Numerical Results

<table>
<thead>
<tr>
<th>Injection Law</th>
<th>Experimental</th>
<th>( f_w = \text{Constant} )</th>
<th>( \rho_w^{v_w} = \text{Constant} )</th>
</tr>
</thead>
<tbody>
<tr>
<td>No VI or TVC</td>
<td>☓</td>
<td>+</td>
<td>☓</td>
</tr>
<tr>
<td>VI Only</td>
<td>☓</td>
<td></td>
<td>☓</td>
</tr>
<tr>
<td>TVC Only</td>
<td>☓</td>
<td>×</td>
<td></td>
</tr>
<tr>
<td>TVC + VI</td>
<td>☓</td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

Flags Denote Number of Iterations

- No Slip

- Faired Experimental Data after King and Talbot

### Fig. 8 Effects of Various Injection Laws on Friction Drag Coefficient

\( \dot{m}, \text{lbm/hr} \)

\( C_{D_f} \)
\[ M_{\infty} = 3.93 \]
\[ Re_{\infty,lin.} = 1765 \]
\[ T_{W}/T_{O} = 0.96 \text{ (No Slip)} \]

**Experimental Data**
Berkeley Low Density Tunnel
King and Talbot

**Numerical Results**

<table>
<thead>
<tr>
<th>Sym</th>
<th>Matching Condition</th>
<th>Injection Law</th>
<th>Source</th>
</tr>
</thead>
<tbody>
<tr>
<td>---</td>
<td>d(\delta^*/dx)</td>
<td>(P_{W}V_{W} = \text{Const.})</td>
<td>Present Results</td>
</tr>
<tr>
<td></td>
<td>d(\delta^*/dx)</td>
<td>(f_{W} = \text{Const.})</td>
<td>King and Talbot</td>
</tr>
<tr>
<td>(\Delta)</td>
<td>(v_{e}^{e}/u_{e}^{e})</td>
<td>(P_{W}V_{W} = \text{Const.})</td>
<td>Present Results</td>
</tr>
</tbody>
</table>

Flag Denotes Slip

---

Fig. 9 Drag Components
$M_\infty = 5.64$
$Re_{\infty}/in. = 6200$
$T_w/T_0 = 0.96$ (No Slip)

**Experimental Data**
Berkeley Low Density Tunnel
King and Talbot

<table>
<thead>
<tr>
<th>Sym</th>
<th>Matching Condition</th>
<th>Injection Law</th>
<th>Source</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>$\delta^+/dx$</td>
<td>$\rho_w v_w = \text{Const.}$</td>
<td>Present Results</td>
</tr>
<tr>
<td></td>
<td>$\delta^+/dx$</td>
<td>$f_w = \text{Const.}$</td>
<td>King and Talbot</td>
</tr>
<tr>
<td>$\Delta$</td>
<td>$v_e/u_e$</td>
<td>$\rho_w v_w = \text{Const.}$</td>
<td>Present Results</td>
</tr>
</tbody>
</table>

Flag Denotes Slip

\[ \delta = 3.5 \text{ in.} \]

\[ 10 \text{ deg} \]

\[ \beta = 0.3 \]

\[ c = 0.02 \quad 0.04 \quad 0.06 \quad 0.08 \quad 0.10 \quad 0.12 \quad 0.14 \]

\[ \dot{m}, \text{lbm/hr} \]

\[ b. \quad M_\infty = 5.64 \]

Fig. 9 Concluded
\[ M_{\infty} = 10 \]
\[ Re_{\infty} = 396 \]
\[ M_{\infty}/Re_{\infty}, \epsilon = 0.326 \]
\[ T_w/T_0 = 0.2 \]
\[ \lambda_{\infty} = 0.037 \text{ in.} \]
\[ \dot{m} = 0.144 \text{ lbm/hr} \]
\[ d\delta^*/dx \text{ Matching Condition} \]
\[ \text{No Slip} \]

Fig. 10 Effects of Iteration with Mass Transfer
\[ M_\infty = 10 \]
\[ Re_\infty/\text{in.} = 396 \]
\[ M_\infty/\sqrt{Re_\infty} \ell = 0.326 \]
\[ \frac{T_W}{T_0} = 0.2 \]
\[ \lambda_\infty = 0.037 \text{ in.} \]
\[ \dot{m} = 0.144 \text{ lbm/hr} \]
\[ \frac{d\phi}{dx} \text{ Matching Condition} \]
\[ \text{No Slip} \]

**b. On Viscous-Induced Pressure**

Fig. 10 Concluded
$M_\infty = 10$
$Re_\infty/\text{in.} = 396$
$T_w/T_D = 0.2$
$\dot{m} = 0.144 \text{ lbm/hr}$
No Slip

**Injection Law**

$\rho_w v_w = \text{Constant}$

Experimental

Fig. 11 Effects of Different Injection Laws on $\delta^*(0)$ with $\delta(0)$ with Transverse Curvature
$M_\infty = 10$
$Re_\infty$/in. = 396
$M_\infty \sqrt{Re_\infty \ell} = 0.326$
$T_\infty/T_0 = 0.2$
$\lambda_\infty = 0.037$ in.

$\frac{\delta}{\delta^*} dx$ Matching Condition

No Slip

**Fig. 12** Effects of Mass Transfer and Iteration on Displacement and Total Boundary-Layer Thicknesses
Zero Injection Matching Condition

\[ \frac{u(\eta = 0)}{u_\infty} \]

Iteration

\( (2s + 2s) \)

\( (4s + 2s) \)

\[ \frac{T(\eta = 0) - T_w}{T_w} \]

Iteration

\( (4s + 2s) \)

\( (2s + 2s) \)

Fig. 13 Wall Slip and Temperature Jump under Rarefied Flow Conditions
Fig. 14 Effects of Slip and Temperature Jump on Displacement and Total Boundary-Layer Thicknesses
0.0
0.2
0.4
0.6
0.8
1.0

0.04
0.08
0.12
0.16
0.20
0.24
0.28
0.32
0.36
0.40

Sta

0.0
0.2
0.4
0.6
0.8
1.0

0.0
0.2
0.4
0.6
0.8
1.0

x

1 1

q

Sta

T

H

q

Sta

T

H

Re/ln. = 396

M = 10

M = 10

T /T = 0.2 (No Slip)

\lambda = 0.037 in.

\lambda = 0.037 in.

11

(2)

(2s + 2s)

(4)

1

1

1

1

1

Sta

to

Fig. 16 Concluded
### Experimental Data

<table>
<thead>
<tr>
<th>Sym</th>
<th>$M_{\infty}$</th>
<th>$Re_{\infty}/$in.</th>
<th>$T_o^0$K</th>
<th>$T_w^0$K</th>
</tr>
</thead>
<tbody>
<tr>
<td>□</td>
<td>9.38</td>
<td>2606</td>
<td>1033</td>
<td>~293</td>
</tr>
<tr>
<td>○</td>
<td>9.37</td>
<td>1602</td>
<td>1662</td>
<td>~293</td>
</tr>
<tr>
<td>△</td>
<td>10.15</td>
<td>388</td>
<td>3020</td>
<td>~293</td>
</tr>
</tbody>
</table>

Flagged Symbols Uncorrected Data

### Numerical Results

<table>
<thead>
<tr>
<th>Sym</th>
<th>$M_{\infty}$</th>
<th>$Re_{\infty}/$in.</th>
<th>$T_o^0$K</th>
<th>$T_w/T_{\infty}$</th>
<th>$T_w/T_o$</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>9.37a</td>
<td>2869</td>
<td>1073</td>
<td>4.95</td>
<td>0.273</td>
</tr>
<tr>
<td></td>
<td>9.37b</td>
<td>1632</td>
<td>1835</td>
<td>2.76</td>
<td>0.160</td>
</tr>
<tr>
<td></td>
<td>10.0</td>
<td>396</td>
<td>3034</td>
<td>2.02</td>
<td>0.097</td>
</tr>
</tbody>
</table>

**Note:** All boundary-layer calculations include viscous interaction, transverse curvature, slip, and temperature jump.

**Fig. 17** Experimental and Theoretically Predicted Surface Pressures on a Water-Cooled 9-deg Half-Angle Cone at $M_{\infty} = 10$
Fig. 18 Experimental and Theoretically Predicted Zero-Lift Drag with Mass Transfer
$M_{\infty} = 10$
$Re_{\infty}/in. = 22,528$
$M_{\infty}/Re_{\infty}, \beta = 0.043$
$T_w/T_0 = 0.33 \rightarrow 0.75$
$\lambda_{\infty} = 0.00066$

Nitrogen Injection

### Numerical Results
- No Slip
- Slip and Temp Jump

### Experimental Results
- AEDC-VKF Tunnel "C"
- Little and Griffith

![Graph](image)

### Fig. 18 Concluded
\[ M_{\infty} = 10 \]
\[ \text{Re}_{\infty}/\text{in.} = 396 \]
\[ M_{\infty}/\sqrt{\text{Re}_{\infty} \cdot \ell} = 0.326 \]
\[ T_w/T_0 = 0.2 \]
\[ \lambda_{\infty} = 0.037 \text{ in.} \]

### Nitrogen Injection

<table>
<thead>
<tr>
<th>Matching Condition</th>
<th>Slip</th>
<th>Experimental Results</th>
</tr>
</thead>
<tbody>
<tr>
<td>( \delta^*/dx )</td>
<td>No</td>
<td>AEDC-VKF Tunnel L</td>
</tr>
<tr>
<td>( \delta^*/dx )</td>
<td>Yes</td>
<td>Little and Griffith</td>
</tr>
<tr>
<td>( \delta^*/dx + p_w v_w r_w / p_e u_e r_e )</td>
<td>No</td>
<td></td>
</tr>
<tr>
<td>( \delta^*/dx + p_w v_w r_w / p_e u_e r_e )</td>
<td>Yes</td>
<td></td>
</tr>
</tbody>
</table>

**Fig. 19** Effects of Iteration, Mass Transfer, Slip, and Temperature Jump on Zero-Lift Drag at \( M_{\infty} = 10 \)
### Experimental Data

<table>
<thead>
<tr>
<th>Sym</th>
<th>$M_{\infty}$</th>
<th>$Re_{\infty}$/in.</th>
<th>$\theta_{C}$ deg</th>
<th>$T_{\infty}$/K</th>
<th>$T_{w}/T_{0}$</th>
<th>$C_{\infty}$</th>
<th>$\lambda_{\infty}$/in.</th>
<th>Tunnel</th>
<th>Source</th>
</tr>
</thead>
<tbody>
<tr>
<td>o</td>
<td>10.15</td>
<td>388</td>
<td>9</td>
<td>3,020</td>
<td>0.30</td>
<td>0.630</td>
<td>0.037</td>
<td>L</td>
<td>Little and Griffith</td>
</tr>
<tr>
<td>△</td>
<td>9.37</td>
<td>1,600</td>
<td>9</td>
<td>1,662</td>
<td>0.50</td>
<td>0.649</td>
<td>0.0085</td>
<td>L</td>
<td>King and Talbot</td>
</tr>
<tr>
<td>△</td>
<td>9.38</td>
<td>2,600</td>
<td>9</td>
<td>1,033</td>
<td>-0.65</td>
<td>0.701</td>
<td>0.0048</td>
<td>L</td>
<td></td>
</tr>
<tr>
<td>o</td>
<td>10.00</td>
<td>23,800</td>
<td>9</td>
<td>958</td>
<td>-0.75</td>
<td>0.660</td>
<td>0.00066</td>
<td>L</td>
<td></td>
</tr>
<tr>
<td>△</td>
<td>3.93</td>
<td>1,765</td>
<td>5</td>
<td>300</td>
<td>0.96</td>
<td>0.821</td>
<td>0.0032</td>
<td>L</td>
<td>Berkeley King and Talbot</td>
</tr>
<tr>
<td>o</td>
<td>5.64</td>
<td>6,200</td>
<td>5</td>
<td>300</td>
<td>0.96</td>
<td>0.815</td>
<td>0.0012</td>
<td>L</td>
<td>Berkeley King and Talbot</td>
</tr>
</tbody>
</table>

### Zero Injection

- $C_{D} = M_{\infty} (C_{\infty}/Re_{\infty})^{1/2}$

### Numerical Results

- $d\delta^{\ast}/dx$
- $\nu_{e}/U_{e}$

(s) Denotes slip and temperature jump included.

**Fig. 20** Experimental and Theoretically Predicted Zero-Lift Drag of Sharp Slender Cones
<table>
<thead>
<tr>
<th>Tunnel</th>
<th>( M_a )</th>
<th>( R_e/\text{in.} )</th>
<th>( P_0, \text{psia} )</th>
<th>( H_0 \times 10^{-3}, \text{R}^2/\text{sec}^2 )</th>
<th>( T_0, ^\circ \text{K} )</th>
<th>( P_m \times 10^3, \text{psia} )</th>
<th>( T_m, ^\circ \text{K} )</th>
<th>( P_m \times 10^3, \text{R}^2/\text{sec}^2 )</th>
<th>( U_m, \text{ft/sec} )</th>
<th>( C_m )</th>
</tr>
</thead>
<tbody>
<tr>
<td><strong>Berkeley Low Density Tunnel</strong></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>3.93</td>
<td>1765</td>
<td>0.0334</td>
<td>0.3245</td>
<td>0.227</td>
<td>300</td>
<td>1.64</td>
<td>73.4</td>
<td>1.04</td>
<td>2215</td>
<td>0.821</td>
</tr>
<tr>
<td>5.64</td>
<td>6200</td>
<td>0.0679</td>
<td>0.3245</td>
<td>1.775</td>
<td>300</td>
<td>1.64</td>
<td>40.7</td>
<td>1.875</td>
<td>2368</td>
<td>0.815</td>
</tr>
<tr>
<td><strong>AEDC-VKF Hypersonic Tunnels</strong></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>( L^b )</td>
<td>10.15</td>
<td>388</td>
<td>0.0507</td>
<td>3.930</td>
<td>18.00</td>
<td>0.397</td>
<td>144.5</td>
<td>0.124</td>
<td>8118</td>
<td>0.630</td>
</tr>
<tr>
<td>(10.00)</td>
<td>(386)</td>
<td>(3.395)</td>
<td>(18.64)</td>
<td>(3034)</td>
<td>(0.392)</td>
<td>(93.0)</td>
<td>(0.461)</td>
<td>(6030)</td>
<td>(6041)</td>
<td>0.728</td>
</tr>
<tr>
<td>9.37</td>
<td>1602</td>
<td>0.1056</td>
<td>2.053</td>
<td>25.00</td>
<td>1662</td>
<td>0.952</td>
<td>98.9</td>
<td>0.429</td>
<td>6194</td>
<td>0.678</td>
</tr>
<tr>
<td>( L )</td>
<td>(1632)</td>
<td>(25.82)</td>
<td>(1833)</td>
<td>(0.930)</td>
<td>(98.9)</td>
<td>(98.9)</td>
<td>(0.429)</td>
<td>(6194)</td>
<td>(6194)</td>
<td>0.678</td>
</tr>
<tr>
<td>9.38</td>
<td>2606</td>
<td>0.0812</td>
<td>1.200</td>
<td>19.50</td>
<td>1033</td>
<td>0.713</td>
<td>56.8</td>
<td>0.565</td>
<td>4778</td>
<td>0.701</td>
</tr>
<tr>
<td>(9.37)</td>
<td>(2869)</td>
<td>(19.70)</td>
<td>(1073)</td>
<td>(0.715)</td>
<td>(57.8)</td>
<td>(0.552)</td>
<td>(4766)</td>
<td>0.710</td>
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</tr>
<tr>
<td>10.00</td>
<td>42,640</td>
<td>0.978</td>
<td>1.076</td>
<td>350</td>
<td>958</td>
<td>7.65</td>
<td>45.6</td>
<td>8.01</td>
<td>4444</td>
<td>0.660</td>
</tr>
<tr>
<td>( C )</td>
<td>(45,057)</td>
<td>(321.3)</td>
<td>(994)</td>
<td>(7.57)</td>
<td>(47.3)</td>
<td>(7.44)</td>
<td>(4526)</td>
<td>(875)</td>
<td></td>
<td></td>
</tr>
<tr>
<td>( C )</td>
<td>10.00</td>
<td>23,820</td>
<td>0.488</td>
<td>1.076</td>
<td>175</td>
<td>958</td>
<td>41.3</td>
<td>4.06</td>
<td>4444</td>
<td>0.685</td>
</tr>
<tr>
<td>( C )</td>
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<td>(160.4)</td>
<td>(894)</td>
<td>(3.78)</td>
<td>(3.2)</td>
<td>(4526)</td>
<td>(3.72)</td>
<td>(4526)</td>
<td></td>
<td>0.675</td>
</tr>
</tbody>
</table>

*Unless otherwise noted ideal gas data computed from \( M_a \), \( P_0 \), and \( \gamma \) shown in parentheses.*

*Ideal gas data computed from \( \gamma \), \( T_m \), and \( \dot{M}_m \) shown in parentheses.*
### TABLE II
EXPERIMENTAL DATA ON THE EFFECTS OF MASS TRANSFER ON ZERO-LIFT DRAG

<table>
<thead>
<tr>
<th>Tunnel</th>
<th>$M_\infty$</th>
<th>$Re_\infty$/in.</th>
<th>$m_\infty$, lbm/hr</th>
<th>$T_w/T_o$</th>
<th>$C_D$</th>
</tr>
</thead>
<tbody>
<tr>
<td><strong>Berkeley Low Density Tunnel</strong></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td></td>
<td>3.93</td>
<td>1765</td>
<td>0</td>
<td>0.95</td>
<td>0.386</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>0.03125</td>
<td></td>
<td>0.339</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>0.0625</td>
<td></td>
<td>0.290</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>0.09375</td>
<td></td>
<td>0.253</td>
</tr>
<tr>
<td></td>
<td>5.64</td>
<td>6200</td>
<td>0</td>
<td>0.96</td>
<td>0.235</td>
</tr>
<tr>
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<td></td>
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<td>0.03125</td>
<td></td>
<td>0.211</td>
</tr>
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<td></td>
<td></td>
<td></td>
<td>0.0625</td>
<td></td>
<td>0.186</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>0.09375</td>
<td></td>
<td>0.167</td>
</tr>
<tr>
<td><strong>AEDC-VKF Hypersonic Tunnels</strong></td>
<td>10.15</td>
<td>388</td>
<td>0</td>
<td>0.3</td>
<td>0.788</td>
</tr>
<tr>
<td><strong>L</strong></td>
<td></td>
<td></td>
<td>0.0254</td>
<td>(0.1)</td>
<td>0.764</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>0.1440</td>
<td>(0.1)</td>
<td>0.662</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>0.1980</td>
<td>(0.1)</td>
<td>0.625</td>
</tr>
<tr>
<td><strong>L</strong></td>
<td>9.37</td>
<td>1602</td>
<td>0</td>
<td>0.5</td>
<td>0.443</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>0.2160</td>
<td>(0.3)</td>
<td>0.340</td>
</tr>
<tr>
<td><strong>L</strong></td>
<td>9.38</td>
<td>2606</td>
<td>0</td>
<td>0.65</td>
<td>0.377</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>0.2160</td>
<td>(0.45)</td>
<td>0.282</td>
</tr>
<tr>
<td><strong>C</strong></td>
<td>10.00</td>
<td>42,640</td>
<td>0</td>
<td>(0.75)</td>
<td>0.146</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>0.2160</td>
<td>(0.33)</td>
<td>0.135</td>
</tr>
<tr>
<td><strong>C</strong></td>
<td>10.00</td>
<td>23,820</td>
<td>0</td>
<td>(0.75)</td>
<td>0.178</td>
</tr>
</tbody>
</table>

*a*Estimated equilibrium wall temperature ratios in parentheses.
### TABLE III
EXPERIMENTAL WALL PRESSURE DATA ON A 9-DEG WATER-COOLED CONE IN TUNNEL L

<table>
<thead>
<tr>
<th>$M_{\infty}$</th>
<th>$x$</th>
<th>$P_m/P_{\infty}$</th>
<th>$P_c/P_{\infty}^a$</th>
</tr>
</thead>
<tbody>
<tr>
<td>9.38</td>
<td>0.222</td>
<td>5.98</td>
<td>8.11</td>
</tr>
<tr>
<td></td>
<td>0.877</td>
<td>5.15</td>
<td>6.83</td>
</tr>
<tr>
<td>9.37</td>
<td>0.222</td>
<td>5.51</td>
<td>6.72</td>
</tr>
<tr>
<td></td>
<td>0.877</td>
<td>4.30</td>
<td>5.23</td>
</tr>
<tr>
<td>10.15</td>
<td>0.222</td>
<td>5.58</td>
<td>8.00</td>
</tr>
<tr>
<td></td>
<td>0.877</td>
<td>4.11</td>
<td>6.17</td>
</tr>
</tbody>
</table>

$^a$Pressures corrected for orifice size after Potter, Kinslow, and Boylan (Ref. 13).

### TABLE IV
EXPERIMENTAL EQUILIBRIUM WALL-TO-STAGNATION TEMPERATURE DATA ON A THIN-WALLED STAINLESS STEEL MODEL IN TUNNEL L

<table>
<thead>
<tr>
<th>$M_{\infty}$</th>
<th>9.38</th>
<th>9.37</th>
<th>10.15</th>
</tr>
</thead>
<tbody>
<tr>
<td>$T_o, ^\circ$K</td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>1033</td>
<td>1662</td>
<td>3020</td>
<td></td>
</tr>
<tr>
<td>$x$</td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>0.079</td>
<td>0.817</td>
<td>0.546</td>
<td>0.307</td>
</tr>
<tr>
<td>0.342</td>
<td>0.675</td>
<td>0.514</td>
<td>0.296</td>
</tr>
<tr>
<td>0.526</td>
<td>0.654</td>
<td>0.507</td>
<td>0.294</td>
</tr>
<tr>
<td>0.658</td>
<td>0.650</td>
<td>0.506</td>
<td>0.286</td>
</tr>
</tbody>
</table>
A theoretical model is developed based on an iterated perfect gas inviscid-viscous flow field which includes first-order displacement (viscous interaction), transverse curvature, wall slip, and temperature jump in addition to mass transfer effects. The effects of inviscid (tangent cone) and viscous (nonsimilar laminar boundary layer) flow field matching conditions are also considered. Numerical results are compared with experimental and analytical results of King and Talbot (AIAA J., 1964) for a 5-deg half-angle cone at $M_\infty = 3.93$ and 5.64. The predicted viscous-induced pressure without mass transfer and the zero-lift drag with and without injection were in agreement with the experimental data within experimental uncertainty. The theoretical model was also used to predict zero-lift drag of a 9-deg half-angle cone at $M_\infty = 9.37$ and 10 and $Re_\infty/\text{in.} = 400$ to 45,000 for a range of wall-to-stagnation temperature ratios. Again, in general, without mass transfer the predictions were within experimental uncertainty. The inability of the theoretical model to adequately treat nonuniform mass transfer distributions is discussed. At the lowest Reynolds number the effects of slip were most significant. At all conditions the effects of inviscid-viscous flow field matching were significant. Experimental zero injection equilibrium wall temperature distributions and cool-wall pressure data are given at $M_\infty \approx 10$ and $Re_\infty/\text{in.} = 400$ to 2600.
mass transfer
boundary layer effects
conical bodies
drag
hypersonic flow
theoretical models
viscous interaction
transverse curvature
wall slip
temperature jump

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